

EXAMPLE — RATE OF HEAT CONDUCTION IN PIPES

CH9

2% (FALL 1993 FE)

4 copper tube, 5 cm inside diameter and 5 mm in wall thickness, is carrying a refrigerant at -30°C . The pipe is covered with two layers of insulating material. The thickness of the inner and outer layers are 1 cm and 2 cm, respectively. The thermal conductivity of the inner layer is 0.3 W/mK . The material for the outer layer is polyurethane foam. The temperature at the outside surface of the foam layer is 10°C .

- Calculate the rate of heat flow per unit length of pipe without any insulation, assuming that the outside surface of the uninsulated pipe is at 0°C .
- Calculate the rate of heat flow per unit length of the insulated pipe.
- Calculate the amount of heat loss in one day from a 100 m long insulated pipe.
- Calculate the temperature at the interface between the two insulation layers.

FORMULA SHEET (continued)

Thermal Expansion of Solids

$$\alpha_L = \frac{1}{L} \frac{dL}{dT}$$

Heat Conduction

Fourier's Law

$$Q = -\kappa A \frac{dT}{dx} = -\kappa A \frac{\Delta T}{\Delta x}$$

Composite Planar Wall

$$Q = \frac{-A \Delta T}{\left[\frac{\Delta x_1}{\kappa_1} + \frac{\Delta x_2}{\kappa_2} + \frac{\Delta x_3}{\kappa_3} + \dots \right]}$$

Simple Cylinder

$$Q = \frac{-2\pi\kappa L \Delta T}{\ln\left(\frac{r_2}{r_1}\right)}$$

Composite Cylinder (Pipe)

$$Q = \frac{-2\pi L \Delta T}{\frac{\ln(r_2/r_1)}{\kappa_1} + \frac{\ln(r_3/r_2)}{\kappa_2} + \frac{\ln(r_4/r_3)}{\kappa_3} + \dots}$$

Stress and Strain in Solids

Normal Stress

$$\epsilon = \frac{1}{E} \sigma$$

$$\nu = -\frac{\epsilon_x}{\epsilon_y}$$

$$\epsilon_x = \frac{1}{E} \sigma_x - \frac{\nu}{E} (\sigma_y + \sigma_z)$$

$$\epsilon_y = \frac{1}{E} \sigma_y - \frac{\nu}{E} (\sigma_x + \sigma_z)$$

$$\epsilon_z = \frac{1}{E} \sigma_z - \frac{\nu}{E} (\sigma_y + \sigma_x)$$

Bulk Modulus for Volume Change

$$\frac{\Delta V}{V} = -\frac{P}{K}$$

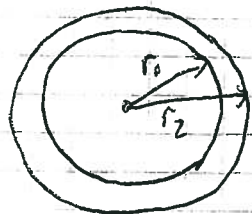
$$K = \frac{E}{3(1-2\nu)}$$

Shear Stress

$$\tau = G\gamma$$

$$G = \frac{E}{2(1+\nu)}$$

A) a) Heat flow/unit length in uninsulated pipe



inside diameter = 5 cm $\rightarrow r_1 = 2.5 \times 10^{-2} \text{ m}$

Thickness = 5 mm $\equiv 5 \times 10^{-3} \text{ m} \rightarrow r_2 = r_1 + t$

$r_2 = 2.5 \times 10^{-2} \text{ m} + 5 \times 10^{-3} \text{ m}$

$T_1 = 273.15 - 30 = 243.15 \text{ K}$

$r_2 = 3.0 \times 10^{-2} \text{ m}$

$T_2 = 273.15 \text{ K}$

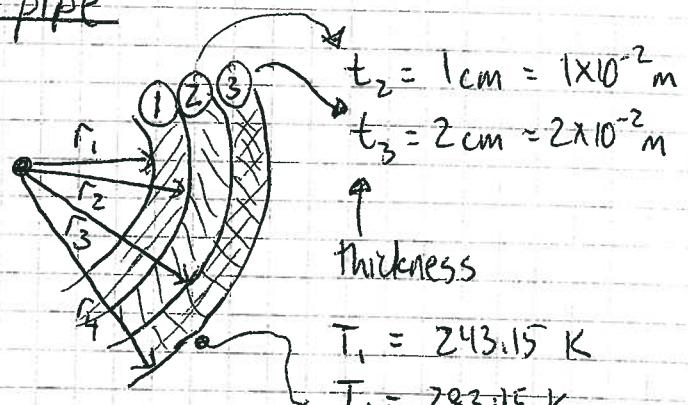
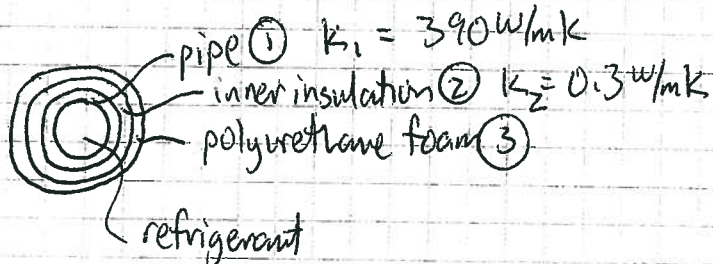
Copper tube Thermal conductivity (TABLE 9-3) $k = 390 \text{ W/mK}$

