

# FORMULAS FOR LIFE

All formulas you'll ever need

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A helpful tool for scientific studies

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# 1 Statistics

## 1.1 Mean

### 1.1.1 Arithmetic mean

$$\bar{x} = \sum_{i=1}^n \frac{x_i}{N}$$

### 1.1.2 Geometric mean

$$\bar{x} = \left( \prod_{i=1}^n x_i \right)^{\frac{1}{n}}$$

### 1.1.3 Harmonic mean

$$\bar{x} = n \left( \sum_{i=1}^n \frac{1}{x_i} \right)^{-1}$$

## 1.2 Standard Deviation

### 1.2.1 Absolute

$$s = \sqrt{\frac{\sum_{i=1}^n (x_i - \bar{x})^2}{N - 1}}$$

### 1.2.2 Relative

$$RSD = \frac{s}{\bar{x}}$$

## 2 Pure Physics

## 3 Pure Chemistry

### 3.1 Concentration

#### 3.1.1 Mole

$$n = \frac{m}{MW}$$

#### 3.1.2 Molarity

$$M = \frac{n}{V}$$

# 4 Thermodynamics

## 4.1 Perfect gases

### 4.1.1 State equation

$$pV = nRT$$
$$pV_m = RT$$

### 4.1.2 Properties

Molar mass

$$d_{gas} \cdot V_m = MW$$

Boyle's law

$$p_1 V_1 = p_2 V_2 \quad T = const$$

Charle's law

$$\frac{V_1}{T_1} = \frac{V_2}{T_2} \quad p = const$$

Gay-Lussac's Law

$$\frac{p_1}{T_1} = \frac{p_2}{T_2} \quad V = const$$

### 4.1.3 Compression factor

$$Z = \frac{PV}{nRT}$$

$Z = 1$  for perfect gases

## 4.2 Real gases

### 4.2.1 Virial equation

$$pV_m = RT \left( 1 + \frac{B}{V_m} + \frac{C}{V_m^2} + \dots \right)$$

### 4.2.2 van der Waals equation

$$p = \frac{nRT}{V - nb} - a \left( \frac{n}{V} \right)^2$$
$$p = \frac{nRT}{V_m - b} - \frac{a}{V_m^2}$$

### 4.2.3 Compression factor

$$Z = \frac{V_m}{V_m - b} - \frac{a}{RTV_m}$$

if  $y = \frac{1}{V_m} \implies \frac{1}{1 - by} - \frac{ay}{RT}$

### 4.2.4 Boyle Temperature

$$\lim_{p \rightarrow 0} \frac{dZ}{dp} = 0 \quad p \rightarrow 0 \implies \frac{1}{V_m} \rightarrow 0$$
$$y = \frac{1}{V_m} \quad \lim_{y \rightarrow 0} \frac{1}{1 - by} - \frac{ay}{RT} =$$
$$T_b = \frac{a}{Rb}$$

### 4.2.5 Critical and reduced variables

$$T_c = \frac{8a}{27Rb} \quad p_c = \frac{a}{27b^2} \quad V_c = 3b \quad Z_c = \frac{p_c V_c}{RT_c}$$

The van der Waals equation can be rewritten :

$$p_r = \frac{8T_r}{3V_r - 1} - \frac{3}{V_r^2}$$

## 4.3 Internal Energy

$$\Delta U = q + w$$

$$dU = \delta w + \delta q$$

$$dU = TdS - pdV$$

$$dU = \left( \frac{\partial U}{\partial S} \right)_V dS + \left( \frac{\partial U}{\partial V} \right)_S dV$$

Is always true that:

$$dU = \int_{T_1}^{T_2} C_V dT$$

$$\Delta U = nC_{v,m} \Delta T$$

## 4.4 Enthalpy

$$H = U + pV$$

$$\Delta H = \Delta U + \Delta pV$$

$$dH = -SdT + Vdp$$

For the perfect gas is also true that:

$$\Delta H = \Delta U + \Delta(nRT)$$

### 4.4.1 Temperature dependence

Pure substance

$$\Delta H(T_2) = \Delta H(T_1) + \int_{T_1}^{T_2} C_p dT.$$

## Chemical reaction or phase transition

$$\Delta H(T_2) = \Delta H_r T_1 + \Delta C_p(T_2 - T_1)$$
$$\Delta C_p = [cC_{p,C} + dC_{p,D}] - [aC_{p,A} + bC_{p,B}]$$

## 4.5 Entropy

$$\Delta S_{TOT} \geq 0$$
$$\Delta S = \frac{q}{T} \implies \Delta S = \int_i^f \frac{q_{rev}}{T}$$

