

COLLEGE OF ENGINEERING  
Department of Metallurgical & Materials Engineering  
The University of Alabama

MTE 562

Thermodynamics

Quiz I

Q. 1

(10 pts) a. Explain the following:

1. Work
2. Compressibility factor (Z)

(20 pts) b.

Estimate the heat capacity  $C_{p,298}$  of  $\text{BaTiO}_3$  using the data listed in Table - 1 and 2. The experimentally determined  $C_p$  for this compound is as follows:

$$C_p = 29.03 + (2.04 \times 10^{-3} T) - (4.58 \times 10^{-5} T^2) \text{ Cal/mole.K}$$

Compare the estimated value with the experimental value.

Q. 2

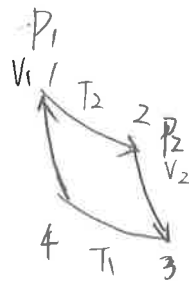
(5 pts) a. Define the Carnot theorem.

(10 pts) c.

Express the entropy of reaction  $[\text{Mg (s, 298 K)} = \text{Mg (l, T K)}]$  of pure Magnesium, Mg,  $(\Delta H_T - \Delta H_{298})$  as a function of temperature from the attached phase diagram.

(20 pts) c.

A Carnot heat engine operates between reservoirs at  $1200^\circ\text{C}$  and  $200^\circ\text{C}$ . The isothermal process at the hotter reservoir consists of an expansion (reversible) from an initial pressure of  $5 \times 10^5 \text{ N/m}^2$  to  $4 \times 10^4 \text{ N/m}^2$ . Assuming that the working substance is 1 kilomole of ideal gas, calculate a) the efficiency of the heat engine, b) the heat absorbed from the hotter reservoir, and c) the heat rejected to the colder reservoir.



Q.3

(5 pts) a. Define the Third Law of Thermodynamics.

(10 pts) b.

Show that the entropy of mixing ( $\Delta S$ ) for one mole of ideal gas mixture is

$$\Delta S = -R \sum_{i=1}^C X_i \ln X_i$$

where  $X_i$  is the mole fraction of  $i^{\text{th}}$  gas and  $R$  is the gas constant.

(20 pts) c.

For the reaction  $\text{C(s)} + 0.5 \text{O}_2 \text{(g)} = \text{CO (g)}$ , the standard Gibbs energy change,  $\Delta G^\circ$ , is given by

$$\Delta G^\circ = -111,710 - 87.66 T \text{ Joules}$$

Find a) the entropy change,  $\Delta S^\circ$ , and b) the enthalpy change,  $\Delta H^\circ$ , for the reaction.

$$\Delta G = -T \Delta S$$

$$\begin{aligned} dU &= C_v dT = 0 \\ Q &= -W = p dV \\ pV &= RT \\ p_1 V_1 &= p_2 V_2 \\ \frac{p_1}{p_2} &= \frac{V_2}{V_1} \end{aligned}$$

Q.1

a. 1. Work is done when a force acts through a distance.

$$W = \int F dl = - \int p dv$$

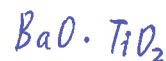
2. Compressibility factor is used to correlate the relationships among  $P, V, T$ for real gases. It's dimensionless empirical factor.  $z = \frac{PV}{RT}$ b. The experimental value of  $C_{p,298}$  is:

$$\begin{aligned} C_{p,298} &= \int_0^{298} C_p dT = \int_0^{298} [29.03 + (2.04 \times 10^{-3} T) - (4.58 \times 10^{-5} T^2)] dT \\ &= (29.03 T + 2.04 \times 10^{-3} \times 0.5 T^2 + 4.58 \times 10^{-5} T^{-1}) \Big|_0^{298} \\ &= 29.03 \times 298 + 2.04 \times 10^{-3} \times 0.5 \times 298^2 + 4.58 \times 10^{-5} \times \frac{1}{298} \\ &= 8650.94 + 90.58 + 1536.91 \quad \text{check!!!} \\ &= 10278.43 \text{ cal/mole} \cdot \text{K} = 43004.95 \text{ J/mole} \cdot \text{K} \end{aligned}$$

