

# **Heat Transfer and Fluid Flow Calculations of Industrial Shell Boilers and Evaluation of Operation Conditions – Draft**

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# Abstract

This thesis develops a three pass fire tube industrial shell boiler model, implemented in Python, the modelling framework integrates (i) detailed fuel-air combustion, (ii) six sequential gas side heat exchange stages representing furnace, tube banks, reversal chambers, and economizer, and (iii) a water/steam circuit governed by saturated boiling in the pressure parts and single phase heating in the economizer. The gas–water energy balance is solved using a one dimensional marching algorithm, which updates local heat transfer coefficients, wall temperatures, and segmental duties based on a full resistance network.

Combustion calculations provide the adiabatic flame temperature, the fully burnt flue gas composition, and the total heat release the natural gas fuel provides. Hydraulic losses are resolved concurrently using friction factor and minor loss correlations yielding complete gas/water pressure drop profiles. Boiler level performance metrics, obtained under different operation conditions and analyzed, demonstrating that efficiency exhibits a shallow optimum near the design excess air setting; that pressure chiefly affects steam quantity rather than boiler efficiency; and that firing rate scales heat duties approximately linearly within the practical load range. The modelling framework provides a physics based tool suitable for analyzing industrial shell boiler behavior, supporting performance evaluation, operational optimization, and design exploration.

# Chapter 1

## Introduction

Industrial shell boilers remain one of the most widely deployed technologies for producing saturated steam and hot water in small to medium industrial plants. Their popularity arises from their compact construction, robust heat transfer surfaces, straightforward operation, and comparatively low installation and maintenance requirements. Typical applications span food and beverage processing, chemicals and pharmaceuticals, textiles, healthcare, and general manufacturing sectors where steady, reliable steam generation is essential for heating, processing, and auxiliary services.

Despite their apparent simplicity, the thermal behavior of shell boilers is governed by tightly coupled processes: multi stage radiative and convective heat transfer, natural circulation boiling inside the pressure parts, complex flue gas property variations, and geometry dependent hydraulic losses. Modern operation demands higher efficiency, reduced emissions, increased reliability, and improved control.

This thesis develops a physics based model for a three pass fire tube shell boiler that integrates combustion calculations, detailed flue gas thermophysical properties, multi stage heat transfer modelling, and hydraulic loss estimation. The model is implemented as a one dimensional marching solver applied to six sequential heat exchange stages:

$$\text{HX}_1 \rightarrow \text{HX}_2 \rightarrow \text{HX}_3 \rightarrow \text{HX}_4 \rightarrow \text{HX}_5 \rightarrow \text{HX}_6, \quad (1.1)$$

representing the furnace, reversal chambers, convective tube banks, and the economizer, see figure 1.1. On the water side, the boiler drum provides a saturated interface for nucleate boiling in the pressure parts, while the economizer section is treated as a single phase internal flow. Gas side properties are supplied by Cantera, enabling temperature dependent transport, specific heat, thermal conductivity, and radiative behavior to be modelled.

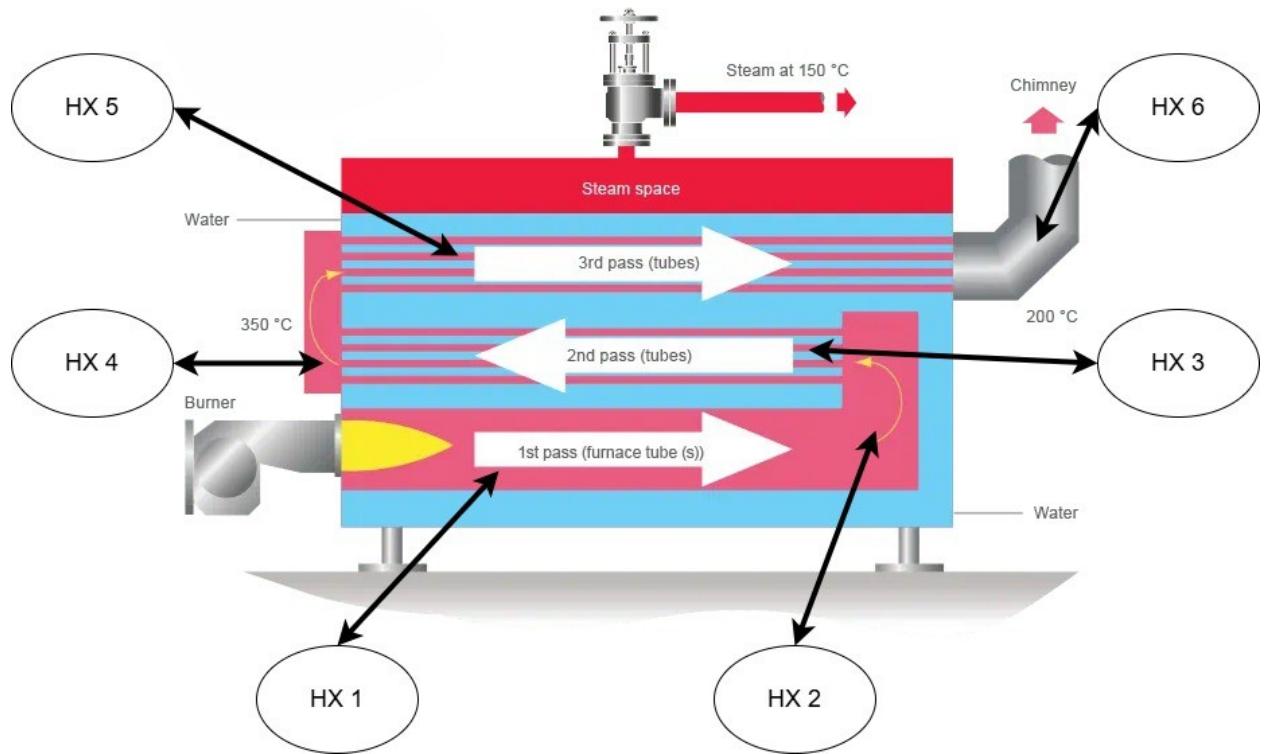


Figure 1.1: Shell boiler labeled stages.

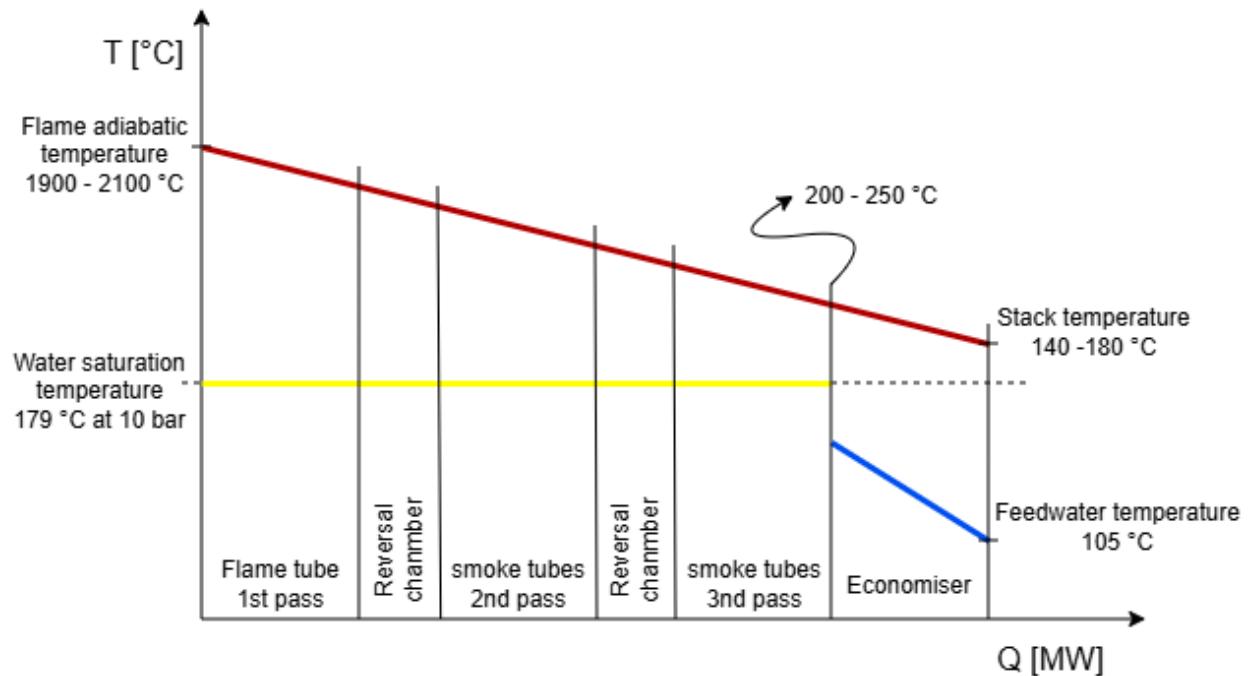


Figure 1.2:  $T-Q$  diagram for the three pass boiler with economizer.

The overall objectives of the study are:

1. To construct a unified combustion-boiler model capable of predicting flue gas temperature, composition, adiabatic flame temperature, and total heat input based on fuel composition and excess air settings.
2. To resolve heat transfer processes along the boiler using stage specific geometries, convection correlations, and a spectral based gas radiation model.
3. To quantify hydraulic losses across each pass using friction factor relations and minor loss coefficients, yielding the total boiler gas side pressure drop.
4. To compute boiler level performance, including useful heat transfer, direct and indirect efficiencies, stack temperature, and stage wise duties.
5. To evaluate sensitivity of boiler performance to key operating parameters, excess air ratio, drum pressure, and fuel mass flow rate.

The numerical framework is structured such that the water/steam mass flow is determined iteratively from the global energy balance. For each operating condition, a fixed point loop between assumed efficiency and resulting steam flow is solved until convergence, ensuring consistency between combustion input, heat transfer output, and steam generation.

The remainder of this thesis is organized as follows. Chapter 2 identifies typical industrial applications of shell boilers and introduces key design features. Chapter 3 describes the boiler geometry and outlines the six heat transfer stages. Chapter 4 develops the combustion and flue gas model, including stoichiometry and adiabatic flame temperature prediction. Chapter 5 covers the heat transfer framework, combining convection and radiation on the gas side with pool boiling and single phase correlations on the water side. Chapter 6 presents the hydraulic model. Chapter 7 reports the resulting boiler performance, while Chapter 8 examines the sensitivity of the system to variations in  $\lambda$ , pressure, and firing rate. Chapter 9 concludes with a summary of findings.

## Chapter 2

# Industrial Application of Shell Boilers

Fire tube boilers- shell boilers

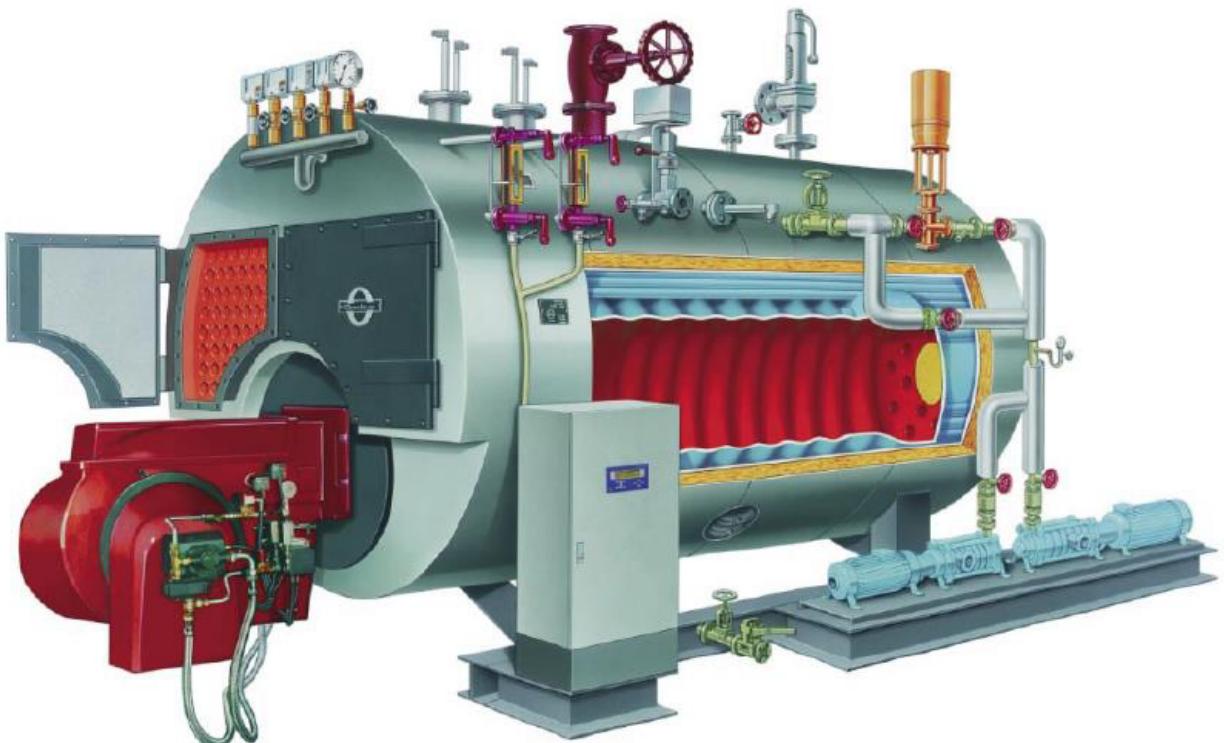


Figure 2.1: Example of a packaged fire tube shell boiler in industrial service.

## 2.1 Typical Industries

Shell (fire tube) boilers are widely used in small to medium steam and hot water duties where compactness, robustness, and simple operation are prioritized over very high pressure or very large throughput. Typical sectors include:

- Food and beverage
  - Breweries, dairies, sugar refineries
  - Canneries, bakeries, confectionery plants
  - CIP (clean-in-place) systems and sterilization
- Chemical and pharmaceutical
  - Fine chemicals, specialty chemicals
  - Active pharmaceutical ingredient (API) and formulation plants
  - Steam for reactors, jacket heating, and clean steam generators
- Textiles and paper
  - Dyeing, washing, drying, and calendaring operations
  - Small paper mills and converting facilities
- Healthcare and institutional
  - Hospitals, clinics, and laboratories (space heating, humidification, sterilizers, autoclaves)
  - Universities, office complexes, district heating sub-plants
- Light manufacturing and general industry
  - Metal finishing, surface treatment, and cleaning
  - Rubber and plastics processing
  - Laundry services and commercial dry-cleaning

## 2.2 Standard Steam Duties

Shell boilers are normally applied in low to medium pressure ranges and moderate steam capacities:

- Typical operating pressure range:
  - Saturated steam: 6–25 bar, occasionally up to 30 bar
  - Hot-water service: 10–16 bar
- Steam-generation rates (order of magnitude):
  - Small units: 0.5–5 t/h
  - Medium units: 5–20 t/h
  - Large shell boilers (upper practical range): 20–40 t/h, beyond which water-tube designs are usually preferred

## 2.3 Advantages and Limitations

### Advantages

- Compact and integrated construction
  - Furnace, passes, and steam/water space are combined in a single pressure body.
  - Relatively small footprint and simple installation.
- Operational simplicity
  - Straightforward start-up and shutdown procedures.
  - Typically tolerant of moderate load swings and cycling (within design limits).
  - Often delivered as packaged units with burner, controls, and safety devices pre-engineered.
- Low-to-moderate capital cost
  - Attractive for small and medium plants, boiler houses, and decentralized steam supply.
- Good part-load performance
  - Large water content provides thermal buffer, reducing short-cycling of the burner.
  - Reasonable efficiency across a wide load range, especially with economizers.
- Maintenance and inspection
  - Accessible gas passes and tube bundles (depending on design) for cleaning and inspection.
  - Long-established technology with wide service and parts availability.

### Limitations

- Pressure and capacity limits
  - Practical upper bounds on shell diameter and plate thickness limit maximum pressure and steam rate.
  - For very high pressure (e.g., >40–60 bar) or very large capacities, water-tube boilers are more suitable.
- Response time
  - Large water inventory slows thermal response to rapid, large load changes compared with water-tube boilers.
- Efficiency ceiling
  - Radiative and convective heat-transfer surfaces are constrained by geometry.

- Very high efficiencies often require additional heat-recovery equipment (economizers, condensing stages, air preheaters).
- Transport and installation constraints
  - Shell diameter and weight can be limited by route and lifting capacity.
  - Retrofitting within existing boiler houses may be constrained by overall envelope.

## 2.4 Multi-Pass Layout

Industrial shell boilers typically adopt multi-pass fire-tube configurations to enhance convective heat transfer and maintain acceptable gas-side velocities:

- Two-pass layout
  - First pass: large diameter furnace tube running from burner front to rear reversal chamber.
  - Second pass: return of flue gas through banks of small-diameter fire-tubes back to the front reversal chamber and flue outlet.
  - Simpler construction but lower total heat-transfer surface compared with three-pass designs.
- Three-pass layout (most common for industrial shell boilers)
  - Pass 1: large diameter furnace tube running from burner front to rear reversal chamber.
  - Pass 2: First bank of smoke-tubes (typically reversing at the rear turnaround chamber).
  - Pass 3: Second bank of smoke-tubes.
  - Provides higher overall heat-transfer surface, more uniform gas cooling, and lower exit-gas temperatures.
- Extended heat-recovery sections
  - Economizer: additional convective heat exchanger in the flue-gas path downstream of the boiler to preheat feedwater.
  - Air preheater / condensing sections: for high-efficiency systems using suitable fuels and materials.
- Flow arrangement
  - Gas-side: burner → furnace (Pass 1) → turnaround chamber → tube bank(s) (Passes 2 and 3) → stack.
  - Water/steam side: natural circulation between heated tube surfaces and the upper steam space within the drum/shell; feedwater introduced at cooler regions (often via economizer), steam drawn from the top of the shell.

This multi-pass concept underpins the subsequent detailed modelling of each convective and radiative heat-transfer stage  $HX_1$ - $HX_6$  in the simulation.

# Chapter 3

## Configuration

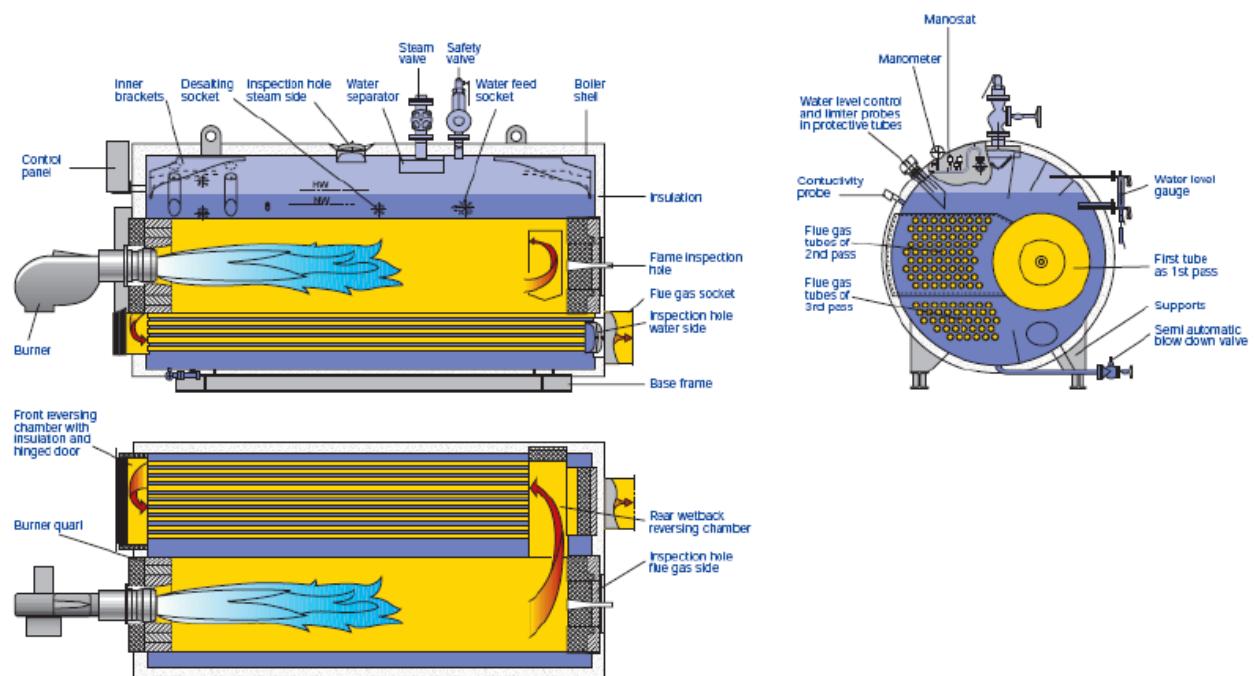


Figure 3.1: Example of shell boiler setup components

The simulated unit is a three pass fire tube shell boiler with six distinct gas side heat transfer stages and a single common steam drum on the water/steam side. Hot flue gas from the burner traverses a radiative furnace, two reversal chambers, two convective tube banks, and a final economizer before leaving to the stack.

