

Spherically Inward Propagating Flame of Type Ia Supernova

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1. Introduction

Supernova represent the catastrophic explosions that mark the end of the life of some stars. The ejected mass is of order 1 to 10 solar masses with bulk velocities ranging from a few thousand to a few tens of thousands of km/s.¹ The traditional single Chandrasekhar mass C–O White Dwarf burning is still considered to be responsible for a large population of type Ia supernova (SN Ia). Specifically, one of the key issues in its modeling is related to the flame acceleration and deflagration-detonation transition (DDT), with flame front instabilities being considered as a possible mechanism in driving the acceleration. The perspective of this proposal is to give a set of solutions of this problem. The milestones of this project are planed to be:

- (a) Complete a set of code that can solve the 1D H_2-O_2 flame.
- (b) Complete a set of code that can solve the simplest reacting flow in SN Ia conditions.
- (c) Try to observe spherical flame acceleration with large Lewis number curvature effect.
- (d) Try to observe pulsation in Xing & Zhao's case.
- (e) Try to observe deflagration-detonation transition (DDT) in (d).

2. Basic Equations

2.1 Planar flame

- Governing equations for 1-dimensional, Cartesian coordinates, compressible and non-viscous reacting flow are:

$$\frac{\partial \mathbf{U}}{\partial t} + \frac{\partial \mathbf{F}(\mathbf{U})}{\partial x} = \frac{\partial \mathbf{D}(\mathbf{U})}{\partial x} + \mathbf{S}$$

where \mathbf{U} is the conserved variables vector, \mathbf{F} is the flux vector, \mathbf{D} is the diffusion flux, and \mathbf{S} is the source term vector. The vectors are given by:

$$\mathbf{U} = \begin{bmatrix} \rho \\ \rho u \\ \rho E \\ \rho Y \end{bmatrix}, \quad \mathbf{F}(\mathbf{U}) = \begin{bmatrix} \rho u \\ \rho u^2 + p \\ \rho u(E + p/\rho) \\ \rho u Y \end{bmatrix}, \quad \mathbf{D}(\mathbf{U}) = \begin{bmatrix} 0 \\ 0 \\ \frac{\mu C_p}{Pr} \frac{\partial T}{\partial x} + \frac{\mu Q}{Sc} \frac{\partial Y}{\partial x} \\ \frac{\mu}{Sc} \frac{\partial Y}{\partial x} \end{bmatrix}, \quad \mathbf{S} = \begin{bmatrix} 0 \\ 0 \\ 0 \\ \rho \omega \end{bmatrix}$$

Here ρ is density, u is velocity, E is the total energy per unit mass and Y is the reactant mass fraction, respectively. The total energy is consisted by internal energy, kinetic energy and the "chemical" energy in reactant:

$$\rho E = \rho e + \frac{1}{2} \rho u^2 + \rho Q Y$$

The viscosity $\mu = \rho \nu$

The Schmidt number $Sc = \nu/D = \mu/\rho D$

The Prandtl number $Pr = \nu/\alpha = \mu c_p/\lambda$

The enthalpy per unit mass $H = E + p/\rho$

The heat value part might need to be put in internal energy part

- In the scenario of methane flame, the internal energy per unit mass is given by:

$$e = \frac{p}{\rho(\gamma - 1)} = \frac{R_u T}{\gamma - 1}$$

and the reaction rate is

$$\omega = -KY \exp(-E_a/R_u T)$$

- In the scenario of supernova flame, the internal energy is described by the equation of state of the relativistic degenerate electron gas ²:

$$e(\rho, T) = \frac{3}{4\rho} (3\pi^2)^{\frac{1}{3}} \hbar c_1 (\rho N)^{\frac{4}{3}} + \frac{1}{2} N \frac{(3\pi^2)^{\frac{2}{3}}}{3\hbar c_1} \left(\frac{1}{\rho N} \right)^{\frac{1}{3}} (kT)^2$$

With pressure being $p = \rho e/3$, one can get the form as: (constant $\gamma = 4/3$)

$$e = \frac{p}{\rho(4/3 - 1)} = \frac{p}{\rho(\gamma - 1)}$$

The reaction rate is adopted from the rate of Carbon-Carbon nuclear reaction ³:

$$\omega = AY^2 \exp\left(-E_a/T_9^{\frac{1}{3}}\right)$$

where $T_9 = T/10^9$ and $E_a = 84.165$ for C12-C12 reaction.

