

两个假设

Tips: 大物这一章物理量及其对应的字母一定要分清

1. 分子数密度  $n = \frac{dN}{dV}$  处处相等
2. 速度的平均值  $\bar{v}_x = \frac{1}{N} \sum_{i=1}^N \bar{v}_{ix}$  各方向运动概率相等  $\bar{v}_x = \bar{v}_y = \bar{v}_z = 0$

引入: 速度平方的平均值  $\bar{v}_x^2 = \frac{1}{N} \sum_{i=1}^N v_{ix}^2$   $\bar{v}_x^2 = \bar{v}_y^2 = \bar{v}_z^2 = \frac{1}{3} \bar{v}^2$ 压强  $p = \frac{\bar{F}}{S} = \frac{\sum f_{ix} t}{\Delta t S}$   $p = \frac{1}{3} n m \bar{v}^2 = \frac{2}{3} n \cdot \frac{1}{2} m \bar{v}^2 = \frac{2}{3} n \bar{\epsilon}_t$  平均平均动能推导:  $I_{ii} = -2\mu v_{ix}$  ( $\mu$ : 单个分子质量)对面的冲量  $I_{ii} = 2\mu v_{ix}$ 

$$T_i = \frac{2x}{v_{ix}} \quad \epsilon_i = \frac{t}{T_i} = \frac{v_{ix} t}{2x}$$

$$I_{i \text{ sum}} = \epsilon_i I_i = \frac{v_{ix} t}{2x} \cdot 2\mu v_{ix} = \frac{\mu t}{x} v_{ix}^2$$

$$I_{\text{sum}} = \sum_{i=1}^N \frac{\mu t}{x} v_{ix}^2$$

$$\bar{F} = \frac{I_{\text{sum}}}{t} = \sum_{i=1}^N \frac{\mu}{x} v_{ix}^2$$

$$p = \frac{\bar{F}}{S} = \frac{1}{yz} \sum_{i=1}^N \frac{\mu}{x} v_{ix}^2 = \frac{1}{xyz} \sum_{i=1}^N \mu v_{ix}^2 = \frac{1}{V} \mu \sum_{i=1}^N v_{ix}^2 = \frac{N}{V} \mu \cdot \left( \frac{1}{N} \sum_{i=1}^N v_{ix}^2 \right)$$

$$= n \cdot \mu \cdot \bar{v}_x^2 = \frac{1}{3} n \mu \bar{v}^2$$

$$pV = \frac{m}{M} RT = \nu RT \quad (R = 8.31 \text{ J} \cdot \text{mol}^{-1} \cdot \text{K}^{-1} \text{ 普适气体常量 or 摩尔气体常量})$$

$$\nu = \frac{m}{M} = \frac{N}{N_A} \quad (M: \text{摩尔质量 kg/mol})$$

$$p = \frac{1}{V} \cdot \frac{N}{N_A} \cdot R \cdot T = \frac{N}{V} \cdot \frac{R}{N_A} \cdot T = n \cdot k \cdot T \quad (k = 1.38 \times 10^{-23} \text{ J} \cdot \text{K}^{-1} \text{ 玻尔兹曼常量})$$

$$\begin{cases} p = nkT \\ p = \frac{2}{3} n \bar{\epsilon}_t \end{cases} \Rightarrow \bar{\epsilon}_t = \frac{3}{2} kT \quad (T = t + 273.15)$$

$$\bar{\epsilon}_t = \frac{3}{2}kT = \frac{1}{2}\mu \bar{v}^2 \Rightarrow \sqrt{\bar{v}^2} = \sqrt{\frac{3kT}{\mu}} = \sqrt{\frac{3RT}{M}} \quad (R = N_A k)$$

自由度

- 单原子分子  $i=3$
- 刚性双原子分子  $i=5$
- 刚性多原子分子  $i=6$

能量均分：分子热运动的每一个平均自由度的平均动能均等于  $\frac{1}{2}kT$

分子自由度  $i \Rightarrow$  平均动能  $\bar{\epsilon} = \frac{i}{2}kT$

$\nu$  mol 理想气体内能

$$\bar{E} = \nu N_A \cdot (\frac{i}{2}kT) = \nu \cdot \frac{i}{2}RT = \frac{i}{2}PV$$

$$\frac{RT}{M} = \frac{PV}{m} = \frac{P}{\frac{m}{V}} = \frac{P}{\rho} \quad (\text{题目涉及密度 } \rho \text{ 可用})$$

