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Modified kalina system for efficient power and water production

Abstract

A new and innovative power and treated water co-generation system is provided that includes a modified Kalina cycle and a forward osmosis (FO) membrane. The Kalina cycle of the provided system is used for power production, whereas the system's FO process is used for water production. The provided system modifies a typical Kalina cycle to include a more efficient and relatively low-temperature heat source, while still utilizing the same working fluid, which is ammonia-water. The draw solution for the provided system's FO process is also ammonia-water, which is known and efficient for desalination and wastewater treatment. In some aspects, the working fluid of the system may be a specific ammonia-water composition including between 30-95% ammonia. The presently disclosed system combines the Kalina process and the FO process into an improved and innovative heat integration system to minimize energy requirements and enable operation at both small and large scales.

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Background/Summary

CROSS-REFERENCE TO RELATED APPLICATIONS (1) The present application is a National Stage filing under 35 U.S.C. 371 of International Application No. PCT/QA2021/050005, filed on Apr. 14, 2021 which claims priority to and the benefit of U.S. Provisional Application 63/009,566, filed Apr. 14, 2020, the entirety of which is herein incorporated by reference.

TECHNICAL FIELD

(1) The present application relates generally to the co-generation of power and fresh water. More specifically, the present application relates to a new and innovative power and treated water co-generation system that combines a Kalina cycle and a forward osmosis (FO) process.

BACKGROUND

(2) Low-grade waste heat cannot be used for steam production in a conventional steam cycle. An alternative way to generate electricity at low temperature is a conventional Kalina power system. A conventional Kalina power system process maximizes the power output with a better heat recovery and without the demand of additional fuels. In general, Organic Rankin cycle (ORC), supercritical Rankin cycle, and Kalina power cycle are typically the suitable thermal technologies for low-grade heat recovery.

(3) Due to the continuous demand for power and fresh water, an efficient and more economically feasible co-generation system than typical low-grade heat recovery systems is needed.

SUMMARY

(4) The present application provides a new and innovative hybrid Kalina system that includes a forward osmosis (FO) membrane. The Kalina cycle of the provided system is used for power production, whereas the system's FO process is used for water production. The provided system modifies a typical Kalina cycle to be more efficient and require a relatively low-temperature heat source, while still utilizing the same working fluid, which is ammonia-water. The draw solution for the provided system's FO process is also ammonia-water, which is known and efficient for desalination and wastewater treatment. In at least some aspects, the provided hybrid Kalina system uses a particular ammonia-water composition (between 30-95% ammonia). The presently disclosed system combines the Kalina process and the FO process into an improved and novel heat integration system to minimize energy requirements and ensure smooth operation at both small and large scales.

(5) In light of the disclosures herein, and without limiting the scope of the invention in any way, in a first aspect of the present disclosure, which may be combined with any other aspect listed herein unless specified otherwise, a power and treated water co-generation system includes a Kalina power turbine, a forward osmosis membrane, and a distillation column. The forward osmosis membrane is in fluid communication with the reject stream of the Kalina power turbine and with an untreated water stream such that the forward osmosis membrane receives the reject stream and the

untreated water stream and thereby forms a product stream and a brine stream. The distillation column is in fluid communication with the product stream of the forward osmosis membrane such that the distillation column receives the product stream and thereby forms a distillation column overhead stream and a distillation column bottom stream. The Kalina power turbine is in fluid communication with the distillation column overhead stream such that the Kalina power turbine receives the distillation column overhead stream and thereby produces power and forms the reject stream. A first portion of the distillation column bottom stream is in fluid communication with a storage tank.

(6) In a second aspect of the present disclosure, which may be combined with any other aspect listed herein unless specified otherwise, a working fluid of the Kalina power turbine is an ammonia-water mixture including ammonia in a range of 30-95% of the composition.

(7) In a third aspect of the present disclosure, which may be combined with any other aspect listed herein unless specified otherwise, the power and treated water co-generation system includes a fluid pump in fluid communication with the product stream and arranged to pump the product stream to the distillation column.

