

INSTRUMENTATION

Components of a process: (Control system)

- (1) Sensors
- (2) Comparator & controller.
- (3) Final Control element.

SENSOR :

- (a) Temperature
- (b) Pressure
- (c) Flow rate (most)
- (d) Concentration - difficult to measure)
- (e) Liquid level

Temperature :

- i) Thermostat
- ii) Thermometer - liquid filled
- iii) Thermocouple
- iv) Resistance Temp. Detector
- v) Semiconductor
- vi) Bi-metallic
- vii) Radiation Pyrometer

Pressure

- i) Manometer
- ii) Diaphragm cell
- iii) Bourdon Tube
- iv) Bellows
- v) Strain gauge
- vi) Piezo (crystals respond electrically to pressure).

Flow

- i) Orifice - II -
 - ii) Venturi meter
 - iii) Variable area meter (Rotameter) → digital display
 - iv) Pitot tube
 - v) Hot wire anemometer - high precision
 - vi) Ultrasonic flow meter (large pipelines)
 - vii) Coriolis meter - (measures mass flow rate directly)
- } works for clean liquid

oysters of hydrocarbons along with
(Gas) hydrocarbons

a) Level

i) Float

ii) Optical / Conductivity & sonic measurements

e) Composition

i) Chromatography - long time for analysis

ii) Turbidimetry

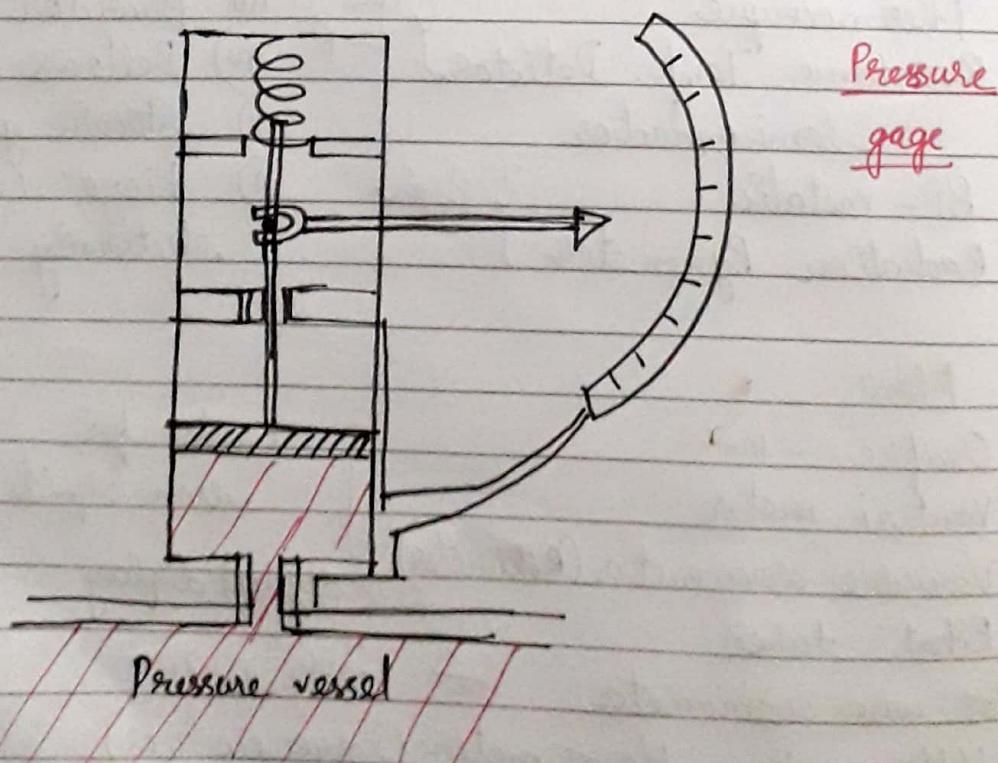
iii) pH measurement / electrical conductivity

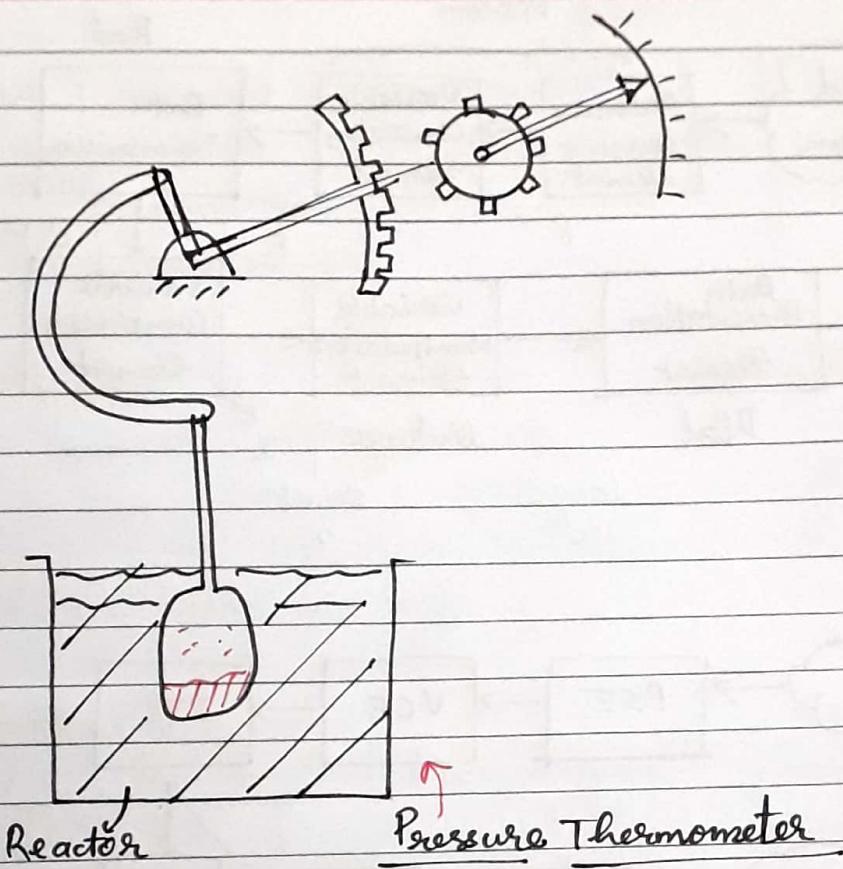
iv) optical measurement / polarization of light

