

Cavitation

Vishnu Vijay
vijay97vishnu@gmail.com

Objective

- The objective of this study is to analyse the cavitation process in an orifice meter.

Geometry

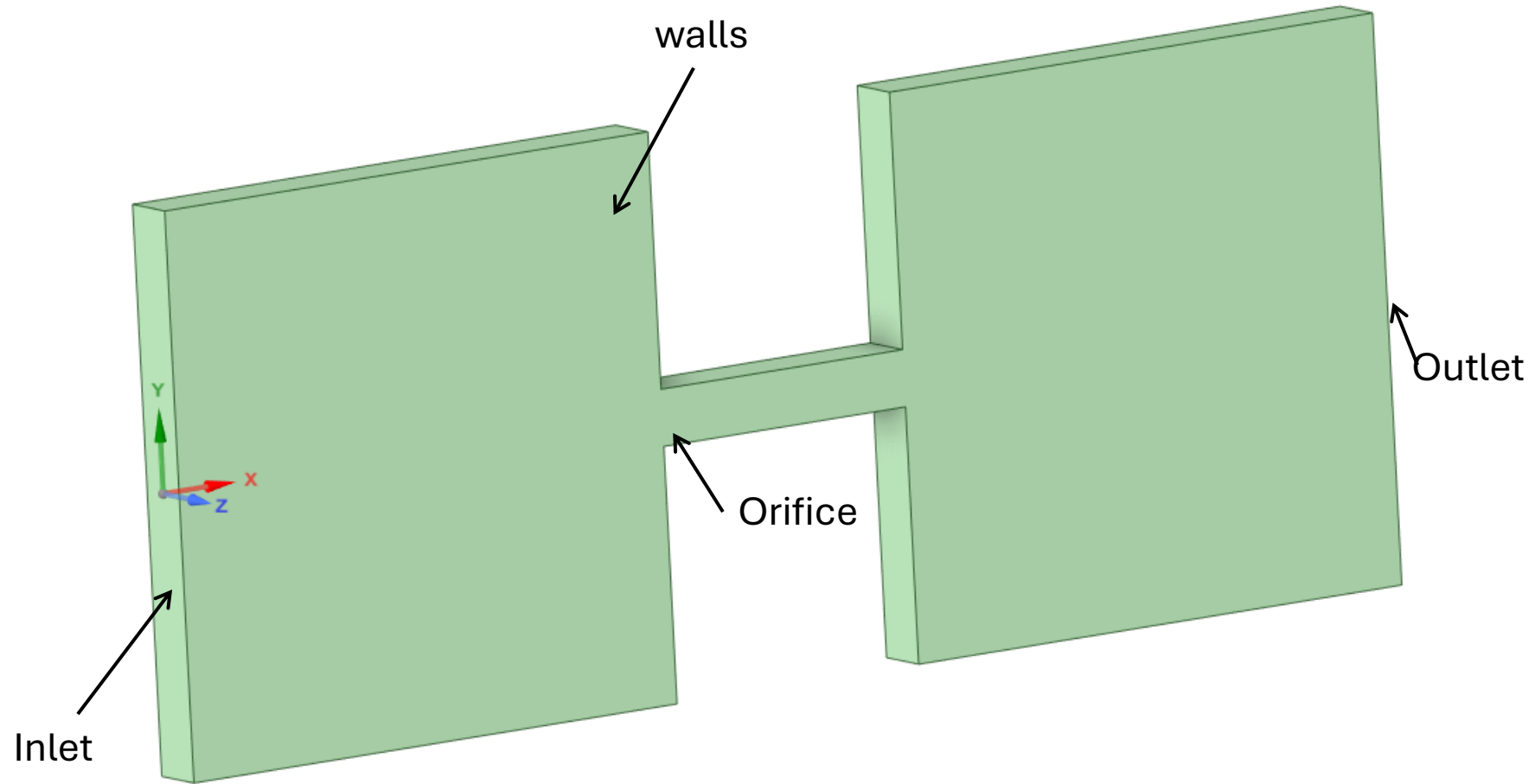


Figure: Orifice geometry

Mesh

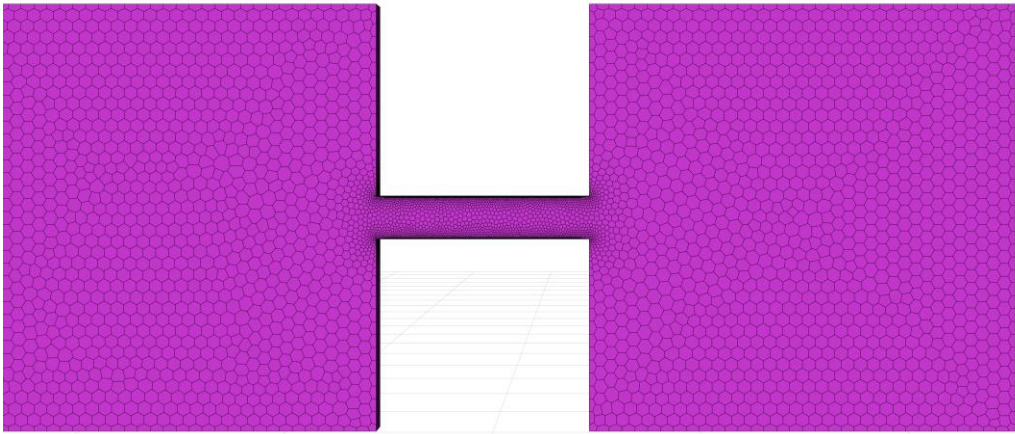


Figure: Mesh

Mesh Details	
Local sizing(face sizing)	yes
Orifice_wall	0.244mm
Max-surface size	3mm
Boundary layers	8
Offset method type	Smooth transition
Transition ratio	0.272
Growth rate	1.2
Cell type	Polyhedra

