

LECTURES

# 5, 6

CY11001  
Spring 2018

- Joule-Thompson Effect
- Second Law of Thermodynamics



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## Variation of enthalpy with $T$ and $p$

$$H = f(p, T)$$

$$dH = \left( \frac{\partial H}{\partial p} \right)_T dp + \left( \frac{\partial H}{\partial T} \right)_p dT$$

$$= \left( \frac{\partial H}{\partial p} \right)_T dp + C_p dT$$

Constant  $p$  process

$$dH_p = C_p dT$$

Constant  $T$  process

$$dH_T = \left( \frac{\partial H}{\partial p} \right)_T dp$$

Special case: Ideal gas

For ideal gas

$$\left( \frac{\partial H}{\partial p} \right)_T = 0 \quad \left( \frac{\partial H}{\partial V} \right)_T = 0$$

$$dH = C_p dT \quad \text{for ideal gas}$$

# Joule-Thompson Experiment:

Purpose is to determine

$$\left( \frac{\partial H}{\partial p} \right)_T$$

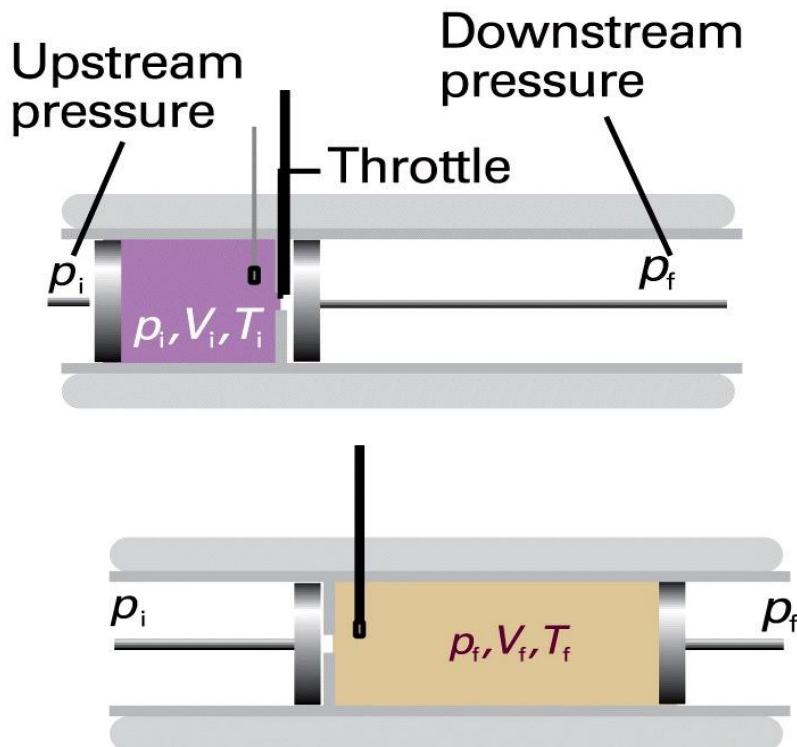


Figure 2-28  
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In this experiment

$$q = 0 \quad w = -p_f(V_f - 0) - p_i(0 - V_i) = p_i V_i - p_f V_f$$

$$\Delta U = U_f - U_i = q + w = -p_f V_f + p_i V_i$$

$$U_f + p_f V_f = U_i + p_i V_i$$

$$H_f = H_i, \Delta H = 0$$

**Isenthalpic process**  
**(Constant H)**

$$H = f(p, T); \quad dH = \left( \frac{\partial H}{\partial p} \right)_T dp + \left( \frac{\partial H}{\partial T} \right)_p dT$$

$$\left( \frac{\partial H}{\partial p} \right)_T = - \left( \frac{\partial H}{\partial T} \right)_p \left( \frac{\partial T}{\partial p} \right)_H = -C_p \times \mu_{JT}$$

Joule-Thompson Coefficient,

$$\mu_{JT} = \left( \frac{\partial T}{\partial p} \right)_H \approx \left( \frac{\Delta T}{\Delta p} \right)$$

