US Patent & Trademark Office Patent Public Search | Text View

United States Patent

Kind Code

B2

Date of Patent

August 19, 2025

Inventor(s)

Allidieres; Laurent et al.

Fluid supply and storage device, vehicle and method including such a device

Abstract

A liquefied fuel cryogenic tank has an inner jacket delimiting a fluid storage volume and an outer jacket disposed around the inner jacket with a vacuum thermal insulation gap therebetween. A withdrawal circuit has an assembly of one or more valves and a withdrawal line that has a first heating heat exchanger located outside the inner jacket and a second heating heat exchanger located inside the inner jacket. Fluid flows through the withdrawal line via the first heat exchanger and then the second heat exchanger or via the first heat exchanger without entering the second heat exchanger.

Inventors: Allidieres; Laurent (Paris, FR), Losco; Jerome (Sassenage, FR)

Applicant: L'Air Liquide, Societe Anonyme pour l'Etude et l'Exploitation des Procedes

Georges Claude (Paris, FR)

Family ID: 1000008764118

Assignee: L'Air Liquide, Societe Anonyme Pour l'Etude et l'Exploitation des Procedes

Georges Claude (Paris, FR)

Appl. No.: 17/719459

Filed: April 13, 2022

Prior Publication Data

Document IdentifierUS 20220325853 A1

Publication Date
Oct. 13, 2022

Foreign Application Priority Data

FR 2103778 Apr. 13, 2021

Publication Classification

Int. Cl.: F17C3/08 (20060101); F17C9/04 (20060101); F17C13/04 (20060101)

U.S. Cl.:

CPC

F17C3/08 (20130101); **F17C9/04** (20130101); **F17C13/04** (20130101); F17C2201/0109 (20130101); F17C2201/035 (20130101); F17C2203/0391 (20130101); F17C2203/0629 (20130101); F17C2205/0326 (20130101); F17C2205/0394 (20130101); F17C2221/012 (20130101); F17C2223/013 (20130101); F17C2223/033 (20130101); F17C2225/0123 (20130101); F17C2227/0302 (20130101); F17C2227/0379 (20130101); F17C2227/0381 (20130101); F17C2227/0388 (20130101); F17C2227/048 (20130101); F17C227/0105 (20130101)

Field of Classification Search

CPC:

F17C (3/08); F17C (9/04); F17C (13/04); F17C (2201/0109); F17C (2201/035); F17C (2203/0391); F17C (2203/0629); F17C (2205/0326); F17C (2205/0394); F17C (2221/012); F17C (2223/013); F17C (2223/033); F17C (2225/0123); F17C (2227/0302); F17C (2227/0379); F17C (2227/0381); F17C (2227/0388); F17C (2227/048); F17C (2270/0105); F17C (2201/054); F17C (2201/056); F17C (2205/0332); F17C (2205/035); F17C (2223/0161); F17C (2223/043); F17C (2225/035); F17C (2227/0107); F17C (2227/0306); F17C (2227/0311); F17C (2227/0316); F17C (2227/0374); F17C (2227/0393); F17C (2250/032); F17C (2250/043); F17C (2250/0439); F17C (2265/066); F17C (2270/0171); F17C (2270/0184); F17C (2270/0189); F17C (7/04); F17C (3/025); F17C (3/085); F17C (13/00); F17C (2203/0619); F17C (2205/0323); F17C (2227/0369); F17C (9/02); F17C (13/025); Y02E (60/32); Y02E (60/34); Y02E (60/50); B60K (15/03006); B60K (2015/03026); B60K (2015/03315); H01M (8/04089); H01M (8/04208); H01M (2250/20); Y02T (90/40)

