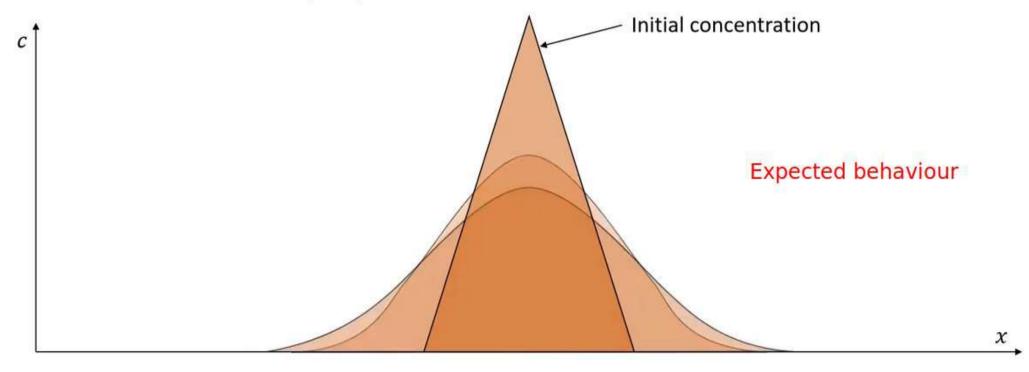
$$\frac{\partial c}{\partial t} = D \frac{\partial^2 c}{\partial x^2}$$

with: $c = \text{concentration of dissolved substance (mg/m}^3)$

D = diffusion coefficient (m²/s)





















$$\frac{\partial c}{\partial t} = D \frac{\partial^2 c}{\partial x^2}$$

with: $c = \text{concentration of dissolved substance (mg/m}^3)$ $D = \text{diffusion coefficient (m}^2/\text{s)}$

$$\frac{\partial c}{\partial t} = \frac{c_{i,j+1} - c_{i,j}}{\Delta t} + O(\Delta t)$$

$$\frac{\partial^2 c}{\partial x^2} = \frac{c_{i+1,j} - 2c_{i,j} + c_{i-1,j}}{\Delta x^2} + O(\Delta x^2)$$

$$\frac{c_{i,j+1} - c_{i,j}}{\Delta t} = D\left(\frac{c_{i+1,j} - 2c_{i,j} + c_{i-1,j}}{\Delta x^2}\right)$$

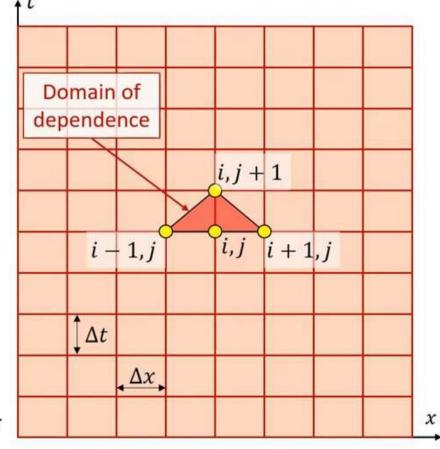
$$c_{i,j+1} = c_{i,j} + r(c_{i+1,j} - 2c_{i,j} + c_{i-1,j})$$

$$c_{i,j+1} = rc_{i+1,j} + (1-2r)c_{i,j} + rc_{i-1,j}$$

 $r = D \frac{\Delta t}{\Delta x^2}$

Fourier number

Notation: $c_{i,j} = c(i\Delta x, j\Delta t)$



Explicit scheme

--> obs. First Order scheme (in time)



















$$\frac{\partial c}{\partial t} = D \frac{\partial^2 c}{\partial x^2}$$

with: $c = \text{concentration of dissolved substance (mg/m}^3)$ $D = \text{diffusion coefficient (m}^2/\text{s)}$

$$\frac{\partial c}{\partial t} = \frac{c_{i,j+1} - c_{i,j}}{\Delta t} + O(\Delta t)$$

$$\frac{\partial^2 c}{\partial x^2} = \frac{c_{i+1,j} - 2c_{i,j} + c_{i-1,j}}{\Delta x^2} + O(\Delta x^2) \qquad \qquad \frac{\partial^2 c}{\partial x^2} = \frac{c_{i+1,j+1} - 2c_{i,j+1} + c_{i-1,j+1}}{\Delta x^2} + O(\Delta x^2)$$

$$\frac{c_{i,j+1} - c_{i,j}}{\Delta t} = \frac{1}{2}D\left(\frac{c_{i+1,j} - 2c_{i,j} + c_{i-1,j}}{\Delta x^2}\right) + \frac{1}{2}D\left(\frac{c_{i+1,j+1} - 2c_{i,j+1} + c_{i-1,j+1}}{\Delta x^2}\right)$$

$$c_{i,j+1} = c_{i,j} + \frac{1}{2}r(c_{i+1,j} - 2c_{i,j} + c_{i-1,j} + c_{i+1,j+1} - 2c_{i,j+1} + c_{i-1,j+1})$$

First order Crank-Nicolson scheme --> (implicit scheme)

$$r = D \frac{\Delta t}{\Delta x^2}$$

Fourier number

$$-\frac{1}{2}rc_{i-1,j+1} + (1+r)c_{i,j+1} - \frac{1}{2}rc_{i+1,j+1} = \frac{1}{2}rc_{i-1,j} + (1-r)c_{i,j} + \frac{1}{2}rc_{i+1,j}$$













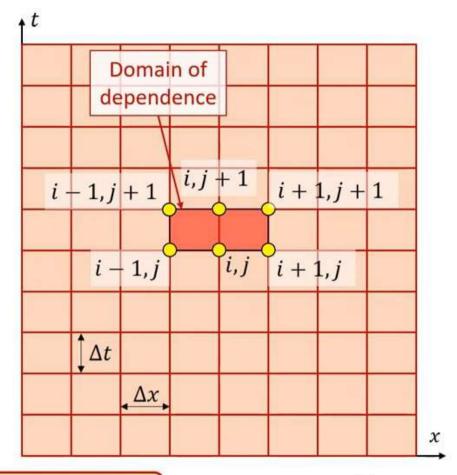






$$\frac{\partial c}{\partial t} = D \frac{\partial^2 c}{\partial x^2}$$

with: c = concentration of dissolved substance (mg/m³) D = diffusion coefficient (m²/s)



First order Crank-Nicolson scheme

$$-\frac{1}{2}rc_{i-1,j+1} + (1+r)c_{i,j+1} - \frac{1}{2}rc_{i+1,j+1} = \frac{1}{2}rc_{i-1,j} + (1-r)c_{i,j} + \frac{1}{2}rc_{i+1,j}$$

$$r = D \frac{\Delta t}{\Delta x^2}$$















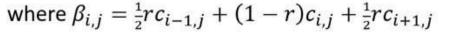


Crank-Nicolson (implicit) scheme

$$\left[-\frac{1}{2}rc_{i-1,j+1} + (1+r)c_{i,j+1} - \frac{1}{2}rc_{i+1,j+1} = \frac{1}{2}rc_{i-1,j} + (1-r)c_{i,j} + \frac{1}{2}rc_{i+1,j} \right] \qquad r = D \frac{\Delta t}{\Delta x^2}$$

Tridiagonal system of equations:

$$\begin{bmatrix} (1+r) & -\frac{1}{2}r & 0 & 0 & \dots & 0 \\ -\frac{1}{2}r & (1+r) & -\frac{1}{2}r & 0 & \dots & 0 \\ 0 & -\frac{1}{2}r & (1+r) & -\frac{1}{2}r & & \vdots \\ \vdots & & & \ddots & \ddots & \ddots & \vdots \\ 0 & & \dots & 0 & 0 & -\frac{1}{2}r & (1+r) & -\frac{1}{2}r \\ 0 & & \dots & 0 & 0 & -\frac{1}{2}r & (1+r) \end{bmatrix} \begin{bmatrix} c_0 \\ c_1 \\ c_2 \\ \vdots \\ c_{N-1} \\ c_N \end{bmatrix}_{j+1} = \begin{bmatrix} \beta_0 \\ \beta_1 \\ \beta_2 \\ \vdots \\ \beta_{N-1} \\ \beta_N \end{bmatrix}_{j}$$



















The diffusion equation: $\frac{\partial c}{\partial t} = D \frac{\partial^2 c}{\partial x^2}$

1.
$$c$$
 is known: $c(0,t) = f(t)$, $c(L,t) = g(t)$, $t \ge 0$. Dirichlet condition

2. No material is leaving the domain:
$$\frac{\partial c}{\partial x}(0,t)=0, \quad \frac{\partial c}{\partial x}(L,t)=0, \quad t\geq 0.$$
 Neumann condition

