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Thapar Institute of Engineering &  
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**Course: Material and Energy Balances  
UCH301**

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# Material Balances with Chemical Reactions



- For writing balances on reacting components we include the consumption/generation terms in the general material balance equation:

$(Flow \ of \ material \ in \ through \ system \ boundaries)$

$- (Flow \ of \ material \ out \ through \ system \ boundaries)$

$+ (Generation \ of \ material \ within \ the \ system)$

$- (Consumption \ of \ material \ within \ the \ system)$

$= (Accumulation \ of \ material \ within \ the \ system)$

- Limiting/excess reactant is determined on the basis of feed i.e. We do not see what is happening in the reactor while determining limiting reactant, but amounts given in the feed are considered



## Fractional conversion:

It is the ratio of the moles of reactant reacted to the moles of reactant fed.

### Fractional conversional of reactant A:

$$f_A = \text{moles of A reacted} / \text{Moles of A fed}$$

And, the fraction unreacted is equal to  $1-f_A$ .



# Exercise

Acrylonitrile is produced in the reaction of propylene, ammonia, and oxygen:



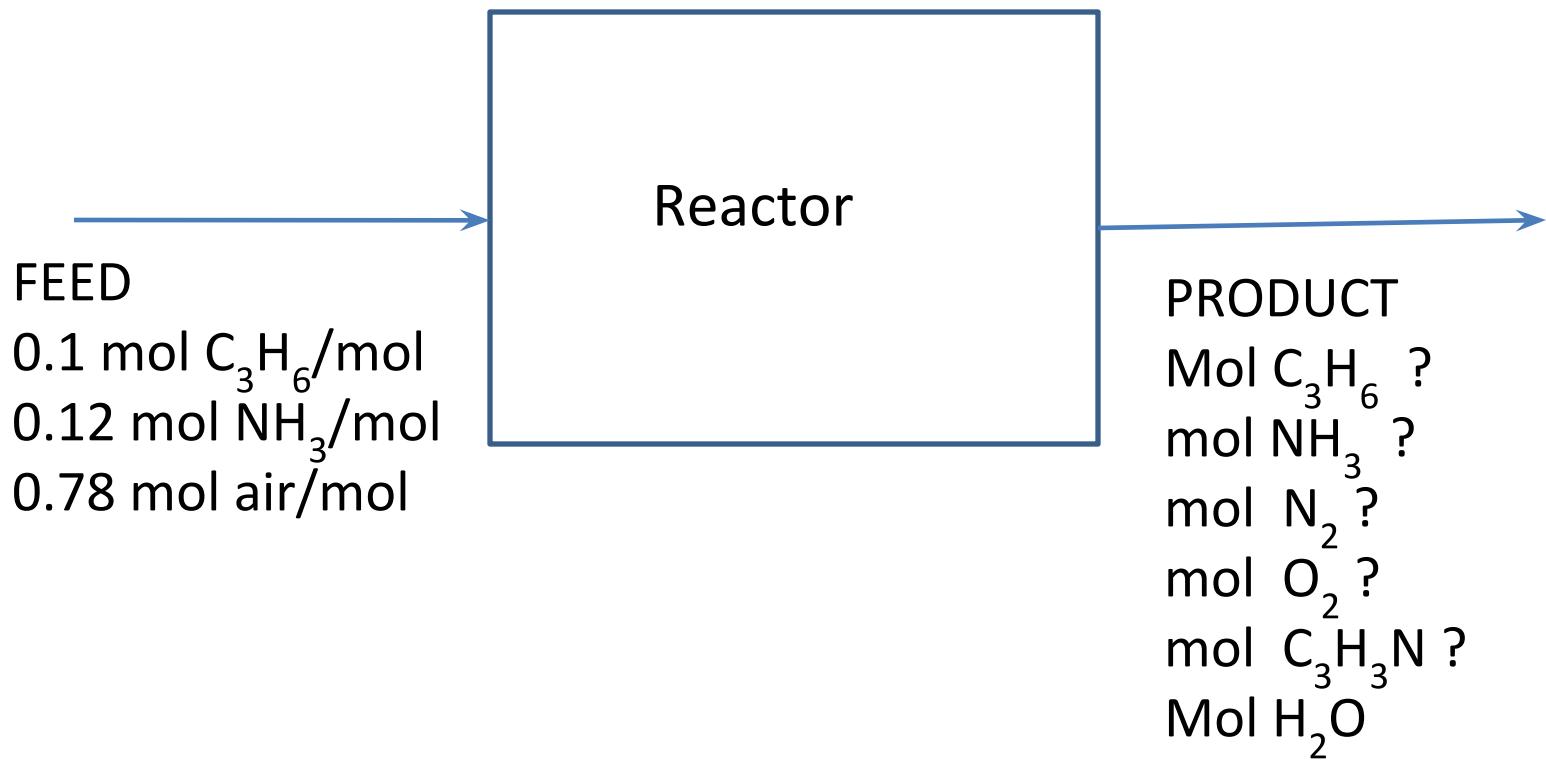
The feed to the reactor contains 10 mol% propylene, 12 mol% ammonia, and 78 mol% air.

