

Hydrodynamic and chemical effects of hydrogen addition on soot evolution in turbulent nonpremixed bluff body ethylene flames

Sili Deng^{a,*}, Michael E. Mueller^a, Qing N. Chan^b, Nader H. Qamar^c, Bassam B. Dally^d, Zeyad T. Alwahabi^d,
Graham J. Nathan^d

^a*Department of Mechanical and Aerospace Engineering, Princeton University, Princeton, USA*

^b*School of Mechanical and Manufacturing Engineering, The University of New South Wales, Australia*

^c*FCT-Combustion, Australia*

^d*Centre for Energy Technology, The University of Adelaide, Australia*

Abstract

A turbulent nonpremixed bluff body ethylene/hydrogen (volume ratio 2:1) flame was investigated using a combination of experiments and Large Eddy Simulations and compared with a neat ethylene counterpart [Mueller *et al.* Combust. Flame, 160, 2013]. Similar to the ethylene bluff body flame, a low-strain recirculation zone, a high-strain neck region, and a downstream jet-like region were observed. However, the maximum soot volume fraction in the recirculation zone and jet-like region of the hydrogen added case are significantly lower than that of the ethylene case. Flamelet calculations demonstrated that hydrogen addition suppressed soot formation due to the reduction of C/H ratio, and a four times soot volume fraction decrease was estimated based on this chemical effect. The downstream jet-like region shows a reduction in soot consistent with this analysis. However, soot reduction in the recirculation zone is substantially larger than this analysis suggested, indicating an additional hydrodynamic effect. Large Eddy Simulation was used to further investigate soot evolution in the recirculation zone and to elucidate the role of hydrogen addition. Since the central jet Reynolds numbers in both cases are the same (approximately 30,900), the jet velocity of the hydrogen added case is higher, resulting in a leaner recirculation zone, which inhibits soot formation and promotes soot oxidation, resulting in the larger magnitude in soot reduction.

Keywords: Soot, Laser-induced incandescence, Large Eddy Simulation (LES), Bluff body flame, Turbulent nonpremixed flame

*Corresponding Author: silideng@princeton.edu

1. Introduction

Due to the importance of soot in practical transportation, propulsion, and power generation systems, soot formation, growth, and oxidation have been extensively studied. Most of these studies focus on laminar configurations since flow conditions are better controlled and characterized, which enables detailed analysis of soot evolution [1]. Nonetheless, most practical devices operate under turbulent conditions. The understanding of soot evolution in turbulent reacting flows and the small-scale interactions among soot, turbulence, and chemistry has been aided by Direct Numerical Simulation (DNS). In the past, these studies have been limited to two-dimensional configurations and/or empirical soot models to limit computational cost [2–5], but, recently, Attili *et al.* [6] performed the first three-dimensional DNS of turbulent nonpremixed jet flames employing a high-order statistical model of soot and detailed chemical mechanism, which includes the soot precursor naphthalene, and investigated Damköhler number effects on soot formation and growth [7]. Nevertheless, similar to all combustion DNS studies, the Reynolds number was limited to 15,000.

To investigate jet flames at high Reynolds numbers, a combination of experiments [8–11] and Large Eddy Simulation (LES) [12–14] has been used. However, the jet flame configuration does not contain more complex fluid dynamics found in practical combustion systems such as recirculating flow. To bridge this gap, recent experiments and LES have been used to understand the role of recirculating flow on soot evolution in simple, canonical geometries. Mueller *et al.* [15] experimentally and computationally investigated a turbulent nonpremixed bluff body ethylene flame. Unlike jet flames, surface growth was found to dominate in the recirculation zone, highlighting the significance of hydrodynamics on soot evolution.

In the present work, an ethylene/hydrogen mixture sooting flame with the same bluff body configuration is investigated. During the thermal decomposition of hydrocarbon fuels, it has been shown that the addition of hydrogen slows down the formation of soot [16]. Extensive laminar studies have been conducted with simplified flow conditions to understand the overall suppression of soot formation in hydrogen added diffusion flames and have attributed such suppression to both dilution and chemistry effects [17–21]. In addition to this chemical effect, to maintain the same Reynolds number as the ethylene bluff body flame [15], a faster central jet is needed, which will change the fuel to coflow air momentum flux ratio and affect the hydrodynamics.

The objective of this investigation is threefold: first, to understand the evolution of soot in the hydrogen added ethylene bluff body flame utilizing a combination of experiments and computations; second, to assess differences between hydrogen added and neat ethylene flames and further validate the LES model; and, third, to differentiate between the hydrodynamic and chemical effects of hydrogen addition.