(8) In a fourth aspect of the present disclosure, which may be combined with any other aspect listed herein unless specified otherwise, the power and treated water co-generation system includes an economizer in fluid communication with a second portion of the distillation column bottom stream. The economizer is configured to heat the second portion of the distillation column bottom stream, and the heated second portion of the distillation column bottom stream is directed to the distillation column.

(9) In a fifth aspect of the present disclosure, which may be combined with any other aspect listed herein unless specified otherwise, the power and treated water co-generation system includes an economizer in fluid communication with the distillation column overhead stream, the economizer configured to heat the distillation column overhead stream.

(10) In a sixth aspect of the present disclosure, which may be combined with any other aspect listed herein unless specified otherwise, the first portion of the distillation column bottom stream is arranged to exchange heat with the distillation column overhead stream thereby heating the distillation column overhead stream.

(11) In a seventh aspect of the present disclosure, which may be combined with any other aspect listed herein unless specified otherwise, the product stream is split into a first product stream and a second product stream prior to the distillation column receiving the product stream.

(12) In an eighth aspect of the present disclosure, which may be combined with any other aspect listed herein unless specified otherwise, the first portion of the distillation column bottom stream is arranged to exchange heat with the second product stream thereby cooling the first portion of the distillation column bottom stream.

(13) In a ninth aspect of the present disclosure, which may be combined with any other aspect listed herein unless specified otherwise, the reject stream of the Kalina power turbine is arranged to exchange heat with the first product stream thereby cooling the reject stream. The forward osmosis membrane is in fluid communication with the cooled reject stream.

(14) In a tenth aspect of the present disclosure, which may be combined with any other aspect listed herein unless specified otherwise, the first product stream and the second product stream join into a third product stream, the distillation column being in fluid communication with the third product stream.

(15) In an eleventh aspect of the present disclosure, which may be combined with any other aspect listed herein unless specified otherwise, the untreated water stream is in fluid communication with a source of seawater or wastewater.

(16) In a twelfth aspect of the present disclosure, which may be combined with any other aspect listed herein unless specified otherwise, a method for power and treated water co-generation includes contacting a forward osmosis membrane with a reject stream of a Kalina power turbine

and a untreated water stream thereby forming a product stream and a brine reject stream. The product stream is distilled with a distillation column thereby forming a distillation column bottom stream and a distillation column overhead stream. The distillation column overhead stream is expanded with the Kalina power turbine thereby producing power and forming the reject stream. A portion of the distillation column bottom stream is directed to a storage tank, the portion of the distillation column bottom stream being treated water.

(17) In a thirteenth aspect of the present disclosure, which may be combined with any other aspect listed herein unless specified otherwise, the forward osmosis membrane is contacted concurrently with the reject stream of a Kalina power turbine and the untreated water stream.

(18) In a fourteenth aspect of the present disclosure, which may be combined with any other aspect listed herein unless specified otherwise, the reject stream of the Kalina power turbine that the forward osmosis membrane is contacted with is a mixture including ammonia and water.

(19) In a fifteenth aspect of the present disclosure, which may be combined with any other aspect listed herein unless specified otherwise, the mixture includes ammonia in the range of 30-95% of the composition.

(20) In a sixteenth aspect of the present disclosure, which may be combined with any other aspect listed herein unless specified otherwise, the product stream formed by the forward osmosis membrane includes a lower concentration of ammonia than the reject stream.

(21) In a seventeenth aspect of the present disclosure, which may be combined with any other aspect listed herein unless specified otherwise, the untreated water stream is saline water.

(22) In an eighteenth aspect of the present disclosure, which may be combined with any other aspect listed herein unless specified otherwise, the method includes only an inorganic working fluid.

(23) In a nineteenth aspect of the present disclosure, which may be combined with any other aspect listed herein unless specified otherwise, the method further includes exchanging heat between the distillation column overhead stream and the portion of the distillation column bottom stream thereby heating the distillation column overhead stream and cooling the portion of the distillation column bottom stream. The heated distillation column overhead stream is heated with an economizer. Heat may be exchanged between the cooled portion of the distillation column bottom stream and a portion of the product stream thereby cooling the cooled portion of the distillation column bottom stream.

