

METALLURGY

Minerals: Naturally occurring chemical substance in which metal exist either in its free state or in combined state is called mineral.

Ore: Mineral from which metal can be conventionaly & economically extracted is called ore & impurities associated with it is called gangue or matrix

TYPES OF ORES:

Sulphide Ores: Galena: PbS, Cinnabar: HgS, Cinnabar: HgS

Zinc bllend : Zns, Chalcopyrite : $CuFeS_2$ Copper glance : CuS_2 Fool's Gold : FeS_2

Oxide Ores :

Bauxite: Al,O,. 2H,O Haematite: Fe,O,

Limonite: Fe₂O₃. 3H₂O Tin stone or Cassiterite: SnO₃

Carbonate Ores : Siderite : FeCO₃ Calamine ZnCO₃

Malacite: Cu(OH), CuCO, Dolomite CaCO, MgCO, 2H,O

lime stone: CaCO,

• **Sulphate Ores :** Gypsom : CaSO₄.2H₂O Anylesite PbSO₄

Glauber's salt: Na₂SO₄. 10 H₂O Mohr's salt: FeSO₄. (NH₄)₂SO₄. 6H₂O

Halide Ores: Rock salt: NaCl Cryolite: Na₃AlF₆

Fluorspar : CaF, Carnallite : KCl. MgCl₂. 6H₂O

Nitrate Ores: Chiele Saltpeter: NaNO, Indian Salt petre: KNO,

• Native Ores: Those metals which are chemically less reactive. They occur in the earth crust in form

of free state (lumbs)

e.g: Cu, Ag, Au, Hg, Pd, Pt, Bi

Pulverization: The crushing of ore to powdered state is called pulverisation.

General principles & processes involved in the extraction of metal from its ore:

The extraction of metal from its ore is completed in three steps:

Step I: concentration or Dressing or Beneficiation of ore

Step II : Extraction of crude metal from conc. ore

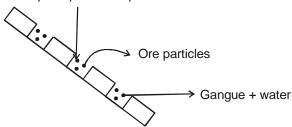
Step III: Refining of impure metal.

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Step I : Concentration or Dressing or beneficiation of Ore

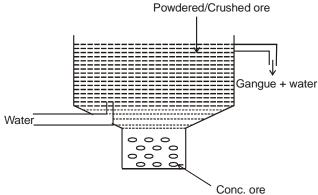
- **(a) By Gravity separation**: Ore particles are heavier than the gangue particles. This is used for the separation of most of the gangue particles:
- ⇒ By Wilfley Table Method

Aq. Suspersion of powdered / Crushed ore

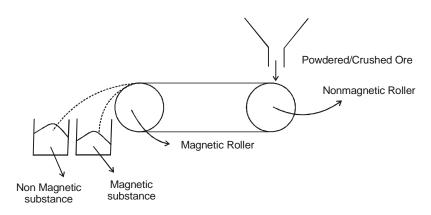




⇒ By Hydraulic Classifier



(b) By Magnetic separator:



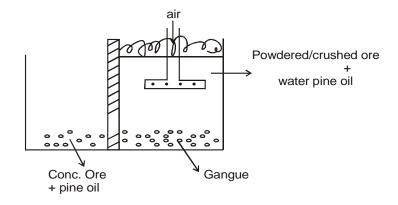
Cassiterite or Tinstone contains impurities of wulframite or wulframates of Fe & Mn.

- \Rightarrow Tin stone : SnO₂ \rightarrow Diamagnetic
- ⇒ Wulframites or wulframates of

Fe & Mn : FeWO₄, MnWO₄ \Rightarrow Paramagnetic.

Ulframates of Fe & Mn from Tin stone by magnetic separator.

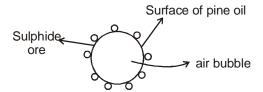
- (c) By Froth Floatation Process: This method is used for the concentration of sulphide ores.
- It is based on the concept that the sulphide ores are prefrentially wetted by pine oil, camphor oil while gangue particles are prefrentially by water.
- This is based on the physical phenomenon of adsorption.







Frother: Pine oil, Camphor oil



Froth Stabilizers: They reduce surface tension of water e.g. cresols, amines.

Collector: Sodium or Potassium xanthates. It combines with sulphide ore & makes them water replent so that its affinity towards pine oil increases (Adsorption tendency increases)

$$KOH + EtOH \rightarrow Et O^- K^+ + H_2O$$

$$S = C = S' + Et O^-K^+$$
 $\longrightarrow S = C$
 S^-K^+

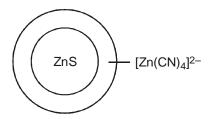
Potassium ethyl xanthate

Depressant: KCN or NaCN

ZnS is found to be an impurity with the lead sulphide. Therefore to separate out PbS from ZnS depressant KCN or NaCN added.

PbS + NaCN \rightarrow No complex formation due to very law K_{sn} of PbS.

$$ZnS + 4NaCN \rightarrow 4Na^{+} + [Zn (CN)_{4}]^{2^{-}} + S^{-}$$
(water soluble)



Thus, ZnS becomes water soluble & it remains with gangue while PbS comes out with the froth.

Activator : CuSO₄

From galena (PbS.ZnS) ZnS is removed

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ZnS + 4NaCN
$$\longrightarrow$$
 4 Na⁺ + [Zn(CN)₄]²⁻ | Cuso₄ \longrightarrow [Cu(CN)₄]³ + ZnS \downarrow + S⁻⁻ (water soluble) (more stable)

& ZnS is taken out by froth floatation second time.

- **(d) By electrostatic Method**: This method is very specific for the separation of ZnS from galena (lead sulphide) because ZnS is poor conductor of electricity & PbS is good conductor of electricity.
- (c) Leaching

Step II: Extraction of Crude Metal from concentrated Ore:

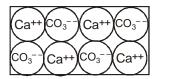
It's completed in two stages:

- (a) Conversion of concentrated ore into metal oxide.
- (b) Reduction of metal oxide/concentrated ore into free metal
- (a) Conversion of concentrated ore into metal oxide:

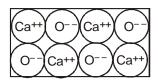


Calcination: (Carbonates ore)

- Calcination is carried out for carbonate, hydrated metal oxide & metal hydroxide ores.
- It is carried out in the absence of air i.e., heating in absence of air.







lattice will remain same

- Due to calcination ore becomes porous.
- Volatile organic impurities get evaporated

eg.
$$CaCO_{3(s)} \xrightarrow{\Delta} CaO + CO_2$$
 $CaCO_3MgCO_3.2H_2O \xrightarrow{\Delta} CaO + MgO + 2CO_2 \uparrow + 2H_2O$
 $2AI(OH)_3 \xrightarrow{\Delta} AI_2O_3 + 2H_2O \uparrow$
 $AI_2O_3.2H_2O \xrightarrow{\Delta} AI_2O_3 + 2H_2O \uparrow$
 $Pb(OH)_2. PbCO_3 \xrightarrow{\Delta} 2PbO + CO_2 \uparrow + H_2O$
 $FeCO_3 \xrightarrow{\Delta} FeO + CO_2 \uparrow$
 $Fe_2O_3. 3H_2O \xrightarrow{\Delta} Fe_2O_3 + 2H_2O \uparrow$
 $Cu(OH)_2. CuCO_3 \xrightarrow{\Delta} 2CuO + CO_2 \uparrow + H_2O$
 $Black powder$
 $ZnCO_3 \xrightarrow{\Delta} ZnO + CO_2 \uparrow$

Roasting: In the presence of air the sulphide are heated in free supply of air below m.p. Impurities of sulphur, phosphorus, arsenic & antimony are converted into their corresponding volatile oxide & thus get removed.