### 3.1 Layout

The gas path is represented as:

$$\text{Burner} \rightarrow \text{HX}_1 \rightarrow \text{HX}_2 \rightarrow \text{HX}_3 \rightarrow \text{HX}_4 \rightarrow \text{HX}_5 \rightarrow \text{HX}_6 \rightarrow \text{stack} \quad (3.1)$$

with the following interpretation:

- $\text{HX}_1$  – Furnace (first pass)  
Large, single furnace tube where combustion products enter directly from the burner and transfer heat mainly by radiation and high-temperature convection to the surrounding water/steam.
- $\text{HX}_2$  – First reversal chamber  
Short cylindrical wet back chamber that turns the flow from the furnace outlet into the first convective tube bank (gas direction change =  $180^\circ$ ).
- $\text{HX}_3$  – First convective tube bank (second pass) Bank of small diameter fire tubes arranged in a staggered pattern inside the shell, to boost convection; flue gas flows inside of the tubes, water/steam outside.
- $\text{HX}_4$  – Second reversal chamber Second turning chamber redirecting gas from the first to the second tube bank.
- $\text{HX}_5$  – Second convective tube bank (third pass) Second fire-tube bundle, representing the last in-boiler convective pass.
- $\text{HX}_6$  – Economizer Separate, downstream tube bank used to preheat feedwater in single-phase operation before entering the drum/boiler circuit, recovering heat, and boosting efficiency of the boiler.

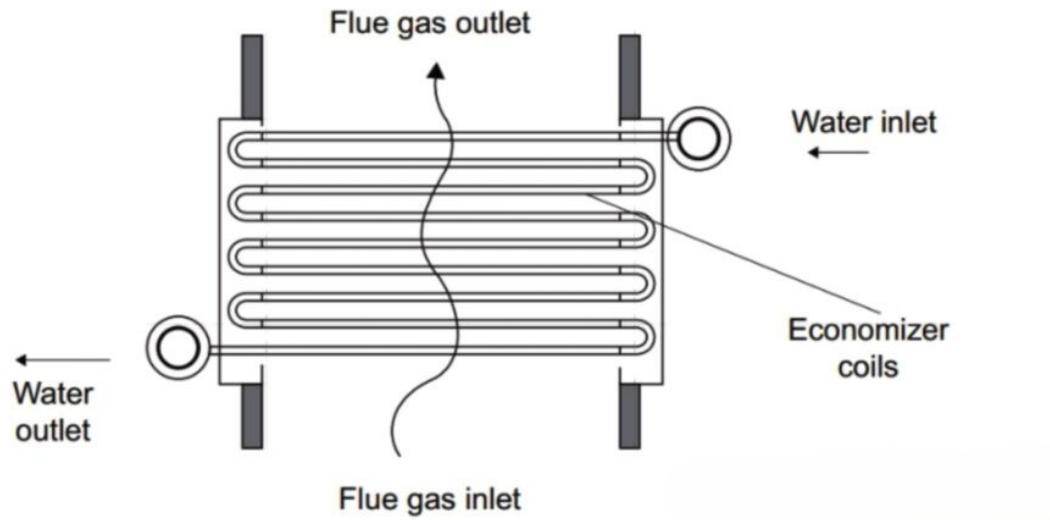
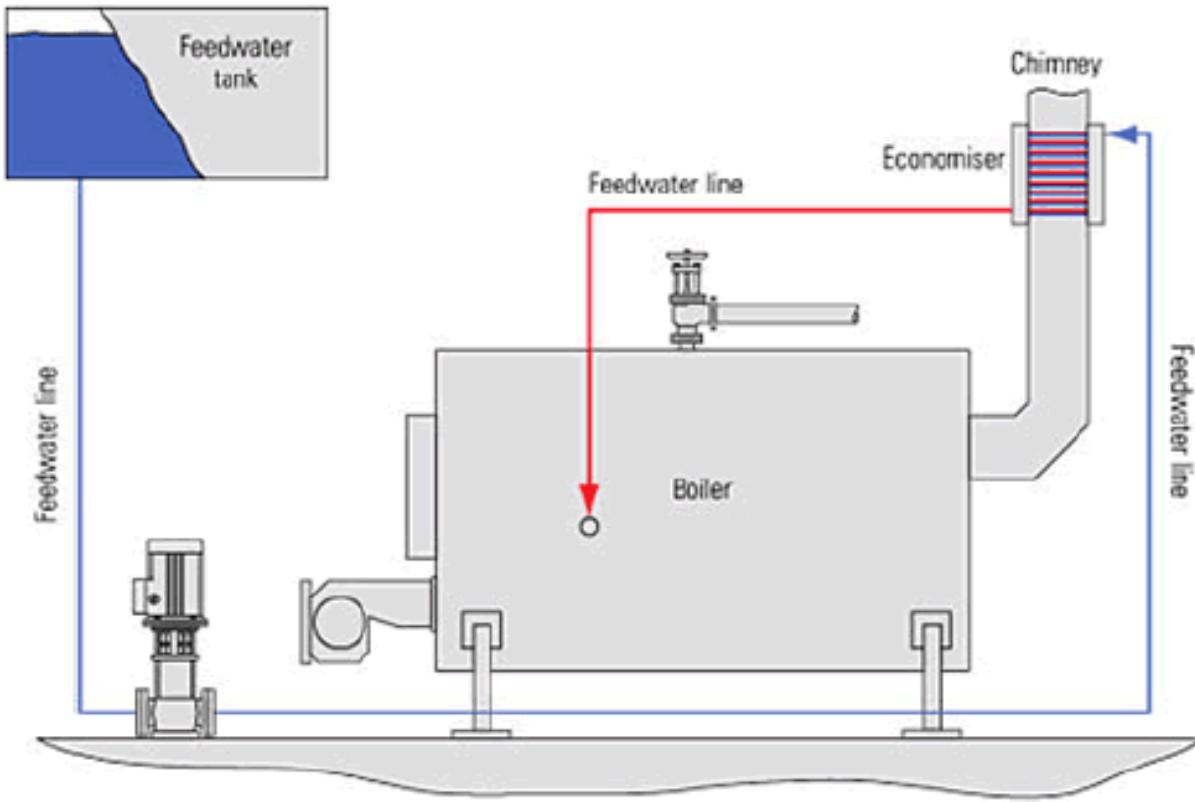


Figure 3.2: Cross-section of the economizer tube bundle  $\text{HX}_6$ , showing gas-side cross-flow and water-side internal flow.



**Figure 1:** Economizer in Fire Tube Steam Boiler.

Figure 3.3: Three-pass shell boiler with rear-mounted economizer for feedwater preheating.

## 3.2 Geometry and surface specification

### Drum configuration

The boiler has a single horizontal steam drum. Its inner diameter is  $D_{i,\text{drum}} = 4.5 \text{ m}$  and its length  $L_{\text{drum}} = 5.0 \text{ m}$ .

The drum is not modelled with internal separators or circulation hardware. It simply supplies the saturated water/steam state at boiler pressure, while all circulation effects are represented by the single 1-D water/steam stream used in the heat-transfer stages.

### Flue gas passes

All six pressure part stages of the simulated boiler are represented with a consolidated geometric and surface specification.

Table 3.1: Flue gas stages key parameters

Element	Kind	Di [m]	L [m]	N_tubes [-]	Wall t [mm]	Roughness [ $\mu\text{m}$ ]	Pool boiling [-]
HX <sub>1</sub>	single_tube	1.40	5.276	1	2.9	0.5	true
HX <sub>2</sub>	reversal_ch.	1.60	0.80	1	2.9	0.5	true
HX <sub>3</sub>	tube_bank	0.076	4.975	118	2.9	0.5	true
HX <sub>4</sub>	reversal_ch.	1.60	0.80	1	2.9	0.5	true
HX <sub>5</sub>	tube_bank	0.076	5.620	100	2.9	0.5	true
HX <sub>6</sub>	economizer	0.0337	8 x 3	40 x 3	2.6	0.5	false
				3			

The input file `stages.yaml`, provided in Annex A, contain the complete detailed specifications and is parsed at runtime by the configuration loader (`new_loader.py`). This separates numerical solution algorithms from geometry and surface data, and allows different boiler variants to be simulated by simply modifying the YAML files.

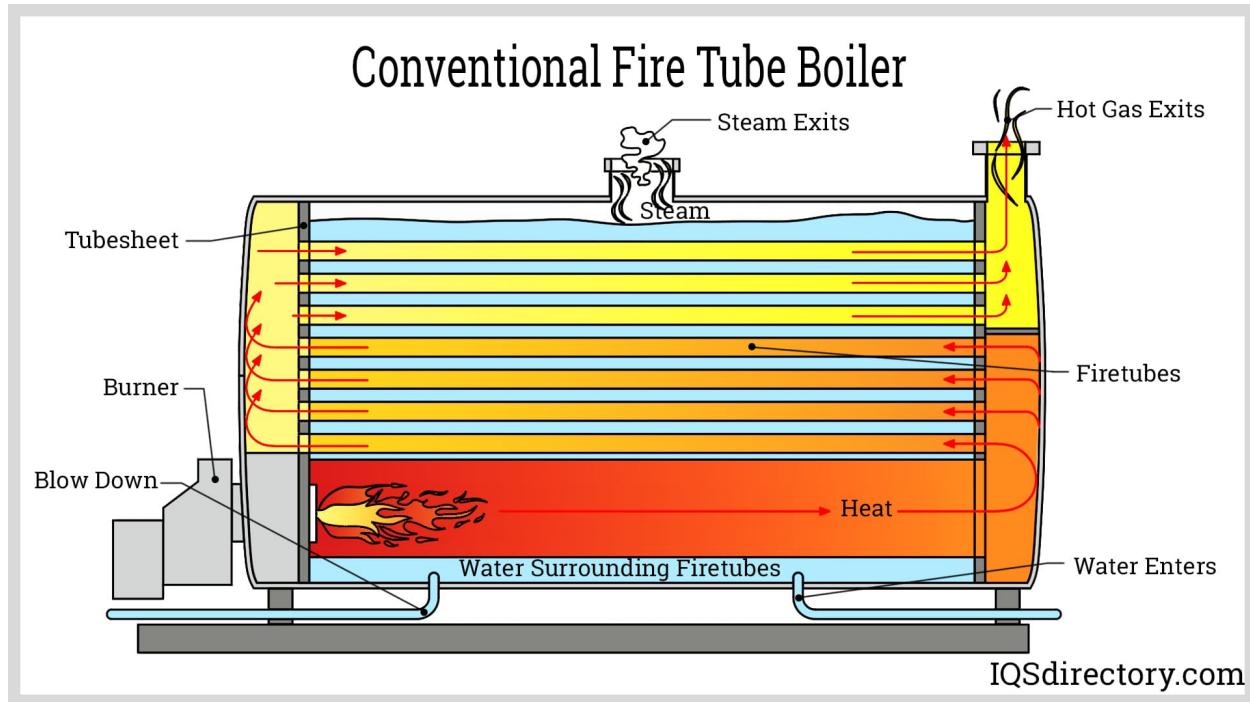


Figure 3.4: Detailed cross-section of the simulated boiler, showing drum, furnace, tube banks and reversal chambers.

All pressure part stages ( $\text{HX}_1$ – $\text{HX}_5$ ) share the same steel wall thermal conductivity of  $k_{\text{wall}} = 50 \text{ W/m/K}$ .

The YAML configuration supplies wall, surface, and hydraulic properties not captured in the tabulated geometry. Each pressure-part exchanger defines wall thickness, wall conduction,

tivity, surface roughness, emissivity, and optional fouling layers with specified thickness and conductivity. Most stages use a uniform carbon-steel wall with smooth surfaces and thin fouling layers, while the economizer uses a thinner, higher-conductivity wall and no fouling to reflect a cleaned section.

The steam drum defines diameter, length, and internal surface properties with its own roughness and fouling settings.

Reversal chambers specify curvature radius and nozzle minor-loss coefficients used in pressure-drop calculations.

Economizer defines shell side cross section, where flue gas flows as a cylindrical drum of 0.95 m diameter, containing 3 circuit of tube bundles where each circuit is of 60 tubes of 33.7 mm.

These YAML entries are translated by the loader into the geometric and hydraulic quantities required for cross-flow areas, Reynolds numbers, and shell-side heat-transfer evaluation.

### 3.3 Assumptions and limitations

#### 1. Combustion and flue gas

- Ideal complete combustion, with fixed excess air,
- Adiabatic flame temperature from equilibrium chemistry, using NASA polynomials.
- Ideal gas mixture  $p = \rho RT$ , with transport properties  $\mu(T)$   $k(T)$   $c_p(T)$  from polynomial data.
- Steady state boiler operation, with fixed fuel air and feedwater.
- Boiler efficiency computed on HHV or LHV basis, using standard energy balance equations.

#### 2. Heat transfer

- One dimensional steady heat transfer per stage.
- Uniform wall conductivity and thickness, radial conduction only.
- Gas side HTC from standard correlations properties **vary** with temperature pressure and composition.
- Gas radiation via band averaged grey model for  $CO_2$  and  $H_2O$ , no spectral resolution, and no soot formation.
- Water side HTC uses IAPWS-IF97 properties, homogenized two phase model.
- Drum at fixed pressure, and perfect steam water separation (no carryover).

#### 3. Hydraulic and thermal performance

- 1D, steady, single phase flow.
- Constant mass flow along each stage.
- Compressibility effects appear only through property variations  $\rho(T, P)$  and  $\mu(T, P)$  in Re and  $\rho V^2/2$ .
- Stage level minor loss coefficients are lumped, and uniformly distributed along the stage.
- Gas side  $\Delta P$  in economizer stage is neglected.

# Chapter 4

## Combustion Model

Determine combustion conditions inside the furnace (1st pass), resulting in a fully burnt flue gas stream, entering the heat transfer model at adiabatic temperature.

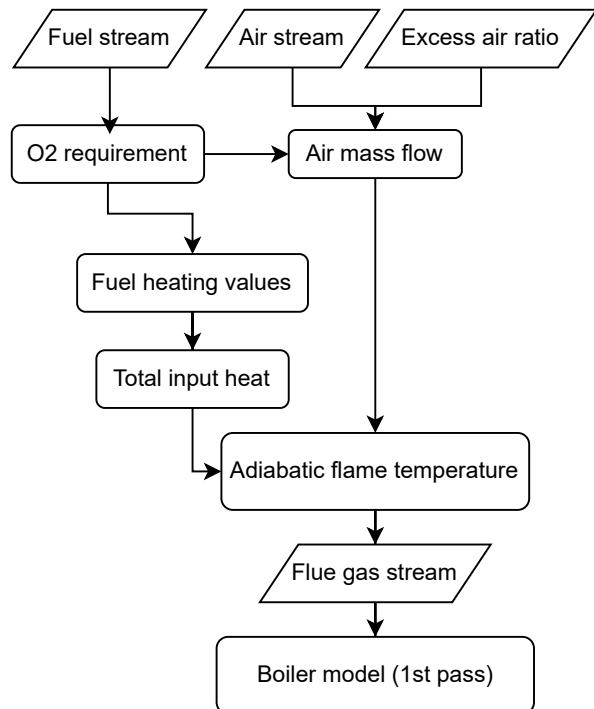


Figure 4.1: Combustion flow

## 4.1 Fuel and Air

### 4.1.1 Fuel Stream

The boiler is fired with a natural-gas-type fuel defined in the simulation input (config/fuel.yaml).

The fuel is supplied at  $300K$  and  $1.013 \times 10^5 Pa$  with a mass flow rate of  $0.1kg/s$ . Its composition is specified by user on a mass fraction.

Table 4.1: Fuel composition in mass fractions. [1]

Component	Formula	Mass fraction $w_i [-]$
Methane	$CH_4$	0.8548
Ethane	$C_2H_6$	0.0622
Propane	$C_3H_8$	0.0207
n-Butane	$C_4H_{10}$	0.00518
Hydrogen sulfide	$H_2S$	0.000104
Nitrogen	$N_2$	0.0414
Carbon dioxide	$CO_2$	0.0155
Water vapour	$H_2O$	0.00
Argon	Ar	0.00

The mass fractions sum to 1.0 by definition. The mole fractions  $x_i$  are obtained from

$$x_i = \frac{\frac{w_i}{M_i}}{\sum_j \frac{w_j}{M_j}} \quad (4.1)$$

which is provided by the function `to_mol` in `combustion/mass_mole.py`, where  $M_i$  is the molar mass of species  $i$  from `molar_masses` in `common/constants.py`.

### 4.1.2 Air Stream

Combustion air is represented as a separate `GasStream` object, analogous to the fuel stream, with:

- temperature  $T_{air} = 300 K$ ,
- pressure  $P_{air} = 1.013 \times 10^5 Pa$ ,
- mass flow rate determined internally from the specified excess air ratio  $\lambda$ ,
- composition:

Table 4.2: Air composition in mass fractions. [2]

Component	Formula	Mass fraction $w_i$ [-]
Oxygen	O <sub>2</sub>	0.233
Nitrogen	N <sub>2</sub>	0.755
Argon	Ar	0.013
Carbon dioxide	CO <sub>2</sub>	0.00006

The mass fractions satisfy  $\sum_i w_i = 1$  and are converted internally to mole fractions whenever stoichiometric or thermophysical properties are required.

