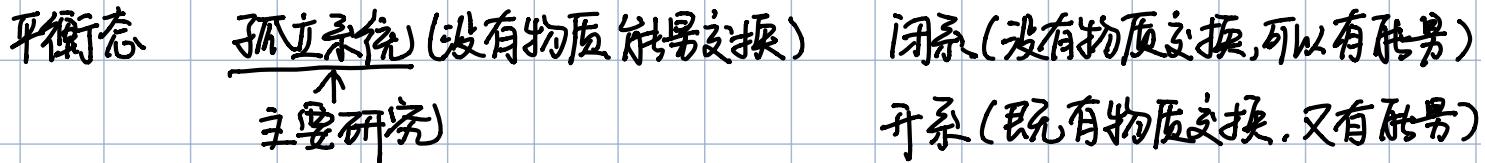


热力学基本规律



Notes: 1° 弛豫时间: 非常快, 很快达到平衡 $\sim 10^{-10}\text{s}$ (气体典型)

2° 热力学平衡:

3° 不考虑涨落: 体系足够大, 分子足够多则涨落比较小

4° 非孤立系统: 处理方法: 所研究的系统 + 环境 = 孤立系统

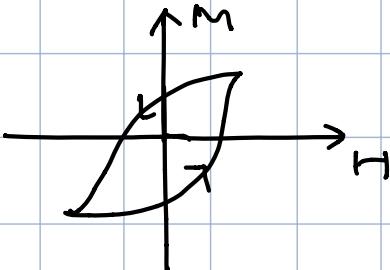
状态参量, 状态函数

$$\underbrace{N\bar{v} = V}_{\text{简单系统}} \quad \text{力学: } P \quad \text{化学: } n_i \quad \text{电磁: } \vec{E}, \vec{P}, \vec{H}, \vec{M}$$

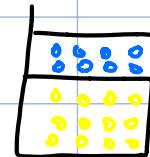
不同组分

↑ 极化强度 ↑ 磁化强度

达到平衡态和达到平衡前没有关系, 与达到平衡的过程无关.



均匀系统: eg 达到平衡后的气体或水+水蒸气 $\underbrace{2\text{液体相}}_{\text{单相系}}$



相: eg. 肉汤, 油里有水, 水里有油

非均匀系统: 复相系

非平衡态:

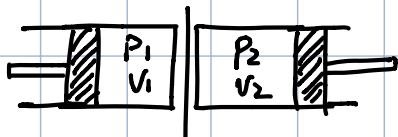
单位: $P: \text{N/m}^2 \quad P_0 = 101325 \text{Pa} \sim 10^5 \text{Pa} \quad \text{mbar} \quad \text{mmHg}$

$1\text{N} = 1\text{kg} \cdot \text{m/s}^2$ 标准大气压

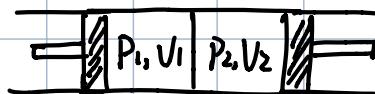
$U: \text{J} \quad 1\text{J} = 1\text{N} \cdot \text{m}$

热平衡定律和温度：

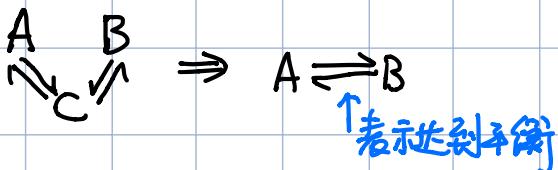
构造一个热平衡系统



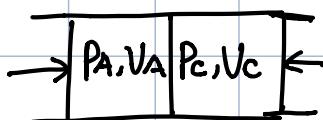
绝热系统



非绝热



热力学第一定律



$A \rightleftharpoons C$, 则存在与P, V有关的状态函数 $f_1(P_A, V_A) = f_2(P_C, V_C)$

$$f_{AC}(P_A, V_A, P_C, V_C) = 0 \Rightarrow P_C = F_{AC}(P_A, V_A, V_C) \quad \}$$

$$B \rightleftharpoons C \quad f_{BC}(P_B, V_B, P_C, V_C) = 0 \Rightarrow P_C = F_{BC}(P_B, V_B, V_C) \quad \}$$

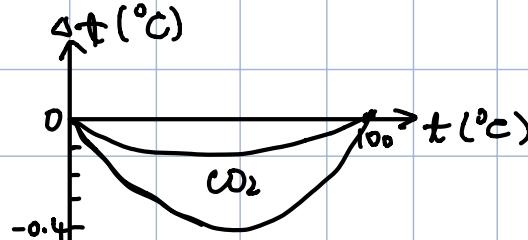
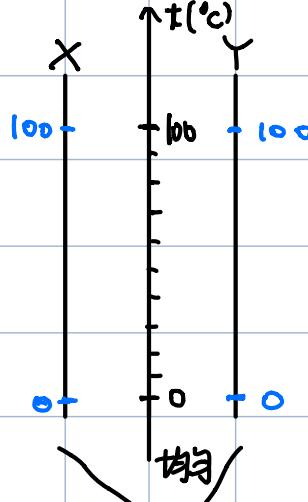
$$\Rightarrow F_{AC}(P_A, V_A, V_C) = F_{BC}(P_B, V_B, V_C) \quad \#$$

$$A \rightleftharpoons B \quad f_{AB}(P_A, V_A, P_B, V_B) = 0 \quad (\text{与 } C \text{ 无关})$$

说明图中不存在与C有关的量

$$\Rightarrow g_A(P_A, V_A) = g_B(P_B, V_B) \quad \text{定义为温度} \quad T_A = T_B.$$

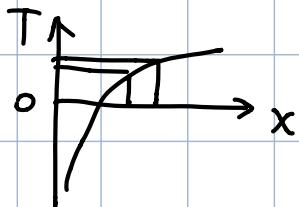
如何测量温度？定义温标 ①刻度 ②零标 ③测温物质



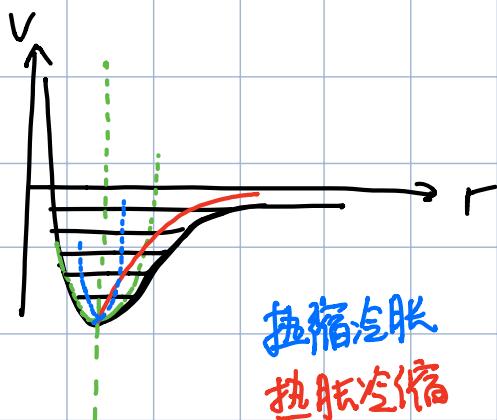
为什么都是往下？

不是线性

$T=k\ln x$ 适用于易高温. 温度变化小对应于分子量变化大.