Moisture & Water of crystallisation are also removed.

eg. (1) PbS +
$$\frac{3}{2}$$
O₂ $\xrightarrow{\triangle}$ PbO + SO₂ \\
PbS + 2O₂ $\xrightarrow{\triangle}$ PbSO₄

(2) $ZnS + \frac{3}{2}O_2$ $\xrightarrow{\triangle}$ $ZnO + SO_2$ \\
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$$ZnS + 2O_2 \xrightarrow{\longrightarrow} ZnSO_4$$

(b) Reduction of Metal oxide / conc. ore into free metal.

This can be carried out

- (i) chemical reduction
- (ii) By self reduction or auto reduction or Air Reduction
- (iii) Metal displacement method
- (iv) By electrolytic Reduction
- (v) By amulgamation.
- (i) & (ii) method are collectively known as Pyrometallurgy
- e.g. Sn, Pb, Fe, Hg, Cu, B, Zn, (Based on Ellinghum diagram)
- (iii) step is called hydrometallurgy Cu, Ag, Au are extracted
- (iv) step is called Electrometallurgy, Alkali, Alkaline earth metals & Al & base electrolysis
- (v) is used for Aq & Au



(I) CHEMICAL REDUCTION:

1. Smelting i.e., carbon Reduction - Reduction of metal oxide by coke, coal & CO

$$M_2O_x(s) + x C_{(s)} \xrightarrow{\Delta} 2M_{(\ell)} + x CO \uparrow$$

$$\cdots \Delta G = \Delta H - T\Delta S$$

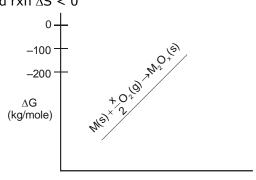
If ΔH is greater than zero then reduction will be feasible on increasing temprature i.e., $|T\Delta S| > |\Delta H|$

Ellingham diagram -

$$M_{(s)} + \frac{x}{2} O_{2(g)} \xrightarrow{\Delta} M_2 O_{x(s)}$$

$$\Delta G = \Delta H - T\Delta S$$

∴ For forward rxn Δ S < 0



(Ellingham diagram for formation of M_2O_2)

Ellingham diagram is a plot of formation of an element oxide between ΔG & ΔT

Ex. Which of the following statements are true:

$$A \rightarrow Mg(s) + \frac{1}{2}O_2(g) \xrightarrow{T_1} MgO(s)$$

$$B \rightarrow Mg(\ell) + \frac{1}{2}O_2(g) \xrightarrow{T_2} MgO(s)$$

$$C \rightarrow Mg(g) + \frac{1}{2}O_2(g) \xrightarrow{T_3} MgO(s)$$

I : Below 1350° Mg can reduce Al_2O_3

II : Above 1350° C Mg Will reduce Al₂O₃
III : Below 1350° Al can reduce MgO

IV : Above 1350° Al can reduce MgO

V : At 1350° C there is no change in free energy i.e., $\Delta G = 0$

Sol.
$$3MgO + 2AI \xrightarrow{\text{then Above } 1350^{\circ}C} \rightarrow AI_2O_3 + 3Mg, \qquad \Delta G < 0$$

(Its $\triangle G$ high) (Its $\triangle G$ less)

$$Al_2O_3 + 3$$
 Mg $\xrightarrow{Below \, 1350^{\circ}C}$ \rightarrow 3 MgO + 2Al At 1350° C both reactions have same G $\therefore \Delta G = 0$

To carry out smelting below 800°C, CO is used as reducing agent while above 800°C, smelting is carried out by coke.

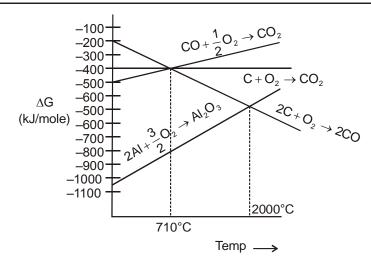
2C(s) +
$$O_2(g) \rightarrow 2CO(g) \Delta H = -221.0 \text{ kJ/mole}$$

$$\Delta S = + 179.4 \text{ J kJ/mol}$$

$$C(s) + O_2(g) \rightarrow CO_2(g)$$
 $\Delta H = -393.5 \text{ kJ/mol}$

$$\Delta S = 2.89 \text{ JK}^{-1} \text{ mole}^{-1}$$

1350°C



- Aluminium can be extracted from Alumina by carbon reduction but the method is highly uneconomical because -
- (i) As the smelting occurs above 200°C hence a part of the aluminium will go into vapour phase (M.P. = 2520°C)
- (ii) At this high temperature the liberated Al will combine with the carbon & aluminium carbide will be formed.
- (iii) ΔH_{for} of alumina is high ve value
 - :. It is thermodynamically more stable & reduction is more difficult
- To extract metal from sulphide ore is carried out by firstly roasting it into metal oxide & followed by its smelting. Metal sulphide or sulphide ore is not directly smelted to metal.

$$2PbS + C \xrightarrow{\Delta} 2Pb + CS_2$$
 (Thermodynamically Not feasible)

$$\begin{array}{l} \text{Pbs} + \frac{3}{2} \, \text{O}_2 & \xrightarrow{\Delta} \, \text{PbO} \, + \text{SO}_2 \!\!\uparrow \\ \\ \text{PbO} + \text{C} & \xrightarrow{\Delta} \, \text{Pb} \, + \text{CO} \, \uparrow \\ \\ \Delta G_{_f} \text{ of PbS} = -21.9 \text{ kcal/mol} \\ \\ \Delta G_{_f} \text{ of CS}_2 = +17.15 \text{ kcal/mol} \\ \\ \Delta G_{_f} \text{ of PbO} = -45.1 \text{ kcal/mol} \\ \\ \Delta G_{_f} \text{ of SO}_2 = -71.7 \text{ kcal/mol} \\ \\ \Delta G_{_f} \text{ of CO} = +32.8 \text{ kcal/mol ial through education} \end{array}$$

(b) Gold Schmidt Thermite Reduction:

Thermite: Al powder

$$Cr_2O_3$$
 + $2Al \xrightarrow{\Delta} 2Cr$ + Al_2O_3
 $(\Delta G_f = -540 \text{ kJ/mole})$ $(\Delta G_3 = -827 \text{ kJ/mole})$
 B_2O_3 + $2Al \xrightarrow{\Delta} 2B + Al_2O_3$
 $2Mn_3O_4 + 8Al \xrightarrow{\Delta} 9Mn + 4 Al_2O_3$
 $Fe_2O_3 + 2Al \xrightarrow{\Delta} 2Fe + Al_2O_3$

This method is used for reduction of those metal oxides which are highly stable if they are reduced by

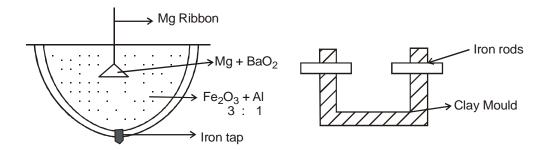




coke it will occur at very high temprature & at this high temperature the liberated metal will combine with the coke & carbide will be formed hence Al powder i.e., thermite is used

Gold schmidt thermite Welding

$$Fe_2O_3 + 2Al \xrightarrow{\Delta} 2Fe + Al_2O_3 \text{ mp. } 1535^{\circ}C$$



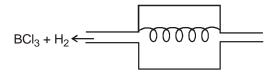
(c) Reduction by Hydrogen:

Because of inflammable nature of hydrogen its use as a reducing agent is very restricted.

$$Cu_2O + H_2 \xrightarrow{\Delta} 2Cu + H_2O$$

$$M_0O_3 + 3H_2 \xrightarrow{\Delta} M_0 + 3H_2O$$

$$B CI_3 + \frac{3}{2} H \xrightarrow{T_0/w} B + 3 HCI$$



Reduction by other metals:

$$SiCl_4 + 2Mg \xrightarrow{\Delta} 2MgCl_2 + Si$$

Kroll process used for extraction of Ti & Zr

$$ZrCl_4 + 2Mg \xrightarrow{\Delta} Zr + 2MgCl_2$$

I.M.I Process (Imperial Metal Industries)

(ii) By Self reduction or Auto reduction or Air Reduction:

This method is used for extraction of copper, lead, mercury i.e., it is used for the extraction of metal from their sulphide ores.

