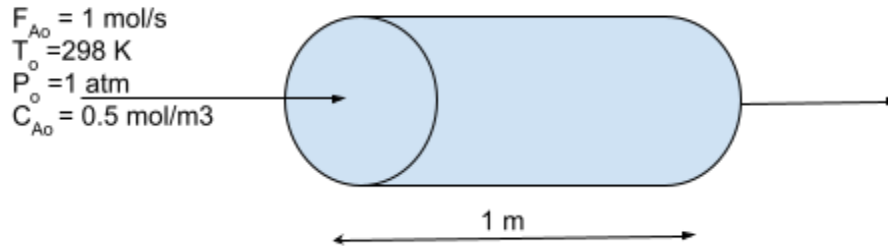


CL 249: Computational Methods Lab

Date: 01/10/24

Assignment 8

The Packed Bed Reactor Problem,



Consider a hypothetical situation in a packed bed flow reactor. Gas A flows through the catalyst bed, and on the surface, the following reaction occurs,



With rate kinetics given as,

$$r' = -k \cdot C_A$$

You are tasked to find the equilibrium conversion in this problem.

(Every information required to find the Conversion is provided in steps)

1. The initial temperature T_o is 298 K. For this particular reactor, the change in temperature is given by the following equation,

$$\frac{dT}{dt} = T^3 - 581T^2 - 8870T - 29800$$

The equilibrium is reached when the temperature reaches a **steady state** value. **Find the final equilibrium temperature (T).**

2. The initial Pressure P_o is 1 atm. The pressure drop in the packed bed reactor follows the **Ergun equation**, which is a function of the density of the gas. For simplicity, the equation is modified to the following equation: $\Delta P = (P_o - P)$

$$\frac{\Delta P}{\Delta L} = A \cdot \rho + B \rho^2 + C \rho^{-2} + D \rho^{-1}$$

Where ρ is density equal to 0.8 kg/m^3

And $x = [A, B, C, \text{ and } D]$ are constants that act as solutions of the following matrix.

$Mx = Y$

$$M = \begin{bmatrix} 1 & 4 & 2 & 3 \\ 0 & 1 & 4 & 4 \\ -1 & 0 & 1 & 0 \\ 2 & 0 & 4 & 1 \end{bmatrix}$$

$$Y = [1 \ 2 \ 3 \ 4]^T$$

Find the final pressure(P) at the reactor outlet. You can consider delta l to be 1 and units of pressure to be in atm.

3. There is one more factor, epsilon, ϵ , (unitless), which is related to the porosity of the bed. Now, you are given an equation that relates the epsilon with the length.

$$\varepsilon = \int_0^1 a \cdot dl$$

For given various values for l and corresponding 'a' values. **Calculate the value of ε**

l (m)	0.1	0.2	0.3	0.6	0.9	1
a	4	1	4	0.5	1	3

4. Arrhenius's equation describes the Rate constant, but instead, you are given the rate constants at some of the temperatures:

T (K)	400	450	500	550	600	650
K (1/s)	0.1	3.2	10.4	20.8	25.5	32.3

Find the Rate constant (k) at equilibrium temperature (T).

5. Now, we come to the most important step:
The design equation of PBR is given as

$$\frac{dF_A}{dW} = r'$$

Where W is the weight of the catalyst bed in kg

Which, on further simplification, takes the form

$$F_{Ao} \frac{dx}{dW} = \left(\frac{W}{(1 + W^2)^2} \right) [k C_{Ao} \varepsilon (1 - x) \left(\frac{P}{P_o} \right) \left(\frac{T_o}{T} \right)]$$

Solve the differential equation and find the following:

(take the initial condition as $x(0) = 0$ and a step size 0.2)

- Plot the solution (Conversion vs Weight of catalyst)
 - Find the equilibrium conversion
 - The corresponding maximum efficient catalyst loading in the reactor and
 - Write the pseudo-code for the 5th part of your submission.
6. Bonus: prove that the equilibrium conversion is reached.

— END of Problem Statement —

Write your answers here.

Conversion = _____

Weight of the Catalyst bed (kg) = _____