

$$\rightarrow P(x) = Y, \quad \omega(t) = X, \quad T(x) = -\frac{Y^2}{8} \rightarrow \text{special case of } \text{SL}$$

If $f(x)$ is odd $\Rightarrow [-L, L] \rightarrow$ expansion of x will work for $[-L, L]$

Fourier cosine series

$$\frac{dy}{dx} + \lambda^2 y = 0 \quad \lambda = \frac{n\pi}{L} \quad n = 0, 1, 2, \dots$$

$$\frac{dy(x)}{dx} = 0 \quad \frac{dy(L)}{dx} = 0$$

$$f(x) = \sum_{n=0}^{\infty} A_n \cos \frac{n\pi x}{L}$$

Period = $2L$

$$f(x) = A_0 + \sum_{n=1}^{\infty} A_n \cos \frac{n\pi x}{L}$$

$$\text{Norm for } n=0 \text{ is } L \quad N_m = \int_0^L \cos^2 \frac{n\pi x}{L} dx$$

$$\int_0^L \cos^2 \frac{n\pi x}{L} dx = \frac{L}{2}$$

$$A_0 = \frac{1}{L} \int_0^L f(x) dx$$

$$A_n = \frac{2}{L} \int_0^L f(x) \cos \frac{n\pi x}{L} dx$$

$$\text{for even function} \rightarrow \text{expansion works for } [-L, L]$$

Fourier Bessel series \rightarrow Heat transfer in cylindrical coordinates

$$\frac{\partial^2 T}{\partial r^2} + \frac{1}{r} \frac{\partial T}{\partial r} + (\lambda^2 r^2 - \nu^2) T = 0 \rightarrow \text{SL problem}$$

(longitudinal
problem)

$$\frac{\partial^2 T}{\partial r^2} + \frac{1}{r} \frac{\partial T}{\partial r} + \lambda^2 r^2 T = 0, \quad \lambda^2 > 0$$

$$\frac{\partial^2 T}{\partial r^2} + \frac{1}{r} \frac{\partial T}{\partial r} + \nu^2 T = 0, \quad \nu^2 > 0$$

$$\text{Solve } \rightarrow R(x) = C_1 J_0(\lambda x) + C_2 Y_0(\lambda x) \quad \text{domain: } [0, L], \quad R(0) = \text{finite} \quad \text{B.C. } \rightarrow C_2 = 0$$

$$Y_0(0) = \text{finite} \rightarrow \int_0^L R(x) dx = 0 \quad C_1 = 0$$

$$d J_0(\lambda x) + \nu^2 J_0(\lambda x) = 0$$

$$d J_0(\lambda x) + d J_0(\lambda x) = 0$$

$$\text{eigen function: } 1 - J_0(\lambda x) \quad \text{eigen value: } -\lambda^2 \quad (n=1, 2, 3, \dots)$$

$$f(x) = \sum_{n=1}^{\infty} A_n J_0(\lambda_n x)$$

$$A_n = \frac{1}{L} \int_0^L f(x) J_0(\lambda_n x) dx \quad N_n = \int_0^L J_0^2(\lambda_n x) dx$$

N_n

$$\text{Separation of variables: } \frac{1}{\alpha} \frac{\partial T}{\partial t} = \frac{\partial^2 T}{\partial x^2} \quad \frac{\partial T}{\partial t} = \nabla^2 T(x, t)$$

Homogeneous, isotropic, axis, stationary, expansible, without heat generation, (constant ρ, k, ϵ)

$$T(x, t) = f(x) \sin \omega t$$

$$\frac{\partial T}{\partial t} = \omega \sin \omega t \quad \frac{\partial^2 T}{\partial x^2} = f''(x) \quad f''(x) = -\omega^2 f(x)$$

$$f''(x) = -\omega^2 f(x) \quad \omega^2 > 0$$

$$\frac{1}{\alpha} \frac{\partial^2 T}{\partial x^2} = \omega^2 T(x, t) \quad \nabla^2 T(x, t) = \omega^2 T(x, t)$$

