

Unit-III

Some Two & Three Dimensional Flows

3.1) Some flows involving Axial Symmetry:

Consider a steady irrotational flow of an incompressible fluid described by scalar velocity potential $\phi = \phi(r, \theta, \psi)$ in spherical polar coordinates.

Eqn of motion is $\nabla^2 \phi = 0$

Then it becomes

$$\frac{1}{r^2} \left(\frac{\partial}{\partial r} \left(r^2 \frac{\partial \phi}{\partial r} \right) + \frac{1}{r^2 \sin \theta} \frac{\partial}{\partial \theta} \left(\sin \theta \frac{\partial \phi}{\partial \theta} \right) + \frac{1}{r^2 \sin \theta} \left(\frac{\partial^2 \phi}{\partial \psi^2} \right) \right) = 0$$

Multiply by $r^2 \sin \theta$,

$$\Rightarrow \sin \theta \left(\frac{\partial}{\partial r} \left(r^2 \frac{\partial \phi}{\partial r} \right) \right) + \frac{\partial}{\partial \theta} \left(\sin \theta \frac{\partial \phi}{\partial \theta} \right) + \frac{1}{\sin \theta} \left(\frac{\partial^2 \phi}{\partial \psi^2} \right) = 0$$

When there is symmetry about the line $\theta=0$ (at $\theta=0$ rotation takes place and no change take place)

$$\phi : \phi(r, \theta, \psi) = \phi(r, \theta)$$

$$\Rightarrow \sin \theta \left(\frac{\partial}{\partial r} \left(r^2 \frac{\partial \phi}{\partial r} \right) \right) + \frac{\partial}{\partial \theta} \left(\sin \theta \frac{\partial \phi}{\partial \theta} \right) = 0$$

(Special) P. solution : $\phi = r \cos \theta$, $\phi = \frac{1}{r^2} \cos \theta$

General soln : $\phi(r, \theta) = \left(A r + \frac{B}{r^2} \right) \cos \theta$

On Irrotational

WS

Symmetry:

Unit - III

flow
by

p)

$$\left(\frac{\partial^2 \phi}{\partial y^2} \right) = 0$$

3.1) Some flows involving Axial Symmetry

- * Irrotational stationary sphere in a uniform stream.
- * Sphere moving with constant velocity in liquid which is otherwise at rest.
- * Accelerating sphere moving in fluid at rest at infinity.
- * Underwater explosion giving spherical gas bubbles.

3.2) Sources, Sinks & Doublets.

- * Doublet in a uniform stream
- * S. A. Abir Problem
- * Illustration of line distributions

3.3) Axi-Symmetric flows; Stoke's Stream Function

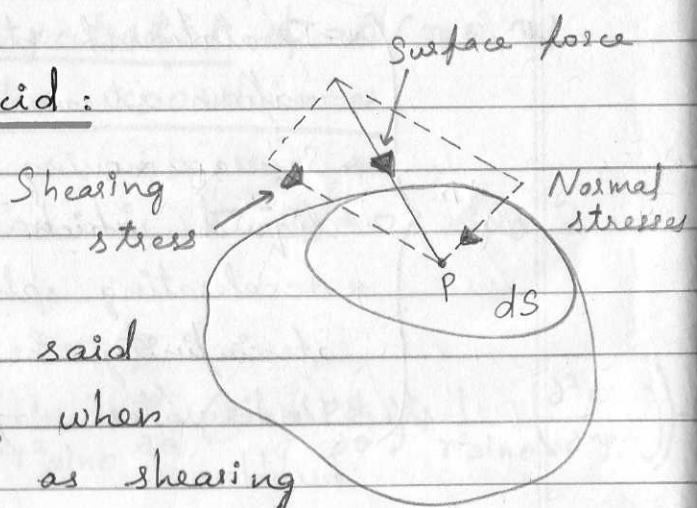
- Some Special Forms of the stream for Axi-Symmetric Irrotational Motions

+ 2 eq in pg. 156

3.4) Meaning of two-Dimensional flows.

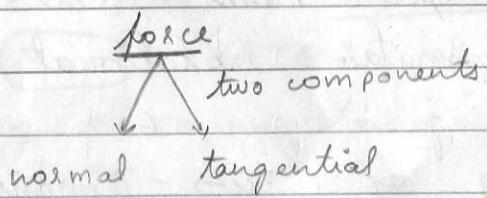
8m Discuss
Problem of a sphere moving with constant velocity in liquid which is otherwise at rest.

Viscous & Inviscid:



* A fluid is said to be viscous when normal as well as shearing stresses exist.

* A fluid is said to be inviscid when it does not exert any shearing stress, whether at rest or in motion.



normal stress } - normal force per unit area
(or pressure)

Shearing stress - tangential force per unit area

Viscosity - resistance to flow

water / air \neq syrup / heavy oil

Rotational & Irrotational :

* The motion of a fluid is said to be irrotational when the vorticity vector of every fluid is zero.

* When the vorticity vector is different from zero, the motion is said to be rotational.

rotational - fluid particles go on rotating about their own axes, while flowing

irrotational - do not rotate about their own axes, while flowing.

Uniform flows - fluid particles possess equal velocity at each section of the channel or pipe

non-uniform flows → possess different velocities

Steady - flow pattern remains unchanged with the time

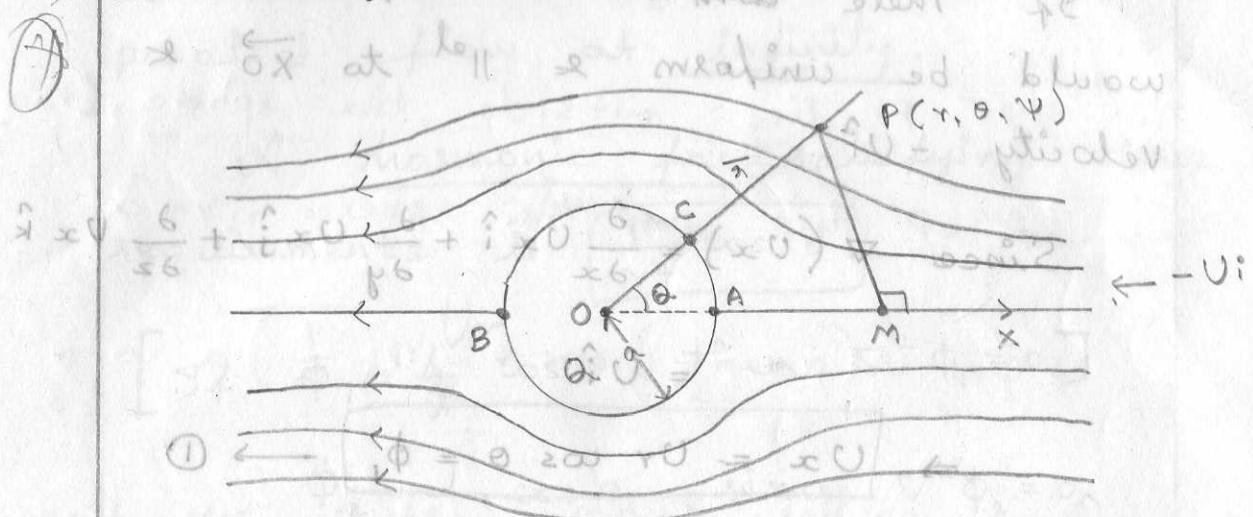
Unsteady - flow pattern varies with time

UNIT - III

$\theta = 0$ will get (115) for Pg.

$$\theta = 0 \quad x = \infty$$

① Stationary Sphere in Uniform Stream:



view at sub horizontal plane (si)

Suppose a solid stationary sphere of radius 'a' is placed in an uniform stream of incompressible fluid flowing with an undisturbed velocity $-U_i$ where U is a constant and i is in the x -increasing axis direction \vec{Ox} , taken to be the axis of symmetry.

Let P be an arbitrary point in the flow described by spherical polar coordinates such that

$$P : P(r, \theta, \psi)$$

Let PM be the perpendicular from P on Ox such that $OM = x$, $\vec{OM} = \vec{x}$, \vec{OX} .

i.e.) i is taken to be the line of symmetry.

i.e.) the line $\theta = 0$.

$$\therefore x = r \cos \theta$$

If there were no sphere, the flow would be uniform & \parallel to $\vec{x_0}$ & velocity $-U\hat{i}$.

$$\text{Since } \nabla (U_x) = \frac{\partial}{\partial x} U_x \hat{i} + \frac{\partial}{\partial y} U_x \hat{j} + \frac{\partial}{\partial z} U_x \hat{k}$$

$$= U\hat{i}$$

$$\Rightarrow U_x = U_r \cos \theta = \phi_i \rightarrow ①$$

i.e.) Velocity potential due to uniform

~~force.~~ provides info. to suggest

When a sphere is inserted, it will produce a local perturbation of the stream.

Stream lines will be disposed

around the sphere as shown in the fig.

Hence undisturbed potential $U_r \cos \theta$

has to be modified by a 'perturbation potential'

which is called due to the presence

of the flow-sphere.

The perturbation must have the following properties:

- i) It must satisfy Laplace eqn for the case of axial symmetry.

ii) It must tend to 0 at large distance ~~off~~ from the sphere so as to recover the condition of uniform parallel flow at infinity.

A harmonic fn satisfying these requirements is $\frac{1}{r^2} \cos \theta$.

$$[\text{If } \phi_1 = \frac{1}{r^2} \cos \theta, \text{ then } \nabla^2 \phi_1 = 0]$$

$$\phi_2 = \frac{1}{r^2} \cos \theta, \text{ since } \nabla^2 \phi_2 = 0$$

Since at the point 'P' in the fluid, when the sphere is inserted in the stream as shown in the fig. the

~~velocity potential~~ field will be

$$\text{Velocity potential, } \phi = \phi_1 + A\phi_2$$

$$V_r \text{ at } r=0 = U \cos \theta + \frac{A}{r^2} \cos \theta \quad \hookrightarrow \text{I}$$

where A determined (from) the constraint that there is no flow normal to the surface at $r=a$.

$$\text{i.e.) } \left[\frac{\partial \phi}{\partial r} \right]_{r=a} = 0$$

$$\frac{\partial}{\partial r} \left[U \cos \theta + \frac{A}{r^2} \cos \theta \right] = - \frac{2A}{r^3} \cos \theta + U \cos \theta = 0$$

$$\text{or } \Rightarrow A = \frac{U a^3}{2} \quad \begin{matrix} \text{to} \\ \text{cancel} \end{matrix} \quad \Rightarrow \left(-\frac{2A}{r^3} + U \right) \cos \theta = 0$$

$$\Rightarrow -\frac{2A}{a^3} + U = 0$$

$$\Phi = Ur \cos \theta + \frac{A}{r^2} \cos \theta \rightarrow \textcircled{I}$$

(I) becomes $\Rightarrow \Phi = Ur \cos \theta + \frac{1}{r^2} \frac{Ua^3}{2} \cos \theta$

$$\Phi = Ur \left(r + \frac{a^3}{2r^2} \right) \cos \theta$$

If P lies outside the sphere, $r > a$

If P lies on the sphere, $r = a$

$$\Phi = U \left(a + \frac{a^3}{2a^3} \right) \cos \theta = U \left(\frac{3}{2} \right) a \cos \theta$$

From earlier known result we have

if S is the boundary of the spherical surface lying wholly within the fluid & the spherical surface is of radius 'a' lying in the fluid in motion, with mean value of velocity potential ϕ on S given by

$$\Phi = \left(\frac{M}{a} \right) = c$$

where 'a' be radius, M & c are constant.

Under the condition that fluid extend to ∞ , and is at rest there.

At any point $P(\phi_p)$ the velocity potential at P tends to c as P tends to ∞ . i.e.) $\phi_p \rightarrow c$ as $P \rightarrow \infty$

Suppose there are more similar surfaces S_n then the kinetic energy of the moving fluid is given by

$$T = \frac{1}{2} \rho \int \vec{v}^2 dv$$

$$= \sum_{n=1}^k \int_{S_n} \phi \frac{\partial \phi}{\partial n} ds$$

Thus, ϕ or $\frac{\partial \phi}{\partial n}$ is prescribed on each surface S_n enclosing a volume V , then ϕ is determined uniquely throughout the volume V within arbitrary constant.

This problem can be extended to fluid in uniform motion at ∞ and $\frac{\partial \phi}{\partial n}$ is prescribed on each of the surface S_n , then ϕ is determined uniquely throughout V .

$$(We) have \phi_1 = Ur \cos \theta \rightarrow ①$$

$$\phi_2 = \frac{1}{r^2} \cos \theta \rightarrow ②$$

$$\phi = \phi_1 + A \phi_2 \rightarrow ③$$

$$\text{at } r=a, \frac{\partial \phi}{\partial r} = 0 \Rightarrow A = \frac{Ua^3}{2}$$

$$\phi = \begin{cases} U \cos \theta \left(r + \frac{a^3}{2r^2}\right), & r > a \\ a U \cos \theta \left(\frac{3}{2}\right), & r = a \end{cases} \rightarrow ④$$

Suppose \vec{q} denote the velocity of fluid at P , then

$$\begin{aligned}\vec{q} \Big|_P &= -\nabla \phi = -\frac{\partial \phi}{\partial r} \hat{e}_r \\ &= -\left(1 \cdot \frac{\partial \phi}{\partial r} \hat{e}_r + \frac{1}{r} \frac{\partial \phi}{\partial \theta} \hat{e}_\theta + \frac{1}{r \sin \theta} \frac{\partial \phi}{\partial \psi} \hat{e}_\psi\right) \\ &= q_r \hat{e}_r + q_\theta \hat{e}_\theta + q_\psi \hat{e}_\psi\end{aligned}$$

$\therefore q_r = -\frac{\partial \phi}{\partial r} = \begin{cases} -U \cos \theta \left(1 - \frac{2a^3}{2r^3}\right), & r > a \\ 0, & r = a \end{cases}$

$q_\theta = -\frac{1}{r} \frac{\partial \phi}{\partial \theta} = \begin{cases} -U \sin \theta \left(1 + \frac{a^3}{2r^3}\right), & r > a \\ 0, & r = a \end{cases}$

$q_\psi = -\frac{1}{r \sin \theta} \frac{\partial \phi}{\partial \psi} = 0$

$\therefore \vec{q} = q_r \hat{e}_r + q_\theta \hat{e}_\theta + q_\psi \hat{e}_\psi \text{ in } \phi \text{ net}$

$$\begin{aligned}&\stackrel{(1)}{=} \begin{cases} -U \cos \theta \left(1 - \frac{a^3}{r^3}\right) \hat{e}_r - U \sin \theta \left(1 + \frac{a^3}{2r^3}\right) \hat{e}_\theta, & r > a \\ \frac{3}{2} a U \sin \theta \hat{e}_\theta, & r = a \end{cases} \\ &\stackrel{(2)}{\leftarrow} \phi A +, \phi = \phi \quad \hookrightarrow (5)\end{aligned}$$

The stagnation pt in the fluid flow are those pt at which $\vec{q} = 0$

$$\begin{aligned}&\stackrel{(1)}{\leftarrow} \phi A +, \phi = \phi \\ &\quad \left. \begin{aligned} r < a &: \left(\frac{a^3}{r^3} + 1\right) \phi = 0 \\ r = a &: \left(\frac{3}{2} a^2 \sin \theta\right) \phi = 0 \end{aligned} \right\} \end{aligned}$$

From (5) we have, $\vec{A} \times \vec{p} = 0$

ie. $q_r = 0 = q_{\theta}$ at the free surface.

$$\Rightarrow \left\{ \begin{array}{l} U \cos \theta \left(1 - \frac{a^3}{r^3} \right) = U \sin \theta \left(1 + \frac{1}{2} \frac{a^3}{r^3} \right) = 0, r > a \\ 0 = \frac{3}{2} U a \sin \theta = 0, r = a \end{array} \right.$$

$$\cos \theta - \sin \theta - \cos \theta \frac{a^3}{r^3} - \frac{\sin \theta}{2} \frac{a^3}{r^3} = 0, r > a$$

$$(t) \cos \theta - \sin \theta - \frac{a^3}{r^3} \left(\cos \theta - \frac{\sin \theta}{2} \right) \neq 0, r > a$$

At $\theta = 0$,

$$1 - \frac{a^3}{r^3} \neq 0, r > a$$

From the above argument we infer that only for $r=a$ & $\sin \theta = 0$ we have $\vec{q} = 0$.

i.e.) Stagnation pt in the fluid occur when $r=a, \theta=0$ which correspond to A & B, shown in the fig.

Let p_0 denote the stagnation pressure at A and p_∞ denote the pressure at infinity.

