

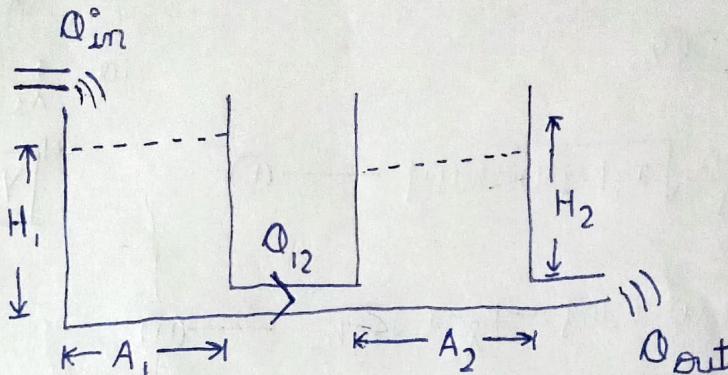
Project Report

group = 6

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$$\text{Rate of flow in a tank} = Q_{in} - Q_{out} = A \frac{dh}{dt}$$

For tank 1

$$A_1 \frac{dh_1(\pm)}{dt} = Q_{in} - B_{12} \alpha_{12} \sqrt{2g[h_1(\pm) - h_2(\pm)]} \quad \therefore Q_{in} = u(\pm)$$

$$\Rightarrow \frac{dh_1(\pm)}{dt} = \frac{u(\pm)}{A_1} - \frac{B_{12} \alpha_{12}}{A_1} \sqrt{2g[h_1(\pm) - h_2(\pm)]} \quad \dots \textcircled{1}$$

for tank 2

$$A_2 \frac{dh_2(\pm)}{dt} = B_{12} \alpha_{12} \sqrt{2g[h_1(\pm) - h_2(\pm)]} - B_2 \alpha_2 \sqrt{2g h_2(\pm)}$$

$$\frac{dh_2(\pm)}{dt} = \frac{B_{12} \alpha_{12}}{A_{12}} \sqrt{2g[h_1(\pm) - h_2(\pm)]} - \frac{B_2 \alpha_2}{A_2} \sqrt{2g h_2(\pm)} \quad \dots \textcircled{2}$$

at eq. for constant water level setpoint, the $\frac{dh}{dt}$ must be zero i.e.
 $h_1 = h_2 = 0$. In addition for the case when $h_1 = h_2$ the system model is
 decoupled. So $h_1 > h_2$.

Let. $x_1 = h_2 > 0$ and $x_2 = h_1 - h_2 > 0$.

$$x = \begin{bmatrix} x_1 \\ x_2 \end{bmatrix} \quad u = v(t)$$

$$b = \frac{\beta_{12} \alpha_{12}}{A_2} \sqrt{2g} \quad u = \frac{\beta_2 c_{12}}{A_2} \sqrt{2g}$$

dynamic eq from ① & ⑪.

$$w = \frac{1}{A_1}$$

$$\frac{dh_1(t)}{dt} = \frac{u(t)}{A_1} - \frac{\beta_{12} \alpha_{12}}{A_1} \sqrt{2g [h_1(t) - h_2(t)]} \quad \text{--- ①}$$

$$Y = Z_1$$

$$\frac{dh_2(t)}{dt} = \frac{\beta_{12} \alpha_{12}}{A_2} \sqrt{2g [h_1(t) - h_2(t)]} - \frac{\beta_2 c_{12}}{A_2} \sqrt{2g h_2} \quad \text{--- ⑪}$$

Modifying ⑩

$$\frac{d\tilde{x}_1(t)}{dt} = w u - b \sqrt{z_2}$$

$$\frac{d\tilde{x}_2(t)}{dt} = b \sqrt{z_2} - w \sqrt{z_1} \quad \Rightarrow \quad \tilde{x}_1 = b \sqrt{z_2} - w \sqrt{z_1}$$

$$\frac{d(x_2 + x_1)}{dt} = au - b \sqrt{z_2}$$

$$\Rightarrow \dot{x}_2 = au - b \sqrt{z_2} - \dot{x}_1$$

$$\Rightarrow \dot{x}_2 = au - 2b \sqrt{z_2} + c \sqrt{z_1}$$

Let $\eta = T(x)$ States are func of η .

by inverse state function.

$$x_1 = z_1$$

$$x_2 = b \sqrt{z_2} - w \sqrt{z_1}$$

$$\tilde{x}_1 = x_1$$

$$x_2 = \left(\frac{c \sqrt{z_1} + z_2}{b} \right)^2$$

$$\dot{x}_1 = \tilde{x}_2$$

$$\dot{x}_2 = \frac{b \tilde{x}_2}{2 \sqrt{z_2}} - \frac{c \tilde{x}_1}{2 \sqrt{z_1}}$$