For an ideal gas it is always true that:

$$\Delta S = nC_m \ln\left(\frac{T_f}{T_i}\right) + nR \ln\left(\frac{V_f}{V_i}\right)$$

Only mixing two gases results in:

$$\Delta S_{mix} = -R \sum_{i=1}^N n_i \ln \chi_i$$

### 4.5.1 Trouton's Rules

$$\Delta S_{trs} = \frac{\Delta H_{trs}}{T_{trs}}$$

### 4.5.2 Temperature dependence

Constant pressure

$$\Delta S = S(T_f) - S(T_i) = C_p \int_i^f \frac{dT}{T} = C_p \ln\left(\frac{T_f}{T_i}\right)$$

Constant volume

$$\Delta S = S(T_f) - S(T_i) = C_v \int_i^f \frac{dT}{T} = C_v \ln\left(\frac{T_f}{T_i}\right)$$

### 4.5.3 Chemical reaction

$$aA + bB \rightarrow cC + dD$$
$$\Delta_r S^0 = (cS_C^0 + dS_D^0) - (aS_A^0 + bS_B^0)$$
$$\Delta_r S^0 = \sum_{i=1}^N \nu_i S_{reagents}^0 - \sum_{i=1}^N \nu_i S_{products}^0$$

If calculating  $T \neq 298K$ :

$$\Delta_r S(T_2) = \Delta_r S(T_1) + \Delta C_p \ln \frac{T_2}{T_1}$$
$$\Delta C_p = (cC_{c,p} + dC_{d,p}) - (aC_{a,p} + bC_{b,p})$$

## 4.6 Isothermal Transformations

### 4.6.1 Free expansion

$$\Delta T = 0 \implies \Delta U = 0 \implies q = w$$
$$w = q = -p_{ext} \Delta V = 0$$
$$\Delta H = \Delta PV \quad (0 \text{ for perfect gas})$$
$$\Delta S = nR \ln\left(\frac{V_f}{V_i}\right) \quad \Delta S' = 0 \quad \Delta S_{tot} = \Delta S$$

### 4.6.2 Expansion vs. $p_{ext}$

$$\Delta T = 0 \implies \Delta U = 0 \implies q = w$$
$$w = q = -p_{ext} \Delta V$$
$$\Delta H = \Delta PV \quad (0 \text{ for perfect gas})$$
$$\Delta S = nR \ln\left(\frac{V_f}{V_i}\right) \quad \Delta S' = \frac{-q_{sistema}}{T}$$
$$\Delta S_{tot} = \Delta S + \Delta S'$$

### 4.6.3 Reversible expansion

$$\Delta T = 0 \implies \Delta U = 0 \implies q = w$$
$$q = w = -nRT \ln\left(\frac{V_f}{V_i}\right)$$
$$\Delta H = \Delta PV \quad (0 \text{ for perfect gas})$$
$$\Delta S = nR \ln\left(\frac{V_f}{V_i}\right) \quad \Delta S' = -nR \ln\left(\frac{V_f}{V_i}\right)$$
$$\Delta S_{tot} = 0$$

## 4.7 Adiabatic Transformations

$$dU = dw$$
$$C_v dT = -pdV$$
$$w_{Adiabatic} = nC_{V,m} \Delta T$$

For an adiabatic process is also true that:

$$\gamma = \frac{C_{p,m}}{C_{V,m}} = \frac{C_p}{C_V} \quad P_1(V_1)^\gamma = P_2(V_2)^\gamma$$

### 4.7.1 Reversible process

$$C_V dT = \frac{-nRT}{V} dV$$
$$\int_{T_1}^{T_2} \frac{C_V dT}{T} = -nR \int_{T_1}^{T_2} \frac{dV}{V}$$
$$C_V \ln\left(\frac{T_1}{T_2}\right) = -R \ln \frac{V_2}{V_1}$$
$$\frac{T_2}{T_1} = \left[\frac{V_2}{V_1}\right]^{-\frac{R}{C_V}}$$

### 4.7.2 Irreversible

Take P as constant

$$\int_{T_1}^{T_2} C_V dT = -p \int_{V_1}^{V_2} dV$$

Assuming  $C_V = \text{const}$

$$C_V \Delta T = -p \Delta V$$

### 4.7.3 Free expansion

$$q = 0, w = -p_{\text{ext}} \Delta V = 0 \implies \Delta U = 0$$

$$\Delta H =$$

$$\Delta S = nR \ln\left(\frac{V_f}{V_i}\right) \quad \Delta S' = 0 \quad \Delta S_{\text{tot}} = 0$$