N is Carbon's electron density

c_1 is the light speed in vacuum

\hbar is the reduced Plank constant

2.2 Spherical flame

- In spherical coordinates, the governing equations change to be:

$$\frac{\partial \mathbf{U}}{\partial t} + \frac{1}{r^2} \frac{\partial r^2 \mathbf{F}(\mathbf{U})}{\partial r} = \frac{1}{r^2} \frac{\partial r^2 \mathbf{D}(\mathbf{U})}{\partial r} + \mathbf{S}$$

or in the expanded form:

$$\frac{\partial \mathbf{U}}{\partial t} + \frac{\partial \mathbf{F}(\mathbf{U})}{\partial r} + \frac{2}{r} \mathbf{F}(\mathbf{U}) = \frac{\mathbf{D}(\mathbf{U})}{\partial r} + \frac{2}{r} \mathbf{D}(\mathbf{U}) + \mathbf{S}$$

with the vectors being:

$$\mathbf{U} = \begin{bmatrix} \rho \\ \rho u \\ \rho E \\ \rho Y \end{bmatrix}, \quad \mathbf{F}(\mathbf{U}) = \begin{bmatrix} \rho u \\ \rho u^2 + p \\ \rho u H \\ \rho u Y \end{bmatrix}, \quad \mathbf{D}(\mathbf{U}) = \begin{bmatrix} 0 \\ 0 \\ \lambda \frac{\partial T}{\partial r} + \rho Q D \frac{\partial Y}{\partial r} \\ \rho D \frac{\partial Y}{\partial r} \end{bmatrix}, \quad \mathbf{S} = \begin{bmatrix} 0 \\ \frac{2p}{r} \\ 0 \\ \rho \omega \end{bmatrix}$$

2.3 Parameters for H_2 - O_2 flame

- Reference state ($H_2 : O_2 = 2 : 1$), examined in [tools/test h2o2 flame.py](#)
 - pressure $p_0 = 1.013 \times 10^5$ [Pa]
 - specific gas constant $R_u = 692.25$ [J/kg/K]
 - temperature $T_0 = 300$ [K]
 - density $\rho_0 = p_0 / R_u T_0 = 0.4879$ [kg/m³]
 - heat capacity ratio $\gamma = 1.4$
 - velocity $u_0 = \sqrt{R_u T_0} = 455.7$ m/s ($S_L \approx 10$ m/s)
 - flame thickness $\delta_f \approx 1$ mm = 1×10^{-3} m
 - time scale $t_0 = \delta_f / u_0 = 1.1 \times 10^{-6}$ [s]
 - heat value $Q \approx 36 R_u T_0$ [J/kg] (300K->3076K)
 - thermal conductivity $\lambda \approx 0.3$ [W/m/K]
 - thermal diffusivity $\alpha \approx 1.5 \times 10^{-3}$ [m²/s]
 - Lewis number $Le \approx 1.2$
 - activation energy $Ea \approx 27 R_u T_0$
 - pre-exponential factor $A \approx 2 \times 10^7$?