Ratio of change in  $T$  to the  $p$  when a gas expands under constant  $H$ .

$$dH = -\mu_{JT} C_p dp + C_p dT$$

# Inversion Temperature and Cooling of gases with JT expansion:

$$\mu_J = \left( \frac{\partial T}{\partial V} \right)_U \quad \mu_{JT} = \left( \frac{\partial T}{\partial p} \right)_H \quad \mu_T = \left( \frac{\partial H}{\partial p} \right)_T = -C_p \mu_{JT}$$

Isothermal Joule-Thomson Coefficient

Sign of  $\mu_{JT}$   
 For ideal gas  $\mu_{JT} = 0$   
 For real gas  $\mu_{JT} \neq 0$

Some inversion temperatures are (at 1 atm):

He	40 K
Ne	231 K
N <sub>2</sub>	621 K
O <sub>2</sub>	764 K

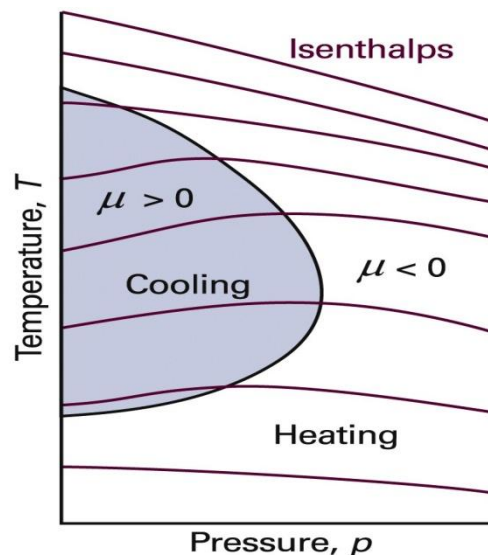
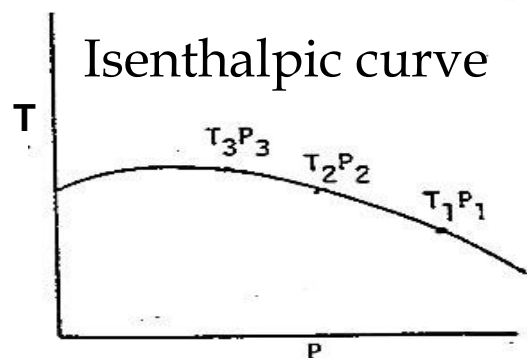
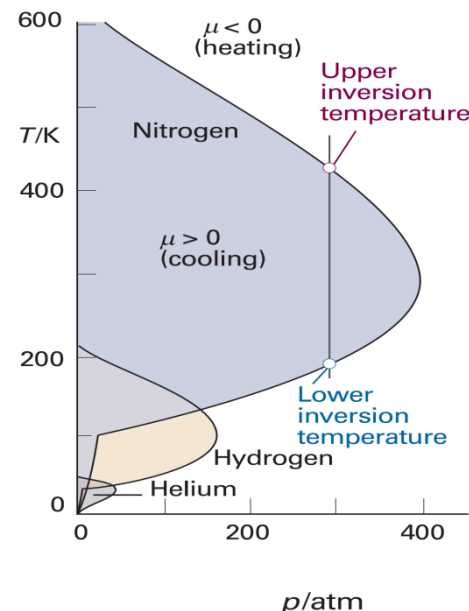


Figure 2-31  
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At room temperature and 1 atmp, N<sub>2</sub> and O<sub>2</sub> will cool upon expansion while He and Ne will warm upon expansion.