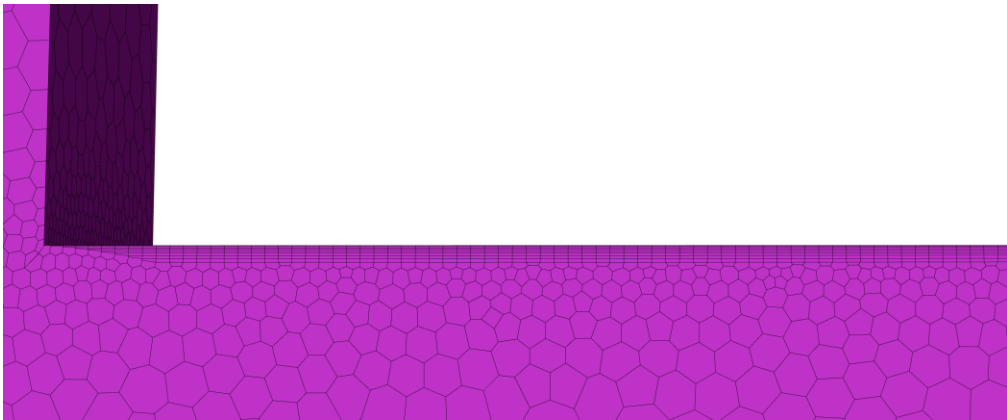


Figure: Boundary layers

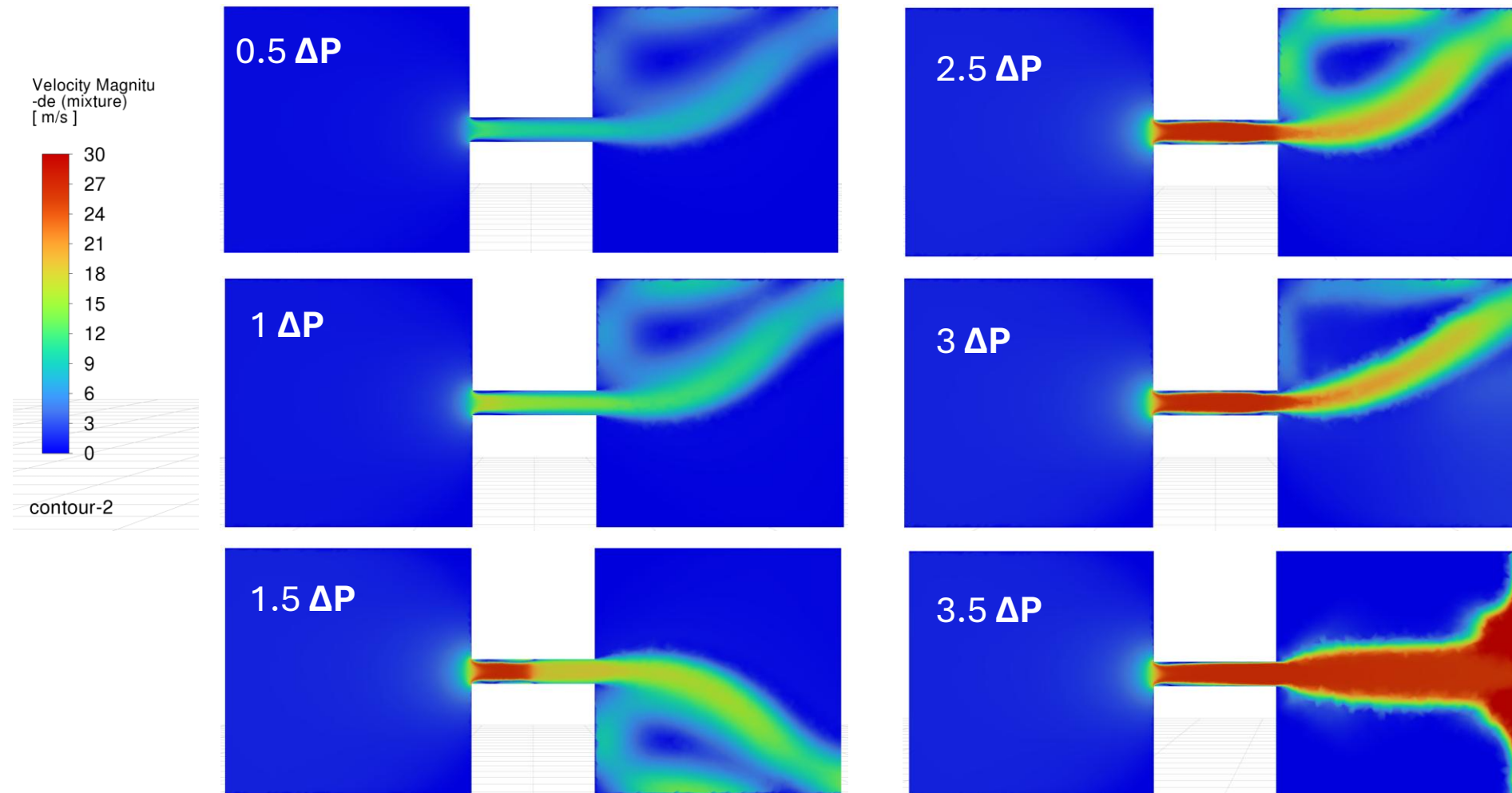
Solver

Boundary Conditions	
Pressure Inlet	3.5e5 Pa
Pressure outlet	3,2.5,2,1.5,1,0.5,0 Pa
wall	wall

Solver details	
Material properties	<ul style="list-style-type: none">Fluid: water at 25CDensity water : 997 kg/m3Viscosity water:0.001003kg/ms
Operating Pressure	0 Pa
Turbulence	Inlet <ul style="list-style-type: none">Specification: intensity & Length scaleTurbulent intensity : 5%Turbulent viscosity ration: 0.01m
Turbulence model	SST k omega
Solution Methods	Pressure velocity coupling scheme: Coupled
Initialisation	Hybrid
Time step method	Automatic
Number of iteration	1000