3. Dimensionless Equations

3.1 References variables

Dimensionless variables	Reference values
$\hat{\rho} = \frac{\rho}{\rho_0}$	$\rho_0 = 3.5 \times 10^{10} \text{ kg/m}^3$
$\hat{u} = \frac{u}{u_0}$	$u_0 = 7.871 \times 10^6 \text{ m/s}, S_L = 466 \text{ m/s}$ (laminar flame speed)
$r = \frac{\hat{r}}{\hat{r}_0}$	$r_0 = \delta_f = \frac{\lambda}{\rho_0 C_p S_t} = 9 \times 10^{-4} \text{ m}$
$\hat{t} = \frac{t}{t_0}$	$t_0 = \frac{r_0}{u_0} = 1.143 \times 10^{-10} \text{ s}$
$\hat{T} = \frac{T}{T_b - T_0}$	$T_0 = 1 \times 10^8 \text{ K}; T_b = 3.2 \times 10^9 \text{ K}$
$\hat{p} = \frac{p}{p_0}$	$p_0 = \rho_0 u_0^2$
$\hat{E} = \frac{E}{p_0/\rho_0} = \frac{E}{u_0^2}$	$e(\rho_0, T_b) = 6.1952 \times 10^{13} \text{ J/kg}$
$\hat{Y} = \frac{Y}{Y_0}$	$Y_0 = 1$
$\hat{\omega} = \frac{\omega}{\omega_0}$	$\rho_0 \omega_0 \delta_f = \rho_0 Y_0 S_t, \omega_0 = \frac{Y_0 u_0}{r_0} \frac{S_t}{u_0}$
$\hat{\alpha} = \frac{\alpha}{u_0 r_0}$	$\hat{D} = \frac{\hat{\alpha}}{Le} = \frac{2}{3} \frac{1}{Le}$
$\hat{Q} = \frac{Q}{u_0^2}$	$\hat{Q} = 0.904$
$\hat{\lambda} = \lambda / (\frac{\rho_0 r_0 u_0^3}{T_b - T_0})$	$\hat{\lambda} = \frac{S_t}{u_0} \frac{C_p (T_b - T_0)}{u_0^2} = 0.14541$

Laminar flame speed: $S_L = 466 \text{ m/s}$

Turbulent flame speed: S_t , assumed to be equal to the speed of sound at burnt state

Therefore, the dimensionless equation can be obtained from: (use planar equation for demonstration)

$$\begin{aligned}
\frac{\partial \rho}{\partial t} + \frac{\partial}{\partial x}(\rho u) &= 0 \\
\frac{\partial(\rho u)}{\partial t} + \frac{\partial}{\partial x}(\rho u^2 + p) &= 0 \\
\frac{\partial \rho E}{\partial t} + \frac{\partial}{\partial x}(\rho u E + u p) &= \lambda \frac{\partial^2 T}{\partial x^2} + \rho Q D \frac{\partial^2 Y}{\partial x^2} \\
\frac{\partial \rho Y}{\partial t} + \frac{\partial}{\partial x}(\rho u Y) &= \rho D \frac{\partial^2 Y}{\partial x^2} + \rho \omega
\end{aligned}$$

\Rightarrow

$$\begin{aligned}
\frac{\rho_0}{t_0} \left[\frac{\partial \hat{\rho}}{\partial \hat{t}} + \frac{\partial}{\partial \hat{x}}(\hat{\rho} \hat{u}) \right] &= 0 \\
\frac{\rho_0 u_0}{t_0} \left[\frac{\partial(\hat{\rho} \hat{u})}{\partial \hat{t}} + \frac{\partial}{\partial \hat{x}}(\hat{\rho} \hat{u}^2 + \hat{p}) \right] &= 0 \\
\frac{\rho_0 u_0^2}{t_0} \left[\frac{\partial \hat{\rho} \hat{E}}{\partial \hat{t}} + \frac{\partial}{\partial \hat{x}}(\hat{\rho} \hat{u} \hat{E} + \hat{u} \hat{p}) \right] &= \frac{\rho_0 u_0^3 r_0 (T_b - T_0)}{r_0^2 (T_b - T_0)} \left[\hat{\lambda} \frac{\partial^2 \hat{T}}{\partial \hat{x}^2} \right] + \frac{\rho_0 u_0^2 u_0 r_0 Y_0}{r_0^2} \left[\hat{\rho} \hat{Q} \hat{D} \frac{\partial^2 \hat{Y}}{\partial \hat{x}^2} \right] \\
\frac{\rho_0 Y_0}{t_0} \left[\frac{\partial \hat{\rho} \hat{Y}}{\partial \hat{t}} + \frac{\partial}{\partial \hat{x}}(\hat{\rho} \hat{u} \hat{Y}) \right] &= \frac{\rho_0 u_0 r_0 Y_0}{r_0^2} \left[\hat{\rho} \hat{D} \frac{\partial^2 \hat{Y}}{\partial \hat{x}^2} \right] + \frac{\rho_0 u_0 Y_0}{r_0} \frac{S_t}{u_0} [\hat{\rho} \hat{\omega}]
\end{aligned}$$