In this method the sulphide ore is roasted in free supply of air to its metal oxide & then air supply is cut off followed by heating by increasing temprature & metal is extracted by self reduction.



$$PbS + \frac{3}{2}O_2 \longrightarrow PbO + SO_2 \uparrow$$

$$PbS + 2O_2 \xrightarrow{\Delta} PbSO_4$$

Now air supply is cut off followed by heating

$$PbS_{(s)} + 2PbO_{(s)} \xrightarrow{\Delta} 3Pb_{(t)} + SO_2 \uparrow$$

Self reduction is responsible for acid rain than roasting because SO_2 dissolves in air, (3927cc CO_2 in 1000cc of H_2O_2)

(iii) By Metal Displacement Method or By Hydrometalurgy:

In this method the concentrated ore is treated/ leached with specific chemical reagent that converts the ore into water soluble salt. Now, on adding more electropositive metal into the aqueous salt solution the metal (less electro positive) is displaced

e.g.

Extraction of Copper from Malacite:

$$Cu(OH)_2 CuCO_3 + H_2SO_4 \longrightarrow 2CuSO_4 + CO_2 \uparrow + 2H_2O$$
or
 $Cu(OH)_2.CuCO_3 \longrightarrow 2CuO + CO_2 \uparrow + H_2O$

$$CuO + H_2SO_4 \longrightarrow CuSO_4 + H_2O$$

 ${
m H_2SO_4} \Rightarrow {
m leaching}$ agent, it leached out Cu as ${
m CuSO_4}$

Now, on adding more electropositive metal:

CuSO₄ + Fe
$$\longrightarrow$$
 FeSO₄ + Cu \downarrow

(Reducing agent)

$$\therefore \quad E^{\circ}_{\text{Cu}^{++}/\text{Cu}} = +0.34$$

$$E^{\circ}_{\text{Fe}^{++}/\text{Fe}} = -0.40$$

$$E^{\circ}_{\text{Cell}} = 0.74$$

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$$\therefore \quad E^{\circ}_{\text{Cell}} = 0.74$$

- Iron is found to be an impurity in the copper ores hence if Zn is added to extract copper, iron will also be displaced along with copper & that is why iron is used.
- Both metals which extracted & by which we extracted are water insoluble
- **(iv) Electro Metallurgy**: The metal is extracted by passing electricity into its fused salt or in aqueous solution.

Extraction of sodium:

⇒ By electrolysis of Aq. NaCl solution :

$$NaCl(s) + x H_2O \longrightarrow Na^+(aq) + Cl^-(aq)$$

 $H_2O \longrightarrow H^+ + OH^-$



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On passing electricity

At cathode :
$$2H^+ + 2e^- \longrightarrow H_2 \uparrow$$

$$\therefore \qquad \mathsf{E}^{\circ}_{\mathsf{H}^{+}/1/2\mathsf{H}_{2}=0}; \, \Delta \mathsf{G} = -\mathsf{nFE}^{\circ}$$

$$E^{\circ}_{Na^{+}/Na} = -2.7 \text{ V}; \quad \Delta G = - \text{ n FE}^{\circ}$$

∴ Na+ does not discharge at cathode

At anode :
$$2CI^- \longrightarrow CI_2^+ + 2e^-$$

$$E^{\circ}_{1/2Cl_2/Cl^-} = -1.36 \text{ Volt}$$

$$E^{\circ}_{1/20^{\circ}/OH^{-}} = -0.44 \text{ V}$$

In sol:
$$Na^+ + OH^- \longrightarrow NaOH$$

$$\Rightarrow$$
 By electrolysis of fused NaCl :

$$NaCl_{(s)} \xrightarrow{\Delta} \underbrace{Na^{+} + Cl^{-}}_{Molten \text{ state}}$$

On Passing electricity

At cathode :
$$2Na^+ + 2e^- \longrightarrow Na$$

At Anode :
$$2Cl^- \longrightarrow Cl_2 \uparrow + 2e^-$$

In sol.
$$Na^+ + OH^- \longrightarrow NaOH$$

In general:

Alkali metals, Alkaline earth metals & Aluminium are extrated by electrolysing their fused salt or molten salts. Metal is not extracted by electrolysing their aq. salt solution because at cathode hydrogen gas is liberated.

⇒ Extraction of Silver :

By electrolysis of Aqueous AgNO₃ solution.

$$AgNO_3 \rightleftharpoons Ag^+ (aq) + NO_3^- (aq)$$

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$$H_2O \rightleftharpoons H^+ + OH^-$$

On passing electricity,

$$\text{At cathode : } Ag^+ \text{ + } e^- \longrightarrow Ag \begin{cases} \because E^\circ_{H^+/1/2H_2} = 0, \ \Delta G = -nFE^\circ \\ E^\circ_{Ag^+/Ag} = +0.80, \ \Delta G = -nFE^\circ \end{cases}$$

Conclusion: The metals which are less electropositive than Hydrogen like Cu, Ag, Au can be obtained by electrolysing their aqueous salt solution.

(v) **By Amulgamation**: (Extraction of Ag & Au by using Mercury) or **Refinning Method**

$$Ag_2S + CuCl_2 \xrightarrow{\Delta} 2AgCl + CuS$$

Now, on adding excess of Mercury:

$$2AgCl + x Hg \longrightarrow Ag. x Hg + HgCl_{2}$$

or

$$Ag + x Hg \longrightarrow Ag. xHg$$

Native ore Amalgam

Now the silver amalgam is heated in a vessel made of iron.

Ag. x Hg 1
$$\xrightarrow{\Delta}$$
 Ag \downarrow + x Hg \uparrow (in vapour phase)

Mercury does not form amulgum with iron & platinum therefore iron vessel are used.

Flux: Flux are those substances which combine with acidic or basic impurities & form fusible mass called slag.

Acidic flux - SiO_2 , P_4O_{10} , B_2O_3 or $Na_2B_{11}O_7$

Basic flux - CaO, MgO

Slag - It is a fusible mass,

Characteristic of slag:

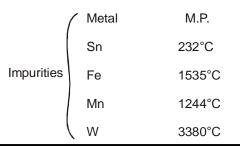
- (i) It is obtained as a fusible mass.
- (ii) It is lighter & immisible with the extracted the molten metal & hence it can easily be skimmed off.
- (iii) Its m.p. is less than the extracted metal.
- (iv) It prevents air oxidation of the molten metal.

