

# UNIT # 06

## THERMODYNAMICS

## EXERCISE # 1

$$1. \quad m_{Zn} \cdot S_{Zn} \cdot (T_f - T_i) + m_{H_2O} \cdot S_{H_2O} \cdot (T_f - T_i) = 0$$

$$(65.38 \text{ gm}) (0.4 \text{ J/g C}) (T_f - 20 \text{ C}) + 180 \text{ gm} (4.20 \text{ J/g C}) (T_f - 100 \text{ C}) = 0$$

$$\Rightarrow [(65.38) (0.4) + 180(4.20)]$$

$$T_f = (65.38) (0.4) (20) + (180) (4.20) (100)$$

$$T_f = \left[ \frac{(65.38)(0.4)(20) + (180)(4.20)(100)}{(65.38)(0.4) + (180)(4.20)} \right] = 97.3^\circ\text{C}$$

$$2. \quad \Delta U = q + w$$

$$\text{heat absorb (q)} = 45 \text{ joule}$$

$$w = -70 \text{ joule since}$$

$$\text{Work done by the system.}$$

$$(\text{तंत्र द्वारा किया गया कार्य})$$

$$\Delta U = q + w = 45 - 70 = -25 \text{ joule}$$

$$3. \quad \text{Decrease in internal energy} = -\Delta U$$

$$(\text{आन्तरिक ऊर्जा में कमी})$$

$$\text{work done by the system} = -w$$

$$-\Delta U = -w \Rightarrow \Delta U = w \Rightarrow q = 0$$

$$\text{The process is adiabatic. (प्रक्रम रूद्धोष्म है)}$$

$$4. \quad \text{At constant volume } w_{PV} = 0$$

$$\Rightarrow \boxed{\Delta U = q} \text{ first law}$$

$$5. \quad \text{The energy due to external field is not included in internal energy like gravitational field, earth's magnetic field etc.}$$

$$(\text{बाह्य क्षेत्र के कारण ऊर्जा को आन्तरिक ऊर्जा में सम्मिलित नहीं किया जाता, जैसे गुरुत्वीय क्षेत्र, पृथ्वी का चुम्बकीय क्षेत्र आदि})$$

$$6. \quad \text{Heat and work are path dependent, or indefinite quantity.}$$

$$(\text{उष्मा तथा कार्य पथ पर निर्भर करते हैं या अपरिमित मात्राएँ हैं})$$

$$7. \quad \text{For monoatomic ideal gas total degree of freedom} = 3$$

$$(\text{एक परमाण्विक आदर्श गैस के लिए स्वतंत्रता की कुल कोटि} = 3)$$

$$\text{Three translational mode of motion (गति के तीन स्थानान्तरण रूप)}$$

$$C_V = 3 \cdot \frac{1}{2} R = \frac{3}{2} R \quad C_P = C_V + R = \frac{5}{2} R$$

$$r = \frac{C_P}{C_V} = \frac{5}{3}$$

$$8. \quad \text{Ar} = \text{monoatomic ideal gas} \quad C_V = \frac{3}{2} R$$

$$\text{At constant pressure } q = \Delta H = nC_P \Delta T$$

$$q = (0.25 \text{ mole}) \frac{5}{2} \cdot (8.314 \text{ J/K mole}) (16)$$

$$9. \quad \text{Reversible process involve infinitesimally small driving force. Hence system and surrounding remains in equilibrium.}$$

$$(\text{उत्क्रमणीय प्रक्रम में प्रेरित बल अत्यन्त सुक्ष्म होता है। अतः तंत्र तथा परिवेश साम्य में होते हैं})$$

$$10. \quad \text{temperature at 'a'} = T_0 = \frac{PV}{R}$$

$$\text{at (a)} \quad T_0 = \frac{P_0 V_0}{R} \dots\dots\dots(i)$$

$$\text{at (c)} \quad T_c = \frac{(2P_0)(4V_0)}{R} = 8 T_0$$

$$\Delta U = nC_V (T_f - T_i) = \frac{3}{2} R (8T_0 - T_0)$$

$$\boxed{\Delta U = \frac{21RT_0}{2} = 10.5 RT_0}$$

$$12. \quad \text{Work done in adiabatic process (रूद्धोष्म प्रक्रम में किया गया कार्य)}$$

$$\Delta U = w = nC_V \Delta T$$

$$w = (2)(12.5)(200 - 300)$$

$$13. \quad \text{The case of irreversible adiabatic process.}$$

$$w = -P(V_f - V_i)$$

$$\Rightarrow nC_V (T_2 - T_1) = -P(V_f - V_i) \quad n = 1$$

$$C_V = \frac{3}{2} R \quad T_1 = T$$

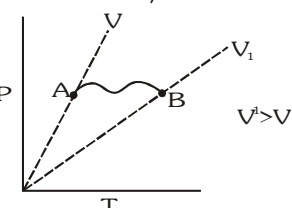
$$T_2 = \frac{-P(V_f - V_i)}{nC_V} + T = T - \frac{(1 \text{ atm})(2L - 1L)}{\frac{3}{2}(R)}$$

$$T_2 = T - \frac{2(L \text{ atm})}{3 \times 0.0821 (L \text{ atm } K^{-1} \text{ mole}^{-1})}$$

$$15. \quad V_B > V_A \text{ and } T_B > T_A$$

$$\Delta H = nC_P (T_B - T_A) > 0$$

$$w = -P_{\text{ext}} (V_B - V_A) < 0$$



$$16. \quad \text{Heat of reaction at const. pressure} = \Delta_r H$$

$$\text{Heat of reaction at const. pressure} = \Delta_r U$$

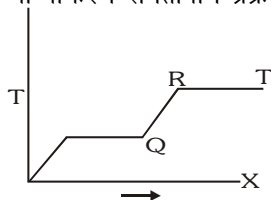
$$\Delta_r H = \Delta_r U + \Delta n_g RT$$

$$\Delta n_g = -3$$

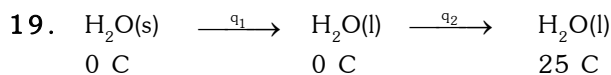
$$\Delta_r H - \Delta_r U = (-3 RT)$$

18. Fusion and vaporisation are example of isothermal processes -

(गलन तथा वाष्पीकरण समतापीय प्रक्रम के उदाहरण हैं)



$$T_f < T_b \quad PQ - T_f \quad RT - T_b$$



$$q_1 = \Delta H_{\text{fusion}} (\text{kJ/mole}) \left( \frac{36}{18} \text{mole} \right)$$

$$q_1 = 6.01 \times 2 = 12.02 \text{ kJ}$$

$$q_2 = mS \Delta T = (36 \text{ gm}) (4.18 \text{ J/K gm}) 25$$

$$q_{\text{NET}} = q_1 + q_2 = \left[ 12.02 + \frac{(36)(25)(4.18)}{1000} \right] \text{kJ}$$