2. Measurement System Application } Ch-2 (Pg 13-38)
& Design by E.O. Dooblin } Ch-3 (Part)

2. Coulson & Richardson (vol-?)

Functional Elements of a measuring instrument

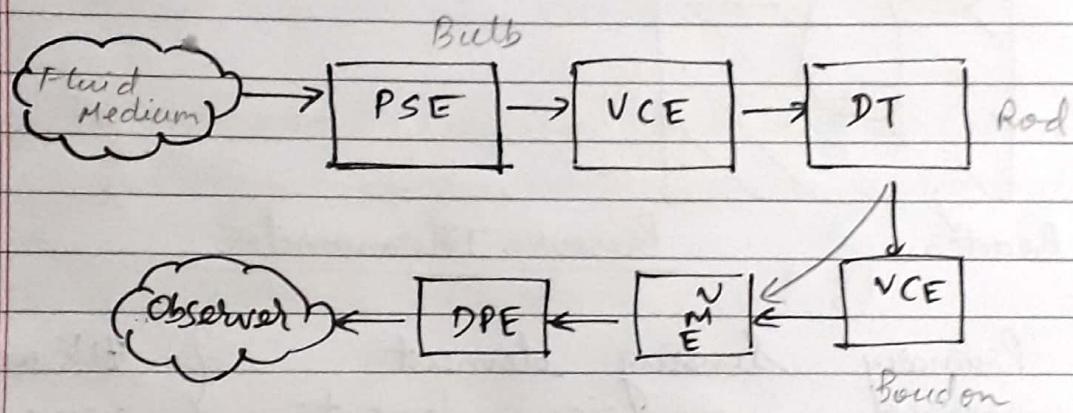
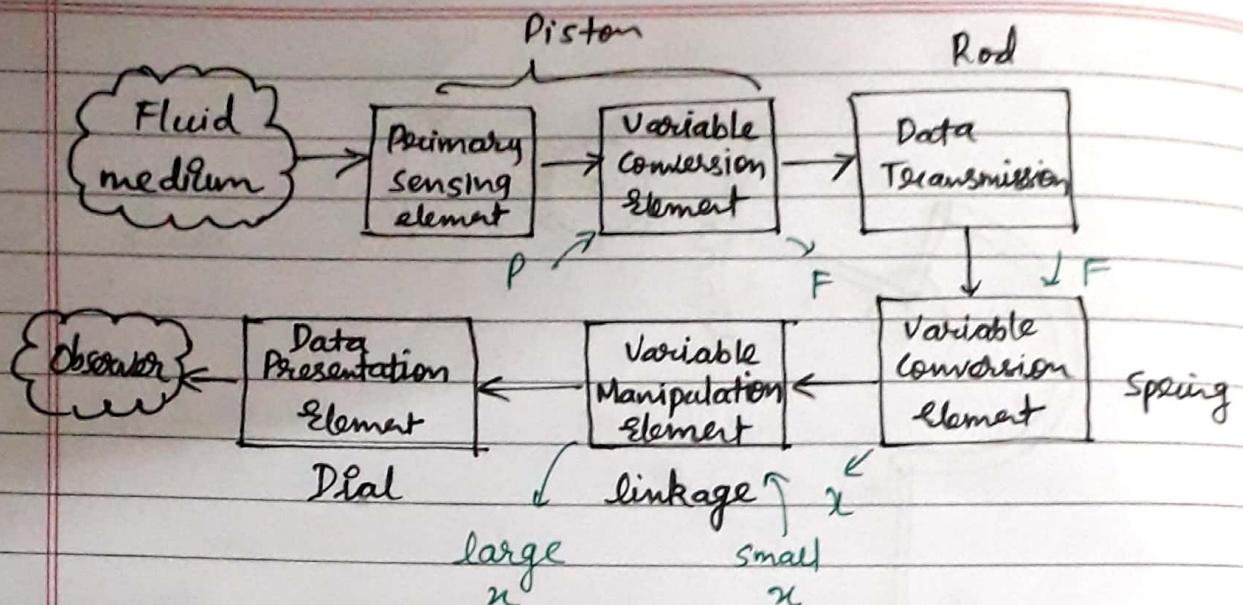




- (a) Primary sensing element
 - (b) Variable conversion element
 - (c) Variable manipulation element.
 - (d) Data transmission element
 - (e) Data presentation element.
- It's not necessary they have to be in this sequence always.

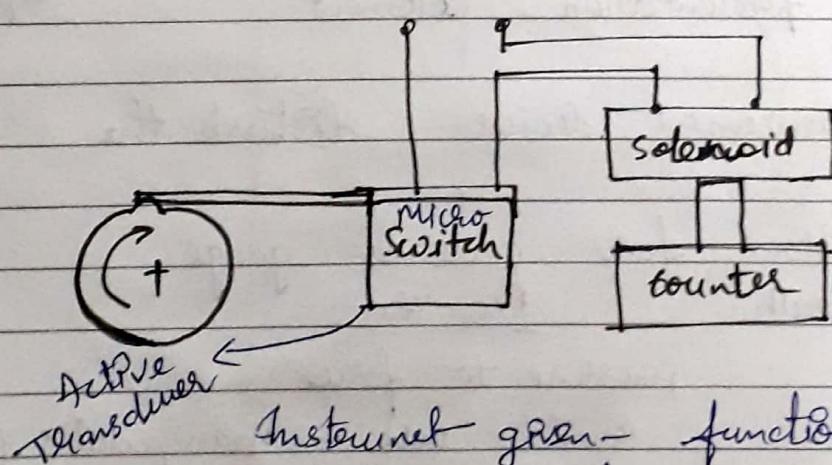
* all measurement devices - disturb the system

- (a) PSE - piston for pressure gauge.
- bulb Pre. Ther
- (b) VCE - pressure to force
- (c) VME - Boudon tube - manipulates (^{magnify}
displacement) of pitot needle
- (d) DTE - transmitting data - without conversion and
manipulation
- (e) DPE - human readable version.



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Mechanical Counter



Instrument given - functional elements?

PSE → Rod → DT

in snam

Sectch &

Variable Conversion

Majority of PSU are of analog type.

For this - Resolution counter - digital instrument

classmate

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Wires	Solenoid - s	Counter	Switch (Mod to sig)
Data transmission	Variable conversion	Data presentation	Variable conversion
	Counter s -		
		Counts the	

Basic diff ^ → Press thermo.

Mechai. Count's

extract energy

from the system

- Transducer/transmitter

① Analog ?

② Digital

Transducer - take one type give
out another

Modes of
operation

Is not an Transducer

energy conversion

element]

Active

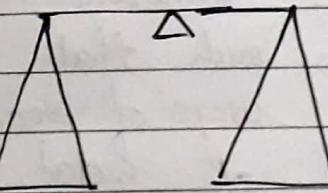
(Power source)

Input signal
needed)

only an
insignificant
portion.

Passive → [output energy supplied entirely or

(Power is drawn almost entirely by
from the system) its Input signal.]



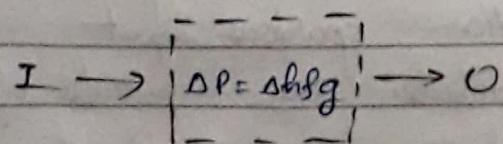
Deflection

Null

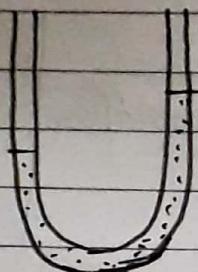
- adv :- can measure
slight amount of deflection

D

Input-Output Configuration



Deflection-type device: The measured quantity produces some physical effect that engenders a similar but opposing effect in some part of the instrument.



$$I = \Delta P$$

specifically intended
↑ to measure

$$O = \Delta h$$

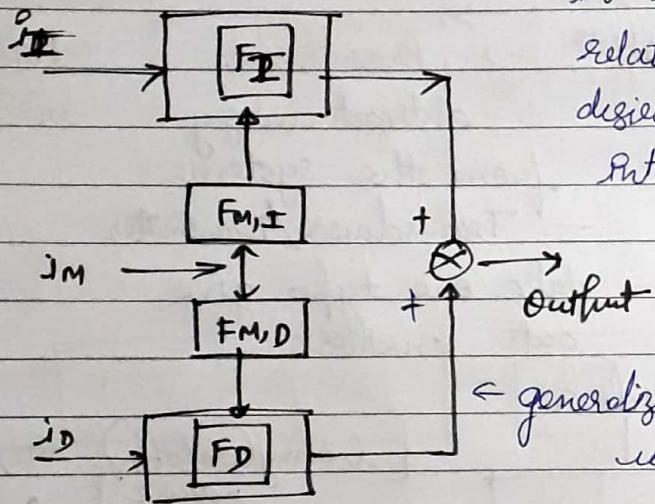
① Desired input

② Interfering input

③ Modifying input

↳ cause a change

in the input-output relations for the desired and interfering inputs.



generalized input-output configuration.

Instrument be inherently sensitive only to desired inputs

Methods for correction of interfering & modifying (spurious) inputs

ⓐ

Method of Inherent non-sensitivity

- design such that it's not much sensitive
e.g. usage of wood in pendulum instead of metal.

ⓑ

High gain feedback

ⓒ

Calculated output correction.

