

① $P_0 = 10 \text{ kPa}$, $T_0 = 216 \text{ K}$, $M_0 = 0.9$, $\alpha = 0.3$, $\dot{m}_0 = 65 \text{ kg/s}$

$$\alpha = \frac{\dot{m}_f}{\dot{m}_c} \quad \& \quad \dot{m}_c + \dot{m}_f = \dot{m}_0 \Rightarrow \begin{aligned} \dot{m}_c &= 50 \text{ kg/s} \\ \dot{m}_f &= 15 \text{ kg/s} \end{aligned}$$

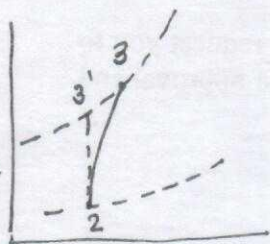
	γ	$C_p \text{ (J/kgK)}$	$R = \frac{\gamma-1}{\gamma} C_p \text{ (J/kgK)}$
Air	1.4	1004	286.85
Turbine	1.4	1004	286.85
Afterburner	1.33	1240	310

$$\begin{aligned} P_{t0} &= P_0 \left[1 + \frac{\gamma-1}{2} M_0^2 \right]^{\gamma/\gamma-1} = 16.913 \text{ kPa} \\ T_{t0} &= T_0 \left[1 + \frac{\gamma-1}{2} M_0^2 \right] = 251 \text{ K} \end{aligned} \quad \left| \begin{aligned} v_0 &= \sqrt{\gamma R T_0} \cdot M_0 \\ v_0 &= \frac{265.087}{265.087} \text{ m/s} \end{aligned} \right.$$

Diffuser section: Adiabatic compression $\Rightarrow T_{t2} = T_{t0} = 251 \text{ K}$ (1)

Loss in total pressure = 5% $\Rightarrow P_{t2} = 0.95 P_{t0} = 16.067 \text{ kPa}$

Compressor section: $\pi_c = 24.5 \quad \therefore \frac{P_{t3}}{P_{t2}} = \frac{P_{t3'}}{P_{t2}} = 24.5$



$$\Rightarrow P_{t3} = P_{t3'} = 393.65 \text{ kPa}$$

$$\frac{T_{t3'}}{T_{t2}} = \left(\frac{P_{t3'}}{P_{t2}} \right)^{\frac{\gamma-1}{\gamma}} \Rightarrow T_{t3'} = 626 \text{ K}$$

$$\eta_c = 0.9 = \frac{T_{t3'} - T_{t2}}{T_{t3} - T_{t2}} \Rightarrow T_{t3} = 667.67 \text{ K} \quad (2)$$

Combustor: Total pressure loss: 6% $\Rightarrow P_{t4} = 0.94 P_{t3} = 370.031 \text{ kPa}$

$$T_{t4} = 1850 \text{ K}, \quad Q = 42000 \text{ kJ/kg}, \quad \eta_b = 0.985$$

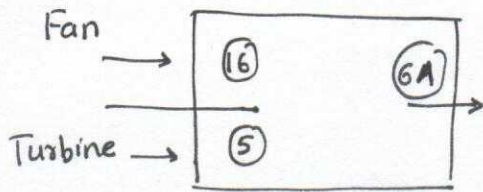
$$\dot{m}_c \cdot C_p \cdot T_{t3} + \eta_b \cdot \dot{m}_f \cdot Q = C_p \cdot T_{t4} \cdot (\dot{m}_c + \dot{m}_f)$$

$$\Rightarrow \dot{m}_f = \frac{\dot{m}_c \cdot C_p (T_{t4} - T_{t3})}{\eta_b \cdot Q - C_p T_{t4}} = 1.502 \text{ kg/s}$$

$$f = \frac{\dot{m}_f}{\dot{m}_c} = 0.03$$

$$\dot{m}_4 = (1+f) \dot{m}_c = 51.50 \text{ kg/s} \quad (2)$$

Fan and turbine section need to be analysed simultaneously by matching conditions at mixer inlet



Fan stream in mixer - 16

Turbine stream in mixer - 5

As per (vi) $\Rightarrow P_{t5} = P_{t16}$

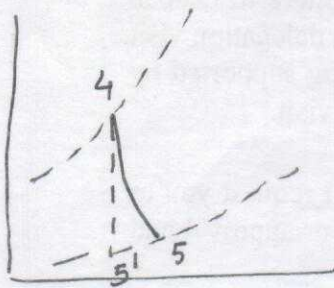
Let fan exit station is (13) & (13) to (16) is bypass duct.