3.
$$\frac{\partial c}{\partial x}(0,t) = F(c,t), \qquad \frac{\partial c}{\partial x}(L,t) = G(c,t), \qquad t \ge 0.$$











$$\frac{\partial c}{\partial x}(0,t) = 0$$

closed BC (Neumann) VOUT[0] = VOUT[1]

yOUT[-1] = yOUT[-2]

return yOUT

Neumann condition
$$\frac{\partial c}{\partial x}(0,t) = 0$$
, $\frac{\partial c}{\partial x}(L,t) = 0$

where L is the length of the solution domain

Forward difference at x = 0

$$\frac{\partial c}{\partial x}(0, j\Delta t) = \frac{c_{1,j} - c_{0,j}}{\Delta x}$$

$$c_{0,j} = c_{1,j}$$

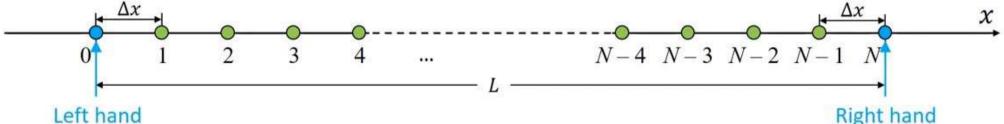
Accurate to $O(\Delta x)$

First order

Backward difference at $x = N\Delta x = L$

$$\frac{\partial c}{\partial x}(L, j\Delta t) = \frac{c_{N,j} - c_{N-1,j}}{\Delta x}$$

$$c_{N,j}=c_{N-1,j}$$



Left hand boundary

```
def oneStepExplicitFirstOrderDiffusion(yIN, Fr):
 yOUT = np.zeros like(yIN)
 # internal points
  for i in range(1,len(x)-1):
   vOUT[i] = Fr*vIN[i-1] + (1.-2*Fr)*vIN[i] + Fr*vIN[i+1]
```

--> First order accurate BC discretization

--> Second Order accurate disc. in space



Finite Difference Schemes for Advection and Diffusion













boundary



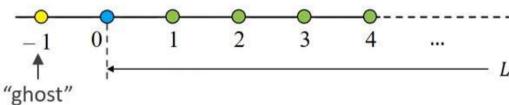


Neumann condition
$$\frac{\partial c}{\partial x}(0,t) = 0$$
, $\frac{\partial c}{\partial x}(L,t) = 0$ where L is the length of the solution domain

```
def oneStepExplicitFirstOrderDiffusion(yIN, Fr):
 yOUT = np.zeros like(yIN)
 # internal points
 for i in range(1,len(x)-1):
   youT[i] = Fr*yIN[i-1] + (1.-2*Fr)*yIN[i] + Fr*yIN[i+1] --> Second Order disc. for internal points
 # closed BC (Neumann)
 yOUT[0] = (1.-2*Fr)*yIN[0] + 2.*Fr*yIN[1]
                                                 --> Second Order disc. for BCs
 yOUT[-1] = 2.*Fr*yIN[-2] + (1.-2*Fr)*yIN[-1]
  return youT
```

"ghost"

node



Central difference approximations

Accurate to $O(\Delta x^2)$

Second order

 $\frac{\partial c}{\partial x}(N\Delta x, j\Delta t) = \frac{c_{N+1,j} - c_{N-1,j}}{2\Delta x}$

$$c_{N+1,j}=c_{N-1,j}$$



Finite Difference Schemes for Advection and Diffusion



node







N-4 N-3 N-2 N-1









Neumann condition
$$\frac{\partial c}{\partial x}(0,t) = 0$$
, $\frac{\partial c}{\partial x}(L,t) = 0$ where L is the length of the solution domain

$$c_{i,j+1} = rc_{i+1,j} + (1-2r)c_{i,j} + rc_{i-1,j}$$
 $r = D\frac{\Delta t}{\Delta x^2}$ Explicit scheme for the diffusion equation

$$r = D \frac{\Delta t}{\Delta x^2}$$

$$c_{-1,j} = c_{1,j}$$

Left hand boundary: $c_{-1,j} = c_{1,j}$ [Direct implementation – requires external node]

$$c_{0,j+1} = rc_{1,j} + (1-2r)c_{0,j} + rc_{-1,j}$$

$$c_{0,j+1} = (1-2r)c_{0,j} + 2rc_{1,j}$$

[Indirect/Implicit implementation]

$$c_{N+1,j} = c_{N-1,j}$$

Right hand boundary: $c_{N+1,j} = c_{N-1,j}$ [Direct implementation]

$$c_{N,j+1} = rc_{N+1,j} + (1-2r)c_{N,j} + rc_{N-1,j}$$

-->
$$y0UT[0] = (1.-2*Fr)*yIN[0] + 2.*Fr*yIN[1]$$

$$c_{N,j+1} = 2rc_{N-1,j} + (1-2r)c_{N,j}$$

[Indirect/Implicit implementation]

Preferable since the order of the discretization error is preserved throughout the domain (second order).











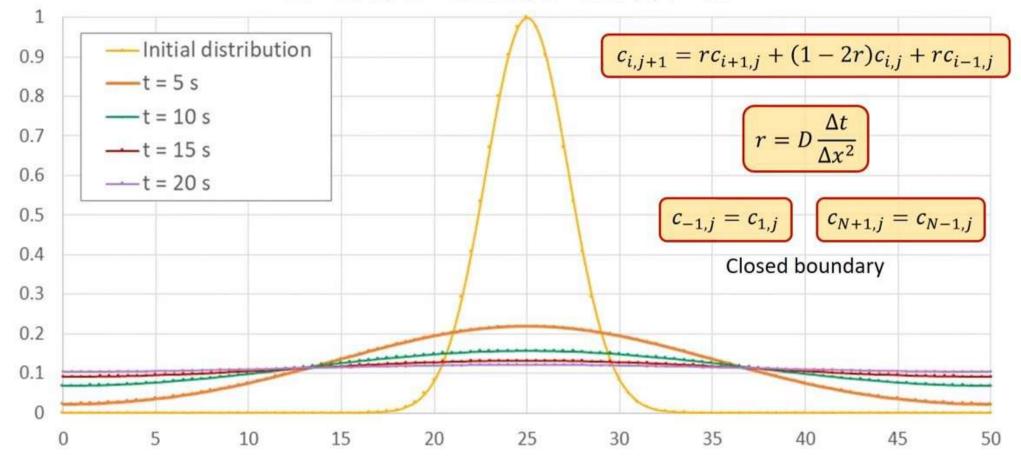






Explicit scheme for the diffusion equation

First order explicit finite difference scheme for the diffusion equation $\Delta x = 0.5$ m, $\Delta t = 0.0125$ s, D = 10 m²/s, r = 0.5





















```
# unkown's initialization
import numpy as np
                                                def yInit (x, yMin, yMax, xc, width, isRectangular = True):
# space discretization
                                                  if isRectangular:
xL = 0.
                                                    # rectangular distribuition
xR = 50
                                                    return np.array([yMax if xc-width < xi and xi < xc+width else yMin for xi in x])
dx = 0.5
                                                  else:
delX = xR - xL
                                                    # Gaussian distribuition
                                                    return yMin + yMax * np.exp(-(x - xc) ** 2 / (2 * width ** 2))
nx = int(delX/dx)
x = np.linspace(xL, xR, nx+1)
                                                vMin = 0.
                                                vMax = 1.
                                                yInit = yInit (x=x,
# time discretization
                                                               yMin=yMin,
Fr = 0.5 # Fourier Number: Fr = D*dt/dx**2
                                                               yMax=yMax,
D = 10.
                                                               xc=25.,
dt = Fr*dx**2/D
                                                               width=2..
delT = 5.
                                                               isRectangular=False)
stepsNbr = int(delT/dt)
                                                y = np.copy(yInit)
def oneStepExplicitFirstOrderDiffusion(vIN, Fr):
                                                                                   for i in range(stepsNbr):
  yOUT = np.zeros like(yIN)
                                                                                     y = oneStepExplicitFirstOrderDiffusion(y, Fr)
  # internal points
  for i in range(1,len(x)-1):
    vOUT[i] = Fr*vIN[i-1] + (1.-2*Fr)*vIN[i] + Fr*vIN[i+1]
                                                                                 1.0
  # closed BC (Neumann)
                                                                                                                                            ylnit
  VOUT[0] = (1.-2*Fr)*VIN[0] + 2.*Fr*VIN[1]
                                                                                 0.9 -
  yOUT[-1] = 2.*Fr*yIN[-2] + (1.-2*Fr)*yIN[-1]
  return youT
                                                                                 0.8
print('dx = ', dx, '\n'
                                                                                 0.7 -
                                                   dx = 0.5
      'Fr = ', Fr, '\n'
                                                   Fr = 0.5
      'D = ', D, '\n'
                                                                                 0.6 -
                                                   D = 10.0
      'dt = ', dt, '\n'
                                                  dt = 0.0125
                                   Output
                                                                                 0.5 -
      'delT = ', delT, '\n'
                                                  delT = 5.0
      'stepsNbr = ', stepsNbr)
                                                   stepsNbr = 400
                                                                                 0.4 -
import matplotlib.pyplot as plt
                                                                                 0.3 -
plt.style.use("ggplot")
plt.xticks(np.arange(xL, xR+.1, 5))
                                                                                 0.2 -
plt.yticks(np.arange(yMin, yMax+.1, .1))
                                                                                 0.1
plt.plot(x, yInit, label='yInit')
                                                  Output
plt.plot(x, y, label='y')
                                                                                 0.0
plt.legend()
plt.show()
                                                                                                 10
                                                                                                       15
                                                                                                            20
                                                                                                                  25
                                                                                                                       30
                                                                                                                             35
                                                                                                                                  40
                                                                                                                                        45
                                                                                                                                             50
```