20. When ice  $\rightleftharpoons$  liquid : the process is reversible fusion. The fusion is isothermal process.

(जब बर्फ  $\rightleftharpoons$  द्रव : प्रक्रम उत्क्रमणीय गलन है। गलन समतापीय प्रक्रम है)

$$C = \frac{dq}{dT} = \frac{dq}{0} \rightarrow \infty$$

21.  $\Delta U = q + w$

$$P = \text{constant since } \Delta H = q_p$$

$$202.6 = \Delta U + 1 \text{ atm (2 litres)}$$

$$\Rightarrow \Delta U = 202.6 - 2(\text{L atm}) (101.325 \text{ J/L atm})$$

$$\Delta U = 0$$

22. For reversible adiabatic process (उत्क्रमणीय रूद्धोष्म प्रक्रम के लिए)

$$q_{\text{rev}} = 0 \quad \Rightarrow \quad \Delta S_{\text{system}} = 0$$

23.  $\Delta S = nC_v \ln \frac{T_2}{T_1} + nR \ln \left( \frac{V_2}{V_1} \right)$

$$\Delta S = 5 \ln \frac{373}{298} + R \ln \left( \frac{10}{1} \right)$$

24. Using  $\Delta S_{\text{transition}} = \frac{\Delta H_{\text{transition}}}{T_{\text{transition}}}$

$$\Delta S_{\text{surr}} = \frac{-\Delta H_{\text{trans}}}{T}$$

$$\Delta S_{\text{trans}} = \frac{-401.7}{368}$$

$$\Delta S_{\text{surr}} = \frac{+401.7}{273}, \because \text{temperature of ice bath} = 273\text{K}$$

$$\Delta S_{\text{total}} = \frac{-401.7}{368} + \frac{401.7}{273}$$

25. Initial pressure  $P = \frac{RT}{V}$

$$P = 300 R = (300 \times 0.0821) \text{ atm}$$

$$\text{final pressure} = 1 \text{ atm}$$

$$\text{final volume ; } P_f V_f = P_i V_i$$

$$\Rightarrow V_f = \frac{P_i V_i}{P_f} = \left( \frac{(300)R}{1} \right) = 24.6 \text{ L}$$

$$\Delta S = nRT \ln \frac{V_2}{V_1}$$

$$\Delta S = R \ln \left( \frac{24.6}{1} \right)$$

26. for spontaneous reactions  $\Delta S_{\text{total}} > 0$

(स्वतः अभिक्रिया के लिए)

$$\Delta S_{\text{total}} = \Delta S_{\text{system}} + \Delta S_{\text{surr}}$$

$$\Delta S_{\text{total}} = \Delta S_{\text{system}} - \left( \frac{-X}{298} \right)$$

$$\Delta S_{\text{total}} > 0 \Rightarrow \Delta S_{\text{sys}} + \frac{X}{298} > 0$$

$$\Delta S_{\text{syst}} > \left( \frac{-X}{298} \right)$$

Hence  $\Delta S_{\text{syst}}$  can be negative but numerically smaller

than  $\frac{X}{298}$ .

(अतः  $\Delta S_{\text{syst}}$  ऋणात्मक हो सकता है, लेकिन आंकिक रूप

से  $\frac{X}{298}$  से छोटा होता है)

27. For dissociation reactions (वियोजन अभिक्रिया के लिए)

$$\Delta H > 0 \text{ and } \Delta n_g > 0 \Rightarrow \Delta_r S > 0$$

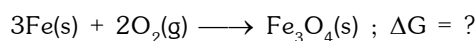
28.  $\Delta G = \Delta H - T\Delta S$

$$\Delta G = -33000 - [\pi(-58)]$$

$$\Delta G = -33000 + 58 \text{ T}$$

spontaneous but less than certain temperature.

29. Formation of  $\text{Fe}_3\text{O}_4$



$$\Delta G = \frac{1}{3} (-19 \text{ kcal}) + \frac{2}{3} (-177 \text{ kcal})$$

$$= -242.3 \text{ kcal/mole}$$

30.  $T = \frac{\Delta H^\circ}{\Delta S^\circ}$

$$\Delta H = -110 - (-266.3)$$

$$\Delta S = 197.6 + 27.28 - 5.74 - 54.49$$

Above this temperature the process becomes spontaneous. (इस ताप के ऊपर प्रक्रम स्वतः होगा)

1. Intensive property (गहन गुण)

$$= \frac{\text{extensive property (विस्तीर्ण गुण)}}{\text{extensive property}}$$

$$pH \propto \text{concentration} = \text{mole/volume}$$

though pH is a dimensionless number and intensive property (यद्यपि pH विमारहित संख्या तथा गहन गुण है)

$$EMF = \frac{\text{energy}}{\text{charge}} = \text{Intensive property}$$

$$\text{Boiling point}(T_b) = \text{temperature} = \text{intensive property}$$

$$\text{entropy (s)} = \frac{q}{T} = \frac{\text{extensive}}{\text{intensive}} = \text{extensive property}$$

2. At constant T, the molecule with maximum atoms have greatest internal energy.

(नियत T पर, अधिकतम संख्या वाले अणु के आन्तरिक ऊर्जा अधिकतम होती है)

3.  $q = 0$   $\Delta U = W$

$$\Rightarrow 3000 = C_V(T_2 - T_1)$$

$$T_2 - T_1 = \frac{3000}{20} = 150 \quad T_2 = T_1 + 150 = 450 \text{ K}$$

4. Irreversible adiabatic process (अनुक्रमणीय रुद्धोष्म प्रक्रम)

$$W = -P_{\text{ext}} \left( \frac{nRT_2}{P_2} - \frac{nRT_1}{P_1} \right) \quad P_2 = P_{\text{ext}} = 2 \text{ atm}$$

$$P_1 = 1 \text{ atm} \quad T_1 = 300 \text{ K}$$

$$W = -(2 \text{ atm}) \left[ \frac{2R \cdot T_2}{2 \text{ atm}} - \frac{2R(350)}{1 \text{ atm}} \right]$$

$$\text{and } W = 2C_V(T_2 - 350) = 2 \cdot \frac{5}{2}R(T_2 - 350)$$

$$5R(T_2 - 350) = (750R - 2RT_2)$$

$$5T_2 - 1750 = 1400 - 2T_2$$

$$7T_2 = 3150$$

$$T_2 = 450 \text{ K}$$

$$W = 2 \cdot C_V(450 - 350)$$

$$= 2 \cdot \frac{5}{2}R \times (100) = 500R$$

$$W = W_{AB} + W_{BC} + W_{CD}$$

$$= -P_0(V_B - V_A) - nRT_B \ln \left( \frac{V_C}{V_B} \right) - \frac{P_0}{2}(V_D - V_C)$$

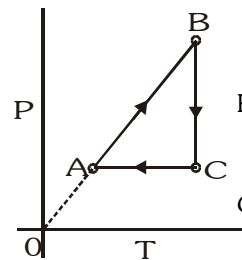
$$W = -P_0(2V_0 - V_0) - 2P_0V_0 \ln$$

$$\left( \frac{4V_0}{2V_0} \right) - \frac{P_0}{2}(2V_0 - 4V_0)$$

$$W = -2P_0V_0 \ln 2 \text{ and } q = -W (\because \Delta U = 0)$$

$$q = 2P_0V_0 \ln 2$$

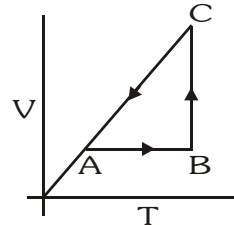
- 5.