The estimated value of  $C_{p,298}$ :

$$\begin{aligned} (C_{p,298})_{\text{est}} &= [C_{p,298}(\text{Ba}) + C_{p,298}(\text{Ti}) + 3C_{p,298}(\text{O})] \cdot N_A \\ &= (27.2 + 23.8 + 3 \times 16.7) \times 6.02 \times 10^{23} \\ &= 6.0862 \times 10^{25} \text{ J/g} \cdot \text{mole} \cdot \text{K} \quad \text{too high} \end{aligned}$$

$$101.1 \text{ J/mole} \cdot \text{K}$$

Comparison between  $C_p(\text{est.})$  &  $C_p(\text{exp.})$ ?

experiment value

$$C_{p,298} = 29.03 + (2.04 \times 10^{-3}) \times 298 - (4.58 \times 10^{-5} \times 298^2) = 24.481 \text{ cal/mol} \cdot \text{K} = 102.43 \text{ J/mol} \cdot \text{K}$$

estimated value:

$$\begin{aligned} C_{p,298} &= C_{p,298}(\text{Ba}) + C_{p,298}(\text{Ti}) + C_{p,298}(10^2)^{+2} + 2C_{p,298}(10^2)^{+4} \\ &= 27.2 + 23.8 + 19.3 + 2 \times 15.9 = 102.1 \text{ J/mol} \cdot \text{K} \end{aligned}$$

Q.2

4 a. Carnot theorem: The reversible cyclic engines operated at two fixed temperatures have the same efficiency. Efficiency =  $1 - \frac{T_1}{T_2}$ .

b. Mg:  $T_{\text{fusion}} = 650^\circ\text{C} = 923\text{K}$ .

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$$\Delta H_T - \Delta H_{298} = \int_{298}^{923} C_p(s) dT + H_{\text{fusion}} + \int_{923}^T C_p(l) dT$$

$$\Delta S_T = \frac{\Delta H_T - \Delta H_{298}}{T} = \int_{298}^{923} \frac{C_p(s)}{T} dT + \frac{H_{\text{fusion}}}{T} + \int_{923}^T \frac{C_p(l)}{T} dT$$

c. a) The efficiency of the heat engine:  $\eta = 1 - \frac{T_1}{T_2} = 1 - \frac{473}{1473} = 0.679$

b)  $Q_{\text{iso}} = -W = \int p dV = \int \frac{nRT_2}{V} dV = nRT_2 \ln \frac{V_2}{V_1}$

"  $T_2$  is constant,  $P_1 V_1 = P_2 V_2$ ,  $V_2/V_1 = P_1/P_2$

20 so  $Q_{\text{iso}} = nRT_2 \ln \frac{P_1}{P_2} = 1000 \times 8.31 \times 1473 \times \ln \frac{5 \times 10^5}{4 \times 10^4} = 3.09 \times 10^7 \text{ J}$

c)  $\eta = \frac{Q_2 + Q_1}{Q_2} = 0.679$ , so  $Q_1 = (0.679 - 1)Q_2 = -9.92 \times 10^6 \text{ J}$

Q3.

a. The entropy of each pure element or pure compound at their stable molecular configuration can be taken to zero at zero Kelvin.

b. The entropy for the  $i$ th gas is

$$\Delta S_i = -n_i R \ln \frac{V_i}{V} = -n_i R \ln X_i$$

$$V_i/V = X_i$$

10 so  $\Delta S = \sum_{i=1}^C \Delta S_i = \sum_{i=1}^C (-n_i R \ln X_i) = -R \sum_{i=1}^C n_i \ln X_i$

for one mole of ideal gas mixture, the mole number of the  $i$ th gas equals

$$n_i = X_i \cdot 1 = X_i$$

so  $\Delta S = -R \sum_{i=1}^C X_i \ln X_i$

c. a)  $\Delta S^\circ = -\frac{\Delta G^\circ}{T} = \frac{-(-111710 - 87.66T)}{T} = \frac{111710}{T} + 87.66 \text{ (J/K)}$