$$\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = 0$$

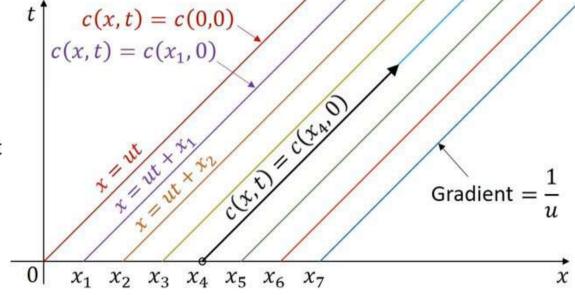
with: $c = c(x, t) = \text{concentration (mg/m}^3)$

u = flow velocity in the x direction (m/s)

Let us assume u > 0 and is constant

Characteristics: $\frac{dx}{dt} = u$

x = ut + constant















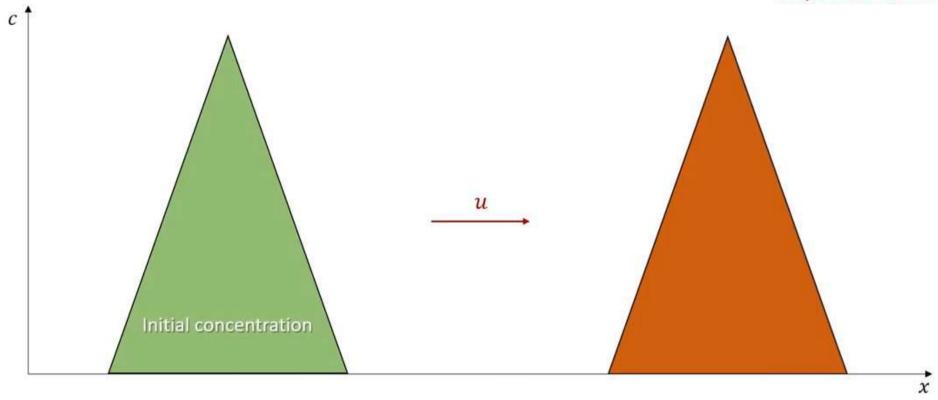






$$\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = 0 , u > 0$$

Expected behaviour





Explicit Upwind Finite Difference Solution to the Advection Equation















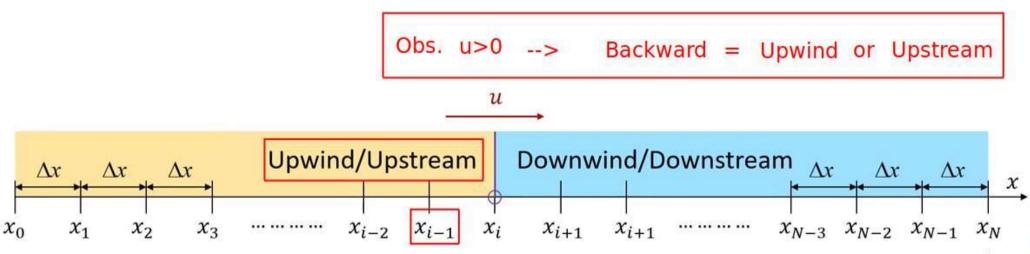
$$\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = 0 , u > 0$$

$$\frac{\partial c}{\partial t} \approx \frac{c(x, t + \Delta t) - c(x, t)}{\Delta t}$$

$$\frac{\partial c}{\partial x} \approx \frac{c(x,t) - c(x - \Delta x,t)}{\Delta x}$$

Forward time difference approximation $(O(\Delta t))$

Backward spatial difference approximation $(O(\Delta x))$ Upwind scheme





Explicit Upwind Finite Difference Solution to the Advection Equation















$$\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = 0 , u < 0$$

$$\frac{\partial c}{\partial t} \approx \frac{c(x, t + \Delta t) - c(x, t)}{\Delta t}$$

$$\frac{\partial c}{\partial x} \approx \frac{c(x + \Delta x, t) - c(x, t)}{\Delta x}$$

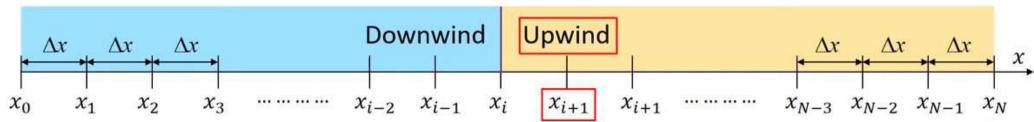
Forward time difference approximation

Forward spatial difference approximation

Upwind scheme









Explicit Upwind Finite Difference Solution to the Advection Equation















$$\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = 0, u > 0$$

Notation: $c_{i,j} = c(i\Delta x, j\Delta t)$

$$\frac{\partial c}{\partial t} \approx \frac{c(x, t + \Delta t) - c(x, t)}{\Delta t} \qquad \frac{\partial c}{\partial t} \approx \frac{c_{i, j+1} - c_{i, j}}{\Delta t}$$

$$\frac{\partial c}{\partial t} \approx \frac{c_{i,j+1} - c_{i,j}}{\Delta t}$$

$$\frac{c_{i,j+1} - c_{i,j}}{\Delta t} + u \frac{c_{i,j} - c_{i-1,j}}{\Delta x} = 0$$

$$\frac{\partial c}{\partial x} \approx \frac{c(x,t) - c(x - \Delta x,t)}{\Delta x} \qquad \qquad \frac{\partial c}{\partial x} \approx \frac{c_{i,j} - c_{i-1,j}}{\Delta x}$$

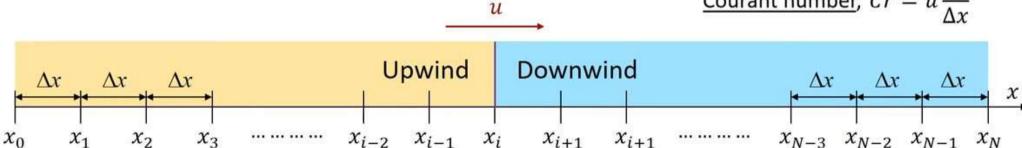
$$\frac{\partial c}{\partial x} \approx \frac{c_{i,j} - c_{i-1,j}}{\Delta x}$$

