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Method of manufacturing zeolite-carbon composite and method of treating exhaust gas

Abstract

Provided is a method of treating an exhaust gas including preparing a rotor provided with a zeolite-carbon composite therein, providing a mixed gas including an organic gas and an alkali gas in the rotor, adsorbing the organic gas and the alkali gas to the zeolite-carbon composite, and desorbing the organic gas and the alkali gas from the zeolite-carbon composite, and the zeolite-carbon composite includes a zeolite and a carbon layer on the zeolite.

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Background/Summary

CROSS-REFERENCE TO RELATED APPLICATIONS

(1) This U.S. non-provisional patent application claims priority under 35 U.S.C. § 119 to Korean Patent Application No. 10-2022-0056060, filed on May 6, 2022, in the Korean Intellectual Property Office, the entire contents of which are hereby incorporated by reference.

BACKGROUND OF THE INVENTION

(2) The inventive concept relates to a method of manufacturing a zeolite-carbon composite and a method of treating an exhaust gas using the zeolite-carbon composite.

(3) An exhaust gas produced in industrial facilities such as various power plants or factories may contain chemical substances. The chemical substances contained in the exhaust gas has been identified as a cause of environmental pollution. Accordingly, research to reduce emission of the chemical substances in the exhaust gas has been actively conducted worldwide. However, because the exhaust gas includes several types of chemical substances, it was difficult to separate and remove different types of chemical substances.

SUMMARY

(4) An embodiment of the inventive concept provides a method of manufacturing a zeolite-carbon composite having high adsorption capacity for different types of gases.

(5) An embodiment of the inventive concept provides a method of treating an exhaust gas which is simplified and has an improved yield.

(6) The inventive concept relates to a method of manufacturing a zeolite-carbon composite and a method of treating an exhaust gas. According to embodiments of inventive concept, a method of treating an exhaust gas may include providing a mixed gas including an organic gas and an alkali gas in a rotor provided with a zeolite-carbon composite therein, adsorbing the organic gas and the alkali gas to the zeolite-carbon composite, and desorbing the organic gas and the alkali gas from the zeolite-carbon composite, and the zeolite-carbon composite may include a zeolite and a carbon layer on the zeolite.

(7) According to embodiments of inventive concept, a method of treating an exhaust gas may include providing a mixed gas including a hydrophobic gas and a hydrophilic gas in a rotor provided with a zeolite-carbon composite therein, adsorbing the hydrophobic gas and the hydrophilic gas to the zeolite-carbon composite under a first temperature condition, desorbing the hydrophobic gas and the hydrophilic gas from the zeolite-carbon composite under a second temperature condition and combusting the desorbed hydrophobic gas and the desorbed hydrophilic gas, the second temperature may be higher than the first temperature, and the zeolite-carbon

composite may include a zeolite and a carbon layer on an outer surface of the zeolite.

(8) According to embodiments of inventive concept, a method of manufacturing a zeolite-carbon composite according to an embodiment of the inventive concept may include preparing a mixture including a zeolite, an acid catalyst, and a saccharide and heat-treating the mixture to form a zeolite-carbon composite, and the zeolite-carbon composite may include the zeolite and a carbon layer on an outer surface of the zeolite.

Description

BRIEF DESCRIPTION OF THE DRAWINGS

(1) Example embodiments will be more clearly understood from the following brief description taken in conjunction with the accompanying drawings. The accompanying drawings represent non-limiting, example embodiments as described herein.

(2) FIG. 1 is a flowchart for explaining a method of manufacturing a zeolite-carbon composite according to embodiments.

(3) FIG. 2A is a schematic diagram illustrating zeolite particles.

(4) FIG. 2B is a view illustrating a zeolite according to embodiments, and corresponds to an enlarged view of part “A” of FIG. 2A.

(5) FIG. 2C is a view for explaining a crystal structure of a zeolite according to embodiments.

(6) FIG. 3 is a view for explaining a preparation of a mixture according to the embodiments.

(7) FIG. 4A is a schematic diagram illustrating composite particles according to embodiments.

(8) FIG. 4B is a view for explaining a zeolite-carbon composite according to embodiments, and corresponds to an enlarged view of part “A” of FIG. 4A.

(9) FIG. 5 is a view for explaining an exhaust gas treatment system according to embodiments.

(10) FIG. 6 is a flowchart illustrating a method of treating an exhaust gas according to embodiments.

(11) FIGS. 7A to 7E are views for explaining a method of treating an exhaust gas according to embodiments,

(12) FIG. 8 shows X-ray diffraction (XRD) analysis results of Comparative Examples and Experimental Examples.

(13) FIG. 9A is a graph illustrating thermogravimetric analysis (TGA) results of Comparative Examples and Experimental Examples.

(14) FIG. 9B is a graph illustrating thermogravimetric analysis (TGA) results of Comparative Examples and Experimental Examples.

(15) FIG. 10A illustrates results of evaluating adsorption capacity of Comparative Examples and Experimental Examples.

(16) FIG. 10B shows results of evaluating adsorption capacity of Comparative Examples and Experimental Examples.

DETAILED DESCRIPTION

(17) Although any methods and materials similar or equivalent to those described herein can be used in the practice or testing of embodiments described herein, some preferred methods, compositions, devices, and materials are described herein. However, before the present materials and methods are described, it is to be understood that this invention is not limited to the particular compositions, methodologies or protocols herein described, as these may vary in accordance with routine experimentation and optimization. It is also to be understood that the terminology used in the description is for the purpose of describing the particular versions or embodiments only, and is not intended to limit the scope of the embodiments described herein.

(18) Unless otherwise defined, all technical and scientific terms used herein have the same meaning as commonly understood by one of ordinary skill in the art to which this invention belongs.

However, in case of conflict, the present specification, including definitions, will control.

Accordingly, in the context of the embodiments described herein, the following definitions apply.

(19) As used herein and in the appended claims, the singular forms “a”, “an” and “the” include plural reference unless the context clearly dictates otherwise. Thus, for example, reference to “a zeolite” is a reference to one or more zeolites and equivalents thereof known to those skilled in the art, and so forth.