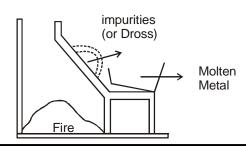
• Refining of impure metal :

- (A) By physical Methods:
- (a) liquation
- (b) Distillation
- (c) Zone refining
- (B) By Chemical Methods
- (a) Oxidation
- (b) Poling
- (c) Vapour Phase Refining potential through education
- (C) By Electrolytic Refining

(A) By Physical Method:

(a) Liquation Method:





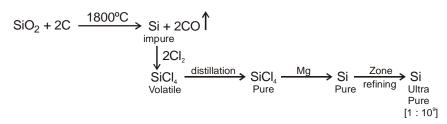
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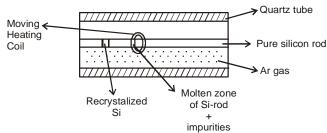


This method is used for refining of those metal which have very low m.p. in comparison to impurity present in them.

e.g. \rightarrow Sn, Pb, Hg, Bi, Zn

- **(b) Distillation Method :** It is used for refining of those metals which are volatile & hence it is used for refining of Zn, Cd, Hg (i.e., is of filled d orbital metal)
- (c) Zone Refining: (Si, Ge, Pb, B, Ga, In)

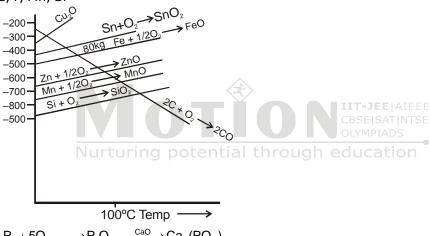




Concept: Impurities are more soluble in the melt than in the solid state.

- (B) By Chemical Methods:
- (a) Oxidation: (Fe, Sn, Pb)
- **eg. Pig iron**: M.P. 1080

Impurities: C, P, Mn, Si



$$P_4 + 5O_2 \longrightarrow P_4O_{10} \xrightarrow{CaO} Ca_3(PO_4)_2$$

$$Si + O_2 \longrightarrow SiO_2$$
 (acidic)

$$Mn + \frac{1}{2}O_2 \longrightarrow MnO$$
 (Basic)

$$MnO + SiO_2 \longrightarrow MnSiO_3 + Heat$$

Slag

$$C + \frac{1}{2}O_2 \longrightarrow CO$$



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This method is used for the refining of metals in which impurtities are more oxidisable than metal itself. When impurities oxidise they are converted into either volatile oxides or non volatile oxides Non-volatile oxides are removed either by slag formation or by removing their skum Oxidation is known by various names: bassemerization (Fe), Cupellation (Ag), Softening (Pb) or Puddling (for iron), tossing (for iron)

Polling: When along with impurities the metal to be refine is also oxidised part then this method is used. In this method the molten impure metal is steared with green wood log, The hydrocarbons released from the log reduce metal oxide into metal while impurity oxides are not reduced. This method is used for refining of Cu & Tin. In both metals during poling iron get oxidised into FeO which in turn is oxidised into Fe₂O₃ while in case of Sn, SnO₂ is reduced to tin (Sn) & in case of Cu copper (I) oxide i.e., cuprous oxide is reduced to Cu,

- (c) Vapour Phase Refining: Impure metal is allowed to react with a suitable reagent such that a volatile unstable compound is formed & then the compound is decomposed to pure free metal when it is subjected to heat.
- Mond's Process: used for refining of Ni

$$\underset{\text{impure}}{\text{Ni}} + 4\text{Cu} \xrightarrow{50^{\circ}\text{C}} \underset{\text{volatile unstable}}{50^{\circ}\text{C}} \xrightarrow{80^{\circ}\text{C}} \underset{\text{pure}}{\text{Ni}} + \text{CO} \uparrow$$

(C) By Electrolytic Refining:

Anode: Impure metal **cathode:** Pure metal

Electrolyte : Aq. salt sol. of metal/fused metal salt + Acid

Anode Mud: Metals which are less electropositive than the metal to be refined.

In electrolyte: More electropositive metals are found.

eg. in Cu: Ag, Au, Fe, Zn



Important Ore: Tin stone or Cassiterite SnO₂ (diamagnetic)

Extraction:

I. Concentration or Dressing or Beneficiation of Ore:

- (A) By Gravity separation
- (B) By Magnetic separator

II. Extraction of crude Metal from concentrated ore:

- (A) Calcination
- (B) Reduction of metal oxide into free metal ⇒ Smelting

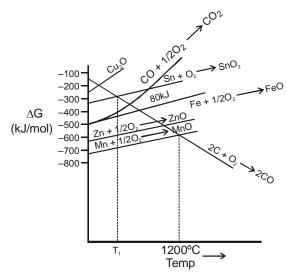
$$SnO_2 + 2C \xrightarrow{1200-1300^{\circ}C} Sn(\ell) + 2CO \uparrow$$



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Coke reduce SnO_2 above 1200°C while CO is not used above 1200°C. If Fe impurities is not present then coke can reduce it also at T_1 temp.



- III. **Refining**: Thus obtain Tin has impurities of Mn (m.p. 1244°C), Fe (1535°C) & W(3380°C) while M.P. of Sn is 232°C
 - $a \rightarrow liquation$: Impurities remain in the form of Dross.
 - $b \rightarrow Polling$
- (C) Electrolytic Refining:

Anode: Impure Tin Cathode: Pure Tin

Electrolyte Aq. SnSO₄ sol. + dil. H₂SO₄

In Anode Mud: CO (It is obtained as biproduct in metallurgy of Sn)

In electrolyte: Fe & Mn

- **Ex.** In which metal's metallurgy tunguston is obtained as biproduct?
- Sol. Tin

<u>LEAD</u>

Imprtant Ores: Galena (PbS), Cerussite (PbCO₃), Anylesite (PbSO₄)

Extraction of lead from galena:

- Concentration or Dressing or Beneficiation of ore: Froth floatation in presence of NaCN because PbS is always with Zns
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- **II.** Extraction of Crude Metal from concentrated ore :

Lead is extracted from concentrated galena by two methods

- (A) By self Reduction or Air Reduction or by Auto Reduction: when galena is rich in lead content / PbS content.
- (B) By Carbon reduction: When galena is poor in lead content / PbS content.
- **A:** By Self Reduction (when ore is rich in lead content)

$$PbS + \frac{3}{2}O_2 \xrightarrow{\Delta} PbO + SO_2 \uparrow$$

$$PbS + 2O_2 \xrightarrow{\Delta} PbSO_4$$

Now, air supply is cut off followed by heating of reasted mass with or without more concentrated



→ CaCO₃ or CaO + PbS

Exhaust gases

→ Coal Fire

0000000

Galena, by raising temp. (
$$\Delta G = \Delta H - T\Delta S$$
)

PbS + 2PbO
$$\xrightarrow{\Delta}$$
 3Pb(ℓ) + SO, \uparrow

$$PbS + PbSO_4 \xrightarrow{\Delta} 2Pb (\ell) + 2SO_2 \uparrow$$

B: By Carbon Reduction - It is completed in two stages.

$$\begin{array}{c} PbS + \frac{3}{2}O_{2} \xrightarrow{\Delta} PbO_{-45.1\,\text{kcal}} + SO_{2} \uparrow \\ kcal \end{array}$$

$$PbS_{-21.9 \text{ kcal}} + 2O_2 \longrightarrow PbSO_4$$

$$_{-159.5 \text{ kcal}}$$



Ist **stage**: Conversion of PbS into PbO by heating it into limited supply of air in a furnace called "Sinterer",

As the formation of $PbSO_4$ is thermodynamically more feasible hence the concentrated galena is roasted in limited supply of air in sinterer.



