

# The role of viscosity on drop impact forces

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A liquid drop impacting a rigid substrate undergoes deformation and spreading due to normal reaction forces, which are counteracted by surface tension. On a non-wetting substrate, the drop subsequently retracts and takes off. Our recent work (Zhang et al., *Phys. Rev. Lett.*, vol. 129, 2022, 104501) revealed two peaks in the temporal evolution of the normal force  $F(t)$  – one at impact and another at jump-off. The second peak coincides with a Worthington jet formation, which vanishes at high viscosities due to increased viscous dissipation affecting flow focusing. In this article, using experiments, direct numerical simulations, and scaling arguments, we characterize both the peak amplitude  $F_1$  at impact and the one at take off ( $F_2$ ) and elucidate their dependency on the control parameters: the Weber number  $We$  (dimensionless impact velocity) and the Ohnesorge number  $Oh$  (dimensionless viscosity). The first peak amplitude  $F_1$  and the time  $t_1$  to reach it depend on inertial timescales for low viscosity liquids, remaining nearly constant for viscosities up to 100 times that of water. For high viscosity liquids, we balance the rate of change in kinetic energy with viscous dissipation to obtain new scaling laws:  $F_1/F_\rho \sim \sqrt{Oh}$  and  $t_1/\tau_\rho \sim 1/\sqrt{Oh}$ , where  $F_\rho$  and  $\tau_\rho$  are the inertial force and time scales, respectively, which are consistent with our data. The time  $t_2$  at which the amplitude  $F_2$  appears is set by the inertia-capillary timescale  $\tau_\gamma$ , independent of both the viscosity and the impact velocity of the drop. However, these properties dictate the magnitude of this amplitude.

**Key words:**

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## 1. Introduction

Drop impacts have piqued the interest of scientists and artists alike for centuries, with the phenomenon being sketched by da Vinci (1508) in the early 16<sup>th</sup> and photographed by Worthington (1876a,b) in the late 19<sup>th</sup> century. It is, indeed, captivating to observe raindrops hitting a solid surface (Kim et al. 2020; Lohse & Villermaux 2020) or ocean spray affecting maritime structures (Berny et al. 2021; Villermaux et al. 2022). The phenomenology of drop impact is extremely rich, encompassing behaviors such as drop

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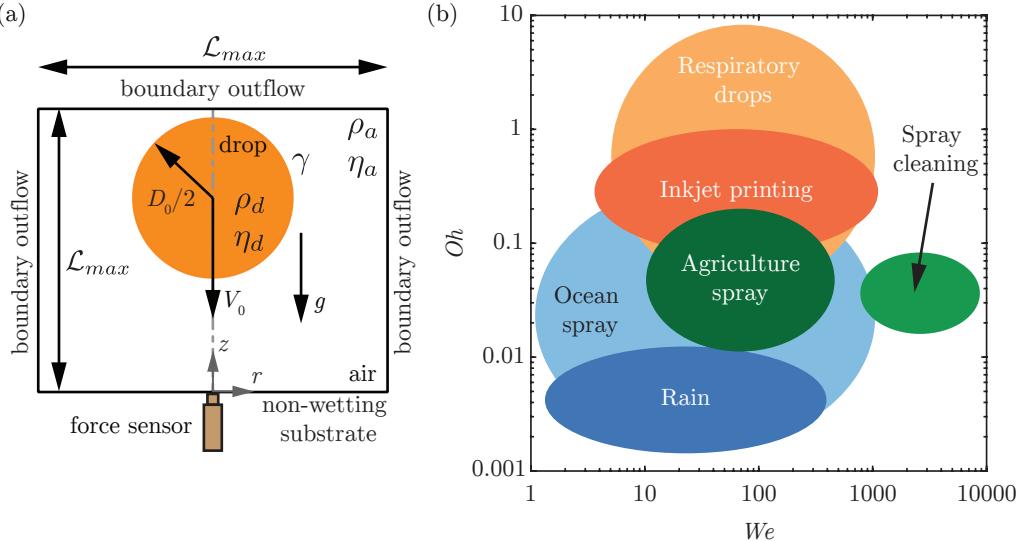


FIGURE 1. (a) Problem schematic with an axisymmetric computational domain used to study the impact of a drop with diameter  $D_0$  and velocity  $V_0$  on a non-wetting substrate. In the experiments, we use a quartz force sensor to measure the temporal variation of the impact force. The subscripts  $d$  and  $a$  denote the drop and air, respectively, to distinguish their material properties, which are the density  $\rho$  and the dynamic viscosity  $\eta$ . The drop-air surface tension coefficient is  $\gamma$ . The grey dashed-dotted line represents the axis of symmetry,  $r = 0$ . Boundary air outflow is applied at the top and side boundaries (tangential stresses, normal velocity gradient, and ambient pressure are set to zero). The domain boundaries are far enough from the drop not to influence its impact process ( $L_{\max} \gg D_0$ ,  $L_{\max} = 8R$  in the worst case). (b) The phase space with control parameters: the Weber number ( $We$ : dimensionless impact velocity) and the Ohnesorge number ( $Oh$ : dimensionless viscosity), exemplifying different applications.

deformation (Biance *et al.* 2006; Moláček & Bush 2012; Chevy *et al.* 2012), spreading (Laan *et al.* 2014; Wildeman *et al.* 2016), splashing Xu *et al.* (2005); Riboux & Gordillo (2014); Thoraval *et al.* (2021), fragmentation (Villermaux & Bossa 2011; Villermaux 2020), bouncing (Richard & Quéré 2000; Kolinski *et al.* 2014; Jha *et al.* 2020; Chubytsky *et al.* 2020; Sharma & Dixit 2021; Sanjay *et al.* 2023a), and wetting (de Gennes 1985; Fukai *et al.* 1995; Quéré 2008; Bonn *et al.* 2009). These behaviors are influenced by the interplay of inertial, capillary, and viscous forces, as well as additional factors like non-Newtonian properties (Bartolo *et al.* 2005, 2007; Smith & Bertola 2010; Gorin *et al.* 2022) of the liquid and even ambient air pressure (Xu *et al.* 2005), making the parameter space for this phenomenon both extensive and high-dimensional.

Naturally, even the process of a Newtonian liquid drop impacting a rigid substrate is governed by a plethora of control parameters, including but not limited to the drop's density  $\rho_d$ , diameter  $D_0$ , velocity  $V_0$ , dynamic viscosity  $\eta_d$ , surface tension  $\gamma$ , and acceleration due to gravity  $g$  (figure 1a). To navigate this rich landscape, we focus on two main dimensionless numbers that serve as control parameters (figure 1b): the Weber number  $We$ , which is the ratio of inertial to capillary forces and is given by

$$We = \frac{\rho_d V_0^2 D_0}{\gamma}, \quad (1.1)$$

and the Ohnesorge number  $Oh$ , which captures the interplay between viscous damping