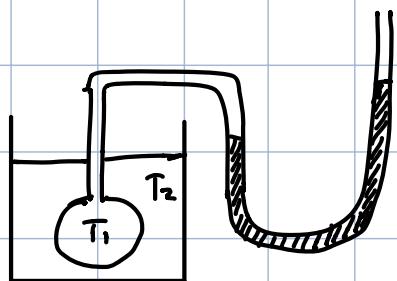


理想气体温标

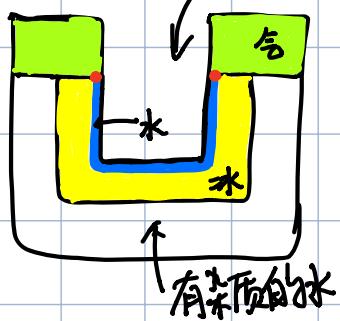


热缩汽胀
热胀冷缩

定容气体温度计 $T \propto P$



三相点 倒热水使冰熔化



$$0.01^\circ\text{C} = 273.16\text{K} P_{tr}$$

$$T_V = \lim_{P \rightarrow 0} \frac{P}{P_{tr}} \cdot 273.16\text{K}$$

热力学希望有一个温标不依赖于测温物质 — 热力学温标 (恰巧与理想气体温标数值相同)

用到了焦耳定律?

物态方程：理想气体： $PV=nRT$ $f(P, V, T)=0$
不能由热力学推导，有一部分可以从统计力学推导。

三个系数：体胀系数

$$V = V_0 + \alpha \Delta T$$

$$\Delta V = \alpha \Delta T \Rightarrow P, V, T \text{ 循环} \\ \left. \begin{aligned} & \left(\frac{\partial V}{\partial P} \right)_T \left(\frac{\partial P}{\partial T} \right)_V \left(\frac{\partial T}{\partial V} \right)_P = -1 \\ & (-V K_T)(P \beta) \left(\frac{1}{\partial V} \right) = -1 \end{aligned} \right\}$$

压力系数

$$\beta = \frac{1}{P} \left(\frac{\partial P}{\partial T} \right)_V$$

等温压缩系数

$$K_T = -\frac{1}{V} \left(\frac{\partial V}{\partial P} \right)_T$$

↑为了使结果是正的

$\alpha = K_T \beta P$
可以用系规则

Homework: 1.1, 1.2

$$PV/T = C \quad PV = \underline{\quad} T \quad \text{what's the coefficient?}$$

$$nR \quad R = 8.3145 \text{ J/T.mol}$$

理想气体：①质量，没有体积。

②没有相互作用。

范德瓦尔斯方程

$$(P + \frac{\alpha n^2}{V^2})(V - nb) = nRT$$

$$(P + \frac{\alpha}{V^2})(V - b) = RT \quad 1 \text{ mol 的情况} \quad \text{考虑与器壁的碰撞}$$

↑ 单位物质的量的体积

$$n=1 \text{ 时} \quad V=22.4 \text{ L} = 22.4 \times 10^{-3} \text{ m}^3/\text{mol} \quad P_n = 10^5 \text{ Pa}$$

$$\text{以大气压为单位} \quad (1 + 20 \times 10^3 \text{ Pa})(V - b) = 8.31 \times 300 \times 10^{-5}$$

$$\alpha \sim 10^{-5} \sim 10^{-6}$$

$$b \sim 10^{-5}$$

昂尼斯方程

$$P = \frac{nRT}{V-nb} - \frac{an^2}{V^2} \approx \frac{nRT}{V} \left(1 + \frac{nb}{V}\right) - \frac{nRT}{V} \left(\frac{an}{TV}\right)$$

$$= \frac{nRT}{V} \left(1 + \frac{nb}{V} - \frac{an}{TV}\right)$$

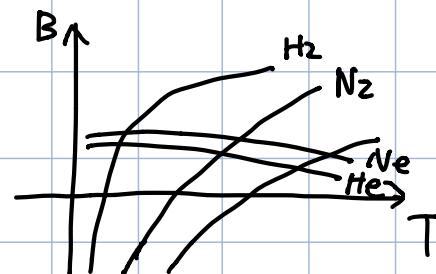
高密度

→ $P = \frac{nRT}{V} \left[1 + \frac{n}{V}B(T) + \left(\frac{n}{V}\right)^2 C(T) + \dots\right]$

零阶项：理想气体方程

- 阶项：范德瓦尔斯方程

维里系数



简单液体和固体的状态方程

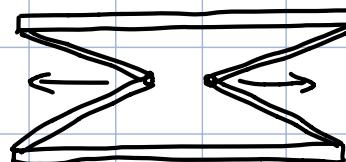
$$V = V(P, T)$$

$$V(T, P) = V_0(T_0, P) \left[1 + \alpha(T - T_0) - k_T P\right]$$

$$\sim 10^{-4}/K \quad \sim 10^{-10}/Pa$$

泊松比 $\frac{\Delta V}{V}$ → 壁面上允许材料拉长时变粗

拉伸材料（没做出来）



顺磁性固体

$$\text{磁化强度 } M = \frac{\sum m}{V}$$

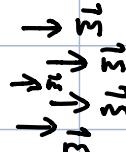
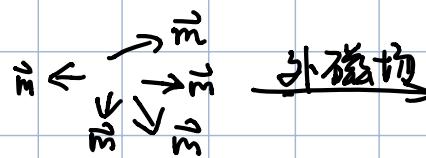
$$\vec{B} = \mu(\vec{H} + \vec{M})$$

$$(\vec{D} = \epsilon_0 \vec{E} + \vec{P})$$

Curie

$$\vec{M} = \chi \vec{H} \text{ 状态方程} = \frac{c}{T} \vec{H}$$

$$\vec{P} = \epsilon_0 \chi E \text{ 状态方程} \quad \text{居里定律}$$



$$\text{后来发现 } \vec{M} = \frac{C}{T-\theta} \vec{H}$$

$T > \theta$ 顺磁

$T < \theta$ 抗磁

所有物质都有抗磁性（楞次定律） 顺磁的磁矩可以转，超过了抗磁性

广延量 m, V, n

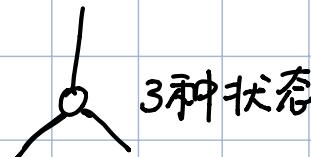
强度量 $T, P, \vec{H}, \vec{E}, \vec{P}$

极化强度

$$\frac{\text{广延量}}{\text{强度量}} = \text{强度量}$$

热力学极限 $N \rightarrow \infty, V \rightarrow \infty, \frac{N}{V} \text{ 有限}$

粒子足够多 体积足够大

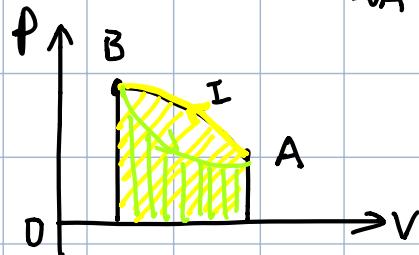


所以高分子一根链 ($N \sim 10^4$)

也可以做统计.