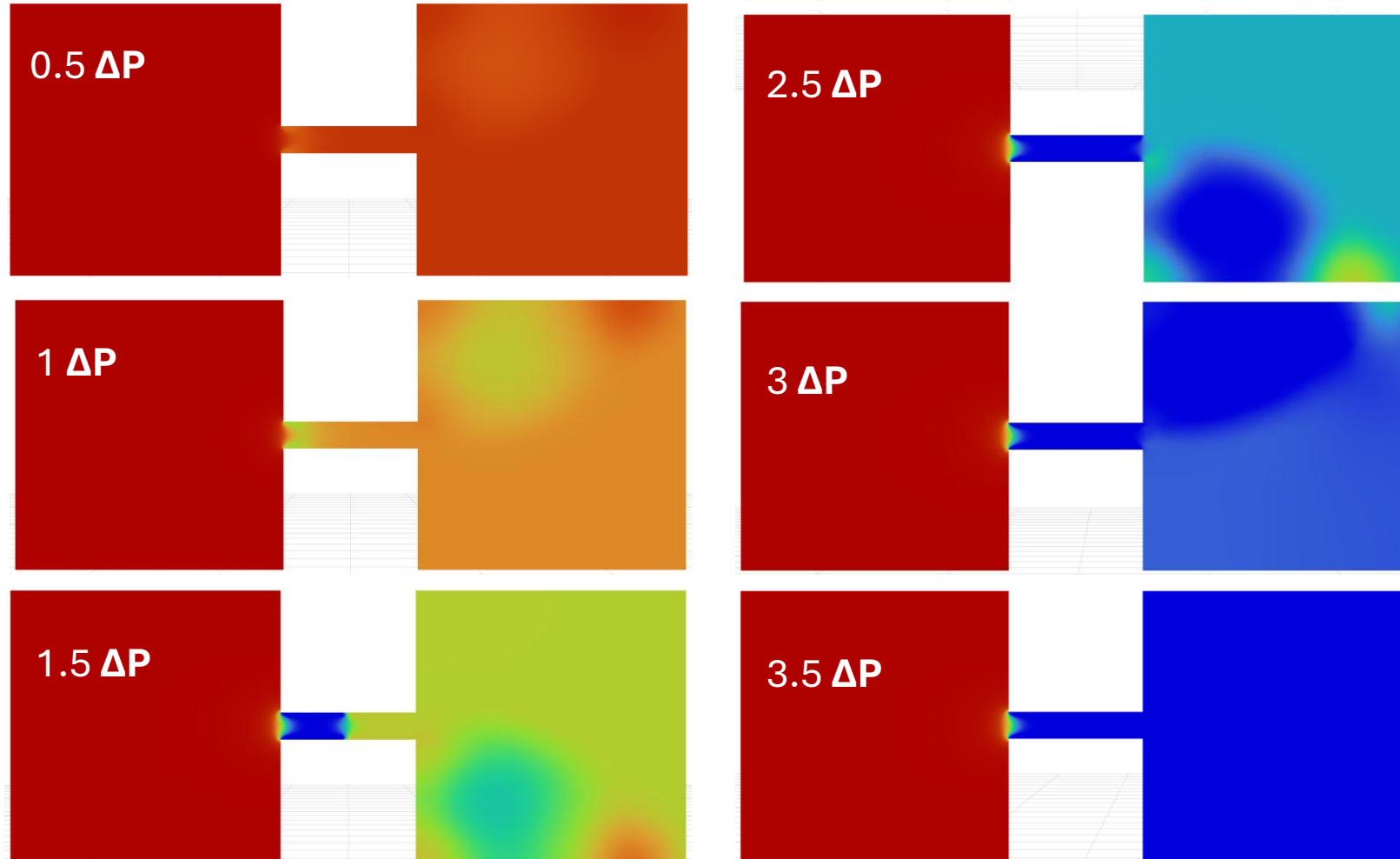
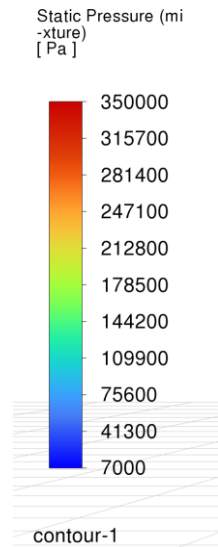
Post processing