\Rightarrow

$$\begin{aligned}
\frac{\partial \hat{\rho}}{\partial \hat{t}} + \frac{\partial}{\partial \hat{x}}(\hat{\rho}\hat{u}) &= 0 \\
\frac{\partial(\hat{\rho}\hat{u})}{\partial \hat{t}} + \frac{\partial}{\partial \hat{x}}(\hat{\rho}\hat{u}^2 + \hat{p}) &= 0 \\
\frac{\partial \hat{\rho}\hat{E}}{\partial \hat{t}} + \frac{\partial}{\partial \hat{x}}(\hat{\rho}\hat{u}\hat{H}) &= \hat{\lambda} \frac{\partial^2 \hat{T}}{\partial \hat{x}^2} + \hat{\rho}\hat{Q}\hat{D} \frac{\partial^2 \hat{Y}}{\partial \hat{x}^2} \\
\frac{\partial \hat{\rho}\hat{Y}}{\partial \hat{t}} + \frac{\partial}{\partial \hat{x}}(\hat{\rho}\hat{u}\hat{Y}) &= \hat{\rho}\hat{D} \frac{\partial^2 \hat{Y}}{\partial \hat{x}^2} + \frac{S_t}{u_0} \hat{\rho}\hat{\omega}
\end{aligned}$$

3.2 Dimensionless parameters

- Reference velocity u_0 :

For simplification, the largest internal energy is normalized to be $\hat{e}(\rho, T_b) = e(\rho_0, T_b)/u_0^2 = 1$. Therefore, one has

$$u_0 = \sqrt{e(\rho_0, T_b)} = \sqrt{6.1952 \times 10^{13}} = 7.871 \times 10^6 \text{ m/s}$$

- Reference length scale $r_0 = 9 \times 10^{-4} \text{ m}$
- Reference time scale $t_0 = r_0/u_0 = 1.143 \times 10^{-10} \text{ s}$
- Speed of sound at the burnt state $c = \sqrt{\gamma p/\rho} = \sqrt{\gamma(\gamma-1)e(\rho_0, T_b)} = 5.247 \times 10^6 \text{ m/s}$
- Heat value $\hat{Q} = Q/u_0^2$, with data from Fowler 1975, for $C^{12} + C^{12} \rightarrow Mg^{24}$, $Q = 13.931 \text{ MeV}$, thus

$$\begin{aligned}
\hat{Q} &= \frac{13.931 \text{ MeV} \times (1.6022 \times 10^{-13} \text{ J/MeV}) \times (6.022 \times 10^{23} \text{ mol}^{-1}) / (0.024 \text{ kg/mol})}{u_0^2} \\
&= \frac{5.6 \times 10^{13} \text{ J/kg}}{6.1952 \times 10^{13} \text{ J/kg}} = 0.904
\end{aligned}$$

- The speed ratio $S_t/u_0 = 2/3$
- Thermal conductivity $\hat{\lambda}$ is related to C_p , while the heat release is related to internal energy:

$$\begin{aligned}
\tilde{C}_p(T_b - T_0) &= \int_{T_0}^{T_b} C_p dT = e(\rho_0, T_b) - e(\rho_0, T_0) \\
\hat{\lambda} &= \frac{S_t}{u_0} \frac{\tilde{C}_p(T_b - T_0)}{u_0^2} = 0.14541
\end{aligned}$$