(i) Prevents the formation of lead sulphate because it diffuses the passed air into it

(ii) PbS +
$$\frac{3}{2}O_2 \xrightarrow{\Delta} PbO + SO_2 \uparrow$$

$$PbO + SiO_2 \xrightarrow{\Delta} PbSiO_3$$

$$PbSiO_3 + CaO \longrightarrow CaSiO_3 + PbO_{Amphoteric or W.B.}$$

Thus by roasting of PbS, lead oxide is obtained. It regenerates PbO from lead silicates if it is formed

IInd stage: Smelting or Carbon Reduction of PbO

PbO + C
$$\xrightarrow{>1000 \, ^{\circ}\text{C}}$$
 Pb (ℓ) + CO \uparrow

Or

PbO $\xrightarrow{\text{PbS}}$ Pb

Cu₂O $\xrightarrow{Q_2}$ Cu₂O $\xrightarrow{Q_2}$ CuyMPIADS

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-100 $\xrightarrow{-200}$ $\xrightarrow{-300}$ $\xrightarrow{-300}$ $\xrightarrow{-500}$ $\xrightarrow{-500}$ $\xrightarrow{-600}$ $\xrightarrow{-700}$ $\xrightarrow{-700}$ $\xrightarrow{-800}$ $\xrightarrow{-700}$ $\xrightarrow{-800}$ $\xrightarrow{-700}$ $\xrightarrow{-800}$ $\xrightarrow{-700}$ $\xrightarrow{-700}$

METALLURGY



III. Refining: Thus obtained lead contains impurities of Cu, Ag, Au, Zn, As, Sb, Bi & Sn.

- **a. Liquation** It removes mainly impurities of Cu.
- **b. softening** Removal of impurities by air oxidation.

Impurelead obtained after softening is called Argentifarous lead which contains 1 - 2% Ag.

- **Desilverization of Argentiferous lead**: It completes by two processes c.
- Pattinson's Process: In this method by repeated Fractional crystallisation of lead from argentifarous (i) lead is carried out till the concentration of silver raised to 2.6% at which it forms unreacted mixture with lead that melts at 303° c while m.p. of pure lattice is 327°C
- Parke's Process: It is based on principle of solvent extraction, Distribution law, partition law. (ii)

Solvent used: Molten zinc.

The characteristics of Zinc to be used as a solvent

- (a) Silver is about 300 times more soluble in Zn than Pb
- (b) Zn is lighter than lead
- (c) Zn is immisible with lead
- (d) M.P. of Zn is 420°C and that of Pb is 327°C
- (e) Zn is volatile while Ag is non-volatile.
- d. **Electrolytic Refining by Bett's Process:**

Anode: Impure lead Cathod; pure lead

Electrolyte : Molten/ Fused (PbSiF₆ + H₂SiF₆ + Gelatin)

Anode Mud: Cu, Ag, Au In Electrolyte: Zn, Sn, Bi

Plumbosolvency: Dissolution of Pb into water in presence of air. plumbosolvency increases in the

presence of CH₃COOH, NO₃, NO₃

To prevent plumbosolvency in electrolytic refining of lead, molten salt is used.

COPPER

Important Ores: Native Ore, Sulphide ore - Chalopyrite (CuFeS₂)

$$2CuFeS_2 \equiv Cu_2S + FeS + FeS_2$$

Chalcocite or copper glance: Cu,S

Bornite or Peacock Ore; Cu_5FeS_4 ($2CuFeS_4 = 5Cu_5S + FeS + FeS_5$)

Oxide ore

Carbonate ore:

CuCO₃. Cu(OH)₂ Malacite (green)

Azurite (blue) 2CuCO₃. Cu(OH)₂

Copper can be extracted by anyone of the following methods.

- (i) By self Reduction or by auto reduction.
- (ii) By Hydrometallurgy
- By carbon Reduction (iii)
- (iv) By electrolysis of aq. copper sulphate
- Reduction of copper oxide by hydrogen. (v)
- Self Reduction or Auto reduction is the commercial method of reduction

Extraction of Copper from chalcopyrite by self Reduction or Auto Reduction or Air Reduction:

Concentration: By froth floatation Process. I.



II. Extraction of Crude Metal from concentrated ore.

A. Roasting:

$$2\mathsf{CuFeS}_2 + \mathsf{O}_2 \xrightarrow{\quad \Delta \quad} \mathsf{Cu}_2\mathsf{S} \atop \mathsf{copper} \text{ (I) sulphide} + 2\mathsf{FeS} + \mathsf{SO}_2$$

B. Smelting:

The roasted mass is mixed with silica & some coke & then it is heated in presence of air in a blast furnace in the temperature range of 1400 – 1450° C

$$FeS + \frac{3}{2}O_2 \xrightarrow{\Delta} FeO + SO_2 \uparrow$$

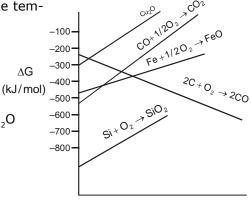
$$Cu_2S + \frac{3}{2}O_2 \xrightarrow{\Delta} Cu_2O + SO_2$$

remaining FeS which is not Oxidised react. with Cu₂O

$$FeS + Cu_2O \xrightarrow{\Delta} FeO + Cu_2S$$

Silica removes FeO in form of slag.

$$FeO + SiO_2 \longrightarrow FeSiO_3$$
 (slag)



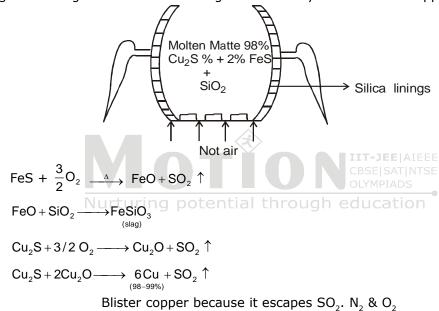
Temp. \longrightarrow

Role of coke:

$$\underset{^{\Delta G--64.2}}{\mathsf{FeO}} \xrightarrow{^{[O]}} \underset{^{-195.5}}{\mathsf{Fe}_2\mathsf{O}_3} \xrightarrow{^{\mathsf{C}}} \mathsf{FeO}$$

When smelting is over the furnace contains 98% of Cu_2S copper (I) sulphide & 2% FeS & this molten mass is called matte over which layer of slag exist.

(c) Bassemerization : The molten matte is mixed with some silica & it is taken into Bassemer converter having silica linings & blast of hot air is given into it. By self reduction copper is obtained.



Here copper (II) oxide is not formed because it is thermodynamically not feasible.

Thus obtained copper is called Blister copper & it is 98 - 99% pure. Blister appearances are due to escape of SO_2 , N_2 & O_2 from molten copper.

III. Refining: Blister copper contains impurity of Ag, Au, Fe, Se, Te, Pt & Sb

a. Poling



METALLURGY

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b. Electrolytic Refining ; Anode : Impure copper

cathode; Pure copper

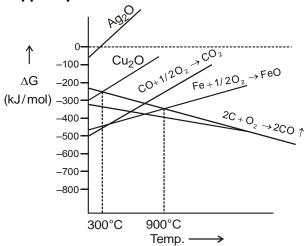
Electrolyte ; Aq. CuSO₄ sol. + dil. H₂SO₄ In Anode Mud/ Slime : Ag, Au, Pt, Se, Te

In Electrolyte: Fe

(Sb during oxidation it completely removes)

The main source of serenium (Se) & telurium (Te) is Anode mud obtained from Cu refining. Se has photoreceptor property hence it is used in zerox machine. Se is also used as decolouriser for glass.

Extraction of Copper by carbon Reduction from Chalcocite.



I. Concentration: By Froth Floatation

II. Extraction of Copper from conc. ore

(a) Roasting:

$$Cu_2S + 3/2 O_2 \rightarrow Cu_2O + SO_2 \uparrow$$

(b) Smelting

$$Cu_2O + C \xrightarrow{2900^{\circ}C} 2Cu + CO \uparrow$$

⇒ Both CO & C can reduce Cu₂O into Cu.

