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# Chapter 6

## Dynamical Systems

*Discrete Mathematics II/Mathematical Modelling*

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# Microclimate forecasting and control in greenhouses

Dynamical Systems

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**Figure:** Greenhouses.

- Optimum growing environment;
- Longer growing season;
- Garden in any weather condition;
- Protection from pests;
- ...

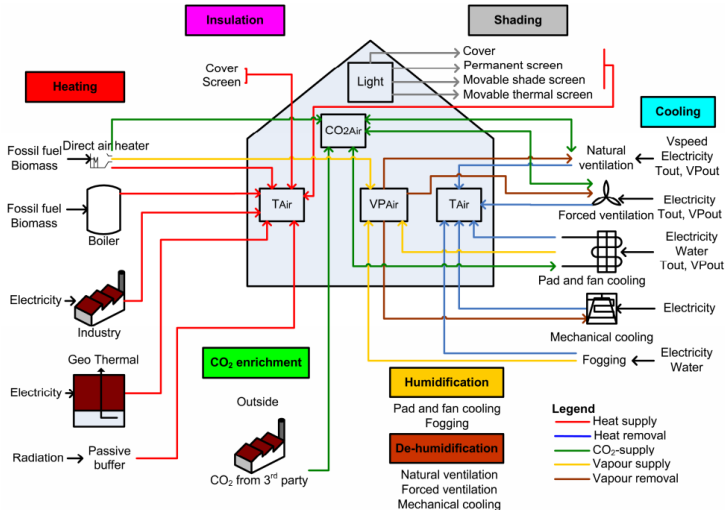
# Greenhouse elements and functions



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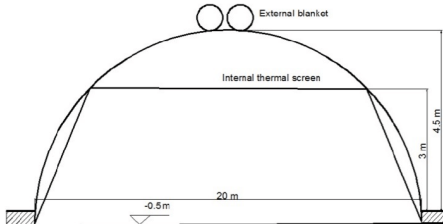
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**Figure:** Greenhouse elements and functions.

# $CO_2$ flow and the photosynthesis of plants



**Figure:** Internal thermal screen that divides the air in a greenhouse into two compartments: above and below the thermal screen.

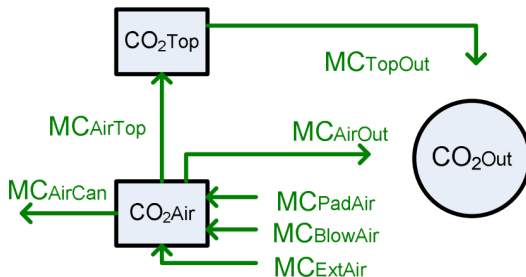


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## $CO_2$ flow and the photosynthesis of plants



**Figure:**  $CO_2$  flow in a greenhouse.

- *Top/Air*: the compartment above/below the thermal screen;
- *Out/Ext*: outside the greenhouse/external source;
- *Blow/Pad*: the direct air heater/pad and fan;
- *Can*: the canopy inside the greenhouse;
- $MC_{AB}$ : the net  $CO_2$  flux from A to B.



# $CO_2$ flow and the photosynthesis of plants

## Balance laws:

$$cap_{CO_2 Air} \dot{CO}_2 Air = MC_{BlowAir} + MC_{ExtAir} + MC_{PadAir} - MC_{AirCan} - MC_{AirTop} - MC_{AirOut}. \quad (1)$$

$$cap_{CO_2 Top} \dot{CO}_2 Top = MC_{AirTop} - MC_{TopOut}. \quad (2)$$

- $cap_{CO_2 Top/Air}$ : capacity of the compartment above/below the thermal screen to store  $CO_2$  (m);
- $\dot{CO}_2 Top/Air$ : the rate change of  $CO_2$  concentration in the compartment above/below the thermal screen in time ( $mg\ m^{-3}\ s^{-1}$ );
- $MC_{AB}$ : the net  $CO_2$  flux from  $A$  to  $B$  ( $mg\ m^{-2}\ s^{-1}$ ).





$$MC_{BlowAir} = \eta_{HeatCO_2} H_{BlowAir} = \frac{\eta_{HeatCO_2} U_{Blow} P_{Blow}}{A_{Flr}}. \quad (3)$$

- $\eta_{HeatCO_2}$ : the amount of  $CO_2$  released when 1 Joule sensible energy is produced by the direct air heater ( $\text{mg } \{CO_2\} \text{ J}^{-1}$ );
- $H_{BlowAir}$ : the heat flux from the direct air heater to the greenhouse air ( $\text{W m}^{-2}$ );
- $U_{Blow}$ : the control valve of the direct air heater ranging in  $[0, 1]$ ;
- $P_{Blow}$ : the heat capacity of the direct air heater (W);
- $A_{Flr}$ : the area of the greenhouse floor ( $\text{m}^2$ ).



# $CO_2$ flow and the photosynthesis of plants



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$$MC_{ExtAir} = \frac{U_{ExtCO_2} \phi_{ExtCO_2}}{A_{Flr}}. \quad (4)$$

- $U_{ExtCO_2}$ : the control valve of the external  $CO_2$  source ranging in  $[0, 1]$ ;
- $\phi_{ExtCO_2}$ : the capacity of the external  $CO_2$  source ( $\text{mg s}^{-1}$ ).



$$\begin{aligned} MC_{PadAir} &= f_{Pad}(CO_{2Out} - CO_{2Air}) \\ &= \frac{U_{Pad}\phi_{Pad}(CO_{2Out} - CO_{2Air})}{A_{Flr}}. \end{aligned} \quad (5)$$

- $f_{Pad}$ : the ventilation flux due to the pad and fan system ( $m s^{-1}$ );
- $U_{Pad}$ : the control valve of the pad and fan system ranging in  $[0, 1]$ ;
- $\phi_{Pad}$ : the capacity of the air flux through the pad ( $m^3 s^{-1}$ ).