A fractional conversion of 30% of the limiting reactant is achieved. Determine the percentages excess of the excess reactants, and the moles of all product components at the outlet of the reactor.



## SOLUTION

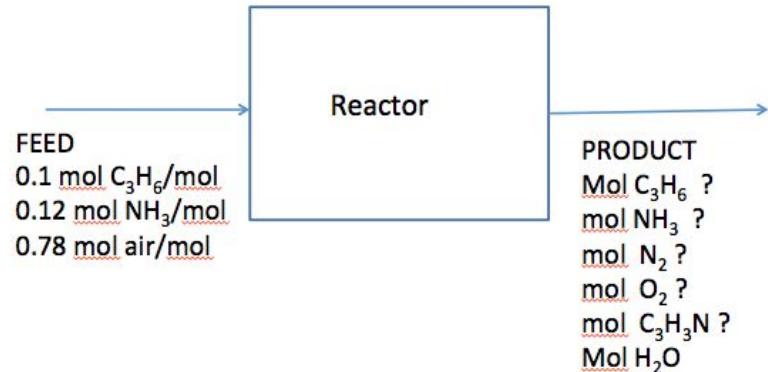
A simple schematic of the problem using the information given in the statement can be made



- Step 1  
Find which of the reactants is limiting reactant
- Step 2  
Based on the moles of limiting reactant converted, calculate the moles of other reactants from stoichiometry.

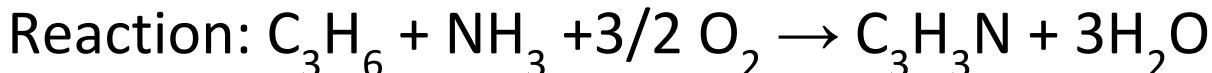


Basis: 100 mol of feed



$$N_2 \text{ in air} = 78 * 0.79 = 61.6 \text{ mol}$$

$$O_2 \text{ in air} = 78 * 0.21 = 16.4 \text{ mol}$$



For 10 mol of C<sub>3</sub>H<sub>6</sub>, NH<sub>3</sub> required is 10 mol

For 10 mol of C<sub>3</sub>H<sub>6</sub>, O<sub>2</sub> required is 15 mol

Therefore

$$\begin{aligned}\% \text{ excess of NH}_3 &= \{(NH_3 \text{ fed}-NH_3 \text{ required})/NH_3 \text{ required}\}*100 \\ &= ((12-10)/10)*100 = 20\%\end{aligned}$$

$$\begin{aligned}\% \text{ excess of O}_2 &= \{(O_2 \text{ fed}-O_2 \text{ required})/O_2 \text{ required}\}*100 \\ &= \{(16.4-15)/15\}*100 = 9.3\%\end{aligned}$$



- Moles of  $\text{C}_3\text{H}_6$  in product =  $10-3 = 7$
- Moles of  $\text{NH}_3$  in the product =  $12-3=9$
- Moles of  $\text{C}_3\text{H}_3\text{N}$  in the product = 3
- Moles of  $\text{H}_2\text{O}$  in the product = 9
- Moles of  $\text{O}_2$  in the product =  $16.4-4.5= 11.9$
- Moles of  $\text{N}_2$  in the product = 61.6



## Yield

It is defined as the moles of product formed to the moles that would have been formed if there were no side reactions and the reaction were complete.