- The diffusivity D is described by Lewis number $D = \alpha/Le = \lambda/\rho C_p Le$, therefore

$$\hat{D} = \frac{\lambda}{\rho C_p Le} \frac{1}{u_0 r_0} = \frac{1}{Le} \frac{S_t}{u_0} \frac{\delta_f}{r_0} = \frac{2}{3} \frac{1}{Le}$$

- The total energy form keeps the same in dimensionless form:

$$\hat{E} = \hat{e} + \frac{1}{2} \hat{u}^2 + \hat{Q}\hat{Y}, \quad \hat{e} = \frac{\hat{p}}{\hat{\rho}(\gamma-1)}$$

with the equation of state as:

$$\begin{aligned}
p &= \rho e(\gamma-1) = \frac{3}{4}(\gamma-1)(3\pi^2)^{\frac{1}{3}} \hbar c_1 (\rho N)^{\frac{4}{3}} + \frac{1}{2}(\gamma-1)N \frac{(3\pi^2)^{\frac{2}{3}}}{3\hbar c_1} \left(\frac{\rho^2}{N}\right)^{\frac{1}{3}} (kT)^2 \\
\hat{p} &= \frac{3}{4} \frac{1}{\rho_0 u_0^2} (\gamma-1)(3\pi^2)^{\frac{1}{3}} \hbar c_1 (\rho_0 N)^{\frac{4}{3}} \hat{\rho}^{\frac{4}{3}} + \frac{1}{2}(\gamma-1)N \frac{(3\pi^2)^{\frac{2}{3}}}{3\hbar c_1} \left(\frac{\rho_0^2}{N}\right)^{\frac{1}{3}} k^2 (T_b - T_0)^2 \hat{\rho}^{\frac{2}{3}} \hat{T}^2 \\
&= C_1 \hat{\rho}^{4/3} + C_2 \hat{\rho}^{2/3} \hat{T}^2
\end{aligned}$$

with $C_1 = 2.60559 \times 10^{-1}$, $C_2 = 6.82973 \times 10^{-2}$

- The source term equation:

$$\omega_0 = \frac{Y_0 u_0}{r_0} \frac{S_t}{u_0} \approx A Y_0^2 \exp\left(-E_a/T_{b9}^{\frac{1}{3}}\right)$$

$$\hat{\omega} = \frac{\omega}{\omega_0} = \hat{Y}^2 \exp\left(-E_a/T_9^{\frac{1}{3}} + E_a/T_{9b}^{\frac{1}{3}}\right) = \hat{Y}^2 \exp\left(-E_a\left(\frac{T_b - T_0}{10^9}\right)^{-\frac{1}{3}}\left(\hat{T}^{-\frac{1}{3}} - \hat{T}_b^{-\frac{1}{3}}\right)\right)$$

to reduce the term S_t/u_0 in previous equation along with $\hat{\omega}$, denoting

$$\begin{aligned}\widehat{Ea} &= -Ea\left(\frac{T_b - T_0}{10^9}\right)^{-\frac{1}{3}} = 57.7224 \\ \hat{A} &= \frac{S_t}{u_0} \exp\left(Ea\left(\frac{T_b - T_0}{10^9}\right)^{-\frac{1}{3}} \hat{T}_b^{-\frac{1}{3}}\right) = 4.25133 \times 10^{24}\end{aligned}$$

then the source term keeps the same in dimensionless form:

$$\hat{\omega} = \hat{A} \hat{Y}^2 \exp\left(-\widehat{Ea}/\hat{T}^{\frac{1}{3}}\right)$$