Extraction of Copper by Hydrometallurgy

• From Malachite (discussed in discussion of hydrometallurgy)

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From Chalcopyrite (CuFeS₃)

Chalcopyrite ore is left open in presence of atomospheric air & moisture for a year long which oxidises copper (I) Sulphide into copper sulphate & FeS into $FeSO_4$ Now, aq. solution of $CuSO_4$ & $FeSO_4$ scrap iron / Fe is added copper is displaced.

$$Cu_2s + O_2 \xrightarrow{Atm \ air} CuSO_4 + CuO$$

$$FeS + 4O_2 + H_2O \xrightarrow{Atm \ air} FeSO_4 + FeO + H_2SO_4$$

$$CuO + H_2SO_4 \longrightarrow CuSO_4 + H_2O$$

On adding scrap Fe/Fe:

$$FeSO_4 + CuSO_4 + Fe \longrightarrow 2FeSO_4 + Cu \downarrow$$

Extraction of copper by electrolysis of Aq. CuSO₄ solution :

At cathode copper is liberated

Extraction of Copper by Reducing Cu₂O with Hydrogen:

Coke, CO, CS can reduce Cu₂O to Cu.

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SILVER

Ores: (a) Native ore

(b) Sulphide Ores: (i) Argentite or silver glance (Ag₂S)

(ii) Pyrargyrite or Ruby silver $3Ag_2S.Sb_2S_3$

(c) Halide Ores : Chorargyrite or Horn silver (AgCl)

(d) As a by Product:

- From ext of Pb.
- From ext of Cu
- From ext. of Zn.

Extraction of Silver:

Feasibility of extraction of Ag by self Reduction from silver glance

It is very slow reaction. By increasing temperature ΔG of Ag₂O becomes +ve

- :. It is not thermodynamically feasible.
- Extraction of Ag by self reduction from silver glance or argentite is thermodynamically not feasible because
- (i) by incresing temp. the roasting of Ag, s is thermodynamically not favourable.
- (ii) The content of Ag₂S is two poor to carry out self reduction.
- Extraction of silver by Cyanidation or Mac Arthur forest method From Argentite or silver glance :
- (i) concentration
- (ii) Concentrated silver glance / Argentite is leached with 0.4 to 0.64 aq. NaCN solution which leached out (converts) Ag into soluble Cyno complex in presence of air.

$$Ag_2S + 4NaCN \xrightarrow{Atm \ air} 2Na [Ag(CN)_2] + Na_2S$$

The role of air is to oxidise Na₂S so that reaction proceed in the forward direction.

From native Ore: Native ore is leached with 0.4 – 0.6% aq. NaCN solution in presence of air & soluble cyno complex is formed.

The role of oxygen is to oxidise Agotential through education

From Horn silver:

Now on adding Zn powder into the soluble complex

$$2[Ag(CN)_2]^- + Zn_{Red. agent} \longrightarrow [Zn(CN)_4]^{2-} + 2Ag \downarrow$$

In place of Zn powder copper is not used because of its less reducing character.

By Amulgamation: (Already discussed)

Refining: Pb, Zn, Cu, Au are impurities.

(i) Here two flux are used: Potassium Nitrate or Borax Ag is refined by using flux of Pot. Nitrate (KNO₃) or Borax. If KNO₃ is used it oxidises the impurities or if Borax is used it will remove impurities in the form of



METALLURGY

meta borates

$$KNO_{3} \xrightarrow{\Delta} KNO_{2} + \frac{1}{2}O_{2}$$

$$Na_{2}B_{4}O_{7} \xrightarrow{\Delta} 2NaBO_{2} \xrightarrow{} B_{2}O_{3}$$

$$\downarrow \quad (ZnO, PbO, Cu_{2}O)$$

$$Zn(BO_{2})_{2}, Pb(BO_{2})_{2}, CuBO_{2})$$

$$(Metaborates)$$

(ii) Cupellation: Air is blown into molten impure Ag which oxidises Pb into litharz (PbO) & which is blown away by air pressure.

When Ag content is more then this method is used unless Park's Method is used.

Cupellation

Removal of lead as an impurity from Ag by air oxidation

Park's

Removal of Ag as an impurity from Pb by using solvent extraction

(iii) **Electrolytic Refining:**

Anode: Impure Ag Cathode: Pure Ag

Electrolyte: Aq. AgNO₃ + dil. H₂SO₄

In Anode mud/slime: Au In Electrolyte: Cu, Zn

GOLD (Au)

Ores: Native Ore (in form of Plaur gold & in form of Vein gold

gold trapped in rocks

As a by Product: From ext. of Cu

> From ext. of Pb from ext. of Ag

Extraction of Gold:

(ii) By Cyanidation or By Mac. Arthur Forest Method:

$$2Au + NaCN_{0.2-0.3\% \text{ aq. sol.}} + H_2O + 1/2O_2$$
 \longrightarrow $2Na[Au_{C.N=2}^{I}(CN)_2] + 2NaOH_{C.N=2}^{I}$

On Adding zn powder In it

$$Zn + 2[Au(CN)_2]^- \longrightarrow [Zn(CN)_4]^{2-} + 2Au$$

Nurturing potential through education Refining:

By electrolytic Method: Anode: Impure Au Cathode: pure Au

Electrolyte: Aq. sol. of AuCl₃ + dil. HCl

In Anode Mud:

In Electrolyte: Αg

Fineness or Purity of Gold: 24 carats = 100% gold For making gold jwelleries it is alloyed with Ag & Cu

In Extraction of Gold

(I) concentration: By Panning based on principle of Gravity separation

Au = 19.3 gm/cc $SiO_2 = 2.5 \text{ gm/cc}$



MERCURY

Ores: • Native Ore

• Cinnabar (HgS): Bright Red coloured

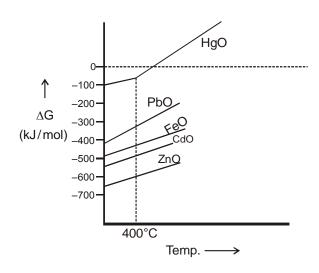
Extraction from Cinnabar

(i) Concentration: By Froth Floatation Process

(II) Extraction of Hg from concentrated Ore: By self Reduction or Auto Redⁿ or Air Reduction

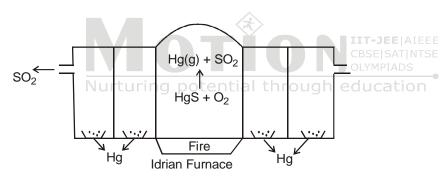
$$HgS + \frac{3}{2}O_2 \xrightarrow{600^{\circ}C} Hg(g) + SO_2 \uparrow$$

$$HgO \xrightarrow{> 400^{\circ}C} Hg(g) + \frac{1}{2}O_2 \uparrow$$



Self Reduction is carried out in

"Idrian Furnace"



III Refining: Now impurities are: Zn, Cd, Pb, Fe

Mercury is refined by

- (a) Air oxidation
- (b) Now impure mercury is treated with $5\%~\mathrm{HNO_3}$ to remove left impure metal oxides into soluble nitrates
- (c) Lastly mercury is refined by vaccum distillation

ZINC

Ore: Zinc blends : ZnS Calamine : ZnCO₃

Zincite : ZnO

Extraction of Zinc from Zinc Blends:

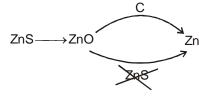
(i) Concentration: By Froth Floatation

(ii) Extraction of Zinc from concentrated ore:

(a) Roasting:

$$ZnS + \frac{3}{2}O_2 \longrightarrow ZnO + SO_2 \uparrow$$

$$ZnO + 2O_2 \longrightarrow ZnSO_4$$

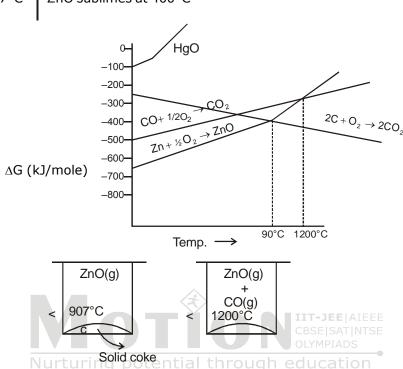


To prevent the formation of $ZnSO_4$, ZnS is roasted in limited supply of air. So that only ZnO can be formed.

