

# SSY190: Homework 1

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## 1 INTRODUCTION

Here, a PID controller is to be implemented on the plant. The transfer function of the plant is given by equation (1.1) and the controller by equation (1.2) as follows:

$$G(s) = \frac{K}{1 + sT} \quad (1.1)$$

$$F(s) = K_p + \frac{K_i}{s} + \frac{K_d s}{1 + T_f s} \quad (1.2)$$

Where,  $K$  and  $T$  are the plant parameters and the  $K_p$ ,  $K_i$ ,  $K_d$ ,  $T_f$  are the controller parameters.

1.1 is the block diagram plant with controller.

## 2 DISCRETIZATION

Discretization is to be performed in order to process the real time data on the processor. Both plant and controller are discretized using the sampling time  $h$ .

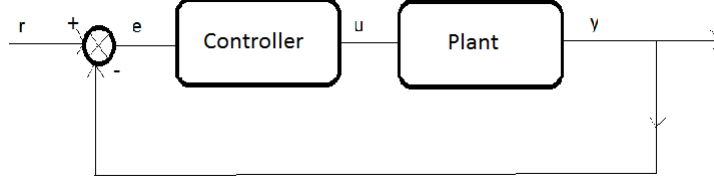


Figure 1.1: Block Diagram of the plant

## 2.1 ZERO ORDER HOLD

The plant is discretized by using the zero order hold. Zero order hold for following continuous time transfer function is given as below.

$$K \frac{a}{a + S} \rightarrow K \frac{(1 - e^{-ah})z^{-1}}{1 - e^{-ah}z^{-1}} \quad (2.1)$$

Using equation (2.1) with some algebraic manipulation, we obtain the following discretized transfer function for the plant.

$$\frac{y}{x} = G(z) = K \frac{(1 - e^{-h/T})z^{-1}}{1 - e^{-h/T}z^{-1}} \quad (2.2)$$

Using discrete time transfer function in (2.2), the following difference equation is obtained showing relation between the input and output of the plant.

$$y(n) = e^{-h/T} y(n-1) + K(1 - e^{-h/T})x(n-1) \quad (2.3)$$

## 2.2 TUSTIN/BILINEAR TRANSFORMATION

The controller is discretized using Tustin bilinear transformation. In this transformation, we replace the 's' in the continuous transfer function by following function in 'z'.

$$s = \frac{2}{T_s} \frac{z - 1}{z + 1} \quad (2.4)$$

We obtain  $F(z)$  using (1.2) and (2.4). Difference equation for the plant and the controller is obtained using  $F(z) = \frac{u}{e}$  as shown in 1.1. Simplified difference equation is given below.

$$\begin{aligned} u(n) = & -(\alpha - 1)u(n-1) + \alpha u(n-2) + (a_0 + T_s K_i + \beta(1 + \alpha^{-1}))e(n) \\ & + (a_0(\alpha - 1) + T_s K_i \alpha - \beta(1 + \alpha^{-1}))e(n-1) \\ & - \alpha a_0 e(n-2) \end{aligned} \quad (2.5)$$

Where,  $\alpha = \frac{T_s - 2T_f}{T_s + 2T_f}$ ,  $\beta = \frac{2K_d}{T_s + 2T_f}$ ,  $a_0 = K_p - \frac{T_s K_i}{2} - \frac{\beta}{\alpha}$  are simplified constants.  $e$  is the feedback error and  $u$  is the control input.

Once we obtain the difference equations, we can implement the system by defining initial conditions.

$K_p$	9.0
$K_d$	6.0
$K_i$	5.0
$T_f$	2.0
$h$	0.1
$T$	3.0
$K$	4.0

Table 3.1: System and controller parameter values

### 3 IMPLEMENTATION IN C

#### 3.1 SYSTEM PARAMETERS AND INITIALIZATION

Since there was no specification, tuning was performed to achieve reference point. These parameters along with the assumed system parameters are given below: All parameters at  $t < 0$  are set to 0 (refer to code). Also, initial output was set to 0. After running the simulation for the above values a significant reference tracking was achieved.