AB = isochoric heating  
(समआयतनिय तापन)

BC = isothermal expansion  
(समतापीय प्रसार)

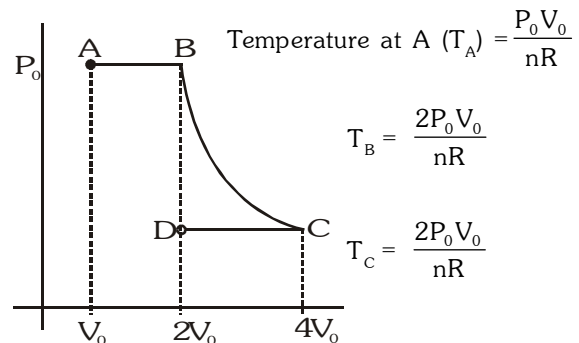
CA = isobaric cooling  
(समदाबीय शीतलन)



AB = isochoric heating

BC =

- 6.



$$\text{Temperature at A } (T_A) = \frac{P_0 V_0}{nR}$$

$$T_B = \frac{2P_0 V_0}{nR}$$

$$T_C = \frac{2P_0 V_0}{nR}$$

$$T_D = \frac{(P_0/2) \cdot 2V_0}{nR} = \frac{P_0 V_0}{nR} = T_A$$

$$\text{now } \because T_D = T_A : \Delta U = \Delta H = 0$$

$$\left\{ \begin{array}{l} \text{remember for ideal gas } \Delta U = nC_V \Delta T \\ \Delta H = nC_P \Delta T \end{array} \right\}$$

7.  $A(P_1, V_1, T_1) \xrightarrow[\Delta H_1]{\text{Isochoric heating}} B(P_2, V_1, T_2)$

$$\downarrow \Delta H_2 \text{ irr. adiabatic process } (q=0)$$

$$\Delta H_{\text{overall}} = \Delta H_1 + \Delta H_2 \quad C(P_3, V_2, T_2)$$

$$\Delta H_1 = \Delta U_1 + (P_2 V_1 - P_1 V_1)$$

$$\Delta H_1 = C_V(T_2 - T_1) + (P_2 V_1 - P_1 V_1)$$

$$\Delta H_2 = \Delta U_2 + (P_3 V_2 - P_2 V_1)$$

$$\Delta H_2 = -P_3(V_2 - V_1) + (P_3 V_2 - P_2 V_1)$$

$$\Delta H_2 = P_3 V_1 - P_2 V_1$$

$$\Delta H_{\text{overall}} = C_V(T_2 - T_1) + (P_2 V_1 - P_1 V_1) + P_3 V_1 - P_2 V_1$$

$$= C_V(T_2 - T_1) + P_3 V_1 - P_1 V_1$$

$$8. \quad \eta = \frac{T_2 - T_1}{T_2}$$

$$\eta = \frac{373 - 298}{373} = \left(\frac{75}{373}\right)$$

$$\eta \quad 100 =$$

$$9. \quad \eta = \frac{T_2 - T_1}{T_2}$$

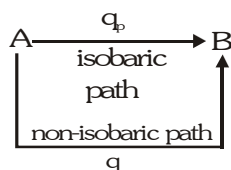
$$\eta = \frac{500 - 300}{500} = \frac{2}{5}$$

$$\eta = \frac{W_{by}}{q_{source}} \Rightarrow W_{by} = (n_C) (q_{source})$$

$$= \left(\frac{2}{5}\right) (2 \text{ kcal}) = 0.8 \text{ kcal}$$

$$10. \quad \Delta H = q_p$$

since H is state function  $\Delta H$  will remain same from both path-isobaric and non-isobaric



But  $q = q_p$  only when path was isobaric.

$\Delta H = q_p$  only for isobaric path.

$$11. \quad \text{Greater the } \Delta n_g \text{ greater the value of } \Delta S.$$

$$12. \quad \Delta S = nC_V \ln \left( \frac{T_2}{T_1} \right) \text{ for isochoric change.}$$

$$\Delta S = 2 \left( \frac{3}{2} R \right) \ln \left( \frac{573}{473} \right)$$

$$\Delta S = 3R \ln \left( \frac{573}{473} \right)$$

$$13. \quad \text{The net heat absorbed by hot and cold body is equal to zero.}$$

$$q_H + q_C = 0$$

Let  $C_V$  is the total heat capacity of hot and cold body.

$$C_V(T_f - T_C) + C_V(T_f - T_H) = 0$$

$$\Rightarrow T_f = \frac{T_H + T_C}{2}$$

$$\text{Entropy change } \Delta S_{\text{Total}} = \Delta S_{\text{hot body}} + \Delta S_{\text{cold body}}$$

$$\Delta S_{\text{hot body}} = C_V \cdot \ln \left( \frac{T_f}{T_H} \right)$$

$$\Delta S_{\text{cold body}} = C_V \cdot \ln \left( \frac{T_f}{T_C} \right)$$

$$\Delta S_{\text{Total}} = C_V \left( \ln \frac{T_f}{T_H} + \ln \frac{T_f}{T_C} \right)$$

$$= C_V \left( \ln \frac{T_f^2}{T_H \cdot T_C} \right)$$

$$\Delta S_{\text{Total}} = C_V \ln \left[ \frac{(T_f + T_C)^2}{4 T_H \cdot T_C} \right]$$

$$14. \quad \Delta G = \Delta H - T \Delta S$$

$$y = C + mX$$

$$\Rightarrow \Delta H = C$$

$$m = -\Delta S$$

from intercept  $C > 0 \Rightarrow \Delta H > 0$

$$m < 0 \Rightarrow -\Delta S < 0$$

$$\Rightarrow \Delta S > 0$$

$$15. \quad \text{Melting of } H_2O(s) \text{ at } 0^\circ C \text{ and } 1 \text{ atm is a reversibly process } \Rightarrow \Delta S_{\text{Total}} = 0$$

Vaporisation of  $H_2O(l)$  at  $373 \text{ K}$  is a reversible process  $\Delta S_{\text{Total}} = 0$

Below  $0^\circ C$  -  $H_2O(s) \longrightarrow H_2O(l)$  is non spontaneous not feasible.