# Calculation of thermodynamic functions for various processes

	reversible <i>phase change</i> at const. $T, p$	const $p$ heating, no phase change	const $V$ heating, no phase change
$w$	$-\int p \, dV = -p\Delta V$	$-\int p \, dV = -p\Delta V$	0
$q$	latent heat	$q_p = \Delta H$	$q_V = \Delta U$
$\Delta U$	$q + w$	$q + w$	$= \int C_V(T) dT$
$\Delta H$	$q (=q_p)$	$= \int C_p(T) dT$	$\Delta U + V\Delta p$

# Calculation of thermodynamic function for various processes for ideal gas

	state 1 – state 2, no phase change			rev, isothermal	rev, adiabatic
	rev	rev, const ext. $p$	irrev, const final $p$		
$w$	$-\int p dV$	$-p_{ex} \Delta V$	$-p_f \Delta V$	$-nRT \ln \frac{V_2}{V_1}$	$= \int C_V(T) dT$
$q$	$\Delta U - w$			$nRT \ln \frac{V_2}{V_1}$	0
$\Delta U$	$= \int C_V(T) dT$			0	$= \int C_V(T) dT$
$\Delta H$	$= \int C_p(T) dT$			0	$= \int C_p(T) dT$

Adiabatic expansion of a perfect gas into vacuum

$$q = 0 \quad \Delta U = 0 \quad w = 0 \quad \Delta H = 0$$

# Limitations of the First Law of Thermodynamics

The first law assures us that the total energy of system plus surroundings remains constant during the reaction. Energy can be transferred/transformed, keeping the total energy fixed.

$$dU_{\text{universe}} = dU_{\text{system}} + dU_{\text{surrounding}} = 0$$

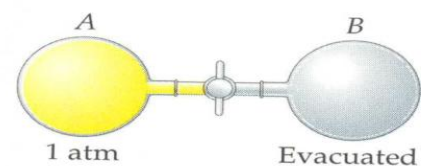
Does not say:

Whether energy will get transferred / transformed?

If yes, in which direction?

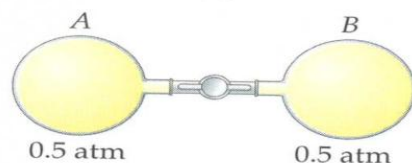
If yes, how long?

If yes, how fast?

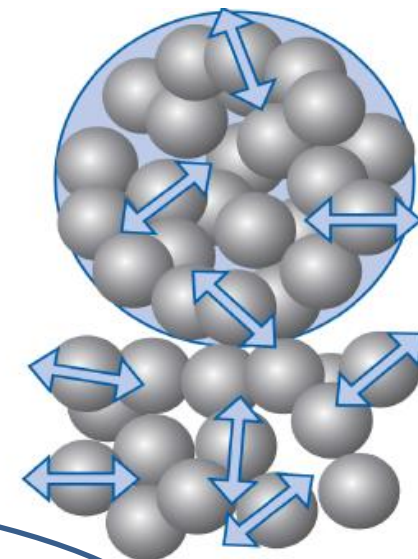
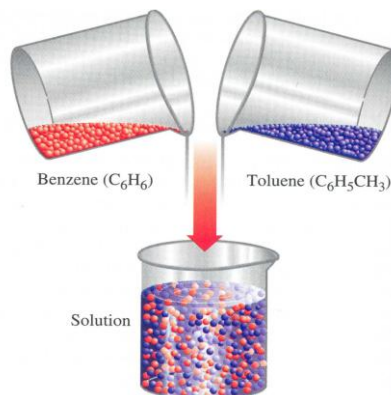
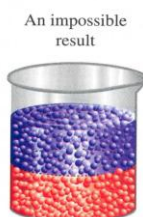


(a)