$$c_{i,j+1} = c_{i,j} - u \frac{\Delta t}{\Delta x} (c_{i,j} - c_{i-1,j})$$

First order explicit upwind finite difference solution to the advection equation

$$c_{i,j+1} = (1 - Cr)c_{i,j} + (Cr)c_{i-1,j}$$

Courant number, $Cr = u \frac{\Delta t}{\Delta x}$





Explicit Upwind Finite Difference Solution to the Advection Equation





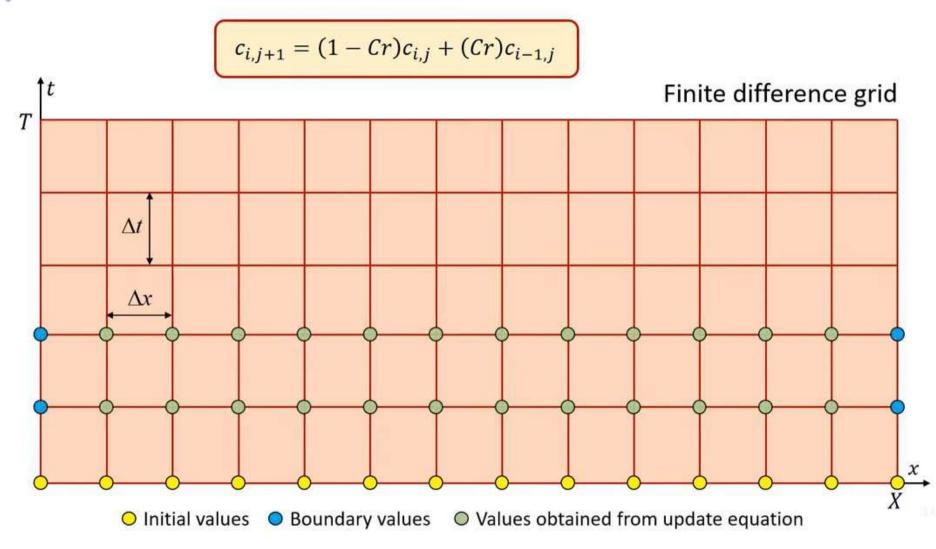














Explicit Upwind Finite Difference Solution to the Advection Equation





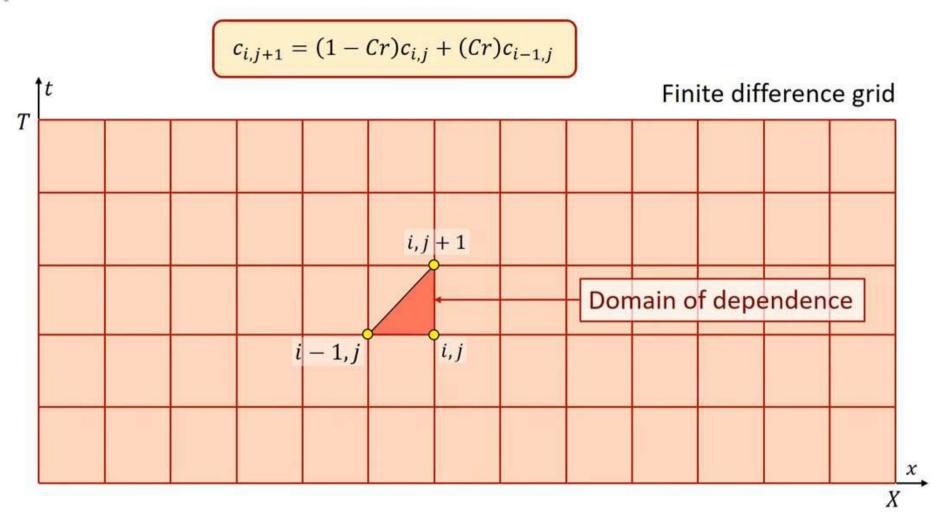




























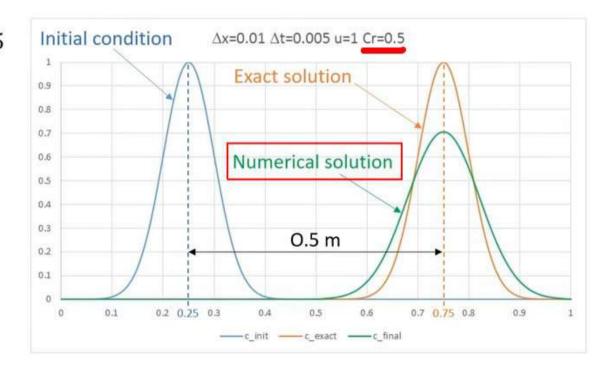


First order explicit upwind finite difference solution to the advection equation:

$$c_{i,j+1} = (1 - Cr)c_{i,j} + (Cr)c_{i-1,j}$$

$$Cr = u \frac{\Delta t}{\Delta x}$$

$$Cr = 0.5$$



After 0.5 s



Explicit Upwind Finite Difference Solution to the Advection Equation











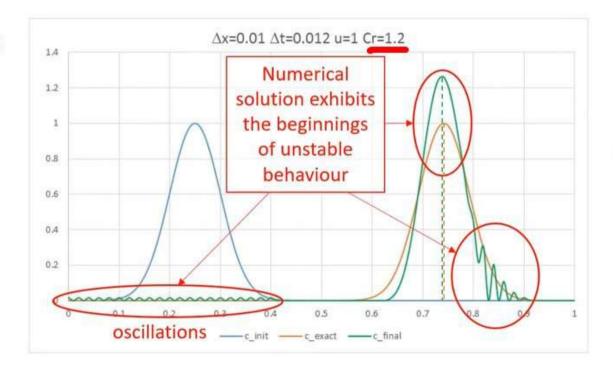


First order explicit upwind finite difference solution to the advection equation:

$$c_{i,j+1} = (1 - Cr)c_{i,j} + (Cr)c_{i-1,j}$$

$$Cr = u \frac{\Delta t}{\Delta x}$$

$$Cr = 1.2$$



After 0.5 s

Unstable

Solution eventually 'blows up'



Explicit Upwind Finite Difference Solution to the Advection Equation













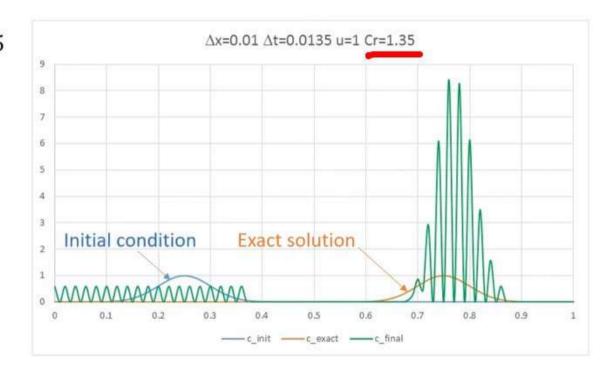


First order explicit upwind finite difference solution to the advection equation:

$$c_{i,j+1} = (1 - Cr)c_{i,j} + (Cr)c_{i-1,j}$$

$$Cr = u \frac{\Delta t}{\Delta x}$$

$$Cr = 1.35$$



After 0.5 s

Unstable



Explicit Upwind Finite Difference Solution to the Advection Equation















First order explicit upwind finite difference solution to the advection equation:

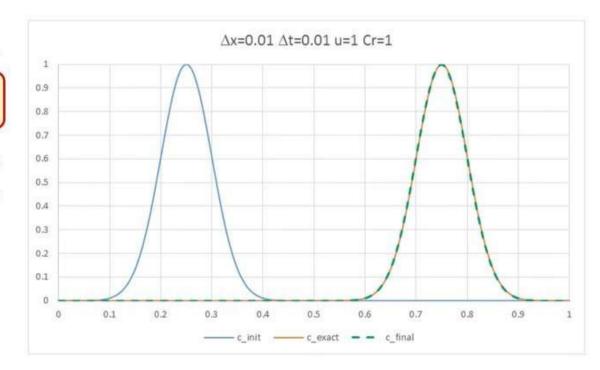
$$c_{i,j+1} = (1 - Cr)c_{i,j} + (Cr)c_{i-1,j}$$

$$Cr = u \frac{\Delta t}{\Delta x}$$

$$Cr = 1$$

$$\Rightarrow \boxed{c_{i,j+1} = c_{i-1,j}}$$

Reproduces the exact solution



After 0.5 s



Explicit Upwind Finite Difference Solution to the Advection Equation













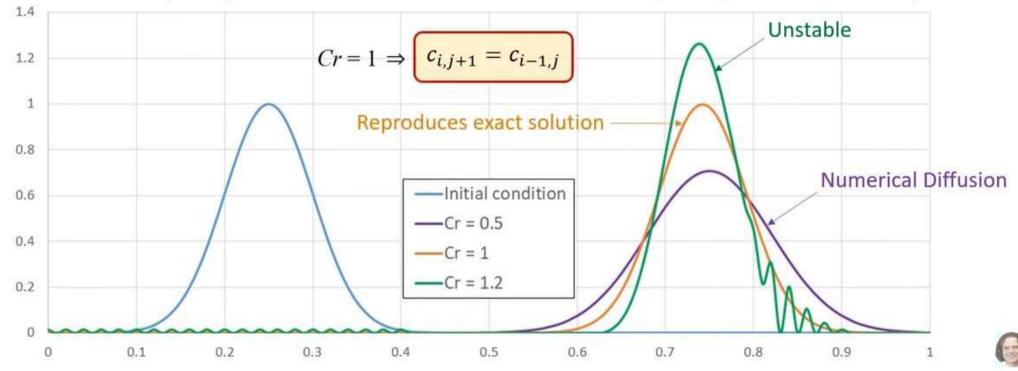


Summary

$$c_{i,j+1} = (1 - Cr)c_{i,j} + (Cr)c_{i-1,j}$$

$$Cr = u \frac{\Delta t}{\Delta x}$$

First Order Explicit Upwind Finite Difference Scheme for the Advection Equation ($\Delta x = 0.01 \text{ m}, u = 1 \text{ m/s}$)