功 准静态过程 $dW = -pdV$

$$V_A \rightarrow V_B \quad W = - \int_{V_A}^{V_B} p dV \quad \text{对体系做功为正}$$



逆时针 外界对体系做正功

顺时针 外界对体系做负功

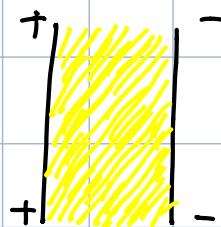
卡诺循环 外界对体系做负功

非准静态过程 ① 等容过程 $W=0$

~~只考虑2过程~~ ② 等压过程 $W = -P \Delta V$

1° 液体表面膜 表面张力系数 $dW = \sigma dA$ 拉肥皂膜时要算₂于表面

2° 电介质



$$dW = V dq$$

$$dW = V d(\frac{1}{2} \epsilon_0 E^2) + V \vec{E} \cdot d\vec{P} \quad (\vec{D} = \epsilon_0 \vec{E} + \vec{P})$$

$$= V \vec{E} \cdot d\vec{D}$$

$$\epsilon_0 = 8.85 \times 10^{-12} F \cdot m^{-1}$$

3° 磁介质 $\vec{B} = \mu_0 (\vec{H} + \vec{M})$

$$\mu_0 = 4\pi \times 10^{-7} H \cdot m^{-1}$$

↑ 定义的
↑ 常数

$$F = \frac{1}{4\pi\epsilon_0} \frac{q_1 q_2}{r^2}$$

测出来的

$$dW = V \vec{H} \cdot d\vec{B}$$

-一般形式下 $\partial W = Y_i dy_i$; $\partial W = -pdV$

↑
广义力
↑
广义坐标

热力学第一定律 做功 传热

能量守恒定律

Joule 1840s-1860s 做的实验
 → 绝热过程中 $U_B - U_A = W_s$

从A点出发, 不是所有的B点都能通过绝热过程达到.

如果不是绝热过程 $U_B - U_A - W_s = Q$

$$\Rightarrow U_B - U_A = W_s + Q$$

$$\Rightarrow dU = \partial W + \partial Q \quad (\text{Carathéodory, 1909})$$

热容 $C = \lim_{\Delta T \rightarrow 0} \frac{\Delta Q}{\Delta T}$ 广延量 J/K

$c = \frac{C}{m}$ $c_m = \frac{C}{n}$ $C = nc_m$

质量热容 摩尔热容

Homework 1.5 1.6

等容过程 $W=0 \Rightarrow \Delta U = \Delta Q + W = \Delta Q$

$$C_V = \lim_{\Delta T \rightarrow 0} \left(\frac{\Delta Q}{\Delta T} \right)_V = \left(\frac{\partial U}{\partial T} \right)_V$$

$$\Rightarrow U = U(T, V) \quad C_V(T, V)$$

等压过程 P 恒定 $\Rightarrow W = -P\Delta V \Rightarrow \Delta Q = \Delta U - W = \Delta U + P\Delta V$

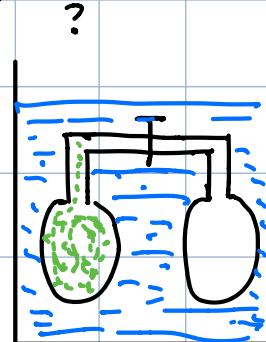
$$\begin{aligned} C_P &= \lim_{\Delta T \rightarrow 0} \frac{\Delta Q}{\Delta T} = \lim_{\Delta T \rightarrow 0} \frac{\Delta U + P\Delta V}{\Delta T} = \left(\frac{\partial U}{\partial T} \right)_P + P \left(\frac{\partial V}{\partial T} \right)_P \\ &= \left(\frac{\partial (U+PV)}{\partial T} \right)_P = \left(\frac{\partial H}{\partial T} \right)_P \quad C_P(T, P) \end{aligned}$$

焓的物理意义 $H = U + PV$ 等压下, 焓变 $\Delta H = \Delta U + P\Delta V = \Delta Q$

所以焓的物理意义就是等压下的吸放热

理想气体 $PV = nRT$ $U = U(T, V)$ U 是 V 的函数吗?

焦耳在1845研究了这个问题



$V \rightarrow 2V$.

U 变了吗？(水的温度是否升高)

($W=0, \Delta U=\Delta Q$)

结论：水的温度不变. $\Rightarrow U$ 不变 $\Rightarrow U = U(T)$

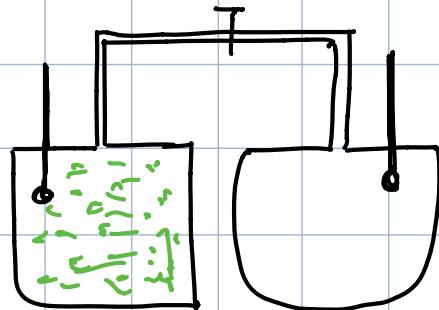
若 $U = U(T, V)$ 则可以构造函数 $f(U, T, V) = 0$

$$\left(\frac{\partial U}{\partial T}\right)_V \left(\frac{\partial T}{\partial V}\right)_U \left(\frac{\partial V}{\partial U}\right)_T = -1 \Rightarrow \left(\frac{\partial U}{\partial V}\right)_T = -\left(\frac{\partial U}{\partial T}\right)_V \left(\frac{\partial T}{\partial V}\right)_U \\ = -C_V \left(\frac{\partial T}{\partial V}\right)_U$$

——焦耳系数 测出来为0

$\Rightarrow U = U(T)$ 焦耳定律

盖·吕萨克 1807



节流实验 1852 焦耳和汤姆逊 (开尔文) $W \neq 0$ 等焓过程

$U = U(T, V)$

玻意耳定律 $PV = C(T)$

阿伏加德罗定律 $V \propto n$

焦耳定律 $U = U(T)$

\Rightarrow 理想气体

U 与 V 无关

$$C_V = \left(\frac{\partial U}{\partial T}\right)_V = \frac{dU}{dT} \Rightarrow dU = C_V dT \Rightarrow U = \int_{T_0}^T C_V dT' + U_0 = C_V \Delta T + U_0$$

理想气体

$$H = U + PV \quad C_P = \left(\frac{\partial H}{\partial T}\right)_P = \frac{dH}{dT} \Rightarrow H = \int_{T_0}^T C_P dT' + H_0 = C_P \Delta T + H_0$$