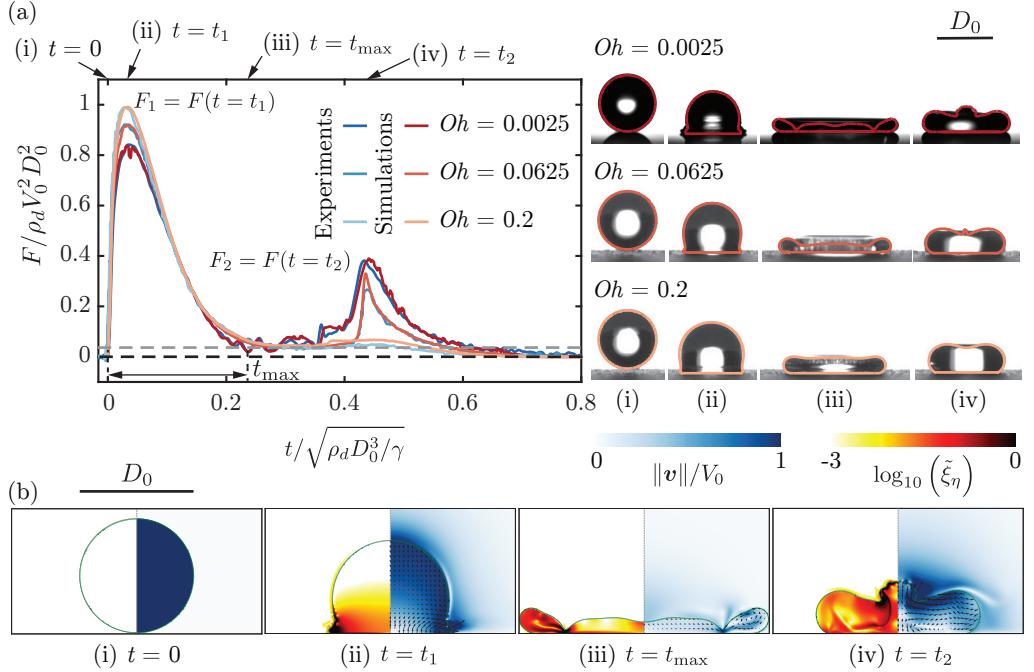


FIGURE 2. Comparison of the drop impact force  $F(t)$  obtained from experiments and simulations for the three typical cases with impact velocity  $V_0 = 1.2 \text{ m/s}, 0.97 \text{ m/s}, 0.96 \text{ m/s}$ , diameter  $D_0 = 2.05 \text{ mm}, 2.52 \text{ mm}, 2.54 \text{ mm}$ , surface tension  $\gamma = 72 \text{ mN/m}, 61 \text{ mN/m}, 61 \text{ mN/m}$  and viscosity  $\eta_d = 1 \text{ mPa s}, 25.3 \text{ mPa s}, 80.2 \text{ mPa s}$ . These parameter give  $Oh = 0.0025, 0.0625, 0.2$  and  $We = 40$ . For the three cases, the two peak amplitudes,  $F_1/\rho_d V_0^2 D_0^2 \approx 0.82, 0.92, 0.99$  at  $t_1 \approx 0.03\sqrt{\rho_d D_0^3/\gamma}$  and  $F_2/\rho_d V_0^2 D_0^2 \approx 0.37, 0.337, 0.1$  at  $t_2 \approx 0.42\sqrt{\rho_d D_0^3/\gamma}$ , characterize the inertial shock from impact and the Worthington jet before takeoff, respectively. The drop reaches the maximum spreading at  $t_{\max}$  when it momentarily stops and retracts until  $0.8\sqrt{\rho_d D_0^3/\gamma}$  when the drop takes off ( $F = 0$ ). The black and gray dashed lines in panel (a) mark  $F = 0$  and the resolution  $F = 0.5 \text{ mN}$  of our piezoelectric force transducer, respectively. (b) Four instances are further elaborated through numerical simulations for ( $We = 40, Oh = 0.0025$ ), namely (i)  $t = 0 \text{ ms}$  (touch-down), (ii)  $t = 0.37 \text{ ms}$  ( $t_1$ ), (iii)  $t = 2.5 \text{ ms}$  ( $t_{\max}$ ), and (iv)  $t = 4.63 \text{ ms}$  ( $t_2$ ). The insets of panel (a) exemplify these four instances for the three representative cases illustrated here. The experimental snapshots are overlaid with the drop boundaries from simulations. We stress the excellent agreement between experiments and simulations without any free parameters. The left part of each numerical snapshot shows the dimensionless local viscous dissipation function  $\tilde{\xi}_\eta \equiv \xi_\eta D_0 / (\rho_d V_0^3) = 2Oh (\tilde{\mathcal{D}} : \tilde{\mathcal{D}})$ , where,  $\mathcal{D}$  is the symmetric part of the velocity gradient tensor, on a  $\log_{10}$  scale and the right part the velocity field magnitude normalized with the impact velocity. The black velocity vectors are plotted in the center of mass reference frame of the drop to clearly elucidate the internal flow. Also see supplementary videos SM1-SM3.

and capillary oscillations, offering insights into how viscosity affects the drop's behavior upon impact,

$$Oh = \frac{\eta_d}{\sqrt{\rho_d \gamma D_0}}. \quad (1.2)$$

Additionally, the Bond number

$$Bo = \frac{\rho_d g D_0^2}{\gamma} \quad (1.3)$$

57 compares gravity to inertial forces and is needed to uniquely define the non-dimensional  
 58 problem.

59 The drop impact is not only interesting from the point of view of fundamental research  
 60 but also finds relevance in inkjet printing (Lohse 2022), the spread of respiratory drops  
 61 carrying airborne microbes (Bourouiba 2021; Ji *et al.* 2021; Pöhlker *et al.* 2023), cooling  
 62 applications (Kim 2007; Shiri & Bird 2017; Jowkar & Morad 2019), agriculture (Bergeron  
 63 *et al.* 2000; Bartolo *et al.* 2007; Kooij *et al.* 2018; Sijs & Bonn 2020; He *et al.* 2021;  
 64 Hoffman *et al.* 2021), criminal forensics (Smith *et al.* 2018; Smith & Brutin 2018), and  
 65 many other industrial and natural processes (Rein 1993; Yarin 2006; Tuteja *et al.* 2007;  
 66 Cho *et al.* 2016; Josserand & Thoroddsen 2016; Yarin *et al.* 2017; Liu *et al.* 2017; Hao  
 67 *et al.* 2016; Yarin *et al.* 2017; Wu *et al.* 2020). For these applications, it is pertinent to  
 68 understand the forces involved in drop impacts, as these forces can lead to soil erosion  
 69 (Nearing *et al.* 1986) or damage to engineered surfaces (Ahmad *et al.* 2013; Amirzadeh  
 70 *et al.* 2017; Gohardani 2011). We refer the readers to Cheng *et al.* (2022) for an overview  
 71 of the recent studies unraveling drop impact forces; see also Li *et al.* (2014); Soto *et al.*  
 72 (2014); Philippi *et al.* (2016); Zhang *et al.* (2017); Gordillo *et al.* (2018); Mitchell *et al.*  
 73 (2019); Zhang *et al.* (2019).

74 These forces have been studied by Zhang *et al.* (2022), employing experiments and  
 75 simulations and deriving scaling laws. A liquid drop impacting a non-wetting substrate  
 76 (figure 2i-vi) undergoes a series of phases—spreading, recoiling, and potentially rebounding  
 77 (Chantelot 2018)—driven by the normal reaction force exerted by the substrate. The  
 78 moment of touch-down (figure 2i-ii) (Wagner 1932; Philippi *et al.* 2016; Gordillo *et al.*  
 79 2018) is not surprisingly associated with a pronounced peak in the temporal evolution of  
 80 the drop impact force  $F(t)$  owing to the sudden deacceleration as high as 100 times the  
 81 acceleration due to gravity (Clanet *et al.* 2004) (figure 2,  $F(t = 0.37\text{ ms}) \approx 5.1\text{ mN}$ ). The  
 82 force diminishes as the drop reaches its maximum spreading diameter (figure 2iii). Zhang  
 83 *et al.* (2022) revealed that also the jump-off is accompanied by a peak in the normal  
 84 reaction force, which was up to then unknown (figure 2,  $F_2(t_2 = 4.63\text{ ms}) \approx 2.3\text{ mN}$   
 85 for the second force peak amplitude—at time  $t_2$  after impact). The second peak in the  
 86 force also coincides with the formation of a Worthington jet, a narrow upward jet of  
 87 liquid that can form due to flow focusing by the retracting drop (figure 2iv-vi). Under  
 88 certain conditions ( $We \approx 9$ ), this peak can be even more pronounced than the first. This  
 89 discovery is critical for superhydrophobicity which is volatile and can fail due to external  
 90 disturbances such as pressure (Lafuma & Quéré 2003; Callies & Quéré 2005; Sbragaglia  
 91 *et al.* 2007; Li *et al.* 2017), evaporation (Tsai *et al.* 2010; Chen *et al.* 2012; Papadopoulos  
 92 *et al.* 2013), mechanical vibration (Bormashenko *et al.* 2007), or the impact forces of  
 93 prior droplets (Bartolo *et al.* 2006a).

94 In contrast to our prior study Zhang *et al.* (2022), which fixed the Ohnesorge number  
 95 to that of a 2 mm diameter water drop ( $Oh = 0.0025$ ), our present investigation reported  
 96 in this paper explores a broader parameter space. We systematically and independently  
 97 vary the Weber and Ohnesorge numbers, extending the range of  $Oh$  to as high as 100.  
 98 This comprehensive approach enables us to develop new scaling laws and provides a  
 99 more unified understanding of the forces involved in drop impact problems. Our findings  
 100 are particularly relevant for applications with varying viscosities and impact velocities  
 101 (figure 1).

102 The structure of this paper is as follows: §2 briefly describes the experimental and  
 103 numerical methods. §3 and §4 offer detailed analyses of the first and second peaks,  
 104 respectively, focusing on their relationships with the Weber number ( $We$ ) and the  
 105 Ohnesorge number ( $Oh$ ). Conclusions and perspectives for future research are presented  
 106 in Section 5.

glycerol (wt %)	$\rho_d$ (kg/m <sup>3</sup> )	$\eta_d$ (mPa.s)	$\gamma$ (mN/m)
0	1000	1	72
50	1124	5	61
63	1158	10	61
74	1188	25.3	61
80	1200	45.4	61
85	1220	80.2	61

TABLE 1. Properties of the water-glycerol mixtures used in the experiments.  $\rho_d$  and  $\eta_d$  are the density and viscosity of the drop, respectively and  $\gamma$  denotes the liquid-air surface tension coefficient. These properties are calculated using the protocol provided in Cheng (2008); Volk & Kähler (2018).

## 2. Methods

### 2.1. Experimental method

In the experimental setup, shown schematically in figure 1(a), a liquid drop impacts a superhydrophobic substrate. For water drops, such a surface is coated with silanized silica nanobeads with a diameter of 20 nm (Glaco Mirror Coat Zero; Soft99) resulting in the advancing and receding contact angles of  $167 \pm 2^\circ$  and  $154 \pm 2^\circ$ , respectively (Gauthier *et al.* 2015; Li *et al.* 2017). On the other hand, for viscous aqueous glycerin drops, the upper surface is coated with an acetone solution of hydrophobic beads (Ultra ever Dry, Ultratech International, a typical bead size of 20 nm), resulting in the advancing and receding contact angles of  $166 \pm 4^\circ$  and  $159 \pm 2^\circ$ , respectively (Jha *et al.* 2020). The properties of the impacting drop are controlled using water-glycerol mixtures with viscosities  $\eta_d$  varying by almost two orders of magnitude, from 1 mPas to 80.2 mPas. Surface tension is either 72, mN/m (pure water) or 61, mN/m (glycerol), while density  $\rho_d$  ranges from 1000, kg/m<sup>3</sup> to 1220, kg/m<sup>3</sup>, as detailed in table 1 (Cheng 2008; Volk & Kähler 2018; Jha *et al.* 2020). We note that using liquids such as silicone oil can provide a broader range of viscosity variation when paired with a superamphiphobic substrate (Deng *et al.* 2012). Additionally, employing drops of smaller radii facilitates the exploration of higher Ohnesorge numbers ( $Oh$ , see (1.2)). The drop diameter  $D_0$  is controlled between 2.05 mm and 2.76 mm by pushing it through a calibrated needle (see appendix A for details). Consequently, we calculate  $Oh$  using the properties in table 1. The Weber number ( $We$ , see (1.1)) is set using the impact velocity  $V_0$  varying between 0.38 m/s and 2.96 m/s by changing the release height of the drops above the substrate. All experiments are conducted at ambient pressure and temperature. The impact force is directly measured using a high-precision piezoelectric force transducer (Kistler 9215A) with a resolution of 0.5 mN. During these measurements, the high-frequency vibrations induced by the measurement system and the surrounding noise are spectrally removed using a low pass filter with a cut-off frequency of 5 kHz, following the procedure in Li *et al.* (2014); Zhang *et al.* (2017); Gordillo *et al.* (2018); Mitchell *et al.* (2019). The experiment also employs a high-speed camera (Photron Fastcam Nova S12) synchronized at 10,000 fps with a shutter speed 1/20,000 s. Throughout the manuscript, the error bars account for repeated trials and are visible if they are larger than the marker size. We refer the readers to the supplementary material of Zhang *et al.* (2022) and appendix A for further details of the experimental setup and error characterization of the dimensionless control parameters, respectively.