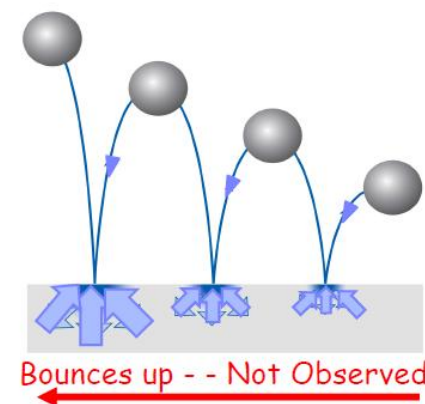
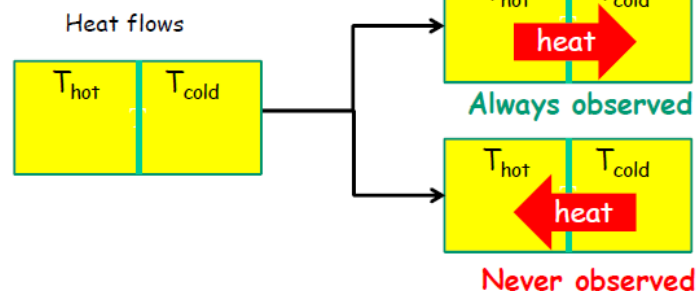
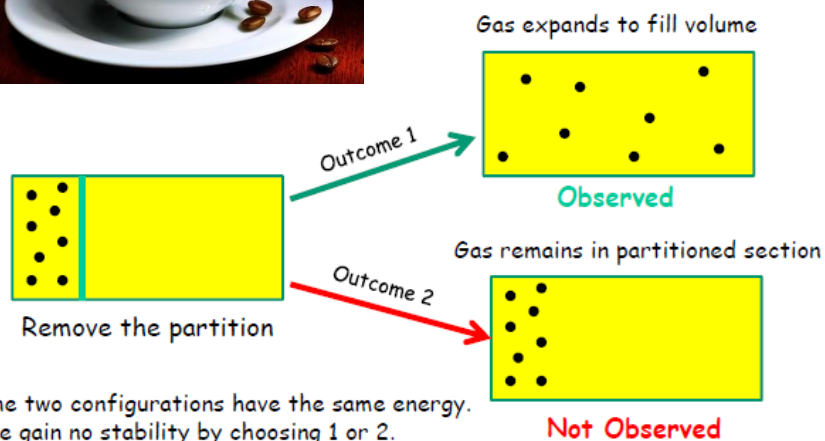
Spontaneous  
↕  
Not spontaneous



(b)



In all the cases first law *allows* either outcomes, but we observe only one outcome *spontaneously*.





## Spontaneity:

A spontaneous process occurs naturally and needs no external source of work. A non-spontaneous process, although allowed by first law of TD, requires an external source of work to drive it.

**Who drives, a spontaneous process?**

# Entropy

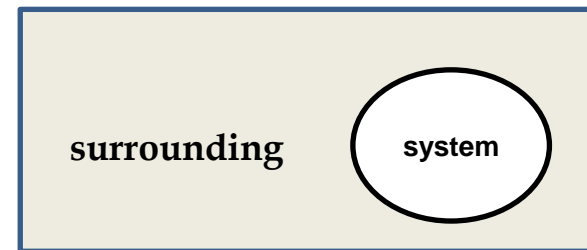
- The thermodynamic property of a system that is related to its degree of randomness or disorder is called **entropy (S)**.
- The **entropy  $S$**  and the **entropy change  $\Delta S = S_2 - S_1$**  are **state functions**.
- The **entropy  $S$**  has a unique value, once the pressure  $p$ , the temperature  $T$  and the composition  $n$  of the system are specified,  $S=S(p,T,n)$ .
- The **entropy is an extensive property**, i.e., increases with the amount of matter in the system.  $S_m = S/n$  (molar entropy).

# Thermodynamic definition of entropy

$dS_{\text{syst}}$  = Change in entropy that occurs during a chemical or physical process

=  $dq_{\text{rev}} / T$  ( $q_{\text{rev}}$  is the heat supplied reversibly)

$$\Delta S_{\text{system}} = \int_1^2 \frac{dq_{\text{rev}}}{T}$$



For surroundings,

$$dS_{\text{surr}} = - dq / T_{\text{surr}}$$

$$\Delta S_{\text{surr}} = \frac{-q}{T_{\text{surr}}}$$

Large change in entropy occurs when heat is dissipated to surrounding at low temperature.

# How do you calculate entropy change?

## For surrounding

$$dS_{surr} = - dq / T_{surr}$$

$$\Delta S_{surr} = \frac{-q}{T_{surr}}$$



Calculate the actual  $q$  for the process from state 1 to state 2 and apply the above formula

## For system

- Find out state 1 and state 2
- Construct reversible pathway(s) from state 1 and state 2
- Apply the formula

$$\Delta S = \int_1^2 \frac{dq_{rev}}{T}$$

• Calculate the entropy change in the surroundings when 1.0 mole of  $\text{H}_2\text{O}(\text{l})$  is formed from its elements under standard conditions at  $25^\circ \text{C}$  (298.15 K).



