

Buoyancy Flow with Darcy's Law—The Elder Problem

Density variations can initiate flow even in a still fluid. In earth systems, density variations can arise from naturally occurring salts, subsurface temperature changes, or migrating pollution. This buoyant or density-driven flow factors into fluid movement in salt-lake systems, saline-disposal basins, dense contaminant and leachate plumes, and geothermal reservoirs, to name just a few.

This example duplicates a benchmark problem for time-dependent buoyant flow in a porous medium. Known as the Elder problem (Ref. 1), it follows a laboratory experiment to study thermal convection. When Voss and Souza (Ref. 2) recast the Elder problem for salt concentrations, it became a benchmark that many researchers have used to test a number of variable-density flow codes including SUTRA (Ref. 3) and SEAWAT (Ref. 4).

This application examines the Elder problem for concentrations through a 2-way coupling of two physics interfaces: Darcy's Law and Transport of Diluted Species in Porous Media.

Model Definition

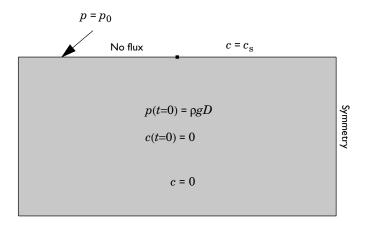


Figure 1: Geometry for modeling the Elder problem with initial conditions and boundary conditions indicated. In this cross section of a water-saturated porous medium, high salt concentrations exist in the top-right region.

In this example (Figure 1) a vertical cross section of a water-saturated porous medium extends 300 m in the x direction and 150 m in the y direction. The material properties are homogeneous and isotropic. A vertical line at x = 300 m represents a symmetry boundary with a mirror image of the cross section extending beyond it. There is no flow across the geometry edges. High salt concentrations exist at the upper boundary (along y = 150 m) from x = 150 m to 300 m. Salt concentration is zero along the lower boundary. The water is initially stationary (with a hydrostatic pressure distribution) and pristine (zero salt concentration). When the density increases near the high-concentration boundary, flow develops. The period of interest is 20 years, According to Ref. 6 and Ref. 7, the length chosen by Elder is close to a critical value that separates downwelling and upwelling plume structures. As a consequence, the problem is particularly sensitive to perturbations.

FLUID FLOW

You can describe the fluid flow in this problem using Darcy's law:

$$\begin{split} &\frac{\partial \varepsilon \rho}{\partial t} + \nabla \cdot \rho \mathbf{u} = 0 \\ &\mathbf{u} = -\frac{\kappa}{\mu} (\nabla p + \rho g \nabla D) \end{split}$$

Here, ρ is the water density (kg/m³), t is the time (s), ε is the porosity, and **u** is the vector of directional seepage rates, also known as the Darcy velocity. The Darcy velocity **u** depends on the permeability κ (m²), the fluid's dynamic viscosity μ (Pa·s), the fluid's pressure p (Pa), and the acceleration of gravity g (m/s²). The gradient of the elevation D(m) indicates the direction of the vertical coordinate, y.

In Elder's problem, the fluid density depends linearly on the salt concentration, $c \pmod{/}$ m³) according to

$$\rho = \rho_0 + \beta c = \rho_0 + \frac{\rho_s - \rho_0}{c_s - c_0}c$$

Here, c_0 and c_s are the normalized salt concentrations of pristine and salty water.

The symmetry or zero flow on all boundaries fix only the change in pressure. For a unique solution, you must also specify a reference pressure. In this example, the pressure at the point (0,0) is fixed. With the Darcy's Law interface, you express all these conditions as

$$\mathbf{n} \cdot \rho \mathbf{u} = 0$$
 $\partial \Omega$ Sides $p = p_0$ $\partial^2 \Omega$ Point $p(x, y, 0) = \rho_0 g D$ $t = 0$ Initial value

where **n** is the unit vector normal to the boundary, and p_0 is the reference pressure.

TRANSPORT OF DILUTED SPECIES IN POROUS MEDIA

The governing equation for this problem is the conservative form of the Transport of Diluted Species in Porous Media interface

$$\frac{\partial \theta_{s} c}{\partial t} + \mathbf{u} \cdot \nabla c - \nabla \cdot \theta_{s} \tau D_{L} \nabla c = 0$$

where D_L is the fluid's diffusion coefficient (m²/d); θ_s is the fluid's volume fraction (porosity); c is the salt concentration (mol/m³), and \mathbf{u} is the Darcy velocity (m/s).