R2

R2

141                   2.2. Numerical framework

142                   In the direct numerical simulations (DNS) employed for this study, the continuity and  
 143                   the momentum equations take the form

$$\nabla \cdot \mathbf{v} = 0 \quad (2.1)$$

144                   and

$$\frac{\partial \mathbf{v}}{\partial t} + \nabla \cdot (\mathbf{v} \mathbf{v}) = \frac{1}{\rho} (-\nabla p + \nabla \cdot (2\eta \mathcal{D}) + \mathbf{f}_\gamma) + \mathbf{g}, \quad (2.2)$$

145                   respectively. Here,  $\mathbf{v}$  is the velocity field,  $t$  is time,  $p$  is pressure, and  $\mathbf{g}$  is acceleration  
 146                   due to gravity. We use the free software program *Basilisk C* that employs the well-  
 147                   balanced geometric volume of fluid (VoF) method (Popinet 2009, 2018). The VoF tracer  
 148                    $\Psi$  delineates the interface between the drop (subscript  $d$ ,  $\psi = 1$ ) and air (subscript  $a$ ,  
 149                    $\psi = 0$ ), introducing a singular force  $\mathbf{f}_\gamma \approx \gamma\kappa\nabla\Psi$  ( $\kappa$  denotes interfacial curvature, see  
 150                   Brackbill *et al.* 1992) to respect the dynamic boundary condition at the interface. This  
 151                   VoF tracer sets the material properties such that density  $\rho$  and viscosity  $\eta$  are given by

$$\rho = \rho_a + (\rho_d - \rho_a)\Psi \quad (2.3)$$

152                   and

$$\eta = \eta_a + (\eta_d - \eta_a)\Psi, \quad (2.4)$$

153                   respectively. This VoF field is advected with the flow, following the equation

$$\frac{\partial \Psi}{\partial t} + \nabla \cdot (\mathbf{v}\Psi) = 0. \quad (2.5)$$

154                   Lastly, we calculate the normal reaction force  $\mathbf{F}(t)$  by integrating the pressure field  $p$  at  
 155                   the substrate,

$$\mathbf{F}(t) = \left( \int_{\mathcal{A}} (p - p_0) d\mathcal{A} \right) \hat{\mathbf{z}}, \quad (2.6)$$

156                   where,  $p_0$ ,  $d\mathcal{A}$ , and  $\hat{\mathbf{z}}$  are the ambient pressure, substrate area element, and the unit  
 157                   vector normal to the substrate, respectively.

158                   We leverage the axial symmetry of the drop impact (figure 1a). This axial symmetry  
 159                   breaks at large  $We$  ( $\geq 100$  for water drops and even larger Weber number for more  
 160                   viscous drops), owing to destabilization by the surrounding gas after splashing (Xu *et al.*  
 161                   2005; Eggers *et al.* 2010; Driscoll & Nagel 2011; Riboux & Gordillo 2014; Josserand &  
 162                   Thoroddsen 2016; Zhang *et al.* 2022). To solve the governing equations (2.1)-(2.5), the  
 163                   velocity field  $\mathbf{v}$  and time  $t$  are normalized by the inertio-capillary scales,  $V_\gamma = \sqrt{\gamma/\rho_d D_0}$   
 164                   and  $\tau_\gamma = \sqrt{\rho_d D_0^3/\gamma}$ , respectively. Furthermore, the pressure is normalized using the  
 165                   capillary pressure scale  $p_\gamma = \gamma/D_0$ . In such a conceptualization,  $Oh$  and  $We$  described in  
 166                   §1 uniquely determine the system. The Ohnesorge number based on air viscosity  $Oh_a =$   
 167                    $(\eta_a/\eta_d)Oh$  and air-drop density ratio  $\rho_a/\rho_d$  are fixed at  $10^{-5}$  and  $10^{-3}$ , respectively  
 168                   to minimize the influence of the surrounding medium on the impact forces. Lastly, we R2  
 169                   keep the Bond number ( $Bo$ , see (1.3)) fixed at 1 throughout the manuscript. In our

system, the relevance of gravity is characterized by the dimensionless Froude number  $Fr = V_0^2/gD_0 = We/Bo$  comparing inertia with gravity. Throughout this manuscript,  $Fr > 1$  and gravity's role is sub-dominant compared to inertia (for detailed discussion, see appendix B). The substrate is modeled as a no-slip and non-penetrable wall, whereas vanishing stress and pressure are applied at the remaining boundaries to mimic outflow conditions for the surrounding air. The domain boundaries are far enough from the drop not to influence its impact process ( $\mathcal{L}_{\max} \gg D_0$ ,  $\mathcal{L}_{\max} = 8R$  in the worst case). At  $t = 0$ , in our simulations, we release a spherical drop whose south pole is  $0.05D_0$  away from the substrate and is falling with a velocity  $V_0$ . It is important to note that experimental drops may deviate from perfect sphericity due to air drag post-needle release and potential residual oscillations from detachment. These shape perturbations are more pronounced in cases with low Weber and Ohnesorge numbers. To quantify this non-sphericity, we measure the drop's aspect ratio (horizontal to vertical diameter) immediately before substrate contact. The precise pre-impact drop shape can significantly influence subsequent impact dynamics (Thoraval *et al.* 2013; Yun 2017; Zhang *et al.* 2019). In our experiments, we constrain our analysis to drops with aspect ratios between 0.96 and 1.05. Given this narrow range, we posit that the impact of these shape variations is negligible compared to the experimental error bars derived from repeated trials under identical nominal conditions. The simulations utilize adaptive mesh refinement to finely resolve the velocity, viscous dissipation, and the VoF tracer fields. A minimum grid size  $\Delta = D_0/2048$  is used for this study.

To ensure a perfectly non-wetting surface, we impose a thin air layer (minimum thickness  $\sim \Delta/2$ ) between the drop and the substrate. This air layer prevents direct contact between the liquid and solid (Kolinski *et al.* 2014; Sprittles 2024), effectively mimicking a perfectly non-wetting surface. The presence of this air layer is crucial for capturing the dynamics of drop impact on superhydrophobic surfaces, as it allows for the formation of an air cushion that can significantly affect the spreading and rebound behavior of the drop (Ramírez-Soto *et al.* 2020; Sanjay *et al.* 2023a). While this approach does not fully resolve the microscopic dynamics within the air layer itself, such as the high-velocity gradients and viscous dissipation inside the gas film once it thins below a critical size ( $\sim 10\Delta$ ), it has been shown to accurately capture the macroscopic behavior of drop impact in the parameter range of interest (Ramírez-Soto *et al.* 2020; Sanjay *et al.* 2023b; Alventosa *et al.* 2023a; García-Geijo *et al.* 2024). We refer the readers to Sanjay (2022) for discussions about this “precursor”, air film method and to Popinet & collaborators (2013–2023); Sanjay (2023); Zhang *et al.* (2022) for details on the numerical framework.

### 3. Anatomy of the first impact force peak

This section elucidates the anatomy of the first impact force peak and its relationship with the Weber  $We$  and Ohnesorge  $Oh$  numbers, first for the inertial limit (§3.1,  $Oh \ll 1$ ) and then for the viscous asymptote (§3.2,  $Oh \gg 1$ ). The results of this section are summarized in figure 3 that shows an excellent agreement between experiments and simulations without any free parameters.