$$MC_{AirTop} = f_{ThScr}(CO_{2Air} - CO_{2Top}), \quad (6)$$

$$f_{ThScr} = U_{ThScr} K_{ThScr} |T_{Air} - T_{Top}|^{\frac{2}{3}} + (1 - U_{ThScr}) \left[ \frac{g(1 - U_{ThScr})}{2\rho_{Air}^{Mean}} |\rho_{Air} - \rho_{Top}| \right]^{\frac{1}{2}}.$$

- $f_{ThScr}$ : the air flux through the thermal screen ( $m\ s^{-1}$ );
- $U_{ThScr}$ : the control of the thermal screen ranging in  $[0, 1]$ ;
- $K_{ThScr}$ : the screen flux coefficient determining the permeability of the screen ( $m\ K^{-\frac{2}{3}}\ s^{-1}$ );
- $g$ : the gravitational acceleration ( $m\ s^{-2}$ );
- $\rho_{Air/Top}$ : the density of the greenhouse air below/above the thermal screen ( $kg\ m^{-3}$ );
- $\rho_{Air}^{Mean}$ : the mean density of the greenhouse air ( $kg\ m^{-3}$ );
- $T_{Air/Top}$ : the temperature below/above the thermal screen (K).



# $CO_2$ flow and the photosynthesis of plants

Dynamical Systems

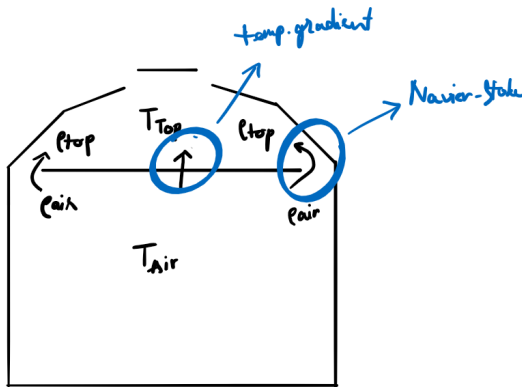
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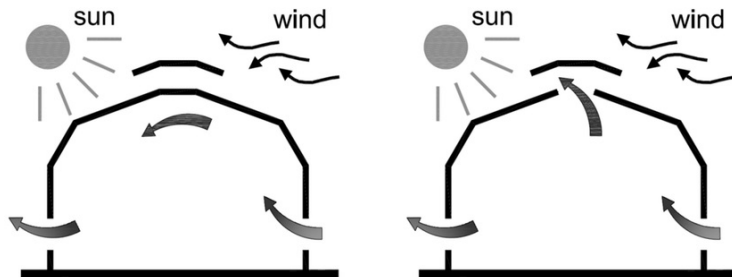
**Figure:** Air flow through the thermal screen.



$$MC_{AirOut} = (f_{VentSide} + f_{VentForced})(CO_{2Air} - CO_{2Out}). \quad (7)$$

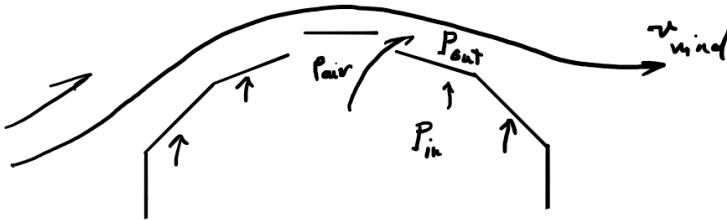
- $f_{VentSide}$ : the rate for the sidewall ventilation system ( $m s^{-1}$ );
- $f_{VentForced}$ : the rate for the forced ventilation system ( $m s^{-1}$ ).

# $CO_2$ flow and the photosynthesis of plants



**Figure:** Without/With Chimney's effect.

# $CO_2$ flow and the photosynthesis of plants



$$\text{Bernoulli: } P_{out} - P_{in} = \frac{1}{2} P_{air} \cdot v_{wind}^2$$

**Figure:** Air flow through the roof opening.



$$f_{VentRoofSide} = \frac{C_d}{A_{Flr}} \left[ \frac{U_{Roof}^2 U_{Side}^2 A_{Roof}^2 A_{Side}^2}{U_{Roof}^2 A_{Roof}^2 + U_{Side}^2 A_{Side}^2} \cdot \frac{2gh_{SideRoof}(T_{Air} - T_{Out})}{T_{Air}^{Mean}} + \left( \frac{U_{Roof} A_{Roof} + U_{Side} A_{Side}}{2} \right)^2 C_w v_{Wind}^2 \right]^{\frac{1}{2}}$$

- $f_{VentRoofSide}$ : the ventilation rate through both the roof and side vents (m s<sup>-1</sup>);
- $C_{d/w}$ : discharge/global wind pressure coefficient depending on the greenhouse shape and the use of an outdoor thermal screen (-);
- $U_{Roof/Side}$ : the control of the roof/side openings ranging in [0,1];
- $A_{Roof/Side}$ : the roof/side opening area (m<sup>2</sup>);
- $h_{SideRoof}$ : the vertical distance between mid-points of side wall and roof ventilation openings (m);
- $T_{Air}^{Mean}$ : the mean temperature between the indoor and outdoor temperatures (K);  $v_{Wind}$ : wind speed (m s<sup>-1</sup>).





## Insect-screen effect:

$$\eta_{InsScr} = \zeta_{InsScr}(2 - \zeta_{InsScr}).$$

- $\eta_{InsScr}$ : reduction factor (-);
- $\zeta_{InsScr}$ : the screen porosity i.e. the area of holes per unit area of the insect screen (-).