(20) As used herein, the term “comprise” and linguistic variations thereof denote the presence of recited feature(s), element(s), method step(s), etc. without the exclusion of the presence of additional feature(s), element(s), method step(s), etc. Conversely, the term “consisting of” and linguistic variations thereof, denotes the presence of recited feature(s), element(s), method step(s), etc. and excludes any unrecited feature(s), element(s), method step(s), etc., except for ordinarily-associated impurities. The phrase “consisting essentially of” denotes the recited feature(s), element(s), method step(s), etc. and any additional feature(s), element(s), method step(s), etc. that do not materially affect the basic nature of the composition, system, or method. Many embodiments herein are described using open “comprising” language. Such embodiments encompass multiple closed “consisting of” and/or “consisting essentially of” embodiments, which may alternatively be claimed or described using such language.

(21) As used herein, the terms “about,” “approximate,” “at or about,” and “substantially” mean that the amount or value in question can be the exact value or a value that provides equivalent results or effects as recited in the claims or taught herein. That is, it is understood that amounts, sizes, formulations, parameters, and other quantities and characteristics are not and need not be exact, but may be approximate and/or larger or smaller, as desired, reflecting tolerances, conversion factors, rounding off, measurement error and the like, and other factors known to those of skill in the art such that equivalent results or effects are obtained. In some circumstances, the value that provides equivalent results or effects cannot be reasonably determined. In such cases, it is generally understood, as used herein, that “about” and “at or about” mean the nominal value indicated $\pm 10\%$ variation unless otherwise indicated or inferred. In general, an amount, size, formulation, parameter or other quantity or characteristic is “about,” “approximate,” or “at or about” whether or not expressly stated to be such. It is understood that where “about,” “approximate,” or “at or about” is used before a quantitative value, the parameter also includes the specific quantitative value itself, unless specifically stated otherwise.

(22) Herein, like reference numerals may refer to like elements throughout the drawings. Herein, a composite may include a zeolite-carbon composite.

(23) The present disclosure provides a method of treating an exhaust gas, the method comprising providing a mixed gas including an organic gas and an alkali gas in a rotor provided with a zeolite-carbon composite there adsorbing the organic gas and the alkali gas to the zeolite-carbon composite, and desorbing the organic gas and the alkali gas from the zeolite-carbon composite, wherein the zeolite-carbon composite comprises a zeolite and a carbon layer on the zeolite. The method may further comprise preparing a rotor provided with a zeolite-carbon composite therein prior to the providing the mixed gas in the rotor. In one embodiment, the carbon layer may be hydrophobic, the alkali gas may be hydrophilic, and the organic gas may be hydrophobic. In another embodiment, the rotor may comprise a first region and a second region, and the adsorbing of the organic gas and the alkali gas may be performed in the first region of the rotor, while the desorbing of the organic gas and the alkali gas may be performed in the second region of the rotor. In one embodiment, the second region of the rotor may be provided at a higher temperature than a temperature of the first region of the rotor. In some embodiment, the method may further comprise transferring the desorbed organic gas and the desorbed alkali gas to a combustion facility, and combusting the organic gas and the alkali gas in the combustion facility. In one embodiment, the providing of the mixed gas may comprise supplying a first gas through a first duct, and supplying a second gas through a second duct where the first gas comprises the organic gas, and the second gas

comprises the alkali gas. In some embodiment, at least one of the first gas and the second gas may further comprise water vapor. In another embodiment, the second gas may further comprise the organic gas.

(24) The present disclosure also provides a method of treating an exhaust gas, the method comprising providing a mixed gas including a hydrophobic gas and a hydrophilic gas in a rotor provided with a zeolite-carbon composite therein, adsorbing the hydrophobic gas and the hydrophilic gas to the zeolite-carbon composite under a first temperature, desorbing the hydrophobic gas and the hydrophilic gas from the zeolite-carbon composite under a second temperature, and combusting the desorbed hydrophobic gas and the desorbed hydrophilic gas, wherein the second temperature is higher than the first temperature, and the zeolite-carbon composite comprises a zeolite and a carbon layer on an outer surface of the zeolite. The method may further comprise preparing a rotor provided with a zeolite-carbon composite therein prior to the providing the mixed gas in the rotor. In one embodiment, the rotor may comprise a first region and a second region, wherein the adsorbing of the organic gas and the alkali gas may be performed in the first region of the rotor, and the desorbing of the organic gas and the alkali gas may be performed in the second region of the rotor. In another embodiment, the combusting of the hydrophobic gas and the hydrophilic gas may be performed in a combustion facility, and the second region of the rotor may be provided between the first region of the rotor and the combustion facility. In some embodiment, the providing of the mixed gas may comprise supplying the hydrophobic gas to a mixing chamber through a first duct; supplying the hydrophilic gas to the mixing chamber through a second duct, the mixed gas being formed in the mixing chamber; and transferring the mixed gas from the mixing chamber into the rotor, wherein the first region of the rotor may be provided between the mixing chamber and the second region of the rotor. In one embodiment, the zeolite may comprise a pore therein, wherein the carbon layer does not block the pore of the zeolite, and the pore of the zeolite is connected to an external space. In some embodiment, the hydrophobic gas may comprise isopropyl alcohol, and the hydrophilic gas comprises ammonia.

(25) The present disclosure also provides a method of manufacturing a zeolite-carbon composite, the method comprising preparing a mixture including a zeolite, an acid catalyst, and a saccharide; and heat-treating the mixture to form a zeolite-carbon composite, wherein the zeolite-carbon composite comprises the zeolite and a carbon layer on an outer surface of the zeolite. In one embodiment, the zeolite may comprise silicon (Si) and aluminum (Al), and a molar ratio of the silicon to the aluminum may be 1 to 250 (or about 1 to about 250). In another embodiment, the zeolite-carbon composite has adsorption capacity for an organic gas and adsorption capacity for an alkali gas. In one embodiment, the heat-treating of the mixture may comprise carbonizing the saccharide to form the carbon layer. In some embodiment, the heat-treating of the mixture may be carried out at a temperature of 150° C. to 1000° C. (or about 150° C. to about 1000° C.). In another embodiment, the acid catalyst may be in an amount of 0.1 wt % to 100 wt % (or about 0.1 wt % to about 100 wt %) of the zeolite, and the acid catalyst may comprise at least one of a p-toluenesulfonic acid, an acetic acid, a hydrochloric acid, a nitric acid; a sulfuric acid, and a phosphoric acid.

