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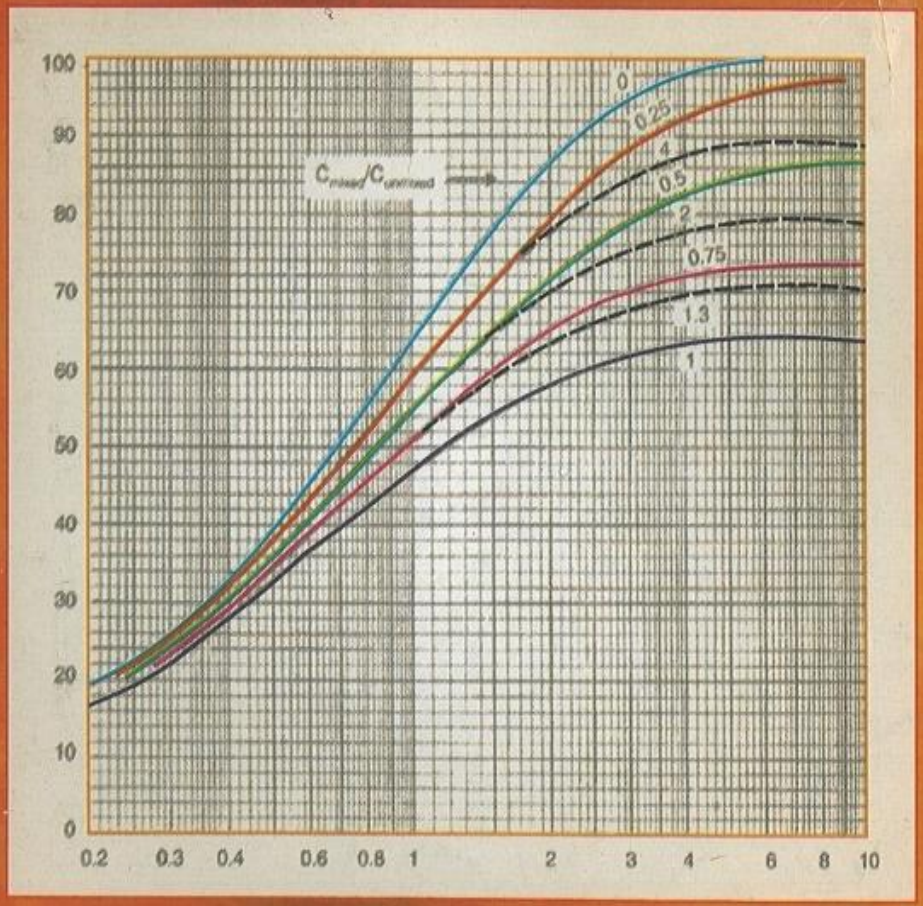
Heat and Mass Transfer Data Book



C.P. KOTHANDARAMAN • S. SUBRAMANYAN

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Heat and Mass Transfer Data Book C.P. KOTHANDARAMAN • S. SUBRAMANYAN

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Sixth Edition

Dr. C.P. Kothandaraman
Former Head of the Department of
Mechanical Engineering
PSG College of Technology, Coimbatore

Dr. S. Subramanyan
Former Principal
PSG College of Technology and
former Vice Chancellor
Bharathiar University, Coimbatore

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To the memory of

PROF. G.R. DAMODARAN

Founder Principal, PSG College of Technology

and

Vice-Chancellor. University of Madras (1978—1981)

PREFACE

The aim of this book is to present to the students, teachers and practising engineers, a comprehensive collection of various material property data and formulae in the field of heat and mass transfer. The material is organized in such a way that a reader who has gone through engineering curriculum could easily use the formulae and data presented in heat transfer calculations. Hence this compilation, intended as an adjunct to a standard text, serves as a quick reference for both the students and practising engineers in the field.

Considerable space has been devoted to property values of materials – solids, liquids and gases – that are commonly used in heat transfer situations. Property values for various materials at different temperatures are also given. They have been arranged in alphabetical order for quick reference with additions to the earlier addition.

The tabular form of presentation of the formulae with symbols, units, the limitations and restrictions in the use of empirical relationships explained alongside, has been retained, as several favourable comments have been received on this point. The empirical formulae and charts have been selected with a view of presenting information with clarity to facilitate straight forward use.

As far as possible, suggestions received since the appearance of the fifth edition have been incorporated in the new edition. A number of charts have been redrawn or added to improve clarity. To avoid ambiguity, property values have been tabulated fully without multiplication factors in the column heading.

The presentation of convection has been enlarged, taking into account the recent publications. Properties for solar application, information for the design of external finned heat exchangers and extensive emissivity values are noteworthy addition. The presentation of data and equations are presented only in SI units. However, appropriate conversion factors have been provided extensively for those who want to use MKS system of units.

The book is an outcome of the authors' teaching the subject to the undergraduate students at the PSG College of Technology for over 25 years. We hope that it serves in training the students with problems of purposeful and practical design situations. The data book has been favourably received by several Indian Universities and many of them have permitted its use in the University examinations for reference.

We acknowledge gratefully the encouragement given in our effort by Professor G.R. Damodaran to whom we dedicate this book. Our thanks are due to our former Principals, Dr. R. Subbayyan, Dr. K. Venkatraman, and Dr. A. Shanmugasundaram for the facilities afforded.

Coimbatore

C.P. Kothandaraman
S. Subramanyan

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REFERENCES

PSYCHROMETRIC CHARTS

PROPERTY VALUES OF METALS AT 20 °C OR AS INDICATED

Metal	*Density* ρ kg/m^3	*Thermal Diffusivity* $\alpha = k/\rho c$ m^2/s	*Specific Heat* c J/kgK	*Thermal Conductivity* k W/mK
Aluminium, Pure	2707	84.18×10^{-6}	896	204.2
Aluminium alloy 2024-T6 (4.5% Cu, 1.5% Mg, 0.6% Mn) *at 27°C*	2770	73.00×10^{-6}	875	177.0
Aluminium alloy 195, cast, (4.5% Cu) *at 27°C*	2790	68.20×10^{-6}	883	168.0
Aluminium Bronze, (95% Cu, 5% Al)	8666	23.30×10^{-6}	410	83.0
Al-Cu, Duralumin (94.96% Al, 3-5% Cu, trace Mg.)	2787	66.76×10^{-6}	883	164.5
Al-Mg-Si (97% Al, 1% Mg, 1% Si, 1% Mn.)	2707	73.11×10^{-6}	892	117.0
Al-Si (Alusil) (78.8% Al, 20.22% Si)	2627	71.72×10^{-6}	854	161.0
Al-Si (Silumin) (86.5% Al, 12.5% Si, 1% Cu)	2659	59.33×10^{-6}	867	136.8
ARMCO IRON (99.75% pure) *as 27°C*	7870	20.70×10^{-6}	447	72.7
Brass, (70% Cu, 30% Zn)	8522	34.12×10^{-6}	385	110.7
Brass, Red (85% Cu, 9% Sn, 6% Zn)	8714	18.04×10^{-6}	385	60.6
Bronze (75% Cu 25% Sn)	8666	8.59×10^{-6}	343	25.9
Bronze, Commercial. (90% Cu, 10% Al) *at 27°C*	8800	14.00×10^{-6}	420	52.0
Bronze, Phosphor (87% Cu, 11% Sn) *at 27°C*	8780	17.00×10^{-6}	355	54.0
Carbon steel, Plain carbon, (Mn ≤ 1%, Si ≤ 0.1%) *at 27°C*	7854	17.70×10^{-6}	434	60.5
Carbon steel, AISI 1010	7832	18.80×10^{-6}	434	63.9
Carbon-Silicon Steel, (Mn ≤ 1%, 0.1% < Si ≤ 0.6%) *at 27°C*	7817	14.90×10^{-6}	446	51.9
Carbon-Manganese-Silicon steel (1% < Mn ≤ 1.65%, 0.1% < Si ≤ 0.6%) *at 27°C*	8131	11.60×10^{-6}	434	41.0
Carbon Steel (Approxcimately 0.5%C)	7833	14.74×10^{-6}	465	53.6
Carbon Steel (Approxcimately 1.0%C)	7801	11.72×10^{-6}	473	43.3

1 W/mK = 0.86 kcal/m hr °C

1 J/kg K = 238.9 × 10^{-6} kacl/kg °C

PROPERTY VALUES OF METALS AT 20 °C OR AS INDICATED

Metal	*Density* ρ kg/m^3	*Thermal Diffusivity* $\alpha = k/\rho c$ m^2/s	*Specific Heat* c J/kgK	*Thermal Conductivity* k W/mK
Carbon Steel, (Approximately 1.5% C)	7753	9.70×10^{-6}	486	36.3
Cast iron (< 4% C)	7272	17.03×10^{-6}	420	52.0
Chromium Steel (low) $\frac{1}{2}$Cr – $\frac{1}{4}$ Mo – Si (0.18% C, 0.65% Cr, 0.23% Mo, 0.6% Si) *at 27°C*	7822	10.90×10^{-6}	444	37.7
Chromium Steel (low) 1Cr – $\frac{1}{2}$ Mo, (0.16% C, 1% Cr, 0.54% Mo, 0.39% Si) *at 27°C*	7858	12.20×10^{-6}	442	42.3
Chromium Steel (low) 1Cr – V, (0.2% C, 1.02% Cr, 0.15% V) *at 27°C*	7836	14.10×10^{-6}	443	48.9
Chrome Steel, (1% Cr)	7865	16.65×10^{-6}	461	60.6
Chrome Steel, (5% Cr)	7833	11.10×10^{-6}	461	39.8
Chrome Steel (20% Cr)	7689	6.35×10^{-6}	461	22.5
Chrome-Nickel Steel (15% Cr, 10% Ni)	7865	5.26×10^{-6}	461	19.1
Chrome-Nickel Steel (18% Cr, 8% Ni), (V2A)	7817	4.44×10^{-6}	461	16.3
Chrome-Nickel Steel (20% Cr, 15% Ni)	7833	4.15×10^{-6}	461	15.1
Chrome-Nickel Steel (25% Cr, 20% Ni)	7866	3.61×10^{-6}	461	12.8
Constantan (60% Cu, 40% Ni)	8922	6.12×10^{-6}	410	22.7
Copper, Pure	8954	112.34×10^{-6}	383	386.0
German Silver (62% Cu, 15% Ni, 22% Zn)	8618	7.33×10^{-6}	394	24.9
Invar (36% Ni)	8137	2.86×10^{-6}	461	10.7
Inconel × 750 (71% Ni, 15% Cr, 6.7% Fe) *at 27°C*	8510	11.70×10^{-6}	439	3.1
Iron, Pure	7897	20.34×10^{-6}	452	72.7

1 W/mK = 0.86 kcal/m hr °C

1 J/kg K = 238.9 × 10^{-6} kcal/kg °C

PROPERTY VALUES OF METALS AT 20 °C OR AS INDICATED *(Contd.)*

Metal	*Density* ρ kg/m^3	*Thermal Diffusivity* $\alpha = k/\rho c$ m^2/s	*Specific Heat* c $J/kg\ K$	*Thermal Conductivity* k W/mK
Lead	11393	23.43×10^{-6}	130	34.7
Magnesium, Pure	1746	97.08×10^{-6}	1013	171.3
Mg-Al (Electrolytic) (6 – 8% Al, 1.2% Zn)	1810	36.05×10^{-6}	1005	65.7
Manganese Steel (5% Mn)	7849	4.83×10^{-6}	460	22.0
Molybdenum	10220	47.90×10^{-6}	251	122.8
Nickel ; Pure (99.9%)	8906	22.66×10^{-6}	446	90.0
Nickel - Chrome (90% Ni, 10% Cr)	8666	4.44×10^{-6}	444	17.2
Nicrome (80% Ni, 20% Cr)	8314	3.43×10^{-6}	444	12.6
Nickel Steel (20% Ni)	7993	5.26×10^{-6}	461	19.1
Nickel Steel (40% Ni)	8169	2.79×10^{-6}	461	10.4
Nickel Steel (80% Ni)	8618	8.72×10^{-6}	461	34.7
Platinum, Pure *at 27°C*	21450	25.10×10^{-6}	133	71.6
Platinum-Rhodium alloy, (60%, Pt, 40% Rh) *at 27°C*	16630	17.40×10^{-6}	162	47.0
Silver, Purest	10524	170.04×10^{-6}	234	419.0
Silver, Pure (99.9%)	10525	165.63×10^{-6}	234	406.8
Silicon Steel (5% Si)	7417	5.55×10^{-6}	460	19.0
Stainless Steels, AISI 302 *at 27°C*	8055	3.91×10^{-6}	480	15.1
Stainless Steels, AISI 304 *at 27°C*	7900	3.95×10^{-6}	477	14.9
Stainless Steel AISI 316 *at 27°C*	8238	3.48×10^{-6}	468	13.4
Stainless Steel AISI 347 *at 27°C*	7978	3.71×10^{-6}	480	14.2
Tin, Pure	7304	38.84×10^{-6}	226	64.1
Tungsten	19350	62.71×10^{-6}	134	162.7
Tungsten Steel, (1% W)	7913	18.58×10^{-6}	448	65.7
Tungsten Steel, (5% W)	8073	15.25×10^{-6}	435	53.6
Tungsten Steel, (10% W)	8314	13.91×10^{-6}	419	48.5
Wrought Iron (C < 0.5%)	7849	16.26×10^{-6}	461	58.9
Zinc, Pure	7144	41.06×10^{-6}	385	112.1

1 W/mK = 0.86 kcal/m hr °C *1 J/kg K = 238.9 × 10^{-6} kcal/kg °C*

PROPERTY VALUES OF METALS AT 20°C OR AS INDICATED

Element		*Density* ρ kg/m^3	*Thermal Diffusivity* $\alpha = k/\rho c$ m^2/s	*Specific Heat* c $J/kg\,K$	*Thermal Conductivity* k W/mK
Beryllium		1850	68.30×10^{-6}	1750	205.0
Bismuth	*at 27°C*	9780	6.59×10^{-6}	122	7.9
Boron		2500	10.90×10^{-6}	1047	28.6
Cadmium		8650	48.50×10^{-6}	231	97.0
Chromium		7160	29.00×10^{-6}	440	69.8
Cobalt		8862	20.24×10^{-6}	389	69.8
Germanium	*at 27°C*	5360	34.70×10^{-6}	322	59.9
Gold		19300	126.90×10^{-6}	129	317.0
Iridium		22500	50.30×10^{-6}	130	147.0
Lithium		534	42.70×10^{-6}	339.1	68.6
Manganese		7290	2.20×10^{-6}	486	7.8
Niobium	*at 27°C*	8570	23.60×10^{-6}	265	53.7
Palladium	*at 27°C*	12020	24.50×10^{-6}	244	71.8
Platinum		21450	25.00×10^{-6}	133	69.8
Potassium		860	161.86×10^{-6}	741	100.0
Rhodium		12450	48.60×10^{-6}	248	150.0
Sodium		971	113.60×10^{-6}	1206	109.3
Silicon		2330	93.40×10^{-6}	703	153.0
Thorium		11700	39.11×10^{-6}	118	54.0
Titanium		4500	8.00×10^{-6}	611	15.12
Tungsten	*at 27°C*	19300	68.5×10^{-6}	132	174.0
Uranium		19070	12.70×10^{-6}	113	27.4
Vanadium		6100	10.30×10^{-6}	502	34.9
Zirconium		6570	12.80×10^{-6}	272	22.7

1 W/mK = 0.86 kcal/m hr °C

1 J/kg K = 238.9 × 10^{-6} kcal/kg °C

VARIATION OF THERMAL CONDUCTIVITY OF METALS WITH TEMPERATURE (W/mK) *(Contd.)*

Metal	*Temperature, °C*									
	– 100	*0*	*100*	*200*	*300*	*400*	*600*	*800*	*1000*	*1200*
Aluminium, pure	214.6	202.5	206.0	214.6	228.2	249.2	—	—	—	—
Al-Cu Duralumin, 94-96% Al, 3-5% Cu Trace Mg.	126.5	159.2	181.8	193.9	—	—	—	—	—	—
Al-Mg-Si, 97% Al, 1% Mg, 1% Si, 1% Mn	—	175	189	204	—	—	—	—	—	—
Al-Si (Alusil) 78-80 % Al, 20-22% Si	144	157	168	175	178	—	—	—	—	—
Al-Si (Silumin, Cu bearing 86.5%, Al, 12.5% Si, 1% Cu)	119.3	136.8	143.6	152.2	161.0	—	—	—	—	—
Brass, 70% Cu, 30% Zn	88.3	—	128.1	143.9	147.1	147.1	—	—	—	—
Bronze, 66.4% Cu, 31.1% Zn, 2.3% Mn	69.78	73.62	73.63	77.92	82.57	88.38	—	—	—	—
Chrome Steel, 1% Cr	—	62.3	55.4	51.9	46.8	41.5	36.3	32.9	32.9	—
Chrome Steel, 5% Cr	—	39.8	38.0	36.3	36.3	32.9	29.4	29.4	29.4	—
Chrome Steel, 20% Cr	—	22.4	22.4	22.4	22.4	24.2	24.2	25.9	29.4	—
Chrome Nickel Steel, 18% Cr, 8% Ni (V2A)	—	16.3	17.3	17.3	19.1	19.1	22.5	27.0	31.2	—
Constantan 60% Cu, 40% Ni	20.8	—	22.1	25.9	—	—	—	—	—	—
Copper, Pure	406.7	386.0	379.0	373.9	368.7	363.6	353.1	—	—	—
German Silver, 62% Cu, 15% Ni, 22% Zn	19.2	—	31.2	39.8	45.0	48.5	—	—	—	—
Iron, Pure	86.5	72.7	67.5	62.3	55.4	48.5	39.8	36.3	34.7	36.3

1 W/mK = 0.86 kcal/m hr °C

VARIATION OF THERMAL CONDUCTIVITY OF METALS WITH TEMPERATURE (W/mK) (*Contd.*)

Metal	*Temperature, °C*									
	– 100	*0*	*100*	*200*	*300*	*400*	*600*	*800*	*1000*	*1200*
Lead	36.9	35.1	33.4	31.4	29.8	—	—	—	—	—
Magnesium, Pure	178.3	171.3	167.8	162.8	157.5	—	—	—	—	—
Mg-Al (Electrolytic) 6-8%, Al, 1,2% Zn	—	52.0	62.3	74.4	83.2	—	—	—	—	—
Molybdenum	138.4	124.6	117.5	114.3	111.0	109.1	105.6	102.1	98.6	91.8
Nickel, Pure, (99.9%)	103.9	93.5	83.2	72.7	64.1	58.0	—	—	—	—
Nickel – chrome 90% Ni, 10% Cr	—	17.1	18.8	20.9	22.9	24.7	—	—	—	—
Nickel – chrome 80% Ni, 20% Cr	—	12.3	13.3	15.6	17.1	18.0	22.5	—	—	
Red Brass, 85% Cu, 9% Sn, 6% Zn	—	58.9	70.9	—	—	—	—	—	—	—
Silver, Pure (99.9%)	418.9	410	415	373.9	362.3	360.5	—	—	—	—
Steel (carbon Steel)										
Approx 0.5% C	—	55.4	51.9	48.5	45.0	41.5	34.7	31.2	29.4	31.2
Approx 1.0% C	—	43.3	43.3	41.5	39.8	36.3	32.9	29.4	27.7	29.4
Approx 1.5% C	—	36.3	36.3	36.3	34.7	32.9	31.2	27.7	27.7	29.4
Tin, Pure	74.4	65.9	58.9	57.1	—	—	—	—	—	—
Tungsten	—	166.2	150.6	141.9	133.4	126.4	112.5	76.2	—	—
Uranium	—	19.18	20.35	23.26	24.19	—	—	—	—	—
Wrought Iron C < 0.5%	—	58.9	57.1	51.9	48.5	45.0	36.3	32.9	32.9	32.9
Zinc, Pure	114.3	112.5	109.1	105.6	100.5	93.5	—	—	—	—
Zirconium	—	—	20.93	20.35	19.89	19.89	21.52	—	—	—
Zirconium 97% Tin 3%	—	—	11.98	13.26	15.54	15.58	18.02	—	—	—

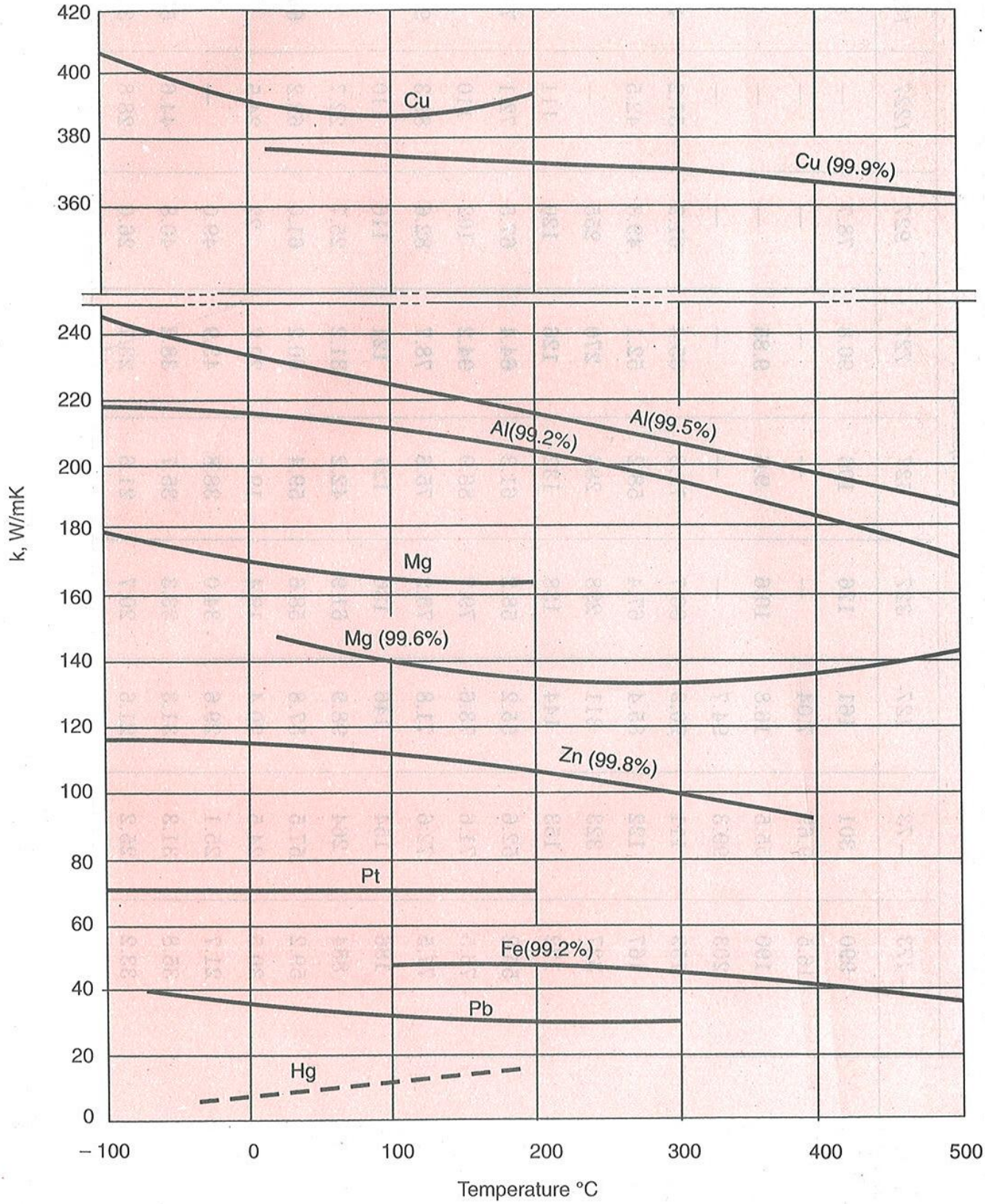
1 W/mK = 0.86 kcal/m hr °C

VARIATION OF THERMAL CONDUCTIVITY OF METALS WITH TEMPERATURE (W/mK)

Element	*Temperature, °C*								
	– 173	*– 73*	*127*	*327*	*527*	*727*	*927*	*1227*	*1727*
Beryllium	990	301	161	126	106	90.8	78.7	—	—
Bismuth	16.5	9.69	7.04	—	—	—	—	—	—
Boron	190	55.5	16.8	10.6	9.6	9.85	—	—	—
Cadmium	203	99.3	94.7	—	—	—	—	—	—
Chromium	159	111	90.9	80.7	71.3	65.4	61.9	57.2	49.4
Cobalt	167	122	85.4	67.4	58.2	52.1	49.3	42.5	—
Gold	327	323	311	298	284	270	255	—	—
Iridium	172	153	144	138	132	126	120	111	—
Niobium	55.2	52.6	55.2	58.2	61.3	64.4	67.5	72.1	79.1
Palladium	76.5	71.6	73.6	79.7	86.9	94.2	102	110	—
Platinum	77.5	72.6	71.8	73.2	75.6	78.7	82.6	89.3	99.4
Rhodium	186	154	146	136	127	121	116	110	112
Silicon	884	264	98.9	61.9	42.2	31.2	25.7	22.7	—
Tantalum	59.2	57.5	57.8	58.6	59.4	60.2	61.0	62.2	64.1
Titanium	30.5	24.5	20.4	19.4	19.7	20.7	22	24.5	—
Uranium	21.7	25.1	29.6	34.0	38.8	43.9	49.0	—	—
Vanadium	35.8	31.3	31.3	33.3	35.7	38.2	40.8	44.6	50.9
Zirconium	33.2	25.2	21.6	20.7	21.6	23.7	26.0	28.8	33.0

1 W/mK = 0.86 kcal/m hr °C

Variation of Thermal Conductivity of metals with temperature



1 W/mK = 0.86 kcal/m hr °C

VARIATION OF THERMAL CONDUCTIVITY OF SOME ALLOYS WITH TEMPERATURE (W/mK)

Alloy	*Temperature, °C*							
	– 173	*– 73*	*127*	*327*	*527*	*727*	*927*	*1227*
Aluminium alloy 2034 – 76 (4.5% Cu, 1.5% Mg, 0.6% Mn)	65	163	186	186	—	—	—	—
Aluminium alloy 195, Cast, 4.5% Cu	—	—	174	185	—	—	—	—
Commercial Bronze 90% Cu, 10% Al	—	42	52	59	—	—	—	—
Phosphor Bronze (89% Cu, 11% Sn)	—	41	65	74	—	—	—	—
ARMCO Iron	95.6	80.6	65.7	53.1	42.2	32.3	28.7	31.4
Plain Carbon Steel (Mn ≤ 1%, Si ≤ 0.1%)	—	—	56.7	48.0	39.2	30.0	—	—
AISI 110	—	—	58.7	48.8	39.2	31.3	—	—
Carbon Silicon Steel (1% < Mn ≤ 1.65%, 0.1% < Si ≤ 0.6%)	—	—	49.8	44	37.4	29.3	—	—
Carbon-Manganese-Silicon Steel (1% < Mn ≤ 1.65%, 0.1% < Si ≤ 0.6%	—	—	42.2	39.7	35.0	27.6	—	—
Low Chromium Steel ($\frac{1}{2}$ Cr – $\frac{1}{4}$ Mo – Si) (0.18% C, 0.65% Cr, 0.21% Mo, 0.6% Si)	—	—	38.2	36.7	33.3	26.9	—	—
-do- 1 Cr – $\frac{1}{2}$ Mo (0.16% C, 1% Cr, 0.54% Mo, 0.39% Si)	—	—	42.0	39.1	34.5	27.4	—	—
-do- 1Cr – V (0.2% C, 1.02% Cr, 0.15% V)	—	—	46.8	42.1	36.3	28.2	—	—
Stainless Steels, AISI 302	—	—	17.3	20.0	22.8	25.4	—	—
Stainless Steels AISI 304	9.2	12.6	16.6	19.8	22.6	25.4	28.0	31.7
Stainless Steels AISI 316	—	—	15.2	18.3	21.3	24.2	—	—
Stainless Steels AISI 347	—	—	15.8	18.9	21.9	24.7	—	—
Nicrome (80% Ni, 20% Cr)	—	—	14	16	21	—	—	—
Inconel X-750 (73% Ni, 15% Cr, rest Fe)	8.7	10.3	13.5	17.0	20.5	24.0	27.6	33.0
Platinum Rhodium Alloy (60% Pt, 40% Rh)	—	—	52	59	65	69	73	76

1 W/mK = 0.86 kcal/m hr °C

PROPERTY VALUES OF SOME NON METALLIC SOLIDS

Material	*Temperature* °C	*Thermal Conductivity* k W/mK	*Density* ρ kg/m^3	*Specific Heat* c J/kgK
Aluminium oxide, Sapphire	27	46	3970	765
Aluminium oxide, Sapphire	127	32.4	—	940
Aluminium oxide, Sapphire	327	18.9	—	1110
Aluminium oxide, Sapphire	527	13.0	—	1180
Aluminium oxide, Poly crystaline	27	36.0	3970	765
Aluminium oxide, Poly crystaline	127	26.4	—	940
Aluminium oxide, Poly crystaline	327	15.8	—	1110
Aluminium oxide, Poly crystaline	527	10.4	—	1180
Beryllium oxide	27	272.0	3000	1030
Beryllium oxide	127	196.0	—	1350
Beryllium oxide	327	111.0	—	1690
Beryllium oxide	527	70.0	—	1865
Beryllium oxide	727	47.0	—	1975
Boron fibre epoxy composite (30% Vol.)				
Parallel to fibre	27	2.29	2080	1122
Perpendicular to fibre	27	0.59	2080	1122
Carbon, Amorphous	27	1.60	1950	—
Carbon, Amorphous	127	1.89	—	—
Carbon, Amorphous	327	2.19	—	—
Carbon, Amorphous	527	2.37	—	—
Diamond type IIa, insulator	27	2300	3500	509
Diamond type IIa, insulator	127	1540	—	853
Graphite, Pyroletic, parallel to grain	27	1950	2210	709
Graphite, Pyroletic, parallel to grain	127	1390	—	992
Graphite, Pyroletic, parallel to grain	327	892	—	1406
Graphite, Pyroletic, parallel to grain	527	667	—	1650
Graphite, Pyroletic, Perpendicular to grain	27	5.70	—	—
Graphite, Pyroletic, Perpendicular to grain	127	4.09	—	992
Graphite, Pyroletic, Perpendicular to grain	327	2.68	—	1406
Graphite, Pyroletic, Perpendicular to grain	527	2.01	—	1650
Graphite fibre Epoxy Composite	27	11.10	1400	935
(25% Volume), Parallel to fibre	127	13.00	—	1216
(25% Volume), perpendicular to fibre	27	0.87	—	642
(25% Volume), perpendicular to fibre	127	1.10	—	1216
Pyroceramics, corning 9606	30	3.98	2600	808
Pyroceramics, corning 9606	127	3.64	—	908
Pyroceramics, corning 9606	327	3.28	—	1038
Pyroceramics, corning 9606	527	3.08	—	1122

1 W/mK = 0.86 kcal/m hr °C *1 J/kgK = 238.9 × 10^{-6} kcal/ kg °C* *Thermal diffusivity* $\alpha = k/\rho C$

PROPERTY VALUES OF SOME NON METALLIC SOLIDS (*Contd.*)

Material	*Temperature* °C	*Thermal Conductivity* k W/mK	*Density* ρ kg/m^3	*Specific Heat* c J/kgK
Silicon carbide	27	490	3160	675
Silicon carbide	727	87	—	1193
Silicon dioxide, Crystalline, (Quartz) Parallel to axis	27	10.4	2650	745
Parallel to axis	127	7.6	—	885
Silicon dioxide, Crystalline (Quartz) Parallel to axis	327	5.0	—	1075
Silicon dioxide, Crystalline, (Quartz) Parallel to axis	527	4.2	—	1250
Silicon dioxide, Crystalline, (Quartz) Perpendicular to grain	27	6.21	—	745
Silicon dioxide, Crystalline, (Quartz) Perpendicular to grain	127	4.70	—	885
Silicon dioxide, Crystalline, (Quartz) Perpendicular to grain	327	3.40	—	1075
Silicon dioxide, Crystalline, (Quartz) Perpendicular to grain	527	3.10	—	1250
Silicon dioxide, Poly crystalline	27	1.38	2220	745
(Fused silica)	127	1.51	—	905
(Fused Silica)	327	1.75	—	1040
(Fused Silica)	527	2.17	—	1105
Silicon Nitride	27	16	2400	691
Silicon Nitride	127	13.9	—	778
Silicon Nitride	327	11.3	—	937
Silicon Nitride	527	9.88	—	1063
Sulphur	27	0.206	2070	708
Sulphur	– 73	0.185	—	606
Thorium dioxide	27	13	9110	235
Thorium dioxide	127	10.2	—	255
Thorium dioxide	327	6.6	—	274
Thorium dioxide	527	4.7	—	285
Thorium dioxide	727	3.68	—	293
Titanium dioxide	27	8.4	4157	710
Poly Crystalline	127	7.01	—	805
Poly Crystalline	327	5.02	—	880
Poly Crystalline	527	3.94	—	910
Poly Crystalline	727	3.46	—	930

1 W/mK = 0.86 kcal/m hr °C *1 J/kg K = 238.9 × 10^{-6} kcal/kg °C* *Thermal diffusivity* $\alpha = k/\rho C$

PROPERTY VALUES OF COMMON MATERIALS

Material	*Temperature °C*	*Thermal Conductivity k W/mK*	*Density ρ kg/m³*	*Specific Heat c J/kgK*
Asphalt	27	0.062	2115	920
Bakelite	27	1.40	1300	1465
Refractory carborundum brick	599	18.5	—	—
Refractory carborundum brick	1399	11.0	—	—
Chrome brick	200	2.3	3010	835
Chrome brick	550	2.5	—	—
Chrome brick	900	2.0	—	—
Diatomaceous silica brick, fired	205	0.25	—	—
Diatomaceous silica brick, fired	872	0.30	—	—
Fire clay brick burnt at 1327°C	500	1.00	2050	960
Fire clay brick burnt at 1327°C	800	1.10	—	—
Fire clay brick burnt at 1327°C	1100	1.10	—	—
Fire clay brick burnt at 1452°C	500	1.30	2325	960
Fire clay brick burnt at 1452°C	800	1.40	—	—
Fire clay brick burnt at 1452°C	1100	1.40	—	—
Fire clay brick	205	1.00	2645	960
Fire clay brick	649	1.50	—	—
Fire clay brick	1205	1.80	—	—
Magnesite brick	205	3.8	—	1130
Magnesite brick	649	2.8	—	—
Magnesite brick	1205	1.9	—	—
Clay	27	1.3	1460	880
Coal, anthracite	27	0.26	1350	1260
Concrete (Stone mix)	27	1.40	2300	880
Cotton	27	0.06	80	—
Food materials. Banana (75.5% water content)	27	0.481	980	3350
Apple (75% water content)	27	0.513	840	3600
Cake batter	27	0.223	720	—
Fully baked cake	27	0.121	280	—
Chicken meat, white	– 75	1.60	—	—
(74.4% water content)	– 40	1.49	—	—
Chicken meat, white (74.4% water content)	– 20	1.35	—	—
Chicken meat, white (74.4% water content)	– 10	1.20	—	—
Chicken meat, white (74.4% water content)	0	0.476	—	—

1 W/mK = 0.86 kcal/m hr °C *Thermal diffusivity* $\alpha = k/\rho c$ *1 J/kg K = 238.9 × 10⁻⁶ kcal/kg °C*

PROPERTY VALUES OF COMMON MATERIALS *(Contd.)*

Material	*Temperature °C*	*Thermal Conductivity k W/mK*	*Density ρ kg/m³*	*Specific Heat c J/kgK*
Chicken meat, white (74.4% water content)	10	0.48	—	—
Chicken meat, white (74.4% water content)	20	0.489	—	—
Glass, plate (Soda lime)	27	1.4	2500	750
Pyrex glass	27	1.4	2225	835
Ice	0	1.88	920	2040
Ice	– 20	2.03	—	1945
Leather sole	27	0.159	998	—
Paper	27	0.180	930	1340
Paraffin	27	0.240	900	2890
Granite	27	2.790	2630	775
Limestone	27	2.150	2320	810
Marble	27	2.80	2680	830
Quartsite	27	5.38	2640	1105
Sand Stone	27	2.90	2150	745
Vulcanized rubber, soft	27	0.13	1100	2010
Vulcanized rubber, hard	27	0.16	1190	—
Sand	27	0.27	1515	800
Soil	27	0.52	2050	1840
Snow	0	0.049	110	—
Snow Compacted	0	0.190	500	—
Teflon	27	0.35	2200	—
Teflon	127	0.45	—	—
Human skin	27	0.37	—	—
Human fat layer	27	0.20	—	—
Human Muscle	27	0.41	—	—
Wood, cross grain				
Wood, Balso	27	0.055	140	—
Wood Cypruss	27	0.097	465	—
Wood Fir	27	0.11	415	2720
Wood Oak	27	0.17	545	2385
Wood yellow pine	27	0.15	640	2805
Wood white pine	27	0.11	435	—
Wood radial				
Wood oak	27	0.19	545	2385
Wood fir	27	0.14	420	2720

1 W/mK = 0.86 kcal/m hr °C *Thermal diffusivity* $\alpha = k/\rho c$ *1 J/kg K = 238.9 × 10⁻⁶ kcal/kg °C*

PROPERTY VALUES OF INSULATING MATERIALS AND SYSTEMS AT 27°C

Material	*Density* ρ kg/m^3	*Thermal Conductivity* k W/mK	*Specific Heat* c J/kgK
Blanket and Batt			
Glass fibre, paper based	16	0.046	—
Glass fibre, paper based	28	0.038	—
Glass fibre, paper based	40	0.035	—
Glass fibre, coated, duct liner	32	0.038	835
Board and slab			
Cellular glass	145	0.058	1000
Glass fibre organic bonded	105	0.036	795
Polystyrene, expanded, extruded	55	0.027	1210
Polystyrene Moulded Beads	16	0.040	1210
Mineral fibre board, roofing material	265	0.049	—
Wood, shredded and Cemented	350	0.087	1590
Cork	120	0.039	1800
Loose fill			
Cork, granulated	160	0.045	—
Diatomaceous silica, Coarse	350	0.069	—
Diatomaceous silica, Powder	400	0.091	—
Glass fibre, poured or blown	16	0.043	835
Vermiculate, flakes	80	0.068	835
Vermiculate, flakes	160	0.063	1000
Formed/Foamed in place			
Mineral wool granules with asbestos inorganic binders, sprayed	190	0.046	—
Polyvinyl acetate cork mastic			
Sprayed and troweled	—	0.100	—
Urethane, two part mixture rigid foam	70	0.026	1045
Reflective :			
Aluminium foil Separating fluffy Glass mats ; 10 to 12 layers, evacuated For cryogenic applications (150 K)	40	160×10^{-6}	—
Aluminium foil and glass paper Laminate 75-150 layers, evacuated For cryogenic applications (150 k)	120	17×10^{-6}	—
Typical silica powder, evacuated	160	1.7×10^{-3}	—

1 W/mK = 0.86 kcal/m hr °C *1 J/kg K = 238.9 × 10^{-6} kcal/kg °C*

PROPERTY VALUES OF INDUSTRIAL INSULATING MATERIALS

Material	*Density* ρ kg/m^3	*Temperature* °C	*Thermal Conductivity* k W/mK
Evacuated super insulation	Variable	– 240 to 1000	$1.5 \times 10^{-6} - 720 \times 10^{-6}$
BLANKETS :			
Alumina silica fibre blanket	48	255	0.071
Alumina silica fibre blanket	48	370	0.150
Alumina silica fibre blanket	64	255	0.059
Alumina silica fibre blanket	64	370	0.087
Alumina silica fibre blanket	96	255	0.052
Alumina silica fibre blanket	96	370	0.076
Alumina silica fibre blanket	128	255	0.049
Alumina silica fibre blanket	128	370	0.068
Elastemeric Sheets	70-100	– 40 to 100	0.036 – 0.039
Felt blanket, semi rigid	50-125	– 3	0.035
Felt blanket, semi rigid	50-125	27	0.038
Felt blanket, semi rigid	50-125	92	0.051
Felt blanket, organic bonded	50	– 3	0.030
Felt blanket, organic bonded	50	27	0.038
Felt blanket, organic bonded	50	92	0.051
Felt blanket, laminated without binder	120	147	0.051
Felt blanket, laminated without binder	120	257	0.065
Felt blanket, laminated without binder	120	372	0.087
Fibre glass blanket, organic bonded	12	27	0.046
Fibre glass blanket, organic bonded	12	92	0.069
Fibre glass blanket, organic bonded	16	27	0.042
Fibre glass blanket, organic bonded	16	92	0.062
Fibre glass blanket, organic bonded	24	27	0.039
Fibre glass blanket, organic bonded	24	92	0.053
Fibre glass blanket, organic bonded	32	27	0.033
Fibre glass blanket, organic bonded	32	92	0.048
Fibre glass blanket, organic bonded	48	27	0.033
Fibre glass blanket, organic bonded	48	92	0.045
Fibre glass blanket with vapour barrier	5 to 70	10 – 32	0.029 – 0.045
Mineral fibre blanket	10	– 3	0.040
Mineral fibre blanket	10	12	0.043

1 W/mK = 0.86 kcal/m hr °C

PROPERTY VALUES OF INDUSTRIAL INSULATING MATERIALS *(Contd.)*

Material	*Density* ρ kg/m^3	*Temperature* °C	*Thermal Conductivity* k W/mK
Mineral fibre blanket	10	27	0.048
Mineral fibre blanket	10	37	0.052
Mineral fibre blanket	90 – 192	37	0.038
Mineral fibre blanket	90 – 192	92	0.046
Mineral fibre blanket	90 – 192	147	0.056
Mineral fibre blanket, metal reinforced	40 – 96	37	0.035
Mineral fibre blanket, metal reinforced	40 – 96	92	0.045
Mineral fibre blanket, metal reinforced	40 – 96	147	0.058
Mineral fibre blanket, metal reinforced	40 – 96	257	0.088
BLOCKS ; Board and Pipe Insulation :			
Asbestos paper laminated and corrugated 4 ply	190	27	0.078
Asbestos paper laminated and corrugated 4 ply	190	92	0.098
Asbestos paper laminated and corrugated 6 ply	255	27	0.071
Asbestos paper laminated and corrugated 6 ply	255	92	0.085
Asbestos paper laminated and corrugated 8 ply	300	27	0.068
Asbestos paper laminated and corrugated 8 ply	300	92	0.082
Calcium Silicate Blocks	190	37	0.055
Calcium Silicate Blocks	190	92	0.059
Calcium Silicate Blocks	190	147	0.063
Calcium Silicate Blocks	190	257	0.075
Cellular glass blocks	145	– 33	0.048
Cellular glass blocks	145	– 3	0.052
Cellular glass blocks	145	27	0.058
Cellular glass blocks	145	92	0.068
Diatomaceous Silica blocks	345	257	0.092
Diatomaceous Silica blocks	345	372	0.098
Diatomaceous Silica blocks	385	257	0.101
Diatomaceous Silica blocks	385	372	0.100
Insulating Cement-mineral fibre	430	37	0.071
– with clay binder	430	92	0.074
– with clay binder	430	147	0.088

1 W/mK = 0.86 kcal/m hr °C

PROPERTY VALUES OF INDUSTRIAL INSULATING MATERIALS *(Contd.)*

Material	*Density* ρ kg/m^3	*Temperature* °C	*Thermal Conductivity* k W/mK
Insulating Cement-mineral with hydraulic binder	560	37	0.108
Insulating Cement-mineral with hydraulic binder	560	92	0.115
Insulating Cement-mineral with hydraulic binder	560	147	0.123
Magnesia, 85% blocks	185	37	0.051
Magnesia, 85% blocks	185	92	0.058
Magnesia, 85% blocks	185	147	0.061
Mineral fibre preformed blocks	125 – 160	upto 650	0.035 – 0.091
Polystyrene, rigid, extruded	56	– 73	0.023
Polystyrene, rigid, extruded	56	– 3	0.025
Polystyrene, rigid, extruded	56	27	0.027
Polystyrene, rigid, extruded	35	– 73	0.023
Polystyrene, rigid, extruded	35	– 3	0.026
Polystyrene, rigid, extruded	35	27	0.029
Polystyrene, Moulded beads	16	– 73	0.026
Polystyrene, Moulded beads	16	– 3	0.036
Polystyrene, Moulded beads	16	27	0.040
Rubber, rigid formed	70	– 3	0.029
Rubber, rigid formed	70	27	0.032
Urethane foam blocks	25 – 65	100 – 150	0.016 – 0.020
Loose Fill :			
Cellulose, wood or paper pulp	45	27	0.039
Cellulose, wood or paper pulp	45	37	0.042
Perlite, expanded	105	– 73	0.036
Perlite, expanded	105	– 33	0.043
Perlite, expanded	105	– 3	0.49
Perlite, expanded	105	27	0.053
Vermiculite expanded	122	– 43	0.056
Vermiculite expanded	122	– 3	0.063
Vermiculite expanded	122	– 27	0.068
Vermiculite expanded	80	– 43	0.049
Vermiculite expanded	80	– 3	0.058
Vermiculite expanded	80	– 27	0.063

1 W/mK = 0.86 kcal/m hr °C

PROPERTY VALUES OF INSULATING BUILDING AND OTHER MATERIALS

Material	*Temperature* t °C	*Thermal Conductivity* k W/mK	*Density* ρ kg/m^3	*Specific Heat* c J/kgK
Aluminium foil	50	0.0465	20	—
Asbestos, fibre	50	0.1105	470	816
Asphalt	20	0.6978	2110	2093
Balsa wood	30	0.0523	128	—
Boiler Scale	65	1.314 to 3.1400	—	—
Building brick	20	0.2330 to 0.2910	800-1500	—
Chrome brick	200	2.320	3000	840
Chrome brick	550	2.470	3000	840
Chrome brick	900	1.990	3000	840
Corrugated card board	20	0.0640	—	—
Cellotex	20	0.0465	215	—
Celluloid	30	0.2093	1400	—
Chalk	50	0.9304	2000	879
Clinker	30	0.1628	1400	1675
Coal	20	0.1861	1400	1306
Coke, powdered	100	0.1907	419	1214
Concrete	20	1.2790	2300	1130
Cork, granulated	20	0.0384	45	—
Cork, plate	30	0.0419	190	1884
Earth, dry	—	0.1384	1500	—
Earth, wet	—	0.6571	1700	2010
Fibre plate	20	0.0489	240	—
Fibre brick	100	0.1396	550	—
Glass	20	0.7443	2500	670
Glass wool	20	0.0372	200	670
Gravel	20	0.3605	1840	—
Granite	20	0.00279	2630	775
Gypsum	—	0.2908	1650	—
Ice	0	2.2500	920	2261
Ice	– 95	3.9540	—	1172
Lamp black	40	0.1477	190	—
Leather Sole	30	0.1593	1000	—
Linoleum	20	0.1861	1180	—
Magnesia, 85% powdered	100	0.0675	216	—

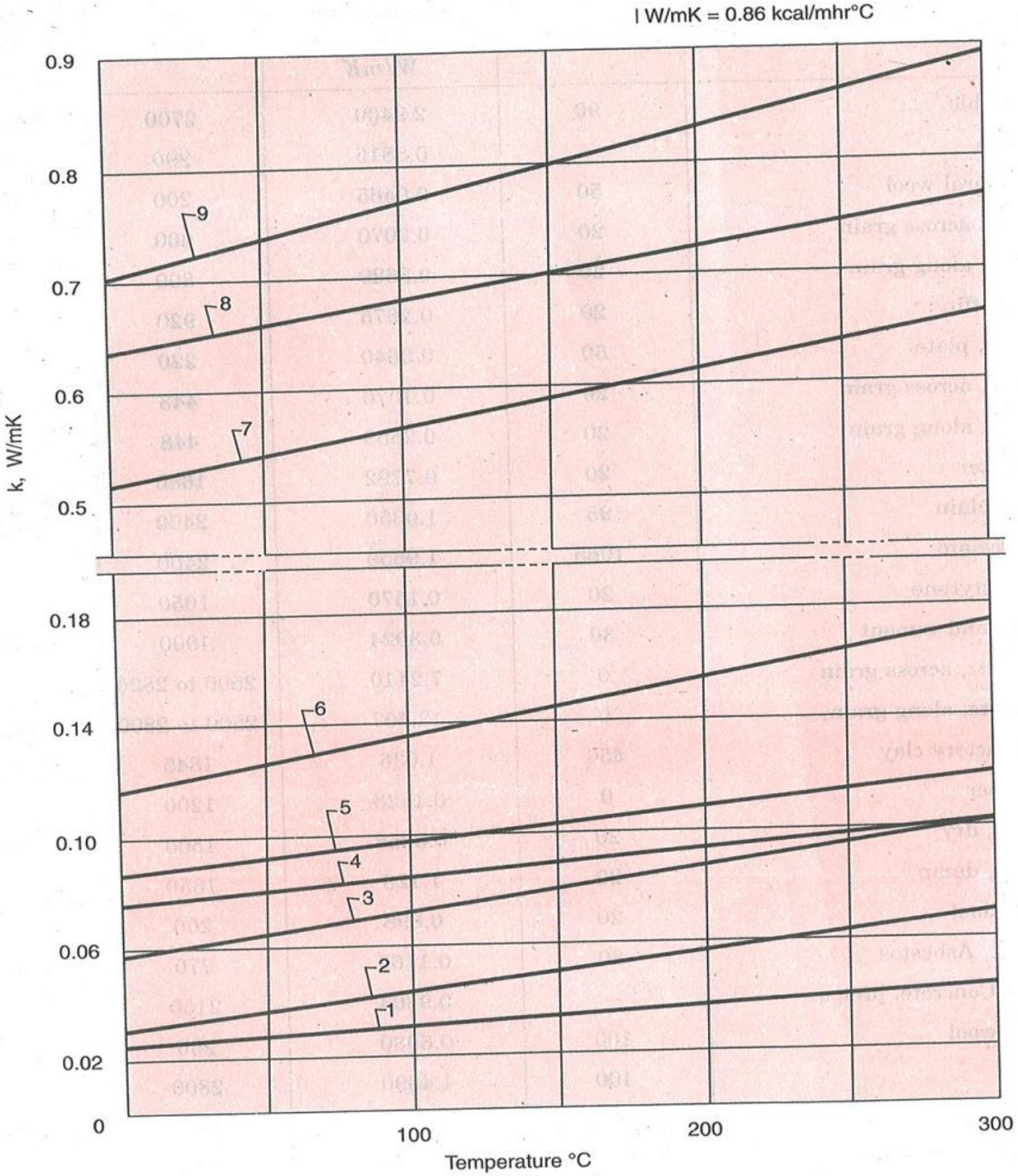
1 W/mk = 0.86 kcal/m hr°C *1 J/kg K = 238.9 × 10^{-6} kcal/ kg°C* *Thermal diffusivity, $\alpha = k/\rho c$.*

PROPERTY VALUES OF INSULATING BULIDING AND OTHER MATERIALS *(Contd.)*

Material	*Temperature* t °C	*Thermal Conductivity* k W/mK	*Density* ρ kg/m^3	*Specific Heat* c J/kgK
Marble	90	2.9400	2700	800
Mica	—	0.5815	290	879
Mineral wool	50	0.0465	200	921
Oak, across grain	20	0.2070	800	1759
Oak, along grain	20	0.3629	800	—
Paraffin	20	0.2675	920	—
Peat, plate	50	0.0640	220	—
Pine, across grain	20	0.1070	448	—
Pine, along grain	20	0.2559	448	—
Plaster	20	0.7792	1680	—
Porcelain	95	1.0350	2400	1089
Porcelain	1065	1.9650	2400	—
Polystyrene	20	0.1570	1050	—
Portland cement	30	0.3024	1900	1130
Quartz, across grain	0	7.2110	2500 to 2800	837
Quartz, along grain	0	13.607	2500 to 2800	837
Refractory clay	450	1.036	1845	1089
Rubber	0	0.1628	1200	1382
Sand, dry	20	0.3256	1500	796
Sand, damp	20	1.128	1650	2093
Saw dust	20	0.698	200	—
Sheet, Asbestos	30	0.1163	770	816
Slag Concrete. lumps	—	0.9304	2150	879
Slag wool	100	0.6980	250	—
Slate	100	1.4890	2800	—
Snow	—	0.4652	560	2093
Sugar, granulated	0	0.5815	1600	1256
Wool, felt	30	0.0523	330	—

1 W/mK = 0.86 kcal/m hr °C *1 J/kg K = 238.9 × 10^{-6} kcal/ kg °C* *Thermal diffusivity, $\alpha = k/\rho c$.*

VARIATION OF THERMAL CONDUCTIVITY OF DIFFERENT INSULATING AND REFRACTORY MATERIALS WITH TEMPERATURE



1 Air
2 Mineral wool
3 Slag wool
4 85% Magnesia
5 Sovelite
6 Diatomaceous earth brick
7 Red brick
8 Slag concrete brick
9 Fire clay brick

PROPERTY VALUES OF LIQUIDS IN SATURATED STATE

	Temperature t °C	Density ρ kg/m^3	Kinematic Viscosity ν m^2/s	Thermal Diffusivity α m^2/s	Prandtl Number Pr	Specific Heat c J/kgK	Thermal Conductivity k W/mK
WATER							
	0	1002	1.788×10^{-6}	0.1308×10^{-6}	13.600	4216	0.5524
	20	1000	1.006×10^{-6}	0.1431×10^{-6}	7.020	4178	0.5978
	40	995	0.657×10^{-6}	0.1511×10^{-6}	4.340	4178	0.6280
	60	985	0.478×10^{-6}	0.1553×10^{-6}	3.020	4183	0.6513
	80	974	0.364×10^{-6}	0.1636×10^{-6}	2.220	4195	0.6687
	100	961	0.293×10^{-6}	0.1681×10^{-6}	1.740	4216	0.6804
	120	945	0.247×10^{-6}	0.1708×10^{-6}	1.446	4250	0.6850
	140	928	0.213×10^{-6}	0.1725×10^{-6}	1.241	4283	0.6838
	160	909	0.189×10^{-6}	0.1728×10^{-6}	1.099	4342	0.6804
	180	889	0.173×10^{-6}	0.1725×10^{-6}	1.044	4417	0.6757
	200	867	0.160×10^{-6}	0.1701×10^{-6}	0.937	4505	0.6652
	220	842	0.149×10^{-6}	0.1681×10^{-6}	0.891	4610	0.6524
	240	815	0.143×10^{-6}	0.1639×10^{-6}	0.871	4756	0.6350
	260	786	0.137×10^{-6}	0.1578×10^{-6}	0.874	4949	0.6106
	280	752	0.135×10^{-6}	0.1481×10^{-6}	0.910	5208	0.5803
	300	714	0.135×10^{-6}	0.1325×10^{-6}	1.019	5728	0.5396
AMMONIA							
	– 50	704	0.435×10^{-6}	0.1742×10^{-6}	2.600	4463	0.5466
	– 40	691	0.406×10^{-6}	0.1775×10^{-6}	2.280	4467	0.5466
	– 30	679	0.387×10^{-6}	0.1800×10^{-6}	2.150	4476	0.5489
	– 20	667	0.381×10^{-6}	0.1819×10^{-6}	2.090	4509	0.5466
	– 10	653	0.378×10^{-6}	0.1825×10^{-6}	2.070	4564	0.5431
	0	640	0.373×10^{-6}	0.1819×10^{-6}	2.050	4635	0.5396
	10	626	0.368×10^{-6}	0.1800×10^{-6}	2.040	4714	0.5315
	20	612	0.358×10^{-6}	0.1775×10^{-6}	2.020	4798	0.5210
	30	596	0.350×10^{-6}	0.1742×10^{-6}	2.010	4890	0.5071
	40	581	0.340×10^{-6}	0.1700×10^{-6}	2.000	4999	0.4931
	50	564	0.330×10^{-6}	0.1656×10^{-6}	1.990	5116	0.4757

For values of β refer page 29 or $\beta = (\Delta\rho)/(\rho \times \Delta T)$ (use $\Delta\rho$, ρ, ΔT from tables), $\mu = \rho\nu$, 1W/mK = 0.86 kcal/m hr °C, 1 J/kg K = 238.9×10^{-6} kcal/kg °C

PROPERTY VALUES OF LIQUIDS IN SATURATED STATE (*Contd.*)

	Temperature t °C	*Density* ρ kg/m^3	*Kinematic Viscosity* ν m^2/s	*Thermal Diffusivity* α m^2/s	*Prandtl Number* Pr	*Specific Heat* c J/kgK	*Thermal Conductivity* k W/mK
CARBON-DIOXIDE							
	– 50	1156	0.119×10^{-6}	0.0403×10^{-6}	2.96	1842	0.0855
	– 40	1118	0.118×10^{-6}	0.0481×10^{-6}	2.46	1884	0.1011
	– 30	1077	0.117×10^{-6}	0.0528×10^{-6}	2.22	1968	0.1117
	– 20	1032	0.115×10^{-6}	0.0544×10^{-6}	2.12	2652	0.1150
	– 10	983	0.113×10^{-6}	0.0514×10^{-6}	2.22	2177	0.1099
	0	927	0.108×10^{-6}	0.0458×10^{-6}	2.38	2470	0.1046
	10	863	0.102×10^{-6}	0.0361×10^{-6}	2.80	3140	0.0971
	20	772	0.091×10^{-6}	0.0222×10^{-6}	4.10	5024	0.0872
	30	598	0.079×10^{-6}	0.0028×10^{-6}	28.70	36425	0.0703
GLYCERINE-$C_3H_5(OH)_3$							
	0	1276	8314×10^{-6}	0.0983×10^{-6}	84700	2261	0.2826
	10	1270	3000×10^{-6}	0.0964×10^{-6}	31000	2320	0.2838
	20	1264	1180×10^{-6}	0.0947×10^{-6}	12500	2387	0.2861
	30	1258	501×10^{-6}	0.0928×10^{-6}	5380	2445	0.2861
	40	1252	223×10^{-6}	0.0914×10^{-6}	2450	2512	0.2861
	50	1245	149×10^{-6}	0.0892×10^{-6}	1630	2583	0.2873
SULPHUR DIOXIDE							
	– 50	1561	0.484×10^{-6}	0.1142×10^{-6}	4.24	1361	0.2419
	– 40	1537	0.423×10^{-6}	0.1131×10^{-6}	3.74	1361	0.2349
	– 30	1521	0.370×10^{-6}	0.1119×10^{-6}	3.31	1361	0.2303
	– 20	1488	0.324×10^{-6}	0.1108×10^{-6}	2.93	1361	0.2256
	– 10	1463	0.288×10^{-6}	0.1197×10^{-6}	2.62	1361	0.2186
	0	1438	0.257×10^{-6}	0.1081×10^{-6}	2.38	1365	0.2117
	10	1412	0.232×10^{-6}	0.1067×10^{-6}	2.18	1365	0.2047
	20	1386	0.209×10^{-6}	0.1050×10^{-6}	2.00	1365	0.1989
	30	1359	0.189×10^{-6}	0.1036×10^{-6}	1.83	1365	0.1919
	40	1329	0.173×10^{-6}	0.1019×10^{-6}	1.70	1369	0.1849
	50	1299	0.162×10^{-6}	0.1000×10^{-6}	1.61	1369	0.1768

For the values of β refer page 29 or $\beta = (\Delta\rho)/(\rho \times \Delta T)$ (use $\Delta\rho$, ρ, ΔT from tables), $\mu = \rho\nu$, 1 W/mK = 0.86 kcal/m hr°C, 1 J/kg K = 238.9×10^{-6} kcal/kg °C

PROPERTY VALUES OF LIQUIDS IN SATURATED STATE *(Contd.)*

Temperature t °C	*Density* ρ kg/m^3	*Kinematic Viscosity* ν m^2/s	*Thermal Diffusivity* α m^2/s	*Prandtl Number* Pr	*Specific Heat* c J/kgK	*Thermal Conductivity* k W/mK
METHYL CHLORIDE (REFRIGERANT-40)-CH_3Cl						
– 50	1052	0.319×10^{-6}	0.1389×10^{-6}	2.31	1474	0.2512
– 40	1033	0.317×10^{-6}	0.1367×10^{-6}	2.32	1482	0.2093
– 30	1016	0.314×10^{-6}	0.1336×10^{-6}	2.35	1491	0.2024
– 20	999	0.309×10^{-6}	0.1300×10^{-6}	2.38	1503	0.1954
– 10	981	0.305×10^{-6}	0.1256×10^{-6}	2.43	1520	0.1872
0	962	0.302×10^{-6}	0.1214×10^{-6}	2.49	1537	0.1779
10	942	0.293×10^{-6}	0.1167×10^{-6}	2.55	1562	0.1710
20	923	0.292×10^{-6}	0.1111×10^{-6}	2.63	1587	0.1628
30	903	0.288×10^{-6}	0.1058×10^{-6}	2.72	1616	0.1535
40	883	0.281×10^{-6}	0.0997×10^{-6}	2.83	1650	0.1442
50	861	0.274×10^{-6}	0.0925×10^{-6}	2.97	1687	0.1338
DICHLORO DIFLURO METHANE (REFRIGERANT-12)-CCl_2F_2						
– 50	1547	0.310×10^{-6}	0.0500×10^{-6}	6.20	875	0.0675
– 40	1518	0.279×10^{-6}	0.0514×10^{-6}	5.40	883	0.0692
– 30	1490	0.253×10^{-6}	0.0528×10^{-6}	4.80	896	0.0692
– 20	1460	0.235×10^{-6}	0.0539×10^{-6}	4.40	909	0.0709
– 10	1429	0.220×10^{-6}	0.0550×10^{-6}	4.00	917	0.0727
0	1397	0.213×10^{-6}	0.0558×10^{-6}	3.80	934	0.0727
10	1364	0.203×10^{-6}	0.0561×10^{-6}	3.60	950	0.0727
20	1330	0.198×10^{-6}	0.0561×10^{-6}	3.50	963	0.0727
30	1295	0.194×10^{-6}	0.0561×10^{-6}	3.50	984	0.0709
40	1257	0.191×10^{-6}	0.0556×10^{-6}	3.50	1005	0.0692
50	1216	0.189×10^{-6}	0.0544×10^{-6}	3.50	1022	0.0672
EUTECTIC CALCIUM CHLORIDE SOLUTION (29.9% $CaCl_2$)						
– 50	1320	36.352×10^{-6}	0.1167×10^{-6}	312	2608	0.4012
– 40	1314	24.971×10^{-6}	0.1200×10^{-6}	208	2634	0.4152
– 30	1310	17.177×10^{-6}	0.1233×10^{-6}	139	2663	0.4292

For values of β refer page 29 or $\beta = (\Delta\rho)/(\rho \times \Delta T)$ (use $\Delta\rho$, ρ, ΔT from tables), $\mu = \rho\nu$, 1 W/mK = 0.86 kcal/m hr°C, 1 J/kg K = 238.9×10^{-6} kcal/kg °C

PROPERTY VALUES OF LIQUIDS IN SATURATED STATE (*Contd.*)

Temperature t °C	Density ρ kg/m^3	Kinematic Viscosity ν m^2/s	Thermal Diffusivity α m^2/s	Prandtl Number Pr	Specific Heat c $J/kg\,K$	Thermal Conductivity k W/mK
29.9% $Ca\,Cl_2$ solution (Contd.)						
– 20	1305	11.036×10^{-6}	0.1267×10^{-6}	87.10	2688	0.4454
– 10	1300	6.956×10^{-6}	0.1300×10^{-6}	53.60	2713	0.4582
0	1296	4.394×10^{-6}	0.1331×10^{-6}	33.00	2738	0.4722
10	1291	3.353×10^{-6}	0.1364×10^{-6}	24.60	2763	0.4850
20	1286	2.722×10^{-6}	0.1394×10^{-6}	19.60	2788	0.4989
30	1282	2.267×10^{-6}	0.1422×10^{-6}	16.00	2813	0.5106
40	1277	1.923×10^{-6}	0.1444×10^{-6}	13.30	2839	0.5234
50	1272	1.654×10^{-6}	0.1469×10^{-6}	11.30	2868	0.5350
ETHYLENE GLYCOL —$C_2H_4(OH)_2$						
0	1131	57.530×10^{-6}	0.0933×10^{-6}	615.00	2294	0.2419
20	1116	19.174×10^{-6}	0.0939×10^{-6}	204.00	2382	0.2489
40	1101	8.686×10^{-6}	0.0939×10^{-6}	93.00	2474	0.2559
60	1087	4.747×10^{-6}	0.0931×10^{-6}	51.00	2562	0.2594
80	1077	2.982×10^{-6}	0.0922×10^{-6}	32.40	2650	0.2617
100	1058	2.025×10^{-6}	0.0908×10^{-6}	22.40	2742	0.2628
ENGINE OIL (UNUSED)						
0	899	4282×10^{-6}	0.0911×10^{-6}	47100.00	1796	0.1477
20	888	901×10^{-6}	0.0872×10^{-6}	10400.00	1880	0.1454
40	876	241×10^{-6}	0.0833×10^{-6}	2870.00	1964	0.1442
60	864	83×10^{-6}	0.0800×10^{-6}	1050.00	2047	0.1407
80	852	37×10^{-6}	0.0769×10^{-6}	490.00	2131	0.1384
100	840	20×10^{-6}	0.0739×10^{-6}	276.00	2219	0.1372
120	828	12×10^{-6}	0.0711×10^{-6}	175.00	2307	0.1349
140	816	8×10^{-6}	0.0686×10^{-6}	116.00	2395	0.1338
160	805	5×10^{-6}	0.0664×10^{-6}	84.00	2483	0.1314

For values of β refer page 29 or $\beta = (\Delta\rho)/(\rho \times \Delta T)$ (use $\Delta\rho$, ρ, ΔT from tables), $\mu = \rho\nu$, 1 W/mK = 0.86 kcal/m hr°C, 1 J/kgK = 238.9×10^{-6} kcal/kg °C

PROPERTY VALUES OF TRANSFORMER OIL (STANDARD 982—68)

Temp. t °C	*Density* ρ kg/m^3	*Kinematic Viscosity* ν m^2/s	*Thermal Diffusivity* α m^2/s	*Prandtl Number* Pr	*Specific Heat* c J/kgK	*Thermal Conductivity* k W/mK	*Absolute Viscosity* μ $N\,s/m^2$
– 50	922	$31{,}800 \times 10^{-6}$	74.2×10^{-9}	42860×10^{-3}	1700	0.116	$29{,}320 \times 10^{-3}$
– 40	916	$4{,}220 \times 10^{-6}$	75.0×10^{-9}	5630×10^{-3}	1680	0.116	$3{,}866 \times 10^{-3}$
– 30	910	$1{,}300 \times 10^{-6}$	76.4×10^{-9}	1700×10^{-3}	1650	0.115	$1{,}183 \times 10^{-3}$
– 20	904	404×10^{-6}	77.8×10^{-9}	520×10^{-3}	1620	0.114	365.6×10^{-3}
– 10	898	120×10^{-6}	78.8×10^{-9}	153×10^{-3}	2788	0.113	108.1×10^{-3}
0	891	67.5×10^{-6}	77.8×10^{-9}	86.7×10^{-3}	2813	0.112	55.24×10^{-3}
10	885	37.8×10^{-6}	76.3×10^{-9}	49.5×10^{-3}	2839	0.111	33.45×10^{-3}
20	879	24.0×10^{-6}	73.6×10^{-9}	32.6×10^{-3}	2868	0.111	21.10×10^{-3}
30	873	15.4×10^{-6}	70.7×10^{-9}	21.8×10^{-3}	2382	0.110	13.44×10^{-3}
40	867	10.8×10^{-6}	68.8×10^{-9}	15.7×10^{-3}	2474	0.109	9.364×10^{-3}