ⓓ

Signal filtering → thermal insulation

ⓔ

Opposing input. - if we can measure disturbance

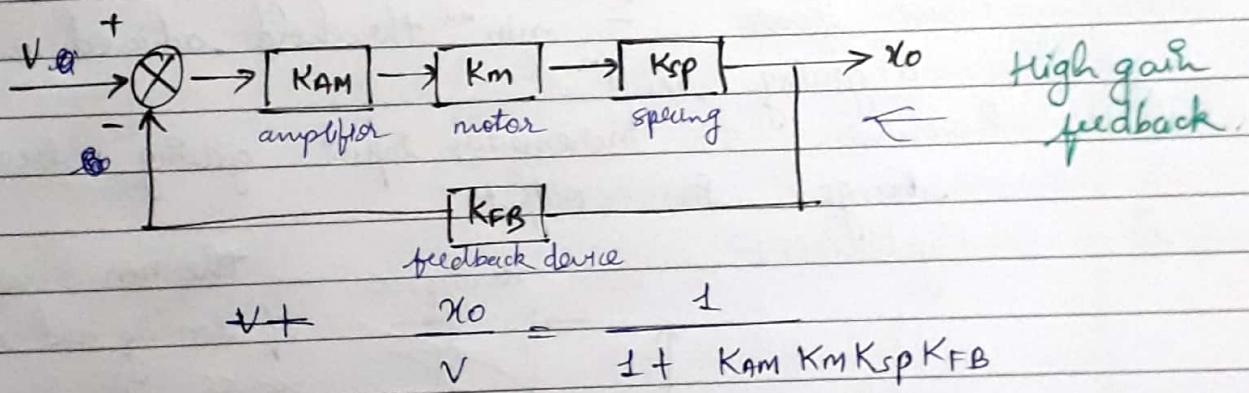
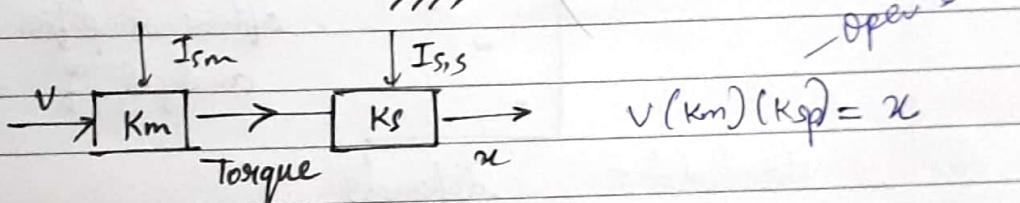
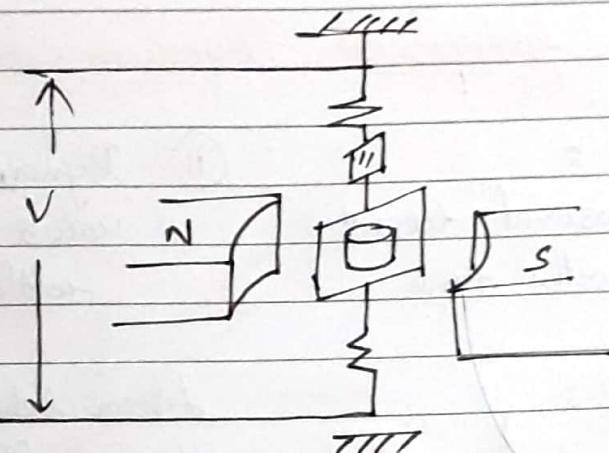
vibration - spurious input

ⓕ

measure or estimate the magnitudes of interfering/modifying inputs and to know quantitatively how they affect the output.

Null \rightarrow Maintain deflection at zero by suitable application of an effect opposing that generated by the measured quantity.

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$$(V+ - K_{FB} x_0) \times K_{AM} K_m K_{SP} = x_0$$

$$V K_{AM} K_m K_{SP} + x_0 = x_0 + x_0 K_{FB} K_{AM} \\ K_m K_{SP}$$

$$\frac{V}{V} \frac{x_0}{x_0} = \frac{K_{AM} K_m K_{SP}}{1 + \underbrace{K_{FB} K_{AM} K_m K_{SP}}_{\geq 1}}$$

Improvements * feedback loop works for many cases.

Adv. ① Amplifier supplies most of the power,
greater accuracy \therefore feedback device can be designed with low power handling capacity.

Also input signal carry negligible power,
 \therefore feedback extracts less energy from measured medium

then $\frac{x_0}{V} = \frac{1}{K_{FB}}$

Now we require only K_{FB} to stay constant

Signal filtering - Introducing certain elements into the system which in some fashion block the signals so that their effects are removed.

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Generalised Performance Criteria

(i) Static :- value measured doesn't change with time

(ii) Dynamic :- values are changing with time.

(a) Linearity :-

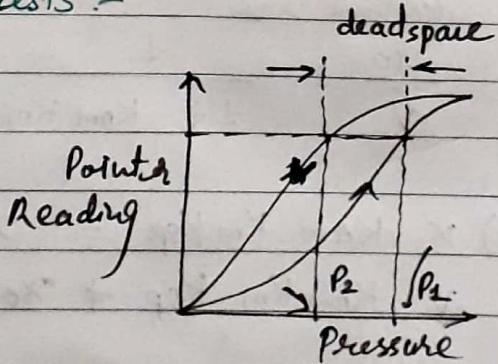
Linear behaviour of the parts often simplifies design and analysis of the whole.

(b) threshold :- depends

(c) Noise floor - minⁱⁿ threshold achieved under for a giving condⁿ

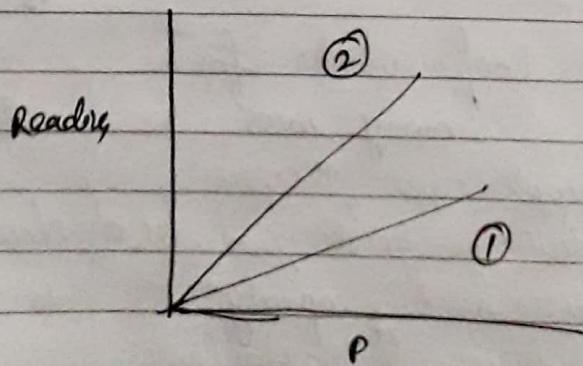
(d) Resolution :- Incremental input giving desired change in output.

(e) Hysteresis :-



The non-coincidence of loading and unloading curves is due to internal friction or hysteresis damping of the stressed parts

(f) Static sensitivity

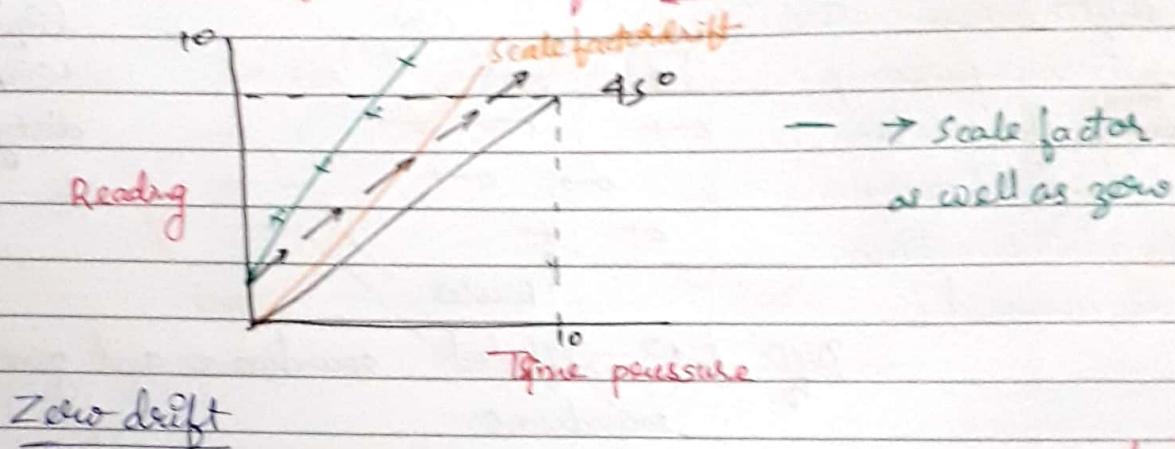


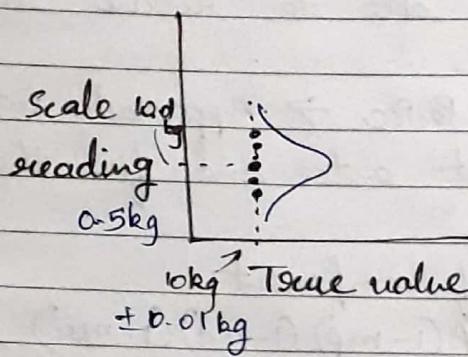
Offsetting effects — Intentionally introducing into the instrument interfacing and/or modifying inputs that tend to cancel bad effects of spurious inputs.

cancelate

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Zero drift & Scale factor drift



Calibration

Random variables \rightarrow

All possible conditions
(that may act as
interfering or modifying
inputs).

