Homework 1

Mikko Karkkainen

August 27, 2017

1.1

$$\mu = 2 \cdot 10^{-2} \text{ Nsm}^{-2}$$
 $V = 61.0 \text{ cms}^{-1} = 0.61 \text{ ms}^{-1}$
 $Y = 2 \text{ mm} = 2 \cdot 10^{-3} \text{ m}$

For flow between two plates, one moving and one stationary:

$$\tau_{xy} = -\mu \frac{\partial v_x}{\partial y} \tag{1}$$

where τ is the momentum flux in the positive y-direction. For steady state:

$$-\mu \frac{\partial v_x}{\partial y} = -\mu \frac{V}{Y}$$

$$= -2 \cdot 10^{-2} \text{ Nsm}^{-2} \cdot \frac{0.61 \text{ ms}^{-1}}{2 \cdot 10^{-3} \text{ m}}$$

$$= -6.1 \text{ Nm}^{-2}$$
(2)

The direction of momentum transfer is from the top plate to the bottom plate (-y direction)

1.2

$$v_x = 3y - y^3$$

 $\rho = 10^3 \text{ kgm}^{-3}$
 $v = 7 \cdot 10^{-7} \text{ m}^2 \text{s}^{-1}$
 $\mu = v\rho = 7 \cdot 10^{-4} \text{ kgm}^{-1} \text{s}^{-1}$

a)

$$\frac{\partial v_x}{\partial y} = 3 - 3y^2 \tag{3}$$

$$\frac{\partial v_x}{\partial y}\Big|_{x=x_1,y=0} = 3 \text{ cms}^{-1}$$

$$= 3 \cdot 10^{-2} \text{ ms}^{-1}$$

$$\tau_{xy}\Big|_{x=x_1,y=0} = -\mu \frac{\partial v_x}{\partial y}\Big|_{x=x_1,y=0}$$

$$= -7 \cdot 10^{-4} \text{ kgm}^{-1} \text{s}^{-1} \cdot 3 \cdot 10^{-2} \text{ ms}^{-1}$$

$$= -2.1 \cdot 10^{-5} \text{ kgs}^{-2}$$

The shear stress at $x = x_1, y = 0$ is $-2.1 \cdot 10^{-5} \text{ kgs}^{-2}$

b)

$$\frac{\partial v_x}{\partial y} = 3 - 3y^2 \text{ cms}^{-1}$$

$$\frac{\partial v_x}{\partial y}\Big|_{y=0.8mm} = 1.08 \text{ cms}^{-1}$$

$$= 1.08 \cdot 10^{-2} \text{ ms}^{-1}$$

$$\tau_{xy}\Big|_{y=0.8mm} = -\mu \frac{\partial v_x}{\partial y}\Big|_{x=x_1,y=0.8mm}$$

$$= -7 \cdot 10^{-4} \text{ kgm}^{-1} \text{s}^{-1} \cdot 1.08 \cdot 10^{-2} \text{ ms}^{-1}$$

$$= -7.56 \cdot 10^{-6} \text{ kgs}^{-2}$$

The shear stress at $x = x_1, y = 0.8$ is $-7.56 \cdot 10^{-6} \text{ kgs}^{-2}$

c)

Momentum flux in the x-direction:

$$\tau_{yx} = -\mu \frac{\partial v_y}{\partial x} \tag{4}$$

Since the velocity profile has no component in y-direction, momentum flux in x-direction is 0

