

Aerodynamics and Numerical Simulation Methods

Karman Momentum Integral Equation



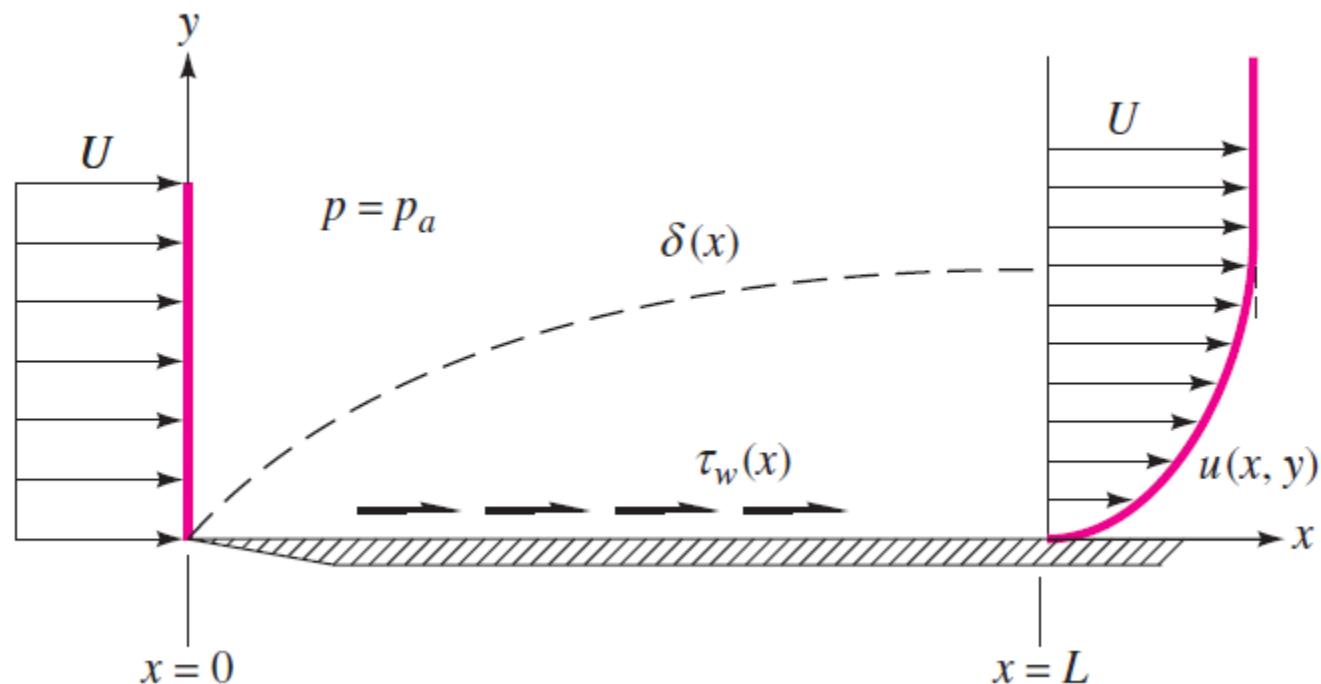
University of
BRISTOL

Topics for today

- Wall and edge boundary conditions
- Conservation of mass and momentum
- Momentum Integral Equation (MIE)
- Use of MIE

Flat-plate boundary layer

- Consider a steady 2D flow over a flat plate in the x direction



Wall Boundary Conditions:

- At the wall, $y=u=v=0$, and hence:

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} = - \frac{1}{\rho} \frac{dp}{dx} + \nu \frac{\partial^2 u}{\partial y^2}$$

$$\frac{dp}{dx} = \mu \left(\frac{\partial^2 u}{\partial y^2} \right)_{wall}$$

Kinematic
viscosity

Edge Boundary Conditions:

- At the boundary layer edge:
 - $u = u_e$, derivatives w.r.t $y = 0$ (by definition of the boundary layer edge). Hence:

$$u \frac{\partial u}{\partial x} + v \cancel{\frac{\partial u}{\partial y}} = -\frac{1}{\rho} \frac{dp}{dx} + v \cancel{\frac{\partial^2 u}{\partial y^2}}$$

$$\frac{dp}{dx} = -\rho_e u_e \frac{du_e}{dx}$$

Kinematic viscosity

$$\boxed{\frac{dp}{dx} = -\rho_e u_e \frac{du_e}{dx} = \mu \left(\frac{\partial^2 u}{\partial y^2} \right)_{wall}}$$