#### 3.1. Low Ohnesorge number impacts

For low  $Oh$  and large  $We$ , inertial force and time scales dictate the drop impact dynamics (figures 3 and 4). As the drop falls on a substrate, the part of the drop immediately in contact with the substrate stops moving, whereas the top of the drop

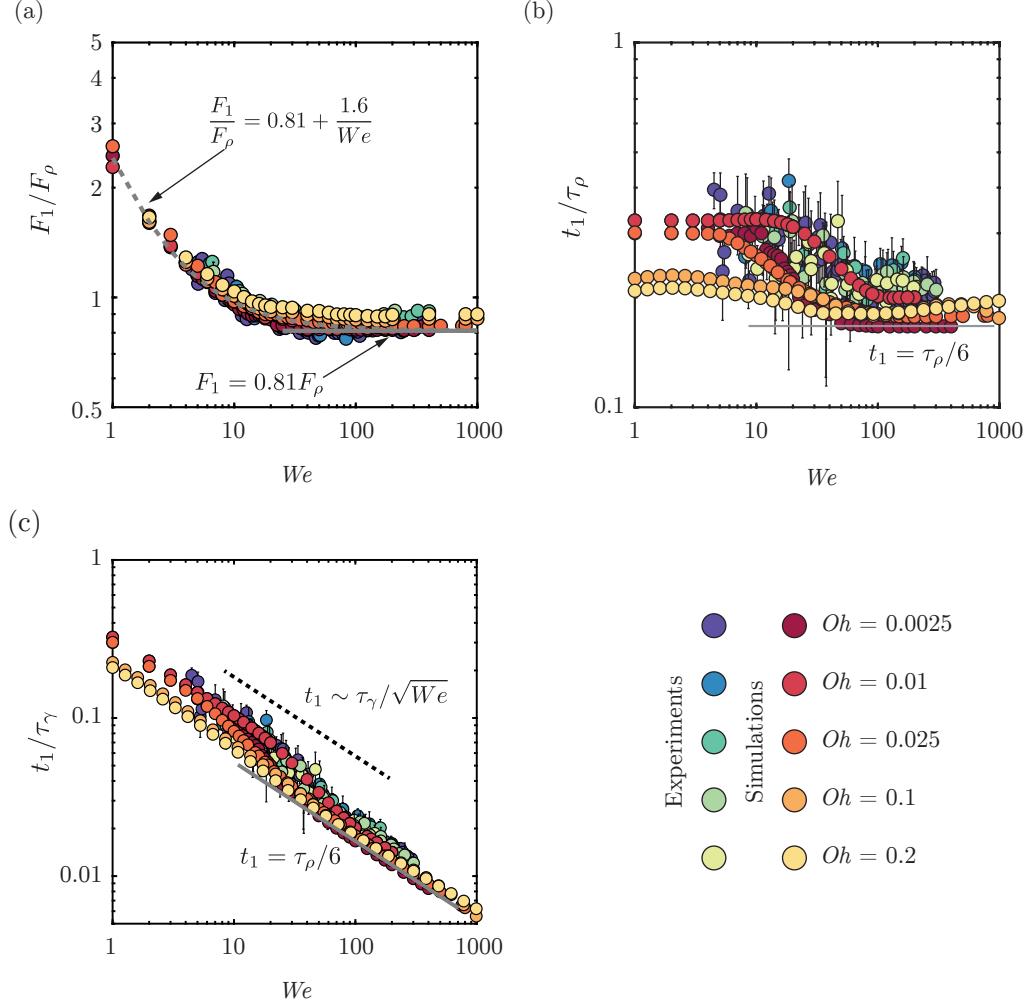


FIGURE 3. Anatomy of the first impact force peak amplitude at low  $Oh$  in between 0.0025 and 0.2, see color legend:  $We$  dependence of the (a) magnitude  $F_1$  normalized by the inertial force scale  $F_\rho = \rho_d V_0^2 D_0^2$  and time  $t_1$  to reach the first force peak amplitude normalized by (b) the inertial timescale  $\tau_\rho = D_0/V_0$  and (c) the inertia-capillary time scale  $\tau_\gamma = \sqrt{\rho_d D_0^3/\gamma}$ .

216 still falls with the impact velocity (figure 4, from  $t = t_1/4$  until  $t = t_1$ ). Consequently,  
 217 momentum conservation implies

$$F_1 \sim V_0 \frac{dm}{dt}, \quad (3.1)$$

218 where the mass flux  $dm/dt \sim \rho_d V_0 D_0^2$  (Soto *et al.* 2014; Zhang *et al.* 2022). As a result,  
 219 the first peak amplitude scales with the inertial pressure force (figure 3a)

$$F_1 \sim F_\rho, \text{ where } F_\rho = \rho_d V_0^2 D_0^2, \quad (3.2)$$

220 for high Weber numbers ( $We > 30$ ,  $F_1 \approx 0.81F_\rho$ ). Furthermore, the time  $t_1$  to reach  $F_1$   
 221 follows

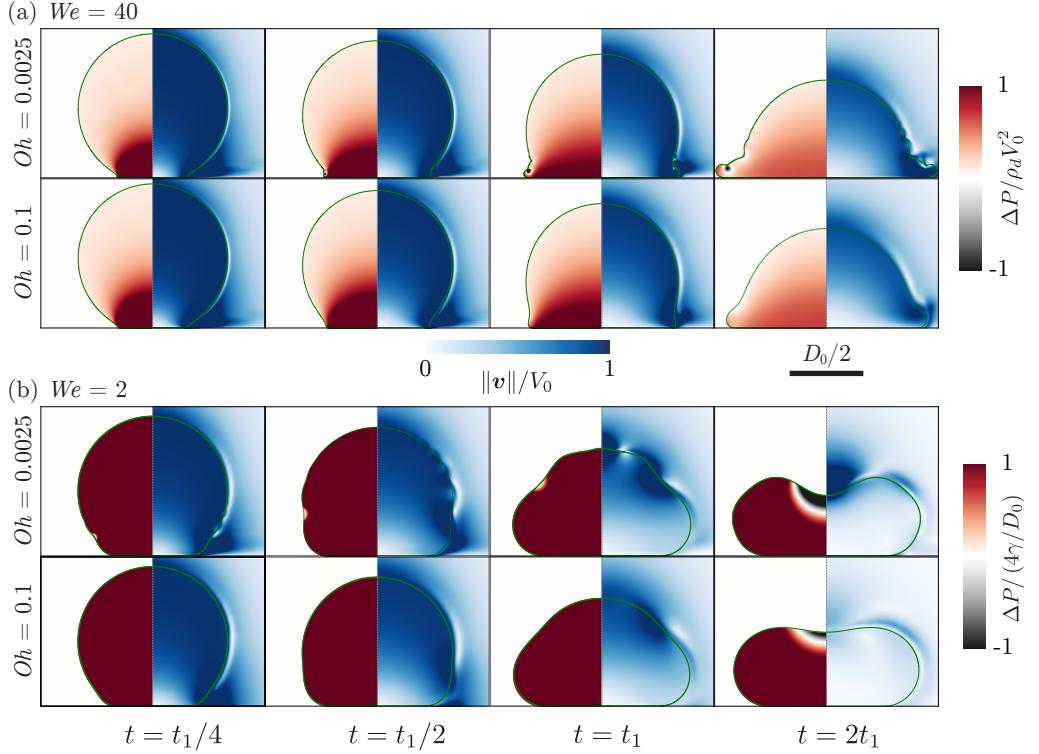


FIGURE 4. Direct numerical simulations snapshots illustrating the drop impact dynamics for  $We$  = (a) 40 and (b) 2. The left-hand side of each numerical snapshot shows the pressure normalized by (a) the inertial pressure scale  $\rho_d V_0^2$  and (b) the capillary pressure scale  $\gamma/D_0$ . The right-hand side shows the velocity field magnitude normalized by the impact velocity  $V_0$ .

$$t_1 \sim \frac{D_0}{V_0} = \tau_\rho, \quad (3.3)$$

where,  $\tau_\rho$  is the inertial timescale. The relation between equations (3.2) and (3.3) is apparent from the momentum conservation which implies that the impulse of the first force peak is equal to the momentum of the impacting drop, i.e.,  $F_1 t_1 \sim \rho_d V_0 D_0^3 = F_\rho \tau_\rho$  (see Gordillo *et al.* 2018, Zhang *et al.* 2022, and figures 3b,c). These scaling laws depend only on the inertial shock at impact and are wettability-independent (Zhang *et al.* 2017; Gordillo *et al.* 2018; Zhang *et al.* 2022). For details of the scaling law, including the prefactors, we refer the readers to Philippi *et al.* (2016); Gordillo *et al.* (2018); Cheng *et al.* (2022).

Figure 3 further illustrates that this inertial asymptote is insensitive to viscosity variations up to 100-fold as  $F_1 \sim F_\rho$  and  $t_1 \sim \tau_\rho$  for  $0.0025 < Oh < 0.2$ . However, deviations from the inertial force and time scales are apparent for  $We < 30$  (figure 3), a phenomenon also reported in earlier work (Soto *et al.* 2014; Zhang *et al.* 2022). In these instances, inertia does not act as the sole governing force but instead complements surface tension, which dictates the pressure inside the drop ( $p \sim \gamma/D_0$  throughout the drop for  $We \lesssim 1$ , figure 4b). Zhang *et al.* (2022) proposed an empirical functional dependence as