$H_2O(l) \longrightarrow H_2O(s)$  (freezing) is feasible above  $0^\circ C$

$H_2O(s) \longrightarrow H_2O(l)$

feasibly  $\Rightarrow \Delta G = -ive$  for melting process  $\Rightarrow \Delta S_{\text{Total}}$  increases

$$19. \quad \Delta G = \Delta H + \Delta E$$

$$\Delta G = -3000 - 1 \quad 2 \quad 300 + 3000$$

$$= -6000 \text{ cal}$$

$$20. \quad H_2O(l) \longrightarrow H_2O(g)$$

$$373 \text{ K} \quad 373 \text{ K}$$

$$1 \text{ atm} \quad 1 \text{ atm}$$

$$\Delta S = \frac{\Delta H_{\text{vap}}}{T}$$

$$\Delta G = \Delta H_f - \Delta H_i = 0$$

**COMPREHENSION # 1**

1.  $U = \alpha \sqrt{V}$  Here  $U$  = Kinetic energy of ideal gas  
(आदर्श गैस की गतिज ऊर्जा)

$$U = nC_v T$$

$$\Rightarrow nC_v T = \alpha \sqrt{V} \dots(i) \quad T = \frac{PV}{nR} \dots(ii)$$

sub. (2) in (1)

$$\left(\frac{C_v}{R}\right) \cdot PV = \alpha \sqrt{V}$$

$$\Rightarrow P = \left(\frac{\alpha R}{C_v}\right) \frac{1}{\sqrt{V}}$$

$$w = -\int P dV = -\left(\frac{\alpha R}{C_v}\right) \int \frac{dV}{\sqrt{V}}$$

$$= -(\alpha)(\gamma - 1) \cdot \frac{1}{(1/2)} (\sqrt{V}) \Big|_{V_1}^{V_2}$$

$$w = -2(\alpha)(\gamma - 1)(\sqrt{V_2} - \sqrt{V_1})$$

work done by the gas =  $-w = 2(\alpha)$

$$(\gamma - 1)(\sqrt{V_2} - \sqrt{V_1})$$

2. For diatomic gas with no vibrational degree of freedom

$$C_v = \frac{3}{2}R + 2 \cdot \frac{1}{2}R$$

$$C_v = 5/2 R$$

$$\Delta U = \alpha(\sqrt{V_2} - \sqrt{V_1}) = 100 \text{ J}$$

$$w = 2(\alpha)(\gamma - 1)(\sqrt{V_2} - \sqrt{V_1}) = (2)(\gamma - 1) \cdot 100$$

$$\therefore \gamma = \frac{C_p}{C_v} = \frac{7}{5}$$

$$(\gamma - 1) = \left(\frac{7}{5} - 1\right) = \left(\frac{2}{5}\right)$$

$$w = (2)\left(\frac{2}{5}\right)(100)\text{J} = 80\text{J}$$

$$3. \quad \Delta U = q + w \Rightarrow 100\text{J} = q - 80\text{J}$$

$$q = 180 \text{ J}$$

**COMPREHENSION # 2**

$$1. \quad \Delta_r S = S(\text{CH}_3\text{OH}, g)$$

$$- [S(\text{CO}, g) + 2 S(\text{H}_2, g)]$$

$$= 240 - 198 - 2 \cdot 29 = -16 \text{ J/K-mole}$$

$$2. \quad \Delta_r H = \Delta_f H(\text{CH}_3\text{OH}, g)$$

$$- \Delta_f H(\text{CO}, g) = -201 - (114) = -315 \text{ kJ/mol}$$

$$3. \quad \Delta_r S_{T_2}^\circ - \Delta_r S_{T_1}^\circ = \Delta C_p^\circ \ln \frac{T_2}{T_1}$$

$$\Delta C_p^\circ = C_{p,m}^\circ(\text{CH}_3\text{OH}) - [C_{p,m}^\circ(\text{CO}) + 2C_{p,m}^\circ(\text{H}_2)]$$

$$= 44 - (29.4 + 2 \cdot 28.8) = -43 \text{ J/K-mol}$$

$$\Delta_r S_{T_2}^\circ - (-16) = (-43) \ln \frac{320}{300}$$

$$\Delta_r S_{T_2}^\circ = -13.225 \text{ J/K-mol}$$

$$4. \quad \Delta_r H_{T_2}^\circ - \Delta_r H_{T_1}^\circ = \Delta_r C_p^\circ (T_2 - T_1)$$

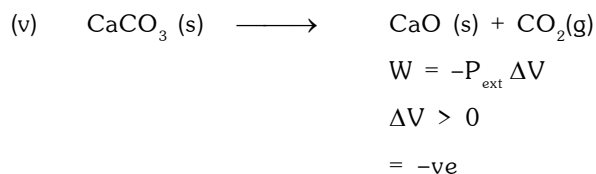
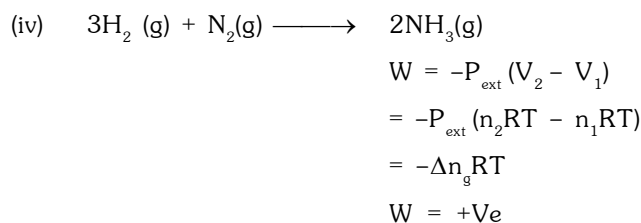
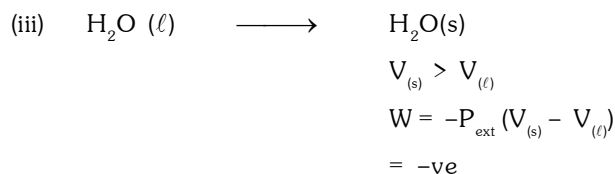
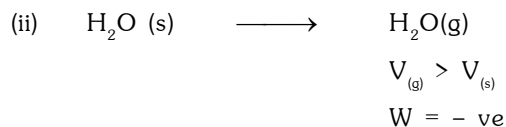
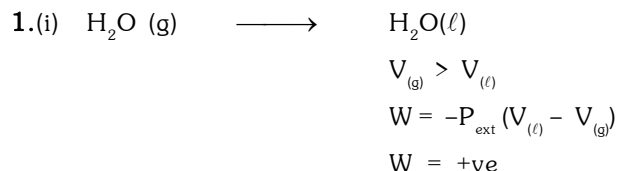
$$\Delta_r H_{T_2}^\circ - (-87) = -43(320 - 300)$$

$$\Delta_r H_{T_2}^\circ = -87.86 \text{ kJ/mol}$$

$$5. \quad \Delta_r G = \Delta_r H_{T_2}^\circ - T \Delta T \Delta S_{T_2}^\circ$$

$$= -87860 - 320(-13.225)$$

$$= -81.91 \text{ kJ/mol}$$



2.  $\Delta E = -65 \text{ J}$   $w = 20 \text{ J}$   
 $\Delta q = \Delta V - w$   $-65 = \Delta V - 20$   
 $\Delta V = -45 \text{ J}$

3.  $\Delta H_{\text{glucose}} = -2808 \text{ kJ mol}$

(a) Energy need to climb  $3\text{m} = Mgh = 62.5 \times 10 \times 3$   
 $\Delta q = 1875 \text{ Joule}$

Now useful energy from 1 mole of glucose  
 $= 2808 \times \frac{1}{4} = 702 \text{ kJ}$

$\Rightarrow$  No. of mole of glucose required  $= \frac{1875}{702 \times 10^3}$

$= 2.67 \times 10^{-3} \text{ mole}$

grams of glucose  $= 180 \times 2.67 \times 10^{-3} = 0.4807 \text{ gm}$

(b) Energy need to climb  $3000 \text{ m}$  will be  $10^3$  time.  
 $\Rightarrow$  wt. should be  $10^3$  time  $= 0.4807 \text{ kg}$