Flat Plate with no Pressure Gradient

- In uniform flow over a flat plate there is no pressure gradient, i.e.

$$\frac{dp}{dx} = 0$$

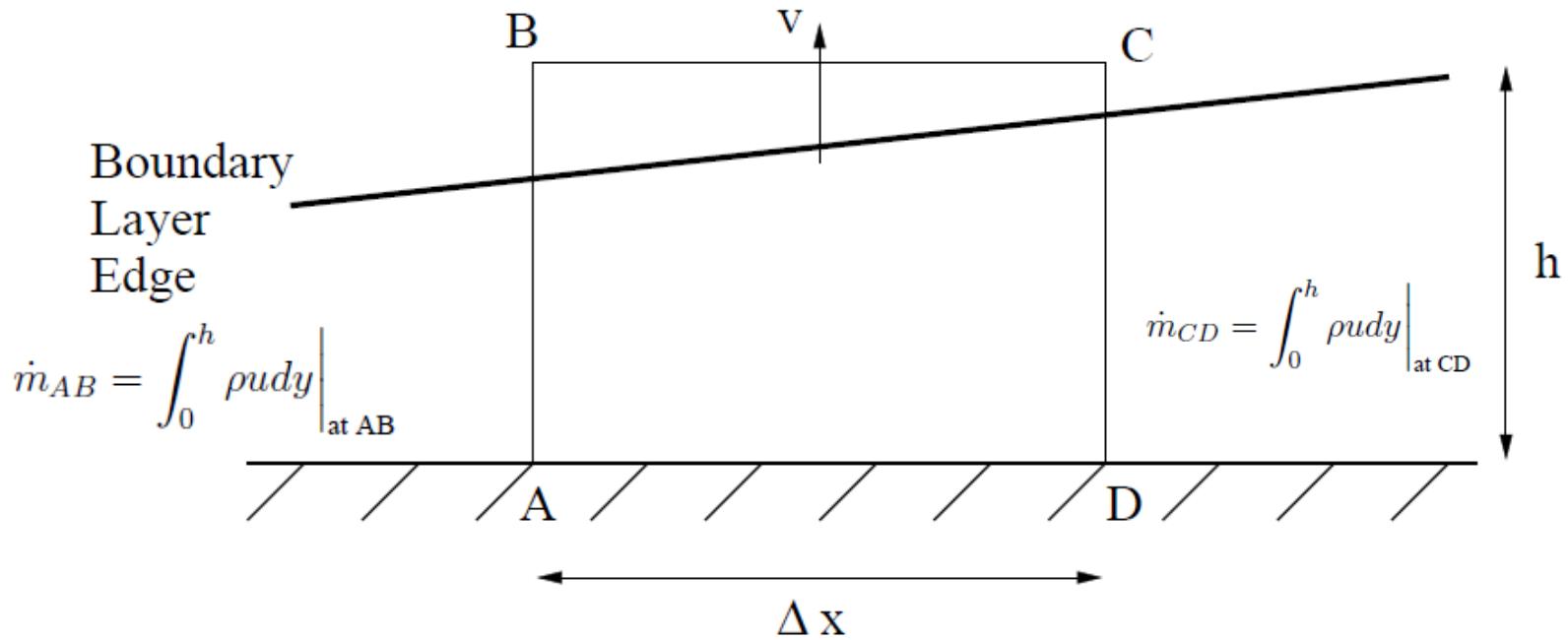
- and hence

$$\left(\frac{\partial^2 u}{\partial y^2} \right)_{wall} = 0$$

- This makes it a special case, reducing the number of boundary conditions to be solved – allows an accurate solution to be derived