(24) In a twentieth aspect of the present disclosure, which may be combined with any other aspect listed herein unless specified otherwise, the method further includes reboiling and a portion of the distillation column bottom stream

(25) Additional features and advantages of the disclosed system and method are described in, and will be apparent from, the following Detailed Description and the Figures. The features and advantages described herein are not all-inclusive and, in particular, many additional features and advantages will be apparent to one of ordinary skill in the art in view of the figures and description. Moreover, it should be noted that the language used in the specification has been principally selected for readability and instructional purposes, and not to limit the scope of the inventive subject matter.

Description

BRIEF DESCRIPTION OF THE DRAWINGS

(1) FIG. 1 illustrates a schematic flow diagram of a conventional Kalina power system.

(2) FIG. 2 illustrates a table of the mass and heat balance of a conventional Kalina power system.

(3) FIG. 3 illustrates a table of turbine process parameters of a conventional Kalina power system.

(4) FIG. 4 illustrates a schematic flow diagram of a system for the co-generation of power and

treated water, according to an aspect of the present disclosure.

DETAILED DESCRIPTION

(5) The present application provides a new and innovative hybrid system and method for the co-generation of power and treated water. The provided system includes a modified Kalina system for generating power and a forward osmosis system for generating treated water. The modified Kalina system and forward osmosis system are integrated in the provided system in a way that enables heat integration to minimize energy requirements of the provided hybrid system thereby enabling operation at both small and large scales. For instance, the provided system overcomes a bottleneck of the typical Kalina power system by reducing the temperature required of a heat source as compared to a typical Kalina power system. Stated differently, the provided system enables using a low-temperature grade heat source as compared to a high-temperature grade heat source. Further, the provided system overcomes a bottleneck of the typical forward osmosis system by reducing the draw solution regeneration energy consumption for water treatment as compared to typical forward osmosis systems. In at least some instances, the provided system may consume about 15% less energy for the same amount of production (e.g., 15% more efficient) as compared to typical Kalina power systems and forward osmosis systems.

(6) The configuration of the provided system is enabled by utilizing the same fluid (e.g., an ammonia-water mixture) for the Kalina turbine's working fluid as the forward osmosis membrane's draw solution. Additionally, some typical Kalina turbines may use an ammonia-water working fluid and some typical forward osmosis system may use an ammonia-water draw solution. As such, the provided system may be implemented by constructing new power plants or by modifying existing power plants.

(7) An additional advantage of the provided method is that it only includes an inorganic working fluid, and is therefore an oil-free process. The oil-free nature of the provided method eliminates the risk of contamination, reduces environmental impact, reduces maintenance costs, and reduces energy costs.

(8) Various components of the presently disclosed system may be in fluid communication with one another, such as through piping. Two components in fluid communication with one another may be in direct fluid communication (e.g., piping directly connects the two components) or may have intermediate components or processing between the two components, such as filters, pumps, heaters, odor removal vessels, etc.

(9) FIG. 1 illustrates a schematic of a conventional Kalina power system **100** that includes a separator **102**, a turbine **104**, a low-temperature regenerator (LTRGN) (not illustrated), a T-junction **106**, a pump **116**, multiple heat exchangers **108-114**, a throttle valve (not illustrated), and a heat source (e.g., streams **172**, **174**, **176**). Superheated vapor in the stream **150** expands in the turbine **104** to form the output stream **152** and to produce power. The output stream **152** is directed to the T-junction **106**, which may mix the output stream **152** with makeup working fluid to compensate for the fluid loss from the turbine **104** and form the stream **156**. The stream **156** exchanges heat with a stream **166** at the heat exchanger **108** thereby cooling the stream **156** into the stream **158** and heating the stream **166** into the stream **168**. The cooled stream **158** is further cooled at the heat exchanger **110** into the stream **164**. An input stream **160** and output stream **162** of cold water are in fluid communication with the heat exchanger **110** to effect the cooling. The stream **164** is input into the pump **116** which outputs the stream **166**. Cooling the output stream **152** at the heat exchanger **108** while heating the pumped fluid in the stream **166** at the heat exchanger **108** is part of a thermodynamic cycle. The LTRGN reduces the load on the heat exchanger **108**. Similarly, a high-temperature regenerator (HTRGN) (not illustrated) also reduces the load on the heat exchanger **108**. The LTRGN and HTRGN components internally recover the heat and increase the cycle thermal efficiency.