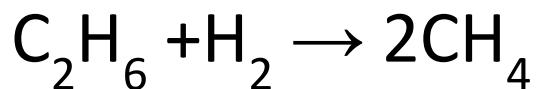
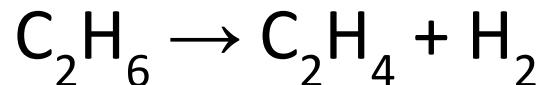
## Selectivity

It is the ratio of moles of desired product formed to the moles of undesired product formed.



# Exercise

The reactions

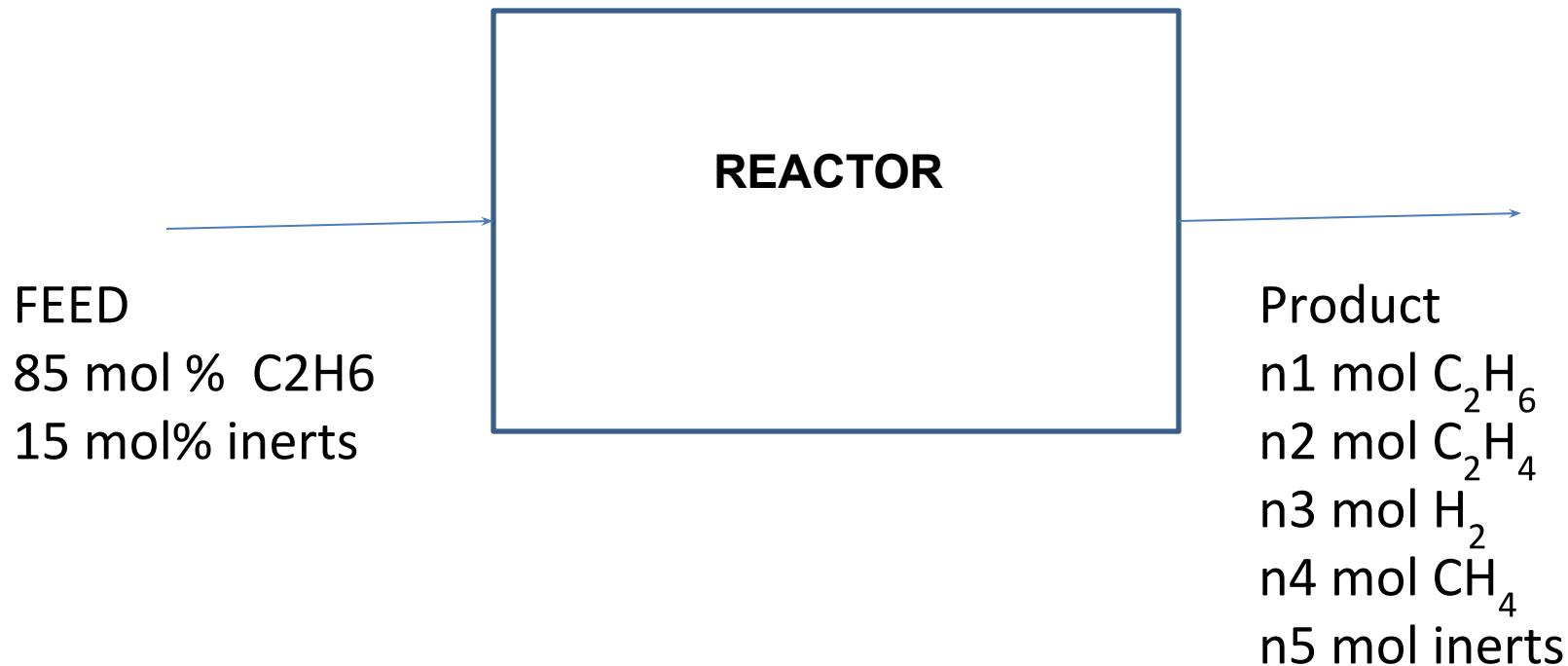


take place in a continuous reactor at steady state. The feed contains 85 mol% ethane and balance inert. The fractional conversion of ethane is 0.501, and the fractional yield of ethylene is 0.471. Calculate the molar compositions of the product gas and the selectivity of ethylene to methane production.