Conservation of mass

$$0 = (\text{mass in}) - (\text{mass out})$$



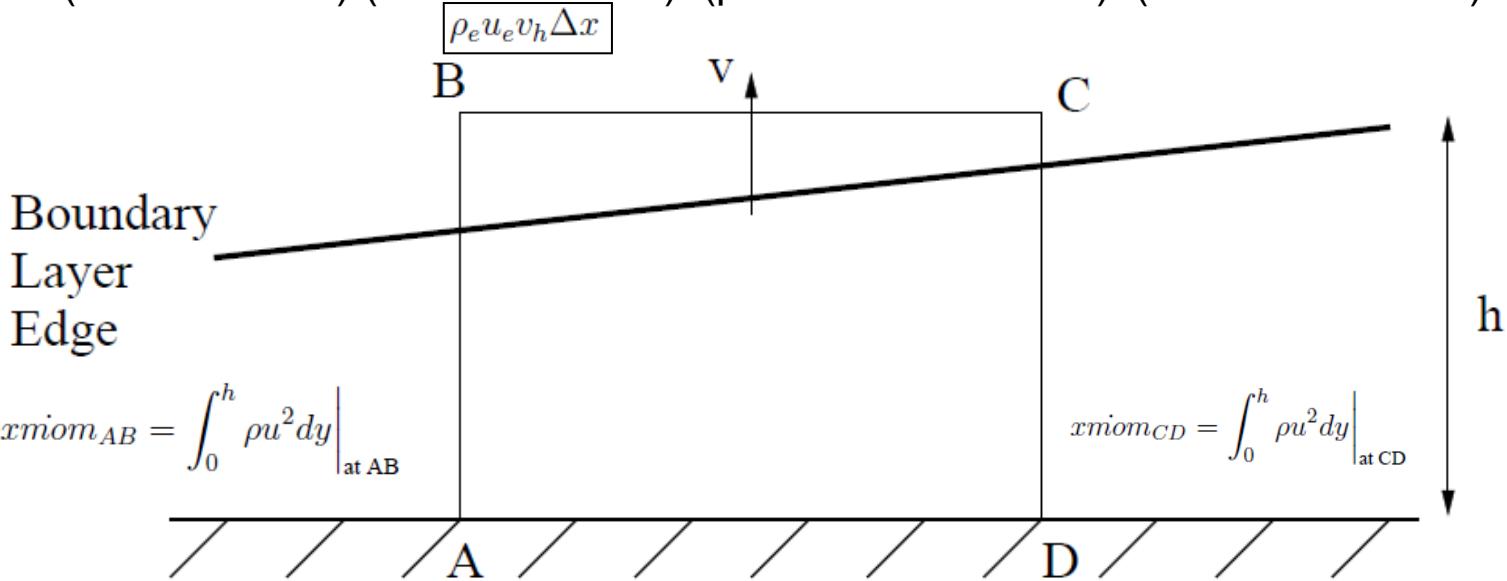
$$\int_0^h \rho u dy \Big|_{\text{at AB}} - \int_0^h \rho u dy \Big|_{\text{at CD}} = \rho_e v_h \Delta x$$

$$\rho_e v_h = - \frac{d}{dx} \left(\int_0^h \rho u dy \right)$$

Conservation of momentum

$$\int_0^h \rho u^2 dy \Big|_{\text{at AB}} \quad \int_0^h \rho u^2 dy \Big|_{\text{at CD}} \quad -(p_{CD} - p_{AB})h \quad -\tau_w \Delta x$$

$0 = (\text{momentum in}) - (\text{momentum out}) + (\text{pressure force L} \rightarrow \text{R}) + (\text{shear force L} \rightarrow \text{R})$



Previously: $\rho_e v_h = -\frac{d}{dx} \left(\int_0^h \rho u dy \right)$

$$\underbrace{- \int_0^h \rho u^2 dy \Big|_{\text{at AB}}}_{\text{Momentum lost due to friction}} + \underbrace{\int_0^h \rho u^2 dy \Big|_{\text{at CD}}}_{\text{Momentum gained due to pressure increase}} + \rho_e u_e v_h \Delta x = -(p_{CD} - p_{AB})h - \tau_w \Delta x$$

$$\frac{d}{dx} \left(\int_0^h \rho u^2 dy \right) - u_e \frac{d}{dx} \left(\int_0^h \rho u dy \right) = -h \frac{dp}{dx} - \tau_w$$