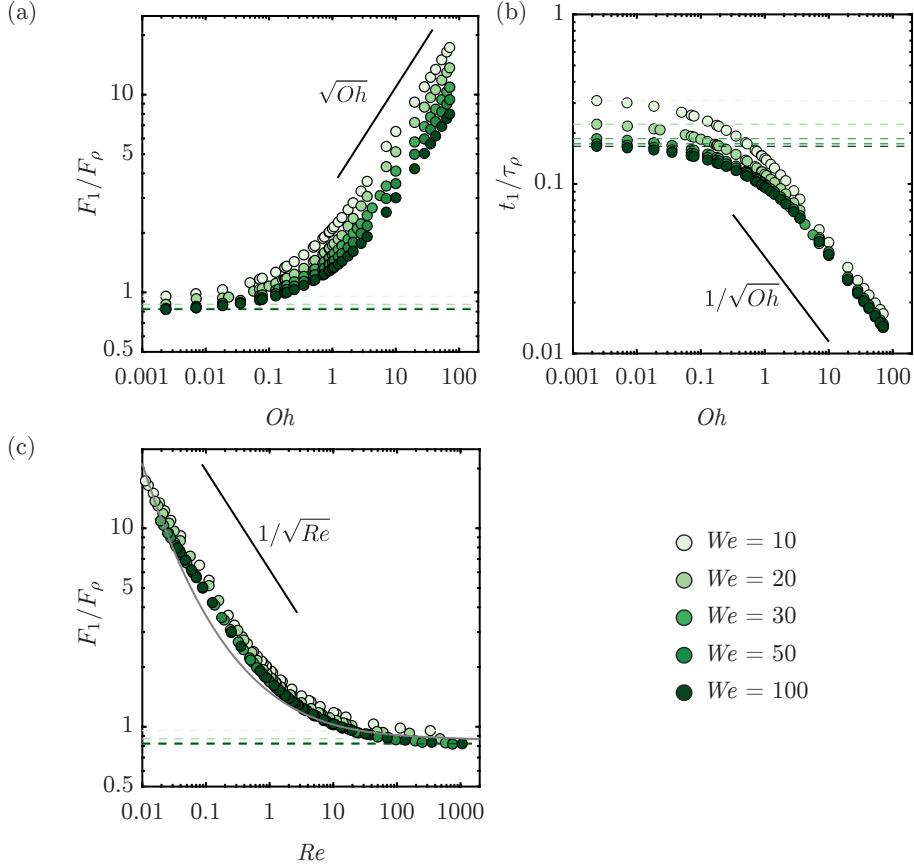


FIGURE 5. Anatomy of the first impact force peak amplitude for viscous impacts from our numerical simulations: the  $Oh$  dependence of (a) the magnitude  $F_1$  normalized by the inertial force scale  $\rho_d V_0^2 D_0^2$  and (b) the time  $t_1$  to reach the first force peak amplitude normalized by inertial timescale  $\tau_\rho = D_0/V_0$ . (c) The  $Re$  dependence of the magnitude  $F_1$  normalized by the inertial force scale  $\rho_d V_0^2 D_0^2$  as compared to the (implicit) theoretical calculation of Gordillo *et al.* (2018). The black line corresponds to the scaling relationship described in §3.2. The Weber number is color-coded.

$$F_1 = \left( \alpha_1 \rho_d V_0^2 + \alpha_2 \frac{\gamma}{D_0} \right) D_0^2, \quad (3.4)$$

based on dimensional analysis, with  $\alpha_1$  and  $\alpha_2$  as free parameters which were determined to be approximately 1.6 and 0.81, respectively for water ( $Oh = 0.0025$ ). These coefficients only deviate marginally in the current work despite the significant increase in  $Oh$  as compared to previous works (Cheng *et al.* 2022; Zhang *et al.* 2022). This consistency underscores the invariance of the pressure field inside the drop to an increase in  $Oh$  (close to the impact region, figure 4a and throughout the drop, figure 4b).

### 3.2. Large Ohnesorge number impacts

Figure 5 reaffirms the findings of §3.1 for low  $Oh$  that the first impact peak amplitude  $F_1$  and the time to reach this peak amplitude  $t_1$  scale with  $F_\rho$  and  $\tau_\rho$ , respectively. As the Ohnesorge number increases further, the first impact force peak amplitude normalized

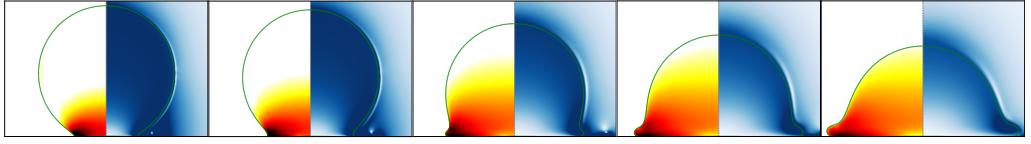
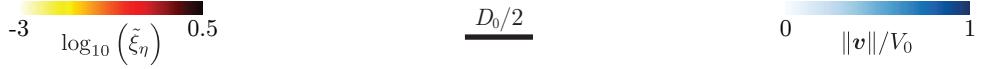
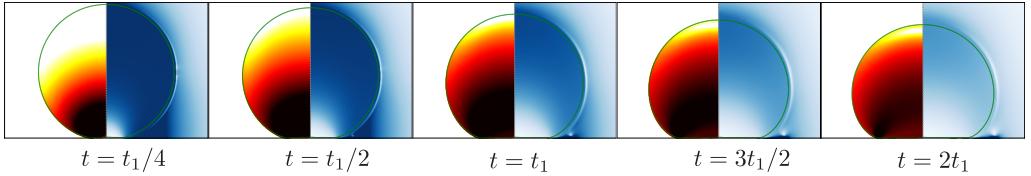
(a)  $Oh = 0.05$ (b)  $Oh = 0.5$ (c)  $Oh = 5$ 

FIGURE 6. Direct numerical simulations snapshots illustrating the drop impact dynamics for  $We = 100$  and  $Oh =$  (a)  $0.05$ , (b)  $0.5$ , and (c)  $5$ . The left-hand side of each numerical snapshot shows the viscous dissipation function  $\xi_\eta$  normalized by the inertial scale  $\rho_d V_0^3 / D_0$ . The right-hand side shows the velocity field magnitude normalized by the impact velocity  $V_0$ .

with  $F_\rho$  begins to increase, indicating a transition around  $Oh \approx 0.1$ , where viscosity starts to play a significant role. At large  $Oh$ , we observe the scaling relationship (figure 5a)

$$F_1 \sim F_\rho \sqrt{Oh}. \quad (3.5)$$

The drop's momentum is still  $\rho_d V_0 D_0^3$  which must be balanced by the impulse from the substrate,  $F_1 t_1$  (see §3.1, Gordillo *et al.* 2018, Zhang *et al.* 2022, and figure 5b). Consequently, the time  $t_1$  follows

$$t_1 \sim \frac{\tau_\rho}{\sqrt{Oh}}. \quad (3.6)$$

Figure 5 further shows that these scaling laws are weakly dependent on the Weber number, as viscous dissipation consumes the entire initial kinetic energy of the impacting drop (figure 6). Once again, we stress that using the water-glycerol mixtures limits the range of  $Oh$  that we can probe experimentally. We further note that the first peak is robust and does not depend on the wettability of the substrate. Consequently, to compare with the existing data such as those in Cheng *et al.* (2022) with different liquids to cover a wider range of liquid viscosities and to account for the apparent  $We$ -dependence, we plot  $F_1$  compensated with  $F_\rho$  against the impact Reynolds number  $Re \equiv \sqrt{We}/Oh = V_0 D_0 / \nu_d$ . For the low  $Re$  regime, such a plot allows us to describe the  $We$  dependence on the prefactor more effectively, as illustrated in figure 5(c). However, it is important to note that some scatter is still observed at high  $Re$  values, which can be attributed to the  $We$  dependence of the impact force peak amplitude. This lack of a pure scaling behavior

demonstrates how the interplay between kinetic energy and viscous dissipation within the drop dictates the functional dependence of the maximum impact force on  $Oh$ .

To systematically elucidate these scaling behaviors in the limit of small  $Re$ , we need to find the typical scales for the rate of change of kinetic energy and that of the rate of viscous dissipation for the drop impact system. First, we can readily define an average rate of viscous dissipation per unit mass as

$$\bar{\varepsilon} \sim \frac{1}{\tau_\rho} \frac{1}{D_0^3} \int_0^{\tau_\rho} \int_{\Omega} \nu_d (\mathcal{D} : \mathcal{D}) d\Omega dt, \quad (3.7)$$

where  $\nu_d$  is the kinematic viscosity of the drop and  $d\Omega$  is the volume element where dissipation occurs. Notice that  $\bar{\varepsilon}$  has the dimensions of  $V_0^3/D_0$ , i.e., length squared over time cubed or velocity squared over time, as it should be for dissipation rate of energy per unit mass. We can estimate  $\Omega = D_{\text{foot}}^2 l_\nu$  (figure 6), where  $D_{\text{foot}}$  is the drop's foot diameter in contact with the substrate and  $l_\nu$  is the viscous boundary layer thickness. This boundary layer marks the region of strong velocity gradients ( $\sim V_0/l_\nu$ ) analogous to the Mirels (1955) shockwave-induced boundary layer. For details, we refer the authors to Schlichting (1968); Schroll *et al.* (2010); Philippi *et al.* (2016). Consequently, the viscous dissipation rate scales as

$$\bar{\varepsilon} \sim \frac{1}{\tau_\rho D_0^3} \int_0^{\tau_\rho} \nu_d \left( \frac{V_0}{l_\nu} \right)^2 D_{\text{foot}}^2 l_\nu dt. \quad (3.8)$$

To calculate  $D_{\text{foot}}$ , we assume that the drop maintains a spherical cap shape throughout the impact (figure 6). To calculate the distance the drop would have traveled if there were no substrate, we use the relation  $d \sim V_0 t$ . Simple geometric arguments allow us to determine the relation between the foot diameter and this distance,  $D_{\text{foot}} \sim \sqrt{D_0 d}$  (Lesser 1981; Mandre *et al.* 2009; Zheng *et al.* 2021; Bilotto *et al.* 2023; Bertin 2023). Interestingly, this scaling behavior is similar to the inertial limit (Wagner 1932; Bouwhuis *et al.* 2012; Philippi *et al.* 2016; Gordillo *et al.* 2019) as discussed by Langley *et al.* (2017); Bilotto *et al.* (2023). Furthermore, the viscous boundary layer  $l_\nu$  can be approximated using  $\sqrt{\nu_d t}$  (Mirels 1955; Eggers *et al.* 2010; Philippi *et al.* 2016). Filling these in (3.8), we get

$$\bar{\varepsilon} \sim \frac{1}{\tau_\rho D_0^2} \int_0^{\tau_\rho} \sqrt{\nu_d} V_0^3 \sqrt{t} dt, \quad (3.9)$$

which on integration gives

$$\bar{\varepsilon} \sim \sqrt{\nu_d \tau_\rho} V_0^3 / D_0^2, \quad (3.10)$$

where  $\tau_\rho$  is the inertial time scale. Here, we assume that for highly viscous drops, all energy is dissipated within a fraction of  $\tau_\rho$ . Filling in (3.10) and normalizing  $\bar{\varepsilon}$  with the inertial scales  $V_0^3/D_0$ ,

$$\frac{\bar{\varepsilon}}{V_0^3/D_0} \sim \sqrt{\frac{\nu_d \tau_\rho}{D_0^2}} = \frac{1}{\sqrt{Re}} = \left( \frac{Oh}{\sqrt{We}} \right)^{1/2}. \quad (3.11)$$