Separation of variables

$$\frac{1}{\alpha} \frac{d\Gamma(t)}{dt} = \frac{1}{\psi(y)} \nabla^2 \psi(y) = \text{const} (-\lambda^2)$$

$$\Gamma(t) = C e^{-\alpha \lambda^2 t}$$

$$\nabla^2 \psi(z) + \lambda^2 \psi(z) = 0$$

$$\text{boundary condition} \quad \frac{\partial \psi}{\partial y} = \psi(0) + \lambda \psi(2) = 0$$

$$\text{General soln: } \Gamma(z, t) = \sum_{n=0}^{\infty} C_n e^{-\alpha \lambda_n^2 t} \psi_n(z)$$

$$C_n = \int_0^2 f(x) \psi_n(x) dx$$

$$\text{Ambient} = T_\infty \quad \text{heat transfer coeff} = h = \text{very large} \\ \text{find steady state } T(z, 0) \\ k = \text{constant} \quad \frac{\partial T}{\partial z} = \frac{k \Delta T}{L} + k \frac{\partial T}{\partial y} \quad \frac{\partial T}{\partial y} = 0 \\ \frac{\partial^2 T}{\partial z^2} = -k \frac{\partial T}{\partial z} \quad \frac{\partial T}{\partial z} = 0 \quad \Rightarrow T(z, 0) = T_\infty$$

Consider an infinitely long 2D fin of thickness L

Examples



$$\frac{\partial^2 T}{\partial x^2} + \frac{\partial^2 T}{\partial y^2} = 0$$

$$\frac{\partial T}{\partial x} + \frac{\partial T}{\partial y} = 0$$

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Separation of variables

can be used if

at least 3 BC are

homogeneous &

DE is linear and

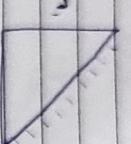
homogeneous

$$\theta(x, y) = f(y) - T_\infty = F(y)$$

$$\theta(x, 0) = 0$$

$$\theta(x, L) = 0$$

Thermal symmetry with an axially boundary.



T_1 (optimal symmetry)
 T_2 (optimal symmetry)

$$\frac{\psi}{R} \frac{\partial}{\partial r} \left(\frac{\partial \psi}{\partial r} \right) + \frac{R}{r^2} \frac{\partial^2 \psi}{\partial \theta^2} = 0$$

$$\frac{\psi}{R} \frac{\partial}{\partial r} \left(\frac{\partial \psi}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 \psi}{\partial \theta^2} = 0$$

$$\frac{1}{R} \frac{\partial \psi}{\partial r} \left(\frac{\partial \psi}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 \psi}{\partial \theta^2} = 0$$

$$\frac{1}{R} \frac{\partial \psi}{\partial r} \left(\frac{\partial \psi}{\partial r} \right) = - \frac{1}{r^2} \frac{\partial^2 \psi}{\partial \theta^2} = \pm \lambda^2$$

$$\frac{\partial \psi}{\partial r} \left(\frac{\partial \psi}{\partial r} \right) = \pm \lambda^2 r^2$$

$$\psi = A n \sin \frac{n\theta}{R}$$

a)



T_1
 T_2
 $k = \text{const}$

$$\frac{\partial \psi}{\partial r} \left(\frac{\partial \psi}{\partial r} \right) + \frac{1}{r^2} \frac{\partial^2 \psi}{\partial \theta^2} = 0$$

$$(\lambda, \theta) \otimes$$

$$(\lambda, r)$$

$$(\lambda, r)$$

$$A_n = n \pi$$

$$R = 1$$

$$R \sin \theta$$

$$R \cos \theta$$

$$R = 1$$

SEPARATION OF VARIABLES

→ finite fourier transform → rectangular coordinates

(exp sine series)

$$f(x) = \sum_{n=0}^{\infty} A_n \cos nx$$

→ TRANSFORM METHODS → Markov Transform → cylindrical coordinates

(a) Laplace transform

(b) Fourier transform

$$K_n(x) = \frac{1}{\sqrt{N_m}} \int_0^{N_m} f(x) \cos nx dx$$

$$N_m = V_2, n = 1, 2, \dots$$

$$(1) \quad 2D PDE \xrightarrow{\text{FFT}} \text{ODE } T(x) \xrightarrow{\text{solve}} \left(\frac{d^2}{dx^2} + k^2 \right)^{-1}$$