Explicit Upwind Finite Difference Solution to the Advection Equation















Consistency

Finite difference equation

1st order upwind explicit scheme for the advection equation: $c_{i,j+1} = (1-\rho)c_{i,j} + \rho c_{i-1,j}$ $\rho = u \frac{\Delta t}{\Delta x}$

$$c_{i,j+1} = (1-\rho)c_{i,j} + \rho c_{i-1,j}$$

$$\rho = u \frac{\Delta t}{\Delta x}$$

Taylor series:

$$c_{i,j+1} = c_{ij} + \Delta t \frac{\partial c}{\partial t} + \frac{\Delta t}{2!} \frac{\partial^2 c}{\partial t^2} + \frac{\Delta t^2}{3!} \frac{\partial^3 c}{\partial t^3} + \cdots \quad \text{and} \quad c_{i-1,j} = c_{i,j} - \Delta x \frac{\partial c}{\partial x} + \frac{\Delta x^2}{2!} \frac{\partial^2 c}{\partial x^2} - \frac{\Delta x^3}{3!} \frac{\partial^3 c}{\partial x^3} + \cdots$$

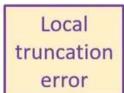
Substituting into the finite difference equation

$$c_{ij} + \Delta t \frac{\partial c}{\partial t} + \frac{\Delta t^2}{2!} \frac{\partial^2 c}{\partial t^2} + \frac{\Delta t^3}{3!} \frac{\partial^3 c}{\partial t^3} + \dots = (1 - \rho)c_{i,j} + \rho \left(c_{i,j} - \Delta x \frac{\partial c}{\partial x} + \frac{\Delta x^2}{2!} \frac{\partial^2 c}{\partial x^2} - \frac{\Delta x^3}{3!} \frac{\partial^3 c}{\partial x^3} + \dots \right)$$

$$\Delta t \frac{\partial c}{\partial t} + \frac{\Delta t^2}{2} \frac{\partial^2 c}{\partial t^2} + \frac{\Delta t^3}{6} \frac{\partial^3 c}{\partial t^3} + \dots = -\rho \Delta x \frac{\partial c}{\partial x} + \rho \frac{\Delta x^2}{2} \frac{\partial^2 c}{\partial x^2} - \rho \frac{\Delta x^3}{6} \frac{\partial^3 c}{\partial x^3} + \dots$$

$$\Delta t \frac{\partial c}{\partial t} + \frac{\Delta t^2}{2} \frac{\partial^2 c}{\partial t^2} + \frac{\Delta t^3}{6} \frac{\partial^3 c}{\partial t^3} + \dots = -u \Delta t \frac{\partial c}{\partial x} + u \Delta t \frac{\Delta x}{2} \frac{\partial^2 c}{\partial x^2} - u \Delta t \frac{\Delta x^2}{6} \frac{\partial^3 c}{\partial x^3} + \dots$$

$$\Delta t \frac{\partial c}{\partial t} + \frac{\Delta t^2}{2} \frac{\partial^2 c}{\partial t^2} + \frac{\Delta t^3}{6} \frac{\partial^3 c}{\partial t^3} + \dots = -u \Delta t \frac{\partial c}{\partial x} + u \Delta t \frac{\Delta x}{2} \frac{\partial^2 c}{\partial x^2} - u \Delta t \frac{\Delta x^2}{6} \frac{\partial^3 c}{\partial x^3} + \dots$$
Advection equation



$$\frac{\partial c}{\partial t} + \frac{\Delta t}{2} \frac{\partial^2 c}{\partial t^2} + \frac{\Delta t^2}{6} \frac{\partial^3 c}{\partial t^3} + \dots = -u \frac{\partial c}{\partial x} + u \frac{\Delta x}{2} \frac{\partial^2 c}{\partial x^2} - u \frac{\Delta x^2}{6} \frac{\partial^3 c}{\partial x^3} + \dots$$

Truncation error

$$\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = \left[-\frac{\Delta t}{2} \frac{\partial^2 c}{\partial t^2} + u \frac{\Delta x}{2} \frac{\partial^2 c}{\partial x^2} \right] - \frac{\Delta t^2}{6} \frac{\partial^3 c}{\partial t^3} - u \frac{\Delta x^2}{6} \frac{\partial^3 c}{\partial x^3} + \cdots$$

















Consistency

1st order upwind explicit scheme for the advection equation

$$c_{i,j+1} = (1-\rho)c_{i,j} + \rho c_{i-1,j} \Rightarrow \frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = -\frac{\Delta t}{2} \frac{\partial^2 c}{\partial t^2} + u \frac{\Delta x}{2} \frac{\partial^2 c}{\partial x^2} - \frac{\Delta t^2}{6} \frac{\partial^3 c}{\partial t^3} - u \frac{\Delta x^2}{6} \frac{\partial^3 c}{\partial x^3} + \cdots$$

Truncation Error (T. E.) =
$$-\frac{\Delta t}{2} \frac{\partial^2 c}{\partial t^2} + u \frac{\Delta x}{2} \frac{\partial^2 c}{\partial x^2} - \frac{\Delta t^2}{6} \frac{\partial^3 c}{\partial t^3} - u \frac{\Delta x^2}{6} \frac{\partial^3 c}{\partial x^3} + \cdots$$

 $\lim_{\Delta x, \Delta t \to 0} (T. E.) = 0 \implies$ The scheme is consistent with the original PDE.

Truncation error analysis

















Consistency

1st order upwind explicit scheme for the advection equation

$$\rho = u \frac{\Delta t}{\Delta x}$$

$$c_{i,j+1} = (1-\rho)c_{i,j} + \rho c_{i-1,j} \Rightarrow \frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = -\frac{\Delta t}{2} \frac{\partial^2 c}{\partial t^2} + u \frac{\Delta x}{2} \frac{\partial^2 c}{\partial x^2} - \frac{\Delta t^2}{6} \frac{\partial^3 c}{\partial t^3} - u \frac{\Delta x^2}{6} \frac{\partial^3 c}{\partial x^3} + \cdots$$

Local Truncation Error (L. T. E.) =
$$-\frac{\Delta t}{2} \frac{\partial^2 c}{\partial t^2} + u \frac{\Delta x}{2} \frac{\partial^2 c}{\partial x^2}$$

$$\frac{\partial c}{\partial t} = -u \frac{\partial c}{\partial x} \implies \frac{\partial^2 c}{\partial t^2} = \frac{\partial}{\partial t} \left(-u \frac{\partial c}{\partial x} \right) = -u \frac{\partial}{\partial t} \left(\frac{\partial c}{\partial x} \right) = -u \frac{\partial}{\partial x} \left(\frac{\partial c}{\partial t} \right) = -u \frac{\partial}{\partial x} \left(-u \frac{\partial c}{\partial x} \right)$$

$$\implies \frac{\partial^2 c}{\partial t^2} = u^2 \frac{\partial^2 c}{\partial x^2} \implies \text{L. T. E.} = -\frac{\Delta t}{2} u^2 \frac{\partial^2 c}{\partial x^2} + u \frac{\Delta x}{2} \frac{\partial^2 c}{\partial x^2}$$

$$\left(\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = 0\right)$$

$$\rho \Delta x = u \Delta t \qquad \Rightarrow \quad \text{L. T. E.} = -u \frac{\rho \Delta x}{2} \frac{\partial^2 c}{\partial x^2} + u \frac{\Delta x}{2} \frac{\partial^2 c}{\partial x^2}$$

L. T. E. =
$$\frac{1}{2}u\Delta x(1-\rho)\frac{\partial^2 c}{\partial x^2}$$
 Source of numerical diffusion







Numerical diffusion (false dispersion)

Courant number

$$\rho = u \frac{\Delta t}{\Delta x}$$

1st order upwind explicit scheme for the advection equation

$$c_{i,j+1} = (1-\rho)c_{i,j} + \rho c_{i-1,j}$$

$$\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = \frac{1}{2}u\Delta x(1-\rho) \frac{\partial^2 c}{\partial x^2} + \text{Higher Order Terms}$$

- If ho < 1 the local truncation error is positive and has a diffusive effect. Numerical diffusion
- If $\rho > 1$ the local truncation error is negative and has an *amplifying* effect and is a cause of instability.
- When $\rho = 1$ the local truncation error is zero. No numerical diffusion.
- When ρ is close to 1 the local truncation error is small and thus so is the numerical diffusion (for ρ < 1).