速率分布函数

$$dN = N_0 f(v) dv \quad (N_0: \text{分子数}) \quad f(v) = \frac{dN}{N_0 dv}$$

$$f(v) dv = \frac{dN}{N_0} \quad \text{占总分子数的百分比}$$

$$N_0 f(v) dv = dN \quad \text{在 } v \sim v+dv \text{ 内的分子数}$$

$$\int_{v_1}^{v_2} f(v) dv \quad \text{曲线下的面积；百分比 or 概率}$$

$$\int_0^{\infty} f(v) dv = 1 \quad \text{归一化条件}$$

最概然速率  $v_p$  (most probable speed)

$$\left. \frac{df}{dv} \right|_{v=v_p} = 0$$

$$\text{平均速率 } \bar{v} = \frac{1}{N_0} \int_0^{N_0} v dN = \frac{1}{N_0} \int_0^{\infty} v N_0 f(v) dv = \int_0^{\infty} v f(v) dv$$

方均根速率  $\sqrt{\bar{v}^2}$

$$\bar{v}^2 = \frac{1}{N_0} \int_0^{N_0} v^2 dN = \frac{1}{N_0} \int_0^{\infty} v^2 N_0 f(v) dv = \int_0^{\infty} v^2 f(v) dv$$

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介于  $v_1 \sim v_2$  之间 电子的

平均速率:  $\bar{v}_{12} = \frac{\int_{v_1}^{v_2} v dN}{\int_{v_1}^{v_2} dN}$  方均根速率  $\sqrt{\bar{v}_{12}^2} = \sqrt{\frac{\int_{v_1}^{v_2} v^2 N_0 f(v) dv}{\int_{v_1}^{v_2} N_0 f(v) dv}}$

$$= \frac{\int_{v_1}^{v_2} v f(v) dv}{\int_{v_1}^{v_2} f(v) dv} = \sqrt{\frac{\int_{v_1}^{v_2} v^2 f(v) dv}{\int_{v_1}^{v_2} f(v) dv}}$$

麦克斯韦速率分布 (那一块不用记)

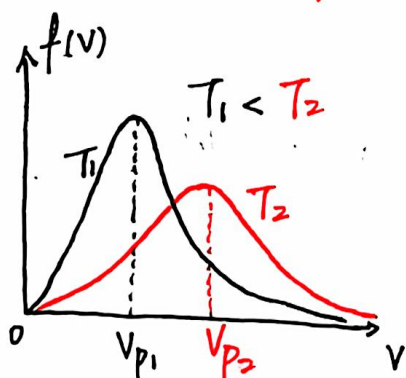
推导: 令  $b = \frac{m}{2kT}$  代入  $\frac{df}{dv} \Big|_{v=v_p} = 0 \Rightarrow v_p = \sqrt{\frac{1}{b}}$

代入  $\bar{v} = \frac{1}{N_0} \int_0^{N_0} v dN \Rightarrow \bar{v} = 2\sqrt{\frac{1}{b\pi}}$

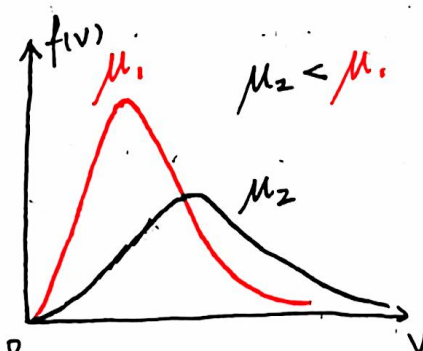
代入  $\sqrt{\bar{v}^2} = \sqrt{\frac{1}{N_0} \int_0^{N_0} v^2 dN} \Rightarrow \sqrt{\bar{v}^2} = \sqrt{\frac{3}{2b}}$

$$\begin{cases} v_p = \sqrt{\frac{2kT}{m}} = \sqrt{\frac{2RT}{M}} \\ \bar{v} = \sqrt{\frac{8kT}{\pi m}} = \sqrt{\frac{8RT}{\pi M}} \\ \sqrt{\bar{v}^2} = \sqrt{\frac{3kT}{m}} = \sqrt{\frac{3RT}{M}} \end{cases}$$

$$v_p : \bar{v} : \sqrt{\bar{v}^2} = \sqrt{2} : \sqrt{\frac{8}{\pi}} : \sqrt{3}$$



