

Thermodynamics and Heat Transfer LE6 Part 2

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Problem 1: Find the heat transfer per unit area through the composite wall in Figure 1. Assume one dimensional heat flow (20 points).

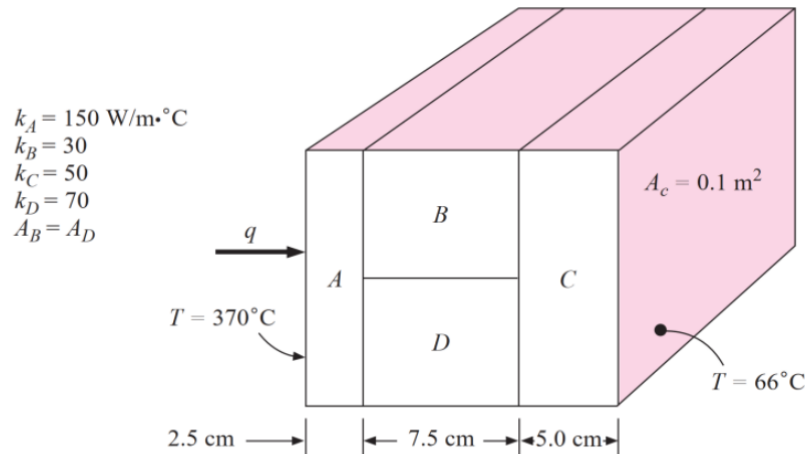


Figure 1

Problem 1:

Formula: $\dot{Q}_{\text{cond, wall}} = \frac{T_1 - T_2}{R_{\text{wall}}}$, $R_{\text{wall}} = \frac{L}{kA}$

$$R_{\text{wall, A}} = \frac{0.025 \text{ m}}{150 \text{ W/m}^\circ\text{C} \times 0.1 \text{ m}^2} = 0.1667 \times 10^{-2} \text{ (C/W)}$$

$$R_{\text{wall, B}} = \frac{0.075 \text{ m}}{30 \text{ W/m}^\circ\text{C} \times \left(\frac{0.1}{2}\right) \text{ m}^2} = 0.05 \text{ C/W}$$

$$R_{\text{wall, C}} = \frac{0.05 \text{ m}}{50 \text{ W/m}^\circ\text{C} \times 0.1 \text{ m}^2} = 0.01 \text{ C/W}$$

$$R_{\text{wall, D}} = \frac{0.075 \text{ m}}{70 \text{ W/m}^\circ\text{C} \times \left(\frac{0.1}{2}\right) \text{ m}^2} = 0.02143 \text{ C/W}$$

$$\Rightarrow \Sigma R_{\text{wall}} = R_A + \frac{R_B R_D}{R_B + R_D} + R_C = 0.02667 \text{ C/W}$$

The heat transfer per unit area through the composite wall would be:

$$\dot{Q}_{\text{wall}} = \frac{T_1 - T_2}{\Sigma R_{\text{wall}}} = \frac{370^\circ\text{C} - 66^\circ\text{C}}{0.02667 \text{ C/W}} = 11398.57 \text{ W (answer)}$$

Problem 2: A steel tube having $k = 46 \text{ W/m} \cdot ^\circ\text{C}$ has an inside diameter of 3.0 cm and a tube wall thickness of 2 mm. A fluid flows on the inside of the tube producing a convection coefficient of $1500 \text{ W/m}^2 \cdot ^\circ\text{C}$ on the inside surface, while a second fluid flows across the outside of the tube producing a convection coefficient of $197 \text{ W/m}^2 \cdot ^\circ\text{C}$ on the outside tube surface. The inside fluid temperature is 223°C while the outside fluid temperature is 57°C . Calculate the heat lost by the tube per meter of length (15 points).

Problem 2:

$$k = 46 \text{ W/m} \cdot ^\circ\text{C}, d_{\text{in}} = 3 \text{ cm}, \text{thickness} = 2 \text{ mm} \Rightarrow d_{\text{out}} = 3.4 \text{ cm}$$

$$h_{\text{in}} = 1500 \text{ W/m}^2 \cdot ^\circ\text{C}, h_{\text{out}} = 197 \text{ W/m}^2 \cdot ^\circ\text{C} \Rightarrow r_{\text{in}} = 1.5 \text{ cm}, r_{\text{out}} = 1.7 \text{ cm}$$

$$T_{\text{in}} = 223^\circ\text{C}, T_{\text{out}} = 57^\circ\text{C} \Rightarrow \text{find heat loss/meter}$$