$$\frac{d}{dx} \left(\int_0^h \rho u^2 dy \right) - u_e \frac{d}{dx} \left(\int_0^h \rho u dy \right) = -h \frac{dp}{dx} - \tau_w$$

$$\frac{d}{dx} \left(u_e \int_0^h \rho u dy \right) = u_e \frac{d}{dx} \left(\int_0^h \rho u dy \right) + \frac{du_e}{dx} \int_0^h \rho u dy$$

$$u_e \frac{d}{dx} \left(\int_0^h \rho u dy \right) = \boxed{\frac{d}{dx} \left(u_e \int_0^h \rho u dy \right) - \frac{du_e}{dx} \int_0^h \rho u dy}$$

Replace using
product rule

$$-\frac{dp}{dx} = \rho_e u_e \frac{du_e}{dx} \quad (\text{from edge BC})$$

$$\frac{d}{dx} \left[\int_0^h \rho u(u - u_e) dy \right] + \frac{du_e}{dx} \left[\int_0^h \rho u dy \right] = h \rho_e u_e \frac{du_e}{dx} - \tau_w$$

$$\delta^* = \int_0^h \left(1 - \frac{\rho u}{\rho_e u_e} \right) dy$$

$$\theta = \int_0^h \frac{\rho u}{\rho_e u_e} \left(1 - \frac{u}{u_e} \right) dy$$

Introduce
 δ^* and θ

$$h \rho_e u_e \frac{du_e}{dx} = \frac{du_e}{dx} \int_0^h \rho_e u_e dy$$

$$\boxed{\frac{d}{dx} (\rho_e u_e^2 \theta) + \frac{du_e}{dx} \rho_e u_e \delta^* = \tau_w}$$

$$\frac{d}{dx}(\rho_e u_e^2 \theta) + \frac{du_e}{dx} \rho_e u_e \delta^* = \tau_w$$

$$\rho_e u_e^2 \frac{d\theta}{dx} + \theta \left(u_e^2 \frac{d\rho_e}{dx} + \rho_e 2u_e \frac{du_e}{dx} \right) + \frac{du_e}{dx} \rho_e u_e \delta^* = \tau_w$$

Expanding derivative

$$\frac{d\theta}{dx} + \theta \left(\frac{1}{\rho_e} \frac{d\rho_e}{dx} + \frac{2}{u_e} \frac{du_e}{dx} \right) + \frac{1}{u_e} \frac{du_e}{dx} \delta^* = \frac{\tau_w}{\rho_e u_e^2}$$

Divide by $\rho_e u_e^2$

$$\frac{d\theta}{dx} + \frac{\theta}{u_e} \frac{du_e}{dx} (H + 2) + \frac{\theta}{\rho_e} \frac{d\rho_e}{dx} = \frac{\tau_w}{\rho_e u_e^2}$$

Define shape factor: $H = \frac{\delta^*}{\theta}$

$$\frac{d\theta}{dx} + \frac{\theta}{u_e} \frac{du_e}{dx} (H + 2) = \frac{\tau_w}{\rho_e u_e^2} = \frac{\frac{1}{2} \tau_w}{\frac{1}{2} \rho_e u_e^2} = \frac{c_f}{2}$$

Incompressible (no density derivatives)

Momentum integral equation

$$c_f = \frac{\tau_w}{\frac{1}{2} \rho_e u_e^2}$$

MIE

- The Momentum Integral Equation is a key part of integral methods
- Read the derivation and make sure you understand the steps
- There are other integral equations, e.g. *kinetic energy integral equation*, and *total energy integral equation*
- These are used in compressible analysis, heat transfer problems, etc

Use of The MIE, worked example

Worked Example: Calculate the drag coefficient of a flat plate at zero incidence with steady flow on one side only, length 1 metre, in a sea level flow at 40 m/s. Assume incompressible, laminar flow, and a linear velocity profile within the boundary layer.