$$Q = \frac{2\pi L k (T_1 - T_2)}{\ln(r_2/r_1)} \rightarrow \frac{Q}{L} = \frac{2\pi k (T_1 - T_2)}{\ln(r_2/r_1)}$$

$$\frac{Q}{L} = \frac{2\pi \times 390 \text{ W/mK} (243.15 - 273.15 \text{ K})}{\ln(3.0 \times 10^{-2} \text{ m} / 2.5 \times 10^{-2} \text{ m})} = -403206 \frac{\text{W}}{\text{m}}$$

$\frac{Q}{L} = -403 \frac{\text{kW}}{\text{m}} \rightarrow \text{negative means heat loss}$

b) Heat flow/unit length insulated pipe



pipe ① $k_1 = 390 \text{ W/mK}$
inner insulation ② $k_2 = 0.3 \text{ W/mK}$
polyurethane foam ③

$r_1 = 2.5 \times 10^{-2} \text{ m}$ (2.5 cm)
 $r_2 = 3.0 \times 10^{-2} \text{ m}$ (3.0 cm)

$r_3 = r_2 + t_2 = 3.0 \times 10^{-2} \text{ m} + 1 \times 10^{-2} \text{ m} = 4 \times 10^{-2} \text{ m}$ (4 cm)

$r_4 = r_3 + t_3 = 4 \times 10^{-2} \text{ m} + 2 \times 10^{-2} \text{ m} = 6 \times 10^{-2} \text{ m}$ (6 cm)

$T_1 = 243.15 \text{ K}$

$T_4 = 283.15 \text{ K}$

(10°C)

Polyurethane foam Thermal conductivity (TABLE 9-3) $k_3 = 0.05 \text{ W/mK}$

$$Q = \frac{-2\pi L \Delta T}{\frac{\ln(r_2/r_1)}{k_1} + \frac{\ln(r_3/r_2)}{k_2} + \frac{\ln(r_4/r_3)}{k_3}}$$

$\Delta T = T_4 - T_1$

$\Delta T = 283.15 - 243.15$

$\Delta T = 40 \text{ K}$

$$\frac{Q}{L} = \frac{-2\pi(40\text{K})}{\frac{\ln\left(\frac{3.0 \times 10^{-2}\text{m}}{2.5 \times 10^{-2}\text{m}}\right)}{390\text{W/mK}} + \frac{\ln\left(\frac{4 \times 10^{-2}\text{m}}{3 \times 10^{-2}\text{m}}\right)}{0.3\text{W/mK}} + \frac{\ln\left(\frac{6 \times 10^{-2}\text{m}}{4 \times 10^{-2}\text{m}}\right)}{0.05\text{W/mK}}}$$

$$\boxed{\frac{Q}{L} = -27.71 \frac{\text{W}}{\text{m}}} \quad \leftarrow \text{Much less than the uninsulated pipe!}$$

c) Heat loss from 100 m of insulated pipe in one day

$$\frac{Q}{L} = -27.71 \frac{\text{W}}{\text{m}} \rightarrow Q = (-27.71 \frac{\text{W}}{\text{m}})(100\text{m}) = -2771 \text{ W}$$

$$Q = -2771 \frac{\text{J}}{\text{s}} \quad \text{one day} = 24\text{h} \times 60 \frac{\text{min}}{\text{h}} \times 60 \frac{\text{s}}{\text{min}} = 86400\text{s}$$

$$\text{Heat loss} = -2771 \frac{\text{J}}{\text{s}} \times 86400\text{s} = \boxed{-239 \text{ MJ}} \quad (-239 \times 10^6 \text{ J})$$

d) Calculate temperature at interface between insulation layers

(see diagram for b))

Overall Rate of heat loss Q = Heat loss rate through each layer

$$Q = Q_1 = Q_2 = Q_3 \quad \text{Need } T_3 \text{ between layer 2 and layer 3}$$

$$\frac{Q_3}{L} = \frac{Q}{L} = \frac{2\pi k_3(T_3 - T_4)}{\ln(r_4/r_3)} = -27.71 \frac{\text{W}}{\text{m}} = \frac{2\pi(0.05 \frac{\text{W}}{\text{mK}})(T_3 - 283.15\text{K})}{\ln(6 \times 10^{-2}\text{m}/4 \times 10^{-2}\text{m})}$$

$$\boxed{T_3 = 247.4 \text{ K} \quad (-25.8^\circ\text{C})}$$

$$T_4 = 10^\circ\text{C} \quad T_1 = -30^\circ\text{C}$$

\leftarrow Large temperature gradient in
outer polyurethane foam insulation,
(good insulator / poor conductor)