$$\int \frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = 0$$

Advection equation



Consistency and Numerical Diffusion











L. T. E. = $\frac{1}{2}u\Delta x(1-\rho)\frac{\partial^2 c}{\partial x^2}$



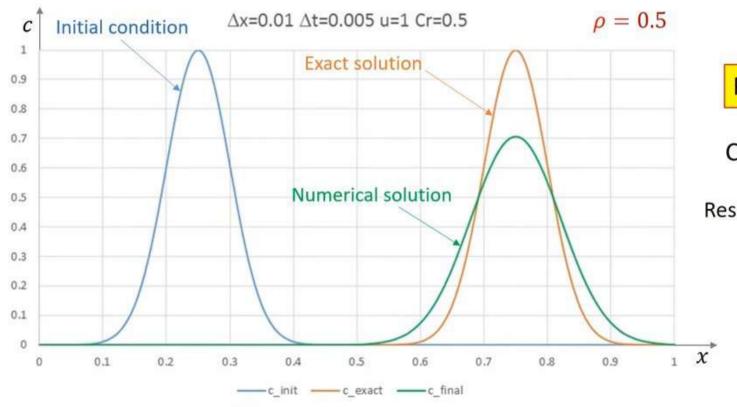


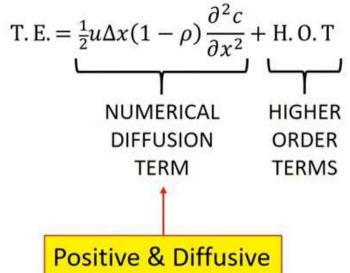


Numerical diffusion

1st order upwind explicit scheme for the advection equation

$$c_{i,j+1} = (1-\rho)c_{i,j} + \rho c_{i-1,j}$$





Courant number, $\rho < 1$

Results obtained for t = 0.5 seconds



















Consistency and Numerical Diffusion

<u>Consistency</u> of a numerical scheme is its property that when the discretization step tends to zero its finite difference approximation tends towards the original differential equation.

To *prove* a scheme is consistent with the differential equation it represents we perform <u>truncation error analysis</u>.

<u>Numerical diffusion</u> is a form of inaccuracy of a numerical scheme that manifests itself through an unrealistic attenuation of the propagated disturbance (wave height or concentration). The effects of numerical diffusion are similar to physical diffusion and therefore it is often very hard to distinguish between the two.

Truncation error can cause <u>amplification</u> of the numerical solution, leading to numerical instability.

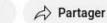
The first order upwind explicit scheme for the advection equation is consistent with the advection equation.

















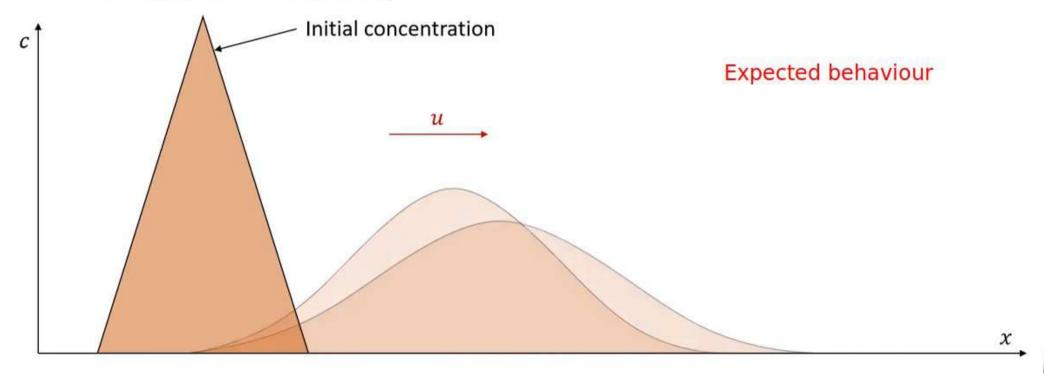
Consider the transport and diffusion of a dissolved substance in one spatial dimension

 $\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = D \frac{\partial^2 c}{\partial x^2}$

with: $c = \text{concentration of dissolved substance (mg/m}^3)$

u = celerity of flow (m/s)

 $D = \text{diffusion coefficient (m}^2/\text{s)}$





Finite Difference Schemes for Advection and Diffusion















Consider the transport and diffusion of a dissolved substance in one spatial dimension $\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = D \frac{\partial^2 c}{\partial x^2}$

$$\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = D \frac{\partial^2 c}{\partial x^2}$$

c = concentration of dissolved substance (mg/m³) with:

u = celerity of flow (m/s)

 $D = \text{diffusion coefficient (m}^2/\text{s)}$

Upwind

$$\frac{\partial c}{\partial t} \approx \frac{c_{i,j+1} - c_{i,j}}{\Delta t},$$

$$\frac{\partial c}{\partial t} \approx \frac{c_{i,j+1} - c_{i,j}}{\Delta t}, \qquad \frac{\partial^2 c}{\partial x^2} \approx \frac{c_{i-1,j} - 2c_{i,j} + c_{i+1,j}}{\Delta x^2}, \qquad \frac{\partial c}{\partial x} \approx \frac{c_{i,j} - c_{i-1,j}}{\Delta x} \quad \text{or} \quad \frac{\partial c}{\partial x} \approx \frac{c_{i+1,j} - c_{i,j}}{\Delta x}$$

$$\partial x$$
 If $u >$

or
$$\frac{\partial c}{\partial x} \approx \frac{c_{i+1,j} - c_i}{\Delta x}$$

$$O(\Delta t)$$

$$O(\Delta x^2)$$

If
$$u > 0$$
 $O(\Delta x)$ If $u < 0$

If
$$u < 0$$

 $O(\Delta t)$ $O(\Delta x^2)$ Courant number, $\rho=u \frac{\Delta t}{\Delta x}$, Fourier number, $r=D \frac{\Delta t}{\Delta x^2}$

If
$$u > 0$$

If
$$u > 0$$

$$\frac{c_{i,j+1} - c_{i,j}}{\Delta t} + u\left(\frac{c_{i,j} - c_{i-1,j}}{\Delta x}\right) = D\left(\frac{c_{i-1,j} - 2c_{i,j} + c_{i+1,j}}{\Delta x^2}\right)$$

$$c_{i,j+1} = c_{i,j} + r(c_{i-1,j} - 2c_{i,j} + c_{i+1,j}) - \rho(c_{i,j} - c_{i-1,j})$$

$$=(r+\rho)c_{i-1,j}+(1-2r-\rho)c_{i,j}+rc_{i+1,j}$$
 Upwind explicit scheme $(u>0)$



Finite Difference Schemes for Advection and Diffusion















Consider the transport and diffusion of a dissolved substance in one spatial dimension $\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = D \frac{\partial^2 c}{\partial x^2}$

$$\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = D \frac{\partial^2 c}{\partial x^2}$$

c = concentration of dissolved substance (mg/m³) with:

u = celerity of flow (m/s)

 $D = \text{diffusion coefficient (m}^2/\text{s)}$

Upwind

$$\frac{\partial c}{\partial t} \approx \frac{c_{i,j+1} - c_{i,j}}{\Delta t},$$

$$\frac{\partial^2 c}{\partial x^2} \approx \frac{c_{i-1,j} - 2c_{i,j} + c_{i+1,j}}{\Delta x^2}$$

$$O(\Delta x^2)$$

$$\frac{\partial c}{\partial t} \approx \frac{c_{i,j+1} - c_{i,j}}{\Delta t}, \qquad \frac{\partial^2 c}{\partial x^2} \approx \frac{c_{i-1,j} - 2c_{i,j} + c_{i+1,j}}{\Delta x^2}, \qquad \frac{\partial c}{\partial x} \approx \frac{c_{i,j} - c_{i-1,j}}{\Delta x} \quad \text{or} \quad \frac{\partial c}{\partial x} \approx \frac{c_{i+1,j} - c_{i,j}}{\Delta x}$$

If
$$u > 0$$
 $O(\Delta x)$ If $u < 0$

$$O(\Delta x)$$

If
$$u < 0$$

 $O(\Delta t)$ $O(\Delta x^2)$ Courant number, $\rho=u \frac{\Delta t}{\Delta x}$, Fourier number, $r=D \frac{\Delta t}{\Delta x^2}$

If
$$u < 0$$

If
$$u < 0$$

$$\frac{c_{i,j+1} - c_{i,j}}{\Delta t} + u \left(\frac{c_{i+1,j} - c_{i,j}}{\Delta x}\right) = D \left(\frac{c_{i-1,j} - 2c_{i,j} + c_{i+1,j}}{\Delta x^2}\right)$$

$$c_{i,j+1} = c_{i,j} + r(c_{i-1,j} - 2c_{i,j} + c_{i+1,j}) - \rho(c_{i+1,j} - c_{i,j})$$

$$= rc_{i-1,j} + (1 - 2r + \rho)c_{i,j} + (r + \rho)c_{i+1,j}$$
 Upwind explicit scheme ($u < 0$)