Velocity plot



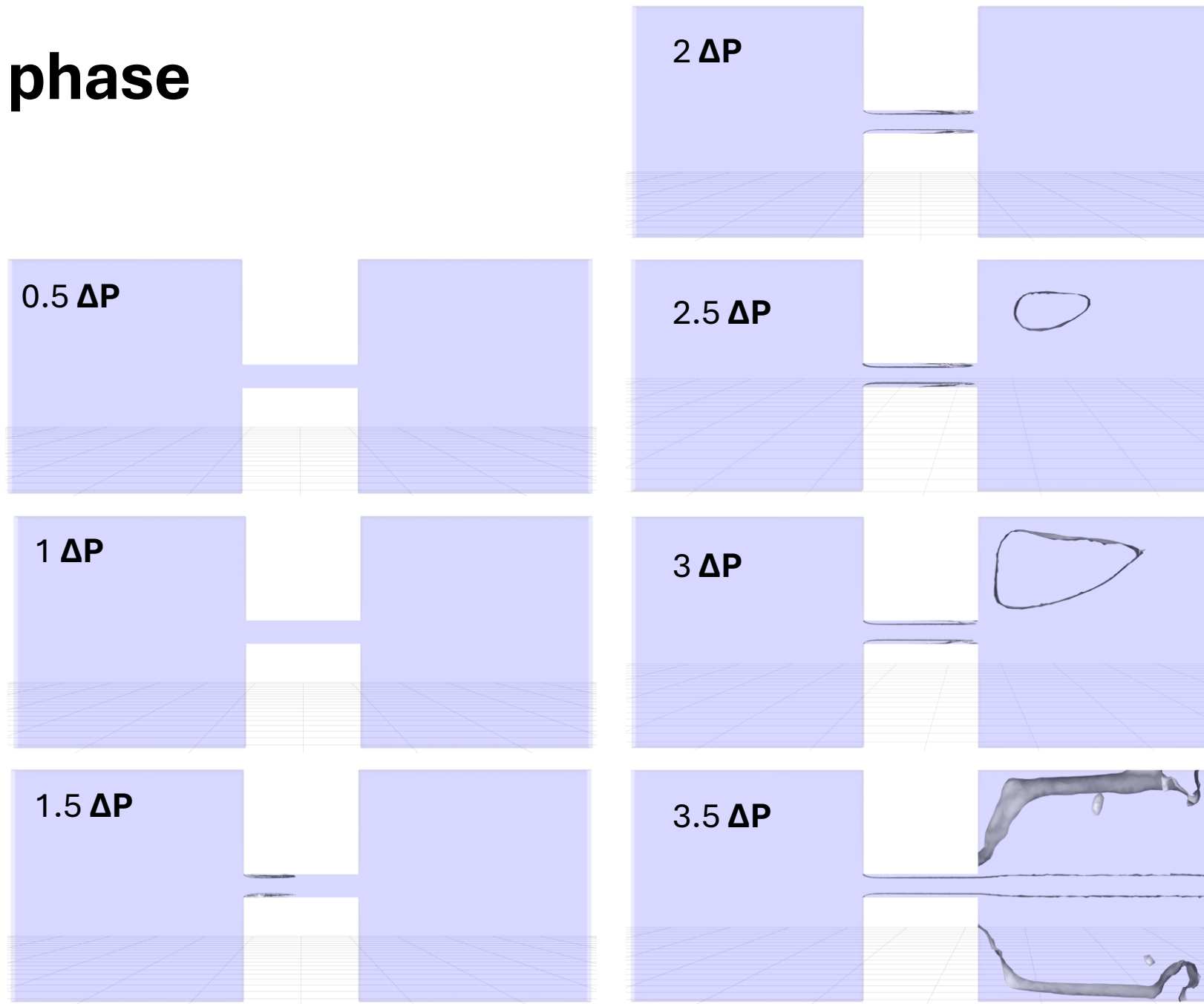
- C_d for $3.5 \Delta P$ is nonphysical. This can be clearly seen from the velocity plot.
- From $0.5 \Delta P$ to $2.5 \Delta P$, the flow accelerates through the orifice and then diffuses downstream. The C_d is stable.
- At $3\Delta P$, the core velocity is red (very high), but overall jet appears distorted, consistent with the flow becoming unstable due to a large vapour cloud.
- At $3.5\Delta P$, the velocity is far higher than what the pressure drop should theoretically allow.