$$\begin{aligned} \text{We have: } R_{\text{total}} &= R_{\text{conv},1} + R_{\text{cyl}} + R_{\text{conv},2} \\ &= \frac{1}{(2\pi r_{\text{in}} L) h_{\text{in}}} + \frac{\ln(r_{\text{out}}/r_{\text{in}})}{2\pi L k} + \frac{1}{(2\pi r_{\text{out}} L) h_{\text{out}}} \\ &= \left[\frac{1}{0.03 \text{ m} \cdot \pi \cdot 1500} + \frac{\ln(0.017/0.015)}{2\pi \cdot 46} + \frac{1}{0.034 \text{ m} \cdot \pi \cdot 197} \right] \frac{1}{L} \\ &= (0.0070735 + 0.000433 + 0.0047523) \frac{1}{L} \\ &= 0.055029 \cdot \frac{1}{L} \end{aligned}$$

The heat loss by the tube per meter of length is

$$\frac{\dot{Q}}{L} = \frac{T_{\infty 1} - T_{\infty 2}}{R_{\text{total}} L} = \frac{223 - 57}{0.055029 L \cdot \frac{1}{L}} = 3016.59 \text{ W/m (answer)}$$

Problem 3: A spherical tank, 1m in diameter, is maintained at a temperature of 120°C and exposed to a convection environment. With $h = 25 \text{ W/m}^2\cdot\text{C}$ and $T_\infty = 15^\circ\text{C}$, what thickness of urethane foam should be added to ensure that the outer temperature of the insulation does not exceed 40°C? What percentage reduction in heat loss results from installing this insulation (15 points)?

Problem 3:

$$T_{\text{tank}} = 120^\circ\text{C}, T_\infty = 15^\circ\text{C}, h = 25 \text{ W/m}^2\cdot\text{C}, k_{\text{foam}} = 0.02 \text{ W/m}\cdot\text{C}$$

$$\Delta x = ? \text{ so } T_{\text{out}} \text{ not exceed } 40^\circ\text{C}. \text{ \% reduction in } \dot{Q} ? \quad d = 1\text{m}$$

□ Heat convection

$$\dot{Q}_{\text{conv}} = hA(T_{\text{tank}} - T_\infty) = 25 \cdot \left(4\pi \left(\frac{1\text{m}}{2}\right)^2\right)(120^\circ\text{C} - 15^\circ\text{C})$$

$$= 8246.68 \text{ W}$$

Without the insulation by urethane foam, the heat transfer rate is $\dot{Q} = 8246.68 \text{ W}$

□ With insulation by the urethane foam

$$\text{Heat conduction: } \dot{Q}_{\text{cond}} = \frac{4\pi k r_{\text{out}} r_{\text{in}} (T_{\text{tank}} - T_{\text{max}})}{r_{\text{out}} - r_{\text{in}}}$$

$$= \frac{4\pi \cdot 0.02 \times r_{\text{out}} \times 0.5 (120 - 40)}{r_{\text{out}} - 0.5} = \frac{10.053 r_{\text{out}}}{r_{\text{out}} - 0.5}$$

$$\text{Heat convection: } \dot{Q}_{\text{conv}} = hA(T_{\text{max}} - T_\infty) = 4\pi r_{\text{out}}^2 \cdot h(T_{\text{max}} - T_\infty)$$

$$= 4\pi r_{\text{out}}^2 \cdot 25(40^\circ\text{C} - 15^\circ\text{C}) = 7853.98 r_{\text{out}}^2$$

The heat transfer of the convection environment is the same as the conduction of heat through the sphere $\Rightarrow \frac{10.053 r_{\text{out}}}{r_{\text{out}} - 0.5} = 7853.98 r_{\text{out}}^2$

$$\Rightarrow r_{\text{out}} \approx 0.502 \text{ m}$$

$$\Rightarrow \text{Thickness of urethane foam should be: } \Delta x = r_{\text{out}} - r_{\text{in}} = 0.502 - 0.5 \text{ (m)}$$

$$= 2 \text{ mm (answer)}$$

With the insulation by the foam, the heat transfer rate is

$$\dot{Q}_{\text{conv}} = 7853.98 r_{\text{out}}^2 = 7853.98 \times (0.502)^2 = 1979.234 \text{ W}$$

Percentage reduction in heat loss from installing the insulation is

$$\% \dot{Q}_{\text{reduce}} = \frac{\dot{Q}_{\text{before}} - \dot{Q}_{\text{after}}}{\dot{Q}_{\text{before}}} \times 100\% = \frac{8246 - 1979.234}{8246} \times 100\%$$

$$= 75.99\% \text{ (answer)}$$