(10) The stream **168** is further heated at the heat exchanger **114** into the stream **170** via heat supplied by the stream **174**. The stream **170** is fed to the separator **102** which thereby physically

separates the stream **170** into an overhead stream **180** and a bottom stream **178**. The separator **102** utilizes gravity to cause a denser fluid (i.e. liquid) to settle to the bottom of the separator **102** to be withdrawn as the bottom stream **178** and to cause a less dense fluid (i.e. vapor) to be withdrawn from the top of the separator **102** as the overhead stream **180**. The separator **102** may be referred to as a flash drum. The overhead stream is heated at the heat exchanger **112** into the stream **150** via heat supplied by the stream **172**. The stream **150** is then recycled back to the turbine **104**. The arrangement of the components in the conventional Kalina power system **100** requires that the heat source (e.g., the streams **172**, **174**, **176**) supplied to the heat exchanger **112** be a high-temperature heat source to sufficiently heat the recycled stream **150** for input into the turbine **104**. As such, this high-temperature heat source is a bottleneck of the conventional Kalina power system **100**.

(11) The conventional low-temperature Kalina power system **100** operates with a temperature at the separator **102** of about 110° C. to 150° C., with about 20% to 80% vapor fraction, and with about 0.85-0.97 turbine concentration. The mass and heat balance of a conventional Kalina power system **100** is shown in the table illustrated in FIG. 2. Turbine process parameters of a conventional Kalina power system **100** are shown in the table illustrated in FIG. 3. Pumping power requirements of a conventional Kalina power system **100** are typically about 3.261 kW. Stated differently, the specific power consumption of a conventional Kalina power system **100** is typically about 115 kW/kg.

(12) FIG. 4 illustrates a schematic flow diagram of an example system **400** for the co-generation of power and treated water. In at least one example, the system **400** may be located in a power plant. The example system **400** modifies the conventional Kalina power system **100** in part by including an arrangement of components that combine a Kalina cycle with a forward osmosis process in order to co-generate power and treated water. The Kalina cycle is a thermodynamic process for converting thermal energy into usable mechanical power that uses a solution of two fluids with different boiling points for its working fluid. Forward osmosis is the process of spontaneous water diffusion across a semi-permeable forward osmosis membrane in response to a difference in solute concentrations (i.e. osmotic pressures) on either side of the semi-permeable membrane. Untreated (e.g., contaminated) water may enter the semi-permeable forward osmosis membrane on one side (e.g., the feed side) and treated (e.g., decontaminated or fresh) water mixed with a draw solution may exit on the other side (e.g., the draw side) of the membrane. The treated water must then be separated from the draw solutes to obtain the treated water as a final product. To effect the combination, the example system **400** includes a forward osmosis (FO) membrane **402**, a distillation column **404**, and a turbine **406** all in fluid communication with one another.

(13) The turbine **406** may be a suitable turbine for use in a Kalina cycle. For example, the turbine **406** may be a typical back-pressure turbine.

(14) The FO membrane **402** may be any suitable membrane for use in a forward osmosis process. For instance, the FO membrane **402** may be semi-permeable. In various examples, the FO membrane **402** may be a cellulosic membrane (e.g., an asymmetric cellulose acetate membrane or asymmetric cellulose triacetate membrane), a polyamide-based thin film composite membrane, a thin film composite polyelectrolyte-based membrane, or another suitable forward osmosis membrane.

