

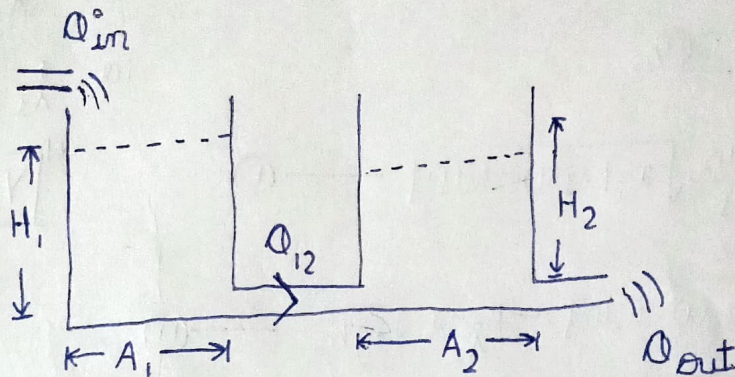
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Rate of flow in a tank =  $Q_{in} - Q_{out} = A \frac{dh}{dt}$

For tank 1

$$A_1 \frac{dh_1(\pm)}{dt} = Q_{in} - B_{12} \alpha_{12} \sqrt{2g[h_1(\pm) - h_2(\pm)]} \quad \therefore Q_{in} = u(\pm)$$

$$\Rightarrow \frac{dh_1(\pm)}{dt} = \frac{u(\pm)}{A_1} - \frac{B_{12} \alpha_{12}}{A_1} \sqrt{2g[h_1(\pm) - h_2(\pm)]} \quad \text{--- (1)}$$

For tank 2

$$A_2 \frac{dh_2(\pm)}{dt} = B_{12} \alpha_{12} \sqrt{2g[h_1(\pm) - h_2(\pm)]} - B_2 \alpha_2 \sqrt{2gh_2(\pm)}$$

$$\frac{dh_2(\pm)}{dt} = \frac{B_{12} \alpha_{12}}{A_{12}} \sqrt{2g[h_1(\pm) - h_2(\pm)]} - \frac{B_2 \alpha_2}{A_2} \sqrt{2gh_2(\pm)} \quad \text{--- (2)}$$

Let eq<sup>n</sup> for constant water level setpoint, the  $\frac{dh}{dt}$  must be zero ; i.e

$h_1 = h_2 = 0$ . In addition for the case when  $h_1 = h_2$ , the system model is decoupled. So  $h_1 > h_2$ .



Let  $z_1 = h_2 > 0$  and  $z_2 = h_1 - h_2 > 0$ .

$$z = \begin{bmatrix} z_1 \\ z_2 \end{bmatrix} \quad u = q(t)$$

$$b = \frac{\beta_{12} \alpha_{12}}{A_2} \sqrt{2g}$$

$$c = \frac{\beta_2 \alpha_{12}}{A_2} \sqrt{2g}$$

dynamic eq from ① & ②

$$a = \frac{1}{A_1}$$

$$\frac{dh_1(t)}{dt} = \frac{u(t)}{A_1} - \frac{\beta_{12} \alpha_{12}}{A_1} \sqrt{2g[h_1(t) - h_2(t)]} \quad \text{--- ①}$$

$$\boxed{y = z_1}$$

$$\frac{dh_2(t)}{dt} = \frac{\beta_{12} \alpha_{12}}{A_2} \sqrt{2g[h_1(t) - h_2(t)]} - \frac{\beta_2 \alpha_2}{A_2} \sqrt{2gh_2} \quad \text{--- ②}$$

Modify ②

$$\frac{dz_2(t)}{dt} = au - b\sqrt{z_2}$$

$$\frac{dz_1(t)}{dt} = b\sqrt{z_2} - c\sqrt{z_1}$$

$$\Rightarrow \boxed{\dot{z}_1 = b\sqrt{z_2} - c\sqrt{z_1}}$$

$$\frac{d(z_2 + z_1)(t)}{dt} = au - b\sqrt{z_2}$$

$$\Rightarrow \dot{z}_2 = au - b\sqrt{z_2} - \dot{z}_1$$

$$\Rightarrow \boxed{\dot{z}_2 = au - 2b\sqrt{z_2} + c\sqrt{z_1}}$$

Let  $x = T(z)$  States are fun<sup>n</sup> of  $z$ .

by inverse transformation.