## Greenhouse leakage:

$$f_{leakage} = \begin{cases} 0.25 \cdot c_{leakage}, & v_{Wind} < 0.25, \\ v_{Wind} \cdot c_{leakage}, & v_{Wind} \geq 0.25. \end{cases}$$

- $f_{leakage}$ : the leakage rate depending on wind speed ( $m\ s^{-1}$ );
- $c_{leakage}$ : the leakage coefficient depending on the greenhouse type (-).



If  $\eta_{Side} \geq \eta_{Side\_Thr}$ ,

$$f_{VentSide} = \eta_{InsScr} f_{VentRoofSide} (A_{Roof} = 0) + 0.5 f_{leakage}.$$

Otherwise,

$$f_{VentSide} = \eta_{InsScr} [U_{ThScr} f_{VentRoofSide} (A_{Roof} = 0) + (1 - U_{ThScr}) f_{VentRoofSide} \eta_{Side}] + 0.5 f_{leakage}.$$

- $\eta_{Side}$ : the ratio between the side vents area and total ventilation area (-);
- $\eta_{Side\_Thr}$ : the threshold value above which no chimney effect is assumed to occur (-).



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$$f_{VentForced} = \frac{\eta_{InsScr} U_{VentForced} \phi_{VentForced}}{A_{Flr}}.$$

- $U_{VentForced}$ : the control valve of the forced ventilation ranging in  $[0, 1]$ ;
- $\phi_{VentForced}$ : the air flow capacity of the forced ventilation system ( $m^3 s^{-1}$ )



$$MC_{TopOut} = f_{VentRoof}(CO_{2Top} - CO_{2Out}). \quad (8)$$

$$f_{VentRoof} = \frac{C_d U_{Roof} A_{Roof}}{2A_{Flr}} \left[ \frac{gh_{Roof}(T_{Air} - T_{Out})}{2T_{Air}^{Mean}} + C_w v_{Wind}^2 \right]^{\frac{1}{2}}.$$

- $h_{Roof}$ : the vertical dimension of a single ventilation opening (m).



$$MC_{AirCan} = M_{CH_2O} h_{C_{Buf}} (P - R). \quad (9)$$

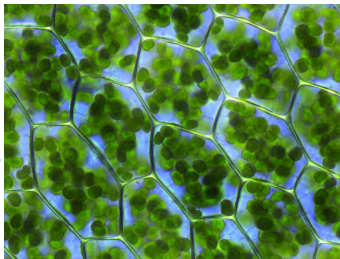
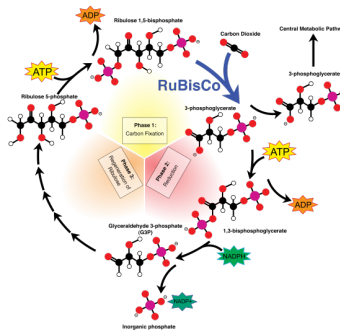
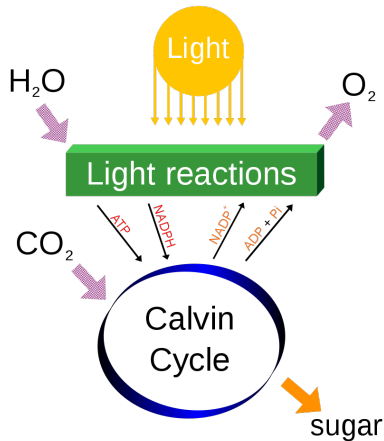
- $M_{CH_2O}$ : the molar mass of  $CH_2O$  ( $\text{mg } \mu\text{mol}^{-1}$ );
- $h_{C_{Buf}}$ : the inhibition of the photosynthesis rate by saturation of the leaves with carbohydrates (-), where

$$h_{C_{Buf}} = \begin{cases} 0, & C_{Buf} > C_{Buf}^{Max}, \\ 1, & C_{Buf} \leq C_{Buf}^{Max}; \end{cases}$$

- $C_{Buf}/C_{Buf}^{Max}$ : the capacity/maximum capacity of carbohydrates storage in the canopy buffer ( $\text{mg } \{CH_2O\} \text{ m}^{-2}$ );
- $P/R$ : the photosynthesis/photorespiration rate of the canopy during the photosynthesis process ( $\mu\text{mol } \{CO_2\} \text{ m}^{-2} \text{ s}^{-1}$ ).

# $CO_2$ flow and the photosynthesis of plants

One leaf:

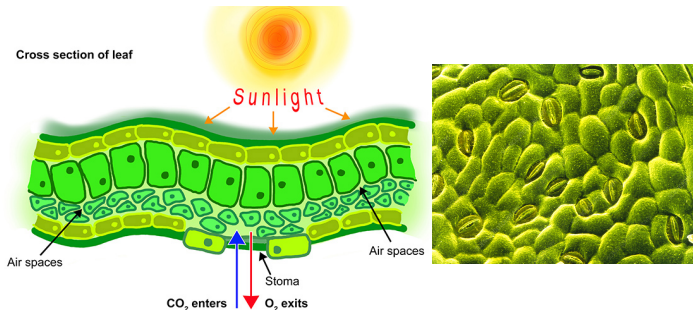


**Figure:** Photosynthesis - Calvin Cycle - Chloroplast.



# $CO_2$ flow and the photosynthesis of plants

## $CO_2$ diffusion:



**Figure:**  $CO_2$  diffuses into leaf cells through stomata.



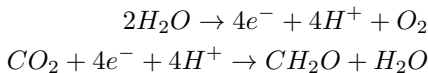
## $CO_2$ flow and the photosynthesis of plants

Fick's law:

$$P = \frac{CO_{2\text{ Air}} - CO_{2\text{ Stom}}}{Res}.$$

- $CO_{2\text{ Stom}}$ : the amount of  $CO_2$  in the chloroplasts ( $\mu\text{mol m}^{-3}$ );
- $Res$ : the resistance to  $CO_2$  diffusion ( $\text{s m}^{-1}$ ).