(15) The FO membrane **402** is in fluid communication with a suitable source of untreated water (not illustrated), such as for example, a source of saline water (e.g., seawater) or a source of waste water. An untreated water stream **452** may be directed from the source of untreated water to the FO membrane **402**. The FO membrane **402** is also in fluid communication with the turbine **406**. A reject stream **488** of the turbine **406** may be directed to the FO membrane **402** as the draw solution for the FO membrane **402**. As will be described more below, in some aspects, the reject stream **488** may be cooled to the reject stream **456**, which is then the draw solution that contacts the FO membrane **402**. Stated differently, in such aspects, a cooled reject stream **488** of the turbine **406** is the draw solution for the FO membrane **402**.

(16) In at least some aspects, the FO membrane **402** may be contacted concurrently by the draw

solution (e.g., the reject stream **456**) and by the untreated water stream **452** thereby forming a brine/waste stream **454** and a product stream **458**. The FO membrane **402** may filter contaminants from the untreated water stream **452** which are then included in the brine/waste stream **454**. For example, the FO membrane **402** may filter salt to desalinate high saline water. In some instances, the untreated water stream **452** may be heated or cooled (e.g., via a heat exchanger) prior to contacting the FO membrane **402** if the temperature of the untreated water stream **452** is not suitable for the FO membrane **402** to function effectively. For example, an FO membrane **402** typically functions effectively at temperatures less than 40° C. and an untreated water stream **452** may exceed that temperature during certain times of the year in certain areas of the world. In an example, the untreated water stream **452** may be about 25° C. when it contacts the FO membrane **402**.

(17) In at least some instances, the working fluid of the turbine **406** is an ammonia-water mixture. In such aspects, the reject stream **456** of the turbine **406**, and thereby the draw solution of the FO membrane **402**, is the same ammonia-water mixture. The ammonia-water mixture may, in some examples, include a concentration of ammonia in a range of 30-95% of the mixture. In such aspects, the working fluid of the turbine **406** and the fluid within the system **400** is therefore inorganic and oil free, which can be beneficial for environmental sustainability.

(18) In at least some aspects, brine/waste stream **454** may be directed to an area of the power plant in which the system **400** is located for disposal. For instance, the FO membrane **402** may be in fluid communication with a storage tank and the brine/waste stream **454** may be directed to the storage tank for later disposal. The product stream **458** is a diluted draw solution stream that includes a lower concentration of ammonia than the reject stream **456**. Stated differently, the product stream **458** is a less contaminated untreated water stream **452** that includes a mixture of treated (e.g., decontaminated or fresh) water and ammonia solutes from the reject stream **456**. The treated water may be separated from the ammonia solutes at the distillation column **404**.

(19) In various aspects, the FO membrane **402** may be in fluid communication with a pump **408**. In such aspects, the pump **408** may be in fluid communication with the distillation column **404**. The product stream **458** may be directed to the pump **408** that pumps the product stream **458** and outputs a product stream **460**. In some examples, the product stream **460** may be at a temperature of about 30-35° C.

(20) In at least some aspects, the product stream **460** may split into a product stream **462** and a product stream **468** at the split **422**. The heat integration that may be provided by the product stream **462** and the product stream **468** will be described more below. In such aspects, these streams may rejoin at the split **424** into the product stream **466** which is directed to the distillation column **404**.

(21) The distillation column **404** is configured to generate an overhead stream **450** and a bottom stream **472** from a feed stream (e.g., the product stream **466**). As compared to the separator **102** that utilizes gravitational separation, the distillation column **404** separates the product stream **466** into its components based on the difference in volatilities (e.g., boiling points) between the components. The bottom stream **472** may be treated (e.g., decontaminated or fresh) water whereas the overhead stream **450** may be a mixture of water and ammonia. In this way, the distillation column **404** adjusts the ammonia-water mixture in the product stream **466** for Kalina expansion in the turbine **406** (e.g., the overhead stream **450**) while also filtering water in the product stream **466** from any traces of ammonia to generate treated water (e.g., the bottom stream **472**).