(26) For instance, the zeolite-carbon composite may be manufacture (as described below.

(27) FIG. 1 is a flowchart for explaining a method of manufacturing a zeolite-carbon composite according to embodiments. FIGS. 2A to 4B are views for explaining a method of manufacturing a zeolite-carbon composite. FIG. 2A is a schematic diagram illustrating zeolite particles. FIG. 2B is a view illustrating a zeolite according to embodiments, and is an enlarged view of part “A” of HG. FIG. 2C is a view for explaining a crystal structure of a zeolite according to embodiments. FIG. 3 is a view for explaining a preparation of a mixture according to embodiments, and corresponds to an enlarged view of part “A” of FIG. 2A. FIG. 4A is a schematic diagram illustrating composite particles according to embodiments. FIG. 4B is a view for explaining a zeolite-carbon composite

according to embodiments, and is an enlarged view of part “A” of FIG. 4A.

(28) Referring to FIGS. 1, 2A, 2B, and 2C, a zeolite **100** may be prepared in **S10**. The zeolite **100** may be provided in the plural. The zeolites **100** may form a zeolite particle **101** as illustrated in FIG. 2A, The zeolite particle **101** may be provided in the plural. Each of the zeolite particles **101** may include the plurality of zeolites **100**. Hereinafter, a single zeolite **100** will be described for simplicity, but the inventive concept is not limited thereto.

(29) The zeolite **100** according to embodiments may be hydrophilic. The zeolite **100** may include silicon (Si) and aluminum (Al). A molar ratio of silicon to aluminum in the zeolite **100** may be 1 to 250 (or about 1 to about 250). When the molar ratio of silicon to aluminum is less than 1, the zeolite **100** may not be formed. When the molar ratio of silicon to aluminum is greater than 250, it may be difficult for a zeolite-carbon composite **10** to be described later to easily adsorb an alkali gas (e.g., an ammonia gas). The zeolite **100** may have a three-dimensional crystal structure. The zeolite **100** may have a pore **109** therein. The pore **109** of the zeolite **100** may be connected to an external space. The zeolite **100** may have an inner surface **100d** and an outer surface **100c** that face each other. The pore **109** may expose the inner surface **100d** of the zeolite **100**.

(30) The zeolite **100** may include a USY zeolite, ZSM zeolite (e.g., ZSM-5 zeolite), FAU zeolite, CHA zeolite, BEA zeolite, MOR zeolite, MFI zeolite, MWW zeolite, LTA zeolite, or a combination thereof. As an example, the zeolite **100** may have a structure as illustrated in FIG. 2C. However, the structure of the zeolite **100** is not limited to the example of FIG. 2C and may be variously modified.

(31) A degassing process of the zeolite **100** may be further performed. The degassing process of the zeolite **100** may be performed in the zeolite **100** at 90° C. to 400° C. (or about 90° C. to about 400° C.). The degassing process may be performed under an inert gas condition. The inert gas may include nitrogen gas, helium gas, or argon gas. As another example, the degassing process may be performed in the atmosphere. When the degassing process is performed at less than 90° C., it may be difficult to remove an internal gas in the zeolite **100**. The internal gas may include air, water vapor, or oxygen. According to embodiments, when the degassing process of the zeolite **100** is performed at a temperature condition of 90° C. or higher, the zeolite **100** may be degassed favorably. When the degassing process is performed at 400° C. or less, a crystal structure of the zeolite **100** may be favorably maintained during the degassing process.

(32) Referring to FIGS. 1 and 3, a mixture **400** including the zeolite **100**, a saccharide **210**, and an acid **300** may be prepared in **S11**. For example, the saccharide **210** and the acid **300** may be added to the zeolite **100** to prepare the mixture **400**. The mixture **400** may be in a liquid state. The saccharide **210** may include a monosaccharide, a disaccharide, an oligosaccharide, and a polysaccharide. For example, the saccharide **210** may include a disaccharide such as sucrose. As another example, the saccharide **210** may include lactose or maltose. The saccharide **210** may serve as a carbon source. The saccharide **210** may be 1 wt % to 500 wt % (or about 1 wt % to about 500 wt %) of the zeolites **100**.

(33) The acid **300** may be an acid catalyst. For example, the acid **300** may include a p-toluenesulfonic acid. As another example, the acid **300** may include an acetic acid, a hydrochloric acid, a nitric acid, a sulfuric acid, a phosphoric acid, or a mixture thereof. The acid **300** may be 0.1 wt % to 100 wt % (or about 0.1 wt % to about 100 wt %) of the zeolite **100**.

(34) The mixture **400** may be stirred, and the zeolite **100**, the saccharide **210**, and the acid **300** may be uniformly dispersed in the mixture **400**.

(35) A drying process of the mixture **400** may be further performed. The drying process may be performed under a condition of an inert gas such as argon gas, helium gas, or nitrogen gas. Alternatively, the drying process may be performed under the atmospheric condition. The drying process may be performed at a temperature condition of 90° C. to 400° C. (or about 0 CC to about 400° C.). When the drying process is performed at a temperature condition of 90° C. or higher, the zeolite **100** may be dried favorably. When the drying process is performed at 400° C. or less, the

crystal structure of the zeolite **100** may be maintained during the drying process.

(36) Referring to FIGS. **1**, **4A**, and **4B**, the mixture **400** may be heat-treated to form a zeolite-carbon composite **10** in **S12**. The heat treatment of the mixture **400** may include a carbonization process. For example, the saccharide **210** may be carbonized to form a carbon layer **200** as illustrated in FIG. **4B**. The carbon layer **200** may be formed on the outer surface **100c** of the zeolite **100**. In the carbonization process, the acid **301**) may act as a catalyst, and thus the saccharide **210** may be favorably carbonized. The carbon layer **200** may conformally cover the outer surface **100c** of the zeolite **100**. For example, a thickness of the carbon layer **200** on the outer surface **100c** of the zeolite **100** may be relatively uniform. The carbon layer **200** may not block the pore **109** in the zeolite **100**. For example, the carbon layer **200** may not cover the inner surface **100d** of the zeolite **100**. Accordingly, the specific surface area of the zeolite-carbon composite **10** may not be reduced. As another example, the carbon layer **200** may cover at least a portion of the inner surface **100d** of the zeolite **100**. Accordingly, composites may be prepared. The composites may be zeolite-carbon composites **10**.

