

The background of the slide features a collection of laboratory glassware, including Erlenmeyer flasks and graduated cylinders, some containing liquids. The glassware is slightly out of focus, creating a professional scientific atmosphere. One flask in the center has a label that reads "1000 CM IN 20°C". Another flask to the left has a label with "10/13 EXELO", "Permagol", "IN 25 cm", and "20°C B". A graduated cylinder on the right has a scale from 1 to 10.

# Optimization of Ethylbenzene Production Process

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A Comprehensive Study on Feed Preparation, Reaction Kinetics, Energy Consumption, Separation, and Process Performance



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# INTRODUCTION TO ETHYLBENZENE PRODUCTION





# OBJECTIVES OF THE STUDY

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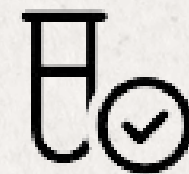
## MAXIMIZE ETHYLBENZENE YIELD

FOCUS ON INCREASING THE PRODUCTION OF ETHYLBENZENE IN THE PROCESS.



## MINIMIZE BYPRODUCTS

REDUCE THE FORMATION AND ACCUMULATION OF BYPRODUCTS LIKE DI-ETHYLBENZENE.



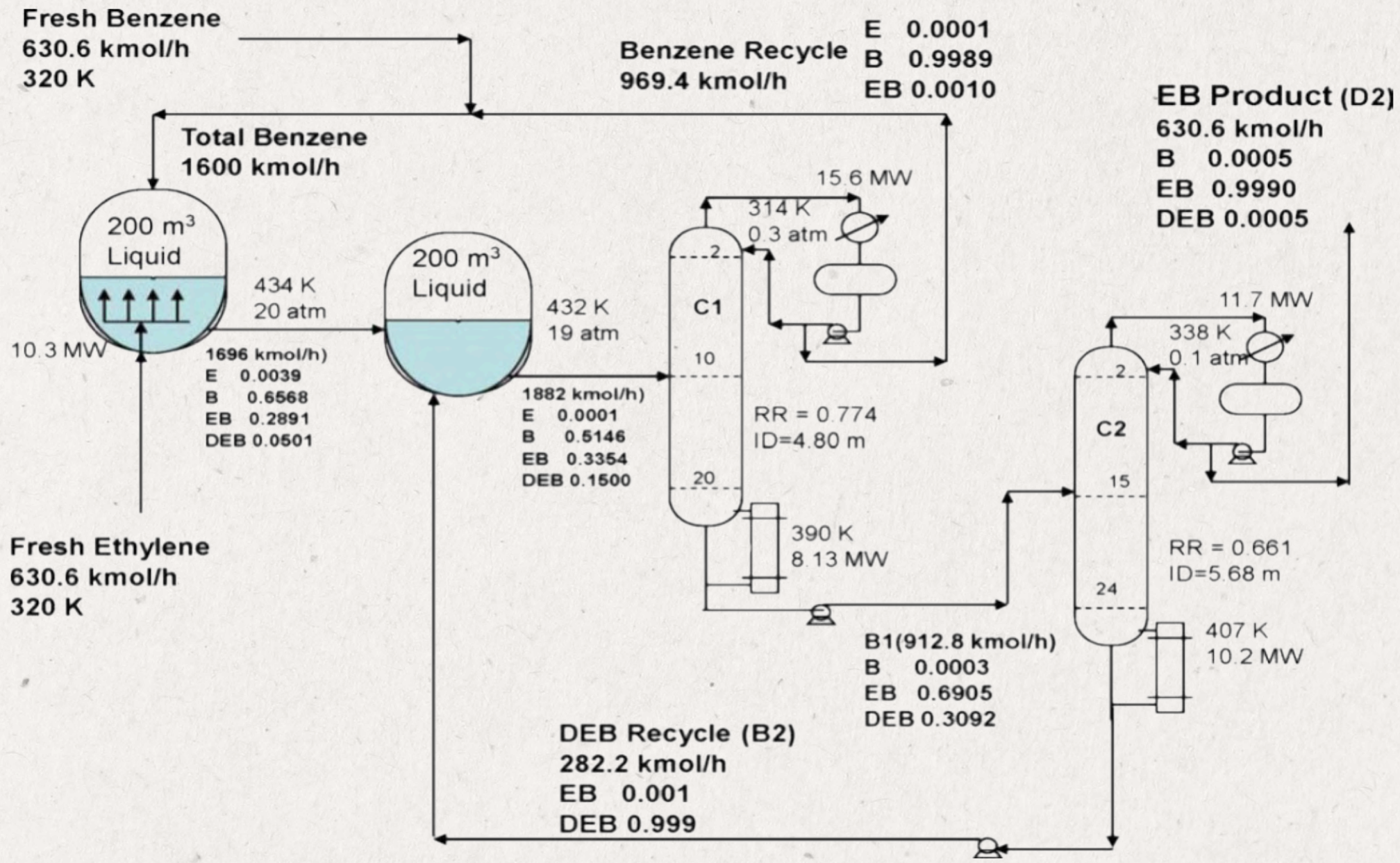
## ADJUST REACTOR PARAMETERS

ADJUST REACTOR PARAMETERS AND RECYCLE FLOWS FOR BETTER SYSTEM PERFORMANCE.





# FLOW SHEET AND BLOCK DIAGRAM OVERVIEW





A photograph of an industrial facility, likely a refinery or chemical plant, at night. The facility is illuminated by various lights, and a tall smokestack is visible on the left. The scene is reflected in a body of water in the foreground.