1 W/mK = 0.86 kcal/m hr°C 1 J/kg K = 238.9×10^{-6} kcal/kg °C 1 Ns/m² = 0.102 kgfs/m²

PROPERTY VALUES OF MOBILTHERM 600

Temp. t °C	*Density* ρ kg/m^3	*Coefficient of thermal expansion* β $1/K$	*Kinematic Viscosity* ν m^2/s	*Thermal Diffusivity* α m^2/s	*Prandtl Number* Pr	*Specific Heat* c $J/kg\,K$	*Thermal Conductivity* k W/mK	*Absolute Viscosity* μ $N\,s/m^2$
10	953	0.621×10^{-3}		83.3×10^{-9}		1549	0.123	
50	929	0.637×10^{-3}	32.60×10^{-6}	76.9×10^{-9}	424	1680	0.120	30.28×10^{-3}
100	899	0.658×10^{-3}	6.10×10^{-6}	69.4×10^{-9}	87.9	1859	0.116	5.48×10^{-3}
150	870	0.680×10^{-3}	2.34×10^{-6}	64.0×10^{-9}	36.6	2031	0.113	2.04×10^{-3}
200	839	0.705×10^{-3}	1.25×10^{-6}	59.4×10^{-9}	21.0	2209	0.110	1.05×10^{-3}
250	810	0.730×10^{-3}	0.790×10^{-6}	54.5×10^{-9}	14.5	2386	0.106	0.64×10^{-3}

1 W/mK = 0.86 kcal/m hr °C 1 J/kg K = 238.9×10^{-6} kcal/kg °C 1 Ns/m² = 0.102 kgfs/m²

PROPERTY VALUES OF *n*-BUTYL ALCOHOL ($C_4H_{10}O$)

Temp. t °C	*Density* ρ kg/m^3	*Coefficient of thermal expansion* β $1/K$	*Kinematic Viscosity* ν m^2/s	*Thermal Diffusivity* α m^2/s	*Prandtl Number* Pr	*Specific Heat* c J/kgK	*Thermal Conductivity* k W/mK	*Absolute Viscosity* μ $N\,s/m^2$
16	809		4.16×10^{-6}	159.1×10^{-9}	0.261	1305	0.168	3.36×10^{-3}
38	796	81×10^{-3}	2.41×10^{-6}	149.8×10^{-9}	0.161	1392	0.166	1.92×10^{-3}
66	777	86×10^{-3}	1.29×10^{-6}	140.5×10^{-9}	0.0916	1502	0.164	1.00×10^{-3}
93	756		0.76×10^{-6}	134.0×10^{-9}	0.056	1609	0.163	0.57×10^{-3}
117.5	737		0.53×10^{-6}	129.6×10^{-9}	0.041	1706	0.163	0.39×10^{-3}
149						1830		0.28×10^{-3}

1 W/mK = 0.86 kcal/m hr °C 1 J/kg K = 238.9×10^{-6} kcal/kg °C 1 Ns/m² = 0.102 kgfs/m²

PROPERTY VALUES OF MOLTEN SALT (EQUIMOLAR KNO_3 54%, $NaNO_3$ 46%)

Temp. t °C	*Density* ρ kg/m^3	*Coefficient of thermal expansion* β $1/K$	*Kinematic Viscosity* ν m^2/s	*Thermal Diffusivity* α m^2/s	*Prandtl Number* Pr	*Specific Heat* c J/kgK	*Thermal Conductivity* k W/mK	*Absolute Viscosity* μ $N\,s/m^2$
357	1864	3.40×10^{-3}	1.189×10^{-6}	$.167 \times 10^{-6}$	7.12	1645	0.512	2.217×10^{-3}
367	1858	3.47×10^{-3}	1.130×10^{-6}	$.169 \times 10^{-6}$	6.68	1633	0.513	2.100×10^{-3}
377	1851	3.53×10^{-3}	1.079×10^{-6}	$.172 \times 10^{-6}$	6.29	1621	0.515	1.997×10^{-3}
387	1845	3.60×10^{-3}	1.033×10^{-6}	$.174 \times 10^{-6}$	5.94	1610	0.517	1.906×10^{-3}
397	1838	3.67×10^{-3}	0.994×10^{-6}	$.177 \times 10^{-6}$	5.62	1598	0.519	1.826×10^{-3}
407	1831	3.74×10^{-3}	0.959×10^{-6}	$.179 \times 10^{-6}$	5.34	1586	0.521	1.755×10^{-3}
417	1824	3.81×10^{-3}	0.928×10^{-6}	$.182 \times 10^{-6}$	5.09	1574	0.523	1.692×10^{-3}
427	1817	3.88×10^{-3}	0.900×10^{-6}	$.185 \times 10^{-6}$	4.87	1562	0.525	1.636×10^{-3}
437	1810	3.95×10^{-3}	0.876×10^{-6}	$.188 \times 10^{-6}$	4.66	1551	0.527	1.585×10^{-3}
447	1803	4.02×10^{-3}	0.854×10^{-6}	$.191 \times 10^{-6}$	4.48	1539	0.529	1.540×10^{-3}

1 W/mK = 0.86 kcal/m hr °C 1 J/kg K = 238.9×10^{-6} kcal/kg °C 1 Ns/m² = 0.102 kgfs/m²

PROPERTY VALUES OF ORGANIC COMPOUNDS AT 20 °C

Liquid	*Chemical formula*	*Density* ρ kg/m^3	*Coefficient of thermal expansion* β $1/K$	*Kinematic Viscosity* ν m^2/s	*Thermal Diffusivity* α m^2/s	*Prandtl Number* Pr	*Specific Heat* c J/kgK	*Thermal Conductivity* k W/mK	*Absolute Viscosity* μ $N\,s/m^2$
Acetic acid	$C_2H_4O_2$	1049	1.07×10^{-3}		90.6×10^{-9}		2031	0.193	
Acetone	C_3H_6O	791	1.43×10^{-3}	0.418×10^{-6}	105.4×10^{-9}	3.97	2160	0.180	0.331×10^{-3}
Chloroform	$CHCl_3$	1489	1.28×10^{-3}	0.390×10^{-6}	89.6×10^{-9}	3.97	967	0.129	0.580×10^{-3}
Ethyl acetate	$C_4H_8O_2$	900	1.38×10^{-3}	0.499×10^{-6}	75.7×10^{-9}	3.97	2010	0.137	0.449×10^{-3}
Ethyl alcohol	C_2H_6O	790	1.10×10^{-3}	1.52×10^{-6}	93.3×10^{-9}	3.97	2470	0.182	0.120×10^{-3}
Ethylene glycol	$C_2H_6O_2$	1115		17.8×10^{-6}	97.1×10^{-9}	3.97	2382	0.258	19.900×10^{-3}
Glycerol	$C_3H_8O_3$	1260	0.50×10^{-3}	1175×10^{-6}	93.2×10^{-9}	3.97	2428	0.285	14.80×10^{-3}
n-Heptane	C_7H_{16}	684	1.24×10^{-3}	0.598×10^{-6}	92.2×10^{-9}	3.97	2219	0.140	0.409×10^{-3}
n-Hexane	C_6H_{14}	660	1.35×10^{-3}	0.485×10^{-6}	110.2×10^{-9}	3.97	1884	0.137	0.320×10^{-3}
Isobutyl alcohol	$C_4H_{10}O$	804	0.94×10^{-3}	4.91×10^{-6}	72.4×10^{-9}	3.97	2303	0.134	3.950×10^{-3}
Methyl alcohol	CH_4O	792	1.19×10^{-3}	0.737×10^{-6}	108.4×10^{-9}	3.97	2470	0.212	0.584×10^{-3}
n-Octane	C_8H_{18}	720	1.14×10^{-3}	0.750×10^{-6}	93.8×10^{-9}	3.97	2177	0.147	0.540×10^{-3}
n-Pentane	C_5H_{12}	626	1.60×10^{-3}	0.366×10^{-6}	99.8×10^{-9}	3.97	2177	0.136	0.229×10^{-3}
Toluene	C_7H_8	866	1.08×10^{-3}	0.677×10^{-6}	104.1×10^{-9}	3.97	1675	0.151	0.586×10^{-3}
Turpentine	$C_{10}H_{16}$	855	0.97×10^{-3}	1.74×10^{-6}	83.2×10^{-9}	3.97	1800	0.128	1.487×10^{-3}

1 W/mK = 0.86 kcal/m hr °C 1 J/kg K = 238.9×10^{-6} kcal/kg °C 1 Ns/m² = 0.102 kgfs/m²

PROPERTY VALUES OF HEAVY WATER (D_2O)

Molecular Weight	: 20.033	Critical Temperature	: 371.5°C
Freezing point	: 3.82°C	Critical Pressure	: 21.44×10^6 N/m²
Boiling point at 9.81×10^4 N/m²	: 101.43°C		

Temperature, °C	*Enthalpy, h kJ/kg*	*Specific heat c, J/kgK*	*Viscosity of Heavy Water, D_2O / Viscosity of Light Water, H_2O* $\frac{\mu D_2O}{\mu H_2O}$
3.82	2321.7	—	—
5.0	—	—	1.309
10	2229.9	4226	1.286
15	—	4218	1.267
20	—	4211	1.249
25	2266.7	4207	1.232
30	—	4205	1.215
35	—	4201	—
40	2224.7	4201	—
45	—	4201	—
50	—	4203	—
60	2176.0	—	—
80	2126.3	—	1.164
100	2074.7	—	1.154
120	2020.7	—	—
125	—	—	1.146
140	1950.9	—	—
160	1903.3	—	—
180	1838.7	—	—
200	1769.4	—	—
220	1693.7	—	—

COEFFICIENT OF CUBICAL EXPANSION, β at 20°C

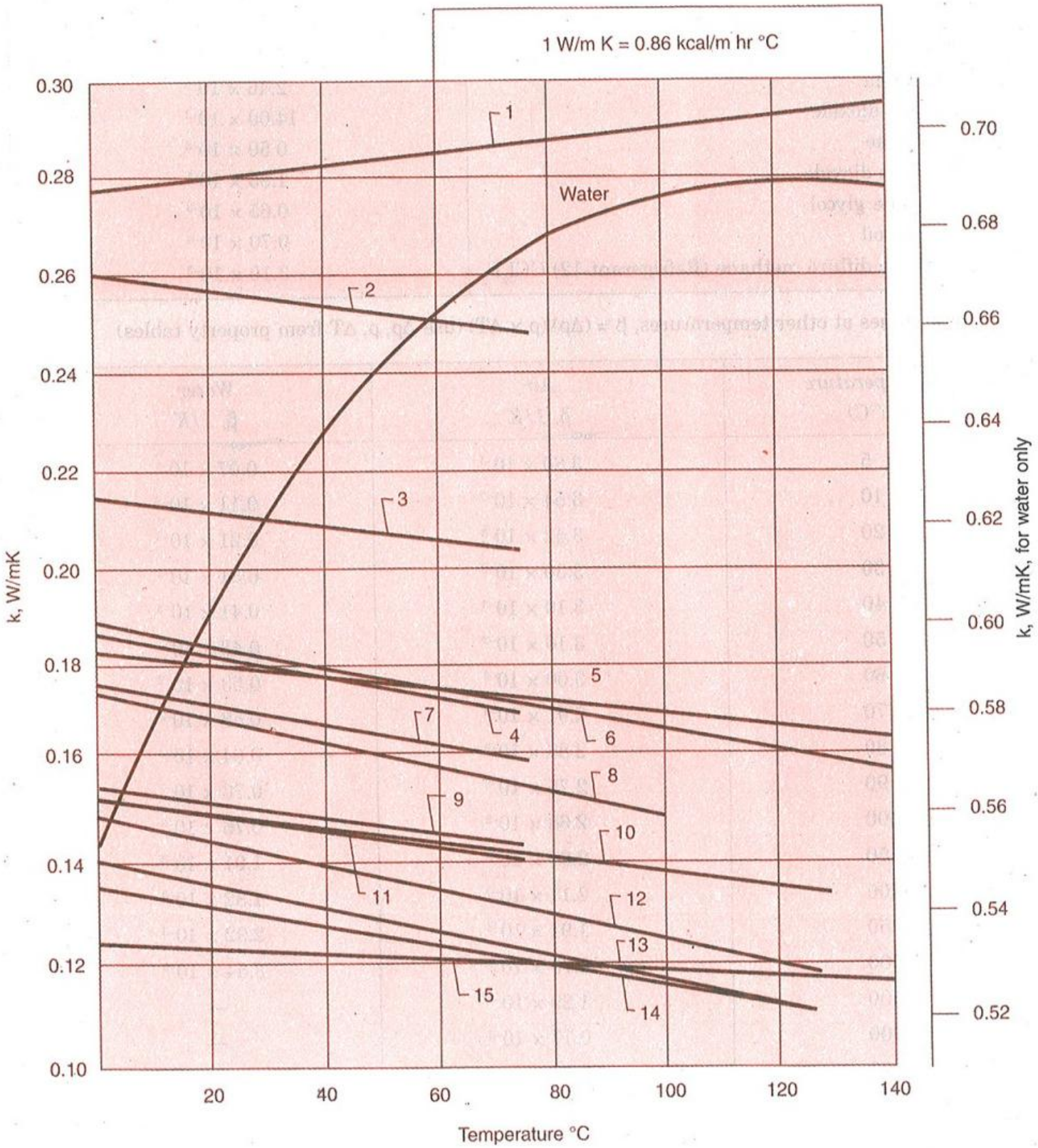
Fluid	β, *1/K*
Water	0.21×10^{-3}
Ammonia	2.46×10^{-3}
Carbon dioxide	14.00×10^{-3}
Glycerine	0.50×10^{-3}
Sulphur dioxide	1.95×10^{-3}
Ethylene glycol	0.65×10^{-3}
Engine oil	0.70×10^{-3}
Dichloro difluro methane (Refrigerant-12) CCl_2F_2	3.10×10^{-3}

For values at other temperatures, $\beta = (\Delta\rho)/(\rho \times \Delta T)$ (use $\Delta\rho$, ρ, ΔT from property tables)

Temperature (°C)	*Air* β, *1/K*	*Water* β, *1/K*
5	3.60×10^{-3}	0.07×10^{-3}
10	3.54×10^{-3}	0.11×10^{-3}
20	3.42×10^{-3}	0.21×10^{-3}
30	3.30×10^{-3}	0.31×10^{-3}
40	3.19×10^{-3}	0.41×10^{-3}
50	3.10×10^{-3}	0.48×10^{-3}
60	3.00×10^{-3}	0.53×10^{-3}
70	2.91×10^{-3}	0.58×10^{-3}
80	2.83×10^{-3}	0.64×10^{-3}
90	2.75×10^{-3}	0.70×10^{-3}
100	2.68×10^{-3}	0.76×10^{-3}
150	2.36×10^{-3}	1.01×10^{-3}
200	2.11×10^{-3}	1.32×10^{-3}
250	1.91×10^{-3}	2.92×10^{-3}
300	1.75×10^{-3}	3.54×10^{-3}
500	1.29×10^{-3}	—
1000	0.77×10^{-3}	—
2000	0.44×10^{-3}	—

For gases $\beta = \frac{1}{T}$, T in K.

VARIATION OF THERMAL CONDUCTIVITY OF LIQUIDS WITH TEMPERATURE



1 Anhydrous glycerine
2 Formic acid
3 Methyl alcohol
4 Ethyl alcohol
5 Castor oil
6 Aniline
7 Acetic acid
8 Acetone
9 Butyl alcohol
10 Nitrobenzene
11 Isopropane
12 Benzoine
13 Toluene
14 Xylene
15 Vaseline oil

PHYSICAL PROPERTIES OF LIQUID METALS

Name of metal t_m *Melting point* t_b *Boiling point*	*Temp.* t °C	*Density* ρ kg/m^3	*Kinematic Viscosity* ν m^2/s	*Thermal Diffusivity* α m^2/s	*Prandtl Number* Pr	*Specific Heat* c J/kgK	*Thermal Conductivity* k W/mK
MERCURY, Hg	20	13550	0.114×10^{-6}	4.361×10^{-6}	0.0272	139.0	7.91
$t_m = -38.9$°C	100	13350	0.094×10^{-6}	4.889×10^{-6}	0.0192	137.3	8.96
	150	13230	0.086×10^{-6}	5.306×10^{-6}	0.0162	137.3	9.65
$t_b = 357$°C	200	13120	0.080×10^{-6}	5.722×10^{-6}	0.0140	137.3	10.35
	300	12880	0.071×10^{-6}	6.639×10^{-6}	0.0107	137.3	11.75
TIN, Sn	250	6980	0.270×10^{-6}	19.167×10^{-6}	0.0141	255.4	34.08
$t_m = 231.9$°C	300	6940	0.240×10^{-6}	19.028×10^{-6}	0.0126	255.4	33.73
	400	6865	0.200×10^{-6}	18.889×10^{-6}	0.0106	255.4	33.15
$t_b = 2270$°C	500	6790	0.173×10^{-6}	18.750×10^{-6}	0.0092	255.4	32.56
BISMUTH, Bi	300	10030	0.171×10^{-6}	8.611×10^{-6}	0.0198	150.7	13.03
$t_m = 271$°C	400	9910	0.142×10^{-6}	9.722×10^{-6}	0.0146	150.7	14.42
$t_b = 1490$°C	500	9785	0.122×10^{-6}	10.833×10^{-6}	0.0113	150.7	15.82
	600	9660	0.108×10^{-6}	11.944×10^{-6}	0.0091	150.7	17.21
LITHIUM, Li	200	515	1.110×10^{-6}	172.22×10^{-6}	0.0643	418.7	37.22
$t_m = 186$°C	300	505	0.927×10^{-6}	183.33×10^{-6}	0.0503	418.7	38.96
$t_b = 1317$°C	400	495	0.817×10^{-6}	202.78×10^{-6}	0.0404	418.7	41.87
	500	484	0.734×10^{-6}	225.00×10^{-6}	0.0328	418.7	45.36
POTASSIUM	149	807.3	0.4608×10^{-6}	69.9×10^{-6}	0.0066	800	45.00
$t_m = 64$°C	427	741.7	0.2397×10^{-6}	70.7×10^{-6}	0.0034	750	39.50
$t_b = 760$°C	704	674.4	0.1905×10^{-6}	65.5×10^{-6}	0.0029	750	33.10

1W/mK = 0.86 kcal/m hr °C 1 J/kg K = 238.9×10^{-6} kcal/kg °C

PHYSICAL PROPERTIES OF LIQUID METALS (*Contd.*)

Name of metal t_m *Melting point* t_b *Boiling point*	*Temperature* t °C	*Density* ρ kg/m^3	*Kinematic Viscosity* ν m^2/s	*Thermal Diffusivity* α m^2/s	*Prandtl Number* Pr	*Specific Heat* c J/kgK	*Thermal Conductivity* k W/mK
SODIUM, Na	150	916	0.594×10^{-6}	68.333×10^{-6}	0.0087	1357	84.90
$t_m = 97.3$°C	200	903	0.506×10^{-6}	67.778×10^{-6}	0.0075	1327	81.41
	300	878	0.394×10^{-6}	63.056×10^{-6}	0.0063	1281	70.94
$t_b = 878$°C	400	854	0.330×10^{-6}	58.889×10^{-6}	0.0056	1273	63.97
	500	829	0.289×10^{-6}	54.167×10^{-6}	0.0053	1273	56.99
ALLOY (Bi-Pb)	150	10550	0.289×10^{-6}	6.389×10^{-6}	0.0450	147	9.77
56.5% Bi + 43.5% Pb	200	10490	0.243×10^{-6}	6.669×10^{-6}	0.0364	147	10.35
$t_m = 123.5$°C	300	10360	0.187×10^{-6}	7.500×10^{-6}	0.0250	147	11.40
	400	10240	0.157×10^{-6}	10.000×10^{-6}	0.0187	147	12.56
$t_b = 1600$ °C	500	10120	0.136×10^{-6}	9.444×10^{-6}	0.0144	147	13.96
ALLOY (Na-K)	100	847	0.607×10^{-6}	24.444×10^{-6}	0.0248	1143	23.84
25% Na + 75% K	200	822	0.452×10^{-6}	26.389×10^{-6}	0.0171	1072	23.26
$t_m = -11$°C	300	799	0.366×10^{-6}	27.500×10^{-6}	0.0134	1038	22.68
$t_b = 184$ °C	400	775	0.308×10^{-6}	26.611×10^{-6}	0.0108	1001	22.10
	500	751	0.267×10^{-6}	29.722×10^{-6}	0.0090	967	21.52
ALLOY (Na-K)	93	887.4	0.652×10^{-6}	25.556×10^{-6}	0.0260	1130	25.6
45% Na + 55% K	371	821.7	0.287×10^{-6}	31.667×10^{-6}	0.0091	1055	27.5
$t_m = 19$ °C	704	740.1	0.217×10^{-6}	37.500×10^{-6}	0.0058	1043	28.9

$\beta = (\Delta\rho)/(\rho \times \Delta T)$ (use $\Delta\rho$, ρ, ΔT from tables), $\mu = \rho\nu$, 1 W/mK = 0.86 kcal/m hr °C, 1 J/kg K = 238.9×10^{-6} kcal/kg °C

PROPERTY VALUES OF GASES AT ONE ATMOSPHERIC PRESSURE (use β = 1/T, T in K)

Fog gases k, c_p, μ and Pr may be taken as not sensitive to pressure. But α, ν, ρ should be corrected for pressure, by calculating the value of ρ at the pressure

Temperature t °C	*Density* ρ kg/m^3	*Absolute Viscosity* μ Ns/m^2	*Kinematic Viscosity* ν m^2/s	*Thermal Diffusivity* α m^2/s	*Prandtl Number* Pr	*Specific Heat* c_p J/kgK	*Thermal Conductivity* k W/mK
DRY AIR							
– 50	1.584	14.61×10^{-6}	9.23×10^{-6}	12.644×10^{-6}	0.728	1013	0.02035
– 40	1.515	15.20×10^{-6}	10.04×10^{-6}	13.778×10^{-6}	0.728	1013	0.02117
– 30	1.453	15.69×10^{-6}	10.80×10^{-6}	14.917×10^{-6}	0.723	1013	0.02198
– 20	1.395	16.18×10^{-6}	11.61×10^{-6}	16.194×10^{-6}	0.716	1009	0.02279
– 10	1.342	16.67×10^{-6}	12.43×10^{-6}	17.444×10^{-6}	0.712	1009	0.02361
0	1.293	17.16×10^{-6}	13.28×10^{-6}	18.806×10^{-6}	0.707	1005	0.02442
10	1.247	17.65×10^{-6}	14.16×10^{-6}	20.006×10^{-6}	0.705	1005	0.02512
20	1.205	18.14×10^{-6}	15.06×10^{-6}	21.417×10^{-6}	0.703	1005	0.02593
30	1.165	18.63×10^{-6}	16.00×10^{-6}	22.861×10^{-6}	0.701	1005	0.02675
40	1.128	19.12×10^{-6}	16.96×10^{-6}	24.306×10^{-6}	0.669	1005	0.02756
50	1.093	19.61×10^{-6}	17.95×10^{-6}	25.722×10^{-6}	0.698	1005	0.02826
60	1.060	20.10×10^{-6}	18.97×10^{-6}	27.194×10^{-6}	0.696	1005	0.02896
70	1.029	20.59×10^{-6}	20.02×10^{-6}	28.556×10^{-6}	0.694	1009	0.02966
80	1.000	21.08×10^{-6}	21.09×10^{-6}	30.194×10^{-6}	0.692	1009	0.03047
90	0.972	21.48×10^{-6}	22.10×10^{-6}	31.889×10^{-6}	0.690	1009	0.03128
100	0.946	21.87×10^{-6}	23.13×10^{-6}	33.639×10^{-6}	0.688	1009	0.03210
120	0.898	22.85×10^{-6}	25.45×10^{-6}	36.833×10^{-6}	0.686	1009	0.03338
140	0.854	23.73×10^{-6}	27.80×10^{-6}	40.333×10^{-6}	0.684	1013	0.03489
160	0.815	24.52×10^{-6}	30.09×10^{-6}	43.889×10^{-6}	0.682	1017	0.03640
180	0.779	25.30×10^{-6}	32.49×10^{-6}	47.500×10^{-6}	0.681	1022	0.03780
200	0.746	25.99×10^{-6}	34.85×10^{-6}	51.361×10^{-6}	0.680	1026	0.03931
250	0.674	27.36×10^{-6}	40.61×10^{-6}	58.500×10^{-6}	0.677	1038	0.04268
300	0.615	29.71×10^{-6}	48.20×10^{-6}	71.556×10^{-6}	0.674	1047	0.04605
350	0.566	31.38×10^{-6}	55.46×10^{-6}	81.861×10^{-6}	0.676	1059	0.04908
400	0.524	33.05×10^{-6}	63.03×10^{-6}	93.111×10^{-6}	0.678	1067	0.05210
500	0.456	36.19×10^{-6}	79.38×10^{-6}	115.306×10^{-6}	0.687	1093	0.05745
600	0.404	39.13×10^{-6}	96.89×10^{-6}	138.611×10^{-6}	0.699	1114	0.06222
700	0.362	41.78×10^{-6}	115.40×10^{-6}	163.389×10^{-6}	0.706	1135	0.06687
800	0.329	44.33×10^{-6}	134.80×10^{-6}	189.444×10^{-6}	0.713	1156	0.07176
900	0.301	46.68×10^{-6}	155.10×10^{-6}	216.222×10^{-6}	0.717	1172	0.07629
1000	0.277	49.03×10^{-6}	178.00×10^{-6}	246.667×10^{-6}	0.719	1185	0.08071
1100	0.257	51.19×10^{-6}	199.30×10^{-6}	276.250×10^{-6}	0.722	1197	0.08502
1200	0.239	53.45×10^{-6}	223.70×10^{-6}	316.500×10^{-6}	0.724	1210	0.09153

1 W/mK = 0.86 kcal/m hr °C, 1 J/kg K = 238.9×10^{-6} kcal/kg °C, Ns/m^2 = 0.102 $kgfs/m^2$

PROPERTY VALUES OF GASES AT ONE ATMOSPHERIC PRESSURE (*Contd..*)

Temperature t °C	*Density* ρ kg/m^3	*Absolute Viscosity* μ Ns/m^2	*Kinematic Viscosity* ν m^2/s	*Thermal Diffusivity* α m^2/s	*Prandtl Number* Pr	*Specific Heat* c_p J/kgK	*Thermal Conductivity* k W/mK
NITROGEN							
0	1.250	16.67×10^{-6}	13.30×10^{-6}	19.139×10^{-6}	0.705	1030	0.02431
100	0.916	20.69×10^{-6}	22.50×10^{-6}	32.222×10^{-6}	0.678	1034	0.03152
200	0.723	24.22×10^{-6}	33.60×10^{-6}	50.833×10^{-6}	0.656	1043	0.03850
300	0.597	27.65×10^{-6}	46.40×10^{-6}	70.833×10^{-6}	0.652	1059	0.04489
400	0.508	30.89×10^{-6}	60.90×10^{-6}	92.500×10^{-6}	0.659	1080	0.05071
500	0.442	33.93×10^{-6}	76.90×10^{-6}	114.167×10^{-6}	0.672	1105	0.05582
600	0.392	36.87×10^{-6}	94.30×10^{-6}	136.389×10^{-6}	0.689	1130	0.06036
700	0.352	39.62×10^{-6}	113.00×10^{-6}	158.333×10^{-6}	0.710	1151	0.06420
800	0.318	42.27×10^{-6}	133.00×10^{-6}	181.667×10^{-6}	0.734	1168	0.06745
900	0.291	45.01×10^{-6}	154.00×10^{-6}	203.056×10^{-6}	0.762	1189	0.07013
1000	0.268	47.46×10^{-6}	177.00×10^{-6}	222.778×10^{-6}	0.795	1202	0.07234
OXYGEN							
0	1.429	19.42×10^{-6}	13.6×10^{-6}	18.889×10^{-6}	0.720	913	0.02466
100	1.050	24.12×10^{-6}	23.1×10^{-6}	33.611×10^{-6}	0.686	934	0.03291
200	0.826	28.54×10^{-6}	34.6×10^{-6}	43.333×10^{-6}	0.674	963	0.04071
300	0.682	32.46×10^{-6}	47.8×10^{-6}	70.556×10^{-6}	0.673	997	0.04803
400	0.580	36.28×10^{-6}	62.8×10^{-6}	92.500×10^{-6}	0.675	1022	0.05501
500	0.504	40.01×10^{-6}	79.6×10^{-6}	116.667×10^{-6}	0.682	1047	0.06152
600	0.447	43.54×10^{-6}	97.8×10^{-6}	141.111×10^{-6}	0.689	1068	0.06745
700	0.402	46.97×10^{-6}	117.0×10^{-6}	166.667×10^{-6}	0.700	1084	0.07280
800	0.363	50.21×10^{-6}	138.0×10^{-6}	194.444×10^{-6}	0.710	1101	0.07769
900	0.333	53.45×10^{-6}	161.0×10^{-6}	221.389×10^{-6}	0.725	1114	0.08199
1000	0.306	56.49×10^{-6}	184.0×10^{-6}	250.000×10^{-6}	0.738	1122	0.08583
CARBON MONOXIDE							
0	1.250	16.57×10^{-6}	13.3×10^{-6}	17.944×10^{-6}	0.740	1038	0.02326
100	0.916	20.69×10^{-6}	22.6×10^{-6}	31.389×10^{-6}	0.718	1043	0.03012
200	0.723	24.42×10^{-6}	33.9×10^{-6}	49.722×10^{-6}	0.708	1059	0.03652
300	0.596	27.95×10^{-6}	47.0×10^{-6}	66.111×10^{-6}	0.709	1080	0.04257
400	0.508	31.19×10^{-6}	61.8×10^{-6}	86.389×10^{-6}	0.711	1105	0.04850
500	0.442	34.42×10^{-6}	78.0×10^{-6}	108.056×10^{-6}	0.720	1130	0.05408
600	0.392	37.36×10^{-6}	96.0×10^{-6}	131.667×10^{-6}	0.727	1156	0.05966
700	0.351	40.40×10^{-6}	115.0×10^{-6}	157.222×10^{-6}	0.733	1181	0.06501
800	0.317	43.25×10^{-6}	135.0×10^{-6}	185.278×10^{-6}	0.739	1197	0.07013
900	0.291	45.99×10^{-6}	157.0×10^{-6}	213.333×10^{-6}	0.740	1214	0.07548
1000	0.268	48.74×10^{-6}	180.0×10^{-6}	244.722×10^{-6}	0.744	1231	0.08060

1 W/mK = 0.86 kcal/m hr °C, 1 J/kg K = 238.9×10^{-6} kcal/kg °C, 1 Ns/m^2 = 0.102 $kgfs/m^2$

PROPERTY VALUES OF GASES AT ONE ATMOSPHERIC PRESSURE (*Contd.*)

Temperature t °C	*Density* ρ kg/m^3	*Absolute Viscosity* μ Ns/m^2	*Kinematic Viscosity* ν m^2/s	*Thermal Diffusivity* α m^2/s	*Prandtl Number* Pr	*Specific Heat* c_p J/kgK	*Thermal Conductivity* k W/mK
CARBON DIOXIDE							
0	1.977	14.02×10^{-6}	7.09×10^{-6}	9.111×10^{-6}	0.780	816	0.01465
100	1.477	18.24×10^{-6}	12.60×10^{-6}	17.250×10^{-6}	0.733	913	0.02279
200	1.143	22.36×10^{-6}	19.20×10^{-6}	27.306×10^{-6}	0.715	992	0.03094
300	0.944	26.38×10^{-6}	27.30×10^{-6}	39.167×10^{-6}	0.712	1055	0.03908
400	0.802	30.20×10^{-6}	36.70×10^{-6}	53.056×10^{-6}	0.709	1109	0.04722
500	0.698	33.93×10^{-6}	47.20×10^{-6}	68.333×10^{-6}	0.713	1156	0.05489
600	0.618	37.66×10^{-6}	58.30×10^{-6}	85.556×10^{-6}	0.723	1193	0.06210
700	0.555	41.09×10^{-6}	71.40×10^{-6}	101.667×10^{-6}	0.730	1223	0.06885
800	0.502	44.62×10^{-6}	85.30×10^{-6}	120.000×10^{-6}	0.741	1248	0.07513
900	0.460	48.15×10^{-6}	100.00×10^{-6}	138.611×10^{-6}	0.757	1273	0.08094
1000	0.423	51.48×10^{-6}	116.00×10^{-6}	158.056×10^{-6}	0.770	1290	0.08629
SULPHUR DIOXIDE							
0	2.926	12.06×10^{-6}	4.14×10^{-6}	4.722×10^{-6}	0.874	607	0.00837
100	2.140	16.08×10^{-6}	7.51×10^{-6}	8.722×10^{-6}	0.863	662	0.01233
200	1.690	20.01×10^{-6}	11.80×10^{-6}	12.444×10^{-6}	0.856	712	0.01663
300	1.395	23.83×10^{-6}	17.10×10^{-6}	20.139×10^{-6}	0.848	754	0.02128
400	1.185	27.56×10^{-6}	23.30×10^{-6}	27.778×10^{-6}	0.834	783	0.02582
500	1.033	31.28×10^{-6}	30.40×10^{-6}	36.667×10^{-6}	0.822	808	0.03070
600	0.916	35.01×10^{-6}	38.30×10^{-6}	47.222×10^{-6}	0.806	825	0.03580
700	0.892	38.64×10^{-6}	46.80×10^{-6}	59.722×10^{-6}	0.788	837	0.04105
800	0.743	42.17×10^{-6}	56.50×10^{-6}	73.333×10^{-6}	0.776	850	0.04629
900	0.681	45.70×10^{-6}	66.80×10^{-6}	88.889×10^{-6}	0.755	858	0.05187
1000	0.626	49.23×10^{-6}	78.30×10^{-6}	106.111×10^{-6}	0.740	867	0.05757
FLUE GASES							
0	1.295	15.78×10^{-6}	12.20×10^{-6}	16.889×10^{-6}	0.720	1043	0.02279
100	0.950	20.38×10^{-6}	21.54×10^{-6}	30.833×10^{-6}	0.690	1068	0.03128
200	0.748	24.49×10^{-6}	32.80×10^{-6}	48.889×10^{-6}	0.670	1097	0.04012
300	0.617	28.22×10^{-6}	45.81×10^{-6}	70.000×10^{-6}	0.650	1122	0.04838
400	0.525	31.68×10^{-6}	60.38×10^{-6}	94.167×10^{-6}	0.640	1151	0.05699
500	0.457	34.84×10^{-6}	76.30×10^{-6}	121.111×10^{-6}	0.630	1185	0.06559
600	0.405	37.85×10^{-6}	93.61×10^{-6}	150.833×10^{-6}	0.620	1214	0.07419

1 W/mK = 0.86 kcal/m hr °C 1 J/kg K = 238.9×10^{-6} kcal/kg °C 1Ns/m^2 = 0.102 kgfs/m^2

PROPERTY VALUES OF GASES AT ONE ATMOSPHERIC PRESSURE (*Contd.*)

Temperature t °C	*Density* ρ kg/m^3	*Absolute Viscosity* μ Ns/m^2	*Kinematic Viscosity* ν m^2/s	*Thermal Diffusivity* α m^2/s	*Prandtl Number* Pr	*Specific Heat* c_p J/kgK	*Thermal Conductivity* k W/mK
FLUE GASES (*Contd.*)							
700	0.363	40.68×10^{-6}	112.10×10^{-6}	183.889×10^{-6}	0.610	1239	0.08269
800	0.329	43.37×10^{-6}	131.80×10^{-6}	219.722×10^{-6}	0.600	1264	0.09153
900	0.301	45.90×10^{-6}	152.50×10^{-6}	258.056×10^{-6}	0.590	1290	0.10013
1000	0.275	48.35×10^{-6}	174.30×10^{-6}	303.333×10^{-6}	0.580	1306	0.10897
1100	0.257	50.69×10^{-6}	197.10×10^{-6}	345.556×10^{-6}	0.570	1323	0.11746
1200	0.240	52.98×10^{-6}	221.00×10^{-6}	392.500×10^{-6}	0.560	1340	0.12677
ARGON							
0	1.784	21.08×10^{-6}	11.8×10^{-6}	17.800×10^{-6}	0.663	519	0.01651
100	1.305	26.97×10^{-6}	20.6×10^{-6}	31.111×10^{-6}	0.661	519	0.02117
200	1.030	32.17×10^{-6}	31.2×10^{-6}	47.778×10^{-6}	0.653	519	0.02559
300	0.850	36.87×10^{-6}	43.4×10^{-6}	67.778×10^{-6}	0.640	519	0.02989
400	0.724	41.09×10^{-6}	56.7×10^{-6}	90.556×10^{-6}	0.628	519	0.03396
500	0.627	45.21×10^{-6}	72.0×10^{-6}	116.667×10^{-6}	0.619	519	0.03791
600	0.558	48.54×10^{-6}	87.0×10^{-6}	144.167×10^{-6}	0.604	519	0.03943
HELIUM							
0	0.178	18.73×10^{-6}	105×10^{-6}	153.33×10^{-6}	0.684	5204	0.14304
100	0.130	22.95×10^{-6}	176×10^{-6}	263.33×10^{-6}	0.667	5204	0.17910
200	0.103	26.97×10^{-6}	270×10^{-6}	397.22×10^{-6}	0.660	5204	0.21283
300	0.085	30.79×10^{-6}	362×10^{-6}	552.78×10^{-6}	0.656	5204	0.24423
400	0.072	34.32×10^{-6}	474×10^{-6}	730.56×10^{-6}	0.648	5204	0.27563
500	0.063	37.56×10^{-6}	611×10^{-6}	933.33×10^{-6}	0.642	5204	0.30471
600	0.056	40.31×10^{-6}	723×10^{-6}	1144.44×10^{-6}	0.631	5204	0.33262
HYDROGEN							
0	0.0899	8.36×10^{-6}	93×10^{-6}	135.00×10^{-6}	0.688	14069	0.17212
100	0.0657	10.30×10^{-6}	157×10^{-6}	231.67×10^{-6}	0.677	14482	0.21981
200	0.0519	12.06×10^{-6}	233×10^{-6}	350.00×10^{-6}	0.666	14504	0.26400
300	0.0428	13.83×10^{-6}	323×10^{-6}	494.44×10^{-6}	0.655	14533	0.30703
400	0.0364	15.40×10^{-6}	423×10^{-6}	655.56×10^{-6}	0.644	14581	0.34774
500	0.0317	16.77×10^{-6}	534×10^{-6}	833.33×10^{-6}	0.640	14662	0.38728
600	0.0281	18.34×10^{-6}	656×10^{-6}	1027.78×10^{-6}	0.635	14779	0.42682
700	0.0252	19.71×10^{-6}	785×10^{-6}	1230.56×10^{-6}	0.637	14930	0.46287

1 W/mK = 0.86 kcal/m hr °C 1 J/kg K = 238.9×10^{-6} kcal/kg °C 1Ns/m^2 = 0.102 kgfs/m^2

PROPERTY VALUES OF GASES AT ONE ATMOSPHERIC PRESSURE (*Contd.*)

Temperature t °C	*Density* ρ kg/m^3	*Absolute Viscosity* μ Ns/m^2	*Kinematic Viscosity* ν m^2/s	*Thermal Diffusivity* α m^2/s	*Prandtl Number* Pr	*Specific Heat* c_p J/kgK	*Thermal Conductivity* k W/mK
HYDROGEN (*Contd.*)							
800	0.0228	21.08×10^{-6}	924×10^{-6}	1452.78×10^{-6}	0.638	15115	0.50009
900	0.0209	22.36×10^{-6}	1070×10^{-6}	1675.00×10^{-6}	0.640	15312	0.53614
1000	0.0192	23.73×10^{-6}	1230×10^{-6}	1911.11×10^{-6}	0.644	15518	0.57103
AMMONIA							
0	0.771	9.36×10^{-6}	12.2×10^{-6}	13.361×10^{-6}	0.908	2043	0.02105
100	0.564	13.04×10^{-6}	23.2×10^{-6}	27.167×10^{-6}	0.852	2219	0.03396
200	0.445	16.67×10^{-6}	38.0×10^{-6}	45.833×10^{-6}	0.818	2399	0.04885
300	0.368	20.59×10^{-6}	56.4×10^{-6}	68.889×10^{-6}	0.812	2583	0.06548
400	0.313	24.32×10^{-6}	78.7×10^{-6}	97.500×10^{-6}	0.796	2747	0.08397
500	0.272	28.15×10^{-6}	105.0×10^{-6}	130.556×10^{-6}	0.793	2918	0.10362
600	0.241	31.97×10^{-6}	134.0×10^{-6}	168.333×10^{-6}	0.792	3082	0.12444
700	0.221	35.99×10^{-6}	168.0×10^{-6}	210.556×10^{-6}	0.791	3245	0.14770
800	0.196	39.82×10^{-6}	205.0×10^{-6}	257.500×10^{-6}	0.793	3404	0.17096
900	0.179	44.13×10^{-6}	247.0×10^{-6}	308.333×10^{-6}	0.798	3555	0.19655
1000	0.165	47.86×10^{-6}	291.0×10^{-6}	363.889×10^{-6}	0.800	3710	0.22213
TOLUENE—C_7H_8							
0	—	6.61×10^{-6}	—	—	0.748	1030	0.01291
100	—	8.86×10^{-6}	—	—	—	1411	—
200	2.38	11.01×10^{-6}	4.65×10^{-6}	—	—	1750	—
300	1.96	13.24×10^{-6}	6.75×10^{-6}	—	—	2047	—
400	1.667	15.40×10^{-6}	9.23×10^{-6}	—	—	2294	—
500	1.45	17.46×10^{-6}	12.00×10^{-6}	—	—	2504	—
600	1.28	19.61×10^{-6}	15.30×10^{-6}	—	—	2671	—
CARBON TETRA CHLORIDE (REFRIGERANT-10) CCl_4							
0	—	9.24×10^{-6}	—	—	0.802	520	0.00599
100	5.020	12.31×10^{-6}	2.45×10^{-6}	2.944×10^{-6}	0.828	588	0.00873
200	3.970	15.30×10^{-6}	3.86×10^{-6}	4.722×10^{-6}	0.816	621	0.01163
300	3.275	18.24×10^{-6}	5.59×10^{-6}	7.000×10^{-6}	0.796	641	0.01465
400	2.790	21.18×10^{-6}	7.64×10^{-6}	9.750×10^{-6}	0.776	654	0.01779
500	2.420	24.03×10^{-6}	9.96×10^{-6}	13.111×10^{-6}	0.758	667	0.02117
600	2.150	26.87×10^{-6}	12.60×10^{-6}	16.889×10^{-6}	0.741	676	0.02454

1 W/mK = 0.86 kcal/m hr °C, 1 J/kg K = 238.9×10^{-6} kcal/kg °C, 1Ns/m^2 = 0.102 kgfs/m^2

PROPERTY VALUES OF GASES AT ONE ATMOSPHERIC PRESSURE *(Contd.)*

Temperature t °C	*Density* ρ kg/m^3	*Absolute Viscosity* μ Ns/m^2	*Kinematic Viscosity* ν m^2/s	*Thermal Diffusivity* α m^2/s	*Prandtl Number* Pr	*Specific Heat* c_p J/kgK	*Thermal Conductivity* k W/mK
ACETONE—C_3H_6O							
0	—	6.86×10^{-6}	—	—	0.886	1256	0.00972
100	1.870	9.41×10^{-6}	5.07×10^{-6}	6.056×10^{-6}	0.840	1537	0.01733
200	1.470	12.06×10^{-6}	8.22×10^{-6}	10.222×10^{-6}	0.806	1788	0.02687
300	1.220	14.71×10^{-6}	12.10×10^{-6}	15.667×10^{-6}	0.774	2022	0.03861
400	1.030	17.36×10^{-6}	16.90×10^{-6}	22.639×10^{-6}	0.743	2236	0.05210
500	0.901	20.01×10^{-6}	22.30×10^{-6}	30.833×10^{-6}	0.720	2428	0.06745
600	0.799	22.75×10^{-6}	28.30×10^{-6}	40.833×10^{-6}	0.695	2587	0.08467
BENZENE—C_6H_6							
0	—	6.98×10^{-6}	—	—	0.716	943	0.00922
100	2.55	7.21×10^{-6}	3.74×10^{-6}	5.111×10^{-6}	0.554	1335	0.01733
200	2.01	12.09×10^{-6}	5.99×10^{-6}	8.361×10^{-6}	0.719	1676	0.02814
300	1.66	14.64×10^{-6}	8.80×10^{-6}	12.833×10^{-6}	0.668	1957	0.04164
400	1.41	17.20×10^{-6}	12.10×10^{-6}	18.611×10^{-6}	0.652	2183	0.05757
500	1.23	19.76×10^{-6}	15.90×10^{-6}	26.222×10^{-6}	0.614	2369	0.07641
600	1.09	22.31×10^{-6}	20.40×10^{-6}	35.000×10^{-6}	0.585	2524	0.09630
STEAM							
100	0.598	11.96×10^{-6}	20.0×10^{-6}	19.222×10^{-6}	1.08	2135	0.02373
200	0.464	15.89×10^{-6}	30.6×10^{-6}	36.667×10^{-6}	0.94	1976	0.03349
300	0.384	20.01×10^{-6}	44.3×10^{-6}	57.222×10^{-6}	0.91	2014	0.04419
400	0.326	24.32×10^{-6}	60.5×10^{-6}	82.778×10^{-6}	0.90	2073	0.05594
500	0.284	28.64×10^{-6}	78.8×10^{-6}	112.778×10^{-6}	0.90	2135	0.06838
600	0.252	33.15×10^{-6}	99.8×10^{-6}	147.500×10^{-6}	0.89	2206	0.08176
700	0.226	37.85×10^{-6}	122.0×10^{-6}	186.111×10^{-6}	0.90	2273	0.09560
800	0.204	42.56×10^{-6}	147.0×10^{-6}	230.278×10^{-6}	0.91	2345	0.11025
900	0.187	47.46×10^{-6}	174.0×10^{-6}	275.833×10^{-6}	0.92	2416	0.12444
1000	0.172	52.37×10^{-6}	204.0×10^{-6}	330.556×10^{-6}	0.92	2483	0.14072

1 W/mK = 0.86 kcal/m hr °C, 1 J/kg K = 238.9×10^{-6} kcal/kg °C, 1Ns/m^2 = 0.102 kgfs/m^2

PROPERTY VALUES OF SATURATED STEAM (1 bar = 10^5 N/m^2)

Saturation Temperature t °C	*Saturation Pressure* P bar	*Density* ρ kg/m^3	*Absolute Viscosity* μ Ns/m^2 or kg/ms	*Kinematic Viscosity* ν m^2/s	*Thermal Diffusivity* α m^2/s	*Prandtl Number* Pr m^2/s	*Specific Heat* c_p J/kgK	*Thermal Conductivity* k W/mK
100	1.013	0.598	11.96×10^{-6}	20.000×10^{-6}	18.583×10^{-6}	1.08	2135	0.02373
110	1.433	0.826	12.45×10^{-6}	15.072×10^{-6}	13.833×10^{-6}	1.09	2177	0.02489
120	1.985	1.12	12.85×10^{-6}	11.473×10^{-6}	10.500×10^{-6}	1.09	2206	0.02593
130	2.701	1.50	13.24×10^{-6}	8.827×10^{-6}	7.972×10^{-6}	1.11	2257	0.02687
140	3.614	1.97	13.53×10^{-6}	6.868×10^{-6}	6.131×10^{-6}	1.12	2315	0.02803
150	4.670	2.55	13.93×10^{-6}	5.463×10^{-6}	4.728×10^{-6}	1.15	2395	0.02884
160	6.181	3.26	14.32×10^{-6}	4.393×10^{-6}	3.722×10^{-6}	1.18	2479	0.03012
170	7.920	4.12	14.71×10^{-6}	3.570×10^{-6}	2.939×10^{-6}	1.21	2583	0.03128
180	10.027	5.16	15.10×10^{-6}	2.926×10^{-6}	2.339×10^{-6}	1.25	2709	0.03268
190	12.551	6.40	15.59×10^{-6}	2.436×10^{-6}	1.872×10^{-6}	1.30	2885	0.03419
200	15.549	7.86	15.98×10^{-6}	2.033×10^{-6}	1.492×10^{-6}	1.34	2973	0.03547
210	19.077	9.58	16.37×10^{-6}	1.709×10^{-6}	1.214×10^{-6}	1.41	3098	0.03722
220	23.198	11.60	16.87×10^{-6}	1.454×10^{-6}	0.983×10^{-6}	1.47	3408	0.03896
230	27.976	14.00	17.36×10^{-6}	1.240×10^{-6}	0.806×10^{-6}	1.54	3634	0.04094
240	33.478	16.80	17.50×10^{-6}	1.042×10^{-6}	0.658×10^{-6}	1.61	3881	0.04291
250	39.776	20.00	18.24×10^{-6}	0.912×10^{-6}	0.544×10^{-6}	1.68	4158	0.04512
260	46.943	23.70	18.83×10^{-6}	0.795×10^{-6}	0.453×10^{-6}	1.75	4467	0.04803
270	55.058	28.10	19.32×10^{-6}	0.688×10^{-6}	0.378×10^{-6}	1.82	4815	0.05106
280	64.202	33.20	19.91×10^{-6}	0.600×10^{-6}	0.317×10^{-6}	1.90	5234	0.05489
290	74.461	39.20	20.59×10^{-6}	0.525×10^{-6}	0.261×10^{-6}	2.01	5694	0.05827
300	85.927	46.20	21.28×10^{-6}	0.461×10^{-6}	0.217×10^{-6}	2.13	6280	0.06269
310	98.700	54.60	21.97×10^{-6}	0.402×10^{-6}	0.175×10^{-6}	2.29	7118	0.06838
320	112.890	64.70	22.85×10^{-6}	0.353×10^{-6}	0.142×10^{-6}	2.50	8206	0.07513
330	128.630	77.00	23.93×10^{-6}	0.311×10^{-6}	0.108×10^{-6}	2.86	9881	0.08257
340	146.050	92.80	25.20×10^{-6}	0.272×10^{-6}	0.081×10^{-6}	3.35	12351	0.09304
350	165.350	114.00	26.58×10^{-6}	0.233×10^{-6}	0.058×10^{-6}	4.03	16245	0.10700
360	186.750	144.00	29.13×10^{-6}	0.202×10^{-6}	0.039×10^{-6}	5.23	23027	0.12793
370	210.540	202.00	33.73×10^{-6}	0.167×10^{-6}	0.014×10^{-6}	11.10	56522	0.17096

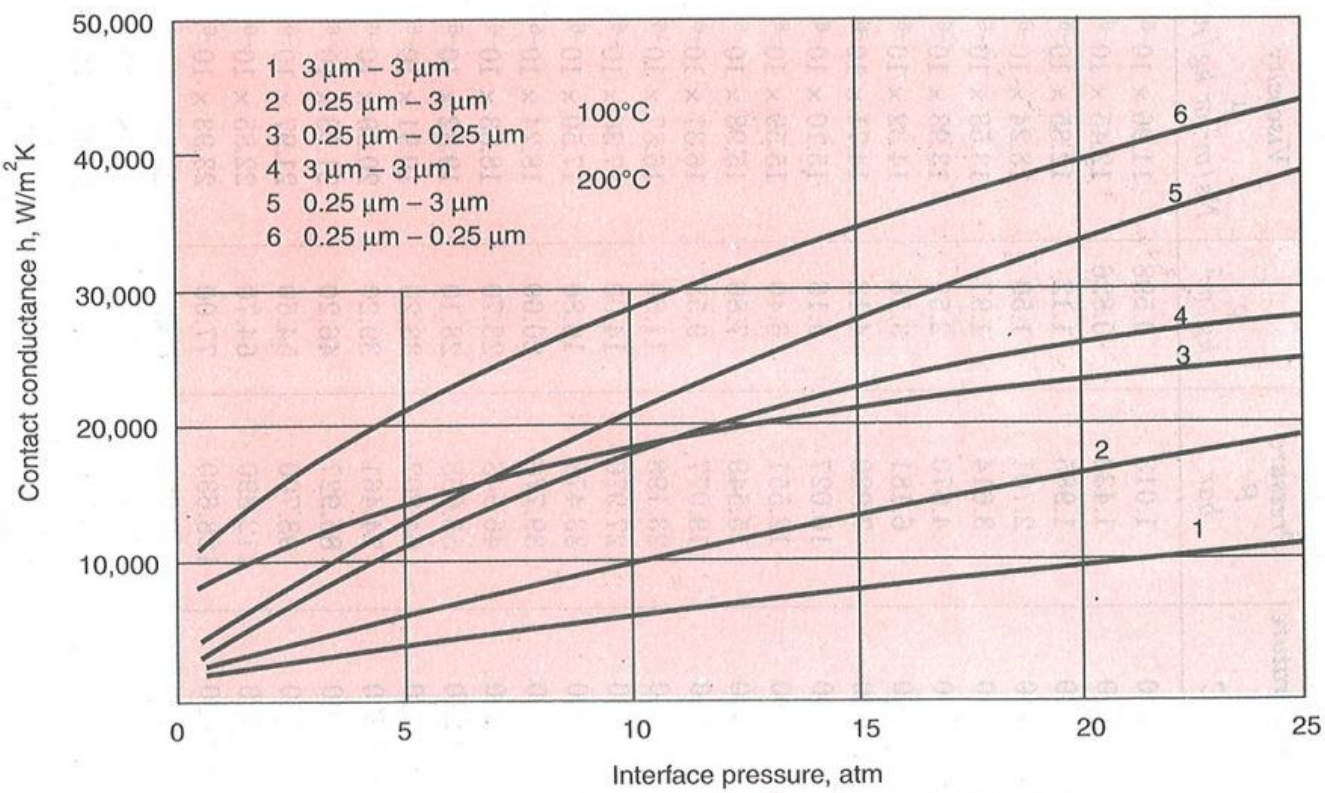
1 W/mK = 0.86 kcal/m hr °C 1 J/kg K = 238.9×10^{-6} kcal/kg °C 1Ns/m^2 = 0.102 kgfs/m^2

CONTACT RESISTANCE, 1/h OF TYPICAL SURFACES

Surface type	*Roughness* μm	*Temperature* °C	*Pressure* atm	*1/h* $m^2 K/W$
416 Stainless, ground, air	2.54	90–200	3–25	0.264×10^{-3}
304 Stainless, ground, air	1.14	20	40–70	0.528×10^{-3}
416 Stainless, ground, with 0.254 mm brass shim, air	2.54	30–200	7	0.352×10^{-3}
Aluminium, ground, air	2.54	150	12–25	0.088×10^{-3}
Aluminium, ground, air	0.25	150	12–25	0.018×10^{-3}
Aluminium, ground, with 0.254 mm brass shim, air	2.54	150	12–200	0.123×10^{-3}
Copper, ground, air	1.27	20	12–200	0.007×10^{-3}
Copper, milled, air	3.81	20	10–50	0.018×10^{-3}
Copper, milled, vacuum	0.25	30	7–70	0.088×10^{-3}

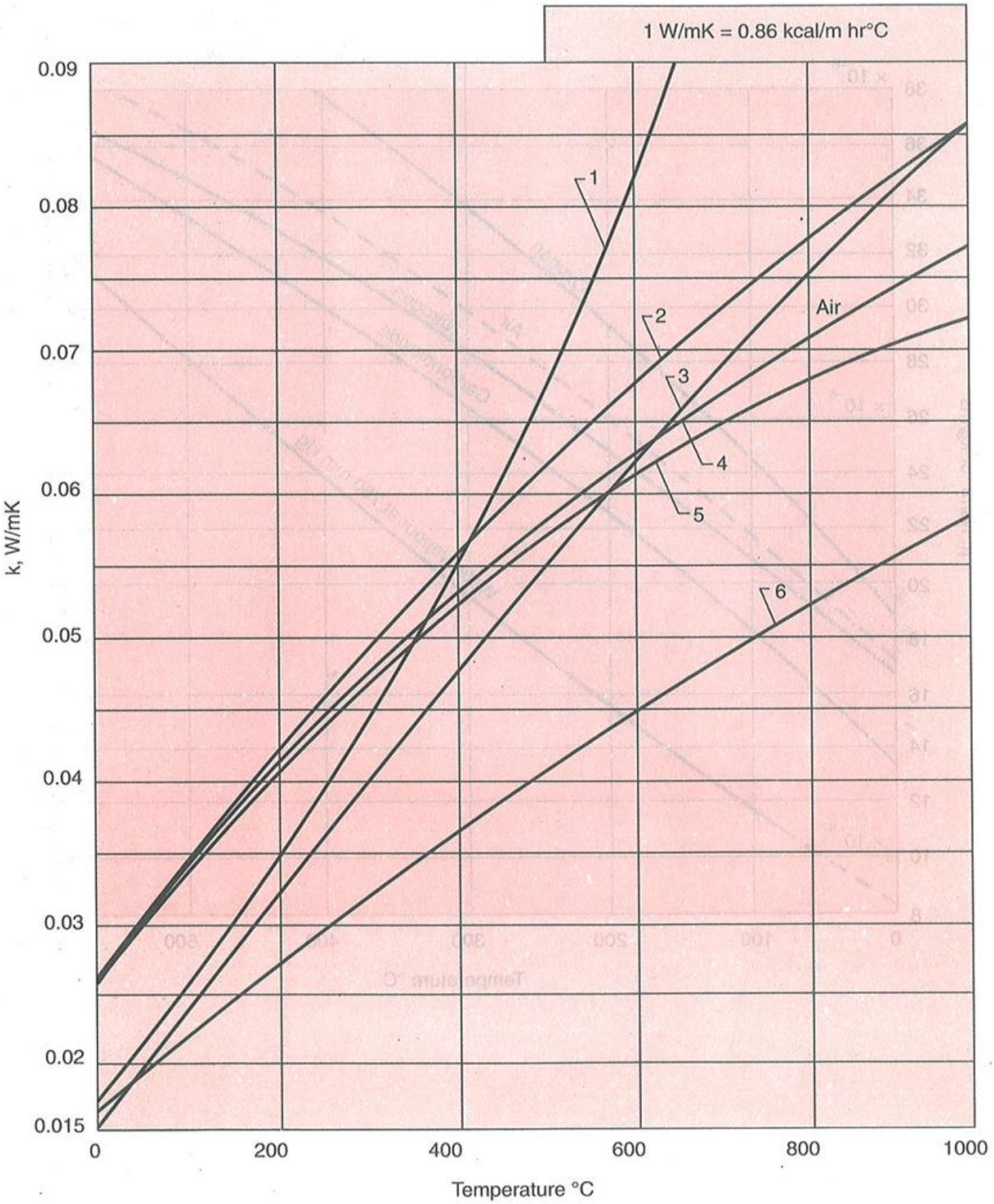
THERMAL CONDUCTIVITY OF AIR AT HIGHER PRESSURES, W/mK

Pressure, atm \ *Temperature °C*	*20*	*100*	*180*
1	0.0258	0.0307	0.0362
100	0.0280	0.0309	0.0367
200	0.0333	0.0372	0.0409
300	0.0385	0.0434	0.0450
400	0.0410	0.0475	0.0485



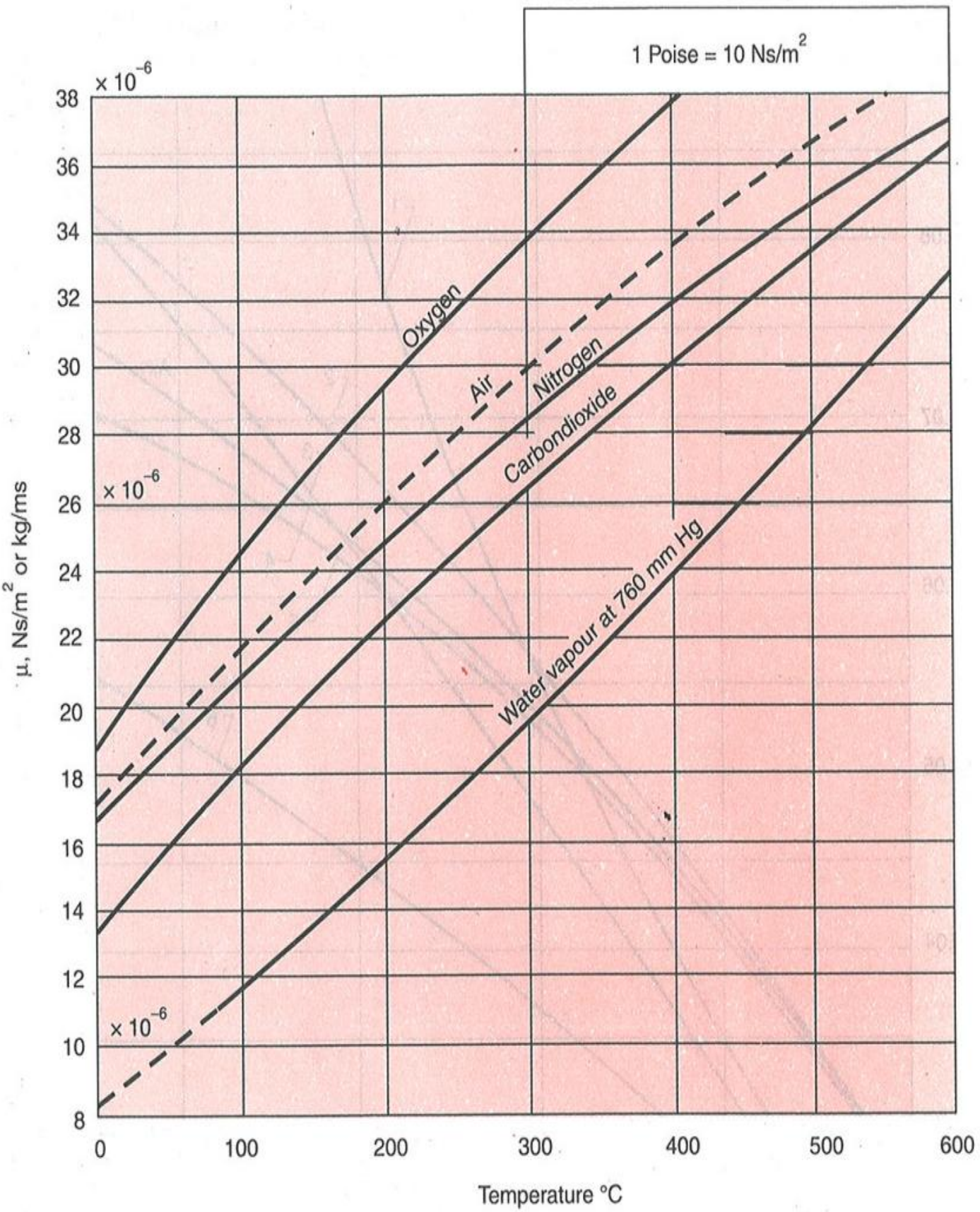
Variation of contact conductance of 7075 T6 aluminium joints

VARIATION OF THERMAL CONDUCTIVITY OF GASES WITH TEMPERATURE



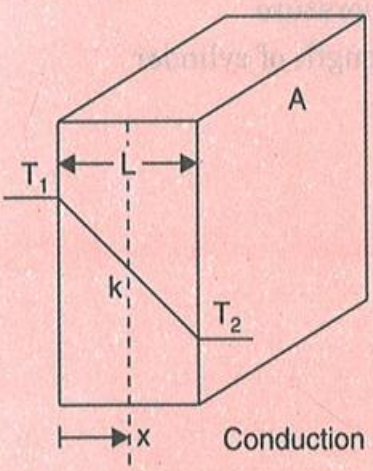
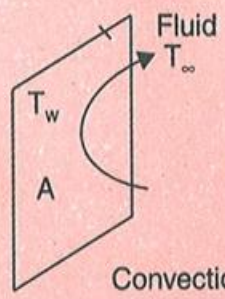
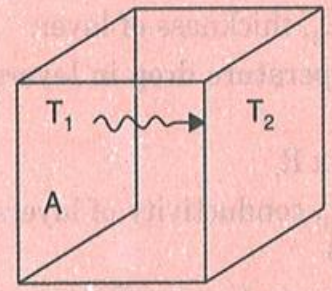
1 Water vapour
2 Oxygen
3 Carbon dioxide
4 Air
5 Nitrogen
6 Argon

RIATION OF ABSOLUTE VISCOSITY, μ, OF GASES WITH TEMPERATURE

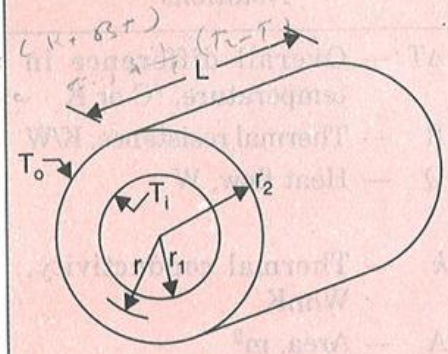
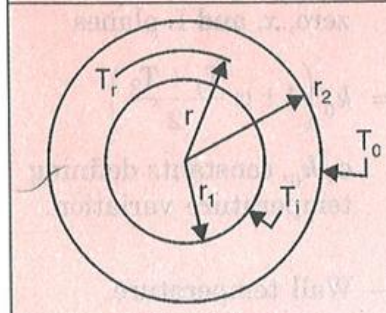
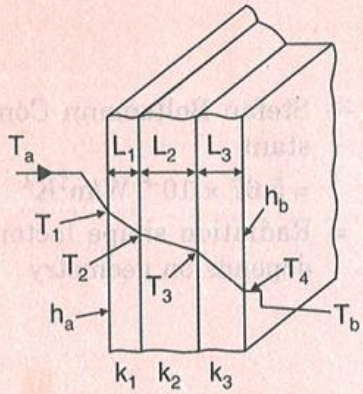


ONE DIMENSIONAL STEADY STATE HEAT TRANSFER

$$\text{Heat flow, } Q = \frac{\Delta T \text{ overall}}{R}$$

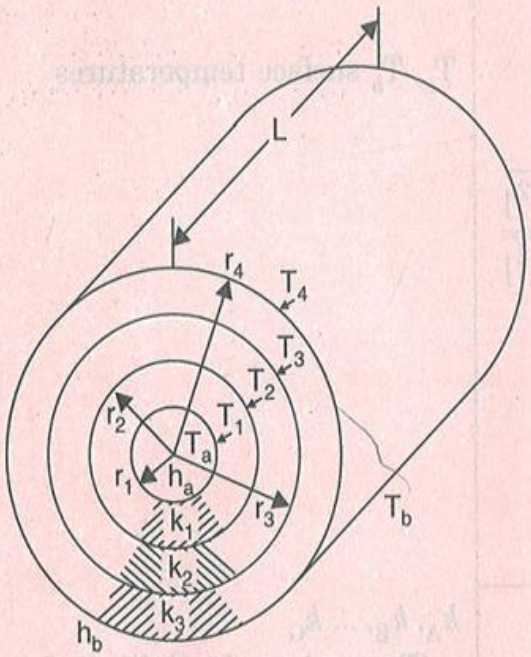
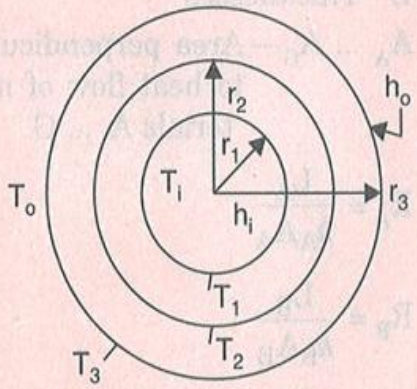
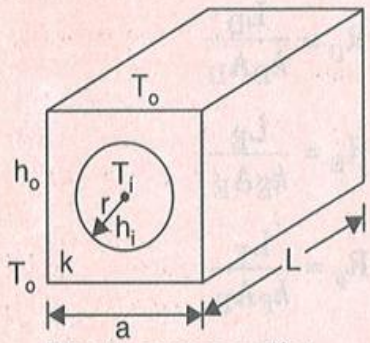
Description	*Correlation and Validity*	*Notations*
 Conduction	$R = \frac{L}{kA}$, $\frac{T_1 - T_x}{T_1 - T_2} = \frac{x}{L}$ Replace k by k_m for linear variation of thermal conductivity	ΔT — Overall difference in temperature, °C or K. R — Thermal resistance, K/W Q — Heat flow, W k — Thermal conductivity, W/mK A — Area, m^2 L — Thickness, m T_1, T_x, T_2 temperature at zero, x, and L planes $k_m = k_0\left(1 \pm \alpha \frac{T_1 + T_2}{2}\right)$ α, k_0, constants defining temperature variation. T_w — Wall temperature T_∞ — Fluid temperature h — Convective heat transfer coefficient, W/m^2K T_1, T_2, Radiating surface temperatures σ — Stefan Boltzmann Constant $= 5.67 \times 10^{-8}$ W/m^2K^4 F = Radiation shape factor, depends on geometry
 Convection	$R = \frac{1}{hA}$	
 Radiation-black surfaces	$\frac{1}{\sigma AF(T_1^2 + T_2^2)(T_1 + T_2)}$	

ONE DIMENSIONAL STEADY STATE HEAT CONDUCTION

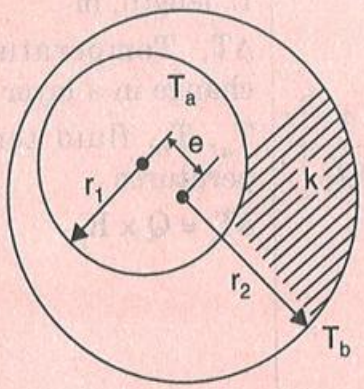
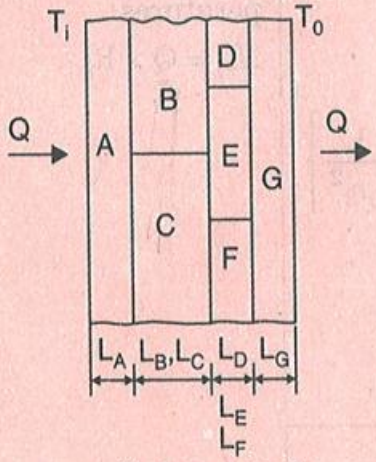
Description	*Correlation and Validity*	*Notations*
 Hollow cylinder	$R = \frac{1}{2\pi k L} \ln \frac{r_2}{r_1}$ $\frac{T_i - T_r}{T_i - T_0} = \frac{\ln \frac{r}{r_1}}{\ln \frac{r_2}{r_1}}$	r_1, r_2, inner and outer radii T_i, T_0, inner and outer surface temperature L, Length of cylinder
 Hollow sphere	$R = \frac{1}{4\pi k}\left(\frac{1}{r_1} - \frac{1}{r_2}\right)$ $\frac{T_i - T_r}{T_i - T_0} = \frac{\frac{1}{r_1} - \frac{1}{r}}{\frac{1}{r_1} - \frac{1}{r_2}}$	
 Composite plane wall, with convection on sides	$R = \frac{1}{A}\left[\frac{1}{h_a} + \frac{L_1}{k_1} + \frac{L_2}{k_2} + \frac{L_3}{k_3} + \frac{1}{h_b}\right]$	T_a, T_b, fluid temperature outside & inside L_1, L_2, L_3, thickness of layer. For temperature drop in layers use $\Delta T_i = Q \times R_i$ k_1, k_2, k_3, conductivity of layers 1, 2, & 3 h_a, h_b, convection coefficient at a and b, may or may not be present.