2. Experimental methodology

The experimental setup used in the current study is similar to previous bluff body studies [22, 23] and was kept the same as the previous ethylene case [15]. In brief, the outer diameter of the bluff body (D_B) is 50 mm, and the diameter

(D_j) of the central fuel jet is 3.6 mm, from which an ethylene/hydrogen mixture (2:1 by volume) issued at 102.1 m/s. The central jet Reynolds number was kept the same as the previous study [15] at 30,900. The bluff body burner was mounted in a contraction with an exit cross section of 150 by 150 mm², from which air coflow issued at 23 m/s.

The 1064 nm beam from an Nd:YAG laser was used for LII excitation. The laser sheet had a height of 80 mm through the measurement volume and had a thickness of 0.3 mm. The operating LII fluence was kept at 0.9 J/cm² to ensure the independence of the signal to variations in the fluence caused by laser extinction [9, 24]. In addition, data were only extracted from the laser-in side of the measurement to avoid non-linear influences of beam steering [25]. A Gaussian distribution of the spatial fluence with a 8% standard deviation was achieved. All images presented in this work have been clipped at the edges where the laser sheet was found to exhibit low fluence.

The LII signal was filtered at 430 ± 10 nm and detected with an intensified CCD camera. A short gate width of 40 ns was used to reduce the size-dependent sensitivity of the signal [26]. The LII signal has been calibrated by laser extinction measurements as previously reported [15]. With this system, the in-plane resolution of the images is 0.26 mm/pixel in each direction, and the detection threshold is about 3 ppb.

The data presented in this work have been corrected for background interference and detector attenuation. According to the previous ethylene bluff body study, the estimated measurement uncertainty is about 25%.

3. Computational methodology

The modeling of soot-chemistry-turbulence interactions is aided by a statistical soot model, a modified Radiation Flamelet/Progress Variable (RFPV) combustion model for sooting flames, and a presumed subfilter PDF for closure. Complete details of the integrated LES model for sooting turbulent nonpremixed flames can be found in Mueller and Pitsch [13] and the references therein.

In brief, soot particles and aggregates are described by their volume (V) and surface area (S), and transport equations are solved for the bivariate moments, $M_{x,y} = \sum_i V_i^x S_i^y N_i$, where x and y are the moment orders for volume and surface area and summation over i implies summation over all particle sizes. Comprehensive physical and chemical processes governing the evolution of the moments are considered: particle nucleation from Polycyclic Aromatic Hydrocarbon (PAH) dimers [27–29], PAH condensation, particle coagulation [30], surface growth by the C₂H₂-addition (HACA) mechanism [31], oxidation [32, 33], and oxidation-induced fragmentation [34]. Moment closure is achieved with the Hybrid Method of Moments (HMOM) [30]. In total, four quantities are used to describe the evolution of the soot population: the total soot number density ($M_{0,0}$), the total soot volume ($M_{1,0}$), the total soot surface area ($M_{0,1}$), and the number density of smaller particles (N_0).

The thermochemical states, such as temperature, species mass fractions (Y), and other derived quantities, are obtained from tabulated chemistry, described with the RFPV model of Ihme and Pitsch [35] with modifications for soot by Mueller and Pitsch [13]. Solutions of the steady and unsteady (for radiation) flamelet equations are parameterized by the mixture fraction (Z), a reaction progress variable ($C = Y_{\text{CO}_2} + Y_{\text{CO}} + Y_{\text{H}_2\text{O}} + Y_{\text{H}_2}$), and a heat loss parameter

(H) to account for heat losses due to radiation. Due to significant unsteady effects for PAH [5], the mass fractions for these species deviate from their steady values in the flamelet database. Therefore, an additional transport equation for a lumped PAH species is solved.

The closure for filtered quantities such as density, gas-phase source terms, and soot source terms are achieved with a presumed subfilter PDF model by Mueller and Pitsch [13, 36]. The joint subfilter PDF of the mixture fraction, progress variable, heat loss parameter, and soot moments ($\tilde{P}(Z, C, H, M_i)$) can be modeled by the product of the thermochemical subfilter PDF, $\tilde{P}(Z, C, H)$, and the soot subfilter PDF, $\tilde{P}(M_i)$, due to the time scale decoupling of the gas-phase and soot evolution [36]. The thermochemical PDF is modeled with a beta distribution for the mixture fraction [37]. Convolution of the flamelet database with the PDF is done *a priori* and tabulated as a function of the filtered mixture fraction, subfilter mixture fraction variance, filtered progress variable, and filtered heat loss parameter. The subfilter mixture fraction variance is obtained from the solution of a transport equation for the filtered square of the mixture fraction with a linear relaxation model [38] for the subfilter scalar dissipation rate. The soot subfilter PDF is modeled with a double delta distribution [36], which requires solving an additional transport equation for the filtered square of the number density.