We note that, at A when the stagnation pressure is p_0 , $\vec{q} = 0$ and at ∞ , when pressure is p_∞ , the velocity $\vec{q} = -U\hat{i}$

Along \vec{XA} , the flow of the fluid, we will be able to write

Bernoulli's eqn

$$\frac{1}{2} \vec{q}^2 + \sigma + \frac{P}{\rho g} = \text{constant}$$

where σ is scalar pt fn denoting the body forces

$$\frac{1}{2} \rho \vec{q}^2 + \sigma + p = \text{constant} \rightarrow (f)$$

At ∞ ,

$$\frac{1}{2} \rho (\vec{q}_\infty)^2 + \sigma + p_\infty = \text{constant}$$

At A,

$$\frac{1}{2} \rho (\vec{q}_A)^2 + \sigma + p_\infty = \text{constant}$$

$$\Rightarrow \frac{1}{2} \rho (\vec{q}_A)^2 + \sigma + p_\infty = \frac{1}{2} \rho (\vec{q}_\infty)^2 + \sigma + p_\infty$$

$$\Rightarrow \frac{1}{2} \rho v^2 + p_\infty = p_0 \rightarrow (6)$$

Pressure at any point $c(a, \theta, \psi)$ on the surface of the sphere can be obtained

$$\text{from } (5) : \quad [q_r]_c = 0$$

$$[q_\theta]_c = -v \frac{3}{2} \sin \theta$$

$$[q_\psi]_c = 0$$

Applying Bernoulli's eqn (f) along XAC,

if p_c denote the pressure at C, then

At A,

$$\frac{1}{2} \rho (\vec{q}_o)^2 + p_o + p_c = \text{constant}$$

edge ext no \Rightarrow pos to \rightarrow

At C, $\frac{\pi}{2} = \theta \Rightarrow r = r$ to \rightarrow blow.

$$\frac{1}{2} \rho (\vec{q}_c)^2 + p_o + p_c = \text{constant}$$

At ∞ ,

$$\frac{1}{2} \rho (\vec{q}_\infty)^2 + p_o + p_\infty = \text{constant}$$

$$\text{We know, } \vec{q}_c = \frac{3}{2} U \sin \theta \hat{e}_\theta$$

$$\text{then } \vec{q}_c \cdot \vec{q}_c = \frac{9}{4} U^2 \sin^2 \theta$$

$\Rightarrow \frac{1}{2} \rho \left(\frac{9}{4} U^2 \sin^2 \theta \right) + p_o + p_c = \text{constant}$

$$\frac{1}{2} \rho (\vec{q}_\infty)^2 + p_o + p_\infty = \frac{1}{2} \rho \frac{9}{4} U^2 \sin^2 \theta + p_o + p_c$$

$$\frac{\rho U^2}{2} \left(1 - \frac{9}{4} \sin^2 \theta \right) + p_\infty = p_c \rightarrow ①$$

but $\sin^2 \theta = 1 \Rightarrow \theta = \frac{\pi}{2}$

To find ①, minimum pressure at C is given by

$$\min p_c = p_\infty + \frac{\rho U^2}{2} \left(1 - \frac{9}{4} \right) \left[\because \max \sin^2 \theta = 1 \Leftrightarrow \theta = \frac{\pi}{2} \text{ (or) } \frac{3\pi}{2} \right]$$

$$= p_\infty - \frac{5}{8} \rho U^2 \rightarrow ⑧A$$

$$\text{and } \max p_c = p_\infty + \frac{\rho U^2}{2} (1-\cos\theta) \quad \left[\because \min \sin^2 \theta = 0 \right]$$

$$\Leftrightarrow \theta = 0 \text{ (or) } \pi$$

$$= p_\infty + \frac{\rho U^2}{2} \rightarrow \textcircled{8B}$$

From $\textcircled{8A}$, note that the minimum pressure at any pt c on the sphere would occur at $r=a$ & $\theta = \frac{\pi}{2}$ along the equatorial line & the minimum pressure possible at c is $p_c = 0$ $\Rightarrow \min p_c = p_\infty - \frac{5}{8} \rho U^2$.

$$\Rightarrow p_\infty = \frac{5}{8} \rho U^2 \quad \leftarrow \theta = p_\infty - \frac{5}{8} \rho U^2$$

$$U = \sqrt{\frac{8}{5} \frac{p_\infty}{\rho}}$$

This indicates that when the speed of undisturbed stream is increased a point will be reached at which pressure everywhere along equatorial line $r=a$ and $\theta = \frac{\pi}{2}$ fall to 0.

At this stage, the fluid will tend to break away from the surface of the sphere along equatorial line & cavitation is said to occur.

Unit - II (continuation)

Corollaries - From Kelvin's Theorem

Corollary - I

Suppose S is an open surface with rim Γ ; a closed circuit under the consid condition that it is an inviscid fluid having a closed circuit Γ of fluid particles moving along with the fluid where the body forces are conservative & the p is a single valued fn of density only, then

$$\int_S \vec{n} \cdot \vec{f} ds = \text{constant}$$

$$2b \left[\vec{p} \times \nabla \cdot \vec{f} \right] = 2b \vec{f} \cdot \vec{n}$$

Proof:

$$\vec{f} = \nabla \times \vec{q}$$

Kelvin's theorem states that,

for any inviscid fluid circulation around any closed circuit of fluid particles, moving along with the fluid remains constant provided the body forces are conservative and the pressure is a single valued fn of density only."

$$\Gamma = \oint_C \vec{q} \cdot d\vec{s} = \text{constant} \rightarrow (f)$$

By Stoke's Theorem which states that,

" Suppose S is an open, two sided surface bounded by a closed, non-intersecting curve C .

Suppose \vec{A} is a vector fn of position with continuous derivatives, then

$$\oint_C \vec{A} \cdot d\vec{r} = \iint_S (\nabla \times \vec{A}) \cdot \hat{n} ds = \iint_S (\nabla \times \vec{A}) d\vec{s} \rightarrow (ff)$$

Consider,

$$\int_S \hat{n} \cdot \vec{q} ds = \int_S \hat{n} \cdot \nabla \times \vec{q} ds$$

$$= \oint_C \vec{q} \cdot d\vec{r} \quad [by (ff)]$$

$$= \oint_C \vec{q} \cdot d\vec{r} \quad [\because C \text{ is a closed circle}]$$

$$= \Gamma = \text{constant} \quad [by (f)]$$

$$\text{i.e., } \Gamma = \iint_S \hat{n} \cdot (\nabla \times \vec{q}) ds \rightarrow (fff) \\ = \text{constant}$$

\therefore also $\vec{q} = \text{constant}$

$$(t) \leftarrow \text{constant} = ab \cdot \vec{q} \cdot \phi - 7$$

$$\text{Corollary} \quad \omega = 2b(\vec{p} \times \vec{\nabla}) \cdot \vec{v} = 0$$

Kelvin's Corollary (Suppose for an inviscid fluid, circulation around any closed circuit of the fluid particles moving along the fluid, where the body forces are conservative & pressure is a single valued fn of density only.)

In particular, if we have ϵ to be rim of some open surface S) and further if any portion of the moving fluid once becomes irrotational, then it remains so for all subsequent times.

Proof:

By corollary - 1 which states that

" Suppose S is an open surface with rim ϵ , a closed circuit under the condition that it is a inviscid fluid having a closed circuit ϵ , of fluid particles moving along with the fluid where the body forces are conservative and the pressure is a single valued fn of density only, then

$$\int_S \vec{h} \cdot \vec{t} ds = \text{constant}$$

$$\text{i.e., } \Gamma = \int_S \hat{n} \cdot (\nabla \times \vec{q}) ds = \text{constant} \rightarrow ①$$

Suppose at some instant, the fluid

on ΔS becomes irrotational

$$\text{i.e., } \nabla \times \vec{q} = \vec{0}$$

$$\Rightarrow \vec{f} = \nabla \times \vec{q} = \vec{0}$$

$$\therefore ① \Rightarrow \int_S \hat{n} \cdot \vec{0} ds = 0$$

$$\text{i.e., } \Gamma = \int_S \hat{n} \cdot \vec{f} ds = 0$$

\textcircled{S} is a non-zero infinitesimal

element, say ΔS .

then to the 1st order

$$\Delta S \hat{n} \cdot \vec{f} = 0$$

which forces $\vec{f} = \vec{0}$ as $\Delta S \neq 0$

\Rightarrow that the flow is irrotational

throughout ΔS .

Since $\textcircled{\Delta S}$ is an arbitrary surface

element, the flow is irrotational everywhere on S.

$$(\text{irrotational} = \text{curl } \vec{f} = 0)$$

Corollary - 3

(Suppose for an inviscid fluid, the circulation around any closed circuit Γ of the fluid particles, moving along the fluid, where the body forces are conservative and pressure is a single valued fn of density only), then the vortex lines move along with the fluid.

Proof:

By corollary - 1 which states that

"Suppose S is an open surface with lim Γ , a closed circuit under the condition that it is an inviscid fluid having a closed circuit Γ of fluid particles moving along with the fluid where the body forces are conservative & the pressure is a single valued fn of density only, then $\int_S \vec{n} \cdot \vec{f} ds = \text{constant}$ "

We have,

$$\Gamma = \int_S \vec{n} \cdot \vec{f} ds \rightarrow ①$$

By Kelvin's theorem which states that

"For an inviscid fluid circulation around any closed circuit of fluid particles, moving along with the fluid remains constant provided the body forces are conservative and the pressure is a single valued fn of density only."

We have,

$$\oint \vec{q} \cdot d\vec{s} = \text{constant} \rightarrow ②$$

For the surface S moving along with the fluid,

from ①,

$$\Gamma = \int_S \vec{n} \cdot \vec{q} ds = \text{constant}$$

The integral represents, the total strength of vortex tubes passing through s and by hypothesis, thus

thus we see that vortex tubes move with the fluid.

Alternative Proof:

By taking (S) to be vanishingly small, we infer that, the vortex lines move with the fluid.

To be more specific, let (c) be the closed curve drawn on the surface of the vortex tube containing an area (S) of the tube not embracing the tube.

Then $\vec{n} \cdot \vec{q} = \vec{n} \cdot (\nabla \times \vec{q}) = 0$ at each pt of S .

Using Stokes theorem which states that

"Suppose S is an open, two sided surface bounded by a closed, non-intersecting curve c .

Suppose \vec{A} is a vector fn of position \vec{r} with continuous derivatives, then

$$\oint \vec{A} \cdot d\vec{r} = \iint_S (\nabla \times \vec{A}) \cdot \vec{n} dS = \iint_S (\nabla \times \vec{A}) d\vec{S}$$

We have,

$$\iint_S \vec{n} \cdot \vec{q} dS = \iint_S \vec{q} \cdot d\vec{S} = 0 \rightarrow \textcircled{3} \quad [\text{from } \textcircled{1} \text{ & } \textcircled{2}]$$

By hypothesis, (2) predict p₂
the closed circuit (l) and the
surface (S) are moving with the fluid.

For an irrotational flow, the
circulation around (l) is 0 or S
remains a surface composed of vortex
lines wherein (3) holds. $\int n \cdot \vec{v} ds = \oint \vec{v} \cdot d\vec{r} = 0$

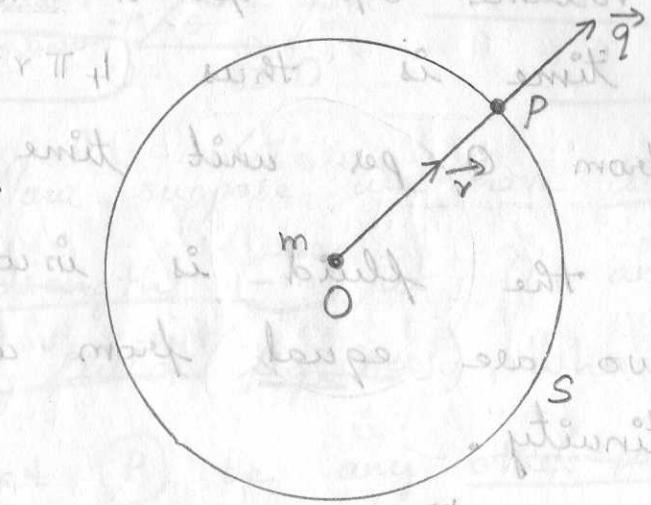
Thus we infer that the vortex
line & vortex tubes move with
the fluid.]

Unit-III (continuation) Some Three-Dimensional Flows

3.2 Sources, Sinks and Doublets:

Suppose at a pt. O in a fluid
the flow is such that it is directed
radially outwards from O in all directions
and in a symmetrical manner. Then
fluid enters the system through O which
is termed as simple source.

and if at O the volume entering per unit time is $4\pi m$, where m is a constant, then the strength of the source is defined to be m .)



(*) If, however, the flow is such that fluid is directed radially inwards to O from all directions in a symmetrical manner, then fluid leaves the system at O which is termed a simple sink. A sink of strength m is a source of strength $-m$.)

Fig (*) shows a simple source of strength m at O in a fluid which is assumed to contain no other sources or sinks and which would otherwise be at rest.

S is the surface of the sphere centre O and radius r and P is a field on S such that $\overrightarrow{OP} = \vec{r}$. Then the fluid

velocity at P is \vec{q} along \vec{OP} and the magnitude q is everywhere constant over S.

The volume of fluid crossing S per unit time is thus $4\pi r^2 q$: that emitted from O per unit time is $4\pi m$.

Since the fluid is incompressible, these two are equal from consideration of continuity.

$$\text{Thus } q = \frac{m}{r^2}, \quad \text{magnitude } \vec{q} = \frac{m}{r^2} \hat{r} \rightarrow \text{①}$$

It is easily shown that $\text{curl } \vec{q} = 0$ (except at $r=0$) so that the flow is of the potential kind.

Let Φ be the velocity potential at P. From considerations of symmetry,

$$\Phi = \Phi(r)$$

$$\text{and } \text{grad } \Phi = \nabla \Phi = \Phi'(r) \hat{r} = \frac{\partial \Phi}{\partial r} \hat{r}$$

$$\text{Thus } \Phi'(r) = -m/r^2,$$

$$\text{and so } \Phi(r) = m/r \rightarrow \text{②}$$

$\text{curl } \vec{q} = \vec{0}$
$\nabla \cdot \vec{q} = 0$
$\nabla \cdot (-\nabla \Phi) = 0$
$\nabla^2 \Phi = 0$

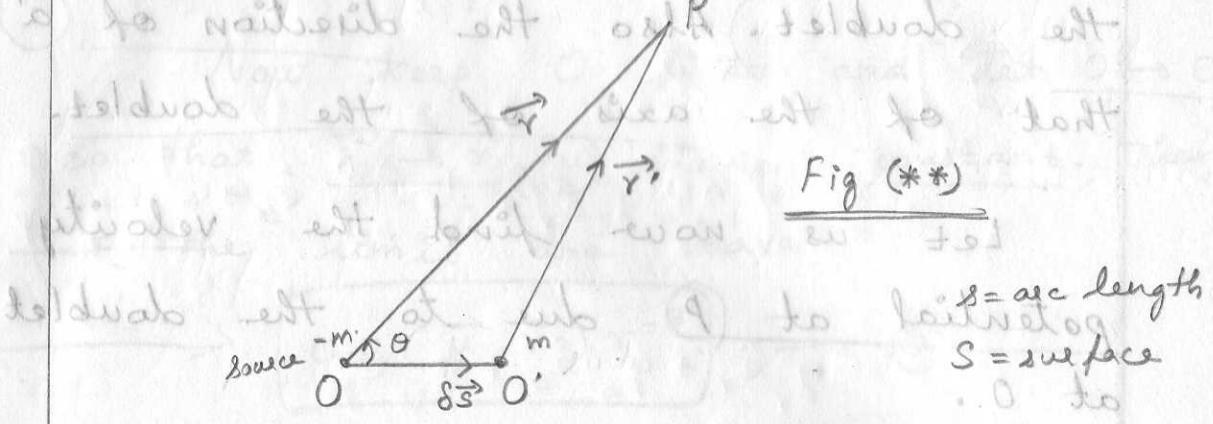


Fig (**)

$s = \text{arc length}$
 $S = \text{surface}$

Now suppose we have simple sources

of strengths $-m$ at O and m at O' in a fluid (fig (**)), where $\overrightarrow{OO'} = 8\vec{s}$.

Let P be any other point in the fluid such that $\overrightarrow{OP} = \vec{r}$, $\overrightarrow{O'P} = \vec{r}'$. In the following we shall use $\vec{r} = |\vec{r}|$, $\vec{r}' = |\vec{r}'|$, $8s = |8\vec{s}|$. Also (let $\mu = m 8s$)

~~doubt~~ Now suppose that $m \rightarrow \infty$, $8s \rightarrow 0$ in such a way that μ remains finite and constant. Then in the limit the two sources $\pm m$, of infinitely great magnitude and coincident at O , are said to constitute a three-dimensional doublet or dipole at O . The quantity μ is

termed the moment (or) strength of the doublet. The quantity $\vec{\mu} = \mu \hat{a}$, whose \hat{a} is the unit vector in the direction $\overrightarrow{OO'}$ is called the vector moment of

2^m

the doublet.) Also the direction of \vec{a}
 that of the axis of the doublet.

Let us now find the velocity potential at P due to the doublet at O .

For the configuration shown, assume the flow to be entirely due to $-m$ at O and m at O' , the velocity potential at P is

$$\phi = \frac{m}{r} - \frac{m}{r'} = \frac{m(x-x')}{xx'} = \frac{m(x-x')}{x^2+x'^2}$$

$$= \frac{m(x-x')}{xx'} \times \frac{(x+x')}{(x+x')}$$

$$= \frac{m(x^2-x'^2)}{xx'(x+x')}$$

$$= \frac{m(\vec{r}-\vec{r}') \cdot (\vec{r}+\vec{r}')} {xx'(x+x')} \quad \left[\because (\vec{r}-\vec{r}').(\vec{r}+\vec{r}') = |\vec{r}|^2 - \vec{r} \cdot \vec{r} + \vec{r} \cdot \vec{r}' - |\vec{r}'|^2 \right]$$

$$= \frac{m\delta\vec{s} \cdot (\vec{r}+\vec{r}')} {xx'(x+x')} \quad \left[\because \text{By vector law addition } \vec{r} = \delta\vec{s} + \vec{x}, \quad \delta\vec{s} = \vec{r} - \vec{x} \right]$$

$$= \frac{\vec{\mu} \cdot (\vec{r}+\vec{r}')} {xx'(x+x')}$$

$$\phi = \frac{\vec{\mu} \cdot (\vec{r} + \vec{r}')}{{\vec{r}}'(\vec{r} + \vec{r}')} = \frac{\vec{\mu} \cdot (\vec{r} + \vec{r})}{\vec{r}(\vec{r} + \vec{r})} = \frac{2\vec{\mu} \cdot \vec{r}}{\vec{r}^2} = \frac{\vec{\mu} \cdot \vec{r}}{r^3}$$

Now keep O fixed and let $O' \rightarrow O$, so that $\vec{r}' \rightarrow \vec{r}$, μ staying constant. Then in the limit we have

$$\phi = (\vec{\mu} \cdot \vec{r}) r^{-3} \rightarrow (3)$$

With $\angle POO' = \theta$, other equivalent forms for ϕ are

$$\begin{aligned} \phi &= (\vec{\mu} \cdot \hat{r}) r^{-2} \\ &= \mu r^{-2} \cos \theta \end{aligned} \rightarrow (3A)$$

The last form shows that $\phi = \phi(r, \theta)$, so that the axis of the doublet is an axis of symmetry as is physically obvious.