(22) In at least some aspects, a portion of the bottom stream **472** may be reboiled. In such aspects, the distillation column **404** may be in fluid communication with an economizer **416** and a portion of the bottom stream **472** may be directed to the economizer **416**. For instance, the bottom stream **472** may be split into the bottom stream **474** and the bottom stream **478**, and the bottom stream **474** may be directed to the economizer **416**. The economizer **416** may boil the bottom stream **474** and inject vapor as the stream **476** into the distillation column **404** to drive separation in the distillation

column **404**. The treated water of the bottom stream **478** may be directed to a storage tank **426** for storing treated/fresh water.

(23) The heat supplied to the economizer **416** to boil the bottom stream **474** can be supplied by any suitable low-temperature grade heat source (not illustrated). In at least some aspects, the low-temperature grade heat source supplies heat to the economizer **416** at a temperature of around 95° C. For example, heat may be supplied by a slip stream (e.g., a low-pressure steam) of a power plant turbine, a solar collector, waste heat generated by a production plant (e.g., cement, iron, steel, ceramics, petrochemical, etc.), or flue gas from an incinerator. The use of a low-temperature grade heat source helps reduce the energy consumption of the system **400** as compared to the conventional Kalina power system **100** that requires a high-temperature grade heat source as described above.

(24) As stated above, the distillation column **404** is in fluid communication with the turbine **406**. The overhead stream **450** is directed to the turbine **406** thereby recycling the working fluid (e.g., ammonia-water mixture) of the turbine **406** back to the turbine **406**. In at least some aspects, the overhead stream **450** may be heated by an economizer **420** to the overhead stream **486** to prepare the overhead stream **450** for expansion in the turbine **406**. In one example, the economizer **420** may heat the overhead stream **450** such that the overhead stream **486** is at a temperature of about 90° C. The heat supplied to the economizer **420** can be supplied by any suitable low-temperature grade heat source (not illustrated). In at least some aspects, the low-temperature grade heat source supplies heat to the economizer **420** at a temperature of around 95° C. For example, heat may be supplied by a slip stream (e.g., a low-pressure steam) of a power plant turbine, a solar collector, waste heat generated by a production plant (e.g., cement, iron, steel, ceramics, petrochemical, etc.), or flue gas from an incinerator. The use of a low-temperature grade heat source helps reduce the energy consumption of the system **400** as compared to the conventional Kalina power system **100** that requires a high-temperature grade heat source as described above.

(25) The turbine **406** may then produce power using, at least in part, the working fluid from the overhead stream **450**. The power produced by the turbine **406** may be directed to where it is needed or to storage. As part of the power production process, the turbine **406** may generate the reject stream **488** that is directed to the FO membrane **402** to be used as draw solution for the FO membrane **402**.

(26) In at least some aspects, the components and streams of the system **400** may be arranged to provide heat integration that reduces the energy consumption of the system **400**. For instance, the FO membrane **402** typically functions effectively at temperatures less than 40° C., though the reject stream **488** of the turbine **406** is above 40° C. In at least some examples, the product stream **468**, which may be at a temperature of about 30-35° C., may exchange heat with the reject stream **488** at a heat exchanger **412** to cool the reject stream **488** to the reject stream **456** and to heat the product stream **468** to the product stream **470**. The reject stream **488** may be cooled such that the reject stream **456** is at a temperature less than 40° C. when it contacts the FO membrane **402**. Cooling the reject stream **456** in this way helps avoid the need for external coolants in the system **400**, which aids in environmental sustainability efforts. Heating the product stream **468** in this way helps increase the temperature of the feed stream (e.g., the heated product stream **470** joins into the product stream **466** at the split **424**) to the distillation column **404**, which can help reduce the energy required for driving separation in the distillation column **404**. For instance, the energy of the heat source required at the economizer **416** may be reduced.