$$\text{MIE} \rightarrow \frac{d\theta}{dx} + \frac{\theta}{u_e} \frac{du_e}{dx} (H + 2) = \frac{c_f}{2}$$

no pressure gradients, so no velocity gradients in external flow

$$\frac{d\theta}{dx} = \frac{c_f}{2} = \frac{\tau_{wall}}{\rho u_e^2}$$

assume linear profile given by:

$$\frac{u}{u_e} = \frac{y}{\delta}$$

Integral properties:

$$\delta^* = \int_0^\delta \left(1 - \frac{u}{u_e}\right) dy = \int_0^\delta \left(1 - \frac{y}{\delta}\right) dy = \left[y - \frac{y^2}{2\delta}\right]_0^\delta = \delta - \frac{\delta}{2} = \frac{\delta}{2}$$

$$\theta = \int_0^\delta \frac{u}{u_e} \left(1 - \frac{u}{u_e}\right) dy = \int_0^\delta \frac{y}{\delta} \left(1 - \frac{y}{\delta}\right) dy = \left[\frac{y^2}{2\delta} - \frac{y^3}{3\delta^2}\right]_0^\delta = \frac{\delta}{2} - \frac{\delta}{3} = \frac{\delta}{6}$$

and

$$\tau_{wall} = \mu \frac{\partial u}{\partial y}$$

and

$$u = \frac{y}{\delta} u_e \Rightarrow \frac{\partial u}{\partial y} = \frac{u_e}{\delta}$$

substitute into the MIE:

$$\frac{d\theta}{dx} = \frac{c_f}{2} = \frac{\tau_{wall}}{\rho u_e^2}$$

$$\frac{d\theta}{dx} = \frac{\mu u_e}{\delta \rho_e u_e^2} \Rightarrow \frac{d\theta}{d\delta} \frac{d\delta}{dx} = \frac{\nu}{\delta u_e} \Rightarrow \frac{1}{6} \frac{d\delta}{dx} = \frac{\nu}{\delta u_e} \Rightarrow \delta d\delta = \frac{6\nu}{u_e} dx$$

Kinematic viscosity

integrate, and ignore constants of integration as delta = 0
when x = 0:

$$\delta^2 = \frac{12\nu x}{u_e} \Rightarrow \frac{\delta}{x} = \sqrt{\frac{12\nu}{xu_e}} = \sqrt{12}Re^{-\frac{1}{2}}$$

Kinematic viscosity

then

$$\frac{\delta^*}{x} = \frac{1}{2} \frac{\delta}{x} = 1.732Re^{-\frac{1}{2}},$$

$$\frac{\theta}{x} = \frac{1}{6} \frac{\delta}{x} = 0.557Re^{-\frac{1}{2}},$$

Shape factor: $H = 3.0$

and based on linear velocity profile:

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$$u = \frac{y}{\delta} u_e \Rightarrow \frac{\partial u}{\partial y} = \frac{u_e}{\delta}$$

Kinematic
viscosity

$$\tau_{wall} = \mu \frac{\partial u}{\partial y}$$

$$\frac{\delta}{x} = \sqrt{\frac{12\nu}{xu_e}} = \sqrt{12} Re^{-\frac{1}{2}}$$

$$c_f = \frac{2\tau_{wall}}{\rho_e u_e^2} = \frac{2\nu}{u_e \delta} = \frac{2\nu}{\sqrt{12} Re^{-\frac{1}{2}} xu_e} = \frac{2}{\sqrt{12}} \frac{Re^{\frac{1}{2}}}{Re} = \frac{\theta}{x} = 0.577 Re^{-\frac{1}{2}}$$

this is for one side of the flat plate, locally

$$C_D = C_F = \frac{1}{c} \int_0^c c_f dx = \frac{0.577}{c} \int_0^c \sqrt{\frac{\nu}{u_e x}} dx = \frac{0.577}{c} \left[2 \sqrt{\frac{x\nu}{u_e}} \right]_0^c$$

$$= \frac{1.155}{c} \sqrt{\frac{\nu c}{u_e}} = 1.155 Re_c^{-\frac{1}{2}}$$

Kinematic
viscosity

$$Re_c = \frac{40 * 1}{1.461 * 10^{-5}} = 2.738 * 10^6$$

$$C_D = 0.00070$$

$\times 2$ to include both sides ($C_D=0.0014$)