Note : ΔK or $\Delta°C$ in this chapter and in Convection indicate degree interval and hence identical.

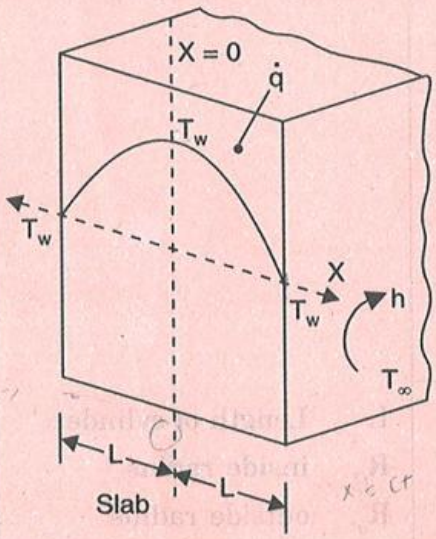
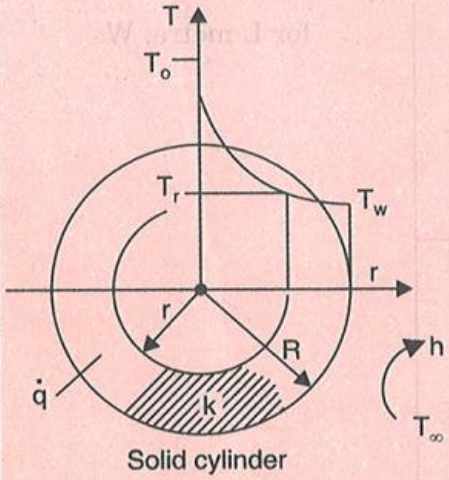
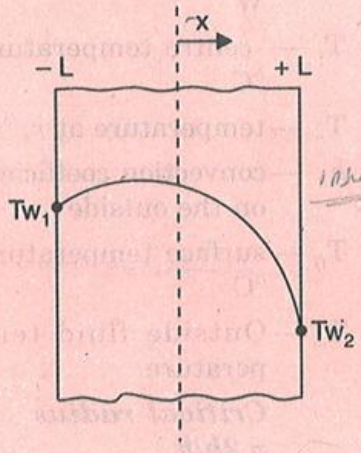
ONE DIMENSIONAL STEADY STATE HEAT CONDUCTION (*Contd.*)

Description	*Correlation and Validity*	*Notations*
 Composite cylinder, with convection	$R = \frac{1}{2\pi L}\left[\frac{1}{h_a r_1} + \frac{1}{k_1}\ln\left(\frac{r_2}{r_1}\right) + \frac{1}{k_2}\ln\left(\frac{r_3}{r_2}\right) + \frac{1}{k_3}\ln\left(\frac{r_4}{r_3}\right) + \frac{1}{h_b r_4}\right]$	r, radius, m L, length, m ΔT, Temperature change in a layer T_a, T_b, fluid temperatures $\Delta T_i = Q \times R_i$
 Composite sphere with convection	$R = \frac{1}{4\pi}\left[\frac{1}{h_i r_i^2} + \frac{1}{k_1}\left[\frac{1}{r_1} - \frac{1}{r_2}\right] + \frac{1}{k_2}\left[\frac{1}{r_2} - \frac{1}{r_3}\right] + \frac{1}{h_0 r_3^2}\right]$	T_i, T_0, fluid temperatures $\Delta T_i = Q \times R_i$
 Pipe in square section	$R = \frac{1}{2\pi L}\left[\frac{1}{h_i r} + \frac{L}{k}\ln\frac{1.08a}{2r} + \frac{\pi}{2h_0 a}\right]$	a side of square r radius of cylinder

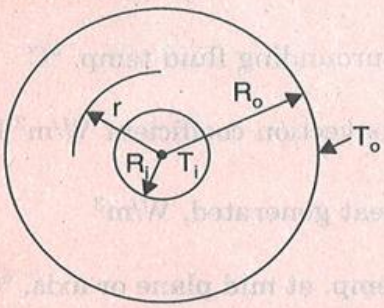
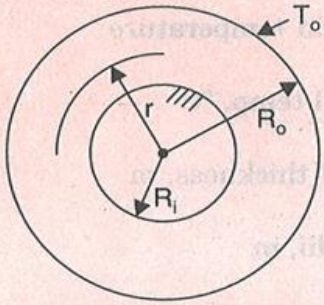
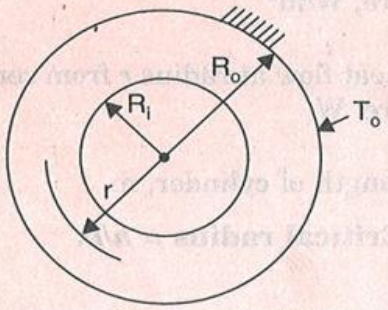
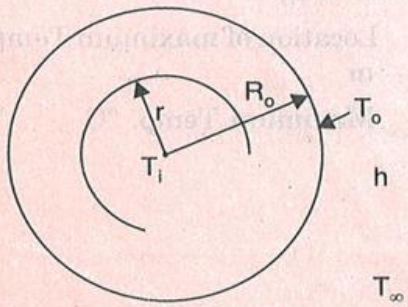
ONE DIMENSIONAL STEADY STATE HEAT CONDUCTION (*Contd.*)

Description	*Correlation and Validity*	*Notations*
 Pipe with eccentric lagging of length L	$R = \frac{1}{2\pi k L} \ln \frac{\sqrt{[(r_2+r_1)^2 - e^2]} + \sqrt{[(r_2-r_1)^2 - e^2]}}{\sqrt{[(r_2+r_1)^2 - e^2]} - \sqrt{[(r_2-r_1)^2 - e^2]}}$	T_a, T_b surface temperatures
Series-Parallel Composite Layers  Surface area-A	$R = R_1 + R_2 + R_3 + R_4$ $R_1 = R_A$ $R_2 = \frac{R_B R_C}{R_B + R_C}$ $R_3 = \frac{R_D R_E R_F}{R_D R_E + R_E R_F + R_F R_D}$ $R_4 = R_G$ $A = A_A = A_B + A_C$ $= A_D + A_E + A_F = A_G$ In case of convection add to R resistances $\frac{1}{h_i A}$ and $\frac{1}{h_o A}$	$k_A, k_B, \ldots k_G$ —Thermal conductivities of A, B, ... G L—Thicknesses $A_A \ldots A_G$—Area perpendicular to heat flow of materials A, ... G $R_A = \frac{L_A}{k_A A_A}$ $R_B = \frac{L_B}{k_B A_B}$ $R_C = \frac{L_C}{k_C A_C}$ $R_D = \frac{L_D}{k_D A_D}$ $R_E = \frac{L_E}{k_E A_E}$ $R_F = \frac{L_F}{k_F A_F}$ $R_G = \frac{L_G}{k_G A_G}$

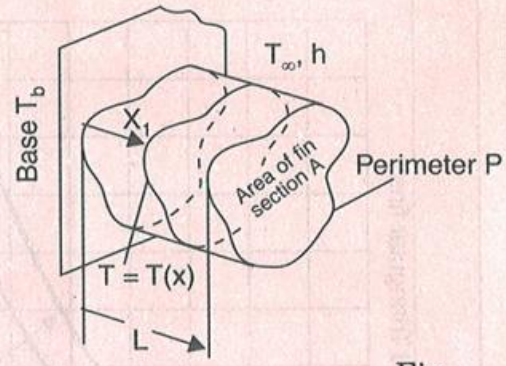
STEADY STATE CONDUCTION WITH HEAT GENERATION

Description	*Correlation and Validity*	*Notations*
	$T_o = T_w + \frac{\dot{q}}{2k} L^2$ $\frac{T_x - T_o}{T_w - T_o} = (x/L)^2$ $T_x = T_o - \frac{\dot{q}}{2k} x^2$ for outside convection $T_w = T_\infty + \frac{\dot{q}L}{h}$ $q_x = \dot{q} \times x$	T_∞ Surounding fluid temp. °C h convection coefficient W/m² K $\dot{q}$ heat generated, W/m³ T_0 temp. at mid plane or axis, °C T_x temp. at distance x from mid plane, °C T_∞ Fluid temperature T_w wall temp. °C L half thickness, m r, R radii, m T_r temp. at any radius r, °C q_x heat flow at plane x from centre, W/m² q_r heat flow at radius r from centre, W L length of cylinder, m **Critical radius = h/k.**
	$T_o = T_w + \dot{q}R^2/4k$ $\frac{T_r - T_w}{T_o - T_w} = 1 - (r/R)^2$ $T_r = T_w + \frac{\dot{q}}{4k}(R^2 - r^2)$ $q_r = \pi r^2 L \times \dot{q}$ for outside convection $T_w = T_\infty + \frac{\dot{q}R}{2h}$	
SLAB Asymmetric boundary condition 	$T_x = \frac{\dot{q}}{2k}(L^2 - x^2) + \frac{x}{2L} \times (T_{w2} - T_{w1}) + \frac{1}{2}(T_{w1} + T_{w2})$ $x_{max} = \frac{k}{2\dot{q}L}(T_{w2} - T_{w1})$ $T_{max} = \frac{\dot{q}L^2}{2k} + \frac{k}{8\dot{q}L^2} \times (T_{w1} - T_{w2})^2 + \frac{1}{2}(T_{w1} - T_{w2})$	T_{w1}, T_{w2} Surface temp. °C L half length x_{max} Location of maximum Temp. m T_{max} Maximum Temp. °C

STEADY STATE CONDUCTION WITH HEAT GENERATION (*Contd.*)

Description	*Correlation and Validity*	*Notations*
Hollow cylinder 	Heat flow on both sides $\frac{T_r - T_i}{T_o - T_i} = \frac{\ln (r/R_i)}{\ln (R_o/R_i)} + \frac{\dot{q}}{4k} \cdot \frac{R_o^2 - R_i^2}{T_o - T_i} \times \left[\frac{\ln \frac{r}{R_i}}{\ln r_o/r_i} - \frac{r^2 - R^2}{R_o^2 - R_i^2} \right]$	See figure R_o, R_i, T_o, T_i, r
Hollow cylinder Inside Adiabatic 	$T_r - T_o = \frac{\dot{q}}{4k} [R_o^2 - R_i^2] + \frac{\dot{q}}{2k} R_i^2 \ln \frac{r}{R_o}$ $T_i = T_o + \frac{\dot{q}}{4k} (R_o^2 - R_i^2) + \frac{\dot{q}}{2k} R_i^2 \ln \frac{R_i}{R_o}$ $q_r = \pi \dot{q} L[r^2 - R_i^2]$	L Length of cylinder R_i, inside radius R_o, outside radius q_r, heat flow at radius r for L metre, W
Hollow cylinder Outside adiabatic 	$T_r - T_i = \frac{\dot{q}}{2k} (R_i^2 - r^2) + \frac{\dot{q}}{2k} R_o^2 \ln \frac{r}{R_i}$ $q_r = \pi q L[R_0^2 - r^2]$ $T_o - T_i = \frac{\dot{q}}{2k} \cdot R_o^2 \ln \frac{R_o}{R_i} - \frac{\dot{q}}{4k} \times (R_o^2 - R_i^2)$	
Solid sphere 	$\frac{T_i - T_r}{T_i - T_o} = \left(\frac{r}{R_0}\right)^2$, $T_i = T_o + \frac{\dot{q}}{6k} \cdot R_o^2$ $\dot{q}_r = \dot{q} \frac{4}{3} \pi r^3$, $T_r - T_o = \frac{\dot{q}}{6k} (R_o^2 - r^2)$ for outside convection : $T_o = T_\infty + \frac{\dot{q} R_o}{3h}$, $T_r = T_i - \frac{\dot{q}}{6k} r^2$	q_r — heat flow at radius r, W T_i — centre temperature, °C T_r — temperature at r, °C h — convection coefficient on the outside T_0 — surface temperature, °C T_∞ — Outside fluid temperature ***Critical radius = 2h/k***

FINS OR EXTENDED SURFACES

Type of FIN boundary	Temperature distribution $\frac{T - T_\infty}{T_b - T_\infty}$	Heat transferred by fin Q	 Fin efficiency* η
LONG FIN ($T_L = T_\infty$)	e^{-mx}	$(T_b - T_\infty)\,(hPkA)^{0.5}$	—
SHORT FIN (end insulated)	$\frac{\cosh m(L - X)}{\cosh (mL)}$	$(hPkA)^{0.5}\,(T_b - T_\infty)\tanh (mL)$	$\frac{\tanh (mL)}{mL}$
SHORT FIN (end not insulated) $\frac{\cosh [m(L - X)] + (h_L/mk)\sinh [m(L - x)]}{\cosh (mL) + (h_L/mk)\sinh (mL)}$	$(T_b - T_\infty)\,\frac{\tanh (mL) + (h_L/mk)}{1 + (h_L/mk)\tanh (mL)}\,(hPkA)^{0.5}$	—	
SPECIFIED END TEMPERATURE at $x = L$, $T = T_L$ $\frac{\frac{T_L - T_\infty}{T_b - T_\infty}\sinh (mx) + \sinh [m(L - x)]}{\sinh (mL)}$	$[(T_b - T_\infty) + (T_L - T_\infty)]\,\frac{\cosh (mL) - 1}{\sinh (mL)}\,.\,(hPkA)^{0.5}$	—	

* Ratio of the actual heat transferred by fin to the heat transferable by fin, if the entire fin area were at base temperature.

$m = \sqrt{(hP/kA)}$, h_L—convection coefficient at the *tip*

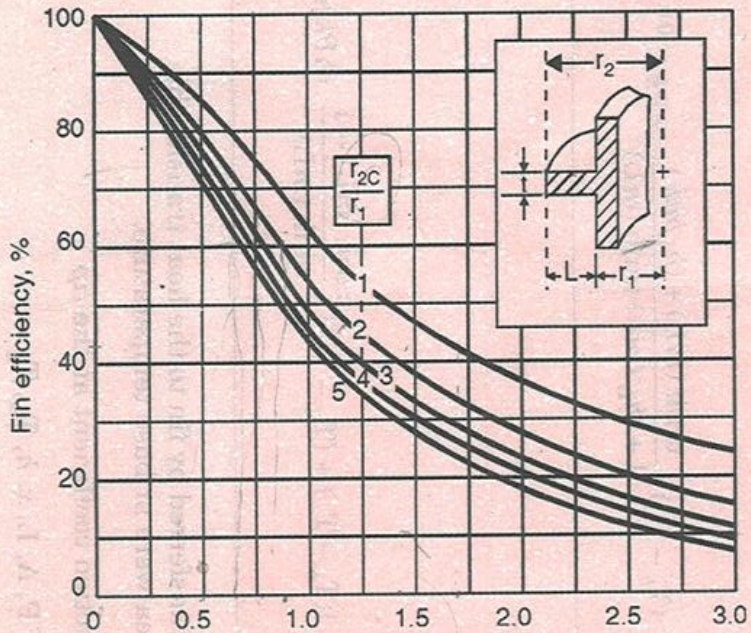
Refer figure for notions of P, A, L, x, h, T_∞, T_b

CIRCUMFERENTIAL, RECTANGULAR, TRIANGULAR FINS

$Q = \eta A_S h\,(T_b - T_\infty)$

η – *fin efficiency, fraction*

Circumferential rectangular fin



$$L_c^{1.5}\left(\frac{h}{kA_m}\right)^{0.5}$$

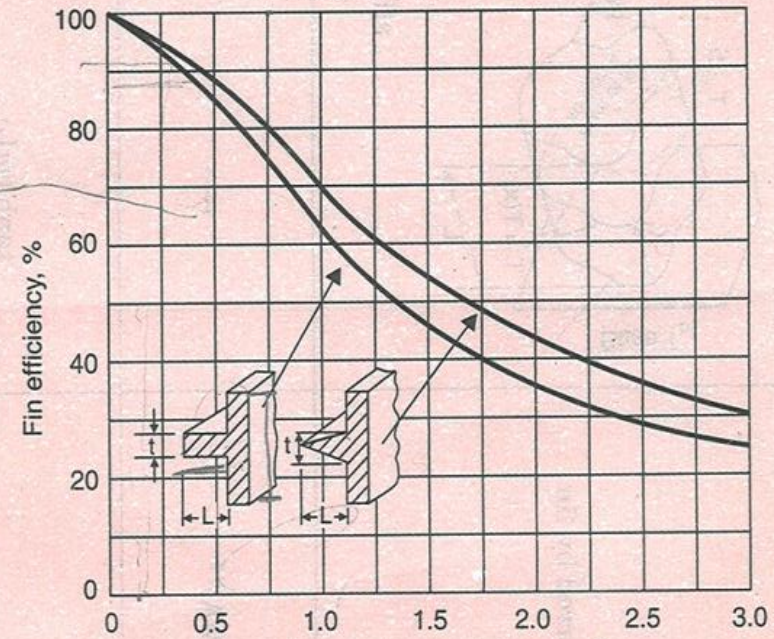
$$L_c = L + \frac{t}{2} \qquad r_{2c} = r_1 + L_c$$

$$A_m = t(r_{2c} - r_1) \qquad A_s = 2\pi\,(r_{2c}^2 - r_1^2)$$

$$\text{Also } \eta = \frac{\tanh\left[mL\sqrt{\left(1+\frac{r_2}{r_1}\right)\Big/2}\right]}{mL\sqrt{\left(1+\frac{r_2}{r_1}\right)\Big/2}}$$

where $m = \sqrt{2h/kt}$

Rectangular and Triangular fins



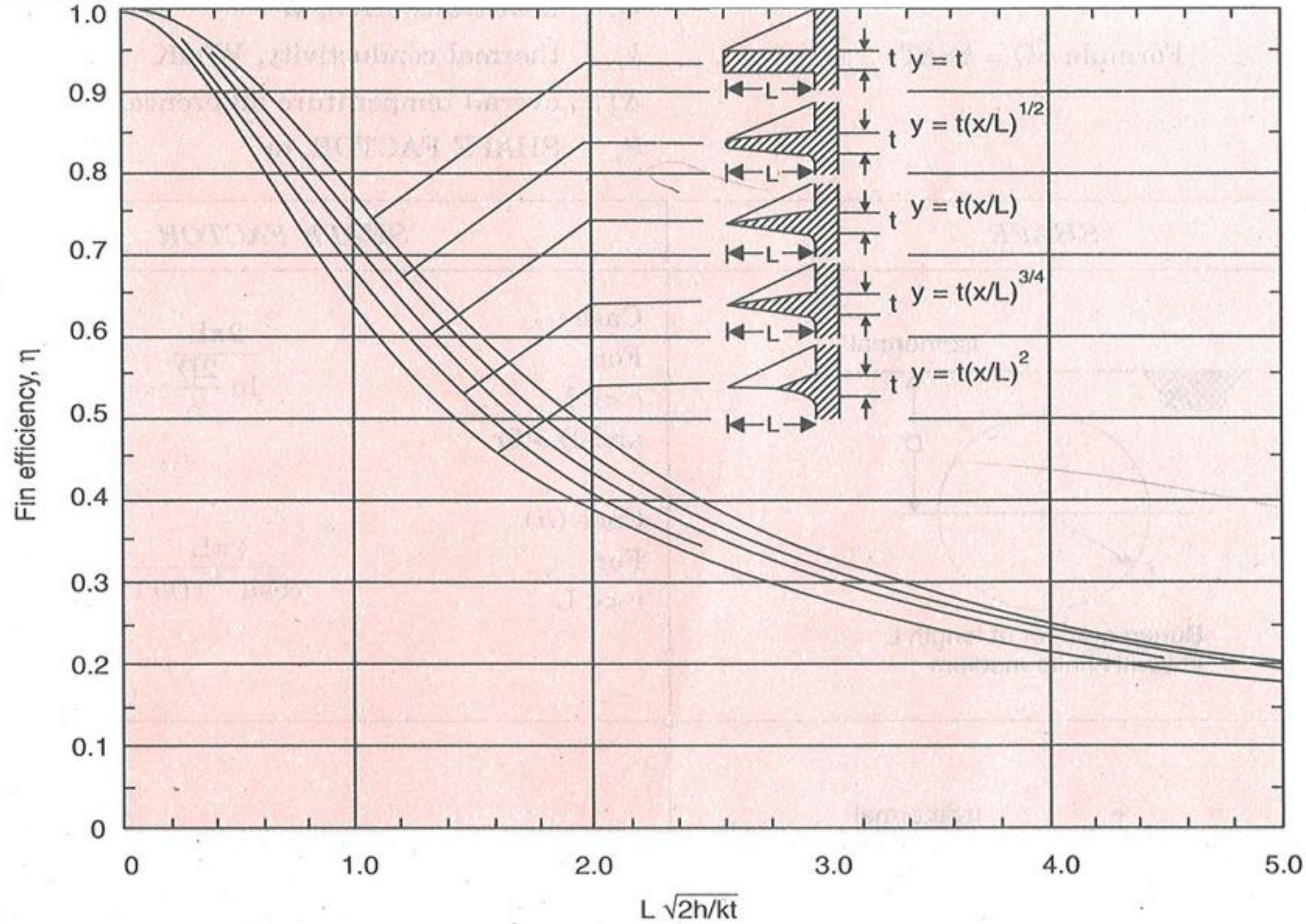
$$L_c^{1.5}\left(\frac{h}{kA_m}\right)^{0.5}$$

$$\left.\begin{aligned} L_c &= L + \frac{t}{2} \\ A_m &= tL_c \end{aligned}\right\} \text{Rectangular fin}$$

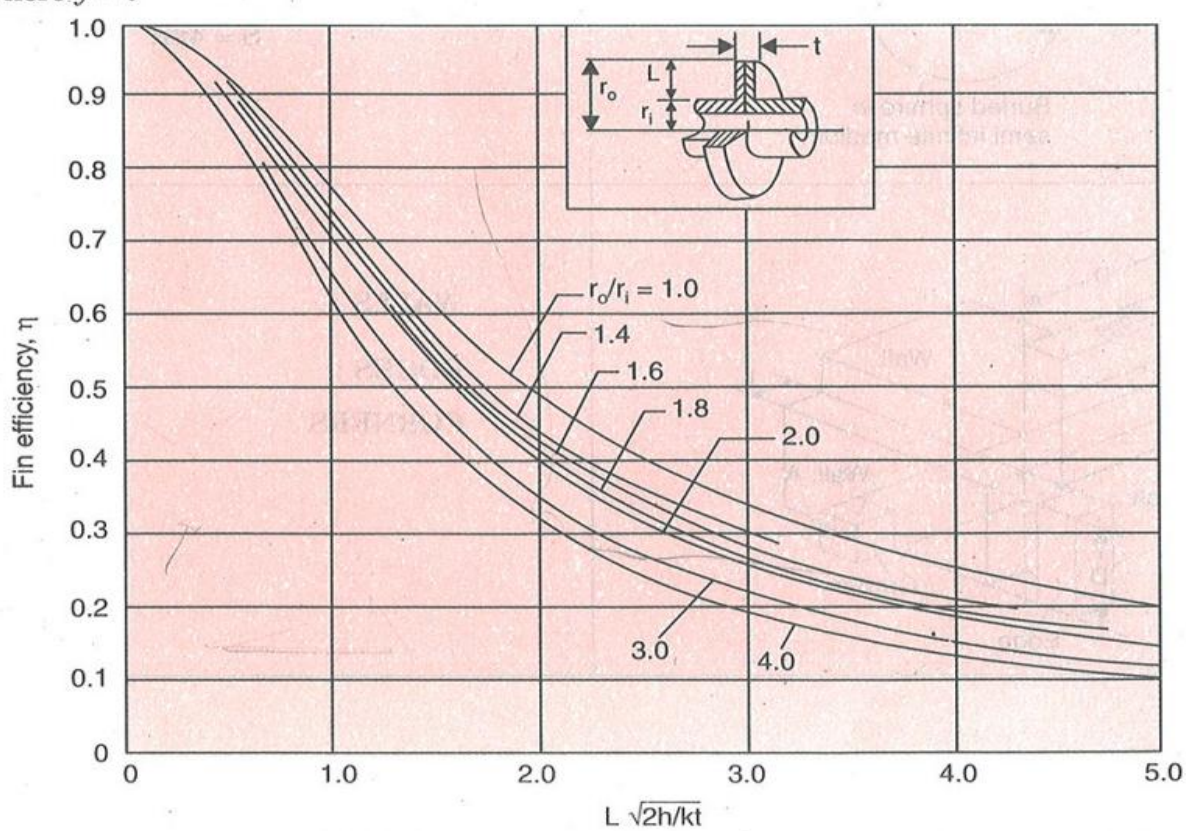
$$\left.\begin{aligned} L_c &= L \\ A_m &= \frac{t}{2}L \end{aligned}\right\} \text{Triangular fin}$$

$$A_s = 2L_c \times \text{Depth}$$

PLATE FINS AND DISC FINS



Efficiency of plate fins where the **fin thickness y** varies with the distance x from the root of the fin where $y = t$



Efficiency of circular disk fins of constant thickness

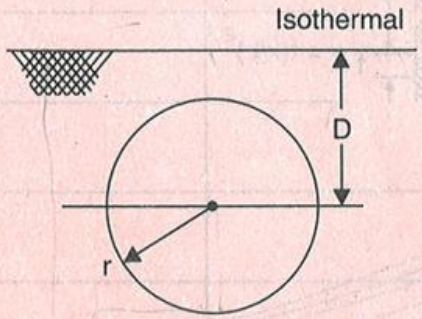
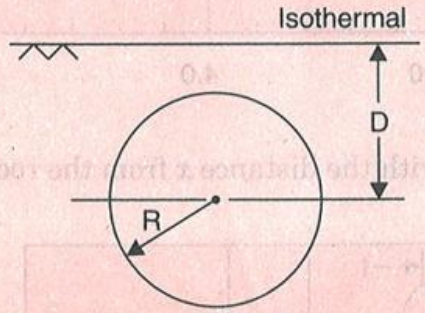
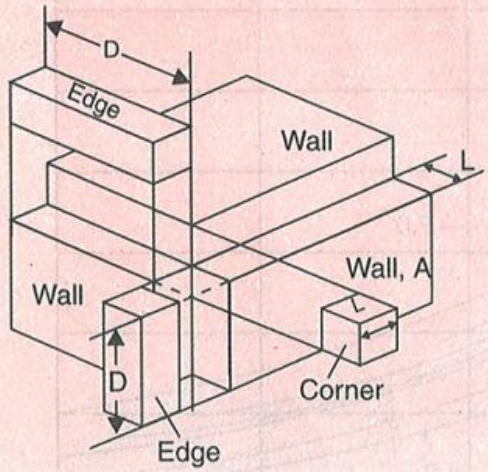
Formula : $Q = kS\Delta T$

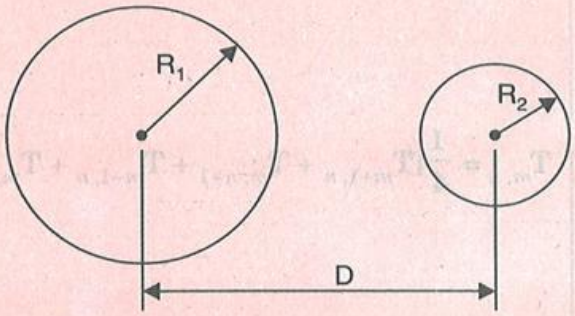
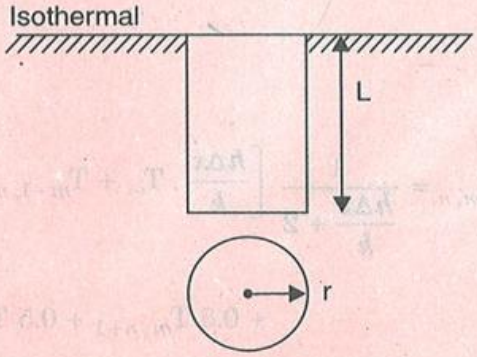
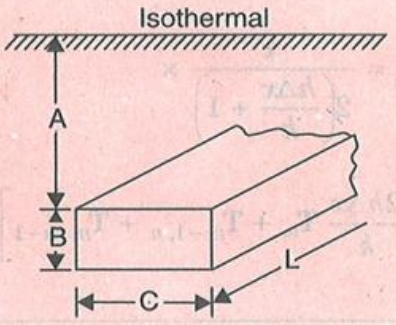
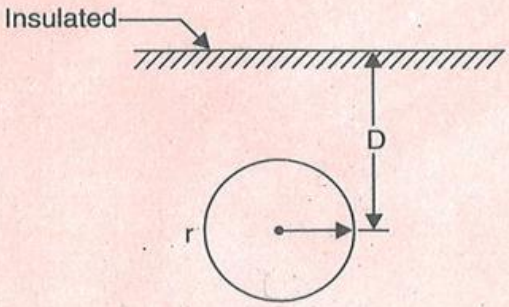
Q, heat transferred, W

k, thermal conductivity, W/mK

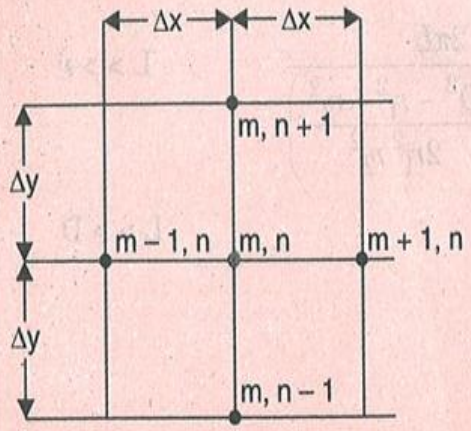
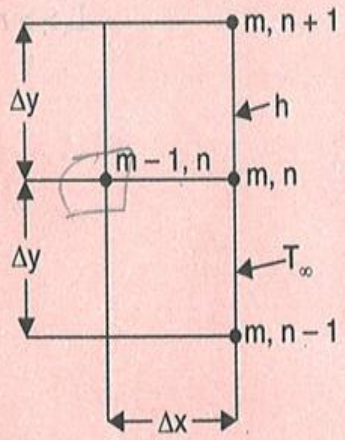
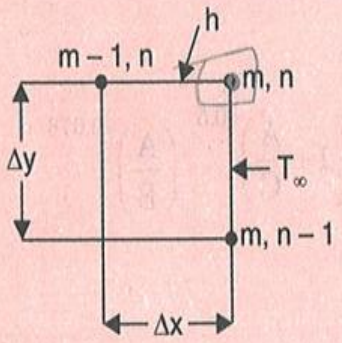
ΔT, overall temperature difference, °C or K

S, SHAPE FACTOR, m

SHAPE	*SHAPE FACTOR*
 Buried cylinder of length L in semi nfinite medium	Case (*i*) For $r << L$ and $D > 3r$ $\dfrac{2\pi L}{\ln \dfrac{2D}{r}}$ Case (*ii*) For $r << L$ $\dfrac{2\pi L}{\cosh^{-1}(D/r)}$
 Buried sphere in semi infinite medium	$\dfrac{4\pi R}{1-\left(\dfrac{R}{2D}\right)}$ In infinite medium $S = 4\pi R$
	WALLS : $\dfrac{A}{L}$ EDGES : 0.54 D CORNERS : 0.15 L

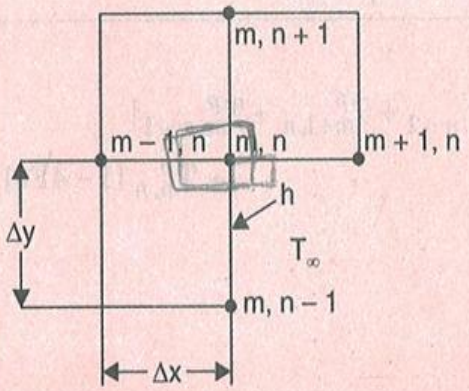
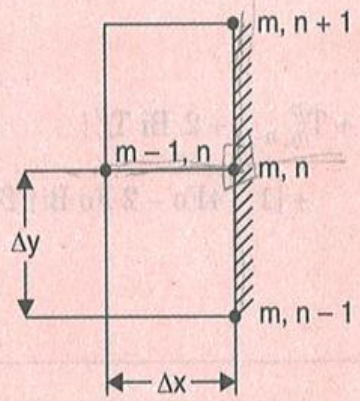
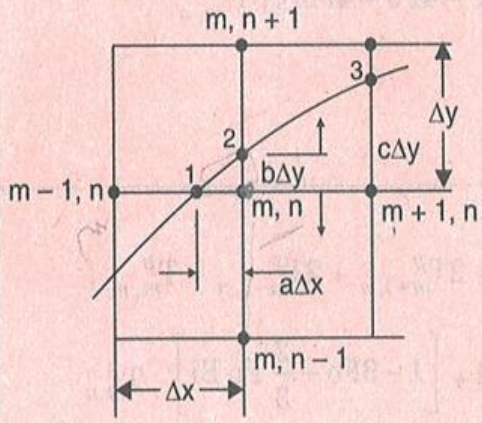
SHAPE	*SHAPE FACTOR*
Heat flow between, buried cylinders of length L 	$\dfrac{2\pi L}{\cosh^{-1}\left(\dfrac{D^2 - r_1^2 - r_2^2}{2r_1^2 r_2^2}\right)}$ L >> r L >> D
Vertical cylinder in semi infinite medium 	$\dfrac{2\pi L}{\ln\left(\dfrac{2L}{r}\right)}$ L >> r
Rectangular pipe in semi infinite medium 	$1.685L\left[\log\left[1+\dfrac{A}{C}\right]^{-0.5}\left(\dfrac{A}{B}\right)^{-0.078}\right.$
Sphere in Semi infinite medium with insulated surface 	$\dfrac{4\pi r}{1 + r/2D}$ D = D epth

TWO DIMENSIONAL NODAL EQUATIONS

	Description	*Nodal Temperature*
	Interior Node	$T_{m,n} = \frac{1}{4}[T_{m+1,n} + T_{m,n+1} + T_{m-1,n} + T_{m,n-1}]$
	Convection Boundary	$T_{m,n} = \frac{1}{\frac{h\Delta x}{k} + 2}\left[\frac{h\Delta x}{k} \cdot T_\infty + T_{m-1,n} + 0.5\,T_{m,n+1} + 0.5\,T_{m,n-1}\right]$
	Exterior Corner with convection boundary	$T_{m,n} = \frac{1}{2\left(\frac{h\Delta x}{k} + 1\right)} \times \left[\frac{2h\Delta x}{k} T_\infty + T_{m-1,n} + T_{m,n-1}\right]$

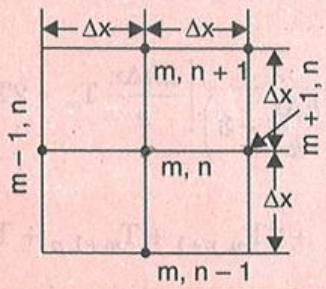
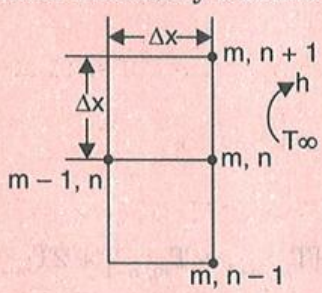
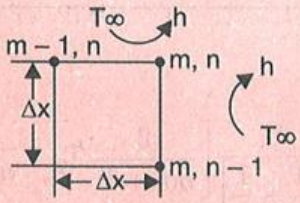
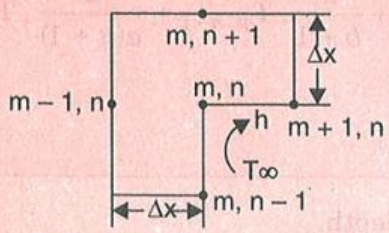
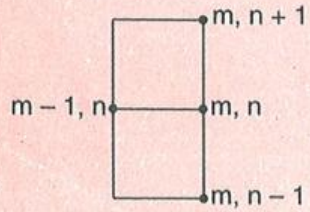
In case of residual equations use RHS – LHS = 0. It is assumed $\Delta x = \Delta y$

TWO DIMENSIONAL NODAL EQUATIONS (*Contd.*) :

	Description	*Nodal Temperature*
	Interior Corner with convection	$T_{m,n} = \frac{1}{2\left(\frac{h\Delta x}{k}+3\right)}\left[\frac{2h\Delta x}{k}T_\infty + 2T_{m-1,n} + 2T_{m,n+1} + T_{m+1,n} + T_{m,n-1}\right]$
	Insulated Boundary	$T_{m,n} = \frac{1}{4}\left[T_{m,n+1} + T_{m,n-1} + 2T_{m-1,n}\right]$
	Curved Boundary	$T_{m,n} = \frac{1}{2\left[\frac{1}{a}+\frac{1}{b}\right]}\left[\frac{2}{b(b+1)}T_2 + \frac{2}{a+1}T_{m+1,n} + \frac{2}{b+1}\cdot T_{m,n-1} + \frac{2}{a(a+1)}\cdot T_1\right]$

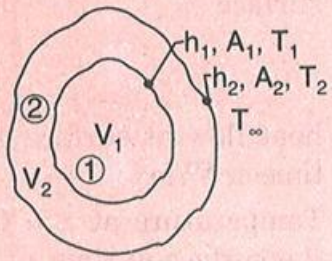
In residual equations take $\Delta x = \Delta y$ for unit depth.

TWO DIMENSIONAL NODAL EQUATIONS, TRANSIENT CONDUCTION m, n, Location, p, p + 1, time interval, $Fo = \frac{\alpha \cdot \Delta\tau}{\Delta x^2}$, $B_i = \frac{h\Delta x}{k}$

Node	*Nodal Temperature*
Internal Node 	$T^{p+1}_{m,n} = Fo\,[T^p_{m-1,n} + T^p_{m,n-1} + T^p_{m+1,n} + T^p_{m,n-1}] + T^p_{m,n}\,[1 - 4Fo]$ $Fo \le 0.25$
Convection Boundary surface Node 	$T^{p+1}_{m,n} = Fo\,[T^p_{m-1,n} + T^p_{m,n+1} + T^p_{m,n-1} + 2.\,Bi\,T^p_\infty] + [1 - 4Fo - 2\,Fo\,Bi]\,T^p_{m,n}$ $Fo\,(2 + Bi) \le 0.5$
External corner node with convection 	$T^{p+1}_{m,n} = 2Fo\,[2T^p_{m-1,n} + T^p_{m,n+1} + 2Bi\,T^p_\infty] + [1 - 4Fo - 4FoBi]\,T^p_{m,n}$ $Fo\,(1 + Bi) \le 0.25$
Internal Corner Node with Convection 	$T^{p+1}_{m,n} = \frac{2}{3}Fo\,[2T^p_{m,n+1} + 2T^p_{m+1,n} + 2T^p_{m-1,n} + T^p_{m,n-1} + 2Bi\,T^p_\infty] + \left[1 - 9Fo - \frac{2}{3}Fo\,Bi\right] \cdot T^p_{m,n}$ $Fo\,(3 + Bi) \le 0.75$
Insulated of surface Node 	$T^{p+1}_{m,n} = Fo\,[2T^p_{m-1,n} + T^p_{m,n+1} + T^p_{m,n-1}] + [1 - 4Fo]T^p_{m,n}$

TRANSIENT CONDUCTION

Lumped Parameter System

Description	*Correlation and Validity*	*Notations*
A body with high thermal conductivity suddenly exposed to a convective atmosphere	**Valid for** $\frac{hL}{k_s} < 0.1$ $\frac{T - T_\infty}{T_o - T_\infty} = \exp\left[-\frac{hA_s}{cV\rho}\tau\right]$ $= \exp[-Bi \cdot F_o]$ Time constant, τ_c = time at which, $\frac{T - T_\infty}{T_o - T_\infty} = \frac{1}{e}$ $\tau_c = c\rho V/hA_s$ $q = hA_s(T - T_\infty)$ $q_t = \rho cV[T - T_o]$	h — average convective heat transfer coefficient on the solid surface L — Significant length = $\frac{V}{A_s}$ V — volume, m^3, A_s — surface area, m^2 k_s — Thermal conductivity of solid τ — time, sec τ_c — time constant, sec T_o — Initial temperature of solid, °C T_∞ — surrounding fluid temperature, °C T — temperature of solid at time τ, Bi — Biot number, $\frac{hL}{k_s}$ F_o — Fourier Number, $\alpha\tau/L^2$ q — instantaneous heat flow rate, W q_t — total heat flow upto time τ, J c — Specific heat of solid, J/kgK ρ — Density of solid, kg/m^3 α — Thermal Diffusivity of solid, m^2/s
For composite system of two bodies  $T_1 = T_2 = T_o$ at $\tau = 0$	$\frac{T_1 - T_\infty}{T_o - T_\infty} = \frac{m_2}{m_1 - m_2} \cdot \exp.(m_1\tau)$ $- \frac{m_1}{m_2 - m_1}\exp(m_2\tau)$ $h_1A_1(T_1 - T_2) = -\rho_1c_1V_1 \cdot \frac{dT_1}{d\tau}$	h_i — contact onductance $m_1 = [-(K_1 + K_2 + K_3) + [(K_1 + K_2 + K_3)^2 - 4K_1K_3]^{0.5}]^{0.5}$ $m_2 = -(K_1 + K_2 + K_3)/2 - \frac{[(K_1 + K_2 + K_3)^2 - 4K_1K_3]^{0.5}}{2}$ $K_1 = \frac{h_1A_1}{\rho_1c_1V_1}$ $K_2 = \frac{h_1A_1}{\rho_2c_2V_2}$ $K_3 = \frac{h_2A_2}{\rho_2c_2V_2}$

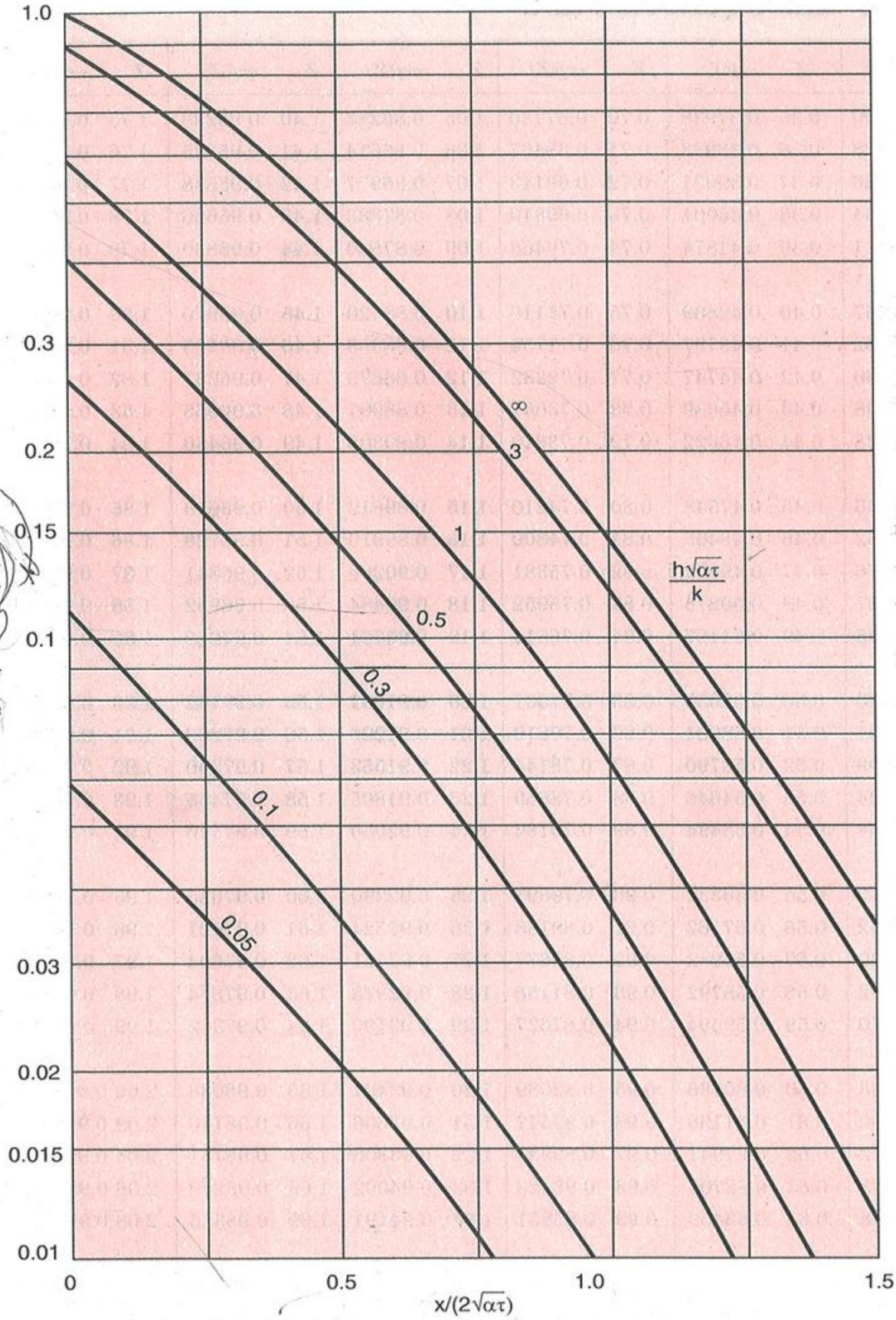
TRANSIENT CONDUCTION

Semi Infinite Solid

Description	*Correlation and Validity*	*Notation*
Surface temperature suddenly changed and maintained constant	$\frac{T_x - T_o}{T_i - T_o} = \text{erf}\,\frac{x}{2\sqrt{\alpha\tau}}$ $q_o = \frac{k(T_o - T_i)}{\sqrt{\pi\alpha\tau}}$ $q_x = \frac{k(T_o - T_i)}{\sqrt{\pi\alpha\tau}} \exp[-x^2/4\alpha\tau]$ $q_\tau = 2k(T_o - T_i]\sqrt{\frac{\tau}{\pi\alpha}}$ erf (Z) $= \frac{2}{\sqrt{\pi}}\left[z - \frac{z^3}{3\times 1!} + \frac{z^5}{5\times 2!} - \frac{z^7}{7\times 3!}\cdots\right]$	Refer charts in *p* 60,61 and 62 erf — error function of – refer tables next page T_x — Temperature at a distance x from surface at time τ T_o — Surface temperature T_i — Initial temperature of solid α — Thermal diffusivity of solid, m^2/s τ — time q_o — heat flux at surface at time τ, W/m^2 q_x — heat flux at location x at time τ. W/m^2 q_τ — Total heat flow into solid upto time τ per unit area, J/m^2
Body at T_i Suddenly exposed to constant heat flux q at surface,	q = applied constant heat flux at surface, per unit area $T_{x\tau} - T_i = \frac{2q(\alpha\tau/\pi)^{0.5}}{k} \cdot \exp\frac{-x^2}{4\alpha\tau} - \frac{qx}{k}\left[1 - \text{erf}\,\frac{x}{2\sqrt{\alpha\tau}}\right]$ At surface $(T_o/T_i) = 2\left(\frac{q}{k}\right)\left(\frac{\alpha\tau}{\pi}\right)^{0.5}$	x — location of plane considered from surface T_∞ — fluid temperature h — convective heat transfer coefficient k — thermal conductivity T_o — Surface temperature q — constant heat flux at surface
Body at T_i Surface suddenly exposed to a convective condition with constant fluid temperature T_∞ and convective heat transfer coefficient, h	$\frac{T_{x\tau} - T_i}{T_\infty - T_i} = \left[1 - \text{erf}\,\frac{x}{2\sqrt{\alpha\tau}}\right] - \exp\left[\frac{hx}{k} + \frac{h^2\alpha\tau}{k^2}\right]\left[1 - \text{erf}\left(\frac{x}{2\sqrt{\alpha\tau}} + \frac{h\sqrt{\alpha\tau}}{k}\right)\right]$ Alternately refer charts on page 60, 61 and 62 $q_s = h\,[T_\infty - T_o']$ At surface $\frac{T_o - T_i}{T_\infty - T_i}$ $= 1 - \left[1 - \text{erf}\left(\frac{h\sqrt{\alpha\tau}}{k}\right)\right] \cdot \exp\left(\frac{h^2\alpha\tau}{k^2}\right)$	q_s — heat flow at surface at time τ, W/m^2 T_o' — Temperature at $x = 0$, the surface at time τ $T_{x\tau}$ — Temperature at x at time τ

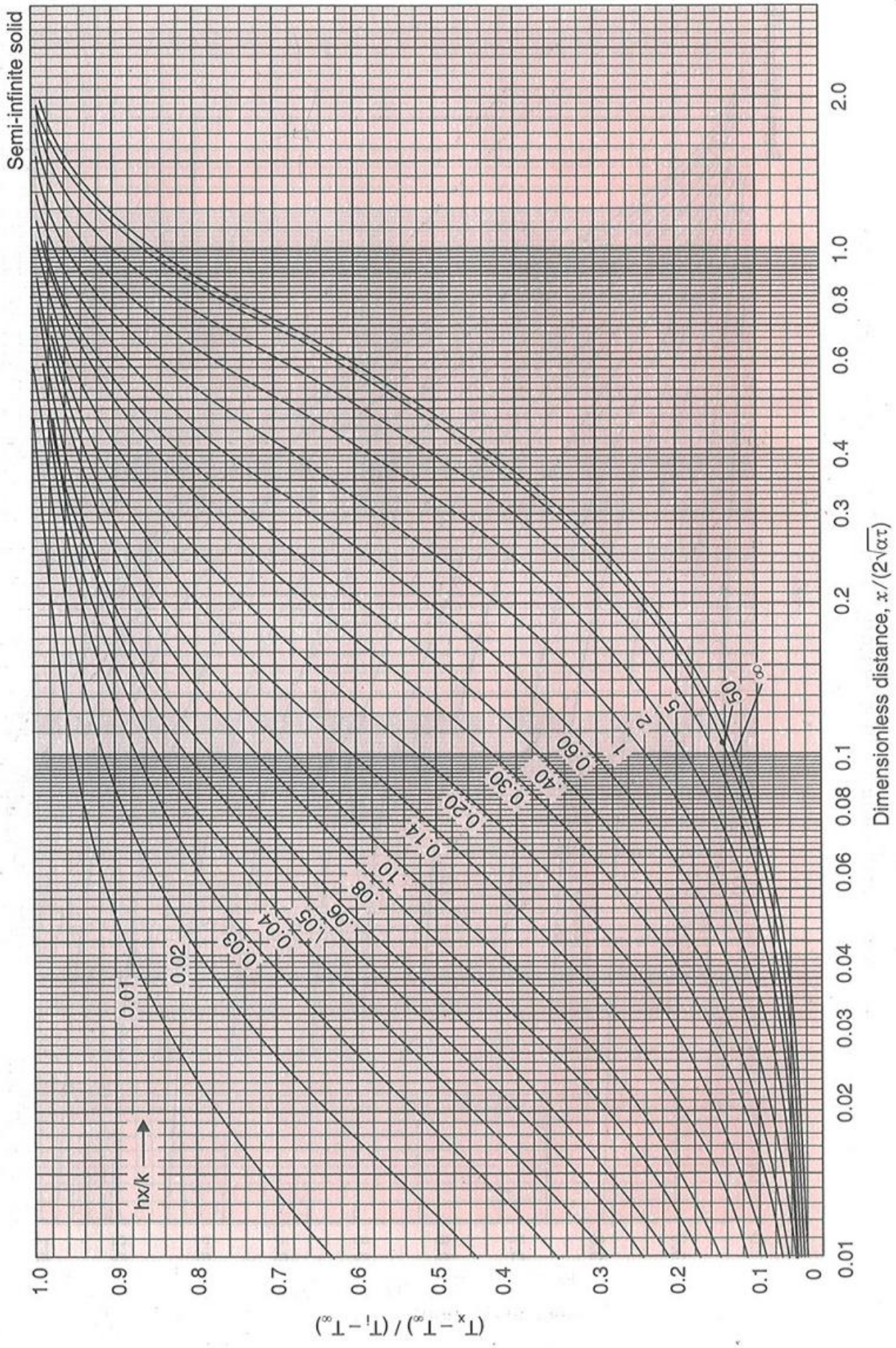
VALUES OF ERROR FUNCTION OF Z

Z	erf(Z)	Z	erf(Z)	Z	erf(Z)	Z	erf(Z)	Z	erf(Z)	Z	erf(Z)	Z	erf(Z)
0.00	0.00000	0.35	0.37938	0.70	0.67780	1.05	0.86244	1.40	0.95228	1.75	0.98667	2.20	0.998137
0.01	0.01128	0.36	0.38933	0.71	0.68467	1.06	0.86614	1.41	0.95385	1.76	0.98719	2.22	0.998308
0.02	0.02256	0.37	0.39921	0.72	0.69143	1.07	0.86977	1.42	0.95538	1.77	0.98769	2.24	0.998464
0.03	0.03384	0.38	0.40901	0.73	0.69810	1.08	0.87333	1.43	0.95686	1.78	0.98817	2.26	0.998607
0.04	0.04511	0.39	0.41874	0.74	0.70468	1.09	0.87680	1.44	0.95830	1.79	0.98864	2.28	0.998738
0.05	0.05637	0.40	0.42839	0.75	0.71116	1.10	0.88020	1.45	0.95970	1.80	0.98909	2.30	0.998857
0.06	0.06762	0.41	0.43797	0.76	0.71754	1.11	0.88353	1.46	0.96105	1.81	0.98952	2.32	0.998966
0.07	0.07886	0.42	0.44747	0.77	0.72382	1.12	0.88679	1.47	0.96237	1.82	0.98994	2.34	0.999065
0.08	0.09008	0.43	0.45689	0.78	0.73001	1.13	0.88997	1.48	0.96365	1.83	0.99035	2.36	0.999155
0.09	0.10128	0.44	0.46622	0.79	0.73610	1.14	0.89308	1.49	0.96490	1.84	0.99074	2.38	0.999237
0.10	0.11246	0.45	0.47548	0.80	0.74210	1.15	0.89612	1.50	0.96610	1.85	0.99111	2.40	0.999311
0.11	0.12362	0.46	0.48466	0.81	0.74800	1.16	0.89910	1.51	0.96728	1.86	0.99147	2.42	0.999379
0.12	0.13476	0.47	0.49374	0.82	0.75381	1.17	0.90200	1.52	0.96841	1.87	0.99182	2.44	0.999441
0.13	0.14587	0.48	0.50275	0.83	0.75952	1.18	0.90484	1.53	0.96952	1.88	0.99216	2.46	0.999497
0.14	0.15695	0.49	0.51167	0.84	0.76514	1.19	0.90761	1.54	0.97059	1.89	0.99248	2.48	0.999547
0.15	0.16800	0.50	0.52050	0.85	0.77067	1.20	0.91031	1.55	0.97162	1.90	0.99279	2.50	0.999593
0.16	0.17901	0.51	0.52924	0.86	0.77610	1.21	0.91296	1.56	0.97263	1.91	0.99309	2.55	0.999689
0.17	0.18999	0.52	0.53790	0.87	0.78144	1.22	0.91553	1.57	0.97360	1.92	0.99338	2.60	0.999764
0.18	0.20094	0.53	0.54646	0.88	0.78669	1.23	0.91805	1.58	0.97455	1.93	0.99366	2.65	0.999822
0.19	0.21184	0.54	0.55494	0.89	0.79184	1.24	0.92050	1.59	0.97546	1.94	0.99392	2.70	0.999866
0.20	0.22270	0.55	0.56332	0.90	0.79691	1.25	0.92290	1.60	0.97635	1.95	0.99418	2.75	0.999899
0.21	0.23352	0.56	0.57162	0.91	0.80188	1.26	0.92524	1.61	0.97721	1.96	0.99443	2.80	0.999925
0.22	0.24430	0.57	0.57982	0.92	0.80677	1.27	0.92751	1.62	0.97804	1.97	0.99466	2.85	0.999944
0.23	0.25502	0.58	0.58792	0.93	0.81156	1.28	0.92973	1.63	0.97884	1.98	0.99489	2.90	0.999959
0.24	0.26570	0.59	0.59594	0.94	0.81627	1.29	0.93190	1.64	0.97962	1.99	0.99511	2.95	0.999970
0.25	0.27633	0.60	0.60386	0.95	0.82089	1.30	0.93401	1.65	0.98038	2.00	0.995322	3.00	0.999978
0.26	0.28690	0.61	0.61168	0.96	0.82542	1.31	0.93606	1.66	0.98110	2.02	0.995720	3.20	0.999994
0.27	0.29742	0.62	0.61941	0.97	0.82987	1.32	0.93806	1.67	0.98181	2.04	0.996086	3.40	0.999998
0.28	0.30788	0.63	0.62705	0.98	0.83423	1.33	0.94002	1.68	0.98249	2.06	0.996424	3.60	1.000000
0.29	0.31828	0.64	0.63459	0.99	0.83851	1.34	0.94191	1.69	0.98315	2.08	0.996734		
0.30	0.32863	0.65	0.64203	1.00	0.84270	1.35	0.94376	1.70	0.98379	2.10	0.997020		
0.31	0.33891	0.66	0.64938	1.01	0.84681	1.36	0.94556	1.71	0.98441	2.12	0.997284		
0.32	0.34913	0.67	0.65663	1.02	0.85084	1.37	0.94731	1.72	0.98500	2.14	0.997525		
0.33	0.35928	0.68	0.66378	1.03	0.85478	1.38	0.94902	1.73	0.98558	2.16	0.997747		
0.34	0.36936	0.69	0.67084	1.04	0.85865	1.39	0.95067	1.74	0.98613	2.18	0.997951		

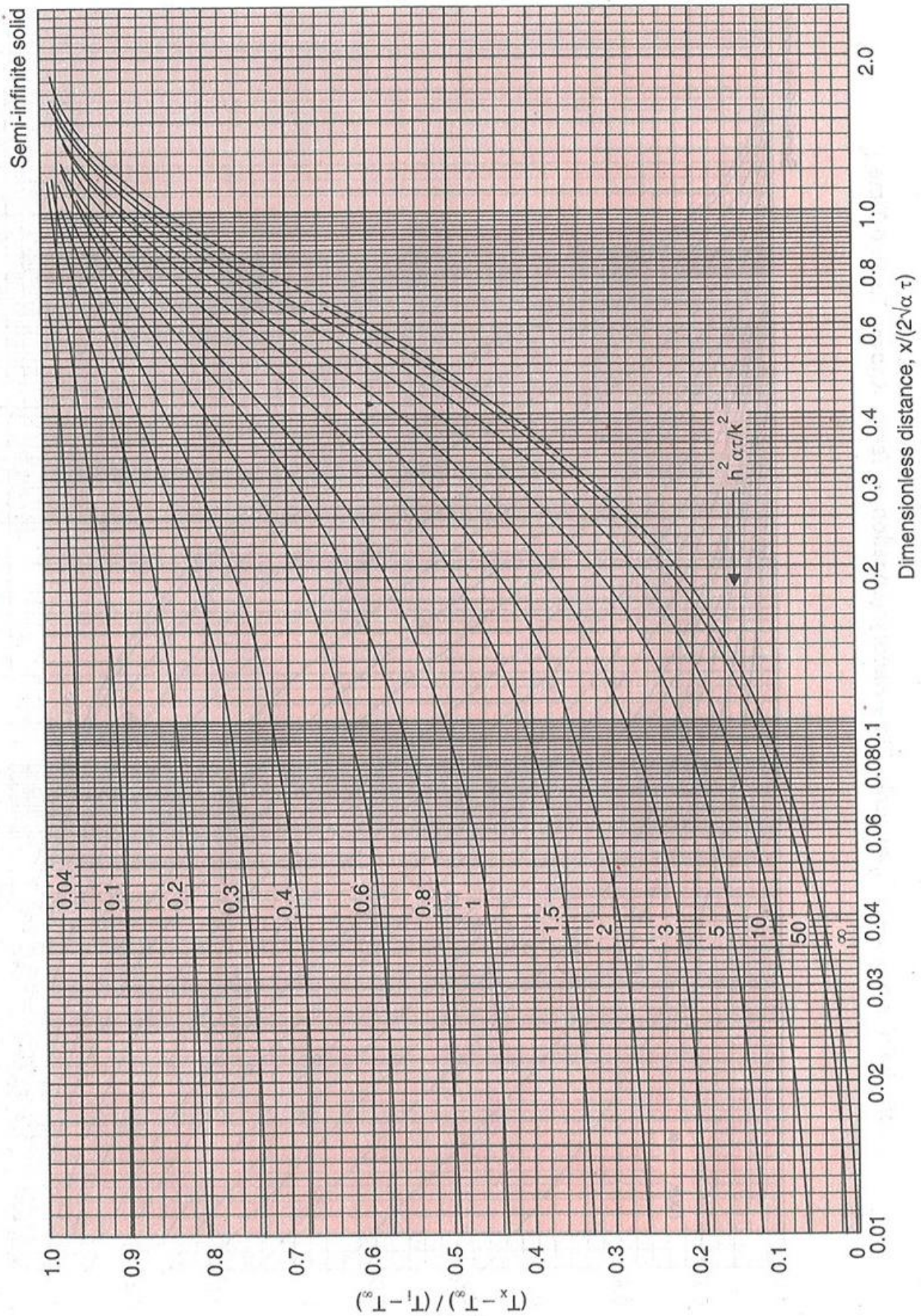


Temperature Distribution in the Semi Infinite Solid with Convection Boundary Condition. $x/(2\sqrt{\alpha\tau}) = 0$ indicates the surface.

Semi Infinite Solid—Temperature—Time History, (Location, x, Temp. Known, To Find Time)

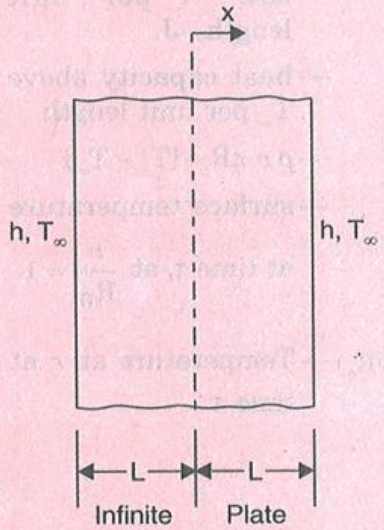


Semi Infinite Solid—Temperature—Time History, (Temp. Time Known, To Find Location, x)



TRANSIENT CONDUCTION

Infinite solids



1 Infinte plate of 2L thickness suddenly exposed on both sides to fluid at T_∞, h

Also for one side insulated plane of thickness L.