Pressure plot

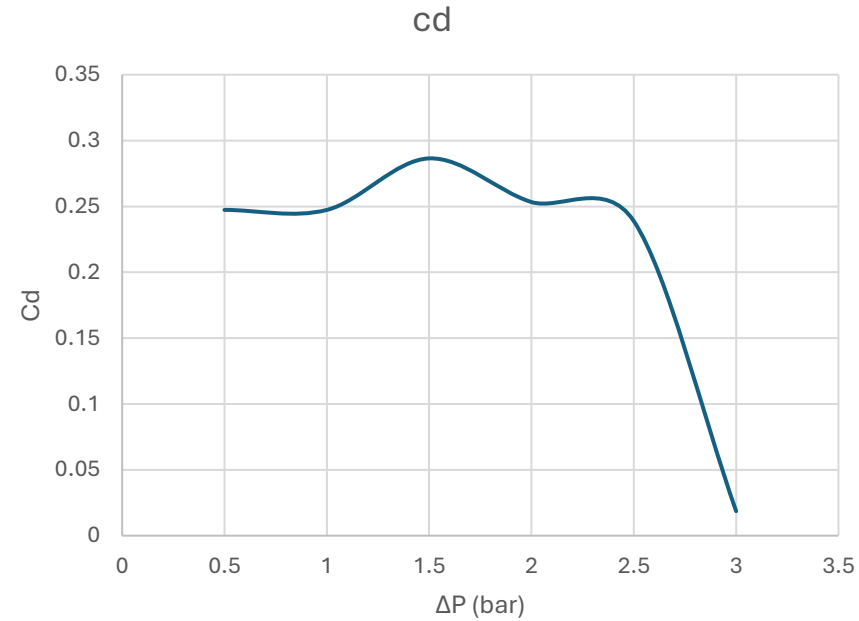
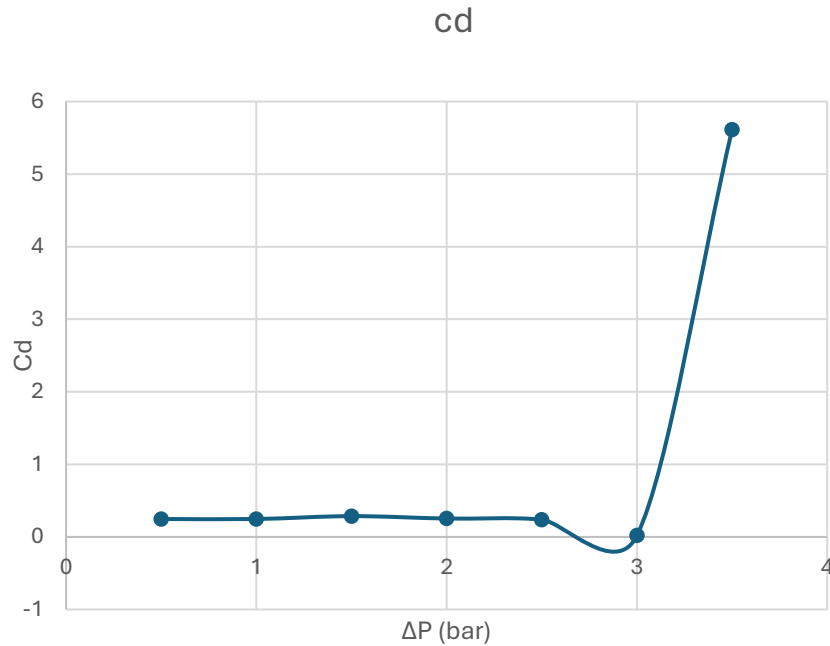