Taking P to have spherical polar coordinates (r, θ, ψ) referred to the axis of the doublet as initial line, the velocity potential at P being

$$\phi(r, \theta) = \frac{(\mu \cos \theta)}{r^2},$$

we find the velocity components at P. Let \vec{v} denotes the velocity of the fluid elt at P.

$$[\vec{q}]_P = -\nabla \phi \quad \text{at free wall}$$

$$= -\left(\frac{\partial \phi}{\partial r} \hat{e}_r + \frac{1}{r} \frac{\partial \phi}{\partial \theta} \hat{e}_\theta + \frac{1}{r \sin \theta} \frac{\partial \phi}{\partial \psi} \hat{e}_\psi\right)$$

$$= q_r \hat{e}_r + q_\theta \hat{e}_\theta + q_\psi \hat{e}_\psi$$

\therefore The velocity components at P are

$$q_r = -\frac{\partial \phi}{\partial r} = \frac{-(-2r^{-2-1}\mu \cos \theta)}{r^3} = \frac{2\mu \cos \theta}{r^3}$$

$$q_\theta = -\frac{1}{r} \frac{\partial \phi}{\partial \theta} = -\frac{1}{r} \left(\frac{\mu(-\sin \theta)}{r^2} \right) = \frac{\mu \sin \theta}{r^3}$$

$$q_\psi = \frac{-1}{r \sin \theta} \frac{\partial \phi}{\partial \psi} = \frac{-1}{r \sin \theta} \cdot 0 = 0$$

The eqn of stream lines is

$$\frac{dr}{q_r} = \frac{r d\theta}{q_\theta} = \frac{r \sin \theta d\psi}{q_\psi}$$

$$\Rightarrow \frac{r^3 dr}{2\mu \cos \theta} = \frac{r^4 d\theta}{\mu \sin \theta} = \frac{r \sin \theta d\psi}{0}$$

$$\Rightarrow \psi = \text{constant}$$

$$\Rightarrow \frac{dr}{2 \cos \theta} = \frac{r d\theta}{\sin \theta}$$

wigmax 3

$$\frac{dr}{r} = 2 \cot \theta d\theta$$

$$\log r = 2 \log \sin \theta + \log A$$

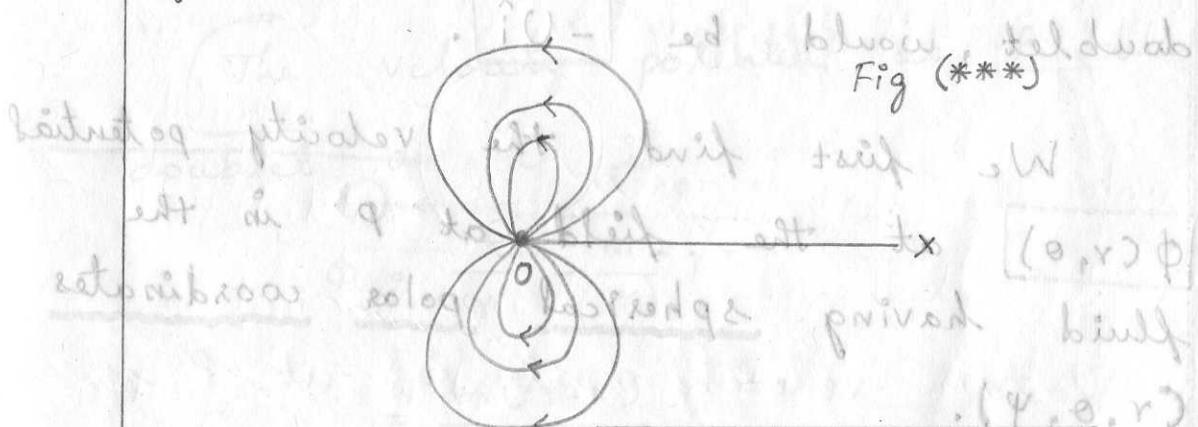
$$\log r = \log (A \sin^2 \theta)$$

$$r = A \sin^2 \theta$$

Thus the streamlines lie in planes passing through the axis of the doublet.

They are symmetrical not only w.r.t. OX but also about the plane $\theta = \frac{1}{2}\pi$.

Fig (****) shows a sketch of them.



The form $\phi(r, \theta) = (\mu \cos \theta)/r^2$ shows

that ϕ , at pts other than O, must satisfy the axially symmetrical spherical polar form of Laplace's eqn.

Examples:

2.1. (i)

Doublet in a uniform stream.

Q. Q. 9 for 2 = $\frac{rb}{r^2 + b^2}$ + 2 deg in Pg. 14

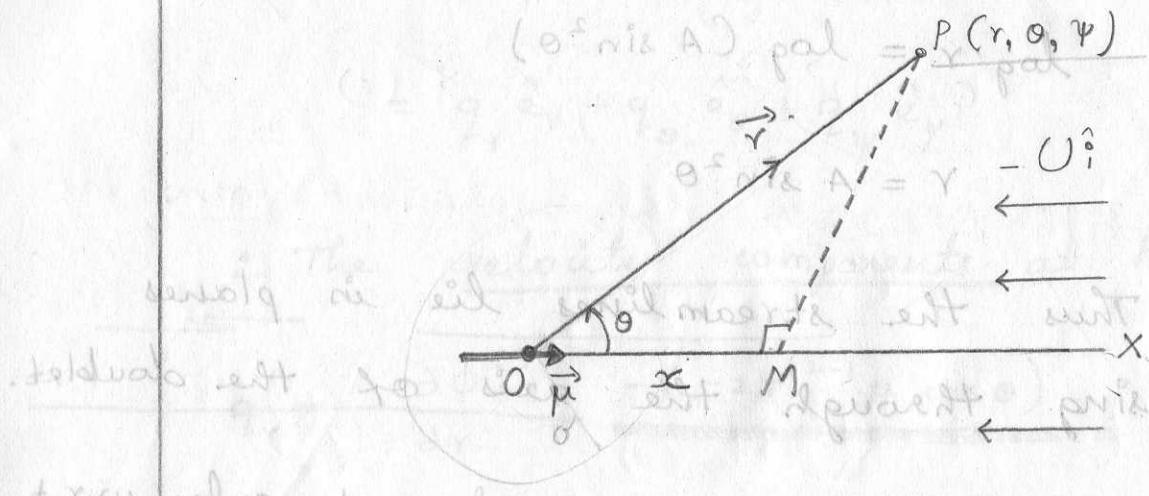


Fig. shows a doublet of vector moment $\bar{\mu} = \mu \hat{i}$ at O in a uniform stream whose velocity, in the absence of the doublet, would be $-U \hat{i}$.

We first find the velocity potential $\phi(r, \theta)$ at the field at P in the fluid having spherical polar coordinates (r, θ, ψ) .

Let $PM = (be)$ the \perp from P on OX

$\Rightarrow OM = x$. i.e., $\theta = 90^\circ$ to, ϕ along the line \overline{OX} places \perp PM to meet OX i.e., \hat{i} is taken to be the line of symmetry.

i.e., the line $\theta = 0$ $\cos \theta = \frac{x}{r}$

$$\therefore x = r \cos \theta$$

If there were no sphere, the flow would be uniform & it'd have to \vec{x}_0 & velocity $-v$.

$$\therefore \nabla (U_x) = \frac{\partial}{\partial x} U_x^i + \frac{\partial}{\partial y} U_x^j + \frac{\partial}{\partial z} U_x^k$$

28m

$$= \overrightarrow{U_i}$$

$$\Rightarrow U_x = U_r \cos \theta - \phi$$

i.e., If PM is the \perp from P on OX
and if $OM = x$, then the velocity potential
at P due to the streamline is

$$U_x = U_A \cos \theta \rightarrow \text{①}$$

The velocity potential at P due to doublet at O is

$$\phi = \frac{m}{\gamma'} - \frac{m}{\gamma}$$

$$= \frac{m(r-r')}{rr'} \text{ pt is also bet } \rightarrow$$

$$\frac{\partial \omega}{\partial r} = \frac{m(r-r')}{r(r+r')} \omega(r+r')$$

$$\textcircled{2} \leftarrow \theta = 2\arctan\left(\frac{-rr' + r_0}{-rr' - r_0}\right) = \frac{-m}{s} \quad s = \sqrt{r^2 + r'^2}$$

$$= \frac{m(r^2 - r'^2)}{rr'(r+r')}$$

to show that $\frac{m(r-r')}{rr'(r+r')}$ is a surjective function.

$$\frac{\vec{r}_1 - \vec{r}_2}{r_1 r_2} = \frac{m(\vec{r} - \vec{r}') \cdot (\vec{r} + \vec{r}')} {r r' (r + r')} \quad \text{--- (P)}$$

Fixed at origin O , $O \rightarrow O' \rightarrow r \rightarrow r'$

$$\Rightarrow \phi = \frac{m \infty s (\hat{r} \cdot \vec{r})}{r^2 (\hat{r} \cdot \vec{r})}$$

$$= \frac{m \infty s \cdot \vec{r}}{r^3}$$

$$= \frac{1}{r^3} (m \infty s \cdot \vec{r})$$

$$= \frac{1}{r^3} (m | \infty s | | \vec{r} | \cos \theta)$$

$$= \frac{1}{r^3} m \infty s \cos \theta$$

$$= \frac{1}{r^2} (\mu \cos \theta)$$

$$= \boxed{\frac{\mu \cos \theta}{r^2}}$$

Total velocity potential at P is

$$\phi(r, \theta) = U_r \cos \theta + \frac{\mu \cos \theta}{r^2}$$

$$= (U_r + \mu r^{-2}) \cos \theta \rightarrow ③$$

Thus the velocity components at P

are

$$\vec{q}_P = -(\nabla \phi) = -\left(\frac{\partial \phi}{\partial r} \hat{e}_r + \frac{1}{r} \frac{\partial \phi}{\partial \theta} \hat{e}_\theta + \frac{1}{r \sin \theta} \frac{\partial \phi}{\partial \phi} \hat{e}_\phi \right)$$

$$[\vec{q}]_P = q_r \hat{e}_r + q_\theta \hat{e}_\theta + q_\psi \hat{e}_\psi$$

$$\Rightarrow q_r = -\frac{\partial \phi}{\partial r}, q_\theta = -\frac{1}{r} \frac{\partial \phi}{\partial \theta}, q_\psi = -\frac{1}{r \sin \theta} \frac{\partial \phi}{\partial \psi}$$

$$q_r = -\left(U - \frac{2\mu}{r^3} \right) \cos \theta$$

$$q_\theta = -\frac{1}{r} (U_r + \mu r^{-2}) (-\sin \theta)$$

$$= \left(\frac{U + \frac{\mu}{r^2}}{r} - U \right) \sin \theta \quad \rightarrow \textcircled{4}$$

$$q_\psi = -\frac{1}{r \sin \theta} (0) = 0$$

From \textcircled{4}, we see that $q_r = 0$ whenever

$$i) \cos \theta = 0 \Rightarrow \theta = \frac{\pi}{2}$$

$$ii) \left(U - \frac{2\mu}{r^3} \right) = 0$$

$$U = \frac{2\mu}{r^3} \quad \theta = \frac{\pi}{2}$$

$$so \frac{2\mu}{r^3} = \frac{2\mu}{U}$$

$$so \frac{r^3}{U} = \left(\frac{2\mu}{U} \right)^{1/3}$$

$$so \frac{r^3}{U} = \left(\frac{2\mu}{U} \right)^{1/3} \text{ meaning that } \mu = \frac{1}{2} U^{2/3}.$$

Then it follows that there is no flow over the surface of the sphere

$$r = a.$$

In fact for $r \geq a$, with $\mu = \frac{1}{2} U a^3$

substituted in (4), we obtain precisely the same velocity potential as was obtained for uniform flow past a stationary sphere of radius a .

$$\text{i.e., } q_r = - \left(U - \frac{\frac{1}{2} U a^3}{r^3} \right) \cos \theta$$

$$= - \left(U - \frac{U a^3}{r^3} \right) \cos \theta$$

$$\text{consequently } q_\theta = - U \cos \theta \left(1 - \frac{a^3}{r^3} \right)$$

$$q_\phi = \left(U + \frac{\frac{1}{2} U a^3}{r^3} \right) \sin \theta \quad (i)$$

$$= U \sin \theta \left(1 + \frac{a^3}{2 r^3} \right) \quad (ii)$$

$$q_\psi = 0$$

Thus, for the region $r \geq a$, the analysis of this sphere problem is the same as that of the dipole of strength $\frac{1}{2} U a^3$ in the uniform stream of velocity $-U$ the axis of the dipole being in the direction

3.3 Axi-Symmetric Flows:

Stokes Stream Function:

Uniform flow past a stationary sphere or a sphere moving with uniform velocity in a fluid at rest are examples of axi-symmetric flows.

Suppose the z -axis be taken as axis of symmetry in an axi-symmetric flow and if P is a point represented in cylindrical polar coordinates system by $P(r, \theta, z)$, then all scalar and vector pt func associated with the flow is independent of θ and [the eqn of continuity for an incompressible fluid flow will be given by,

$$\nabla \cdot \vec{q} = 0 \quad \left[\frac{\psi_6}{r^6} - \frac{1}{r} = 0 \right]$$

where \vec{q} is the velocity at P .

$$\text{i.e. } \vec{q}_6 = q_r \hat{e}_r + q_z \hat{e}_z + 0 \cdot \hat{e}_\theta$$

$$\nabla \cdot \vec{q} = \left[\frac{1}{h_1} \frac{\partial}{\partial r} \left(\frac{h_1}{h_2 h_3} \right) \hat{e}_r + \frac{1}{h_2} \frac{\partial}{\partial \theta} \left(\frac{h_2}{h_1 h_3} \right) \hat{e}_\theta + \frac{1}{h_3} \frac{\partial}{\partial z} \left(\frac{h_3}{h_1 h_2} \right) \hat{e}_z \right] \cdot (q_r \hat{e}_r + q_\theta \hat{e}_\theta + q_z \hat{e}_z)$$

$$= \left(\frac{\partial}{\partial x} q_r + \frac{1}{r} \frac{\partial}{\partial \theta} q_\theta + \frac{\partial}{\partial z} q_z \right) \cdot (q_{r,r}^2 + q_{\theta,\theta}^2 + q_{z,z}^2)$$

$$\vec{q} = -\nabla \phi \Rightarrow \nabla \cdot \vec{q} = \nabla^2 \phi$$

$$\nabla^2 \phi = \frac{1}{h_1 h_2 h_3} \left[\frac{\partial}{\partial x} (h_2 h_3 q_r) + \frac{\partial}{\partial \theta} (h_3 h_1 q_\theta) + \frac{\partial}{\partial z} (h_1 h_2 q_z) \right]$$

$$= \frac{1}{r} \left[\frac{\partial}{\partial x} (r q_r) + \frac{\partial}{\partial \theta} (q_\theta) + \frac{\partial}{\partial z} (r q_z) \right] = 0$$

$$\frac{1}{r} \left[\frac{\partial}{\partial x} (r q_r) + \frac{\partial}{\partial z} (r q_z) \right] = 0$$

i.e., $\lambda \neq 0$

$$\Rightarrow \boxed{\frac{\partial}{\partial x} (r q_r) + \frac{\partial}{\partial z} (r q_z) = 0} \rightarrow \textcircled{1}$$

Consider a scalar pt function $\psi(x, z)$

satisfying

$$q_r = \frac{1}{r} \frac{\partial \psi}{\partial z} \quad \left. \begin{array}{l} \frac{\partial \psi}{\partial z} = r q_r \\ \text{at pt } (x, 0, z) \end{array} \right\} \rightarrow \textcircled{2}$$

$$q_z = -\frac{1}{r} \frac{\partial \psi}{\partial r} \quad \left. \begin{array}{l} \frac{\partial \psi}{\partial r} = -q_z \\ \text{at pt } (x, 0, z) \end{array} \right\} \rightarrow \textcircled{2}$$

∴ substituting $\textcircled{2}$ in $\textcircled{1}$,

$$\text{L.H.S of } \textcircled{1} = \frac{\partial}{\partial x} \left(\frac{\partial \psi}{\partial z} \right) - \frac{\partial}{\partial z} \left(\frac{\partial \psi}{\partial r} \right)$$

$$= \frac{\partial^2 \psi}{\partial x \partial z} - \frac{\partial^2 \psi}{\partial z \partial r} = 0$$

= R.H.S of $\textcircled{1}$

[since ψ represents a scalar pt fn continuous defining the flow.]

i.e., ψ is a scalar pt fn defined by ② satisfying ①. Such a fn ψ is called stokes stream function.

continues

N.V.

Pg. 14



Examples :

Unit : 1

- At the point in an incompressible fluid having spherical polar coordinates (r, θ, ϕ) , the velocity components are $[2Mr^{-3} \cos \theta, Mr^{-3} \sin \theta, 0]$, where M is a constant. Show that the velocity is of the potential kind. Find the velocity potential and the equations of the streamline.

Soln:

In general, curvilinear orthogonal system, we have

$$\text{curl } \vec{F} = \frac{1}{h_1 h_2 h_3} \begin{vmatrix} h_1 \hat{a}_1 & h_2 \hat{a}_2 & h_3 \hat{a}_3 \\ \frac{\partial}{\partial x} & \frac{\partial}{\partial y} & \frac{\partial}{\partial z} \\ h_1 F_1 & h_2 F_2 & h_3 F_3 \end{vmatrix}$$

where $ds = (h_1 dx) \hat{a}_1 + (h_2 dy) \hat{a}_2 + (h_3 dz) \hat{a}_3$

$$F = F_1 \hat{a}_1 + F_2 \hat{a}_2 + F_3 \hat{a}_3$$

$$0 \neq \hat{a}_1 \omega_b =$$

- Q. For an incompressible fluid, $\vec{q} = [-\omega y, \omega x, 0]$ ($\therefore \omega = \text{const}$). Discuss the nature of the flow.

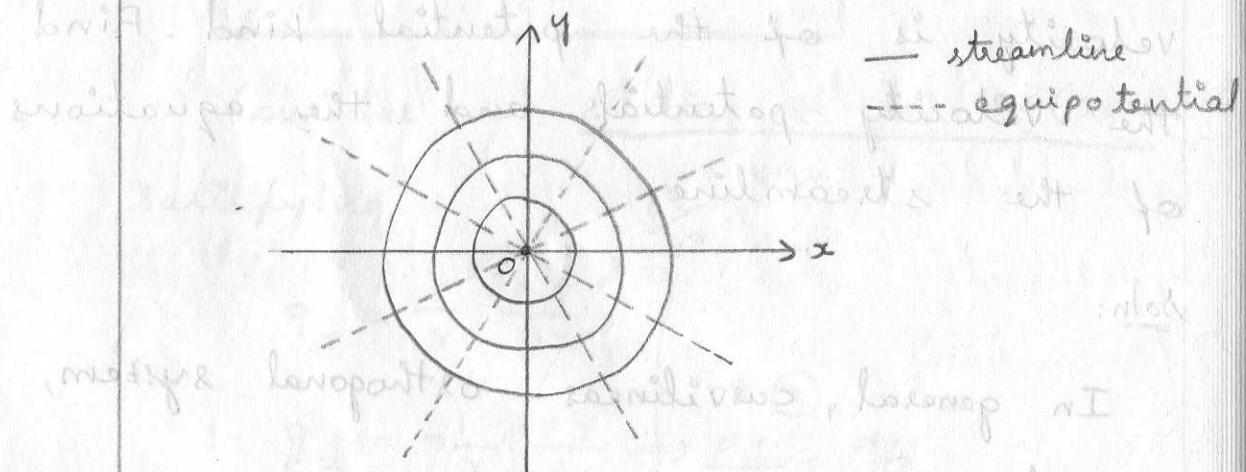
Soln:

$$\text{Here } \nabla \cdot \vec{q} = \frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0 + 0 + 0 = 0$$

$\Rightarrow \nabla \cdot \vec{q} = 0$, so that such a flow is possible.

$$[\therefore u = -\omega y, v = \omega x, w = 0]$$

To find whether the flow is of potential kind:



$$\nabla \times \vec{q} = \begin{vmatrix} \hat{i} & \hat{j} & \hat{k} \\ \frac{\partial}{\partial x} & \frac{\partial}{\partial y} & \frac{\partial}{\partial z} \\ -\omega y & \omega x & 0 \end{vmatrix}$$

$$\begin{aligned} &= \hat{i}(0) + \hat{j}(0) + \hat{k}(\omega + \omega) \\ &= 2\omega \hat{k} \neq 0 \end{aligned}$$

Thus the flow is not potential kind.