Heat flow at surface at time τ

Instantaneous heat flow at surface

Valid for Fo > 0.1

Dimensionless position $\frac{x}{L}$

For centre plane temperature

$$\frac{T_o - T_\infty}{T_i - T_\infty}$$

Refer chart p. 65

For dimensionless position temperature referred to centre line temperature

$$\frac{T_{(x/L)} - T_\infty}{T_o - T_\infty}$$ refer chart p. 66

To find x-plane temperature with respect to initial temperature at any time, use the product of the above two expressions *i.e.*,

$$\frac{T_o - T_\infty}{T_i - T_\infty} \cdot \frac{T_{(x/L)} - T_\infty}{T_o - T_\infty} = \frac{T_{(x/L)} - T_\infty}{T_i - T_\infty}$$

For dimensionless heat flow

$$\frac{Q}{Q_o}$$ – refer chart p. 67

$$q = hA\,[T_s - T_\infty]$$

$\frac{hL}{k}$ Biot number, Bi

$\frac{\alpha\tau}{L^2}$ Fourier number, Fo

T_o — Centre plane temperature at time τ

T_i Initial temperature of plate

T_∞ — Fluid temperature

$T_{(x/L)}$ — Temperature of plane at x at time τ

T_s — Surface Temperature at time τ, use $\frac{x}{L} = 1$

Q_o = heat capacity of the body above T_∞ for unit area

For plate

Q_o = $\rho c L\,[T_i - T_\infty]$, J

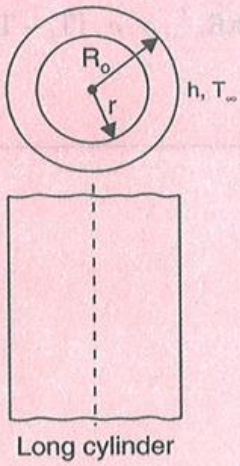
Q = Total heat flow upto time τ, J

q = instantaneous heat flow at surface, W

T_s = surface temp. at time τ. at $\frac{r}{R_0} = 1$

2. Long cylinder, surface

Suddenly exposed to fluid at T_∞, h



Dimensionless position, $\frac{r}{R_0}$

For dimensionless centre line temp. ratio $\frac{T_o - T_\infty}{T_i - T_\infty}$,

refer chart p. 68

For dimensionless position temperature ratio referred to centre line temperature ratio

$$\frac{T_{(r/R_0)} - T_\infty}{T_o - T_\infty}$$, refer chart p. 69

For local temperature use the product of the above two to get expression

$$\frac{T_{(r/R_0)} - T_\infty}{T_i - T_\infty}$$

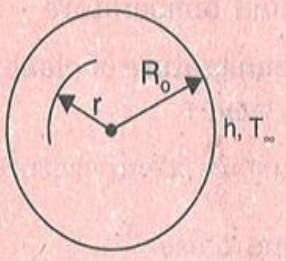
B_i = $\frac{hR_o}{k}$

F_o = $\frac{\alpha\tau}{R_o^2}$

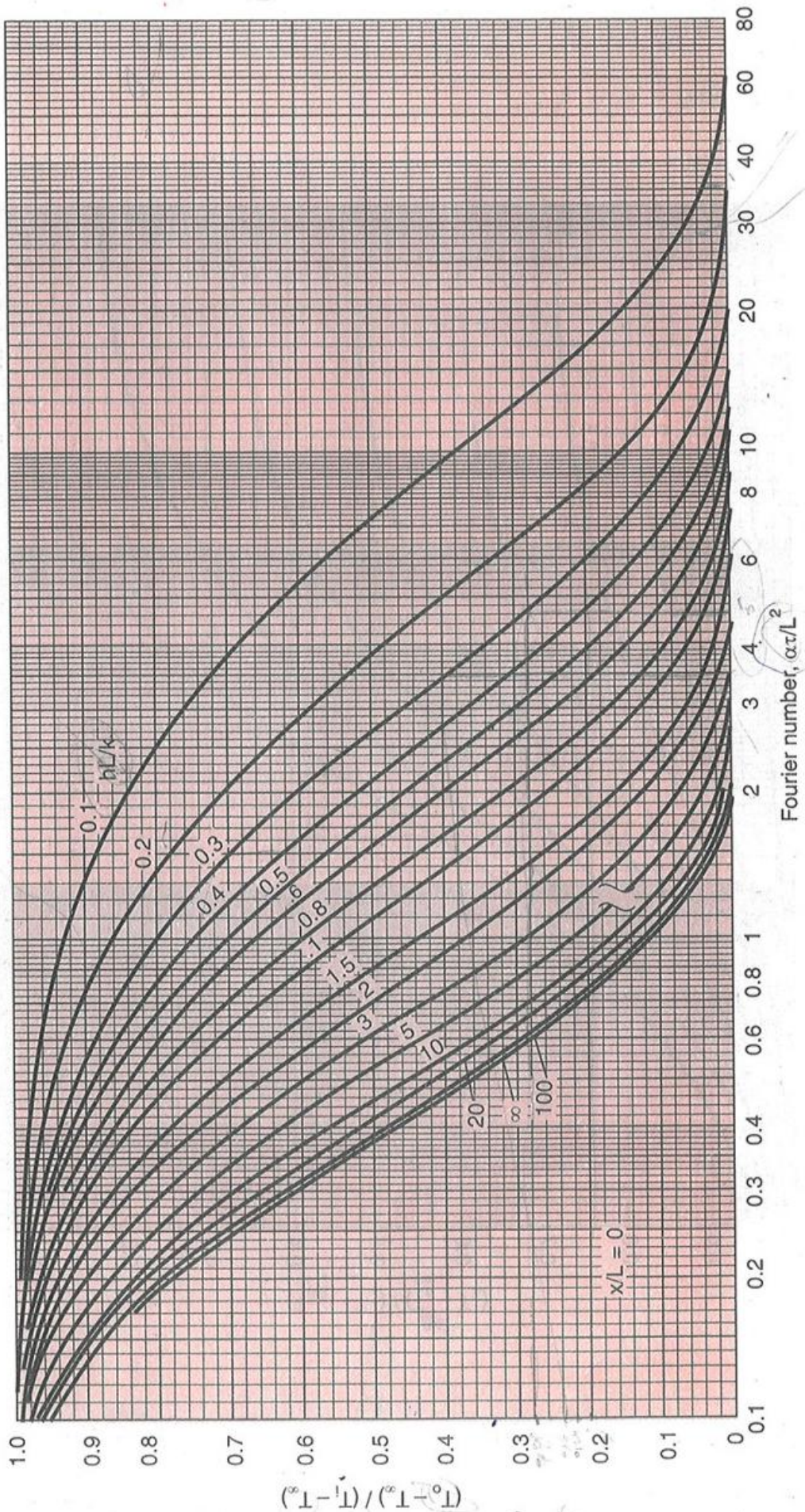
r — any radius

R_o — outside radius

$T_{(r/R_o)}$ = Temperatue at radius r at time τ

Description	*Correlation and Validity*	*Notations*
Heat flow upto time τ	$\frac{Q}{Q_o}$ – refer chart p. 70	Q — Total heat flow upto time τ per unit length, J
Instantaneous heat flow at surface per unit length	$q = 2\pi h R_o (T_s - T_\infty)$	Q_o — heat capacity above T_∞ per unit length
		Q_o — $\rho\, c\, \pi R_o^2 [T_i - T_\infty]$
		T_s — surface temperature at time τ, at $\frac{r}{R_0} = 1$
3 Sphere suddenly exposed to fluid at T_∞, h  Sphere	Dimensionless position $\frac{r}{R_o}$	
	For dimensionless centre temperature ratio $\frac{T_o - T_\infty}{T_i - T_\infty}$ refer chart p. 71	$T_{(r/R_o)}$ — Temperature at r at time τ
	For dimensionless position temperature ratio referred to centre temperature $\frac{T_{(r/R_0)} - T_\infty}{T_o - T_\infty}$ refer chart p. 72	
	For position temperature use the product of the above two expressions $\frac{T_{(r/R_0)} - T_\infty}{T_i - T_\infty} = \frac{T_o - T_\infty}{T_i - T_\infty} \frac{T_{(r/R_o)} - T_\infty}{T_o - T_\infty}$	
Total heat flow upto time τ	For total heat flow $\frac{Q}{Q_o}$ – refer chart p. 73	$Q_o = \frac{4}{3}\pi R_o^3 . \rho . c . [T_i - T_\infty]$
Instantaneous heat flow	$q = 4\pi R_0^2 h\, [T_s - T_\infty]$	

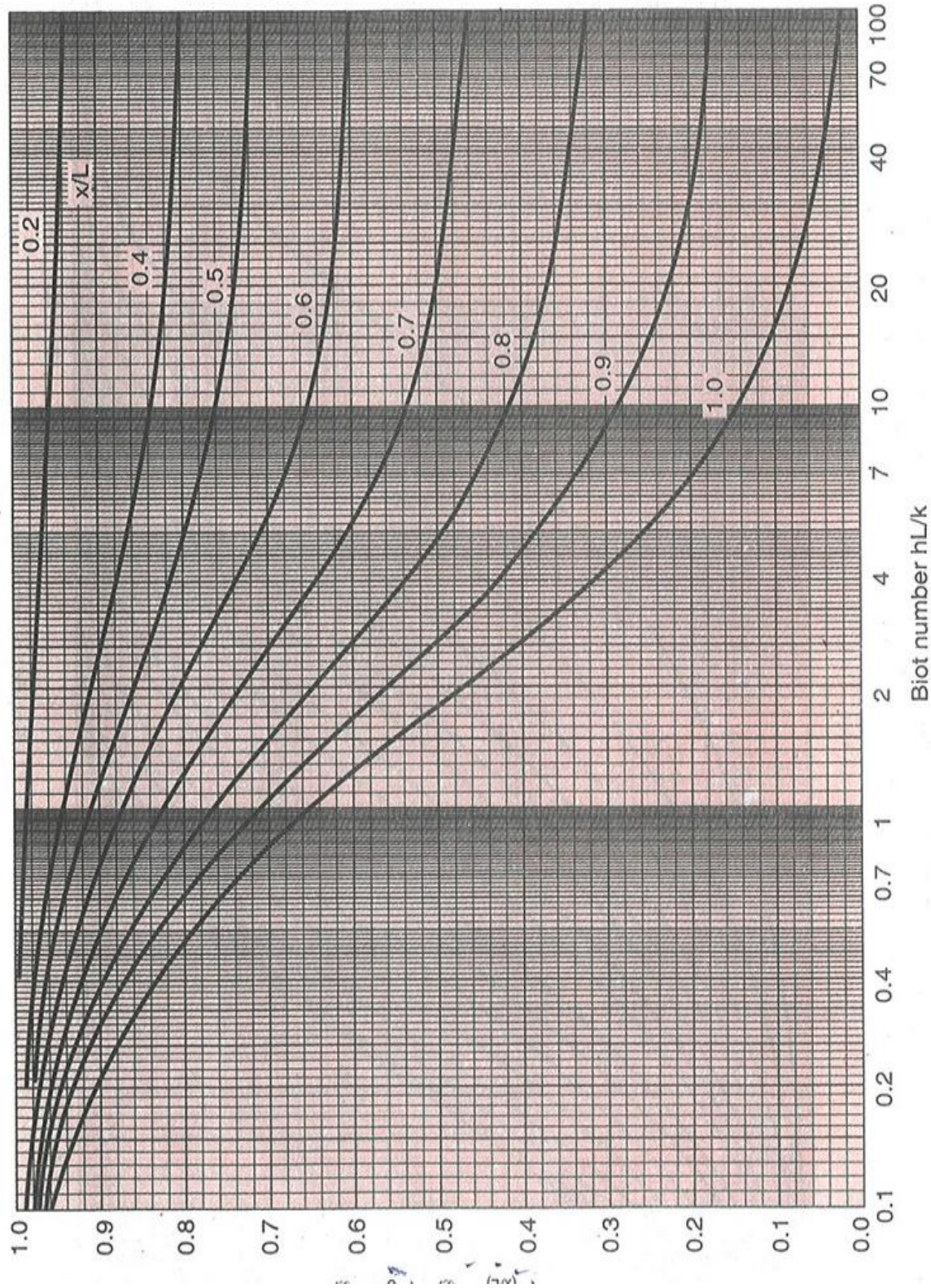
INFINITE PLATE—TEMPERATURE—TIME HISTORY AT MID PLANE



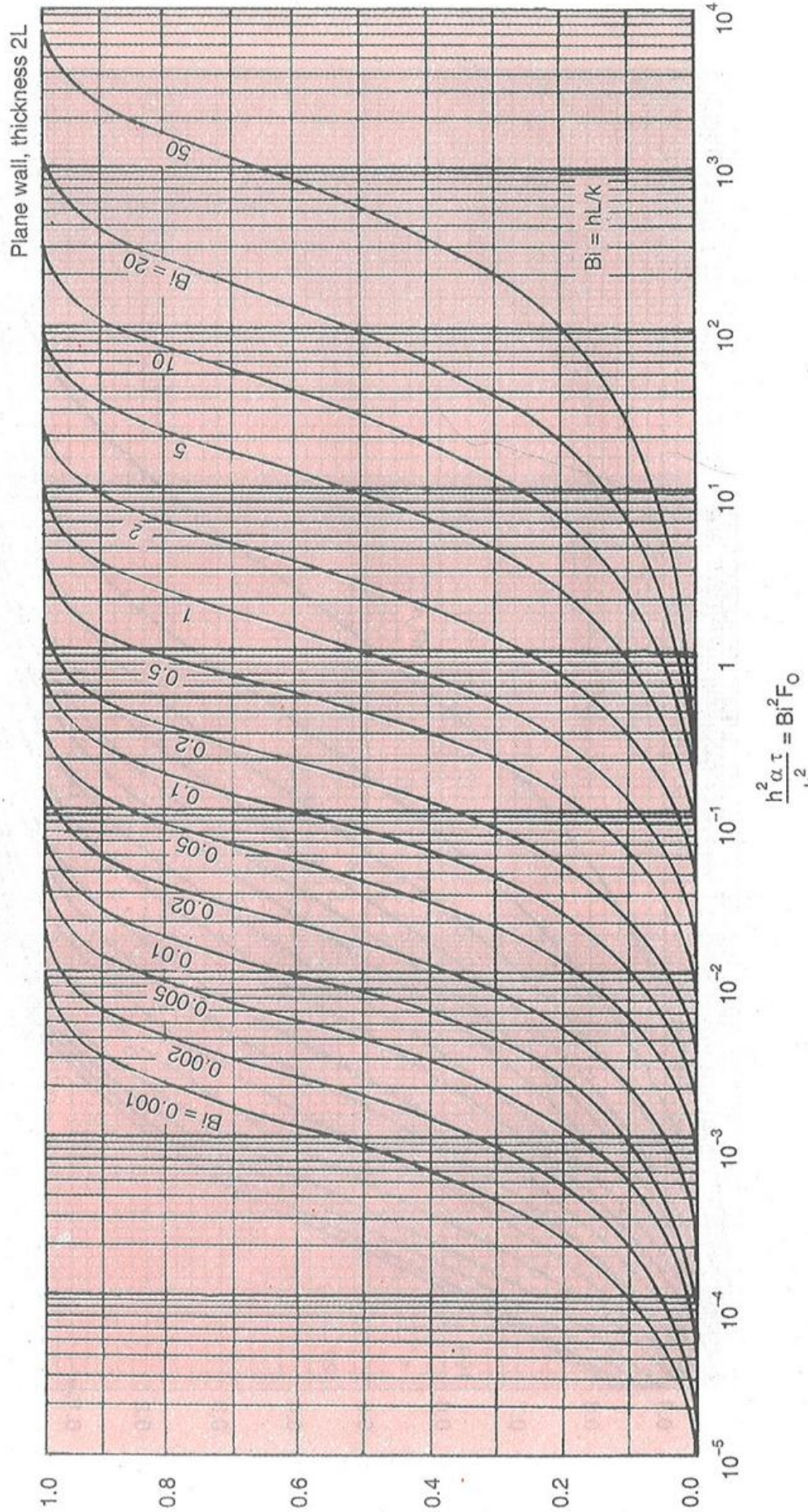
4-18

no center

INFINITE PLATE—TEMPERATURE—TIME HISTORY AT ANY POSITION x,

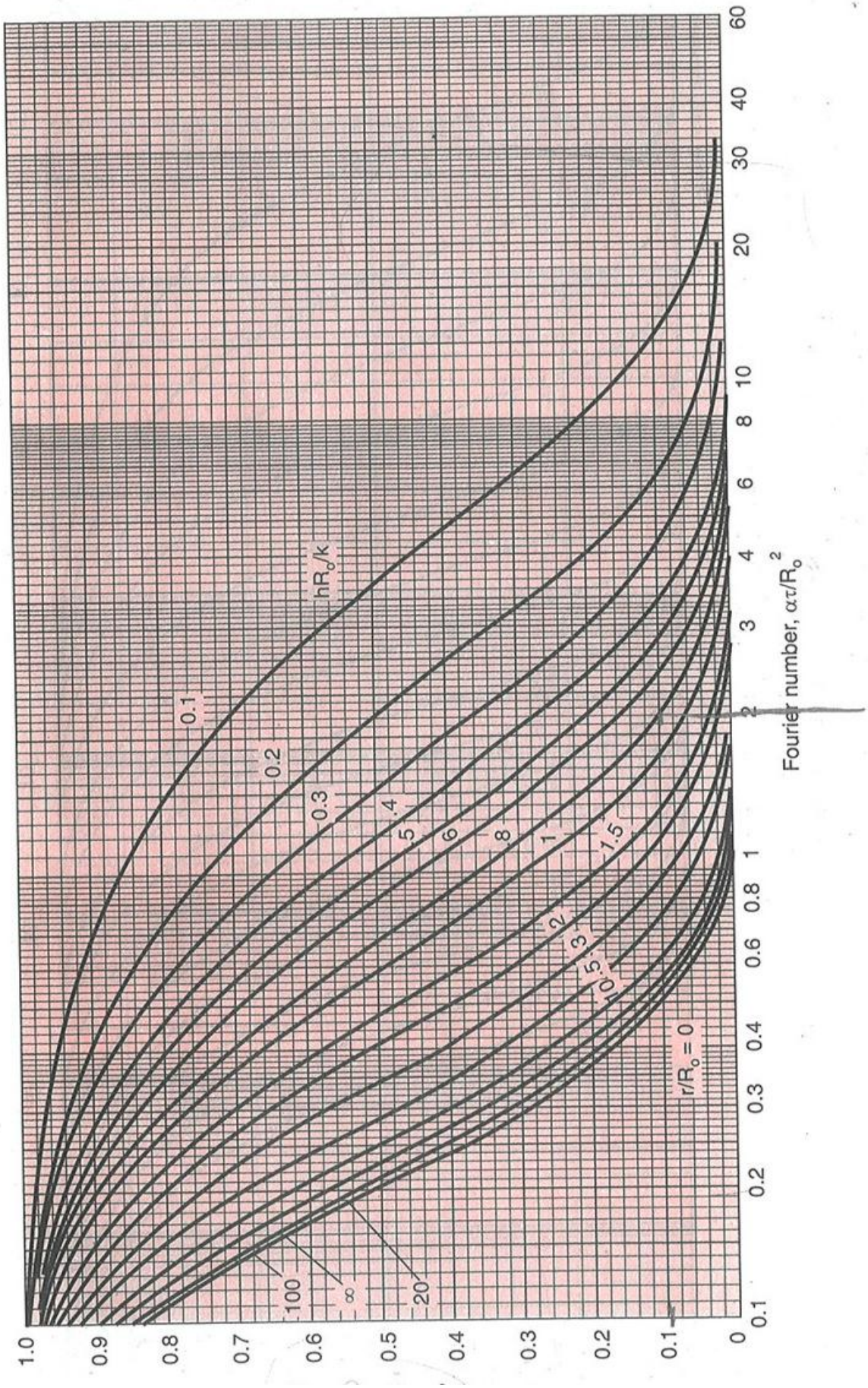


HEAT FLOW—INFINITE PLATE

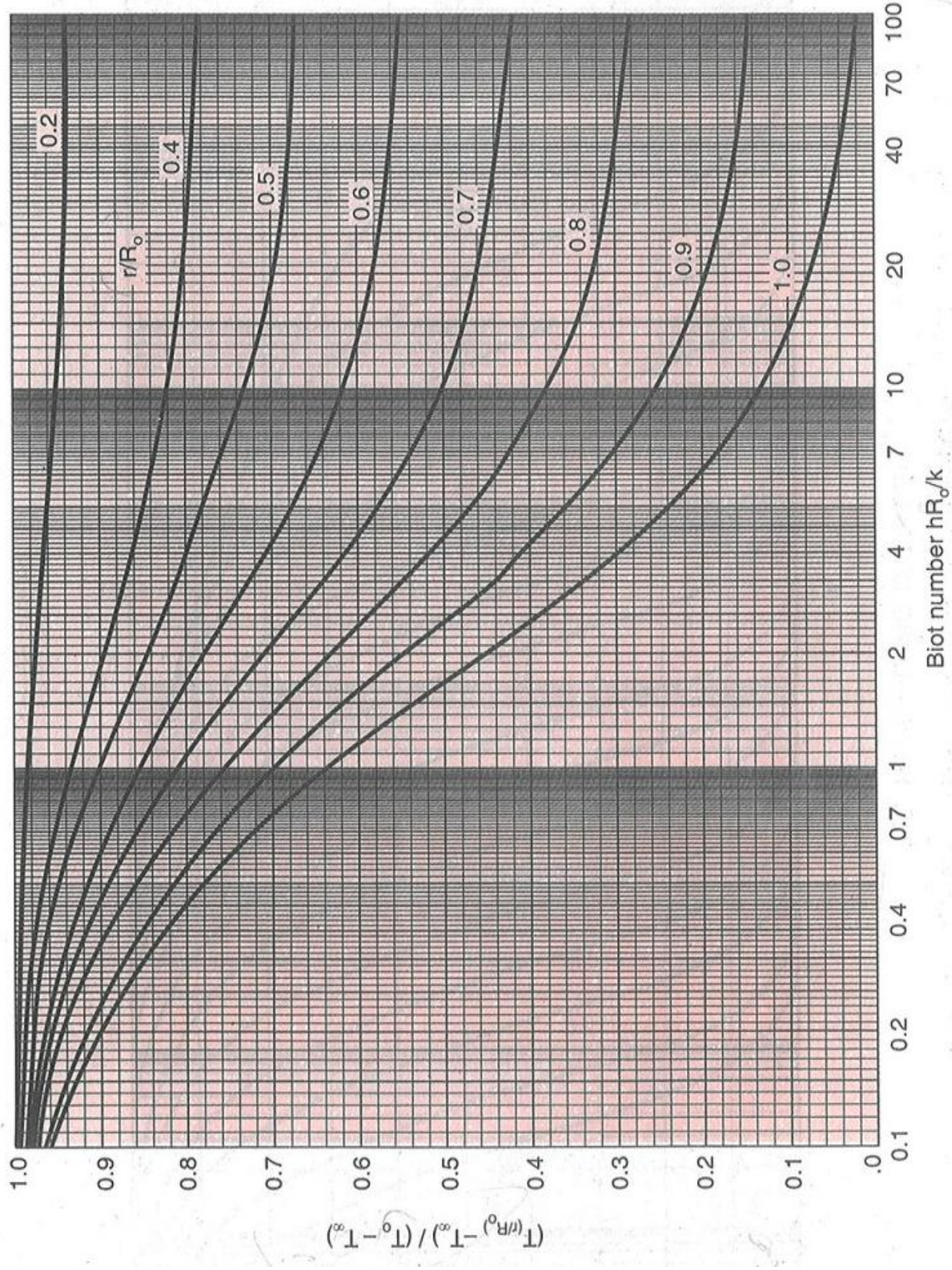


4-8

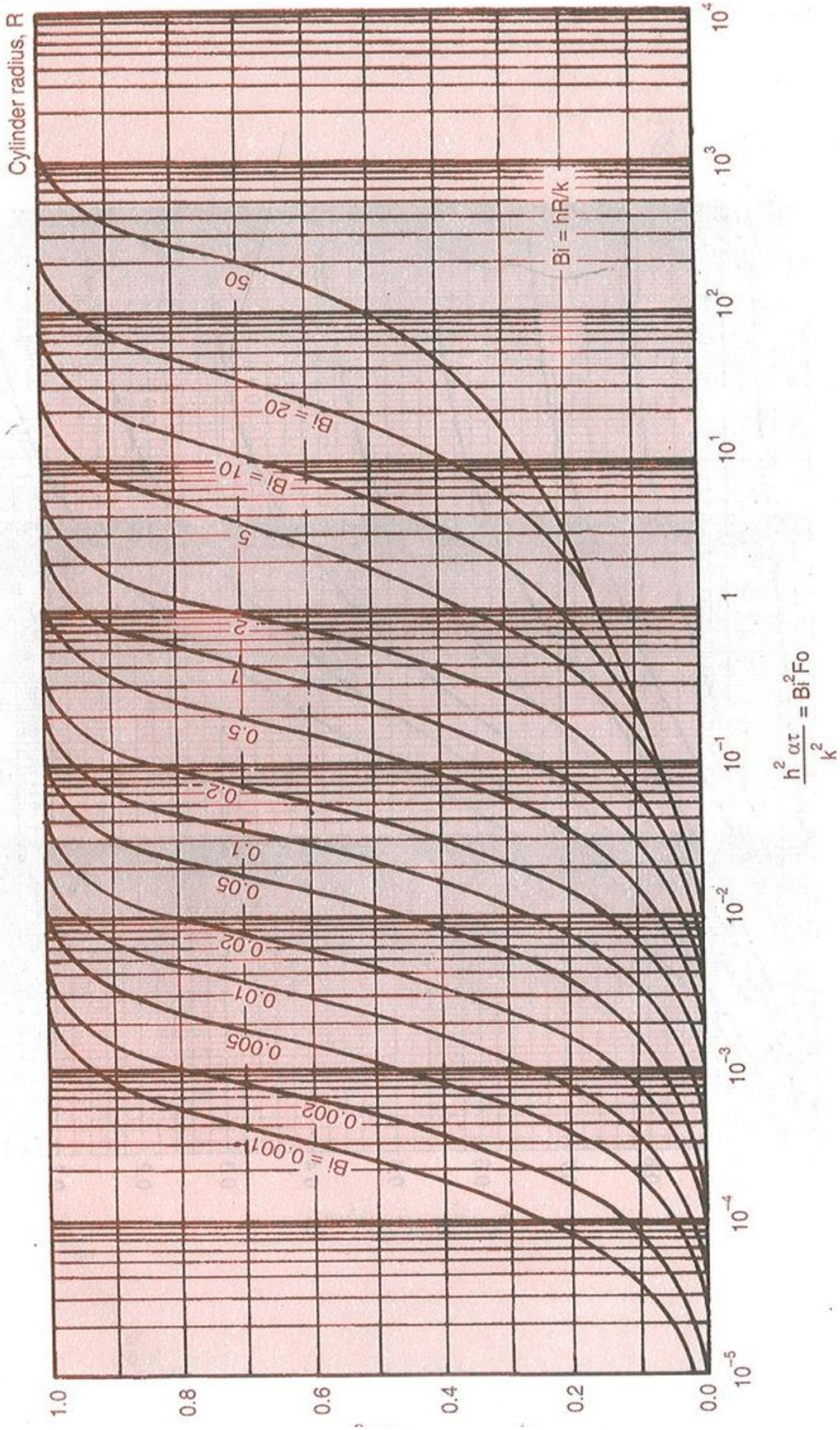
LONG CYLINDER—TEMPERATURE—TIME HISTORY AT CENTRELINE



LONG CYLINDER—TEMPERATURE—TIME HISTORY AT ANY RADIUS, r

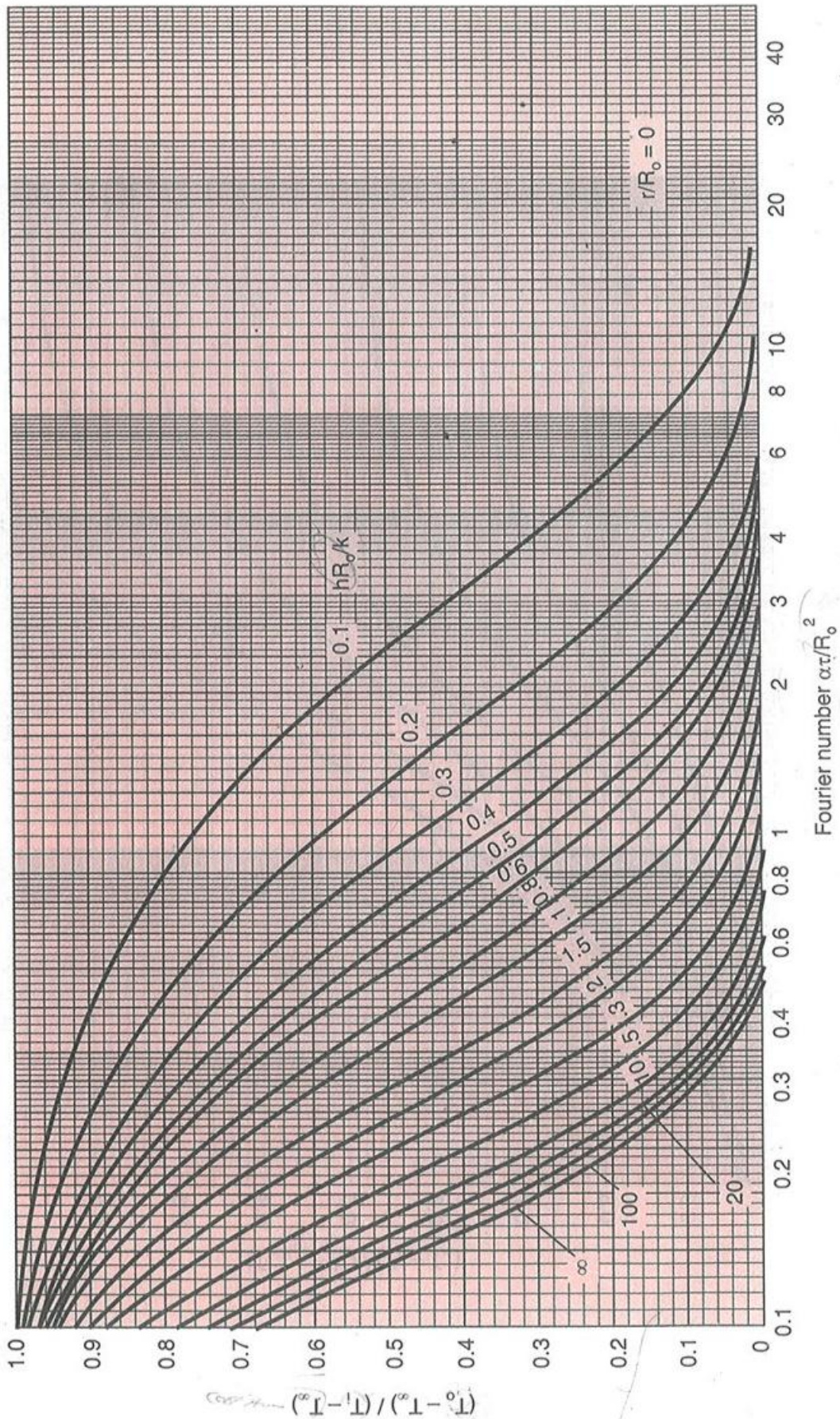


HEAT FLOW—LONG CYLINDER

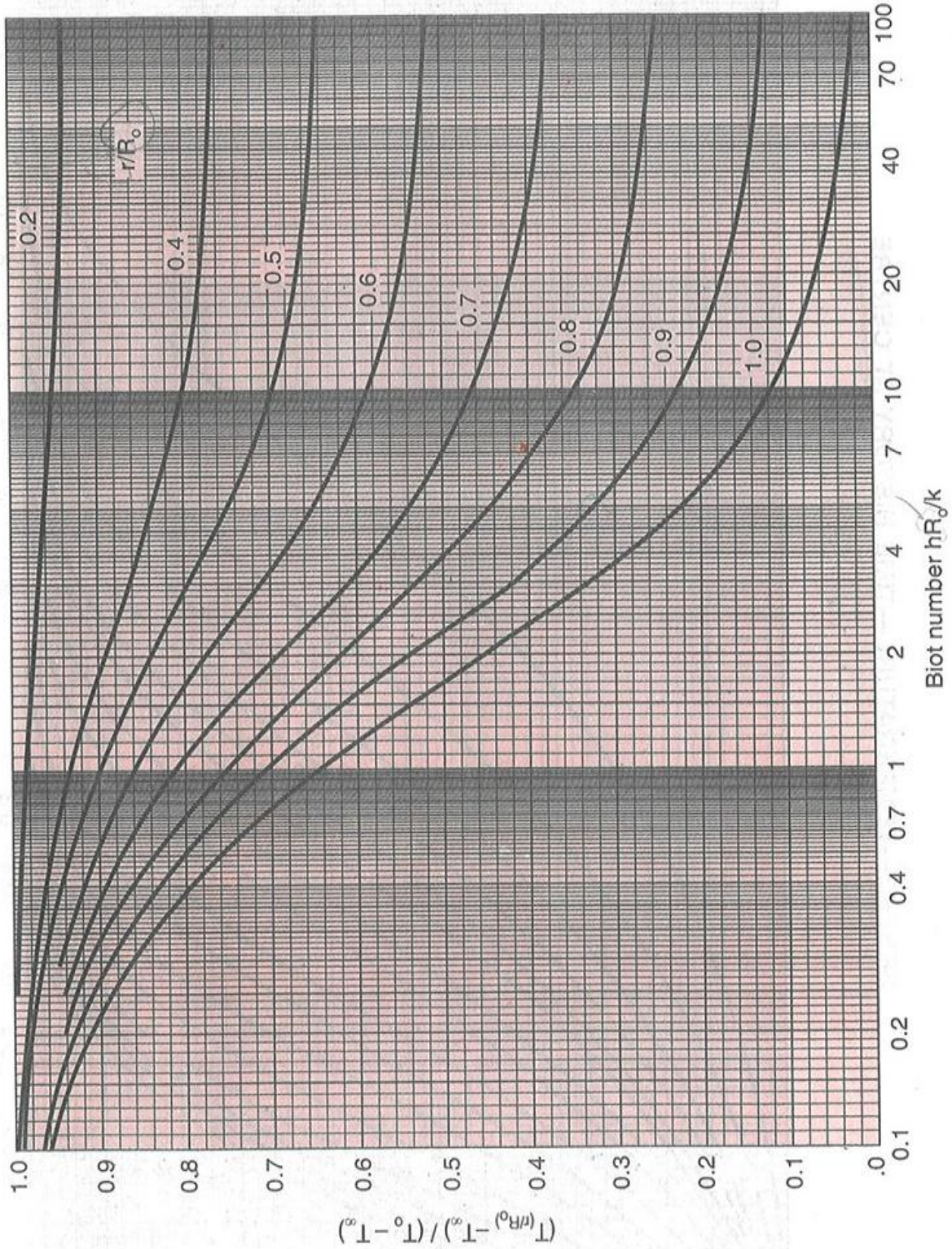


4-9

SPHERE—TEMPERATURE—TIME HISTORY AT CENTRE

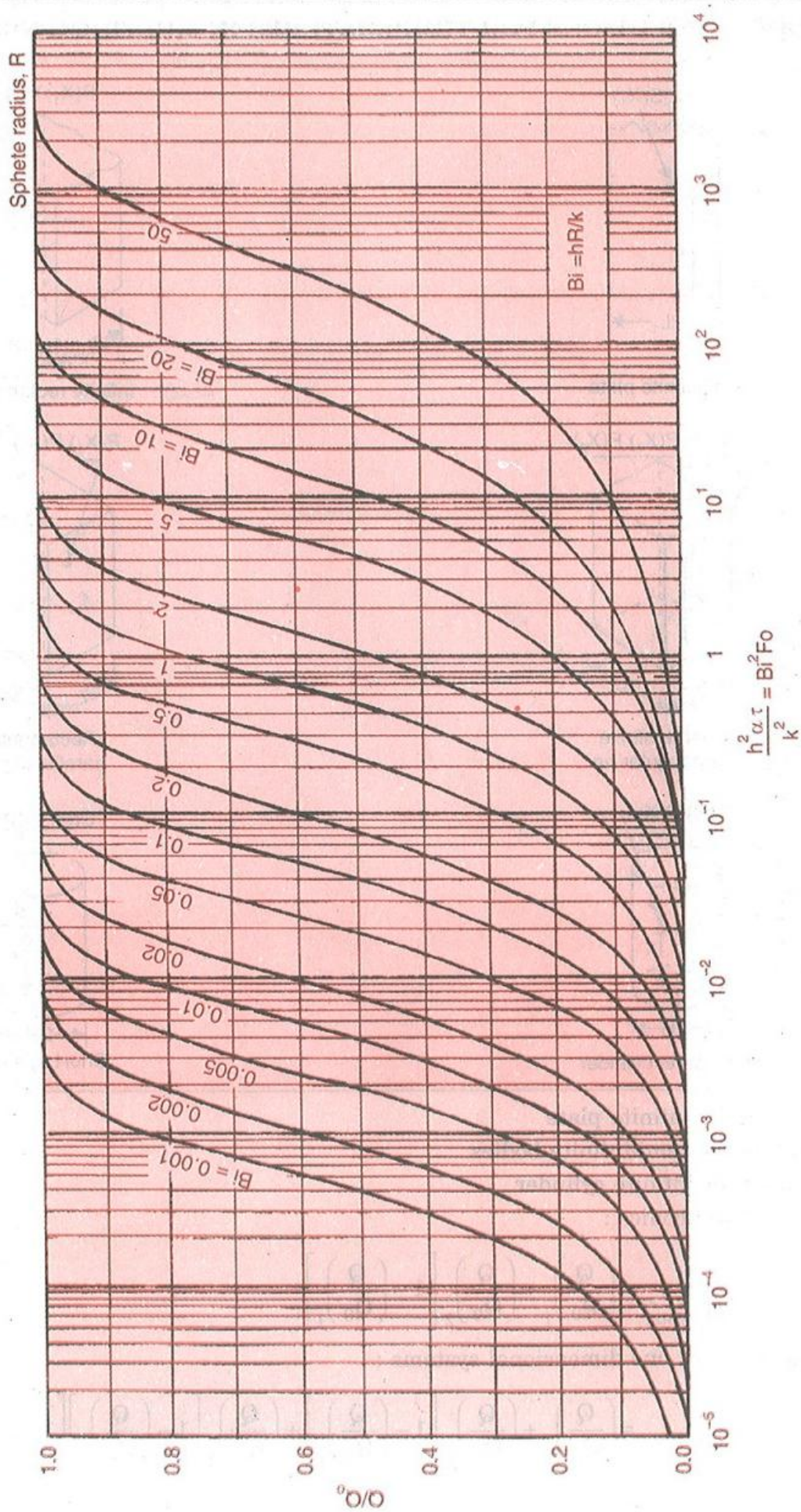


SPHERE—TEMPERATURE—TIME HISTORY AT ANY RADIUS, r

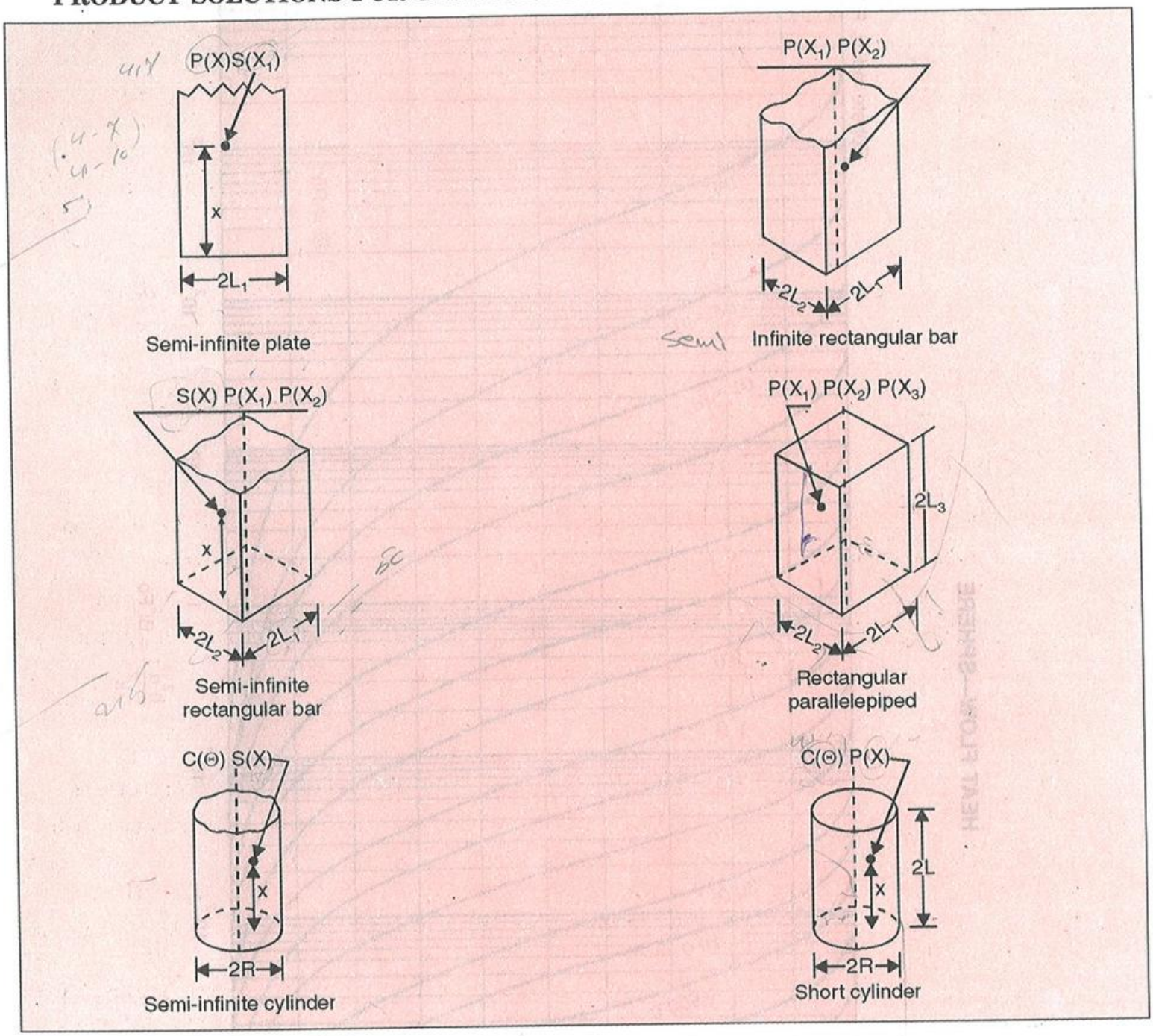


9-12

HEAT FLOW—SPHERE



PRODUCT SOLUTIONS FOR TEMPERATURES IN MULTIDIMENSIONAL SYSTEMS



P(X) Solution for infinite plate

S(X) Solution for semi-infinite bodies

C(θ) Solution for infinite cylinder

Intersection of two bodies :

$$\left(\frac{Q}{Q_0}\right)_{Total} = \left(\frac{Q}{Q_0}\right)_1 + \left(\frac{Q}{Q_0}\right)_2 \left[1 - \left(\frac{Q}{Q_0}\right)_1\right]$$

Intersection of three one dimensional systems :

$$\left(\frac{Q}{Q_0}\right)_{Total} = \left(\frac{Q}{Q_0}\right)_1 + \left(\frac{Q}{Q_0}\right)_2 \left[1 - \left(\frac{Q}{Q_0}\right)_1\right] + \left(\frac{Q}{Q_0}\right)_3 \left[1 - \left(\frac{Q}{Q_0}\right)_1\right]\left[1 - \left(\frac{Q}{Q_0}\right)_2\right]$$

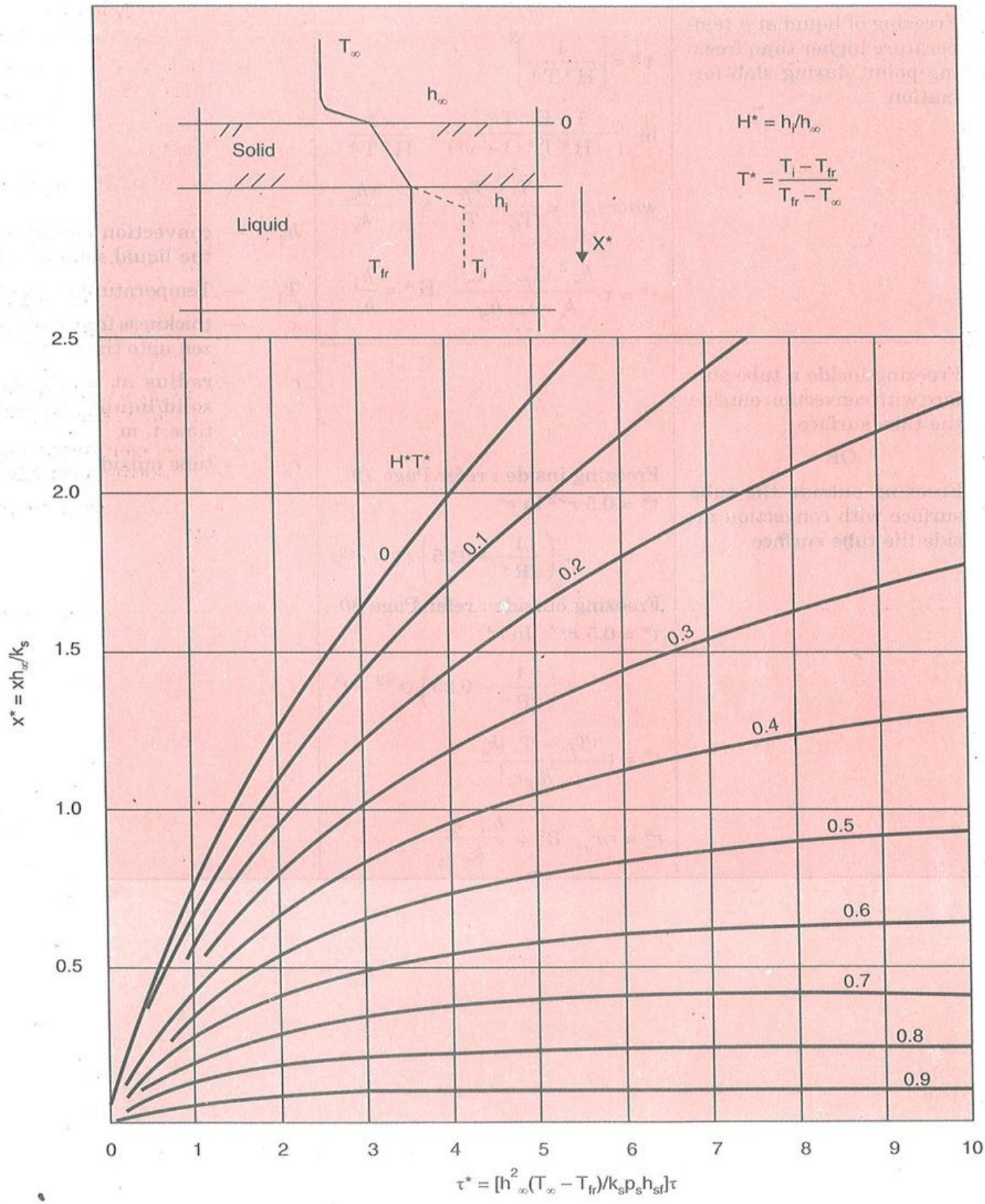
PERIODIC HEAT FLOW

Description	*Correlation and Validity*	*Notation*
1. Solid with high value of thermal conductivity exposed to fluid with periodic temperature variation. Fluid Temperature Variation : $T_f = T_a \cdot \cos\left(\frac{2\pi\tau}{\tau_o}\right)$	$\delta = \tan^{-1}\left(\frac{2\pi}{\tau_o} \cdot \frac{\rho c V}{hA}\right)$ $\frac{T_s}{T_a} = \frac{1}{(1+\tan^2\delta)^{0.5}}$	T_f — fluid temperature at time τ, K T_a — Amplitude of temperature variation of fluid, K τ — Time, s τ_o — Period of oscillation, s δ — Angle of lag in the temperature variation of the solid with reference to fluid temperature variation δ_x — δ at x plane ρ — Solid density, m^3/kg c — Solid specific heat, J/kgK V — Solid volume, m^3 A — Solid surface area, m^2 T_s — Temperature amplitude of the solid, K $\frac{T_s}{T_a}$ — Amplitude ratio T_w — Surface temperature, K α — Thermal diffusivity of solid, m^2/s T_{sx} — Amplitude at depth x, K $T_{x\tau}$ — Temperature at x plane at time τ. δ_x — Angle of lag of temperature at depth x, with reference to surface temperature x_o — Depth upto which the temperature variation penetrates, at steady state. $\frac{q}{A}$ — Heat flow rate at time τ, $\frac{W}{m^2}$ $\frac{Q}{A}$ — Total heat flow during half period, J k — Solid thermal conductivity h — Convective heat transfer coefficient.
2. Semi infinite solid-surface temperature varied periodically Surface Temperature variation : $T_w = T_a \cos\frac{2\pi\tau}{\tau_o}$	$\frac{T_{sx}}{T_a} = e^{-x(\pi/\alpha\tau_o)^{0.5}}$ $\frac{T_{x\tau}}{T_{sx}} = \cos\left(\frac{2\pi\tau}{\tau_o} - x\sqrt{\frac{\pi}{\alpha\tau_o}}\right)$ $\delta_x = 0.5\, x(\tau_o/\alpha\pi)^{0.5}$ Depth of penetration at steady state : $x_o = 1.6\,(\pi\alpha\tau_o)^{0.5}$ $\frac{q}{A} = kT_a\,(2\pi/\alpha\tau_o)^{0.5} \cdot \sin\left(\frac{\pi}{4} - \frac{2\pi\tau}{\tau_0}\right)$ $\frac{Q}{A} = k \cdot T_a\left(\frac{2\tau_o}{\pi\alpha}\right)^{0.5}$	
3. Semi infinite solid surface exposed to convection with periodic temperature variation of fluid.	$T_f = T_a \cos\left(\frac{2\pi\tau}{\tau_0}\right)$ $\frac{T_{sx}}{T_a} = \frac{1}{[1+2A^{0.5}+2A]^{0.5}}$ where $A = (\pi k^2/\alpha\tau_o h^2)$	

FREEZING/MELTING

Description	*Correlation*	*Notation*
LIQUID/SOLID SURFACE Suddenly exposed to fluid at T_∞ liquid or solid at melting temperature T_{fr}. Flat surface Refer next page 77	$x^* = [2\tau^* + 1]^{0.5} - 1$ $\tau^* = x^* + 0.5\, x^{*2}$ where $x^* = \dfrac{x \,.\, h_\infty}{k_1}$ melting $x^* = \dfrac{x \,.\, h_\infty}{k_s}$ freezing $\tau^* = \tau \dfrac{h_\infty{}^2 (T_\infty - T_{fr})}{k_1 \,.\, \rho_s \,.\, h_{sf}}$ – melting $\tau^* = \tau \dfrac{h_\infty{}^2 (T_{fr} - T_\infty)}{k_s \,.\, \rho_1 \,.\, h_{sf}}$ – freezing	x — thickness melted/frozen from surface upto time τ, m x^* — dimensionless distance parameter τ^* — dimensionless time parameter k_s, k_1 — thermal conductivity of solid, liquid ρ_s, ρ_1 — density of solid, liquid h_{sf} — enthalpy of melting/freezing, J/kg h_∞ — convective heat transfer coefficient at surface, W/m^2K T_∞ — free stream temperatue of fluid flowing over surface T_{fr} — melting/freezing temperature, τ — time, s

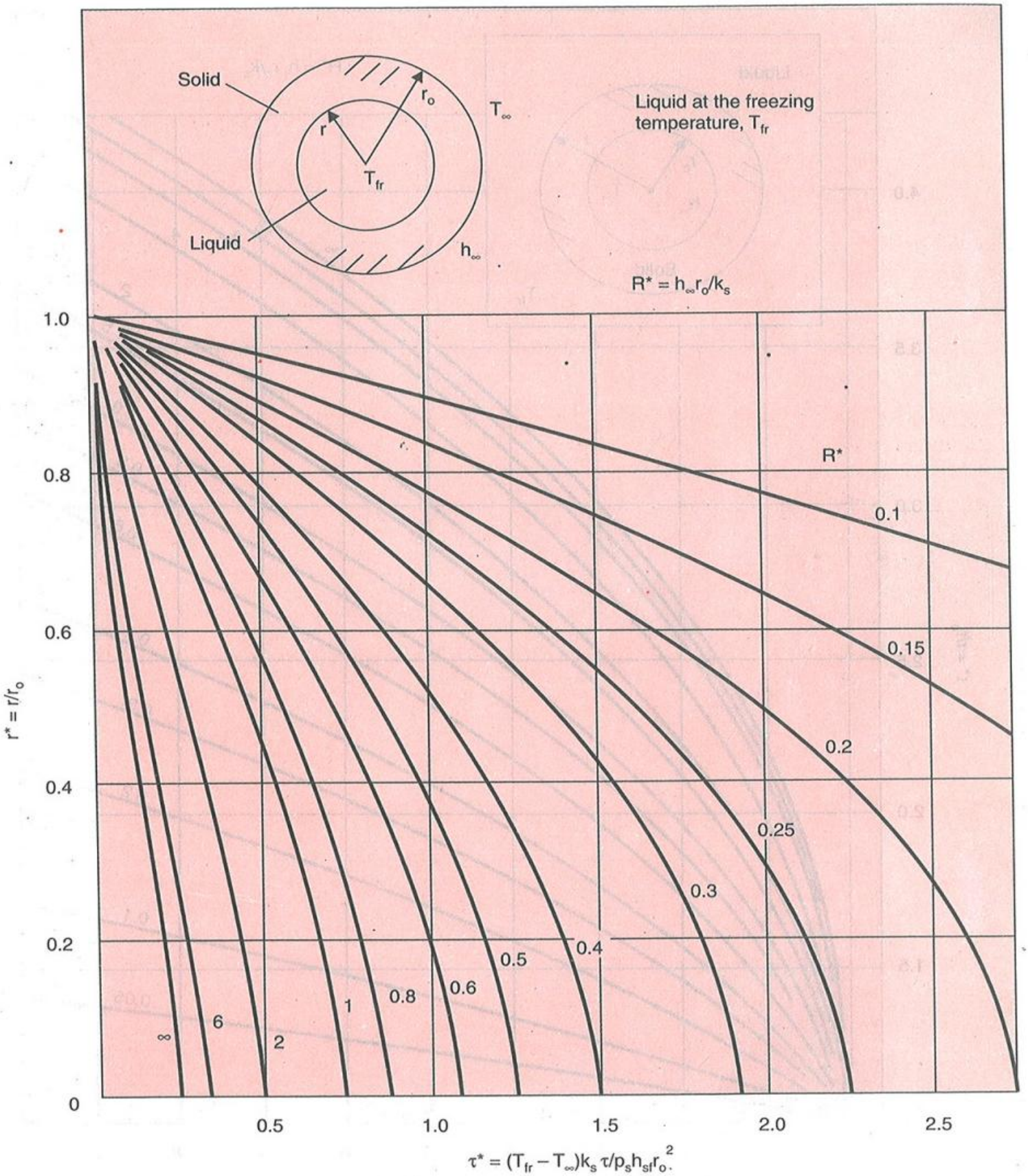
FREEZING/MELTING FLAT SURFACE



Variation of the Freezing Thickness x^* with Dimensionless Time τ^* During Slab Formation of the Solid Phase

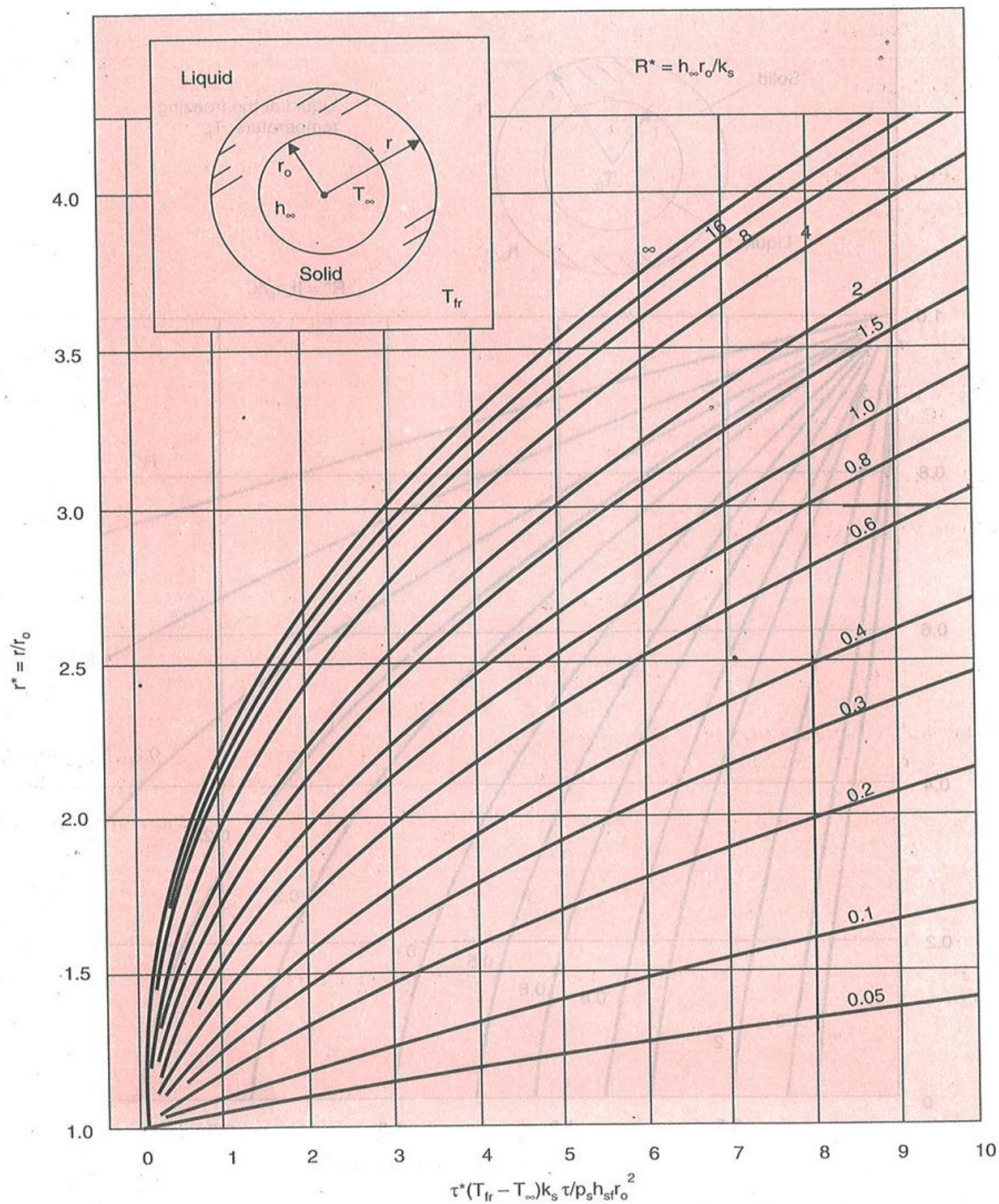
Description	*Correlation*	*Notation*
Freezing of liquid at a temperature higher than freezing point, during slab formation	$\tau^* = \left[\frac{1}{H^*T^*}\right]^2$ $\ln \frac{1 - H^*T^*}{1 - H^*T^*(1 + x^*)} - \frac{x^*}{H^*T^*}$ where $T^* = \frac{T_i - T_{fr}}{T_{fr} - T_\infty}$, $x^* = \frac{x h_\infty}{k_s}$ $\tau^* = \tau \frac{h_\infty^2 (T_{fr} - T_\infty)}{k_s \cdot \rho_s \cdot h_{sf}}$, $H^* = \frac{h_1}{h_\infty}$	h_1 — convection coefficient at the liquid solid interface T_1 — Temperature of liquid x — thickness from surface frozen upto time τ, m r — radius at the (freezing) solid/liquid interface at time τ, m r_o — tube outside radius, m,
Freezing inside a tube surface with convection outside the tube surface OR Freezing outside the tube surface with convection inside the tube surface	Freezing inside : refer Page 79 $\tau^* = 0.5\, r^{*2} \ln r^* + \left(\frac{1}{2R^*} + 0.25\right)(1 - r^{*2})$ Freezing outside : refer Page 80 $\tau^* = 0.5\, r^{*2} . \ln r^* + \left(\frac{1}{2R^*} - 0.25\right)(r^{*2} - 1)$ $\tau^* = \tau \frac{(T_{fr} - T_\infty) k_s}{\rho_s\, h_{sf} r_o^2}$ $r^* = r/r_o$, $R^* = \frac{h_\infty \cdot r_o}{k_s}$	

FREEZING—INSIDE TUBE



Variation of r^* with Dimensionless Time τ^* for Freezing Inside a Tube of Negligible Thermal Resistance Having Convection on the Outside and Ambient Sink Temperature T_∞

FREEZING—OUTSIDE TUBE



Variation of r^* with Nondimensional Time τ^* for Freezing on the Outside of Tube of Negligible Thermal Resistance Having Convection on the Inside and Sink Temperature T_∞

RADIATION

Description	*Equation*	*Notation*
Wavelength	$\lambda = \frac{c}{v}$	λ wavelength, m c speed of light = 3×10^8 m/s
Radiant Property	$\rho + \alpha + \tau = 1$	ρ reflectivity α absorptivity τ transmissivity
Kirchhoff's Law	$\varepsilon_\lambda = \alpha_\lambda$ for gray bodies $\varepsilon_\lambda = \alpha_\lambda = \varepsilon = \alpha$	v frequency ε emissivity = $\frac{E}{E_b}$
Wien's Law	$\lambda_{max} T = 2898$ μmK	
Stefan-Boltzmann Law for BLACK bodies	$E_b = \sigma T^4$	α_λ monochromatic absorptivity ε_λ monochromatic emissivity
Planck's Law	$E_{b\lambda} = \frac{C_1 \lambda^{-5}}{\exp.(C_2/\lambda T) - 1}$	T temperature K *C_1 = $0.374177107 \times 10^{-15}$ W/m^2 3.74 C_2 = 0.014387752 mK 1.438
Energy leaving gray bodies	$Q = \frac{\varepsilon}{\rho} A(E_b - J)$ $J = \rho G + \varepsilon E_b$	E_b emissive power of black body, W/m^2 $E_{b\lambda}$ emissive power for black body per unit wave length Q net heat interchange
Solar Constant	1395 W/m^2	
Wave Lengths : Thermal Radiation range Visible Radiation range	0.1 – 100 μm 0.35 – 0.75 μm	J radiosity (total rate at which radiation leaves a given surface)
Stefan-Boltzmann constant, σ	$\sigma = 5.67 \times 10^{-8}$ W/m^{2}K^4	G irradiation (total incident radiation on a surface)
Reciprocity theorem	$A_1 F_{1-2} = A_2 F_{2-1}$	F_{1-2}, F_2, Shape factors

*The constant C_1 is to be divided by 2π for polarised radiation normal to the surface.

RATIO OF BLACK BODY RADIANT ENERGY UPTO THE WAVE LENGTH λ, TO TOTAL EMISSIVE POWER OF BLACK BODY AT THE SAME TEMPERATURE

BLACK BODY RADIATION FUNCTION, $E_{b0\text{-}\lambda}/\sigma T^4$

λT, μm-K	$E_{b0\text{-}\lambda}/\sigma T^4$	λT, μm-K	$E_{b0\text{-}\lambda}/\sigma T^4$
800	0.000016	6800	0.796129
1000	0.000321	7000	0.808109
1200	0.002134	7200	0.819217
1400	0.007790	7400	0.829527
1600	0.019718	7600	0.839102
1800	0.039341	7800	0.848005
2000	0.066728	8000	0.856288
2200	0.100888	8500	0.874608
2400	0.140256	9000	0.890090
2600	0.183120	9500	0.903085
2800	0.227897	10000	0.914199
3000	0.273232	10500	0.923710
3200	0.318102	11000	0.931890
3400	0.361735	11500	0.939959
3600	0.403607	12000	0.945098
3800	0.443382	13000	0.955139
4000	0.480877	14000	0.962898
4200	0.516014	15000	0.969981
4400	0.548796	16000	0.973814
4600	0.579280	18000	0.980860
4800	0.607559	20000	0.985602
5000	0.633747	25000	0.992215
5200	0.658970	30000	0.995340
5400	0.680360	40000	0.997967
5600	0.701046	50000	0.998953
5800	0.720158	75000	0.999713
6000	0.737818	100000	0.999905
6200	0.754140		
6400	0.769234		
6600	0.783199		

RADIANT HEAT EXCHANGE BETWEEN SURFACES

General Equations $Q_{ij} = [E_{bi} - E_{bj}]\, F_{ij} A_i$		Q_{ij} *Net heat exchange between i and j*
$F_{ij} A_i = F_{ji} A_j$	E_{bj} *emissive power of body j*	E_{bi} *emissive power of body i* F_{ij} *shape factor of surface i with respect to j*

Geometry	*Shape factor F_{ij} for black bodies*	*For gray bodies* $A_i F_{ij}$
Equal and parallel squares, rectangles and discs	Refer pages 90 to 92	
Adjacent rectangles at right angles	Refer pages 93 to 94	
Non intersecting perpendicular squares	Refer page 95	
Offset non intersecting perpendicular squares	Refer page 96	
Parallel discs of different size	Refer page 97	$\dfrac{1}{\dfrac{1-\varepsilon_i}{A_i \varepsilon_i} + \dfrac{1}{A_i F_{ij}} + \dfrac{1-\varepsilon_j}{A_j \varepsilon_j}}$
Opening in walls of thickness L	Refer page 98	
Surface element and a parallel rectangular surface	Refer page 99	
Surface element and a perpendicular rectangular surface	Refer page 100	
Differential spherical surface and a rectangular surface	Refer page 100	
A plane with parallel rows of tubes	Refer page 101 and 102	
Short concentric cylinders	Refer page 103	
Parallel infinite planes	1	
Totally enclosed small body *i* [small compared with a large enclosing body *j*]	1	
Totally enclosed large convex body	1	
Concentric infinite long cylinders,	1	
Concentric spheres	1	

RELATION BETWEEN SHAPE FACTORS

Emissivity ε_n of radiation in the normal direction to the surface and ε_h of the total hemispherical emissivity for various surfaces.

Surface	*Temperature t °C*	ε_n	ε_h
Aluminium, bright rolled	170	0.039	0.049
Aluminium, bright rolled	500	0.050	—
Aluminium paint	100	0.20 to 0.40	—
Bakelite lacquer	80	0.935	—
Bismuth, bright	80	0.340	0.366
Brick, mortar, plaster	20	0.930	—
Chrome, polished	150	0.058	0.071
Clay, fired	70	0.910	0.860
Copper, polished	20	0.030	—
Copper, lightly oxidised	20	0.037	—
Copper, scraped	20	0.070	—
Copper, black oxidised	20	0.780	—
Copper, oxidised	131	0.760	0.725
Corrundum, emery rough	80	0.855	0.840
Enamel, lacquer	20	0.85–0.95	—
Glass	90	0.940	0.876
Gold, polished	130	0.018	—
Gold, polished	400	0.022	—
Ice, smooth and water	0	0.966	0.918
Ice, rough crystals	0	0.985	—
Iron, bright etched	150	0.128	0.158
Iron bright abrased	20	0.240	—
Iron, red rusted	20	0.610	—
Iron, hot rolled	20	0.770	—
Iron, hot rolled	130	0.600	—
Iron, hot cast	100	0.800	—
Iron, heavity rusted	0	0.850	—
Iron, heat resistant, oxidised	80	0.613	—
Iron, heat resistant, oxidised	200	0.630	—

Surface	*Temperature t °C*	ε_n	ε_h
Lacquer, black matte	80	0.970	—
Lacquer, white	100	0.925	—
Lead, gray oxidised	20	0.280	—
Manganin, bright rolled	118	0.048	0.057
Nickel, bright matte	100	0.041	0.046
Nickel, Polished	100	0.045	0.053
Paper	95	0.920	0.890
Porcelain	20	0.92 – 0.94	—
Red Lead	100	0.930	—
Silver, pure, polished	200-600	0.02 – 0.03	—
Silumin, cast polished	150	0.186	—
Tar paper	20	0.930	—
Water glass	20	0.960	—
Wood, beach	70	0.935	0.910
Zinc, gray oxidised	20	0.23 – 0.28	—

*Where ε_h is not specified take :

For bright metal surfaces, $\varepsilon_h = 1.2\ \varepsilon_n$

For other smooth surfaces = $\varepsilon_h = 0.95\ \varepsilon_n$

For rough surfaces $\varepsilon_h = 0.98\ \varepsilon_n$.

Emissivity along normal direction ε_n and total hemispherical emissivity ε_h for various non metallic Surfaces.

Surface	*Temperature °C*	ε_h	ε_n
Aluminium, oxide	327	—	0.69
Aluminium, oxide	727	—	0.55
Aluminium oxide	1227	—	0.41
Alumina brick	527	—	0.40
Alumina brick	727	—	0.33
Alumina brick	1127	—	0.28
Alumina brick	1327	—	0.33
Asphalt pavement	27	0.85 – 0.93	—
Brick, red	27	0.93 – 0.96	—
Cloth	27	0.75 – 0.90	—
Concrete	27	0.88 – 0.93	—
Glass, window	27	0.90 – 0.95	—
Gypsum or plaster board	27	0.90 – 0.92	—
Ice	0	0.95 – 0.98	—
Kaolin insulating brick	527	—	0.70
Kaolin insulating brick	927	—	0.57
Kaolin insulating brick	1127	—	0.47
Kaolin insulating brick	1327	—	0.53
Magnesia brick	527	—	0.45
Magnesia brick	727	—	0.36
Magnesia brick	1127	—	0.31
Magnesia brick	1327	—	0.40
Paints, Black	27	0.98	—
Paints, white acrylic	27	0.90	—
Paints white, zinc oxide	27	0.92	—
Paper, white	27	0.92 – 0.97	—
Pyrex	27	—	0.82
Pyrex	327	—	0.80
Pyrex	727	—	0.71
Pyrex	927	—	0.62

(Contd.)