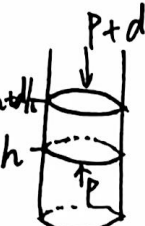
温度越高  
分子热运动越强烈



分子质量越小  
分子越容易运动



等温气压公式  $P = P_0 e^{-\frac{Mgh}{RT}} = P_0 e^{-\frac{\rho gh}{RT}}$



$$P S - (P + dp) S - \rho g S dh = 0 \Rightarrow -dp = \rho g dh$$

$$P = \frac{PM}{RT} \quad -dp = \frac{PM}{RT} g dh \Rightarrow \frac{dP}{P} = -\frac{Mg}{RT} dh$$

$$\int_{P_0}^P \frac{dP}{P} = \int_0^h -\frac{Mg}{RT} dh \Rightarrow \frac{P}{P_0} = e^{-\frac{Mgh}{RT}}$$

分子数密度按高度分布

$$n = \frac{P}{kT} = \frac{P_0}{kT} e^{-\frac{\rho gh}{kT}} \quad \left( \frac{P_0}{kT} = n_0 \text{ } h=0 \text{ 处的分子数密度} \right)$$

碰撞频率  $\bar{z}$

其他分子静止  $dv = \bar{v}_r dt \sigma \quad \sigma = \pi d^2 \quad dN = n dv = n \bar{v}_r dt \sigma$

$$\bar{z} = \frac{dN}{dt} = n \bar{v}_r \sigma = n \bar{v}_r \pi d^2 \quad (\bar{v}_r = \sqrt{2} \bar{v})$$

其他分子也动  $\bar{z} = \sqrt{2} \pi d^2 \bar{v} n$

特别地, 若为电子  $\bar{z} = \frac{1}{4} n \pi d^2 \bar{v}_e$

平均自由程  $\bar{\lambda} = \frac{\bar{v}}{\bar{z}} = \frac{\bar{v}}{\sqrt{2} \pi d^2 n \bar{v}} = \frac{1}{\sqrt{2} \pi d^2 n} = \frac{kT}{\sqrt{2} \pi d^2 P}$

范德瓦尔斯方程

$$\left( P + a \frac{v^2}{V^2} \right) (V - vb) = \nu R T$$

$a$ : 压强修正值

$b$ : 1 mol 气体分子的体积, 体积修正值

热力学第一定律:  $\Delta E = Q + A \quad dQ = dE + (-dA)$   
 外界传递热量 外界对系统做功

做功  $-A = \int_{V_1}^{V_2} P dV$

$$\Delta E = \nu \cdot \frac{1}{2} R T_2 - \nu \cdot \frac{1}{2} R T_1 = \nu \cdot \frac{1}{2} R \Delta T = \frac{m}{M} \cdot \frac{1}{2} R \Delta T = \frac{1}{2} (P_2 V_2 - P_1 V_1)$$

$$dE = \nu \cdot \frac{1}{2} R dT = \frac{m}{M} \frac{1}{2} R dT \quad Q = \Delta E + (-A) = \nu \cdot \frac{1}{2} R \Delta T + \int_{V_1}^{V_2} P dV$$

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热容  $C = \frac{dQ}{dT}$  比热  $c = \frac{dQ}{m dT} = \frac{C}{m}$

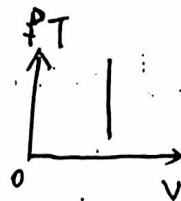
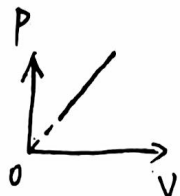
$$dQ = m c dT = \int_{T_1}^{T_2} m c dT = m c \Delta T$$