Next, the kinetic energy of the falling drop is given by

$$\dot{K}(t) \equiv \frac{dK(t)}{dt} \sim \rho_d D_0^3 \bar{\varepsilon}, \quad \text{where } K(t) = \frac{1}{2} m (V(t))^2, \quad (3.12)$$

294 and  $V(t)$  is the drop's center of mass velocity. The left-hand side of (3.12) can be written  
 295 as

$$\dot{K}(t) = mV(t) \frac{dV(t)}{dt} = F(t)V(t). \quad (3.13)$$

296 In equation (3.13),  $F(t)$  and  $V(t)$  scale with the first impact force peak amplitude  $F_1$   
 297 and the impact velocity  $V_0$ , respectively, giving the typical scale of the rate of change of  
 298 kinetic energy as

$$\dot{K}^* \sim F_1 V_0. \quad (3.14)$$

299 We stress that (3.14) states that the rate of change of kinetic energy is equal to the power  
 300 of the normal reaction force, an observation already made by [Wagner \(1932\)](#) and [Philippi  
 et al. \(2016\)](#) in the context of impact problems. Lastly, at large  $Oh$ , viscous dissipation  
 302 enervates kinetic energy completely giving (figure 6c, also see: [Philippi et al. \(2016\)](#) and  
 303 [Wildeman et al. \(2016\)](#)),

$$\dot{K}^* \sim F_1 V_0 \sim \rho_d D_0^3 \bar{\varepsilon} \quad (3.15)$$

304 Additionally, we use the inertial scales to non-dimensionalize (3.15) and fill in (3.11),  
 305 giving

$$\frac{F}{F_\rho} \sim \frac{\bar{\varepsilon}}{V_0^3/D_0} \sim \frac{1}{\sqrt{Re}} = \left( \frac{Oh}{\sqrt{We}} \right)^{1/2} \quad (3.16)$$

306 and using  $F_1 t_1 \sim \rho_d V_0 D_0^3 = F_\rho \tau_\rho$ ,

$$\frac{t_1}{\tau_\rho} \sim \left( \frac{\sqrt{We}}{Oh} \right)^{1/2}. \quad (3.17)$$

307 In summary, we use energy and momentum invariance to elucidate the parameter  
 308 dependencies of the impact force as illustrated in figure 5. The scaling arguments  
 309 capture the dominant force balance during the impact process, considering the relative  
 310 importance of inertial, capillary, and viscous forces. As the dimensionless viscosity of  
 311 impacting drops increases, the lack of surface deformation increases the normal reaction  
 312 force (3.16). Further, the invariance of incoming drop momentum implies that this  
 313 increase in normal reaction force occurs on a shorter timescale (3.17).

#### 314 4. Anatomy of the second impact force peak

315 This section delves into the anatomy of the second impact force peak amplitude  $F_2$  as a  
 316 function of the Weber  $We$  and Ohnesorge  $Oh$  numbers, summarized in figure 7. We once  
 317 again note the remarkable agreement between experiments and numerical simulations in  
 318 this figure.

319 Similar to the mechanism leading to the formation of the first peak (§3), also the

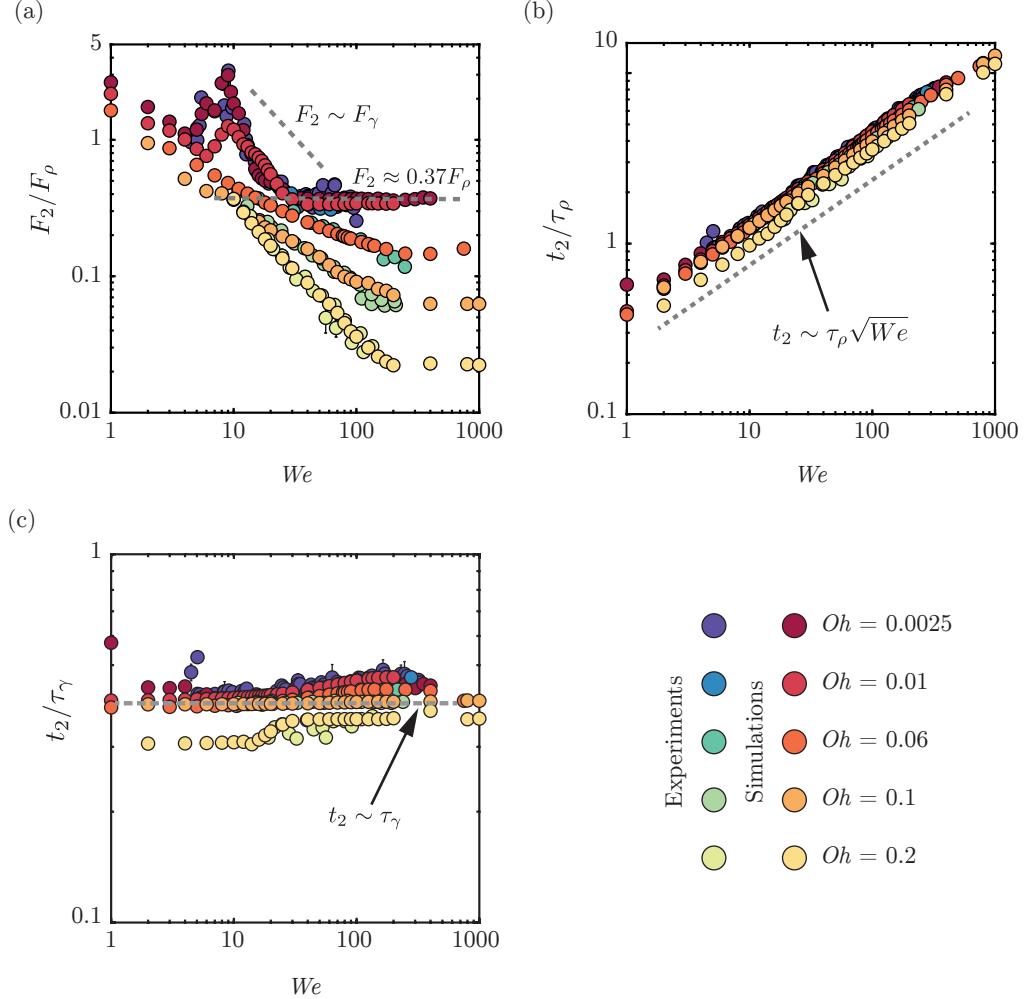


FIGURE 7. Anatomy of the second impact force peak amplitude:  $We$  dependence of the (a) magnitude  $F_2$  normalized by the inertial force scale  $F_\rho = \rho_d V_0^2 D_0^2$  and time  $t_2$  to reach the second force peak amplitude normalized by (b) the inertio-capillary time scale  $\tau_\gamma = \sqrt{\rho_d D_0^3 / \gamma}$  and (c) inertial timescale  $\tau_\rho = D_0 / V_0$ .

mechanism for the formation of this second peak is momentum conservation. As the drop takes off the surface, it applies a force on the substrate. As noted in §1 and Zhang *et al.* (2022), this force also coincides with the formation of a Worthington jet (figure 2iv). The time  $t_2$  at which the second peak is observed scales with the inertio-capillary timescale and is insensitive to  $We$  and  $Oh$  (figure 7b,c). Once again, we invoke the analogy between drop oscillation and drop impact to explain this behavior (Richard *et al.* 2002; Chevy *et al.* 2012). At the time instant  $t_2 \approx 0.44\tau_\gamma$ , the drop's internal motion undergoes a transition from a predominantly radial flow to a vertical one due to the formation of the Worthington jet (Chantelot 2018; Zhang *et al.* 2022). Figure 8 exemplifies this jet in the  $Oh$ - $We$  parameter space, which is intricately related to the second peak in the drop impact force. For low  $Oh$  and large  $We$ , the drop retraction follows a modified Taylor-Culick dynamics (Bartolo *et al.* 2005; Eggers *et al.* 2010; Sanjay *et al.* 2022). As  $We$  is

