

# INDIAN INSTITUTE OF TECHNOLOGY-KHARAGPUR

Mid-Spring Semester 2017-18 (Closed Book)

Course No.: CH 61016

Course Title: Process Dynamics and Control

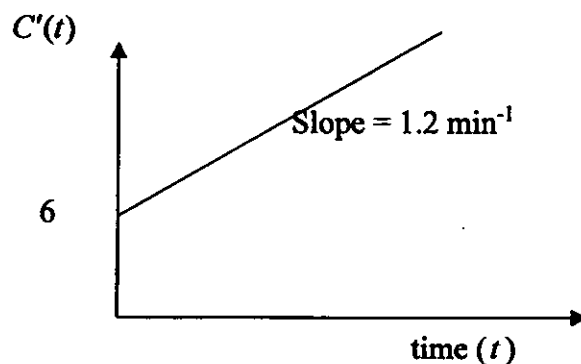
Department: Chemical Engineering

Max. Time: 2 hrs

Total Marks: 30

**Answer all questions**

- Q1.** (a) Develop the real PID controller with derivative of output rather than error and its block diagram. [(1+1)+(1+2)+2+5+2+1=15]
- (b) If  $\tau_f = 10\Delta t$  (where,  $\tau_f$  is the filter time constant and  $\Delta t$  the sampling instant), find the filter factor ( $f$ ) for a digital first-order filter with deriving concerned correlation.
- (c) The input error signal to a PI controller changes stepwise with a magnitude of 2 and the controller output ( $C'$ ) changes initially as shown below:



Find the values of the controller gain ( $K_C$ ) and integral time constant ( $\tau_I$ ).

- (d) Consider a feedback loop having the following transfer functions:

$$G_P = G e^{-t_d s} = \frac{e^{-0.5s}}{0.8s + 1} \quad G_m = G_f = 1$$

Although the model is perfectly known (i.e.  $G = G'$ ), the dead-time ( $t_d$ ) value is wrongly determined as 0.45 min. Discuss the impact of dead-time on the effectiveness of smith predictor when the process operates under P-only controller with  $K_C = 30$ .

- (e) Configure the cascade control scheme for the bottom composition loop of a distillation column.
- (f) One type of ratio controller has divider, another one has ratio station; which one is better and why?

[Please Turn Over]

- Q2.** Consider the dynamic model of a jacketed stirred tank heating system where the water temperature ( $T$ ) in the tank is to be controlled by manipulating the flow rate of hot oil in the jacket ( $F_j$ ). All other variables are remaining constant at their steady state values.

$$\frac{dT}{dt} = \frac{F}{V}(T_i - T) + \frac{UA}{\rho C_p V}(T_j - T)$$

$$\frac{dT_j}{dt} = \frac{F_j}{V_j}(T_{ji} - T_j) - \frac{UA}{\rho_j C_{pj} V_j}(T_j - T)$$

**Parameter and steady state values**

$F = 30 \text{ l/m}; F_j = 50 \text{ l/m}; T_i = 15^\circ\text{C};$   
 $T_{ji} = 93^\circ\text{C}; V = 300 \text{ l}; V_j = 30 \text{ l};$   
 $\rho C_p = 1; \rho_j C_{pj} = 1.384; UA = 100;$

Derive the following for this system:

[1+3+3]

- Non-linear state space model
- Linear state space model
- Transfer function model

- Q3.** Consider the transfer function of a system defined by the following equation

$$\frac{y(s)}{u(s)} = g(s) = \frac{6s^3 + 55s^2 + 168s + 168}{s^4 + 12s^3 + 53s^2 + 102s + 72}$$

- Derive Jordan canonical form of state-space realization for this transfer function
  - Derive observer canonical form of state-space realization for this transfer function
- [4+4]

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