In summary, the continuity, momentum equations, and transport equations for \tilde{Z} , \tilde{Z}^2 , \tilde{C} , \tilde{H} , $\widetilde{Y_{PAH}}$, $\overline{M_{0,0}}$, $\overline{M_{1,0}}$, $\overline{M_{0,1}}$, $\overline{N_0}$, and $\overline{M_{0,0}^2}$ are solved in the simulation. All of the subfilter stresses and scalar fluxes are closed with dynamic models [39] with Lagrangian averaging [40]. The unfiltered soot source terms are closed with HMOM, and the filtered density, gas-phase source terms, and soot source terms are closed with presumed subfilter PDF.

The simulation details are similar to the previous ethylene bluff body flame [15]. Flamelet solutions were computed using FlameMaster [41] with the chemical mechanism, including PAH, of Pitsch and co-workers [42, 43]. The soot and combustion models were implemented in NGA [44]. The continuity and momentum equations are discretized with a centered, second-order scheme, and the scalar equations are discretized with a bounded QUICK scheme [45]. The computational domain is discretized on a structured, non-uniform grid, with $384 \times 192 \times 64$ points in the axial, radial, and circumferential directions, respectively. Following from the results of a boundary condition sensitivity study for the neat ethylene case, turbulence intensity in the central jet is increased by 10% compared to the reported experimental condition (fully developed turbulent pipe flow), and a turbulent boundary layer condition is specified for the coflow.

4. Results and discussion

4.1. Overall flame structure

The overall structure of the turbulent nonpremixed hydrogen added ethylene bluff body flame is shown and compared with the neat ethylene counterpart in Fig. 1. Qualitatively, three distinct regions are identified: a sooting recirculation zone, a non-sooting, high-strain neck region, and a sooting jet-like region. Quantitatively, the clipped, time-averaged LII images of soot volume fraction are also compared. Soot is formed close to the bluff body, where

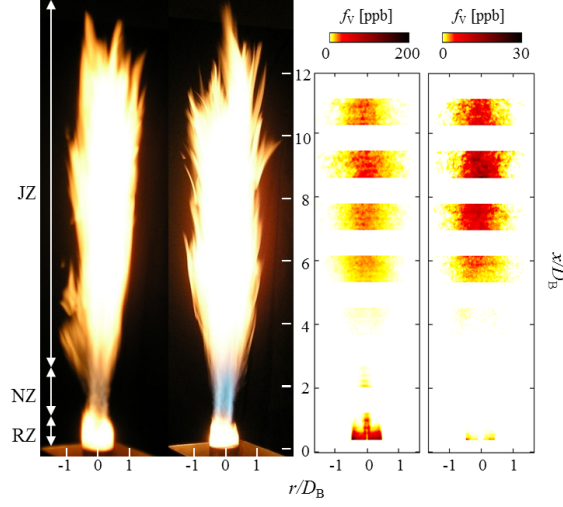


Figure 1: Photographs of the neat ethylene (left) and ethylene/hydrogen (right) bluff body flame, and the corresponding collages of the time-averaged LII images of the soot volume fraction distribution. Three distinct regions are identified as follows: RZ (recirculation zone), NZ (neck zone), and JZ (jet-like zone).

the residence time is long and turbulence intensity is low. No detectable soot is convected into nor formed in the high-strain neck region. Further downstream in the jet-like region, where the scalar dissipation rate decreases as mixing proceeds, soot formation once again occurs. Since the burner is equivalent and the Reynolds number sufficiently large, the overall flame lengths are similar, but the recirculation zone of the hydrogen added flame appears shorter, based on the soot volume fraction measurements.

Although the two flames share similar flow and soot formation patterns, the ethylene/hydrogen flame is significantly less sooting than the neat ethylene flame. As demonstrated in Fig. 2, the axial profiles of the radially integrated soot volume fraction ($\text{ppm}\cdot\text{mm}^2$) are compared for the two flames. Two distinct maxima are observed for both flames and correspond to the upstream recirculation zone and downstream jet-like zone. Furthermore, the reduction in the integrated soot volume fraction is more pronounced in the recirculation zone than in the downstream jet-like region. Specifically, according to both Figs. 1 and 2, the soot reduction in the recirculation zone is more than an order of magnitude, while, in the jet-like zone, the reduction is about a factor of four to six. The difference in the soot reduction rate with hydrogen addition indicates different soot reduction mechanisms and different roles that hydrogen addition plays in these two regions.