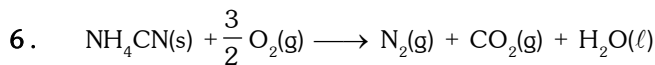
4.  $q_p = q_v + \Delta n_g RT$   
 $40.66 - 2 = q_v + 2 \times 8.314 \times 373$   
 $\Rightarrow q_v = (81.32 - 6.202) \text{ kJ}$   
 $q_v = 75.118 \text{ kJ}$

5.  $\Delta H = 1 \text{ kcal}$   
 $\Delta H = \Delta E + P\Delta V$

$1 \times 10^3 \times 4.18 = \Delta E + 1.013 \times 10^5 \times 3 \times 10^{-3}$

$\Delta E = (4180 - 30.39) \text{ Joule} = \left( \frac{4149.61}{4.18} \right) \text{ cal}$

$\Delta E = 0.993 \text{ kcal}$



$\Delta H_{298} = \Delta E + \Delta n_g RT = -742.7 + \frac{1}{2} \times 8.314 \times 298$

$= -742.7 + 1.239$

$\Delta H_{298} = -741.46$

7.  $\Delta H = 1440 \text{ cal}$

$\Delta H = \Delta E + P(V_2 - V_1)$

$1440 = \Delta E + 1.013 \times 10^5 (0.0180 - 0.0196) \times 10^{-3}$

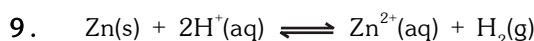
$\Delta E = 1440 - 1.013 \times 0.0016 \times 10^{-3}$

$\Delta E = 1440.168$

8.  $W = \int P_{\text{ext}} dV$

$= - \int P(V_2 - V_1) = -1.01 \times 10^5 (0.1) \times 10^{-3}$

$W = -10.1 \text{ J}$



$\Delta H = -36.5 \text{ kJ}$

$\Delta Q = \Delta E - W -36.5 \text{ kJ}$

$= \Delta E + 1.01 \times 10^5 (500 - 50) \times 10^{-6}$

$\Delta E = -39.03 \text{ kJ}$

$W = -P_{\text{ext}}(V_2 - V_1) = -1.013 \times 10^5 \times 500 \times 50 \times 10^{-6}$

$W = -2.53$

10.  $W_{\text{irr}} = -nRT \left( 1 - \frac{P_2}{P_1} \right) = -5 \times 8.314 \times 300 \left( 1 - \frac{1}{4} \right)$

$W_{\text{irr}} = -9.353 \text{ kJ}$

$W_{\text{rev}} = -2.303 nRT \log \left( \frac{V_2}{V_1} \right)$

$W_{\text{rev}} = -2.303 \times 5 \times 8.314 \times 300 \log 4$

$W_{\text{rev}} = -17.29 \text{ kJ}$

and  $\Delta q = \Delta E - W$

at  $\Delta T \rightarrow 0 \Delta E \rightarrow 0 \quad \Delta H \rightarrow 0$

$W_{\text{rev}} = -q = 17.29 \text{ kJ}$

11.  $n_1 = 1$   
 $T_1 = 300 \quad V_2 = 27 V_1 \quad T_1 V_1^{\gamma-1} = T_2 V_2^{\gamma-1}$   
 $\left(\frac{T_1}{T_2}\right) = \left(\frac{V_2}{V_1}\right)^{\gamma-1} \quad T_2 = 300 \left(\frac{1}{27}\right)^{\frac{1}{3}}$   
 $T_2 = 100 \text{ K}$   
 Adiabatic condition  $\Delta Q = 20 \Rightarrow \Delta E = W = nC_v(T_2 - T_1)$   
 $W = 1 \cdot 25 \cdot -200 \quad W = -5.000 \text{ kJ/mole}$

12. Process reversibly adiabatic

$T_1 = 298.15 \text{ K} \quad V_2 = 2V_1$   
 $T_2 = 248.44 \text{ K} \quad P V^\gamma = K \quad PV = nRT$   
 $\frac{T}{V} \cdot V^\gamma = K \quad T_1 V_1^{\gamma-1} = T_2 V_2^{\gamma-1}$   
 $\left(\frac{T_1}{T_2}\right) = \left(\frac{V_2}{V_1}\right)^{\gamma-1} \quad \left(\frac{298.15}{248.44}\right) = 2^{\gamma-1}$   
 $1.2 = 2^{\gamma-1} \quad \log 1.2 = \log 2 \cdot (\gamma-1)$   
 $\gamma - 1 = \frac{\log 1.2}{\log 2} \quad \gamma - 1 = 0.263$

Now  $nC_v (T_2 - T_1) = \frac{P_2 V_2 - P_1 V_1}{\gamma - 1}$   
 $C_{v,m} = \left(\frac{R}{\gamma - 1}\right) = \frac{nR(T_2 - T_1)}{(\gamma - 1)}$   
 $C_{v,m} = \frac{8.314}{0.263} \quad C_{v,m} = 31.61$

13.  $W = -2.303 nRT \log\left(\frac{P_1}{P_2}\right)$   
 $= -2.303 \cdot 1 \cdot 8.314 \cdot 298 \log\left(\frac{1}{5}\right)$   
 $W = -3.988 \text{ kJ}$

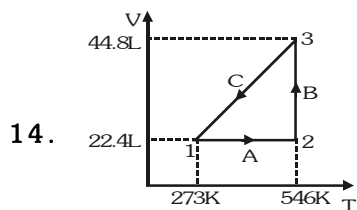


Table-1			
State	P	V	T
1	1	22.4L	273
2	2atm	22.4	546K
3	1atm	44.8	546K

State - 1

$$PV = nRT \Rightarrow P = 1 \text{ atm}$$

State - 2

$$\frac{P_1}{T_1} = \frac{P_2}{T_2} \Rightarrow P_2 = 2 \text{ atm}$$

$$P_2 = \frac{546}{273} \times 1 \text{ atm}$$

State - 3

$$P_1 V_1 = P_2 V_2$$

$$\frac{1}{2} \cdot 22.4 = 44.8 \quad P_2$$

$$P_2 = 1 \text{ atm}$$

Step	Name of process	q	w	$\Delta E$	$\Delta H$
A	Isochoric	$\frac{3}{2}R(273)$	0	$\frac{3}{2}R(273)$	$\frac{5}{2}R(273)$
B	Isotherm	$546R \ln 2$	$-546R \ln 2$	0	0
C	Isotherm	$-\frac{5}{2}R(273)$	$R(273)$	$\frac{3}{2}R(273)$	$\frac{5}{2}R(273)$
overall					