15 b)  $\Delta H^\circ = T \Delta S^\circ = T \left( \frac{111710}{T} + 87.66 \right) = 111710 + 87.66 T \text{ (J)}$

$$\Delta G = -111710 - 87.66 T$$

$$= \Delta H - \Delta S T$$

$$\Delta H = -111710 \text{ J}; \Delta S = 87.66 \text{ J/K}$$

$$\Delta G = \Delta H - T \Delta S$$

$$\Delta G = -111710 - 87.66 T \text{ J}$$

$$\Delta H = -111710 \text{ J}$$

$$\Delta S = 87.66 \text{ J/K}$$

Table 1: Atomic contributions to  $C_{P298}$ 

Ag 25.5	H 6.3 <sup>b</sup>	Pt 26.4
Al 14.6 (23.4)	Hf 26.4	Rb 26.4
As 21.3	Hg 26.4	Rh 25.9
Au 26.4	I [28.5]	S [20.9]
B 5.4 (10.9)	In 23.4	Sb 25.5
Ba 27.2	Ir 26.4	Sc 20.1
Be 7.5 (11.7)	K 25.9	Se [27.2]
Bi 27.2	La 27.2	Si 12.6 (20.1)
Br [27.6]	Lanthanides 26.4	Sn 25.5
C [8.4] [10.5] <sup>a</sup>	Li 20.5	Sr 25.5
Ca 23.4 [25.1]	Mg 18.4 (23.8)	Ta 26.4
Cd 25.1	Mn 25.1	Te ?
Cl [25.1]	Mo 25.5	Th 28.0
Co 25.1	N 18.8 (18.8)	Ti 23.8
Cr 25.1	Na 25.1	Tl 25.5
Cs 26.8	Nb 25.9	U 28.9
Cu 25.1	Ni 25.1	V 25.1
F [22.2]	<u>O [16.7]</u>	W 27.2
Fe 25.5	P 15.1	Y 23.4
Ga 20.1	Pb 27.2	Zn 22.6 (25.1)
Ge 21.8	Pd 25.5	Zr 25.5

Note: Units are J/g·atom·°K. Use the values in parentheses for intermetallics, carbides, silicides, borides, and non-valence nitrides. Use the values in square brackets to estimate values not listed in Table 3-2.

<sup>a</sup>For saltlike carbides, such as  $CaC_2$  and  $Al_4C_3$ , use  $C = 16.7$ .

<sup>b</sup>For H in acids, acid salts, and hydrides.

Special values:  $NH_4^+ = 57.3$ ;  $H_2O = 41.0$  in hydrates.

Source: Kellogg (reference 4), p. 363.

Table 2: Anion contributions to  $C_{P298}$ 

Species	Cation charge					
	+1	+2	+3	+4	+5	+6
$F^-$	23.0	22.2	21.3	20.9	21.3	(22.6)
$Cl^-$	25.5	25.1	24.3	23.8		(23.8)
$Br^-$	27.6	27.6	27.6	26.4		
$I^-$	28.5	28.5	(29.3)	(28.5)		
$O^{2-}$	17.6	<u>19.3</u>		17.2	15.1	(17.2)
$S^{2-}$	29.3	23.8	23.0	20.9		
$Se^{2-}$	(31.4)	(27.2)				
$Te^{2-}$		(46.0)	(36.8)	(25.1)		
$N^{3-}$	(15.9)	22.2	16.7	16.7	(19.7)	
$OH^-$	(32.2)	29.7				
$SiH^-$	(52.7)					
$SeH^-$	(46.9)					
$CO_3^{2-}$	60.7	57.7				
$NO_3^-$	69.0	62.8	(58.6)			
$SO_3^{2-}$	(69.9)	(68.2)				
$ClO_3^-$	75.7	(71.1)				
$BrO_3^-$	(79.1)	75.3				
$IO_3^-$	(79.5)					
$SO_4^{2-}$	79.1	76.2	74.9	(72.8)		
$ClO_4^-$	80.3					
$CrO_4^{2-}$	92.9					
$Cr_2O_7^{2-}$		107.5				
$BiH_4^-$	64.9					
$CN^-$	(37.7)	(37.7)	(33.5)			

Note: The values in parentheses are based on scant evidence. The units are J/g·atom·°K.  
Source: Kellogg (reference 4), p. 364.