References Cited

U.S. PATENT DOC	UMENTS
-----------------	--------

Patent No.	Issued Date	Patentee Name	U.S. Cl.	CPC
5644921	12/1996	Chowdhury	N/A	N/A
6634178	12/2002	Michel	62/48.1	F17C 13/025
6983611	12/2005	Reese	62/50.1	F17C 9/04
9746132	12/2016	Gustafson et al.	N/A	N/A
2007/0144183	12/2006	Sakajo	62/7	B60H 1/14
2009/0288426	12/2008	Lilletvedt et al.	N/A	N/A
2013/0061608	12/2012	Lurken	62/53.2	F17C 9/00
2015/0072260	12/2014	Brunner et al.	N/A	N/A
2018/0306383	12/2017	Poag et al.	N/A	N/A
2019/0113259	12/2018	Levin	N/A	F25B 17/086
2021/0372565	12/2020	Beuneken	N/A	F17C 5/06
2021/0372570	12/2020	Stubenrauch	N/A	F17C 3/00
2022/0026028	12/2021	Beuneken	N/A	F17C 13/025
2022/0146047	12/2021	Bensadoun	N/A	F17C 5/007

FOREIGN PATENT DOCUMENTS

Patent No.	Application Date	Country	CPC
103615657	12/2013	CN	N/A
106989272	12/2016	CN	N/A
43 20 556	12/1993	DE	N/A
1 521 933	12/2008	EP	N/A
2 813 746	12/2013	EP	N/A
2 706 822	12/1993	FR	N/A
WO-9954657	12/1998	WO	F02M 21/0221

OTHER PUBLICATIONS

French Search Report for FR 2 103 778, mailed Jan. 14, 2022. cited by applicant

Primary Examiner: Atkisson; Jianying C

Assistant Examiner: Adeniji; Ibrahim A. Michael

Background/Summary

CROSS-REFERENCE TO RELATED APPLICATIONS

(1) This application claims the benefit of priority under 35 U.S.C. § 119 (a) and (b) to French patent application No. FR 2103778, filed Apr. 13, 2021, the entire contents of which are incorporated herein by reference.

BACKGROUND

Field of the Invention

- (2) The invention relates to a fluid supply and storage device, to a vehicle and to a method including such a device.
- (3) The invention relates more particularly to a fluid supply and storage device, in particular an onboard device for storing hydrogen and supplying it to a user member, comprising a cryogenic tank for storing liquefied fluid of the double-wall and vacuum-insulated type comprising an inner jacket delimiting the fluid storage volume and an outer jacket disposed around the inner jacket with a vacuum thermal insulation gap between the two jackets, a withdrawal circuit comprising a withdrawal line comprising a first, upstream end connected to the upper part of the inner jacket and a second, downstream end intended to be connected to a user member, the withdrawal line comprising a first heating heat exchanger located outside the inner jacket and a second heating heat exchanger located inside the inner jacket, the withdrawal circuit comprising an assembly of one or more valves that is configured to ensure the passage of a flow of fluid circulating from the first end to the second end, in the process entering the first heat exchanger and then the second heat exchanger or in the process entering the first heat exchanger without entering the second heat exchanger.

Related Art

- (4) Such a device is described in document DE4329566A, for example.
- (5) The storage of hydrogen on board vehicles supplied with hydrogen fuel makes use of compressed gaseous hydrogen or hydrogen in liquid form.
- (6) If the stored capacities required are greater than 50 kg, on-board storage in liquid form is preferred. The liquid hydrogen is generally stored in a tank at low pressure (less than 13 bar absolute). At equilibrium, the temperature of the hydrogen is set by the pressure in the tank via the saturation curve between the liquid phase and the gaseous phase. This is applicable up to the

critical point of the hydrogen, which occurs at a pressure slightly less than 13 bar absolute.

- (7) The liquid hydrogen is generally produced at a pressure close to atmospheric pressure, generally between 1.15 and 1.3 bar absolute, corresponding to a temperature of between 20.8 K and 21.2 K. It is transported and transferred into the on-board tank using cryogenic trucks and a filling station. Since the transport and transfer are sources of heat influx, the temperature of the hydrogen in the tank corresponds to a saturation pressure of about 2 bar absolute, or 22.9 K.
- (8) Fuel cells (or possibly hydrogen-powered internal combustion engines "ICE") operate in general at a pressure less than 2 bar absolute in the heart of the cell. However, for various operational reasons, most manufacturers require an interface pressure with the tank of between 3 and 5 bar absolute.
- (9) Since the full tank is initially at a lower pressure, it is then necessary to increase its pressure up to a pressure greater than that of the fuel cell (ICE) and to control this pressure as the gas is consumed. It is therefore necessary to include in the tank a means for controlling its pressure.
- (10) The abovementioned document provides a supply of pressurized gas in the tank. This makes the installation more complex. This mode of control is not used in industry likewise because of the large quantities of gas required.
- (11) Moreover, in the known devices, the relative arrangements of cold lines, hot lines, cold exchangers and hot exchangers generate heat losses which adversely affect the efficiency of the installation.