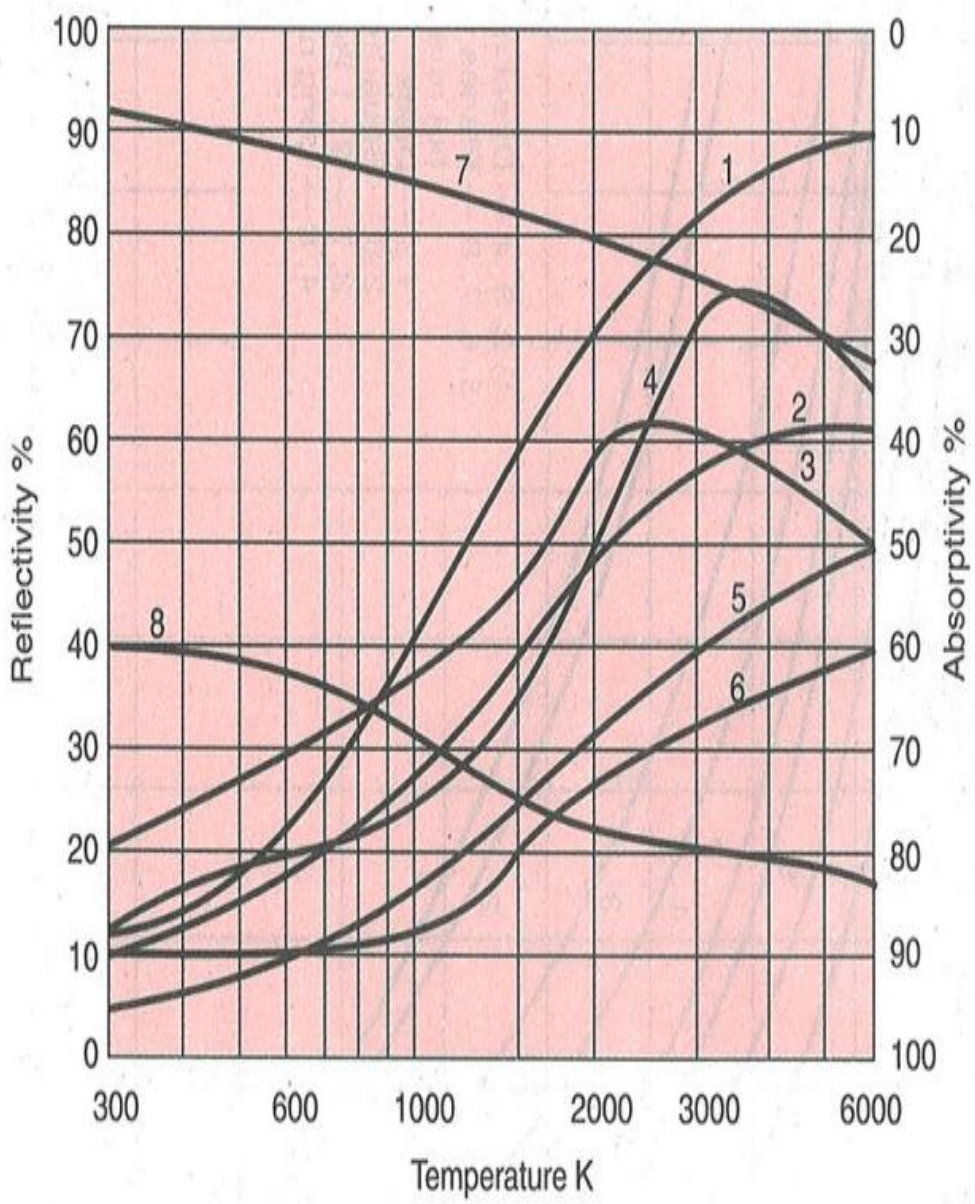
Surface	*Temperature °C*	ε_h	ε_n
Pyroceram	27	—	0.85
Pyroceram	327	—	0.78
Pyroceram	727	—	0.69
Pyroceram	1227	—	0.57
Rocks	27	0.88 – 0.95	—
Sand	27	0.90	—
Silicon carbide	327	—	0.87
Silicon carbide	727	—	0.87
Silicon carbide	1227	—	0.85
Skin	27	0.95	—
Snow	0	0.82 – 0.90	—
Soil	27	0.93 – 0.96	—
Teflon	27	0.85	—
Teflon	127	0.87	—
Teflon	227	0.92	—
Vegetation	27	0.92 – 0.96	—
Water	27	0.96	—
Wood	27	0.82 – 0.92	—

SOLAR RADIATIVE PROPERTIES FOR SELECTED MATERIALS

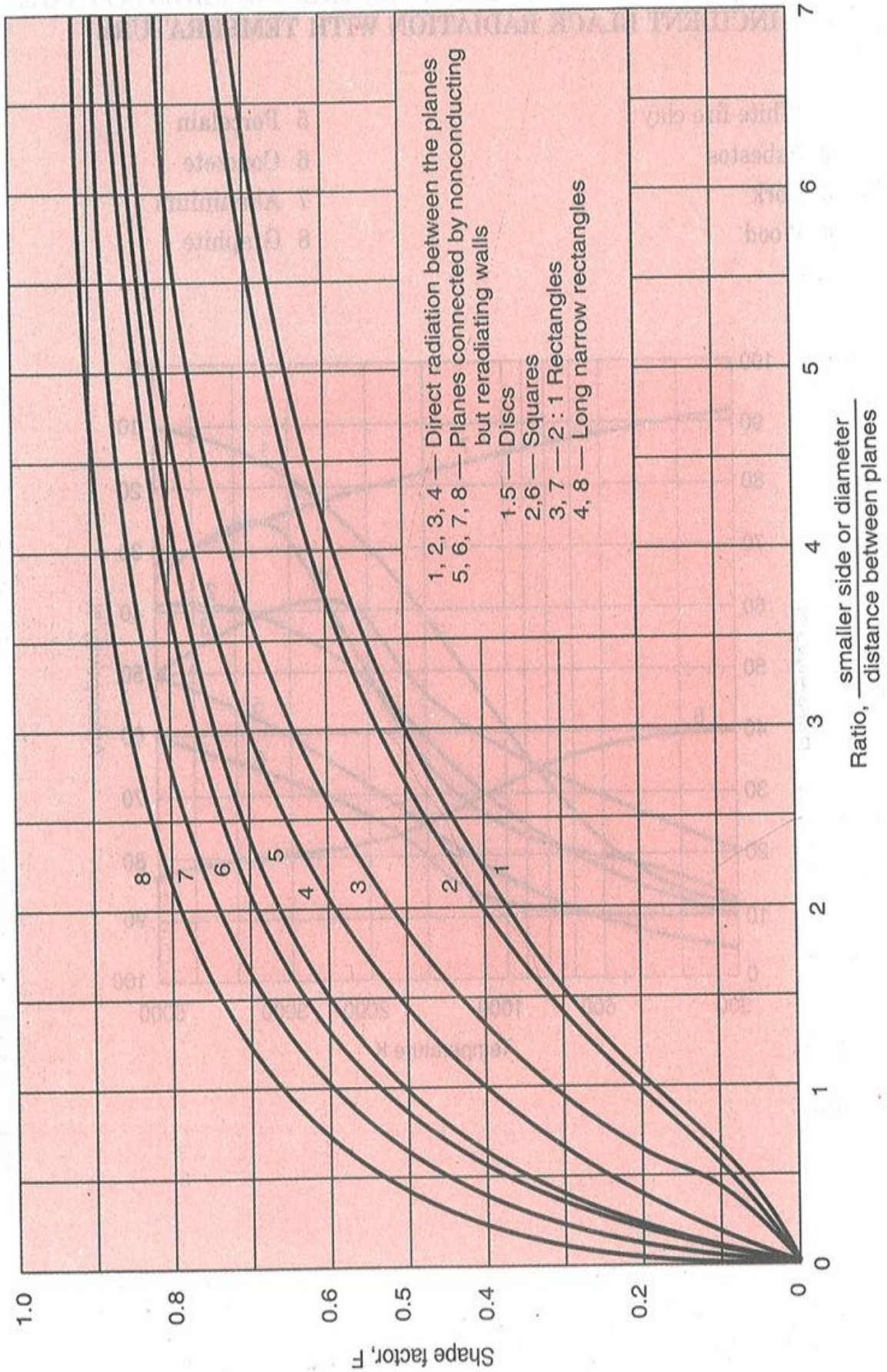
Material	*Absorptivity* α	*Emissivity at 300 K* ε	*transmissivity* τ	$\alpha/\in$
Aluminium, polished	0.09	0.03	—	3.0
Aluminium, anodised	0.14	0.84	—	0.17
Aluminium coated over quartz	0.11	0.37	—	0.30
Aluminium foil	0.15	0.05	—	3.0
Brick, red	0.63	0.93	—	0.68
Concrete	0.60	0.88	—	0.68
Galvanised sheet metal, clean	0.65	0.13	—	5.0
Galvanised oxidised, weathered	0.80	0.28	—	2.9
Glass, 3.2 mm, thickness :				
Float or tempered	—	—	0.78	—
Low iron oxide type	—	—	0.88	—
Metals, plated :				
Black sulfide	0.92	0.10	—	9.2
Black cobalt oxide	0.93	0.30	—	3.1
Black Nickel oxide	0.92	0.08	—	11.0
Black chrome	0.87	0.09	—	9.7
Mylar, 0.13 mm thickness	—	—	0.87	—
Paints : Black	0.98	0.98	—	1.0
White acrylic	0.26	0.90	—	0.29
White zinc oxide	0.16	0.92	—	0.17
Plexi glass, 3.2 mm thickness	—	—	0.90	
Snow, fresh, fine particles	0.13	0.82	—	0.16
Snow ice granules	0.33	0.89	—	0.37
Tedlar, 0.10 mm	—	—	0.92	—
Teflon, 0.13 mm	—	—	0.92	—

VARIATION OF TOTAL REFLECTIVITY AND ABSORBTIVITY FOR INCIDENT BLACK RADIATION WITH TEMPERATURE

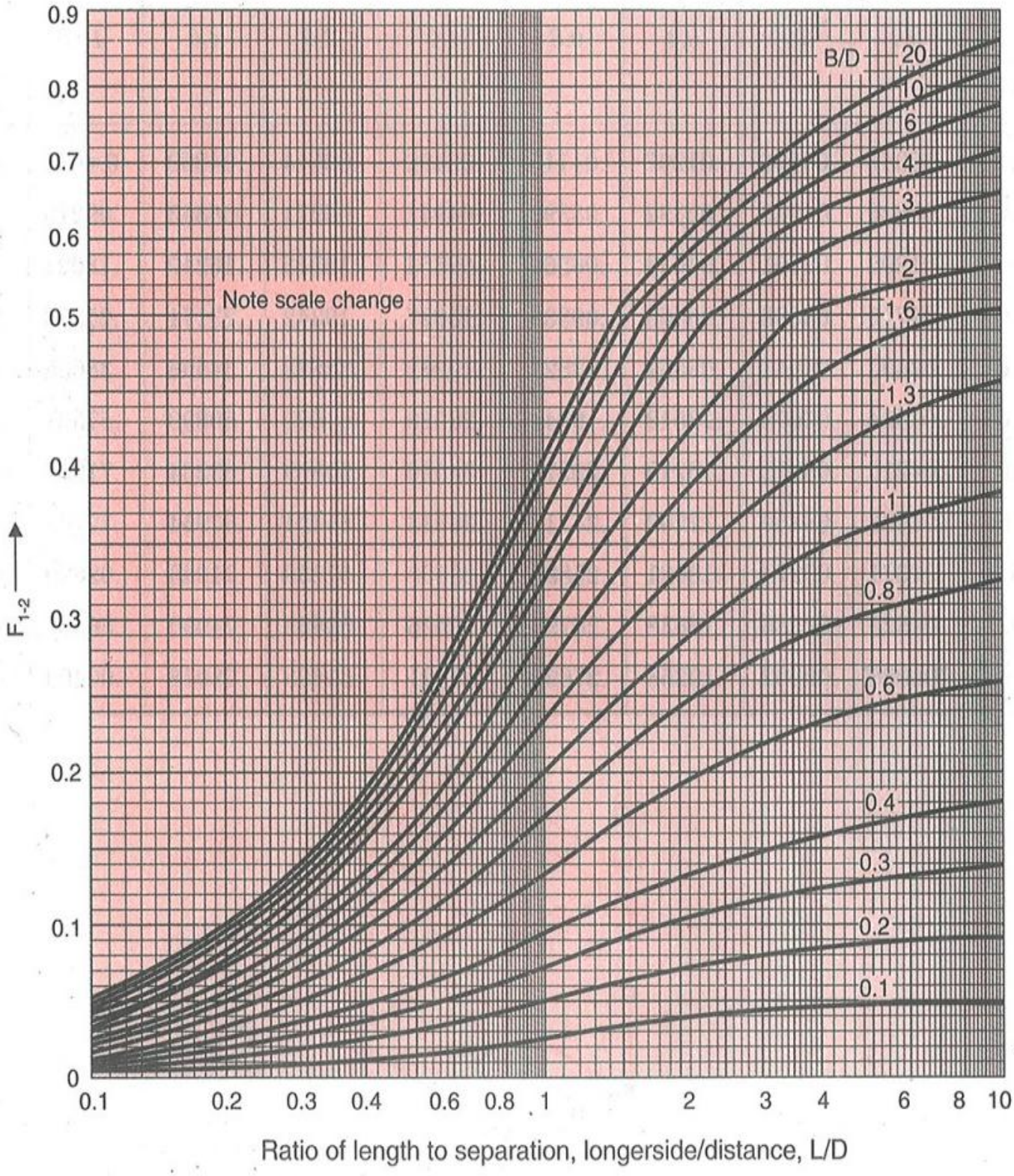
1 White fire clay
2 Asbestos
3 Cork
4 Wood
5 Porcelain
6 Concrete
7 Aluminium
8 Graphite



SHAPE FACTORS FOR EQUAL AND PARALLEL SQUARES, RECTANGLES AND DISCS



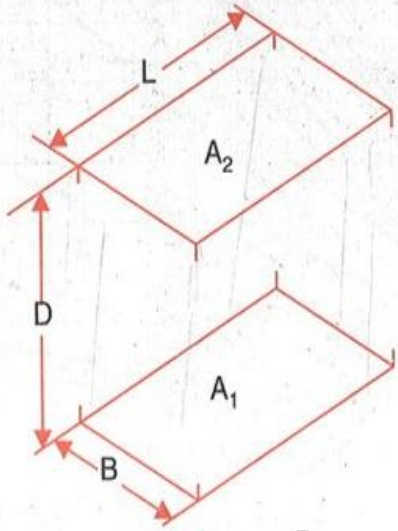
SHAPE FACTOR FOR EQUAL PARALLEL RECTANGLES IN OPPOSITE LOCATION



(See next page for notations)

SHAPE FACTORS $F_{1\text{-}2}$: EQUAL PARALLEL RECTANGLES IN OPPOSITE LOCATION

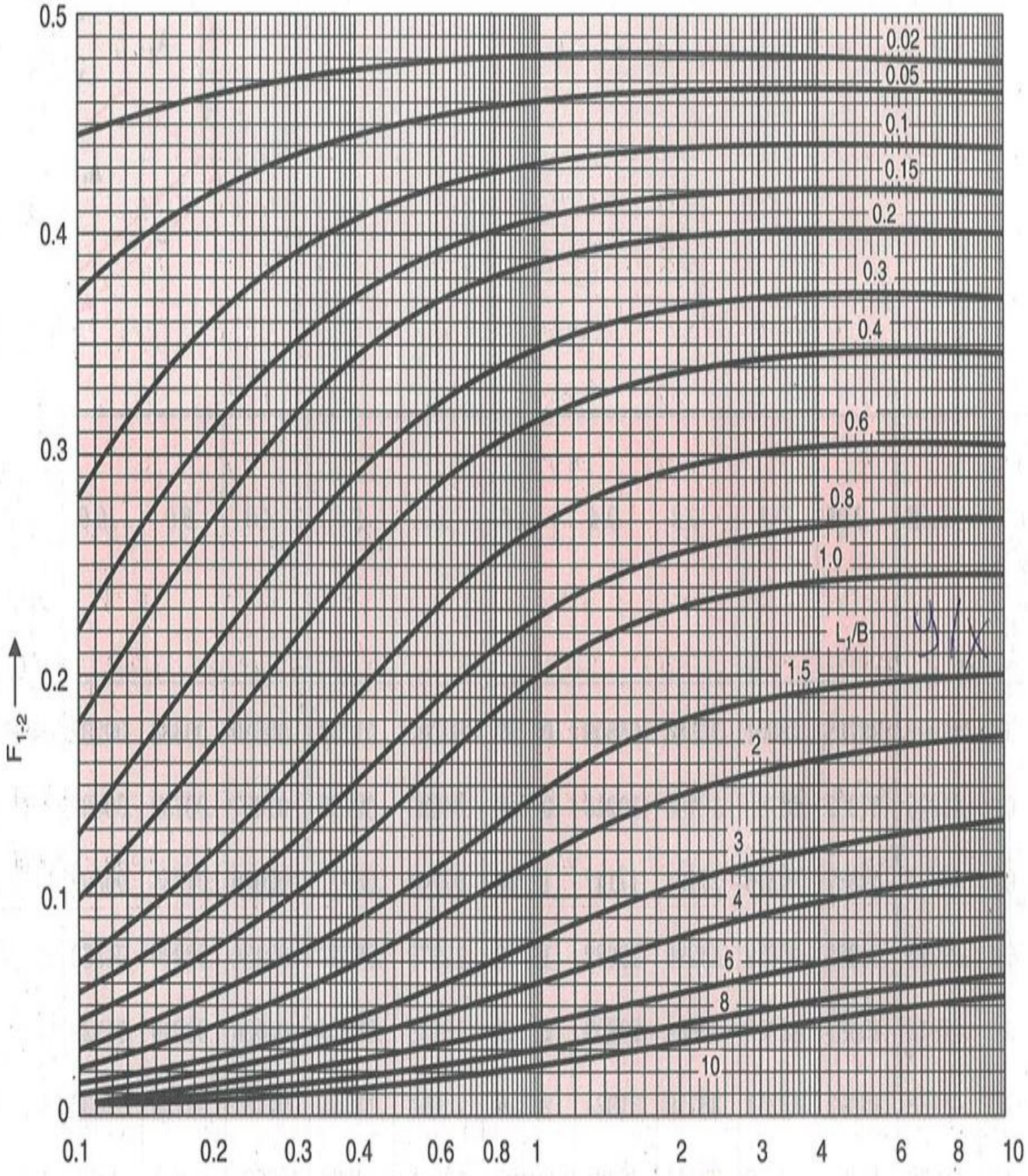
$Y_{B/D}$ ↓ \ X → L/D	*0.1*	*0.2*	*0.4*	*0.6*	*1.0*	*2.0*	*4.0*	*10.0*	∞
0.1	.00316	.00626	.01207	.01715	.02492	.03514	.04209	0.4671	.04988
0.2	.00626	.01240	.02392	.03398	.04941	.06971	.08353	.09270	.09901
0.4	.01207	.02391	.04614	.06560	.09554	.13513	.16219	.18021	.19258
0.6	.01715	.03398	.06560	.09336	.13627	.19342	.23171	.25896	.27698
1.0	.02492	.04941	.09554	.13627	.19982	.28588	.34596	.38638	.41421
2.0	.03514	.06971	.13513	.19341	.28588	.41525	.50899	.57361	.61803
4.0	.04210	.08353	.16219	.23271	.34596	.50899	.63204	.71933	.78078
6.0	.04463	.08859	.17209	.24712	.36813	.54421	.67954	.77741	.84713
10.0	.04671	.09272	.18021	.25896	.38638	.57338	.71933	.82699	.90499
20.0	.04829	.09586	.18638	.26795	.40026	.59563	.74990	.86563	.95125
∞	.04988	.09902	.19258	.27698	.41421	.61803	.78078	.90499	1.00000



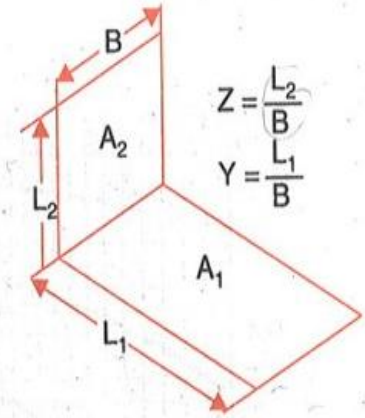
$X = \frac{L}{D}, Y = \frac{B}{D}$

See previous page for chart

SHAPE FACTORS $F_{1\text{-}2}$—PERPENDICULAR RECTANGLES (*See next page for notations*)



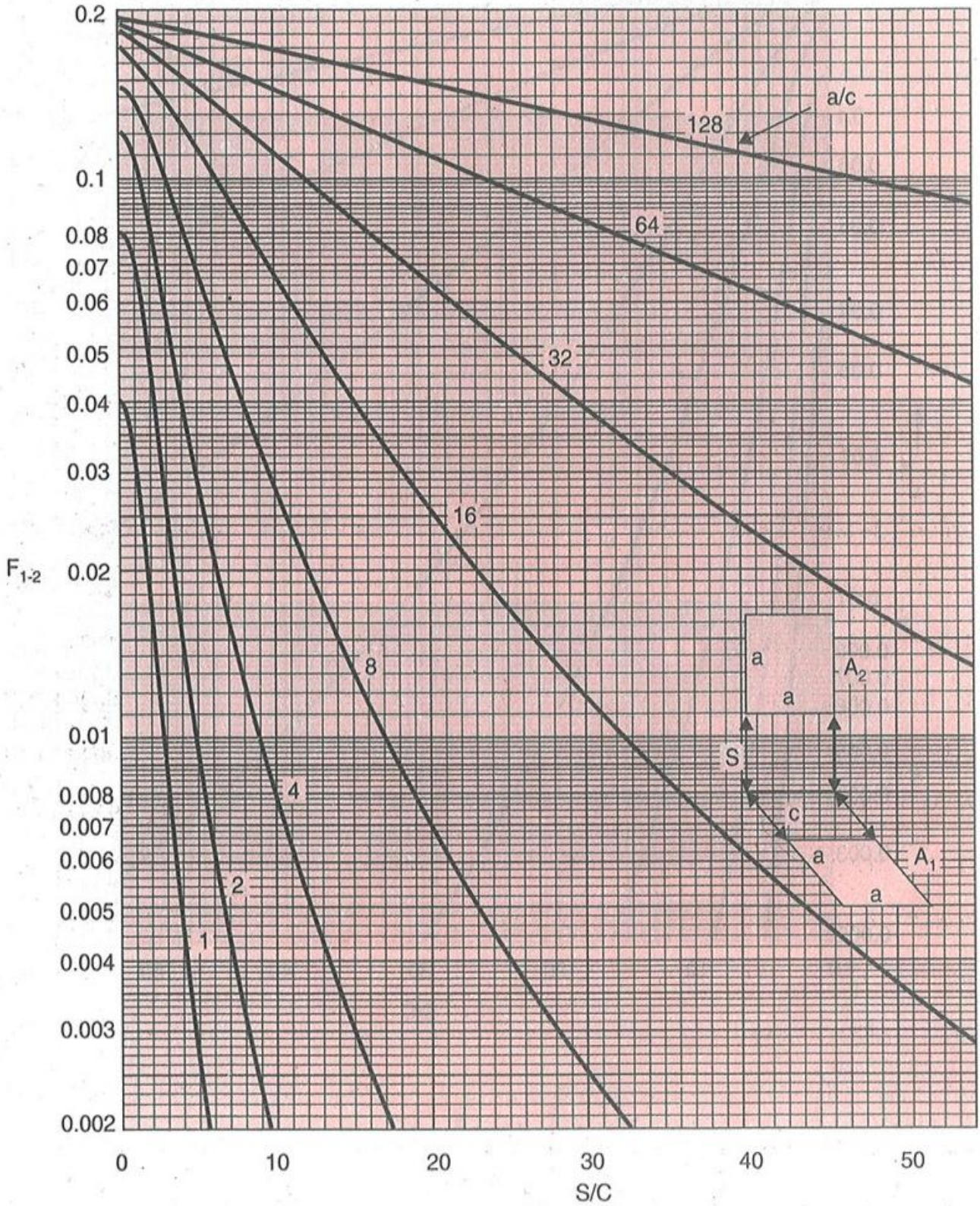
SHAPE FACTORS F_{1-2} : PERPENDICULAR RECTANGLES



$Y \rightarrow$ L_1/B / Z L_2/B $\downarrow$	0.02	0.05	0.1	0.2	0.4	0.6	1.0	2.0	4.0	6.0	10.0	20.0
.05	.39908	.28738	.18601	.10584	.05606	.03799	.02304	.01158	.00580	.00388	.00232	.00116
0.1	.44375	.37202	.28189	.18108	.10215	.07048	.04326	.02188	.01097	.00732	.00439	.00220
0.2	.46615	.42337	.36216	.27104	.17147	.12295	.07744	.03971	.02000	.01335	.00802	.00401
0.4	.47725	.44852	.40859	.34295	.25032	.19206	.12770	.06757	.03434	.02296	.01380	.00691
0.6	.47943	.45587	.42290	.36884	.28809	.23147	.16138	.08829	.04536	.03040	.01829	.00916
1.0	.48138	.46073	.43251	.38719	.31924	.26896	.20004	.11643	.06131	.04130	.02492	.01249
2.0	.48239	.46327	.43756	.39711	.33784	.29429	.23285	.14930	.08365	.05731	.03491	.01757
4.0	.48267	.46397	.43898	.39994	.34339	.30238	.24522	.16731	.10136	.07184	.04484	.02285
6.0	.48273	.46411	.43925	.40048	.34447	.30399	.24783	.17193	.10776	.07822	.04998	.02587
10.0	.48275	.46418	.43939	.40076	.34503	.30482	.24921	.17455	.11210	.08331	.05502	.02938
20.0	.48276	.46421	.43943	.40089	.34528	.30518	.24980	.17571	.11427	.08624	.05876	.03302
∞	.48277	.46422	.43947	.40092	.34535	.30530	.25000	.17611	.11505	.08738	.06053	.03578

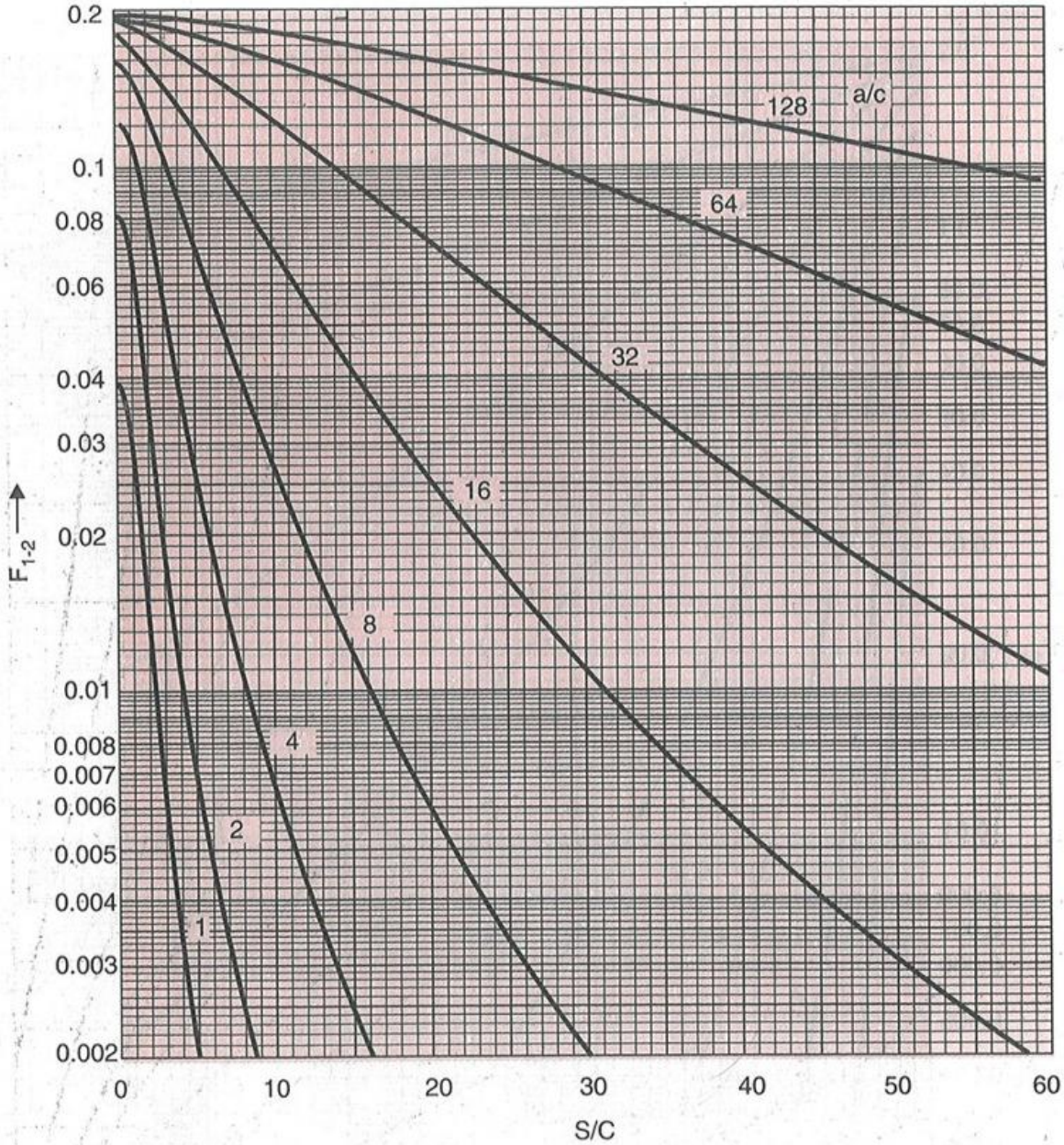
Note carefully positions of A_1 and A_2

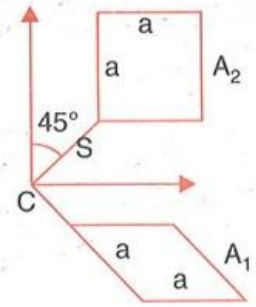
SHAPE FACTOR—NON INTERSECTING PERPENDICULAR EQUAL SQUARES



Note positions of A_1 and A_2 carefully.

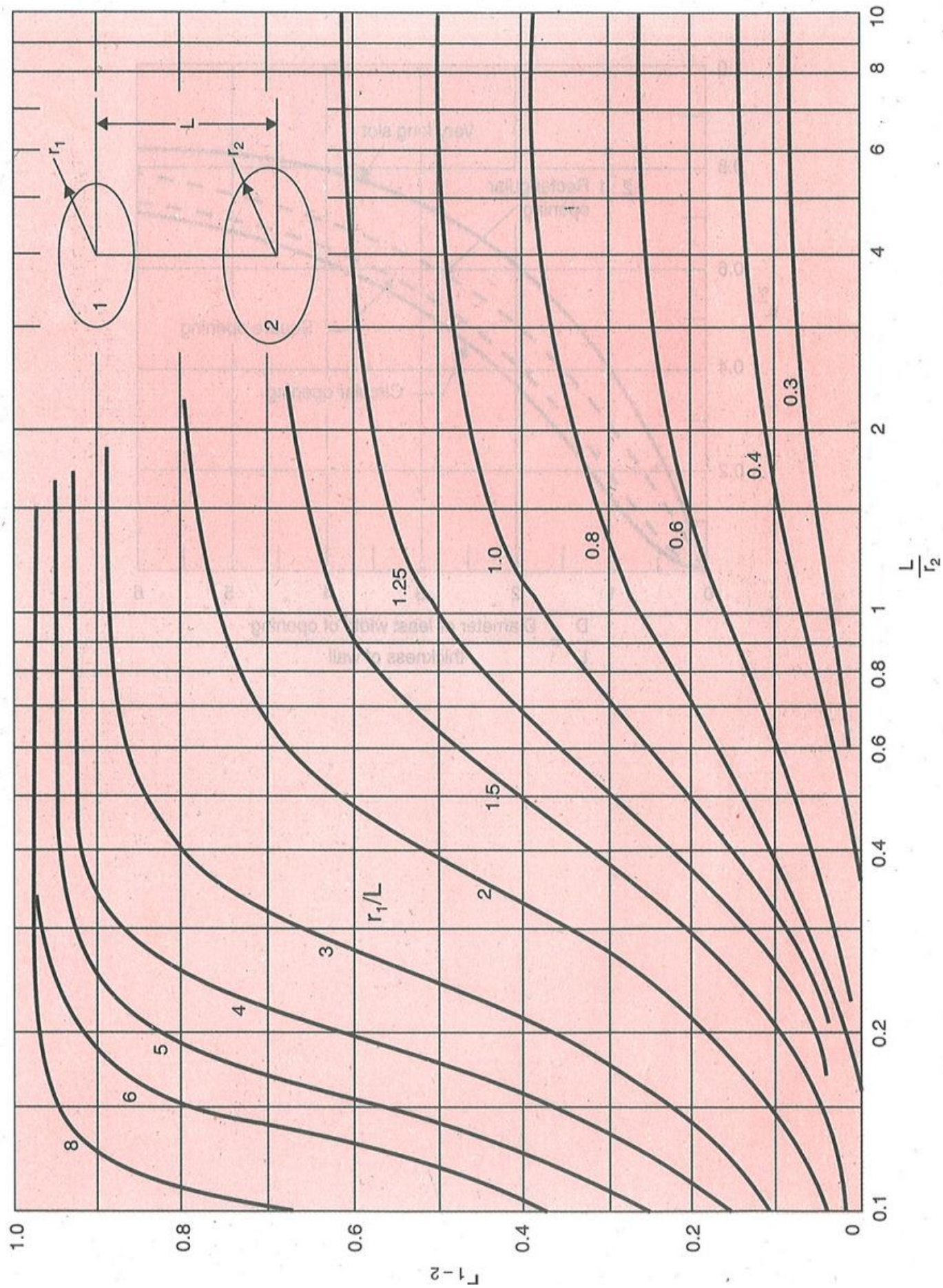
SHAPE FACTOR—OFFSET NON INTERSECTING PERPENDICULAR SQUARES



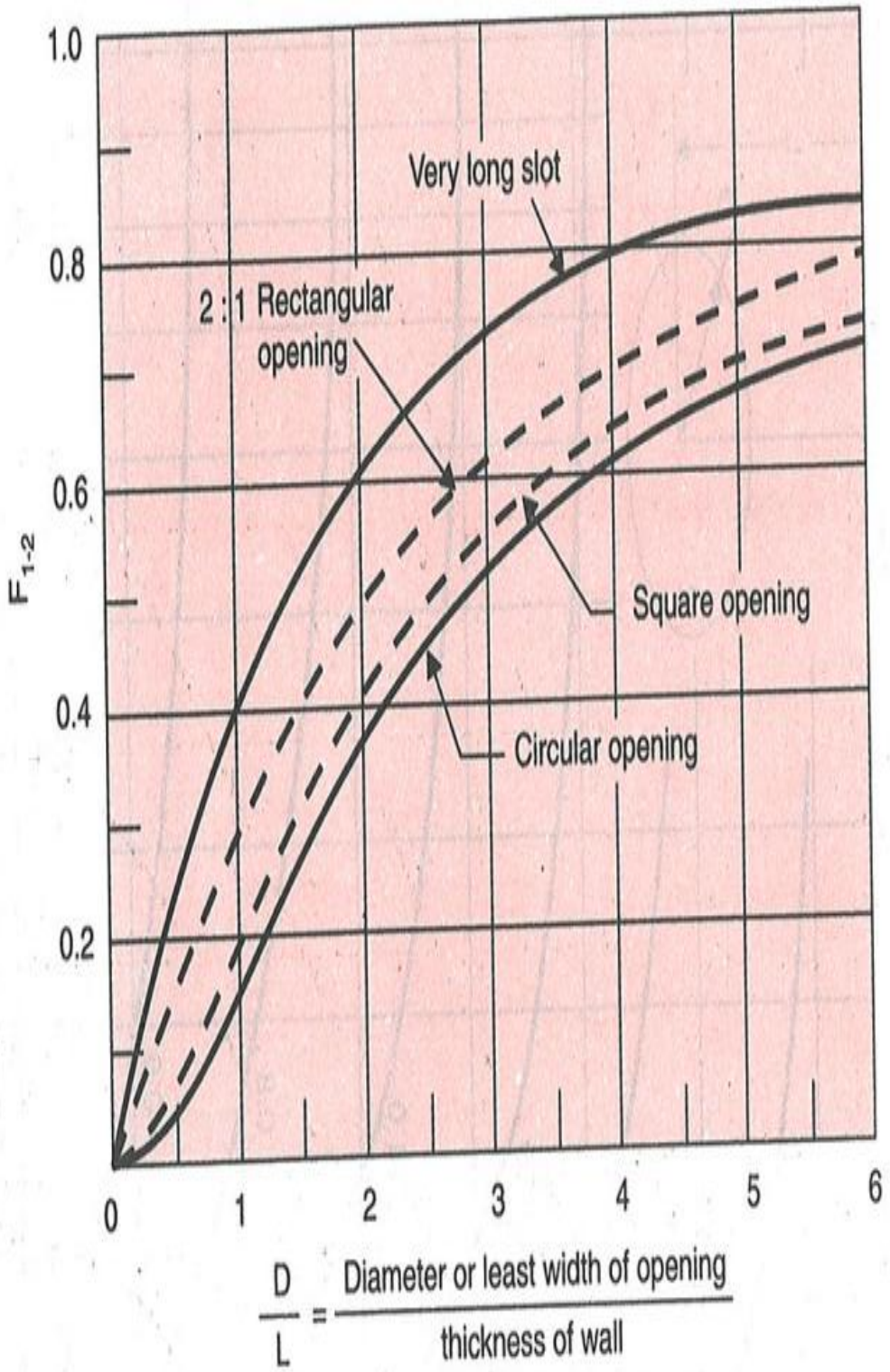


Note positions of A_1 and A_2 carefully

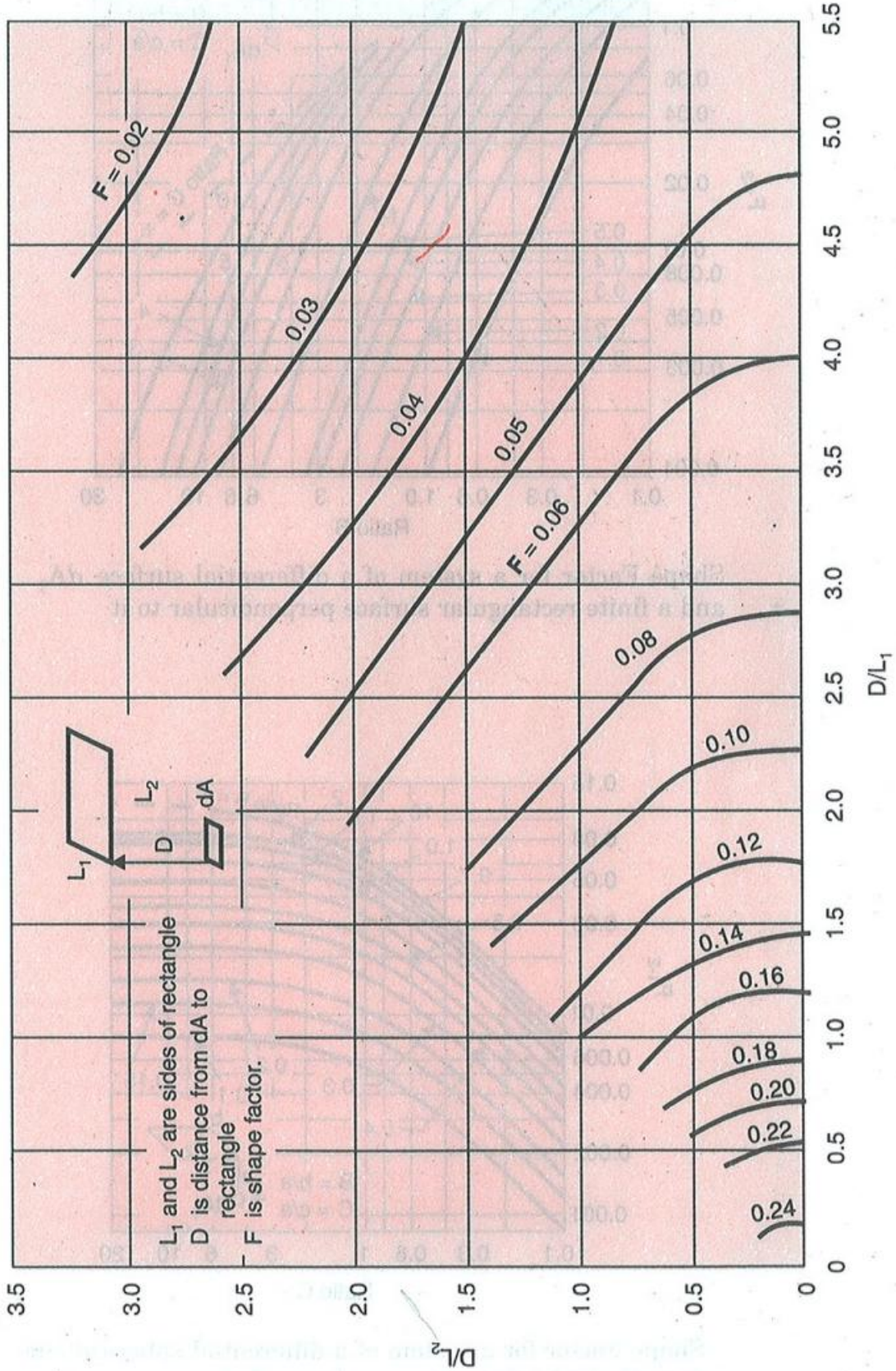
SHAPE FACTOR—COAXIAL DISCS OF DIFFERENT RADII

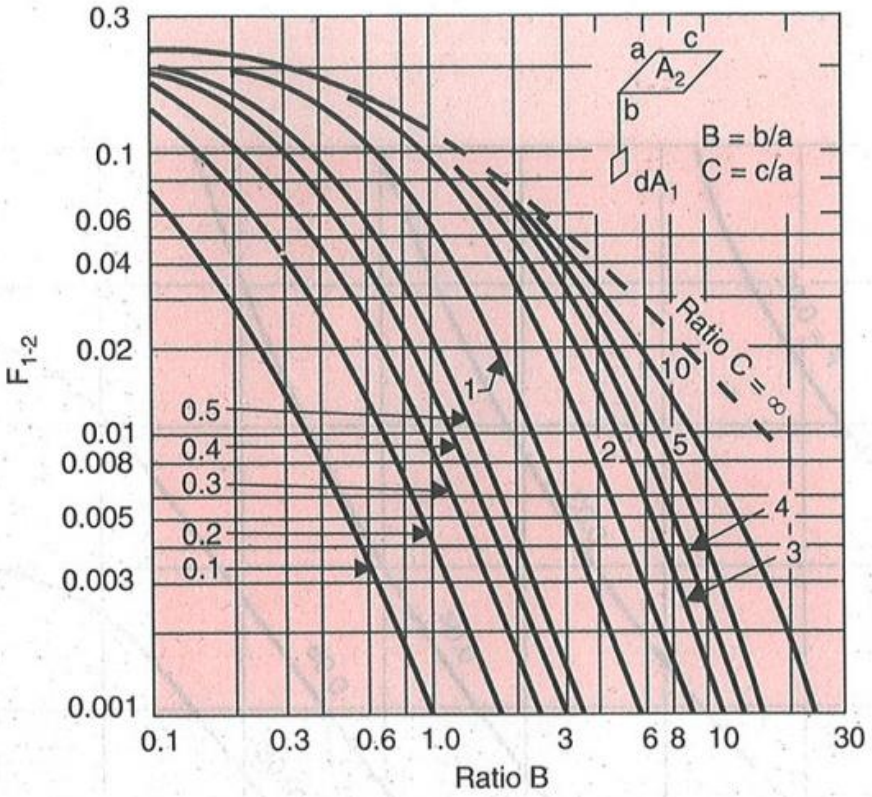


SPAPE FACTOR F_{1-2} : FOR SLOTS AND OPENINGS IN WALL OF THICKNESS, L

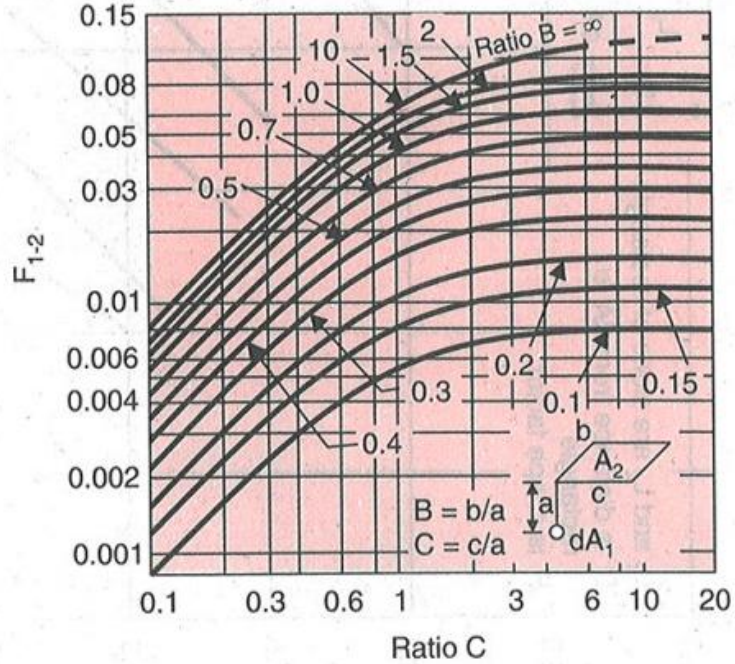


SHAPE FACTOR FOR A SURFACE ELEMENT dA TO A RECTANGULAR SURFACE PARALLEL TO IT AT CORNER



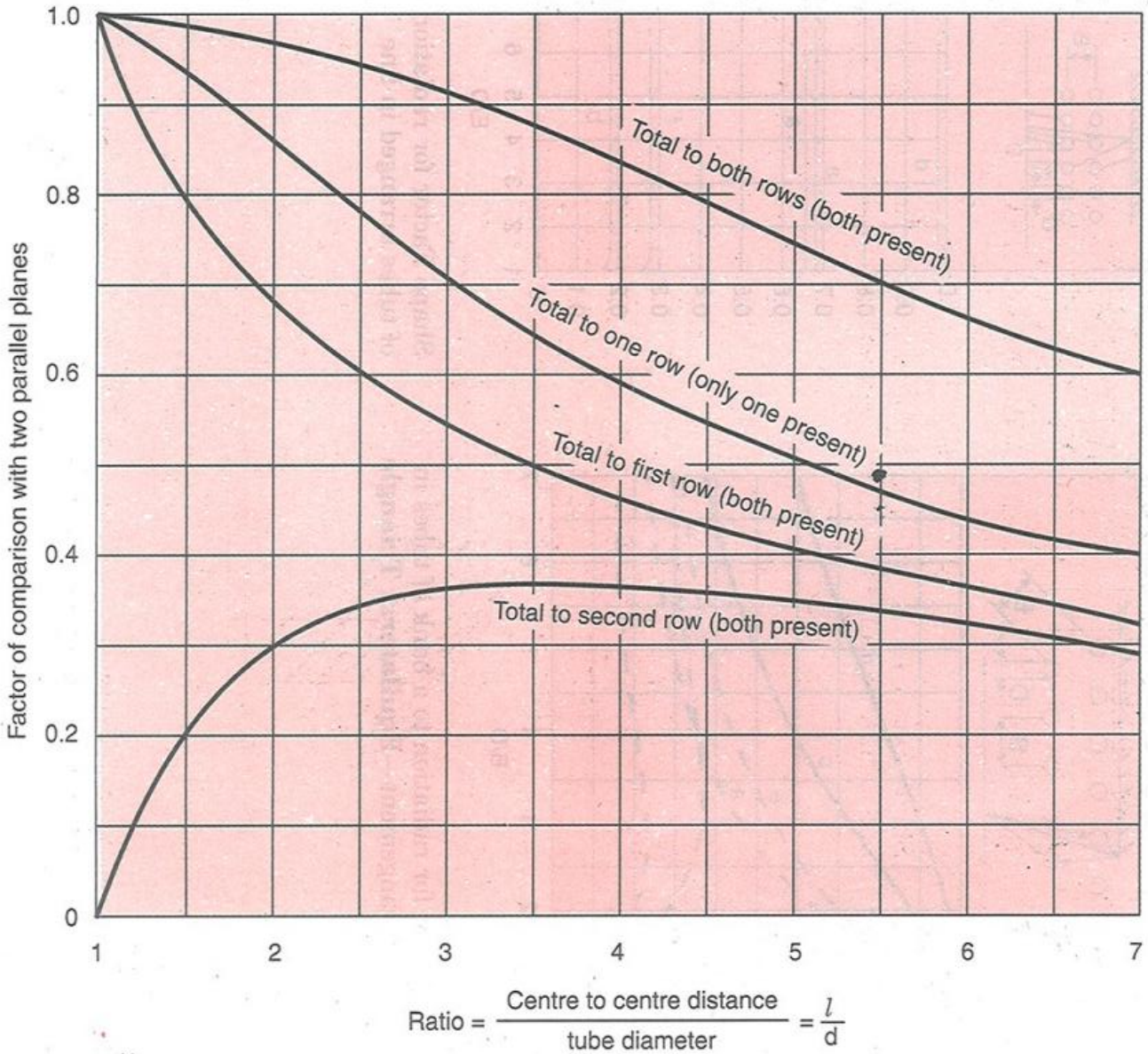


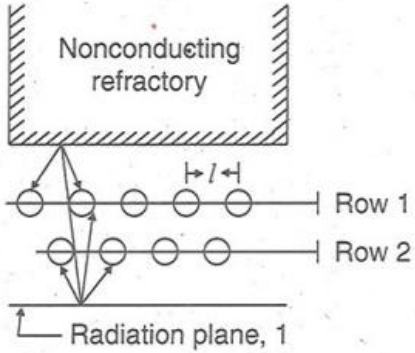
Shape Factor for a system of a differential surface dA_1 and a finite rectangular surface perpendicular to it



Shape Factor for a system of a differential spherical surface dA_1 and a finite rectangular surface

SHAPE FACTOR COMPARED TO PARALLEL PLANES, FOR A PLANE AND ONE OR TWO ROWS OF TUBES PARALLEL TO IT





Ordinate is fraction of heat radiated from the plane to an infinite number of row of tubes or to a plane replacing the tubes

SHAPE FACTOR FOR RADIATION TO BANKS OF TUBES IN VARIOUS ARRANGEMENTS

Curve a : Direct radiation to row 1

Curve b : Direct radiation to row 2

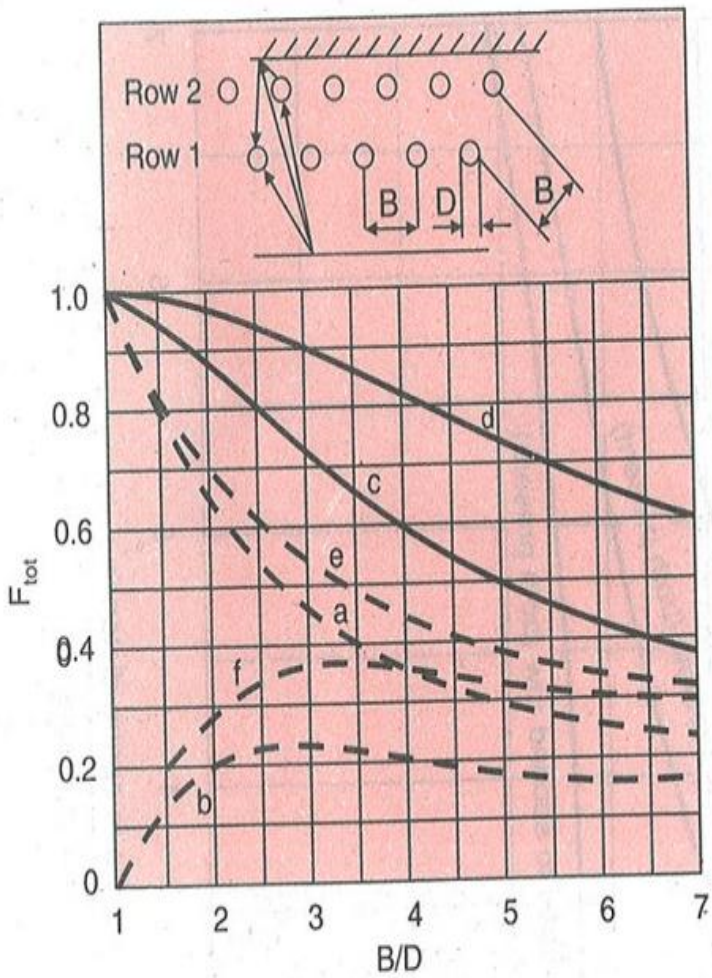
Curve c : Total radiation to row 1 if bank consists of one row only

Curve d : Total radiation to rows 1 and 2

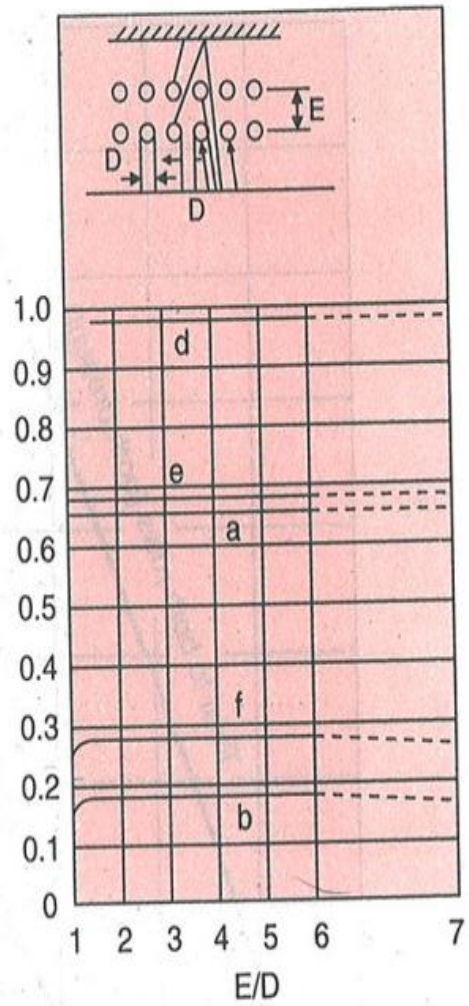
Curve e : Total radiation to row 1

Curve f : Total radiation to row 2

} if bank consists of two rows

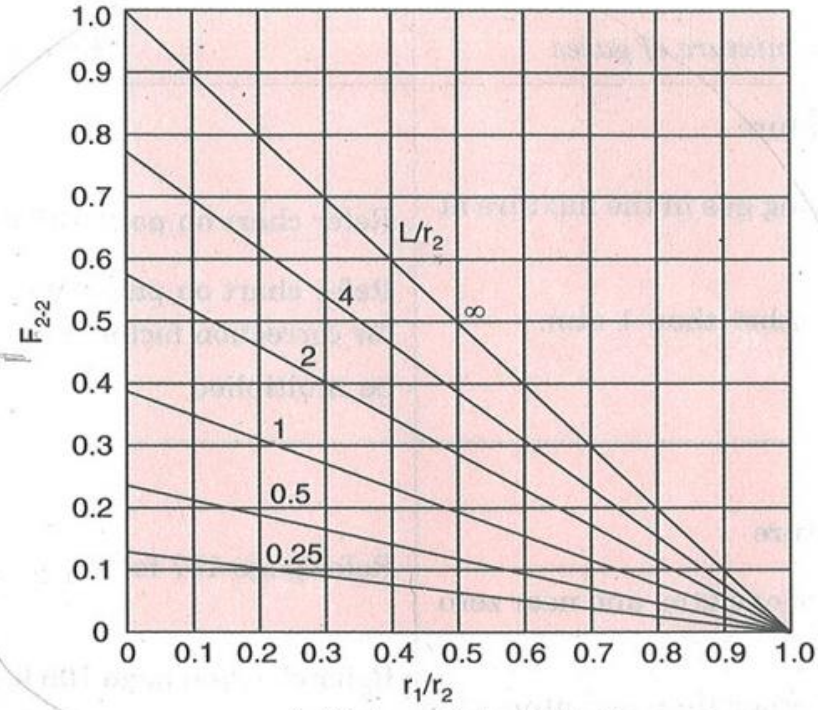


Shape Factor for radiation to a bank of tubes in staggered arrangement—**Equilateral Triangle**

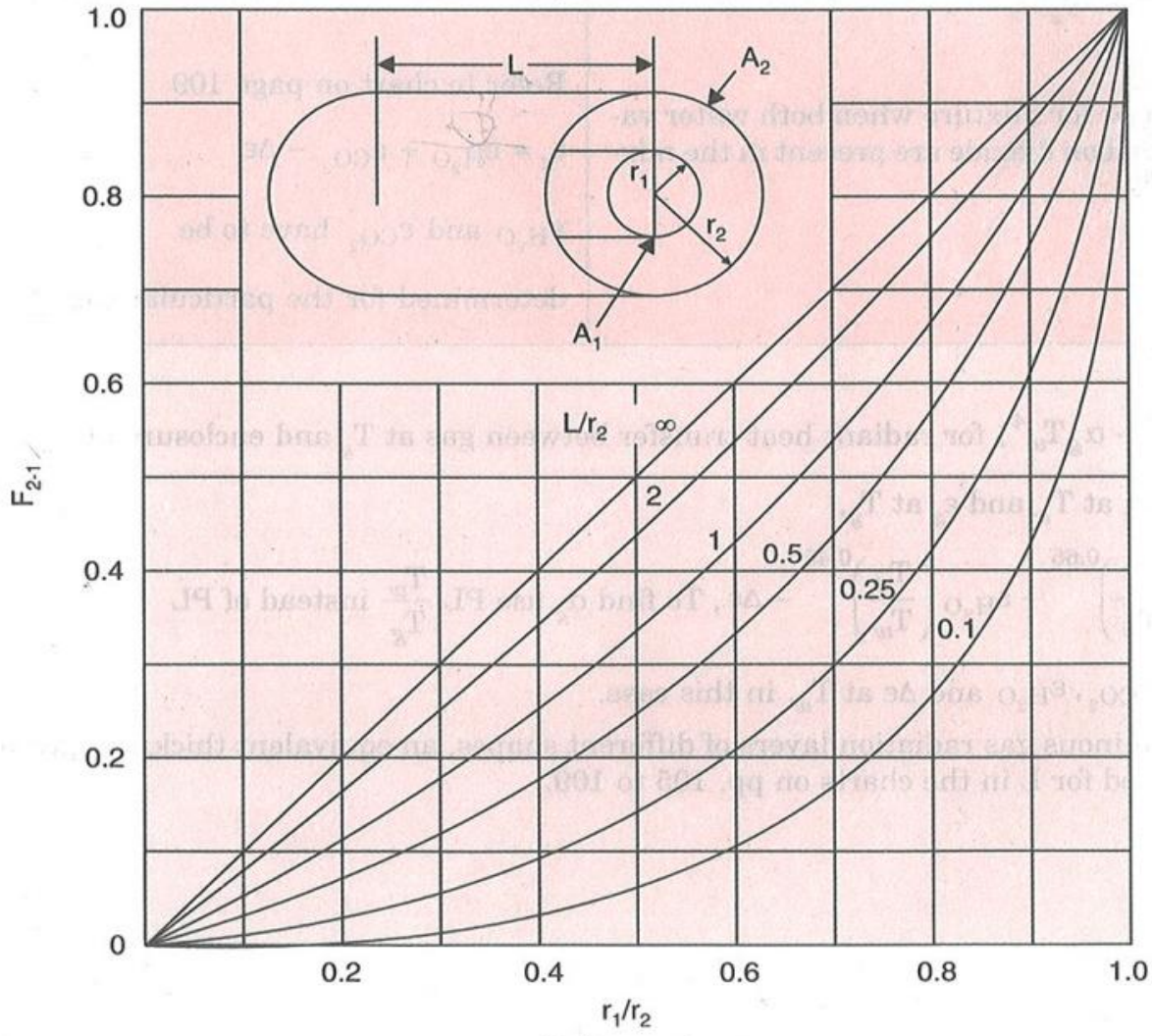


Shape Factor for radiation to a bank of tubes arranged in line

SHAPE FACTOR—SHORT CONCENTRIC CYLINDERS



(a) Outer cylinder to itself



(b) Outer to inner

GAS RADIATION

Condition of gas or mixture of gases	**Emissivity, ε_R*
1. Carbon dioxide in mixture	
(*i*) Only CO_2 as radiating gas in the mixture at 1 atm.	Refer chart on page 105 for ε_{CO_2}
(*ii*) Mixture pressures other than 1 atm.	Refer chart on page 106 for correction factor, C_{CO_2}, by which ε_{CO_2} has to be multiplied
2. Water Vapour in mixture	
(*i*) at a total pressure of one atm. and near zero partial pressure	Refer page 107 for ε_{H_2O}
(*ii*) Mixture pressures other than one atm.	Refer chart on page 108 for correction factor C_{H_2O} By which ε_{H_2O} has to be multiplied
3. Correction $\Delta\varepsilon$ for mixture when both water vapour and carbon dioxide are present in the mixture	Refer to chart on page 109 $\varepsilon_g = \varepsilon_{H_2O} + \varepsilon_{CO_2} - \Delta\varepsilon$ ε_{H_2O} and ε_{CO_2} have to be determined for the particular cases.

$\frac{Q}{A} = \sigma[\varepsilon_s T_s^4 - \alpha_g T_w^4]$ for radiant heat transfer between gas at T_g and enclosure at T_w.

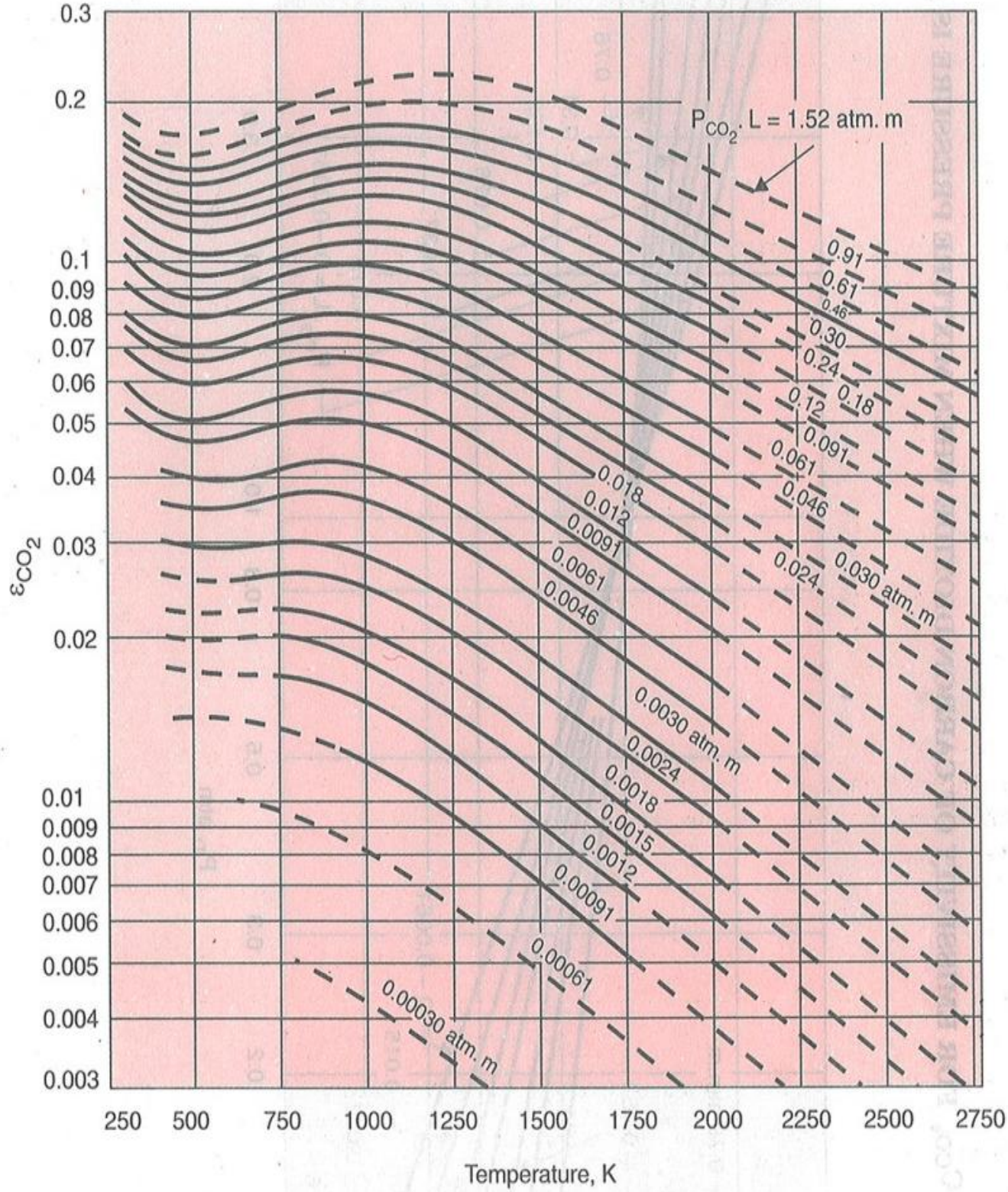
Determine α_g at T_w and ε_g at T_g,

$$\alpha_g = \varepsilon_{CO_2}\left(\frac{T_g}{T_w}\right)^{0.65} + \varepsilon_{H_2O}\left(\frac{T_g}{T_w}\right)^{0.45} - \Delta\varepsilon$$, To find α_g use PL $\frac{T_w}{T_g}$ instead of PL

Determine ε_{CO_2}, ε_{H_2O} and $\Delta\varepsilon$ at T_w, in this case.

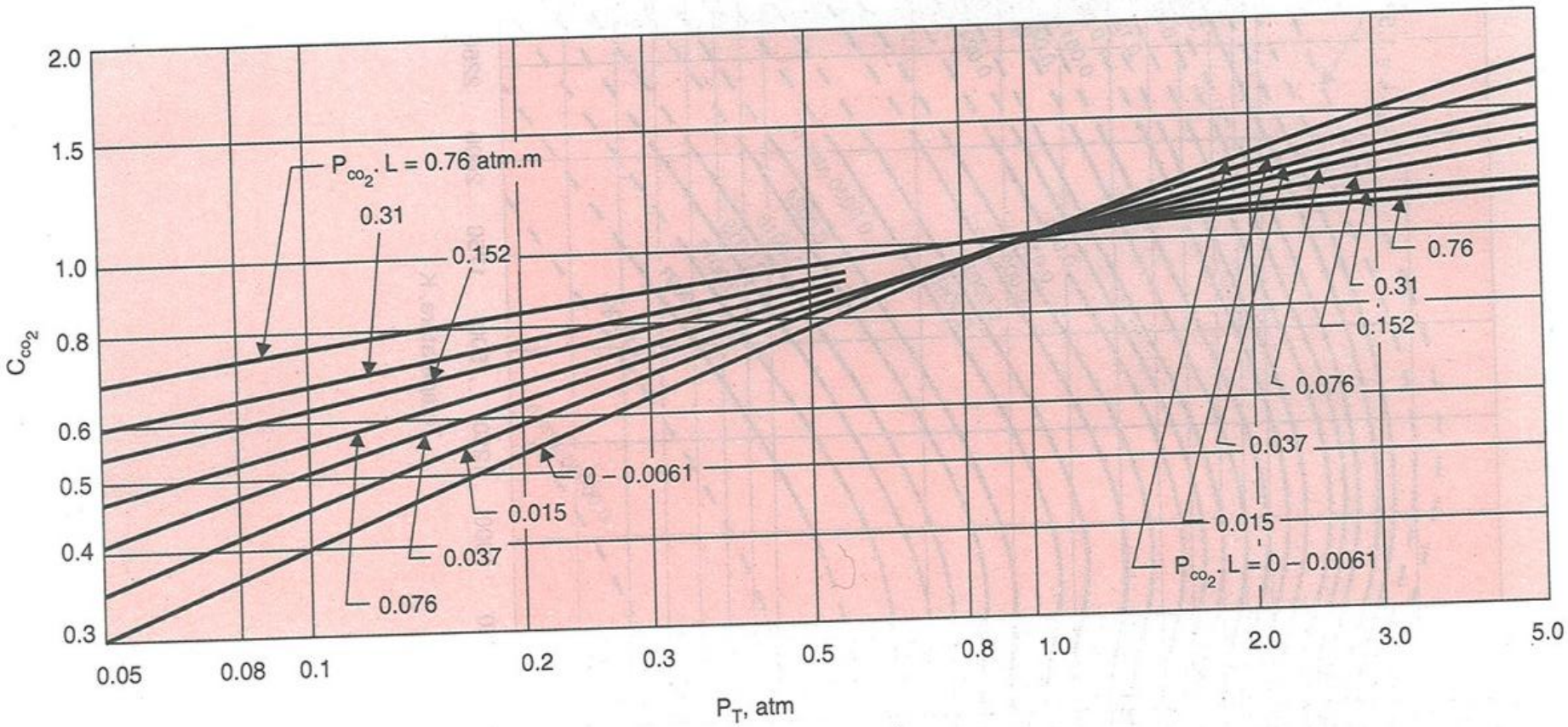
*For non-luminous gas radiation layers of different shapes, an equivalent thickness given on page should be used for L in the charts on pp. 105 to 109.