摩尔热容  $C_{l,m} = \frac{dQ}{\nu dT} = \frac{C}{\nu} = \frac{C}{\frac{m}{M}} = cM$

1 mol 物质  $T \uparrow 1K$   
所吸收的热量

$$Q_l = \int_{T_1}^{T_2} \nu C_{l,m} dT$$

等体过程  $V = \text{Const}$   $\frac{P}{T} = P T^{-1} = \frac{\nu R}{V}$



$(-A_V) = 0$  (体积无变化)

$$\Delta E = \nu \cdot \frac{1}{2} R \cdot \Delta T \quad Q = \Delta E + (-A_V) = \Delta E$$

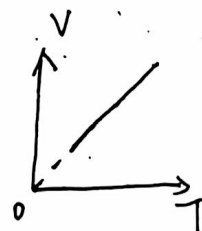
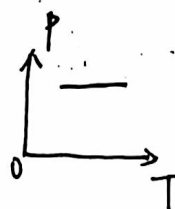
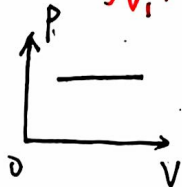
定体摩尔热容  $C_{V,m} = \frac{1}{2} R$

$$dE = \nu \cdot \frac{1}{2} R dT = \nu C_{V,m} dT$$

$$dQ = dE + (-dA_V) = \nu C_{V,m} dT + P dV$$

$$Q = \Delta E + (-A) = \int_{T_1}^{T_2} \nu C_{V,m} dT + \int_{V_1}^{V_2} P dV$$

等压过程  $dp = 0$   $\frac{V}{T} = \frac{\nu R}{P} = \text{Const}$



$$(-A_P) = \int_{V_1}^{V_2} P dV = P(V_2 - V_1) = \nu R(T_2 - T_1)$$

$$\Delta E = \nu \cdot \frac{1}{2} R \Delta T = \nu \cdot \frac{1}{2} R(T_2 - T_1) = \nu C_{V,m}(T_2 - T_1)$$

$$Q = \Delta E + (-A_P) = \nu \cdot (C_{V,m} + R)(T_2 - T_1)$$

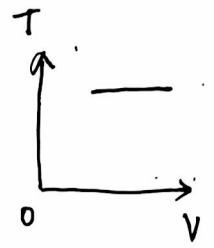
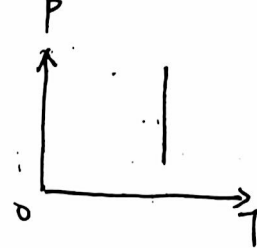
定压摩尔热容  $C_{P,m} = \frac{dQ_P}{\nu dT} = C_{V,m} + R = \frac{1}{2} R + R = (\frac{1}{2} + 1) R$

定压摩尔热容计算等压过程

$$Q_p = \nu C_{p,m} dT \quad Q_p = \int_{T_1}^{T_2} \nu C_{p,m} dT$$

摩尔热容比  $\gamma = \frac{C_{p,m}}{C_{v,m}} = \frac{C_{v,m} + R}{C_{v,m}} = 1 + \frac{R}{C_{v,m}} = 1 + \frac{2}{i} \quad \gamma - 1 = \frac{R}{C_{v,m}}$

等温过程  $PV = \nu RT = \text{Const.}$



$$\Delta E = \nu \cdot \frac{1}{2} R \Delta T = \nu C_{v,m} \Delta T = 0$$

$$Q_T = -A_T = \int_{V_1}^{V_2} P dV = \int_{V_1}^{V_2} \frac{\nu RT}{V} dV = \nu RT \ln \frac{V_2}{V_1} = \nu RT \ln \frac{P_1}{P_2}$$