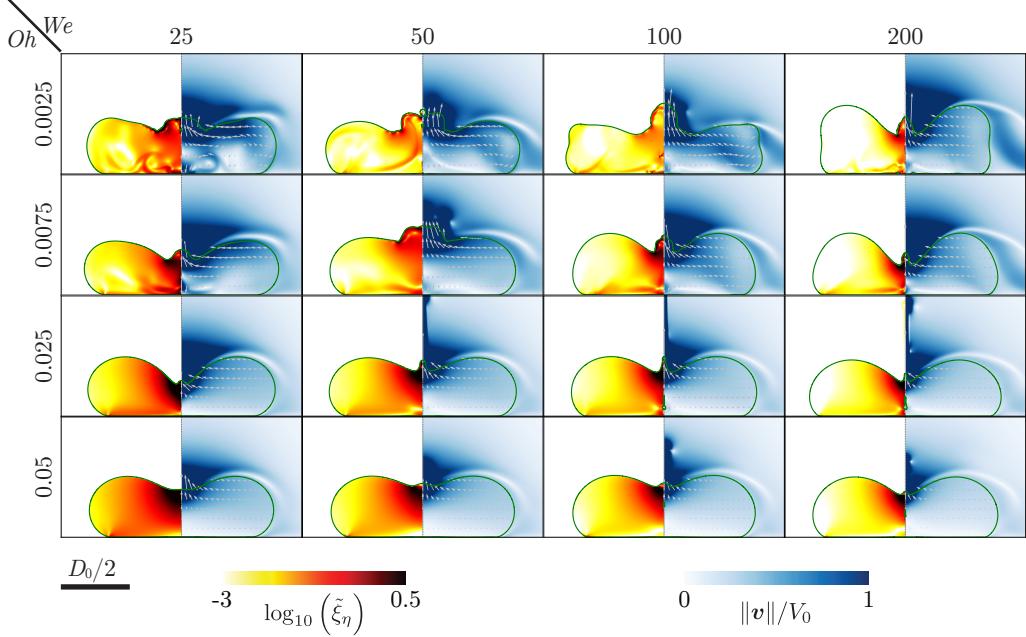
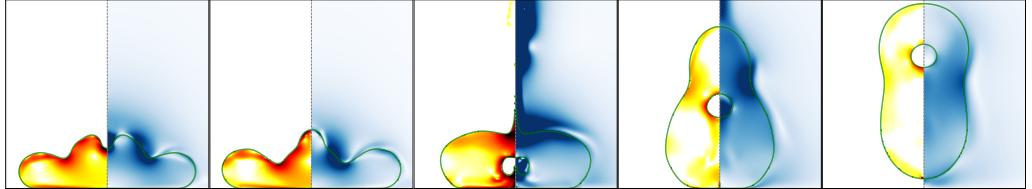
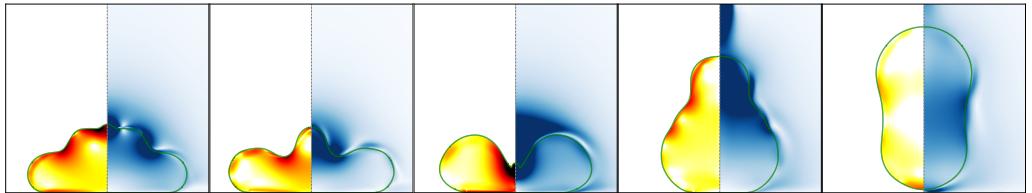
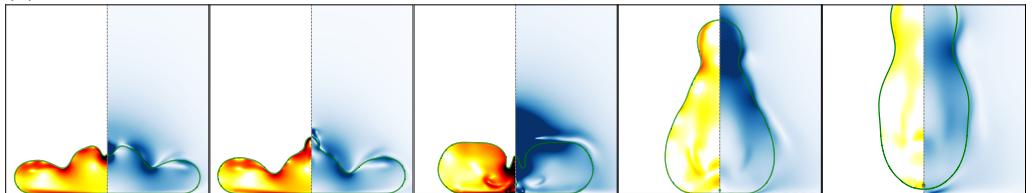
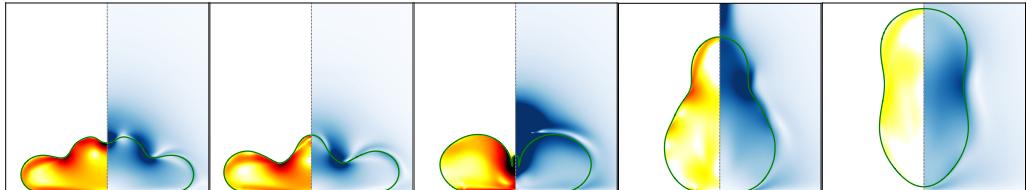
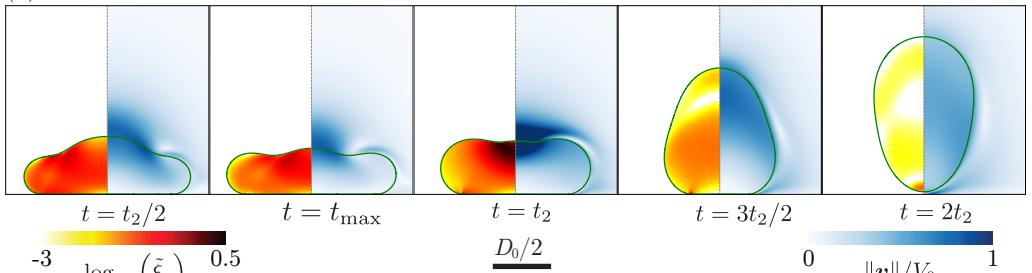


FIGURE 8. Direct numerical simulations snapshots illustrating the influence of  $We$  and  $Oh$  on the inception of the Worthington jet. All these snapshots are taken at the instant when the second peak appears in the temporal evolution of the normal reaction force ( $t = t_2$ ). The left-hand side of each numerical snapshot shows the viscous dissipation function  $\xi_\eta$  normalized by the inertial scale  $\rho_d V_0^3 / D_0$ . The right-hand side shows the velocity field magnitude normalized by the impact velocity  $V_0$ . The gray velocity vectors are plotted in the center of mass reference frame of the drop to clearly elucidate the internal flow.

increased, the jet gets thinner but faster, maintaining a constant momentum flux  $\rho_d V_j^2 d_j^2$ , where  $V_j$  and  $d_j$  are the jet's velocity and diameter, respectively (figure 8, Zhang *et al.* 2022). This invariance leads to the observed scaling  $F_2 \sim F_\rho$  in this regime ( $F_2 \approx 0.37 F_\rho$  for  $We \geq 30, Oh \leq 0.01$ ).

Furthermore, the low  $We$  and  $Oh$  regime relies entirely on capillary pressure (figure 4). Subsequently,  $F_2 \sim F_\gamma = \gamma D_0$  for  $Oh < 0.01$  and  $We < 30$  (figure 7). This flow focusing (figure 8) is most efficient for  $We = 9$  (figure 9a,  $t_2/2 < t < t_2$ , Renardy *et al.* 2003; Bartolo *et al.* 2006b) where the capillary resonance leads to a thin-fast jet, accompanied by a bubble entrainment, reminiscent of the hydrodynamic singularity (figure 9, Zhang *et al.* 2022; Sanjay *et al.* 2021). The characteristic feature of this converging flow is a higher magnitude of  $F_2$  compared to  $F_1$  (figure 7).

However, this singular jet regime is very narrow in the  $Oh$ - $We$  phase space. Figure 9b shows two cases for water drops ( $Oh = 0.0025$ ) at different  $We$  (5 and 12 for figures 9b-i and b-ii, respectively). Bubble entrainment does not occur in either of these cases. Consequently, the maximum force amplitude diminishes for these two cases (figure 7). Nonetheless, these cases are still associated with high local viscous dissipation near the axis of symmetry owing to the singular nature of the flow. Another mechanism to inhibit this singular Worthington jet is viscous dissipation in the bulk. As the Ohnesorge number increases, this singular jet formation disappears ( $Oh = 0.005$ , figure 9c-i), significantly reducing the second peak of the impact force. For even higher viscosities, the drop no longer exhibits the sharp, focused jet formation seen at lower viscosities, and the second peak in the force is notably diminished ( $Oh = 0.05$ , figure 9c-ii).

(a)  $We = 9, Oh = 0.0025$ (b)  $Oh = 0.0025$ (i)  $We = 5$ (ii)  $We = 12$ (c)  $We = 9$ (i)  $Oh = 0.005$ (ii)  $Oh = 0.05$ 

$$\begin{array}{cc} t = t_2/2 & t = t_{\max} \\ \text{---} & \text{---} \\ -3 & \log_{10} (\tilde{\xi}_\eta) & 0.5 \\ & \text{---} & \text{---} \\ & D_0/2 & \\ & \text{---} & \text{---} \\ t = t_2 & t = 3t_2/2 & t = 2t_2 \\ \text{---} & \text{---} & \text{---} \\ 0 & \|v\|/V_0 & 1 \end{array}$$

FIGURE 9. Direct numerical simulations snapshots illustrating the influence of  $We$  and  $Oh$  on the singular Worthington jet. (a)  $(We, Oh) = (9, 0.0025)$ , (b)  $Oh = 0.0025$  with  $We =$  (i) 5 and (ii) 12, and (c)  $We = 9$  with  $Oh =$  (i) 0.005 and (ii)  $Oh = 0.05$ . The left-hand side of each numerical snapshot shows the viscous dissipation function  $\xi_\eta$  normalized by inertial scale  $\rho_d V_0^3 / D_0$ . The right-hand side shows the velocity field magnitude normalized by the impact velocity  $V_0$ .