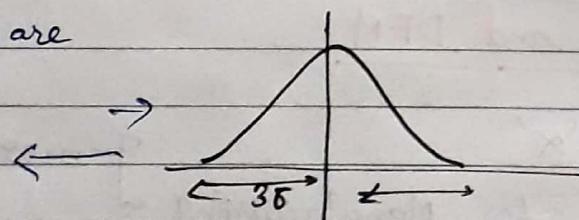
$$\text{Ambient Temp} = 20 \pm 2^\circ\text{C}$$

Level of vibration :

Atmospheric P :

	$10 \pm 0.01 \text{ kg}$	\rightarrow Preliminary Std.	\uparrow imprecision
Total	1	10.02 Reading	
2	10.20	(Std dev)	$\bar{x} = 10.04 \pm 0.39$
3	9.97	(Std dev)	$s = 0.147$
4	10.20		0.165
5	9.81		

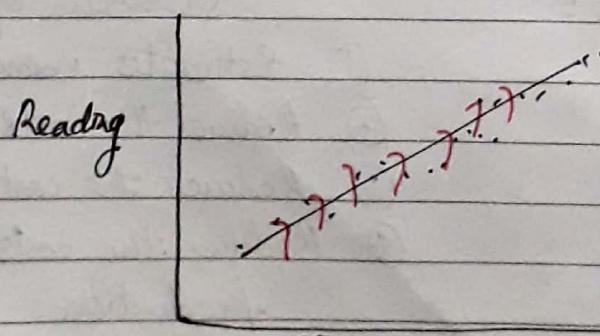
We are



0.997 is probability
the reading will be
bet'n $10.04 - 0.39$
 $10.04 + 0.39$

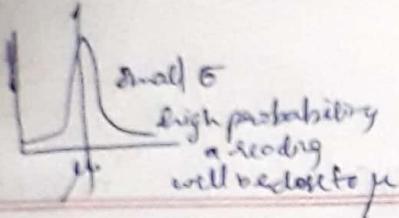
$$\text{Bias} = 10.04 - 10.0 = 0.04$$

Measure
Scatter s



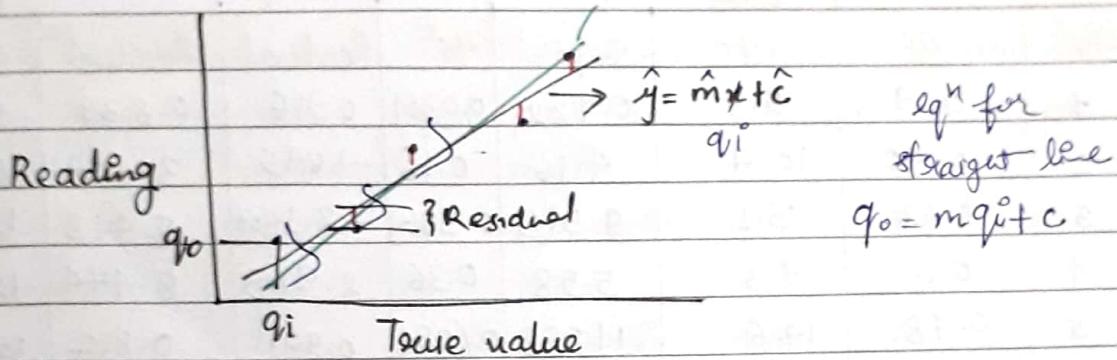
{ The straight line or the
perfect Gaussian line "would
be perfectly followed by
data from an infinitely
large sample of Gaussian data"

which had the same μ and σ values as our
actual data sample



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$$L = \sum_{q_0} (y_i^o - \hat{y})^2 = \sum_i (y_i^o - \hat{m} q_i^o - \hat{c})^2$$

$$\frac{dL}{dm} = 0 \quad \frac{dL}{dc} = 0$$

$$m = \frac{N \sum q_i^o q_0 - \sum q_i^o \sum q_0}{N \sum q_i^{o^2} - (\sum q_i^o)^2}$$

$$c = \frac{\sum q_0 \sum q_i^{o^2} - (\sum q_i^o)(\sum q_i^o)}{N \sum q_i^{o^2} - (\sum q_i^o)^2}$$

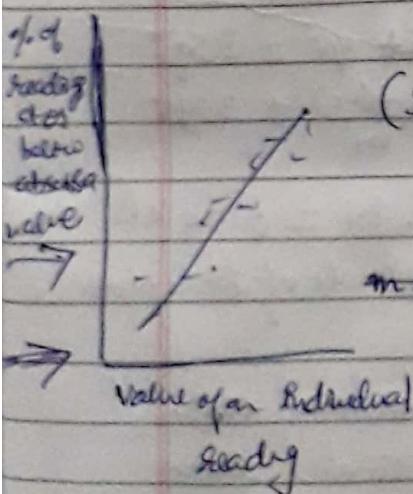
Slope and Intercept has certain randomness, because those points fall within some distribution.

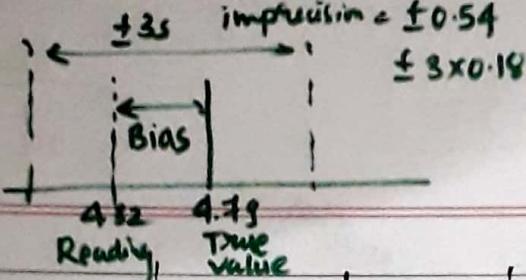
$$S_m^2 = \frac{N (sq_0)^2}{N \sum q_i^{o^2} - (\sum q_i^o)^2} \quad S_c^2 = \frac{(sq_0)^2 \sum q_i^o}{N \sum q_i^{o^2} - (\sum q_i^o)^2}$$

$$(sq_0)^2 = \frac{1}{N-2} \underbrace{\sum [(m q_i^o + b) - q_0]^2}_{\text{Residual}}$$

$$m = 6 (sq_0)^2 = \frac{1}{N-2} \sum \left(\frac{q_0 - b}{m} - q_i^o \right)^2$$

$$= \frac{\sum \text{Residual}^2}{m^2}$$



 $m q_i$ $m q_i + c$

	q_i	q_0	$q_i q_0$	q_i^2	Residual	Residual ²	\hat{a}
1	0.19	3.8	0.722	0.0361	0.916	0.839	4.716
2	0.40	10.4	4.16	0.16	-1.895	3.404	8.5549
3	0.63	15.1	9.513	0.3969	-2.3407	5.478	12.7593
4	0.6	9.3	5.58	0.36	2.9109	8.474	12.2109
5	0.78	14.6	11.388	0.6084	0.901	0.812	15.5013
6	1.05	20.9	21.945	1.1025	-0.463	0.219	20.4369
7	1.74	31.3	54.462	3.0276	1.75	3.062	33.0501
8	1.62	32.7	52.974	2.6244	-1.843	3.396	30.8565
	$\sum 7.01$	$\sum 138.1$	$\sum 160.794$	$\sum 8.3159$		$\sum 25.679$	$\sum 138.08$

$c = 1.2428$

$m = \frac{8 \times 160.794 - 7.01 \times 138.1}{8 \times 8.3159 - (7.01)^2}$

$8m = 1.4034$

$m = \frac{8 \times 8.3159 - (7.01)^2}{8 \times 8.3159 - (7.01)^2}$

$S_k = 1.3137$

$m = 18.28$

$S q_i^2 = 0.0768$

$C = \frac{138.1 \times 8.3159 - 160.794 \times 7.01}{8 \times 8.3159 - (7.01)^2}$

$C = 1.2429$

frequency
range
from 0 to 1

(C-f-0.5)