As per (vi) $\Rightarrow P_{t16} = 0.99 P_{t13}$ & $T_{t16} = T_{t13}$

Turbine section: $\dot{W}_C + \dot{W}_F = \eta_m \dot{W}_T$

$$\dot{m}_c \cdot c_p (T_{t3} - T_{t2}) + \alpha \cdot \dot{m}_c \cdot c_p (T_{t13} - T_{t2}) = \eta_m \dot{m}_c (1+f) c_p (T_{t4} - T_{t5})$$

$$\Rightarrow (T_{t3} - T_{t2}) + \alpha (T_{t13} - T_{t2}) = \eta_m (1+f) (T_{t4} - T_{t5})$$



$$\eta_T = \frac{T_{t4} - T_{t5}}{T_{t4} - T_{t5'}} \quad \text{and} \quad \frac{T_{t5'}}{T_{t4}} = \left(\frac{P_{t5}}{P_{t4}} \right)^{\frac{\gamma-1}{\gamma}}$$

$$T_{t4} - T_{t5} = \eta_T \cdot T_{t4} \left[1 - \left(\frac{P_{t5}}{P_{t4}} \right)^{\frac{\gamma-1}{\gamma}} \right] = \eta_T \cdot T_{t4} \left[1 - \left(\frac{0.99 P_{t13}}{P_{t4}} \right)^{\frac{\gamma-1}{\gamma}} \right]$$

Compression in fan is isentropic $\Rightarrow \frac{T_{t13}}{T_{t2}} = \left(\frac{P_{t13}}{P_{t2}} \right)^{\frac{\gamma-1}{\gamma}}$

$$\Rightarrow (T_{t3} - T_{t2}) + \alpha \cdot T_{t2} \left[\left(\frac{P_{t13}}{P_{t2}} \right)^{\frac{\gamma-1}{\gamma}} - 1 \right] = \eta_m (1+f) \eta_T \cdot T_{t4} \left[1 - \left(\frac{0.99 P_{t13}}{P_{t4}} \right)^{\frac{\gamma-1}{\gamma}} \right]$$

Solving for P_{t13} , $\Rightarrow P_{t13} = 115.78 \text{ kPa}$

\therefore Fan pressure ratio, $\frac{P_{t13}}{P_{t2}} = 7.2$ & $T_{t13} = 441.3 \text{ K}$

Also, $P_{t16} = 114.622 \text{ kPa}$ & $T_{t16} = T_{t13} = 441.3 \text{ K}$

\therefore Turbine exit pressure, $P_{t5} = 114.622 \text{ kPa}$

$T_{t5} = 484.3 \text{ K}$
 $\underline{1365.69}$

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Energy balance in mixer:

$$\dot{m}_c \cdot (1+f) \cdot C_p \cdot T_{t5} + \alpha \cdot \dot{m}_c \cdot C_p \cdot T_{t16} = \dot{m}_c (1+f+\alpha) C_p \cdot T_{t6A}$$

$$\therefore T_{t6A} = \frac{1157.18}{474.6} \text{ K}$$

Pressure loss in mixer, = 5%.

$$\therefore P_{t6A} = 0.95 P_{t5} = 108.89 \text{ kPa}$$

Afterburner:- $\dot{m}_{6A} = \dot{m}_c (1+f) + \dot{m}_c \cdot \alpha = 66.5 \text{ kg/s}$