To find the eqn of stream lines

It can easily be shown that a rigid body rotating about the z -axis with constant vector angular velocity $\omega \hat{z}$ gives the same type of motion. (For the velocity at (x, y, z) in the body is $-\omega y \hat{i} + \omega x \hat{j}$)

To find the eqn of stream line:

The eqn of stream lines are given by

$$\left(\frac{\partial}{\partial x} - \omega y \hat{i}\right) \frac{dx}{u} = \frac{dy}{v} = \frac{dz}{w}$$

i.e. $\frac{dx}{-\omega y} = \frac{dy}{\omega x} = \frac{dz}{0}$

or $\frac{dx}{-\omega y} = \frac{dy}{\omega x}; dz = 0$

$$xdx = -ydy; dz = 0$$

$$xdx + ydy = 0; dz = 0$$

i.e. the streamlines are the circles

$$x^2 + y^2 = a \text{ (constant)}, \quad z = \text{constant}$$

$$z = a \text{ (constant)}. \quad a = \text{constant}$$

3. AB is a tube of small uniform bore forming a quadrant arc of a circle of radius a and centre O, OA being horizontal and OB vertical with B below O. The tube is full of liquid of density ρ , the end B being closed. If B is suddenly opened, show that initially $\frac{du}{dt} = \frac{2g}{\pi}$, where $u=u(t)$ is the velocity, and that the pressure at a point whose angular distance from A is θ immediately drops to $\rho g a \left(\sin \theta - \frac{\omega}{\pi} \right)$ above atmospheric pressure. Prove further that when the liquid remaining in the tube subtends an angle β at the centre, $\frac{d^2 P}{dt^2} = - \frac{2g}{\alpha \beta} \sin^2 \left(\frac{\beta}{2} \right)$.

Soln:

Let at time 't', $\theta = \omega t + \alpha$

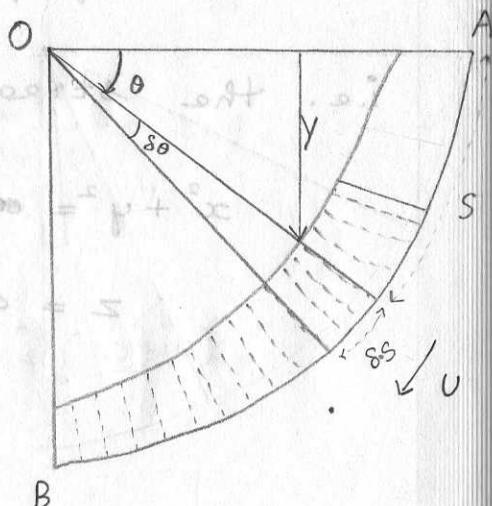
$$* S = \text{arc AP}$$

$$* S + 8S = \text{arc AP'}$$

$$* Y = \text{Depth of P below OA}$$

$$* \angle AOP = \theta . (\text{true + error})$$

$$POP' = 8\theta$$



$$\text{rotation contribution} = \left[-\frac{\cos^3 \theta}{a^3 \sin^3 \theta} \right]_0^\pi$$

$$\text{translation} = \frac{1}{2 \times 3} \rho a^3 \pi v^3 \left[-\frac{\cos^3 \theta}{\sin^3 \theta} \right]_0^\pi$$

$$= \frac{1}{6} \rho a^3 v^2 \pi \left[-\frac{\cos 3\theta - 3 \cos \theta}{4} \right]_0^\pi$$

bentrigon position = ϕ

$$\phi \text{ next } \phi = \frac{1}{6} \rho \pi a^3 v^2 \left[\frac{-(-1) - 3(-1) - (-1 - 3)}{4} \right]$$

$$\text{e.g. } \phi = \frac{1}{6} \rho \pi a^3 v^2 \left[\frac{1 + 3 + 1 + 3}{4} \right]$$

$$\text{kinetic} = \frac{1}{6} \rho \pi a^3 v^2 [2] \text{ as virtual}$$

$$\text{kinetic} = \frac{1}{3} \rho \pi a^3 v^2 \text{ as virtual}$$

at horizon '99' equivalent to virtual unit

$$= \frac{1}{4} \cdot \frac{4}{3} \rho \pi a^3 v^2$$

$$(p_{3u} - p_{3v})^2 / 28 (x_{3u} - x_{3v})^2$$

$$\cdot \frac{1}{4} M' v^2 \text{ mass of fluid in unit unit}$$

where M' is the mass of fluid

displaced. The total kinetic energy of

the sphere and fluid is thus $\frac{1}{2} (M + \frac{1}{2} M') v^2$.

The quantity $M + \frac{1}{2} M'$ is called the virtual mass of the sphere.

Continuation... (*)

Pg. 97
After this Stream fn for 2-D flow \rightarrow Vorticity
for 2-D flow:

In addition if the flow is irrotational
then $\vec{\omega} = \vec{0}$

$$\Rightarrow \nabla^2 \psi = 0$$

$\Rightarrow \psi$ satisfies Laplace's eqn.

Also for such a flow if ϕ = velocity po
given by scalar point function : $\vec{q} = -\nabla \phi$ then
satisfies $\nabla^2 \phi = 0$.

Thus in case when the flow is incomp
irrotational for an inviscid fluid, both ϕ & ψ
satisfies Laplace equation.

Velocity component at P along the normal
from right to left as we travel from A to
is $v \cos \alpha - u \sin \alpha$.

Hence mass of the fluid that crosses unit
thickness of surface elt through PP' normal to
plane of flow per unit time is

$$\rho(v \cos \alpha - u \sin \alpha) \delta s = \rho(v \delta x - u \delta y)$$

This flux is constant : denote it by $\delta \psi$.

$$\therefore \delta \psi = \rho(v \delta x - u \delta y)$$

$$(or) d \psi = \rho(v dx - u dy) \rightarrow (f)$$

The total mass flux per unit thickness p
unit time from right to left across AB is

$$\Psi_B - \Psi_A = \int_A^B \rho(v dx - u dy) \rightarrow (ff)$$

A & B are fixed and (ft) is independent of path joining A & B hence is independent of \$ joining A & B.

$\therefore d\psi$ is a perfect differential.

i.e., both velocity potential and stream fn in this case satisfies Laplace eqn and are hence Harmonic functions.

Equipotentials:

For a 2D III flow equipotentials are given by $\phi(x, y) = \text{const}$ & the direction ratios of normal at P to the surfaces $\phi(x, y) = \text{const}$ are (i.e. dir. of $\nabla \phi$)

$$\left(\frac{\partial \phi}{\partial x}, \frac{\partial \phi}{\partial y}, 0 \right) \quad (\Leftrightarrow (a_1, a_2, 0))$$

Now considering (6) $\psi(x, y) = \text{const}$

$\text{curl } \vec{q} = 0$
the surfaces $\phi(x, y, z, t) = \text{const}$
are called equipotentials

Remark:

III flow

$$(*) \quad u = -\phi_x = -\psi_y \quad \& \quad v = -\phi_y = \psi_x \\ \Rightarrow \phi_x = \psi_y \quad \& \quad \phi_y = -\psi_x$$

$$(*) \quad \nabla^2 \phi = 0 ; \quad \nabla^2 \psi = 0$$

$$\frac{\partial \phi}{\partial x} \cdot \frac{\partial \psi}{\partial x} + \frac{\partial \phi}{\partial y} \cdot \frac{\partial \psi}{\partial y} = 0$$

$$\Rightarrow \nabla \phi \perp \nabla \psi.$$

curves &

surfaces is
lines.

orthogonal.
particular

for 2D III flow.

$A \& B$ are fixed and (f) is independent of path joining $A \& B$ hence is independent of ϕ joining $A \& B$.

$\therefore d\psi$ is a perfect differential.

i.e., both velocity potential and stream fn in this case satisfies Laplace eqn and are hence Harmonic functions.

Equipotentials:

For a 2D III flow equipotentials are given by $\phi(x, y) = \text{const}$ & the direction ratios of normal at P to the surfaces $\phi(x, y) = \text{const}$ are (i.e. dir. of $\nabla \phi$)

$$\left(\frac{\partial \phi}{\partial x}, \frac{\partial \phi}{\partial y}, 0 \right) \Leftrightarrow (a_1, a_2, 0)$$

Now, considering ⑥ $\psi(x, y) = \text{const}$ the normal at P to $\psi(x, y) = \text{const}$ has direction ratios

$$\left(\frac{\partial \psi}{\partial x}, \frac{\partial \psi}{\partial y}, 0 \right) \Leftrightarrow (v_1, v_2, 0)$$

$$a_1 v_1 + a_2 v_2 + 0 = \psi_x \phi_x + \psi_y \phi_y + 0$$

$$\vec{q} = -\nabla \phi \Rightarrow u = -\phi_x; v = -\phi_y$$

$$\text{Also } u = -\psi_y, v = \psi_x$$

$$\Rightarrow \psi_x = -\phi_y; \psi_y = \phi_x$$

$$\Rightarrow a_1 v_1 + a_2 v_2 = \underline{\quad} + \phi_x \phi_y = 0$$

\Rightarrow that the two families of equipotential curves & streamlines are mutually orthogonal.

In other words, the family of equipotential surfaces is cut orthogonally by the family of stream lines.

i.e., the st. lines & equipotentials are mutually orthogonal.

Such a feature exists for any flow & in particular for 2D III flow.

Call $\vec{q} = \vec{0}$
the surfaces $\phi(x, y, z, t) = \text{const}$
are called equipotentials

At equipotentials
stream lines cut
orthogonally.

PG. 73

Examples:

2. Illustration of line distributions.

Prove that the velocity potential at a point P due to a uniform finite line source AB of strength 'm' per unit length is of the form $\phi = m \log f$, where

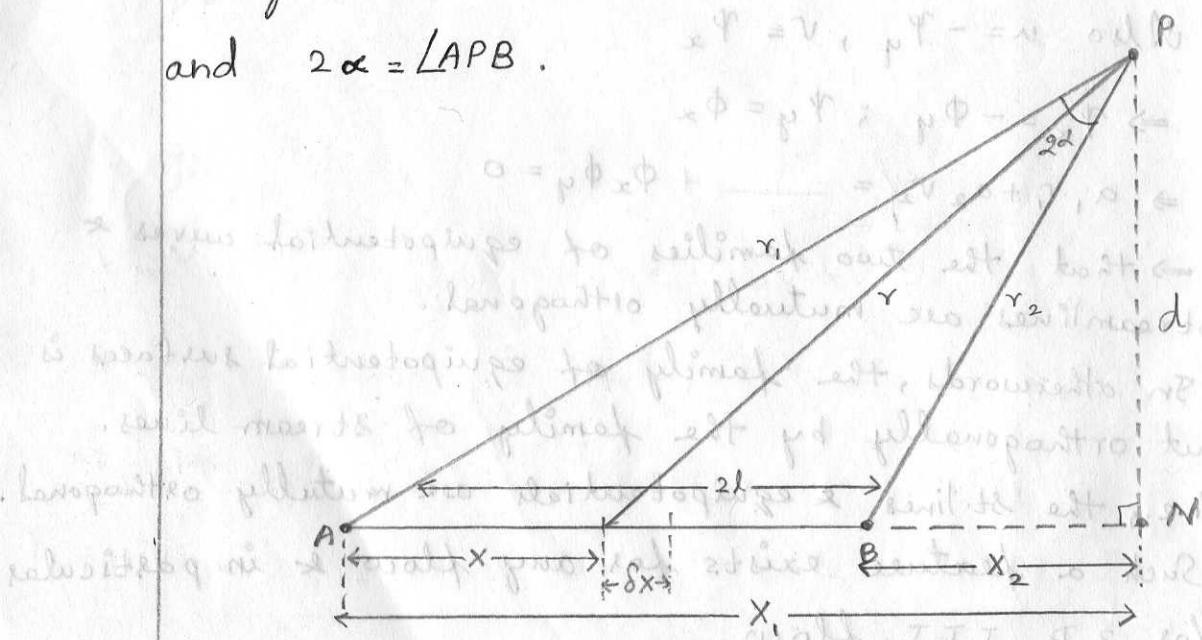
$$f = \frac{r_2 + x_2}{r_1 + x_1} = \frac{r_1 - x_1}{r_2 - x_2} = \frac{a+l}{a-l}$$

in which $AB = 2l$, $PA = r_1$, $PB = r_2$, $NA = x_1$, $NB = x_2$, N being the foot of the perpendicular from P on the line AB, and $2a$ the length of the major axis of the spheroid through P having A, B as foci.

Show that the velocity at P is

$$\frac{(2ml\cos\alpha)}{(a^2 - l^2)\alpha} \hat{u}, \text{ where } \hat{u} \text{ is the unit vector}$$

along the normal to the spheroid at P and $2\alpha = \angle APB$.



The line-section of length $8x$ in AB at distance x from A is effectively a point source of strength $m8x$ giving a velocity potential at P of amount $\frac{(m8x)}{r_1}$,
 $AP = r_1$.

From Pythagoras Theorem,

$$r^2 = d^2 + (x_1 - x)^2$$

$$\therefore d^2 = r_1^2 - x_1^2$$

$$\left[\left(\frac{x}{b} \right)^2 - d^2 = d^2 + (x_1^2 + x^2 - 2x_1 x) \right]$$

$$r_1^2 = d^2 + x_1^2$$

$$= r_1^2 - x_1^2 + x_1^2 + x^2 - 2x_1 x$$

$$= r_1^2 + x^2 - 2x_1 x$$

and so the total velocity potential at P due to the entire line distribution is

$$\phi = m \int_0^{2l} \frac{dx}{r}$$

$$= m \int_0^{2l} \frac{dx}{\sqrt{d^2 + (x_1 - x)^2}}$$

$$= m \int_0^{2l} \frac{dx}{\sqrt{[d^2 + (x_1 - x)^2]^{1/2}}}$$

$$= m \int_0^{2l} \frac{dx}{\sqrt{[r_1^2 - x_1^2 + (x_1 - x)^2]^{1/2}}}$$

$$= m \left[-\sinh^{-1} \left(\frac{x_1 - x}{d} \right) \right]_0^{2l}$$

$$\therefore \int_0^{2l} \frac{dx}{\sqrt{(x^2 + a^2)^{1/2}}} = -\sinh^{-1} \frac{a}{x}$$

$$\phi = m \left[-\sin^{-1} \left(\frac{x_1 - 2d}{d} \right) + \sin^{-1} \left(\frac{x_1}{d} \right) \right]$$

$$= m \left[\sin^{-1} \left(\frac{x_1}{d} \right) - \sin^{-1} \left(\frac{x_1 - 2d}{d} \right) \right]$$

$$\left[\because \sin^{-1} x = \log(x + \sqrt{x^2 + 1}) \quad \& \quad x_1 - 2d = x_2 \right]$$

$$= m \left[\sin^{-1} \left(\frac{x_1}{d} \right) - \sin^{-1} \left(\frac{x_2}{d} \right) \right]$$

$$= m \log \left[\frac{x_1 + \sqrt{x_1^2 + d^2}}{x_2 + \sqrt{x_2^2 + d^2}} \right]$$

$$\phi = m \log \left(\frac{x_1 + r_1}{x_2 + r_2} \right) - \left[\because r_1^2 = d^2 + x_1^2 \right]$$

↪ ①

Now,

$$r_1^2 - x_1^2 = d^2$$

$$r_2^2 - x_2^2 = d^2$$

$$\text{i.e.) } r_1^2 - x_1^2 = r_2^2 - x_2^2$$

$$(r_1 - x_1)(r_1 + x_1) = (r_2 - x_2)(r_2 + x_2)$$

So that

$$\frac{r_1 + x_1}{r_2 + x_2} = \frac{r_2 - x_2}{r_1 - x_1} = \frac{r_2 - x_2 + r_1 + x_1}{r_1 - x_1 + r_2 + x_2} = \frac{r_1 + r_2 + 2d}{r_1 + r_2 - 2d}$$

At P on the spheroid through P having A, B as foci,

$$r_1 + r_2 = 2a$$

Hence

$$\frac{r_1 + x_1}{r_2 + x_2} = \frac{r_2 - x_2}{r_1 - x_1} = \frac{r_1 + r_2 + 2l}{r_1 + r_2 - 2l} = \frac{2a + 2l}{2a - 2l} = \frac{\lambda(a+l)}{\lambda(a-l)}$$

Thus sub in eqn ①,

$$\phi = m \log \left(\frac{a+l}{a-l} \right)$$

The equipotentials are given by

$$\phi = \text{const} \quad (\text{or}) \quad \frac{a+l}{a-l} = \text{const}$$

Thus they are $a = \text{const}$ (or) $r_1 + r_2 = \text{const}$.

These surfaces are confocal ellipsoids of revolution about AB with A, B as foci.