(b) smelting:

Žn: M.P. 420°C B.P. 907°C

ZnO sublimes at 400°C



CO is preferred.

- Zinc is obtained by reduction of ZnO only above 907°C.
- As ZnO sublimes above 400°C therefore its reduction above 907°C will be more efficiently be carried out by CO.
- To obtain zinc from gaseous product cooling is carried out but during cooling a part of zinc gets reoxidised into ZnO.
- To prevent reoxidation of zinc during its isolation from gaseous oproduct
 - (i) Zinc is obtained by shock colling or rapid cooling
 - (ii) Reduction is carried out in presence of excess of coke.
 - so that the formed CO₂ can be reduced into CO.

$$ZnO(g) + CO(g) \xrightarrow{1200^{\circ}C} Zn(g) + CO_2(g)$$

Thus obtained zinc is called spelter which contain impurities of Cd, Ag, Pb & Fe, Ag.

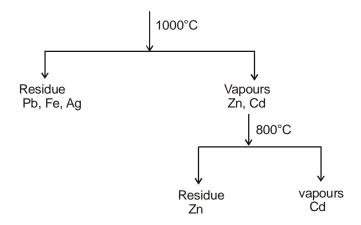




III Refining:

In spelter 99% zinc is pure from this zinc (pure) is obtained by vaccum distillation.

spelter (zn, Cd, Pb, Fe, Ag) B.p. 907°C 765°C 1751°C 2750°C 2155°C



- Extraction of zinc By electrolysis of Aq. $ZnSO_4$ solution : from zinc Blende :
- (I) Concentration: By Froth Floatation:
- (II) Ext. by Electrolysis of ZnSO₄ solution.
 - (A) Roasting Free supply of air (because to make ZnSO₄)

$$ZnS + \frac{3}{2}O_2 \xrightarrow{\Delta} ZnO + SO_2 \uparrow$$

$$ZnS + 2O_2 \xrightarrow{\Delta} ZnSO_4$$

- (B) Electrolysis of Aq. ZnSO₄
- The roasted mass is leached with dil. H₂SO₄ to convert it into ZnSO₄
- Zn powder is added into aq. ZnSO₄ solution to remove impurities of Cd.

$$Zn \ + \ Cd^{\scriptscriptstyle ++} \ \rightarrow \qquad \quad Cd^{\;\downarrow} \ + \ Zn^{\scriptscriptstyle ++} \quad E^{\circ}_{\; cell} = +0.36 \ V$$

- Now elecrolysis of aq. ZnSO₄ is carried out by using Al cathode and Pb anode.
- **Ex**. In extraction of zinc by electrolysis of Aq. ZnSO₄ solution from zinc blends, why zinc powder is added.
 - (a) To reduce ZnO
 - (b) for self reduction.
 - (c) To remove impurities of Cdg potential through education
 - (d) To ppt. Cd
- **Sol.** c,d

Ex. In this, in electrolysis what metals are used for anode & cathode?

Sol. Cathode : Aluminium (Al) Anode : Lead (Pb)

MAGNESIUM

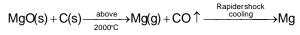
Sources / Ores: Magnesite: MgCO₃,

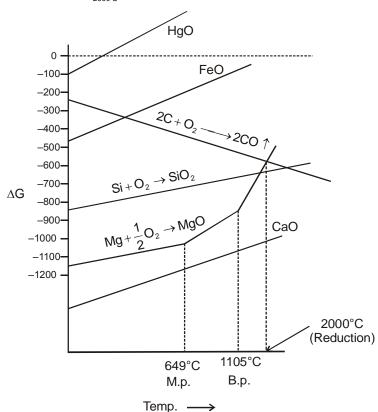
Dolomite: CaCO₃. MgCO₃ Carnallite: KCl. MgCl₂.6H₂O Epsom's salt: MgSO₄. 7H₂O

Extraction

From Magnesite:

- Smelting or Carbon Reduction





Extraction of Mg by Pidgeon Process;

$$CaCO_{3}.MgCO_{3} \xrightarrow[Co_{2}\uparrow]{} CaO + MgO \xrightarrow[(Si,Fe)_{\Delta}]{} Ferrosilicon Alloy} Mg + CaSiO_{3}$$

Extraction of Mg by Electrolytic Reduction of MgCl₂: By Dow's Process

It is completed in two steps

Step I : Isolation of MgCl₂ (Anhydrous MgCl₂) from sea water By Dow's sea water process

$$\underset{\text{(sea water)}}{\text{Mg}} \overset{\scriptscriptstyle ++}{} + \underset{\text{slaked lime}}{\text{Ca(OH)}}_2 \longrightarrow \underset{\text{Mg(OH)}}{\longrightarrow} \text{Mg(OH)}_2 \downarrow + \text{Ca}^{\scriptscriptstyle ++}$$

Conversion of Mg(OH)₂ into MgCl₂. 6H₂O

$$Mg(OH)_2^{\downarrow} + 2 HCI \longrightarrow MgCl_2 \xrightarrow{Crystallisation} MgCl_2.6H_2O$$

Conversion MgCl₂. 6H₂O into anhydrous MgCl₂

$$MgCl_2.6H_2O \xrightarrow{\Delta} MgCl_2 + 6H_2O \uparrow$$

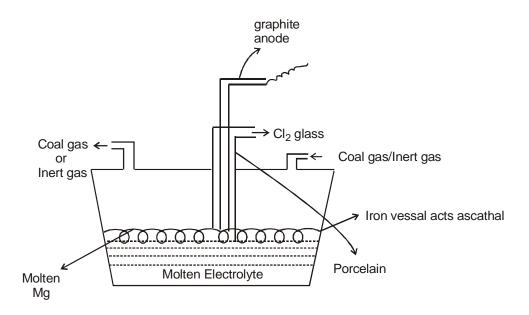
If MgCl₂. 6H₂O is heated in absence of dry HCl to make Anhydrous

$$MgCl_2$$
. $6H_2O \Longrightarrow Mg(OH) Cl + HCl \uparrow \xrightarrow{\Delta} MgOCl_2 \xrightarrow{\Delta} MgO$ fumes of HCl is formed



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Step II: Electrolysis of fused MgCl₂



Coal gas is continuously passed because Mg has geat affinity towards ${\rm O_2}$, ${\rm N_2}$ etc.

Impurities are of more eletro positive metals (Mg has less electropositive than Na and Ca).

Electrolyte: 35% MgCl₂ + 50% NaCl + 15% CaCl₂

M.P. of the electrolyte: 700°C under this composition.