### 4.7.4 Expansion vs. $p_{\text{ext}}$

$$q = 0 \implies \Delta U = w$$

$$\Delta U = nC_{V,m} \Delta T = w = -p_{\text{ext}} \Delta V$$

$$\Delta T = -\frac{p_{\text{ext}} \Delta V}{nC_{V,m}}$$

$$\Delta H = V \Delta p$$

$$\Delta S = nC_{V,m} \ln\left(\frac{T_f}{T_i}\right) + nR \ln\left(\frac{V_f}{V_i}\right)$$

$$\Delta S' = 0 \implies \Delta S_{\text{TOT}} = \Delta S$$

### 4.7.5 Reversible expansion

$$q = 0 \implies \Delta U = w$$

$$\Delta U = nC_{V,m} \Delta T$$

$$\Delta S = \Delta S' = \Delta_{\text{tot}} = 0$$

## 4.8 Isobaric transformations

$$dp = 0$$

$$q = \Delta H = nC_{p,m} \Delta T$$

$$w = -p \Delta V$$

$$\Delta S = nC_{p,m} \ln\left(\frac{T_f}{T_i}\right) \quad \Delta S' = -nC_{p,m} \ln\left(\frac{V_f}{V_i}\right)$$

$$\implies \Delta S_{\text{TOT}} = 0$$

## 4.9 Thermodynamic cycles

$$\Delta U = 0, \Delta S = 0, \Delta H = 0.$$

### 4.9.1 Carnot cycle

There is 4 stage (ABCD):

#### AB Reversible Isothermal expansion

$$\Delta U = 0 \implies q_{AB} = -w_{AB}$$

$$w_{AB} = -q_{AB} = -nRT_h \ln\left(\frac{V_B}{V_A}\right)$$

#### BC Reversible Adiabatic Expansion

$$q_{BC} = 0 \implies \Delta U_{BC} = w_{BC}$$

$$w_{BC} = nC_{V,m}(T_C - T_h)$$

#### CD Reversible Isothermal compression

$$\Delta U = 0 \implies q_{CD} = -w_{CD}$$

$$w_{CD} = -q_{CD} = -nRT_h \ln\left(\frac{V_D}{V_C}\right)$$

#### DA Reversible Adiabatic compression

$$q_{DA} = 0 \implies \Delta U_{DA} = w_{DA}$$

$$w_{DA} = nC_{V,m}(T_C - T_h)$$

## 4.10 Helmholtz's Energy

$$A = U - ST$$

$$\Delta A_V = \Delta U_V - T \Delta S_V$$

$\Delta A$  is the maximum (more negative) work that can be done by the system if  $dT=0$ .

$$0 \geq w \geq \Delta A$$

It can also be expressed with natural variables:

$$dA = -SdT - pdV$$

$$dA = \left(\frac{\partial A}{\partial T}\right)_V dT + \left(\frac{\partial A}{\partial V}\right)_T dV$$

## 4.11 Gibbs's Energy

$$G = H - ST$$

$$\Delta G_p = \Delta H_p - T \Delta S_p$$

$\Delta G$  is the maximum (more negative) work that can be done by the system if  $dT=0$ .

$$0 \geq w_{ne} \geq \Delta G$$

It can also be expressed with natural variables:

$$dG = -SdT + Vdp$$

$$dG = \left(\frac{\partial G}{\partial T}\right)_p dT + \left(\frac{\partial G}{\partial p}\right)_T dp$$

### 4.11.1 Gibbs-Helmholtz's equation

$$\frac{\partial}{\partial T} \left( \frac{\Delta G}{T} \right)_p = -\frac{\Delta H}{T^2}$$

$$\frac{\Delta G(T_2)}{T_2} - \frac{\Delta G(T_1)}{T_1} = \Delta H \left( \frac{1}{T_2} - \frac{1}{T_1} \right)$$



### 4.11.2 Pressure dependence

$$\Delta G = G(p_2) - \Delta G(p_1) = nRT \ln \left( \frac{p_2}{p_1} \right)$$

It can be also used to find  $G_m(T_2)$  for a reaction:

$$\begin{aligned} nA &\rightarrow mB \\ nG(A, p_2) &= nG^0 + nRT \ln p_2 \\ nG(B, p_2) &= mG^0 + mRT \ln p_2 \\ \Delta G(p_2) &= mG(B, p_2) - nG(A, p_2) = \\ &\Delta G^0 + (m - n)RT \ln p_2 \end{aligned}$$

## 4.12 Chemical potential

G is an extensive variable, otherwise a p, T = const it would be always true that dG = 0. G depends on the composition of the system:  $G = G(p, T, n_1, n_2, \dots)$ . The partial derivative of G is the chemical potential:

$$\mu = \left( \frac{\partial G}{\partial n_i} \right)_{p, T, n_j} \implies dG = \sum_{i=1}^N \mu_i dn_i$$