State - A  $\rightarrow$  (Isochoric)

$$W = 0 \quad \Delta q = \Delta E$$

$$\Rightarrow 1 \cdot \frac{3}{2}R(273)$$

$$\Delta H = nC_p dT \quad \Delta H = 1 \cdot \frac{5}{2}R(273)$$

State - B  $\rightarrow$  (Isothermal)

$$\Delta E = 0 \quad \Delta H = 0$$

$$\therefore \Delta H = \Delta E + \Delta PV$$

$$\text{is } Q = -w = +2.303 \cdot 1 \cdot 8.314 \log(2) \cdot 546$$

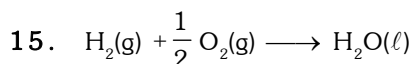
$$Q = 546 R \ln 2 \quad W = -546 R \ln 2$$

$$\Delta E = nC_v \Delta T \quad W = nR(T_2 - T_1)$$

State - C  $\rightarrow$  (Isobaric)

$$\Delta q = \Delta E - w = \Delta E + P(V_2 - V_1)$$

$$\text{or } \Delta H = \Delta E + P\Delta V = \frac{5}{2}R(-273)$$



$$\Delta C_{p, \text{reaction}} = C_{p, \text{H}_2\text{O}(\ell)} - C_{p, \text{H}_2(\text{g})} - \frac{1}{2} C_{p, \text{O}_2(\text{g})}$$

$$= 75.312 - 38.83 - \frac{1}{2} \cdot 29.16$$

$$\Delta C_{p, \text{reaction}} = 21.90 \text{ kJ}$$

$$\Delta H_{373} = \Delta H_{298} + nC_p \Delta T$$

$$= (-285.76 + 1 \cdot 21.9 \cdot 75 \cdot 10^{-3}) \text{ kJ}$$

$$\Delta H_{373} = -284.12 \text{ kJ}$$

16.  $C_p = 22.34 + 48.1 \cdot 10^{-3} T \text{ JK}^{-1} \text{ mol}^{-1}$

$$\Delta H = \int_{T_1}^{T_2} nC_p dT = \int_{273}^{546} (22.34 + 48.1 \times 10^{-3} T) dT =$$

$$22.34 \cdot 273 + \frac{48.1 \times 10^{-3} \times 273 \times 3}{2} \cdot 273$$

$$\Delta H = 13.064 \text{ kJ/mole}$$

$$W = -P(V_2 - V_1) = -nR(T_2 - T_1)$$

$$W = -20477$$

$$\Delta E = 13.064 - 2.477$$

$$\Delta E = 10.587 \text{ kJ}$$

$$17. \Delta S = 28.8 \text{ J/K} \quad \Delta H = 30.5 \text{ kJ}$$

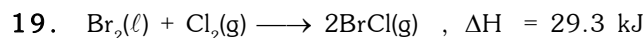
$$\Delta H = T \Delta S \quad \frac{30.5 \times 10^3}{28.8} = T = 1059 \text{ K}$$

$$18. \Delta S = \frac{n C_p dT}{T}$$

$$= 1 \int \left( \frac{25.5}{T} + 13.6 \cdot 10^{-3} - 42.5 \cdot 10^{-7} T \right) dT$$

$$= 2.303 \cdot 25.5 \log 2 + 13.6 \cdot 10^{-3} \cdot 300 - 42.5 \cdot 10^{-7} \frac{(600^2 - 300^2)}{2}$$

$$\Delta S = 20.618 \text{ kJ}$$



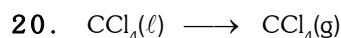
$$\Delta S_{\text{Br}} = 152.3 \quad \Delta S_{\text{Cl}_2(g)} = 223.0$$

$$\Delta S_{\text{BrCl}(g)} = 239.7 \text{ J mol}^{-1} \text{ K}^{-1}$$

$$\Delta S_R = 2 \cdot 239.7 - 223 - 152.3 = 104.4$$

$$\Delta_r G = \Delta H - T \Delta S$$

$$= 29300 - 298 \cdot 104.4 = -1721.8 \text{ J}$$



$$P = 1 \text{ atm}$$

$$T = 298 \text{ K} \quad \Delta S = 94.98 \text{ JK}^{-1}$$

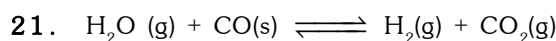
$$\Delta_r H = \Delta H_p - \Delta H_r = (-106.7 + 139.3) \text{ kJ}$$

$$= 32.6 \text{ kJ/mol}$$

$$\Delta_r G = \Delta H_R - T \Delta S$$

$$\Delta_r G = 32.6 \cdot 10^3 - 298 \cdot 94.98$$

$$\Delta_r G = 4.296 \text{ kJ/mol}$$



$$(i) \Delta_r H_{298}$$

$$= \Delta_r H_{\text{H}_2(g)} + \Delta_r H_{\text{CO}_2(g)} - \Delta_r H_{\text{CO}(s)} - \Delta_r H_{\text{H}_2\text{O}(g)} =$$

$$-94.05 + 26.42 + 57.8 = -9.83 \text{ k cal/mol}$$

$$(ii) \Delta_r G = -94.24 + 0 + 32.79 + 54.64$$

$$\Delta_r G = -6.81$$

$$(iii) \Delta_r G = \Delta_r H - T \Delta_r S \quad -6.81 = -9.83 - 298 \Delta_r S$$

$$\frac{9.83 - 6.81}{298} = -\Delta_r S$$

$$\Delta_r S = -10.13 \text{ cal/mole}$$

$$(iv) \text{ but at constant P}$$

$$\Delta H = \Delta E + \Delta PV \quad \therefore \Delta n_g = 0$$

$$\Delta_r H = \Delta_r E_{298} = -9.83 \text{ k cal/mol}$$

$$(v) S_{298} [\text{H}_2\text{O}(g)]$$

$$\Delta_r S = \Delta_s \text{H}_2\text{O}(g) + \Delta S_{\text{CO}} - \Delta_r S_{\text{H}_2} - \Delta_r S_{\text{CO}}$$

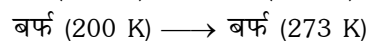
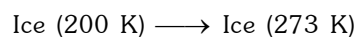
$$-10.13 = -\Delta_r S_{\text{H}_2\text{O}(g)} + 47.3 + 31.2 + 51.1$$

$$\Delta_r S_{\text{H}_2\text{O}(g)} = 45.13 \text{ cal/K mole}$$

## THERMODYNAMICS

## EXERCISE # 4[B]

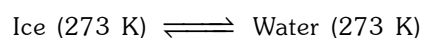
1. Step-1 (पद-1)



$$\Delta S_1 = m C_p \ln \frac{T_2}{T_1} = 1 \cdot 2.09 \cdot 10^3 \ln \frac{273}{200}$$

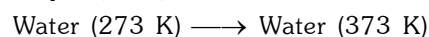
$$\Delta S_1 = 650.312 \text{ J/C}$$

Step-2 (पद-2)



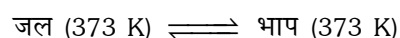
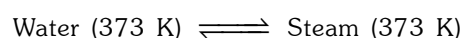
$$\Delta S_2 = \frac{\Delta H_f}{273} = \frac{3.34 \times 10^5}{273} = 1223.44 \text{ J/C}$$

Step-3 (पद-3)



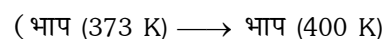
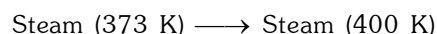
$$\Delta S_3 = 1 \cdot 4.18 \cdot 10^3 \ln \frac{373}{273} = 1304.6 \text{ J/C}$$