Carbon fixation:



Michaelis–Menten kinetic model

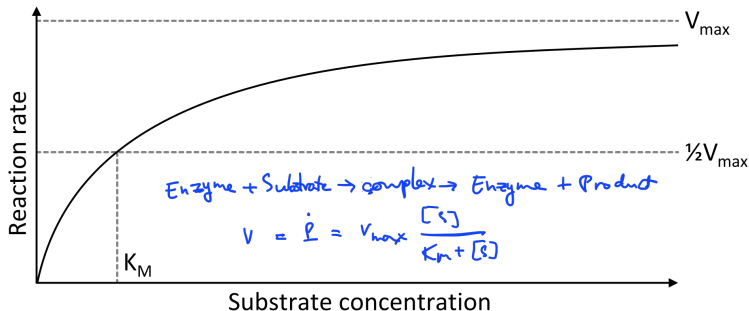
$$P = \frac{P_{Max}}{1 + \frac{CO_{20.5}}{CO_{2\text{ Stom}}}}.$$

- $P_{Max}$ : the photosynthesis rate at saturating  $CO_{2\text{ Stom}}$  ( $\mu\text{mol } \{CO_2\} \text{ m}^{-2} \text{ s}^{-1}$ );
- $CO_{20.5}$ : the amount of  $CO_{2\text{ Stom}}$  such that  $P = P_{Max}/2$  ( $\mu\text{mol m}^{-3}$ ).





## $CO_2$ flow and the photosynthesis of plants



**Figure:** Michaelis–Menten kinetic model.

Solve for  $CO_{2\text{Stom}}$ ,  $P$  satisfies

$$ResP^2 - (CO_{2\text{Air}} + CO_{20.5} + ResP_{Max})P + CO_{2\text{Air}}P_{Max} = 0.$$

Only  $P$  that  $P \rightarrow P_{Max}$  as  $CO_{2,Air} \rightarrow +\infty$ .



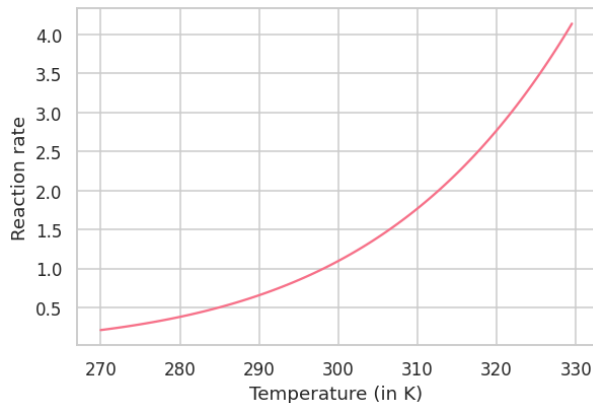


$P_{Max}$  and the Arrhenius model:

$$k(T) = k(T_0)e^{-\frac{H_a}{R}\left(\frac{1}{T} - \frac{1}{T_0}\right)}.$$

- $T$ : the temperature of the leaf (K);
- $T_0$ : a specific temperature of the leaf that we know the reaction rate (K);
- $K(T)$ : the reaction rate (-);
- $H_a$ : the activation energy ( $J \text{ mol}^{-1}$ );
- $R$ : the ideal gas constant ( $J \text{ mol}^{-1} \text{ K}^{-1}$ ).

## $CO_2$ flow and the photosynthesis of plants



**Figure:** Arrhenius model with  $T_0 = 298.15$ ,  $k(T_0) = 1$ ,  $H_a = 37000$ .





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## Enzyme activity:

$$f(T) = \frac{1 + e^{-\frac{H_d}{R} \left( \frac{1}{T_0} - \frac{1}{\frac{H_d}{S}} \right)}}{1 + e^{-\frac{H_d}{R} \left( \frac{1}{T} - \frac{1}{\frac{H_d}{S}} \right)}}.$$

- $f(T)$ : the enzyme activity rate (-);
- $H_d$ : the deactivation energy ( $J \text{ mol}^{-1}$ );
- $S$ : the entropy term ( $J \text{ mol}^{-1} \text{ K}^{-1}$ ).

# $CO_2$ flow and the photosynthesis of plants

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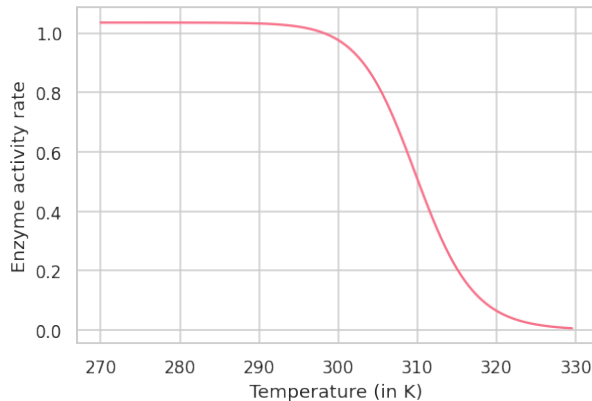
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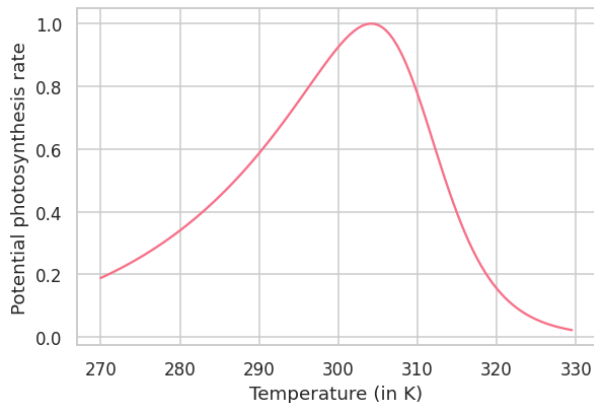
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**Figure:** Enzyme activity model with  $H_d = 220000$  and  $S = 710$ .