### 4.1.3 Stoichiometric Oxygen requirement

Evaluated the stoichiometric oxygen requirement via `stoich_o2_required_per_mol_fuel` in `combustion/flue.py`. The algorithm is:

1. Use per mole of species stoichiometric O<sub>2</sub> factors  $\nu_{O_2,i}$  from `o2_per_mol` in `common/constants.py`:

Table 4.3: Combustion reactions and stoichiometric factors

Species	Global reaction (complete combustion)	$\nu_{O_2,i}$ [mol O <sub>2</sub> / mol species]
CH <sub>4</sub>	CH <sub>4</sub> + 2 O <sub>2</sub> → CO <sub>2</sub> + 2 H <sub>2</sub> O	2.0
C <sub>2</sub> H <sub>6</sub>	C <sub>2</sub> H <sub>6</sub> + 3.5 O <sub>2</sub> → 2 CO <sub>2</sub> + 3 H <sub>2</sub> O	3.5
C <sub>3</sub> H <sub>8</sub>	C <sub>3</sub> H <sub>8</sub> + 5 O <sub>2</sub> → 3 CO <sub>2</sub> + 4 H <sub>2</sub> O	5.0
C <sub>4</sub> H <sub>10</sub>	C <sub>4</sub> H <sub>10</sub> + 6.5 O <sub>2</sub> → 4 CO <sub>2</sub> + 5 H <sub>2</sub> O	6.5
H <sub>2</sub> S	H <sub>2</sub> S + 1 O <sub>2</sub> → SO <sub>2</sub> + H <sub>2</sub> O	1.0
N <sub>2</sub> , CO <sub>2</sub> , H <sub>2</sub> O	Inert/fully oxidized → no additional O <sub>2</sub>	0.0

2. Compute the stoichiometric O<sub>2</sub> requirement per mole of fuel mixture as

$$\nu_{O_2,\text{stoich}} = \sum_i x_i \nu_{O_2,i} \quad (4.2)$$

Using the mole fractions from Section 4.1 for the present fuel:

3. For later hydraulic and performance interpretation, it is also useful to express this on a mass basis.

For 1 kg of fuel, the total fuel moles are

$$n_{\text{fuel},\text{total}} = \sum_i \frac{w_i}{M_i} \quad (4.3)$$

Thus the stoichiometric  $O_2$  requirement per unit fuel mass is

$$n_{O_2,\text{stoich}}^{(m)} = \nu_{O_2,\text{stoich}} n_{\text{fuel},\text{total}} \quad (4.4)$$

Converting to mass of  $O_2$  per kg of fuel:

$$\dot{m}_{O_2,\text{stoich}} = n_{O_2,\text{stoich}}^{(m)} M_{O_2} \quad (4.5)$$

For the current working fuel:

- Stoichiometric oxygen requirement:  $\nu_{O_2,\text{stoich}} = 2.09$  mol  $O_2$  per mol fuel mixture
- Equivalent mass requirement:  $\dot{m}_{O_2,\text{stoich}} = 3.75$  kg  $O_2$  per kg fuel

#### 4.1.4 Air-fuel ratio and excess air $\lambda$

The simulation specifies an excess air ratio  $\lambda = 1.1$

in config/operation.yaml. This value enters the calculation through air\_flow\_rates(air, fuel, excess) in combustion/flue.py.

#### Actual $O_2$ supplied

Using:

$$\dot{n}_{O_2,\text{actual}} = \lambda \dot{n}_{O_2,\text{stoich}} = \lambda \nu_{O_2,\text{stoich}} \dot{n}_{\text{fuel}} \quad (4.6)$$

#### Air required

Air  $O_2$  mole fraction (from air.yaml):  $x_{O_2,\text{air}} = 0.2095$

Air molar flow, given by air\_flow\_rates():

$$\dot{n}_{\text{air}} = \frac{\dot{n}_{O_2,\text{actual}}}{x_{O_2,\text{air}}} \quad (4.7)$$

The air molar mass (mixture weighted) is:  $M_{\text{air}} = 0.02897$  kg/mol

Therefore the air mass flow rate:

$$\dot{m}_{\text{air}} = \dot{n}_{\text{air}} M_{\text{air}} \quad (4.8)$$

## Air-fuel ratio

Mass based air fuel ratio:

$$AFR = \frac{\dot{m}_{air}}{\dot{m}_f} \quad (4.9)$$

## 4.2 Heating values and firing rate

The fuel lower and higher heating values, and the corresponding firing rate, are evaluated in `combustion/heat.py` by the function `compute_LHV_HHV(fuel)` and then used by `total_input_heat()`.

### 4.2.1 HHV and LHV

For each fuel species, complete combustion is considered:

- $CH_4 + 2 O_2 \rightarrow CO_2 + 2 H_2O$
- $C_2H_6 + 3.5 O_2 \rightarrow 2 CO_2 + 3 H_2O$

Builds product formation enthalpies for:

- HHV assumption: water as liquid (condensed)
- LHV assumption: water as vapour (no condensation heat recovered)

### Latent heat of water

Obtain the latent heat of vaporization of water at the reference pressure  $P_{ref} = 101,325 \text{ Pa}$  from the IAPWS-97 correlation:

```
latent_H2O = WaterProps.h_g(P_ref) - WaterProps.h_f(P_ref)
```

where:

- $h_g$  is the saturated vapour enthalpy,
- $h_f$  is the saturated liquid enthalpy.

### Reference formation enthalpies

Standard formation enthalpies  $\Delta h_f^\circ$  (at 298.15 K, 1 bar) are taken from `common/constants.py` in kJ/mol:

Table 4.4: Standard enthalpy of formation of selected species [3]

Species	$\Delta h_f^\circ$ (kJ mol $^{-1}$ )
CH <sub>4</sub>	-74.8
C <sub>2</sub> H <sub>6</sub>	-84.7
C <sub>3</sub> H <sub>8</sub>	-103.8
C <sub>4</sub> H <sub>10</sub>	-126.1
SO <sub>2</sub>	-296.8
CO <sub>2</sub>	-393.5
H <sub>2</sub> O(l)	-285.5

## Methodology

The mixture molar higher and lower heating values are:

$$\text{HHV}_{\text{mol}} = h_{\text{react}} - h_{\text{prod,HHV}}, \quad \text{LHV}_{\text{mol}} = h_{\text{react}} - h_{\text{prod,LHV}} \quad (4.10)$$

These are converted to mass based heating values.

For each species  $i$  in the fuel, the reaction enthalpy contribution is

$$\Delta h_i = x_i [\Delta h_{f,\text{products}}^\circ - \Delta h_{f,\text{reactants}}^\circ], \quad (4.11)$$

and mixture HHV and LHV are obtained by summing these contributions over all fuel components, enforcing the appropriate water phase:

- HHV: water in products is liquid
- LHV: water in products is vapour

After obtaining the mixture molar heating values, conversion to mass basis uses

$$\text{HHV}_{\text{mix}} = \frac{\text{HHV}_{\text{mol}}}{M_{\text{mix}}}, \quad \text{LHV}_{\text{mix}} = \frac{\text{LHV}_{\text{mol}}}{M_{\text{mix}}}, \quad (4.12)$$

The firing rate corresponding to a fuel mass flow  $\dot{m}_f$  then follows directly:

$$P_{\text{HHV}} = \dot{m}_f \text{HHV}_{\text{mix}}, \quad P_{\text{LHV}} = \dot{m}_f \text{LHV}_{\text{mix}}. \quad (4.13)$$

For the fuel specified above, the mixture heating values are:

Table 4.5: Heating values and firing rates, returned by `compute_LHV_HHV()`

Variable	Value
$\text{HHV}_{\text{mix}}$	52 MJ/kg
$\text{LHV}_{\text{mix}}$	47 MJ/kg
$P_{\text{HHV}}$	26 MW
$P_{\text{LHV}}$	23.6 MW

## 4.2.2 Total heat input

The function `total_input_heat()` combines chemical and sensible contributions:

where `sensible_heat()` uses:

$$Q_{\text{sens}} = \dot{m} c_p (T - T_{\text{ref}}) \quad (4.14)$$

Both fuel and air enter at 300 K, while the reference is 298.15 K; the resulting sensible contributions are very small compared with the chemical term  $P_{\text{LHV}}$  (on the order of tens of kW versus tens of MW). Therefore:

$$Q_{\text{in}} = P_{\text{LHV}} + Q_{\text{sens,fuel}} + Q_{\text{sens,air}} \quad (4.15)$$

## 4.3 Adiabatic flame temperature

The adiabatic flame temperature  $T_{\text{ad}}$  is evaluated in the model by the function `adiabatic_flame_T()` in `combustion/adiabatic_flame_temperature.py`. This routine uses Cantera and an enthalpy–pressure equilibrium (HP) function to determine the equilibrium temperature and composition of the flue gas, assuming:

- complete mixing of fuel and air,
- no heat losses to the surroundings (adiabatic),
- constant system pressure (equal to the air/fuel inlet pressure),
- chemical equilibrium among all gas species.

The total inlet enthalpy rate of the unmixed reactants is

$$\dot{H}_{\text{react}} = \dot{m}_{\text{air}} h_{\text{air}}(T_{\text{air}}, P, X_{\text{air}}) + \dot{m}_{\text{fuel}} h_{\text{fuel}}(T_{\text{fuel}}, P, X_{\text{fuel}}) \quad (4.16)$$

The total mass flow is

$$\dot{m}_{\text{tot}} = \dot{m}_{\text{air}} + \dot{m}_{\text{fuel}} \quad (4.17)$$

so the mixture-averaged specific enthalpy of the reactants is

$$h_{\text{target}} = \frac{\dot{H}_{\text{react}}}{\dot{m}_{\text{tot}}} \quad (4.18)$$

The adiabatic, constant-pressure equilibrium state is then defined by the constraints:

$$\begin{aligned} h_{\text{products}}(T_{\text{ad}}, P, \mathbf{X}_{\text{eq}}) &= h_{\text{target}} \\ P_{\text{out}} &= P \\ \mathbf{X}_{\text{eq}} &\text{satisfies chemical equilibrium at } (T_{\text{ad}}, P) \end{aligned} \quad (4.19)$$

Cantera is used to enforce this condition via its HP equilibrium mode.

Build the overall reactant composition  $\mathbf{X}_{\text{react}}$  from the molar flow rates of each component in each stream:

Determine molar flow rates of all species in the air and fuel streams,

$$\dot{n}_i^{(\text{air})}, \quad \dot{n}_i^{(\text{fuel})}. \quad (4.20)$$

Form the total species molar flow rate,

$$\dot{n}_i = \dot{n}_i^{(\text{air})} + \dot{n}_i^{(\text{fuel})}. \quad (4.21)$$

Compute the overall reactant mole fractions,

$$X_{i,\text{react}} = \frac{\dot{n}_i}{\sum_j \dot{n}_j} \quad (4.22)$$

Initialize the mixture and perform HP equilibrium:

Initialize the reacting mixture at temperature  $T = 300$  K, pressure  $P$ , and composition  $X_{\text{react}}$ .

Impose the constraint of fixed enthalpy and pressure,

$$h = h_{\text{target}}, \quad P = P, \quad (4.23)$$

and compute the chemical equilibrium state under  $(H, P)$  conditions.

Obtain the equilibrium mass fractions

$$Y_{i,\text{eq}} \quad (4.24)$$

The HP-equilibrium calculation yields an adiabatic flame temperature on the order of:

$$T_{\text{ad}} = 2,050 \text{ K} \quad (= 1,780^\circ\text{C}) \quad (4.25)$$

This value is consistent with typical adiabatic flame temperatures for natural gas with around 10 % excess air and confirms that the combustion zone (furnace) operates at very high gas temperatures [4], driving strong radiative and convective heat transfer to the shell-side water/steam.

## 4.4 Flue gas composition

In the combustion model two different flue gas streams are distinguished, represented as `GasStream` objects and stored in the `CombustionResult`, but they serve different purposes in the boiler calculation:

### 1. Equilibrium flue gas (`f1ue_ad`)

- Defined as the flue gas mixture at adiabatic flame conditions, obtained from a high-temperature HP equilibrium calculation in Cantera.
- Contains all equilibrium species permitted by the reaction mechanism.
- Its purposes are:
  - determining the adiabatic flame temperature  $T_{\text{ad}}$ ,
  - providing the equilibrium composition for diagnostics.

### 2. Fully burnt flue gas (`f1ue`)

- Defined as a chemically frozen, fully burnt mixture at the same temperature and pressure as the equilibrium (`f1ue_ad`).
- Contains only standard engineering combustion products.
- Used as the hot side working gas for all boiler heat transfer and pressure drop calculations throughout the heat-exchanger network.

The equilibrium flue gas provides a physically consistent high temperature reference, while the fully burnt flue gas represents the practical working fluid in the convective radiative sections of the boiler.

## Fully burnt boiler flue gas

Starting from the fuel and air known `GasStream` objects, compute molar formation rates and flow rate as:

Using the fuel and air molar flow rates,  $\dot{n}_{\text{fuel}}$  and  $\dot{n}_{\text{air}}$ , and their mole fractions  $x_i^{(\text{fuel})}$  and  $x_i^{(\text{air})}$ , for any product species  $k$ , the molar flow rate is written generically as

$$\dot{n}_k = \dot{n}_{\text{fuel}} \Phi_k^{(\text{fuel})} + \dot{n}_{\text{air}} \Phi_k^{(\text{air})}, \quad (4.26)$$

where

- $\Phi_k^{(\text{fuel})}$  is the amount of species  $k$  that comes from the fuel: species already present in the fuel plus any of  $k$  formed by complete oxidation of the fuel components.
- $\Phi_k^{(\text{air})}$  is the amount of species  $k$  that comes from the air: species originally present in the air plus any portion that remains unreacted.

Oxygen additionally satisfies

$$\dot{n}_{O_2} = \dot{n}_{\text{air}} x_{O_2}^{(\text{air})} - \dot{n}_{\text{fuel}} \nu_{O_2, \text{stoich}}, \quad (4.27)$$

where  $\nu_{O_2, \text{stoich}}$  is the stoichiometric oxygen demand of the fuel.

The total molar flow rate of the fully burnt flue gas is

$$\dot{n}_{\text{tot}} = \sum_k \dot{n}_k. \quad (4.28)$$

The molar fractions of the products are then

$$x_k^{(\text{flue})} = \frac{\dot{n}_k}{\dot{n}_{\text{tot}}}. \quad (4.29)$$

These molar fractions are converted to product mass fractions by `to_mass()`:

$$w_k^{(\text{flue})} = \frac{x_k^{(\text{flue})} M_k}{\sum_j x_j^{(\text{flue})} M_j}. \quad (4.30)$$

Finally, the flue gas total mass flow rate is obtained from the molar composition and total molar flow via `mass_flow()`:

$$\dot{m}_{\text{flue}} = \sum_k x_k^{(\text{flue})} \dot{n}_{\text{tot}} M_k. \quad (4.31)$$

The function `from_fuel_and_air()` returns the fully burnt flue gas composition  $w_k^{(\text{flue})}$  and the total flue mass flow  $\dot{m}_{\text{flue}}$ .

This separation allows the model to retain a realistic high temperature reference from chemical equilibrium while employing a reduced, engineering flue gas composition for subsequent heat transfer and hydraulic calculations.

# Chapter 5

## Heat Transfer Model

This model simulates heat transfer from hot flue gas to the water/steam mixture in the drum, flue gas entering first pass, is specified by the results of the combustion model as fully burnt gas at adiabatic temperature with known mass flow rate, and water entering the economizer, specified by user at 10bar pressure and 105°C temperature with the mass flow to be calculated iteratively until convergence of water in and steam produced.

### 5.1 Fundamental heat balance equations

The boiler is modelled as a one dimensional counter current heat exchanger composed of six stages ( $HX_1-HX_5$ ). Heat transfer is resolved along the gas flow direction  $x$ , while water flows in the opposite direction. Each stage is discretized into segments of length  $dx$ ; all local quantities are defined per unit length.

- Notation (per segment)
- $x$  – axial coordinate along the gas flow [m]
- $dx$  – marching step in  $x$  [m]
- $\dot{m}_g, \dot{m}_w$  – gas and water mass flow rates [kg/s]
- $T_g(x), T_w(x)$  – bulk gas and water temperatures [K]
- $T_{gw}(x), T_{ww}(x)$  – gas-side and water-side wall temperatures [K]
- $h_g(x), h_w(x)$  – total gas-side and water-side heat-transfer coefficients [ $W/m^2 \cdot K$ ]
- $P_g, P_w$  – gas-side and water-side wetted perimeters [m]
- $q'(x)$  – linear heat flux (heat per unit length) [ $W/m$ ]
- $UA'(x)$  – overall conductance per unit length [ $W/K/m$ ]

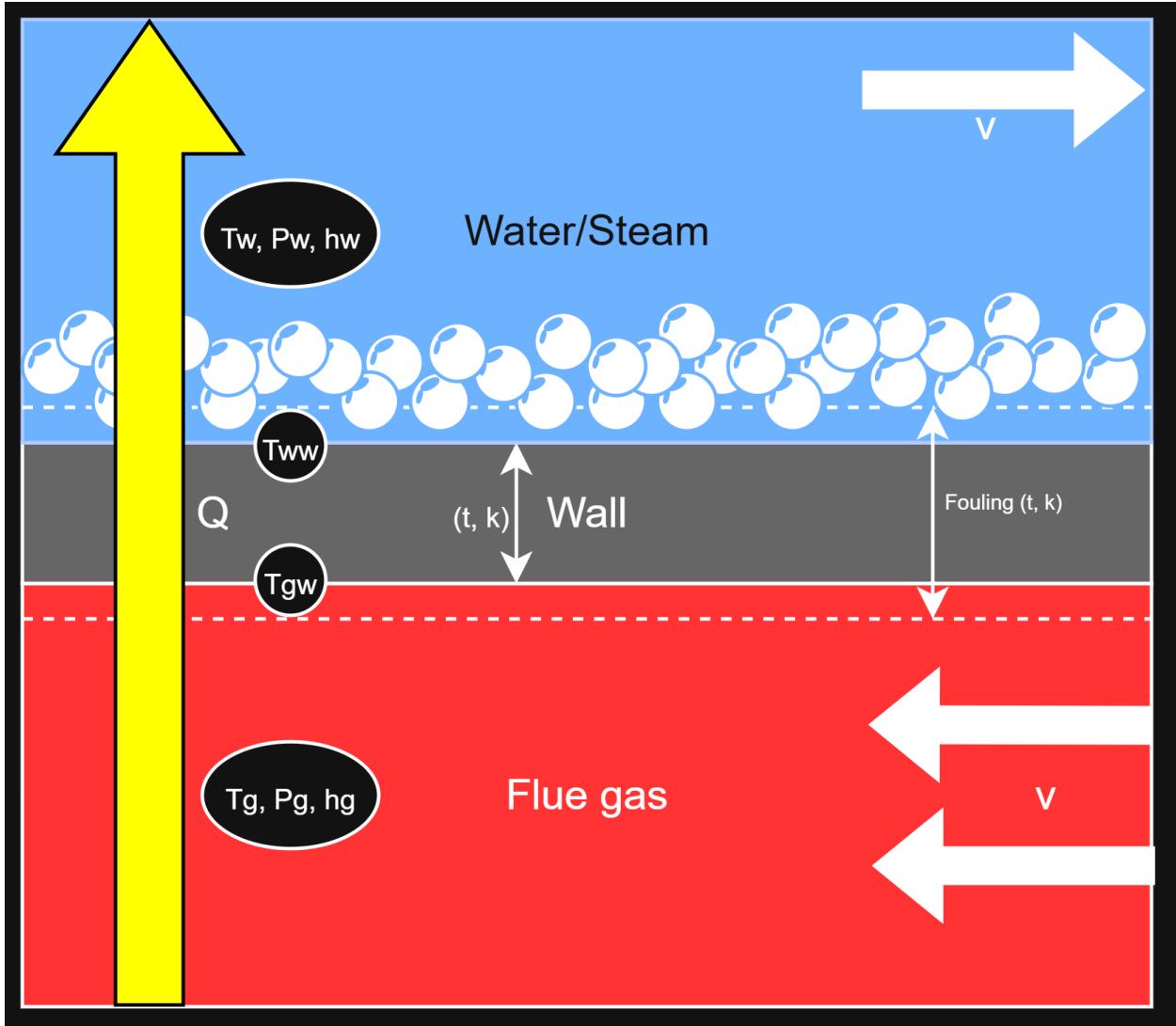


Figure 5.1: Cross section of heat transfer network from gas to water/steam

## 5.2 Local energy balance

For each differential segment of length  $dx$ , the model enforces a one dimensional steady state energy balance between the gas, the water and the tube wall:

- Heat transferred across the wall:

$$q'(x) = UA'(x) [T_g(x) - T_w(x)] \quad (5.1)$$

- Relation to the segment duty:

$$dQ(x) = q'(x) dx \quad (5.2)$$

- Gas stream:

$$dQ(x) = -\dot{m}_g dh_g(x) \Rightarrow \frac{dh_g}{dx} = -\frac{q'(x)}{\dot{m}_g} \quad (5.3)$$

- Water stream:

$$dQ(x) = +\dot{m}_w dh_w(x) \Rightarrow \frac{dh_w}{dx} = +\frac{q'(x)}{\dot{m}_w} \quad (5.4)$$

In the numerical implementation these equations are applied in finite difference form over each marching step:

$$Q_{\text{step}} = q'(x) \Delta x \quad (5.5)$$

$$\Delta h_g = -\frac{Q_{\text{step}}}{\dot{m}_g}, \quad \Delta h_w = +\frac{Q_{\text{step}}}{\dot{m}_w} \quad (5.6)$$

### 5.3 Overall conductance and resistance network

The overall conductance per unit length  $UA'(x)$  is obtained from a radial series of thermal resistances per unit length:

- Gas side convection:

$$R'_g = \frac{1}{h_g(x) P_g} \quad (5.7)$$

- Gas side fouling:

$$R'_{fg} = R'_{fi}(P_g) \quad (\text{from specified fouling thickness and conductivity}) \quad (5.8)$$

- Tube wall:

$$R'_w = \frac{\ln(D_o/D_i)}{2\pi k_w} \quad (5.9)$$

- Water side fouling:

$$R'_{fc} = R'_{fo}(P_w) \quad (5.10)$$

- Water side convection:

$$R'_c = \frac{1}{h_w(x) P_w} \quad (5.11)$$

where  $D_i$  and  $D_o$  are the tube inner and outer diameters and  $k_w$  is the tube wall thermal conductivity. Combining these contributions:

$$\frac{1}{UA'(x)} = R'_g + R'_{fg} + R'_w + R'_{fc} + R'_c \quad (5.12)$$

or equivalently,

$$UA'(x) = \left[ \frac{1}{h_g P_g} + R'_{fg} + R'_w + R'_{fc} + \frac{1}{h_w P_w} \right]^{-1} \quad (5.13)$$

The linear heat flux then follows directly:

$$q'(x) = UA'(x) [T_g(x) - T_w(x)] \quad (5.14)$$

## 5.4 Wall temperature update and thermal convergence

The tube wall temperatures on the gas and water sides,  $T_{gw}$  and  $T_{ww}$ , are updated using a two node wall model in each marching step.