SUMMARY OF THE INVENTION

- (12) An aim of the present invention is to overcome all or some of the drawbacks of the prior art that are set out above.
- (13) To that end, the device according to the invention, moreover in accordance with the generic definition given in the preamble above, is essentially characterized in that the inlet of the first heat exchanger receiving the flow of fluid coming from the first end of the withdrawal line is located in the vacuum thermal insulation gap between the two jackets.
- (14) Furthermore, embodiments of the invention may include one or more of the following features: at least a part of the first heat exchanger which is adjacent to the inlet receiving the flow of fluid coming from the first end of the withdrawal line is located in the vacuum thermal insulation gap between the two jackets, the first heat exchanger is housed in an exchanger housing, at least one portion of which is located in the vacuum thermal insulation gap between the two jackets, the housing comprises a first inlet receiving the flow of fluid coming from the first end of the circuit, said first inlet being located in the vacuum thermal insulation gap between the two jackets, the housing accommodates a part of the withdrawal circuit connecting the second heat exchanger to the second end, the housing comprising a second inlet receiving the flow of fluid coming from the second exchanger, said second inlet being located in the vacuum thermal insulation gap between the two jackets, the withdrawal circuit has a third heat exchanger disposed in series downstream of the second heat exchanger such that the third heat exchanger receives the flow that has passed into the second heat exchanger, the third heat exchanger is located outside the vacuum thermal insulation gap between the two jackets and in particular at least partially outside the outer jacket, the first heat exchanger and the third heat exchanger are housed in one and the same exchanger housing in a heat-exchange relationship with at least one flow of heat-transfer fluid, the assembly of one or more valves comprises a three-way valve, the ports of which are connected respectively to an outlet of the first heat exchanger, to an inlet of the second heat exchanger, and to the second end of the withdrawal line via a portion of the withdrawal circuit forming a bypass of the third heat exchanger, the portion of the withdrawal circuit forming a bypass of the third heat exchanger comprises a flow rate limiting member, such as a calibrated orifice, the device moreover comprises a system for pressurizing the tank, comprising a pressurization line separate from the withdrawal circuit and comprising two ends connected respectively to the upper part and the lower part of the inner jacket, a so vaporization heat exchanger and an assembly of one

or more valves that is configured to allow liquid to be withdrawn from the tank, to be heated in the vaporization heat exchanger and to be reintroduced into the tank, the first heat exchanger, the third heat exchanger and the vaporization heat exchanger are housed in the same exchanger housing, the device has an electronic controller configured to control all or some of the assembly of one or more valves of the device, the device comprises a fuel cell or a motor connected at the second, downstream end.

- (15) The invention also relates to a vehicle, in particular a boat, comprising a device according to any one of the features mentioned above or below.
- (16) The invention also relates to a method for supplying fluid to a user member, by means of such a device or such a vehicle, wherein the user member is connected to the second end of the withdrawal circuit, the method comprising a step of supplying fluid from the tank to the user member by withdrawing liquefied fluid from the tank via the first withdrawal line, wherein, prior to the fluid supplying step, if the pressure within the tank is less than a determined threshold, the method comprises a step of pressurizing the tank via the system for pressurizing the tank up to a determined pressure level.
- (17) The invention may also relate to any alternative device or method comprising any combination of the features above or below within the scope of the claims.

Description

BRIEF DESCRIPTION OF THE FIGURES

- (1) Further particular features and advantages will become apparent upon reading the following description, which is given with reference to the figures, in which:
- (2) FIG. **1** is a schematic and partial view illustrating the structure and the operation of a first exemplary embodiment of the invention,
- (3) FIG. **2** is a schematic and partial view illustrating the structure and the operation of a second exemplary embodiment of the invention,
- (4) FIG. **3** is a schematic and partial, perspective cross-sectional view of an example of such a device, illustrating the arrangement of a heat exchanger housing in the tank,
- (5) FIG. **4** is a schematic and partial, perspective side view of an example of a heat exchanger housing.