等温摩尔热容  $C_{T,m} = \frac{dQ}{\nu dT} \rightarrow +\infty$

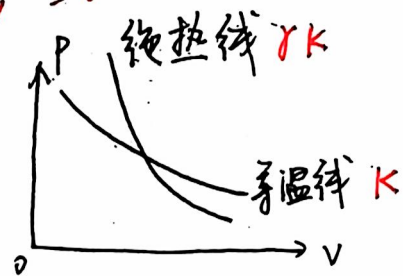
绝热过程  $Q = 0$

$$-dA = P dV \quad dE = \nu C_{v,m} dT \quad 0 = dE + (-dA)$$

$$PV = \nu RT \rightarrow \nu R dT = P dV + V dP \Rightarrow \frac{dP}{P} + \gamma \frac{dV}{V} = 0$$

$$\nu C_{v,m} dT + P dV = 0$$

$$\Rightarrow PV^\gamma = C_1 \quad TV^{\gamma-1} = C_2 \quad P^{\gamma-1} T^{-\gamma} = C_3$$



$$Q = 0$$

$$PV^\gamma = P_1 V_1^\gamma = P_2 V_2^\gamma \rightarrow P = P_1 V_1^\gamma V^{-\gamma}$$

$$-A_Q = \int_{V_1}^{V_2} P dV = \int_{V_1}^{V_2} P_1 V_1^\gamma V^{-\gamma} dV = \frac{\Delta(PV)}{1-\gamma} = \frac{P_2 V_2 - P_1 V_1}{1-\gamma}$$

$$Q = \Delta E + (-A_Q) = 0 \Rightarrow -A_Q = -\Delta E = -\nu C_{v,m} \Delta T$$

$$\Delta E = A_Q = \frac{P_2 V_2 - P_1 V_1}{\gamma - 1}$$

绝热摩尔热容  $C_{Q,m} = \frac{dQ}{\nu dT} = 0 \quad C_{v,m} = \frac{R}{\gamma - 1}$

多方过程  $PV^n = \text{Const} \quad n: \text{多方指数}$



$$PV^n = P_1 V_1^n = P_2 V_2^n$$

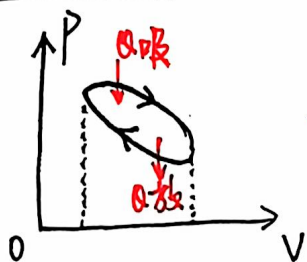
$$-A_n = \frac{P_2 V_2 - P_1 V_1}{1-n} = \frac{\nu R \Delta T}{1-n} \quad \Delta E = \nu C_{v,m} \Delta T$$

$$Q_n = \Delta E + (-A_n) = \nu \cdot \frac{n-\gamma}{n-1} C_{v,m} \Delta T$$

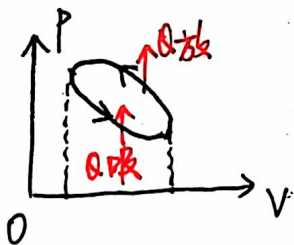
$$C_{n,m} = \frac{dQ_n}{\nu dT} = \frac{n-\gamma}{n-1} C_{v,m}$$

$$Q_n = \int_{T_1}^{T_2} \nu C_{n,m} dT = \nu C_{n,m} \Delta T = \nu \cdot \frac{n-\gamma}{n-1} C_{v,m} \Delta T$$

循环过程  $\Delta E = 0$   $Q = \Delta E + (-A) = -A$  顺时针为正循环



$$-A = Q_{\text{吸}} - |Q_{\text{放}}| > 0 \quad \text{正循环}$$



$$-A = Q_{\text{吸}} - |Q_{\text{放}}| < 0 \quad \text{逆循环}$$

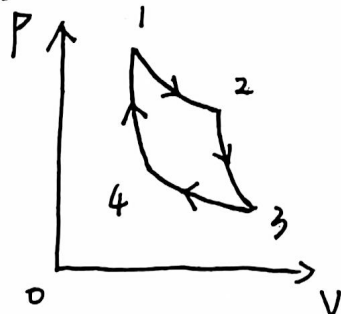
正循环  $\rightarrow$  热机

$$\eta = \frac{-A}{Q_{\text{吸}}} = \frac{Q_{\text{吸}} - |Q_{\text{放}}|}{Q_{\text{吸}}} = 1 - \frac{|Q_{\text{放}}|}{Q_{\text{吸}}}$$