In Elder's problem, the contaminant spreads only by advection and molecular diffusion, and the salt concentration is normalized to unit values.

The only contaminant source in the model domain is the salt concentration along the right half of the upper boundary. The vertical edge at x = 300 m is a symmetry boundary. The remaining boundaries have zero flux. The initial concentration is zero. The following equations represent these conditions:

$$\mathbf{n} \cdot [c\mathbf{u} - \theta_s \tau D_L \nabla c] = 0$$
 $\partial \Omega$ Sides $c = c_s$ $\partial \Omega$ Salt $c(x, y, 0) = 0$ $t = 0$ Initial value

where **n** is the unit vector normal to the boundary.

Model Data

The example works with the following data:

PARAMETER	NAME	VALUE	
ρ_0	Fresh-water density	1000 kg/m ³	
$ ho_{ m s}$	Salt-water density	1200 kg/m ³	
κ	Permeability	0.5 Darcy	
μ	Dynamic viscosity	0.001 Pa·s	

PARAMETER	NAME	VALUE
g	Gravity	9.81 m/s ²
ε	Porosity	0.1
$ au_L D_L$	Molecular diffusion rate	3.56·10 ⁻⁶ m ² /s
$c_{ m s}$	Salt-water concentration	I mol/m ³
c_0	Fresh-water concentration	0 mol/m ³
β	Increase of water density due to concentration changes	200 kg/mol

Note that the original set of parameters for the Elder problem gives a global Peclet number equal to

$$Pe = \frac{(\rho_s - \rho_0)g\kappa L}{\mu \varepsilon D_L} \sim 408$$

Here, the difference in water density is $\rho_s - \rho_0 = \beta(c_s - c_0) = 200 \text{ kg/m}^3$, and the length scale L is 150 m. This high Peclet number poses extra difficulties to numerical schemes; see for instance (Ref. 5 to Ref. 7).

Results and Discussion

The following results come from the COMSOL Multiphysics solution to a benchmark buoyancy problem that is often used for both temperatures (Ref. 1) and concentrations (Ref. 2).

Figure 2 gives snapshots of concentrations at six times during the 20-year simulation period. Initially the water is pristine. By the end of the first year, concentrations spread by diffusion, creating a density gradient. The buoyancy flow begins at the edge of the salt contact, where there is a sharp contrast in fluid density. By the end of year three, the fingering of high concentrations into the reservoir is mature. By year 10, the salt concentrations have spread over roughly 60% of the model domain. The COMSOL Multiphysics solution in Figure 2 is in excellent agreement with that from Elder (Ref. 1).

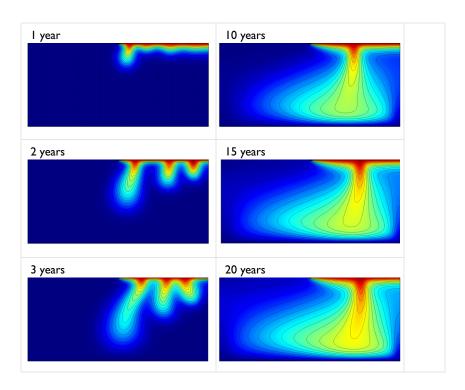
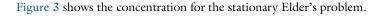


Figure 2: Snapshots of concentrations from the COMSOL Multiphysics solution to the buoyancy-flow benchmark developed by Voss and Souza (Ref. 2) for the Elder problem.



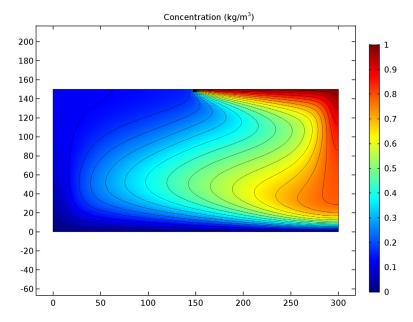


Figure 3: Concentration distribution from the COMSOL Multiphysics solution to the buoyancy-flow benchmark for the stationary Elder problem.

Of interest in the Elder problem is the development of convection cells. The COMSOL Multiphysics plots in Figure 4 reveal the convection cells with the help of velocity streamlines, which the figure shows simultaneously with concentrations for years 3, 10, 15, and 20. At early times, small convection cells develop between the individual fingers of the plume. At late times, a single convection cell covers the model domain.