DETAILED DESCRIPTION OF THE INVENTION

- (6) The fluid supply and storage device **1** illustrated may be a device which is on board a vehicle (boat or other vehicle) for storing hydrogen and supplying it to a user member, such as a fuel cell or a motor, for example.
- (7) The device **1** comprises a cryogenic tank **2** for storing liquefied fluid of the double-wall and vacuum-insulated type comprising an inner jacket **22** delimiting the fluid storage volume and an outer jacket **32** disposed around the inner jacket **22** with a vacuum thermal insulation gap **42** between the two jackets.
- (8) The device **1** has a withdrawal circuit comprising a withdrawal line **3** provided with a first, upstream end **13** connected to the inner jacket **22** (and preferably at the upper part) and a second, downstream end **23** intended to be connected to a user member.
- (9) The withdrawal line **3** comprises a first heating heat exchanger **4** located outside the inner jacket **22** and a second heating heat exchanger **5** located inside the inner jacket **22**.
- (10) The withdrawal circuit moreover comprises an assembly of one or more valves **6** that is configured to ensure the passage of a flow of fluid circulating from the first end **13** to the second end **23**, in the process entering the first heat exchanger **4** and then the second heat exchanger **5** or in the process entering solely the first heat exchanger **4**.
- (11) That is to say that the withdrawal circuit has a line in which the first heat exchanger 4 and the

- second heat exchanger **5** are disposed in series between the first end **13** and the second end **23** and a bypass portion **75** connecting the outlet of the first heat exchanger **4** to the second end **23** without passing through the second heat exchanger **5**.
- (12) The assembly of one or more valves **6** comprises for example a three-way valve, the ports of which are connected respectively to an outlet of the first heat exchanger **4**, to an inlet of the second heat exchanger **5**, and to the second end **23** via a bypass portion **75** bypassing the second heat exchanger **5**.
- (13) This portion **75** of the withdrawal circuit preferably comprises a flow rate limiting member **70**, such as a calibrated orifice or a valve, for example.
- (14) The three-way valve **6** may be of the proportional type (with, for example, some of the flow of fluid being directed to the second heat exchanger **5**). Of course, any other type of valve(s) can be envisaged to ensure the routing or the distribution of the flows of fluid.
- (15) The inlet of the first exchanger **4** (the inlet receiving the flow of fluid coming from the first end **13** of the withdrawal line **3**) is located in the vacuum thermal insulation gap **42** between the two jackets.
- (16) This makes it possible to localize the cold interfaces in the vacuum-insulated space.
- (17) Advantageously, at least a part of the first heat exchanger **4** which is adjacent to the inlet **40** receiving the flow of fluid coming from the first end **13** of the withdrawal line **3** is located in the vacuum thermal insulation gap **42**. For example, a volume may be provided for this purpose at one end (for example longitudinal end) of the tank (which can be a vertical or horizontal tank).
- (18) As shown, the entirety of the first heat exchanger **4** may be housed in this inter-wall space **42**.
- (19) For example, this first heat exchanger **4** may be housed in a sealed exchanger housing **15**, at least one portion of which is located in the vacuum thermal insulation gap **42** between the two jackets.
- (20) The housing **15** may thus comprise a first inlet **40** receiving the flow of fluid coming from the first end **13** of the circuit. This first inlet **40** may be located at a terminal end of the housing **15** located in the vacuum thermal insulation gap **42** between the two jackets.
- (21) As illustrated, this housing **15** may also accommodate a part of the withdrawal circuit connecting the second heat exchanger **5** to the second end **23**. To that end, the housing **15** may have a second inlet **50** receiving the flow of fluid coming from the second heat exchanger **5**.
- (22) This second inlet **50** may be located adjacently to the first inlet **40**, in the vacuum thermal insulation gap **42** between the two jackets.
- (23) The withdrawal circuit may have a third heat exchanger **12** disposed in series downstream of the second heat exchanger **5** such that the third heat exchanger **12** receives the flow that has passed into the second heat exchanger **5**.
- (24) This third heat exchanger **12** is located outside the vacuum thermal insulation gap **42** between the two jackets and in particular at least partially outside the outer jacket **32**.
- (25) As illustrated, this third heat exchanger **12** may also be housed in the housing **15**. Of course, it could be disposed outside the housing and in particular further downstream of the latter.
- (26) In the example shown, the first heat exchanger **4** and the third heat exchanger **12** are housed in one and the same exchanger housing **15** which may be in a heat-exchange relationship with at least one flow **14** of heat-transfer fluid.
- (27) This housing **15** may be a heat exchanger of the multichannel plate type (different channels for the different exchangers described above).
- (28) As illustrated, the device **1** preferably moreover comprises a system for pressurizing the tank **2**, having a pressurization line **8** separate from the withdrawal circuit and comprising two ends respectively connected to the upper part and the lower part of the inner jacket **22**. A vaporization heat exchanger **9** and an assembly of one or more valves **10**, **11** are provided for this line **8** and are configured to allow liquid to be withdrawn from the tank **2**, to be heated in the vaporization heat exchanger **9** and to be reintroduced into the tank **2**. For example, two valves **10**, **11** are disposed on