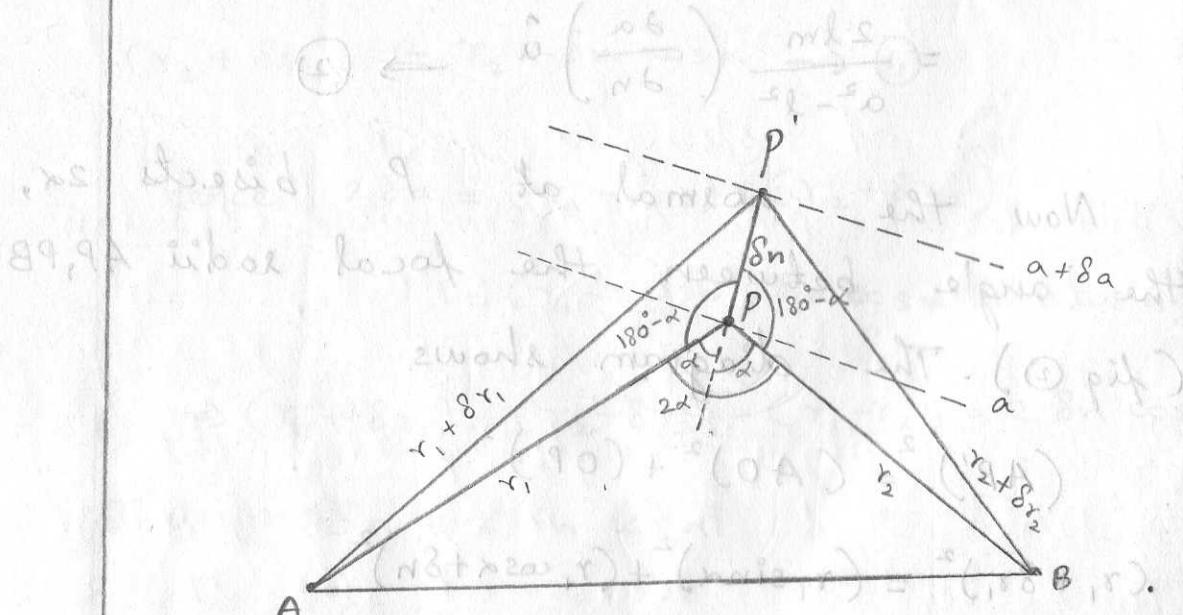


Fig ②

Let P be any point on the ellipsoid specified by parameters a, P' a pt on the neighbouring ellipsoid specified by parameters $(a+8a)$, where $\overline{PP'} = 8n \hat{u}$.

Then the velocity at P is

$$\begin{aligned} \frac{(a+l)}{(l-a)} \frac{\partial \phi}{\partial n} &= \frac{\partial \phi}{\partial n} = -\nabla \phi = -\frac{\partial \phi}{\partial x}, \quad x = r + l \\ \Rightarrow -\nabla \phi &= -\frac{\partial \phi}{\partial n} \hat{u} \\ &= -\frac{\partial}{\partial n} \left[m \log \left(\frac{a+l}{a-l} \right) \right] \hat{u} \\ &= -m \hat{u} \frac{\partial}{\partial n} \left[\log(a+l) - \log(a-l) \right] \\ &= -m \hat{u} \frac{\partial a}{\partial n} \left(\frac{1}{a+l} - \frac{1}{a-l} \right) \\ &= -m \hat{u} \frac{\partial a}{\partial n} \left(\frac{2l}{a^2 - l^2} \right) \end{aligned}$$

$$\begin{aligned} \text{to obtain } \frac{\partial a}{\partial n} &= -m \hat{u} \frac{\partial a}{\partial n} \left(\frac{-2l}{a^2 - l^2} \right) \\ &= \frac{2lm}{a^2 - l^2} \left(\frac{\partial a}{\partial n} \right) \hat{u} \rightarrow ② \end{aligned}$$

Now the normal at P bisects 2α , the angle between the focal radii AP, PB (fig ②). The diagram shows

$$(AP')^2 = (AO)^2 + (OP')^2$$

$$(r_1 + 8r_1)^2 = (r_1 \sin \alpha)^2 + (r_1 \cos \alpha + 8n)^2$$

$$\begin{aligned}
 (r_1 + 8r_1)^2 &= r_1^2 \sin^2 \alpha + r_1^2 \cos^2 \alpha + (8n)^2 + 2r_1 8n \cos \alpha \\
 &= r_1^2 (\sin^2 \alpha + \cos^2 \alpha) + (8n)^2 + 2r_1 8n \cos \alpha \\
 &= r_1^2 + (8n)^2 + 2r_1 8n \cos \alpha
 \end{aligned}$$

$$(r_1 + 8r_1) = \left[r_1^2 + (8n)^2 + 2r_1 8n \cos \alpha \right]^{1/2}$$

$$(r_1 + 8r_1) \underset{\text{Top row, } (3) \text{ & } (2) \text{ prilla}}{=} r_1 + 8n \cos \alpha \rightarrow (3)$$

Similarly,

$$(BP')^2 = (BO)^2 + (OP')^2$$

$$(r_2 + 8r_2)^2 = (r_2 \sin \alpha)^2 + (r_2 \cos \alpha + 8n)^2$$

$$= r_2^2 \sin^2 \alpha + r_2^2 \cos^2 \alpha + (8n)^2$$

$$+ 2r_2 8n \cos \alpha$$

$$= r_2^2 (\sin^2 \alpha + \cos^2 \alpha) + (8n)^2 + 2r_2 8n \cos \alpha$$

$$= r_2^2 + (8n)^2 + 2r_2 8n \cos \alpha$$

$$(r_2 + 8r_2) = \left[r_2^2 + (8n)^2 + 2r_2 8n \cos \alpha \right]^{1/2}$$

$$(r_2 + 8r_2) \underset{\text{Top row, } (3) \text{ & } (2) \text{ prilla}}{=} r_2 + 8n \cos \alpha \rightarrow (4)$$

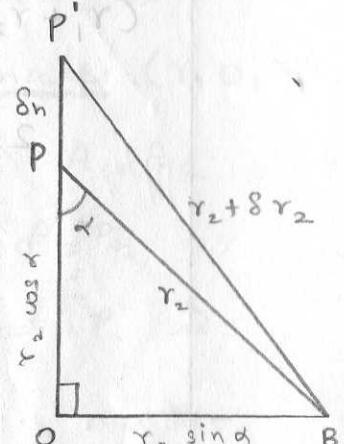
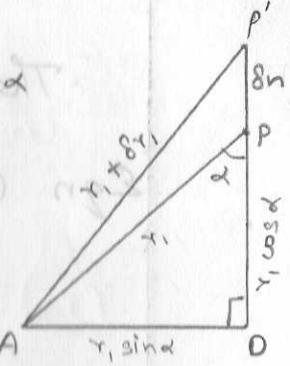
$$\text{Hence } 2\delta a = (r_1 + 8r_1) + (r_2 + 8r_2)$$

$$\text{Hence } (2, 0, 0) = (r_1 + r_2) + (8n \cos \alpha + 8n \cos \alpha)$$

$$\Rightarrow (r_1 + 8r_1) + (r_2 + 8r_2) - (r_1 + r_2) = 2 \cdot 8n \cos \alpha$$

$$\text{Thus } 2\delta a = 2 \cdot 8n \cos \alpha$$

$$\frac{\delta a}{8n} = \cos \alpha$$



The velocity at P is $2lm \cos \alpha$

Eqn ③, we can written as

$$r_1 + 8r_1 - r_1 = 8n \cos \alpha \rightarrow ⑤$$

Eqn ④, we can written as

$$r_2 + 8r_2 - r_2 = 8n \cos \alpha \rightarrow ⑥$$

Adding ⑤ & ⑥, we get

$$(r_1 + r_2) + (8r_1 + 8r_2) - (r_1 + r_2) = 8n \cos \alpha + 8n \cos \alpha$$

$$2a + (8r_1 + 8r_2) - 2a = 2.8n \cos \alpha$$

$$\therefore 8a = 2.8n \cos \alpha \quad [8r_1 + 8r_2 = 2a]$$

$$\frac{8a}{8n} = \cos \alpha \rightarrow ⑦$$

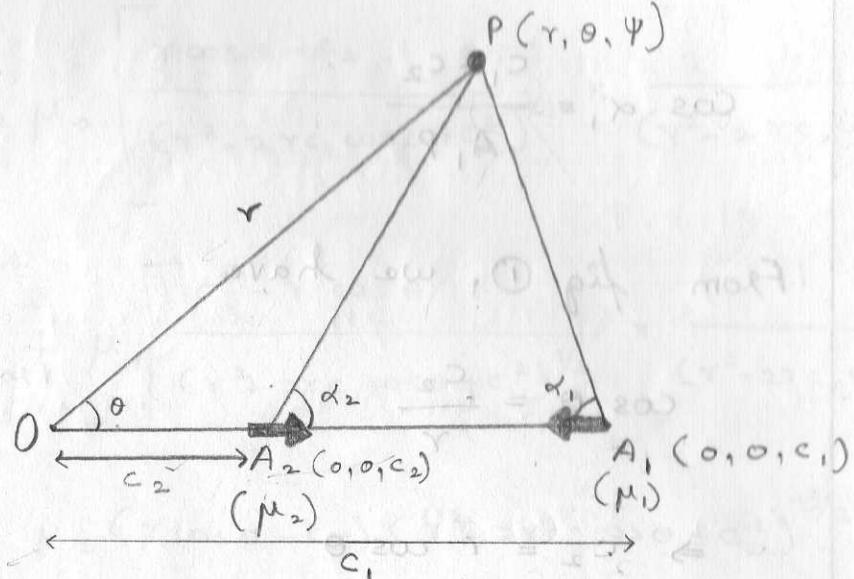
The velocity at P is

$$\nabla \phi = \frac{2lm \cos \alpha}{a^2 - l^2} \hat{u}$$

2. Doublets of strengths μ_1, μ_2 are situated at pts A_1, A_2 whose Cartesian coordinates are $(0, 0, c_1), (0, 0, c_2)$, their axes being directed towards and away from the origin respectively. Find the condition that there is no transport of fluid over the surface of the sphere.

$$x^2 + y^2 + z^2 = c_1, c_2$$

Fig ①



Let initial line be $OA_2 A_1$, θ

P has spherical polar coordinates (r, θ, ϕ)

The axes of the doublets at A_1, A_2
make angles α_1, α_2 with $A_1 P, A_2 P$.

Then the velocity Potential at P is

$$\phi = \phi_1 + \phi_2$$

$$\phi = \frac{\mu_1 \cos \alpha_1}{A_1 P^2} + \frac{\mu_2 \cos \alpha_2}{A_2 P^2}$$

$$\boxed{\phi = \frac{\mu_1 \cos \alpha_1}{A_1 P^2} + \frac{\mu_2 \cos \alpha_2}{A_2 P^2}} \rightarrow \textcircled{*}$$

$$\text{where } \phi_1 = \frac{\mu_1 \cos \alpha_1}{A_1 P^2}, \phi_2 = \frac{\mu_2 \cos \alpha_2}{A_2 P^2}$$

Now

$$\text{Let } A_1 P^2 = r^2 - 2rc_1 \cos \theta + c_1^2 \rightarrow \textcircled{1}$$

$$A_2 P^2 = r^2 - 2rc_2 \cos \theta + c_2^2 \rightarrow \textcircled{2}$$

Since

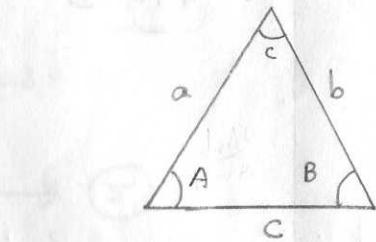
$$a = r, b = c_1, c_2$$

$$c^2 = a^2 - 2ab \cos \theta + b^2$$

$$\cos \alpha_1 = \frac{c_1 - c_2}{A_1 P}$$

From fig ①, we have

$$\cos \theta = \frac{c_2}{r}$$



From cosine formula

$$a^2 = b^2 + c^2 - 2bc \cos A$$

$$\Rightarrow c_2 = r \cos \theta$$

$$\therefore \boxed{\cos \alpha_1 = \frac{c_1 - r \cos \theta}{A_1 P}}$$

(r, θ, r) ~~refer to doublet~~ refer to initial point

by A to initial point to final point

$$\therefore \cos \alpha_2 = \frac{c_1 - c_2}{A_2 P} \times \text{refers to final}$$

θ to final position of point

From fig ①, we have

$$\phi + \phi = \phi$$

$$\circlearrowleft \quad \cos \theta = \frac{c_1}{r} \quad \text{refers to final} \quad \phi$$

$$\Rightarrow c_1 = r \cos \theta$$

$$\therefore \boxed{\cos \alpha_2 = \frac{r \cos \theta - c_2}{A_2 P}} \quad \phi \text{ refers to final}$$

Sub. a_1, a_2, b_1, b_2 in \circlearrowleft

Also taking P to have spherical polar co-ordinates (r, θ, ψ) referred to the axis of the doublet as initial line, the velocity potential at P being

$$\phi(r, \theta) = \underline{\underline{\frac{\mu \cos \theta}{r^2}}}$$

$$\phi(r, \theta) = \mu_2 \left[\frac{r \cos \theta - c_2}{(r^2 - 2rc_2 \cos \theta + c_2^2)^{1/2}} \right] + \mu_1 \left[\frac{c_1 - r \cos \theta}{(r^2 - 2rc_1 \cos \theta + c_1^2)^{1/2}} \right]$$

$$= \mu_2 (r \cos \theta - c_2) (r^2 - 2rc_2 \cos \theta + c_2^2)^{-3/2} \\ + \mu_1 (c_1 - r \cos \theta) (r^2 - 2rc_1 \cos \theta + c_1^2)^{-3/2}$$

Differentiate $\phi(r, \theta)$ w.r.t. r ,

$$\frac{\partial \phi}{\partial r} = \mu_2 \left[(r \cos \theta - c_2) \left[-\frac{3}{2} (r^2 - 2rc_2 \cos \theta + c_2^2)^{-5/2} \right. \right. \\ \left. \left. (2r - 2c_2 \cos \theta) \right] + (r^2 - 2rc_2 \cos \theta + c_2^2)^{-3/2} \right. \\ \left. \left. (c_1 - r \cos \theta) \right[-\frac{3}{2} (r^2 - 2rc_1 \cos \theta + c_1^2)^{-5/2} \right. \right. \\ \left. \left. (2r - 2c_1 \cos \theta) \right] + (r^2 - 2rc_1 \cos \theta + c_1^2)^{-3/2} \right]$$

$$= \mu_2 \left[\cos \theta (r^2 - 2rc_2 \cos \theta + c_2^2)^{-3/2} \right. \\ \left. - 3(r \cos \theta - c_2)(r - c_2 \cos \theta)(r^2 - 2rc_2 \cos \theta + c_2^2)^{-5/2} \right]$$

$$+ \mu_1 \left[\cos \theta (r^2 - 2rc_1 \cos \theta + c_1^2)^{-3/2} \right. \\ \left. + 3(c_1 - r \cos \theta)(r^2 - 2rc_1 \cos \theta + c_1^2)^{-5/2} (r - c_1 \cos \theta) \right]$$

rical
to the
line,
9

We require that $\frac{\partial \phi}{\partial r} = 0$ when $r = (c_1, c_2)^{1/2}$

(**) [W.K.T,

the sphere eqn is $x^2 + y^2 + z^2 = r^2$ with
the center in the origin.

From the gn,

$$r = (c_1, c_2)^{1/2}$$

$$\mu_2 \left[\cos \theta \left\{ c_1 c_2 - 2(c_1, c_2)^{1/2}, c_2 \cos \theta + c_1^2 \right\}^{-3/2} \right]$$

$$- 3 \left\{ (c_1, c_2)^{1/2} \cos \theta - c_2 \right\} \left\{ (c_1, c_2)^{1/2} - c_2 \cos \theta \right\}$$

$$\left\{ (c_1, c_2) - 2(c_1, c_2)^{1/2} c_2 \cos \theta + c_1^2 \right\}^{-5/2}$$

$$(\theta 200) = \mu_1 \left[\cos \theta \left\{ c_1 c_2 - 2 c_1 (c_1, c_2)^{1/2} \cos \theta + c_1^2 \right\}^{-3/2} \right]$$

$$+ 3 \left\{ (c_1, c_2)^{1/2} c_1 - (c_1, c_2)^{1/2} \cos \theta \right\} \left\{ (c_1, c_2)^{1/2} - c_1 \cos \theta \right\}$$

$$\left\{ c_1 c_2 - 2 c_1 (c_1, c_2)^{1/2} \cos \theta + c_1^2 \right\}^{-5/2}$$

$$\text{per } \mu_2 \quad 4/3 \sqrt{(c_1, c_2)^{1/2} \cos \theta / c_2} \sqrt{(c_1, c_2)^{1/2} / c_1}$$

$$\text{per } \mu_1 \quad (\theta 200, \theta - r) (\theta - \theta 200, r)$$

$$\Rightarrow \frac{\mu_2}{\mu_1} = \left(\frac{c_2}{c_1} \right)^{3/2}$$

$$(\theta 200, \theta - r) (\theta - \theta 200, r) (\theta 200, \theta - r)$$

3.4) Meaning of 2D flows:

A fluid flow is called 2-D if the fluid moves in such a way that at any given instant of time the flow pattern in a certain plane is the same as that in all other parallel planes moves in the same plane.

Suppose we consider the flow of fluid to be in the xoy -plane $\Leftrightarrow z=0$ plane in the cartesian co-ordinate system.

It follows that any point P in the fluid with fluid velocity $\vec{q}(x, y, 0, t)$ independent of z .

i.e.) velocity is the same at all pts. on planes \parallel to z -axis.

Hence the fluid flows in such a way that at any given instant the flow pattern in a certain plane is the same as that in all planes parallel to $z=0$ plane.

Physical quantities like (velocity, pressure, density, etc.) are independent of z coordinate $P : P(x, y)$.

$\vec{q} : \vec{q}(x, y, t)$ vector quantity

$p : p(x, y, t)$ scalar

$\rho : \rho(x, y, t)$ scalar

An infinitesimal volume in a 2D

flow is considered to be of unit thickness & hence elementary volume element considered, denoted by δV ,

defined by

$$\delta V = \delta x \cdot \delta y \cdot 1$$

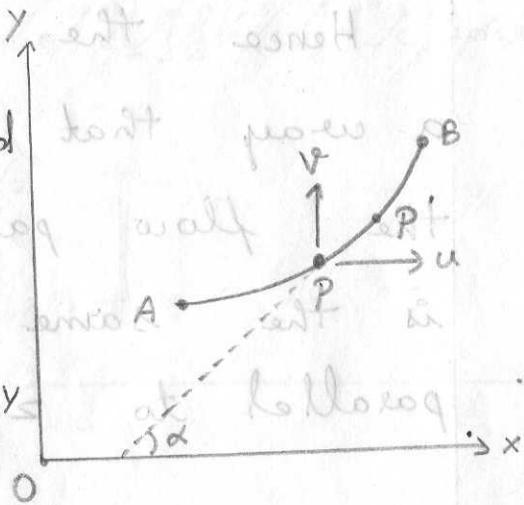
$$= \delta x \cdot \delta y$$

Not in the syllabus

Stream function for 2-D flows:

Consider an inviscid, incompressible 2D fluid and flow.