T(x,y) $\xrightarrow{\text{take inverse}}$

$$\frac{d^2y}{dx^2} + k^2 y = 0$$

finite fourier transform

$f(x)$ which is piecewise differentiable in $[0, L]$ can be expanded in sine series.

$$f(x) = \sum_{n=1}^{\infty} A_n \sin\left(\frac{n\pi}{L}x\right)$$

$$A_n = \frac{2}{L} \int_0^L f(x) \sin\left(\frac{n\pi}{L}x\right) dx$$

$$f(x) = \frac{2}{L} \sum_{n=1}^{\infty} \left[\int f(x) \sin\left(\frac{n\pi}{L}x\right) dx \right] \sin\left(\frac{n\pi}{L}x\right)$$

assuming: let $k_n = \frac{2}{L} \sin\left(\frac{n\pi}{L}x\right)$ → kernel of transformation

normalized eigen value eigen function

$$K_n(x) = \frac{1}{\sqrt{N_m}} \phi_n(x)$$

$\phi_n(x) = \frac{2}{L} \sin\left(\frac{n\pi}{L}x\right)$ → Inversion formula

exp function

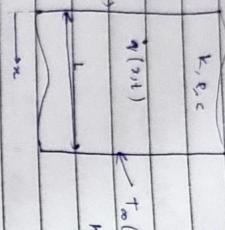
for $\sin\left(\frac{n\pi}{L}x\right)$

it is $\frac{1}{L}$

Q)

$$At \lim t \rightarrow \infty, T(x, t) = T_1(x)$$

$\psi(x, t) \rightarrow T_\infty(t)$
1D unsteady state heat conduction with space time dependent h_2 and environment temperature



[Consider h_1, h_2 high]

$$\frac{1}{k} \frac{\partial T(x, t)}{\partial x} - \frac{\partial^2 T(x, t)}{\partial x^2} - \frac{\partial^2 T(x, t)}{\partial t^2} = 0 \quad (\text{cannot solve using separation of variables})$$

$$T(x, 0) = T_0(x)$$

$$T(0, t) = T_\infty(t)$$

define transformation of $T(x, t)$

operator in linear

U(t). you are applying it

$$\bar{T}_n(t) = \int_0^L T(x, t) k_n(x) dx$$

Kernel \rightarrow normalized eigen value function

(how to get kernel?)

Kernel is $\int_0^L k_n(x) T(x, t) dx$ \rightarrow linear homogenous DE

$$\frac{1}{k} \frac{\partial^2 U}{\partial x^2} = \frac{\partial^2 U}{\partial t^2}$$

get eigen function from this

$\psi(x, t) = T_0(x) + \psi_1(x, t)$ \rightarrow then get kernel from this

$$\psi_1(x, t) = 0$$

$$U(x, t) = X(x) T(t)$$

$$d^2U + \lambda^2 U = 0$$

$$X(0) = 0$$

$$X(L) = 0$$

$$\sin(\lambda L) = 0$$

$$\lambda L = n\pi$$

$$X(x) = \sqrt{\frac{2}{L}} \sin \frac{n\pi}{L} x$$

$$U_n(x) = \sqrt{\frac{2}{L}} \sin \frac{n\pi}{L} x$$

$$U_n''(x) = \sqrt{\frac{2}{L}} \times n\pi \cos \frac{n\pi}{L} x$$

$$U_n(x) = \sqrt{\frac{2}{L}} \sin \frac{n\pi}{L} x$$

3. b steady state

$$\frac{1}{a} \frac{d\bar{T}_n(t)}{dt} = T_{\infty}(t) \left[\sqrt{\frac{2}{L}} \frac{\partial}{\partial x} - \sqrt{\frac{2}{L}} \frac{\partial}{\partial x} \cos nx \right] \bullet \int_0^L \left(\frac{2}{L} \bar{n}^2 \sin nx \cdot T(x,t) \right) dx + \frac{\dot{q}_n(t)}{k}$$

$$\frac{1}{a} \frac{d\bar{T}_n(t)}{dt} = T_{\infty}(t) \left[\sqrt{\frac{2}{L}} \frac{\partial}{\partial x} - \sqrt{\frac{2}{L}} \frac{\partial}{\partial x} \cos nx \right] \left[- \frac{n^2}{L^2} \bar{T}_n(t) + \frac{\dot{q}_n(t)}{k} \right]$$