## Calculation of Entropy Changes (A few special cases)

$$\Delta S_{\text{system}} = \int_1^2 \frac{dq_{\text{rev}}}{T}$$

1. Cyclic Process  $\Delta S_{\text{syst}} = 0$  ( $S$  is a state function)

2. Reversible adiabatic process  $\Delta S_{\text{syst}} = 0$  ( $dq_{\text{rev}} = 0$ )

3. Reversible phase-change at constant  $p$  and  $T$

$$\Delta S_{\text{syst}} = \int_1^2 \frac{dq_{\text{rev}}}{T} = \frac{1}{T} \int_1^2 dq_{\text{rev}} = \frac{q_{\text{rev}}}{T} = \frac{\Delta H}{T}$$

4. Constant  $p$  heating (reversibly) with no phase change:

$$dq_{\text{rev}} = dq_p = C_p dT \quad \Delta S_{\text{syst}} = \int_{T_1}^{T_2} \frac{dq_{\text{rev}}}{T} = C_p \int_{T_1}^{T_2} \frac{dT}{T} = C_p \ln \left( \frac{T_2}{T_1} \right)$$

5. Reversible isothermal process:

$$\Delta S_{\text{syst}} = \int_1^2 \frac{dq_{\text{rev}}}{T} = \frac{1}{T} \int_1^2 dq_{\text{rev}} = \frac{q_{\text{rev}}}{T}$$

6. For ideal gas:

$$dS = \frac{dq_{\text{rev}}}{T} = \frac{dU - w_{\text{rev}}}{T} = \frac{C_V dT + p dV}{T} = C_V \frac{dT}{T} + nR \frac{dV}{V}$$

$$\Delta S = C_V \ln \frac{T_2}{T_1} + nR \ln \frac{V_2}{V_1}$$

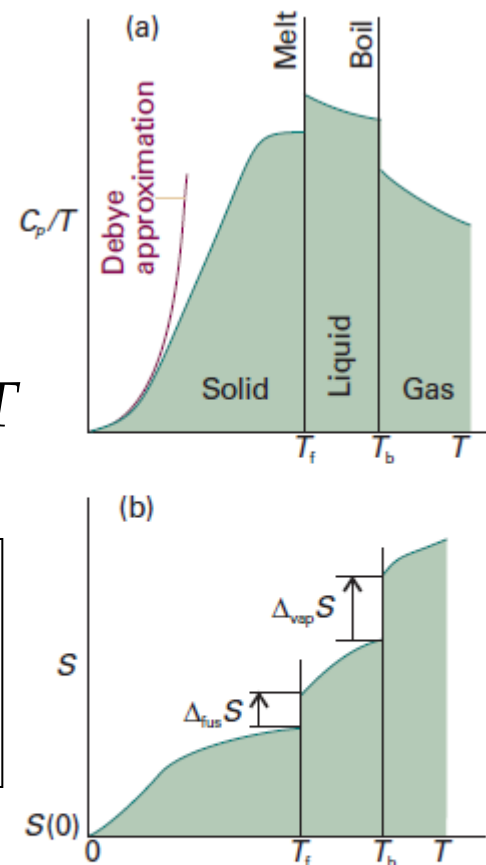
$$\Delta S = C_p \ln \frac{T_2}{T_1} + nR \ln \frac{p_1}{p_2}$$

# Calculation of Entropy at *any* temperature

Heating at constant pressure/Volume

$$\Delta S_p = \int \frac{C_p}{T} dT = C_p \ln \frac{T_2}{T_1}$$
$$\Delta S_V = \int \frac{C_V}{T} dT = C_V \ln \frac{T_2}{T_1}$$

Debye approx:  
 $C_p \propto T^3$  at low  $T$



Entropy at any temperature,

$$S(T) = S(0) + \int_0^{T_f} \frac{C_p^{(s)}}{T} dT + \frac{\Delta H_{\text{fus}}}{T_{\text{fus}}} + \int_{T_f}^{T_b} \frac{C_p^{(l)}}{T} dT + \frac{\Delta H_{\text{vap}}}{T_{\text{vap}}} + \int_{T_b}^T \frac{C_p^{(g)}}{T} dT$$