(37) The heat treatment may be performed at a temperature condition of 150° C. to 1000° C. (or about 150° C. to about 1000° C.), When the heat treatment is performed at a temperature lower than 150° C., it may be difficult for the saccharide **210** to be carbonized. When the heat treatment is performed at a temperature of 1000° C. or less, the structure of the zeolite **100** may be maintained. The heat treatment process may be performed for about 1 hour to 5 hours, but the inventive concept is not limited thereto.

(38) When the acid **300** described in FIG. **3B** is less than 0.1 wt % of the zeolite **100**, the carbon layer **200** may non-uniformly cover the outer surface **100c** of the zeolite **100**. According to embodiments, when the acid **300** is 0.1 wt % or more of the zeolite **100**, the carbon layer **200** may uniformly cover the outer surface **100c** of the zeolite **100**. When the acid **300** is 100% or less of the zeolite **100**, decomposition of the saccharide **210** or the zeolite **100** during the carbonization process may be prevented or reduced.

(39) The zeolite-carbon composite **10** may be one of a plurality of zeolite-carbon composites **10**. A plurality of zeolite-carbon composites **10** may constitute a composite particle **102** as illustrated in FIG. **4A**. The composite particle **102** may be formed from the zeolite particle **101** described with reference to FIG. **2A**. The composite particle **102** may be provided in the plural. Preparation of the zeolite-carbon composites **10** may be completed according to a production example described above.

(40) Each of the zeolite-carbon composites **10** may have an adsorption capacity for an organic gas and an adsorption capacity for an alkali gas. The organic gas may be a hydrophobic gas. The alkali gas may be hydrophilic.

(41) In addition, for instance, a method of treating an exhaust gas using zeolite-carbon composites according to embodiments is performed as described below.

(42) FIG. **5** is a view for explaining an exhaust gas treatment system according to embodiments. FIG. **6** is a flowchart illustrating a method of treating an exhaust gas according to embodiments. FIGS. **7A** to **7E** are views for explaining a method of treating an exhaust gas according to embodiments.

(43) Referring to FIGS. **5**, **6**, and **7A**, an exhaust gas treatment system may be provided. An exhaust gas may include an organic gas **G1** and an alkali gas **G2**. The exhaust gas treatment system may include a first duct **610**, a second duct **620**, a mixing chamber **600**, a rotor **500**, and a combustion facility **700**. A first end of the first duct **610** and a first end of the second duct **620** may be connected to the mixing chamber **600**. A second end of the first duct **610** may be connected to an apparatus for manufacturing a semiconductor device. A second end of the second duct **620** may be connected to an apparatus for manufacturing a semiconductor device. The apparatus for manufacturing a semiconductor device connected to the first duct **610** may be the same as or different from the apparatus for manufacturing a semiconductor device connected to the second

duct **620**. The organic gas **G1** and the alkali gas **G2** may be generated in a process for manufacturing a semiconductor device. A first gas **G100** may be supplied to the mixing chamber **600** through the first duct **610**. The first gas **G100** may include the organic gas **G1**. The organic gas **G1** may include volatile organic compounds (VOC). The organic gas **G1** may be a hydrophobic gas. For example, the organic gas **G1** may include isopropyl alcohol (IPA). The first gas **G100** may further include water vapor. The first gas **G100** may further include an alkali gas as an impurity. In this case, a concentration of the organic gas **G1** in the first gas **G100** may be greater than a concentration of the alkali gas in the first gas **G100**.

(44) A second gas **G200** may be supplied to the mixing chamber **600** through the second duct **620**. The second gas **G200** may include a different type of gas from the first gas **G100**. The second gas **G200** may include an alkali gas **G2**. The alkali gas **G2** may be a hydrophilic gas. The alkali gas **G2** may include an ammonia gas. The second gas **G200** may further include water vapor. The second gas **G200** may further include an organic gas as an impurity. In this case, a concentration of the alkali gas **G2** in the second gas **G200** may be greater than a concentration of the alkali gas in the second gas **G200**.

(45) A mixed gas **G** by supplying the first gas **G100** and the second gas **G200** as illustrated in FIG. 7B may be formed in the mixing chamber **600**. The mixed gas **G** may be a mixed gas of the first gas **G100** and the second gas **G200**. In detail, the mixed gas **G** may include the organic gas **G1** and the alkali gas **G2**. The mixed gas **G** may further include water vapor.

(46) The rotor **500** including the zeolite-carbon composites **10** may be prepared in **S20**. The zeolite-carbon composites **10** may be provided inside the rotor **500**. In detail, the rotor **500** may include the composite particles **102** described with reference to FIG. 4A, and each of the composite particles **102** may include the zeolite-carbon composites **10** as illustrated in FIG. 7A.

(47) The rotor **500** may be provided on one side of the mixing chamber **600** and may be connected to the mixing chamber **600**. The rotor **500** may include a first region **501** and a second region **502**. The zeolite-carbon composites **10** may be provided in the first region **501** and the second region **502** of the rotor **500**. The first region **501** of the rotor **500** may be a region adjacent to the mixing chamber **600**. The first region **501** of the rotor **500** may be provided between the second region **502** and the mixing chamber **600**. The first region **501** of the rotor **500** may be provided at, for example, a first temperature condition. The first temperature condition may be 10° C. to 100° C. (or about 10° C. to about 100° C.).

(48) Referring to FIGS. 5, 6, and 7B, the mixed gas may be provided in the rotor **500** from the mixing chamber **600** in **S21**. For example, the mixed gas **G** may move from the mixing chamber **600** into the rotor **500**.

(49) Unlike that illustrated in FIG. 5, the exhaust gas treatment system may not include the mixing chamber **600**. The first duct **610** and the second duct **620** may be directly connected to the rotor **500**. The first gas **G100** may be supplied to the rotor **500** through the first duct **610**, and the second gas **G200** may be supplied to the rotor **500** through the second duct **620**. In this case, providing the mixed gas **G** may include supplying the first gas **G100** and the second gas **G200** into the rotor **500** to form the mixed gas **G**.