Given  $q'(x)$ , the wall side energy balances yield:

$$T_{gw} = T_g - \frac{q'}{h_{g,\text{tot}}} \quad (5.15)$$

$$T_{ww} = T_w + \frac{q'}{h_w} \quad (5.16)$$

The wall conduction temperature drop is:

$$\Delta T_{\text{wall}} = T_{gw} - T_{ww} \quad (5.17)$$

which is also equal to:

$$\Delta T_{\text{wall}} = q' [R'_{fg} + R'_w + R'_{fc}] \quad (5.18)$$

A consistency check is applied; if the implied wall temperature difference from conduction differs from the one implied by convection, the marching solver iterates the HTC evaluation once with relaxed updates (default under-relaxation factor 0.35).

In the actual implementation this consistency check is performed by iterating on  $T_{gw}$ ,  $T_{ww}$ , and  $q'$  using the full resistance network (gas convection, gas fouling, wall, water fouling, water convection), with an under-relaxation factor applied to both wall temperatures and the linear heat flux.

If temperature overshoot (negative film coefficient, reversed driving force) is detected within a step, the step is automatically halved and recomputed.

## 5.5 Stage and boiler level duties

For a stage of length  $L_j$ , the stage heat duty and stage level conductance are obtained by integrating the local quantities along  $x$ :

$$Q_{\text{stage},j} = \int_0^{L_j} q'(x) \, dx \approx \sum_i q'_i \Delta x_i \quad (5.19)$$

$$(UA)_j = \int_0^{L_j} UA'(x) \, dx \approx \sum_i UA'_i \Delta x_i \quad (5.20)$$

The total useful boiler duty is the sum of all stage duties:

$$Q_{\text{useful}} = \sum_{j=1}^6 Q_{\text{stage},j} \quad (5.21)$$

These integrated quantities are later used in the performance and efficiency evaluation (Section 7) and for constructing stage-wise summary tables.

## 5.6 Gas side

Gas side heat transfer is computed with geometry aware correlations based on local gas properties from Cantera (GasProps) and stage specific geometry from the GeometryBuilder. For each marching step, the total gas side HTC is split into a convective and a radiative contribution:

$$h_{g,\text{tot}} = h_{g,\text{conv}} + h_{g,\text{rad}} \quad (5.22)$$

The implementation uses the helper `gas_htc_parts(g, spec, T_{gw})`, which returns  $(h_{g,conv}, h_{g,rad})$  in  $\text{W/m}^2\cdot\text{K}$ , and then sums them in `gas_htc`.

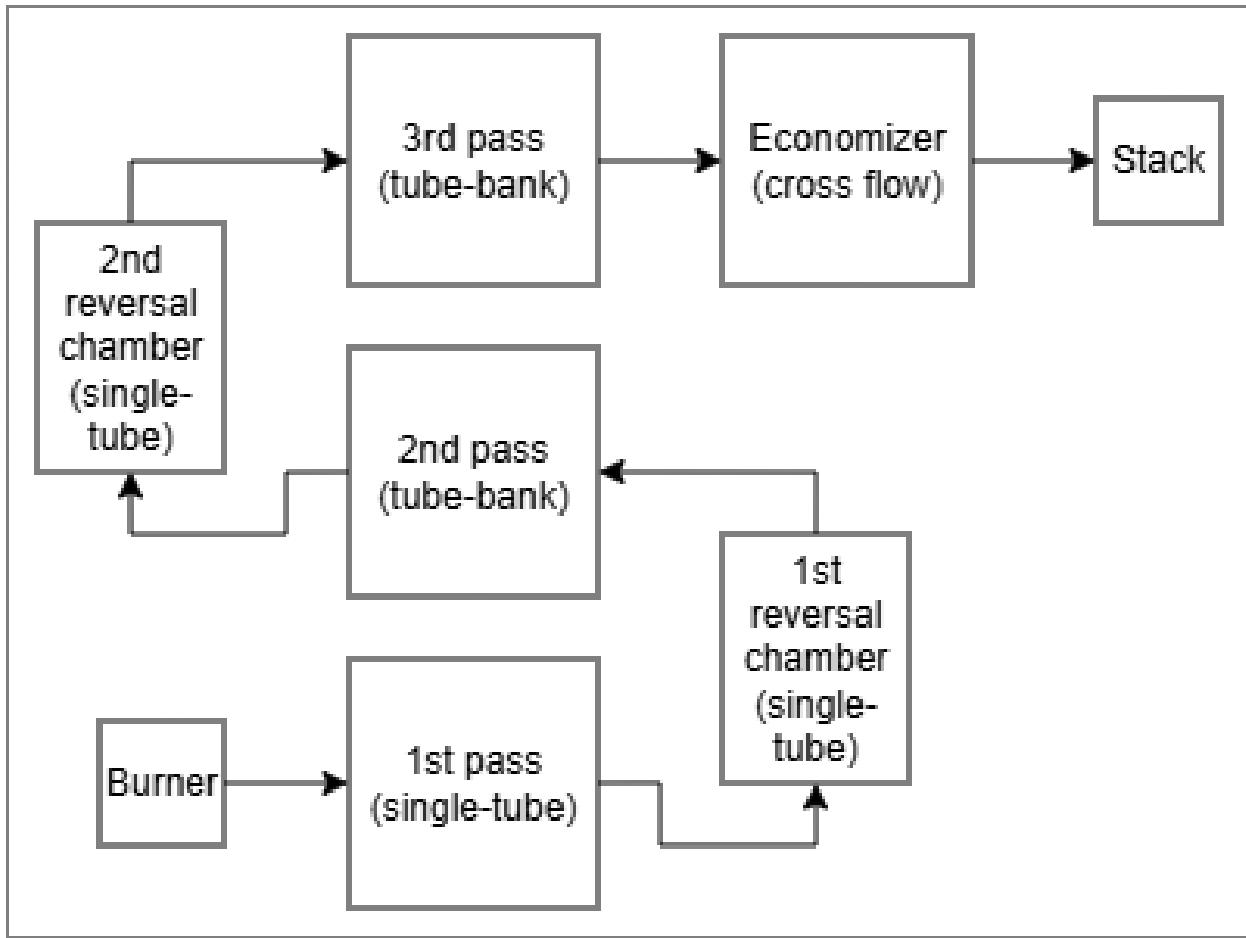


Figure 5.2: Path of flue gas through the 6 stages

### 5.6.1 Single tube and reversal chamber

Stages of kind `single_tube` and `reversal_chamber`, corresponding to furnace (first pass), and both reversal chambers, are treated as internal forced convection in a circular duct. The characteristic quantities are:

- Diameter:  $D$  (supplied by `stages.yaml`)
- Length:  $L$  (supplied by `stages.yaml`)
- Flow area:  $A = \frac{1}{4} \pi D^2$  (calculated by geometry builder)
- Velocity:

$$V = \frac{\dot{m}_g}{\rho_g A} \quad (5.23)$$

- Reynolds and Prandtl numbers:

$$\text{Re} = \frac{\rho_g V D}{\mu_g}, \quad \text{Pr} = \frac{c_{p,g} \mu_g}{k_g} \quad (5.24)$$

Local gas properties  $\rho_g, \mu_g, k_g, c_{p,g}$  are obtained from the Cantera mixture via the functions defined in `common\props.py`, at the local gas temperature and pressure. [5]

### Laminar/developing flow (Graetz-type)

For  $\text{Re} < 2300$ , uses a Graetz correlation for thermally developing laminar flow:

$$Gz = \text{Re} \text{Pr} \frac{D}{L} \quad (5.25)$$

$$\text{Nu} = 3.66 + \frac{0.0668 Gz}{1 + 0.04 Gz^{2/3}} \quad (5.26)$$

[6]

### Turbulent flow (Gnielinski with Petukhov friction factor)

For  $\text{Re} \geq 2300$ , the Gnielinski correlation is applied with a Petukhov friction factor:

$$f = (0.79 \ln \text{Re} - 1.64)^{-2} \quad (5.27)$$

[7]

$$\text{Nu} = \frac{\frac{f}{8}(\text{Re} - 1000) \text{Pr}}{1 + 12.7 \sqrt{\frac{f}{8}} (\text{Pr}^{2/3} - 1)} \quad (5.28)$$

[6] The local convective heat-transfer coefficient is then:

$$h_{g,\text{conv}} = \frac{\text{Nu} k_g}{D} \quad (5.29)$$

[6]

This same internal correlation is used for `single_tube`, `reversal_chamber` and `tube_bank` gas-side flow (see below).

## 5.6.2 Tube bank

Stages `tube_bank` correspond to tube bundles inside the shell, ie. first and second passes. In this model, the gas side is still treated as internal flow inside the tubes:

- Hot side (gas): inside tubes (inner diameter  $D_i$ ), using the same internal forced convection model as in Section 5.2.1.

Thus the gas side convective HTC in tube-bank stages is:

$$h_{g,\text{conv}}^{(\text{HX3,5})} = \frac{\text{Nu}(\text{Re}, \text{Pr}) k_g}{D_i} \quad (5.30)$$

with Nu given by the Graetz/Gnielinski formulation above, and Re, Pr computed from the local gas properties and tube hydraulic diameter.

## 5.6.3 Economizer

The economizer `economiser` stage reverses the roles: gas flows outside the tubes in cross flow, while water flows inside. The gas side convection is then modelled as external cross flow over a tube bank.

Key geometry quantities (from `GeometryBuilder` for the economizer):

- Tube outer diameter:  $D = D_o$
- Gas side cross flow area:  $A_{\text{bulk}} = A_{\text{hot,flow}}$
- Optional maximum/mean velocity factor:

$$V_{\text{bulk}} = \frac{\dot{m}_g}{\rho_g A_{\text{bulk}}}, \quad V = u_{\max} V_{\text{bulk}} \quad (5.31)$$

where  $u_{\max}$  is calculated depending on the tube bank arrangement and spacing between tubes.

- Reynolds and Prandtl numbers:

$$\text{Re} = \frac{\rho_g V D}{\mu_g}, \quad \text{Pr} = \frac{c_{p,g} \mu_g}{k_g} \quad (5.32)$$

For "economiser" stages the primary correlation is a banded Zukauskas form for cross flow over tube banks:

$$\text{Nu} = C \text{Re}^m \text{Pr}^n \quad (5.33)$$

[6]

where the coefficients  $C, m$  are selected from standard bands as a function of Reynolds number and tube arrangement (inline vs staggered), and the exponent  $n$  is:

$$n = \begin{cases} 0.36, & \text{Pr} \leq 10 \\ 0.25, & \text{Pr} > 10 \end{cases} \quad (5.34)$$

If  $\text{Re}$  falls outside the tabulated bands, the model falls back to the Churchill–Bernstein correlation for cross flow over a single cylinder:

$$\text{Nu} = 0.3 + \frac{0.62 \text{Re}^{1/2} \text{Pr}^{1/3}}{\left[1 + (0.4/\text{Pr})^{2/3}\right]^{1/4}} \left[1 + \left(\frac{\text{Re}}{282000}\right)^{5/8}\right]^{4/5} \quad (5.35)$$

[6] The gas-side convective HTC in the economizer is then:

$$h_{g,\text{conv}}^{(\text{HX6})} = \frac{\text{Nu} k_g}{D_o} \quad (5.36)$$

[6]

#### 5.6.4 Radiation model

Radiative heat transfer from the flue gas to the furnace surfaces is explicitly accounted for by a participating medium model for the  $H_2O/CO_2$  mixture. The implementation follows a simplified Smith–Shen–Friedman style four gray model.

For each step, the gas emissivity is computed as:

1. Partial pressures of participating species:

$$p_{H_2O} = y_{H_2O} P, \quad p_{CO_2} = y_{CO_2} P \quad (5.37)$$

[8] where  $y_i$  are molar (or mass-fraction-equivalent) composition entries from the flue gas stream, and  $P$  is the local gas pressure.

2. Mean beam length:

$$L_b = \begin{cases} L_{\text{rad,override}}, & \text{if specified in the stage} \\ 0.9 D_{h,\text{gas}}, & \text{otherwise} \end{cases} \quad (5.38)$$

[8] with  $D_{h,\text{gas}}$  the gas-side hydraulic diameter.

3. Effective optical thickness in each gray band:

$$p_{\text{ratio}} = \frac{p_{\text{H}_2\text{O}} + p_{\text{CO}_2}}{P_{\text{atm}}} \quad (5.39)$$

[8]

$$\tau_j = K_j \left( \frac{T}{1000 \text{ K}} \right)^{T_{\text{exp}}} p_{\text{ratio}} L_b \quad (5.40)$$

[8]

where  $K_j$  and weighting factors  $A_j$  are fixed band coefficients,  $T$  is the gas temperature, and  $T_{\text{exp}}$  is a temperature exponent (default 0.65, configurable per stage via `rad_Texp`).

4. Total gas emissivity:

$$\varepsilon_g = 1 - \sum_{j=1}^4 A_j \exp(-\tau_j) \quad (5.41)$$

[8] with  $\varepsilon_g$  constrained to  $[0, 1]$ .

A mean-film temperature is used for the linearized radiative HTC:

$$T_{\text{film}} = \frac{T_g + T_{gw}}{2} \quad (5.42)$$

$$h_{g,\text{rad}} = 4 \sigma F \varepsilon_g T_{\text{film}}^3 \quad (5.43)$$

[8]

where:

- $\sigma$  is the Stefan–Boltzmann constant,
- $F$  is an effective view factor (default 1.0 or stage-specific `rad_F`).

The gas-side total HTC reported and used in the resistance network is then:

$$h_{g,\text{tot}} = h_{g,\text{conv}} + h_{g,\text{rad}} \quad (5.44)$$

and the corresponding convective/radiative contributions to the linear heat flux are tracked via:

$$q'_{\text{conv}} = q' \frac{h_{g,\text{conv}}}{h_{g,\text{tot}}}, \quad q'_{\text{rad}} = q' - q'_{\text{conv}} \quad (5.45)$$

These diagnostics are later integrated on a per-stage basis to quantify the share of convective vs radiative heat transfer in each section of the boiler.

## 5.7 Water side

Water side heat transfer is computed with geometry dependent correlations using local water properties from IAPWS97 (WaterProps), with stage specific geometry from the GeometryBuilder. The solver always works with a single effective water side heat transfer coefficient  $h_w(x)$  per marching step, which may represent:

- pure pool boiling at a saturated surface,
- a Chen type combination of forced convection and nucleate boiling, or
- single phase forced convection.

In the implementation this logic is encapsulated in `water_htc`, which returns ( $h_w$ ) for each step.

### 5.7.1 General formulation and boiling treatment

The six stages of the boiler are divided, from the water-side point of view, into:

- $\text{HX}_1\text{--}\text{HX}_5$ : pool-boiling stages  
(`pool_boiling = true` in the stage specification)
- $\text{HX}_6$ : economizer stage  
(`pool_boiling = false`)

## Process in boilers drawn in T-S chart

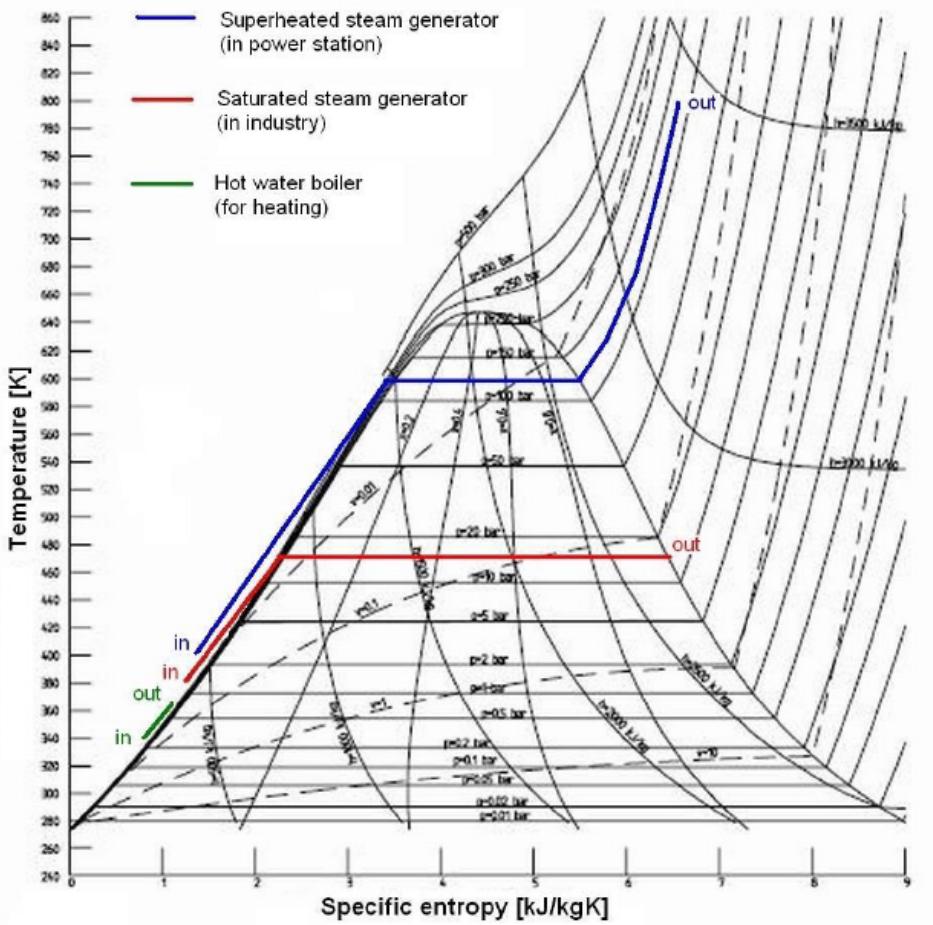


Figure 5.3: Temperature–entropy ( $T$ – $s$ ) representation of the feedwater heating and evaporation process across economiser and boiler at the operating pressure.

