at room temperature is forced through a pipe of circular cross-section by pump that maintains a gauge pressure of 950 Pa. The pipe has diametes of 2.6 cm and length 65 cm. The castor oil emerges from free end of pipe is collected at atmospheric pressure. After 905, a total y 1.23 kg has been collected what is the welficient of viscocity of castor oil at that temperature.

Sola:

Qiven,

density of castor oil (8) = 0.96×10³ kg/m³

Qauge pressure (P) = 950 N/m²

radiu g hipe (r) = 2 1.3 cm = 1.3 ×10⁻² m

Length of hipe (L) = 65 cm = 65×10⁻² m

mass g oil collected (m) = 1.23 kg

Time interval (t) = 905

flow rate (v) =?

Coefficient of viscouity of castor oil (1) =?

We know,

Using Roiseuille's law, $V = \frac{11 \text{ PYY}}{8 \text{ pL}} \quad \text{or} \quad \Omega = \frac{11 \times 950 \times (1.3 \times 10^{-2})^{4}}{8 \times 13.12 \times 65 \times 10^{-2}}$

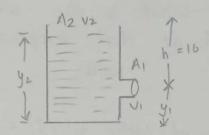
.12= 1.15 Ns/m2

(Q.2): A large storage tank, open at the top and filled with water, develops a small hole in its side at a point 16-0 m below water level. The rate of flow from the leak is 2.50 x10⁻³ m³/mm. Detamine:

a) the speed at which the water leaves the hole. b) the cliameter of the table.

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Given, Rate of flow from leak(v) = $2.5 \times 10^{-3} \, \text{m}^3/\text{min}$ = $4.16 \times 10^{-5} \, \text{m}^3/\text{sec}$



Height of small hole (h)= 16 m.

As A2 >> A1, 80 V2×0 se, water at top y the tank remains at rest.

Now, using Bernoulli's equation, $\begin{array}{ll}
P_0 + \frac{9}{2}V_1^2 + 9gy, &= P_0 + \frac{9}{2}V_2^2 + 9gy_2 \\
P_0 + \frac{1}{2}V_1^2 + 9y_1 &= gy_2 \\
P_0 + \frac{1}{2}V_1^2 + 9y_1 &= gy_2 \\
P_0 + \frac{1}{2}V_1^2 + gy_1 &= \frac{1}{2}V_2^2 + \frac{1}{2}V_1^2 \\
P_0 + \frac{1}{2}V_1^2 + \frac{1}{2}V_1^2 + \frac{1}{2}V_1^2 + \frac{1}{2}V_1^2 \\
P_0 + \frac{1}{2}V_1^2 + \frac{1$

Now $e_1^n \cdot g$ continuity, A V = V

or,
$$\frac{\prod d^2}{4} \times 17.7 = 4.16 \times 10^{-5}$$

or, $d = \sqrt{\frac{4 \times 4.16 \times 10^{-5}}{17.7 \times 10}}$
 $\therefore d = 1.7 \times 10^{-3} \text{ m} = 4.723 \text{ mm}$

- (Q.3) In ideal flow, a liquid of density 850 lg/m³ moves from a horizontal tube of radius 1 cm into a second horizontal tube of radius 0.500 cm. A pressure difference AP exists between the tubes.
- a) find the volume flow rate as function of AP.
- b) Evaluate the volume flow rate for DP= 6.00 kPa
- c) State how the volume flow rate depends on AP. Sola:

Given, density g liquid $(g) = 850 \text{ kg/m}^3$ radius of 1st horizontal tube $(r_1) = 1 \text{ cm} = 10^{-2} \text{ m}$ radius g and horizontal tube $(r_2) = 0.5 \times 10^{-2} \text{ m}$ Now, we know,

Flow rate (V)= A1V1= A2V2.

$$v_1 = \frac{A_1}{V} = \frac{A_1}{\Pi r_1} - (i)$$

and
$$V_2 = \frac{A_2}{V} = \frac{A_2}{\Pi r_2} - (\overline{n})$$

Using Bernoulli's equation, we get.

$$P1 + S \frac{V_1^2}{2} = P2 + S \frac{V_2^2}{2} \quad [i'] \text{ Tube is horizontal}$$

$$or_1 \left(P_1 - P_2 \right) = \frac{S}{2} \left(V_2^2 - V_1^2 \right)$$

$$or_1 \frac{2 \Delta P}{850} = \frac{V^2}{\Pi^2} \left(\frac{1}{r_2^2} - \frac{1}{r_1^4} \right)$$

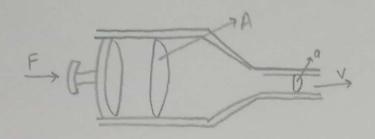
or,
$$\frac{2 \Delta P \pi^2}{850} = v^2 \left(\frac{1}{(0.5 \times 10^{-2})^2} - \frac{1}{(40^{-2})^4} \right)$$

$$V = \sqrt{\frac{2.3 \times 10^{-2}}{108 \times 1.5}} \Delta P$$
 ... $V = 3.93 \times 10^{-6} \sqrt{\Delta P} \text{ m}^{3} \text{ls}$.

If $\Delta P = 6.00 \text{ kPa}$ So, Flow rate $(V) = 3.93 \times 10^{-6} \times \sqrt{6 \times 10^{-3}}$ $= 3.04 \times 10^{-4} \text{ m}^3 \text{ls}$.

Here, we see that VX JAP

density of swater as shown in figure. The barrel of the syringe has a cross-sectional area $A=2.50\times10^{-2}m$ of the needle has cross-sectional area $a=1\times10^{-8}m^2$. and the needle has cross-sectional area $a=1\times10^{-8}m^2$. In the absence of fine on the plunger, the pressure is 10 the absence of fine on the plunger, the pressure is 1 atm everywhere. A first F magnitude 2.00 N acks 1 atm everywhere he fine squirt horizontally form on plunger making medicine squirt horizontally form the needle. Determine the speed of the medicine the needle.



Given,

Quage pressure (AP) =
$$\frac{2.00}{2.5\times10^5}$$
 = 8×10^4 N/m²

from areque of continuity,

AIVI = AZVZ

$$V_1 = \frac{A_2}{A_1} \times V_2$$
 or, $V_1 = \frac{r_2^2}{r_1^2} \times V_2$

Using Bernoullis theorem,

$$P_1 + \frac{gv_1^2}{2} + ggy_1 = P_2 + gu_2^2 + ggy_2$$

Since 41=42,

Since, $v_1^2 \ll v_2^2$. v_1^2 is negligible.

AP= 500 X V22

.. V2 = 12-6 m/s.