(50) Referring to FIGS. 5, 6, and 7C, the organic gas **G1** and the alkali gas **G2** may be adsorbed to the zeolite-carbon composites **10** in **S22**. The adsorption of the organic gas **G1** and the alkali gas **G2** may be performed in the first region **501** of the rotor **500**.

(51) The organic gas **G1** may be hydrophobic. The zeolite-carbon composites **10** may have high adsorption capacity for the organic gas **G1** because the carbon layer **200** is hydrophobic. For example, the organic gas **G1** may be adsorbed to the carbon layer **200**. Herein, adsorption capacity for the organic gas may be adsorption capacity for the organic gas **G1**.

(52) The alkali gas **G2** may be hydrophilic. The zeolite-carbon composites **10** may have high adsorption capacity for the alkali gas **G2** because the zeolite **100** according to the embodiments is hydrophilic. For example, the alkali gas **G2** may be adsorbed to the zeolite **100**. Alternatively, the

alkali gas G2 may be adsorbed to the carbon layer 200. Hereinafter, adsorption capacity for the alkali gas may be adsorption capacity for the alkali gas G2.

(53) When the carbon layer 200 is omitted, the hydrophobic gas may have a low adsorption for the zeolite 100. When the exhaust gas is treated using the zeolite 100, it may be difficult for the hydrophobic gas to be adsorbed to the zeolite 100. For example, the organic gas G1 may be difficult to adsorb to the zeolite 100. In this case, after the organic gas G1 and the alkali gas G2 are separated from each other, a process of treating the organic gas G1 may be performed by a process separate from a process treating of the alkali gas G2. Accordingly, the treating of the exhaust gas may be complicated, and the exhaust gas treatment system may have a large size. In this case, when the first gas G100 of FIG. 5 includes the alkali gas G2 as an impurity, it may be difficult to remove the alkali gas G2 in the process of treating the first gas G100. When the second gas G200 of FIG. 5 includes the organic gas G1 as an impurity, it may be difficult to remove the organic gas G1 in the process of treating the second gas G200.

(54) According to embodiments, the zeolite-carbon composites 10 may have the adsorption capacity for the organic gas and the adsorption capacity for alkali gas, and thus one type of zeolite-carbon composites 10 may be used to treat the organic gas G1 and the alkali gas G2. For example, the organic gas G1 and the alkali gas G2 may be adsorbed onto the zeolite-carbon composites 10 substantially simultaneously in a single process. Accordingly, the process of treating the exhaust gas may be simplified. The organic gas G1 and the alkali gas G2 may be treated in a single exhaust gas treatment system. For example, an adsorption process of the organic gas G1 and an adsorption process of the alkali gas G2 may be performed in the single rotor 500. Accordingly, the exhaust gas treatment system may be downsized.

(55) According to the embodiments, although the first gas G100 supplied from the first duct 610 of FIG. 5 contains the alkali gas as an impurity, the treating of the organic gas G1 and the alkali gas G2 may be performed in a single process, and thus the impurity (e.g., alkali gas) in the first gas G100 may be favorably removed. Likewise, although the second gas G200 of FIG. 5 includes the organic gas as an impurity, the impurity (e.g., organic gas) in the second gas G200 may be favorably removed by the zeolite-carbon composites 10. A removal yield of the exhaust gas may be improved.

(56) According to embodiments, although the mixed gas G of FIG. 7B further includes water vapor, the zeolite-carbon composites 10 may have high adsorption capacity for the organic gas and high adsorption capacity for the alkali gas. That is, the zeolite-carbon composites 10 may have improved the adsorption capacity for the organic gas and the adsorption capacity for the alkali gas under a high humidity condition.

(57) The adsorption capacity for the organic gas and the adsorption capacity for the alkali gas may have a trade-off relationship with each other. According to embodiments, a thickness, the area, and weight of the carbon layer 200 may be adjusted. For example, as described in the example of FIGS. 3A and 3B, the saccharide 210 in the mixture 400 may be from 1 wt % to 500 wt (or from about 1 wt % to about 500 wt of the zeolite 100, and the acid 300 may be 0.1 wt % to 100 wt % of the zeolite 100. Accordingly, the carbon layer 200 may cover the outer surface 100c of the zeolite 100, but may not block the pore 109 of the zeolite 100. The zeolite-carbon composites 10 prepared according to the embodiments may have the high adsorption capacity for the organic gas and the high adsorption capacity for the alkali gas.

(58) The carbonization process temperature described in the example of FIGS. 4A and 4B may be adjusted, and thus the carbon layer 200 may have a loose packing structure. Accordingly, ammonia adsorption capacity of the zeolite-carbon composite 10 may be increased. When the carbonization process temperature is higher than 1000° C., the carbon layer 200 may have an excessively rigid packing structure. In this case, the adsorption capacity of the zeolite-carbon composite 10 may be reduced. According to embodiments, the carbonization process may be performed under a temperature condition of 150° C. to 1000° C. (or about 150° C. to about 1000° C.) to form the

zeolite-carbon composites **10**. The zeolite-carbon composites **10** may have improved adsorption capacity for the organic gas and adsorption capacity for the alkali gas.

(59) Referring to FIGS. 5, 6, and 7D, the zeolite-carbon composites **10** of the first region **501** of the rotor **500** may move to the second region **502** of the rotor **500** by rotation of the rotor **500**.

Accordingly, the zeolite-carbon composites **10** to which the organic gas G1 and the alkali gas G2 are adsorbed may be provided in the second region **502** of the rotor **500**. The second region **502** of the rotor **500** may be adjacent the combustion facility **700**. For example, the second region **502** of the rotor **500** may be provided between the first region **501** of the rotor **500** and the combustion facility **700**. The second region **502** of the rotor **500** may be provided at a second temperature condition higher than the first temperature of the rotor **500**. For example, the second temperature condition may be approximately 150° C. to 350° C. (or about 1.50° C. to about 350° C.).