$$\frac{1}{a} \frac{d\bar{T}_n(t)}{dt} = T_{\infty}(t) \left[\sqrt{\frac{2}{L}} \frac{\partial}{\partial x} - \sqrt{\frac{2}{L}} \frac{\partial}{\partial x} \cos nx \right] \left[- \frac{n^2}{L^2} \bar{T}_n(t) + \frac{\dot{q}_n(t)}{k} \right]$$

$$2\frac{d\bar{T}}{dt} + 2\frac{d\bar{T}}{dt} = 0$$

$$\frac{d\bar{T}_n(t)}{dt} + \alpha \lambda_n^2 \bar{T}_n(t) = \alpha \int_{\infty}(t) \lambda_n \sqrt{\frac{2}{L}} \left[1 - (-1)^n \right] + \frac{\dot{q}_n(t)}{k}$$

$\bar{T}_n(t)$

$$\frac{d\bar{T}_n(t)}{dt} + \alpha \lambda_n^2 \bar{T}_n(t) = \alpha F_n(t)$$

$\frac{d\bar{T}_n(t)}{dt}$

→ eigen value problem in x domain

$$\bar{T}_n(t) e^{\alpha \lambda_n^2 t} = \int_0^L F_n(t) e^{\alpha \lambda_n^2 t} dt$$

$$\bar{T}_n(t) = e^{-\alpha \lambda_n^2 t} \int_0^L F_n(t) e^{\alpha \lambda_n^2 t} dt + \bar{T}_n(0)$$

$$\bar{T}_n(t) = \int_0^L T(x,0) k_n(x) dx = \int_0^L T_n(x) k_n(x) dx$$

$$\Psi = X(x) Y(y)$$

$$\frac{1}{x} \frac{dX}{dx} = - \frac{1}{Y} \frac{dY}{dy} = \lambda_n^2$$

$$\lambda_n = \frac{n\pi}{L} \rightarrow$$

$$T(x,t) = \sum_{n=1}^{\infty} k_n(x) \bar{T}_n(t)$$

49

$\lambda = 0$
const. c, ϵ, μ

$$\begin{cases} \tau = f_1(x) \\ y = 0 \end{cases}$$

$$\begin{cases} T(x,y) = 0 \\ \tau = 0 \end{cases}$$

x

y

$$\begin{cases} x = 0, T(0,y) = 0 \\ \tau(a,y) = 0 \end{cases}$$

$$y = 0, T(x,0) = 0$$

x

y

τ

$$\bar{T}_n(y) = \int_0^a k_n(x) T(x,y) dx$$

x

y

τ

$$T(x,y) = \sum_{n=1}^{\infty} k_n(x) \bar{T}_n(y)$$

x

y

τ

$$k_n(x) = \sqrt{\frac{2}{a}} \sin \frac{n\pi x}{a}$$

x

y

τ

→ solved with some infinite width

$$\frac{1}{\pi} \frac{\partial \theta}{\partial x} = \frac{\partial^2 \theta}{\partial x^2}$$

$$\theta(x, 0) = \gamma \tau_i(x)$$

$$\theta(a, t) = \alpha \tau_i(t)$$

$$\theta(b, t) = \theta(T_2, t)$$

applying FFT
convert the domain
(0, π)

Calculation
Change of variable
 $y = x + a$

$$\frac{1}{\pi} \frac{\partial \theta}{\partial y} = \frac{\partial^2 \theta}{\partial y^2}$$

$$\theta(x, 0) = (x + a) \tau_i(x)$$

$$\theta(x+a, t) = (x+a) \tau_i(t)$$

Plane change - the
problem moves with time

Heat conduction with plane change

location of interface is not known
Moving boundary problem
(interface)

Solidification of liquid - (steady state is not possible)

Consider a semi-infinite pool of liquid. (1D)

→ moving boundary problem
→ moving boundary problem

Initially liquid at temp $\geq T_f$
solidifying. At time $t = 0$, bring the

$$\frac{\partial \theta}{\partial x} = \frac{d^2 \theta}{dx^2} + \alpha^2 \theta = 0$$