(27) In at least some aspects, the distillation column **404** includes a heat integration system in an overhead condenser section of the distillation column **404**. For instance, the bottom stream **478**, which may be at a temperature of about 90° C., may exchange heat with the overhead stream **450** at a heat exchanger **418** to cool the bottom stream **478** to the bottom stream **480** and to heat the overhead stream **450** to the overhead stream **484**. In at least some aspects, the bottom stream **480** may further exchange heat with the product stream **462** at a heat exchanger **414** to cool the bottom

stream **480** to the bottom stream **482** and to heat the product stream **462** to the product stream **464**. The bottom stream **482** may be at about room temperature (e.g., about 20-22° C.). Cooling the bottom stream **478** in this way helps avoid the need for external coolants in the system **400**, which aids in environmental sustainability efforts. Heating the product stream **462** in this way helps increase the temperature of the feed stream (e.g., the heated product stream **464** joins into the product stream **466** at the split **424**) to the distillation column **404**, which can help reduce the energy required for driving separation in the distillation column **404**. For instance, the energy of the heat source required at the economizer **416** may be reduced.

(28) Additionally, heating the overhead stream **450** at the heat exchanger **418** to the overhead stream **484** prior to the economizer **420** helps reduce the energy required at the economizer **420** to heat the overhead stream **484** to the about 90° C. of the overhead stream **486**. For instance, the heat exchange at the heat exchanger **418** heats the overhead stream **450** partway and therefore the economizer **420** has to effect less of a temperature increase from the overhead stream **484** to the overhead stream **486**.

(29) In addition, by using the reject stream **456** (e.g., the heated reject stream **488**) as the draw solution to the FO membrane **402**, the provided system **400** reduces the energy consumption to regenerate the draw solution as compared to typical forward osmosis systems.

(30) In the preceding description and in FIG. **4**, various streams have been split into multiple reference numerals for purposes of describing different portions of the system **400**. It should be appreciated where a single stream has been split merely for descriptive purposes. For example, the overhead stream **486** is a heated overhead stream **484** which is a heated overhead stream **450**. As such, the overhead stream **450** is directed from the distillation column **404** to the turbine **406**. In another example, the product stream **470** is a heated product stream **468**, and the product stream **464** is a heated product stream **462**, which then join into the product stream **466**. As such, the product stream **466** is a heated product stream **460** which is a pumped product stream **458**. In another example, the bottom stream **482** is a cooled bottom stream **480** which is a cooled bottom stream **478** which is a portion of the bottom stream **472**. As such, a portion of the bottom stream **472** may be in fluid communication with a storage tank **426**.

(31) As used herein, “about,” “approximately” and “substantially” are understood to refer to numbers in a range of numerals, for example the range of -10% to +10% of the referenced number, preferably -5% to +5% of the referenced number, more preferably -1% to +1% of the referenced number, most preferably -0.1% to +0.1% of the referenced number.

(32) Furthermore, all numerical ranges herein should be understood to include all integers, whole or fractions, within the range. Moreover, these numerical ranges should be construed as providing support for a claim directed to any number or subset of numbers in that range. For example, a disclosure of from 1 to 10 should be construed as supporting a range of from 1 to 8, from 3 to 7, from 1 to 9, from 3.6 to 4.6, from 3.5 to 9.9, and so forth.

(33) Without further elaboration, it is believed that one skilled in the art can use the preceding description to utilize the claimed inventions to their fullest extent. The examples and aspects disclosed herein are to be construed as merely illustrative and not a limitation of the scope of the present disclosure in any way. It will be apparent to those having skill in the art that changes may be made to the details of the above-described examples without departing from the underlying principles discussed. In other words, various modifications and improvements of the examples specifically disclosed in the description above are within the scope of the appended claims. For instance, any suitable combination of features of the various examples described is contemplated.