Step-4 (पद-4)



$$\Delta S_4 = \frac{\Delta H_v}{373} = \frac{22.6 \times 10^5}{373} = 6058.98 \text{ J/C}$$

Step-5 (पद-5)



$$\Delta S_5 = 1 \cdot 2.09 \cdot 10^3 \ln \frac{400}{373} = 146.06 \text{ J/C}$$

$$\Delta S_T = 9383.4 \text{ J/C}$$

$$2. \gamma = \frac{5}{3}, P_1 = 1 \text{ atm}, T_1 = 300 \text{ K}, P_2 = 2 \text{ atm}$$

$$(a) PV^\gamma = \text{constant (नियतांक)}$$

$$P^{1-\gamma} T^\gamma = \text{constant}$$

$$TP^{(1-\gamma)/\gamma} = \text{constant}$$

$$T_1 P_1^{(1-\gamma)/\gamma} = T_2 P_2^{(1-\gamma)/\gamma}$$

$$T_2 = 300 \left( \frac{1}{2} \right)^{-2/5} = 395.85$$

$$w = \Delta U = n C_v dT = 1 \cdot \frac{3}{2} \cdot 8.314 \cdot 95.85$$

$$w = 1195.37 \text{ J}$$

$$V_2 = \frac{nRT_2}{P_2} = 16.25 \text{ L}$$



(b)  $\Delta U = w$   
 $1 \quad 1.5 \quad 8.314 (T_2 - 300)$   
 $= -2 \quad 101.3 \left( \frac{RT_2}{P_2} - \frac{RT_1}{P_1} \right)$   
 $(T_2 - 300) = 1.333 \left( 300 - \frac{T_2}{2} \right)$   
 $T_2 = 420 \text{ K} \quad V_2 = \frac{nRT_2}{P_2} = 17.24 \text{ L}$   
 $w = \Delta U = 1.5 \quad 8.314 (420 - 300)$   
 $w = 1496.52 \text{ J}$

3.  $V_1 = 20 \text{ L}, \gamma = 7/5, T_1 = 673 \text{ K},$   
 $P_1 = 0.2 \text{ MPa} = 2 \text{ atm}, P_2 = 0.7 \text{ MPa} = 7 \text{ atm}$   
 $n = \frac{P_1 V_1}{RT_1} = 2.5$

(i)  $\Delta U = \Delta H = 0$   
 $q = -w = nRT \ln \frac{P_1}{P_2} = 2.5 \quad 8.314 \quad 673 \ln \frac{7}{2}$   
 $q = 17.52 \text{ kJ} \quad w = -17.52 \text{ kJ}$

(ii)  $P_1 V_1^\gamma = P_2 V_2^\gamma$   
 $7(20)^\gamma = 2(V_2)^\gamma \Rightarrow V_2 = (3.5)^{5/7} = 48.92 \text{ L}$   
 $T_2 = \frac{P_2 V_2}{nR} = 470.46 \text{ K}$   
 $q = 0, w = \Delta U = 2.5 \quad 2.5 \quad 8.314 (470.46 - 673)$   
 $w = \Delta U = -10.524 \text{ kJ}$   
 $\Delta H = 2.5 \quad 3.5 \quad 8.314 (470.46 - 673) = -14.73 \text{ kJ}$

(iii)  $q = w = \Delta U = \Delta H = 0$

(iv)  $q = 0, \Delta U = w$   
 $2.5 \quad 2.5 \quad 8.314 (T_2 - 673)$   
 $= -101.3 \quad 2 \quad 2.5 \quad 0.0821 \left( \frac{T_2}{2} - \frac{T_1}{7} \right)$   
 $T_2 - 673 = -0.79 \left( \frac{T_2}{2} - 96.142 \right)$   
 $T_2 = 536.91 \text{ K}$   
 $w = \Delta U = 2.5 \quad 2.5 \quad 8.314 (-136) = -7.1 \text{ kJ}$   
 $\Delta H = 2.5 \quad 3.5 \quad 8.314 (-136) = -9.9 \text{ kJ}$

(v)  $\Delta U = \Delta H = 0$   
 $V_2 = \frac{nRT}{P_2} = \frac{2.5 \times 0.821 \times 673}{2} = 69 \text{ L}$   
 $w = -P_2 (V_2 - V_1) = -2 \quad 49 = -98.13 \text{ L-atm}$   
 $w = -98.13 \quad 101.3 = -9940.9 \text{ J}$   
 $w = -9.94 \text{ kJ} \quad q = -w = 9.94 \text{ kJ}$

4.(i) The entropy change of the system  $\Delta S_{\text{sys.}}$  will be same in all the three process as it is state function. (तंत्र की एण्ट्रॉपी में परिवर्तन  $\Delta S_{\text{तंत्र}}$  जैसा कि एक अवस्था फलन है सभी तीनों प्रक्रमों में समान रहेगा।)

$\Delta S_{\text{sys.}} = nR \ln \frac{V_2}{V_1} = 1 \quad 8.314 \ln 3 = 9.134 \text{ J/K}$   
 For reversible process (उत्क्रमणीय प्रक्रम के लिए)  
 $\Delta S_T = 0$   
 $\Delta S_{\text{surr.}} = -\Delta S_{\text{sys.}} = -9.134 \text{ J/K}$

(ii)  $\Delta S_{\text{sys.}} = 9.134 \text{ J/K}$   
 $\Delta S_{\text{surr.}} = \frac{-q_{\text{irrev.}}}{T} = - \left[ \frac{q_{\text{rev.}} - 836.6}{298} \right]$   
 $= -\Delta S_{\text{sys.}} + 2.807$   
 $\Delta S_T = \Delta S_{\text{sys.}} + (-\Delta S_{\text{sys.}} + 2.807) = 2.807 \text{ J/K}$

(iii) For free expansion system doesn't absorb any heat so  $q = 0$   
 (मुक्त प्रसार में तंत्र कोई उष्मा अवशोषित नहीं करता है अतः  $q = 0$ )  
 $\Delta S_{\text{sys.}} = 0$   
 $\Delta S_T = \Delta S_{\text{sys.}} = 2.807 \text{ J/K}$

5.(i)  $\Delta S_{\text{sys.}} = 0, \Delta S_{\text{surr.}} = 0, \Delta S_T = 0$

(ii)  $\Delta U = w, \Rightarrow n C_v (T_2 - T_1) = -P_2 (V_2 - V_1)$   
 $0.5 \quad 1.5 \quad 8.314 (T_2 - 473)$   
 $= -101.3 \quad 2 \quad 0.5 \quad 0.0821 \left( \frac{T_2}{2} - \frac{473}{5} \right)$   
 $T_2 - 473 = -1.333 \left( \frac{T_2}{2} - 94.6 \right)$   
 $T_2 = 359.49 \text{ K}$   
 $\Delta S_{\text{sys.}} = n \left[ C_p \ln \frac{T_2}{T_1} + R \ln \frac{P_1}{P_2} \right]$   
 $= 0.5 \left[ 2.5 \times 8.314 \ln \frac{359.49}{473} + 8.314 \ln \frac{5}{2} \right]$   
 $\Delta S_{\text{sys.}} = 0.957 \text{ J/K}$   
 since no heat is transferred (चूंकि ऊर्जा स्थानान्तरित नहीं होती है)  $q = 0$   
 $\Delta S_{\text{surr.}} = 0$   
 $\Delta S_T = \Delta S_{\text{sys.}} = 0.957 \text{ J/K}$