EMISSIVITY OF CARBON-DI-OXIDE IN A MIXTURE AT 1 ATM



* for L refer page 110

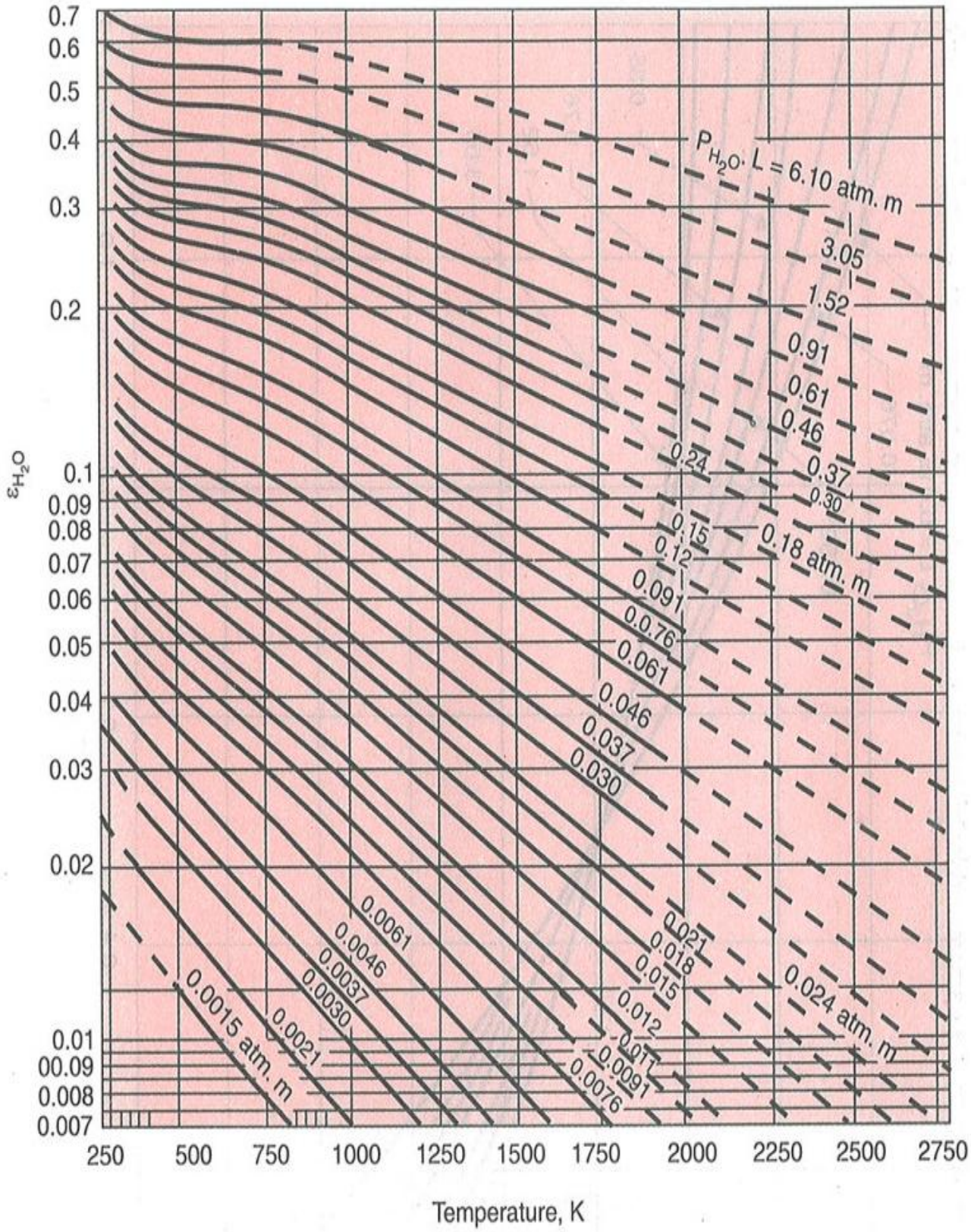
CORRECTION FATOR FOR C_{CO_2} FOR EMISSIVITY OF CARBON DIOXIDE WHEN MIXTURE PRESSURE IS OTHER THAN 1 atm.



* for L refer page 110

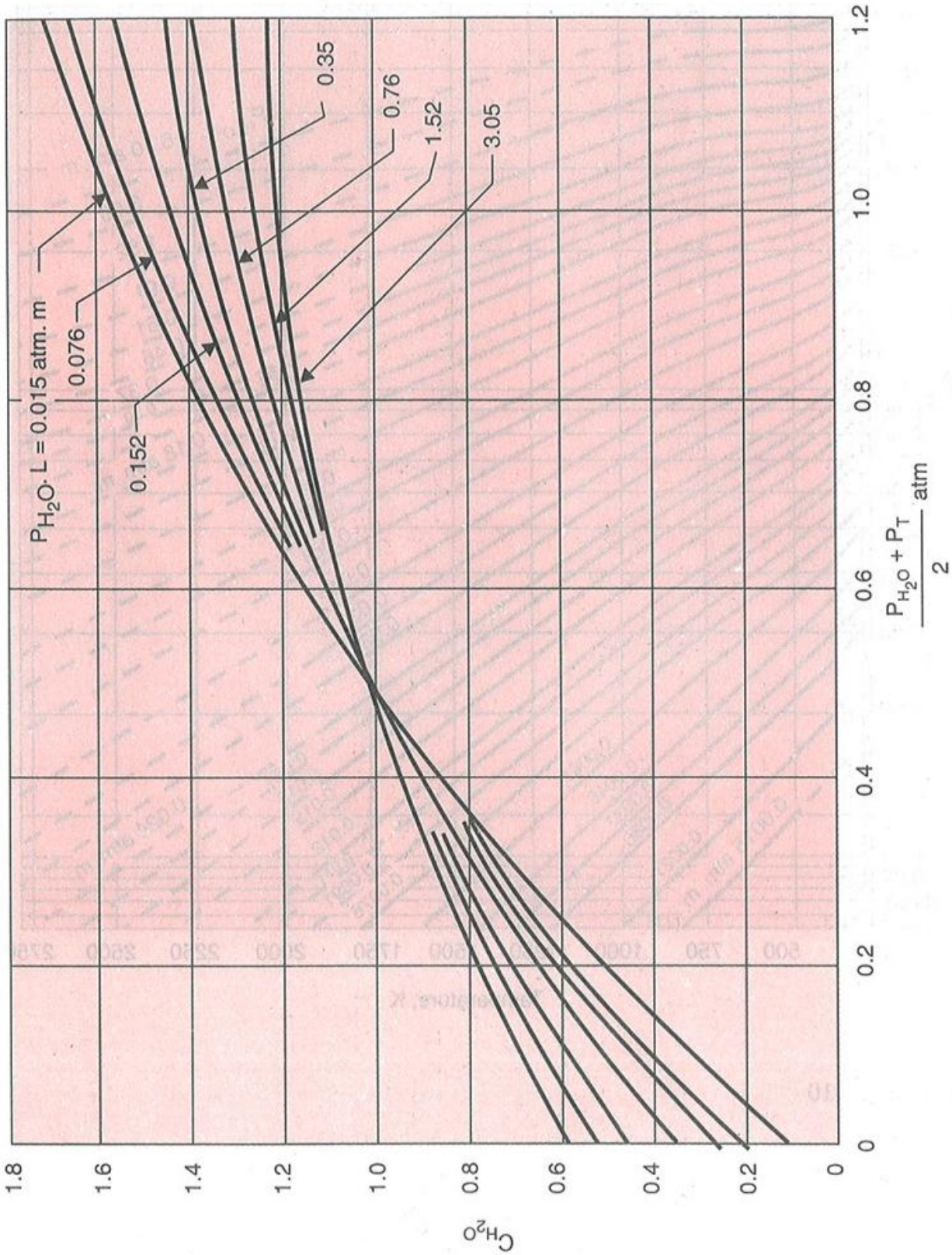
Flow conditions	*Correlation and Validity*	*Notations*
1.2.1 for liquid metals or silicones Constant heat flux	$Nu_x = \dfrac{[0.4637\, Re_x^{0.5}\, Pr^{0.333}]}{[1+(0.0207/Pr)^{0.67}]^{0.25}}$ Valid for : $Pr > 50$ and $Pr \le 0.05$ and for $Re_x\, Pr > 100$	$\overline{Nu_L}$ = Average Nusselt Number upto length L Nu_L = Nusselt Number at location L St = Stanton Number $= \dfrac{Nu}{Re\,.\,Pr}$ C_f = Average friction coefficient
1.3 Average values for constant heat flux or constant wall temperature	$\overline{Nu_L} = 2Nu_L$ $St\,.\,Pr^{2/3} = C_f/2$	
1.4 **FLAT PLATE TURBULENT FLOW** $5 \times 10^5 > Re_x < 10^7$	$\delta_{hx} = 0.381x\, Re^{-0.2}$ $\delta_{tx} \approx \delta_{hx}$	x = distance from leading edge δ_{hx} = hydrodynamic boundary layer thickness at x
1.4.1 Fully Turbulent from leading edge	$\delta_x = \delta_{hx}/8$ $\delta_{ix} = (7/72)\,\delta_{hx}$, $Nu_x = 0.0296\, Re_x^{0.8}\, Pr^{0.33}$ $\overline{Nu_L} = 0.037\, Re^{0.8}\, Pr^{0.33}$ Or by analogy Nu_x $= \dfrac{(C_{fx}/2)\, Re_x\, Pr}{1+12.8\,(C_{fx}/2)^{0.5}\,(Pr^{0.68}-1)}$ $C_{fx} = 0.0592\, Re_x^{-0.2}$: $5 \times 10^5 < Re < 10^7$ $C_{fx} = 0.37\,[\log_{10} Re_x]^{-2.584}$; $10^7 < Re < 10^9$	δ_{tx} = thermal boundary layer thickness at x δ_x = displacement thickness at x δ_{ix} = momentum thickness at x
1.4.2 FLAT PLATE, Turbulent Constant heat flux	Nu_x = 1.04 times Nu_x calculated as per constant wall temperature	
1.5 Laminar-Turbulent (combined)	δ_{hx} = $0.381x\, Re_x^{-0.2} - 10256x\, Re_x^{-1.0}$	C_{fx} = local friction coefficient defined by $\tau_{wx}/(\rho u_\infty^2/2)$

EMISSIVITY OF WATER VAPOUR IN A MIXTURE AT 1 atm



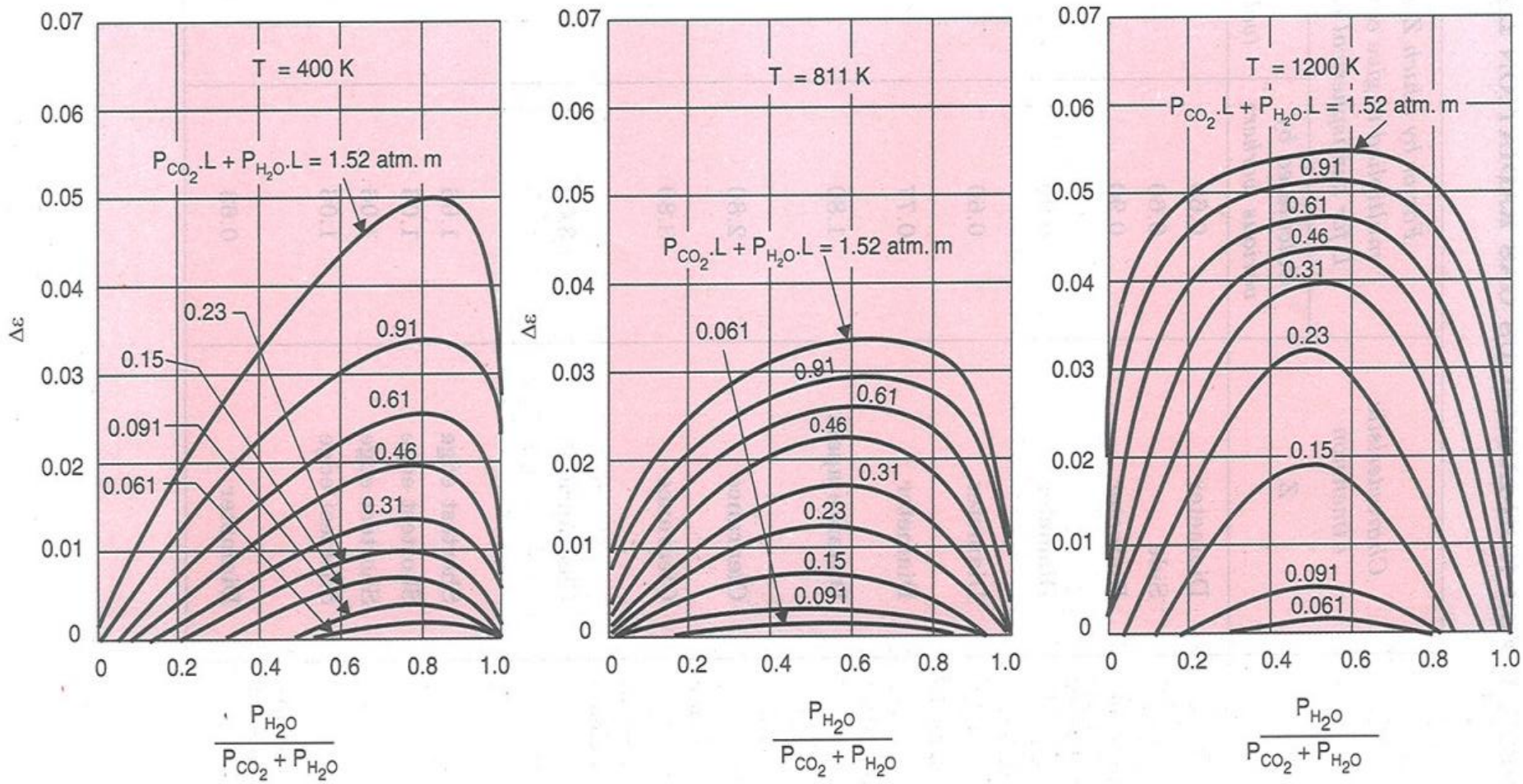
* for L refer page 110

CORRECTION FACTOR C_{H_2O} FOR ε_{H_2O} WHEN MIXTURE PRESSURE IS OTHER THAN 1 atm.



* for L refer page 110

CORRECTION FACTOR FOR EMISIVITY WHEN BOTH CO_2 AND H_2O ARE PRESENT IN THE MIXTURE



* for L refer page 110

EQUIVALENT THICKNESS, L FOR NON-LUMINOUS GAS RADIATION LAYERS OF DIFFERENT SHAPES

Shape	*Characteristic dimension Z*	*Factor by which Z is to be multiplied to give equivalent L for hemispherical radiation*	
		Calculated by various workers	*3.4 × (volume / area)*
Sphere	Diameter	0.60	0.57
Cube	Side	0.60	0.57
Infinite cylinder radiating to walls	Diameter	0.90	0.85
Infinite cylinder radiating to centre of base	Diameter	0.90	0.85
Cylinder, height = diameter, radiating to whole surface	Diameter	0.60	0.57
Cylinder, ht = diam., radiating to centre of base	Diameter	0.77	0.57
Space between infinite parallel planes	Distance apart	1.80	1.70
Space outside infinite bank of tubes with centres on equilateral triangles, tube diameter = clearance	Clearance	2.80	2.89
Same as above, with tube diameter = one half clearance	Clearance	3.80	3.78
Same as above, with tube centres on squares, and tube diameter = clearance	Clearance	3.50	3.49
Rectangular parallelepiped,			
1 × 2 × 6 radiating to :			
2 × 6 face	Shortest edge	1.06	1.01
1 × 6 face	Shortest edge	1.06	1.05
1 × 2 face	Shortest edge	1.06	1.01
all faces	Shortest edge	1.06	1.02
Infinite cylinder of semicircular cross-section radiating to centre of flat side	Diameter	0.63	0.52

DIMENSIONLESS GROUPS : (D—diffusion coefficient, *d*—diameter)

Groups	*Symbol*	*Name*	*Significance*
hL/k_s, hR/k	Bi	Biot Number	$\frac{\text{Internal conduction resistance}}{\text{Surface convection resistance}}$
$\Delta P/\rho u^2$	Eu	Euler Number	Pressure force / Inertia force
$\frac{\alpha\tau}{R^2}, \frac{\alpha\tau}{L^2}$	Fo	Fourier Number	$\frac{\text{Characteristic body dimension}}{\text{Temperature wave penetration depth in time, } \tau}$
u^2/gL	Fr	Froude Number	Inertia force / gravity force
$RePr\ \frac{d}{x}$	Gz	Graetz Number	$\frac{\text{Heat transfer by conduction}}{\text{Heat transfer by convection}}$ (with entrance region consideration)
$g\beta\Delta TL^3\rho^2/\mu^2$	Gr	Grashof Number	$\left(\frac{\text{Buoyant force}}{\text{Viscous force}}\right)\left(\frac{\text{Inertia force}}{\text{viscous force}}\right)$
λ/L	Kn	Knudson Number	$\frac{\text{Mean free path}}{\text{Characteristic body dimension}}$
α/D, Sc/Pr	Le	Lewis Number	$\frac{\text{Heat diffusivity}}{\text{Mass diffusivity}}$
$\frac{hL}{k}, \frac{hd}{k}$	Nu	Nusselt Number	Ratio of temperature gradients by conduction and convection at the surface
$uL\rho C_p/k$, $uD\rho C_p/k$	Pe = RePr	Peclet Number	$\frac{\text{Heat transfer by convection}}{\text{Heat transfer by conduction}}$
$\frac{C_p\mu}{k}$	Pr	Prandtl Number	$\frac{\text{Molecular diffusivity of momentum}}{\text{Molecular diffusivity of heat}}$
$\frac{g\beta\Delta TL^3\rho^2C_p}{\mu k}$	Ra = GrPr	Rayleigh Number	Refer Pr and Gr
$\frac{uL}{v}, \frac{ud}{v}, \frac{ud\rho}{\mu}$	Re	Reynolds Number	Inertia force / viscous force
$\mu/\rho D$, $\frac{v}{D}$	Sc	Schmidt Number	$\frac{\text{Molecular diffusivity of momentum}}{\text{Molecular diffusivity of mass}}$
h_mL/D, h_md/D	Sh	Sherwood Number	Ratio of concentration gradients at the boundary by diffusion and by convection
$\frac{h}{c_p\rho u}$	$St = \frac{Nu}{RePr}$	Stanton Number	$\frac{\text{Wall heat transfer rate}}{\text{Heat transfer by convection}}$

EXTERNAL FLOW

NOTE : Properties are to be evaluated (unless otherwise stated) at film temperature $T_f = (T_w + T_\infty)/2$.

1. Flat Plate

Flow conditions	*Correlation and Validity*
1.0 LAMINAR FLOW ($Re_x < 5 \times 10^5$)	$\delta_{hx} = 5\, x\, Re_x^{-0.5}$
Boundary Layer Thicknesses :	$\delta_{Tx} = \delta_{hx}\, Pr^{-0.333}$ $\delta_x = \delta_{hx}/3$ $\delta_{ix} = \delta_{hx}/7$
Friction Factor :	$C_{fx} = 0.664\, Re_x^{-0.5}$ $\overline{C_{fL}} = 1.328\, Re_L^{-0.5}$
1.1 Constant Wall Temperature	$Nu_x = 0.332\, Re_x^{0.5}\, Pr^{0.333}$ $0.6 < Pr < 50$
1.1.1 If heating starts from a distance x_o from leading edge	$Nu_x = 0.332\, Re_x^{0.5}\, Pr^{0.333} \cdot [1 - (x_o/x)^{0.75}]^{-0.333}$
1.1.2 For liquid metals (low Prandtl numbers) and for silicones (High Prandtl numbers)	$Nu_x = \dfrac{[0.3387\, Re_x^{0.5}\, Pr^{0.333}]}{[1 + (0.0468/Pr)^{0.67}]^{0.25}}$ $Pr < 0.05$, $Re_x\, Pr > 100$, also for $Pr > 50$
1.1.3 For Liquid Metals only	$Nu_x = 0.565\, [Re_x \cdot Pr]^{0.5}$ $Pr \le 0.05$
1.2 Constant heat flux	$Nu_x = 0.453\, Re_x^{0.5}\, Pr^{0.333}$, $0.6 < Pr < 50$ $\overline{T_w - T_\infty} = \dfrac{(qL/k)}{[0.6795\, Re_L^{0.5}\, Pr^{0.333}]}$

Notations

- T_f = Film temperature $= (T_w + T_\infty)/2$
- T_∞ = Free stream fluid temperature
- T_w = Plate surface temperature
- Re_x = Reynolds number at a distance x from leading edge
- Re_L = Reynolds number at location L
- δ_{hx} = Hydrodynamic boundary layer thickness at a distance x from leading edge
- δ_{Tx} = Thermal boundary layer thickness at a distance x from leading edge
- δ_x = Displacement thickness at x
- δ_{ix} = Momentum thickness at x
- C_{fx} = Local friction coefficient defined by $\tau_{wx}/(\rho u_\infty^2/2)$ (Fanning friction factor)
- τ_{wx} = wall shear stress at x, N/m^2
- $\overline{C_{fL}}$ = Average friction coefficient upto the distance L from leading edge
- Pr = Prandtl number
- x_o = Distance from leading edge at which heating starts
- ρ = density
- u_∞ = free stream velocity
- q = heat flux W/m^2
- k = Thermal conductivity of fluid
- $\overline{T_w - T_\infty}$ — Average temperature difference between plate and fluid.

Flow conditions	*Correlation and Validity*	*Notations*
1.5.1 Laminar-Turbulent (Laminar length considered)	$C_{fL} = 0.074\ Re_L^{-0.2} - 1742\ Re_L^{-1.0}$ (Critical Reynolds Number $= 5 \times 10^5$) OR $C_{fL} = \dfrac{0.455}{(\log_{10} Re_L)^{2.584}} - \dfrac{A}{Re_L}$ where *Critical Reynolds Number* — *Value of A* 3×10^5 — 1050 5×10^5 — 1700 1×10^6 — 3300 3×10^6 — 8700	C_{fL} = Average friction coefficient upto length L.
1.5.2 Laminar-turbulent constant wall temperature	$\overline{Nu}_L = Pr^{0.333}[0.037\ Re_L^{0.8} - 871]$ Critical Reynolds Number $= 5 \times 10^5$ $Re_L \le 10^8,\ 0.6 < Pr < 60$ *OR* generally $\overline{Nu}_L = Pr^{0.333}[0.037\ Re_L^{0.8} - A]$ $A = 0.037\ Re_{cr}^{0.8} - 0.664\ Re_{cr}^{0.5}$	Re_{cr} = Critical Reynolds Number $\overline{Nu}_L$ — Average Nusselt Number upto length L
1.5.3 By Analogy	$St_x \cdot Pr^{2/3} = \dfrac{C_{fx}}{2}$ Properties to be evaluated at T_∞	T_∞ — Free stream temperature
1.6 High speed flow, constant wall temperature	The heat transfer equation to be used is : $q = hA\,[T_w - T_{ad}]$ and h is calculated as in low speed flow, using the properties at a temperature T defined by $T = T_\infty + 0.5(T_w - T_\infty) + 0.22\,(T_{ad} - T_\infty)$ where T_{ad} is calculated using the recovery factor R $R = \dfrac{T_{ad} - T_\infty}{T_o - T_\infty}$ where $T_o = T_\infty \left[1 + \left(\dfrac{\gamma - 1}{2}\right) M_\infty^2\right]$	γ = ratio of specific heats R = to be specified < 1 M_∞ = free stream Mach Number

2. FLOW OVER CYLINDERS

Flow condition	*Correlation and Validity*	*Notation*
2.1.1 Across cylinders Generalised equation	@ $Nu_D = C.Re_D^m . Pr^{0.333}$ (for C, m refer below) Properties at $T_f = (T_\infty + T_w)/2$	Nu_D = Nusselt Number based on diameter Re_D = Reynolds Number based on diameter D = Diameter m = Coefficient C = Constant

Re_D	C	m
0.4 – 4.0	0.989	0.330
4.0 – 40.0	0.911	0.385
40.0 – 4000	0.683	0.466
4000.0 – 40,000	0.193	0.618
40,000.0 – 400,000	0.0266	0.805

2.1.2 Flow over non circular shapes	$Nu = 1.1\ C_1\ Re_D^n\ Pr^{0.33}$, $5 \times 10^3 < Re_D < 10^5$ Refer page 118 for C_1 and n	@ Applicable for mass transfer also

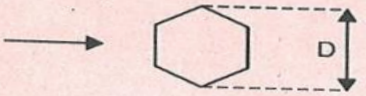
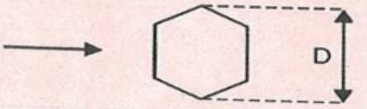
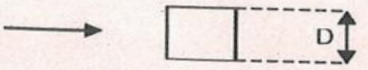
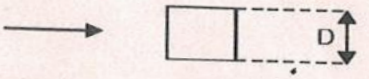
FLOW OVER CYLINDERS (*Contd.*)

Flow condition	*Correlation and Validity*	*Notation*
2.1.3 ACROSS CYLINDERS For liquids	$Nu_D = [0.35 + 0.56 \,.\, Re_D^{0.52}]\, Pr^{0.333}$ $10^{-1} < Re_D < 10^5$, Properties at T_f	
For liquids and gases	$Nu = [0.43 + 0.50\, Re^{0.5}]\, Pr^{0.38} \left[\frac{Pr_f}{Pr_w}\right]^{0.25}$ $1 < Re < 10^3$	
2.1.4 When property variation is large due to temperature variation	$Nu = 0.25\, Re^{0.6}\, Pr^{0.38} \left(\frac{Pr_f}{Pr_w}\right)^{0.25}$ $10^3 < Re < 2 \times 10^5$ gases – properties at T_f (film temp.) liquids – properties at free stream temperature T_∞ $Nu = [0.4\, Re_D^{0.5} + 0.06\, Re_D^{0.67}] \times Pr^{0.4} \left[\frac{\mu_\infty}{\mu_w}\right]^{0.25}$ $10 < Re < 10^5$; $0.67 < Pr < 300$ $0.25 < \left(\frac{\mu_\infty}{\mu_w}\right) < 5.3$, properties for Re, Pr at T_∞	Pr_f = Prandtl Number at film temperature Pr_w = Prandtl Number at wall temperature μ_∞ = Dynamic viscosity at free stream temperature μ_w = Dynamic viscosity at wall temperature
2.1.5 Generalised form	$Nu = C.Re^m Pr^n \,.\, \left(\frac{Pr_\infty}{Pr_w}\right)^{0.25}$ $0.7 < Pr < 500$ $1 < Re < 10^6$ Properties at T_∞ $n = 0.37$ for $Pr < 10$ $n = 0.36$ for $Pr > 10$	C, m tables (not suitable for liquid metal)

Re	*C*	*m*
1 – 40	0.75	0.4
40 – 1000	0.51	0.5
$10^3 - 2 \times 10^5$	0.26	0.6
$2 \times 10^5 - 10^6$	0.076	0.7

FLOW OVER NON CIRCULAR SECTIONS

CH-6

Flow direction and profile	Re_D		n	C_1
	From	*To*		
	5,000	100,000	0.588	0.222
	2,500	7,500	0.624	0.261
	2,500	15,000	0.612	0.224
	3,000	15,000	0.804	0.085
	5,000	100,000	0.638	0.138
	5,000	19,500	0.638	0.144
	19,500	100,000	0.782	0.035
	5,000	100,000	0.675	0.092
	2,500	8,000	0.699	0.160
	4,000	15,000	0.731	0.205

3. FLOW OVER SPHERES

Flow condition	*Correlation and Validity*	*Notation*
FLOW OVER/ACROSS SPHERES 3.1 For various ranges of Reynolds Numbers For Gases	$Nu = 0.37 \cdot Re^{0.6}$; $17 < Re < 70{,}000$ Properties at T_f $Nu = 2 + (0.25\,Re + 3 \times 10^{-4}\,Re^{1.6})^{0.5}$ $100 < Re < 3 \times 10^5$, $Pr \approx 0.71$	
For Air	$Nu = 430 + 5 \times 10^{-3}\,Re + 0.025 \times 10^{-9}\,Re^2 - 3.1 \times 10^{-17}\,Re^3$ $3 \times 10^5 < Re < 5 \times 10^6$; $Pr \simeq 0.71$	
For Liquids	$Nu\,(Pr)^{-0.3} = 0.97 + 0.68\,Re^{0.5}$; $1 < Re \cdot < 2000$ Properties at T_f	all Re based on diameter
3.2 Large Property variation Oils and Water	$Nu \cdot Pr^{-0.3} \left(\frac{\mu_w}{\mu_\infty}\right)^{0.25} = 1.2 + 0.53 \cdot Re^{0.54}$ $1 < Re < 200{,}000$ Properties at T_∞	
3.2 Large Property Variations Gases and Liquids	$Nu = 2 + (0.4\,Re^{0.5} + 0.06\,Re^{0.67}) \times Pr^{0.4} \left(\frac{\mu_\infty}{\mu_w}\right)^{0.25}$, $3.5 < Re < 8 \times 10^4$; $0.7 < Pr < 380$, Properties at T_∞ $1.0 < \frac{\mu_\infty}{\mu_w} < 3.2$	
3.3 Falling Liquid Drops	$Nu = 2 + 0.6\,Re^{0.5}\,Pr^{0.333}\,[25(x/D)^{-0.7}]$ Properties at T_∞	x — falling distance, measured from rest D — Diameter of droplet.
3.4 Liquid Metal	$Nu = 2 + 0.386\,(Re \cdot Pr)^{0.5}$ $3.56 \times 10^4 < Re < 1.525 \times 10^5$	

4. ACROSS TUBE BANKS

3

Flow condition	*Correlation and Validity*	*Notation*
4.1 Number of rows of tubes 10 or more	$Nu = C\,Re^n$ Re to be calculated on the basis of max. fluid velocity V_{max} $N \geq 10$; $2000 < Re < 40000$; Properties at T_f n, C from table page 122	V_{max} = calculated from free stream velocity and the actual flow area allowing for tube obstruction S_t = Pitch transverse to flow S_l = Pitch along the flow N —Number of tubes u_∞ —free stream velocity just before entry
4.2 For less than 10 rows	Multiply the above Nu by C_1 C_1 – see tables page 122 Check : $(S_t - D) < \left\{2\sqrt{\left(\frac{S_t}{2}\right)^2 + S_l^2} - 2D\right\}$ In line : $V_{max} = [S_t/(S_t - D)] \cdot u_\infty$ Staggered : maximum of the above and $V_{max} = \frac{S_l}{2(S_D - D)} u_\infty$ where, $S_D = \left[S_l^2 + \left(\frac{S_t}{2}\right)^2\right]^{0.5}$	$Nu = C \cdot Re^m \cdot Pr^{\frac{1}{3}}$ هر دو برای تعلیق کامل تر بود
4.3 Across Tube Banks with 20 or more rows Valid from 4 rows for air	$Nu = C\,Re^m\,Pr^{0.36}\left[\frac{Pr_\infty}{Pr_w}\right]^{0.25}$ $N \geq 20$: $0.7 < Pr < 500$; $1000 < Re < 2 \times 10^6$ Properties at T_∞ ; Re based on V_{max}	Pr_∞ = Prandtl at free stream temperature Pr_w = Prandtl at wall temperature. (زیاد در شرایط کوئتر) $\dot{m}\, s\, \rho\, V_\infty\, S\, n\, \eta\, L$ local

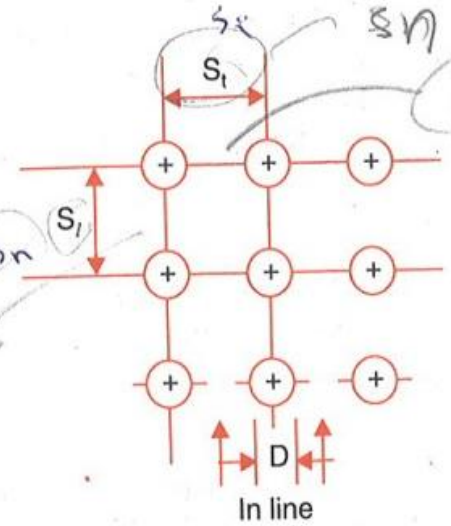
Condition	*Re range*	*C*	*m*
In line	$10^3 < Re < 2 \times 10^5$	0.27	0.63
In line	$2 \times 10^5 < Re < 2 \times 10^6$	0.021	0.84
Staggered			
$S_t/S_l < 2$	$10^3 < Re < 2 \times 10^5$	$0.35\left(\frac{S_t}{S_l}\right)^{0.2}$	0.6
$S_t/S_l > 2$	$10^3 < Re < 2 \times 10^5$	0.4	0.6
	$2 \times 10^5 < Re < 10^6$	0.022	0.84

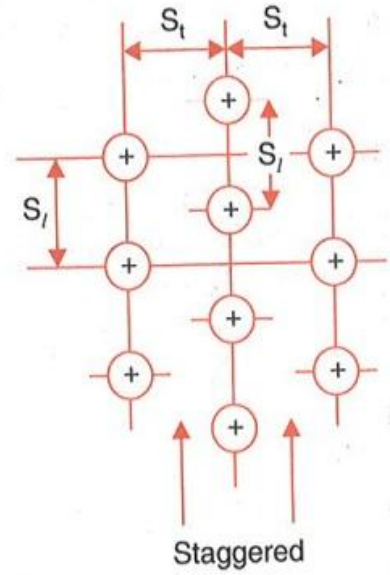
Flow condition	*Correlation and Validity*	*Notation*
4.3.1 Liquid Metals	$Nu_D = 4.03 + 0.228\,(Pe)^{0.67}$ $20{,}000 < Re < 80{,}000$	$Pe = Re\,Pr$
4.4 Pressure drop and friction factor	$\Delta P = \dfrac{f\,G^2_{max}\,N}{2.09\,\rho g_o}\left[\dfrac{\mu_w}{\mu_b}\right]^{0.14}$ For in line $f = \left[0.044 + \dfrac{0.08\left(\dfrac{S_t}{d}\right)}{\left(\dfrac{S_l - d}{d}\right)^{0.43+1.13\,(d/St)}}\right] Re_{max}^{-0.1}$ For staggered $f = \left[0.25 + \dfrac{0.118}{\left(\dfrac{S_l - d}{d}\right)^{1.08}}\right] Re_{max}^{-0.16}$	G_{max} = mass velocity at minimum flow area, kg/m^2 s ρ = density at t_∞, kg/m^3 N = Number of transverse rows ΔP = Pressure drop in Pascal μ_∞ = absolute viscosity at bulk mean temp. μ_w = absolute viscosity at wall temp. d = Tube diameter

FLOW ACROSS BANKS OF TUBES

Note : $Nu = C\,Re^n$

The values of C given in table below are for air. For other fluids multiply these tabulated values of C only, by $1.13\,Pr^{0.33}$





FOR TUBE BANKS OF 10 ROWS OR MORE

Arrangement	$\frac{S_t}{D}$	S_l/D = 1.25 C	1.25 n	1.5 C	1.5 n	2.0 C	2.0 n	3.0 C	3.0 n
In Line	1.25	.348	.592	.275	.608	.100	.704	.0633	.752
	1.50	.367	.586	.250	.620	.101	.702	.0678	.744
	2.00	.418	.570	.299	.602	.229	.632	.1980	.648
	3.00	.290	.601	.357	.584	.374	.581	.2860	.608
Staggered	0.6	—	—	—	—	—	—	.213	.636
	0.9	—	—	—	—	.446	.571	.401	.581
	1.0	—	—	.497	.558	—	—	—	—
	1.125	—	—	—	—	.478	.565	.518	.560
	1.25	.518	.556	.505	.554	.519	.556	.522	.562
	1.5	.451	.568	.460	.562	.452	.568	.488	.568
	2.0	.404	.572	.416	.568	.482	.556	.449	.570
	3.0	.310	.592	.356	.580	.440	.562	.421	.574

C_1, Ratio of values of h for N rows deep to that for 10 rows deep $\left[\frac{h_N}{h_{10}}\right]$

N	1	2	3	4	5	6	7	8	9	10
Staggered tubes	.68	.75	.83	.89	.92	.95	.97	.98	.99	1.0
In-line tubes	.64	.80	.87	.90	.92	.94	.96	.98	.99	1.0

INTERNAL FLOW

Note : Properties to be evaluated at BULK MEAN temperature

$T_m = (T_{mi} + T_{mo})/2$ unless otherwise stated.

1.0 TUBES : LAMINAR

Flow Condition	*Correlation and Validity*
1.1 Tubes, $Re_D < 2300$	$f = \dfrac{64}{Re_D}$, smooth or rough tubes Hydrodynamic entry length $x \simeq 0.04\ D\ Re_D$ Thermal entry length $x \simeq 0.04\ D\ Re_D\ .\ Pr$
1.2 Entry Region Hydrodynamic layer fully developed. Thermal layer developing	$Nu = 3.66 + \dfrac{0.0668\,(D/L)\,Re_D\,Pr}{1 + 0.04\,[D/L)\,Re_D\,Pr]^{0.67}}$ $Pr > 0.7$. Smooth pipe. Constant wall temp. Also refer chart on page 129
1.2.1 For short lengths for small values of $\dfrac{x}{D}$ constant wall temp.	For $\left(\dfrac{x}{D}\right)/Re_D\,Pr < 0.01$ $Nu = 1.67[Re_D\,Pr/(x/D]^{0.333}$
1.2.2 Fully developed Thermal layer	$Nu = 3.66$, $L >> D$ constant wall temp. refer chart on page 114
1.2.3 Simultaneous development of Hydrodynamic and Thermal layers :	$Nu = 3.66 + \dfrac{0.104\,(Re_D\,Pr\,.\,D/x)}{1 + 0.16\,(Re_D\,Pr\,.\,D/x)^{0.8}}$ $Pr > 0.6$, constant wall temperature
1.2.4 As above for liquids	$Nu = 1.86\left[\dfrac{Re_D\,Pr}{x/D}\right]^{0.333} \times \left(\dfrac{\mu}{\mu_w}\right)^{0.14}$, $RePr\,\dfrac{D}{x} > 10$, $Pr > 0.6$, constant wall temperature

Notation

T_m — Bulk mean temperature $(T_{mi} + T_{mo})/2$

T_{mi} — mean temperature at inlet

T_{m0} — mean temperature at outlet

$f = \dfrac{\Delta P_f}{\rho\,.\,(L/D)\,.\,(u_m^2/2)}$; $C_f = f/4$

ΔP_f — pressure drop due to friction

ρ — density

L — length

D — diameter

u_∞ — free stream velocity

f — Darcy friction factor

x — length

u_m — mean velocity in tube

Re_D — Reynolds Number based on diameter

μ — dynamic viscosity of fluid at bulk mean temperature

μ_w — dynamic viscosity of fluid at wall temperature

$Re_D = \dfrac{4m}{\pi D \mu}$

m — mass flow rate, kg/s

C_f — coefficient of friction

Flow Condition	*Correlation and Validity*	*Notation*
1.2.5 For non circular tubes, fully devloped flow	Refer page 127 for values of nusselt numbers	
1.2.6 Short Tubes Thermal developing, hydrodynamic fully developed	$Nu = 1.30 \left[\frac{Re_D\ Pr}{x/D}\right]^{0.333}$ $Re\ Pr\ \frac{D}{x} > 10$, constant heat flux $Pr > 0.6$. Also see chart on page 129	
1.2.7 Fully developed : constant heat flux	$Nu = 4.36$, $Pr > 0.6$	
1.2.8 Colburn analogy	$St\ Pr^{0.67} = f/8$	

$D_H = \frac{4 \times \frac{\pi}{4}(d_1 - d_1)}{4\pi\left(\frac{d_1 + d_1}{2}\right)}$

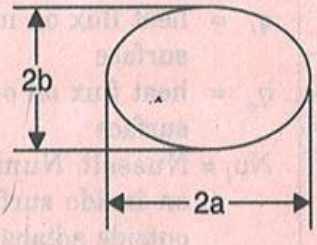
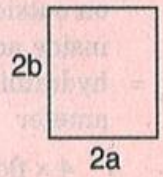
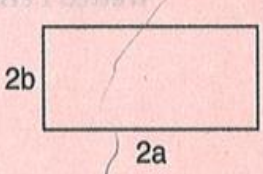
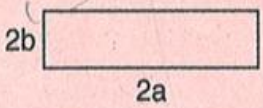
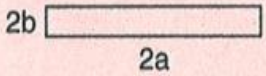
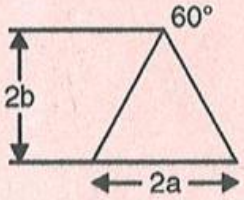
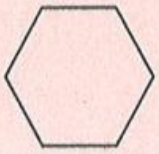
2.0 TUBES : TURBULENT

Flow Condition	*Correlation and Validity*	*Notation*
$Re_D > 2300$ 2.1 Friction factors : Smooth tubes	$f = 0.25[1.82 \cdot \log_{10} Re_D - 1.64]^{-2}$ or $f = 0.184\ Re_D^{-0.2} : Re_D > 10^4$	ε — surface roughness f — friction factor, also refer chart on page 131
2.1.1 Rough tubes	$f = \frac{1.325}{\left[\ln\left(\frac{\varepsilon}{3.7D} + 5.74/Re^{0.9}\right)\right]^2}$ $10^{-6} \le \frac{\varepsilon}{D} < 10^{-2}$; $5000 < Re < 10^8$	
2.1.2 for transitional turbulent flow	$f = 0.316 \cdot Re_D^{-0.25}$	
2.2.1 Entry length :	$10 \le \frac{x}{D} < 60$	

Flow Condition	*Correlation and Validity*	*Notation*
2.2.2 Entrance region	$Nu = 0.036\ Re_D^{0.8}\ Pr^{0.33} \times (D/L)^{0.055}$ $10 < \frac{L}{D} < 400$ See also figure on page 130	
2.2.3 Short Pipe :	$\overline{Nu} = Nu\left(1 + \frac{C}{x/D}\right)$; $\frac{x}{D} \geq 10$ C = 1.4 for hydrodynamic fully developed C = 6.0 for hydrodynamic not developed $\overline{Nu} = Nu\ [1 + (D/x)^{0.7}]$; $2 < \frac{x}{D} < 20$	Nu — evaluated at fully developed condition $\overline{Nu}$ — average Nusselt number for the short tube
2.3.1 Fully developed flow Dittus—Boelter eq.	$Nu = 0.023\ Re_D^{0.8} . Pr^n$ $n = 0.4$ for heating of fluids $n = 0.3$ for cooling of fluids $0.6 < Pr < 100,\ 2500 < Re < 1.25 \times 10^6$; $\frac{L}{D} > 60$ Generally used equation, independent of thermal boundary. Properties at bulk mean temp.	
2.3.2 Smooth tubes : Fully developed Large property variations. Sieder—Tate eq.	$Nu = 0.027\ Re_D^{0.8}\ Pr^{0.333} \left(\frac{\mu_m}{\mu_w}\right)^{0.14}$ $0.7 < Pr < 16700$; $Re_D \geq 10{,}000$; $\frac{L}{D} \geq 60$	μ_m — dynamic viscosity at T_m
2.3.3 Fully developed turbulent $1 < \frac{\mu_m}{\mu_w} < 40$	$Nu = \frac{(f/8)Re_D\ Pr}{1.07 + 12.7(f/8)^{0.5}\ [Pr^{0.67} - 1]} \times \left(\frac{\mu_m}{\mu_w}\right)^n$ $n = 0.11$ for heating of fluids constant wall temp. $n = 0.25$ for cooling of fluids constant wall temp. $n = 0$ for constant heat flux or gases Rough/smooth tubes properties at film temp. $10^4 < Re < 5 \times 10^6$ $0.5 < Pr < 200$; 6 per cent accuracy. $200 < Pr < 2000$; 10 per cent accuracy. Replace $\frac{\mu_m}{\mu_w}$ by $\frac{T_w}{T_m}$ for gases.	μ_w — dynamic viscosity at wall temperature T_w T_w — wall temperature f — calculated by equation given earlier in 2.1 or from chart on page 131

Flow Condition	*Correlation and Validity*	*Notation*
2.3.4 Rough Tubes : By Colburn analogy	$St_b \cdot Pr_m^{0.67} = \frac{f}{8}$	St_b — Stanton Number at bulk temperature Pr_m — Prandtl Number at T_m
2.4.1 Liquid Metals : Constant wall temperature	$Nu = 5 + 0.025\,[Re_D\,Pr]^{0.8}$ $Re_D\,Pr > 100 : \frac{L}{D} > 60$	
2.4.2 Constant Heat Flux	$Nu = 4.82 + 0.0185\,(Re_D\,Pr)^{0.827}$ $3.6 \times 10^3 < Re_D < 9.05 \times 10^5$ $10^2 < Re_D\,Pr < 10^4$	
2.4.3 Smooth Tubes, fully developed As above but simpler	$Nu = 0.625\,[Re_D\,Pr]^{0.4}$ $10^2 < Re_D\,Pr < 10^4 : \frac{L}{D} > 60$ Constant heat flux	
2.4.4 For Thermal entry region.	$Nu = 3.0\,Re_D^{0.0833}$, $Re_D\,Pr < 100$	
2.5 Non-Circular Sections	The correlation listed above to be used with $D_h = \frac{4A}{P}$ where D_h is known as hydraulic diameter.	A — Flow area P — Wetted perimeter

NUSSELT NUMBER FOR FULLY DEVELOPED INTERNAL FLOW, LAMINAR

Geometry ($L/D_h > 100$)		Nu_1 *q = constant heet flux*	Nu_2 T_w *= const.*
		4.364	3.657
	$\frac{2b}{2a} = 0.9$	5.331	4.439
	$\frac{2b}{2a} = 1$	3.608	2.976
	$\frac{2b}{2a} = \frac{1}{2}$	4.123	3.391
	$\frac{2b}{2a} = \frac{1}{4}$	5.099	3.66
	$\frac{2b}{2a} = \frac{1}{8}$	6.490	5.597
	$\frac{2b}{2a} = \frac{\sqrt{3}}{2}$	3.111	2.47
		4.002	3.34

Flow Condition	*Correlation and Validity*	*Notation*
2.6 Concentric tube annulus	$D_h = D_o - D_i$ $Nu_i = \frac{h_i D_h}{k}$; $Nu_o = \frac{h_o D_h}{k}$	D_o = outside tube diameter D_i = Inside tube diameter h_i = convective heat transfer coefficient on inside surface h_o = convective heat transfer coefficient on outside surface q_i = heat flux on inner surface q_o = heat flux on outer surface Nu_i = Nusselt Number on inside surface, outside adiabatic Nu_o = Nusselt Number on outside surface, inside adiabatic D_h = hydraulic mean diameter $= \frac{4 \times \text{flow area}}{\text{Wetted Perimeter}}$
2.6.1 Fully developed Laminar Constant wall temp.	Values are tabulated below :	

D_i/D_o	0	0.05	0.10	0.25	0.50	1.0
Nu_i	—	17.46	11.56	7.37	5.74	—
Nu_o	3.66	4.06	4.11	4.23	4.43	4.86

2.6.2 Constant heat flux

$$Nu_i = \frac{A_i}{1-(q_o/q_i)B_i} \; ; \; Nu_o = \frac{A_o}{1-(q_i/q_o)B_o}$$

Values are tabulated below :

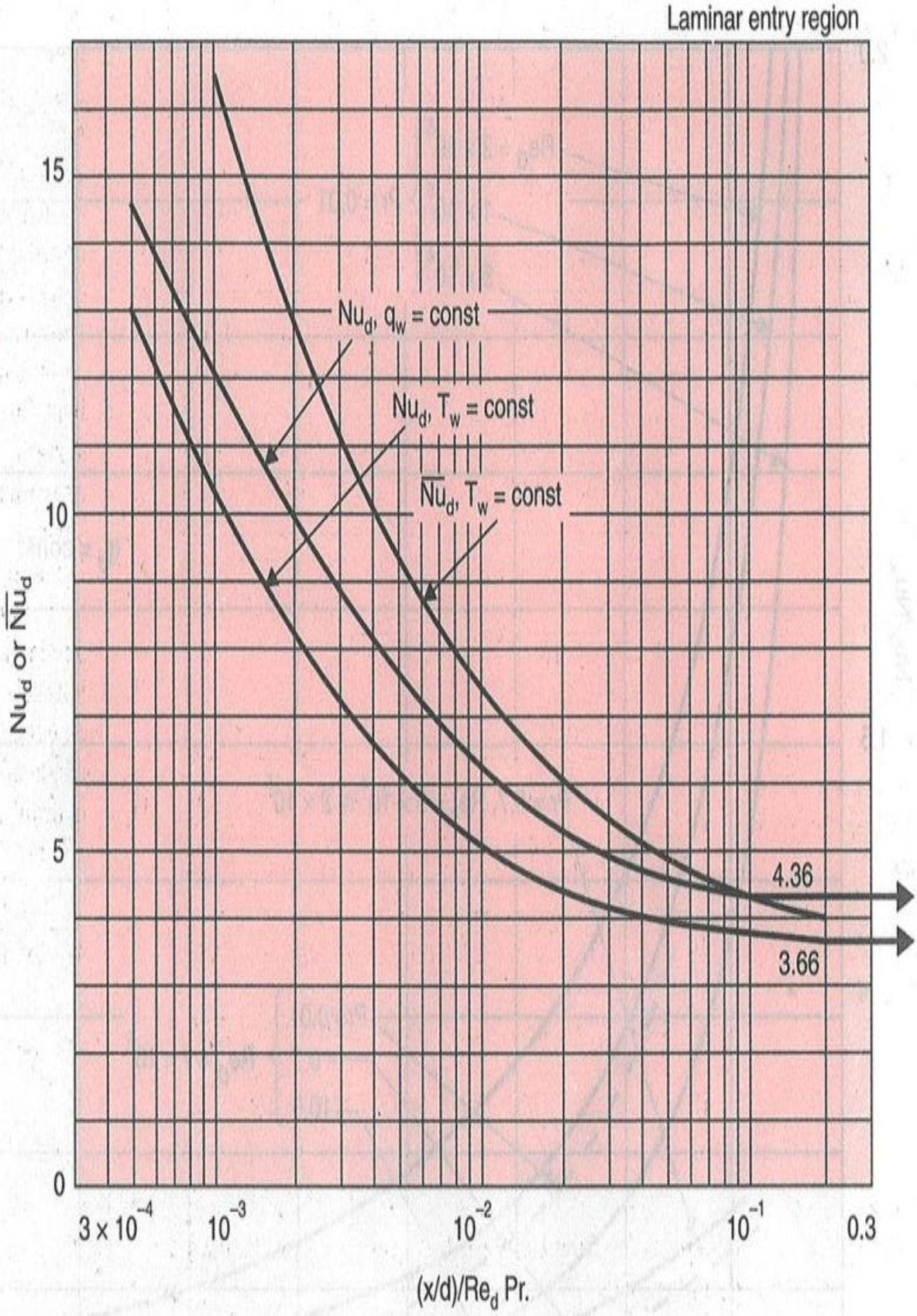
Flux can be negative or positive depending on the flow.

D_i/D_o	0	0.05	0.10	0.20	0.40	0.60	0.80	1.0
A_i	—	17.81	11.91	8.50	6.58	5.91	5.58	5.39
B_i	∞	2.18	1.38	0.91	0.60	0.47	0.40	0.35
A_o	4.36	4.79	4.83	4.83	4.98	5.10	5.24	5.39
B_o	0	0.029	0.056	0.104	0.182	0.246	0.299	0.346

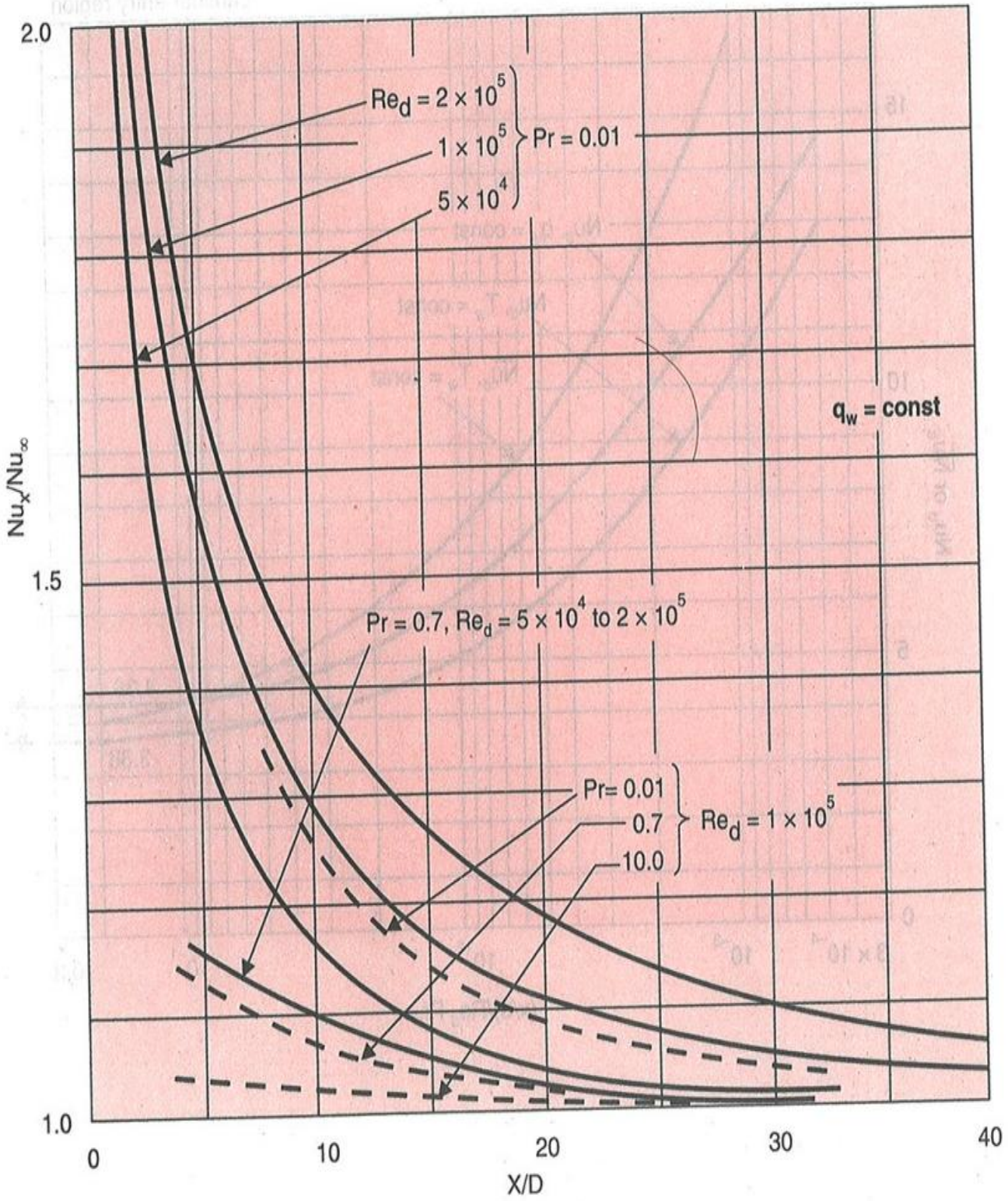
2.6.3 Turbulent

Same as for **flow inside tubes** except D_h is to be used in place of 'D'

LAMINAR ENTRY REGION NUSSELT NUMBERS

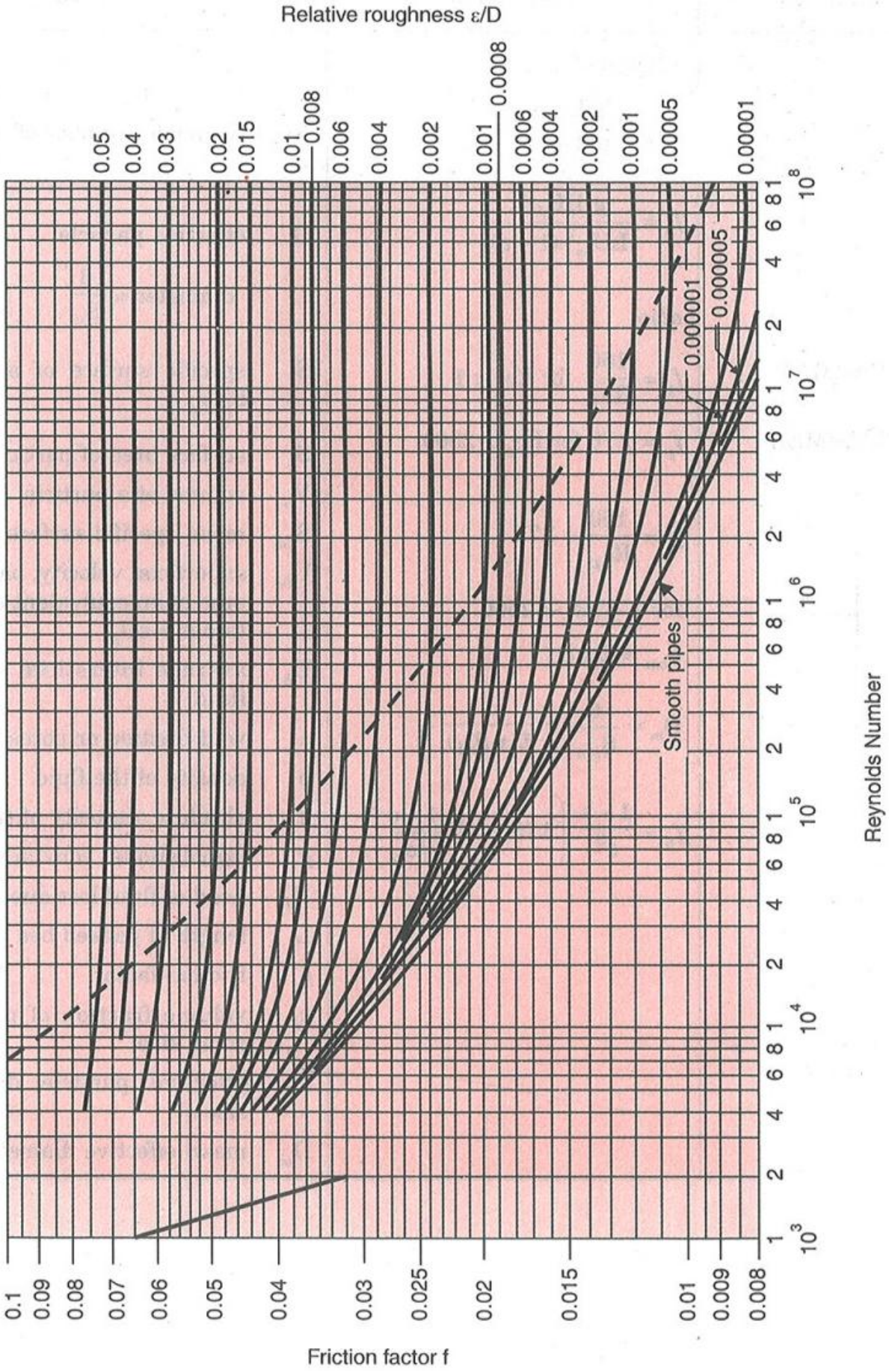


TURBULENT FLOW ENTRY REGION NUSSELT NUMBERS



Nu_x — local Nusselt Number
Nu_∞ — Nusselt Number at fully developed region

FRICTION FACTOR (See p. 124)



PACKED BEDS

Author	*Correlation*	*Notation*
	LIQUIDS :	
ERGUN	$Re_p = \dfrac{DU_{bs}\rho}{\mu(1-\varepsilon)}$	Re_p Reynolds Number of packed bed
ERGUN	$f_p = \dfrac{g\,DH_f\varepsilon^3}{LU_{bs}^{\,2}(1-\varepsilon)}$	D effective particle diameter $= \dfrac{6}{S_v}$
	also	
KOZENY-CARMAN	$f_p = \dfrac{150}{Re_p}$ for $Re_p < 1$	S_v specific surface of a particle = S_p/V_p
BURKE-PLUMMER	$f_p = 1.75$ for $Re_p > 2500$	S_p surface area of particle
		V_p volume of a particle
ERGUN	$f_p = \dfrac{150}{Re_p} + 1.75$	S_{vm} mean specific surface
	for $1 < Re_p < 2500$	U_{bs} superficial velocity, based on the area of an equivalent empty container = εU_b
	$S_{vm} = \Sigma\, x_i S_{vi}$	U_b average interstitial velocity of fluid
	$D_m = \dfrac{6}{S_{vm}} = \dfrac{1}{\Sigma(x_i/D_i)}$	ε void fraction or porosity
		ρ density of the fluid
BEEK	$f_p = \dfrac{1-\varepsilon}{\varepsilon^3}\left(1.75 + 150\dfrac{1-\varepsilon}{Re_p}\right)$	μ absolute viscosity of the fluid
		g gravitational constant
		H_f head of fluid lost due to friction
		L length of packed bed
		f_p friction factor
		x_i volume fraction of particles of same size
		D_i effective particle diameter of size i
		D_m mean effective diameter

PACKED BEDS (*Contd.*)

Author	*Correlation*	*Notation*
	GASES : Pressure drop, $\Delta P = \frac{2 f_p L G^2}{D \rho_{av}}$ for $\frac{\Delta p}{p} < 0.1$	G mass velocity of the gas per unit area, kg/m^2 ρ_{av} density of gas at the arithmetic mean pressure p pressure of gas at entry
ECKERT	HEAT TRANSFER : $Nu_p = \frac{h D_p}{k} = 0.8\ Re_p^{0.7}\ Pr^{0.333}$	St Stanton number h heat transfer coeff. Nu_p Nusselt Number for packed bed D_p effective particle diameter k thermal conductivity of fluid j_d COLBURN j factor $= \frac{h_D}{u_\infty} Sc^{0.667}$ h_D convective mass transfer coefficient, m/s Sc Schmidt number
WHITAKER	$\frac{h D_p}{k} = \frac{1-\varepsilon}{\varepsilon}[0.5\ Re_p^{0.5} + 0.2\ Re_p^{0.67}]\ Pr^{1/3}$	
BEEK	From wall to gas, cylinder like filling $\frac{h D_p}{k} = 2.58\ Re_p^{0.33}\ Pr^{0.33} + 0.094\ Re_p^{0.8}\ Pr^{0.4}$ For sphere like filling $\frac{h D_p}{k} = 0.203\ Re_p^{0.33}\ Pr^{0.33} + 0.22\ Re_p^{0.8}\ Pr^{0.4}$ $40 < Re_p < 2000$	
UPADHYAY	$St = \frac{1}{\varepsilon} 1.075\ Re_p^{-0.826}$ $0.01 < Re_p < 10$ $St = \frac{1}{\varepsilon} 0.455\ Re_p^{-0.4}$ $10 < Re_p < 200$	
	MASS TRANSFER : $j_d = 1.82\ Re_p^{-0.51}$ for $Re_p < 350$ $= 0.989\ Re_p^{-0.41}$ for $Re_p > 350$	

Natural

FREE CONVECTION

Note : Properties are to be evaluated at $T_f = (T_w + T_\infty)/2$ unless otherwise mentioned.

Description	*Correlation and Validity*	*Notations*
1.1 Vertical Surface : Plate or cylinder with $D \geq \frac{35}{Gr_x^{0.25}}$. Laminar : $Gr \,.\, Pr \,. < 10^9$	$\delta_x = 3.93\, Pr^{-0.5}\,(0.952 + Pr)^{0.25}\,.\,Gr_x^{-0.25}$ $h_x = \frac{2k}{\delta_x}$; $Nu_x = 2\,\frac{x}{\delta_x}$ constant wall temperature $Nu_x = 0.508\, Pr^{0.5}\,(0.952 + Pr)^{-0.25}\,.\,Gr_x^{0.25}$ for constant heat flux $Nu_x = 0.6\,(Gr_x Nu_x\, Pr)^{0.2}$ for $10^5 < Gr_x\, Nu_x < 10^{11}$ $Nu_x = 0.6\,(Gr^*\, Pr)^{0.2}$ $Nu_x = C(Gr_x)^{0.25}$ where C is a function of Prandtl number as tabulated below : Both constant wall temperature and constant heat flux	T_f —film temperature T_w —wall temperature T_∞ —free stream fluid temp. δ_x —boundary layer thickness at x from leading edge $Gr_x = \frac{g\,.\,\beta\,.\,x^3\,\Delta T}{v^2}$ Nu_x —local Nusselt Number $\overline{Nu}$ —average Nusselt Number upto length L Nu_L —Nusselt Number at L from leading edge k —Thermal conductivity of fluid v —kinematic viscosity of fluid $Gr^* = \frac{g\beta q\, x^4}{k v^2}$ q —heat flux, W/m^2
Average Nusselt Number upto L	$\overline{Nu} = \frac{4}{3}\, Nu_L$	

Pr	0.01	0.72	1.0	2.0	10	100	1000
C	0.057	0.357	0.401	0.506	0.827	1.549	2.804

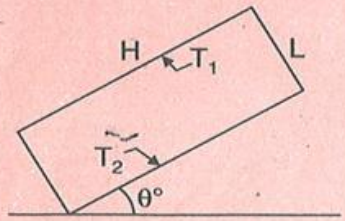
*For inclined plates replace Gr_x by $Gr_x \cos\theta$, where θ is angle with vertical.