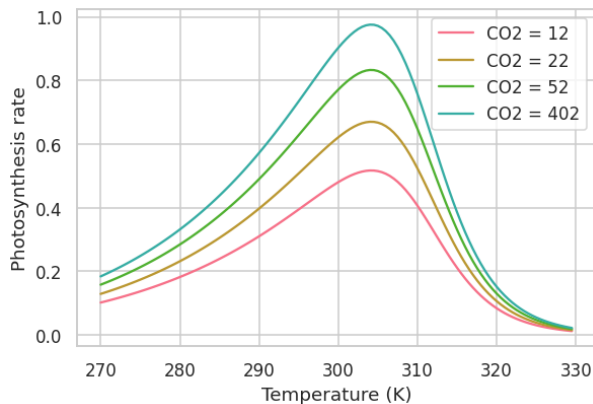
## $CO_2$ flow and the photosynthesis of plants



**Figure:** (Potential photosynthesis rate  $P_{Max}(T) = k(T)f(T)$  (normalized)).



## $CO_2$ flow and the photosynthesis of plants

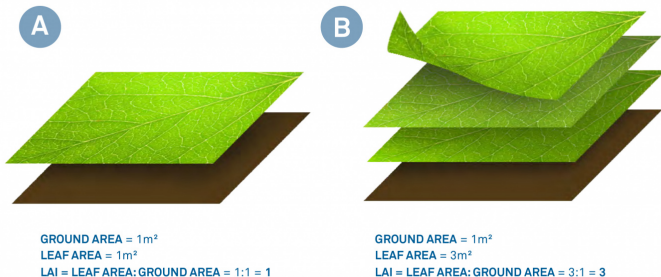


**Figure:** Photosynthesis rate with different value of  $CO_2$  in the greenhouse air and resistance  $Res = 2.5$  (normalized).



# $CO_2$ flow and the photosynthesis of plants

## Canopy:



**Figure:** Leaf area index.







$P_{Max}$  and the Arrhenius model:

$$k(T) = LAI \cdot k(T_0) \cdot e^{-\frac{H_a}{R} \left( \frac{1}{T} - \frac{1}{T_0} \right)}.$$

- $T$ : the temperature of the canopy (K);
- $T_0$ : a specific temperature of the canopy that we know the reaction rate (K);
- $k(T)$ : the reaction rate of the canopy at  $T$  (-);
- $k(T_0)$ : the reaction rate in the stroma of a leaf at  $T_0$  (-).



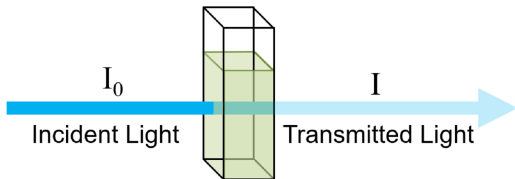
## Michaelis–Menten model:

$$P_{Max}(L, T) = \frac{P_{MLT} \cdot P_{Max}(T)}{1 + \frac{L_{0.5}}{L}}.$$

- $L$ : the photosynthetically active radiation absorbed by the canopy ( $\mu\text{mol \{photons\} m}^{-2} \text{ s}^{-1}$ );
- $L_{0.5}$ : the photosynthetically active radiation at which  $P_{Max}(L, T) = P_{MLT} \cdot P_{Max}(T)/2$  ( $\mu\text{mol \{photons\} m}^{-2} \text{ s}^{-1}$ );
- $P_{MLT}$ : the value of  $P_{Max}$  at saturation  $L$  and optimum  $T$  ( $\mu\text{mol \{CO}_2\} \text{ m}^{-2} \text{ s}^{-1}$ ).

# CO<sub>2</sub> flow and the photosynthesis of plants

## Beer's law:



$$I = \frac{I_0 \cdot K \cdot e^{-K \cdot LAI}}{1 - m}.$$

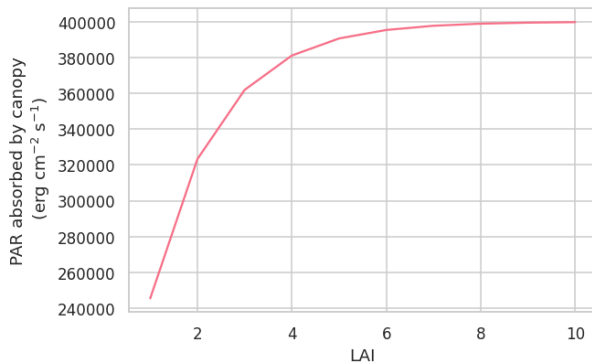
- $K$ : the extinction coefficient in between 0.7-1.0 if the leaves are not inclined. Otherwise 0.3-0.5;
- $I$ : the  $L$  measured at the ground surface ( $\mu\text{mol}\{\text{photons}\} \text{m}^{-2} \text{s}^{-1}$ );
- $I_0$ : the  $L$  measured above the canopy ( $\mu\text{mol}\{\text{photons}\} \text{m}^{-2} \text{s}^{-1}$ );
- $m$ : the transmittance of the leaves, which set as default 0.1.