- And the final dimensionless equations are:

$$\begin{aligned}\frac{\partial \hat{\rho}}{\partial \hat{t}} + \frac{\partial}{\partial \hat{x}}(\hat{\rho} \hat{u}) &= 0 \\ \frac{\partial(\hat{\rho} \hat{u})}{\partial \hat{t}} + \frac{\partial}{\partial \hat{x}}(\hat{\rho} \hat{u}^2 + \hat{p}) &= 0 \\ \frac{\partial \hat{\rho} \hat{E}}{\partial \hat{t}} + \frac{\partial}{\partial \hat{x}}(\hat{\rho} \hat{u} \hat{H}) &= \hat{\lambda} \frac{\partial^2 \hat{T}}{\partial \hat{x}^2} + \hat{\rho} \hat{Q} \hat{D} \frac{\partial^2 \hat{Y}}{\partial \hat{x}^2} \\ \frac{\partial \hat{\rho} \hat{Y}}{\partial \hat{t}} + \frac{\partial}{\partial \hat{x}}(\hat{\rho} \hat{u} \hat{Y}) &= \hat{\rho} \hat{D} \frac{\partial^2 \hat{Y}}{\partial \hat{x}^2} + \hat{\rho} \hat{\omega} \\ \hat{E} &= \hat{e} + \frac{1}{2} \hat{u}^2 + \hat{Q} \hat{Y} \\ \hat{e} &= \frac{\hat{p}}{\hat{\rho}(\gamma - 1)} \\ \hat{p} &= C_1 \hat{\rho}^{4/3} + C_2 \hat{\rho}^{2/3} \hat{T}^2 \\ \hat{\omega} &= \hat{A} \hat{Y}^2 \exp\left(-\widehat{Ea}/\hat{T}^{\frac{1}{3}}\right)\end{aligned}$$

4. Numerical methods

- Discrete methods:

- Time evolution: 3 order TVD Runge-Kutta

$$\begin{aligned}U^{(1)} &= U_n + L(U_n) \Delta t \\ U^{(2)} &= \frac{3}{4} U_n + \frac{1}{4} (U^{(1)} + L(U^{(1)}) \Delta t) \\ U_{n+1} &= \frac{1}{3} U_n + \frac{2}{3} (U^{(2)} + L(U^{(2)}) \Delta t)\end{aligned}$$

- Convection term:

Roe method: solve convection flux by eigen vector

- Diffusion term: 7 order central difference

$$\frac{\partial m_i}{\partial x} = \frac{1}{\Delta x} \left(\frac{1}{60} m_{i+3} - \frac{9}{60} m_{i+2} + \frac{45}{60} m_{i+1} - \frac{45}{60} m_{i-1} + \frac{9}{60} m_{i-2} - \frac{1}{60} m_{i-3} \right)$$

- Initial conditions:
 - Pressure: whole field the same pressure $\hat{P}(\rho_0, T_0)/\hat{P}_0$
 - Velocity: $u = 0$
 - Concentration: $Y_0 = 1$
 - Temperature: $T_0 \rightarrow T_b$, $\tanh(x)$ profile for about 1 flame thickness area
- Boundary conditions: (cartesian coordinates)
 - Inner boundary conditions: opening / freeflow / inletOutlet
 - Outlet boundary conditions: opening / freeflow / inletOutlet
- Boundary conditions: (spherical coordinates)
 -

5. Results

Appendix

A1. Speed of sound

- Pressure from equation of state:

$$\begin{aligned} p &= \rho e(\gamma - 1) = \frac{3}{4}(\gamma - 1)(3\pi^2)^{\frac{1}{3}} \hbar c_1 (\rho N)^{\frac{4}{3}} + \frac{1}{2}(\gamma - 1) N \frac{(3\pi^2)^{\frac{2}{3}}}{3\hbar c_1} \left(\frac{\rho^2}{N} \right)^{\frac{1}{3}} (kT)^2 \\ &= C_1 \rho^{\frac{4}{3}} + C_2 \rho^{\frac{2}{3}} \end{aligned}$$