1 g·atom = 1 mole



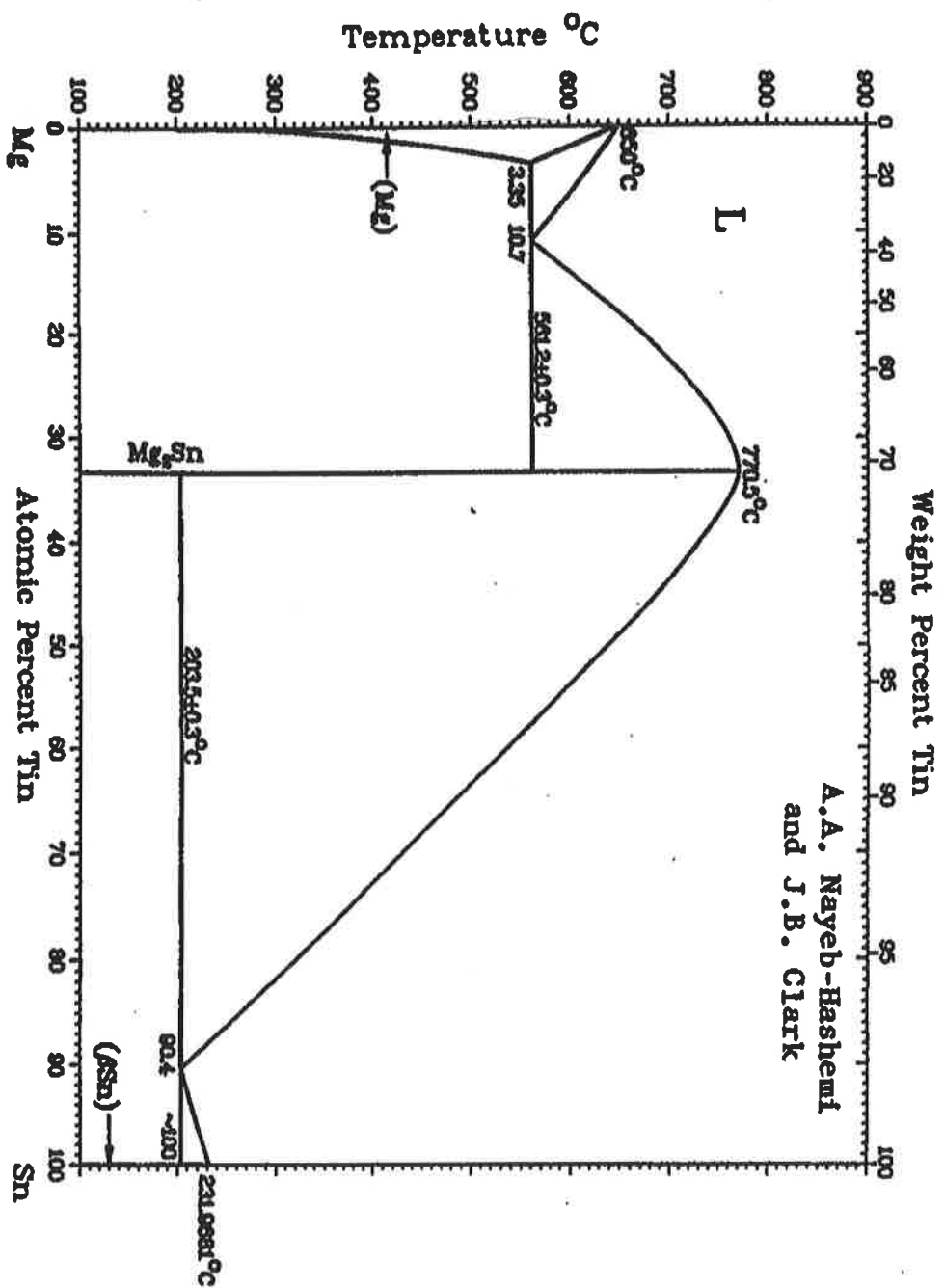


Fig. 15.36 Mg-Sn phase diagram.