## $CO_2$ flow and the photosynthesis of plants

Absorbed  $L$ :

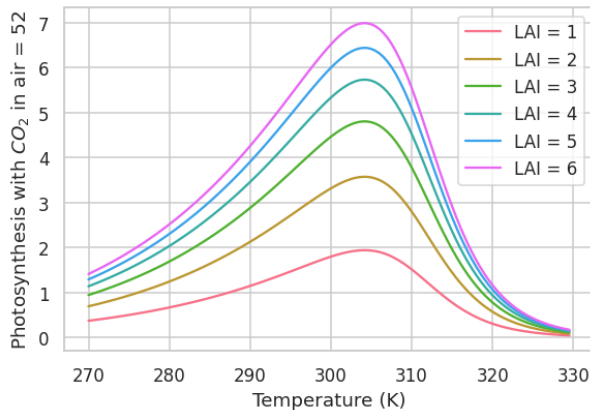
$$L = L_0 \left( 1 - \frac{K \cdot e^{-K \cdot LAI}}{1 - m} \right).$$



**Figure:** Dependence of PAR on LAI.



## $CO_2$ flow and the photosynthesis of plants



**Figure:** Photosynthesis with fixed  $CO_{2\text{ Air}}$  and different LAI.



First-order differential equation:

$$\begin{cases} \dot{x} = f(t, x), \\ x(t_0) = x_0. \end{cases} \quad (10)$$

Taylor expansion:

$$\begin{aligned} x(t+h) &= x(t) + \dot{x}(t)h + O(h^2) \\ &= x(t) + f(t, x(t))h + O(h^2). \end{aligned} \quad (11)$$

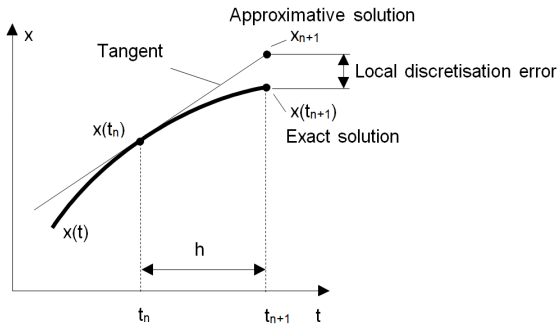
## Forward Euler method

Forward Euler formula:

$$x_{n+1} = x_n + f(t_n, x_n)h, \quad (12)$$

where

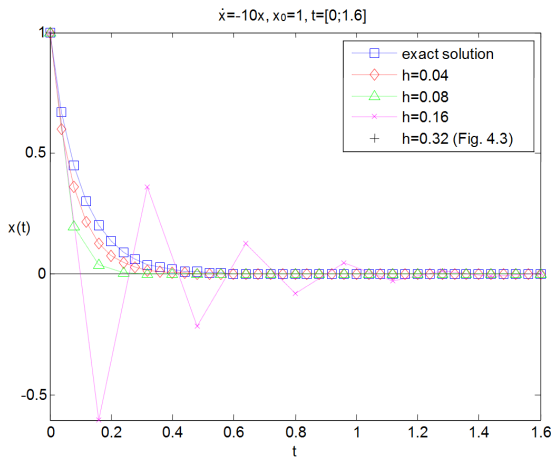
$$x_n := x(t_n) \quad n = 0, 1, 2, \dots$$



**Figure:** Forward Euler numerical scheme.



# Forward Euler method

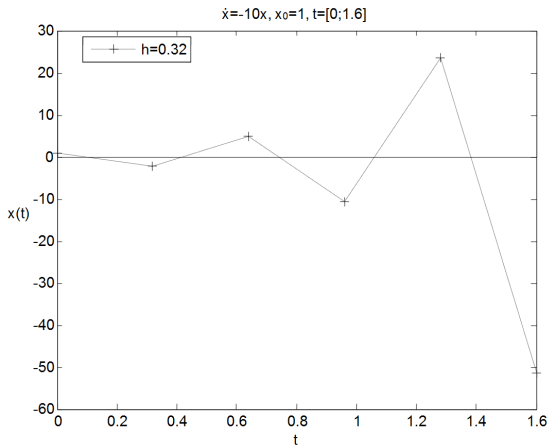


**Figure:** Example  $\dot{x} = -10x, x_0 = 1$  with different  $h < 0.32$ .





# Forward Euler method



**Figure:** Example  $\dot{x} = -10x, x_0 = 1$  with  $h = 0.32$ .





Test equation:

$$\begin{cases} \dot{x} = \alpha x, & \alpha \in \mathbb{R}, \\ x(t_0) = x_0. \end{cases} \quad (13)$$

Applying the Forward Euler method

$$x_{n+1} = (1+\alpha h)x_n = (1+\alpha h)^2 x_{n-1} = \cdots = (1+\alpha h)^{n+1} x_0. \quad (14)$$

Stability condition:

$$|1 + \alpha h| < 1. \quad (15)$$



Stability function and stability region:

$$x_{n+1} = \Phi(\alpha h)x_n. \quad (16)$$

Then  $\Phi = \Phi(z)$  for  $z \in \mathbb{C}$  is called stability function and the region

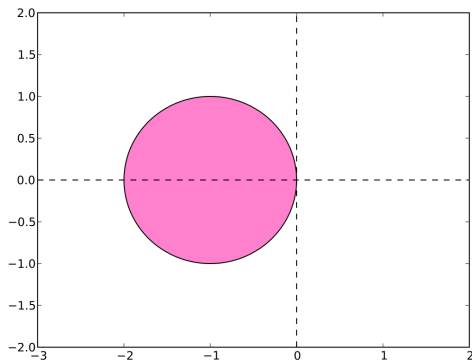
$$\{z \in \mathbb{C} : |\Phi(z)| < 1\} \quad (17)$$

is called the stability region for the numerical scheme.

A-stable numerical scheme: A numerical scheme is  $A$ -stable if its stability region contains the left half complex plane.