- The theoretical speed of sound is obtained by:

$$c = \sqrt{\left(\frac{\partial p}{\partial \rho} \right)_s} = \sqrt{\frac{4}{3} C_1 \rho^{\frac{1}{3}} + \frac{2}{3} C_2 \rho^{-\frac{1}{3}}} \approx \sqrt{\gamma \frac{p}{\rho}}$$

A2. Eigenvector of Jacobian

- Eigen vector for Roe method:

$$U = [\rho, \rho u, \rho E, \rho Y] = [m_1, m_2, m_3, m_4]$$

$$F = [\rho u, \rho u^2 + p, \rho u E + up, \rho u Y] = [m_2, m_2^2/m_1 + p, (m_3 + p)m_2/m_1, m_4 m_2/m_1]$$

$$\text{where } p = (\gamma - 1)\rho(E - \frac{1}{2}u^2 - QY)$$

- Solve by Matlab symbolic calculation:

```
% definition
syms m1 m2 m3 m4 real
syms Q gamma real
syms m1 m3 m4 gamma Q positive

% declaration
rho = m1;
u = m2/m1;
E = m3/m1;
Y = m4/m1;
e = E-1/2*u*u-Q*Y
```

```

p = (gamma-1)*rho*e;
Um = [m1 m2 m3 m4];
Fm = [rho*u, rho*u*u+p; rho*u*E+u*p; rho*u*Y];

% solve
J = jacobian(Fm,Um);
[RM,RD] = eig(J);
[LM,LD] = eig(J');

```

- The Jacobian matrix is:

$$\mathbf{J} = \begin{bmatrix} 0 & 1 & 0 & 0 \\ -u^2 + K_1 & 2u + K_2 & K_3 & K_4 \\ -uH + uK_1 & H + uK_2 & u(1 + K_3) & uK_4 \\ -uY & Y & 0 & u \end{bmatrix}$$

where $K_1 = (\gamma - 1)u^2/2$, $K_2 = (\gamma - 1)(-u)$, $K_3 = (\gamma - 1)$, $K_4 = (\gamma - 1)(-Q)$

- Eigenvalue Λ is:

$$\mathbf{\Lambda} = \begin{bmatrix} u - c & & & \\ & u & & \\ & & u & \\ & & & u + c \end{bmatrix}$$

where c is the numerical speed of sound:

$$c = \frac{2}{3} \sqrt{E - \frac{1}{2}u^2 - QY} = \frac{2}{3} \sqrt{\frac{p}{\rho} \frac{1}{\gamma - 1}} = \sqrt{\gamma p / \rho}$$

- Right eigen matrix \mathbf{R} is: (each column is an eigenvector)

$$\mathbf{R} = \begin{bmatrix} 1 & 1 & 0 & 1 \\ u - c & u & 0 & u + c \\ H - uc & u^2/2 & Q & H + uc \\ Y & 0 & 1 & Y \end{bmatrix}$$

- Left eigen matrix \mathbf{L} is: (each row is an eigenvector)

$$\mathbf{L} = \begin{bmatrix} -\frac{u}{2c} - \frac{K_1}{2c^2} & \frac{1}{2c} + \frac{uK_3}{2c^2} & -\frac{K_3}{2c^2} & -\frac{K_4}{2c^2} \\ -\frac{1}{2} + \frac{K_1}{2c^2} & -\frac{uK_3}{2c^2} & \frac{K_3}{2c^2} & \frac{K_4}{2c^2} \\ -Y & 0 & 0 & 1 \\ -\frac{u}{2c} + \frac{K_1}{2c^2} & \frac{1}{2c} - \frac{uK_3}{2c^2} & \frac{K_3}{2c^2} & \frac{K_4}{2c^2} \end{bmatrix}$$