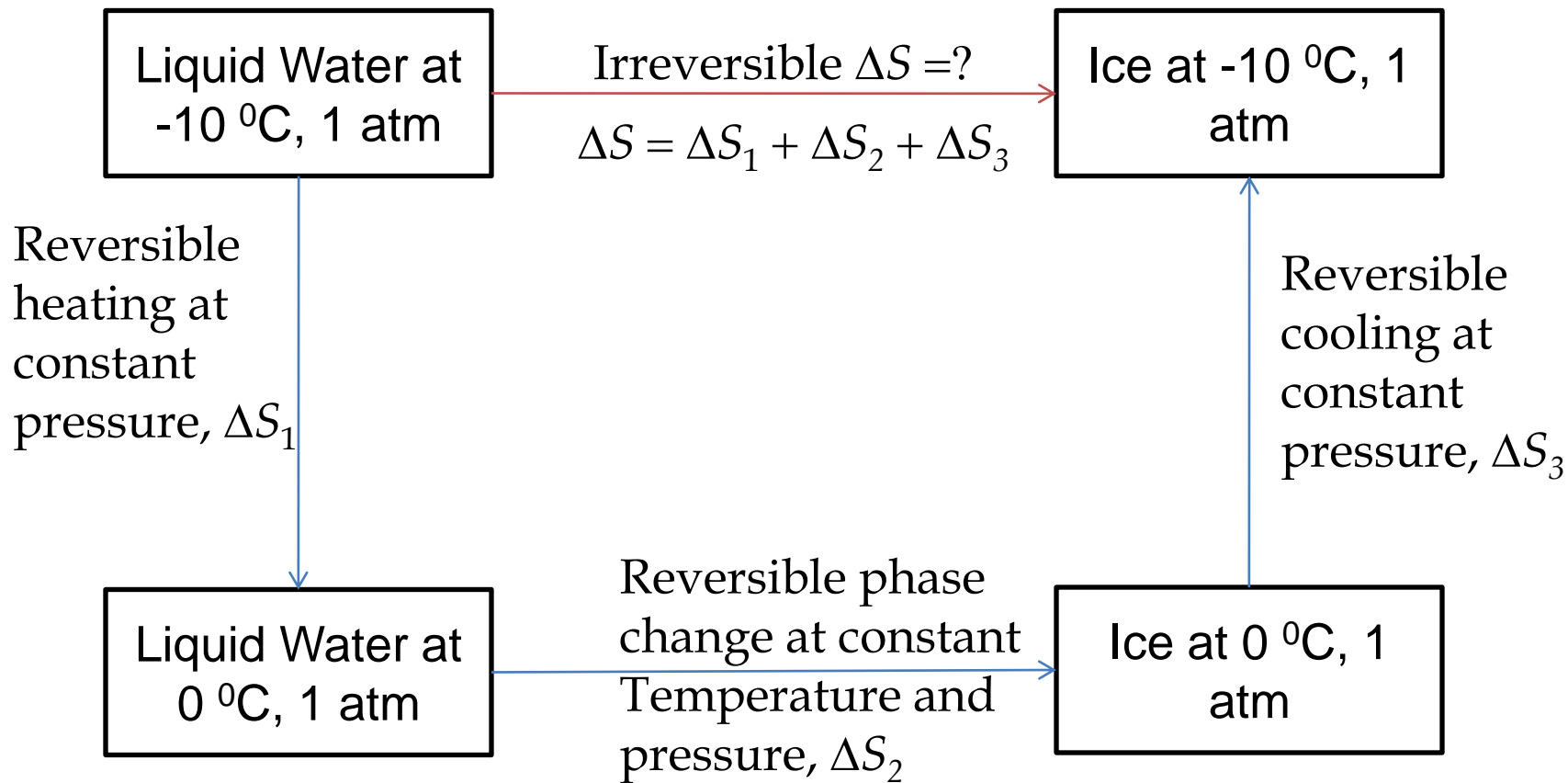
**Fig. 3.14** The calculation of entropy from heat capacity data. (a) The variation of  $C_p/T$  with the temperature for a sample. (b) The entropy, which is equal to the area beneath the upper curve up to the corresponding temperature, plus the entropy of each phase transition passed.