4.2. Effects of hydrogen addition

Two effects of hydrogen addition are potentially relevant: chemical and hydrodynamic effects. Chemically, due to the reduced C/H ratio, PAH formation will be inhibited in the hydrogen added flame, and, therefore, soot formation is inhibited. Hydrodynamically, since the fuel jet velocity is increased to match the Reynolds number, the fuel jet to air coflow momentum flux ratio is also increased. As Dally *et al.* [46] demonstrated, the increase in the fuel jet momentum flux decreases the strength of the mixture in the outer vortex in the recirculation zone, further inhibiting

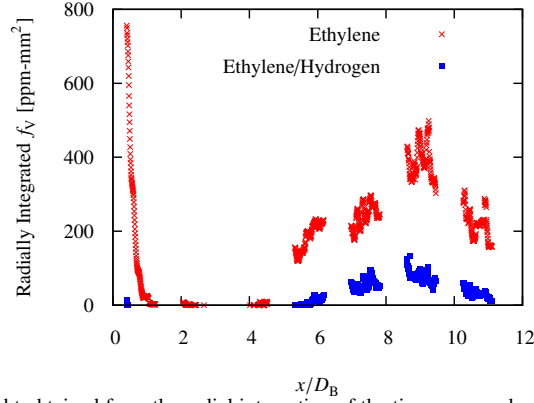


Figure 2: Total soot volume per unit height obtained from the radial integration of the time-averaged soot volume fraction from the LII measurements at each height. For clarity, only every second measurement point is shown.

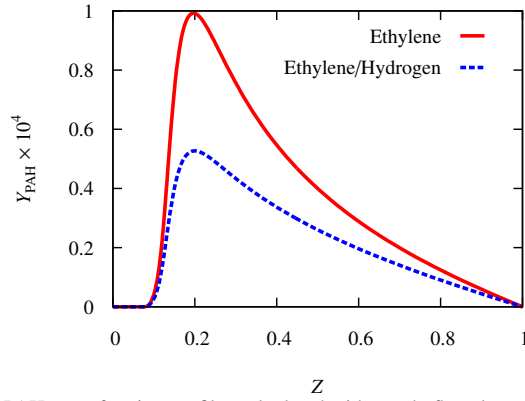


Figure 3: PAH mass fraction profiles calculated with steady flamelets at $\chi = 1 \text{ s}^{-1}$.

soot formation. The relative significance of these two effects in the two sooting regions of the flames are analyzed in this section.

To first quantify the chemical effect, steady flamelets at a moderate scalar dissipation rate ($\chi_{\text{st}} = 1 \text{ s}^{-1}$) were calculated, and the total PAH mass fraction is shown in Fig. 3. PAH forms at rich mixture fractions (the stoichiometric mixture fraction for both cases is about 0.06, differing by less than 5%) and peaks at $Z = 0.2$. Y_{PAH} decreases at even richer mixture fractions due to the temperature drop. The maximum Y_{PAH} decreases by a factor of two with hydrogen addition. In the soot model adopted in the LES, PAH-based soot formation and growth, which has been shown to dominate in turbulent jet flames [5–7, 13, 15], scales as the square of the PAH mass fraction. Therefore, this chemical effect is expected to result in a reduction of soot volume fraction by a factor of four in the jet-like region. This reduction is consistent with the experimental measurements, indicating that chemical effects alone are responsible for soot suppression in the downstream jet-like region.

Conversely, noting that the chemical effect predicted by the steady flamelet solution is less than the total soot reduction in the recirculation zone, soot evolution in this region is further analyzed with LES. Specifically, radial profiles of the time-averaged soot volume fraction are compared for both cases at two axial locations in the recirculation zone,

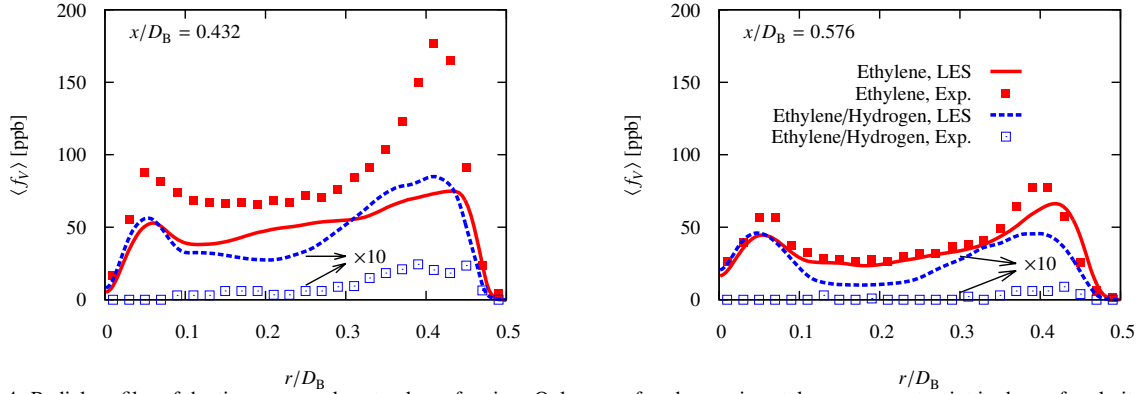


Figure 4: Radial profiles of the time-averaged soot volume fraction. Only every fourth experimental measurement point is shown for clarity. The ethylene flame is reproduced from [15], and the ethylene/hydrogen flame is from this work. Both experimental and computational results for the ethylene/hydrogen flame are scaled up by a factor of ten.