- either side of the vaporization heat exchanger **9**.
- (29) Thus, this auxiliary pressurization system allows the initial pressurization of the tank and in particular the starting up of a fuel cell **123** connected to the second end **23**.
- (30) This pressurization without using the withdrawal circuit allows initial pressurization, in particular when the necessary pressure is greater than the filling pressure, without consuming fluid.
- (31) In the embodiment of [FIG. 1], the vaporization heat exchangee **9** is located outside the housing **15** mentioned, whereas in the embodiment of [FIG. 2] the third heat exchanger **12** and the vaporization heat exchanger **9** are housed in the same exchanger housing **15**.
- (32) As illustrated, this housing **15** may be integral with a mounting plate **19** which may be fixed to the outer face of the outer jacket **32**. In the mounted position, this housing **15** may thus pass through the outer jacket **32** in a sealed manner (cold inlets **40**, **50** for fluid in the vacuum-insulated cold part and hot outlets **140**, **150** on the outside of the tank).
- (33) A control and/or safety valve **17** is preferably provided downstream of the third heat exchanger **12** at the second end **23** (upstream of the user member **123**). A temperature and/or pressure sensor may also be provided at the outlet of this heat exchanger **12** (similarly at the first end **13** of the withdrawal circuit).
- (34) Thus, the assembly of one or more valves **6** makes it possible to withdraw gas from the tank **2**, which is circulated in the first heat exchanger **4** then in the second heat exchanger **5** and subsequently in the third heat exchanger **12** before the second end **23**. As an alternative, the assembly of one or more valves **6** makes it possible to withdraw gas from the tank **2**, which is circulated solely in the first heat exchanger **4** before arriving at the second end **23**.
- (35) As indicated above, a flow rate regulating and/or limiting member **70** is preferably provided in the withdrawal line **3** downstream of the assembly of one or more valves **6** and the second, downstream end **23**, in the bypass portion bypassing the third heat exchanger **12**.
- (36) This member **70** makes it possible to compensate for the pressure drops in the second heat exchanger **5** in particular.
- (37) As illustrated, preferably, a safety device **18** with a pressure relief valve is provided at the first end **13** so as to vent possible excess pressures from the tank **2**.
- (38) A possible mode of operation of the device for supplying fluid to a user member **123** will now be described.
- (39) When the pressure in the tank **2** (in the inner jacket **22**) is less than a determined threshold, the three-way valve **6** can be configured to transfer the fluid withdrawn from the tank **2** (and heated in the first heat exchanger **4**) into the second heat exchanger **5** (in order to supply heat energy in the tank **2** and therefore increase its pressure). This fluid is then reheated in the third heat exchanger **12** before being supplied to the user member **123**.
- (40) When the pressure in the tank is greater than a determined level, the three-way valve **6** can be configured to transfer the fluid withdrawn from the tank **2** (and heated in the first heat exchanger **4**), without it passing through the second heat exchanger located in the tank **2**, towards the user **123** (preferably via a flow rate limiting member **70**).
- (41) In this mode, the liquid and gas phases can be kept in thermodynamic equilibrium. Thus, in steady-state operation, the withdrawn gas in the tank 2 comes from the evaporation of liquid caused by the second heat exchanger 5. Since this gas has bubbled through the liquid present in the tank, it is in thermodynamic equilibrium with the liquid. The pressure in the tank 2 is therefore set by the temperature of the liquid and of the gas. This mode of operation therefore makes it possible to have a tank 2 in which the liquid is in thermal equilibrium with the gas. In this case, if the tank is shaken, the mixture of the liquid and gas phase does not affect the pressure since they are at the same temperature.
- (42) As illustrated, an electronic controller **16** (comprising a microprocessor and/or a computer) may be provided and configured to control all or some of the assembly of one or more valves of the device.