Claims

1. A power and treated water co-generation system comprising: a Kalina power turbine; a forward osmosis membrane in fluid communication with a reject stream of the Kalina power turbine and

with an untreated water stream such that the forward osmosis membrane receives the reject stream and the untreated water stream and thereby forms a product stream and a brine stream; a distillation column in fluid communication with the product stream of the forward osmosis membrane such that the distillation column receives the product stream and thereby forms a distillation column overhead stream and a distillation column bottom stream, wherein the Kalina power turbine is in fluid communication with the distillation column overhead stream such that the Kalina power turbine receives the distillation column overhead stream and thereby produces power and forms the reject stream, and wherein a first portion of the distillation column bottom stream is in fluid communication with a storage tank.

2. The power and treated water co-generation system of claim 1, wherein a working fluid of the Kalina power turbine is an ammonia-water mixture including ammonia in a range of 30-95% of the composition.

3. The power and treated water co-generation system of claim 1, further comprising a fluid pump in fluid communication with the product stream and arranged to pump the product stream to the distillation column.

4. The power and treated water co-generation system of claim 1, further comprising an economizer in fluid communication with a second portion of the distillation column bottom stream, the economizer configured to heat the second portion of the distillation column bottom stream, wherein the heated second portion of the distillation column bottom stream is directed to the distillation column.

5. The power and treated water co-generation system of claim 1, further comprising an economizer in fluid communication with the distillation column overhead stream, the economizer configured to heat the distillation column overhead stream.

6. The power and treated water co-generation system of claim 1, wherein the first portion of the distillation column bottom stream is arranged to exchange heat with the distillation column overhead stream thereby heating the distillation column overhead stream.

7. The power and treated water co-generation system of claim 1, wherein the product stream is split into a first product stream and a second product stream prior to the distillation column receiving the product stream.

8. The power and treated water co-generation system of claim 7, wherein the first portion of the distillation column bottom stream is arranged to exchange heat with the second product stream thereby cooling the first portion of the distillation column bottom stream.

9. The power and treated water co-generation system of claim 7, wherein the reject stream of the Kalina power turbine is arranged to exchange heat with the first product stream thereby cooling the reject stream, the forward osmosis membrane being in fluid communication with the cooled reject stream.

10. The power and treated water co-generation system of claim 7, wherein the first product stream and the second product stream join into a third product stream, the distillation column being in fluid communication with the third product stream.

11. The power and treated water co-generation system of claim 1, wherein the untreated water stream is in fluid communication with a source of seawater or wastewater.

12. A method for power and treated water co-generation comprising: contacting a forward osmosis membrane with a reject stream of a Kalina power turbine and a untreated water stream thereby forming a product stream and a brine reject stream; distilling the product stream with a distillation column thereby forming a distillation column bottom stream and a distillation column overhead stream; expanding the distillation column overhead stream with the Kalina power turbine thereby producing power and forming the reject stream; and directing a portion of the distillation column bottom stream to a storage tank, the portion of the distillation column bottom stream being treated water.

13. The method for power and treated water co-generation of claim 12, wherein the forward

- osmosis membrane is contacted concurrently with the reject stream of a Kalina power turbine and the untreated water stream.
14. The method for power and treated water co-generation of claim 12, wherein the reject stream of the Kalina power turbine that the forward osmosis membrane is contacted with is a mixture including ammonia and water.
15. The method for power and treated water co-generation of claim 14, wherein the mixture includes ammonia in the range of 30-95% of the composition.
16. The method for power and treated water co-generation of claim 14, wherein the product stream formed by the forward osmosis membrane includes a lower concentration of ammonia than the reject stream.
17. The method for power and treated water co-generation of claim 12, wherein the untreated water stream is saline water.
18. The method for power and treated water co-generation of claim 12, wherein the method includes only an inorganic working fluid.
19. The method for power and treated water co-generation of claim 12, further comprising: exchanging heat between the distillation column overhead stream and the portion of the distillation column bottom stream thereby heating the distillation column overhead stream and cooling the portion of the distillation column bottom stream; heating the heated distillation column overhead stream with an economizer; and exchanging heat between the cooled portion of the distillation column bottom stream and a portion of the product stream thereby cooling the cooled portion of the distillation column bottom stream.
20. The method for power and treated water co-generation of claim 12, further comprising reboiling a portion of the distillation column bottom stream.
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