Putting the value back in eq(3)

$$\dot{z}_2 = \frac{abc}{2} \left[\frac{\sqrt{z_1}}{\sqrt{z_2}} - \frac{\sqrt{z_2}}{\sqrt{z_1}} \right] + \frac{c^2 - b^2}{2} + \frac{ab}{2\sqrt{3}c} u(t)$$

$$0 = \frac{abc}{2} \left[\frac{\sqrt{3} \times b}{\sqrt{3}c} - \frac{\sqrt{3}c}{b \times \sqrt{3}} \right] + \frac{c^2 - b^2}{2} + \frac{ab}{2\sqrt{3}c} \times b \times u(t).$$

\Rightarrow
$$\boxed{u(t) = \frac{\sqrt{3}c}{a}}$$
 $u^* = \frac{\sqrt{3}c}{a}$

$$\Delta \overset{\circ}{x} = A \Delta \bar{x} + B \Delta \bar{u}$$

$$A = \frac{\partial f}{\partial x} \quad \begin{cases} \bar{x} = \bar{x}^* \\ u = u^* \end{cases}$$

$$B = \frac{\partial f}{\partial u} \quad \begin{cases} \bar{x} = \bar{x}^* \\ u = u^* \end{cases}$$

$y = z_1$
The objective of the control scheme
to regulate $y(t) = z_1(t) = h_2(t)$

$$A = \begin{bmatrix} \frac{\partial f_1}{\partial x_1} & \frac{\partial f_1}{\partial x_2} \\ \frac{\partial f_2}{\partial x_1} & \frac{\partial f_2}{\partial x_2} \end{bmatrix} \quad \begin{cases} \bar{x} = \bar{x}^* \\ u = u^* \end{cases}$$

$$B = \begin{bmatrix} \frac{\partial f_1}{\partial u} \\ \frac{\partial f_2}{\partial u} \end{bmatrix} \quad \begin{cases} \bar{x} = \bar{x}^* \\ u = u^* \end{cases} = \begin{bmatrix} 0 \\ \phi \end{bmatrix}$$

$$Y = C \bar{x} + D \bar{u}$$

$$C = [1, 0]$$

$$D = [0]$$

$$B = \begin{bmatrix} 0 \\ \frac{ab^2}{2\sqrt{3}c} \end{bmatrix}$$

\therefore final matrix are-

$$A = \begin{bmatrix} 0 & 1 \\ 0 & 0 \end{bmatrix}$$

$$B = \begin{bmatrix} 0 \\ \frac{ab^2}{2\sqrt{3}c} \end{bmatrix}$$

$$C = [1 \ 0]$$

$$D = [0]$$

$$\ddot{x}_2 = \frac{bc}{2} \left[\frac{\sqrt{z_1}}{\sqrt{z_2}} - \frac{\sqrt{z_2}}{\sqrt{z_1}} \right] + \frac{c^2}{2} - b^2 + \frac{ab}{2\sqrt{z_2}} u(t). \quad \text{--- } (3)$$

$$\det f = \frac{bc}{2} \left[\frac{\sqrt{z_1}}{\sqrt{z_2}} - \frac{\sqrt{z_2}}{\sqrt{z_1}} \right] + \frac{c^2}{2} - b^2 \quad \phi = \frac{ab}{2\sqrt{z_2}}$$

finally

$$\begin{bmatrix} \ddot{x}_1 \\ \ddot{x}_2 \end{bmatrix} = \begin{bmatrix} x_2 \\ \dot{x}_2 + \phi u \end{bmatrix} \xrightarrow{\text{this is } f \text{ matrix.}} \begin{array}{l} f_1 \\ f_2 \end{array}$$

$$\ddot{x} = f(\bar{x}^*, \bar{u}^*) + \frac{\partial f}{\partial x} \Big|_{\substack{x=\bar{x}^* \\ u=\bar{u}^*}} (x-\bar{x}^*) + \frac{\partial f}{\partial u} \Big|_{\substack{x=\bar{x}^* \\ u=\bar{u}^*}} (u-\bar{u}^*)$$

$$\ddot{x} = \bar{f}(\bar{x}, \bar{u}) \rightarrow \text{original syst.}$$

$$\ddot{x} - \ddot{x}^* = \frac{\partial f}{\partial x} \Big|_{\substack{x=\bar{x}^* \\ u=\bar{u}^*}} (x-\bar{x}^*) + \frac{\partial f}{\partial u} \Big|_{\substack{x=\bar{x}^* \\ u=\bar{u}^*}} (u-\bar{u}^*)$$