The solver applies the following decision tree at each marching step:

1. Pool-boiling stages ( $\text{HX}_1$ – $\text{HX}_5$ )

If the stage is flagged as `pool_boiling = true`, the bulk water temperature entering the wall-energy balance is fixed at the saturation temperature at the local pressure:

$$T_w = T_{\text{sat}}(p_w), \quad (5.46)$$

and the water-side HTC is computed from the Cooper pool boiling correlation for nucleate boiling correlation:

$$h_{\text{Cooper}} = 55 p_r^{0.12} R_p^{-0.55} M_w^{-0.5} (q'')^{0.67} \quad (5.47)$$

where

$$p_r = \frac{p}{p_{\text{crit}}} = \text{reduced pressure}, \quad R_p = \text{surface roughness } (\mu\text{m}), \quad q'' = \text{heat flux}. \quad (5.48)$$

[6]

This nucleate-boiling HTC is then used directly:

$$h_w = h_{w,\text{nb}}, \quad (5.49)$$

and the step is always marked as boiling in the post processing.

In other words, the main boiling surfaces of the boiler (furnace, passes, reversal chambers) are represented as heated surfaces in a saturated pool, with the HTC governed by the local heat flux and surface roughness rather than by a detailed prediction of liquid velocity. This matches the natural circulation character of these sections.

## 2. Non pool boiling stages (HX<sub>6</sub>, economizer)

For stages with `pool_boiling = false`, the model can represent both single phase convection and flow boiling via a Chen type formulation.

### a. Boiling detection

A helper determines whether the local state is boiling based on the bulk enthalpy  $h$  and, when needed, the wall temperature  $T_{\text{wall}}$ :

- if

$$h_f(p_w) \leq h \leq h_g(p_w) \quad (5.50)$$

the state is inside the saturation interval and is treated as two phase;

- if  $h < h_f(p_w)$  (slightly subcooled liquid) but the wall superheat is sufficiently high,

$$T_{\text{wall}} > T_{\text{sat}}(p_w) + \Delta T_{\text{crit}}, \quad (5.51)$$

the state is also treated as boiling;

- otherwise the flow is treated as single-phase liquid.

Here  $h_f$  and  $h_g$  are saturated-liquid and saturated vapor enthalpies at the local pressure, obtained via IAPWS97.

### b. Single-phase regime

If boiling is not detected, the water side HTC is purely convective:

$$h_w = h_{w,\text{conv}}, \quad (5.52)$$

with  $h_{w,\text{conv}}$  obtained from a geometry dependent forced convection correlation (internal tube, external tube bank, or external single tube/bend) as detailed in Sections [5.7.2]–[5.7.4].

### c. Flow boiling regime (Chen model)

When boiling is detected in a non pool boiling stage, the HTC is constructed as a Chen type superposition of:

- a liquid only convective term  $h_{\text{lo}}$ , and
- a nucleate-boiling term  $h_{\text{nb}}$  using the same Cooper correlation as in pool boiling.

The liquid only HTC is evaluated at the saturation temperature  $T_{\text{sat}}(p)$  and using the appropriate geometry correlation:

$$h_{\text{lo}} = h_{\text{single-phase}}(T_{\text{sat}}(p), \text{geometry}), \quad (5.53)$$

while the nucleate-boiling term is

$$h_{\text{nb}} = h_{\text{Cooper}}(p, q''). \quad (5.54)$$

The Chen combination used in the code is:

$$h_w = F h_{\text{lo}} + S h_{\text{nb}}. \quad (5.55)$$

[6]

The convection enhancement factor  $F$  is based on a Martinelli type parameter  $X_{tt}$ ,

$$X_{tt} = \left(\frac{1-x}{x}\right)^{0.9} \left(\frac{\mu_l}{\mu_g}\right)^{0.1} \left(\frac{\rho_g}{\rho_l}\right)^{0.5}, \quad (5.56)$$

where  $x$  is the local vapor quality and  $\rho_l, \rho_g, \mu_l, \mu_g$  are liquid/vapor densities and viscosities at saturation. A bounded form of the Chen factor is then used:

$$F = 1 + 0.12 X_{tt}^{-0.8}, \quad (5.57)$$

The suppression factor  $S$  modulating the nucleate boiling contribution is a function of mass flux and Reynolds number:

$$S = \frac{1}{1 + C \text{Re}_{\text{lo}}^\alpha}, \quad (5.58)$$

where  $\text{Re}_{\text{lo}}$  is a liquid only Reynolds number based on the mass flux

$$G = \frac{\dot{m}_w}{A_{\text{flow}}}, \quad (5.59)$$

and the liquid properties at saturation. In the implementation the constants and bounds are chosen such that  $S$  remains between about 0.1 and 1.0, reducing the nucleate boiling influence at very high mass flux (strong forced convection).

In the present thesis this Chen type flow boiling capability is only exercised in the economizer stage; the main boiling sections ( $\text{HX}_1$ – $\text{HX}_5$ ) use the pure pool boiling representation above.

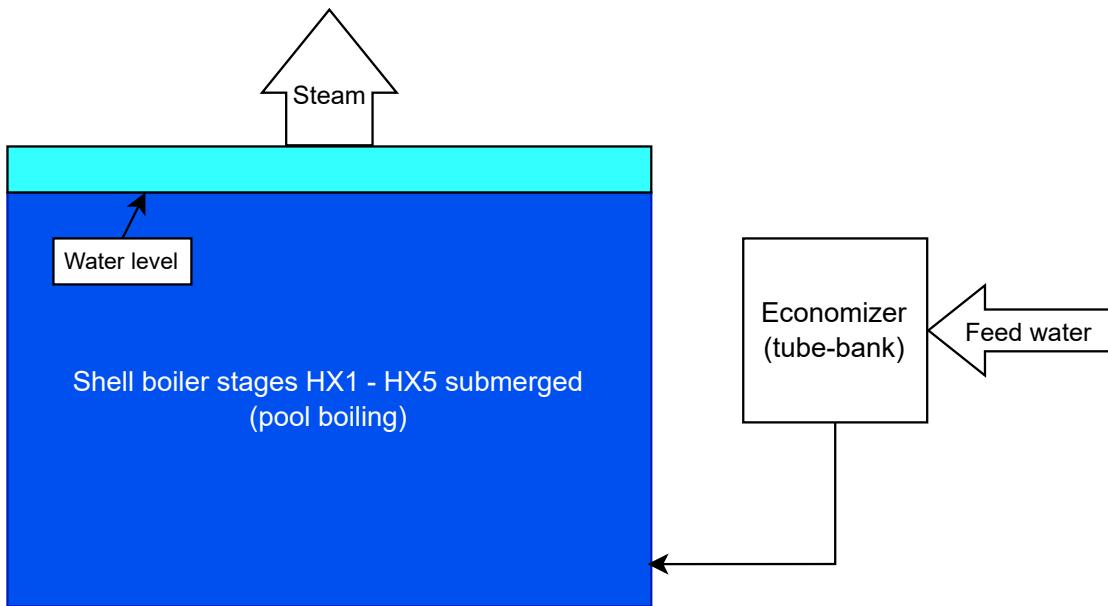


Figure 5.4: Path of water/steam through the 6 stages

### 5.7.2 Economizer

In the economizer stage ( $\text{HX}_6$ , kind = "economiser"), water flows inside the tubes and is heated by the flue gas flowing externally in cross flow. This stage is the only one where `pool_boiling = false` and where the full single phase/Chen type boiling formulation is used.

#### Velocity and dimensionless groups

The relevant geometric quantities for the water side are:

- tube inner diameter:  $D_i$ ,
- tube length:  $L$ ,

- cold-side flow area:  $A_{\text{cold,flow}}$ .

The bulk water velocity, Reynolds and Prandtl numbers are:

$$V_w = \frac{\dot{m}_w}{\rho_w A_{\text{cold,flow}}}, \quad (5.60)$$

$$\text{Re}_w = \frac{\rho_w V_w D_i}{\mu_w}, \quad \text{Pr}_w = \frac{c_{p,w} \mu_w}{k_w}, \quad (5.61)$$

with  $\rho_w, \mu_w, k_w, c_{p,w}$  evaluated from IAPWS97 at the film temperature. [9]

### Single phase internal flow correlation

When no boiling is detected in the economizer, the Nusselt number is computed using a Gnielinski type internal flow correlation with a viscosity ratio correction:

- Laminar / developing regime ( $\text{Re}_w < 2300$ ): a Graetz type form is used

$$\text{Gz}_w = \text{Re}_w \text{Pr}_w \frac{D_i}{L}, \quad (5.62)$$

$$\text{Nu}_w = 3.66 + \frac{0.0668 \text{Gz}_w}{1 + 0.04 \text{Gz}_w^{2/3}}. \quad (5.63)$$

- Turbulent regime ( $\text{Re}_w \geq 2300$ ): Gnielinski correlation with friction factor

$$f_w = (0.79 \ln \text{Re}_w - 1.64)^{-2}, \quad (5.64)$$

[7]

$$\text{Nu}_w = \frac{\frac{f_w}{8} (\text{Re}_w - 1000) \text{Pr}_w}{1 + 12.7 \sqrt{\frac{f_w}{8}} (\text{Pr}_w^{2/3} - 1)}, \quad (5.65)$$

[6] scaled by a viscosity-ratio correction:

$$\text{Nu}_w \leftarrow \text{Nu}_w \left( \frac{\mu_b}{\mu_w} \right)^{0.11}, \quad (5.66)$$

where  $\mu_b$  is evaluated at the bulk temperature and  $\mu_w$  at the wall temperature.

The single phase water side HTC in the economizer is then:

$$h_{w,\text{conv}}^{(\text{HX6})} = \frac{\text{Nu}_w k_w}{D_i}. \quad (5.67)$$

[6]

## Flow boiling in the economizer

If boiling is detected in the economizer (according to the criteria in the general formulation), the same geometry and mass flux information are used to form the liquid only HTC  $h_{lo}$  and the Cooper nucleate boiling HTC  $h_{nb}$ . The total water side HTC is then:

$$h_w = F h_{lo} + S h_{nb}, \quad (5.68)$$

with  $F$  and  $S$  given by the Chen type relations described above, using the local vapor quality, mass flux, and saturation properties. This provides a smooth transition between predominantly convective and predominantly nucleate boiling regimes in the economizer.

### 5.7.3 Tube bank stages

For completeness, the water side model also includes correlations for cross flow over tube banks on the cold side (`kind = "tube_bank"`), although in the present thesis these stages are operated in pool boiling mode (so that only the Cooper correlation is used). When a tube bank description is required on the water side, the geometry is:

- tube outer diameter:  $D_o$ ,
- cold-side flow area:  $A_{\text{cold,flow}}$ ,
- number of rows:  $N_{\text{rows}}$ ,
- transverse and longitudinal pitches:  $S_T, S_L$ ,
- bundle arrangement: inline or staggered.

The water velocity, Reynolds and Prandtl numbers are:

$$V_w = \frac{\dot{m}_w}{\rho_w A_{\text{cold,flow}}}, \quad (5.69)$$

$$\text{Re}_w = \frac{\rho_w V_w D_o}{\mu_w}, \quad \text{Pr}_w = \frac{c_{p,w} \mu_w}{k_w}. \quad (5.70)$$

A Zukauskas-type banded correlation is then applied:

$$\text{Nu}_w = C \text{Re}_w^m \text{Pr}_w^n, \quad (5.71)$$

[6] where:

- $C, m$  are selected from standard Zukauskas bands based on  $\text{Re}_w$  and the arrangement (inline or staggered),
- the exponent  $n$  is

$$n = \begin{cases} 0.36, & \text{Pr}_w \leq 10 \\ 0.25, & \text{Pr}_w > 10 \end{cases} \quad (5.72)$$

The raw Nusselt number is further modified by:

- a row factor  $f_{\text{row}}(N_{\text{rows}})$  that accounts for the finite number of tube rows, and
- a spacing factor  $\phi(S_T, S_L, D_o)$  that accounts for maximum velocity effects in the tube bank (greater constriction  $\Rightarrow$  higher HTC).

If  $\text{Re}_w$  falls outside the Zukauskas validity range, the model falls back to the Churchill Bernstein correlation for cross flow over a single cylinder:

$$\text{Nu}_w = 0.3 + \frac{0.62 \text{Re}_w^{1/2} \text{Pr}_w^{1/3}}{\left[1 + (0.4/\text{Pr}_w)^{2/3}\right]^{1/4}} \left[1 + \left(\frac{\text{Re}_w}{282000}\right)^{5/8}\right]^{4/5}. \quad (5.73)$$

[6]

The corresponding water side HTC for a tube-bank configuration is:

$$h_{w,\text{conv}}^{(\text{bank})} = \frac{\text{Nu}_w k_w}{D_o}. \quad (5.74)$$

[6]

When such a tube bank model is used inside the Chen formulation,  $h_{l_0}$  is taken from this  $h_{w,\text{conv}}^{(\text{bank})}$ .

### 5.7.4 Single tube and reversal chamber stages

Stages of kind `single_tube` and `reversal_chamber` correspond, on the water side, to external flow around one or more tubes within the drum/shell region. In the current thesis these are also operated in pool boiling mode (`pool_boiling = true`), so the Cooper pool boiling correlation described in the general formulation dominates their behavior. Nevertheless, the implementation includes external forced convection correlations for completeness.

For these stages the characteristic length for the water side is the tube outer diameter  $D_o$ , and the cold side flow area  $A_{\text{cold,flow}}$  is defined by the drum cross section minus the tube area(s). When a cross flow description is used for single-phase or liquid only HTC:

- water velocity, Reynolds and Prandtl numbers:

$$V_w = \frac{\dot{m}_w}{\rho_w A_{\text{cold,flow}}}, \quad (5.75)$$

$$\text{Re}_w = \frac{\rho_w V_w D_o}{\mu_w}, \quad \text{Pr}_w = \frac{c_{p,w} \mu_w}{k_w}. \quad (5.76)$$

For a single tube in cross flow (or, by approximation, a relatively open bundle) a Churchill Bernstein style correlation is used:

$$\text{Nu}_w = 0.3 + \frac{0.62 \text{Re}_w^{1/2} \text{Pr}_w^{1/3}}{\left[1 + (0.4/\text{Pr}_w)^{2/3}\right]^{1/4}} \left[1 + \left(\frac{\text{Re}_w}{282000}\right)^{5/8}\right]^{4/5}, \quad (5.77)$$

[6] leading to

$$h_{w,\text{conv}}^{(\text{single})} = \frac{\text{Nu}_w k_w}{D_o}. \quad (5.78)$$

In reversal chamber segments, the tubes are bent, and the model applies the same base correlation multiplied by a curvature (bend) factor:

$$h_{w,\text{conv}}^{(\text{rev})} = \phi_{\text{bend}}(D_o, R_c) \frac{\text{Nu}_w k_w}{D_o}, \quad (5.79)$$

where  $R_c$  is the bend radius and  $\phi_{\text{bend}} \geq 1$  is a modest enhancement (up to roughly 1.25) for tight bends, reflecting locally increased turbulence around the bend region.

In pool boiling operation these external convection correlations are only used implicitly inside the liquid only component  $h_{\text{lo}}$  when the Chen type formulation is invoked. For the main boiling sections in this thesis, however, the water side is predominantly controlled by the Cooper pool boiling correlation with  $T_w = T_{\text{sat}}(p)$ .

# Chapter 6

## Hydraulic Model

Hydraulic behavior is extracted directly from the solver through the per step pressure drop decomposition implemented in `heat/solver.py` (`_gas_dp_components`, `pressure_drop_gas`) and accumulated at the stage level in `heat/solver.py::solve_stage`.

The model divides gas side pressure losses into:

- Frictional losses
- Minor losses (inlet, outlet, bends, etc.)
- Total pressure drop (sum of the above)

### 6.1 Frictional losses

#### Gas and water sides

The per step frictional pressure drop follows a standard 1D Darcy formulation:

$$\Delta P_{\text{fric}} = -f \frac{\Delta x}{D_h} \left( \frac{\rho V^2}{2} \right) \quad (6.1)$$

[10]

Here:

- $f$  is the Darcy friction factor,
- $D_h$  is the relevant side hydraulic diameter ( $D_h = \text{hot\_Dh}$  for gas,  $D_h = \text{cold\_Dh}$  for water),
- $\rho$  and  $V$  are local density and velocity on the relevant side,
- $\Delta x$  is the current marching step length.

The friction factor is computed from Reynolds number and relative roughness via `_friction_factor`:

- Laminar ( $\text{Re} < 2300$ ):

$$f = \frac{64}{\text{Re}} \quad (6.2)$$

[10]

- Transitional ( $2300 \leq \text{Re} < 4000$ ): linear blend between laminar and turbulent values:

$$f = (1 - w)f_{\text{lam}} + wf_{\text{turb}}, \quad w = \frac{\text{Re} - 2300}{4000 - 2300} \quad (6.3)$$

[11]

- Turbulent ( $\text{Re} \geq 4000$ ): Colebrook–White is solved iteratively, seeded by the Swamee–Jain explicit approximation.

Swamee–Jain seed (used as the initial guess):

$$f_{\text{SJ}} = \frac{0.25}{\left[ \log_{10} \left( \frac{\varepsilon/D_h}{3.7} + \frac{5.74}{\text{Re}^{0.9}} \right) \right]^2} \quad (6.4)$$

[12]

Colebrook–White equation solved iteratively in the code:

$$\frac{1}{\sqrt{f}} = -2 \log_{10} \left( \frac{\varepsilon/D_h}{3.7} + \frac{2.51}{\text{Re}\sqrt{f}} \right) \quad (6.5)$$

[10]

The iteration is performed on  $1/\sqrt{f}$  until convergence.

Local velocity and Reynolds number are evaluated using the side flow area  $A$  and properties:

$$V = \frac{\dot{m}}{\rho A}, \quad \text{Re} = \frac{\rho V D_h}{\mu} \quad (6.6)$$

Frictional losses are only applied for the economiser water side branch in `_water_dp_components`; for other stage kinds the current model sets  $\Delta P_{\text{fric}} = 0$ .

## 6.2 Gas-side pressure drop in the economiser

The economiser gas-side hydraulics differ fundamentally from all other modeled stages. While other stages assume **internal flow** and apply a Darcy–Weisbach formulation, the economiser models **external crossflow over a tube bank**, and gas-side pressure losses are therefore computed using a **bundle loss (drag-based) formulation** rather than a wall-friction model.

Accordingly, the standard Darcy friction term described above is **not used** for the economiser gas side.