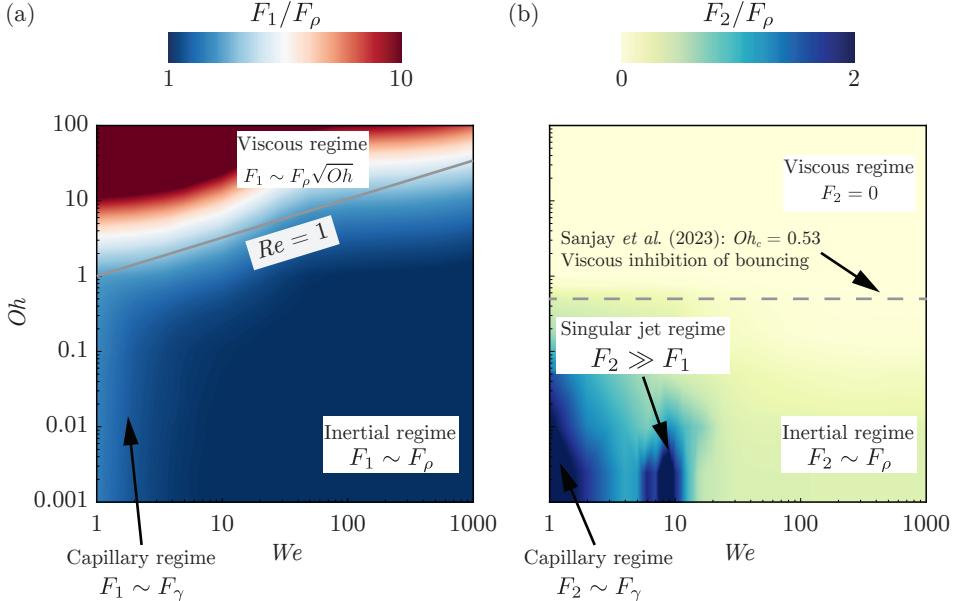


FIGURE 10. Regime map in terms of the drop Ohnesorge number  $Oh$  and the impact Weber number  $We$  to summarize the two peaks in the impact force by showing the different regimes described in this work based on (a) the first peak in the impact force peak amplitude  $F_1$  and (b) the second peak in the impact force peak amplitude  $F_2$ . Both peaks are normalized by the inertial force scale  $F_\rho = \rho_d V_0^2 D_0^2$ . These regime maps are constructed using  $\sim 1500$  simulations in the range  $0.001 \leqslant Oh \leqslant 100$  and  $1 \leqslant We \leqslant 1000$ . The gray solid line in (a) and dashed line in (b) mark the inertial-viscous transition ( $Re = 1$ ) and the bouncing-no-bouncing transition ( $Oh_c = 0.53$  for  $Bo = 1$ , see [Sanjay et al. \(2023a\)](#)), respectively.

Lastly, as  $Oh$  increases, bulk dissipation becomes dominant (apparent from increasing  $Oh$  at fixed  $We$  in figure 8) and can entirely inhibit drop bouncing. Recently, [Jha et al. \(2020\)](#); [Sanjay et al. \(2023a\)](#) showed that there exists a critical  $Oh$ , two orders of magnitude higher than that of a 2 mm diameter water drop, beyond which drops do not bounce either, irrespective of their impact velocity. Consequently, the second peak in the impact force diminishes for larger  $Oh$ , which explains the monotonic decrease of the amplitude  $F_2$  observed in figure 7 for  $We > 30, Oh > 0.01$ .

## 5. Conclusion and outlook

In this work, we study the forces and dissipation encountered during the drop impact process by employing experiments, numerical simulations, and theoretical scaling laws. We vary the two dimensionless control parameters—the Weber ( $We$ : dimensionless impact velocity) and the Ohnesorge number ( $Oh$ : dimensionless viscosity) independently to elucidate the intricate interplay between inertia, viscosity, and surface tension in governing the forces exerted by a liquid drop upon impact on a non-wetting substrate.

For the first impact force peak amplitude  $F_1$ , owing to the momentum balance after the inertial shock at impact, figure 10(a) summarizes the different regimes in the  $Oh$ - $We$  phase space. For low  $Oh$ , inertial forces predominantly dictate the impact dynamics, such that  $F_1$  scales with the inertial force  $F_\rho$  ([Philippi et al. 2016](#); [Gordillo et al. 2018](#); [Mitchell et al. 2019](#); [Cheng et al. 2022](#); [Zhang et al. 2022](#)) and is insensitive to viscosity variations up to 100-fold. As  $Oh$  increases, the viscosity becomes significant, leading to a new scaling law:  $F_1 \sim F_\rho \sqrt{Oh}$ . The paper unravels this viscous scaling behavior by accounting for

375 the loss of initial kinetic energy owing to viscous dissipation inside the drop. Lastly, at  
 376 low  $We$ , the capillary pressure inside the drop leads to the scaling  $F_1 \sim F_\gamma$  (Moláček &  
 377 Bush 2012; Chevy *et al.* 2012).

378 The normal reaction force described in this work is responsible for deforming the  
 379 drop as it spreads onto the substrate, where it stops thanks to surface tension. If the  
 380 substrate is non-wetting, it retracts to minimize the surface energy and finally takes off  
 381 (Richard & Quéré 2000). In this case, the momentum conservation leads to the formation  
 382 of a Worthington jet and a second peak in the normal reaction force, as summarized in  
 383 figure 10(b). For low  $Oh$  and high  $We$ , the second force peak amplitude scales with the  
 384 inertial force ( $F_\rho$ ), following a modified Taylor-Culick dynamics (Eggers *et al.* 2010). In  
 385 contrast, capillary forces dominate at low  $We$  and low  $Oh$ , leading to a force amplitude  
 386 scaling of  $F_2 \sim F_\gamma$ . We also identify a narrow regime in the  $Oh$ - $We$  phase space where a  
 387 singular Worthington jet forms, significantly increasing  $F_2$  (Bartolo *et al.* 2006b; Zhang  
 388 *et al.* 2022), localized in the parameter space for  $We \approx 9$  and  $Oh < 0.01$ . As  $Oh$  increases,  
 389 bulk viscous dissipation counteracts this jet formation, diminishing the second peak and  
 390 ultimately inhibiting drop bouncing.

391 Our findings have far-reaching implications, not only enriching the fundamental  
 392 understanding of fluid dynamics of drop impact but also informing practical applications  
 393 in diverse fields such as inkjet printing, public health, agriculture, and material science  
 394 where the entire range of  $Oh$ - $We$  phase space is relevant (figures 1b and 10). While this  
 395 has identified new scaling laws, it also opens avenues for future research. For instance,  
 396 it would be interesting to use the energy accounting approach to unify the scaling laws  
 397 for the maximum spreading diameter for arbitrary  $Oh$  (Laan *et al.* 2014; Wildeman  
 398 *et al.* 2016). Although, the implicit theoretical model summarized in Cheng *et al.* (2022)  
 399 describes most of data in figure 5, we stress the importance of having a predictive model  
 400 to determine  $F_1$  for given  $We$  and  $Oh$  (Sanjay & Lohse 2024). The  $We$  influence on  
 401 the impact force also warrants further exploration, especially in the regime  $We \ll 1$  for  
 402 arbitrary  $Oh$  (Chevy *et al.* 2012; Moláček & Bush 2012) and drop impact on compliant  
 403 surfaces (Alventosa *et al.* 2023b; Ma & Huang 2023). Another potential extension of this  
 404 work is to non-Newtonian fluids (Martouzet *et al.* 2021; Agüero *et al.* 2022; Bertin 2023;  
 405 Jin *et al.* 2023).

406  
 407 **Code availability.** The codes used in the present article are permanently available at  
 408 Sanjay (2023).

409  
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420  
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428

429 **Appendix A. Note on the parametric error characterization**

430 This appendix outlines the methodology for characterizing experimental errors in quantification of the drop's size and impact velocities which is crucial for accurate calculation  
 431 of dimensionless control parameters,  $We$  and  $Oh$ . The drop diameter determination  
 432 involves multiple steps. First, we measure the total mass ( $M_{100}$ ) of 100 drops using an  
 433 electric balance. From this mass, using the liquid density and assuming spherical shape,  
 434 we calculated the drop diameter ( $D_0$ ). We repeated this process five times, yielding  
 435  $D_{0,1}$  through  $D_{0,5}$ . The average of these measurements provided the final drop diameter  
 436 ( $D_0$ ) and its standard error. For impact velocity determination, we extracted data from  
 437 experimental high-speed imagery. By tracking the drop center's position in successive  
 438 frames prior to substrate contact, and knowing the frame rate, we calculated the impact  
 439 velocity. We repeated this process for five trials, obtaining  $V_{0,1}$  through  $V_{0,5}$ . The average  
 440 of these values gave the final impact velocity ( $V_0$ ) and its standard error.

441 The standard errors for drop diameters do not exceed 0.13 mm. For instance, drops with  
 442 Ohnesorge numbers of 0.0025, 0.0625, and 0.2 have diameters of  $2.05 \pm 0.13$  mm,  $2.52 \pm$   
 443  $0.11$  mm, and  $2.54 \pm 0.09$  mm, respectively. The standard errors for impact velocities did  
 444 not exceed 0.02 m/s. For the same  $Oh$  values, the impact velocities were  $1.2 \pm 0.002$  m/s,  
 445  $0.97 \pm 0.01$  m/s, and  $0.96 \pm 0.01$  m/s, respectively. The combined errors in  $D_0$  and  $V_0$   
 446 resulted in approximately  $\pm 7\%$  error in Weber number  $We$  and  $\pm 3\%$  error in Ohnesorge  
 447 number  $Oh$ . Consequently, the horizontal error bars, which relate to errors in the control  
 448 parameters, are smaller than the symbol sizes in our figures.

450 **Appendix B. Role of gravity on drop impact forces**

451 The results are Bond invariant in the leading order. Therefore, we chose a representative  
 452 value of Bond = 1: this if for a diameter 0.00256 mm, density 1000 kg/m<sup>3</sup>, acceleration  
 453 due to gravity 10 m/s<sup>2</sup>, surface tension 0.06 N/m. The dimensionless number that matter  
 454 is the Froude number  $Fr = V^2/gD_0 = We/Bo$  which is larger than 1 throughout the  
 455 paper. The difference as compared to [Zhang et al. \(2022\)](#) is in the length scale (2 mm in  
 456 PRL and 2.56 mm in this work).

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