L-stable numerical scheme: A numerical scheme is  $L$ -stable if it is  $A$ -stable and  $\Phi(z) \rightarrow 0$  as  $z \rightarrow \infty$ .

# Forward Euler method



**Figure:** Stability region of Forward Euler  $\{z \in \mathbb{C} : |1 + z| < 1\}$ .



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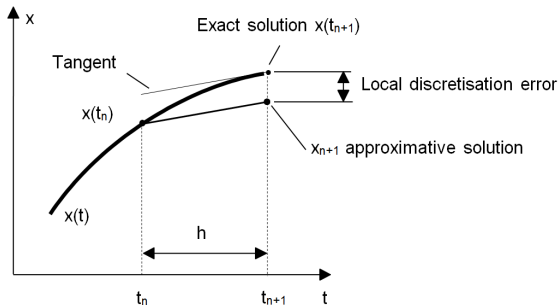
## Backward Euler method

Backward Euler formula:

$$x_{n+1} = x_n + f(t_n, x_{n+1})h, \quad (18)$$

where

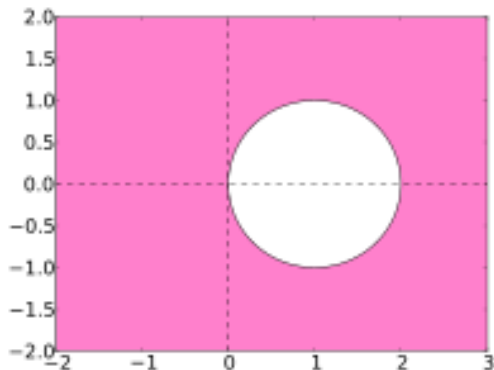
$$x_n := x(t_n) \quad n = 0, 1, 2, \dots$$



**Figure:** Backward Euler numerical scheme.



# Backward Euler method



**Figure:** Stability region of Backward Euler  $\{z \in \mathbb{C} : \frac{1}{|1-z|} < 1\}$ .



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$$f(x) = 0, \quad (19)$$

where  $f = (f_1, \dots, f_N)$  is differentiable and  $x = (x_1, \dots, x_N)$ .

Newton iteration formula:

$$x_{n+1} = x_n - J(x_n)^{-1} f(x_n), \quad (20)$$

where

$$J(x) := \begin{pmatrix} \frac{\partial f_1}{\partial x_1} & \cdots & \frac{\partial f_1}{\partial x_N} \\ \vdots & \ddots & \vdots \\ \frac{\partial f_N}{\partial x_1} & \cdots & \frac{\partial f_N}{\partial x_N} \end{pmatrix} \quad (21)$$



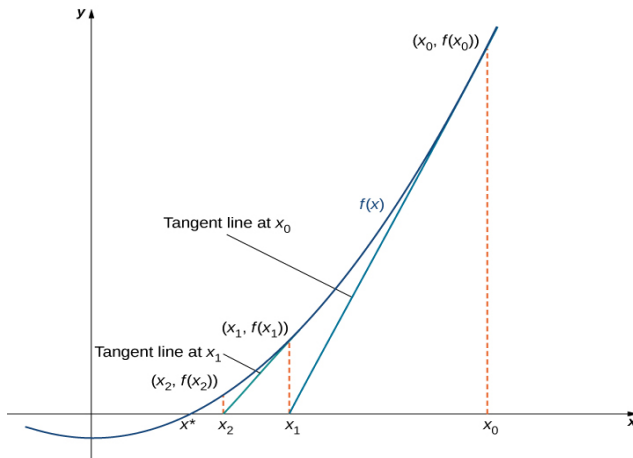
# Newton–Raphson scheme



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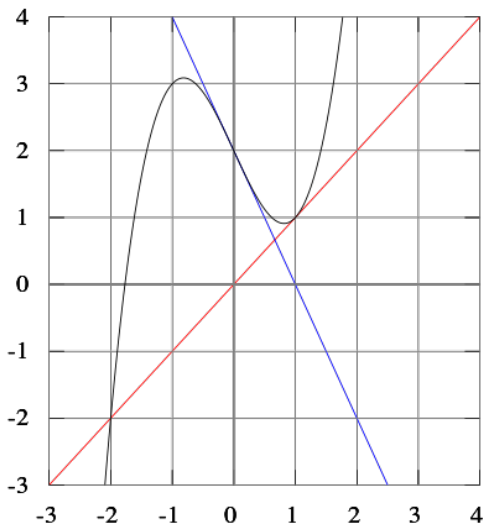
## Numerical methods