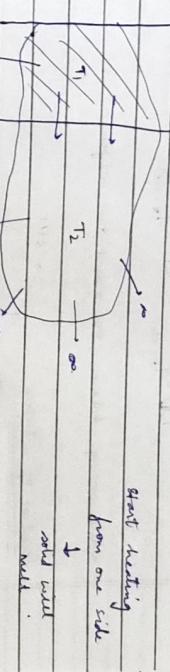
$$\psi = (\sin \lambda x + C_0 \cos \lambda x)$$

$$\sin \lambda (L-a) = 0$$

$$\lambda = \frac{\pi}{L-a}$$

$$\lambda = \frac{\pi}{b-a}$$

$$\ln(\theta) = \sqrt{\frac{2}{b-a}} \int_{b-a}^b \sin \lambda x \, dx$$



$$\frac{1}{\gamma} \frac{\partial(\gamma T_S)}{\partial x} = \frac{1}{\alpha_S} \frac{\partial T_S}{\partial t}$$

$$\frac{1}{\gamma} \frac{\partial}{\partial x} \left(\frac{\gamma T_L}{\gamma - 1} \right) = \frac{1}{\alpha_L} \frac{\partial T_L}{\partial t}$$

$$T_S(0, t) = T_0$$

$$T_0$$

$$\frac{\partial T_S}{\partial x}(0, t) = 0$$

$$T_S(0, t) = T_0$$

$$T_L(2 = s(t), 2, t) = T_3$$

$$k_L \frac{\partial T_L}{\partial x} \Big|_{x=2, t} = k_S \frac{\partial T_S}{\partial x} \Big|_{x=2, t} + \text{exch} \frac{\partial T_L}{\partial t} = 0$$

$$s(t=0) = 0$$

$$T_S(x, t) \Big|_{s(t)} = T_L(x, t) \Big|_{s(t)} = T_3$$

$$\frac{1}{\alpha_S} \frac{\partial T_S(x, t)}{\partial t} = \frac{1}{\alpha_L} \frac{\partial T_L(x, t)}{\partial t}$$

$$T_L(2, t) = T_3$$

$$T_L(2 = s(t), t) = T_3$$

$$k_L \left(- \frac{\partial T_L}{\partial x} \right) \Big|_{s(t)} + k_S \left(\frac{\partial T_S}{\partial x} \right) \Big|_{s(t)} + \text{exch} \frac{\partial T_L}{\partial t} \Big|_{s(t)} = 0$$

solidification

line heat sink

line heat sink

initially

heat a line

solid source line

line

solid source line

line

line

line

non-linear

isolate

isolate, k_S , α_S , k_L , α_L

constant

it says that

move with a velocity

which is the difference in the

jump between the heat

fluxes of solid & liquid phases

Non-dimensional form

$$\theta_2 = \frac{T_2 - T_3}{T_3 - T_0} \quad \theta_L = \frac{k_L}{k_3} \frac{T_L - T_3}{T_3 - T_0}$$

$$\theta = \frac{\theta_2}{L} \quad \tau = \frac{k_3}{L^2} \theta L \quad \text{Biot number}$$

$$St = \text{Stefan number} = \frac{\theta_2}{L} \frac{T_3 - T_0}{k_3} \quad \text{for wall}$$

specific heat latent heat capacity of soil

if θ is very small \rightarrow we can assume quasi steady state approx.

6 small Stefan number ($St = < 0.1$)

Case 1: θ is small

thermal diffusivity α is very large \rightarrow mean heat propagates with no species

Case 2: heat is very little \rightarrow $ds/dt = 0$.

boundary is not of stationary

moment natural mass is achieved

$$\frac{\partial T_2}{\partial t} = 0, \frac{\partial T_2}{\partial x} = 0$$

1) quasi steady state $\rightarrow T_L(x, t) = T_F$

2)

$$\frac{\partial^2 T_2}{\partial x^2} = 0$$

3) boundary condition

1) boundary

2) boundary

3) boundary

4) boundary

5) boundary

6) boundary

7) boundary

8) boundary

9) boundary

10) boundary

11) boundary

12) boundary

13) boundary

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Penne Bio-heat equation

$B = \text{const}$
parameter α must also be a const, independent of time.