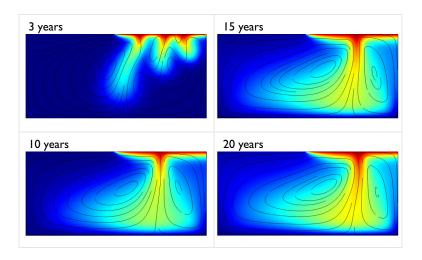


Figure 4: Salt concentrations (surface plot) and velocities (streamlines) from the COMSOL Multiphysics solution to a buoyancy benchmark problem (Ref. 2).

This example shows COMSOL Multiphysics applied to a well-known benchmark problem applicable to flow driven by density variations related to either temperature or concentration. The COMSOL Multiphysics results, here for concentration, closely match the benchmark solution (Ref. 2). This buoyant flow is straightforward to set up directly on top of a standard fluid flow and solute-transport model.

References

- 1. J.W. Elder, "Transient Convection in a Porous Medium," J. Fluid Mechanics, vol. 27, no. 3, 609-623, 1967.
- 2. C.I. Voss and W.R. Souza, "Variable Density Flow and Solute Transport Simulation of Regional Aquifers Containing a Narrow Freshwater-saltwater Transition Zone," Water Resources Research, vol. 23, no. 10, pp. 1851-1866, 1987.
- 3. C.I. Voss, "A Finite-element Simulation Model for Saturated-unsaturated, Fluid-density-dependent Ground-water Flow with Energy Transport or Chemically-reactive Single-species Solute Transport," U.S. Geological Survey Water-Resources Investigation Report, 84-4369, 1984.

- 4. W. Guo and C.D. Langevin, User's Guide to SEAWAT: A Computer Program for Simulation of Three-Dimensional Variable-Density Ground-Water Flow, U.S. Geological Survey Techniques of Water-Resources Investigations 6-A7, 2002.
- 5. P. Frolkovic and H. De Schepper, "Numerical modelling of convection dominated transport coupled with density driven flow in porous media," Advances in Water Resources, vol. 24, no. 1, pp. 63-72, 2000.
- 6. G.F. Carey, W. Barth, J. A. Woods, B. S. Kirk, M. L. Anderson, S. Chow, and W. Bangerth, "Modelling error and constitutive relations in simulation of flow and transport, " Int. J. Numer. Meth. Fluids, vol. 46, pp. 1211-1236, 2004.
- 7. J.A. Woods and G.F. Carey, "Upwelling and downwelling behavior in the Elder-Voss-Souza benchmark," Water Resour. Res., vol. 43, W12403, 2007.

Application Library path: Subsurface Flow Module/Solute Transport/ buoyancy darcy elder

Modeling Instructions

From the File menu, choose New.

NEW

In the New window, click Model Wizard.

MODEL WIZARD

- I In the Model Wizard window, click 2D.
- 2 In the Select Physics tree, select Fluid Flow>Porous Media and Subsurface Flow>Darcy's Law (dl).
- 3 Click Add.
- 4 In the Select Physics tree, select Chemical Species Transport>Transport of Diluted Species in Porous Media (tds).
- 5 Click Add.
- 6 Click Study.
- 7 In the Select Study tree, select Preset Studies for Selected Physics Interfaces>Time Dependent.
- 8 Click Done

GLOBAL DEFINITIONS

Parameters

- I On the Home toolbar, click Parameters.
- 2 In the Settings window for Parameters, locate the Parameters section.
- **3** In the table, enter the following settings:

Name	Expression	Value	Description	
L	150[m]	150 m	Basin depth	
rho0	1000[kg/m^3]	1000 kg/m³	Pristine water density	
rho_s	1200[kg/m^3]	1200 kg/m³	Brine density	
c0	O[mol/m^3]	0 mol/m³	Zero salt concentration	
c_s	1[mol/m^3]	I mol/m³	Normalized salt concentration	
beta	(rho_s-rho0)/ (c_s-c0)	200 kg/mol	Increase in density due to salt concentration	
р0	O[atm]	0 Pa	Reference pressure	
mu	1e-3[Pa*s]	0.001 Pa·s	Dynamic viscosity	
kappa	500[mD]	4.9346E-13 m ²	Permeability	
epsilon	0.1	0.1	Porosity	
D_L	3.56e-6[m^2/s]	3.56E-6 m ² /s	Molecular diffusion	
Pe	<pre>beta*(c_s-c0)* g_const*kappa*L/ (mu*epsilon*D_L)</pre>	407.8	Peclet number	

GEOMETRY I

Rectangle I (rI)

- I On the Geometry toolbar, click Primitives and choose Rectangle.
- 2 In the Settings window for Rectangle, locate the Size and Shape section.
- 3 In the Width text field, type 2*L.
- 4 In the Height text field, type L.