理想气体

$$C_p - C_v = R \quad C_p - C_v = nR \quad \frac{dH}{dT} - \frac{dU}{dT} = nR$$

$$\frac{C_p}{C_v} = \gamma \quad \text{可以解出 } C_v = \frac{nR}{\gamma-1} \quad C_p = \gamma \frac{nR}{\gamma-1}$$

γ是温度的函数吗？

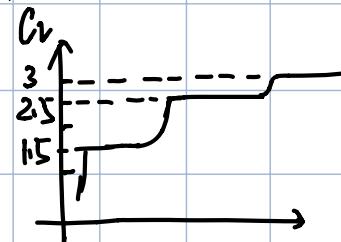
$$U = U(T), H = H(T) \Rightarrow C_p = C_p(T), C_v = C_v(T) \Rightarrow \gamma = \gamma(T)$$

但是理想气体 γ 是常数

$$U = \frac{3}{2}nRT = \frac{3}{2}Nk_B T \quad C_v = \frac{3}{2}R \quad (\text{单原子})$$

$$C_v = \frac{5}{2}R$$

(双原子, 中等温度) (双原子高温)



理想气体分子有内部自由度。

理想气体绝热过程

$$dU = dQ + dW = dW = -pdV$$

$$C_v dT + pdV = 0 \quad \xrightarrow{PV=nRT} pdV + Vdp = nRdT \quad \left. \begin{array}{l} \\ C_v dT + pdV = 0 \end{array} \right\} \Rightarrow pdV + Vdp = -\frac{nR}{C_v} pdV$$

$$\Rightarrow pdV \left(1 + \frac{nR}{C_v}\right) + Vdp = 0$$

$$\Rightarrow \gamma pdV + Vdp = 0$$

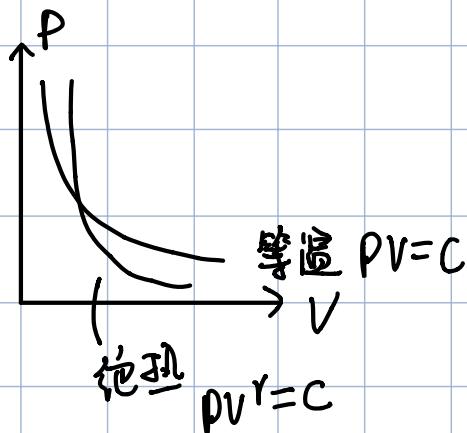
$$\Rightarrow \frac{dp}{p} = -\frac{dv}{v} \cdot \gamma$$

$$\Rightarrow \ln p = -\ln v \cdot \gamma + C$$

$$\Rightarrow p v^\gamma = C$$

$$\xrightarrow{PV=nRT} V^{\gamma-1} T = C$$

$$P^{\gamma-1} T^{-\gamma} = C$$



推导声速用绝热过程

$$\text{牛顿用等温过程} \quad V = \left(\frac{dp}{d\rho}\right)^{\frac{1}{\gamma}} = \sqrt{\rho / \rho}$$

Laplace (绝热) 1KHz, 热量来不及传递

$$V_S = \sqrt{\left(\frac{\partial P}{\partial V}\right)_S} = \sqrt{\left(\frac{\partial P}{\partial V}\right)_S} = \sqrt{\left(\frac{\partial P}{\partial V}\right)_S \left(\frac{\partial V}{\partial P}\right)_S}$$

$$= \sqrt{\left(-\frac{P\gamma}{V}\right)(-V^2)} = \sqrt{PV} = \sqrt{\gamma P/V}$$

$$\rho = \frac{m}{V} = \frac{1}{V}$$

$$PV^\gamma = C$$

$$(V_S)_{\text{Laplace}} = \sqrt{\gamma} (V_S)_{\text{Newton}}$$

$$\approx 1.2 (V_S)_{\text{Newton}}$$

$$0^\circ\text{C}, 1 \text{ atm}, V_S = 33 \text{ m/s}, M_m = 29 \text{ g/mol} \Rightarrow \gamma = 1.4$$

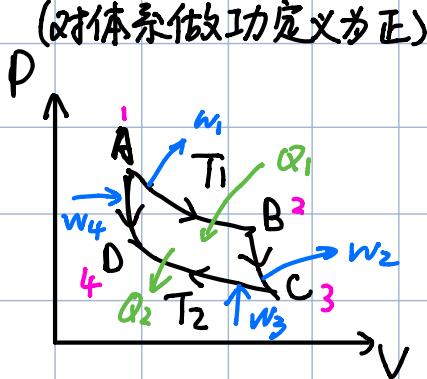
卡诺循环 (Carnot) 1mol

$$PV = RT$$

$$A \rightarrow B \rightarrow C \rightarrow D \rightarrow A$$

$$V_A \quad V_B \quad V_C \quad V_D \quad V_A$$

$$A \rightarrow B \quad \delta W = -pdV$$



$$W_1 = - \int_{V_A}^{V_B} \frac{RT_1}{V} dV = -RT_1 \ln \frac{V_B}{V_A}$$

$$dU = \delta W + \delta Q \quad Q_1 = -W_1 = +RT_1 \ln \frac{V_B}{V_A}$$

$$B \rightarrow C \quad \delta W = -pdV \quad Q = 0$$

$$W = - \int_{V_B}^{V_C} \frac{C}{V^\gamma} dV = \frac{C}{\gamma-1} \left(\frac{1}{V_C^{\gamma-1}} - \frac{1}{V_B^{\gamma-1}} \right) = \frac{1}{\gamma-1} (P_C V_C - P_B V_B)$$

$$= \frac{R}{\gamma-1} (T_C - T_B) = C_V (T_C - T_B) = U_C - U_B.$$

Homework. 1.10, 1.11

$$C \rightarrow D \quad W_3 = RT_2 \ln \frac{V_3}{V_4}$$

$$Q_2 = W_3 = RT_2 \ln \frac{V_3}{V_4}$$

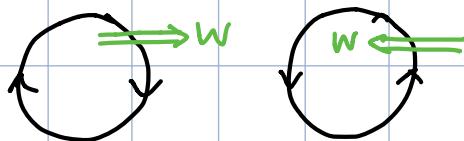
$$D \rightarrow A \quad Q = 0$$

$$\Delta U = W + Q \Rightarrow W = Q_1 - Q_2 = RT_1 \ln \frac{V_2}{V_1} - RT_2 \ln \frac{V_3}{V_4}$$

$$\begin{aligned} B \rightarrow C & \quad V_2^{y-1} T_1 = V_3^{y-1} T_2 \\ D \rightarrow A & \quad V_1^{y-1} T_1 = V_4^{y-1} T_2 \end{aligned} \left\{ \Rightarrow \frac{V_2}{V_1} = \frac{V_3}{V_4} \right.$$

$$\Rightarrow W = R(T_1 - T_2) \ln \frac{V_2}{V_1}$$

$$\text{效率 } \eta = \frac{W}{Q_1} = \frac{R(T_1 - T_2) \ln V_2/V_1}{R T_1 \ln V_2/V_1} = 1 - \frac{T_2}{T_1} \quad \text{与具体过程无关, 只限两个热源的温度有关.}$$