**Figure:** Newton iteration scheme.



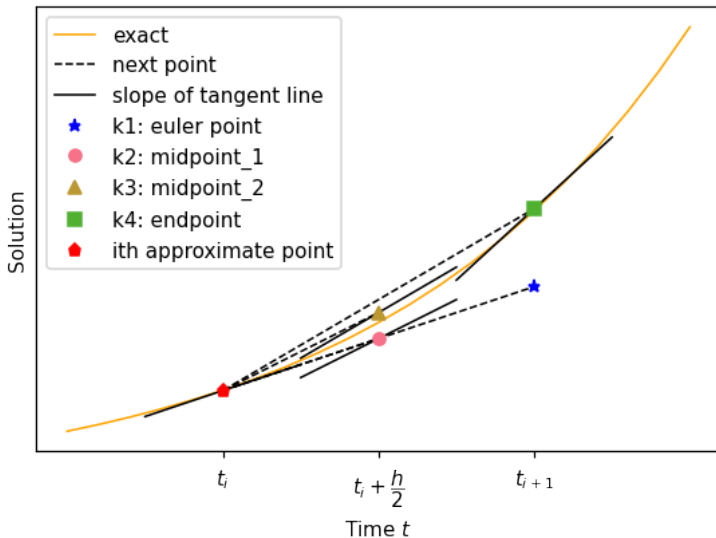
## Newton–Raphson scheme



**Figure:** Intersection of two tangent line at 0 and 1 of  $f(x) = x^3 - 2x + 2$ .



# Explicit Midpoint Runge–Kutta method



**Figure:** Improvement of Forward Euler.



# Explicit Midpoint Runge–Kutta method



## Explicit Midpoint method:

Step 1. Compute the slope at  $x_n$

$$k_1 = f(t_n, x_n). \quad (22)$$

Step 2. Compute the slope at the midpoint

$$k_2 = f\left(t_n + \frac{1}{2}h, x_n + \frac{1}{2}hk_1\right). \quad (23)$$

Step 3. Compute  $x_{n+1}$

$$x_{n+1} = x_n + hk_2. \quad (24)$$

# Explicit Midpoint Runge–Kutta method



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Proof for multi-variate scalar case of  $f$ :

$$k_1 = f(t_n, x_n). \quad (25)$$

$$k_2 = f(t_n + \alpha h, x_n + \beta h k_1). \quad (26)$$

$$x_{n+1} = x_n + a h k_1 + b h k_2. \quad (27)$$



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Taylor expansion:

$$\begin{aligned} f(t_n + \alpha h, x_n + \beta h k_1) &= f(t_n, x_n) + \alpha h \frac{\partial f}{\partial t}(t_n, x_n) \\ &\quad + \beta h k_1 \frac{\partial f}{\partial x}(t_n, x_n) + O(h^2) \end{aligned} \quad (28)$$

Substituting in (25)-(27)

$$\begin{aligned} x_{n+1} &= x_n + (a + b)h f(t_n, x_n) \\ &\quad + bh^2 \left( \alpha \frac{\partial f}{\partial t} + \beta f \frac{\partial f}{\partial x} \right) (t_n, x_n) + O(h^3). \end{aligned} \quad (29)$$

# Explicit Midpoint Runge–Kutta method



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Taylor expansion:

$$\begin{aligned}x(t_{n+1}) &= x(t_n) + h\dot{x}(t_n) + \frac{h^2}{2}\ddot{x}(t_n) + O(h^3) \\&= x(t_n) + hf(t_n, x_n) \\&\quad + \frac{h^2}{2} \left( \frac{\partial f}{\partial t} + f \frac{\partial f}{\partial x} \right) (t_n, x_n) + O(h^3) \quad (30)\end{aligned}$$

From (29)

$$a + b = 1, \quad \alpha b = \frac{1}{2}, \quad \beta b = \frac{1}{2}. \quad (31)$$

Choose  $a = 0, b = 1, \alpha = \beta = \frac{1}{2}$ .

## Explicit order-4 Runge–Kutta method

### Explicit order-4 Runge–Kutta method:

Step 1. Compute the slope at  $x_n$

$$k_1 = f(t_n, x_n). \quad (32)$$

Step 2. Compute the slope at the midpoint from  $k_1$

$$k_2 = f\left(t_n + \frac{1}{2}h, x_n + \frac{1}{2}hk_1\right). \quad (33)$$

Step 3. Compute the slope at the midpoint from  $k_2$

$$k_3 = f\left(t_n + \frac{1}{2}h, x_n + \frac{1}{2}hk_2\right). \quad (34)$$

Step 4. Compute the slope at the endpoint from  $k_3$

$$k_4 = f(t_n + h, x_n + hk_3). \quad (35)$$

Step 5. Compute  $x_{n+1}$

$$x_{n+1} = x_n + \frac{h}{6}(k_1 + 2k_2 + 2k_3 + k_4). \quad (36)$$



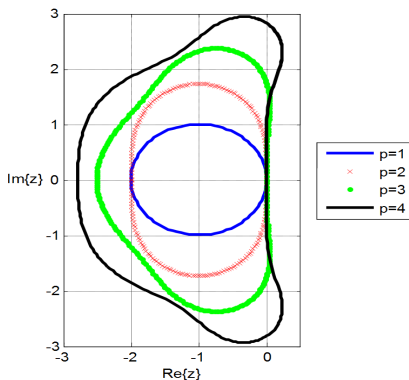
# Explicit Runge–Kutta method



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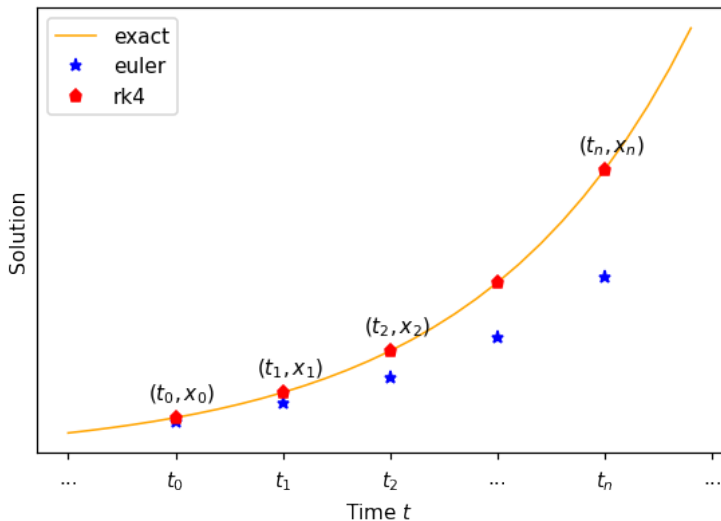


**Figure:** Stability region of Runge–Kutta of order  $1 \leq p \leq 4$  where

$$\Phi(z) = \sum_{i=0}^p \frac{z^i}{i!}.$$



# Explicit Runge–Kutta method



**Figure:** Forward Euler and Runge–Kutta of order 4.