shown in Fig. 4. Qualitatively, two distinct sooting peaks are found in the radial profiles. Mueller *et al.* [15] found in the ethylene bluff body flame that the inner and outer peak corresponds to the PAH-based growth and acetylene-based surface growth pathway, respectively. Quantitatively, the soot volume fraction of the ethylene case is slightly under-predicted but within experimental uncertainty [15]. For the hydrogen added case, the soot volume fraction appears to be overpredicted. However, the mean soot volume fraction from the LES is only slightly higher than the experimental threshold of 3 ppb. Therefore, the LII measurements may underestimate the soot volume fraction by as much as 3 ppb, which easily accounts for the discrepancy between the measurements and LES.

Hydrogen addition not only induces chemical effects through modification of the fuel stream C/H ratio but also hydrodynamically influences mixing, that is, the local mixture fraction, as well as residence time in the recirculation zone. The residence time effect is first estimated by comparing the streamline patterns in the recirculation zone of the two flames, as shown in Fig. 5. In both flames, the circulation vortex appears as single vortex near the outer shear layer between the air coflow and the recirculation zone due to sufficiently large jet/coflow momentum flux ratio [23, 46]. The location and structure of these two vortices are almost identical. Estimating residence time [22] by dividing the length of the recirculation zone by the coflow velocity (identical between these flames), it is found that residence time in the recirculation zone is similar between these two flames. Therefore, differences in residence time plays little role in dictating the difference in soot volume fraction in the recirculation zone in the two flames, and the difference beyond the chemical effects must be a result of different degrees of mixing in the recirculation zone.

As discussed above, the increase of the fuel/coflow momentum flux ratio inhibits entrainment from the jet, resulting in a leaner recirculation zone than the neat ethylene case (recall that the stoichiometric mixture fraction is essentially the same for the two mixtures). The mixture fraction radial profiles from LES as well as the characteristic time scales of the soot formation and oxidation processes from a lightly strained ($\chi_{st} = 1 \text{ s}^{-1}$) steady flamelet solution are shown in Fig. 6. The characteristic time scales of the acetylene-based growth and oxidation processes remain the same, while that of the PAH-based growth slows down due to reduced PAH concentration as discussed previously.

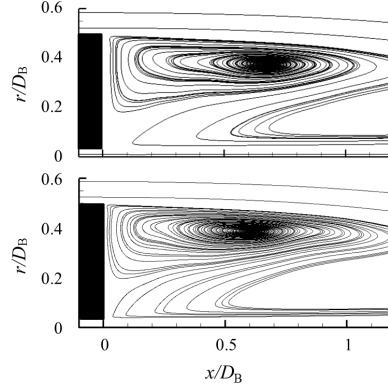


Figure 5: Streamlines in the recirculation zone of the neat ethylene flame (top) and ethylene/hydrogen flame (bottom).

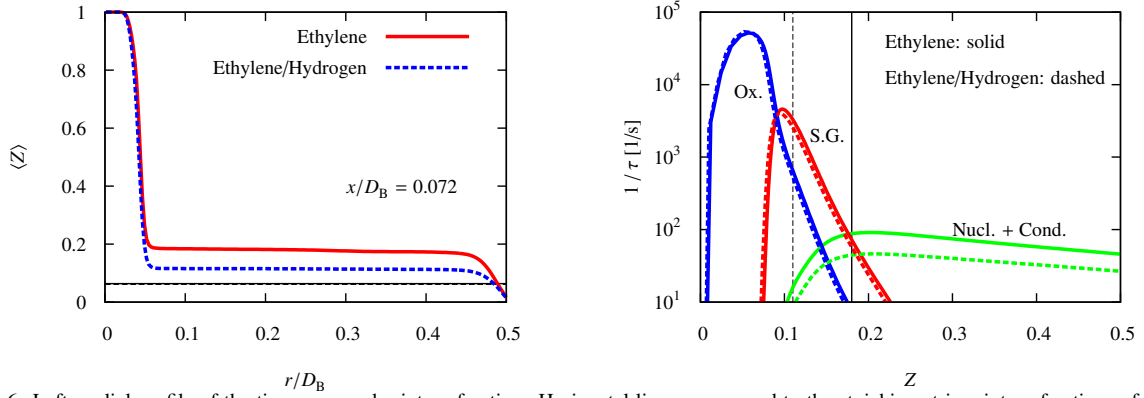


Figure 6: Left: radial profile of the time-averaged mixture fraction. Horizontal lines correspond to the stoichiometric mixture fractions of these two flames and almost overlap. Right: characteristic inverse time scales of the soot processes from the steady flamelet calculations at $\chi_{st} = 1 \text{ s}^{-1}$. Vertical lines correspond to the mixture fraction in the flat regions of the radial plot.