- (43) This withdrawal at the gaseous portion is more advantageous than a liquid withdrawal since it allows better renewal of the gas phase. Moreover, it limits the thermal gradient of this phase, and consequently minimizes the deviation from the equilibrium between the liquid and the vapours of the phases.
- (44) The device therefore makes it possible to control the pressure in the tank **2** with a gaseous withdrawal and a loop for internal recirculation in the liquid phase, if appropriate. The device can be movable and in particular can be subject to rotations with respect to three axes (Oxyz) which are greater than five degrees ° and accelerations along these axes which are greater than 0.5 g (which can result in liquid/gas mixtures, potentially giving rise to pressure instabilities in the devices of the prior art).
- (45) The device may be on board a boat, aircraft, truck at a fixed station or in the "full for empty" mode of use.
- (46) The device **1** advantageously has an auxiliary pressurization heater **9** for the initial pressurization of the tank and the starting up of the cell without withdrawal of fluid (before the mode of operation of permanent withdrawal described above).
- (47) Thus, the tank **2** is pressurized by the pressurization system separately from the withdrawal circuit preferably solely to ensure the starting up.
- (48) While the invention has been described in conjunction with specific embodiments thereof, it is evident that many alternatives, modifications, and variations will be apparent to those skilled in the art in light of the foregoing description. Accordingly, it is intended to embrace all such alternatives, modifications, and variations as fall within the spirit and broad scope of the appended claims. The present invention may suitably comprise, consist or consist essentially of the elements disclosed and may be practiced in the absence of an element not disclosed. Furthermore, if there is language referring to order, such as first and second, it should be understood in an exemplary sense and not in a limiting sense. For example, it can be recognized by those skilled in the art that certain steps can be combined into a single step.
- (49) The singular forms "a", "an" and "the" include plural referents, unless the context clearly dictates otherwise.
- (50) "Comprising" in a claim is an open transitional term which means the subsequently identified claim elements are a nonexclusive listing i.e. anything else may be additionally included and remain within the scope of "comprising." "Comprising" is defined herein as necessarily encompassing the more limited transitional terms "consisting essentially of" and "consisting of"; "comprising" may therefore be replaced by "consisting essentially of" or "consisting of" and remain within the expressly defined scope of "comprising".
- (51) "Providing" in a claim is defined to mean furnishing, supplying, making available, or preparing something. The step may be performed by any actor in the absence of express language in the claim to the contrary.
- (52) Optional or optionally means that the subsequently described event or circumstances may or may not occur. The description includes instances where the event or circumstance occurs and instances where it does not occur.
- (53) Ranges may be expressed herein as from about one particular value, and/or to about another particular value. When such a range is expressed, it is to be understood that another embodiment is from the one particular value and/or to the other particular value, along with all combinations within said range.
- (54) All references identified herein are each hereby incorporated by reference into this application in their entireties, as well as for the specific information for which each is cited.