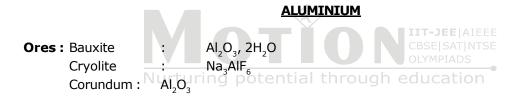
At cathode:

$$Mq^{++} + 2e^- \rightarrow Mq$$

At Anode

$$2Cl^{-} \rightarrow Cl_{2} \uparrow + 2e^{-}$$

impurties are of more electropositive metals (Mg has less electropositive than Na & Ca)



Extraction of Al

It completes in three steps:

Step I: concentration or Purification of Bauxite

Step II: Electrolytic Reduction of Alumina

Step III: Refining of Impure Aluminium

Step I : Concentration or purification of Bauxite :

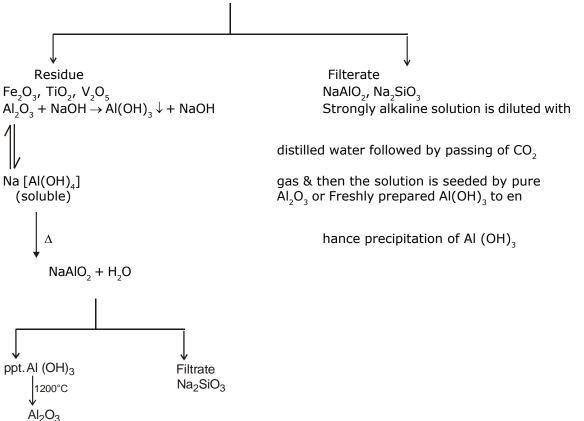
(A) By Bayer's Process: It is used for the purification of red Bauxite by leaching with sodium hydroxide.

Red Bauxite contains : Al_2O_3 . $2H_2O$, Fe_2O_3 , SiO_2 , TiO_2 & 0.2 – 0.3 % V_2O_5 due to the presence of Fe_2O_3 change transfer phenonmena takes place in Fe_2O_3) Bauxite colour is red.

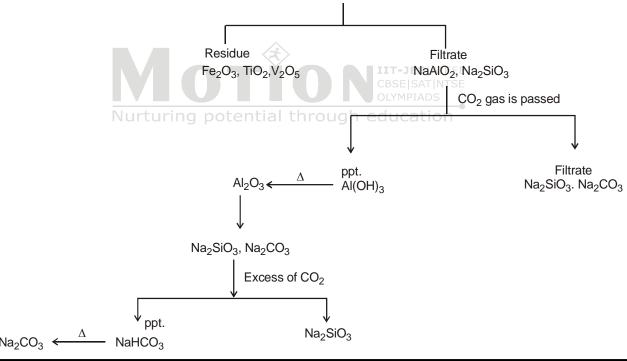




Red Bauxite is leached/ digested with conc. NaOH at 200 – 250°C at 35 atm pressure and filtered.



(B) By Hall's Process: - It is also used for purification of red Bauxite. Solid Red Bauxite is fused with solid sodium carbonate Na₂CO₃ & then fused mass is extracted with water & filtered



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(C) By Serpek's Method: This is used for purification of white Bauxite (that has impurity mainly of silica). White Bauxite is mixed with coke & it is heated in presence of N_2 gas in temprature range of $1800^{\circ} - 2000^{\circ}$ C

$$Al_2O_3 + 3C + N_2 \xrightarrow{1800-2000^{\circ}C} 2AIN + 3CO \uparrow$$

 $SiO_2 + 2C \xrightarrow{1800-2000^{\circ}C} Si + 2CO \uparrow$

Now, AIN is treated with steam:

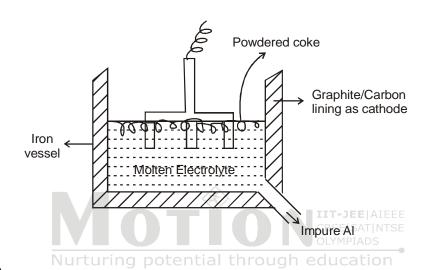
$$\begin{array}{c} \text{AIN} + 3\text{H}_2\text{O} \longrightarrow \text{AI(OH)}_3^{\downarrow} + \text{NH}_3^{\uparrow} \\ \text{steam} & \downarrow 1200^{\circ}\text{C} \\ \text{AI}_2\text{O}_3 \end{array}$$

Note: Only Bayer's process comes under leaching because in leaching aq. reagent is used & in other two process it is fused.

Step II: Electrolytic Reduction of pure Alumina by Hall Heroult's Process:

M.P. of Al : 660°C M.P. of Al $_2$ O $_3$: 2000°C B.P. of Al : 2467°C Al $_2$ O $_3$ is not good conductor

Electrolyte: $85\% \text{ Na}_3 \text{AIF}_6 + 5\% \text{ AIF}_3 + 5\% \text{ CaF}_2 + 5\% \text{ AI}_2 \text{O}_3$ M.P. of electrolyte under this composition: 950°C



At cathode

$$AI^{3+} + 3e^{-} \rightarrow AI$$

At Anode:

$$2O^{-} \longrightarrow O_{2}^{\uparrow} + 2e^{-}$$
: $C + 4F^{-} \longrightarrow CF_{4}^{\uparrow} + 4e^{-}$
 $C + O^{-} \longrightarrow CO_{2} + 2e^{-}$
 $2F^{-} \longrightarrow F_{2}^{\uparrow} + 2e^{-}$

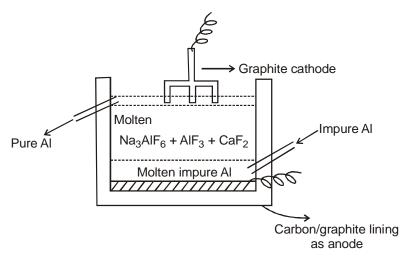
In place of cryolite, Lithium carbonate can be used. Li₂CO₃ place following growths:

- (i) It reduces m.p. of alumina & also increases its electrical conductivity.
- (ii) By its use fluorine & fluorocarbons are not evolved at anode.





Step III: Refining of impure Aluminium By Hoop's Process:



$$E^{\circ}_{\Delta I/\Delta I^{3+}} = +1.66 V$$

Hoop's method is based on density. Molten impure Al has higher density so it is found at bottom level.

BORON

Ores / Sources:

Borax : $Na_2B_4O_7$. $10H_2O$ Colemanite : $Ca_2B_6O_{11}$. $5H_2O$ Panderinite : $Ca_2B_6O_{11}$. $3H_2O$

Boronatrocalcite: CaB₄O₇. NaBO₂. 8H₂O

Extraction

⇒ From Borax:

$$Na_2B_4O_7 \xrightarrow{conc.} H_2SO_4 \xrightarrow{dH_3BO_3} \xrightarrow{\Delta} B_2O_3 \xrightarrow{Mg} 2B$$
or All CBROSSES AT INTSE

⇒ By Van Arkel Process :

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$$BI_3(g) \xrightarrow{\text{W or Ta (tantalum)}} B + \frac{3}{2}I_2 \uparrow$$

{BI₃ is formed when orthobonic acid react with HI}

⇒ By Reduction of BCl₃

$$BCI_3 + \frac{3}{2}H_2 \xrightarrow[Filamant]{W \text{ or Ta}} B + 3HCI$$

⇒ By Thermal decomposition of B,H,

$$B_2H_6(g) \xrightarrow{\Delta} 2B + 3H_2$$

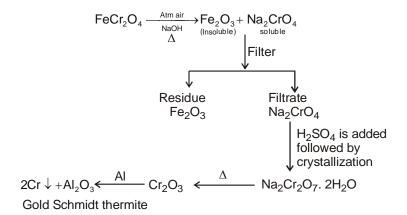
⇒ B is also isolated from B₄C (Boron carbide)



CHROMIUM

Ore: Chromite: $FeCr_2O_4$ (FeO + Cr_2O_3)

Extraction:



SODIUM

Isolation by electrolysis of fused NaOH ⇒ Castner's Process

$$NaOH(s) \xrightarrow{\Delta} \underbrace{Na^{+} + OH^{-}}_{Molten \ state}$$

At anode (Ni):
$$2OH^{-} \longrightarrow H_2O + \frac{1}{2}O_2 \uparrow +2e^{-}$$

At Cathode (Iron) : $2Na^+ + 2e^- \longrightarrow 2Na$