Let the plane of flow be closed as xoy plane.



Let $\$$ be an arc of a curve joining 2 pts in XOY plane.

Let P be the position of any fluid elt with co-ordinates $P(x, y, t)$ at time t , on $\$$.

Let $\vec{q} : \vec{q}(x, y, t)$ be the fluid velocity at P at time t .

$$\text{Then } \vec{q} = u\hat{i} + v\hat{j} \text{ at time } t \quad \rightarrow ①$$

$$\left. \begin{array}{l} \text{where } u = u(x, y, t) \\ v = v(x, y, t) \end{array} \right\} \rightarrow ②$$

The (eqn of) continuity (for incompressible fluid flow) is

$$\Rightarrow \left(\frac{\partial \vec{q}}{\partial x} + \frac{\partial \vec{q}}{\partial y} \right) \cdot (u\hat{i} + v\hat{j}) = 0 \quad \rightarrow ③$$

Let $P' = P'(x+8x, y+8y, t+8t)$ be a neighbouring pt on $\$$. So that $PP' = 8s$.

Let the tangent at P to $\$$ make angle α with horizontal axis Ox .

For this flow define a scalar pt fn that is differentiable and uniform throughout the region of flow given by

$$\psi = \Psi(x, y) \rightarrow (4)$$

Subj to conditions

$$u = -\psi_y \quad v = \psi_x$$

$$u = -\frac{\partial \psi}{\partial y} \quad v = +\frac{\partial \psi}{\partial x} \rightarrow (5)$$

$$\text{both part } = -\psi_y = \psi_x$$

Sub (5) in (3), we have

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = \frac{\partial}{\partial x} \left(-\frac{\partial \psi}{\partial y} \right) + \frac{\partial}{\partial y} \left(\frac{\partial \psi}{\partial x} \right)$$

$$= -\frac{\partial^2 \psi}{\partial x \partial y} + \frac{\partial^2 \psi}{\partial y \partial x} = 0$$

$\Rightarrow \psi$ satisfies (eqn. $\nabla \cdot \vec{g} = 0$) eqn of continuity.

\Rightarrow existence of such a scalar pt fn $\psi = \Psi(x, y)$ defining a 2D inviscid incompressible fluid flow.

The stream lines for the above flow are gn by

$$\frac{dx}{u} = \frac{dy}{v} = \frac{dz}{0}$$

$$\Rightarrow \frac{dx}{-\psi_y} = \frac{dy}{\psi_x} = \frac{dz}{0}$$

measuring bns adiabatic eff is const.

$$dz = 0 \Rightarrow z = \text{const.}$$

$$\psi_x dx = -\psi_y dy$$

$$\Rightarrow \psi_x dx + \psi_y dy = 0$$

$$\frac{\partial \psi}{\partial x} dx + \frac{\partial \psi}{\partial y} dy = 0$$

$$\Rightarrow d\psi = 0 \Rightarrow \psi = \text{const} \rightarrow (6)$$

Thus the streamlines for the flow are given by $\psi = \text{const}$ at $z = \text{const}$.

$$\psi(x, y) = \text{const} \text{ in } z = \text{const} \text{ plane.}$$

$\Rightarrow \psi = \psi(x, y)$ is called the stream function for 2-D inviscid incompressible flow.

Vorticity vector for 2D flow:

At $P(x, y)$, the vorticity vector $\vec{\omega} = \nabla \times \vec{V}$

is given by

$$\vec{\omega} = \begin{vmatrix} \hat{i} & \hat{j} & \hat{k} \\ \frac{\partial}{\partial x} & \frac{\partial}{\partial y} & \frac{\partial}{\partial z} \\ u & v & w \end{vmatrix}$$

$$= \left(\frac{\partial v}{\partial x} - \frac{\partial u}{\partial y} \right) \hat{k}$$

$$\Rightarrow \vec{\omega} = \nabla \times \vec{V} = \left[\frac{\partial}{\partial x} \left(\frac{\partial \psi}{\partial x} \right) - \frac{\partial}{\partial y} \left(-\frac{\partial \psi}{\partial y} \right) \right] \hat{k}$$

$$= \left(\frac{\partial^2 \psi}{\partial x^2} + \frac{\partial^2 \psi}{\partial y^2} \right) \hat{k}$$

$$\Rightarrow \vec{\omega} = (\nabla^2 \psi) \hat{k}$$

→ vorticity vector for 2D inviscid flow is at right angles to the plane of flow.

i.e. $\vec{\omega}$ is $|\vec{\omega}| = \frac{1}{\rho} \sqrt{(\frac{\partial u}{\partial y} - \frac{\partial v}{\partial x})^2 + (\frac{\partial w}{\partial x} - \frac{\partial u}{\partial z})^2 + (\frac{\partial v}{\partial z} - \frac{\partial w}{\partial y})^2}$ is along the \hat{k} direction.

i.e. z -axis of plane of flow is ~~the wall ext. will meet ext. end~~

$\Rightarrow \vec{\omega}$ is \perp to plane of flow.

[Continue - before (Meaning of 2D flow - 1 example) (*)]

Eg:

Liquid flows through a pipe whose surface is the surface of revolution of the curve $y = a + kx^2/a$ about the x -axis ($-a \leq x \leq a$).

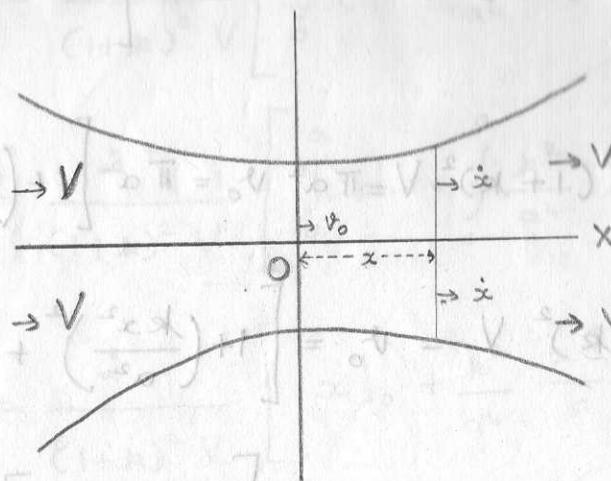
If the liquid enters at the end $x = -a$ of the pipe with velocity V , show that the time taken by a liquid particle to traverse the entire length of the pipe from $x = -a$ to $x = +a$ is

$$\left(\frac{2a}{V(1-k)^2} \right) \left(1 + \frac{2}{3}k + \frac{1}{5}k^2 \right).$$

[Assume that k is so small that the flow remains appreciably one-dimensional throughout.]

flow
of

Soln:



Let v_0 be the velocity at the section

$x = 0.0010$ yields β in units

$$\pi a^2 (1+k)^2$$

The area of the section $x=0$ is

$$\pi(\alpha^2)$$

The area of the section distant x
from O is

$$\pi \left(a + \left(\frac{kx^2}{a} \right) \right)^2$$

So the eqn of continuity (expressing equal rates of volumetric flow across the three sections) is

$$\frac{\pi a^2 (1+k)^2 V}{\pi a^2 V_0} = \frac{1}{b} \left(a + \left(\frac{kx^2}{a} \right) \right)^2$$

$$\Rightarrow \pi a^2 (1+k)^2 V = \pi a^2 v_0 = \pi \left[\frac{(kx^2)}{a^2} + 2a \frac{kx^2}{a} \right] \dot{x}$$

$$\Rightarrow \pi a^2 (1+k)^2 V = \pi a^2 v_0 = \pi a^2 \left[1 + \left(\frac{kx^2}{a^2} \right)^2 + 2 \frac{kx^2}{a^2} \right] \dot{x}$$

$$\Rightarrow (1+k)^2 V = v_0 = \left[1 + \left(\frac{kx^2}{a^2} \right)^2 + 2 \frac{kx^2}{a^2} \right] \dot{x}$$

$$\Rightarrow (1+k)^2 V = v_0 = \left[1 + \frac{kx^2}{a^2} \right]^2 \dot{x}$$

no longer set to potential at end (0) to start

since \dot{x} is the velocity across the plane-distance x from 0.

Then

$$dt = \left(1 + \frac{kx^2}{a^2} \right)^2 \frac{dx}{(1+k)^2 V}$$

Integrating it on both sides,

$$\int_{-a}^a dt = \int_{-a}^a \left(1 + \frac{kx^2}{a^2} \right)^2 \frac{dx}{(1+k)^2 V}$$

$$t = \frac{2}{(1+k)^2 V} \int_0^a \left(1 + \frac{kx^2}{a^2} \right)^2 dx$$

$$= \frac{2}{(1+k)^2 V} \int_0^a \left(1 + \frac{kx^2}{a^2} \right)^2 dx$$

$$\Rightarrow t = \frac{2}{(1+k)^2 V} \left[\int_0^a \left(1 + \frac{k^2 x^4}{a^4} + 2 \frac{k x^2}{a^2} \right) dx \right]$$

$$= \frac{2}{(1+k)^2 V} \left[\int_0^a dx + \int_0^a \frac{k^2}{a^4} x^4 dx + \int_0^a \frac{2k}{a^2} x^2 dx \right]$$

$$= \frac{2}{(1+k)^2 V} \left[x \Big|_0^a + \frac{k^2}{a^4} \cdot \frac{x^5}{5} \Big|_0^a + \frac{2k}{a^2} \cdot \frac{x^3}{3} \Big|_0^a \right]$$

$$= \frac{2}{(1+k)^2 V} \left\{ a + \frac{k^2}{a^4} \cdot \frac{a^5}{5} + \frac{2k}{a^2} \cdot \frac{a^3}{3} \right\}$$

$$= \frac{2}{(1+k)^2 V} \left\{ a + \frac{k^2 a}{5} + \frac{2ka}{3} \right\}$$

$$\text{To vibrate} = \frac{2a}{(1+k)^2 V} \left(1 + \frac{k^2}{5} + \frac{2k}{3} \right)$$

Thus the required time of flow is

$$\frac{2a}{(1+k)^2 V} \left(1 + \frac{1}{5} k^2 + \frac{2}{3} k \right)$$

$$\text{i.e. } \frac{2a}{(1+k)^2 V} \left(1 + \frac{2}{3} k + \frac{1}{5} k^2 \right)$$

$$2. \text{ If } \dot{V}(x \pi) = \dot{V}(x \pi')$$

$$\frac{\dot{V}''}{\dot{V}} = \frac{1}{R}$$

initially both are \dot{V} & \dot{V}' new

2. Underwater explosion giving spherical gas bubble.



An explosion takes place under water initially at rest. As a result, a spherical gas bubble of center O , is formed. During expansion gas obeys adiabatic law $pV^\gamma = \text{const}$. where p is the pressure, V is the volume of the gas and γ is a constant. Find the radius R of the gas bubble at any time t after the explosion, taking R_0 as the radius when $t=0$.

At time t , when the gas bubble has radius R , let $\epsilon \geq R$ be the radius of a concentric spherical surface in the water. Since the water is incompressible, by eqn of continuity the no

\therefore the water is incompressible,
by eqn of continuity,

the mass of fluid leaving the fluid elt $\{$ = $\{$ the mass of fluid entering the fluid elt

$$\rho(4\pi R^2) \dot{R} = \rho(4\pi \epsilon^2) \dot{\epsilon}$$

$$\frac{\dot{\epsilon}}{\dot{R}} = \frac{R^2 \dot{R}}{\dot{\epsilon}}$$

where $\dot{\epsilon}$ & \dot{R} are radial velocities.

The spherical co-ordinates are (\vec{r}, θ, ψ) on the sphere of radius \vec{r} . The bubble changes shape with spherical symmetry, hence the flow is irrotational and there is a velocity potential:

If $\phi(\vec{r}, t)$ is the velocity potential, then $\vec{v} = -\nabla \phi$

We know that,

$$\nabla \phi = \hat{e}_r \frac{\partial \phi}{\partial r} + \hat{e}_\theta \frac{\partial \phi}{\partial \theta} + \frac{\hat{e}_\psi}{r \sin \theta} \frac{\partial \phi}{\partial \psi} = \frac{\partial \phi}{\partial r} \hat{e}_r$$

Here,

$$\nabla \phi = \frac{\partial \phi}{\partial \vec{r}} = \frac{1}{r} + \frac{1}{r^2}$$

$$\therefore \vec{v} = -\frac{\partial \phi}{\partial \vec{r}} = \frac{R^2 \vec{R}}{r^2}$$

$$\text{Then } (\phi =) - \int \frac{R^2 \vec{R}}{r^2} dr$$

$$= + \frac{R^2 \vec{R}}{r^2}$$

The most general form of Bernoulli's eqn is

$$\frac{1}{2} \vec{q}^2 + \sigma + \int \frac{dp}{\rho} - \frac{\partial \phi}{\partial t} = f(t)$$

for an inviscid flow, where

where $\vec{q} = -\nabla \phi$ is the velocity

$\vec{F} = -\nabla \sigma$ is the conservative body forces

(r, θ, t) are variables, ϕ is the pressure

ρ is the density

$f(t)$ is an arb. constant

Here the flow is unsteady, the fluid is incompressible with no body forces, the Bernoulli's eqn can be written as

$$\frac{1}{2} \vec{v}^2 + \phi + \int \frac{dp}{\rho} - \left(\frac{\partial \phi}{\partial t} \right)_{\vec{x}} = f(t)$$

$$\frac{1}{2} \vec{v}^2 + \frac{1}{\rho} \int p \cdot \left(\frac{\partial \phi}{\partial t} \right)_{\vec{x}} = f(t)$$

$$\frac{1}{2} \vec{v}^2 + \frac{p}{\rho} - \left(\frac{\partial \phi}{\partial t} \right)_{\vec{x}} = f(t)$$

Assume pressure to be 0 at ∞ ,

$$\frac{p}{\rho} + \frac{1}{2} \frac{R^4 \vec{v}^2}{x^4} - \frac{1}{\vec{x}} \frac{\partial}{\partial t} (R^2 \vec{v}) = 0$$

Hence, sub in ②,

$$\frac{3}{2} R^2 + \frac{R}{2} \frac{d}{dR} (R^2) = \left(\frac{R_0}{R} \right)^{3/2} \frac{P}{\rho}$$

$$\frac{d}{dR} (R^2) + 3 \frac{R^2}{R} = \frac{2P}{\rho} \frac{R_0^{3/2}}{(R)^{3/2+1}}$$

R^3 is an integrating factor for the above

eqn.

Multiplying it throughout gives,

$$R^3 \frac{d}{dR} (\dot{R}^2) + 3R^2 \ddot{R}^2 = \frac{2P}{\rho} \frac{R_0^{3\gamma} R^3}{R^{3\gamma+1}}$$

$$\frac{d}{dR} (R^3 \dot{R}^2) = \frac{2P}{\rho} \frac{R_0^{3\gamma}}{R^{3\gamma-2}}$$

Integrating from R_0 to R ,

$$R^3 \dot{R}^2 = \frac{2P}{\rho} R_0^{3\gamma} \left[\frac{R}{-3\gamma+3} \right]_R^{R_0}$$

$$= \frac{-2P}{3\rho} \frac{R_0^{3\gamma}}{(\gamma-1)} \left(R^{-3(\gamma-1)} - R_0^{-3(\gamma-1)} \right)$$

$$= \frac{2P}{3\rho} \frac{R_0^{3\gamma}}{(\gamma-1)} \left(\frac{R_0^{-3(\gamma-1)}}{R} - \frac{R_0^{-3(\gamma-1)}}{R_0} \right)$$

$$R^3 \dot{R}^2 = \frac{2P}{3\rho(\gamma-1)} \left[\frac{R_0^{3\gamma-3(\gamma-1)+3}}{R} - \frac{R_0^{3\gamma}}{R_0} \right] = R^{6-3(\gamma-1)}$$

$$\left(\frac{\dot{R}^2}{R} \right) = \frac{2P}{3\rho(\gamma-1)} \left[\frac{R_0^3}{R^3} - \frac{R_0^{3\gamma}}{R^{3\gamma+3}} \right]$$

$$= \frac{2P}{3\rho(\gamma-1)} \left[\left(\frac{R_0}{R} \right)^3 - \left(\frac{R_0}{R} \right)^{3\gamma} \right]$$

Putting $\lambda = R$, $\frac{P}{\rho} + \frac{R^4 \dot{R}^2}{2R^4} - \frac{1}{R} \frac{d}{dt} (R^2 \dot{R}) = 0$

$$\frac{P}{\rho} + \frac{\dot{R}^2}{2} - \frac{1}{R} \left(2 \vec{R} \cdot \ddot{\vec{R}} + R^2 \vec{R} \cdot \vec{R} \right) = 0$$

$$\frac{P}{\rho} + \frac{\dot{R}^2}{2} - \left(2 \vec{R} \cdot \ddot{\vec{R}} + R^2 \vec{R} \cdot \vec{R} \right) = 0$$

$$\frac{P}{\rho} = \left(\frac{3 \dot{R}^2}{2} + \vec{R} \cdot \ddot{\vec{R}} \right)$$

$$P = \rho \left(\frac{3 \dot{R}^2}{2} + \vec{R} \cdot \ddot{\vec{R}} \right) \rightarrow (*)$$

Considering the boundary conditions in the above eqn, we see the ' P ' is also the pressure in the gas.

Let P be the pressure in the bubble at $t=0$ when $R=R_0$.