$$x_1 = z_1$$

$$z_1 = x_1$$

$$x_2 = b\sqrt{z_2} - c\sqrt{z_1}$$

$$z_2 = \left( \frac{c\sqrt{x_1} + x_2}{b} \right)^2$$

$$\dot{x}_1 = x_2$$

$$\dot{x}_2 = \frac{b\dot{z}_2}{2\sqrt{z_2}} - \frac{c\dot{z}_1}{2\sqrt{z_1}}$$



Putting the value back in eq (3)

$$\dot{x}_2 = \frac{dc}{2} \left[ \frac{\sqrt{x_1}}{\sqrt{x_2}} - \frac{\sqrt{x_2}}{\sqrt{x_1}} \right] + \frac{c^2 - b^2}{2} + \frac{ab}{2\sqrt{x_2}} u(t)$$

$$0 = \frac{dc}{2} \left[ \frac{\sqrt{3c}}{\sqrt{3c}} - \frac{\sqrt{3c}}{b\sqrt{3c}} \right] + \frac{c^2 - b^2}{2} + \frac{ab}{2\sqrt{3c}} \times b \times u(t)$$

$$\Rightarrow \boxed{u(t) = \frac{\sqrt{3c}}{a}}$$

$$u^* = \frac{\sqrt{3c}}{a}$$

$$\Delta \dot{\bar{x}} = A \Delta \bar{x} + B \Delta \bar{u}$$

$$A = \frac{\partial f}{\partial \bar{x}} \bigg|_{\substack{\bar{x} = \bar{x}^* \\ \bar{u} = \bar{u}^*}}$$

$$B = \frac{\partial f}{\partial \bar{u}} \bigg|_{\substack{\bar{x} = \bar{x}^* \\ \bar{u} = \bar{u}^*}}$$

$y = x_1$   
The objective of the control scheme to regulate.  
 $y(t) = x_1(t) = h_2(t)$

$$A = \begin{bmatrix} \frac{\partial f_1}{\partial x_1} & \frac{\partial f_1}{\partial x_2} \\ \frac{\partial f_2}{\partial x_1} & \frac{\partial f_2}{\partial x_2} \end{bmatrix} \bigg|_{\substack{\bar{x} = \bar{x}^* \\ \bar{u} = \bar{u}^*}} = \begin{bmatrix} 0 & 1 \\ 0 & 0 \end{bmatrix}$$

$$B = \begin{bmatrix} \frac{\partial f_1}{\partial u} \\ \frac{\partial f_2}{\partial u} \end{bmatrix} \bigg|_{\substack{\bar{x} = \bar{x}^* \\ \bar{u} = \bar{u}^*}} = \begin{bmatrix} 0 \\ \phi \end{bmatrix}$$

$$y = C\bar{x} + D\bar{u}$$

$$C = [1, 0]$$

$$D = [0]$$

$$B = \begin{bmatrix} 0 \\ \frac{ab^2}{2\sqrt{3c}} \end{bmatrix}$$

∴ Final matrix are-

$$A = \begin{bmatrix} 0 & 1 \\ 0 & 0 \end{bmatrix}$$

$$B = \begin{bmatrix} 0 \\ \frac{ab^2}{2\sqrt{3c}} \end{bmatrix}$$

$$C = [1 \quad 0]$$

$$D = [0]$$



$$\dot{x}_2 = \frac{bc}{2} \left[ \frac{\sqrt{x_1}}{\sqrt{x_2}} - \frac{\sqrt{x_2}}{\sqrt{x_1}} \right] + \frac{c^2}{2} - b^2 + \frac{ab}{2\sqrt{x_2}} u(t). \quad (3)$$

$$\text{def } f = \frac{bc}{2} \left[ \frac{\sqrt{x_1}}{\sqrt{x_2}} - \frac{\sqrt{x_2}}{\sqrt{x_1}} \right] + \frac{c^2}{2} - b^2 \quad \phi = \frac{ab}{2\sqrt{x_2}}$$

# finally

$$\begin{bmatrix} \dot{x}_1 \\ \dot{x}_2 \end{bmatrix} = \begin{bmatrix} x_2 \\ \phi + \phi u \end{bmatrix} \begin{matrix} \xrightarrow{f_1} \\ \xrightarrow{f_2} \end{matrix} \quad \text{this is } f \text{ matrix.}$$

$$\dot{\bar{x}} = f(\bar{x}^*, \bar{u}^*) + \left. \frac{\partial f}{\partial \bar{x}} \right|_{\substack{\bar{x}=\bar{x}^* \\ \bar{u}=\bar{u}^*}} (\bar{x} - \bar{x}^*) + \left. \frac{\partial f}{\partial \bar{u}} \right|_{\substack{\bar{x}=\bar{x}^* \\ \bar{u}=\bar{u}^*}} (\bar{u} - \bar{u}^*)$$

$$\dot{\bar{x}} = \bar{f}(\bar{x}, \bar{u}) \rightarrow \text{original system.}$$

$$\begin{aligned} \dot{\bar{x}} - \dot{\bar{x}}^* &= \left. \frac{\partial f}{\partial \bar{x}} \right|_{\substack{\bar{x}=\bar{x}^* \\ \bar{u}=\bar{u}^*}} (\bar{x} - \bar{x}^*) + \left. \frac{\partial f}{\partial \bar{u}} \right|_{\substack{\bar{x}=\bar{x}^* \\ \bar{u}=\bar{u}^*}} (\bar{u} - \bar{u}^*) \\ &= \Delta \dot{\bar{x}} \end{aligned}$$