斯特令循环 $\eta' = \frac{Q_2}{W} = \frac{T_2}{T_1 - T_2}$ 可以大于 1

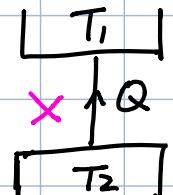
热力学第二定律

1842 卡诺

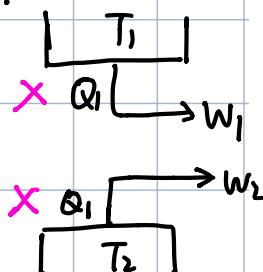
1850 克劳修斯 Clausius

1851 开尔文 Kelvin

Clausius: 不可能把热量从低温物体传递到高温物体而不引起其它变化.

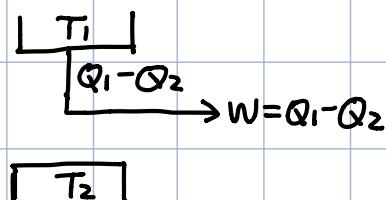
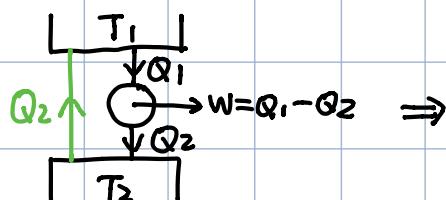


Kelvin: 不可能从单一热源吸收热量, 使之完全变成有用功而不引起其它变化.



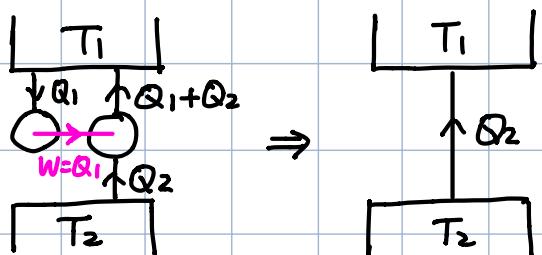
两种说法的等价性

① 如果 Clausius 说法不成立



则开氏说法不成立

②如果 Kelvin 说法不成立



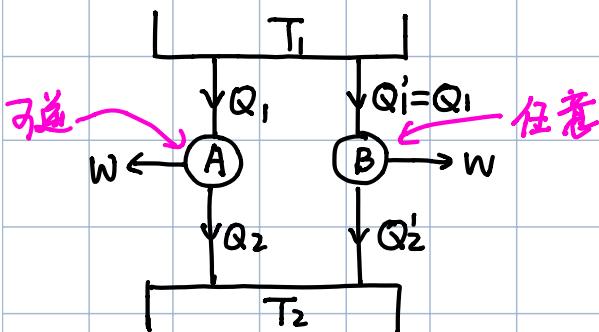
则克氏说法不成立

可逆过程：没有摩擦力的准静态过程。

自然界真实存在的过程都是不可逆过程。 破镜难圆、覆水难收

态函数：熵

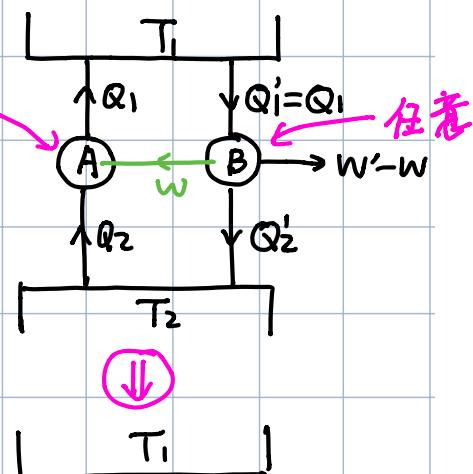
卡诺定理(律)：所有工作于两个热源之间的热机，可逆机的效率最高。



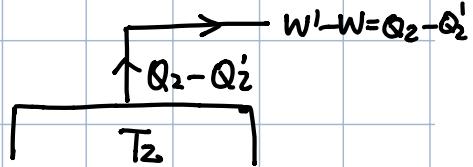
欲证 $\eta_A \geq \eta_B$

若 $\eta_A < \eta_B$

$$\left. \begin{array}{l} \eta_A = \frac{W}{Q_1} \\ \eta_B = \frac{W'}{Q'_1} \end{array} \right\} \Rightarrow W < W'$$



Kelvin表述不成立 \Leftarrow



推论：所有工作在两个温度间的可逆机的效率都相等。

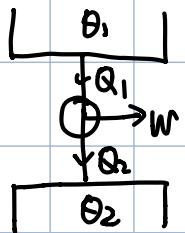
$$\left. \begin{array}{l} A \text{可逆: } \eta_A \leq \eta_B \\ B \text{可逆: } \eta_B \leq \eta_A \end{array} \right\} \Rightarrow \eta_A = \eta_B$$

热力学温标 (θ)

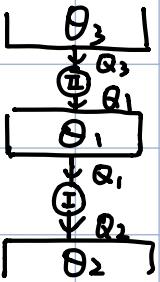
$$\text{卡诺循环 } \eta = \frac{W}{Q} = \frac{Q_1 - Q_2}{Q_1} = 1 - \frac{Q_2}{Q_1} = 1 - \frac{T_2}{T_1}$$

开尔文温标

Q₁ 不依赖于工质物质

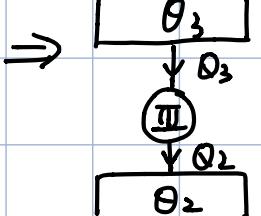


$$\frac{Q_1}{Q_2} = F(\theta_1, \theta_2)$$



$$\frac{Q_3}{Q_1} = F(\theta_3, \theta_1)$$

$$\frac{Q_1}{Q_2} = F(\theta_1, \theta_2)$$



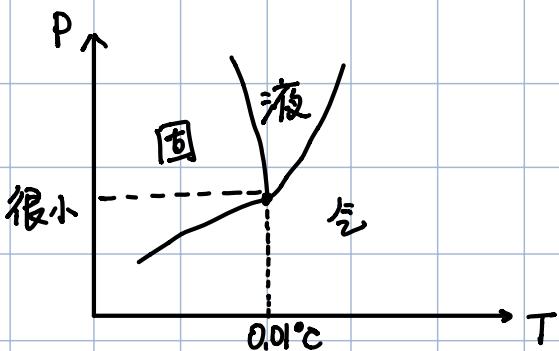
$$\frac{Q_3}{Q_2} = F(\theta_3, \theta_2)$$

$$\Rightarrow \frac{Q_3}{Q_2} = F(\theta_3, \theta_1) \quad F(\theta_1, \theta_2) = F(\theta_3, \theta_2)$$

$$\Rightarrow F(\theta_1, \theta_2) = \frac{F(\theta_3, \theta_2)}{F(\theta_3, \theta_1)} = \frac{f(\theta_2)}{f(\theta_1)} = \frac{T_2^*}{T_1^*}$$