$$Q(\eta) = \alpha f(\eta)$$

$$\frac{T_f - T_0}{T_f - T_0} = \frac{\alpha f(\frac{\eta}{2\sqrt{kt}})}{\alpha f(1)}$$

$$\frac{k \frac{\partial T}{\partial \eta}}{\eta = s(t)} + \text{other terms} \rightarrow \frac{d}{dt} \int_{\eta=0}^1 e^{\eta^2/4kt} d\eta = \frac{1}{\sqrt{\pi}} s(t)$$

use separation of variables
to find

function λ \rightarrow eigenvalues

$s(t) = c(\frac{T_f - T_0}{\lambda}) \rightarrow$ variable heat

heat loss \rightarrow latent heat

$s(t) \ll 1$, simplification process is very rapid

$s(t) \gg 1 \rightarrow$ simplification is shown

$$s(t) \approx \frac{1}{\lambda} s(t) \rightarrow \text{non-linear homogeneous algebraic}$$

equation and cannot be solved

\rightarrow $s(t) = \frac{1}{\lambda} \int_0^t \text{exp}(-\lambda(t-s)) \text{exp}(s) ds$

\rightarrow $s(t) = \frac{1}{\lambda} \text{exp}(-\lambda t) \int_0^t \text{exp}(\lambda s) ds$

$$s(t) = \frac{1}{\lambda} \text{exp}(-\lambda t) \int_0^t \text{exp}(\lambda s) ds$$

$$\text{but } s(t) \text{ is small, } \lambda \text{ is also small}$$

$$s(t) \approx \frac{1}{\lambda} \text{exp}(-\lambda t)$$

$$\text{numerical solution}$$

$$(\text{with time step adjustment})$$

heat resistance η

Heat exchange through the skin

advection \rightarrow convection \rightarrow complex nature of heat transfer in living tissue precludes exact mathematical model

Assumptions
1. Equilibrium state \rightarrow heat exchange takes place between blood & tissue only
2. Blood perfusion \rightarrow no effect of direction
3. Vascular network

4. Blood temperature \rightarrow temp in the artery is assumed to be same as body core temp
5. Fourier's law \rightarrow $\frac{dQ}{dA} = -k \frac{\partial T}{\partial x}$
6. $\text{Q} = \text{Q}_b + \text{Q}_m + \text{Q}_v + \text{Q}_s$
 $\text{Q}_b = \text{Q}_b \text{exp}(-\lambda t) \rightarrow$ blood perfusion is an exponential function of heat
 $\text{Q}_m = \text{Q}_m \text{exp}(-\lambda t) \rightarrow$ metabolic heat loss \rightarrow volume of tissue
 $\text{Q}_v = \text{Q}_v \text{exp}(-\lambda t) \rightarrow$ latent heat loss \rightarrow volume of tissue
 $\text{Q}_s = \text{Q}_s \text{exp}(-\lambda t) \rightarrow$ sensible heat loss \rightarrow volume of tissue

$$\text{Eq} = \int_{\text{skin}}^{\text{blood}} \text{heat flux} dx = (\text{Q}_b + \text{Q}_m + \text{Q}_v) dx \text{ for } dx$$

specifying heat flux

$$\text{Q}_b = \text{Q}_b \text{exp}(-\lambda t) (\text{T}_{\text{core}} - \text{T})$$

blood volumetric flow rate per unit tissue volume

$$\text{Q}_m = \text{Q}_m \text{exp}(-\lambda t) (\text{T}_{\text{core}} - \text{T})$$

heat flux

$$\text{Q}_v = \text{Q}_v \text{exp}(-\lambda t) (\text{T}_{\text{core}} - \text{T})$$

heat loss

$$\text{Q}_s = \text{Q}_s \text{exp}(-\lambda t) (\text{T}_{\text{core}} - \text{T})$$

heat loss

$$\text{Q} = \text{Q}_b + \text{Q}_m + \text{Q}_v + \text{Q}_s$$

$\frac{dQ}{dt} = \text{Q}_b \text{exp}(-\lambda t) (-\lambda) + \text{Q}_m \text{exp}(-\lambda t) (-\lambda) + \text{Q}_v \text{exp}(-\lambda t) (-\lambda) + \text{Q}_s \text{exp}(-\lambda t) (-\lambda)$

$$\frac{dQ}{dt} = -\lambda (\text{Q}_b + \text{Q}_m + \text{Q}_v + \text{Q}_s)$$

Penne Bio-heat

$$\frac{\partial C}{\partial r} = -\frac{\partial \eta}{\partial r} + (C_C)_{\text{heat}}(T_b - \eta) + \eta_m$$

