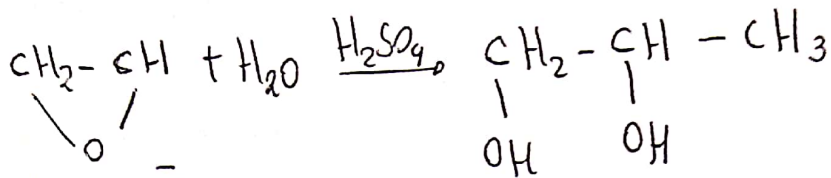


## Exemplo

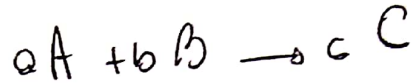
(2)

### Produção de propileno glicol



→ Declara reação

A = óxido de propileno



B = H<sub>2</sub>O

$$a = 1$$

C = propileno glicol

$$b = 1$$

M = metanol

$$c = 1$$

→ declarar infos

$$C_p A = 35 \text{ BTU/lbmol} \cdot ^\circ\text{F}$$

$$H_A^\circ(68^\circ\text{F}) = -66600 \text{ BTU/lbmol}$$

$$C_p B = 18 \quad "$$

$$C_p C = 46 \quad "$$

$$H_B^\circ(68^\circ\text{F}) = -123000$$

$$C_p M = 29.5 \quad "$$

$$H_C^\circ(68^\circ\text{F}) = -226000$$

→ Balanço molar

$$\text{CSTR} \quad V = \frac{\bar{F}_{\text{Ao}} \cdot X}{-r_A}$$

\* Desejo conversão

$$V \cdot (-r_A) = \bar{F}_{\text{Ao}} \cdot X$$

$$1. \quad f(x) \quad V \cdot (-r_A) - \bar{F}_{\text{Ao}} \cdot X = 0$$

$$X(0) = 0.8 \rightarrow \text{chute}$$

$$V = 40.1 \text{ ft}^3 \rightarrow 300 \text{ gal}$$

$$\bar{F}_{\text{Ao}} = 43.04 \text{ lbmol/h}$$

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2. Lei de velocidade

$$M_A = - (R \cdot C_A)$$

$$R = A \cdot \exp(-E/RT)$$

$$A = 16.96 \cdot 10^{12} \text{ h}^{-1}$$

$$E = 32400 \text{ BTU/lbmol}$$

$$R = 1.987 \text{ BTU/lbmol} \cdot ^\circ R$$

3. Estequiometria

Reação fase líquida

$$C_A = C_{A0} (1 - x)$$

$$C_{A0} = F_{A0} / v_0 \text{ lbmol/ft}^3$$

$$v_0 = v_{A0} + v_{B0} + v_{M0} \text{ ft}^3/\text{h}$$

$$v_{A0} = 46.62 \text{ ft}^3/\text{h}$$

$$v_{B0} = 233.1 \text{ ft}^3/\text{h}$$

$$v_{M0} = 46.62 \text{ ft}^3/\text{h}$$

4. Balanço de energia

adiabático, trabalho de eixo desprezível

$$f(T) = -F_{A0} \sum \alpha_i C_{pi} (T - T_0) - \Delta H_{Rx} \cdot F_{A0} \cdot X = 0$$

$$T(0) = 600 \text{ } ^\circ R$$

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$$\Delta H_{Rx} = \Delta \dot{H}_{Rx}^0(T_a) + \Delta C_p(T - T_a)$$

$$\Delta \dot{H}_{Rx}^0(T_a) = \frac{c}{a} \dot{H}_C^0 - \frac{b}{a} \dot{H}_B^0 - \dot{H}_A^0$$

$$\Delta C_p = \frac{c}{a} C_{pC} - \frac{b}{a} C_{pB} - C_{pA}$$

$$T_a = 528^\circ R \rightarrow 68^\circ F$$

$$T_o = 535^\circ R \rightarrow 75^\circ F$$

$$\sum Q_i p_i = C_{pA} + Q_B C_{pB} + Q_M C_{pM}$$

$$Q_B = \frac{F_{B0}}{F_{M0}}$$

$$Q_M = \frac{F_{M0}}{F_{M0}}$$

$$F_{B0} = 802.8 \text{ lbmol/h}$$

$$F_{M0} = 71.87$$

Inserindo a Serpentina

B. E

$$\frac{\dot{Q}}{\dot{F}_{H_2O}} - \sum \dot{Q}_i \cdot C_{p,i} (T - T_0) - \Delta H_{Rx} \cdot X = 0$$

$$Q = UA (T_a - T)$$

$$F(T) = \frac{UA}{\dot{F}_{H_2O}} \cdot (T_a - T) - X \cdot \Delta H_{Rx} - \sum \dot{Q}_i \cdot C_{p,i} (T - T_0)$$

$$T(0) = 600^\circ R$$

$$\frac{UA}{\dot{F}_{H_2O}} = \frac{(200 \times 40)}{\dot{F}_{H_2O}}$$

$$T_a = 545^\circ R$$