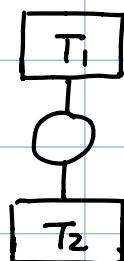
1954 水三相点 $T_{tr} = 273.16\text{K}$ $\rightarrow P_{tr} = 611\text{Pa} = 0.006\text{atm}$

冰点 $T_0 = 273.15\text{K}$ $\rightarrow 1\text{atm} = 10^5\text{Pa}$



Homework.

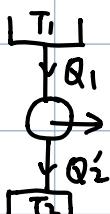
1.16. 1.13



$$T = \sqrt{T_1 T_2}$$

Clausius 等式与不等式

$$\eta = 1 - \frac{Q_2}{Q_1} \leq 1 - \frac{T_2}{T_1}$$



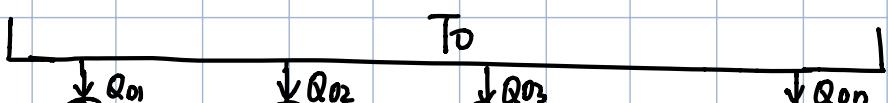
(对外放热为正)

证明思路

直接不等式 \Leftrightarrow 热力学第二定律 \Leftrightarrow 卡诺定理

$$\boxed{\frac{Q_2}{Q_1} \geq \frac{T_2}{T_1}}$$

$$\text{假设 } \frac{Q_1}{T_1} + \frac{Q_2}{T_2} + \dots + \frac{Q_n}{T_n} \leq 0$$

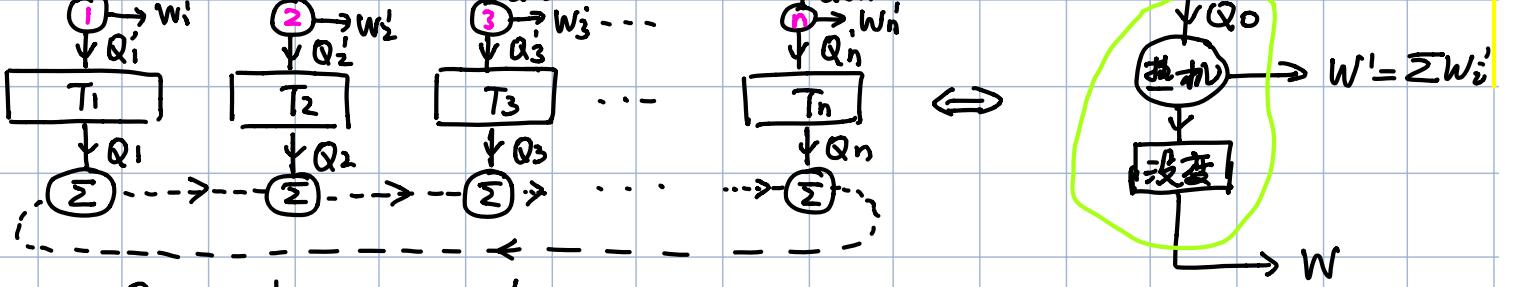


$$\Delta S = \frac{Q}{T}$$

熵增加

$$\sum \frac{Q_i}{T_i} \leq 0$$





$$\frac{Q_{0i}}{T_0} = \frac{Q_i}{T_i} \Rightarrow Q_{0i} = \frac{Q_i}{T_i} T_0$$

$$Q_0 = \sum Q_{0i} = \sum \frac{Q_i}{T_i} T_0 = T_0 \sum \frac{Q_i}{T_i} = T_0 \sum \frac{Q_i}{T_i}$$

热力学第二定律
对物体做的功不
可是正的

如果有两个热源

$$\frac{Q_1}{T_1} + -\frac{Q_2}{T_2} = \frac{Q_1}{T_1} - \frac{Q_2}{T_2}$$

$$Q_2' \downarrow -Q_2'$$



$$l = \frac{W'}{Q_1} = \frac{Q_1 - Q_2}{Q_1} = 1 - \frac{Q_2}{Q_1} \leq 1 - \frac{T_2}{T_1}$$

$$\rightarrow \frac{Q_2}{Q_1} \geq \frac{T_2}{T_1} \Rightarrow \frac{Q_2}{T_2} \geq \frac{Q_1}{T_1} \Rightarrow \frac{Q_1}{T_1} - \frac{Q_2}{T_2} \leq 0.$$

对于可逆热机 \rightarrow 反转 $\rightarrow [Q_i \rightarrow -Q_i]$

$$\sum -\frac{Q_i}{T_i} \leq 0 \Rightarrow \sum \frac{Q_i}{T_i} \geq 0 \Rightarrow \sum \frac{Q_i}{T_i} = 0$$

卡诺定理 \Leftrightarrow $\left. \begin{array}{l} \text{开氏表述} \\ \text{克氏表述} \end{array} \right\} \Leftrightarrow$ 贝劳修斯不等式

$$\oint \frac{dQ}{T} \leq 0$$

熵 entropy
 $\frac{dQ}{T}$ energy transfer

态函数



$$\int_A^B \frac{dQ_R}{T} + \int_B^A \frac{dQ_R}{T} = 0$$

$$\rightarrow T_B dQ - T_A dQ = 0$$

$$R' \rightarrow JA \frac{\partial Q}{T} - JA \frac{\partial Q}{T} = 0$$

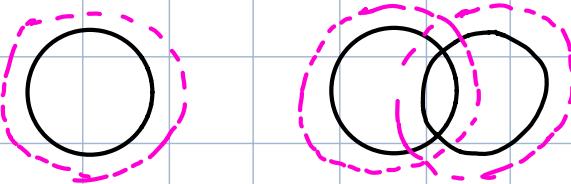
\Rightarrow 态函数

$$S_B - S_A = \int_A^B \frac{\partial Q}{T}$$

$$dS = \frac{\partial Q}{T} = \frac{dU - dW}{T} = \frac{dU + PdV}{T} \Rightarrow dU = TdS - PdV$$