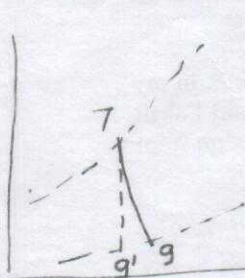
$$T_{t7} = 2000 \text{ K (Given)} ; P_{t7} = 0.9 P_{t6A} = 98.001 \text{ kPa}$$

$$\dot{m}_{6A} \cdot C_p \cdot T_{t6A} + \dot{m}_{f,AB} \cdot Q = (\dot{m}_{6A} + \dot{m}_{f,AB}) \cdot C_{pAB} \cdot T_{t7}$$

$$\Rightarrow \dot{m}_{f,AB} = \frac{2.218}{3.37} \text{ kg/s}$$

$$\text{Further } P_{t7} = 0.9 P_{t6A} \Rightarrow P_{t7} = 98.001 \text{ kPa}$$

Nozzle: To check if nozzle is choked: $P_{tg} = P_{t7} = 98.001 \text{ kPa}$



$$P_{tg} = P_{g*} \cdot \left[1 + \frac{\gamma-1}{2} M_{g*}^2 \right]^{\frac{\gamma}{\gamma-1}}$$

$$\text{Let } M_{g*} = 1 \Rightarrow P_{g*} = 52.95 \text{ kPa} > P_0$$

\therefore Nozzle will be choked.

$$\therefore M_g = 1, P_g = 52.95 \text{ kPa}$$

$$\eta_N = \frac{T_{t7} - T_g}{T_{t7} - T_{g'}} \quad \& \quad T_{tg} = T_{g'} \left(\frac{P_{tg}}{P_g} \right)^{\frac{\gamma-1}{\gamma}} \Rightarrow T_{g'} = 1716.68 \text{ K}$$

$$\Rightarrow T_g = 1730.84 \text{ K} \Rightarrow v_g = a_g = \sqrt{\gamma_g R_g T_g} = 844.76 \text{ m/s}$$

$$\rho_g = \frac{P_g}{R_g \cdot T_g} = 0.0986 \text{ kg/m}^3$$

$$\dot{m}_g = \dot{m}_{6A} + \dot{m}_{f,AB} = 68.718 \text{ kg/s} = \rho_g A_g \cdot v_g$$

$$\Rightarrow A_g = 0.8388 \text{ m}^2$$

Thrust, $F = (\dot{m}_g v_g - \dot{m}_o v_o) + A_g (p_g - p_o)$

$$F = \cancel{39.88} + \cancel{36.02} 41.79 + 36.02$$

$$\boxed{F = \cancel{75.9} \text{ kN}} \quad \boxed{F = \cancel{77.81} \text{ kN}} \quad F = 76.84 \text{ kN}$$

$$sfc = \frac{\dot{m}_f + \dot{m}_{fAB}}{F} = \frac{0.06425 \text{ kg}}{0.0478 \text{ s} \cdot \text{kN}}$$



Problem 2] Total compressor pressure ratio, $\pi_c = 8.9$

$$\pi_c = [\pi_{CLP}]^{\eta_{LP}} \cdot [\pi_{CHP}]^{\eta_{HP}} \quad \left. \begin{array}{l} \pi_{CLP} = 1.2, \eta_{LP} = 3 \\ \eta_{HP} = 5 \end{array} \right\}$$

$$\pi_{CHP} = 1.388$$

$$M_0 = 2, \quad P_0 = 10 \text{ kPa}, \quad T_0 = 210 \text{ K}$$

$$T_{t0} = T_0 \left[1 + \frac{\gamma-1}{2} M_0^2 \right] = 378 \text{ K}, \quad P_{t0} = P_0 \left(\frac{T_{t0}}{T_0} \right)^{\frac{\gamma}{\gamma-1}} = 78.244 \text{ kPa}$$