Then using the adiabatic property, law,

$$P \left(\frac{4}{3} \pi R^3 \right)^{\gamma} = \text{const} = P \left(\frac{4}{3} \pi R_0^3 \right)^{\gamma}$$

$$\frac{P}{P} = \left(\frac{R_0^3}{R^3} \right)^{\gamma} = \left(\frac{R_0}{R} \right)^{3\gamma}$$

Sub. in $(*)$,

$$P \left(\frac{R_0}{R} \right)^{3\gamma} = \rho \left(\frac{3}{2} \dot{R}^2 + \vec{R} \cdot \ddot{\vec{R}} \right) \rightarrow (**)$$

\ddot{R} can be expressed as

$$\ddot{R} = \dot{R} \left(\frac{d\dot{R}}{dR} \right) \quad \left[\dot{R} \left(\frac{d\dot{R}}{dR} \right) = \frac{dR}{dt} \left(\frac{d}{dR} \left(\frac{dR}{dt} \right) \right) \right.$$

$$= \frac{d}{dR} \left(\frac{1}{2} \dot{R}^2 \right) \quad \left. = \frac{d^2 R}{dt^2} = \ddot{R} \right]$$

In the special case, when $\gamma = \frac{4}{3}$

$$\dot{R}^2 = \frac{2P}{3 \left[\frac{4}{3} - 1 \right] \rho} \left[\left(\frac{R_0}{R} \right)^3 - \left(\frac{R_0}{R} \right)^4 \right]$$

$$\dot{R} = \frac{dR}{dt} = \left\{ \frac{2P}{\rho} \left[\left(\frac{R_0}{R} \right)^3 - \left(\frac{R_0}{R} \right)^4 \right] \right\}^{1/2}$$

$$\frac{dR}{dt} = \left[\frac{2PR_0^3}{\rho R^4} (R - R_0) \right]^{1/2}$$

$$= \left[\frac{2PR_0^3(R - R_0)}{\rho} \right]^{1/2} \frac{1}{R^2}$$

$$= \frac{R^2 dR}{\left[\frac{2PR_0^3(R - R_0)}{\rho} \right]^{1/2}}$$

Sub. $R = R_0 + x$, we get on integration,

$$dt = \int \frac{(R_0 + x)^2 dx}{\left[\frac{2PR_0^3}{\rho} x \right]^{1/2}} \quad \text{with } R = R_0 + x \quad dR = dx$$

$$\begin{aligned}
 t &= \int \frac{\frac{R_o^2 + x^2 + 2R_o x}{x^{y_2}} \left(\frac{2PR_o}{e}\right)^{-\frac{1}{2}} dx}{\left(\frac{R_o^2 + x^2 + 2R_o x}{x^{y_2}}\right)^{\frac{1}{2}}} \\
 &= \int \left(\frac{R_o^2}{x^{y_2}} + x^{\frac{3}{2}} + 2R_o x^{\frac{1}{2}} \right) \left(\frac{2PR_o}{e}\right)^{-\frac{1}{2}} dx \\
 &= \left(2R_o^2 x^{\frac{y_2}{2}} + \frac{2}{5} x^{\frac{5}{2}} + \frac{4}{3} R_o x^{\frac{3}{2}} \right) \left(\frac{2PR_o}{e}\right)^{-\frac{1}{2}} \\
 &= \left[R_o^2 + \frac{x^{\frac{5}{2}-\frac{1}{2}}}{5} + \frac{2}{3} R_o x^{\frac{3}{2}-\frac{1}{2}} \right] \left(\frac{2PR_o}{e}\right)^{-\frac{1}{2}} \\
 &= \left(R_o^2 + \frac{x^2}{5} + \frac{2}{3} R_o x \right) \left(\frac{2ex}{2PR_o}\right)^{\frac{y_2}{2}} \\
 &= \left(R_o^2 + \frac{x^2}{5} + \frac{2R_o x}{3} \right) \left(\frac{2ex}{2PR_o}\right)^{\frac{y_2}{2}}
 \end{aligned}$$

3.3) Axi-Symmetric flow:

(Continued)

Stokes Stream Function

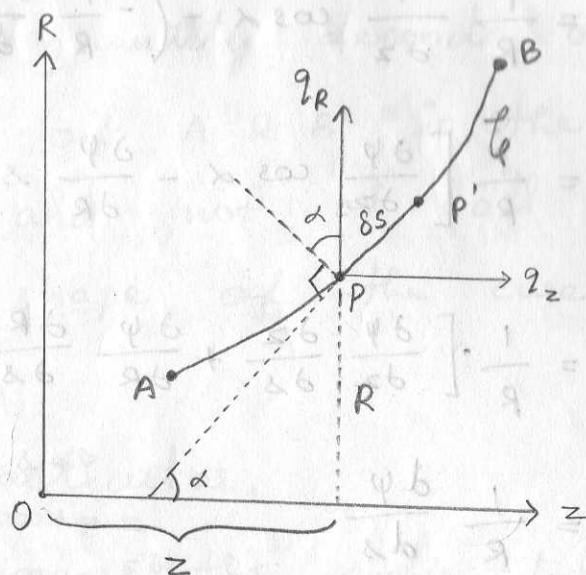
Physical Meaning for ψ :

Consider the axi-symmetric flow about the meridian plane, $\theta = 0$.

In this type of flow there is no velocity component \perp to the meridian plane.

↳ (f)

Fig (*)



In the fig, let \widehat{AB} be an arc of the plane curve, P be a point with distance R from Oz and z from OR .

Let PP' be of length ss such that P' is a neighbouring point of P .

We need to find

the volume of fluid crossing the surface of revolution AB about Oz per unit time from right to left.

Let α be the angle with tangent at P to the curve C with Oz . The normal component of velocity at P from right to left is given by

$$q_R \cos \alpha + q_z \cos(90 + \alpha)$$

$$= q_R \cos \alpha - q_z \sin \alpha = 46 \text{ m/s}$$

$$= \frac{1}{R} \frac{\partial \psi}{\partial z} \cos \alpha - \left(-\frac{1}{R} \frac{\partial \psi}{\partial R} \right) \sin \alpha$$

$$= \frac{1}{R} \left[\frac{\partial \psi}{\partial z} \cos \alpha - \frac{\partial \psi}{\partial R} \sin \alpha \right]$$

$$= \frac{1}{R} \left[\frac{\partial \psi}{\partial z} \frac{\partial z}{\partial s} + \frac{\partial \psi}{\partial R} \frac{\partial R}{\partial s} \right]$$

$$= \frac{1}{R} \frac{\partial \psi}{\partial s}$$

$$l = s \quad \theta = \alpha$$

$$z = l \cos \alpha \quad R = s \sin \alpha$$

$$\frac{\partial z}{\partial s} = \cos \alpha \quad \frac{\partial R}{\partial s} = \sin \alpha$$

$$\text{For } s \rightarrow 0, \frac{\partial \psi}{\partial s} = \frac{1}{R} \frac{\delta \psi}{\delta s} \quad \left[\because \lim_{\delta s \rightarrow 0} \frac{\delta \psi}{\delta s} = \frac{d\psi}{ds} \right]$$

The volume of fluid crosses the surface of revolution at PP' about Oz per unit time is

$$\frac{1}{R} \frac{\delta \psi}{\delta s} \cdot 2\pi R \cdot \delta s$$

and pressure built up is

$$= \frac{\delta \psi}{\delta s} \cdot 2\pi \delta s$$

$$\delta \psi = \psi_{P'} - \psi_P$$

$$= 2\pi \delta \psi \quad \text{where } \delta \psi = \psi_{P'} - \psi_P$$

Hence the total volume of fluid crossing the surface of revolution of AB about Oz per unit time from left to right is

$$\int_A^B 2\pi \delta \psi = 2\pi [\psi_B - \psi_A]$$

This quantity depends only on the positions of A & B in the meridian section and not at all dependent on the shape of the curve, ^{le} for particular.

In particular,

Suppose the curve falls on the oz axis, it is convenient to consider,

$$\psi_A = 0$$

So that the volume crossing the surface of revolution of AP about oz per unit time from right to left is

$$2\pi [\psi_p - \psi_A] = 2\pi [\psi_p - 0] (\because \psi_A = 0)$$

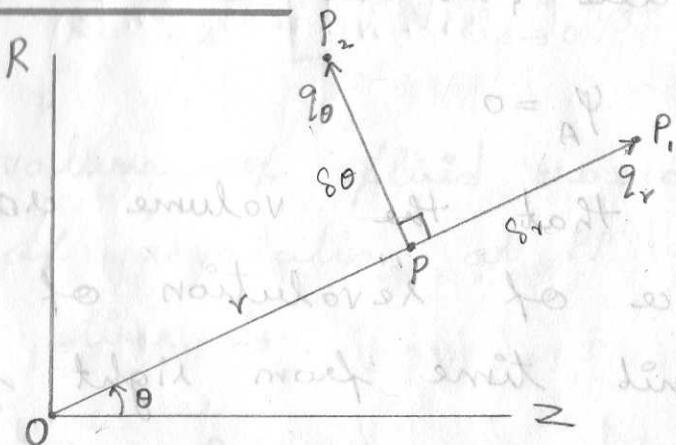
$$= 2\pi \psi (\because \psi_p = \psi)$$

Note:

The dimensions of ψ are, $L^3 T^{-1}$ from eqn ② & those of the velocity potential is $L^2 T^{-1}$. Also from (f), there is no fluid that crosses a stream and hence $\psi = \text{const}$ along stream line. Also $\psi = \text{const.}$

over a stream surface, whose where
 stream surface is the surface obtained
 by the surface of the revolution of
 the stream line about the axis of
 symmetry.

Velocity components in terms of spherical
 polar co-ordinates:



($\theta = \alpha$:) [$\theta - \varphi$] Fig. (*) [$\psi - \varphi$] It is
 The fig shows ^{the} a meridian section
 through the axis of the symmetry.

Let (P) be a pt at a distance r
 from O & at angular distance θ
 from Oz. The azimuthal coordinates is
 redundant.

The fluid velocity components at P are
 in q_x along OP & q_θ at slight angles to it
 in the sense of α^i .

The length

$$PP_1 = s_x$$

$$PP_2 = 2s_\theta$$

ned
of

1) If $\delta s = \delta x$, then the area of surface of revolution of δs about Oz is

$$2\pi x \sin \theta \delta x.$$

Volume of fluid crossing this per unit time over

$$\left. \begin{array}{l} \text{Volume of fluid} \\ \text{crossing this per unit time} \end{array} \right\} = 2\pi x \sin \theta q_0.$$

So if ψ is the stream fn at P,

$$\text{then } 2\pi x \sin \theta q_0 = 2\pi x \sin \theta \cdot x \sin \theta q_0.$$

$$q_0 = \frac{1}{x \sin \theta} \frac{\partial \psi}{\partial x} \rightarrow ③$$

2) If $\delta s = x \delta \theta$, then the area of surface of revolution of δs about Oz is

$$2\pi x \sin \theta (x \delta \theta) = 2\pi x^2 \sin \theta \delta \theta.$$

Volume of fluid crossing this per unit time

$$\left. \begin{array}{l} \text{Volume of fluid crossing} \\ \text{this per unit time} \end{array} \right\} = 2\pi x^2 \sin \theta \cdot x \sin \theta (-q_r).$$

If ψ is the stream fn at P,

$$\text{then } 2\pi x \sin \theta q_0 = 2\pi x^2 \sin \theta \sin \theta q_r.$$

$$q_r = \frac{-1}{x^2 \sin \theta} \frac{\partial \psi}{\partial \theta} \rightarrow ④$$

Some Special Forms of the Stream

function for Axi-Symmetric Irrotational

Motions:

i) Uniform Stream:

Suppose we have a flow where the velocity is $-U\hat{k}$, where U is a constant. Let P be the point in the stream having cylindrical polar coordinates $P(R, \theta, z)$ and let P_0 be its projection on the z -axis.

Taking ψ to be the stream function associated with P and zero so that for P_0 , since the volume flowing from right to left through the circular disc obtained by revolving PP_0 about the z -axis is $\pi R^2 U$, it follows that

$$2\pi\psi = \pi R^2 U$$

$$\psi = \frac{1}{2} R^2 U$$

This is expressible in spherical polar coordinates, taking $R = r \sin \theta$ where $r = OP$.

If Simple Works Substitute the value of R ,

we get

$$\psi = \frac{1}{2} (r \sin \theta)^2 U$$

$$= \frac{U}{2} r^2 \sin^2 \theta$$

ii) Simple Source:

For a simple source of strength m at the origin the value of ψ at P is obtained from ③ & ④.

In the spherical coordinate notation used

$$q_x = \frac{m}{x^2}, q_0 = 0$$

Using ③ & ④,

$$q_x = \frac{-1}{x^2 \sin\theta} \frac{\partial \psi}{\partial \theta}$$

$$q_0 = \frac{1}{x \sin\theta} \frac{\partial \psi}{\partial x}$$

$$\therefore \frac{m}{x^2} = \frac{-1}{x^2 \sin\theta} \frac{\partial \psi}{\partial \theta} + \frac{1}{x \sin\theta} \frac{\partial \psi}{\partial x} = 0$$

$$\Rightarrow \frac{\partial \psi}{\partial \theta} = -m \sin\theta \quad \frac{\partial \psi}{\partial x} = 0$$

$$\text{Hence } d\psi(x, \theta) = \frac{\partial \psi}{\partial x} dx + \frac{\partial \psi}{\partial \theta} d\theta$$

$$= 0 dx + (-m \sin\theta) d\theta$$

Integrating,

$$\psi(x, \theta) = -m \int \sin\theta d\theta$$

$$= -m(-\cos\theta)$$

$$= m \cos\theta$$

$$= (x, \theta) \psi_b$$

$$= \left(\frac{\sin\theta \cos M}{x} \right) + \left(\frac{\sin\theta M}{x} \right)$$

iii) Doublet at O, Axis along \overline{Oz} : (ii)

In spherical polar coordinates, the velocity potential at P is ~~is~~ $\frac{M \cos \theta}{r^2}$ half period

$$\phi(r, \theta) = \frac{M \cos \theta}{r^2}$$

where M is the strength of the doublet.

$$q_r = -\frac{\partial \phi}{\partial r}$$

$$q_\theta = \frac{-1}{r} \frac{\partial \phi}{\partial \theta}$$

$$= -M \cos \theta (-2r^{-3})$$

$$= \frac{-1}{r} \frac{M}{r^2} (-\sin \theta)$$

$$= 2M \cos \theta r^{-3}$$

$$= \frac{M \sin \theta}{r^3}$$

$$= \frac{2M \cos \theta}{r^3}$$

Also,

$$q_r = \frac{-1}{r^2 \sin \theta} \frac{\partial \psi}{\partial \theta}$$

$$q_\theta = \frac{1}{r \sin \theta} \frac{\partial \psi}{\partial r}$$

$$\therefore \frac{2M \cos \theta}{r^3} = \frac{-1}{r^2 \sin \theta} \frac{\partial \psi}{\partial \theta} \quad \frac{M \sin \theta}{r^3} = \frac{1}{r \sin \theta} \frac{\partial \psi}{\partial r}$$

$$\frac{\partial \psi}{\partial \theta} = -\frac{2M \cos \theta \sin \theta}{r^2} \quad \frac{\partial \psi}{\partial r} = \frac{M \sin^2 \theta}{r^2}$$

Hence

$$d\psi(r, \theta) = \frac{\partial \psi}{\partial r} dr + \frac{\partial \psi}{\partial \theta} d\theta$$

$$= \frac{M \sin^2 \theta}{r^2} dr + \left(-\frac{2M \cos \theta \sin \theta}{r} \right) d\theta$$

Integrating,

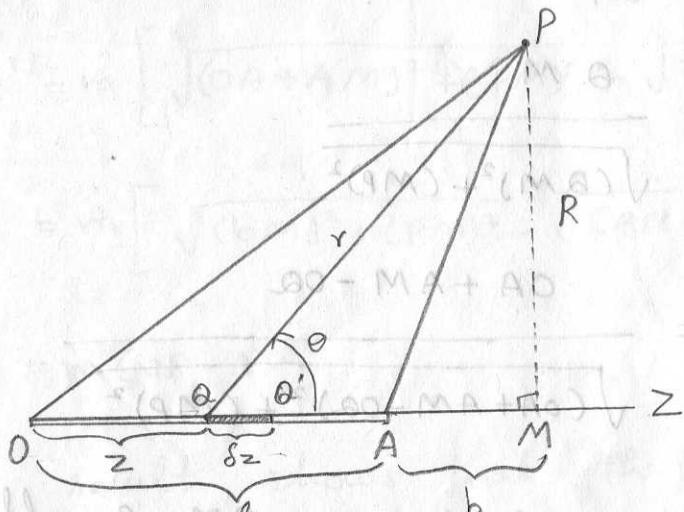
$$\psi(x, \theta) = M \sin^2 \theta \int x^{-2} dx - \frac{2M}{x} \int \sin \theta \cos \theta dx$$

$$= M \sin^2 \theta \left(-\frac{1}{x}\right) - \frac{2M}{x} \int x dx \quad x = \sin \theta \\ = M \sin^2 \theta \left(\frac{-1}{x}\right) - \frac{2M}{x} \frac{\sin^2 \theta}{2}$$

$$= -\frac{2M}{x} \sin^2 \theta \quad \text{Let } x = \sin \theta = \psi$$

Let.

iv) Uniform line source along \overline{Oz} :



The fig. depicts uniform line source of fluid extending along \overline{Oz} from \overline{O} to \overline{A} .

Let $\overline{aa'}$ be the neighbouring points on \overline{OA} .

$$\therefore OQ = z, QQ' = \delta z \quad \text{Let } \overline{OP} = r \quad \text{and } \overline{PA} = \theta$$

$$QQ' = z + \delta z$$

Also,

Suppose $\overline{QP} = r$ and $\overline{PAA'} = \theta$.

If m denotes the strength per unit length of the line source, then $\overline{aa'}$ is

effectively a simple source, at Q of strength $m\delta z$.

Hence the contribution to ψ at P from this source is $\delta\psi$.