广延量 $\propto V$ (正比的前提是相互作用可以忽略不计)

depletion



理想气体的熵

$$dU = C_V dT \quad PV = nRT$$

$$dS = \frac{dU + PdV}{T} = \frac{C_V dT + nRT \frac{dV}{V}}{T} = C_V \frac{dT}{T} + nR \frac{dV}{V}$$

$$\Rightarrow S - S_0 = C_V \ln T + nR \ln V = S(T, V)$$

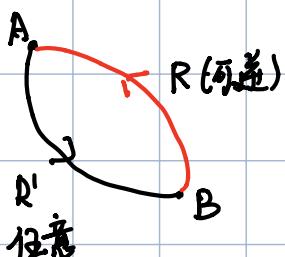
$$dS = \frac{dU + PdV}{T} = \frac{dU + nRdT - VdP}{T} = (C_V + nR) \frac{dT}{T} - \frac{nR}{P} dP$$

$$\Rightarrow S - S_0 = C_p \ln T - nR \ln P$$

等温过程 $V_A \Rightarrow V_B$ $\Delta S = nR \ln \frac{V_B}{V_A}$

$V_B > V_A \Rightarrow \Delta S > 0$, 吸热, 体积功

$V_B < V_A \Rightarrow \Delta S < 0$, 放热, 外界对体系做功



$$\int_A^B \frac{\partial Q_{R'}}{T} + \int_B^{A'} \frac{\partial Q_R}{T} \leq 0$$

$$\int_A^B \frac{\partial Q_R'}{T} - \int_A^B \frac{\partial Q_R}{T} \leq 0$$

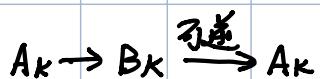
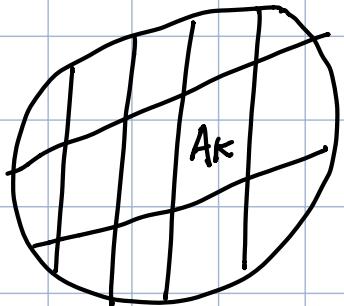
$$\int_A^B \frac{\partial Q_R'}{T} \leq \int_A^B \frac{\partial Q_R}{T}$$

$$\int_A^B \frac{\partial Q_{R'}}{T} \leq \int dS = \Delta S.$$

$$dS \geq \frac{\partial Q}{T} \quad \text{绝热系统 } \partial Q=0, dS \geq 0 \text{ 熵增加原理}$$

$$dU = \partial Q + \partial W \leq TdS + \partial W$$

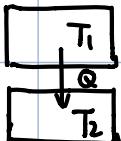
Examples.



$$\left. \begin{aligned} \int_A^B \frac{dQ}{T} + \sum_{k=1}^N \int_{B_k}^{A_k} \frac{dQ}{T} &< 0 \\ \int_{B_k}^{A_k} \frac{dQ}{T} &= S_{A_k} - S_{B_k} \end{aligned} \right\} \Rightarrow \sum_{k=1}^N (S_{B_k} - S_{A_k}) > \int_A^B \frac{dQ}{T}$$

$$\Rightarrow S_B - S_A > \int_A^B \frac{dQ}{T}$$

$$S_B > S_A$$



$$\Delta S = \Delta S_1 + \Delta S_2 = -\frac{Q}{T_1} + \frac{Q}{T_2} = Q\left(\frac{1}{T_2} - \frac{1}{T_1}\right) > 0$$

两杯水混合 (假定质量相等)

$$T = \frac{T_1 + T_2}{2} \quad (T_1, p), (T_2, p) \longrightarrow (T, p)$$

$$dS = \frac{dU - dW}{T} = \frac{dU + pdV}{T} = \frac{dH}{T} = \frac{C_p dT}{T}$$

$$\Delta S_1 = \int_{T_1}^T \frac{C_p dT}{T} = C_p \ln \frac{T}{T_1} = C_p \ln \frac{T_1 + T_2}{2T_1}$$

$$\Delta S_2 = \int_{T_2}^T \frac{C_p dT}{T} = C_p \ln \frac{T}{T_2} = C_p \ln \frac{T_1 + T_2}{2T_2}$$

$$\Delta S = \Delta S_1 + \Delta S_2 = C_p \ln \frac{(T_1 + T_2)^2}{4T_1 T_2} = C_p \ln \frac{4T_1 T_2 + (T_1 - T_2)^2}{4T_1 T_2} > 0$$

理想气体自由膨胀 (等温)

$$(T, V_A) \longrightarrow (T, V_B)$$

$$\left. \begin{aligned} S_A &= C_v \ln T + nR \ln V_A + S_0 \\ S_B &= C_v \ln T + nR \ln V_B + S_0 \end{aligned} \right\} \Rightarrow \Delta S = nR \ln \frac{V_B}{V_A} > 0$$

自由能 F (亥姆霍兹自由能)

吉布斯函数 G (吉布斯自由能, 自由焓)

考虑了等温过程 $(A, T) \rightarrow (B, T)$ $dQ \leq T dS$ $Q \leq T(S_B - S_A)$

$$\Rightarrow U_B - \underbrace{U_A - W}_{\text{体系对外做功}} \leq T S_B - T S_A$$

体系对外做功

$$\Rightarrow -W \leq (U_A - T S_A) - (U_B - T S_B)$$

也就是说体系对外做的最大的功

$$(-W)_{\max} = F_A - F_B$$

自由能，可以用来做功
束缚能，不能用来做功 ↗

$$F = U - TS \Rightarrow U = F + TS$$

$$U_A - U_B = (-W)_{\max} + Q$$

(等温且) 没有体积变化的话 $W=0$, $F_A \geq F_B$

自由能只减小

等温等压下 $dP=0$ $V_A \rightarrow V_B$ $W = -P(V_B - V_A)$

$$F_A - F_B \geq (-W)_{\max} = +PV_B - PV_A$$

$$(F_A + PV_A) - (F_B + PV_B) \geq 0$$

$$G_A - G_B \geq 0 \quad \text{吉布斯自由能只减小} \quad G = F + PV = U - TS + PV = H - TS$$

$$H = G + TS$$

↑
自由焓

均匀物质的热力学

内能、焓、自由能、吉布斯函数

$$\left. \begin{array}{l} U \\ F = U - TS \\ G = U - TS + PV = H - TS = F + PV \\ H = U + PV \end{array} \right\}$$