Finite Difference Schemes for Advection and Diffusion















Consider the transport and diffusion of a dissolved substance in one spatial dimension $\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = D \frac{\partial^2 c}{\partial x^2}$

$$\frac{\partial c}{\partial t} + u \frac{\partial c}{\partial x} = D \frac{\partial^2 c}{\partial x^2}$$

$$\frac{\partial^2 c}{\partial x^2} \approx \frac{c_{i-1,j+1} - 2c_{i,j+1} + c_{i+1,j+1}}{\Delta x^2}, \ \frac{\partial c}{\partial x} \approx \frac{c_{i,j+1} - c_{i-1,j+1}}{\Delta x}$$

$$[\times \theta]$$

$$\frac{\partial c}{\partial t} \approx \frac{c_{i,j+1} - c_{i,j}}{\Delta t}$$

$$\frac{\partial c}{\partial t} \approx \frac{c_{i,j+1} - c_{i,j}}{\Delta t}, \qquad \frac{\partial^2 c}{\partial x^2} \approx \frac{c_{i-1,j} - 2c_{i,j} + c_{i+1,j}}{\Delta x^2}, \qquad \frac{\partial c}{\partial x} \approx \frac{c_{i,j} - c_{i-1,j}}{\Delta x}$$

$$\frac{\partial c}{\partial x} \approx \frac{c_{i,j} - c_{i-1,j}}{\Delta x}$$

$$[\times (1-\theta)]$$

weighting

If u > 0

Courant number, $ho=urac{\Delta t}{\Delta x}$, Fourier number, $r=Drac{\Delta t}{\Delta x^2}$

$$\frac{c_{i,j+1} - c_{i,j}}{\Delta t} + u \left((1 - \theta) \left(\frac{c_{i,j} - c_{i-1,j}}{\Delta x} \right) + \theta \left(\frac{c_{i,j+1} - c_{i-1,j+1}}{\Delta x} \right) \right) = D \left(\frac{(1 - \theta) \left(\frac{c_{i-1,j} - 2c_{i,j} + c_{i+1,j}}{\Delta x^2} \right)}{\Delta x^2} \right) + \theta \left(\frac{c_{i-1,j+1} - 2c_{i,j+1} + c_{i+1,j+1}}{\Delta x^2} \right) \right)$$

Upwind implicit scheme
$$(u > 0)$$
: $-\theta(r + \rho)c_{i-1,j+1} + (1 + \theta(2r + \rho))c_{i,j+1} - \theta r c_{i+1,j+1} = \alpha_{i,j}$

where
$$\alpha_{i,j} = c_{i,j} + (1-\theta)\left((r+\rho)c_{i-1,j} - (2r+\rho)c_{i,j} + rc_{i+1,j}\right)$$



Finite Difference Schemes for Advection and Diffusion















Assume u > 0.

Left hand boundary (x = 0): 1. Dirichlet condition $c(0, t) = f(t), t \ge 0$

2. Neumann condition $\frac{\partial c}{\partial x}(0,t) = g(t), t \ge 0$

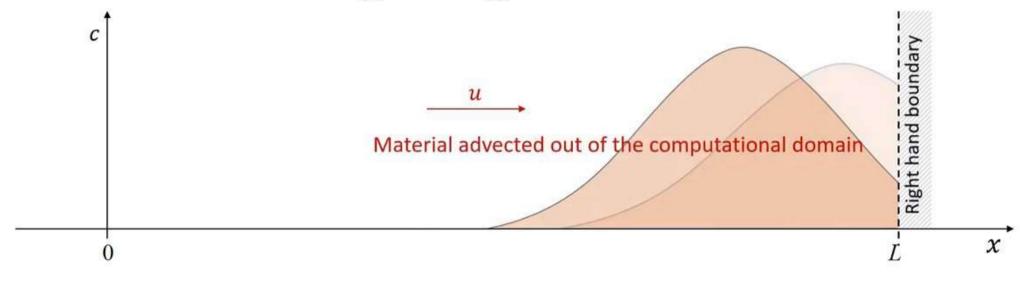
Right hand boundary (x = L):

Absorbing boundary condition

= Negligible diffusion at downstream BC

$$\frac{\partial c}{\partial t}(L,t) + u \frac{\partial c}{\partial x}(L,t) = 0$$

[Advection equation]



Finite Difference Schemes for Advection and Diffusion















Assume u > 0. Absorbing boundary condition at x = L

$$\frac{\partial c}{\partial t}(L,t) + u\frac{\partial c}{\partial x}(L,t) = 0$$

Explicit upwind scheme: $c_{i,j+1}=(r+\rho)c_{i-1,j}+(1-2r-\rho)c_{i,j}+rc_{i+1,j}$ where $\rho=u\frac{\Delta t}{\Delta r}$, $r=D\frac{\Delta t}{\Delta r^2}$

Downstream boundary condition:
$$c_{N,j+1} = \rho c_{N-1,j} + (1-\rho)c_{N,j}$$

Dirichlet upstream and Absorbing BC downstream vOUT[0] = vUpstream yOUT[-1] = Cr*yIN[-2] + (1.-Cr)*yIN[-1]

Weighted average implicit upwind scheme:

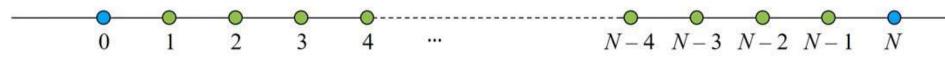
$$-\theta(r+\rho)c_{i-1,j+1} + (1+\theta(2r+\rho))c_{i,j+1} - \theta r c_{i+1,j+1} = c_{i,j} + (1-\theta)((r+\rho)c_{i-1,j} - (2r+\rho)c_{i,j} + r c_{i+1,j})$$

Downstream boundary condition:

$$-\rho\theta c_{N-1,j+1} + (1+\rho\theta)c_{N,j+1} = \rho(1-\theta)c_{N-1,j} + (1-\rho(1-\theta))c_{N,j}$$

Exercise:

Derive an implicit upwind scheme for the advection-diffusion equation for the case u < 0, including the downstream boundary condition.





Finite Difference Schemes for Advection and Diffusion









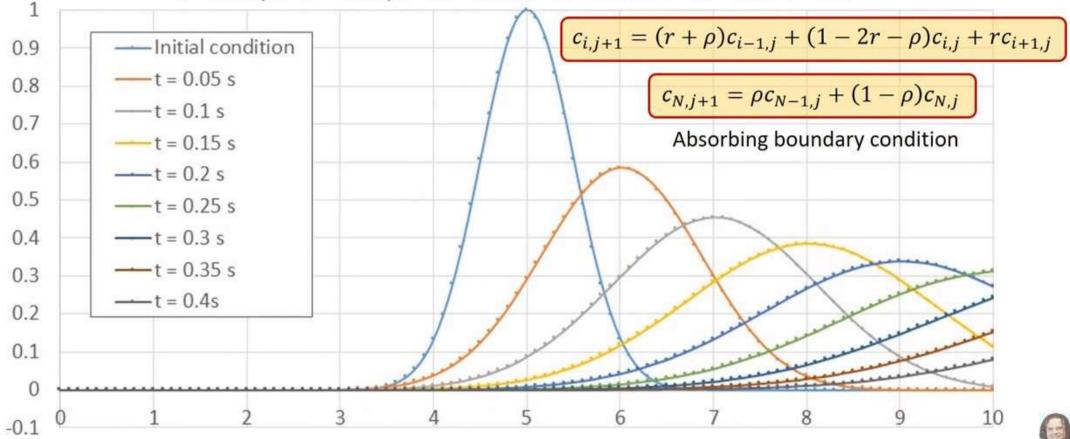






Explicit scheme for the diffusion equation

Classic First Order Explicit Scheme for the Advection-Diffusion Equation u = 20 m/s D = 4 m²/s dx = 0.1 m dt = 0.001 s Cr = 0.2 r = 0.4





Finite Difference Schemes for Advection and Diffusion













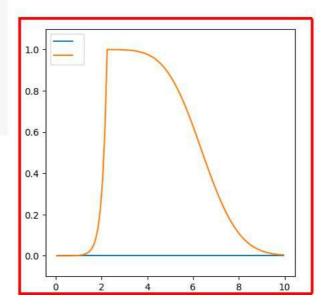


```
2 from fipy import *
 4 # space discretization
 5 xL = 0.
 6 xR = 10.
 7 dx = 0.1
 8 \text{ delX} = xR - xL
 9 \text{ nx} = int(delX/dx)
10 mesh = Grid1D(nx=nx, dx=dx) + xL
11
12 # time discretization
13 # Advection
14 Cr = 0.2 # Courant Number: Cr = u*dt/dx
15 u = 20.
16 dtAdv = abs(Cr*dx/u)
17 # Diffusion
18 Fr = 0.4 # Fourier Number: Fr = D*dt/dx**2
19 D = 4.
20 dtDiff = abs(Fr*dx**2/D)
21 # Advection-Diffusion
22 dt = min(dtAdv, dtDiff)
23 \text{ delT} = 0.2
24 stepsNbr = int(delT/dt)
26 # unkown's initialization
27 \text{ yMin} = 0.
28 \text{ yMax} = 1.
29 yInit = CellVariable(mesh=mesh, value=yMin)
30 y = CellVariable(mesh=mesh, value=yInit)
31
```