If we equal,

$$\delta\psi = m\delta z \cos\theta \quad [\text{using (ii)}]$$

$$\cos\theta = \frac{QM}{QP}$$

$$= \frac{QM}{\sqrt{(QM)^2 + (MP)^2}}$$

$$= \frac{OA + AM - OQ}{\sqrt{(OA + AM - OQ)^2 + (MP)^2}}$$

Denoting $OA = l$, $AM = b$, $PM = R$ all of which are constant elements

$$\cos\theta = \frac{l+b-z}{\sqrt{(l+b-z)^2 + R^2}}$$

$$u = (l+b-z)^2 + R^2$$

$$\delta\psi = m\delta z \frac{l+b-z}{\sqrt{(l+b-z)^2 + R^2}} \quad du = [2(l+b-z)(-1) + 0]dz$$

$$(l+b-z)dz = -\frac{1}{2}du$$

Integrating,

$$\psi = m \int_0^l \frac{l+b-z}{\sqrt{(l+b-z)^2 + R^2}} dz \quad z \Big|_0^l \quad u \Big|_0^l \quad \frac{l}{b^2 + R^2}$$

$$\psi = m \int_{b^2 + R^2}^{b^2 + R^2} -\frac{1}{2} \frac{1}{\sqrt{u}} du$$

$$(l+b)^2 + R^2$$

$$\psi = -m \int_{b^2+R^2}^{(l+b)^2+R^2} \frac{1}{2} u^{-\frac{1}{2}} du$$

$$= -m \left[\frac{u^{\frac{1}{2}}}{\frac{1}{2}} \right]_{b^2+R^2}^{(l+b)^2+R^2}$$

$$= -m \left[(b^2+R^2)^{\frac{1}{2}} - ((l+b)^2+R^2)^{\frac{1}{2}} \right]$$

$$= m \left[\sqrt{(l+b)^2+R^2} - \sqrt{b^2+R^2} \right]$$

$$= m \left[\sqrt{(OA+AM)^2+(PM)^2} - \sqrt{(AM)^2+(PM)^2} \right].$$

$$= m \left[\sqrt{(OM)^2+(PM)^2} - \sqrt{(AM)^2+(PM)^2} \right]$$

$$= m(OP-AP)$$

This result shows that the stream function

$\psi = \text{constant}$, $OP-AP = \text{constant}$. These are confocal hyperboloids of revolution about Oz

having O & A as foci.

v) Doublet in Uniform Stream:

Suppose the doublet specified in (iii) is in a uniform stream whose undisturbed velocity is $-U\hat{k}$.

Then combining the results of (i) & (iii), the stream function at P in spherical polar is

$$\psi(x, \theta) = \frac{1}{2} Ux^2 \sin^2 \theta - \frac{2M}{x} \sin^2 \theta$$

Thus the stream surfaces are

$$\left(\frac{1}{2} Ux^2 - \frac{2M}{x} \right) \sin^2 \theta = \text{constant}$$

In particular the surfaces for which

$\psi = 0$ are given by,

$$\sin \theta = 0 \quad ; \quad \frac{1}{2} Ux^2 - \frac{2M}{x} = 0$$

$$\theta = 0, \pi \quad ; \quad \frac{1}{2} Ux^2 = \frac{2M}{x}$$

$$x^3 = \frac{4M}{U}$$

$$\Rightarrow x = \left(\frac{4M}{U} \right)^{1/3}$$

The former is the z -axis $\theta = 0, \pi$,

the latter the sphere with centre O and

radius $\left(\frac{4M}{U} \right)^{1/3}$

Ex 5.4 Complex potential for two dimensional, irrotation, incompressible flow:

Consider an inviscid incompressible fluid having an irrotational flow.

Egn of motion is

$$\frac{1}{\rho} \frac{\partial p}{\partial t} + \nabla \cdot \bar{q} = 0$$

where \bar{q} is the velocity vector of the fluid

(i) motion is

$\therefore p$ is independent of time $\frac{\partial p}{\partial t} = 0$,

$$\therefore \nabla \cdot \bar{q} = 0 \quad \frac{1}{\rho} = (\theta, \phi) \psi$$

\therefore The flow is irrotational $\nabla \cdot \bar{q} = 0 \rightarrow (f)$

$$\Rightarrow \bar{q} = -\nabla \phi, \text{ where scalar point fn } \phi \text{ defines velocity potential.}$$

$$\therefore \nabla \cdot \bar{q} = \nabla \cdot (-\nabla \phi) = -\nabla^2 \phi = 0$$

$$\Rightarrow \nabla^2 \phi = 0 \rightarrow (1)$$

which is the eqn of motion in this case,
where the function $\phi = \phi(x, y)$

\because The flow is considered to be in
two dimensional.

Let $P(x, y)$ be any arbitrary point in
the flow \rightarrow w.r.t origin fixed in the
fluid, $\overline{OP} = z$ where $z = x + iy$, we are able
to consider the 2D flow to be expressed
on the organ plane.

For the flow defined by (f) define a
scalar point function ψ , that is differentiable
and uniform throughout the region of
the flow $\psi = \psi(x, y)$ subject to the
condition, $u = -\psi_y \& v = \psi_x$ where $\bar{q} = \bar{q}(u, v)$

ψ satisfies (f)

$$\Rightarrow \psi \text{ satisfies } \nabla^2 \psi = 0 \rightarrow (2)$$

From the description of ψ , we obtain

$$d\psi = 0$$

$\Rightarrow \psi = \psi(x, y)$ is constant

$\psi = \text{constant}$ defines stream function
in the $z = \text{constant}$ plane for an inviscid
incompressible fluid with irrotational flow.

(b) The velocity potential $\phi(x, y)$ and a stream function $\psi(x, y)$ are differentiable and also possess continuous partial derivatives everywhere in the region of flow.

$$\text{Let } \omega = \phi(x, y) + i\psi(x, y)$$

$$\text{Then } \omega = \omega(x, y)$$

$$\Leftrightarrow \omega = f(z), \text{ where } z = z(x, y)$$

At any point in the region of flow

$$\frac{d\omega}{dz} = f'(z) \text{ exists}$$

\Rightarrow It is unique & hence $\omega = f(z) + \text{will be analytic at that point.}$

defn Whenever this condition hold for every point on the region of the flow then $\omega = f(z)$ is called a "regular function" throughout the region of flow.

$$\frac{d\omega}{dz} = f(z) \text{ exists uniquely at } P \text{ means}$$

$$\lim_{\delta z \rightarrow 0} \frac{\delta \omega}{\delta z} \text{ exists.}$$

(t) $\delta \phi$ & $\delta \psi$

$$\text{i.e. } \lim_{\begin{array}{l} \delta x \rightarrow 0 \\ \delta y \rightarrow 0 \end{array}} \frac{\delta(\phi + ix)}{\delta(x+iy)} = \lim_{\begin{array}{l} \delta x \rightarrow 0 \\ \delta y \rightarrow 0 \end{array}} \frac{\delta \phi + i \delta x}{\delta x + i \delta y} \rightarrow (3)$$

$$\text{where } \delta \phi = \phi(x+\delta x, y+\delta y) - \phi(x, y)$$

$$\text{& } \delta \psi = \psi(x+\delta x, y+\delta y) - \psi(x, y)$$

with $\delta z = \delta x + i\delta y$

The limit in ③ can be computed based on the differentials δx & δy from various possible ways.

Consider the path where $x = \text{constant}$ & y varies.

$$x = \text{constant} \Rightarrow dx = 0 \Rightarrow \delta x \rightarrow 0$$

Then ③ becomes

$$\lim_{\delta z \rightarrow 0} \frac{\delta w}{\delta z} = \lim_{\substack{\delta x \rightarrow 0 \\ \delta y \rightarrow 0}} \frac{\delta \phi + i \delta \psi}{\delta x + i \delta y}$$

$$= \lim_{\delta y \rightarrow 0} \frac{\delta \phi}{i \delta y} + \frac{\delta \psi}{\delta y}$$

$$= \frac{1}{i} \lim_{\delta y \rightarrow 0} \frac{\delta \phi}{\delta y} + \lim_{\delta y \rightarrow 0} \frac{\delta \psi}{\delta y} \rightarrow ④$$

Consider the path $y = \text{constant}$ & x alone varies.

$$y = \text{constant} \Rightarrow dy = 0 \Rightarrow \delta y \rightarrow 0$$

∴ ③ becomes

$$\lim_{\delta z \rightarrow 0} \frac{\delta w}{\delta z} = \lim_{\substack{\delta x \rightarrow 0 \\ \delta y \rightarrow 0}} \frac{\delta \phi + i \delta \psi}{\delta x}$$

$$= \lim_{\delta x \rightarrow 0} \frac{\delta \phi}{\delta x} + i \lim_{\delta x \rightarrow 0} \frac{\delta \psi}{\delta x} \rightarrow ⑤$$

③ $\Rightarrow \lim_{\delta z \rightarrow 0} \frac{\delta w}{\delta z}$ exists uniquely.

$\therefore (4)$ & (5) expresses the same and hence comparing real and imaginary parts, we have

$$\lim_{\delta x \rightarrow 0} \frac{\delta \phi}{\delta x} = \lim_{\delta y \rightarrow 0} \frac{\delta \psi}{\delta y} \quad \text{as the path}$$

$$\lim_{\delta y \rightarrow 0} \frac{\delta \phi}{\delta y} = - \lim_{\delta x \rightarrow 0} \frac{\delta \psi}{\delta x} \quad \text{as the path}$$

along which the motion takes place is immaterial, we have

$$-\frac{\delta \phi}{\delta y} = \frac{\delta \psi}{\delta x} \quad \text{and} \quad$$

$$(or) \frac{\delta \phi}{\delta x} = \frac{\delta \psi}{\delta y} \quad \left. \begin{array}{l} \\ \end{array} \right\} \rightarrow (7)$$

$$\& \frac{\delta \phi}{\delta y} = -\frac{\delta \psi}{\delta x} \quad \left. \begin{array}{l} \\ \end{array} \right\}$$

i.e. $w = f(z) = \phi + i\psi$ satisfies the C-R eqns.

In a nutshell we thus find an incompressible inviscid fluid having an irrotational at every pt in the region of flow, both the velocity potential and stream function are differentiable possessing continuous partial derivatives satisfying C-R and Laplace eqn.

In this context the complex fn $w = f(z) = \phi(x, y) + i\psi(x, y)$ is defined as the complex velocity potential for the incompressible inviscid fluid having

irrotational flow. And the complex constant $w = f(z)$ is analytic in general throughout the region of the flow. This analytic function has for its real part velocity potential and for its imaginary part stream function.

Note that, $\text{ext. w.r.t. } \bar{z} = \frac{w}{\bar{z}}$

$$\begin{aligned} w &= \phi + i\psi \\ \Rightarrow \frac{dw}{dz} &= \frac{\partial \phi}{\partial x} + i \frac{\partial \psi}{\partial x} \\ &= \frac{\partial \psi}{\partial y} - i \frac{\partial \phi}{\partial y} \end{aligned}$$

$$\left(\frac{dw}{dz} = \phi_x + i\psi_x = -i\phi_y + \psi_y \right)$$

$$= \phi_x - i\psi_y = i\psi_y + \psi_x \rightarrow (8) \checkmark$$

The velocity vector \bar{q} defined by the velocity potential ϕ is

$$\bar{q} = -\nabla \phi = -\left(\frac{\partial \phi}{\partial x} \hat{i} + \frac{\partial \phi}{\partial y} \hat{j}\right)$$

$$\text{i.e. } u\hat{i} + v\hat{j} = -\left(\frac{\partial \phi}{\partial x} \hat{i} + \frac{\partial \phi}{\partial y} \hat{j}\right)$$

$$\bar{q} = \bar{q}(u, v) \Rightarrow u = -\frac{\partial \phi}{\partial x} \quad v = -\frac{\partial \phi}{\partial y} \rightarrow (9)$$

$\therefore (8)$ becomes

$$\begin{aligned} \frac{dw}{dz} &= \phi_x - i\phi_y = -u + iv \text{ using (9)} \\ &= (-u) - i(-v) \end{aligned}$$

$\omega = \frac{dw}{dz} = +\sqrt{(u^2 + v^2)}$
 Let $w = u + iv$ is the speed of
 fluid at $P(x, y)$.

Stagnation pts are obtained when
 when $\frac{dw}{dz} = 0$. Thus the complex potentials
 enable us to determine and characterise
 an irrotational 2D flow of an inviscid
 incompressible fluid.

Discuss the flow described by $\omega = z^2$

Soln:

The complex volume potential ϕ is defined
 by $\omega = \nabla \phi$ where ϕ is the volume potential
 and ψ is the stream function where $z = x + iy$.

$$\omega = z^2 = (x+iy)^2 = x^2 - y^2 + i2xy - \text{2D, Izz. flow}$$

$$\rightarrow \nabla^2 \phi = 0, \nabla^2 \psi = 0$$

Incomp. $\nabla \cdot \phi$

$$\frac{\partial}{\partial x} (x^2 - y^2) + \frac{\partial}{\partial y} (2xy) = 2x - 2y$$

$$P \leftarrow \frac{\partial}{\partial x} (2x - 2y) + \frac{\partial}{\partial y} (2x - 2y) = 2 + 2 = 0 = P$$

$$\Rightarrow \nabla^2 \phi = 0$$

∴ $\nabla^2 \phi = 0$

$$\nabla^2 \phi = \rho b i - \frac{\omega b}{\rho} = \frac{\omega b}{\rho}$$

$$(v-i) - (u-i) =$$

Eg:

Discuss the flow described by $\omega = z^2$.

Soln:

The complex velocity potential ω is defined by $\omega = \phi + i\psi$ where ϕ is velocity potential & ψ is stream function where $z = x + iy$.

$$\omega = z^2 = (x+iy)^2 = x^2 - y^2 + i2xy$$

$$\phi = x^2 - y^2$$

$$\psi = 2xy$$

$$\nabla^2 \phi = \frac{\partial^2}{\partial x^2} (x^2 - y^2) + \frac{\partial^2}{\partial y^2} (x^2 - y^2) = 2 + (-2) = 0$$

$$\nabla^2 \psi = \frac{\partial^2}{\partial x^2} (2xy) + \frac{\partial^2}{\partial y^2} (2xy) = 0 + 0 = 0$$

$$\nabla \times \phi = \begin{vmatrix} \hat{i} & \hat{j} & \hat{k} \\ \frac{\partial}{\partial x} & \frac{\partial}{\partial y} & \frac{\partial}{\partial z} \\ x^2 & -y^2 & 0 \end{vmatrix}$$

$$\nabla \times \psi = \begin{vmatrix} \hat{i} & \hat{j} & \hat{k} \\ \frac{\partial}{\partial x} & \frac{\partial}{\partial y} & \frac{\partial}{\partial z} \\ 2x & 2y & 0 \end{vmatrix}$$

$$= \hat{i}(0) - \hat{j}(0) + \hat{k}(0)$$

$$= \vec{0}$$

Equipotentials are given by

$$\phi = \text{constant}$$

$$\Rightarrow x^2 - y^2 = \text{const} = c \rightarrow ①$$

$$\Rightarrow \frac{x^2}{c} - \frac{y^2}{c} = 1$$

and streamlines are given by

$$\psi = \text{constant}$$

$$\Rightarrow xy = \text{const} = d \rightarrow ②$$

⑩ By eqn ①,

$$① \Rightarrow \frac{x^2}{c} - \frac{y^2}{c} = 1 \text{ is a hyperbola.}$$

∴ ② $\Rightarrow xy = d$ is a rectangular hyperbola.

Asymptotes for the hyperbola $x^2 - y^2 = c$ is

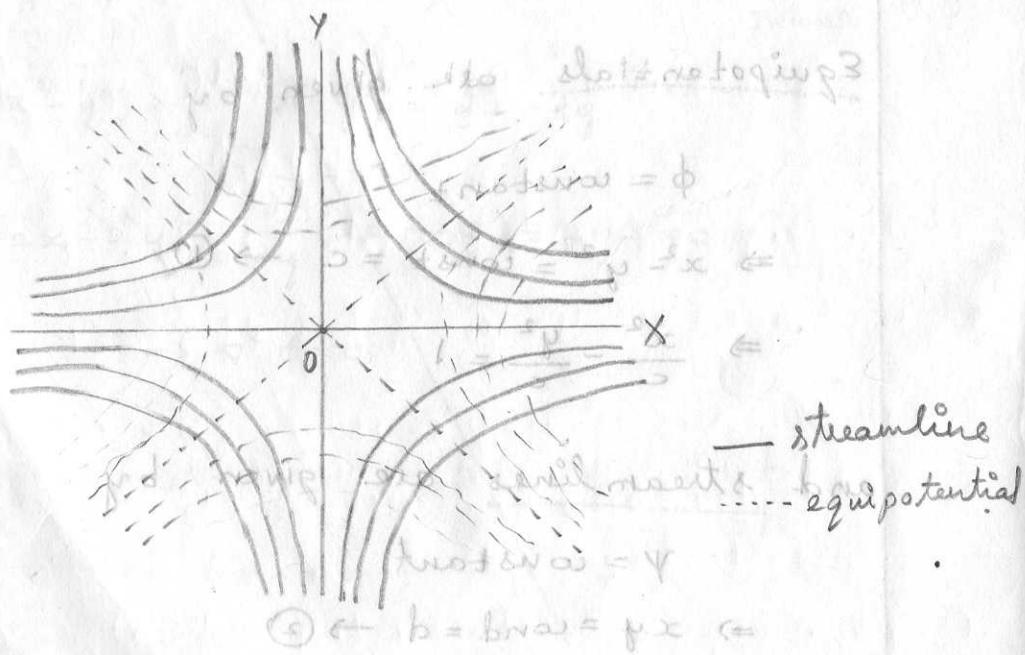
given by $x^2 - y^2 = 0 \Rightarrow \left\{ \begin{array}{l} x = \pm y \\ y = \pm x \end{array} \right. \quad \text{③}$

Asymptotes to the rectangular hyperbola

$xy = d$ is given by $xy = 0 \Rightarrow \left\{ \begin{array}{l} x = 0 \text{ or } y = 0 \\ \text{ & axes } y = \pm x \end{array} \right. \quad \text{④}$

i.e., Axes of ① are asymptotes of ② &
asymptotes of ② are axes of ①.

③ & ④ \Rightarrow equipotentials are orthogonal to streamlines.



Stagnation pts are obtained when $\frac{dw}{dz} = 2z = 0$

Origin is the stagnation pt of the flow & speed of the fluid is given by

$$\left| \frac{dw}{dz} \right| = |2z| = 2|z| = 2(\sqrt{x^2 + y^2})$$

which is speed of the fluid at any pt $P(x, y)$.

Unit

4.1) Complex Velocity Potentials for Standard 2-D Flows:

We shall consider some common type of 2D flows, namely flow due to stream a uniform stream, to a line source & sink, and a line doublet and some properties related to them. (III flow only).

1) Uniform Stream:

Case (i):

Consider a uniform stream having velocity $-U\hat{i}$.

$$\text{i.e. } \vec{g} = -U\hat{i} + 0\hat{j} + 0\hat{k}$$

$$\nabla \times \vec{g} = \begin{vmatrix} \hat{i} & \hat{j} & \hat{k} \\ \frac{\partial}{\partial x} & \frac{\partial}{\partial y} & \frac{\partial}{\partial z} \\ -U & 0 & 0 \end{vmatrix} = \hat{i}(0) - \frac{\partial U}{\partial z}\hat{j} + \frac{\partial(-U)}{\partial z}\hat{k} = 0$$