## Trouton's Rule

A wide range of liquid give approx. the same standard entropy of vaporization  $\sim 85 \text{ J K}^{-1} \text{ mol}^{-1}$ . Exception: water, it is  $109 \text{ J/K/mol}$

# Construction of Reversible Steps to Describe an Irreversible Process:

Example 1:

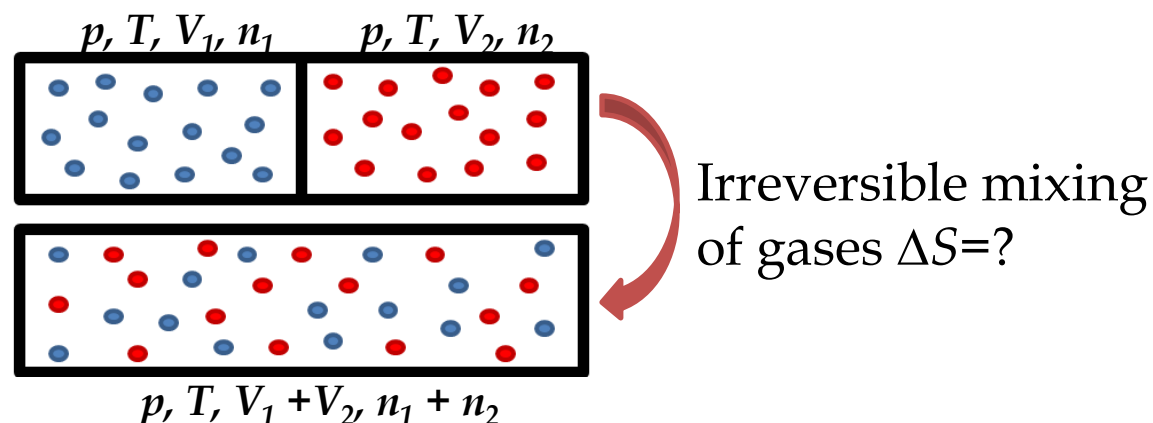


Home work

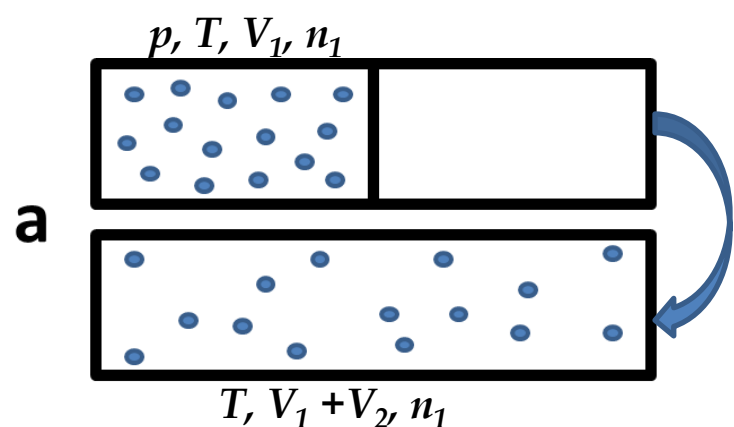
Entropy is an extensive property.  $\Delta S = \Delta S_1 + \Delta S_2 + \Delta S_3$