Additionally, as expected, the mixture fraction profile near the bluff body surface is affected substantially by hydrogen addition. As shown in Fig. 6, in between the central jet and coflow air, the mixture fraction drops by 25%. Consequently, the mixture fraction shifts from where PAH-based growth is favored ($Z \sim 0.18$) to where oxidation becomes as fast as acetylene-based surface growth ($Z \sim 0.11$), suppressing soot formation and growth. Therefore, soot formation in the recirculation zone is further inhibited by this hydrodynamic effect that results in a leaner recirculation zone, in addition to the chemical effect.

Similar to the previous study [15], the PAH-based, acetylene-based, and oxidation source terms are shown in Fig. 7 to elucidate the evolution of soot. Soot nucleation mainly occurs near the inner shear layer between the fuel jet and recirculation zone where mixture fraction is high. Some of this soot is entrained by the recirculation zone and transported back upstream toward the bluff body then radially outward toward the outer shear layer by the recirculation vortex. This trend is consistent with the neat ethylene case. In the neat ethylene flame, acetylene-based surface growth becomes dominant in the outer shear layer close to the stoichiometric mixture fraction contour, and oxidation is almost negligible except close to the neck zone. However, due to the lean shift of the mean mixture fraction near the bluff

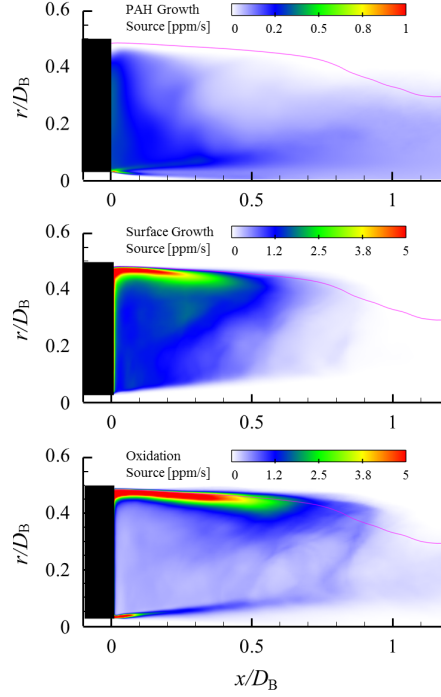


Figure 7: Time-averaged soot volume fraction source term [ppm/s] in the recirculation zone of the ethylene/hydrogen flame. The magenta line correspond to the stoichiometric mixture fraction contour.

body in the hydrogen added flame, oxidation becomes comparable to the acetylene-based growth. Consequently, soot nucleation in the recirculation zone of the hydrogen added flame is first suppressed due to reduced PAH concentration, and soot surface growth is further inhibited by soot oxidation, resulting in a less sooting recirculation zone than the neat ethylene flame.

5. Conclusions

A sooting turbulent bluff body stabilized ethylene/hydrogen flame was studied both experimentally and computationally and compared with a previously analyzed neat ethylene counterpart [15]. Laser-induced incandescence (LII) was utilized to measure the soot volume fraction in the flame. An integrated Large Eddy Simulation (LES) model was adopted to elucidate the interactions between soot, turbulence, and chemistry. The statistical soot model was based on the Hybrid Method of Moments (HMOM), considering detailed nucleation, condensation, particle collision, surface growth, oxidation, and fragmentation processes that influence soot evolution. The combustion model for the gas-phase was based on the Radiation Flamelet/Progress Variable (RFPV) model with modifications to account for the removal of Polycyclic Aromatic Hydrocarbon (PAH) from the gas-phase. A presumed PDF was utilized to model unresolved subfilter scale interactions.

Similar to the neat ethylene bluff body flame, three distinct flow regions were observed experimentally: a sooting recirculation zone, a non-sooting, high-strain neck region, and a sooting jet-like zone. Although the hydrogen

added bluff body flame is significantly less sooting than the neat ethylene counterpart overall, soot reduction in the recirculation zone near the bluff body is more pronounced than in the downstream jet-like region. Both chemical and hydrodynamic effects were identified as reasons for this decrease.

The chemical effect was first quantified from a steady flamelet calculation. Due to the hydrogen addition, PAH mass fraction was found to decrease by a factor of two, indicating a factor of four decrease in the PAH-based growth rate that includes both nucleation and PAH condensation. This is consistent with the soot reduction in the downstream jet-like region, where PAH-based growth is dominant. Therefore, the chemical effect is dominant in this region.