### Crossflow bundle formulation

For an economiser stage, the solver uses a tube-bank pressure loss model implemented in

`heat/solver.py::_gas_dp_economiser_crossflow`.

The gas flows across a bank of tubes arranged either inline or staggered.

A characteristic velocity is defined using a bulk velocity corrected by a geometry-dependent maximum-velocity factor:

$$V_{\text{bulk}} = \frac{\dot{m}}{\rho A_{\text{hot}}}, \quad V_{\text{char}} = u_{\max} V_{\text{bulk}} \quad (6.7)$$

where:

- $A_{\text{hot}}$  = `hot_flow_A` is the free crossflow area,
- $u_{\max}$  = `umax_factor` accounts for flow acceleration between tubes.

#### Note on velocity definitions.

For economiser gas-side pressure losses, the solver uses the *maximum inter-tube velocity*  $V_{\text{char}} = u_{\max} V_{\text{bulk}}$  to form Reynolds number and dynamic pressure.

However, reported gas velocities in summaries and post-processing are based on the bulk velocity  $V_{\text{bulk}}$ .

As a result, economiser pressure losses should not be correlated directly with reported average velocities without accounting for  $u_{\max}$ .

The Reynolds number is formed using the tube outer diameter:

$$\text{Re}_D = \frac{\rho V_{\text{char}} D_o}{\mu} \quad (6.8)$$

with  $D_o$  = `outer_diameter`.

## Bundle loss coefficient

The pressure loss per tube row is expressed via a dimensionless bundle loss coefficient:

$$\zeta_{\text{row}} = C_0 \text{Re}_D^m \Phi_{\text{geom}} \quad (6.9)$$

where:

- $C_0$  and  $m$  depend on tube arrangement (inline or staggered),
- $\Phi_{\text{geom}}$  accounts for pitch ratios:

$$\Phi_{\text{geom}} = \left( \frac{S_T/D_o}{1.5} \right)^{-0.2} \left( \frac{S_L/D_o}{1.5} \right)^{-0.2} \quad (6.10)$$

with transverse pitch  $S_T$  and longitudinal pitch  $S_L$ .

The total bundle loss coefficient is then:

$$\zeta_{\text{bundle}} = N_{\text{rows}} \zeta_{\text{row}} \quad (6.11)$$

where  $N_{\text{rows}} = \text{n\_rows}$  is the number of tube rows in the flow direction.

## Distributed pressure loss

The dynamic pressure is evaluated using the characteristic velocity:

$$q = \frac{\rho V_{\text{char}}^2}{2} \quad (6.12)$$

The total bundle pressure drop is:

$$\Delta P_{\text{bundle}} = -\zeta_{\text{bundle}} q \quad (6.13)$$

This loss is **distributed uniformly** along the economiser length  $L$  across the marching steps:

$$\Delta P_{\text{fric,step}} = \Delta P_{\text{bundle}} \frac{\Delta x}{L} \quad (6.14)$$

where  $\Delta x$  is the local marching step length.

## Minor losses in the economiser

In addition to the distributed bundle loss, inlet, outlet, and bend losses are applied using standard  $K$ -coefficients:

$$\Delta P_{\text{minor}} = -K_{\text{minor}} q \quad (6.15)$$

with:

$$K_{\text{minor}} = K_{\text{bend,per-step}} + \mathbb{1}_{i=0} K_{\text{hot,inlet}} + \mathbb{1}_{i=n-1} K_{\text{hot,outlet}} \quad (6.16)$$

The bend loss is distributed uniformly across the  $n$  marching steps.

## Total gas-side pressure drop (economiser)

For an economiser step, the total gas-side pressure change is therefore:

$$\Delta P_{\text{total}} = \Delta P_{\text{bundle,step}} + \Delta P_{\text{minor}} \quad (6.17)$$

This value replaces the Darcy-based formulation used in all other stages and is applied step-wise in the same manner:

$$P_{i+1} = P_i + \Delta P_{\text{total}} \quad (6.18)$$

Gas compressibility effects are captured through the dependence of  $\rho(T, P)$  and  $\mu(T, P)$  on the local thermodynamic state.

## 6.3 Minor losses

Minor losses are applied using per-stage catalogue  $K$  values and the standard dynamic-pressure formulation:

$$\Delta P_{\text{minor}} = -K_{\text{minor}} \left( \frac{\rho V^2}{2} \right) \quad (6.19)$$

[11]

The total minor-loss coefficient  $K_{\text{minor}}$  is assembled differently for gas and water sides, but applied through the same formulation.

## Coefficient assembly

### Gas side.

For each stage, the total loss coefficient is assembled from geometry and user inputs:

$$K_{\text{minor}} = K_{\text{contraction}} + K_{\text{expansion}} + K_{\text{bend}} \quad (6.20)$$

Where:

- $K_{\text{contraction}}$ : accounts for sudden expansion of flow area (e.g.  $\text{HX}_2 \rightarrow \text{HX}_3$ ), default = 0.5.
- $K_{\text{expansion}}$  (Borda–Carnot): losses caused by sudden expansion of flow area (e.g.  $\text{HX}_1 \rightarrow \text{HX}_2$ ), default = 1.
- $K_{\text{bend}}$ : losses due to gas flow rotation in reversal chambers, default = 0.

### Water side.

Water-side minor losses are applied via per-stage catalogue coefficients in `heat/solver.py`::`_water_dp_coefficients`:

- $K_{\text{cold,bend}} = \text{k\_cold\_bend}$
- $K_{\text{cold,inlet}} = \text{k\_cold\_inlet}$
- $K_{\text{cold,outlet}} = \text{k\_cold\_outlet}$

The bend loss is distributed uniformly across the  $n$  marching steps:

$$K_{\text{bend,per-step}} = \frac{K_{\text{cold,bend}}}{n} \quad (6.21)$$

The per-step assembled coefficient is:

$$K_{\text{minor}} = K_{\text{bend,per-step}} + \mathbb{1}_{i=0} K_{\text{cold,inlet}} + \mathbb{1}_{i=n-1} K_{\text{cold,outlet}} \quad (6.22)$$

## Application

For both gas and water sides, the minor-loss pressure drop is computed using the local dynamic pressure:

$$V = \frac{\dot{m}}{\rho A}, \quad q = \frac{\rho V^2}{2}, \quad \Delta P_{\text{minor}} = -K_{\text{minor}} q \quad (6.23)$$

where  $A$  is the relevant side flow area ( $A = \text{cold\_flow\_A}$  for water, gas-side area otherwise).

## 6.4 Total pressure drop

For each step, the total side pressure change is the sum of frictional and minor components:

$$\Delta P_{\text{total}} = \Delta P_{\text{fric}} + \Delta P_{\text{minor}} \quad (6.24)$$

[10]

This is what `pressure_drop_gas/water` return and what is applied to the streams in `update_gas/water_after_step`.

## 6.5 Coupling of $\Delta P$ into the energy solver

Gas/water pressure is updated step-wise using the same  $\Delta P$  model:

$$P_{i+1} = P_i + \Delta P_{\text{total}}(P_i, T_i, \dots) \quad (6.25)$$

After each step:

1. The local gas/water state ( $T_i, P_i$ , composition) is used to evaluate  $\rho, \mu, k$ , and  $c_p$ .
2. The friction factor and dynamic pressure are computed from these properties.
3.  $\Delta P_{\text{fric}}$  and  $\Delta P_{\text{minor}}$  are formed.
4. The updated pressure  $P_{i+1}$  is used for the next step.

In this way, compressibility enters through the pressure dependence of  $\rho(T, P)$  and  $\mu(T, P)$  and their effect on  $V$ ,  $\text{Re}$ , and  $f$ .

# Chapter 7

## Performance

This section summarizes the boiler level performance obtained from the coupled combustion heat transfer simulation. All numerical values are extracted from the stages summary and boiler summary data produced by the post-processing step `heat/postproc.py`.

### 7.1 solution procedure

For any given operating conditions, the main solver `run_boiler_case()` performs an outer fixed point iteration, on boiler efficiency, and water mass flow:

1. The combustion sub-model called by `Combustor.run()`, returns:
  - the lower heating value based firing rate  $P_{\text{LHV}}$ ,
  - the total combustion heat release  $Q_{\text{in}}$ ,
  - the adiabatic flame temperature  $T_{\text{ad}}$ ,
  - the fully burnt flue-gas stream at burner exit.
2. Given a current efficiency guess  $\eta^{(n)}$  and the combustion result, the corresponding feedwater/steam mass flow  $\dot{m}_w^{(n)}$  is computed by `_water_mass_from_efficiency()` as

$$h_{\text{in}} = h_{\text{fw}}(P_{\text{fw}}), \quad h_{\text{steam}} = h_g(P_{\text{fw}}), \quad (7.1)$$

$$\Delta h = h_{\text{steam}} - h_{\text{in}}, \quad (7.2)$$

$$Q_{\text{target}}^{(n)} = \eta^{(n)} Q_{\text{in}}, \quad (7.3)$$

$$\dot{m}_w^{(n)} = \frac{Q_{\text{target}}^{(n)}}{\Delta h}. \quad (7.4)$$

3. A WaterStream with mass flow  $\dot{m}_w^{(n)}$  is created and passed, together with the combustion flue gas GasStream and the drum/stage definitions, to the multi stage heat exchanger solver `run_hx()`.
4. `run_hx()` returns per stage and boiler level summary tables.
5. The new efficiency estimate is set to the indirect efficiency,

$$\eta^{(n+1)} := \eta_{\text{indirect}}^{(n)}, \quad (7.5)$$

And the procedure is repeated until the change in water mass flow between iterations is below the specified tolerance

$$|\dot{m}_w^{(n)} - \dot{m}_w^{(n-1)}| < 10^{-3} \text{ kg/s}, \quad (7.6)$$

or a maximum number of iterations is reached.

At convergence, returning:

- converged water/steam mass flow  $\dot{m}_{w,\text{base}}$ ,
- converged indirect efficiency  $\eta_{\text{indirect},\text{base}}$ ,

together with the corresponding boiler summary quantities (stack temperature, total pressure drop, etc.). These and more are exported to CSV as `boiler_summary.csv` and `stages_summary.csv`.

## 7.2 Energy balance

The total useful heat transferred from the flue gas to the water/steam side is obtained by integrating the local line heat flux  $q'(x)$  over all stages:

$$Q_{\text{useful}} = \sum_{k=1}^6 Q_{\text{stage},k} = \sum_{k=1}^6 \int_q' (x) dx \quad (7.7)$$

The total input heat from combustion  $Q_{\text{in}}$  is taken from the combustion module as the rate of heat release from complete fuel burnout:

## 7.3 Efficiency

Two boiler efficiencies are reported:

- Direct efficiency (LHV):

$$\eta_{\text{direct}} = \frac{Q_{\text{useful}}}{P_{\text{LHV}}} \quad (7.8)$$

- Indirect efficiency:

$$\eta_{\text{indirect}} = 1 - \frac{Q_{\text{losses}}}{Q_{\text{in}}} \quad (7.9)$$

## 7.4 Water/Steam flow rate convergence

The water/steam mass flow rate is obtained iteratively from an assumed overall boiler efficiency and the combustion heat input. At each iteration  $n$  the code:

1. Assumes an efficiency  $\eta^{(n)}$ .
2. Computes the target useful duty:

$$Q_{\text{target}}^{(n)} = \eta^{(n)} Q_{\text{in}} \quad (7.10)$$

3. Determines the required water mass flow  $\dot{m}_w^{(n)}$  from the enthalpy rise between feed-water and saturated steam at drum pressure:

$$\dot{m}_w^{(n)} = \frac{Q_{\text{target}}^{(n)}}{h_{\text{steam}}(P_{\text{drum}}) - h_{\text{fw}}} \quad (7.11)$$

4. Runs the full multi-stage heat-exchanger model with  $\dot{m}_w^{(n)}$  and reads back the resulting indirect efficiency  $\eta_{\text{indirect}}^{(n)}$ .
5. Sets the next efficiency guess  $\eta^{(n+1)} = \eta_{\text{indirect}}^{(n)}$  and repeats until the mass flow change is below the specified tolerance:

$$|\dot{m}_w^{(n)} - \dot{m}_w^{(n-1)}| < 10^{-3} \text{ kg/s} \quad (7.12)$$

# Chapter 8

## Performance analysis

The present chapter evaluates the thermal and hydraulic performance of the fire tube boiler model based on steady state simulations of a reference control case and systematic parameter variations.

### 8.1 Control case

The control case is defined by a fuel mass flow of  $\dot{m}_{\text{fuel}} = 0.1 \text{ kg s}^{-1}$ , an excess air ratio of  $\lambda = 1.1$ , and a drum pressure of  $P_{\text{drum}} = 10 \text{ bar}$ . These values represent the nominal operating point of the boiler and are used as the reference state throughout this chapter.

Table 8.1: Control case performance.

control	control
fuel mass flow[kg/s]	0.1
air flow[kg/s]	1.77
excess air ratio[-]	1.1
feedwater flow[kg/s]	1.8
steam capacity[t/h]	6.48
$\eta_{\text{direct}}$ [-]	0.89
$\eta_{\text{indirect}}$ [-]	0.89
conductance [MW/K]	0.01
input heat [MW]	4.7
useful heat [MW]	4.2
pressure drop fric total[kpa]	-0.34
pressure drop minor total[kpa]	-0.76
pressure drop total[kpa]	-1.1
water pressure drop fric total[kpa]	-6.92
water pressure drop minor total[kpa]	-0.24
water pressure drop total[kpa]	-7.16

control	control
lhv [mj/kg]	46.97
firing rate [MW]	4.7
adiabatic temperature [°C]	1915.54
stack temperature[°c]	169.39
feedwater pressure[kpa]	1007.16
drum pressure[kpa]	1000

## 8.2 Global boiler performance

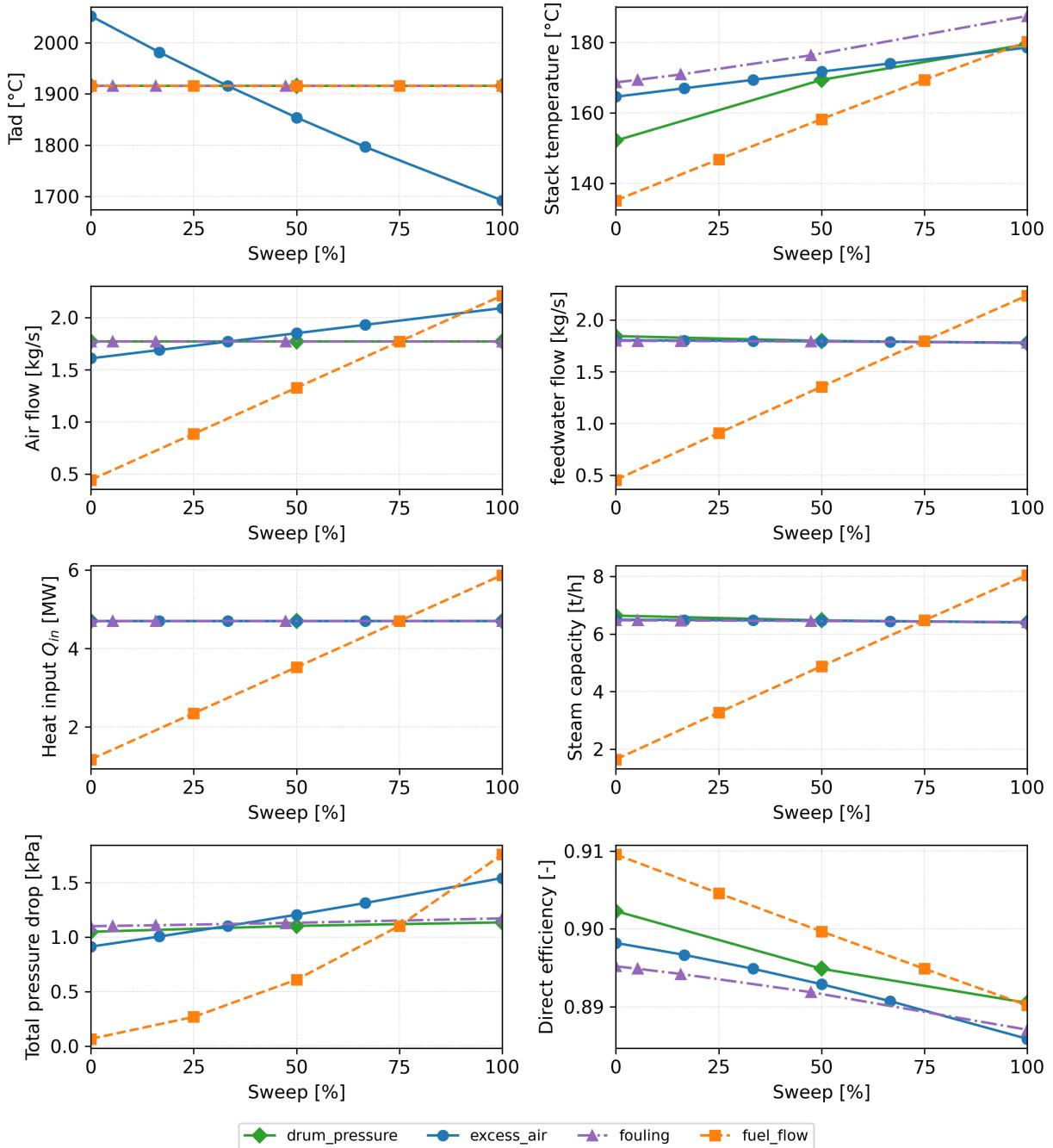


Figure 8.1: Overview of key boiler performance indicators for all parameter groups