(60) In the second temperature condition, the organic gas G1 and the alkali gas G2 may be desorbed from the zeolite-carbon composites **10** in S23. When the second region **502** of the rotor **500** is lower than 1.50° C., it may be difficult for the organic gas G1 or the alkali gas G2 to be desorbed from the zeolite-carbon composites **10**. When the second region **502** of the rotor **500** is higher than 350° C., the zeolite **100** may be damaged. According to embodiments, the desorption process may be performed at 150° C. to 350° C. (or about 150° C. to about 350° C.), and thus the organic gas G1 and the alkali gas G2 may be favorably desorbed from the zeolite-carbon composites **10**. The zeolite-carbon composites **10** according to the embodiments may have, thermal stability at the second temperature. Accordingly, during the desorption process, the zeolite-carbon composites **10** may not be damaged.

(61) Referring to FIGS. 5, 6, and 7E, the desorbed organic gas G1 and alkali gas G2 may move from the second region **502** of the rotor **500** to the combustion facility **700**.

(62) The organic gas G1 and the alkali gas G2 may be combusted in the combustion facility **700** in S24. Accordingly, the organic gas G1 and the alkali gas G2 may be removed.

(63) Referring back to FIGS. 6 and 7A, after the desorption process, the zeolite-carbon composites **10** desorbed may move from the second region **502** of the rotor **500** to the first region **501** of the rotor **500** by the rotation of the rotor **500**. The adsorption process and the desorption process may be repeatedly performed using the zeolite-carbon composites **10**. The zeolite-carbon composites **10** may be reused in the adsorption process and the desorption process, thereby simplifying the process.

(64) [Preparation of Zeolite-Carbon Composite]

1. Comparative Examples

(1) Comparative Example 1

(65) USY zeolite was prepared. Here, a Si/Al molar ratio in the zeolite is 30.

(2) Comparative Example 2

(66) ZSM-5 zeolite was prepared. Here, a Si/Al molar ratio in the zeolite is 50.

2. Experimental Examples

(67) Zeolite-carbon composites according to Comparative Examples 3 and 4, and Experimental Examples were prepared under conditions as illustrated in Table 1 below.

(68) First, a USY zeolite was prepared. Here, a Si/Al molar ratio in the zeolite is illustrated in Table 1 below. 10 g of zeolite was dried in an oven at 120° C. for 12 hours to perform a degassing process of the zeolite. An aqueous solution in which a sucrose and a p-toluenesulfonic acid were dissolved in the degassed zeolite was added to prepare a mixture. The mixture was stirred at 25° C. at a speed of 2000 rpm for 10 minutes to disperse the sucrose, the p-toluenesulfonic acid, and the zeolite. The mixture was dried in an oven at 120° C. for 12 hours to remove moisture in the zeolite. Under atmospheric conditions, the mixture was calcined for 2 hours at an elevated temperature of 2° C./min to perform a carbonization process. Accordingly, zeolite-carbon composites such as Experimental Example 1-5, Experimental Example 1-10, Experimental Example 1-25, Experimental Example 1-50, and Experimental Example 1-100, Experimental Example 2-300,

Experimental Example 2-500, Experimental Example 2-700, and Experimental Example 2-900 were prepared.

(69) TABLE-US-00001 TABLE 1 Weight of Weight zeolite:weight Carbonization Si/Al molar Weight of percent of of p- process ratio in zeolite:weight sucrose to toluenesulfonic temperature zeolite of sucrose zeolite (wt %) acid (° C.) Experimental 30 1:0.05 5 1:0.065 900 Example 1-5 Experimental 1:0.1 10 1:0.13 Example 1-10 Experimental 1:0.25 25 1:0.325 Example 1-25 Experimental 1:0.5 50 1:0.65 Example 1-50 Experimental 1:1 100 1:1.3 Example 1-100 Experimental 1:0.75 75 1:0.975 300 Example 2-300 Experimental 500 Example 2-500 Experimental 700 Example 2-700 Experimental 900 Example 2-900 Comparative 1100 Example 3 Comparative 1:0 0 0 900 Example 4

[Evaluation of Characteristics of Zeolite-Carbon Composite]

1. X-Ray Diffraction Analysis

(70) FIG. 8 is X-ray diffraction (XRD) analysis results of Comparative Example 1, Comparative Example 3, Experimental Example 2-300, Experimental Example 2-500, Experimental Example 2-700, and Experimental Example 2-900,

(71) Referring to FIG. 8, the zeolite of Comparative Example 1 (C1) has a crystal structure. Experimental Example 2-300 (E2-300), Experimental Example 2-500 (E2-500), Experimental Example 2-700 (E2-700), and Experimental Example 2-900 (E2-900) are carried out at 300° C., 500° C., 700° C., and 900° C., respectively. The zeolite-carbon composites of Experimental Example 2-300 (E2-300), Experimental Example 2-500 (E2-500), Experimental Example 2-700 (E2-700), and Experimental Example 2-900 (E2-900) have a crystal structure, respectively.

(72) Comparative Example 3 (C3) do not have a crystal structure. In the case of Comparative Example 3 (C3), the carbonization process is performed at 1100° C., and the crystal structure of the zeolite may be damaged.

(73) According to embodiments, the carbonization process is performed at 150° C. to 1000° C., the crystal structure of the zeolite may be maintained although the carbon layer is formed.

(74) 2. Thermogravimetric Analysis

(75) FIG. 9A is a graph illustrating thermogravimetric analysis (TGA) results of Comparative Example 4, Experimental Example 1-5, Experimental Example 1-10, Experimental Example 1-25, Experimental Example 1-50, and Experiment 1-100. FIG. 9B is a graph illustrating thermogravimetric analysis (TGA) results of Comparative Example 3, Comparative Example 4, Experimental Example 2-300, Experimental Example 2-500, Experimental Example 2-700, and Experimental Example 2-900. The thermogravimetric analysis is evaluated by measuring a change in weight depending on temperature. In FIGS. 9A and 9B, a horizontal axis is temperature, and a vertical axis is a weight of the remaining zeolite-carbon composite relative to a weight of an original zeolite-carbon composite.