# Solution

Basis: 100 Mol of feed



ethane ( $C_2H_6$ ) converted =  $85 * 0.501 = 42.6$  mol

( $C_2H_6$ ) in product =  $n_1 = 85 - 42.6 = 42.4$  mol

Maximum possible ethylene ( $C_2H_4$ ) that could have formed = 85 mol (from definition of yield)

Yield = ethylene formed / maximum ethylene that could have been formed

Therefore,

Ethylene formed = yield \* maximum possible  
=  $0.471 * 85 = 40$  mol =  $n_2$



- Therefore, 40 mol of ethane are consumed in reaction 1 (as 1 mol of ethane gives 1 mol of ethylene)

And

Ethane consumed in reaction 2 is

= total moles of ethane converted – moles of ethane converted in reaction 1

$$= 42.6 - 40 = 2.6 \text{ mol}$$

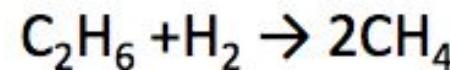
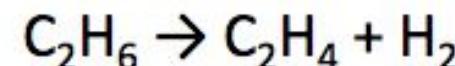
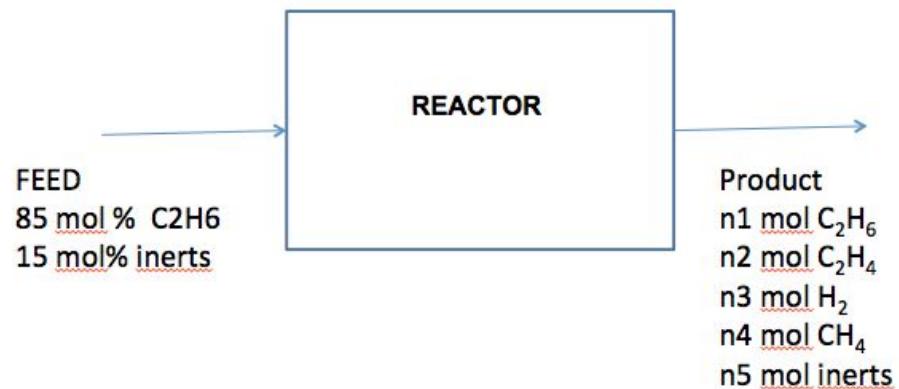
Therefore,

$$n_2 = 40 \text{ mol}$$

$$n_3 = 40 - 2.6 = 37.4 \text{ mol}$$

$$n_4 = 2 * 2.6 = 5.2 \text{ mol}$$

$$n_5 = 15 \text{ mol}$$



Total moles of product stream

$$\begin{aligned} &= n_1 + n_2 + n_3 + n_4 + n_5 = 42.4 + 40 + 37.5 + 5.2 + 15 \\ &= 140.1 \text{ mol} \end{aligned}$$