Assume that

$$\nabla \cdot \mathbf{u} (r, t) + \eta_{\text{convection}} (T_b - \eta) + \eta_m = \rho C \frac{\partial \eta}{\partial r}$$

Convection
(convection)

radiative heat generation Strong

Cattaneo and Venetis

$$\eta(t, r) = -k \nabla T(t, r) \rightarrow \text{fourth law holds}$$

heat flows with no speed.

~~Stokes~~
 $\delta_r(r, t)$ → radiation of heat source term

fourth law will not work when η is high temp nature.

$$\rightarrow k \frac{\partial \eta}{\partial r} + \eta_{\text{radiation}} (T_b - \eta) + \eta_m + \delta_r(r, t) = \rho C \frac{\partial \eta}{\partial r}$$

similar to fin

mathematical role of $\delta_r(r, t)$ in finned ex is identical to surface convection in fin, the same effect no difference in ~~porous~~ porous

$$= \rho C \frac{\partial \eta}{\partial r} + (C_C + \kappa \delta_r) \frac{\partial \eta}{\partial r} = k \frac{\partial \eta}{\partial r} + \eta_m + \eta_{\text{radiation}}$$

Convection

similar to
heat transfer in circular rod

Heat conduction with 2-phase system

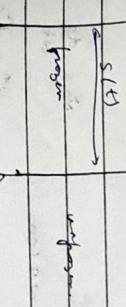
Moving region → melts at range of temperature instead of sharp temp change

unfrozen → melting tissue (alive metabolism)
frozen → ischemia (killed cells) (No blood perfusion) (No blood)

$$\frac{d\eta(r)}{dr} \rightarrow \eta(r) = \text{finite}$$

Exogen:

$$\frac{d\eta(r)}{dr} = h(\eta(r) - T_m)$$



Phase change

$$\frac{d\eta(r)}{dr} = h(\eta(r) - T_m)$$

Steady state equation

$$\frac{\partial u}{\partial x} + \frac{\partial u}{\partial y} + \frac{\partial u}{\partial z} = 0 \quad \text{for } 0 \leq x \leq l, 0 \leq y \leq b, 0 \leq z \leq h$$

tissue

blood

artery

Conditions at interface

$$T_{\text{in}}(x, 0) + \frac{\partial T}{\partial z}(x, 0) = (1 + \beta + \gamma) T_{\text{in}}(x, 0)$$

vein

artery

$$\frac{\partial T}{\partial z}(x, h) = T_{\text{out}} = T_{\text{in}}(x, h)$$

artery

vein

Some care for bone surgery

Non-porous case

Conjugate (hyperbolic)

non-porous case

step function with change

→

$$\begin{aligned} & \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2} = 0 \quad \text{in } 0 \leq x \leq l, 0 \leq y \leq b, 0 \leq z \leq h \\ & u(x, 0) = u_{\text{in}}(x) \\ & u(x, h) = u_{\text{out}}(x) \\ & \frac{\partial u}{\partial z}(x, 0) = \frac{u_{\text{in}}(x) - u_{\text{out}}(x)}{h} \\ & \frac{\partial u}{\partial z}(x, h) = 0 \end{aligned}$$

Laplace transform

$$\tilde{f}(p) = \mathcal{L}\{f(t)\} = \int e^{-pt} f(t) dt$$

Laplace transformation is linear

$$\mathcal{L}\{u_1(t) + u_2(t)\} = \mathcal{L}\{u_1(t)\} + \mathcal{L}\{u_2(t)\}$$

Existence of Laplace transform

It will not exist if

- (1) $f(t)$ has infinite discontinuities for some values of t ,
- (2) $f(t)$ has singularity at $t \rightarrow 0$,
- (3) $f(t)$ is not bounded.