(76) Referring to FIG. 9A, although the temperature is increased up to 400° C. or less, the weights of Comparative Example 4 (C4), Experimental Example 1-5 (E1-5), Experimental Example 1-10 (E1-10), Experimental Example 1—The weights of 25 (E1-25), Experimental Example 1-50 (E1-50), and Experimental 1-100 (E1-100) are kept unchanged. It may be seen that the zeolite-carbon composites of Experimental Example 1-5 (E1-5), Experimental Example 1-10 (E1-10), Experimental Example (E1-25), Experimental Example 1-50 (E1-50), and Experimental 1-100 (E1-100) have thermal stability at the temperature condition of 400° C. or less.

(77) Referring to FIG. 9B, although the temperature is increased up to 400° C. or less, the weights of Comparative Example 3 (C3), Comparative Example 4 (C4), Experimental Example 2-300 (E2-300), Experimental Example 2-500 (E2-500), Experimental Example 2-700 (E2-700), and Experimental Example 2-900 (E2-900) are kept unchanged. It may be seen that the zeolite-carbon composites of Experimental Example 2-300 (E2-300), Experimental Example 2-500 (E2-500), Experimental Example 2-700 (E2-700), and Experimental Example 2-900 (E2-900) have thermal stability at the temperature condition of 400° C. or less.

(78) According to embodiments, adsorbing the organic gas and the alkali gas to the zeolite-carbon composites in S22 described in FIGS. 4, 5, and 7C and desorbing the organic gas and the alkali gas from the zeolite-carbon composites in S23 may be performed at a temperature condition of 400° C. or less. The zeolite-carbon composites according to the embodiments may have thermal stability at a temperature condition of 400° C. or less. Accordingly, the zeolite-carbon composites may not be damaged during the adsorption process and the desorption process. The adsorption process and the desorption process may be repeatedly performed using the zeolite-carbon composites.

(79) 3. Evaluation of Adsorption Capacity

(80) 0.3 g of a zeolite-carbon composite or 0.3 g of a zeolite was heat-treated under vacuum conditions of 300° C. for 4 hours, to perform a degassing process. The adsorption capacity evaluation was performed at 1 bar, 25° C., and 70% relative humidity using a fixed bed continuous flow reactor. The adsorption capacity evaluation was performed using a mixed gas, and the mixed gas may include 200 ppm of isopropyl alcohol (IPA), 1000 ppm of ammonia (NH₃), and helium (He). The mixed gas was supplied to the fixed bed continuous flow reactor at 100 ccm (cc/min). The adsorption capacity was evaluated by measuring a break point curve. The adsorption capacity may be evaluated by an adsorption amount. The adsorption capacity evaluation was performed on the zeolites of Comparative Example 1, Comparative Example 2, and Comparative Example 4 and the zeolite-carbon composites of Experimental Examples 1-5, Experimental Examples 1-10, Experimental Examples 1-25, Experimental Examples 1-50, Experiments 1-100, Experiments Example 2-300, Experimental Example 2-500, Experimental Example 2-700, and Experimental Example 2-900, respectively.

(81) FIG. 10A illustrates results of evaluating adsorption capacity of Comparative Example 1, Comparative Example 2, Experimental Example 1-5, Experimental Example 1-10, Experimental Example 1-25, Experimental Example 1-50, and Experiment 1-100. In FIG. 10A, IPA means isopropyl alcohol.

(82) Referring to FIG. 10A, Experimental Example 1-5 (E1-5), Experimental Example 1-10 (E1-10), Experimental Example 1-25 (E1-25), Experimental Example 1-50 (E1-50), and Experimental Example 1-100 (E1-100) have a greater adsorption amount of an isopropyl gas than that of Comparative Example 1 (C1). The adsorption amount of the isopropyl gas in Experimental Example 1-5 (E1-5) is 7% greater than that of Comparative Example 1 (C1). The adsorption amount of the isopropyl gas in Experimental Example 1-10 (E1-10) is 16% greater than that of Comparative Example 1 (C1). The adsorption amount of the isopropyl gas in Experimental Example 1-25 (E1-25) is 26 greater than that of Comparative Example 1 (C1). The adsorption amount of the isopropyl gas in Experimental Example 1-50 (E1-50) is 39% greater than that of Comparative Example 1 (C1). The adsorption amount of the isopropyl gas in Experimental Example 1-100 (E1-100) is 81% greater than that of Comparative Example 1 (C1). Comparative Example 1 (C1) is a zeolite without a carbon layer.

(83) Experimental Example 1-5 (E1-5), Experimental Example 1-10 (E1-10), Experimental Example 1-25 (E1-25), Experimental Example 1-50 (E1-50), and in the experiment 1-100 (E1-100) have a larger adsorption amount of ammonia gas than that of Comparative Example 2 (C2). Experimental Example 1-5 (E1-5) has the same or similar ammonia gas adsorption capacity as/to Comparative Example 2 (C2). Comparative Example 2 (C2) is a zeolite without a carbon layer.

(84) According to embodiments, the carbon layer may be coated on the outer surface of the zeolite by the carbonization process. Isopropyl alcohol may be hydrophobic. The zeolite-carbon composites may have high adsorption capacity for isopropyl alcohol because the carbon layer is hydrophobic. The zeolite according to embodiments may be hydrophilic. The zeolite-carbon composites may have high adsorption capacity for ammonia because an ammonia gas is hydrophilic.

(85) FIG. 10B is results of evaluating adsorption capacity of Comparative Example 2, Comparative Example 3, Experimental Example 2-300, Experimental Example 2-500, Experimental Example 2-

700, and Experimental Example 2-900. In FIG. 10B, IPA means isopropyl alcohol.

(86) Referring to FIG. 10B, Comparative Example 3 (C3) may be prepared by performing a carbonization process at a temperature of 1100° C. The zeolite-carbon composites of Experimental Example 2-300 (E2-300), Experimental Example 2-500 (E2-500), Experimental Example 2-700 (E2-700), and Experimental Example 2-900 (E2-900) may be formed by performing carbonization processes at 300° C., 500° C., 700° C., and 900° C., respectively. Experimental Example 2-300 (E2-300), Experimental Example 2-500 (E2-500), Experimental Example 2-700 (E2-700), and Experimental Example 2-900 (E2-900) have a greater adsorption amount of isopropyl gas than that of Comparative Example 3 (C3).