$Z = \frac{x - u}{\sigma}$

Cumulative
frequencyUncertainty
Bias

Probability plot

C.f

-0.91	1	0.0625	+ eg if $q_0 = 4.32$ kPa
1.85	2	0.1875	To determine q_0 True value
2.34	3	0.3125	
-2.91	4	0.4375	$= q_0 + q_i \pm 3 S q_i$
-0.90	5	0.5625	$= q_0 + (-c) \pm 3 S q_i$
+0.46	6	0.6875	m
-1.75	7	0.8125	$= 4.79 \pm 0.54$ kPa
+1.84	8	0.9375	estimate of true pressure

* error due to ~~less~~ imprecision - random error
 # bias is also called systematic error

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Measurement Equipment (Selection & Functioning)

Transmitter

Electric signal → vibrator

Carried by fluid
↓

Vibration feet → produce
receiver electric signal

P₁

U_e →

U_scosθ + U_s

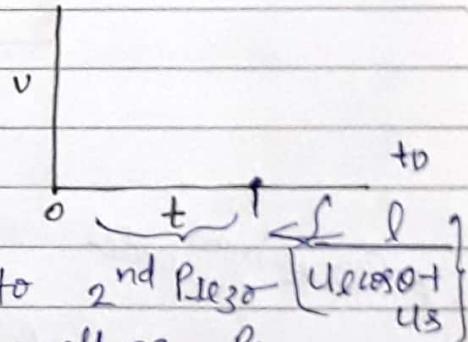
Time of Flight

Ultrasonic

This method is
not dependable on
the particles in the fluid

Velocity of sound = U_s

l_{iq} = U_e



Pressure fluctuation (sound → propagates to 2nd P₂)
at t=0 no pressure → to voltage P₁

P₂ receives voltage sends pressure signal

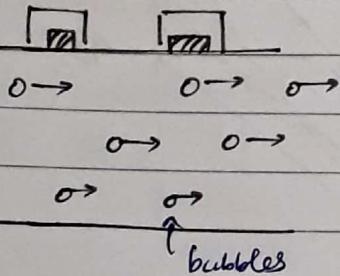
$$\Delta V = \frac{l}{U_s - U_e \cos \theta}$$

$$\frac{\Delta V}{\Delta t} = \frac{U_s + U_e \cos \theta}{U_s - U_e \cos \theta}$$

* By measuring frequency shift between the ultrasonic frequency source ~~and~~, the receiver and fluid carries, the relative motion are measured.

Doppler

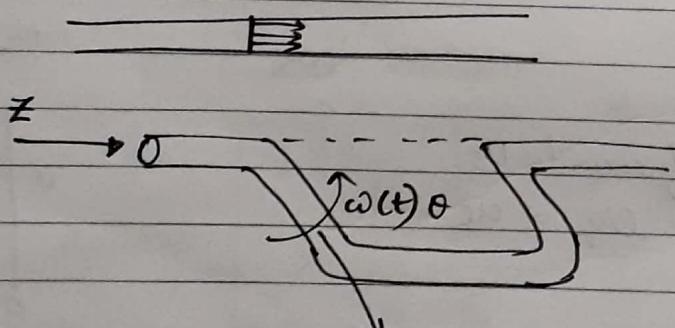
- will not work for clean liquid.



works for dirty liquid.

Diff bet reflected soundwave and generated soundwave.

2 phase flow - mass flow meter

Coriolis Flow meter

ΔV_{θ} mass flow rate

The swinging is generated by vibrating the tube in which

$$\frac{d}{dt} \left(\frac{\partial \theta}{\partial t} + \omega_r \frac{\partial V_\theta}{\partial r} + \frac{V_\theta}{r} \frac{\partial \omega}{\partial \theta} + \frac{V_r V_\theta}{r} + \frac{V_z}{r} \frac{\partial V_\theta}{\partial z} \right) = -\frac{1}{r} \frac{\partial P}{\partial \theta} + \mu \left[\frac{\partial^2 \theta}{\partial t^2} \right] + g \rho_0 \frac{\partial \theta}{\partial z} \quad \text{no gravity}$$

(viscosity is negligible)

θ section - not much press. variation
 $V_\theta = r \omega(t)$

Twist & mass flow rate

- * Selection of instrument for given
- * Coulson Richardson

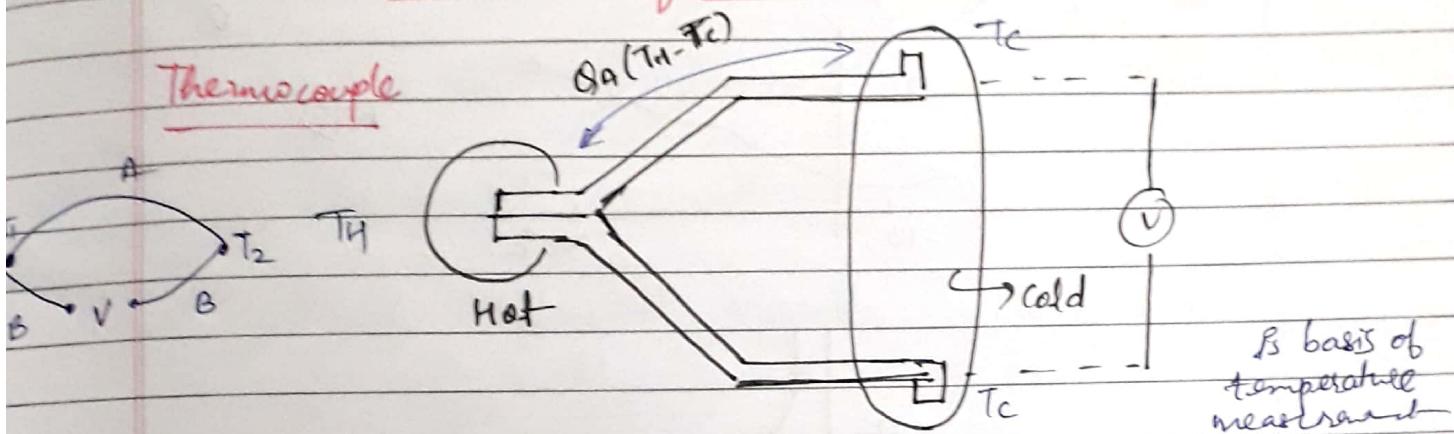
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Measurement of temp

Thermocouple



is basis of
temperature
measurement

Seebeck effect - Relation betⁿ voltage and Temperature T_H, T_C
One end at hot junction and one at cold junction - these
is voltage diffⁿ

$$V = \int_{T_1}^{T_2} (\vartheta_A - \vartheta_B) dT = \alpha_{AB} (T_2 - T_1)$$

* Voltage created by thermocouple
is very small. $5 \mu V/m$

* It will measure temp diffⁿ and not the
absolute temp.

what is reference function \rightarrow need not be
Thermocouple requires reference temp.

\rightarrow a resistor whose
 \rightarrow resistance depends
 \rightarrow on temp

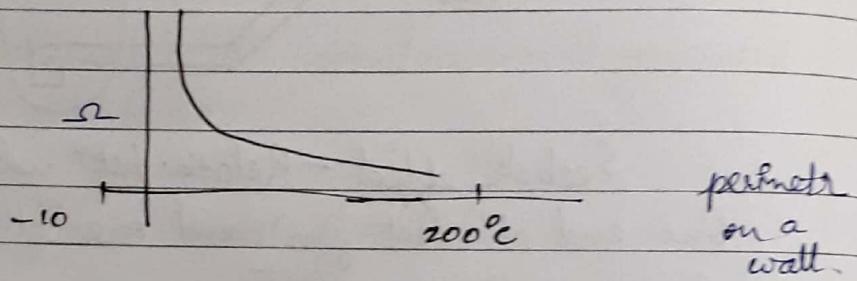
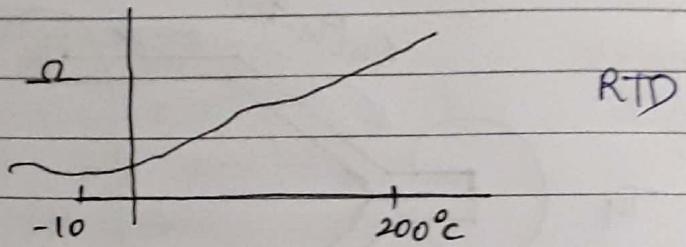
① Resistor Temp Detector
CRTD Types of thermocouple High accuracy

② Thermistor - Linearity
Sensitivity & Material
Freeness

①	J	Cu	Constantan
②	K		

-100°C 1200°C

Slope of Input-Output curve - sensitivity

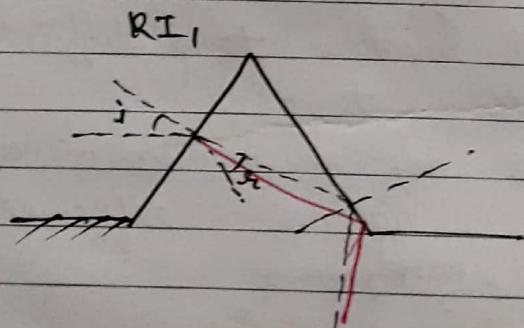


perimeter
on a
wall.