Claims

- 1. A fluid supply and storage device, comprising: a cryogenic tank configured to store liquefied fluid of a double-wall and vacuum-insulated type comprising an inner jacket delimiting a storage volume of the liquefied fluid and an outer jacket disposed around said inner jacket with a vacuum thermal insulation gap between said inner and outer jackets; and a withdrawal circuit comprising an assembly of one or more valves and a withdrawal line that comprises a first, upstream end connected to an upper part of said inner jacket and a second, downstream end configured to connect to a user member, said withdrawal line comprising a first heat exchanger located outside said inner jacket and a second heat exchanger located inside said inner jacket: a bypass line that fluidly connects the assembly of one or more valves with the second, downstream end, wherein: said assembly of one or more valves is configured to ensure passage of a flow of fluid circulating from said first, upstream end to said second, downstream end by switching between a first flow path in which the flow of fluid enters said first heat exchanger and then the flow of fluid enters said second heat exchanger and a second flow path in which the flow of fluid enters said first heat exchanger and the bypass line without entering said second heat exchanger; and an inlet of said first heat exchanger receiving the flow of fluid coming from said first, upstream end is located in said vacuum thermal insulation gap.
- 2. The device of claim 1, wherein at least a part of said first heat exchanger which is adjacent to said first heat exchanger inlet is located in said vacuum thermal insulation gap.
- 3. The device of claim 1, wherein said first heat exchanger is housed in an exchanger housing and at least one portion of said exchanger housing is located in said vacuum thermal insulation gap.
- 4. The device of claim 3, wherein said exchanger housing comprises a first inlet that receives the flow of fluid coming from said first, upstream end, said exchanger housing first inlet being located in said vacuum thermal insulation gap.
- 5. The device of claim 3, wherein said xchanger housing accommodates a part of said withdrawal circuit connecting said second heat exchanger to said second, downstream end, said exchanger housing further comprising a second inlet receiving the flow of fluid coming from said second exchanger, said exchanger housing second inlet being located in said vacuum thermal insulation gap.
- 6. The device of claim 1, wherein said withdrawal circuit further comprises a third heat exchanger disposed in series with, and downstream of, said second heat exchanger such that said third heat exchanger receives the flow of fluid that has passed into said second heat exchanger.
- 7. The device of claim 6, wherein said third heat exchanger is located outside said vacuum thermal insulation gap.
- 8. The device of claim 6, wherein said first heat exchanger and said third heat exchanger are housed in one and a same exchanger housing in a heat-exchange relationship with at least one flow of heat-transfer fluid.
- 9. The device of claim 6, wherein said assembly comprises a three-way valve, ports of said three-way valve being connected, respectively, to an outlet of said first heat exchanger, to an inlet of said second heat exchanger, and to said second, downstream end via a portion of said withdrawal circuit forming a bypass of said third heat exchanger.
- 10. The device of claim 9, wherein said portion of said withdrawal circuit forming a bypass of the third heat exchanger comprises a flow rate limiting calibrated orifice.
- 11. The device of claim 1, wherein said device further comprises a tank pressurization system for pressurizing said cryogenic tank, said tank pressurization system comprising a pressurization line separate from said withdrawal circuit that comprises: two ends connected, respectively, to said upper part of said inner jacket and a lower part of said inner jacket; a vaporization heat exchanger; and an assembly of one or more valves that is configured to allow liquid to be withdrawn from said cryogenic tank, to allow the withdrawn liquid to be heated in said vaporization heat exchanger, and to allow the heated withdrawn liquid be reintroduced into said cryogenic tank.

- 12. The device of claim 11, wherein said first heat exchanger, said third heat exchanger, and said vaporization heat exchanger are housed in a same exchanger housing.
- 13. The device of claim 1, further comprising an electronic controller configured to control all or some of said assembly of one or more valves.
- 14. The device of claim 1. wherein the, user member is fluidly connected with the second, downstream end, wherein the user member comprises a fuel cell or a motor connected said second, downstream end.
- 15. The device of claim 1, wherein said device is an on-board device for storing hydrogen and supplying it to a user member.
- 16. A vehicle that includes said device of claim 1.
- 17. The vehicle of claim 16, wherein said vehicle is a boat.
- 18. A method for supplying fluid to the user member using said device of claim 11, wherein the user member is connected to said second, downstream end, said method comprising the steps of: supplying fluid from said tank to said user member by withdrawing liquefied fluid from said tank via said withdrawal line; and prior to said step of supplying fluid, when a pressure within said tank is less than a determined threshold, pressurizing said tank via said device of claim 11 up to a determined pressure level.