- $0.5\Delta P$ to $2.5\Delta P$, pressure drops smoothly across the orifice and recovers partially downstream.
- The downstream pressure is physically plausible.
- At $3\Delta P$, the downstream pressure is very low (dark blue), consistent with high velocity and choking.
- At $3.5\Delta P$, the pressure downstream is completely dark blue, indicating it is completely vapour or a highly lower pressure. This non-physical drop causes different physics, which the solver cannot calculate.

Vapor phase



ΔP Multiple	Observation	Inference
0.5 to 1ΔP	No vapor is visible (pure liquid flow).	C_d should be constant, as observed in data ($C_d \approx 0.247$).
1.5ΔP	A small, thin vapor cloud (cavity) starts to form just downstream of the sharp inlet corner.	Cavitation Inception. This is the point where the local pressure drops to the vapor pressure. C_d remains stable for now ($C_d \approx 0.286$).
2ΔP	The vapor cavity is larger and more pronounced.	Cavitation is now well-established.
2.5ΔP	The vapor cavity has grown significantly.	Flow is now fully cavitating.
3ΔP	A very large, distinct vapor structure forms and detaches.	Choking Onset. The massive vapor cavity is restricting the flow, which aligns with the sudden, non-physical drop in the discharge cfd (and $C_d \approx 0.0186$) due to flow instability or a choking calculation error.
3.5ΔP	The vapor cavity now fills the entire cross-section and extends far downstream.	Choked Flow/Supercavitation. The flow is completely choked, meaning the flow rate should no longer increase with increasing ΔP . The resulting $C_d \approx 5.61$ is a severe numerical error caused by the single-phase solver failing to handle this massive phase change correctly (as previously discussed, predicting non-physical negative pressures).



- The second plot on the right shows a typical C_d vs ΔP plot for an orifice. The first plot shows the actual simulation results with the error.
- The plot shows non-cavitating flow in the 0.5 to 1 ΔP range, a cavitating flow till the 2.5 ΔP range and then choked flow at 3 ΔP and then at 3.5 ΔP ; there is a numerical error of the solver.