Intake: Adiabatic $\Rightarrow T_{t2} = T_{t0} = 378 \text{ K}$

$$\pi_d = 0.88 \Rightarrow P_{t2} = 0.88 P_{t0} = 68.855 \text{ kPa}$$

$$\eta_d = \frac{\left(1 + \frac{\gamma-1}{2} M_0^2 \right) (\pi_d)^{\frac{\gamma}{\gamma-1}} - 1}{\frac{\gamma-1}{2} M_0^2} = \frac{(1.8 \times 0.964) - 1}{0.8}$$

$$\eta_d = 0.919 \text{ or } 91.9 \%$$

Compressor inlet: $P_{t2} = 68.855 \text{ kPa}$ $T_{t2} = 378 \text{ K}$

Inlet mach no. for first stage, $M_2 = 0.5$

$$T_{t2} = T_2 \left[1 + \frac{\gamma-1}{2} M_2^2 \right] \Rightarrow T_2 = 360 \text{ K}$$

$$\text{Before IGV, air velocity} = M_2 \cdot \sqrt{\gamma R T_2}$$

$$\therefore = 190.16 \text{ m/s}$$

IGV, turn the flow by 20° w.r.t. Z-direction without any loss.

$$\therefore C_2 = 190.16 \text{ m/s} \quad \& \quad C_{Z2} = C_2 \cos 20 = 178.69 \text{ m/s}$$

$$\alpha_2 = 20^\circ$$

$$\gamma = 1.4$$

$$R = 287 \text{ J/kg K}$$

$$C_p = \frac{\gamma}{\gamma-1} R$$

$$C_p = 1004.5 \text{ J/kg K}$$

$$\frac{P_{t2}}{P_2} = \left(\frac{T_{t2}}{T_2} \right)^{\frac{\gamma}{\gamma-1}} \Rightarrow P_2 = 58.046 \text{ kPa}$$

$$\rho_2 = \frac{P_2}{RT_2} \Rightarrow \rho_2 = 0.5618 \text{ kg/m}^3$$

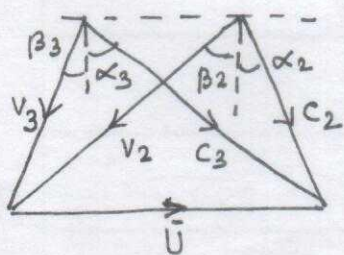
$$\text{Hub-to-tip ratio, } = \frac{r_h}{r_t} = 0.2 \Rightarrow r_h = 0.2 r_t$$

$$\dot{m} = \rho_2 \cdot C_{z2} \cdot \pi (r_t^2 - r_h^2) \Rightarrow r_t = 0.445 \text{ m}$$

$$\therefore r_h = 0.089 \text{ m}$$

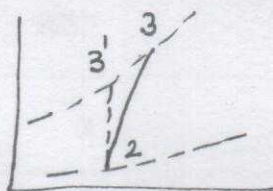
$$\bar{r} = \frac{r_h + r_t}{2} \Rightarrow \bar{r} = 0.267 \text{ m}$$

Degree of reaction = $\Lambda = 0.5 \Rightarrow$ symmetric velocity triangles



$$\alpha_2 = \beta_3 \text{ and } \alpha_3 = \beta_2$$

$$\text{Stage pressure ratio, } \pi_{cs} = 1.2$$



$$T_{t3'} = T_{t2} (\pi_{cs})^{\frac{\gamma-1}{\gamma}}$$

$$T_{t3'} = 398.21 \text{ K}$$

$$\eta_c = \frac{T_{t3'} - T_{t2}}{T_{t3} - T_{t2}} = 0.92 \Rightarrow T_{t3} = 399.96 \text{ K}$$

$$\text{Work done by stage, } W = C_p (T_{t3} - T_{t2}) = 22066.24 \text{ J/kg}$$

$$\text{But } W = \bar{U} (C_{\theta 3} - C_{\theta 2})$$

$$\therefore 22066.24 = \bar{U} [\bar{U} - 65.03 - 65.03]$$

$$\Rightarrow \bar{U}^2 - 130.06 \bar{U} - 22066.24 = 0$$

$$\bar{U} = 227.18 \text{ m/s}$$

(Solving for \bar{U} & taking +ve root)