Point I (pt I)

- I On the Geometry toolbar, click Primitives and choose Point.
- 2 In the Settings window for Point, locate the Point section.

- 3 In the x text field, type L.
- 4 In the y text field, type L.
- 5 Click Build All Objects.

DEFINITIONS

Add a variable for the buoyancy force due to concentration gradients.

Variables 1

- I On the Home toolbar, click Variables and choose Local Variables.
- 2 In the Settings window for Variables, locate the Variables section.
- **3** In the table, enter the following settings:

Name	Expression	Unit	Description
rho	rho0+beta*c*(c>0)	kg/m³	Water density

DARCY'S LAW (DL)

Gravity I

- I On the Physics toolbar, click Domains and choose Gravity.
- 2 In the Settings window for Gravity, locate the Domain Selection section.
- 3 From the Selection list, choose All domains.
- 4 Locate the Gravity section. From the Specify list, choose Elevation.
- 5 In the D text field, type y-L.

Fluid and Matrix Properties 1

- I In the Model Builder window, under Component I (compl)>Darcy's Law (dl) click Fluid and Matrix Properties I.
- 2 In the Settings window for Fluid and Matrix Properties, locate the Fluid Properties section.
- **3** From the ρ list, choose **User defined**. In the associated text field, type rho.
- **4** Locate the Matrix Properties section. From the κ list, choose User defined. In the associated text field, type kappa.
- **5** Locate the Fluid Properties section. From the μ list, choose User defined. In the associated text field, type mu.
- 6 Locate the Matrix Properties section. From the $\varepsilon_{\rm p}$ list, choose User defined. In the associated text field, type epsilon.

Initial Values 1

- I In the Model Builder window, under Component I (compl)>Darcy's Law (dl) click Initial Values 1.
- 2 In the Settings window for Initial Values, locate the Initial Values section.
- 3 In the p text field, type p0+rho*g const*dl.D. This defines the hydrostatic pressure distribution as reasonable initial condition.

Symmetry I

- I On the Physics toolbar, click Boundaries and choose Symmetry.
- **2** Select Boundary 5 only.
- 3 In the Model Builder window's toolbar, click the Show button and select Advanced Physics **Options** in the menu.

Pointwise Constraint I

- I On the Physics toolbar, click Points and choose Pointwise Constraint.
- 2 In the Settings window for Pointwise Constraint, locate the Pointwise Constraint section.
- 3 In the Constraint expression text field, type p0-p.
- 4 Select Point 2 only.

Since the pressure is not set explicitly by a boundary condition, you need to fix it at least at one point to get a unique solution for Darcy's Law.

TRANSPORT OF DILUTED SPECIES IN POROUS MEDIA (TDS)

Porous Media Transport Properties 1

- I In the Model Builder window, expand the Component I (compl)>Transport of Diluted Species in Porous Media (tds) node, then click Porous Media Transport Properties 1.
- 2 In the Settings window for Porous Media Transport Properties, locate the Matrix **Properties** section.
- **3** From the ε_p list, choose **User defined**. In the associated text field, type epsilon.
- **4** Locate the **Diffusion** section. In the $D_{F,c}$ text field, type D_L.
- 5 From the Effective diffusivity model list, choose Tortuosity model.
- 6 In the $\tau_{F,\,c}$ text field, type 1.
- 7 Locate the Model Inputs section. From the u list, choose Darcy's velocity field (dl).

Initial Values 1

I In the Model Builder window, under Component I (compl)>Transport of Diluted Species in Porous Media (tds) click Initial Values I.

- 2 In the Settings window for Initial Values, locate the Initial Values section.
- **3** In the c text field, type c0.
- 4 In the Model Builder window, click Transport of Diluted Species in Porous Media (tds).

Symmetry I

- I On the Physics toolbar, click Boundaries and choose Symmetry.
- **2** Select Boundary 5 only.

Concentration I

- I On the Physics toolbar, click Boundaries and choose Concentration.
- **2** Select Boundary 2 only.
- 3 In the Settings window for Concentration, locate the Concentration section.
- 4 Select the **Species c** check box.
- **5** In the $c_{0,c}$ text field, type c0.