1 import numpy as np

```
60 print('dx = ', dx, '\n'
         'delX = ', delX, '\n'
61
         'nx = ', nx, '\n'
62
         'Cr = ', Cr, '\n'
63
         'u = ', u, '\n'
64
65
         'dtAdv = ', dtAdv, '\n'
         'Fr = ', Fr, '\n'
66
         'D = ', D, '\n'
'dtDiff = ', dtDiff, '\n'
67
68
         'dt = min(dtAdv,dtDiff) = ', dt, '\n'
69
70
         'delT = ', delT, '\n'
         'stepsNbr = ', stepsNbr)
71
```

```
dx = 1.00e-01
delX = 10.0
nx = 100
Cr = 0.2
u = 20.0
dtAdv = 1.00e-03
Fr = 0.4
D = 4.0
dtDiff = 1.00e-03
dt = min(dtAdv,dtDiff) = 1.00e-03
delT = 0.2
stepsNbr = 199
```



```
1 import numpy as np
                                                                                    56 z.faceGrad.constrain((0.,), where=mesh.exteriorFaces)
 2 from fipy import *
                                                                                    57
                                                                                    58 # Defining the discritized equation
 4 # space discretization
                                                                                    59 convCoeff = (vx, vy)
 5 \text{ w} = \text{h} = 1000 \# \text{m}
                                                                                    60 eq = (TransientTerm(coeff=1.0)
 6 dx = dy = 10 # m
                                                                                          + PowerLawConvectionTerm(coeff=convCoeff)
 7 \text{ nx}, ny = int(w/dx), int(h/dy)
                                                                                    62
                                                                                          == DiffusionTerm(coeff=D)
 8 \text{ mesh} = \text{Grid2D}(\text{nx=nx}, \text{dx=dx}, \text{ny=ny}, \text{dy=dy})
                                                                                    63

    ImplicitSourceTerm(s1Mask*le10) + s1Mask*le10*zs1)

 9 print('cellsNbr = ', mesh.globalNumberOfCells)
                                                                                   64
10
                                                                                    65 # Ploting the results
11 # time discretization
                                                                                    66 viewer = Viewer(vars = (z),
12 # Advection
                                                                                    67
                                                                                                          datamin = z.min() - .1,
13 \text{ vx} = \text{vy} = 10. \# \text{m/s}
                                                                                    68
                                                                                                          datamax = z.max()+.1)
14 \, \text{Cr} = 0.5
                                                                                    69
15 dtAdv = abs(Cr*dx/max(vx,vy))
                                                                                    70 # Iterating in time
16 # Diffusion
                                                                                    71 for step in range(stepsNbr):
17 D = 80.
                                                                                    72
                                                                                            eq.solve(var=z, dt=dt)
18 Fr = 0.5 # Courant Number: Cr = u*dt/dx
                                                                                    73
                                                                                            viewer.plot()
19 dtDiff = abs(Fr*dx/max(vx,vy))
                                                                                   74
20 dt = min(dtAdv,dtDiff)
21 \text{ stepsNbr} = 100
                                                                                                75 print('dx = ', dx, '\n
                                                                                                           'dy = ', dy,
                                                                                                                         '\n'
22
                                                                                                76
                                                                                                          'nx = ', nx, '\n'
                                                                                                77
23 def sourceMask(x, y, xcs, ycs, width, isRectangular = False):
                                                                                                          'ny = ', ny, '\n'
                                                                                                78
24
        # rectangular
                                                                                                          'vx = ', vx, '\n'
'vy = ', vy, '\n'
                                                                                                79
25
        if isRectangular:
                                                                                                80
26
             return ((xcs-width<x) & (x<xcs+width) \
                                                                                                          'Cr = ', Cr, '\n'
                                                                                                81
                                                                                                          'dtAdv = ', dtAdv, '\n'
'D = ', D, '\n'
'Fr = ', Fr, '\n'
27
                 & (ycs-width<y) & (y<ycs+width))
                                                                                                82
28
        # circular
                                                                                                83
29
        else:
                                                                                                84
30
             ds = DistanceVariable(mesh=mesh.
                                                                                                          'dtDiff = ', dtDiff, '\n'
                                                                                                85
31
                                       value=numerix.sqrt((x-xcs)**2+(y-ycs)**2)
                                                                                                86
                                                                                                          'dt = min(dtAdv,dtDiff) = ', dt, '\n'
32
             return (ds <= width)
                                                                                                87
                                                                                                          'stepsNbr = ', stepsNbr, '\n'
33
                                                                                                          'xcs1 = ', xcs1, '\n'
'ycs1 = ', ycs1, '\n'
                                                                                                88
                                                                                                89
34 # prepare SourceTerm (at the closest grid cell to xsl)
                                                                                                          'zs1 = ', zs1, '\n')
35 \times 1, y \times 1 = 250, 250
36 ds1 = DistanceVariable(mesh=mesh,
                                                                                               cellsNbr =
37
                              value=numerix.sqrt((mesh.x-xs1)**2+(mesh.y-ys1)**2))
                                                                                               dx = 10
38 \text{ slCellMask} = (dsl == dsl.min())
39 xcs1, *_ = mesh.x[s1CellMask]
40 ycs1, *_ = mesh.y[s1CellMask]
                                                                                               dt = min(dtAdv, dtDiff) = 0.5
                                                                                       1000
                                                                                                                                                1200
41 \text{ slWidth} = 40
42 slMask = sourceMask(x=mesh.x,
43
                           y=mesh.y,
                                                                                        800
                                                                                                                                                1000
44
                           xcs=xcs1.
45
                          ycs=ycs1,
46
                           width=slWidth,
                                                                                        600
                                                                                                                                                800
47
                           isRectangular=False)
48 \text{ zs1} = 1200.
50 # unkown's initialization
                                                                                        400
                                                                                                                                                600
51 zInit = CellVariable(mesh=mesh, value=200.)
52 zInit.setValue(value=zs1, where=s1Mask)
53 z = CellVariable(mesh=mesh, value=zInit)
54
                                                                                        200
                                                                                                                                                400
 General
                                    \nabla \cdot (\vec{u}\phi) = \left[\nabla \cdot (\Gamma_i \nabla)\right]^n \phi + S_{\phi}
 Conservation
                                                                                          0
                                                                                                                                                200
 Equation
                                                                                            0
                                                                                                    200
                                                                                                             400
                                                                                                                      600
                                                                                                                               800
                                                                                                                                       1000
                       transient
                                     convection
                                                           diffusion
                                                                             source
```

55 # closed BC (Neumann), i.e. grad(y) = 0

```
1 import numpy as np
 2 from fipy import *
4 # space discretization
 5 dx = 60.
 6 geoFileName = '/content/drive/MyDrive/lago.geo.txt'
 7 mesh = Gmsh2D(geoFileName)
 8 print('cellsNbr = ', mesh.globalNumberOfCells)
33 # prepare SourceTerm (at the closest grid cell to xsl)
34 \times 1, y \times 1 = 1500, 200
74 print('dx = ', dx, '\n'
         'vx = ', vx, '\n'
75
         'vy = ', vy, '\n'
76
         'Cr = ', Cr, '\n'
77
78
         'dtAdv = ', dtAdv, '\n'
79
         'D = ', D, ' \ n'
         'Fr = ', Fr, '\n'
80
         'dtDiff = ', dtDiff, '\n'
81
82
         'dt = min(dtAdv,dtDiff) = ', dt, '\n'
83
         'stepsNbr = ', stepsNbr, '\n'
         'xcs1 = ', xcs1, '\n'
84
85
         'ycs1 = ', ycs1, '\n'
         'zs1 = ', zs1, '\n')
86
```

```
mesh.globalNumberOfCells = 1466
dx = 60.0
vx = 10.0
vy = 10.0
Cr = 0.5
dtAdv = 3.0
D = 80.0
Fr = 0.5
dtDiff = 3.0
dt = min(dtAdv,dtDiff) = 3.0
stepsNbr = 10
xcs1 = 1511.5147564586898
ycs1 = 196.30208451099128
zs1 = 1200.0
```

