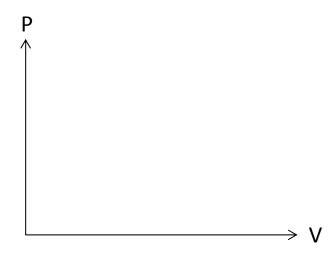
Name: SID: Discussion Section:

## Chemical Engineering Thermodynamics 141 – Spring 2011 Tuesday, February 22, 2011 Midterm I – 70 minutes – 100 total points One one-sided 8.5"x 11" equation sheet allowed

(20 points) 1. Consider an ideal gas.

i) (2 points) On the P-V diagram shown below, draw an isothermal curve at T<sub>1</sub>.

ii) (3 points) Show graphically the reversible work for compression from  $2V_1$  to  $V_1$  at constant temperature  $T_1$ .



iii) (6 points) Show mathematically that the reversible work done on the system at  $T_1$  is greater than at  $T_2$  where  $T_1 > T_2$ . Begin from the definition of work.

iv) (3 points)	Which one of the following expressions does not remain constant in the
	reversible and adiabatic expansion of an ideal gas?

a) TV<sup>R/Cv</sup>

b)  $TV^{\gamma-1}$  c)  $TV^{\gamma}$ 

d)  $PV^{\gamma}$ 

v) (6 points) Prove that all the other expressions remain constant. Begin from the 1<sup>st</sup> Law.

- (20 points)

  2. Consider you are working as an engineer in an oil refinery. A new dock is added to the refinery port. The dock will service tanker ships which have capacities of 4.5 x 10<sup>7</sup> kg. The refinery tank farm is situated at a distance of 2 km from the dock at an elevation of 50 m. Your task is to size the pump located on the dock. The station must be able to empty the tanker ships in one 8-hour shift. The density of oil is 900 kg/m<sup>3</sup>.
  - ii) (5 points) If there is no pressure drop due to friction, what is the absolute discharge pressure of the pump?

iii) (15 points) What is the power output of the pump (in kW)?

(40 points)	3.	A 2 kg copper block is taken out of a furnace at 250°C and quenched in a 10 L oil bath at an initi temperature of 40°C. The specific heat ( $C_P = C_V$ ) for oil and copper are 1.7 kJ kg <sup>-1</sup> K <sup>-1</sup> and 0.39 kg <sup>-1</sup> K <sup>-1</sup> respectively. The density of oil is 0.9 g/cm <sup>3</sup> .	
		i) (5 points)	What is the final temperature of the system?

ii) (5 points) How much heat does the copper transfer to the bath?

iv) (15 points) How long does it take to cool the oil bath back to  $40^{\circ}\text{C}$  if the ambient temperature,  $T_o$ , is equal to  $20^{\circ}\text{C}$ ? The oil loses heat at a rate of:

$$\dot{Q} = U \cdot A(T - T_o) = B(T - T_o)$$

where B =  $5 \text{ J K}^{-1} \text{ s}^{-1}$ .

(20 points) 4. The thermal expansion coefficient,  $\alpha$ , and the isothermal compressibility,  $\kappa$ , of a gas are given by the following expressions:

$$\alpha = \frac{1}{V} \left( \frac{\partial V}{\partial T} \right)_{P} = k_{1} \frac{C_{P}}{C_{V}} T^{(C_{P} - C_{V})/C_{V}}$$

$$\kappa = \frac{-1}{V} \left( \frac{\partial V}{\partial P} \right)_{T} = \frac{k_{2}}{P}$$

where  $k_1$  and  $k_2$  are constants.  $C_P$  and  $C_V$  may assumed to be independent of temperature.

i) (14 points) Derive a volume explicit equation of state, i.e. V = f(T,P).

ii) (6 points) Does this fluid have a critical point? Why?

Table A.1: Conversion Factors

Quantity	Conversion
Length	1 m = 100 cm = 3,28084(ft) = 39,3701(in)
Mass	$1 \text{ kg} = 10^3 \text{ g}$ = 2.20462(lb <sub>m</sub> )
Force	$1 \text{ N} = 1 \text{ kg m s}^{-2}$ = $10^5 (\text{dyne})$ = $0.224809 (\text{lb}_f)$
Pressure	1 bar = $10^5$ kg; m <sup>-1</sup> s <sup>-2</sup> = $10^5$ N m <sup>-2</sup> = $10^5$ Pa = $10^2$ kPa = $10^6$ (dyne) cm <sup>-2</sup> = $0.986923$ (atm) = $14.5038$ (psia) = $750.061$ (torr)
Volume	$1 \text{ m}^3 = 10^6 \text{ cm}^3$ = 35.3147(ft) <sup>3</sup> = 264.172(gal)
Density	1 g cm <sup>-3</sup> = $10^3$ kg m <sup>-3</sup> = $62.4278(lb_m)(ft)^{-3}$
Energy	$\begin{split} 1J &= 1kgm^2s^{-2} = 1Nm \\ &= 1m^3Pa = 10^{-5}m^3bar = 10cm^3bar \\ &= 9.86923cm^3(atm) \\ &= 10^7(dyne)cm = 10^7(erg) \\ &= 0.239006(cal) \\ &= 5.12197\times 10^{-3}(ft)^3(psia) = 0.737562(ft)(lb_f) \\ &= 9.47831\times 10^{-4}(Btu) \end{split}$
Power	$\begin{array}{l} 1 \text{ kW} = 10^3 \text{ W} = 10^3 \text{ kg m}^2 \text{ s}^{-3} = 10^3 \text{ J s}^{-1} \\ = 239.006(\text{cal}) \text{ s}^{-1} \\ = 737.562(\text{ft})(\text{lb}_f) \text{ s}^{-1} \\ = 0.947831(\text{Btu}) \text{ s}^{-1} \\ = 1.34102(\text{hp}) \end{array}$

Table A.2: Values of the Universal Gas Constant

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\begin{split} R &= 8.314 \text{ J mol}^{-1} \text{ K}^{-1} = 8.314 \text{ m}^3 \text{ Pa mol}^{-1} \text{ K}^{-1} \\ &= 83.14 \text{ cm}^3 \text{ bar mol}^{-1} \text{ K}^{-1} = 8,314 \text{ cm}^3 \text{ kPa mol}^{-1} \text{ K}^{-1} \\ &= 82.06 \text{ cm}^3 (\text{atm}) \text{ mol}^{-1} \text{ K}^{-1} = 62,356 \text{ cm}^3 (\text{torr}) \text{ mol}^{-1} \text{ K}^{-1} \\ &= 1.987 (\text{cal}) \text{ mol}^{-1} \text{ K}^{-1} = 1.986 (\text{Btu}) (\text{lb mole})^{-1} (\text{R})^{-1} \\ &= 0.7302 (\text{ft})^3 (\text{atm}) (\text{lb mol})^{-1} (\text{R})^{-1} = 10.73 (\text{ft})^3 (\text{psia}) (\text{lb mol})^{-1} (\text{R})^{-1} \\ &= 1.545 (\text{ft}) (\text{lb}_{\text{f}}) (\text{lb mol})^{-1} (\text{R})^{-1} \end{split}
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