1.4

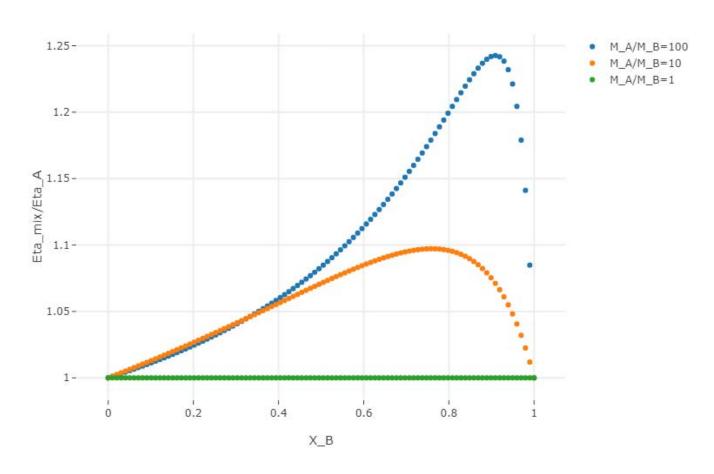
$$\eta_{mix} = \sum_{i=1}^{n} \frac{x_i \eta_i}{\sum_{j=1}^{n} x_j \phi_{ij}}$$
 (5)

$$\phi_{ij} = \frac{1}{\sqrt{8}} \left[1 + \frac{M_i}{M_j} \right]^{-1/2} \left[1 + \left[\frac{\eta_i}{\eta_j} \right]^{1/2} \left[\frac{M_j}{M_i} \right]^{1/4} \right]^2$$
 (6)

For a binary gas with $\eta_A = \eta_B$:

$$\frac{\eta_{mix}}{\eta_A} = \frac{(1 - x_B)}{1 - x_B + x_B \left(\frac{1}{\sqrt{8}} \left[1 + \frac{M_A}{M_B}\right]^{-1/2} \left[1 + \left[\frac{M_B}{M_A}\right]^{1/4}\right]^2\right)} + \frac{x_B}{x_B + (1 - x_B) \left(\frac{1}{\sqrt{8}} \left[1 + \frac{M_B}{M_A}\right]^{-1/2} \left[1 + \left[\frac{M_A}{M_B}\right]^{1/4}\right]^2\right)}$$
(7)

Eta_mix/Eta_A vs. X_B



1.8

$$T = 2273 \text{ K}$$

 $T_M = 1575 \text{ K}$
 $M = 52 \text{ gmol}^{-1} = 5.2 \cdot 10^{-2} \text{ kgmol}^{-1}$
 $\rho = 7100 \text{ kgm}^{-3}$
 $\delta = 0.272 \text{ nm}$

$$\frac{\epsilon}{K_B} = 5.20 T_M \text{ K}$$

$$= 5.20 \cdot 1575 \text{ K}$$

$$= 8.19 \cdot 10^3 \text{ K}$$
(8)

$$T^* = \frac{K_B T}{\epsilon}$$

$$= \frac{2273 \text{ K}}{8.19 \cdot 10^3 \text{ K}}$$

$$= 0.2775$$
(9)

From Figure 1.10 in the book:

$$\eta^*(V^*)^2 = 2.05$$

$$V^* = \frac{1}{n\delta^3}$$

$$= \frac{1}{\left[\frac{6.023 \cdot 10^{23} \text{ atoms}}{5.2 \cdot 10^{-2} \text{ kg}}\right] \left[\frac{7100 \text{ kg}}{\text{m}^3}\right] \left(0.272 \cdot 10^{-9} \text{ m}\right)^3}$$

$$= 0.604$$
(10)

$$\eta^* = \frac{2.05}{0.604^2} = 5.62$$

$$\eta = \frac{\eta^* (MRT)^{1/2}}{\delta^2 N_A}$$

$$= \frac{5.62 \cdot \left(5.2 \cdot 10^{-2} \text{ kgmol}^{-1} \cdot 8.3144 \text{ Jmol}^{-1} \text{K}^{-1} \cdot 2273 \text{ K}\right)^{1/2}}{\left(0.272 \cdot 10^{-9} \text{ m}\right)^2 \cdot 6.023 \cdot 10^{23} \text{ mol}^{-1}}$$

$$= 3.954 \cdot 10^{-3} \text{ kgm}^{-1} \text{s}^{-1}$$
(11)

The viscosity for Cr at 2273K is approximately $3.954 \cdot 10^{-3} \text{ kgm}^{-1}\text{s}^{-1}$