# Construction of Reversible Steps to Describe an Irreversible Process:

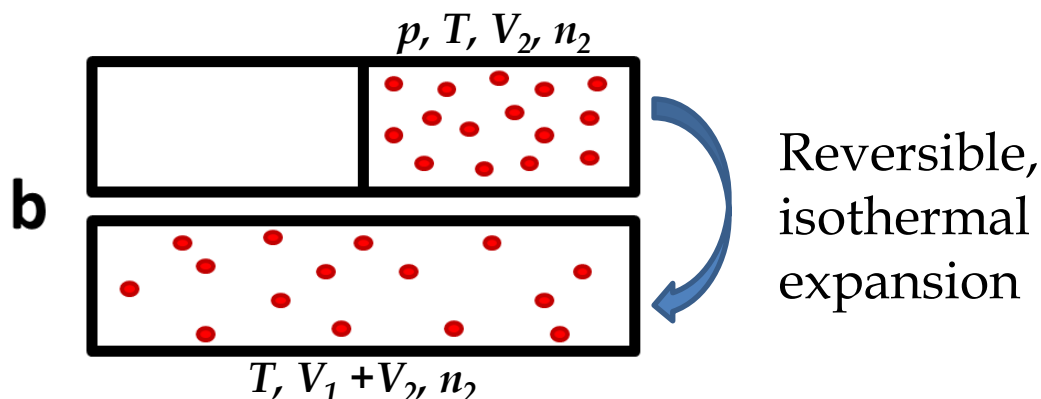
## Example 2: Entropy of Mixing of ideal gases



$$\Delta S_{\text{mix}} = \Delta S_1 + \Delta S_2$$



$$\Delta S_1 = n_1 R \ln \frac{V_1 + V_2}{V_1}$$

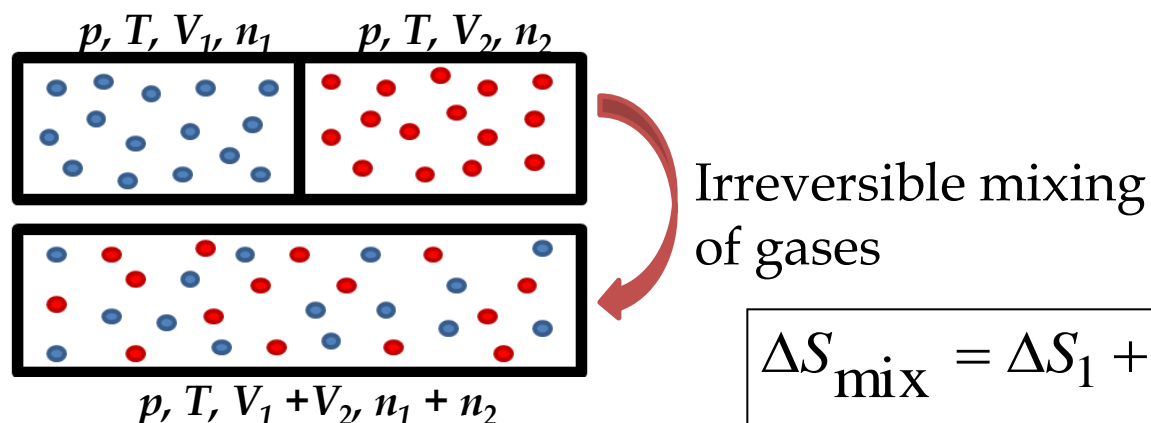


$$\Delta S_2 = n_2 R \ln \frac{V_1 + V_2}{V_2}$$



# Construction of Reversible Steps to Describe an Irreversible Process:

## Example 2: Entropy of Mixing of ideal gases



Irreversible mixing  
of gases

$$\Delta S_{\text{mix}} = \Delta S_1 + \Delta S_2$$

$$\Delta S_1 = n_1 R \ln \frac{V_1 + V_2}{V_1}, \Delta S_2 = n_2 R \ln \frac{V_1 + V_2}{V_2}$$

$$\frac{V_1}{V_1 + V_2} = \frac{\frac{n_1 RT}{p}}{\frac{n_1 RT}{p} + \frac{n_2 RT}{p}} = \frac{n_1}{n_1 + n_2} = X_1$$

$$\Delta S_{\text{mix}} = -n_1 R \ln X_1 - n_2 R \ln X_2$$

$$= -nR(X_1 \ln X_1 + X_2 \ln X_2)$$

\*Find out  $X_1$  for  
which  $\Delta S_{\text{mix}}$  is  
maximum.

Home work