Now let us try to linearize about point  $x_1^* = 3 \text{ cm}$  ( $h_2$ )

$$x_1^* = 3 \quad x_2^* = \dot{x}_1^* = 0. \quad x^* = \begin{bmatrix} 3 \\ 0 \end{bmatrix}$$

For finding  $u^*$  we need  $x_1$  &  $x_2$

$$\boxed{x_1 = x_1 = 3.}$$

$$x_2 = \left( \frac{c\sqrt{x_1} + x_2}{b} \right)^2$$

$$= \frac{c^2(3)^{3/2}}{b^2} = \boxed{\frac{3c^2}{b^2} = 2 \frac{3}{2}}$$



$$\frac{Y(s)}{U(s)} = C (SI - A)^{-1} B + D$$

$$\therefore D = [0]$$

$$\frac{Y(s)}{U(s)} = C (SI - A)^{-1} B$$

$$= [1 \ 0] \left[ S \begin{bmatrix} 1 & 0 \\ 0 & 1 \end{bmatrix} - \begin{bmatrix} 0 & 1 \\ 0 & 0 \end{bmatrix} \right]^{-1} \begin{bmatrix} 0 \\ \frac{ab^2}{2\sqrt{3}c} \end{bmatrix}$$

$$= [1 \ 0] \begin{bmatrix} S & -1 \\ 0 & S \end{bmatrix}^{-1} \begin{bmatrix} 0 \\ \frac{ab^2}{2\sqrt{3}c} \end{bmatrix}$$

$$= [1 \ 0] \begin{bmatrix} S & 1 \\ 0 & S \end{bmatrix} \frac{1}{s^2} \begin{bmatrix} 0 \\ \frac{ab^2}{2\sqrt{3}c} \end{bmatrix}$$

$$= \begin{bmatrix} S & 1 \\ - & \end{bmatrix} \frac{1}{s^2} \begin{bmatrix} 0 \\ \frac{ab^2}{2\sqrt{3}c} \end{bmatrix}$$

$$\frac{Y(s)}{U(s)} = \frac{ab^2}{2\sqrt{3}cs^2}$$

$$\text{let } \frac{ab^2}{2\sqrt{3}c} = K$$

$\frac{K}{s^2}$  so we can use PD controller.

$$\Rightarrow G(s) = \frac{(K_p + K_d s) K}{s^2 + (K_p + K_d s) K}$$

using Routh Hurwitz criteria

$K_d K > 0$  &  $K_p K > 0$   
for stability

$$G(s) = \frac{(K_p + K_d s) K}{s^2 + K_d K s + K_p K}$$



$h_1$  and  $h_2 \rightarrow$  height of liquid in tank 1 and 2

$A_1$  and  $A_2 \rightarrow$  cross sectional area of tank 1 and 2

$\alpha_2 \rightarrow$  cross sectional area of outlet pipe in tank 2

$\alpha_{12} \rightarrow$  cross sectional area of interaction pipe between tank 1 and 2

$B_{12} \rightarrow$  valve ratio of interaction pipe between tank 1 and 2

$B_2 \rightarrow$  valve ratio of ~~interaction~~ outlet pipe of tank 2

$$A_1, A_2 = 154 \text{ cm}^2$$

$$\alpha_2, \alpha_{12} = 0.5 \text{ cm}^2$$

$$B_{12} = 1.53$$

$$B_2 = 0.68$$

$$g = 981 \text{ cm/s}^2$$



Trying using PID controller.

$$\frac{K}{s^2}$$

$$G_{CL}(s) = \frac{\frac{K(K_p + K_d s + k_i/s)}{s^2}}{1 + \frac{K(K_p + K_d s + k_i/s)}{s^2}}$$

$$\Rightarrow \frac{K(K_p s + K_d s^2 + k_i)}{\cancel{s} \times \cancel{s^2}} \times \frac{s^2}{s^3 + K(K_p s + K_d s^2 + k_i)}$$

$$\Rightarrow \frac{K(K_p s + K_d s^2 + k_i)}{s^3 + K_d K s^2 + K_p K s + k_i}$$

$$G_{CL}(s) = \frac{K(K_p s + K_d s^2 + k_i)}{s^3 + K_d K s^2 + (K_p K) s + k_i}$$