$$\bar{U} = \frac{2\pi \bar{r} N}{60} \Rightarrow N = 8125.12 \text{ rpm}$$

$$C_{\theta 3} = \bar{U} - 65.03 = 162.15 \text{ m/s}$$

From velocity triangle,

$$C_{\theta 2} = C_{z2} \cdot \tan \alpha_2 = 65.03 \text{ m/s}$$

$$C_{\theta 3} = \bar{U} - C_{z2} \cdot \tan \beta_3$$

$$= \bar{U} - C_{z2} \tan \alpha_2$$

$$C_{\theta 3} = \bar{U} - 65.03$$

$$\tan \beta_2 = \frac{\bar{U} - C_{z2} \tan \alpha_2}{C_{z2}}$$

$$\beta_2 = 42.22^\circ$$

1st stage design parameters:

$$r_h = 0.089 \text{ m, } r_t = 0.445 \text{ m, } \bar{r} = 0.267 \text{ m, } N = 8125.12 \text{ rpm}$$

$$\text{Blade angles, } \beta_2 = 42.22^\circ, \beta_3 = 2^\circ$$

Design of LP turbine stage: LP turbine drives the LP compressor.

\therefore Rotational speed of LP turbine = 8125.15 rpm

Total pressure ratio of LP compressor = $(1.2)^3 = 1.728$

Overall. $\eta_c = 0.92$.

Let 2 & 3 represent inlet and exit of LP comp^r.

$$\eta_c = \frac{T_{t3'} - T_{t2}}{T_{t3} - T_{t2}} \quad \text{and} \quad \frac{T_{t3'}}{T_{t2}} = \left(\frac{P_{t3}}{P_{t2}} \right)^{\frac{\gamma-1}{\gamma}} \Rightarrow T_{t3'} = 441.938 \text{ K}$$

$$\therefore T_{t3} - T_{t2} = 69.498 \text{ K}$$

$$W_{LPC} = C_p (T_{t3} - T_{t2}) = 69810.741 \text{ J/kg}$$

$$W_{LPC} = W_{LPT} = 69810.741 \text{ J/kg}$$

Let 4 & 5 be inlet & outlet of LP turbine.

Impulse turbine with $\alpha_4 = 72^\circ$, $\eta_T = 0.95$, $T_{t4} = 900 \text{ K}$

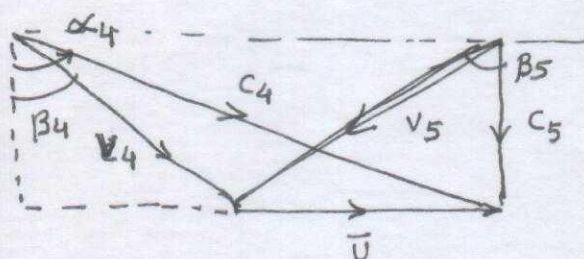
Given $C_5 = \text{axial}$ and $V_4 = V_5$

C_5 is purely axial $\Rightarrow C_{\theta 5} = 0$

$$C_{\theta 4} = 2 \bar{U} \quad \text{as } V_4 = V_5$$

$$\therefore W_{LPT} = 2 \bar{U}^2$$

$$\therefore \bar{U} = 186.83 \text{ m/s}$$



$$\text{Mean turbine radius, } \bar{r} = \frac{\bar{U} \times 60}{2\pi N} \Rightarrow \bar{r} = 0.22 \text{ m}$$

$$C_{z4} \cdot \tan \alpha_4 = C_{\theta 4} = 2 \bar{U} \Rightarrow C_{z4} = 121.4 \text{ m/s}$$

$$\beta_4 = \beta_5 = \tan^{-1} \left(\frac{\bar{U}}{C_{z4}} \right) = 56.98^\circ$$

$$W_{LPT} = C_p (T_{t4} - T_{t5}) \Rightarrow T_{t5} = 830.5 \text{ K}$$

$$\eta_T = 0.95 = \frac{T_{t4} - T_{t5}}{T_{t4} - T_{t5'}} \Rightarrow T_{t5'} = 826.84 \text{ K}$$

$$\text{LPT pressure ratio, } \pi_t = \left(\frac{P_{t5}}{P_{t4}} \right) = \left(\frac{T_{t5'}}{T_{t4}} \right)^{\frac{\gamma}{\gamma-1}}$$

$$\therefore \pi_t = 0.743$$