三个基本热力学函数 $U, S, (P, V, T) = 0$

$$1^{\circ} dU = T dS - P dV = \left(\frac{\partial U}{\partial S}\right)_V dS + \left(\frac{\partial U}{\partial V}\right)_S dV$$

$$U = U(S, V) \quad \left(\frac{\partial U}{\partial S}\right)_V = T \quad \left(\frac{\partial U}{\partial V}\right)_S = -P \quad \left(\frac{\partial T}{\partial V}\right)_S = -\left(\frac{\partial P}{\partial S}\right)_V$$

$$2^{\circ} dH = dU + P dV + V dP = T dS + V dP$$

$$H = H(S, P) \quad \left(\frac{\partial H}{\partial S}\right)_P = T \quad \left(\frac{\partial H}{\partial P}\right)_S = V \quad \left(\frac{\partial T}{\partial P}\right)_S = \left(\frac{\partial V}{\partial S}\right)_P$$

$$3^{\circ} dF = dU - T dS - S dT = -P dV - S dT$$

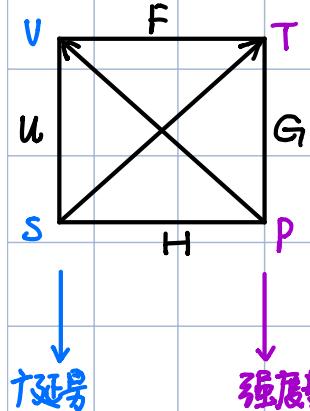
$$F = F(V, T) \quad (\frac{\partial F}{\partial V})_T = -P \quad (\frac{\partial F}{\partial T})_V = -S \quad (\frac{\partial P}{\partial T})_V = (\frac{\partial S}{\partial V})_T$$

$$4^{\circ} dG = dH - TdS - SdT = Vdp - SdT$$

$$G = G(P, T) \quad (\frac{\partial G}{\partial P})_T = V \quad (\frac{\partial G}{\partial T})_P = -S \quad (\frac{\partial V}{\partial T})_P = -(\frac{\partial S}{\partial P})_T$$

密闭 (T, V, P, S)

特属性数 (U, F, G, H)



$$\begin{aligned} dU &= \cancel{TdS} - \cancel{pdV} = \cancel{\delta Q} + dW \quad TdS = \cancel{\delta Q} \quad (\frac{\partial S}{\partial V})_T = (\frac{\partial P}{\partial T})_V \\ dF &= \cancel{-SdT} - \cancel{pdV} = \cancel{dW} \quad -pdV = \cancel{dW} \quad -(\frac{\partial V}{\partial T})_P = (\frac{\partial S}{\partial P})_T \\ dG &= \cancel{-SdT} + \cancel{Vdp} = ? \quad -SdT = ? \quad -(\frac{\partial T}{\partial P})_S = -(\frac{\partial V}{\partial S})_P \\ dH &= \cancel{TdS} + \cancel{Vdp} = \cancel{\delta Q} \quad Vdp = ? \quad (\frac{\partial P}{\partial S})_V = -(\frac{\partial T}{\partial V})_S \end{aligned}$$

Homework: 1.23 2.3 2.5

$$U = U(S, V) \text{, 不直观} \quad U = U(T, V) \quad dU = (\frac{\partial U}{\partial T})_V dT + (\frac{\partial U}{\partial V})_T dV \\ = C_V dT + (\frac{\partial U}{\partial V})_T dV$$

$$dU = TdS - pdV$$

$$dS = (\frac{\partial S}{\partial T})_V dT + (\frac{\partial S}{\partial V})_T dV$$

$$\Rightarrow dU = T(\frac{\partial S}{\partial T})_V dT + T(\frac{\partial S}{\partial V})_T dV - pdV$$

$$= [T(\frac{\partial S}{\partial T})_V] dT + [T(\frac{\partial S}{\partial V})_T - P] dV$$

$$\Rightarrow (\frac{\partial U}{\partial T})_V = T(\frac{\partial S}{\partial T})_V = C_V$$

$$(\frac{\partial U}{\partial V})_T = T(\frac{\partial S}{\partial V})_T - P = T(\frac{\partial P}{\partial T})_V - P$$

$$(\frac{\partial H}{\partial P})_T = -T(\frac{\partial V}{\partial T})_P + V$$

$$C_P - C_V = T(\frac{\partial S}{\partial T})_P - T(\frac{\partial S}{\partial T})_V$$

$$S(T, P) = S[T, V(T, P)] \Rightarrow (\frac{\partial S}{\partial T})_P = (\frac{\partial S}{\partial T})_V + (\frac{\partial S}{\partial V})_T (\frac{\partial V}{\partial T})_P \\ = (\frac{\partial S}{\partial T})_V + (\frac{\partial P}{\partial T})_V (\frac{\partial V}{\partial T})_P$$

$$\Rightarrow C_P - C_V = T(\frac{\partial P}{\partial T})_V (\frac{\partial V}{\partial T})_P \quad \underline{\text{理想气体}} \quad nR \quad V$$

$$= T \beta P \cdot \alpha V = \frac{V\alpha^2}{k_T} \geq 0 \quad \alpha = 0 \Leftrightarrow$$



Hg 0°C $C_p = 28.0 \text{ J/(K/mol)}$ $V = 1.4 \times 10^{-5} \text{ m}^3/\text{mol}$

$$\alpha = 181 \times 10^{-6} \text{ K}^{-1} \quad k_T = 3.94 \times 10^{-6} \text{ atm}^{-1} = 3.89 \times 10^{-6} \text{ Pa}^{-1}$$

$$\Rightarrow C_p - C_V = 3.4 \text{ J/(mol K)}$$

Jacobi

$$(x, y) \rightarrow (u, v) \quad u = u(x, y), \quad v = v(x, y)$$

$$\frac{\partial(u, v)}{\partial(x, y)} = \begin{vmatrix} \frac{\partial u}{\partial x} & \frac{\partial u}{\partial y} \\ \frac{\partial v}{\partial x} & \frac{\partial v}{\partial y} \end{vmatrix} = \frac{\partial u}{\partial x} \frac{\partial v}{\partial y} - \frac{\partial u}{\partial y} \frac{\partial v}{\partial x}$$

性质 1. $\left(\frac{\partial u}{\partial x}\right)_y = \frac{\partial(u, y)}{\partial(x, y)}$

2. $\frac{\partial(u, v)}{\partial(x, y)} = -\frac{\partial(v, u)}{\partial(x, y)}$

3. $\frac{\partial(u, v)}{\partial(x, y)} = \frac{\partial(u, v)}{\partial(r, s)} \cdot \frac{\partial(r, s)}{\partial(x, y)}$

4. $\frac{\partial(u, v)}{\partial(x, y)} \cdot \frac{\partial(x, y)}{\partial(u, v)} = 1$

$$\begin{vmatrix} \frac{\partial u}{\partial x} & \frac{\partial u}{\partial y} \\ \frac{\partial v}{\partial x} & \frac{\partial v}{\partial y} \end{vmatrix} = \left(\frac{\partial u}{\partial x}\right)_y.$$