- ① Radiation Temp Detector - Infrared radiation at the
- ② Thermopile. — thermocouple in series

Reaction vessel

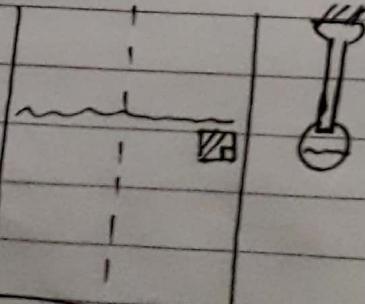
Online
method



$$RI_1 \sin i = RI_2 \sin r$$

Location of laser spot is captured.

Level sensor



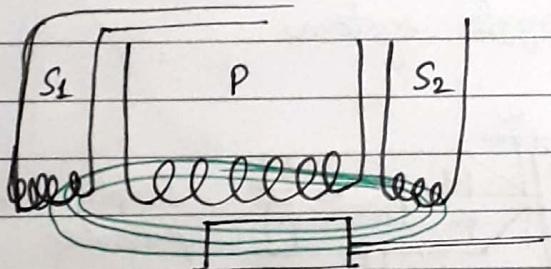
which sensor



Voltage \rightleftharpoons Displacement

Displacement to voltage

Linear Differential Variable Transformer



Coils in opposite dirⁿ and in opp.

Coulson Richardson Vol 3 Chapter 6

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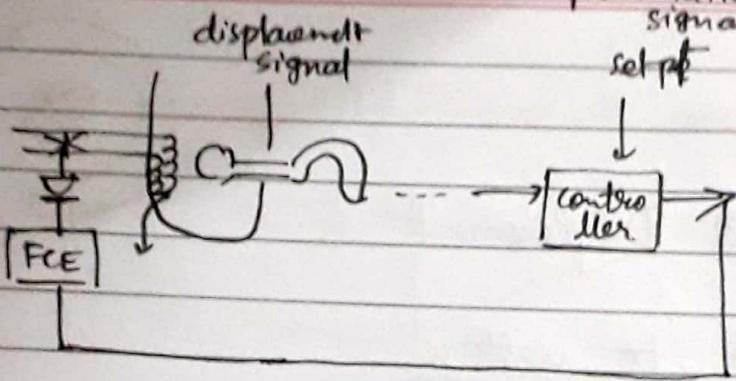
Types of thermocouple,

J	Iron	constantan ($Cu + Ni^0 + Mn$)	-190 to 760
K	Chromel ($Cr + Ni$)	Alumel ($Al + Ni^0 + Mn$)	-190 to 1260
E	Chromel	Constantan	-100 to 1260
T	Copper	Constantan	-200 to 371

Pneumatic :- air

Complete hardware of a pneumatic control system

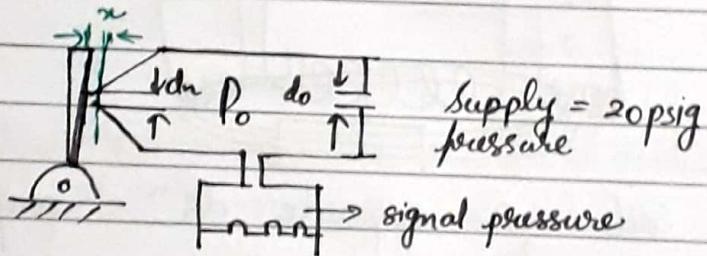
Pneumatic controls → use compressed air as the power source, are very simple and inherently analog making them ideal for controlling temp, humidity and pressure.



No voltage signal, everything - air pressure. 3-15 psi

① Sensor

② Flapper - Nozzle system



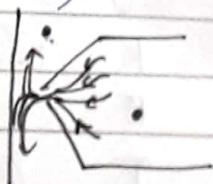
$$\frac{1}{2} \rho v^2 + \text{constant} = P$$

v_n → velocity at nozzle side

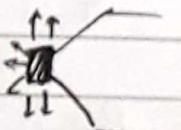
$$\text{flow through nozzle} = Q_n = \frac{C_o}{\sqrt{1-\beta^4}} \sqrt{\frac{2(P_s - P_0)}{\rho}} P_{atm}$$

Bernoulli

$$\frac{P_0}{\rho} = \frac{d_n^2}{2}$$



Flow area : πd_n^2



$$v_n = \sqrt{\frac{2P_0}{\rho}}$$

$$\frac{\pi d_n^2}{4} \sqrt{\frac{2(P_s - P_0)}{\rho}} = \pi d_n w \sqrt{\frac{2P_0}{\rho} \cdot g}$$

$$d_n^4 \frac{2(P_s - P_0)}{\rho} = (d_n w)^2 2P_0$$

$$2d_n^4 P_s - 2d_n^4 P_0 = 2P_0(d_n w)^2 \times 4$$

The hardware consists of pressure to electric transducers for analog which accept digital outputs.

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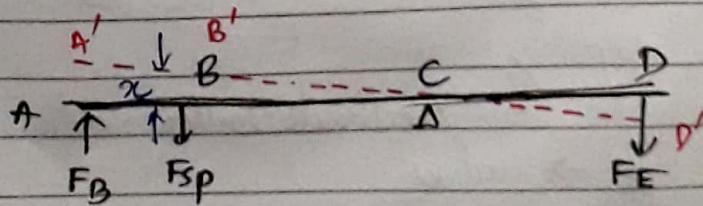
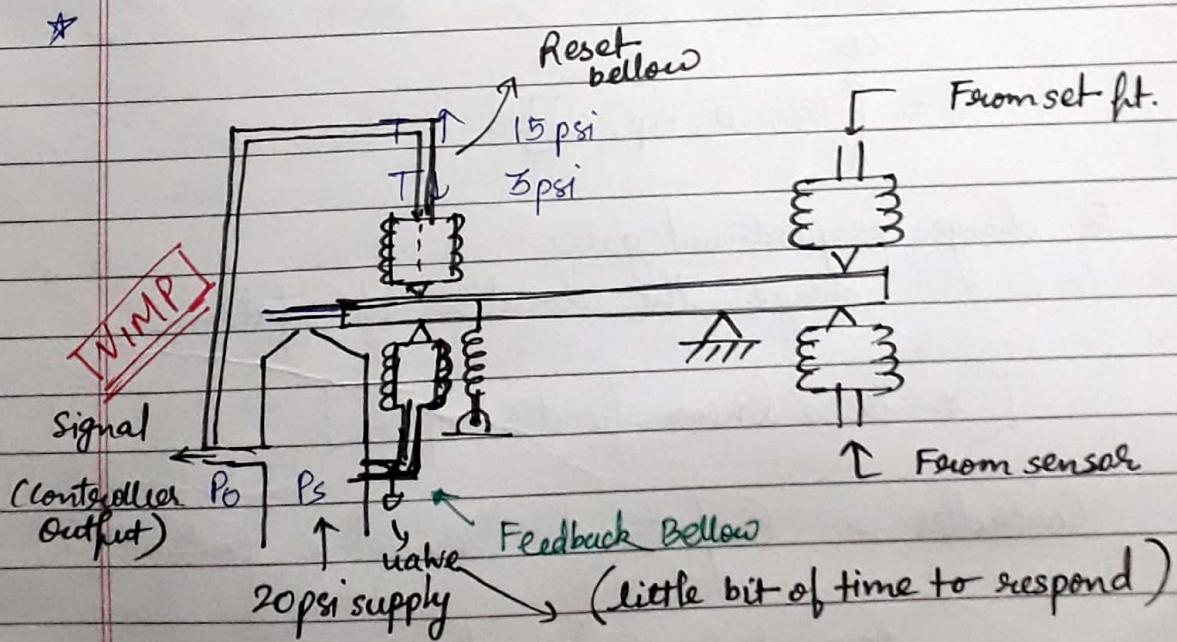
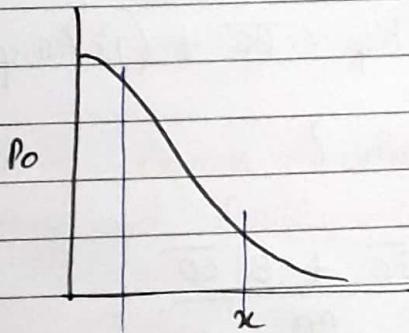
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$$2d_0^4 P_s = 2d_0^4 P_0 + 2P_0(d_n x)^2 \times 16$$