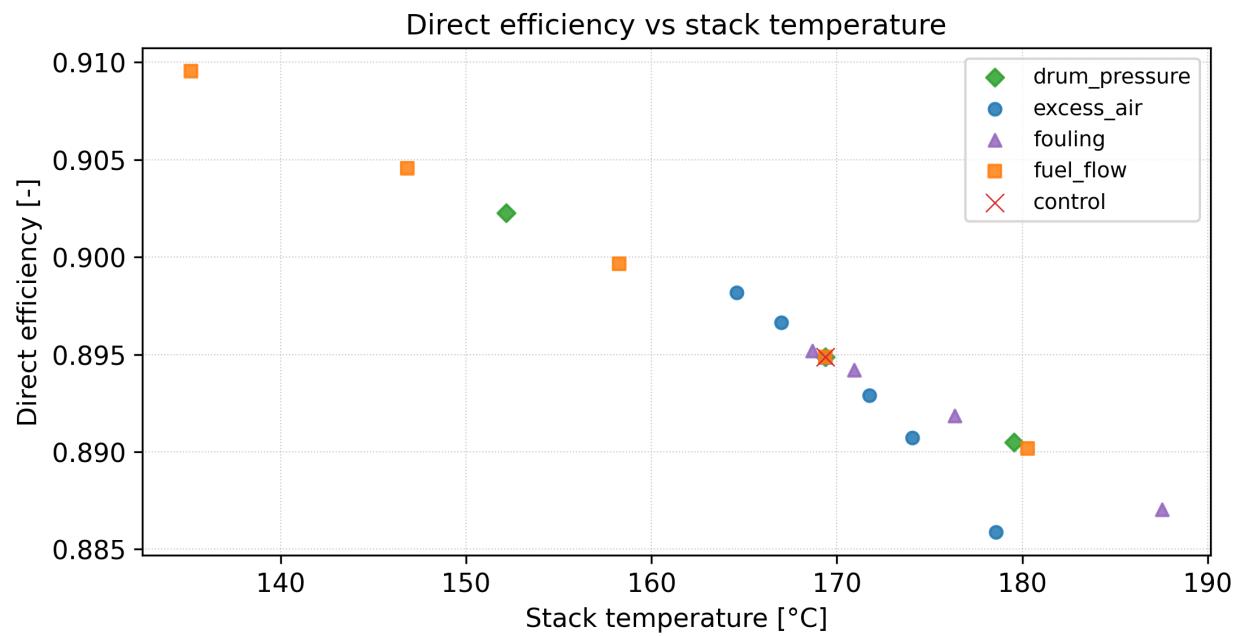


Figure 8.2: Scatter diagram showing stack temperature and direct efficiency

### 8.3 Influence of excess air factor

$$\lambda = [1.00, 1.05, 1.10, 1.15, 1.20, 1.30] [-] \quad (8.1)$$

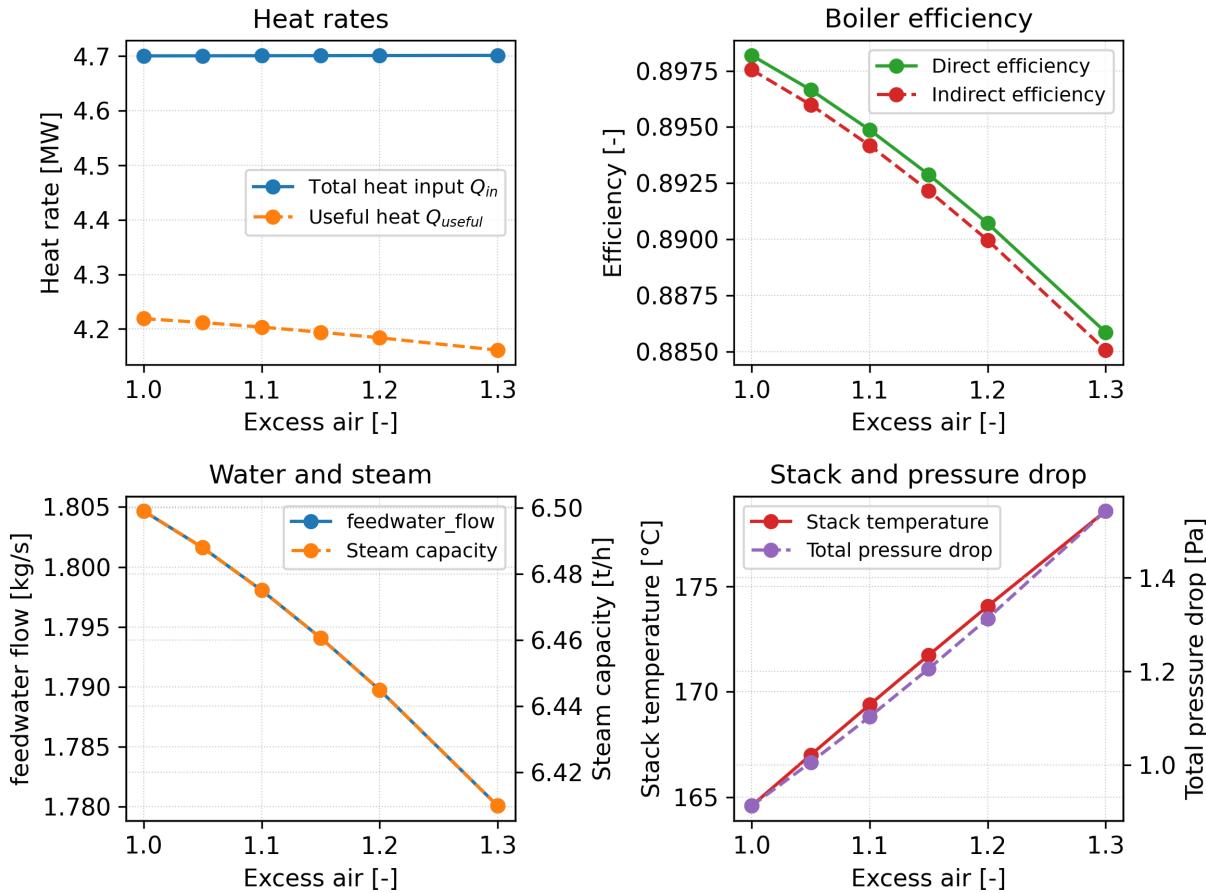


Figure 8.3: Boiler performance as a function of excess air factor

At low excess air levels, a moderate increase in  $\lambda$  improves combustion completeness and slightly stabilizes heat release, resulting in nearly constant efficiency around the control point. Beyond this region, additional air primarily increases the sensible heat carried by the flue gas, which directly increases stack losses and reduces efficiency.

Table 8.2: Excess air performance analysis.

excess air [-]	1.00	1.05	1.10	1.15	1.20	1.30
fuel mass flow[kg/s]	0.1	0.1	0.1	0.1	0.1	0.1
air flow[kg/s]	1.61	1.69	1.77	1.85	1.93	2.09
excess air ratio[-]	1	1.05	1.1	1.15	1.2	1.3
feedwater flow[kg/s]	1.8	1.8	1.8	1.79	1.79	1.78

excess air [-]	1.00	1.05	1.10	1.15	1.20	1.30
steam capacity[t/h]	6.5	6.49	6.48	6.46	6.44	6.41
$\eta_{\text{direct}}$ [-]	0.9	0.9	0.89	0.89	0.89	0.89
$\eta_{\text{indirect}}$ [-]	0.9	0.9	0.89	0.89	0.89	0.89
conductance [MW/K]	0.01	0.01	0.01	0.01	0.01	0.01
input heat [MW]	4.7	4.7	4.7	4.7	4.7	4.7
useful heat [MW]	4.22	4.21	4.2	4.19	4.18	4.16
pressure drop fric total[kpa]	-0.29	-0.31	-0.34	-0.37	-0.41	-0.47
pressure drop minor total[kpa]	-0.63	-0.69	-0.76	-0.83	-0.91	-1.07
pressure drop total[kpa]	-0.91	-1.01	-1.1	-1.21	-1.31	-1.54
water pressure drop fric total[kpa]	-6.97	-6.94	-6.92	-6.89	-6.86	-6.79
water pressure drop minor total[kpa]	-0.24	-0.24	-0.24	-0.24	-0.24	-0.24
water pressure drop total[kpa]	-7.21	-7.19	-7.16	-7.13	-7.1	-7.02
lhv [mj/kg]	46.97	46.97	46.97	46.97	46.97	46.97
firing rate [MW]	4.7	4.7	4.7	4.7	4.7	4.7
adiabatic temperature [°C]	2052.36	1981.5	1915.54	1854.03	1796.53	1692.05
stack temperature[°c]	164.6	167.01	169.39	171.74	174.05	178.56
feedwater pressure[kpa]	1007.21	1007.19	1007.16	1007.13	1007.1	1007.02
drum pressure[kpa]	1000	1000	1000	1000	1000	1000

Increasing the excess air ratio increases the total gas side pressure drop as higher air flow leads to greater flue gas mass flow.

## 8.4 Influence of fuel mass flow

$$\dot{m}_{\text{fuel}} = [0.025, 0.050, 0.075, 0.10, 0.125] \frac{\text{kg}}{\text{s}} \quad (8.2)$$

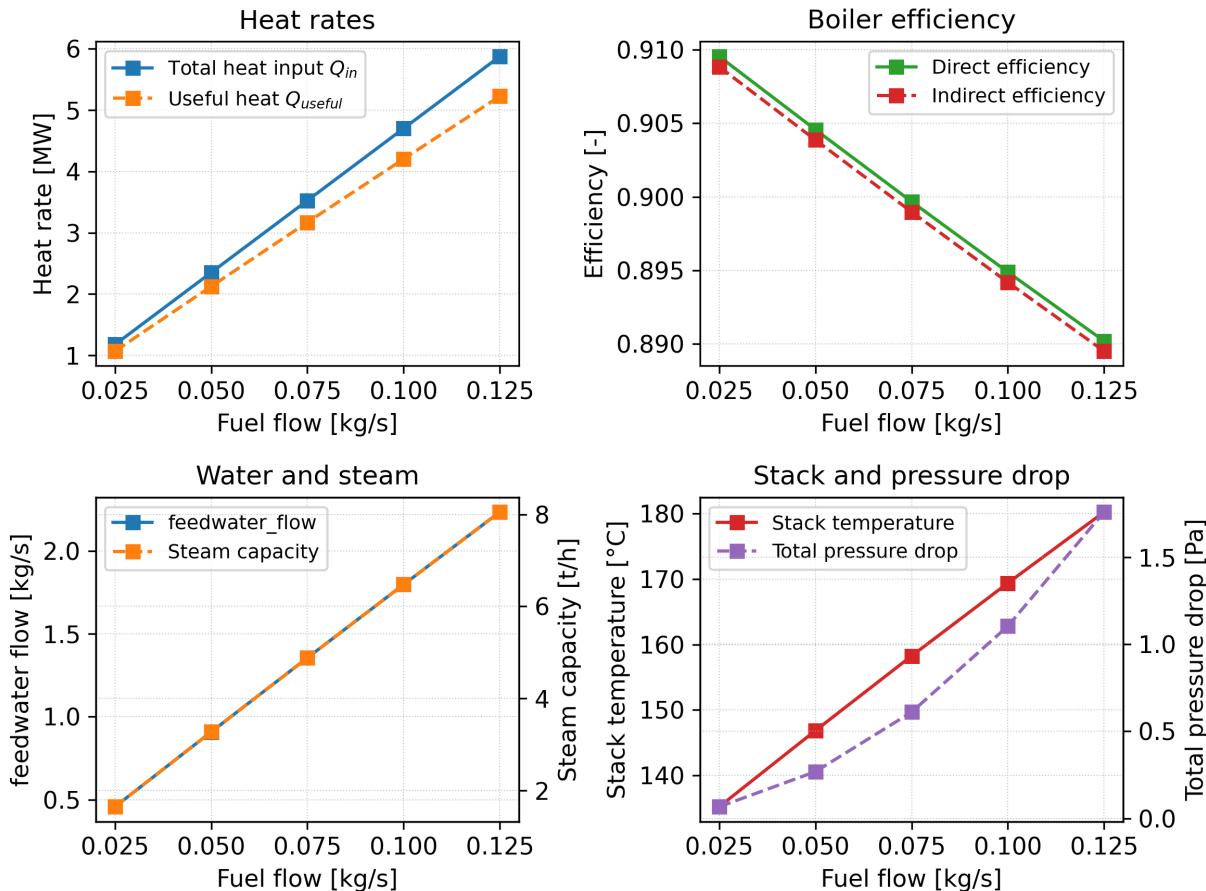


Figure 8.4: Boiler performance as a function of fuel mass flow

Steam capacity increases approximately linearly with fuel input, indicating that the available heat transfer surface is sufficient to absorb the additional duty. As the firing rate approaches the nominal design value, deviations from linearity become apparent, reflecting increasing limitations in heat transfer effectiveness rather than fuel input.

Table 8.3: Fuel flow performance analysis.

fuel flow [kg/s]	0.02	0.05	0.08	0.10	0.12
fuel mass flow[kg/s]	0.02	0.05	0.08	0.1	0.12
air flow[kg/s]	0.44	0.89	1.33	1.77	2.21
excess air ratio[-]	1.1	1.1	1.1	1.1	1.1

fuel flow [kg/s]	0.02	0.05	0.08	0.10	0.12
feedwater flow[kg/s]	0.46	0.91	1.36	1.8	2.24
steam capacity[t/h]	1.65	3.27	4.88	6.48	8.05
$\eta_{\text{direct}}$ [-]	0.91	0.9	0.9	0.89	0.89
$\eta_{\text{indirect}}$ [-]	0.91	0.9	0.9	0.89	0.89
conductance [MW/K]	0	0.01	0.01	0.01	0.01
input heat [MW]	1.18	2.35	3.53	4.7	5.88
useful heat [MW]	1.07	2.12	3.17	4.2	5.23
pressure drop fric total[kpa]	-0.02	-0.09	-0.19	-0.34	-0.54
pressure drop minor total[kpa]	-0.04	-0.18	-0.42	-0.76	-1.22
pressure drop total[kpa]	-0.07	-0.27	-0.61	-1.1	-1.76
water pressure drop fric total[kpa]	-0.57	-1.97	-4.11	-6.92	-10.38
water pressure drop minor total[kpa]	-0.02	-0.06	-0.14	-0.24	-0.37
water pressure drop total[kpa]	-0.59	-2.04	-4.24	-7.16	-10.75
Ihv [mj/kg]	46.97	46.97	46.97	46.97	46.97
firing rate [MW]	1.17	2.35	3.52	4.7	5.87
adiabatic temperature [°C]	1915.54	1915.54	1915.54	1915.54	1915.54
stack temperature[°c]	135.16	146.82	158.25	169.39	180.27
feedwater pressure[kpa]	1000.59	1002.04	1004.24	1007.16	1010.75
drum pressure[kpa]	1000	1000	1000	1000	1000

## 8.5 Influence of drum pressure

$$P_{\text{Drum}} = [4.0, 10.0, 16.0] \text{ bar} \quad (8.3)$$

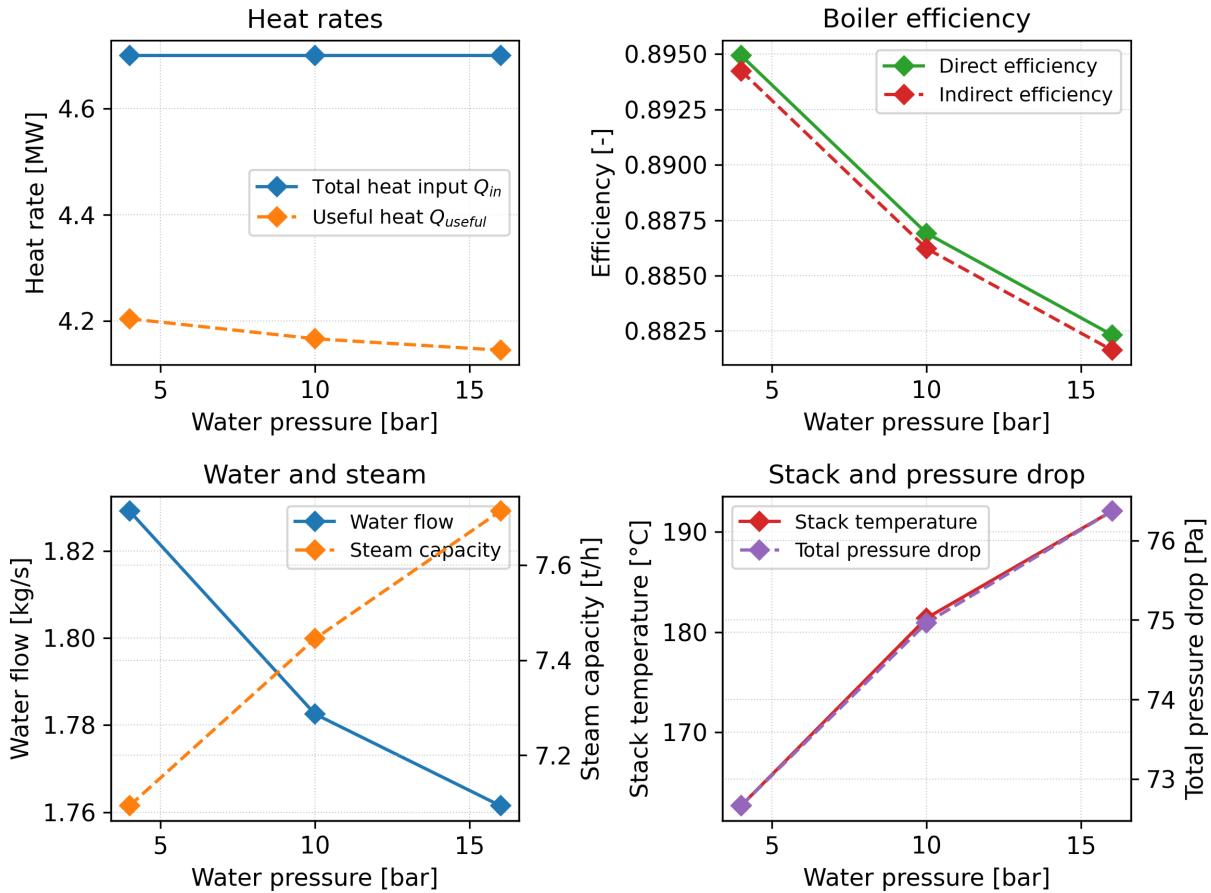


Figure 8.5: Boiler performance as a function of drum pressure

The drum pressure variation modifies the steam saturation temperature and thus the driving temperature difference between flue gas and water/steam on each heat exchanger surface.

Table 8.4: Drum pressure performance analysis.

drum pressure [bar]	4.00	10.00	16.00
fuel mass flow[kg/s]	0.1	0.1	0.1
air flow[kg/s]	1.77	1.77	1.77
excess air ratio[-]	1.1	1.1	1.1
feedwater flow[kg/s]	1.84	1.8	1.78
steam capacity[t/h]	6.64	6.48	6.4

drum pressure [bar]	4.00	10.00	16.00
$\eta_{\text{direct}}$ [-]	0.9	0.89	0.89
$\eta_{\text{indirect}}$ [-]	0.9	0.89	0.89
conductance [MW/K]	0.01	0.01	0.01
input heat [MW]	4.7	4.7	4.7
useful heat [MW]	4.24	4.2	4.18
pressure drop fric total[kpa]	-0.32	-0.34	-0.35
pressure drop minor total[kpa]	-0.72	-0.76	-0.78
pressure drop total[kpa]	-1.05	-1.1	-1.14
water pressure drop fric total[kpa]	-7.26	-6.92	-6.77
water pressure drop minor total[kpa]	-0.25	-0.24	-0.24
water pressure drop total[kpa]	-7.51	-7.16	-7
lhv [mj/kg]	46.97	46.97	46.97
firing rate [MW]	4.7	4.7	4.7
adiabatic temperature [°C]	1915.54	1915.54	1915.54
stack temperature[°c]	152.15	169.39	179.55
feedwater pressure[kpa]	407.51	1007.16	1607
drum pressure[kpa]	400	1000	1600

Increasing the drum pressure, raises the steam capacity because the latent heat of vaporization decreases with increasing pressure, allowing a larger steam mass flow to be generated for the same absorbed thermal duty. The direct efficiency decreases, since higher water and steam temperatures reduce the available driving temperature difference on the gas side. Consistent with this, the stack temperature increases, indicating a diminished potential for further heat recovery.