The hydrodynamic effect was then analyzed, since both the experimental measurements and LES calculations demonstrated additional soot reduction in the recirculation zone, which could not be explained with the chemical effect alone. The streamline patterns in the recirculation zone of the two flames are similar according to LES, and therefore, differences in residence time plays little role in the difference in soot volume fraction in the recirculation zone.

Conversely, in the experiment, to attain the same Reynolds number in the hydrogen added flame as the neat ethylene flame, the central jet velocity was increased. This increase in the fuel to air coflow momentum flux ratio allows relatively less fuel and more air in the recirculation zone near the bluff body surface, compared to the neat ethylene flame. Due to the leaner mixture fraction in the recirculation zone, soot nucleation and surface growth is inhibited and soot oxidation is promoted. This hydrodynamic effect together with the chemical effect accounts for the soot reduction in the recirculation zone.

Acknowledgments

The Australian authors gratefully acknowledge funding from the Australian Research Council (ARC) through the Discovery and the Linkage Infrastructure, Equipment, and Facilities (LIEF) grant programs.

References

- [1] H. Wang, *Proc. Combust. Inst.* 33 (2011) 41–67.
- [2] C. S. Yoo, H. G. Im, *Proc. Combust. Inst.* 31 (2007) 701–708.
- [3] D. O. Lignell, J. H. Chen, P. J. Smith, T. Lu, C. K. Law, *Combust. Flame* 151 (2007) 2–28.
- [4] D. O. Lignell, J. H. Chen, P. J. Smith, *Combust. Flame* 155 (2008) 316–333.
- [5] F. Bisetti, G. Blanquart, M. E. Mueller, H. Pitsch, *Combust. Flame* 159 (2012) 317–335.
- [6] A. Attili, F. Bisetti, M. E. Mueller, H. Pitsch, *Combust. Flame* 161 (2014) 1849–1865.
- [7] A. Attili, F. Bisetti, M. E. Mueller, H. Pitsch, *Proc. Combust. Inst.* 35 (2015) 1215–1223.
- [8] N. H. Qamar, G. J. Nathan, Z. T. Alwahabi, K. D. King, *Proc. Combust. Inst.* 30 (2005) 1493–1500.
- [9] N. H. Qamar, Z. T. Alwahabi, Q. N. Chan, G. J. Nathan, D. Roekaerts, K. D. King, *Combust. Flame* 156 (2009) 1339–1347.
- [10] S.-Y. Lee, S. R. Turns, R. J. Santoro, *Combust. Flame* 156 (2009) 2264–2275.
- [11] J. Zhang, C. R. Shaddix, R. W. Schefer, *Rev. Sci. Instrum.* 82 (2011) 074101.
- [12] H. El-Asrag, S. Menon, *Combust. Flame* 156 (2009) 385–395.