$$d_0^4 P_s = P_0 [d_0^4 + 16(d_n x)^2]$$

$$P_0 = \frac{d_0^4 P_s}{d_0^4 + (d_n x)^2}$$

$$\frac{P_0}{P_s} = \frac{d_0^4}{d_0^4 + (x d_n)^2 \times 16}$$



$$-F_B AC + F_{sp} BC - F_E CD = 0$$

$$-F_{B'} AC + F_{sp'} BC - F_{ECD} = 0$$

$$(F_B - F_{B_0}) AC - (F_{sp} - F_{sp_0}) BC + (F_E - F_{E_0}) CD = 0$$

$\rightarrow F \propto k_x$ (opening)

$$AB(P_0 - P_{0,0}) \cdot AC - K_{sp} \times \overline{BC} + AB, E \cdot \epsilon = 0$$

↑ error signal

at steady state : zero

$$ABC(P_0 - P_{0,0}) AC - K_{sp} \times \overline{BC} + (P_{s AB, sp} - P_{s en AB, sp}) \cdot \overline{AB} = 0$$

Proportional gain ?

$$\begin{aligned} P_0 &= \frac{K_{sp} \times \overline{BC} + \epsilon \cdot \overline{CD}}{AB} \\ &\quad \underbrace{\qquad}_{\overline{CD}} \\ &= [\overline{BC}, \overline{CD}, K_{sp}, AB] \epsilon \end{aligned}$$

To change proportional gain
change the location of fulcrum

[π is a linear function of ϵ]

Controller \rightarrow Proportional Derivative Controller ?

$$P_0 = k \cdot \epsilon + k_{y_i} \frac{d\epsilon}{dt}$$

15 psi \rightarrow

Feedback below action delay slightly
 $T_D \rightarrow$ valve

$$P_0 = k \cdot E + k_y \frac{dE}{dt} + k_I \frac{t}{\tau_i} \int E dt$$

- ① how to relate α to E ?
- ② how the reset below acts as integral action

PNID - ?

16/11/19

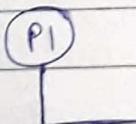
PFD - Process Flow Diagrams.

Piping and Instrumentation Diagram - PID

CS - Carbon Steel

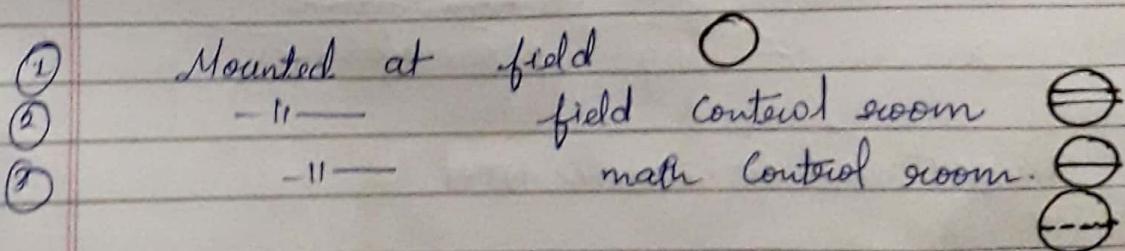
A thick solid line \rightarrow process stream.

- ① Cooling water
- ② C.W. Return
- ③ 265 PSIA Steam
- ④ Condensate
- ⑤ Sample port
- ⑥ Chemical sewer
- ⑦ Vent to (flare) \rightarrow
- ⑧ Clear sewer
- ⑨ Vent to atmosphere



Any circle indicates display of a dial

[] \rightarrow computer display



CLASSMATE
Date _____
Page _____

FFC
Flow controller

2nd variable

$y \rightarrow$ Converter

$c \rightarrow$ Controller

$I \rightarrow$ Indicator

$R \rightarrow$ Recorder

$E \rightarrow$ Sensor

$T \rightarrow$ Transmitter

1st variable

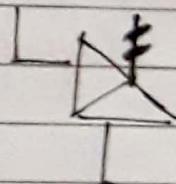
$TI \rightarrow$ Temp Indicator

$FI \rightarrow$ Flow - II -

 \rightarrow hand operated valve



V-109 \rightarrow Reflux drum
Chemical sewer \rightarrow chemical discharge



Pressure release valve

Vent and drain - Important

Fuel gas from reflux drum - some vapor generated taken as fuel gas.

$MV \rightarrow$ fuel gas flowrate

$CV \rightarrow$ Pressure of reflux drum

Sensor - senses the pressure

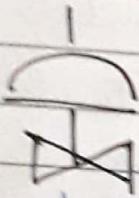
Transmitter - transmits.

----- \rightarrow electrical signal

PAL \rightarrow Pressure low ~~alarm~~ alarm

PAH \rightarrow + high press. alarm

current signal to pneumatic signal.



~~if - then~~ Pneumatic

Nematic control valve

Pressure in reflux drum is controlled by flow rate

P-102A & P-102B → reflux pumps

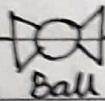
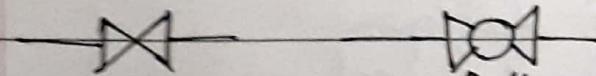
— solid line process fluid

— / — electrical

[VIMP]

- ① Identify certain things in diagram
- ② various lines and their symbols.
- ③ Location of instruments and its accessibility.
- ④ what do letters indicate?

Various valve symbols.



automatically
controlled

control of gas
& vapor

Butterfly (large
pipelines)



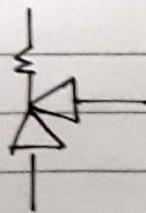
Gate

needle

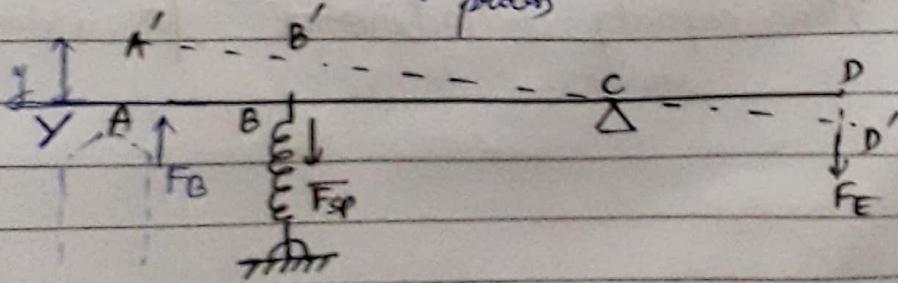
Non Return

outlet of the
displacement
pump

to prevent
back flow
of fluid in a
process



Pressure
relief



$K_{FN} \rightarrow -ve$ number

$$\overline{CD} \epsilon = \overline{BC} K_{sp} BB' - \overline{AC} AB (P_0 - P_{0,0})$$

Flapper Nozzle - linear

$$\overline{CD} \epsilon = \overline{BC} K_{sp} BB' - \overline{AC} AB (K_{FN}, y)$$