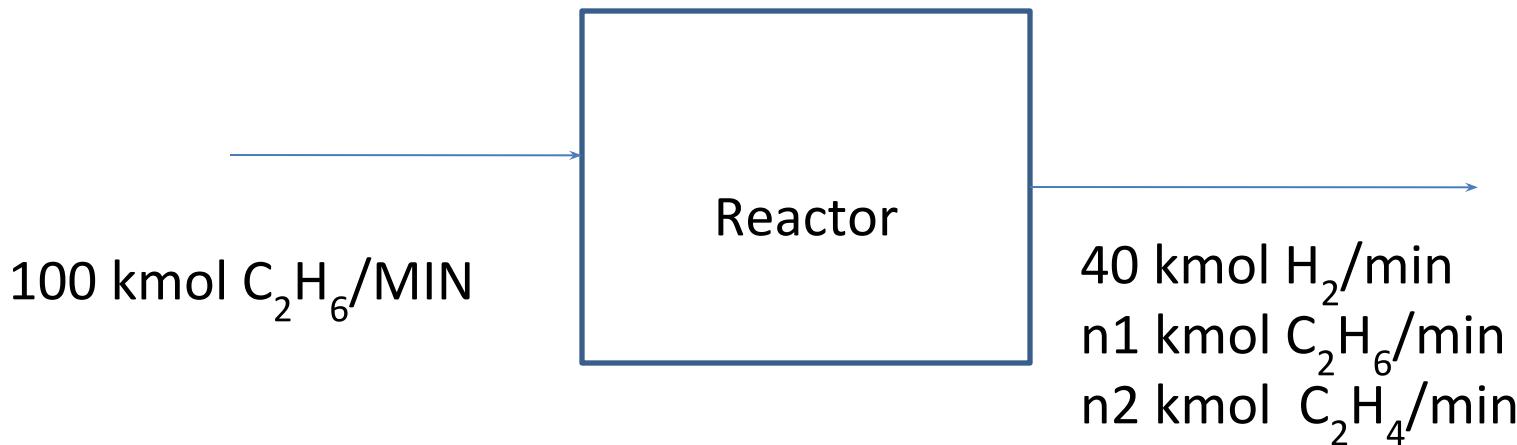
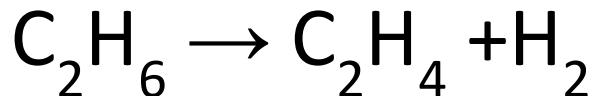
Composition of the product stream:

- $\text{C}_2\text{H}_6 = (42.4/140.1)*100 = 30.3\%$
- $\text{C}_2\text{H}_4 = (40/140.1)*100 = 28.6\%$
- $\text{H}_2 = (37.5/140.1)*100 = 26.7\%$
- $\text{CH}_4 = (5.2/140.1)*100 = 3.7\%$
- Inerts =  $(15/140.1)*100 = 10.7\%$



# Problem (molecular and elemental balances)

- Consider the following process:

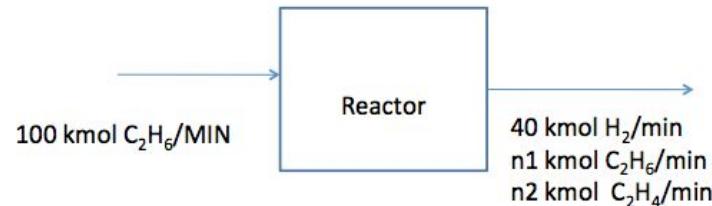


- Solve for n<sub>1</sub> and n<sub>2</sub> using molecular species and elemental species balances.



We may write the following molecular species balances:

H<sub>2</sub> balance:



Generation of H<sub>2</sub> = output of H<sub>2</sub> = 40 kmol/min

C<sub>2</sub>H<sub>6</sub> Balance:

Input = output +consumption

$$100 = n1 + 40 ; \quad n1 = 60 \text{ kmol/min}$$

C<sub>2</sub>H<sub>4</sub> balance:

Generation of C<sub>2</sub>H<sub>4</sub> = output of C<sub>2</sub>H<sub>4</sub>

$$40 = n2$$



- Or we may write **elemental species balance**

There are two species: C & H

C balance:

Mol C In = mol C out

So,  $200 = 2n_1 + 2n_2$  (Since 100 Kmol of  $C_2H_6$  have 200 Kmol of C)

H balance:

Mol H In = mol H out

$$600 = 40*2 + n_1*6 + n_2*4$$

Solving the above two equations simultaneously

$$n_1 = 60 \text{ kmol/min}$$

$$n_2 = 40 \text{ kmol/min}$$