- [13] M. E. Mueller, H. Pitsch, *Combust. Flame* 159 (2012) 2166–2180.
- [14] Y. Xuan, G. Blanquart, *Proc. Combust. Inst.* 35 (2015) 1911–1919.
- [15] M. E. Mueller, Q. N. Chan, N. H. Qamar, B. Dally, H. Pitsch, *Combust. Flame* 160 (2013) 1298–1309.
- [16] P. A. Tesner, *Proc. Combust. Inst.* 7 (1958) 546–553.
- [17] P. Dearden, R. Long, *J. Appl. Chem.* 18 (1968) 243–251.
- [18] D. X. Du, R. L. Axelbaum, C. K. Law, *Comb. Flame* 102 (1995) 11–20.
- [19] O. L. Gülder, D. R. Snelling, R. A. Sawchuk, *Proc. Combust. Inst.* 26 (1996) 2351–2358.
- [20] H. Guo, F. Liu, G. J. Smallwood, O. L. Gülder, *Combust. Flame* 145 (2006) 324–338.
- [21] H. Zhao, R. Stone, B. Williams, *Energy Fuels* 28 (2014) 2144–2151.
- [22] B. B. Dally, A. R. Masri, R. S. Barlow, G. J. Fiechtner, D. F. Fletcher, *Proc. Combust. Inst.* 26 (1996) 2191–2197.
- [23] B. B. Dally, D. F. Fletcher, A. R. Masri, *Combust. Theor. Model.* 2 (1998) 193–219.
- [24] C. Schulz, B. F. Kock, M. Hofmann, H. Michelsen, S. Will, B. Bougie, R. Suntz, G. Smallwood, *Appl. Phys. B* 83 (2006) 333–354.
- [25] Z. W. Sun, Z. T. Alwahabi, D. H. Gu, S. M. Mahmoud, G. J. Nathan, B. B. Dally, *Appl. Phys. B* 119 (2015) 731–743.
- [26] H. Bladh, P. E. Johnsson, J. Bengtsson, *Appl. Phys. B* 90 (2008) 109–125.
- [27] C. A. Schuetz, M. Frenklach, *Proc. Combust. Inst.* 29 (2002) 2307–2314.
- [28] D. Wong, C. A. Schuetz, M. Frenklach, in: H. Bockhorn, A. D’Anna, A. Sarofim, H. Wang (Eds.), *Combustion Generated fine Carbonaceous Particles*, KIT Scientific Publishing, 2009, pp. 247–257.
- [29] G. Blanquart, H. Pitsch, in: H. Bockhorn, A. D’Anna, A. Sarofim, H. Wang (Eds.), *Combustion Generated fine Carbonaceous Particles*, KIT Scientific Publishing, 2009, pp. 439–466.
- [30] M. E. Mueller, G. Blanquart, H. Pitsch, *Combust. Flame* 156 (2009) 1143–1155.
- [31] M. Frenklach, H. Wang, *Proc. Combust. Inst.* 23 (1991) 1559–1566.
- [32] A. Kazakov, H. Wang, M. Frenklach, *Combust. Flame* 100 (1995) 111–120.
- [33] K. G. Neoh, J. B. Howard, A. F. Sarofim, in: *Particulate Carbon Formation during Combustion*, Plenum Press, 1981, pp. 162–282.
- [34] M. E. Mueller, G. Blanquart, H. Pitsch, *Proc. Combust. Inst.* 33 (2011) 667–674.
- [35] M. Ihme, H. Pitsch, *Phys. Fluids* 20 (2008) 055110.
- [36] M. E. Mueller, H. Pitsch, *Phys. Fluids* 23 (2011) 115104.
- [37] A. W. Cook, J. J. Riley, *Phys. Fluids* 6 (1994) 2868–2870.
- [38] M. Ihme, H. Pitsch, *Combust. Flame* 155 (2008) 90–107.
- [39] M. Germano, U. Piomelli, P. Moin, W. H. Cabot, *Phys. Fluids A* 3 (1991) 1760–1765.
- [40] C. Meneveau, T. S. Lund, W. H. Cabot, *J. Fluid Mech.* 319 (1996) 353–385.
- [41] H. Pitsch, *FlameMaster*, a C++ computer program for 0D combustion and 1D laminar flame calculations.
- [42] G. Blanquart, P. Pepiot, H. Pitsch, *Combust. Flame* 156 (2009) 588–607.
- [43] K. Narayanaswamy, G. Blanquart, H. Pitsch, *Combust. Flame* 157 (2010) 1879–1898.
- [44] O. Desjardins, G. Blanquart, G. Balarac, H. Pitsch, *J. Comput. Phys.* 227 (2008) 7125–7159.
- [45] M. Herrmann, G. Blanquart, V. Raman, *AIAA J.* 44 (2006) 2879–2886.
- [46] B. B. Dally, A. R. Masri, R. S. Barlow, G. J. Fiechtner, *Combust. Flame* 114 (1998) 119–148.

List of Figures

1	Photographs of the neat ethylene (left) and ethylene/hydrogen (right) bluff body flame, and the corresponding collages of the time-averaged LII images of the soot volume fraction distribution. Three distinct regions are identified as follows: RZ (recirculation zone), NZ (neck zone), and JZ (jet-like zone).	4
2	Total soot volume per unit height obtained from the radial integration of the time-averaged soot volume fraction from the LII measurements at each height. For clarity, only every second measurement point is shown.	4
3	PAH mass fraction profiles calculated with steady flamelets at $\chi = 1 \text{ s}^{-1}$	5
4	Radial profiles of the time-averaged soot volume fraction. Only every fourth experimental measurement point is shown for clarity. The ethylene flame is reproduced from [15], and the ethylene/hydrogen flame is from this work. Both experimental and computational results for the ethylene/hydrogen flame are scaled up by a factor of ten.	5
5	Streamlines in the recirculation zone of the neat ethylene flame (top) and ethylene/hydrogen flame (bottom).	6
6	Left: radial profile of the time-averaged mixture fraction. Horizontal lines correspond to the stoichiometric mixture fractions of these two flames and almost overlap. Right: characteristic inverse time scales of the soot processes from the steady flamelet calculations at $\chi_{\text{st}} = 1 \text{ s}^{-1}$. Vertical lines correspond to the mixture fraction in the flat regions of the radial plot.	6
7	Time-averaged soot volume fraction source term [ppm/s] in the recirculation zone of the ethylene/hydrogen flame. The magenta line correspond to the stoichiometric mixture fraction contour.	7