(iii) In free expansion (मुक्त प्रसार में)  $q = w = \Delta U = 0$   
 $T$  is constant. ( $T$  स्थिर है।)

$\Delta S_{\text{sys.}} = nR \ln \frac{P_1}{P_2} = 0.5 \quad 8.314 \ln \frac{5}{2} = 3.81 \text{ JK}$   
 $\Delta S_{\text{surr.}} = 0$   
 $\Delta S_T = \Delta S_{\text{sys.}} = 3.81 \text{ J/K}$

6.  $P_1 = 1 \text{ atm}, V_1 = 1 \text{ L}$   
 $P_2 = 1001 \text{ atm}, V_2 = 0.99 \text{ L}$  Let  $P = a + bV$   
 On finding (प्राप्त करने पर)  $a = 100001, b = -10^5$   
 so  
 $P = (100001 - 10^5 V)$   
 $w = -\int P dV = -\int_{V_1}^{V_2} (100001 - 10^5 V) dV$   
 $w = -100001 (V_2 - V_1) + \frac{10^5}{2} (V_2^2 - V_1^2)$   
 $w = -100001 (-0.01) + \frac{10^5}{2} (-0.0199) = 5.01$   
 $\text{L-atm}$   
 $w = 501 \text{ J} \quad \Delta U = w = 501 \text{ J}$   
 $\Delta H = \Delta U + (P_2 V_2 - P_1 V_1)$   
 $= 501 + (1001 \quad 0.99 - 1 \quad 1) \quad 100 = 99500 \text{ J}$   
 $\Delta H = 99.5 \text{ kJ}$

$$7.(i) \Delta S_{\text{sys.}} = n C_v \ln \frac{T_2}{T_1} = 1 \cdot \frac{3}{2} R \ln \frac{1000}{100} = \frac{3}{2} R \ln 10$$

$$\Delta S_T = 0 \quad (\text{Reversible process (उत्क्रमणीय प्रक्रम)})$$

$$\Delta S_{\text{surr.}} = -\Delta S_{\text{sys.}} = -\frac{3}{2} R \ln 10$$

$$(ii) \Delta S_{\text{sys.}} = \frac{3}{2} R \ln 10$$

$$w = 0$$

$$q = \Delta U = -\frac{3}{2} R (900)$$

$$\Delta S_{\text{surr.}} = -\frac{q}{T} = \frac{-3R(900)}{2 \times 1000} = -\frac{3}{2} R (0.9)$$

$$\Delta S_T = \frac{3}{2} R \ln 10 - \frac{3}{2} R (0.9) = \frac{3}{2} R (1.402)$$

$$8. \quad G = H - TS = U + PV - TS$$

$$dG = dU + PdV + VdP - TdS - SdT$$

$$w = 0, dV = 0, dU = dq = T dS \text{ so}$$

$$dG = TdS + VdP - TdS - SdT$$

$$dG = VdP - SdT \Rightarrow \Delta G = V\Delta P - \int SdT$$

$$VdP = V(P_2 - P_1)$$

$$\frac{P_2}{T_2} = \frac{P_1}{T_1} \Rightarrow \frac{P_2}{400} = \frac{1}{300} \Rightarrow P_2 = \frac{4}{3}$$

$$VdP = 24.6 (4/3 - 1) = 8.2 \text{ L-atm} = 820 \text{ J}$$

$$\int SdT = \int_{T_1}^{T_2} (10 + 0.01T) dT = 10(T_2 - T_1) + 0.005(T_2^2 - T_1^2)$$

$$SdT = 10(100) + 0.005 (400^2 - 300^2) = 1350$$

$$\Delta G = 820 - 1350 = -530 \text{ J}$$

$$9. \quad n = 2$$

$$V_1 = \frac{2 \times 0.0821 \times 300}{1} = 49.26 \text{ L}$$

$$\frac{V_1}{T_1} = \frac{T_2}{V_2} \Rightarrow \frac{49.26}{300} = \frac{V_2}{550} \Rightarrow V_2 = 90.31 \text{ L}$$

$$(i) \quad w = -P\Delta V = 1(90.31 - 49.26) = -41.05 \text{ L-atm}$$

$$w = -41.05 \cdot 101.3 = -4158.36 \text{ J} = -4.15 \text{ k}$$

$$q = \Delta H = \int n C_p dT$$

$$= 2 \left[ 12.552(T_2 - T_1) + \frac{8.368 \times 10^{-3}}{2} (T_2^2 - T_1^2) \right]$$

$$q = \Delta H = 2 \left[ 12.552(250) + \frac{8.368 \times 10^{-2}}{2} (212500) \right]$$

$$q = \Delta H = 24.04 \text{ kJ}$$

$$C_v = C_p - R = 4.238 + 8.368 \cdot 10^{-2} \text{ T}$$

$$\Delta U = \int n C_v dT = 19.9 \text{ kJ}$$

$$(iii) \quad w = 0$$

$$q = \Delta U = 19.9 \text{ kJ}$$

$$\Delta H = \int n C_p dT = 24.04 \text{ kJ}$$

$$10. \quad \text{At } 298 \text{ K,}$$

$$\Delta G = -6333 \text{ kJ/mole}$$

$$\Delta H = -5737 \text{ kJ/mole}$$

$$\& \quad \Delta G = \Delta H - T\Delta S$$

$$\text{so } \Delta S = 2 \text{ kJ/mole}$$

$$\text{At } 310 \text{ K}$$

$$\Delta G = -5737 - 2 \cdot 310 = -6357 \text{ kJ/mole}$$

$$\text{Additional non-PV work (अतिरिक्त अन-PV कार्य) =}$$

$$|\Delta G - \Delta G| = 24 \text{ kJ/mole}$$

$$11. \quad \Delta_r C_p = 33.305 - 75.312 = -42.007 \text{ J/K mole}$$

$$\Delta_r S_{323} = \frac{\Delta H}{T} = \frac{40639}{323} = 108.95 \text{ J/K mole}$$

$$d(\Delta_r S) = \frac{\Delta_r C_p dT}{T}$$

$$\Delta_r S_{373} - \Delta_r S_{323} = \Delta_r C_p \ln \frac{T_2}{T_1}$$

$$\Delta_r S_{373} = 108.95 - \left( -42.007 \ln \frac{373}{323} \right)$$

$$= 115 \text{ J/K mole}$$

$$d(\Delta_r H) = \Delta_r C_p dT$$

$$\Delta_r H_{373} - \Delta_r H_{323} = -42.007 (50)$$

$$\Delta_r H_{373} = 42739.35 \text{ J/mole}$$

$$\Delta_r G_{323} = 42739.35 - 323 (115)$$

$$= 5594.35 \text{ J} = 5.59 \text{ kJ/mole}$$