Now let us try to linearize about point $x_1^* = 3 \text{ cm}$ (λ_2)

$$x_1^* = 3 \quad x_2^* = \dot{x}_1^* = 0. \quad x^* = \begin{bmatrix} 3 \\ 0 \end{bmatrix}$$

for finding u^* we need x_1 & x_2

$$\boxed{x_1 = x_1 = 3.}$$

$$\begin{aligned} x_2 &= \left(\frac{c\sqrt{x_1} + x_2}{b} \right)^2 \\ &= \frac{c^2(3)^{1/2}}{b^2} = \boxed{\frac{3c^2}{b^2} = x_2^*} \end{aligned}$$

$$\frac{Y(s)}{U(s)} = C(SI - A)^{-1}B + D \quad \therefore D = [0]$$

$$\begin{aligned}\frac{Y(s)}{U(s)} &= C(SI - A)^{-1}B \\ &= [1 \ 0] \left[S \begin{bmatrix} 1 & 0 \\ 0 & 1 \end{bmatrix} - \begin{bmatrix} 0 & 1 \\ 0 & 0 \end{bmatrix} \right]^{-1} \left[\begin{bmatrix} 0 \\ \frac{ab^2}{2\sqrt{3}c} \end{bmatrix} \right] \\ &= [1 \ 0] \left[\begin{bmatrix} s & -1 \\ 0 & s \end{bmatrix} \right]^{-1} \left[\begin{bmatrix} 0 \\ \frac{ab^2}{2\sqrt{3}c} \end{bmatrix} \right] \\ &= [1 \ 0] \left[\begin{bmatrix} s & 0 \\ 0 & s \end{bmatrix} \right] \left[\begin{bmatrix} 0 \\ \frac{ab^2}{2\sqrt{3}c} \end{bmatrix} \right] \\ &= \left[\begin{bmatrix} s & 1 \\ 0 & s \end{bmatrix} \right] \left[\begin{bmatrix} 0 \\ \frac{ab^2}{2\sqrt{3}c} \end{bmatrix} \right]\end{aligned}$$

$$\frac{Y(s)}{U(s)} = \frac{ab^2}{2\sqrt{3}c s^2}$$

but ~~ab~~ $\frac{ab^2}{2\sqrt{3}c} \rightarrow K$.

$\frac{K}{s^2}$ so we can use PD controller.

$$G_c(s) = \frac{(K_p + K_d s) K}{s^2 + (K_p + K_d s) K}$$

$$G_c(s) = \frac{(K_p + K_d s) K}{s^2 + K_d K s + K_p K}$$

using Routh Hurwitz criteria

$$K_d K > 0 \quad \& \quad K_p K > 0$$

for stability

h_1 and $h_2 \rightarrow$ height of liquid in tank 1 and 2

A_1 and $A_2 \rightarrow$ cross sectional area of tank 1 and 2

$\alpha_2 \rightarrow$ cross sectional area of outlet pipe in tank 2

$\alpha_{12} \rightarrow$ cross sectional area of interaction pipe between tank 1 and 2

$B_{12} \rightarrow$ valve ratio of interaction pipe between tank 1 and 2

$B_2 \rightarrow$ valve ratio of interaction pipe of tank 2 outlet

$$A_1, A_2 = 154 \text{ cm}^2$$

$$\alpha_2, \alpha_{12} = 0.5 \text{ cm}^2$$

$$B_{12} = 1.53$$

$$B_2 = 0.68$$

$$g = 981 \text{ cm/s}^2$$

Trying using PID control.

$$\frac{K}{s^2}$$

$$U_{CL}(s) = \frac{\frac{K(K_p + K_d s + K_i/s)}{s^2}}{1 + \frac{K(K_p + K_d s + K_i/s)}{s^2}}$$

$$\Rightarrow \frac{\frac{K(K_p s + K_d s^2 + K_i)}{s \cancel{s^2}}}{s^3 + \frac{K(K_p s + K_d s^2 + K_i)}{\cancel{s^2}}} \Rightarrow$$

$$\frac{K(K_p s + K_d s^2 + K_i)}{s^3 + K_d s^2 + K_p k_s s + K_i}$$

$$U_{CL}(s) = \boxed{\frac{K(K_p s + K_d s^2 + K_i)}{s^3 + K_d K_p s^2 + (K_p K_d)s + K_i}}$$