

Formulae for Solid Oxide Fuel Cells

Output Voltage

Output Voltage = Nernst Voltage – (Activation Loss + Concentration loss + Ohmic Loss)

$$V_{fc} = E_{ernst} - (V_{act} + V_{con} + V_{ohmic})$$

Nernst Equation

$$E = E_0 + \frac{RT}{2F} \ln \left(\frac{P_{H_2} * P_{O_2}^{0.5}}{P_{H_2O}} \right)$$

Where

E₀ = 1.1 V is the standard potential

R = 8.314 kJ/ kmol .K is the universal gas constant

T = operating temperature of the fuel cell in kelvins

F = 96486 C/mol is the Faraday constant

Output current Density

$$I_{fc} = I_0 \left(e^{(\alpha_1 n F / RT) V_{act}} - e^{(-\alpha_2 n F / RT) V_{act}} \right)$$

where -

I₀ is the exchange current

α_i is the coefficient of charge transfer

n = 2 is the number of moles of electrons transferred

Exchange Current Density

$$I_0 = A(e^{-E_{act}})/RT$$

where –

A = 101.2 kA/cm² is a preexponential factor obtained by curve fitting with the distributed model

$E_{act} = 120 \text{ kJ/mol}$ is the activation energy of the electrochemical reaction

Partial Pressures

$$P_{H_2} = \left(\frac{1}{\frac{K_{H_2}}{1 + \tau_{H_2}}} \right) (q_{H_2} - 2K_r I_{fc})$$

$$P_{O_2} = \left(\frac{1}{\frac{K_{O_2}}{1 + \tau_{O_2}}} \right) (q_{O_2} - 2K_r I_{fc})$$

$$P_{H_2O} = \left(\frac{1}{\frac{K_{H_2O}}{1 + \tau_{H_2O}}} \right) (2K_r I_{fc})$$

$$q_{H_2} = \frac{2K_r}{U_{opt}} \left(\frac{1}{1 + \tau_f s} \right)$$

$$q_{O_2} = \frac{q_{H_2}}{r_{OH}}$$

Where

- q_{H_2} is the fuel flow rate
- q_{O_2} is the oxygen flow rate
- K_{H_2} , K_{O_2} , K_{H_2O} are the molar valve constants of hydrogen, oxygen and water respectively,
- τ_{H_2} , τ_{O_2} , τ_{H_2O} , are the response times of hydrogen, oxygen and water respectively,
- τ_f is the fuel response time in seconds,
- U_{opt} is the optimum fuel utilization,
- r_{OH} is the ratio of hydrogen to oxygen
- $K_r = 1/(8F)$.

Activation Loss

$$V_{act} = \frac{RT}{F} \left(z + \sqrt{1 + z^2} \right)$$

Where

I_0 is the exchange current

α_i is the coefficient of charge transfer

$n = 2$ is the number of moles of electrons transferred.

Concentration Loss

$$V_{\text{con}} = \frac{RT}{nF} \ln \left(\frac{C_b}{C_{\infty}} \right)$$

OR

$$V_{\text{conc}} = -\frac{RT}{nF} \ln \left(1 - \frac{I_{fc}}{I_L} \right)$$

Where

C_b is the concentration at the triple-phase boundary (tpb) where the gas, electrolyte,

C_{∞} is the bulk concentration of reactant

n is the number of moles of electrons participating in the reaction

I_L is the maximum possible current density of the cell at a given flowrate

I_{fc} is the given current density

Ohmic Loss

$$V_{\text{ohmic}} = \left(\gamma \exp \left[\beta \left(\frac{1}{T_0} - \frac{1}{T} \right) \right] \right) I_{fc} = rI$$

where

T is the fuel cell temperature

$T_0 = 973 \text{ K}$

$\gamma = 0.2 \Omega$, and $\beta = -2870 \text{ K}$ are the constant coefficients of the fuel cell

r is the internal resistance of the SOFC

Constants and Parameters Used

Parameter	Value	Unit
E_O	1.1	V
R	8.314	KJ/Kmol.K
F	98486	C/mol
K_{H_2}	8.43×10^{-4}	Kmol/atm
K_{O_2}	2.81×10^{-4}	Kmol/atm
K_{H_2O}	2.52×10^{-3}	Kmol/atm
τ_{H_2}	26.1	seconds
τ_{O_2}	2.91	seconds
τ_{H_2O}	78.3	seconds
τ_f	5	seconds
U_{opt}	0.85	-
r_{OH}	1.145	ohm

References:

1. Modeling and Simulation of Solid Oxide Fuel Cell Based Distributed Generation System 1Mukesh Kumar Baliwal, 2Dr.A.Bhargava, 3Mr. S.N. Joshi, 4 Sunil kumar - International Journal of Engineering Research & Technology (IJERT) Vol. 2 Issue 8, August - 2013 IJERT ISSN: 2278-0181
2. Solid Oxide Fuel Cell Modeling Abraham Gebregergis, Member, IEEE, Pragasen Pillay, Fellow, IEEE, Debangsu Bhattacharyya, and Raghunathan Rengaswemy
3. Mathematical modelling of solid oxide fuel cell using Matlab/Simulink TVVS Lakshmi, P Geethanjali and Krishna Prasad S - International Conference on Microelectronics, Communication and Renewable Energy (ICMiCR-2013)