## 8.6 Influence of fouling

$$f = [0.5, 1.0, 2.0, 5.0, 10.0] [-] \quad (8.4)$$

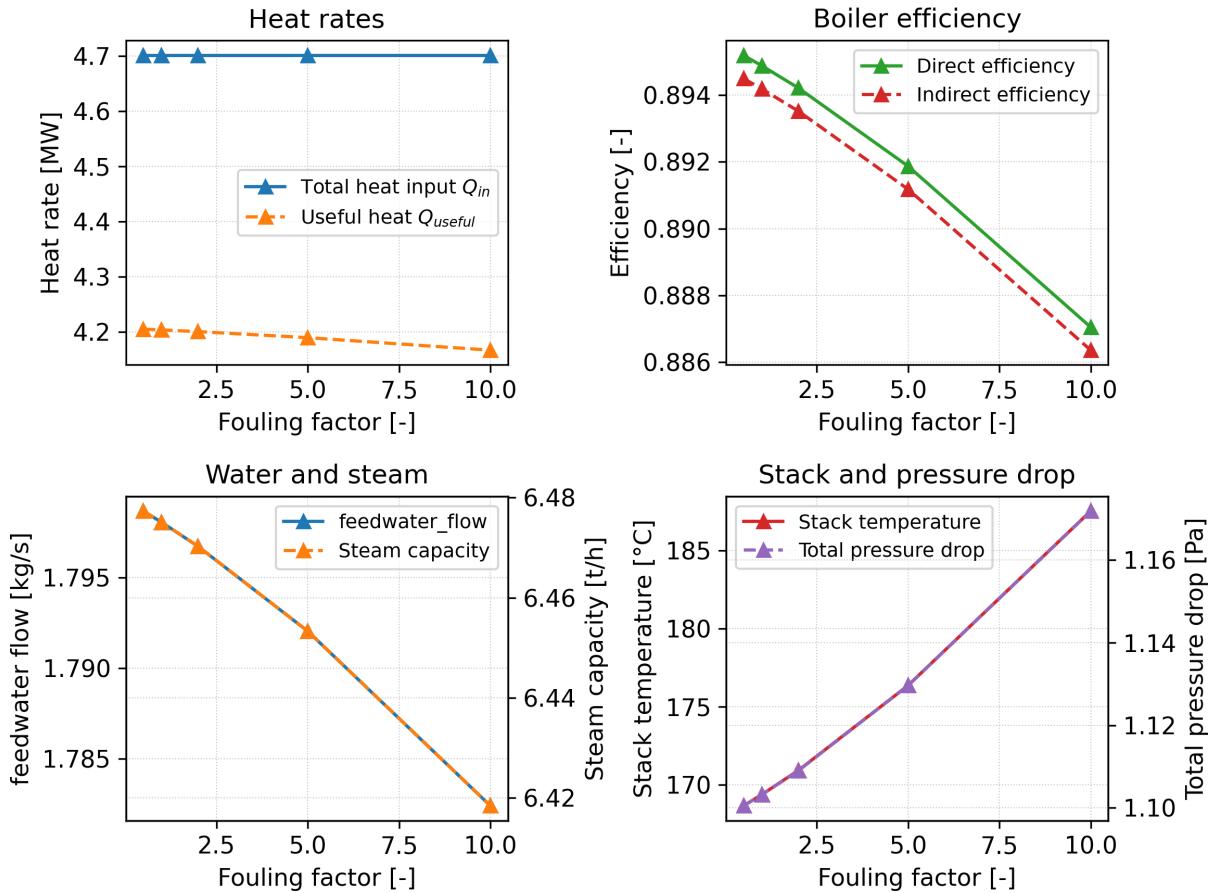


Figure 8.6: Boiler performance as a function of fouling factor

The fouling factor represents a degradation of the effective heat transfer surfaces on the gas side and water side heat exchangers. Increasing fouling reduces the overall heat transfer coefficient, directly lowering the effective conductance, weakening heat recovery throughout the boiler, resulting in higher stack temperatures and reduced boiler efficiency.

The effect of fouling is distributed across all stages, but its impact is most pronounced in the downstream convective sections where heat transfer is already limited by smaller temperature differences. As fouling increases, these sections lose effectiveness first.

Table 8.5: Fouling performance analysis.

fouling [-]	0.50	1.00	2.00	5.00	10.00
fuel mass flow[kg/s]	0.1	0.1	0.1	0.1	0.1
air flow[kg/s]	1.77	1.77	1.77	1.77	1.77
excess air ratio[-]	1.1	1.1	1.1	1.1	1.1
feedwater flow[kg/s]	1.8	1.8	1.8	1.79	1.78
steam capacity[t/h]	6.48	6.48	6.47	6.45	6.42
$\eta_{\text{direct}}$ [-]	0.9	0.89	0.89	0.89	0.89
$\eta_{\text{indirect}}$ [-]	0.89	0.89	0.89	0.89	0.89
conductance [MW/K]	0.01	0.01	0.01	0.01	0.01
input heat [MW]	4.7	4.7	4.7	4.7	4.7
useful heat [MW]	4.2	4.2	4.2	4.19	4.17
pressure drop fric total[kpa]	-0.34	-0.34	-0.34	-0.35	-0.37
pressure drop minor total[kpa]	-0.76	-0.76	-0.76	-0.78	-0.8
pressure drop total[kpa]	-1.1	-1.1	-1.11	-1.13	-1.17
water pressure drop fric total[kpa]	-6.92	-6.92	-6.91	-6.87	-6.8
water pressure drop minor total[kpa]	-0.24	-0.24	-0.24	-0.24	-0.24
water pressure drop total[kpa]	-7.16	-7.16	-7.15	-7.11	-7.04
lhv [mj/kg]	46.97	46.97	46.97	46.97	46.97
firing rate [MW]	4.7	4.7	4.7	4.7	4.7
adiabatic temperature [°C]	1915.54	1915.54	1915.54	1915.54	1915.54
stack temperature[°c]	168.67	169.39	170.94	176.36	187.53
feedwater pressure[kpa]	1007.16	1007.16	1007.15	1007.11	1007.04
drum pressure[kpa]	1000	1000	1000	1000	1000

While the boiler can continue to operate under fouled conditions, the results highlight the importance of maintaining clean heat transfer surfaces to ensure higher efficiency.

## 8.7 Stage-wise heat transfer and hydraulics

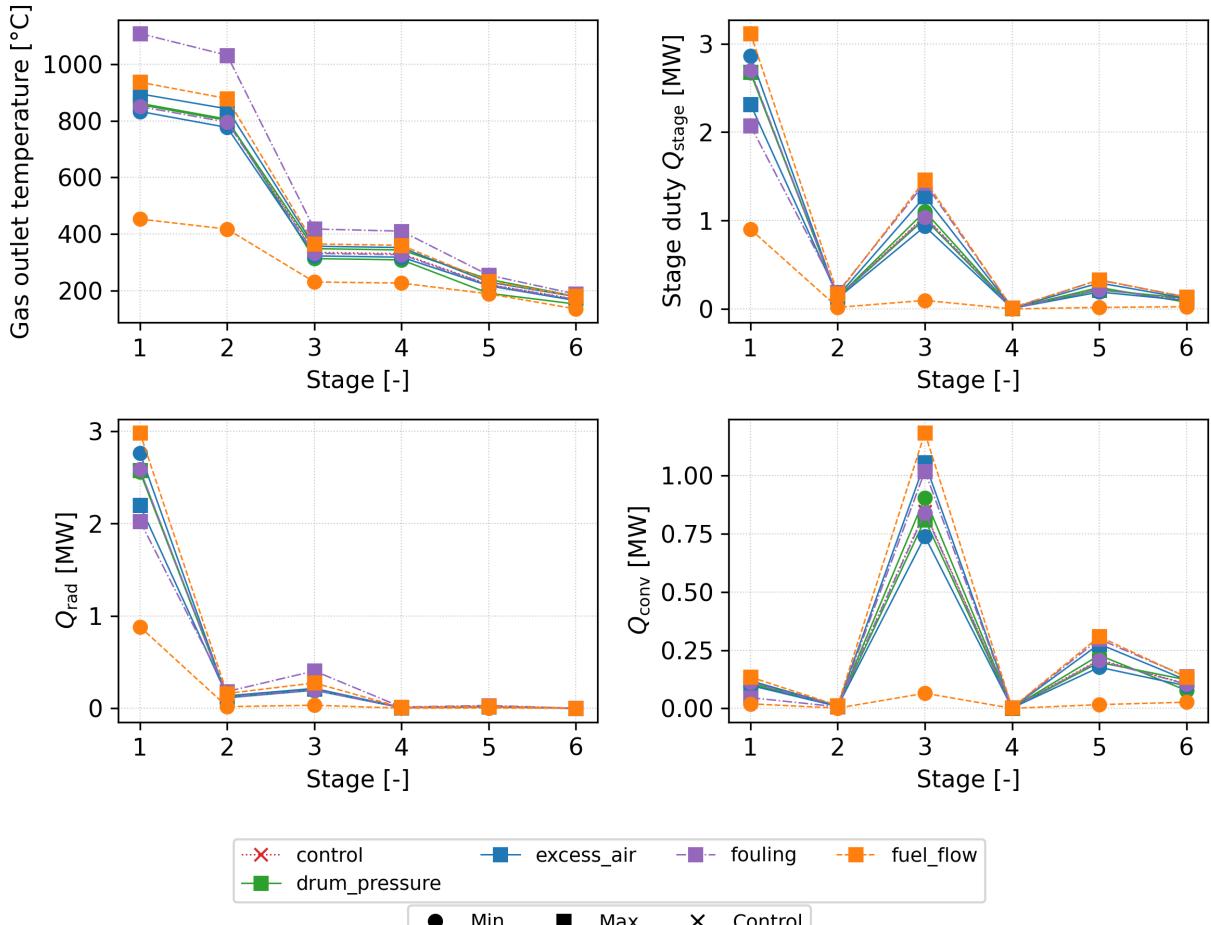


Figure 8.7: Stage wise heat transfer profile

Across all runs the stage pattern stays the same: gas temperature drops from HX 1 to HX 6, stage heat duty is highest in the first stages and decreases downstream, and early stages are driven mainly by radiative transfer while later stages are relatively more convective. Control cases sit between the minimum and maximum parameter cases, showing smooth scaling rather than any stage wise regime change.

Excess air mainly shifts and weakens heat transfer: higher excess air lowers upstream gas temperatures and reduces early stage duties, pushes a larger share of recovery downstream, and increases gas velocity and total pressure drop across stages. Fuel flow scales everything up or down: higher fuel flow increases gas temperatures, stage duties, and both convective and radiative contributions in all stages, with the biggest absolute changes in the first tube bank section and upstream units, while also increasing pressure drop. Drum pressure has a smaller gas side impact but adjusts downstream recovery through water side conditions, slightly shifting late stage duties and conductance without changing the overall stage wise shape.

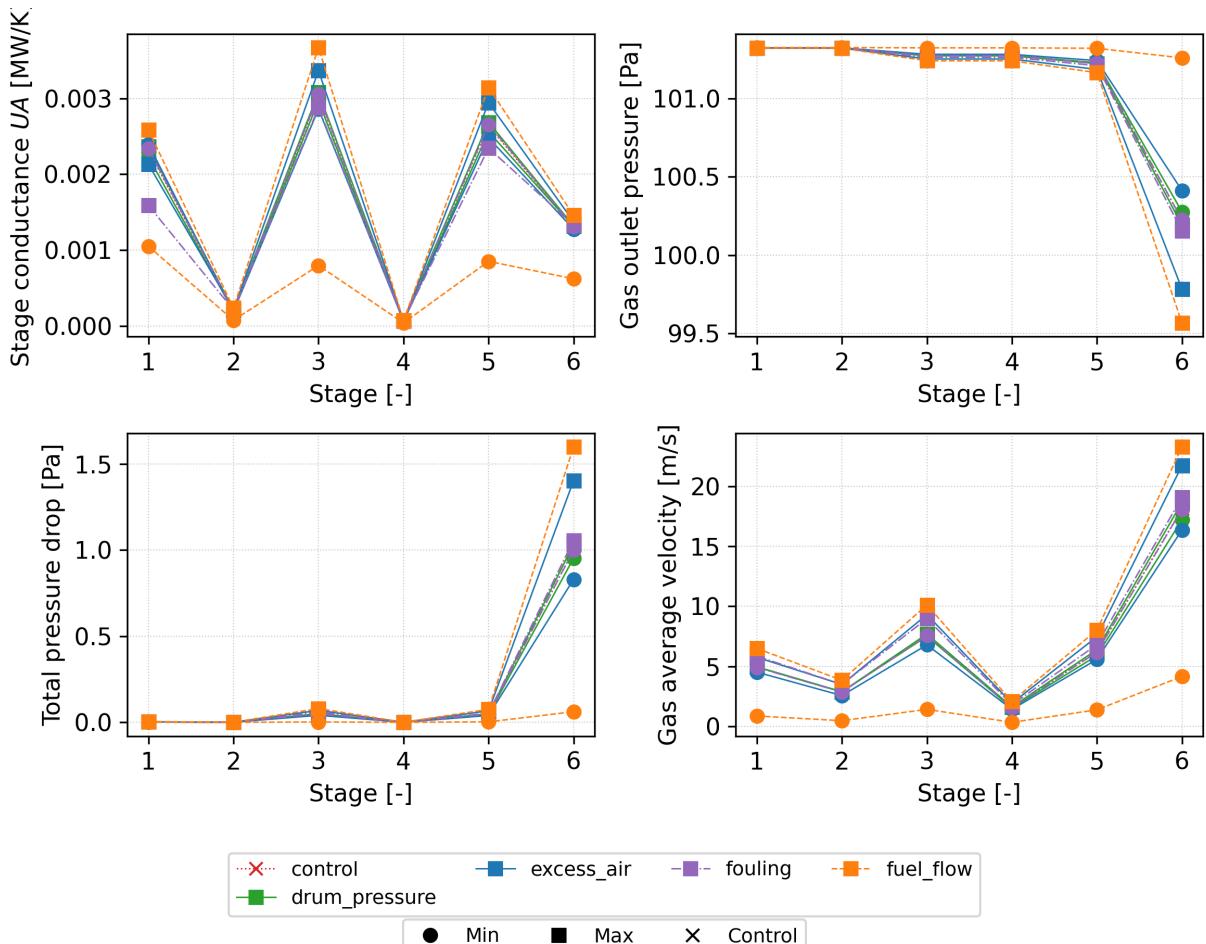


Figure 8.8: Stage wise hydraulics and conductance profile

# Chapter 9

## Summary

This thesis presented a physics based modelling framework for a three pass fire tube industrial shell boiler, integrating combustion, heat transfer, and hydraulic behavior within a single tool. The model was implemented in Python and structured around a one dimensional marching solver that resolves gas side and water/steam side processes consistently along the boiler flow path.

The developed framework couples three main sub models:

- A detailed fuel air combustion model.
- Heat transfer is resolved across six sequential gas side stages.
- Gas side pressure losses are computed concurrently with heat transfer, Water side pressure losses are evaluated for the economizer circuit.

The performance analysis demonstrates that boiler efficiency is most sensitive to the excess air ratio, which directly controls flue gas mass flow, adiabatic flame temperature, and stack losses. The firing rate primarily governs the absolute thermal duty and steam production. Drum pressure mainly influences steam quantity through its effect on latent heat and saturation temperature, while having only a secondary impact on overall thermal efficiency; higher pressures reduce the available temperature driving force, elevating stack temperatures.

Across all cases, the coupled model captures the interplay between combustion conditions, heat transfer effectiveness, and hydraulic constraints, providing a physically consistent basis for assessing operational trade offs and identifying efficiency critical control parameters in industrial fire tube boilers.

# Appendix A

## config and input

### A.1 Air Properties (*config/air.yaml*)

Table A.1: Air parameters.

Quantity / Species	Symbol	Value	Units
Temperature	$T$	300.0	K
Pressure	$P$	101325	Pa
Oxygen (molar fraction)	$x_{O_2}$	0.23067	(–)
Nitrogen (molar fraction)	$x_{N_2}$	0.755866	(–)
Argon (molar fraction)	$x_{Ar}$	0.01287	(–)
Carbon dioxide (molar fraction)	$x_{CO_2}$	0.000594	(–)
Water vapour (molar fraction)	$x_{H_2O}$	0.0	(–)

### Drum Geometry and Wall Properties (*config/drum.yaml*)

Table A.2: Drum parameters.

Quantity	Symbol	Value	Units
Inner diameter	$D_{drum}$	4.5	m
Length	$L_{drum}$	5.0	m
Wall thickness	$\delta_{wall}$	0.05	m
Wall thermal conductivity	$k_{wall}$	40	$W m^{-1} K^{-1}$
Inner surface roughness	$\varepsilon$	5	$\mu m$

Quantity	Symbol	Value	Units
Inner surface emissivity	$\varepsilon_r$	0.80	(–)
Fouling thickness	$\delta_f$	$1.0 \times 10^{-4}$	m
Fouling conductivity	$k_f$	0.2	$\text{W m}^{-1} \text{K}^{-1}$

## Fuel Properties (*config/fuel.yaml*)

Table A.3: Fuel parameters.

Quantity / Species	Symbol	Value	Units
Temperature	$T$	300.0	K
Pressure	$P$	101325	Pa
Mass flow rate	$\dot{m}_{\text{fuel}}$	0.1	$\text{kg s}^{-1}$
Methane (molar fraction)	$\text{CH}_4$	0.849546	(–)
Ethane (molar fraction)	$\text{C}_2\text{H}_6$	0.061889	(–)
Propane (molar fraction)	$\text{C}_3\text{H}_8$	0.020597	(–)
Butane (molar fraction)	$\text{C}_4\text{H}_{10}$	0.005154	(–)
Hydrogen sulfide (molar fraction)	$\text{H}_2\text{S}$	0.000103	(–)
Nitrogen (molar fraction)	$\text{N}_2$	0.041293	(–)
Carbon dioxide (molar fraction)	$\text{CO}_2$	0.016418	(–)
Water (molar fraction)	$\text{H}_2\text{O}$	0.005	(–)
Argon (molar fraction)	Ar	0.0	(–)

## Operating Conditions (*config/operation.yaml*)

Table A.4: Operation parameters.

Quantity	Symbol	Value	Units
Excess air ratio	$\lambda$	1.1	(–)
Drum pressure	$P_{\text{drum}}$	10	bar

## Heat Exchange Stages (*config/stages.yaml*)

Table A.5: Stages parameters.

Quantity	Symbol	HX-1	HX-2	HX-3	HX-4	HX-5	HX-6	Units
Inner diameter	$D_i$	1.4	1.6	0.076	1.6	0.076	0.0337	m
Inner / tube length	$L_i, L$	5.276	0.8	4.975	0.8	5.620	80	m
Wall thickness	$\delta$	0.02	—	—	—	—	—	m
Thermal conductivity	$k$	50	—	—	—	—	—	$\text{W m}^{-1} \text{K}^{-1}$
Curvature radius	$R$	—	0.8	—	0.8	—	—	m
Number of tubes	$N$	—	—	118	—	100	60	(—)
Number of rows	$N_{\text{rows}}$	—	—	6	—	6	20	(—)
Number of circuits	$n_c$	—	—	—	—	—	4	(—)
Transverse pitch	$S_T$	—	—	0.11	—	0.11	0.09	m
Longitudinal pitch	$S_L$	—	—	0.11	—	0.11	0.10	m
Baffle spacing	$B$	—	—	0.45	—	0.45	0.25	m
Baffle cut	$c$	—	—	0.25	—	0.25	0.25	(—)
Bundle clearance	—	—	—	0.010	—	0.010	0.010	m
Shell inner diameter	$D_{\text{shell}}$	—	—	—	—	—	0.95	m
Hot inlet loss	$K_{\text{hot,in}}$	0.5	—	0.5	—	0.5	0.5	(—)
Hot outlet loss	$K_{\text{hot,out}}$	0.0	—	1.0	—	1.0	1.0	(—)
Hot bend loss	$K_{\text{hot,bend}}$	0.0	0.3	—	0.3	—	—	(—)
Cold inlet loss	$K_{\text{cold,in}}$	0.0	—	—	—	—	0.5	(—)
Cold outlet loss	$K_{\text{cold,out}}$	0.0	—	—	—	—	1.0	(—)
Cold bend loss	$K_{\text{cold,bend}}$	0.0	—	—	—	—	0.3	(—)

## Water Properties (*config/water.yaml*)

Table A.6: Water parameters.

Quantity	Symbol	Value	Units
Specific enthalpy	$h$	$4.40 \times 10^5$	$\text{J kg}^{-1}$
Composition	$x_{\text{H}_2\text{O}}$	1.0	(-)

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