Description	*Correlation and Validity*	*Notation*
1.2 For Low Values of Gr Pr < 10^4	$\overline{Nu} = 0.68 + \dfrac{0.67\,(GrPr)^{0.25}}{\left\{1+\left[\dfrac{0.492}{Pr}\right]^{0.5625}\right\}^{0.444}}$ Constant wall temperature For constant heat flux, use 0.437 in place of 0.492	θ, angle with vertical
Higher values of Gr Pr Constant heat flux/ constant wall temperature	$\overline{Nu} = 0.59\,(GrPr)^{0.25}$ $10^4 < GrPr < 10^9$	
All values of Gr Pr	$Nu = \left[0.825 + \dfrac{0.387\,(Gr\,Pr)^{0.167}}{\left\{1+\left[\dfrac{0.492}{Pr}\right]^{0.5625}\right\}^{0.296}}\right]^2$ for Constant wall temperature For constant heat flux, use 0.437 in place of 0.492	
Inclined plates upto 60° with vertical	Multiply Gr by cos θ	
2.1 **TURBULENT** **GrPr > 10^9**	$Nu = 0.10\,(GrPr)^{0.333}$ (more popularly used) OR $Nu = 0.021\,(GrPr)^{0.4}$	
Both constant heat flux and constant wall temperature	$10^9 > GrPr < 10^{13}$ $Nu_x = 0.17\,(Gr_x Nu_x Pr)^{0.25}$ for $2 \times 10^{13} < Gr_x Nu_x Pr < 10^{16}$ Also $Nu_x = 0.17\,(Gr^* Pr)^{0.25}$ $\overline{Nu} = \dfrac{5}{4}\,Nu_L$	$\overline{Nu}$ — Average Nu upto L $Gr^* = \dfrac{g\beta q x^4}{k\nu^2}$
2.1.1 Horizontal plate : upper surface heated or lower surface cooled constant wall temperature	Gr to be calculated with L = Area/Perimeter $Nu = 0.54\,(GrPr)^{0.25}$; $2 \times 10^4 < GrPr < 8 \times 10^6$ $Nu = 0.15\,(GrPr)^{0.333}$; $8 \times 10^6 < GrPr < 10^{11}$	q — heat flux, W/m^2

Description	*Correlation and Validity*	*Notation*
2.1.2 Upper surface cooled or lower surface heated Constant wall temperature	$Nu = 0.27\ (GrPr)^{0.25}$ $10^5 < GrPr < 10^{11}$	Nu = average Nusselt number
2.2.1 Horizontal Plate : Heated Surface up Constant heat flux	Properties except β to be evaluated at $T_e = T_w - 0.25\ (T_w - T_\infty)$ $Nu = 0.13\ (Gr_e Pr_e)^{0.333}$; $Gr_e Pr_e < 2 \times 10^8$ $Nu = 0.16\ (Gr_e Pr_e)^{0.333}$; $2 \times 10^8 < Gr_e Pr_e < 10^{11}$	Gr_e = Grashof with properties evaluated at T_e $T_e = T_w - 0.25\ (T_w - T_\infty)$ Pr_e = Prandtl at Te β — evaluated at T_∞ T_w — Average wall temp.
2.2.2 Heated surface down constant heat flux	$Nu = 0.58\ (Gr_e \cdot Pr_e)^{0.2}$ $10^6 < Gr_e Pr_e < 10^{11}$	
2.3.1 Inclined Plates Heated surface facing down constant heat flux	$Nu = 0.56\ (Gr_e Pr_e \cos\theta)^{0.25}$ $\theta < 88°,\ 10^5 < Gr_e Pr_e \cos\theta < 10^{11}$ $Nu_x = 0.17\ (Gr_x^* \cdot Nu_x \cdot Pr)^{0.25}$ $10^{10} < Gr_x^* Nu_x \cdot Pr < 10^{15}$ for heated face facing down, multiply Gr* by $\cos^2\theta$, $Nu = 0.58\ (Gr_e Pr_e)^{0.2}$ $88° < \theta < 90°$ $10^6 < GrPr < 10^{11}$	θ = angle with vertical $Gr^* = \dfrac{g\beta q x^4}{k v^2}$ q = heat flux, W/m²
2.3.2 Heated Surface up Constant heat flux	$Nu = 0.14\ [(Gr_e Pr_e)^{0.333} - (APr_e)^{0.333}]$ $+ 0.56\ (Gr_e\ Pr_e \cos\theta)^{0.25}$ $10^5 < Gr_e\ Pr_e \cos\theta < 10^{11}$ A is found from the tabulation below :	Z = 0.25 + 0.083 $(\sin\theta)^{1.75}$

θ	15	30	60	75
A	5×10^9	2×10^9	10^8	10^6

2.4 Inclined Cylinders constant heat flux	$Nu_L = [0.60 - 0.488\ (\sin\theta)^{1.03}]\ (Gr_L Pr)^Z$ $Gr_L\ Pr < 2 \times 10^8$,	Gr_L — Based on length of cylinders

Description	*Correlation and Validity*	*Notation*
3.1 Horizontal cylinders (long cylinders)	$Nu = C\,(Gr_D Pr)^m$ (constant wall temp.) $Gr_D Pr$ — C — m 10^{-10} to 10^{-2} — 0.675 — 0.058 10^{-2} to 10^{2} — 1.02 — 0.148 10^{2} to 10^{4} — 0.85 — 0.188 10^{4} to 10^{7} — 0.48 — 0.25 10^{7} to 10^{12} — 0.125 — 0.333	
3.2 Horizontal Cylinder	$Nu_D = \left\{0.60 + 0.387\left[\dfrac{Gr_D\,Pr}{\left\{1+\left(\dfrac{0.559}{Pr}\right)^{0.5625}\right\}^{0.296}}\right]^{0.167}\right\}^2$ $10^{-5} < Gr_D Pr < 10^{12}$ $Nu_D = 0.36 + \dfrac{0.518\,(Gr_D Pr)^{0.25}}{\left[1+\left(\dfrac{0.559}{Pr}\right)^{0.5625}\right]^{0.444}}$ $10^{-6} < Gr_D Pr < 10^{9}$	Gr_D — based on diameter
3.3 Liquid Metals	$Nu_D = 0.53\,[Gr_D (Pr)^2]^{0.25}$	
4.1 Spheres	$Nu = 2 + 0.43\,(Gr_D Pr)^{0.25}$ $1 < Gr_D Pr < 10^5$; $Pr \simeq 1$ $Nu = 2 + 0.50\,(Gr_D Pr)^{0.25}$ $3 \times 10^5 < Gr_D Pr < 8 \times 10^8$	α = Thermal diffusivity L = Refer figure
5.1 Rectangular Cavities (Enclosed space)  	Surfaces of height H displaced by distance L and inclined at θ° to horizontal, surfaces at T_1 and T_2 $Q = hA\,[T_1 - T_2]$ $Nu_L = 0.069\,Ra_L^{0.333}\,.\,Pr^{0.074}$ $3 \times 10^5 < Ra_L < 7 \times 10^9$, $\theta = 0°$	Properties at T = $(T_1 + T_2)/2$ A = H × length of cavity $Ra_L = \dfrac{g\,.\,\beta\,(T_1 - T_2)\,L^3}{\alpha\nu}$ Q = heat transferred

Description	*Correlation and Validity*	*Notation*
5.2 Medium aspect ratio (H/L)	$Nu_L = 0.22 \left(\frac{Pr}{0.2 + Pr} . Ra_L\right)^{0.28} (H/L)^{-0.25}$ $Pr < 10,\ 2 < \frac{H}{L} < 10,\ Ra_L < 10^{10},\ \theta = 90°$	
5.3 Small aspect ratio (H/L)	$Nu_L = 0.18 \left(\frac{Pr}{0.2 + Pr} . Ra_L\right)^{0.29}$ $1 < \frac{H}{L} < 2,\ 10^{-3} < Pr < 10$ $10^3 < [Ra_L . Pr/(0.2 + Pr)]\ ;\ \theta = 90°$	
5.4 Large aspect ratio, lower Ra_L	$Nu_L = 0.42\ Ra_L^{0.25}\ Pr^{0.012} \left(\frac{H}{L}\right)^{-0.3}$ $10 < \frac{H}{L} < 40,$ $10^4 < Ra_L < 10^7$ $1 < Pr \quad \theta = 90°$	$Ra_L = \frac{g\beta (T_1 - T_2) L^3}{\alpha\nu}$ α = Thermal diffusivity
5.5 Large aspect ratio, higher Ra_L	$Nu_L = 0.046\ Ra_L^{0.333}$ $1 < \frac{H}{L} < 40\ ;\ 1 < Pr < 20,$ $10^6 < Ra_L < 10^9 \quad \theta = 90°$	
5.6 Inclined cavities (below critical angle)	$Nu_L = 1 + 1.44 \left[1 - \frac{1708}{Ra_L . \cos\theta}\right]^{@} \times \left[1 - \frac{1708 (\sin 1.8\,\theta)^{1.6}}{Ra_L . \cos\theta}\right] + \left[\left(\frac{Ra_L \cos\theta}{5830}\right)^{0.333} - 1\right]^{@}$ @ If the value of the expression is –ve set it to zero. $\frac{H}{L} \geq 12 \qquad 0° < \theta \leq \theta^*$	θ^* = critical angle dependent on aspect ratio, refer table

H/L	1	3	6	12	> 12
θ^*	25	53	60	67	70

Description	*Correlation and Validity*	*Notation*
5.7 Inclined cavities below critical angle θ^* small aspect ratio	$Nu_L = Nu_{L\theta=0} \left[\frac{Nu_{L\theta=90}}{Nu_{L\theta=0}}\right]^{\theta/\theta^*} (\sin\theta^*)^{\theta/4\theta^*}$ $\frac{H}{L} < 12 ; 0 < \theta < \theta^*$	To calculate $Nu_{L\theta=0}$ and $Nu_{L\theta=90°}$ use equations in section 5.6.
5.8 Inclined cavities above critical angle	$Nu_L = Nu_{L(\theta=90)} (\sin\theta)^{0.25}$ $\theta^* < \theta < 90°$ $Nu_L = 1 + [Nu_{L(\theta=90)} - 1] \sin\theta$ $90° < \theta < 180°$	
6.1 Annular space between concentric cylinders	$q' = \frac{2\pi k_{eff}}{\ln\left(\frac{D_o}{D_i}\right)} [T_i - T_o]$ $\frac{k_{eff}}{k} = 0.386 \left(\frac{Pr}{0.861 + Pr}\right)^{0.25} (Ra_C)^{0.25}$ where $Ra_C = \frac{\left[\ln\frac{D_o}{D_i}\right]^4}{L^3[D_i^{-0.6} + D_o^{-0.6}]^5} \cdot Ra_L$ $10^2 < Ra_C < 10^7$	k_{eff} = effective thermal conductivity, a stationary fluid should have to transfer the same amount of heat by conduction D_0 = outside diameter D_i = inside diameter T_0 = outside surface temperature T_i = inside surface temperature k = thermal conductivity of fluid L = $(D_o - D_i)/2$ Ra_L = Rayleigh number based on L
6.2 Space between concentric spheres	$q = k_{eff}\pi (D_i D_o/L)(T_i - T_o) = \frac{4\pi k_{eff} \cdot r_1 r_2 \Delta T}{r_2 - r_1}$ $\frac{k_{eff}}{k} = 0.74 \left(\frac{Pr}{0.861 + Pr}\right)^{0.25} (Ra_C)^{0.25}$ where $Ra_C = \left[\frac{L}{(D_o D_i)^4} \frac{Ra_L}{[D_i^{-1.4} + D_o^{-1.4}]^5}\right]^{0.25}$ $10^2 < Ra_C \le 10^4$	q' —heat transfer per unit length, W/m q —heat transfer between concentric spheres L —Gap length $= (r_2 - r_1)$

7.0 FREE CONVECTION : SIMPLIFIED EXPRESSIONS FOR CONVECTIVE HEAT TRANSFER COEFFICIENT FOR AIR AT ATMOSPHERIC PRESSURE

Geometry and Validity	*h, W/m²K*
7.1 LAMINAR ($10^4 < GrPr < 10^9$)	
Vertical plane or cylinder	$1.42 \left(\frac{\Delta T}{L}\right)^{0.25}$
Horizontal cylinder	$1.32 \left(\frac{\Delta T}{D}\right)^{0.25}$
Horizontal plate heated face up/cooled face down (L = Area/Perimeter)	$1.32 \left(\frac{\Delta T}{L}\right)^{0.25}$
Heated face down or cooled face up	$0.59 \left(\frac{\Delta T}{L}\right)^{0.25}$
7.2 TURBULENT ($GrPr > 10^9$)	
Vertical plane or cylinder	$1.31\ (\Delta T)^{0.333}$
Horizontal cylinder	$1.24\ (\Delta T)^{0.333}$
Horizontal plate :	
Heated face up or cooled face down	$1.52\ (\Delta T)^{0.333}$
Heated face down or cooled face up.	$0.59 \left(\frac{\Delta T}{L}\right)^{0.25}$

For metric units divide the constant by 1.164

Note : For pressure other than atmospheric pressure multiply h by $\left(\frac{P}{atm.pr}\right)^{0.5}$ for laminar flow and by $\left(\frac{P}{atm.pr}\right)^{0.67}$ for turbulent flow. $\Delta T = T_w - T_\infty$

Geometry and Validity	*Correlation*	*Notation*
8.1 **COMBINED FREE AND FORCED CONVECTION**	$Gr/Re^2 >> 1$ Free convection $Gr/Re^2 \approx 1$ Mixed convection $Gr/Re^2 << 1$ Forced convection	Gz = Graetz number $Gz = Re_D.Pr\ \frac{D}{L}$
8.2 Mixed convection through tubes $(Gr/Re^2) \simeq 1$	LAMINAR $Nu = 1.75\left[\frac{\mu}{\mu_w}\right]^{0.14}[Gz + 0.012\,(Gz.Gr^{0.333})^{1.333}]^{0.333}$ TURBULENT $Nu = 4.69\ Re_D^{0.27}\ Pr^{0.21}\ Gr_D^{0.07}\ (D/L)^{0.36}$ $Re_D > 2000$ and $Ra_D\ \frac{D}{L} < 5000$ OR $Re_D > 800$ and $Ra_D\ \frac{D}{L} > 2 \times 10^4$	μ at bulk mean temp. μ_w at wall temp.
9.1 Rotating Cylinder in a fluid	$Nu_D = 0.11\,[0.5\ Re_w^2 + Gr_D Pr]^{0.35}$ $Re_w > 8000$ in air	$Re_w = \frac{\omega \pi D^2}{\upsilon}$ Peripheral speed Reynolds Number ω = rotational speed in rad/s
9.2 Rotating discs in a fluid	$Nu_D = \frac{\bar{h} D}{k} = 0.36\left(\frac{\omega D^2}{\upsilon}\right)^{0.5}$ Rotational Reynolds No. $= \frac{\omega D^2}{\upsilon} < 5 \times 10^5$ $Nu_r = 0.0195\,(\omega R^2/\upsilon)^{0.8}$ $\frac{\omega D^2}{\upsilon} < 5 \times 10^5$ $Nu_r = \frac{\bar{h} r_o}{k} = 0.36\left(\frac{\omega r_o^2}{\upsilon}\right)^{0.5}\left(\frac{r_c}{r_o}\right)^2 + 0.015\left(\frac{\omega r_o^2}{\upsilon}\right)^{0.8}\left\{1 - \left(\frac{r_c}{r_o}\right)^{2.6}\right\}$	$D = 2r_o$ υ = kinematic viscosity of fluid Nu_r = local Nusselt Number based on radius R r_0 = outside radius r_c = radius at which turbulence starts *i.e.* $\frac{\omega D_C^2}{\upsilon} = 5 \times 10^5$ $Re_D = \frac{\omega D^2}{\upsilon}$ $D_C = 2r_c$
9.3 Rotating Spheres	$Nu = 0.43\ Re_D^{0.5}\ Pr^{0.4}$ $Re_D < 5 \times 10^4$ $Nu_D = 0.066\ Re_D^{0.67}\ Pr^{0.4}$ $5 \times 10^4 < Re_D < 7 \times 10^5$	

BOILING

Description	*Correlation and Validity*	*Notations*
Nucleate Pool Boiling	$\frac{Q}{A} = \mu_1 \cdot h_{fg} \left[g \frac{(\rho_l - \rho_v)}{\sigma} \right]^{0.5} \left[\frac{c_1 \Delta T}{C_{sf} h_{fg} Pr^n} \right]^{3.0}$	n = 1 for water and 1.7 for other fluids μ_l = dynamic viscosity of liquid μ_v = dynamic viscosity of vapour h_{fg} = enthalpy of evaporation, refer page 144, 147 g = acceleration due to gravity 9.81 m/s^2 ρ_l = density of liquid ρ_v = density of vapour σ = surface tension for liquid vapour interface. Refer p. 144, 146. c_l = specific heat of liquid ΔT = Excess temperature $T_w - T_{sat}$ T_w = surface temperature C_{sf} = constant, see tables on page 143 Pr_l = Prandtl Number for liquid Q/A= heat flux, W/m^2 T_l = liquid temp, K. k_l —Thermal conductivity of liquid k_v —Thermal conductivity of vapour c_{pv} —Specific heat of vapour at constant pressure σ_r —Stefan Boltzmann constant (see radiation) ε —Emissivity h —heat transfer coefficient in film boiling h_c —heat transfer coefficient due to convection h_r —heat transfer coefficient due to radiation T_w —wall temperature, K T_{sat}—saturation temperature of vapour, K D —diameter
	Critical or maximum heat flux $\frac{Q}{A} = 0.18 h_{fg} \rho_v \left[\frac{\sigma \cdot g \cdot (\rho_l - \rho_v)}{\rho_v^2} \right]^{0.25}$ properties at $(T_w + T_{sat})/2$	
	$\frac{Q}{A} = 1.464 \times 10^{-9} \left[\frac{c_1 k_l^2 (\rho_l - \rho_v) \rho_l^{0.5}}{\mu_l^{0.5} \rho_v h_{fg}} \right]^{0.5} \left[\frac{h_{fg} \cdot \rho_v \Delta T}{\sigma T_l} \right]^{2.3}$	
	$\frac{Q}{A} = C \left[\frac{c_1 k_l^2 h_{fg}^3 (\rho_l - \rho_v) \rho_l^{0.5} \rho_v^3}{\mu_l^{0.5} \sigma^4 T_l^4} \right]^{0.5} (\Delta T)^{3.5}$ for C refer page 144	
Stable Film Boiling Horizontal tube Radiation prevails	$h_c = 0.62 \left[\frac{k_v^3 \rho_v (\rho_l - \rho_v) \cdot g (h_{fg} + 0.68 c_{pv} \Delta T)}{\mu_v D \Delta T} \right]^{0.25}$ $h_r = \sigma_r \varepsilon \left[\frac{T_w^4 - T_{sat}^4}{T_w - T_{sat}} \right]$ $h = h_c + 0.75 h_r$ Vapour properties at film temperature $\left(\frac{Q}{A}\right) \min = 0.09 h_{fg} \cdot \rho_v \left[\frac{g \sigma (\rho_l - \rho_v)}{(\rho_l + \rho_v)^2} \right]^{0.25}$	

VALUES OF THE COEFFICIENT C_{sf} FOR VARIOUS LIQUID SURFACE COMBINATIONS.

Liquid	*Heating surface*	C_{sf}
Benzene	Chromium	0.010
Carbon Tetra Chloride	Copper	0.013
Carbon Tetra Chloride	Emery polished copper	0.007
Ethyl alcohol	Chromium	0.027
Isopropyl alcohol	Copper	0.00225
n – Butyl alcohol	Copper	0.00305
n – Pentane	Chromium	0.015
n – Pentane	Emery polished copper	0.0154
n – Pentane	Emery polished Nickel	0.0127
n – Pentane	Lapped copper	0.0049
n – Pentane	Emery rubbed copper	0.0074
Potassium carbonate K_2CO_3, 35%	Copper	0.0054
Potassium carbonate K_2CO_3, 50%	Copper	0.00275
Water	Copper	0.013
Water	Platinum	0.013
Water	Brass	0.0060
Water	Emery polished copper	0.0128
Water	Emery polished and paraffin treated copper	0.0147
Water	Scored copper	0.0068
Water	Teflon coated stainless Steel	0.0058
Water	Ground and polished stainless Steel	0.0080
Water	Chemically etched stainless Steel	0.0133
Water	Mechanically polished stainless Steel	0.0132

SIMPLIFIED EXPRESSIONS FOR BOILING HEAT TRANSFER COEFFICIENT FOR WATER AT ONE ATMOSPHERE.*

Type of Surface	*Range of Validity, W/m^2*	*h, W/m^2K*	*Notation*
Horizontal	$(Q/A) < 16000$	$1042.6\ (\Delta T)^{0.333}$	(Q/A) — Heat Flux, W/m^2
	$16000 < (Q/A) < 24000$	$5.56(\Delta T)^3$	h_p — Heat transfer coefficient at pressure, P
Vertical	$(Q/A) < 3000$	$537.3\ (\Delta T)^{0.143}$	h — Heat transfer coefficient at atmospheric pressure, P_a
	$3000 < (Q/A) < 63000$	$7.96\ (\Delta T)^3$	

*For other pressures, $h_p = h \times (P/P_a)^{0.4}$

C, CONSTANT FOR NUCLEATE BOILING, (SI Units)

Liquid	*Surface*	*Apparatus*		*C*
Water	Brass	Horizontal	Tube	7.6350×10^{-9}
Water	Brass Dirty	Horizontal	Plate	2.1400×10^{-9}
Water	Brass Clean	Horizontal	Plate	0.4890×10^{-9}
Water	Nickel	Horizontal	Wire	7.6350×10^{-9}
Water	Chromium	Horizontal	Tube	1.2200×10^{-9}
Water	Chromium	Horizontal	Plate	0.0460×10^{-9}
Acetone	Chromium	Horizontal	Plate	0.1070×10^{-9}
Ethanol	Copper	Horizontal	Plate	0.1830×10^{-9}
Ethanol	Chromium	Horizontal	Plate	0.0460×10^{-9}
n-Butanol	Brass	Horizontal	Tube	0.4890×10^{-9}
Propane	Copper	Horizontal	Tube	0.0915×10^{-9}
Propane	Chromium	Horizontal	Plate	0.0092×10^{-9}
n-Heptane	Chromium	Horizontal	Plate	0.0153×10^{-9}
CCl_4	Brass	Horizontal	Tube	0.6300×10^{-9}
CCl_4	Chromium	Vertical	Tube	0.0460×10^{-9}
Methyl Chloride	Copper	Horizontal	Tube	0.1373×10^{-9}

*LATENT HEAT OF VAPORISATION FOR WATER

Temp. °C	*Latent Heat* *kJ/kg*
0	2501.6
50	2382.9
100	2256.9
150	2113.2
200	1938.6
250	1714.6
300	1406.0
350	895.7
374.15	0.0

SURFACE TENSION, σ OF WATER AGAINST AIR

Temperature, °C	*σ, N/m*
0	0.0776
10	0.0742
20	0.0729
30	0.0711
40	0.0697
50	0.0679
60	0.0662
70	0.0644
80	0.0627
100	0.0588

*Also refer steam tables

RELATIVE MAGNITUDE OF HEAT TRANSFER COEFFICIENT IN NUCLEATE BOILING AT 1 atm RELATIVE TO VALUE FOR WATER.

Fluid	*h fluid / h water*
Water	1.0
Water 20% Sugar	0.87
10% Sodium sulphate, Na_2SO_4	0.94
26% Glycerin	0.83
55% Glycerin	0.75
24% Sodium Chloride, NaCl	0.61
Ispropanol	0.70
Methanol	0.53
Toluene	0.36
Carbon tetra Chloride	0.35
n – Butanol	0.32

APPROXIMATE BURNOUT HEAT VALUE AT 1 atm.

Fluid-surface combination	*(Q/A)max kW/m²*	*ΔT critical*
Water-copper	620-850	—
Water copper chrome plated	940-1260	23-28
Water steel	1290	30
Benzene-copper	130	—
Benzene-Aluminium	160	—
Propanol-Nickel plated copper	210-340	42-50
Butanol-Nickel plated copper	250-330	33-39
Ethanol-Aluminium	170	—
Ethanol-copper	250	—
Methanol-copper	390	—
Methanol-chrome plated copper	350	—
Methanol-steel	390	—
Liquid hydrogen	30	2
Liquid nitrogen	100	11
Liquid oxygen	150	11

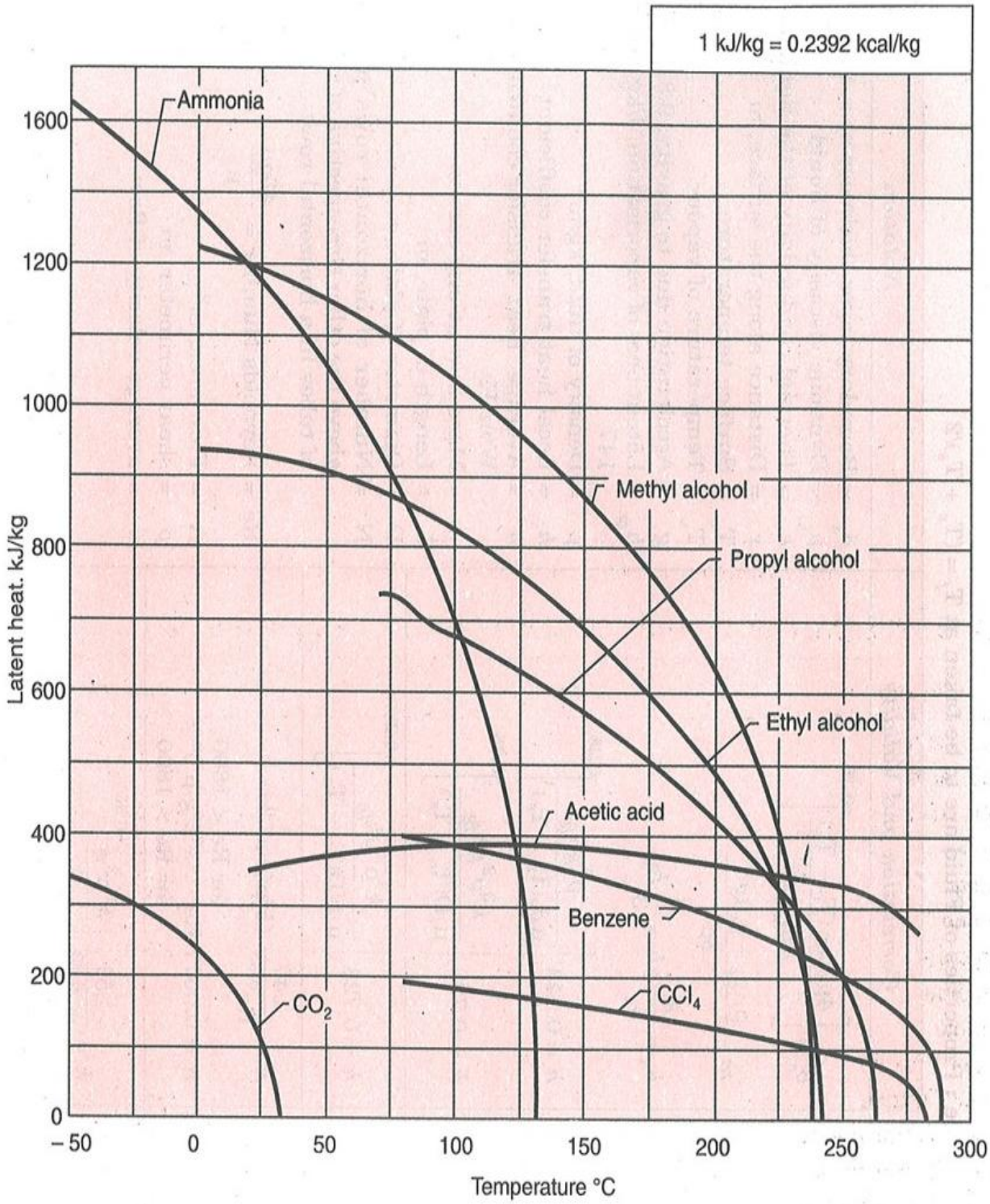
SURFACE TENSION, σ OF WATER AGAINST ITS VAPOUR

Temperature, °C	σ, *N/m*
0	0.0755
20	0.0729
40	0.0695
60	0.0661
80	0.0627
100	0.0589
150	0.0487
160	0.0462
200	0.0378
250	0.0261
300	0.0143
350	0.0036
360	0.00156
374.1	0.0000

Approximately for water $\sigma = 0.1232\ (1 - 0.001467\ T)$ N/m, T in K

SURFACE TENSION, σ OF LIQUIDS IN CONTACT WITH THEIR VAPOUR

Substance	*Temperature, °C*	σ, *N/m*
Acetic Acid	10	0.02890
Acetic Acid	20	0.02790
Acetic Acid	50	0.02480
Acetone	0	0.02630
Acetone	20	0.02370
Acetone	40	0.02120
Ammonia	11	0.02340
Ammonia	34	0.01820
Bromine	20	0.04150
Carbon Dioxide	20	0.00118
Carbon Dioxide	– 10.55	0.00912
Carbon Tetrachloride	20	0.02700
Carbon Tetrachloride	100	0.01730
Carbon Tetrachloride	200	0.00660
Ethyl Alcohol	10	0.02360
Ethyl Alcohol	20	0.02270
Ethyl Alcohol	30	0.02190
Hydrazine	25	0.01710
Hydrogen Peroxide	18	0.01340
Methyl Alcohol	50	0.09180
Methyl Ether	– 10	0.07640
Methyl Ether	– 40	0.02010
Napthalene	127	0.02890
Tetrachlorethylene	20	0.03170
Toluene	10	0.02770
Toluene	20	0.02850
Toluene	30	0.02750



Note. For refrigerants, tables are available.

CONDENSATION

$$Q = hA\,[T_v - T_s]$$

Note : Properties of Fluid are to be taken at $T_f = (T_v + T_s)/2$

Description	*Correlation and Validity*	*Notation*
FILM CONDENSATION : (Laminar) (*i*) VERTICAL SURFACES	$\delta_x = \left[\dfrac{4\mu_l\, kx\,(T_v - T_s)}{gh_{fg}\,\rho^2}\right]^{0.25}$ $\dot{m} = \dfrac{\rho_l(\rho_l - \rho_v)g\delta^3}{3\mu}$ $h_x = \dfrac{k}{\delta_x}\,;\; h = \dfrac{4}{3}\,h_L$ $h = 0.943\left[\dfrac{k^3\rho^2 gh_{fg}}{\mu_l L(T_v - T_s)}\right]^{0.25}$	δ_x = Boundary layer thickness at x, m μ_l = Dynamic viscosity of liquid k = Thermal conductivity of the liquid, W/mK x = Distance along the surface, m T_s = Surface temperature, T_v — Temperature of vapour g = Acceleration due to gravity, 9.81 m/s^2 h_{fg} = Latent heat of vaporisation, J/kg, refer page 147 ρ = Density of fluid, kg/m^3 h_x = Local heat transfer coefficient h = Average heat transfer coefficient upto L, W/m^{2}K $\dot{m}$ = Mass flow at any section L = Length of plate, m D = Diameter of plate, m N = Number of horizontal rows placed one above the other (irrespective of the number of tubes in a horizontal row) Re = Reynolds Number = $\dfrac{4\delta\rho u}{\mu}$ A = Flow area, m^2 p = shear perimeter, m u = average velocity of flow
(*ii*) HORIZONTAL TUBES	$h = 0.728\left[\dfrac{k^3\rho^2 gh_{fg}}{\mu_l D(T_v - T_s)}\right]^{0.25}$	
(*iii*) BANK OF N TUBES	$h = 0.728\left[\dfrac{k^3\rho^2 gh_{fg}}{\mu_l ND(T_v - T_s)}\right]^{0.25}$	
(*iv*) VERTICAL TUBES	$h = \dfrac{1.47}{Re^{0.33}}\,(k^3\rho^2 g/\mu^2)^{0.33}$ for Re < 1800 $h = 0.0077\,Re^{0.4}\,(k^3\rho^2 g/\mu^2)^{0.33}$ for Re > 1800	
(*v*) VERTICAL SHEET CONTAINING HORIZONTAL TUBES	$h = \dfrac{1.51}{Re^{0.33}}\left[\dfrac{k^3\rho^2 g}{\mu^2}\right]^{0.33}$ for Re < 1800	

CONDENSATION(*Continued*)

Description	*Correlation and Validity*	*Notation*
(*vi*) INSIDE HORIZONTAL TUBES (Short tubes)	$h_D = 0.555 \left[\frac{g\rho_1(\rho_1 - \rho_v)k_1^3 h'_{fg}}{\mu_l(T_v - T_s)D}\right]^{0.25}$ $\frac{D \cdot G_v}{\mu_v} < 35{,}000$	G_v = mass flow rate of vapour per unit area G_l = mass flow rate of liquid per unit area c_l — Specific heat of liquid $h'_{fg} = h_{fg} + \frac{3}{8} c_l(T_{sat} - T_s)$ k_f, Pr_f at film temprature.
(*vii*) HIGHER VAPOUR VELOCITIES	$\frac{h_D D}{k_f} = 0.026\ Pr_f^{0.33}\ Re_m^{0.8}$ where $Re_m = \frac{D}{\mu_l}\left[G_l + G_v\left(\frac{\rho_l}{\rho_v}\right)^{0.5}\right]$ for $5000 < \frac{D \cdot G_v}{\mu_v} < 20{,}000$	

For inclined surfaces θ° with horizontal replace g by $g \sin \theta$

SIMPLIFIED EXPRESSIONS

Description	*Correlation*	*Notation*
(*i*) SINGLE VERTICAL TUBE	$h = 1.26\ Z \left[\frac{\pi d}{W}\right]^{0.33}$	Z = condensation coefficient (Refer table on page 150) W = Weight of condensate in Newton/*hr* N_v = Number of vertical columns L = length of tube, **cm** N = total number of tubes d = diameter (outer) of tubes, **cm**
(*ii*) A BANK OF HORIZONTAL TUBES	$h = Z \left[\frac{N_v L}{W}\right]^{0.33}$	
(*iii*) VERTICAL CONDENSERS	$h = 1.26\ Z \left[\frac{N\pi d}{W}\right]^{0.33}$	

For inclined surfaces in place of g use $g \sin \theta$, angle θ with horizontal

or

$g \cos \theta$, angle θ with vertical.

CONDENSATION COEFFICIENT, Z, FOR FLUIDS. (SI Units)

Fluid	*Condensation coefficient, z*					
	0°C	*50°C*	*100°C*	*150°C*	*200°C*	*300°C*
Acetone	3125	3215	3182			
Ammonia	9860					
Benzene	2410	2801	2928	3187		
Deccine		1922	2042	2062	1922	
Dodeccine			1967	2019	2019	1785
Dowtherm–A					2398	2490
Ethyl Alcohol	1922	2398	2809			
Ethyl Glycol		2121	2639	2864		
Gasoline		2042	2104	2104		
Hexane	2156	2241	2258	2179		
Kerosene			1985	2042	1997	
Methyl Alcohol	2864	3389	3904			
Natural Gasoline	2121	2316	2428			
Octane	1985	2104	2196	2139		
Pentane	2333	2333	2258	2216		
i–Propyl alcohol		1780	2443			
Steam		11354	15413	19298		
Tetradeccine			1848	1942	1967	1820
Toluene		2667	2861			
Xylene		2876	2761			

For use with MKS units divide the above values of Z by 2.49

Approximate values of condensation heat-transfer coefficients for vapours at 1 atm.

Fluid	*Geometry*	$W/m^2.K$	$T_v - T_w$, °C
Steam	Vertical surface	4000–11,300	22–3
	Horizontal tubes, 15 to 76 mm diameter	9600-24,400	20–2
Diphenyl	Vertical surface, turbulent, 3.66 m	680–2400	72–13
	Horizontal tube, 43 mm diameter	1280–2270	15–5
Dowtherm A	Vertical surface 3.66 m turbulent	680–3060	40–20
Ethanol	Vertical surface, 152 mm	1130–2000	55–11
	Horizontal tube, 51 mm diameter	1800–2550	22–6
Propanol	Horizontal tube, 51 mm diameter	1400–1700	26–13
Butanol	Horizontal tube, 51 mm diameter	1400–1700	26–13
Benzene	Horizontal tubes, 15 to 33 mm diameter	1300–2150	45–13

T_v–Vapour temperature, T_w–Surface temperature

HEAT EXCHANGERS, $Q = UA\,(\Delta T)_{lm}$

Description	*Correlation*
SINGLE PASS (*i*) Parallel flow	$(\Delta T)_{lm} = \dfrac{(T_1 - t_1) - (T_2 - t_2)}{\ln\left[\dfrac{T_1 - t_1}{T_2 - t_2}\right]}$
(*ii*) Counter flow	$(\Delta T)^*_{lm} = \dfrac{(T_1 - t_2) - (T_2 - t_1)}{\ln\left[\dfrac{T_1 - t_2}{T_2 - t_1}\right]}$
MULTIPASS and CROSS FLOW	$Q = FUA\,(\Delta T)^*_{lm}$
NTU METHOD	$Q = \varepsilon C_{min}(T_1 - t_1)$ [**Note.** $\dfrac{C_{min}}{C_{max}}$ is zero when one of the fluids is condensing or evaporating and equal to 1 when $m_h c_h = m_c c_c$] $\varepsilon = \dfrac{m_h c_h}{C_{min}}\left[\dfrac{T_1 - T_2}{T_1 - t_1}\right]$ for $m_h C_h = C_{min}$ $= \dfrac{m_c c_c}{C_{min}}\left[\dfrac{t_2 - t_1}{T_1 - t_1}\right]$ for $m_c C_c = C_{min}$

Notation

Q	Heat exchanged, W
U	Overall heat transfer coefficient W/m²K (Refer pages 155 and 156)
$(\Delta T)_{lm}$	Logarithmic mean temperature difference "LMTD"
A	area, m²
T_1	Entry temperature of hot fluid
T_2	Exit temperature of hot fluid
t_1	Entry temperature of cold fluid
t_2	Exit temperature of cold fluid
F	CORRECTION FACTOR depending on R, P and type of exchanger
	For F, R and P definition refer chart on pages 158 to 161
NTU	Number of Transfer Units = AU/C_{min}
C_{min}	Smaller value of $m_h c_h$ and $m_c c_c$; W/K
m_c	Mass flow rate of cold fluid, kg/s
m_h	Mass flow rate of hot fluid
c_h	Specific heat of cold fluid, J/kg K
c_c	Specific heat of cold fluid, J/kg K
ε	Effectiveness (depends on C_{min}/C_{max}, charts on pages, 162 to 167

HEAT EXCHANGERS EFFECTIVENESS RELATIONS

Description	*Correlation*	*Notation*
Double pipe Parallel flow	$\varepsilon = \dfrac{1-\exp[-N(1+C)]}{1+C}$	$N = NTU = UA/C_{min}$
Counter flow	$\varepsilon = \dfrac{1-\exp[-N(1-C)]}{1-C\exp[-N(1-C)]}$	$C = \dfrac{G_{min}}{C_{max}}$
Counter flow C = 1	$\varepsilon = \dfrac{N}{N+1}$	$C_{min} = (mc)_{min}$
Cross flow Both fluids unmixed	$\varepsilon = 1-\exp\left[\dfrac{\exp(-NC.n)-1}{Cn}\right]$	$n = N^{-0.22}$
Both fluids mixed	$\varepsilon = \left[\dfrac{1}{1-\exp(-N)} + \dfrac{C}{1-\exp(-NC)} - \dfrac{1}{N}\right]^{-1}$	ε, Effectiveness
C_{max} mixed and C_{min} unmixed	$\varepsilon = (1/C)\left\{1-\exp[-C(1-e^{-N})]\right\}$	m —flow rate kg/s
C_{max} unmixed and C_{min} mixed	$\varepsilon = 1-\exp[-(1/C)(1-\exp(-NC)]$	
Shell and tube : one shell pass and 2, 4, 6 tube passes	$\varepsilon = 2\left[1+C+(1+C^2)^{0.5}\dfrac{1+\exp[-N(1+C^2)^{0.5}}{1-\exp[-N(1+C^2)^{0.5}]}\right]^{-1}$	
All exchangers with C = 0	$\varepsilon = 1-e^{-N}$	

Heat Exchangers NTU Relations

Description	*Correlation*	*Notation*
Double pipe parallel flow	$N = \dfrac{-\ln[1-(1+C)\varepsilon]}{1+C}$ †	N NTU $C = \dfrac{C_{min}}{C_{max}}$ ε effectiveness † expression may become indeterminate if $\Sigma(1+C) = 1$
Counter flow	$N = \dfrac{1}{C-1}\ln\left(\dfrac{\varepsilon-1}{C\varepsilon-1}\right)$	
Counter flow C = 1	$N = \dfrac{\varepsilon}{1-\varepsilon}$	
Cross flow : C_{max} mixed and C_{min} unmixed	$N = -\ln\left[1+\dfrac{1}{C}.\ln(1-C\varepsilon)\right]$	
C_{max} unmixed C_{min} mixed	$N = \dfrac{-1}{C}[1+C.\ln(1-\varepsilon)]$	
Shell and Tube One shell pass and 2, 4, 6 tube passes	$N = -(1+C^2)^{-0.5}.\ln\dfrac{2/\varepsilon-1-C-(1+C^2)^{0.5}}{2/\varepsilon-1-C+(1+C^2)^{0.5}}$	
All exchangers C = 0	$N = -\ln(1-\varepsilon)$	h = convective heat transfer coefficient A_L — heat transfer surface area for unit length of matrix c — specific heat of fluid $\dot{m}$ — mass flow rate of fluid τ — time c_s — specific heat of matrix material M_L — mass of solid per unit length of matrix
Storage type heat exchanger filled with matrix of solid material heated and cooled alternately.	Definitions : Location factor : at distance x $E = \dfrac{hA_L}{c\dot{m}}x$ Time factor at time τ, $\eta = \dfrac{hA_L}{c_s M_L}\tau$	

Description	*Correlation*	*Notation*
Solid Temperature	$\frac{T - T_{go}}{T_o - T_{go}} = f_1\,[E, \eta]$, refer chart on page 168	T_g — fluid temperature at location x, time τ T — matrix temperature at location x, time τ T_o — Initial temperature of matrix T_{go} — Entry temperature of fluid Q — heat transfer per unit time h_H — convective heat transfer coefficient during heating h_C — Convective heat transfer coefficient during cooling k — thermal conductivity of matrix material A — Total material surface area T_{gh} — Average fluid temperature during heating period T_{gC} — Average fluid temperature during cooling period N — revolutions per hour.
Gas Temperature	$\frac{T_g - T_{go}}{T_o - T_{go}} = f_2\,[E, \eta]$, refer chart on page 168	
Heat Transfer rate (Heating Period = cooling period)	$Q = \frac{1}{\frac{1}{h_H} + \frac{1}{h_C} + \frac{b}{3k}} \frac{A}{2} [T_{gH} - T_{gC}]$	
Effectiveness : (as per other heat exchangers)	Refer chartson page 169 Definitions for use of charts : $NTU_o = \frac{1}{C_{min}} \left[\frac{1}{\frac{1}{(hA)_H} + \frac{1}{(hA)_C}} \right]$ C_r = Matrix capacity rate = $c_s M_L N$ $(hA)^* = \frac{(hA)_C}{(hA)_H}$	

APPROXIMATE OVER-ALL HEAT TRANSFER COEFFICIENTS FOR PRELIMINARY ESTIMATES

Duty	*Overall heat transfer coefficient, U* W/m^2K
Steam to water-instantaneous heater	2300–3500
Steam to water-storage-tank heater	1000–1800
Steam to heavy fuel oil	60–175
Steam to light fuel oil	175–350
Steam to light petroleum distillate	300–1200
Steam to aqueous solutions	600–3500
Steam to gases	30–300
Gas to gas	10–30
Water to compressed air	60–175
Water to water, jacket water coolers	900–1600
Water to lubricating oil	100–350
Water to condensing oil vapours	230–600
Water to condensing alcohol	250–700
Water to condensing Refrigerant-12	450–900
Water to condensing ammonia	900–1500
Water to organic solvents, alcohol	300–900
Water to boiling Refrigerant-12	300–900
Water to gasoline	350–550
Water to gas oil	200–350
Water to brine	600–1200
Light organics to light organics	250–450
Medium organics to medium organics	100–350
Heavy organics to heavy organics	60–250
Heavy organics to light organics	60–350
Crude oil to gas oil	175–350

FOULING RESISTANCE, R_f

Fluid	*Fouling Resistance, R_f m^2K/W*
Sea Water below 52°C	0.0000827
Sea Water above 52°C	0.0017540
Treated Boiler Feed Water above 52 °C	0.0001754
Fuel Oil	0.0008770
Quenching Oil	0.0007051
Alcohol vapours	0.0000877
Steam, not mixed with Oil	0.0000877
Industrial Air	0.0003525
Refrigerants	0.0001754

Dirt layers that gradually build up on heat transfer surfaces increase thermal resistance. This is accounted for by the use of Fouling Factors R_{fo} and R_{fi}.

EXPRESSIONS FOR OVERALL HEAT TRANSFER COEFFICIENTS, U_o and U_i FOR TUBULAR SECTIONS

U_o

$$\frac{1}{U_o} = \frac{1}{h_o} + R_{fo} + \frac{r_o}{k}\ln\frac{r_o}{r_i} + \frac{r_o}{r_i}R_{fi} + \frac{r_o}{r_i}\frac{1}{h_i}$$

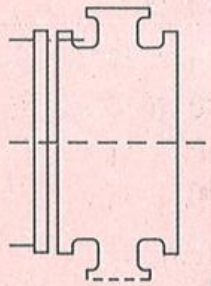
U_i

$$\frac{1}{U_i} = \frac{1}{h_i} + R_{fi} + \frac{r_i}{k}\ln\frac{r_o}{r_i} + \frac{r_i}{r_o}R_{fo} + \frac{r_i}{r_o}\frac{1}{h_o}$$

TEMA NOTATIONS FOR HEAT EXCHANGERS

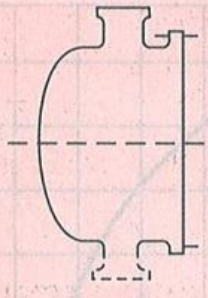
Front and stationary head types

A



Channel and removable cover

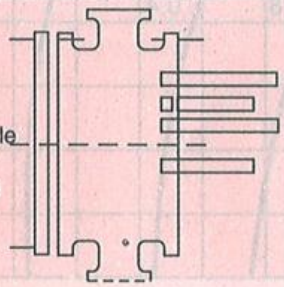
B



Bonnet (integral cover)

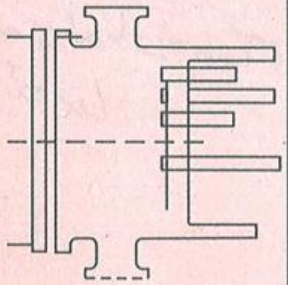
C

Re-movable tube bundle only



Channel integral with tube sheet and removable cover

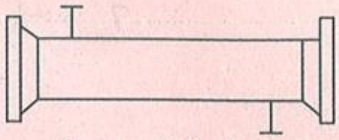
N



Channel integral with tube sheet and removable cover

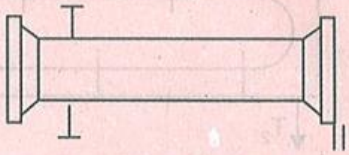
Shell type

E



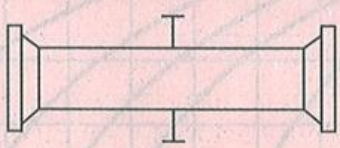
One pass shell

F



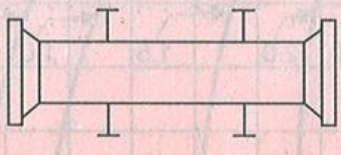
Two pass shell with longitudinal bottle

G



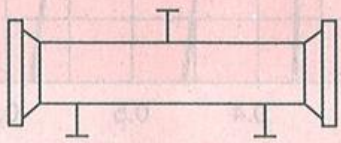
Split flow

H



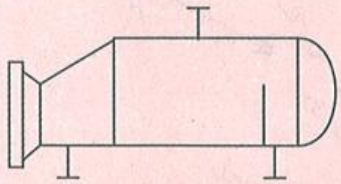
Double split flow

J



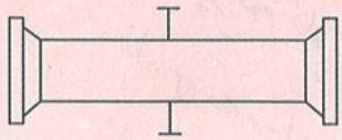
Divided flow

K



Kettle type reboiler

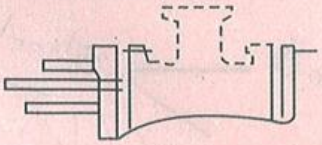
X



Cross flow

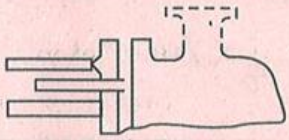
Rear and head types

L



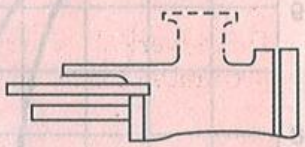
Fixed tube sheet like a stationary head

M



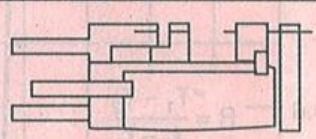
Fixed tube sheet like stationary head B

N



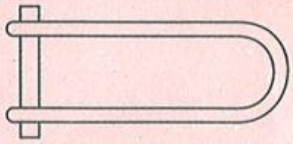
Fixed tube sheet like A-stationary head

P



Outside packed floating head

U

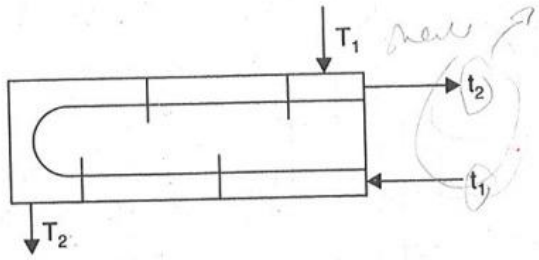


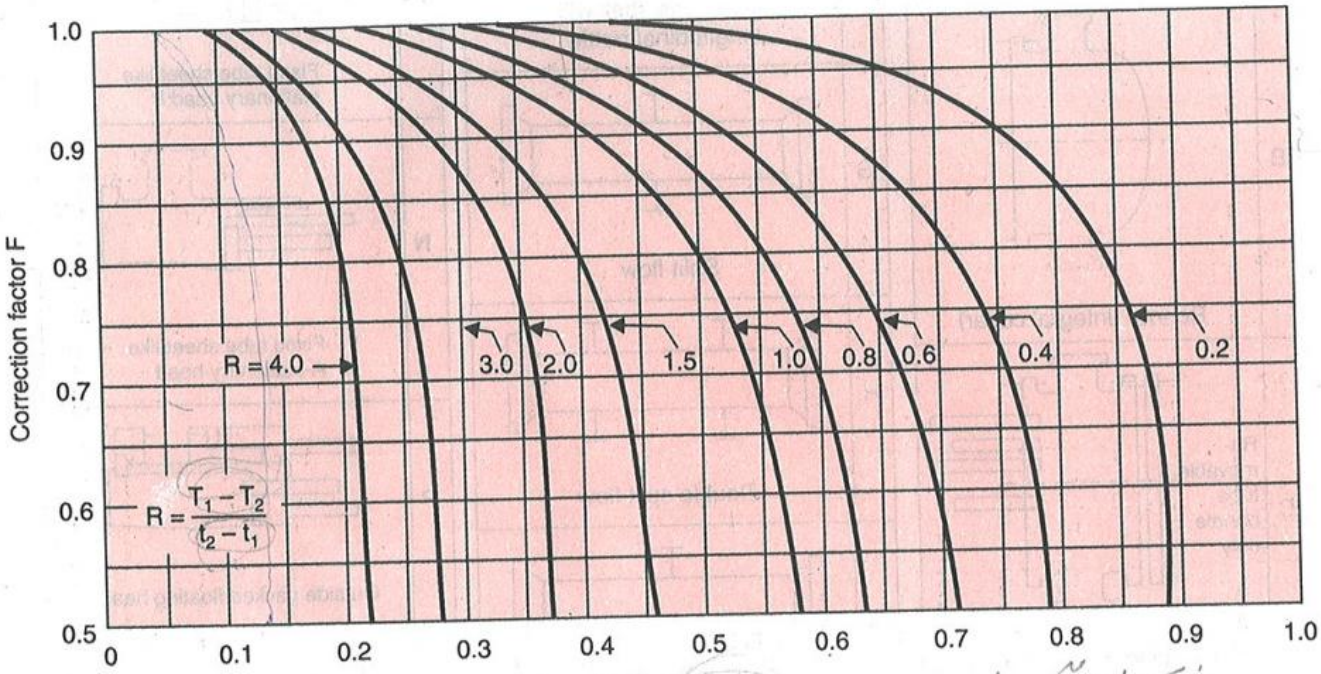
U-tube bundle

CORRECTION FACTOR PLOT FOR EXCHANGER WITH ONE SHELL PASS AND TWO, FOUR OR MULTIPLE TUBE-PASSES

2 Tube
4 Tube
6 Tube
8 Tube
10 Tube
Shell 1

2 و 4 و 6 و 8 و 10





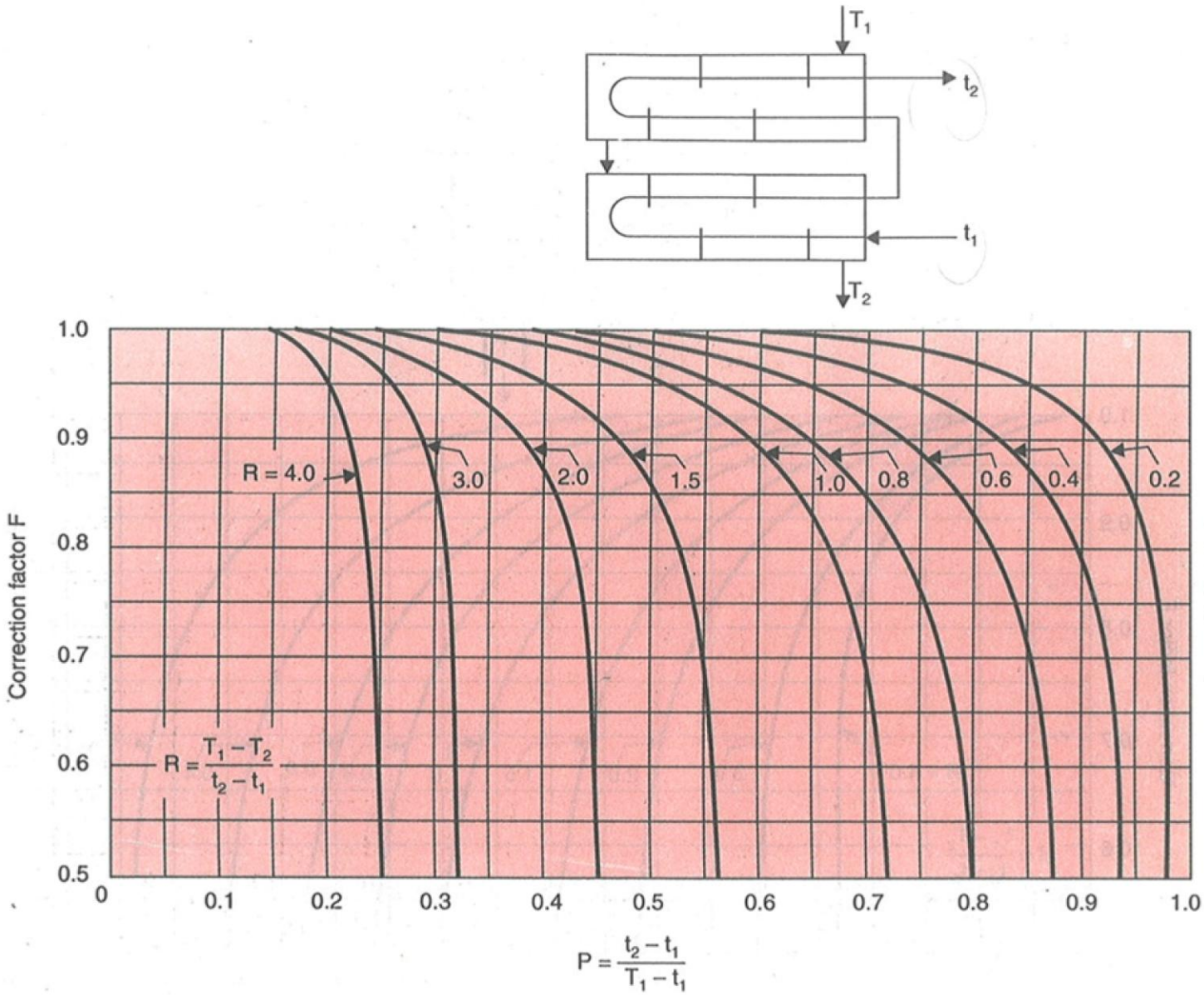
$P = \frac{t_2 - t_1}{T_1 - t_1}$

فرق پله ی گرمای شله ی ناو (Tube) به که به رو

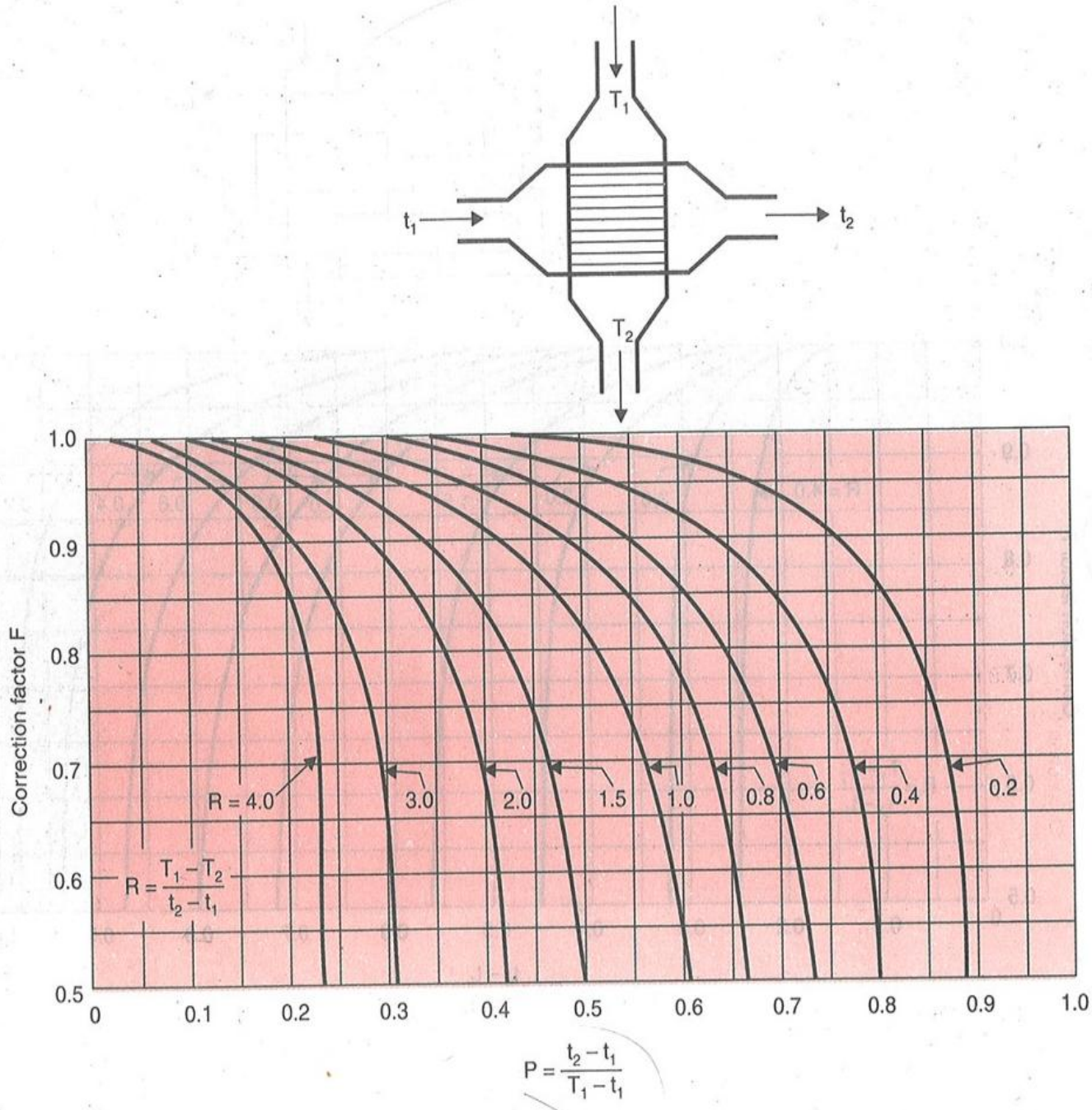
که ورودی پله ی گرما ناقص
بچوکترین پله ی گرما

پله ی گرمای شله ی گرمای که وشله که پله ی
که چیته ناو heat exchang er ناقص
پله ی گرمای که وشله ساده ی که چیته
ناو Tube

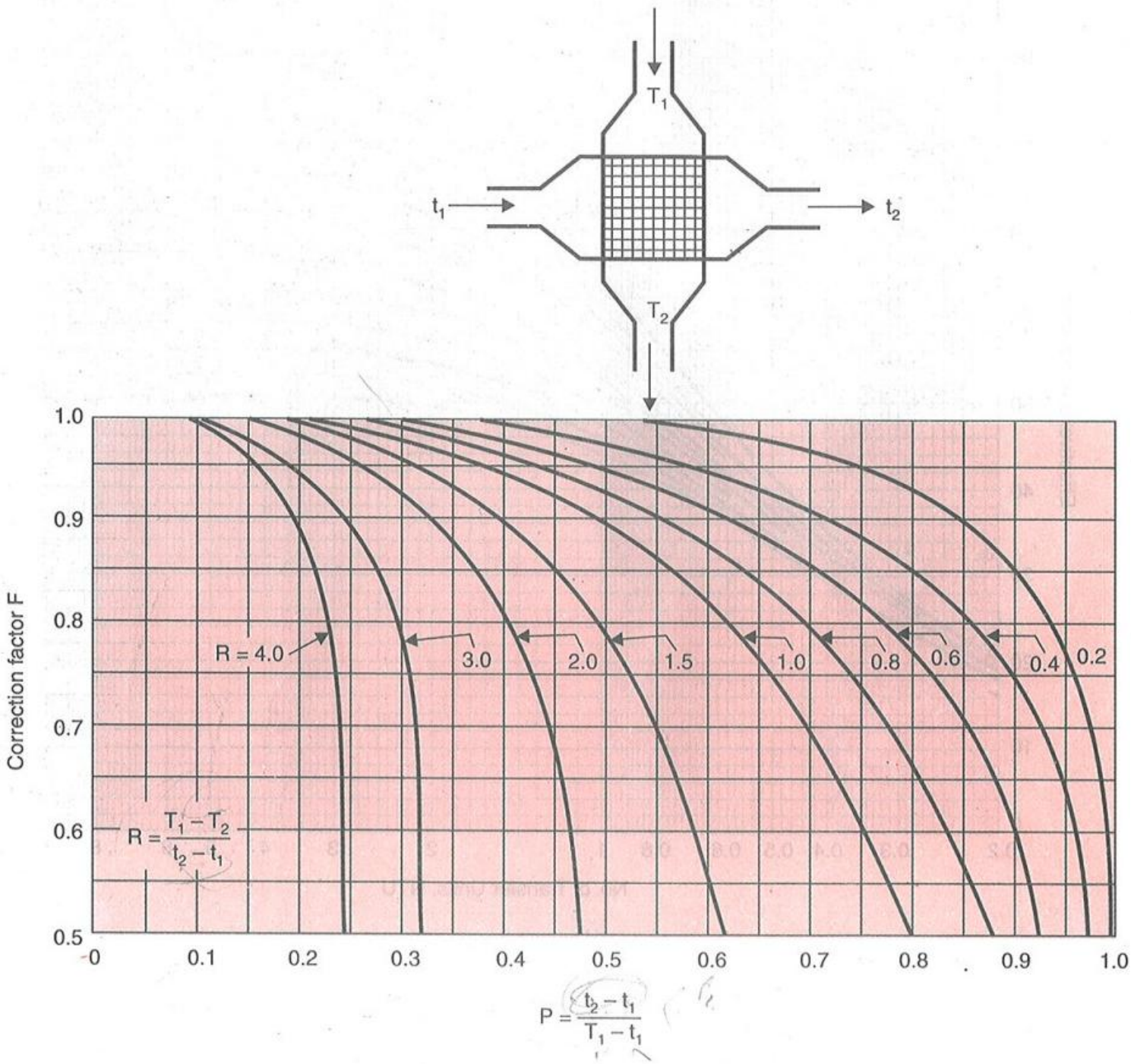
CORRECTION FACTOR PLOT FOR EXCHANGER WITH TWO SHELL PASSES AND FOUR, EIGHT, OR ANY MULTIPLE NUMBER OF TUBE PASSES



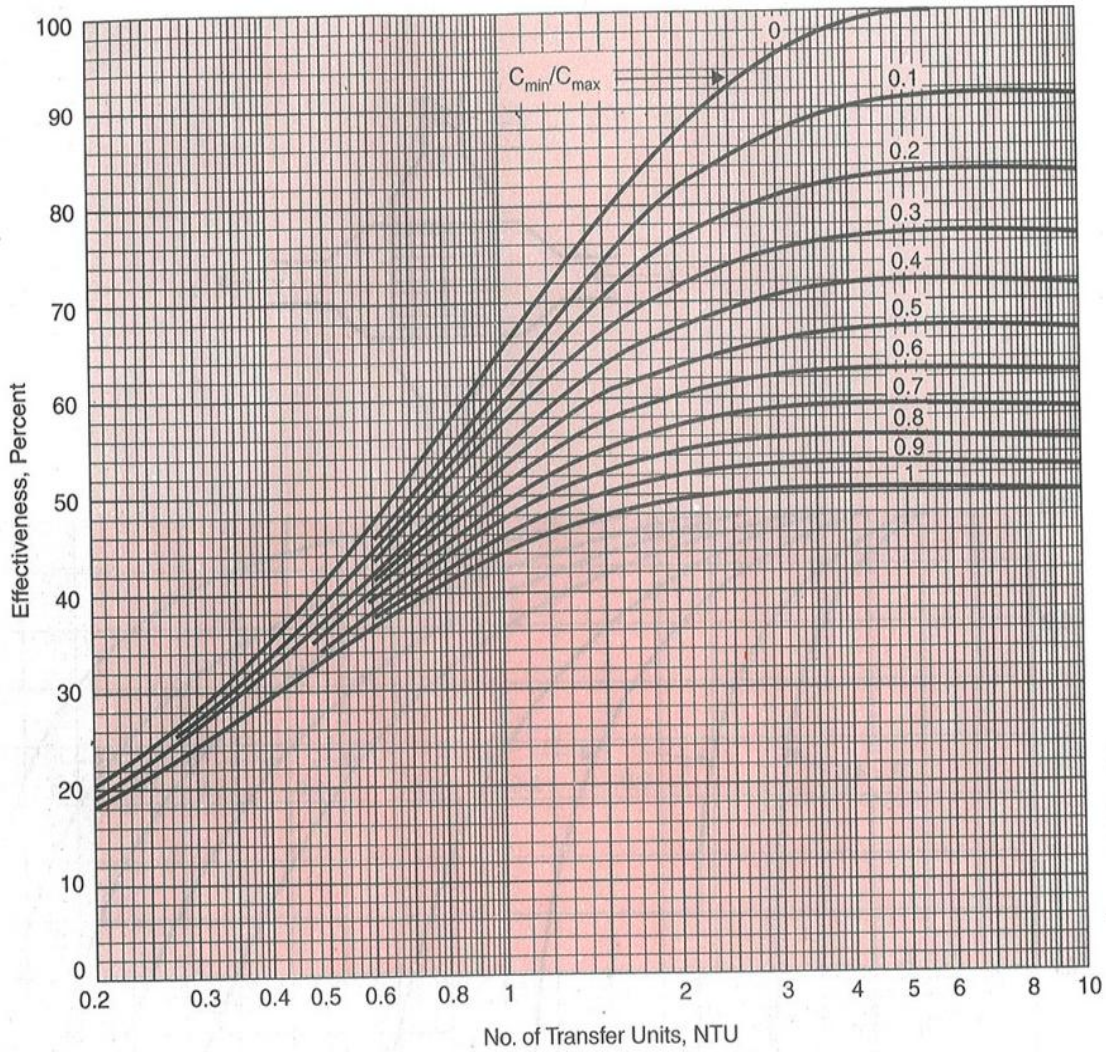
CORRECTION FACTOR PLOT FOR SINGLE PASS CROSS-FLOW EXCHANGER, ONE FLUID MIXED ; OTHER UNMIXED