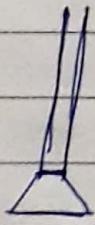
$$\frac{y}{BB'} = \frac{cy}{CB}$$

$$\overline{CD} \epsilon = \frac{\overline{BC} K_{sp} y \cdot CB}{cy} - \overline{AC} AB K_{FN} y$$

$$y = \frac{\overline{CD}}{\left(\overline{BC} K_{sp} \frac{CB}{cy} - \overline{AC} AB K_{FN} \right)} \epsilon$$

$$(P_0 - P_{0,0}) = K_{FN} \overline{CD} \epsilon$$

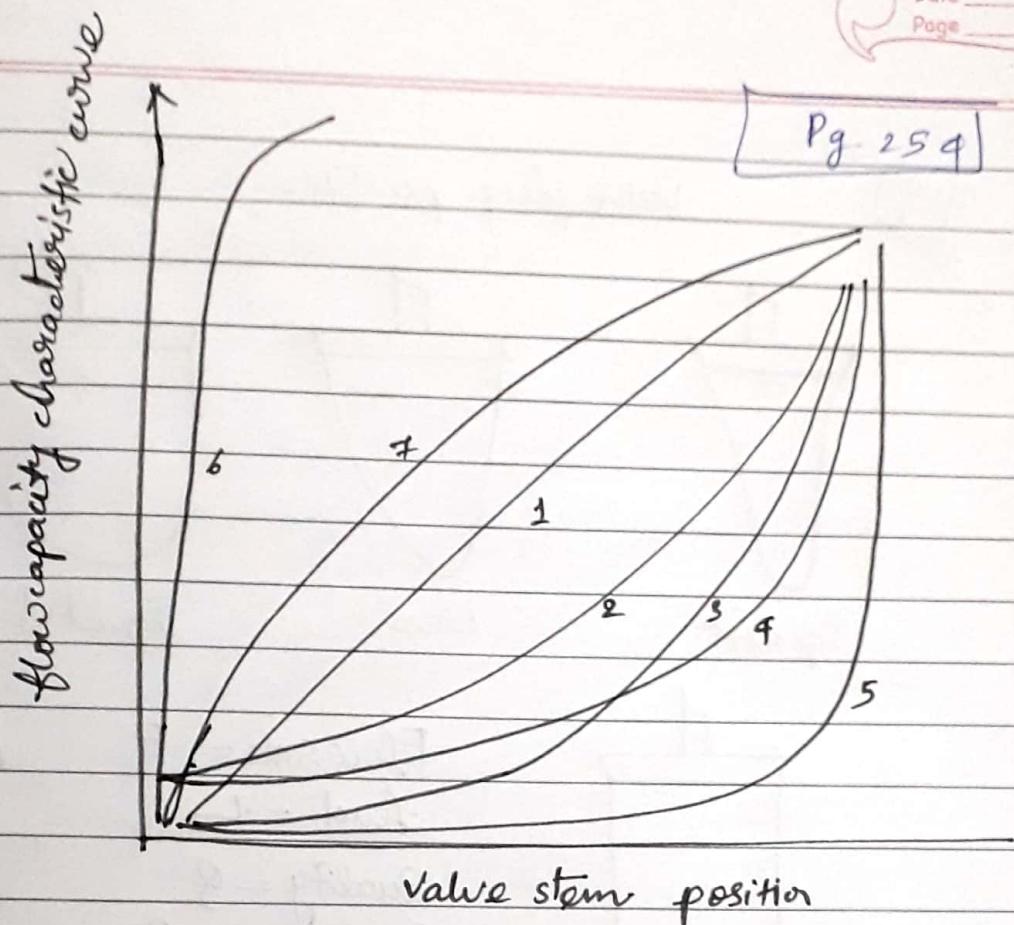
- Control valve
- Pneumatic valves
- ① fail open
 - ② fail closed
 - fail closed fail open



Control valve curve

Flow capacity characteristics for various valves.

Pg. 259



1 Linear

2 Equal % $\alpha = 10$ 3 $\alpha = 50$

4 Hyperbolic

5

6

7

For non flashing liquids the flow through the valve is given by

$$F = K_f(x) \sqrt{\frac{\Delta P}{\rho}}$$

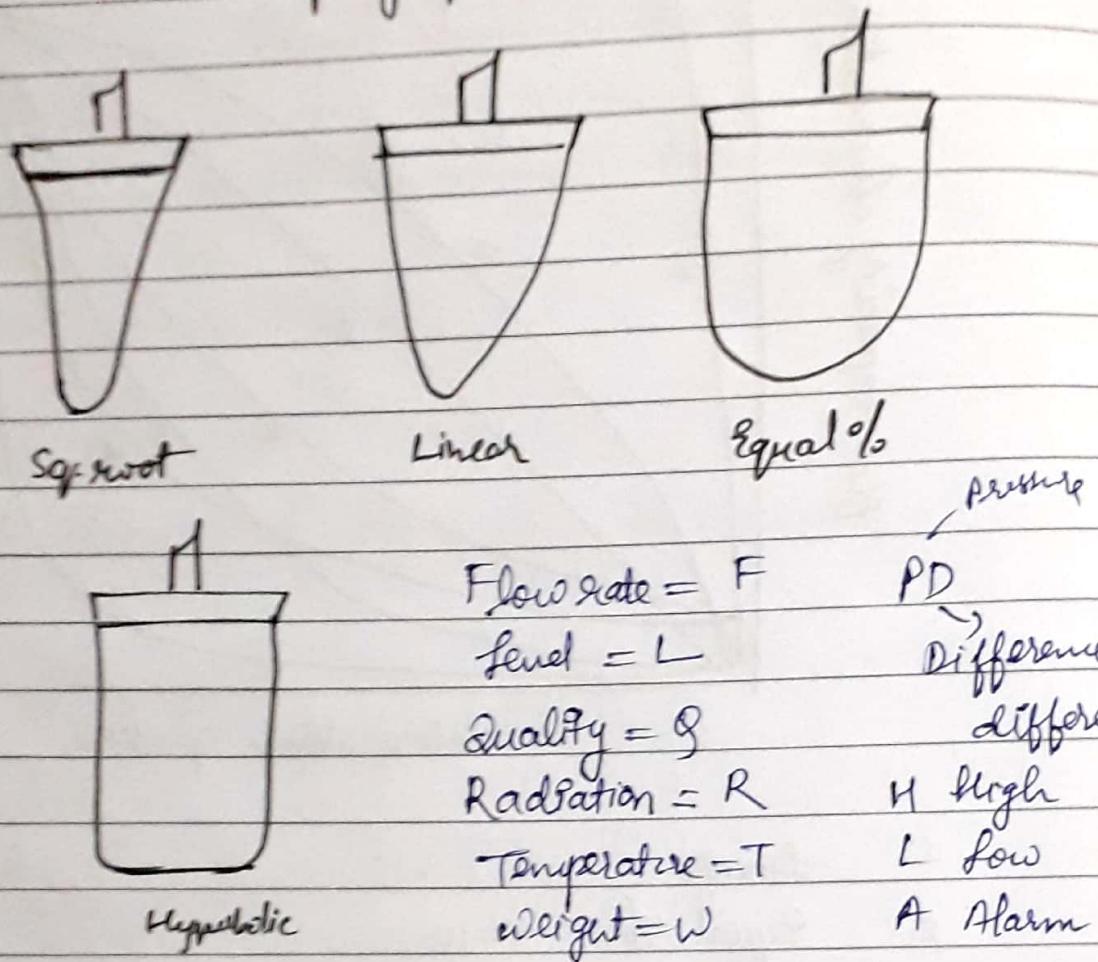
ΔP = pressure drop across the valve

K_f = constant which depends on the valve size

ρ = specific gravity

Study
sheet

Valve plug profile



Advantages of null over deflection &

① Accuracy attained is higher level than that of deflection method.

② Detector can be made very sensitive because it need to cover only small stage around probe while for deflection lots sensitive as it covers large magnitude.

Disadvantages → difficulty in kee

Unless the forces changes very fast or transmission lines are very long, the dynamic behaviors of a pneumatic transmission line can be neglected