First shift property : $\tilde{f}(p) = \mathcal{L}\{f(t)\}$

$$\mathcal{L}\{e^{at} f(t)\} = \tilde{f}(p-a)$$

Second shifting property : $\tilde{f}(p) = \mathcal{L}\{f(t-a)\}$

$$f(t) = \begin{cases} f(t-a) & t > a \\ 0 & t < 0 \end{cases}$$

$$\mathcal{L}\{f(t-a)\} = e^{-at} \tilde{f}(p)$$

change of scale property

$$\tilde{f}(p) = \mathcal{L}\{f(x)\}$$

$$\mathcal{L}\{f(ax)\} = \frac{1}{a} \tilde{f}\left(\frac{p}{a}\right)$$

$$\mathcal{L}\left\{ \frac{dt}{dt} \right\} = p \tilde{f}(p) - f(0)$$

Convolution theorem

$$\mathcal{L}^{-1}\{\tilde{f}(p)\} = t^{-1} \mathcal{L}^{-1}\{\tilde{g}(p)\} = \int g(t-t') h(t') dt'$$

$$\tilde{T}(z, p) = C_1 \cosh(pz) + C_2 \sinh(pz) + \frac{T_1}{p}$$

$z=0$

$\rightarrow \infty$

$$z=L \rightarrow \infty \rightarrow C_2 = 0$$

$$C_1 = \frac{T_1 - T_{L0}}{p}$$

\rightarrow cash out.

$$g * h = h * g$$

Q) 1D plane wall

$$\frac{d\theta}{dx} = 0, \quad t=0, \quad T = T_i$$

$$\frac{1}{2} \frac{d\tilde{T}}{dt} = \frac{2\tilde{T}}{2x}, \quad \left. \begin{array}{l} x=\pm L, \quad T=T_{L0} \\ t=0, \quad T=T_i \end{array} \right\} \quad \frac{1}{2} \frac{d\tilde{T}}{dt} = \frac{2\tilde{T}}{2x}, \quad \left. \begin{array}{l} t=0, \quad T(0,0)=T_i \\ T(0,0)=T_{L0} \end{array} \right\} \quad \frac{1}{2} \frac{d\theta}{dt} = \frac{2\theta}{2x}$$

$$\theta(0,0) = 0$$

$$\theta(0,t) = T_{L0} - T_i$$

$$t \rightarrow \infty$$

(no plane damage)

→ semi-infinite solid

40 min 9 questions

$$\frac{\partial \tilde{T}}{\partial x} = \frac{1}{2} \frac{d\tilde{T}}{dt} = \frac{2\tilde{T}}{2x}$$

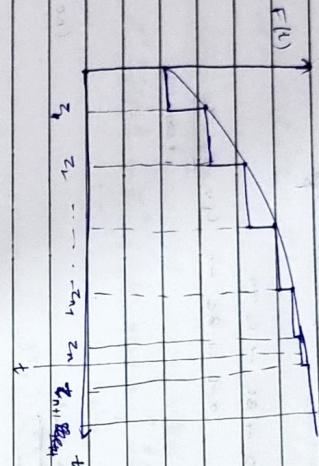
$$\frac{\partial \tilde{T}}{\partial x} = 0, \quad T(0,t) = T_{L0}$$

$$T(0,0) = T_i$$

Duhamel method

linear system with time dependent B.C. or time dependent internal energy generation.

$F(t)$



Semi infinite domain

$$z_1, z_2, \dots, z_n, z_{n+1}, t$$

$$\frac{\partial^2 \theta}{\partial x^2} = \frac{1}{\alpha} \frac{\partial \theta}{\partial t}$$

$$\theta(x, 0) = 0$$

$$\theta(0, t) = f(t) \text{ and } \theta(x, t) = 0 \text{ for } x > 0.$$

$$f(t) = f(t) - T_1$$

approximate $f(t)$ as a piecewise ~~step~~ function.

let $f(t)$ be solved

(will now do direct 1D forward heat conduction)

Inverse heat conduction

Given a solid, \mathbf{g} have the temp distribution and want to find B.C. \rightarrow This is called inverse heat conduction.

$$\text{Assume } g(t) = P_0 + P_1 t + P_2 t^2 + \dots + P_n t^n.$$