逆循环  $\rightarrow$  制冷机

$$e = \frac{Q_{\text{放}}}{A} = \frac{Q_{\text{放}}}{|Q_{\text{放}}| - Q_{\text{吸}}}$$

卡诺循环



$$1 \rightarrow 2 \text{ 等温膨胀 } Q_{12} = \nu R T_1 \ln \frac{V_2}{V_1} > 0 \text{ 吸热}$$

$$2 \rightarrow 3 \text{ 绝热膨胀 } Q_{23} = 0 \quad T_1 V_2^{\gamma-1} = T_2 V_3^{\gamma-1}$$

$$3 \rightarrow 4 \text{ 等温压缩 } Q_{34} = \nu R T_2 \ln \frac{V_4}{V_3} < 0 \text{ 放热}$$

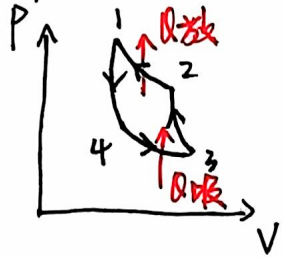
$$4 \rightarrow 1 \text{ 绝热压缩 } Q_{41} = 0 \quad T_1 V_1^{\gamma-1} = T_2 V_4^{\gamma-1}$$

$$\frac{V_2}{V_1} = \frac{V_3}{V_4}$$

$$\eta_c = \frac{-A}{Q_{\text{吸}}} = 1 - \frac{vRT_2 \ln \frac{V_3}{V_4}}{vRT_1 \ln \frac{V_2}{V_1}} = 1 - \frac{T_2}{T_1}$$

$$-\frac{Q_{T_2}}{T_2} = \frac{Q_{T_1}}{T_1} \Rightarrow \frac{Q_{T_1}}{T_1} + \frac{Q_{T_2}}{T_2} = 0 \quad \text{克劳修斯等式} \quad \oint \frac{dQ}{dT} = 0$$

制冷 (图)



$$Q_{\text{吸}} = Q_{43}$$

$$Q_{\text{放}} = Q_{21}$$

$$e = \frac{Q_{\text{吸}}}{A} = \frac{Q_{\text{吸}}}{|Q_{\text{放}}| - Q_{\text{吸}}} = \frac{T_2}{T_1 - T_2}$$

熵  $\oint \frac{dQ}{dT} = 0$  卡诺循环中,  $\frac{dQ}{T}$  总和为 0

$$dS = \frac{dQ}{T} \quad (\text{J/K}) \quad dQ = TdS \quad Q = \int_{S_1}^{S_2} T dS$$

$$dQ = TdS = dE + (-dA) = dE + PdV$$

绝热可逆

$$dS = \int_a^b \frac{dQ}{T} = 0 \quad \text{等熵过程}$$

等体可逆

$$\Delta S = \int_a^b \frac{dQ_{\text{等体}}}{T} = \int_{T_1}^{T_2} \frac{v C_{v,m} dT}{T} = v C_{v,m} \ln \frac{T_2}{T_1}$$

等压可逆

$$\Delta S = \int_a^b \frac{dQ_{\text{等压}}}{T} = \int_{T_1}^{T_2} \frac{v C_{p,m} dT}{T} = v C_{p,m} \ln \frac{T_2}{T_1}$$

等温可逆

$$\Delta S = \int_a^b \frac{dQ_{\text{等温}}}{T} = \frac{Q_{\text{等温}}}{T} = \frac{1}{T} vRT \ln \frac{V_2}{V_1} = vR \ln \frac{V_2}{V_1}$$

熵变计算

已知 V & T

$$S_B - S_A = v C_{v,m} \ln \frac{T_B}{T_A} + vR \ln \frac{V_B}{V_A}$$

已知 P & T

$$S_B - S_A = v C_{p,m} \ln \frac{T_B}{T_A} - vR \ln \frac{P_B}{P_A}$$

已知 P & V

$$S_B - S_A = v C_{p,m} \ln \frac{V_B}{V_A} + v C_{v,m} \ln \frac{P_B}{P_A}$$