Concentration 2

- I On the Physics toolbar, click Boundaries and choose Concentration.
- 2 Select Boundary 4 only.
- **3** In the **Settings** window for Concentration, locate the **Concentration** section.
- **4** Select the **Species c** check box.
- **5** In the $c_{0,c}$ text field, type c_s.

MESH I

In the Model Builder window, under Component I (compl) right-click Mesh I and choose Mapped.

Size

- I In the Settings window for Size, locate the Element Size section.
- 2 From the Predefined list, choose Extremely fine.
- 3 Click Build All.

STUDY I

Step 1: Time Dependent

- I In the Settings window for Time Dependent, locate the Study Settings section.
- 2 From the Time unit list, choose a.
- 3 In the Times text field, type range (0,1,20).

4 On the Home toolbar, click Compute.

RESULTS

Pressure (dl)

I Click the **Zoom Extents** button on the **Graphics** toolbar.

The first default plot group shows the pressure distribution due to gravity.

Concentration (tds)

The second default plot group shows the concentration after 20 years. To reproduce the series of plots in Figure 2, add a Contour node and plot for different times.

Contour I

- I In the Model Builder window, under Results right-click Concentration (tds) and choose
- 2 In the Settings window for Contour, click Replace Expression in the upper-right corner of the Expression section. From the menu, choose Model>Component I>Transport of Diluted Species in Porous Media>c - Concentration.
- 3 Locate the Coloring and Style section. Clear the Color legend check box.
- 4 From the Coloring list, choose Uniform.
- 5 From the Color list, choose Black.

Concentration (tds)

- I In the Model Builder window, under Results click Concentration (tds).
- 2 In the Settings window for 2D Plot Group, click to expand the Title section.
- 3 From the Title type list, choose Manual.
- 4 In the **Title** text area, type Concentration (kg/m³).
- 5 Click to collapse the Title section. On the Concentration (tds) toolbar, click Plot.
- 6 Locate the Data section. From the Time (a) list, choose 1.
- 7 On the Concentration (tds) toolbar, click Plot.

Compare the result with the upper-left plot in Figure 2.

Repeat the previous two steps for the Time values 2 years, 3 years, 10 years, 15 years, and 20 years to reproduce the remaining five plots in the series.

To reproduce the combined concentration/velocity plots in Figure 4, proceed as follows.

8 Right-click Results>Concentration (tds) and choose Duplicate.

Contour I

In the Model Builder window, expand the Concentration (tds) I node.

Concentration (tds) I

I Right-click Contour I and choose Delete.

Click **Yes** to confirm.

Streamline 1

- I In the Model Builder window, under Results right-click Concentration (tds) I and choose Streamline.
- 2 In the Settings window for Streamline, locate the Streamline Positioning section.
- **3** From the **Positioning** list, choose **Uniform density**.

Concentration (tds) I

- I In the Model Builder window, under Results click Concentration (tds) I.
- 2 In the **Settings** window for 2D Plot Group, locate the **Data** section.
- 3 From the Time (a) list, choose 3.
- 4 Click to expand the Title section. In the Title text area, type Surface: Concentration (kg/m < sup > 3 < / sup >)Streamlines: Velocity field.
- 5 Click to collapse the **Title** section. On the **Concentration (tds) I** toolbar, click **Plot**.

Compare the result with the upper-left plot in Figure 4.

Repeat the previous two steps for the Time values 10 years, 15 years, 20 years to reproduce the remaining three plots in the series.

ADD STUDY

- I On the Home toolbar, click Add Study to open the Add Study window.
- 2 Go to the Add Study window.
- 3 Find the Studies subsection. In the Select Study tree, select Preset Studies>Stationary.
- 4 Click Add Study in the window toolbar.
- 5 On the Home toolbar, click Add Study to close the Add Study window.

STUDY 2

- I In the Model Builder window, click Study 2.
- 2 In the Settings window for Study, locate the Study Settings section.
- 3 Clear the Generate default plots check box.
- 4 On the Home toolbar, click Compute.

RESULTS

To visualize the stationary concentration distribution, use the second plot group as the starting point.

Concentration (tds)

In the Model Builder window, under Results right-click Concentration (tds) and choose Duplicate.

Concentration (tds) 2

- I In the **Settings** window for 2D Plot Group, locate the **Data** section.
- 2 From the Data set list, choose Study 2/Solution 2 (sol2).
- 3 On the Concentration (tds) 2 toolbar, click Plot.
- **4** Click the **Zoom Extents** button on the **Graphics** toolbar.

Compare the resulting plot with that in Figure 3.