(87) Experimental Example 2-300 (E2-300), Experimental Example 2-500 (E2-500), Experimental Example 2-700 (E2-700), and Experimental Example 2-900 (E2-900) have an adsorption amount of an ammonia gas greater than that of Comparative Example 3 (C3).

(88) Comparative Example 2 (C2) includes zeolite, but does not include a carbon layer. Each of Experimental Example 2-300 (E2-300), Experimental Example 2-500 (E2-500), Experimental Example 2-700 (E2-700), and Experimental Example 2-900 (E2-900) may have a zeolite and a carbon layer. Experimental Example 2-500 (E2-500), Experimental Example 2-700 (E2-700), and Experimental Example 2-900 (E2-900) have a higher isopropyl gas adsorption amount than that of Comparative Example 2 (C2). The adsorption amount of isopropyl gas of Experimental Example 2-500 (E2-500) is 13% greater than the adsorption amount of isopropyl gas of Comparative Example 2 (C2). The adsorption amount of isopropyl gas of Experimental Example 2-700 (E2-700) is 16 greater than the adsorption amount of isopropyl gas of Comparative Example 2 (C2). The adsorption amount of isopropyl gas of Experimental Example 2-900 (E2-900) is 3% greater than the adsorption amount of isopropyl gas of Comparative Example 2 (C2).

(89) Experimental Example 2-300 (E2-300), Experimental Example 2-500 (E2-500), Experimental Example 2-700 (E2-700), and Experimental Example 2-900 (E2-900) have a higher adsorption amount of ammonia gas than Comparative Example 2 (C2). The ammonia gas adsorption amount of Experimental Example 2-300 (E2-300) is 49% greater than the ammonia gas adsorption amount of Comparative Example 2 (C2). The ammonia gas adsorption amount of Experimental Example 2-500 (E2-500) is 32% greater than the ammonia gas adsorption amount of Comparative Example 2 (C2). The ammonia gas adsorption amount of Experimental Example 2-700 (E2-700) is 24% greater than the ammonia gas adsorption amount of Comparative Example 2 (C2). The adsorption amount of ammonia gas of Experimental Example 2-900 (E2-900) is 5% greater than the adsorption amount of ammonia gas of Comparative Example 2 (C2).

(90) According to the inventive concept, the zeolite-carbon composite may have the high adsorption capacity for the organic gas and the high adsorption capacity for the alkali gas. Using the zeolite-carbon composite, the organic gas and the alkali gas may be adsorbed by a single process. The desorption process of the organic gas and the alkali gas may be performed as a single process. Accordingly, the process of treating the exhaust gas may be simplified, and the exhaust gas treatment process yield may be improved.

(91) While embodiments are described above, a person skilled in the art may understand that many modifications and variations are made without departing from the spirit and scope of the inventive concept defined in the following claims. Accordingly, the example embodiments of the inventive concept should be considered in all respects as illustrative and not restrictive, with the spirit and scope of the inventive concept being indicated by the appended claims.

Claims

1. A method of treating an exhaust gas, the method comprising: providing a mixed gas including an organic gas and an alkali gas in a rotor provided with a zeolite-carbon composite therein; adsorbing the organic gas and the alkali gas to the zeolite-carbon composite; and desorbing the organic gas

and the alkali gas from the zeolite-carbon composite, wherein the zeolite-carbon composite includes: a zeolite and a carbon layer on the zeolite.

2. The method of claim 1, wherein the carbon layer is hydrophobic, and wherein the alkali gas is hydrophilic, and the organic gas is hydrophobic.

3. The method of claim 1, wherein the rotor has a first region and a second region, wherein the adsorbing of the organic gas and the alkali gas is performed in the first region of the rotor, and wherein the desorbing of the organic gas and the alkali gas is performed in the second region of the rotor.

4. The method of claim 3, wherein the second region of the rotor is provided at a temperature that is higher than a temperature of the first region of the rotor.

5. The method of claim 1, further comprising: transferring the desorbed organic gas and the desorbed alkali gas to a combustion facility; and combusting the organic gas and the alkali gas in the combustion facility.

6. The method of claim 1, wherein the providing of the mixed gas comprises: supplying a first gas through a first duct; and supplying a second gas through a second duct, wherein the first gas comprises the organic gas, and wherein the second gas comprises the alkali gas.

7. The method of claim 6, wherein at least one of the first gas and the second gas further comprises water vapor.

8. The method of claim 6, wherein the second gas further comprises the organic gas.

9. A method of treating an exhaust gas, the method comprising: providing a mixed gas including a hydrophobic gas and a hydrophilic gas in a rotor provided with a zeolite-carbon composite therein; adsorbing the hydrophobic gas and the hydrophilic gas to the zeolite-carbon composite under a first temperature; desorbing the hydrophobic gas and the hydrophilic gas from the zeolite-carbon composite under a second temperature; and combusting the desorbed hydrophobic gas and the desorbed hydrophilic gas, wherein the second temperature is higher than the first temperature, wherein the zeolite-carbon composite includes: a zeolite and a carbon layer on an outer surface of the zeolite.

10. The method of claim 9, wherein the rotor has a first region and a second region, wherein the adsorbing of the organic gas and the alkali gas is performed in the first region of the rotor, and wherein the desorbing of the organic gas and the alkali gas is performed in the second region of the rotor.

11. The method of claim 10, wherein the combusting of the hydrophobic gas and the hydrophilic gas is performed in a combustion facility, and wherein the second region of the rotor is provided between the first region of the rotor and the combustion facility.

12. The method of claim 10, wherein the providing of the mixed gas comprises: supplying the hydrophobic gas to a mixing chamber through a first duct; supplying the hydrophilic gas to the mixing chamber through a second duct, the mixed gas being formed in the mixing chamber; and transferring the mixed gas from the mixing chamber into the rotor, wherein the first region of the rotor is provided between the mixing chamber and the second region of the rotor.

13. The method of claim 9, wherein the zeolite has a pore therein, wherein the carbon layer does not block the pore of the zeolite, and wherein the pore of the zeolite is connected to an external space.

14. The method of claim 9, wherein the hydrophobic gas comprises isopropyl alcohol, and wherein the hydrophilic gas comprises ammonia.