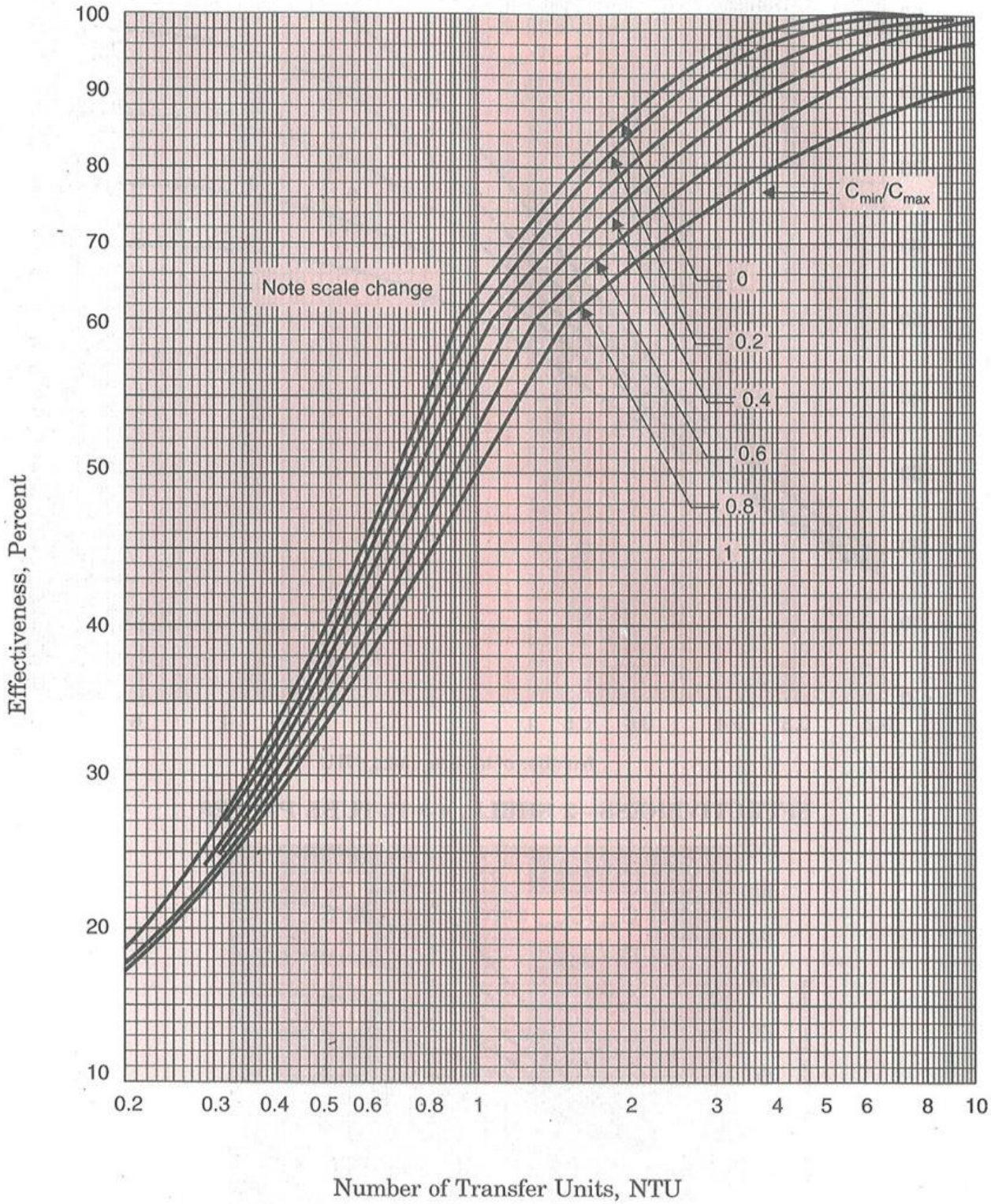
CORRECTION FACTOR PLOT FOR SINGLE PASS CROSS-FLOW EXCHANGER, BOTH FLUID UNMIXED



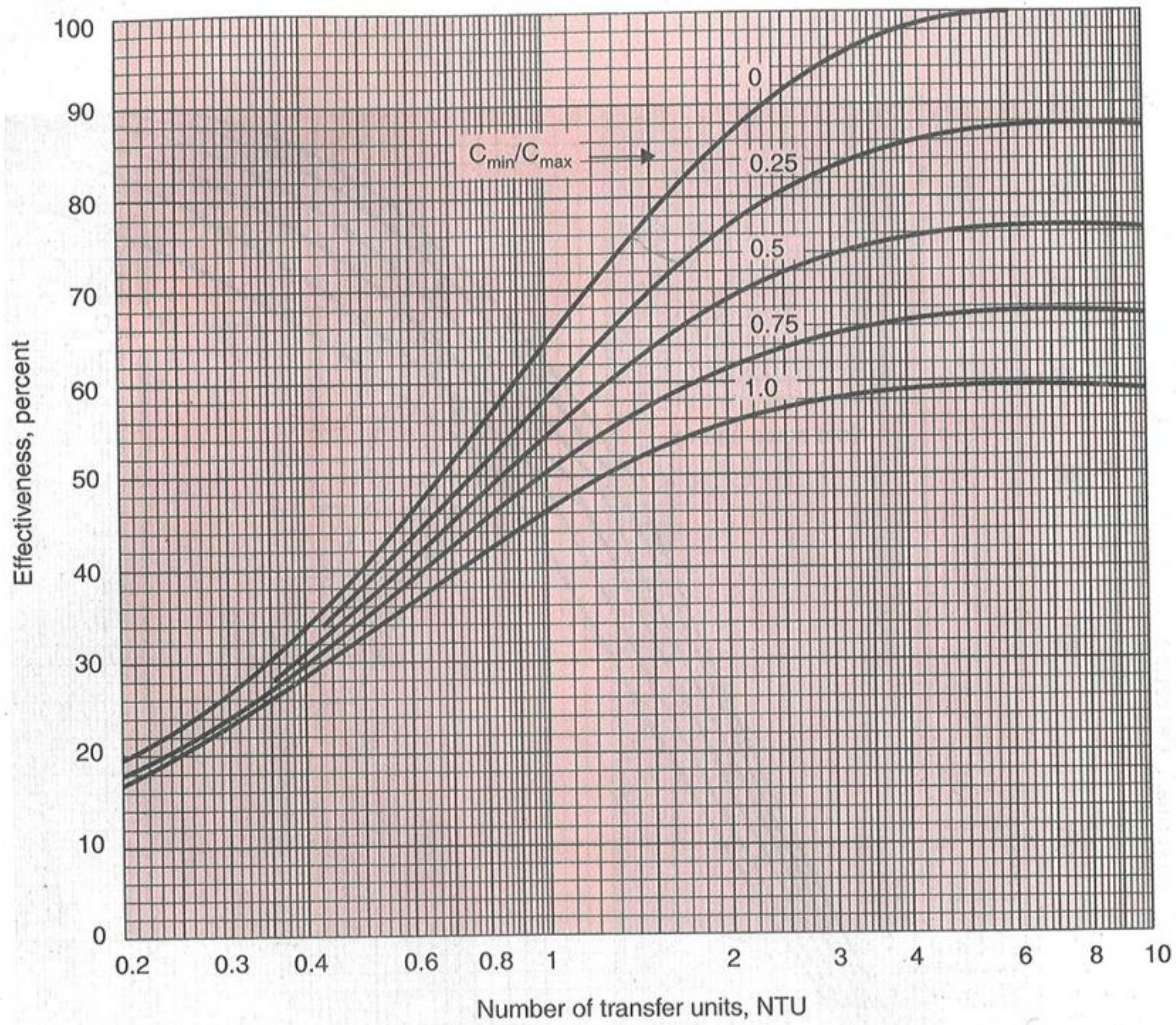
EFFECTIVENESS—PARALLEL FLOW



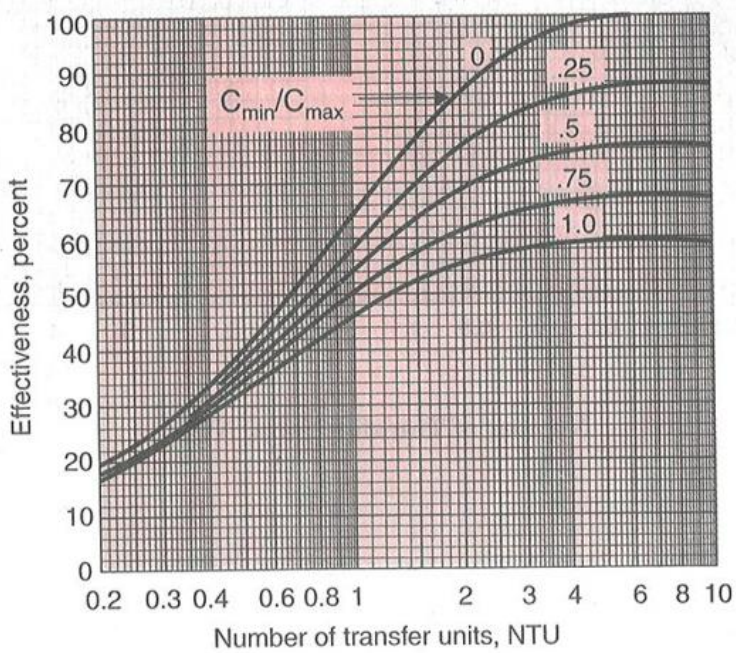
EFFECTIVENESS—COUNTER FLOW



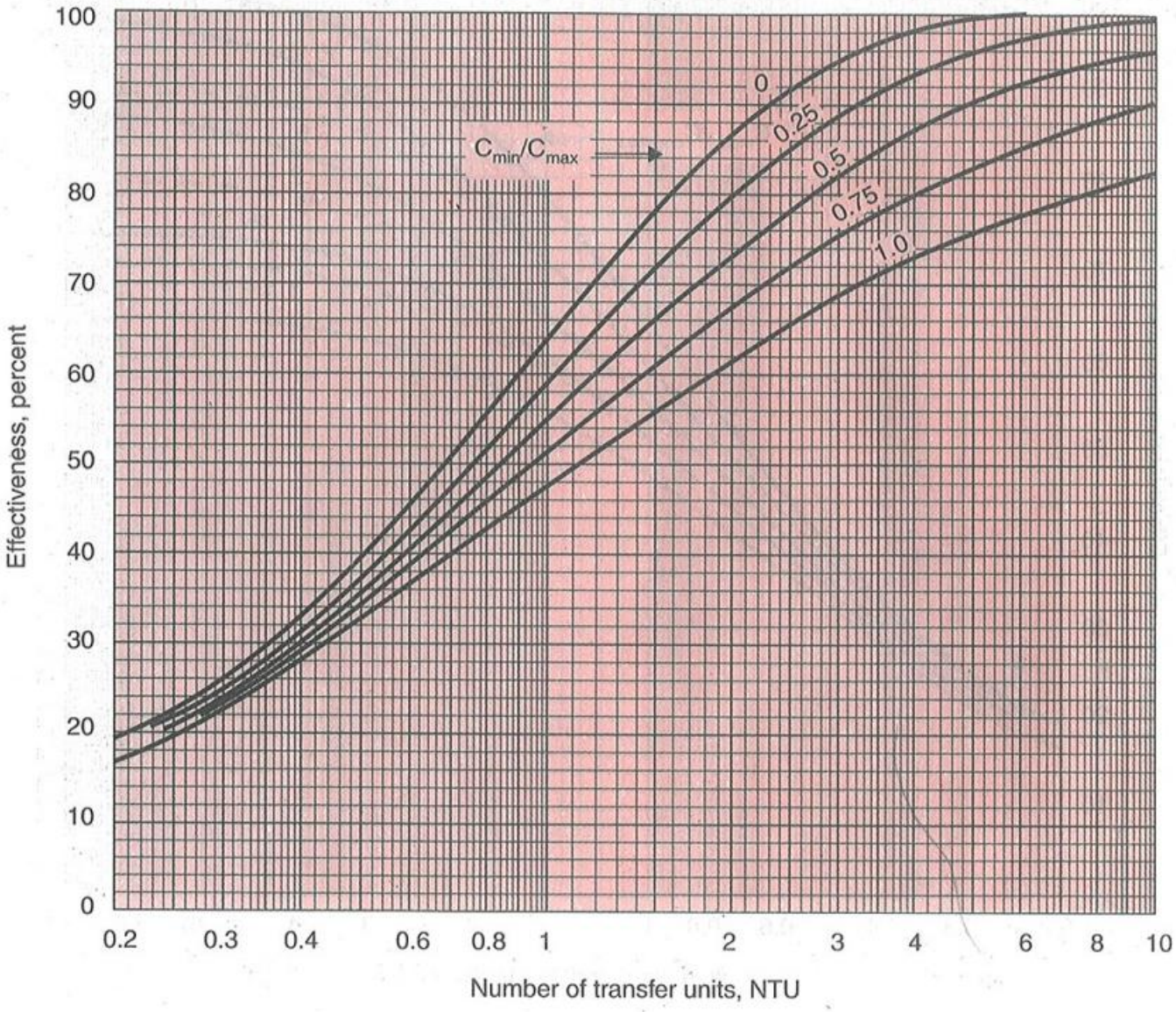
EFFECTIVENESS—1 SHELL PASS, 2, 4, 6 TUBE PASSES



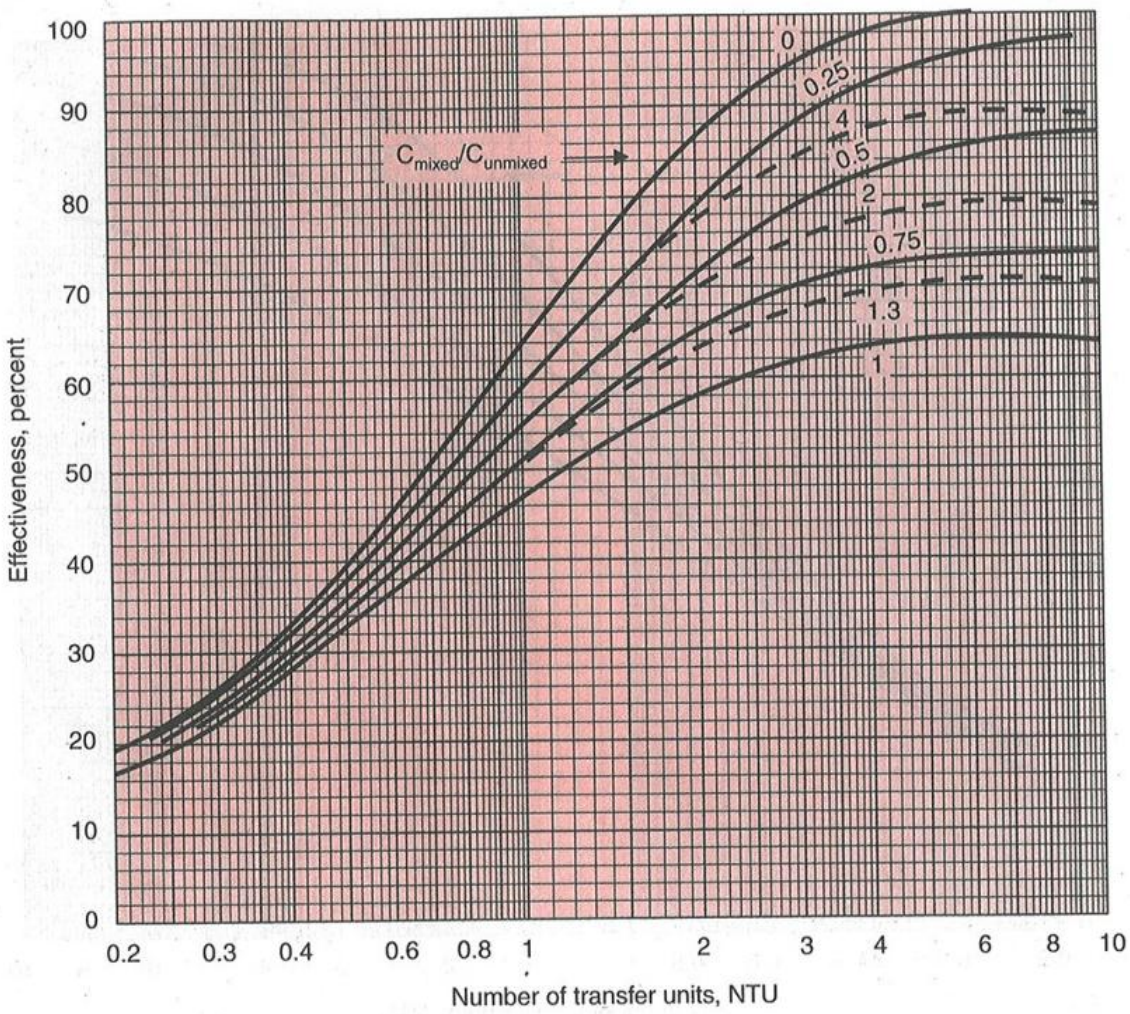
EFFECTIVENESS—2 SHELL, 4-8-12-TUBE PASSES



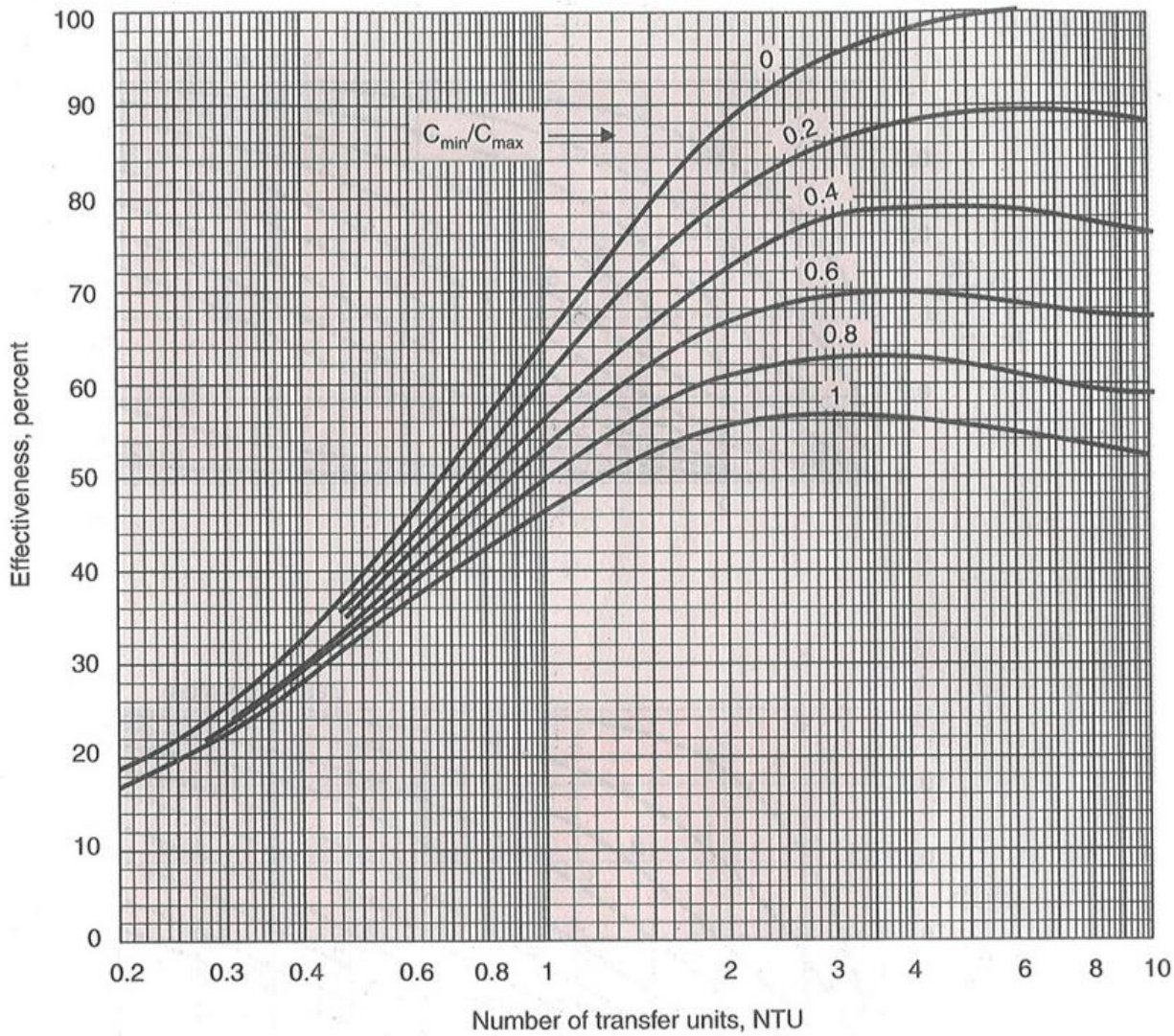
EFFECTIVENESS—CROSS FLOW, BOTH FLUIDS UNMIXED



EFFECTIVENESS—CROSS FLOW, ONE FLUIDMIXED

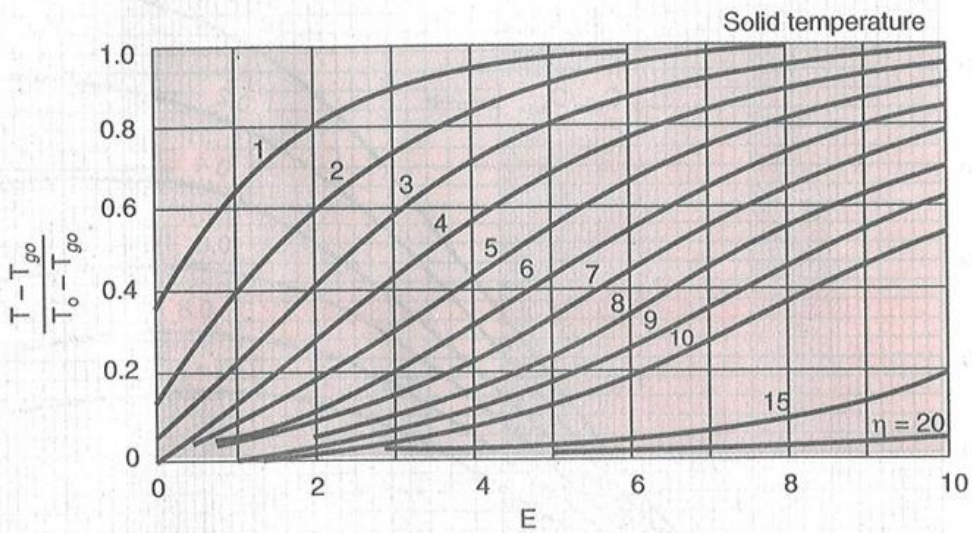


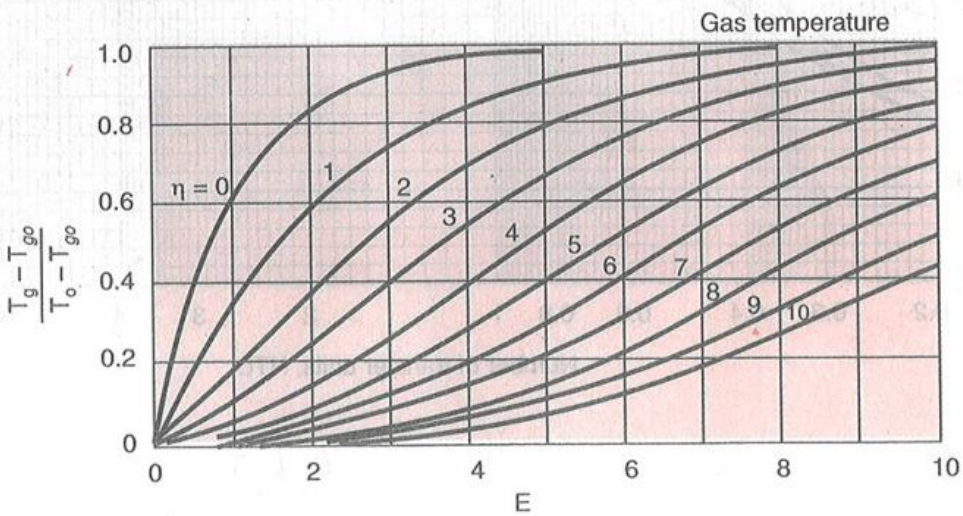
EFFECTIVENESS—CROSS FLOW—BOTH FLUIDS MIXED



UA/Cmin

STORAGE TYPE HEAT EXCHANGER—TEMPERATURE VARIATION ALONG FLOW DIRECTION

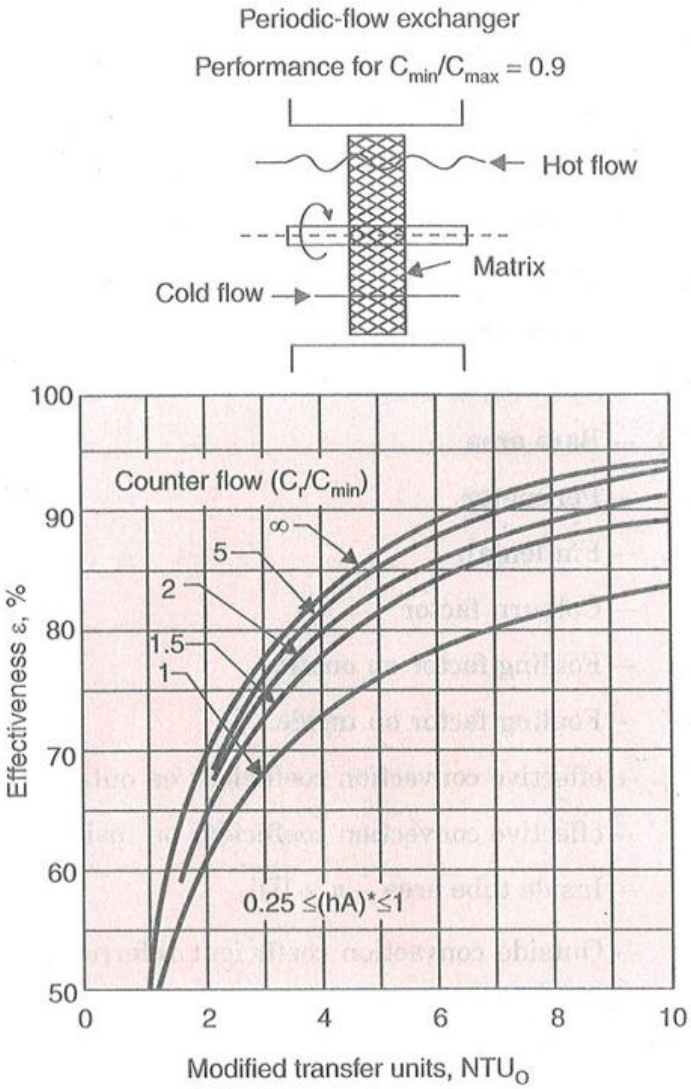


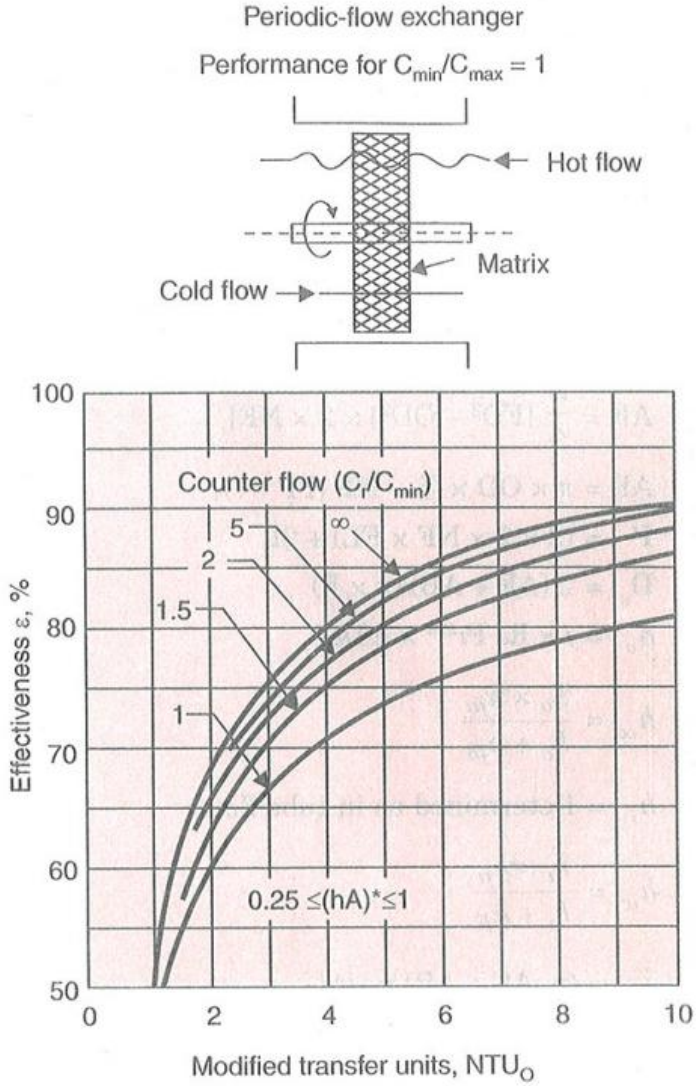


$$E = \frac{hA_L x}{c\dot{m}}, \qquad \eta = \frac{hA_L}{c_s M_L}\,\tau$$

Refer page 153 and 154 for notations.

STORAGE TYPE EXCHANGER—EFFECTIVENESS

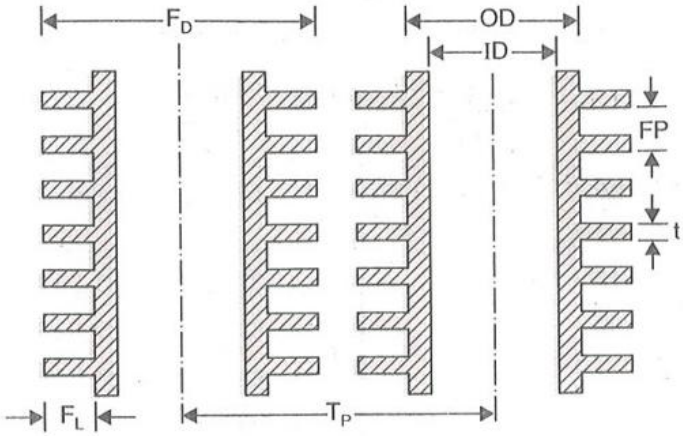




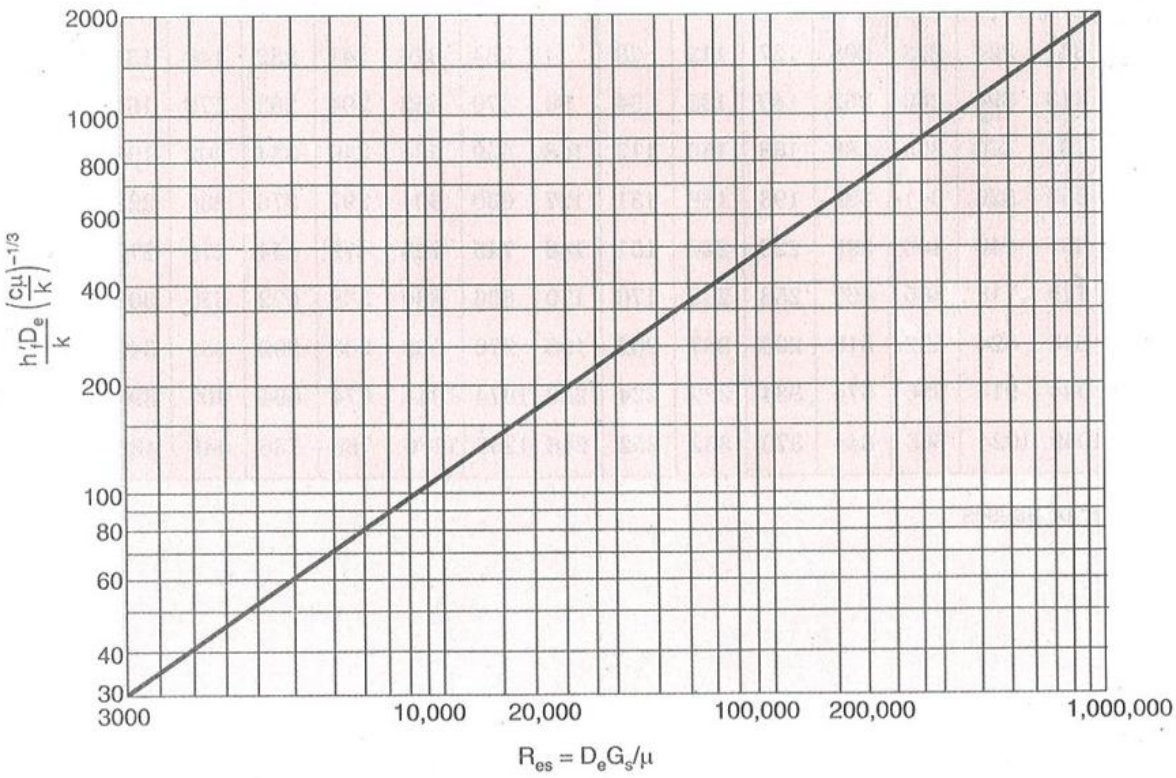
Note. For NTU_0 and C_r refer to page 154.

TRANSVERSE FIN HEAT EXCHANGER

Equations	*Notation*
Note : Refer figure next page for notations.	St — Stanton number = N*u*/Re Pr.
$j = \text{St. Pr}^{1/3} = \exp\left[ln\ 30 + 0.731\ ln\left(\frac{Re}{3000}\right)\right]$	Pr — Prandtl number.
$\text{Re} = \frac{GD_e}{\mu}$	G — mass flux, kg/sm^2
$D_e = \frac{2(\text{Fin area, AF} + \text{Bare area, AB})}{\pi(\text{Projected Perimeter P})}$	D_e — Equivalent Diameter.
$\text{AF} = \frac{\pi}{4}\ [\text{FD}^2 - \text{OD}^2] \times 2 \times \text{NF}]$	NF — Number of fins in length L = L/FP
$\text{AB} = \pi \times \text{OD} \times [\text{L} - \text{NF}\ (\text{FP} - t)]$	L — Heater height.
$\text{P} = (2 \times 2 \times \text{NF} \times \text{FL}) + 2\text{L}$	FP — Fin pitch.
$D_e = 2\ (\text{AF} + \text{AB})/(\pi \times \text{P})$	AF — Fin surface area
$h_o = j \times \text{Re Pr}^{2/3} \times k/\text{De}$	AB — Bare area
$h_{oe} = \frac{h_o \times h_{fo}}{h_o + h_{fo}}$	P — Perimeter
h_i = Determined as in tube flow.	FL — Fin length
$h_{ie} = \frac{h_i \times h_{fi}}{h_i + h_{fi}}$	j — Colburn factor
$\bar{h} = (n_f\,\text{AF} + \text{AB})\ h_{oe}/\text{AI}$	h_{fo} — Fouling factor on outside.
$U = \frac{\bar{h} \times h_{ie}}{\bar{h} + h_{ie}}$	h_{fi} — Fouling factor on inside.
$A = \frac{Q}{U\ (LMTD)_e}$	h_{oe} — effective convection coefficient on outside.
G = mass flow/Sec/frontal area	h_{ie} — effective convection coefficient on inside
Frontal area = L × NT × TP	AI — Inside tube area – π × IDL
	$\bar{h}$ — Outside convection coefficient referred to inside area.
	n_f — Fin efficiency.
	TP — Tube pitch
	NT — Number of tubes in a row.
	ID — Inner diameter.



FIN CONFIGURATION



Transverse-fin heat transfer

NUMBER OF TUBES PER SHELL FOR DIFFERENT TUBE SHEET LAYOUT

	Square Pitch Arrangement								*Triangular Pitch Arrangement*							
Tube ID, OD, mm	*19.0 25.4*		*25.4 31.0*		*31.0 39.7*		*38.1 47.6*		*19.0 25.4*		*25.4 31.0*		*31.0 39.7*		*38.1 47.6*	
Shell dia mm	*1P*	*2P*	*1P*	*2P*	*1P*	*2P*	*1P*	*2P*	*1P*	*2P*	*1P*	*2P*	*1P*	*2P*	*1P*	*2P*
203.2	32	26	21	16	—	—	—	—	37	30	21	16	—	—	—	—
254.0	52	52	32	32	16	12	—	—	61	52	32	32	20	18	—	—
304.8	81	76	48	45	30	24	16	16	92	82	55	52	32	30	18	34
336.6	97	90	61	56	32	30	22	22	109	106	68	66	38	36	27	22
387.4	137	124	81	76	44	40	29	29	151	138	91	86	54	51	36	34
438.2	177	166	112	112	56	53	39	39	203	196	131	118	69	66	48	44
489.0	224	220	138	132	78	73	50	48	262	250	163	152	95	91	61	58
539.8	277	270	177	166	96	90	62	60	316	302	199	188	117	112	76	72
590.6	341	324	213	208	127	112	78	74	384	376	241	232	140	136	95	91
635.0	413	394	260	252	140	135	94	90	470	452	294	282	170	164	115	110
685.8	481	460	300	288	166	160	112	108	559	534	349	334	202	196	136	131
736.6	553	526	341	326	193	188	131	127	630	604	397	376	235	228	160	154
787.4	657	640	406	398	226	220	151	146	745	728	472	454	275	270	184	177
838.2	749	718	465	460	258	252	176	170	856	830	538	522	315	305	215	206
889.0	845	824	522	518	293	287	202	196	970	938	608	592	357	348	246	238
939.8	934	914	596	574	334	322	224	220	1074	1044	674	664	407	390	275	268
990.6	1049	1024	665	644	370	362	252	246	1206	1176	766	736	449	436	307	299

P — number of passes

BASIC EQUATION FOR DIFFUSION COEFFICIENT

$$D_{AB} = \frac{0.04357\, T^{1.5}}{P[V_A^{0.333} + V_B^{0.333}]^2} \sqrt{\frac{1}{M_A} + \frac{1}{M_B}}$$

D_{AB} — Diffusion coefficient of material A into material B, m^2/s

T — Temperature, K

P — Pressure in Pascal

V_A, V_B — Atomic volume of A and B – refer table

M_A, M_B — Molecular mass of A and B

Material	*Atomic Volume*
Air	29.9
Carbon	14.8
Carbon Dioxide	34.0
Hydrogen	14.3
Nitrogen	15.6
Oxygen	7.40
Oxygen, in union with S, P, N	8.30
Oxygen, in acids	12.0
Water	18.8
Chlorine	21.6
Bromine	27.0
Iodine	37.0
Fluorine	8.70
Sulphur	25.6
Phosphorus	27.0

MASS TRANSFER

Conditions	*Correlation and Validity*	*Notations*
MOLECULAR DIFFUSION 1. Fick's Law—steady state equimolal counter diffusion of a component A into another component B (Solids, liquids, gases)	$\frac{N_a}{A} = -D_{ab}\frac{\partial C_a}{\partial y}$ $\frac{\dot{m}_a}{A} = -D_{ab}\frac{\partial \rho_a}{\partial y}$	$\frac{N_a}{A}$ = mole flux of diffusing component A in kg mole/m^2 s. $\frac{\dot{m}_a}{A}$ —mass flux of diffusing component A in kg/m^2 s. A —Area, m^2, normal to the direction of diffusion – y. C_a —concentration of component A per unit volume of mixture of components A and B. kg mole/m^3. When used with $\frac{N_a}{A}$ and kg/m^3 when used with $\dot{m}$/A. D_{ab} —diffusion coefficient when component A diffuses into component B, m^2/s. Refer p. 179 and 180.
2. Steady state equimolal counter diffusion between liquids along y direction $\frac{N_a}{A} = \frac{N_b}{A}$	$\frac{N_a}{A} = D_{ab}\frac{C_{a1} - C_{a2}}{y_2 - y_1}$ $\frac{\dot{m}_a}{A} = D_{ab}\frac{\rho_{a1} - C_{a2}}{y_2 - y_1}$	
3. Fick's law for **gases** (steady state equimolal counter diffusion) $N_a = N_b$	$\frac{\dot{m}_a}{A} = -D_{ab}\frac{1}{R_aT}\frac{dP_a}{dy}$	P_a, P_b partial pressures of components A and B in the gas mixture R_a —gas constant for component A R —universal gas constant T —Temperature in K P —Total pressure = $P_a + P_b$ P_b —Partial pressure of non-diffusing component P_{bm} —logarithmic mean partial pressure difference $(P_{b2} - P_{b1})/\ln(P_{b2}/P_{b1})$ ρ —density
4. Equimolal counter diffusion of gases	$\frac{N_a}{A} = -D_{ab}\cdot\frac{1}{RT}\frac{dP_a}{dy}$ $\frac{m_a}{A} = \frac{D_{ab}}{R_aT}\cdot\frac{P_{a1} - P_{a2}}{y_2 - y_1}$	
5. Steady state diffusion of component A into a stagnant component B (gas/vapour) $N_b = 0$	$\frac{\dot{m}_a}{A} = D_{ab}\frac{P}{R_aT.(y_2 - y_1)} \times \ln(P_{b2}/P_{b1})$ $= D_{ab}\cdot\frac{P}{R_aT.(y_2 - y_1)P_{bm}}$ Note : $P_{a1} - P_{a2} = P_{b2} - P_{b1}$	
6. Steady state diffusion of component A into a stagnant mixture of components B, C, etc.	$\frac{\dot{m}_a}{A} = D_{a.mix}\frac{P}{R_aT.(y_2 - y_1)} \times \ln\frac{P_{mix2}}{P_{mix1}}$	$D_{a.mix}$— diffusion coefficient when component A diffuses into a mixture of components B, C, D, etc.

Conditions	*Correlation and Validity*	*Notations*
7. Steady state diffusion of liquid A into stagnant liquid B. ($N_b = 0$)	$\frac{N_a}{A} = D_{a\,mix} \cdot \frac{\rho_{a1} - \rho_{a2}}{y_2 - y_1} \frac{C}{C_{bm}}$	$D_{a.mix} = \frac{1}{\frac{N_b}{D_{ab}} + \frac{N_C}{D_{ac}} + \frac{N_D}{D_{ad}} + \ldots}$
8. Diffusion through solid boundary (similar to conduction)	Plate $\frac{m_a}{A} = \frac{D_{ab}}{L} \cdot (\rho_{a1} - \rho_{a2})$ Hollow cylinder of length l, $\dot{m}_a = \frac{2\pi D_{ab} \cdot l(\rho_{a1} - \rho_{a2})}{\ln \frac{r_2}{r_1}}$ Sphere $\dot{m}_a = \frac{4\pi r_1 r_2(\rho_{a1} - \rho_{a2})}{(r_2 - r_1)}$	N_b, N_c, N_D mole fraction of component B,C, D in the mixture before diffussion. P — total pressure P_{mix} — sum of the partial pressure of components other than the diffusing component. $C = C_a + C_b$ $C_{bm} = (C_{b2} - C_{b1})/\ln(C_{b2}/C_{b1})$ $\dot{m}_a$ — mass diffusing rate ρ_{a1}, ρ_{a2} — concentration, kg/m^3
Transient Diffusion into a semi infinite solid.	**Note :** The charts, tables and equations used for transient conduction can be used with the following equivalents. $\frac{T - T_\infty}{T_i - T_\infty} = \frac{\rho_a - \rho_{a\infty}}{\rho_{ai} - \rho_{a\infty}}$ $\frac{\alpha\tau}{L^2} = \frac{D_{ab}\tau}{L^2}$ $\frac{hL}{k} = \frac{h_m L}{D_{ab}}$ $\frac{x}{2\sqrt{\alpha\tau}} = \frac{x}{2\sqrt{D_{ab}\tau}}$	$\rho_{a\infty}$ — concentration of component A in the free stream ρ_{ai} — initial concentration of component A h_m — convective mass transfer coefficient m/s defined through, $\frac{\dot{m}}{A} = h_m [\rho_{a1} - \rho_{a2}]$
9. Convective mass transfer : 9.1 External flow : Flat Plate : Laminar	**Note :** For situations where heat and mass transfer analogy is valid, the corresponding mass transfer correlations can be obtained by substituting Sh and Sc in the place of Nu and Pr. $\delta_{mx} = \delta_x \cdot Sc^{-0.333}$ $Sh_x = 0.332\, Re_x^{0.5}\, Sc^{0.333}$ $Sh = 0.664\, Re^{0.5}\, Sc^{0.333}$ $\frac{h_m}{u_\infty} Sc^{0.67} = \frac{0.322}{Re^{0.5}} = \frac{C_f}{2} = \frac{f}{8}$	D — diffusion coefficient, m^2/s δ_{mx} — mass transfer boundary layer thickness at x δ_x — hydrodynamic boundary layer thickness at x Sh_x — local sherwood number, $h_m x/D$ Sc — Schmidt number, $\mu/\rho D$, refer p. 181, 182, 183 Re_x — local Reynolds number Sh — average Sherwood number h_m — convective mass transfer coefficient. m/s. St_m — mass transfer Stanton Number = h_m/u_∞.
Turbulent	$\delta_m \simeq \delta_t \simeq \delta_h$	

Conditions	*Correlation and Validity*	*Notations*
Flat Plate Turbulent	$Sh_x = 0.0296\ Re_x^{0.8} \cdot Sc^{0.333}$ $0.6 < Sc < 3000$ $Sh = 0.037\ Re^{0.8}$ $5 \times 10^5 < Re < 10^8$ $0.6 < Sc < 3000$ Short laminar length	C_f —drag coefficient h_m —convective mass transfer coefficient, u_∞ —free stream velocity f —friction factor—equations for the factor are given in the convection chapter h —heat transfer coefficient, W/m^2K ρ —density, kg/m^3 c_p —specific heat at constant pressure, J/kg K L_e —Lewis Number = Sc/Pr = α/D α —thermal diffusivity, m^2/s h_{m1}—mass transfer coefficient from A to interface h_{m2}—mass transfer coefficient from interface to medium B H —Henry's constant (see tables) page 183
9.2 Combined-Laminar Turbulent flow	$Sh = (0.037\ Re^{0.8} - 871)\ Sc^{0.33}$ $\frac{h_m}{u_\infty} \cdot Sc^{0.67} = \frac{0.0286}{Re^{0.2}} = \frac{C_f}{2}$	
9.3 Internal flow Turbulent	$Sh = 0.023\ Re^{0.83}\ Sc^{0.44}$ $2000 < Re < 35000,$ $0.6 < Sc < 2.5$ $\frac{h_m}{u_\infty} \cdot Sc^{0.67} = \frac{f}{8}$, Rough pipes	
10. Simultaneous convective heat and mass transfer	$\frac{h}{h_m} = c_p \rho\ Le^{0.67}$	
11. Mass transfer through liquid gas interface	$\frac{1}{h_m} = \frac{1}{h_{m1}H_1} + \frac{1}{h_{m2}}$	
12. Packed beds	Refer packed beds under "CONVECTION".	

HUMIDIFICATION

Conditions	*Equation*	*Notation*
1. Water and air in equilibrium—air at constant temperature	$P_w - P_\infty = \frac{h}{h_{fg} h_m} (T_\infty - T_w)$ $T_\infty - T_w = \frac{h_{fg}\left[\frac{P_w}{T_w} - \frac{P_\infty}{T_\infty}\right]}{R_w \rho c_p Le^{0.67}}$ $T_\infty - T_w \simeq \frac{h_{fg}[P_w - P_\infty]}{R_w \rho c_p . Le^{0.67} T_f}$ $T_\infty - T_w = \frac{0.622 h_{fg}}{c_p Le^{0.67}} \left[\frac{P_w}{P} - \frac{P_\infty}{P}\right]$	P_w partial pressure of water vapour at wet bulb temperature, T_w P_∞ partial pressure of water vapour in air h convective heat transfer coefft. for air to water h_{fg} enthalpy of evaporation for water at temperature, T_w Y_w abs. humidity of air at temp. T_w Y_∞ abs. humidity of air at temp. T_∞ p total pressure T_∞ temperature of air (dry bulb) T_f —Mean temperature R_w —gas constant of water vapour. Y_a abs. humidity of air at the final equilibrium air temperature T_a, kg/kg Y_g abs. humidity of the initial air at the initial air temperature T_g c_p specific heat of air c_{pw} specific heat of water vapour Z height of tower G mass velocity of air per unit area kg/m²s h_{mg} gas phase mass transfer coefficient, kg/m²s a interfacial area per unit volume of tower packing, 1/m Y abs. humidity of air
2. – do –	$\frac{Y_w - Y_\infty}{T_a - T_w} = \frac{c_p}{h_{fg}} . Le^{0.67}.$	
3. Water and air in equilibrium, water at constant temperature	$Y_a - Y_g = \frac{1}{h_{fg}} [c_p + Y_g c_{pw}] [T_g - T_a]$	
4. Adiabatic humidification	$Z = \frac{G}{h_{mg}} \ln [(Y_a - Y_1)/(Y_a - Y_2)$	

HUMIDIFICATION (*Contd.*)

Conditions	*Equation*	*Notation*
5. Dehumidification	$h_l(T_i - T_l) = h_g(T_g - T_i) + h_{fg}\, h_{mg}(Y_g - Y_i)$	Y_1 humidity of air at entry to tower Y_2 humidity of air at exit of tower A total area for mass transfer = a s Z $\dot{m}$ mass flux per unit time s cross sectional area of tower a interfacial area unit volume h_l liquid phase heat transfer coefficient, W/m^2K h_g gas phase heat transfer coefficient, W/m^2K T_i temperature at the interface T_g bulk gas temperature (dry bulb) T_l liquid layer temperature Y_i abs. humidity at temperature T_i.

DIFFUSION COEFFICIENTS

Diffusing material, Solute	*Medium of Diffusion, Solvent*	*Temperature °C*	*Concentration of Solute, kg mole / m³*	*Diffusion Coefficient, D, m²/s*
Acetic acid	Water	12.5	0.01	0.9111×10^{-9}
Acetic acid	Water	12.5	1.0	0.8222×10^{-9}
Acetic acid	Water	18.0	1	0.9611×10^{-9}
Ammonia	Water	5	3.5	1.2389×10^{-9}
Ammonia	Water	15	1	1.7694×10^{-9}
Carbon dioxide	Water	10	$\simeq 0$	1.4611×10^{-9}
Carbon dioxide	Water	20	$\simeq 0$	1.7694×10^{-9}
Carbon dioxide	Ethanol	17	$\simeq 0$	3.1944×10^{-9}
Chlorine	Water	16	0.12	1.2611×10^{-9}
Chloroform	Ethanol	20	2	1.2500×10^{-9}
Copper	Aluminium	462	—	0.8472×10^{-9}
Ethanol	Water	10	0.05	0.8306×10^{-9}
Ethanol	Water	16	2	0.9000×10^{-9}
Ethanol	Water	10	3.75	0.5000×10^{-9}
Hydro chloric acid	Water	16	0.5	2.4416×10^{-9}
Hydro chloric acid	Water	0	2	1.8000×10^{-9}
Hydro chloric acid	Water	10	2.5	2.5000×10^{-9}
Hydro chloric acid	Water	0	9	2.7028×10^{-9}
Hydro chloric acid	Water	10	9	3.3056×10^{-9}
Mercury	Lead	177	—	0.1956×10^{-9}
Mercury	Lead	197	—	0.5000×10^{-9}
Methanol	Water	15	$\simeq 0$	1.2806×10^{-9}
n-Butanol	Water	15	$\simeq 0$	0.7722×10^{-9}
Sodium Chloride	Water	18	0.05	1.2611×10^{-9}
Sodium Chloride	Water	18	0.2	1.2083×10^{-9}
Sodium Chloride	Water	18	1	1.2389×10^{-9}
Sodium Chloride	Water	18	3	1.3611×10^{-9}
Sodium Chloride	Water	18	5.4	1.5417×10^{-9}

DIFFUSION COEFFICIENTS AND SCHMIDT NUMBER

Diffusing Component Solute	*Diffusion medium Solvent*	*Temperature °C*	*Diffusion Coefficient D, m^2/s.*	*Schmidt Number Sc.*
Air	Ethanol	0	10.19×10^{-6}	—
Air	*n*-Butanol	26	8.69×10^{-6}	—
Air	*n*-Butanol	59	10.19×10^{-6}	—
Air	Ethyl acetate	26	8.69×10^{-6}	—
Air	Ethyl acetate	59	10.39×10^{-6}	—
Air	Aniline	26	8.69×10^{-6}	—
Air	Aniline	59	10.61×10^{-6}	—
Air	Chlorobenzene	26	7.39×10^{-6}	—
Air	Chlorobenzene	59	9.00×10^{-6}	—
Air	Toluene	26	7.39×10^{-6}	—
Air	Toluene	59	9.00×10^{-6}	—
Ammonia	Air	0	21.60×10^{-6}	0.634
Benzene	Air	0	7.50×10^{-6}	1.83
Benzene	Carbhon dioxide	0	5.14×10^{-6}	1.37
Benzene	Hydrogen	0	29.44×10^{-6}	3.26
Carbon dioxide	Air	0	11.89×10^{-6}	1.14
Carbon dioxide	Hydrogen	18	60.56×10^{-6}	0.158
Carbon dioxide	Oxygen	0	18.47×10^{-6}	—
Carbon disulphide	Air	20	8.81×10^{-6}	1.68
Carbon monoxide	Oxgyen	0	18.50×10^{-6}	—
Ether	Air	20	7.69×10^{-6}	1.93
Ethyl alcohol	Air	0	10.11×10^{-6}	1.36
Ethyl alcohol	Air	40.3	11.81×10^{-6}	1.45
Hydrogen	Air	0	54.72×10^{-6}	0.25
Hydrogen	Oxygen	14	77.50×10^{-6}	0.182
Hydrogen	Nitrogen	12.5	73.89×10^{-6}	0.187
Hydrogen	Methane	0	62.50×10^{-6}	—
Mercury	Nitrogen	19	3250×10^{-6}	0.00424
Oxygen	Air	0	15.28×10^{-6}	0.895
Oxygen	Nitrogen	12	20.17×10^{-6}	0.621
Water	Air	8	20.58×10^{-6}	0.615
Water	Air	16	28.06×10^{-6}	0.488
Water	Air	26	25.83×10^{-6}	—
Water	Air	59	30.56×10^{-6}	—

SCHMIDT NUMBER OF VARIOUS SUBSTANCES at 20°C, S_c*

when in dilute solution in water, ethyl alcohol or benzene.†

Solute	*Solvent*	S_c*
Acetic acid	Water	1140
Acetic acid	Benzene	384
Acetylene	Water	645
Allyl alcohol	Water	1080
Ammonia	"	570
Bromine	"	840
Butyl alcohol	"	1310
Carbon dioxide	"	559
–do–	Ethyl alcohol	445
Chlorine	Water	824
Chloroform	Ethyl alcohol	1230
Chloroform	Benzene	350
Ethylene dichlorde	Benzene	301
Ethyl alcohol	Water	1005
Glycerol	"	1400
Hydrogen	"	196
Hydrogen Sulphide	"	712
Hydrochloric acid	"	381
Hydroquinone	"	1300
Lactose	"	2340
Manitol	"	1730
Methyl alcohol	"	785
Nitrogen	"	613
Nitric acid	"	390
Nitrous oxide	"	665
Oxygen	"	558
Phenol	"	1200
Phenol	Ethyl acohol	1900
Phenol	Benzene	479
Propyl alcohol	Water	1150
Pyrogallol	"	1440
Raffinose	"	2720
Resorcinol	"	1260
Sodium chloride	"	745
Sodium hydroxide	"	665
Sucrose	"	2230
Sulphuric acid	"	580
Urea	"	944
Urethane	"	1090

†Schmidt Number at any other temperature, may be found from the following relationship :

$$\frac{Sc}{Sc^*} = \left(\frac{\mu}{\mu^*}\right)^2 \left(\frac{\rho^*}{\rho}\right)\left(\frac{T^*}{T}\right)$$

where

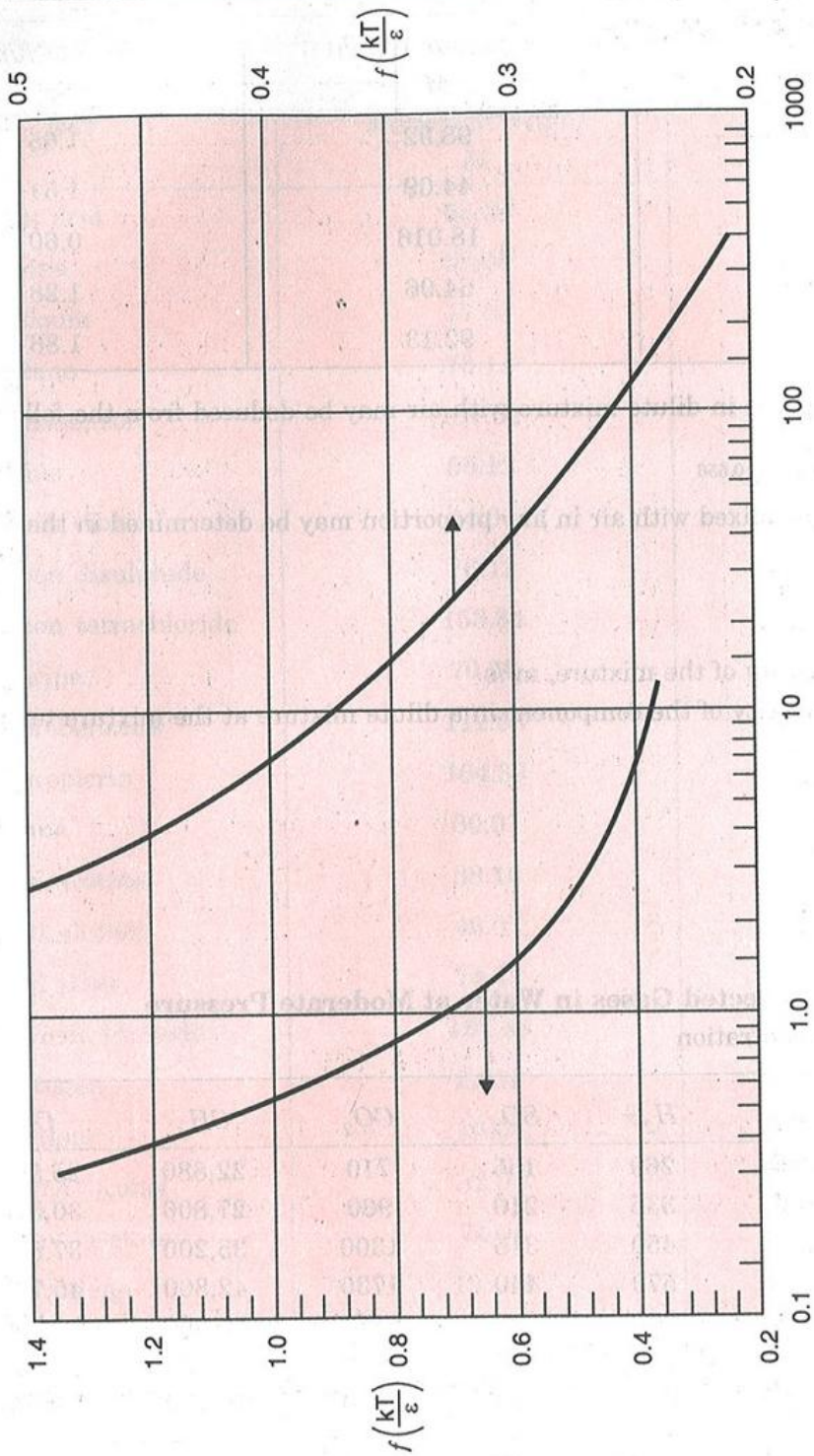
μ, absolute viscosity at absolute temperature T

ρ, density at absolute temperature T

ρ^*, density at 20°C

μ^*, absolute viscosity at 20°C

$T^* = 293$ K



Collision function for diffusion

UNIT CONVERSION CONSTANTS.

Quantity	*SI to Metric*	*Metric to SI*
Force	1 N = 0.1019 kg_f	1 kg_f = 9.81 N
Pressure	1 $N/m^2 = 10.19 \times 10^{-6}$ kg_f/cm^2	1 kg_f/cm^2 = 98135 N/m^2, (Pascal)
	1 bar = 1.0194 kg_f/cm^2	1 kg_f/cm^2 = 0.9814 bar
Energy	1 kJ = 0.2389 kcal	1 kcal = 4.186 kJ
(heat, work)	1 Nm (= 1J) = 0.1019 kg_f m	1 kg_f m = 9.81 Nm, (J)
	1 kW hr = 1.36 hp hr	1 hp hr = 0.736 kW hr
Power (metric)	1 W = 1.36×10^{-3} hp	1 hp = 736 W
Heat flow	1 W = 0.86 kcal/hr	1 kcal/hr = 1.163 W
Specific heat	1 kJ/kg K = 0.2389 kcal/kg °C	1 kcal/kg °C = 4.186 kJ/kg K
Surface Tension	1 N/m = 0.1019 kg_f/m	1 kg_f/m = 9.81 N/m
Thermal Conductivity	1 W/m K = 0.86 kcal/hr m °C	1 kcal/hr m °C = 1.163 W/m K
Convection Coefficient	1 W/m^2 K = 0.86 kcal/hr m^2 °C	1 kcal/hr m^2 °C = 1.163 W/m^2 K
Dynamic Viscosity	1 kg/ms, (Ns/m^2) = 0.1 Poise	1 Poise = 10 kg/ms, (Ns/m^2), Pa s
Kinematic Viscosity	1 m^2/s = 3600 m^2/hr,	1 $m^2/hr = 2.778 \times 10^{-4}$ m^2/s
	1 Stoke = 10^{-4} m^2/s	

Universal gas constant	= 8314.41 J/kg mol K = 847.54 mkg_f/kg mol K = 1.986 kcal/kg mol K
Gas Constant for Air	= 287 J/kg K, c_p = 1005 J/kg K = 0.24 kcal/kg K
Stefan-Boltzmann constant	= 5.67×10^{-8} W/m^2K^4 = 4.876×10^{-8} kcal/hr m^2 K^4

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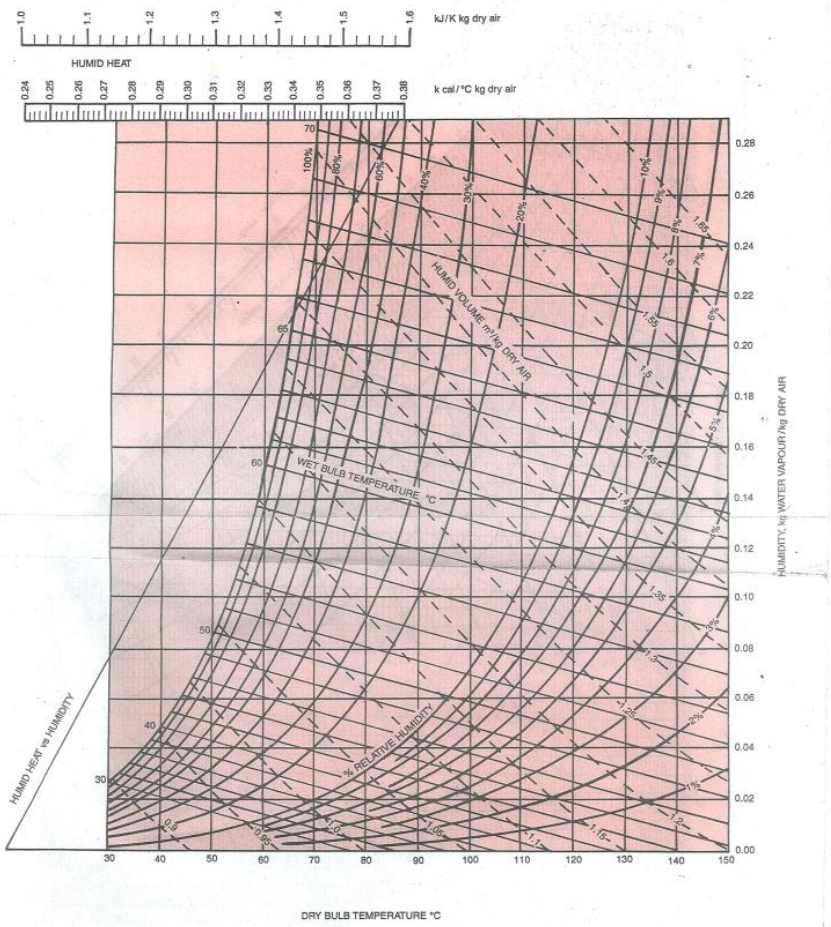
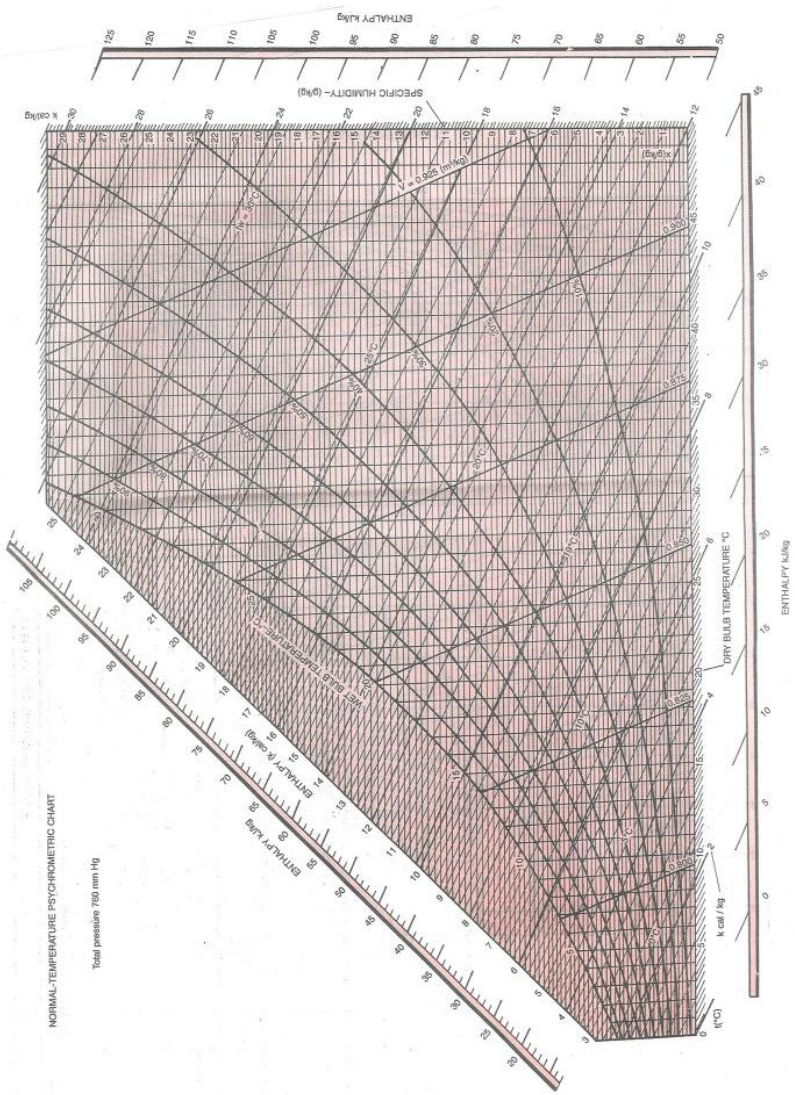


HIGH TEMPERATURE PSYCHROMETRIC CHART

(Courtesy : ATIRA, Ahmedabad)



NORMAL-TEMPERATURE PSYCHROMETRIC CHART

Total pressure 760 mm Hg

Heat and Mass Transfer Data Book

The aim of this book is to present to the students, teachers and practising engineers, a comprehensive collection of various material property data and formulae in the field of heat and mass transfer. The material is organized in such a way that a reader who has gone through the engineering curriculum could easily use the formulae and data presented in heat transfer calculations. Hence, this compilation is primarily intended as an adjunct to a standard text.

The data book devotes considerable space to the property values of materials—solids, liquids and gases—that are commonly used in heat transfer situations. Property values for various materials at different temperatures are given for the use of designers.

The formulae for conduction, convection, radiation, boiling, condensation, freezing, melting, heat exchangers and mass transfer are arranged in an easily usable tabular form with symbols and units explained alongside. The limitations and restrictions in the use of empirical relationships are also mentioned alongside. The empirical formulae and charts have been selected.

Suggestions received since the appearance of the fifth edition have been incorporated, as far as possible, in the new edition. A number of charts and data have been added to enhance the value of the book. The presentation on convection has been enlarged, taking into account the recent publications. This book is a comprehensive collection of heat transfer information in SI units for students and practitioners.

Dr. C.P. Kothandaraman, former Head of the Department of Mechanical Engineering at the PSG College of Technology, Coimbatore had his education at College of Engineering, Guindy, Chennai and Michigan State University, USA. He had been on the faculty of Mechanical Engineering of the PSG College of Technology during 1957 to 1992. He serves as a consultant to several industries in the field of design of heat exchangers and heaters. He has to his credit books in the field of Thermal Engineering, Heat Transfer and Fluid Mechanics.

Dr. S. Subramanyan, former Principal, PSG College of Technology and former Vice Chancellor, Bharathiar University, Coimbatore had his education at PSG College of Technology, Coimbatore, Imperial College, London and Manchester Institute of Science and Technology. He had been a post doctoral Fellow at the University of Kingston and University of Alberta. He had been on the faculty of PSG College of Technology from 1959 to 1994. He also served PSG College of Technology as Controller of Examinations and later as Registrar for a few years. He has considerable experience in teaching subjects related to Thermal Engineering including Heat Transfer. At present he serves as Advisor for several engineering institutions.

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