### 4.12.1 Gibbs-Duhem equation

$$\sum_{i=1}^N n_i d\mu_i = -SdT + Vdp$$

If temperature and pressure are constant:

$$\sum_{i=1}^N n_i d\mu_i = 0$$

### 4.12.2 Natural variables

$$\left( \frac{d\mu}{dp} \right)_T = V_m \quad \left( \frac{d\mu}{dT} \right)_p = -S_m$$

### 4.12.3 Perfect gas chemical potential

$$\begin{aligned} \left( \frac{d\mu}{dp} \right)_T &= V_m \\ \int_{p_0}^p \frac{d\mu}{dp} dp &= \int_{p_0}^p \frac{RT}{p} dp \\ \mu(p, T) &= \mu_0(p_0, T) + RT \ln \left( \frac{p}{p_0} \right) \end{aligned}$$

## 4.13 Chemical equilibrium

$\Delta_r G$  is related to G variation at constant temperature and pressure

$$\Delta_r G = \left( \frac{\partial G}{\partial \xi} \right)_{p, T} = \sum_{i=1}^n \nu_i \mu_i$$

Is possible to relate  $\Delta_r G^0$  and K :

$$K = e^{-\frac{\Delta_r G^0}{RT}}$$

Different K calculation are related easily:

$$\begin{aligned} K_c &= K_n \left( \frac{1}{V} \right)^{\Delta \nu} & K_\chi &= K_n \left( \frac{1}{n_{tot}} \right)^{\Delta \nu} \\ K_p &= K_n \left( \frac{p_{tot}}{n_{tot}} \right)^{\Delta \nu} \end{aligned}$$

### 4.13.1 Pressure dependence

$$\begin{aligned} \frac{\partial \ln K}{\partial p} &= -\frac{1}{RT} \left( \frac{\partial \Delta_r G}{\partial p} \right) \\ \frac{\partial \ln K}{\partial p} &= -\frac{\Delta_r V}{RT} \\ \Delta_r V &\approx 0 \implies \left( \frac{\partial K}{\partial p} \right)_T = 0 \end{aligned}$$

Still, the equilibrium's composition is not independent of the pressure.

### 4.13.2 Temperature dependence

$$\begin{aligned} \frac{\partial \ln K}{\partial \frac{1}{T}} &= -\frac{\Delta_r H^0}{R} \\ \ln \left( \frac{K_2}{K_1} \right) &= -\frac{\Delta_r H^0}{R} \left( \frac{1}{T_2} - \frac{1}{T_1} \right) \\ K_2 &= e^{\left( -\frac{\Delta_r H^0}{R} \left( \frac{1}{T_2} - \frac{1}{T_1} \right) \right)} \cdot K_1 \end{aligned}$$

## 4.14 Clausius-Clapeyron equation

$$\begin{aligned} \text{Clausius' equation} & \quad \frac{dp}{dT} = \frac{\Delta S_m}{\Delta V_m} \\ \text{Clausius-Clapeyron} & \quad \frac{dp}{dT} = \frac{\Delta H_m}{T \Delta V_m} \end{aligned}$$

### 4.14.1 Solid-liquid equilibrium

$$\begin{aligned} \frac{dp}{dT} &= \frac{\Delta_{fus} H_m}{\Delta V_{fus}} \frac{dT}{T} \\ p_2 &= p_1 + \frac{\Delta_{fus} H_m}{\Delta_{fus} V_m} \ln \left( \frac{T_2}{T_1} \right) \end{aligned}$$

### 4.14.2 Liquid-vapor equilibrium

Temperature dependence

$$\begin{aligned} \frac{dp}{dT} &= \frac{\Delta_{vap} H_m}{T \Delta_{vap} V_m} \\ d \ln p &= \frac{\Delta_{vap} H_m}{RT^2} dT \\ p_2 &= p_1 \cdot e^{\frac{\Delta_{vap} H_m}{RT^2} \left( \frac{1}{T_2} - \frac{1}{T_1} \right)} \end{aligned}$$

Pressure dependence

$$p = p^* \cdot e^{\left( \frac{V_{m, liq}}{RT} \Delta p \right)}$$

#### 4.14.3 Solid-vapor equilibrium

$$\begin{aligned}\frac{dp}{dT} &= \frac{\Delta_{sub}H_m}{T\Delta_{sub}V_m} \\ d\ln p &= \frac{\Delta_{sub}H_m}{RT^2}dT \\ p_2 &= p_1 \cdot e^{\frac{\Delta_{sub}H_m}{RT^2}\left(\frac{1}{T_2} - \frac{1}{T_1}\right)}\end{aligned}$$

## 5 Radiations

### 5.1 Bragg Equation

$$n\lambda = 2d_{hkl} \sin \theta$$