- To meet the eigen-decomposition criteria and to be used in the eigen-space projection, re-projection step, one can get the eigen-space as: (let $\gamma_1 \equiv \gamma - 1$, then $K_1 = \gamma_1 u^2/2$, $K_3 = \gamma_1$, $K_4 = -\gamma_1 Q$)

$$\mathbf{R}_F = \begin{bmatrix} \frac{1}{c} & \frac{1}{c} & 0 & \frac{1}{c} \\ \frac{u}{c} - 1 & \frac{u}{c} & 0 & \frac{u}{c} + 1 \\ \frac{H}{c} - u & \frac{u^2}{2c} & \frac{Q}{c} & \frac{H}{c} + u \\ \frac{Y}{c} & 0 & \frac{1}{c} & \frac{Y}{c} \end{bmatrix}, \quad \mathbf{R}_F^{-1} = \begin{bmatrix} \frac{u}{2} + \frac{\gamma_1 u^2}{4c} & -\frac{1}{2} - \frac{\gamma_1 u}{2c} & \frac{\gamma_1}{2c} & -\frac{\gamma_1 Q}{2c} \\ c - \frac{\gamma_1 u^2}{2c} & \frac{\gamma_1 u}{c} & -\frac{\gamma_1}{c} & \frac{\gamma_1 Q}{c} \\ -\frac{\gamma_1 u^2 Y}{2c} & \frac{\gamma_1 u Y}{c} & -\frac{\gamma_1 Y}{c} & c + \frac{\gamma_1 Q Y}{c} \\ -\frac{u}{2} + \frac{\gamma_1 u^2}{4c} & \frac{1}{2} - \frac{\gamma_1 u}{2c} & \frac{\gamma_1}{2c} & -\frac{\gamma_1 Q}{2c} \end{bmatrix}^T$$

which satisfies $\mathbf{R}_F \mathbf{R}_F^{-1} = \mathbf{I}$ and $\mathbf{R}_F \mathbf{\Lambda} \mathbf{R}_F^{-1} = \mathbf{J}$.

- This has been validated in `Matlab` code:


```

syms u real
syms rho E Y real positive
syms Q gamma real positive

e = (E - 1/2*u*u - Q*Y);
p = (gamma-1)*rho*e;
c = sqrt(gamma*p/rho);
H = E + p/rho;

K1 = (gamma-1)*u*u/2;
K2 = (gamma-1)*(-u);
K3 = (gamma-1);
K4 = (gamma-1)*(-Q);

J = [
    [ 0, 1, 0, 0];
    [-u*u+K1, 2*u+K2, K3, K4]
    [-u*H+u*K1, H+u*K2, u*(1+K3), u*K4]
    [-u*Y, Y, 0, u];
];

D = [
    [u-c, 0, 0, 0];
    [ 0, u, 0, 0];
    [ 0, 0, u, 0];
    [ 0, 0, 0, u+c];
];

RF = [
    [1/c, 1/c, 0, 1/c];
    [u/c-1, u/c, 0, u/c+1];
    [H/c-u, u*u/2/c, Q/c, H/c+u];
    [Y/c, 0, 1/c, Y/c];
];

g1 = gamma-1;
c2 = 2*c;
c4 = 4*c;
LF = [
    [ u/2+g1*u*u/c4, -1/2-g1*u/c2, g1/c2, -g1*Q/c2];
    [ c-g1*u*u/c2, g1*u/c, -g1/c, g1*Q/c ];
    [ -Y*g1*u*u/c2, Y*g1*u/c, -Y*g1/c, c+Y*g1*Q/c ];
    [-u/2+g1*u*u/c4, 1/2-g1*u/c2, g1/c2, -g1*Q/c2];
]';

simplify(RF*LF') % output is [ 1, 0, 0, 0]
% [ 0, 1, 0, 0]
% [ 0, 0, 1, 0]
% [ 0, 0, 0, 1]

simplify(RF*D*LF' - J) % output is [ 0, 0, 0, 0]
% [ 0, 0, 0, 0]
% [ 0, 0, 0, 0]
% [ 0, 0, 0, 0]

```

Reference

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