Journal Script

```
/file/read-case-data "orifice.cas.h5"  
ok
```

```
/solve/monitors/residual/print? yes  
/solve/monitors/residual/plot? yes
```

```
/solve/report-definitions/add  
mfr_outlet  
flux  
zone-names  
outlet  
()  
quit
```

```
; --- Outlet 0.5 bar (50000 Pa) ---  
/define/boundarypressure-conditions  
set  
pressure-outlet  
outlet  
()  
mixture  
gauge-pressure  
no  
50000  
quit
```

```
/solve/initialize/hyb-initialization  
yes  
/solve/iterate 50  
yes  
/file/write-case-data "orifice0.5p.cas.h5"  
yes  
/file/write-data "orifice0.5p.dat.h5"  
yes
```

```
; --- Outlet pressure 1.0 bar (100000 Pa) ---  
/define/boundary-conditions  
set  
pressure-outlet  
outlet  
()  
mixture  
gauge-pressure  
no  
100000
```

```
quit
```

```
/solve/initialize/hyb-initialization  
yes  
/solve/iterate 50  
yes  
/file/write-case-data "orifice1p.cas.h5"  
yes  
/file/write-data "orifice1p.dat.h5"  
yes
```

```
; --- Outlet pressure 1.5 bar (150000 Pa) ---  
/define/boundary-conditions  
set  
pressure-outlet  
outlet  
()  
mixture  
gauge-pressure  
no  
150000  
quit
```

```
/solve/initialize/hyb-initialization  
yes  
/solve/iterate 50  
yes  
/file/write-case-data "orifice1.5p.cas.h5"  
yes  
/file/write-data "orifice1.5p.dat.h5"  
yes
```

```
; --- Outlet pressure 2.0 bar (200000 Pa) ---  
/define/boundary-conditions  
set  
pressure-outlet  
outlet  
()  
mixture  
gauge-pressure  
no  
200000  
quit
```

```
/solve/initialize/hyb-initialization  
yes  
/solve/iterate 50  
yes
```
















```
/file/write-case-data "orifice2p.cas.h5"  
yes  
/file/write-data "orifice2p.dat.h5"  
yes
```

```
; --- Outlet pressure 2.5 bar (250000 Pa) ---  
/define/boundary-conditions  
set  
pressure-outlet  
outlet  
()  
mixture  
gauge-pressure  
no  
250000  
quit
```

```
/solve/initialize/hyb-initialization  
yes  
/solve/iterate 50  
yes  
/file/write-case-data "orifice2.5p.cas.h5"  
yes  
/file/write-data "orifice2.5p.dat.h5"  
yes
```

```
; --- Outlet pressure 3.0 bar (300000 Pa) ---  
/define/boundary-conditions  
set  
pressure-outlet  
outlet  
()  
mixture  
gauge-pressure  
no  
300000  
quit
```

```
/solve/initialize/hyb-initialization  
yes  
/solve/iterate 50  
yes  
/file/write-case-data "orifice3p.cas.h5"  
yes  
/file/write-data "orifice3p.dat.h5"  
yes
```

 report-def-0-rfile_1_426.out	09-11-2025 22:16	OUT File	1 KB
 discharge_out-rfile_6_1.out	09-11-2025 22:24	OUT File	2 KB
 report-def-0-rfile_6_1.out	09-11-2025 22:24	OUT File	2 KB
 discharge_out-rfile_7_1.out	09-11-2025 23:05	OUT File	2 KB
 report-def-0-rfile_7_1.out	09-11-2025 23:05	OUT File	2 KB
 discharge_out-rfile_8_1.out	09-11-2025 23:09	OUT File	2 KB
 report-def-0-rfile_8_1.out	09-11-2025 23:09	OUT File	2 KB
 discharge_out-rfile_9_1.out	09-11-2025 23:16	OUT File	2 KB
 report-def-0-rfile_9_1.out	09-11-2025 23:16	OUT File	2 KB
 discharge_out-rfile_10_1.out	09-11-2025 23:19	OUT File	2 KB
 report-def-0-rfile_10_1.out	09-11-2025 23:19	OUT File	2 KB
 discharge_out-rfile_11_1.out	09-11-2025 23:21	OUT File	2 KB
 report-def-0-rfile_11_1.out	09-11-2025 23:21	OUT File	2 KB
 discharge_out-rfile_12_1.out	09-11-2025 23:23	OUT File	2 KB
 report-def-0-rfile_12_1.out	09-11-2025 23:23	OUT File	2 KB

- Every run produced a written file as dated and timed as shown.

Conclusion

- The extreme nonphysical velocity is a direct consequence of single-phase CFD solvers calculating nonphysical, highly negative static pressures.
- The instability is probably because of the presence of turbulence due to phase 2, and the solver is solving in steady state.
- The simulation was run successfully to understand, plot and visualise the vapour phase.
- It is easy to simulate multiple runs using the Journal script.
- Automations save time in setting up the cases.