# FEED PREPARATION PROCESS

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## Purification of Benzene and Ethylene

Remove impurities from benzene and ethylene.

Ensure high-quality feed for the reaction process.

## Compression of Feed

Compress benzene and ethylene for optimal conditions.

Increase pressure to enhance reaction efficiency.

## Heating for Reaction Conditions

Heat the compressed feed to the required temperature.

Achieve optimal conditions for the reactor operation.

## Feed Preparation Conclusion

Critical step to ensure purity and efficiency.

Sets the foundation for successful ethylbenzene production.



# REACTION KINETICS ANALYSIS

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## ENERGY CONSUMPTION BREAKDOWN

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**10 kWh**

### Compression

Compression of feed mixture.

**8 kWh**

### Heating

Heating to reaction temperature.

**15 kWh**

### Distillation

Separation of products and unreacted feed.

**12 kWh**

### Reactor Operation

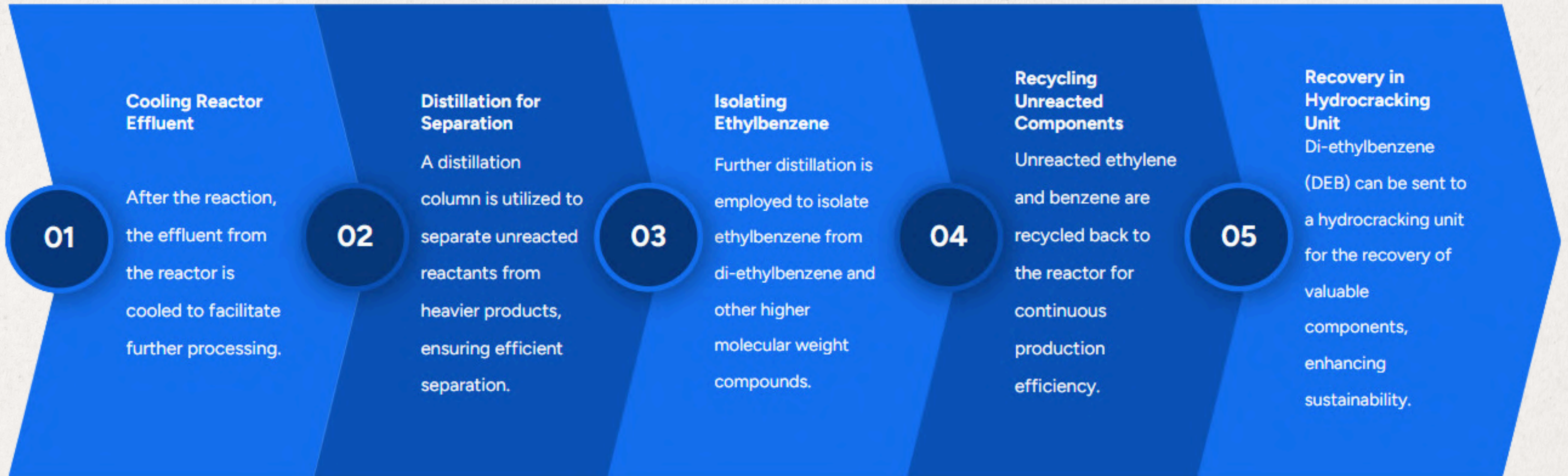
Operation of CSTR.





# SEPARATION AND RECYCLE PROCESSES

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# ASPEN SIMULATION SETUP

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## **Define Thermodynamic Properties**

Utilize the Peng-Robinson equation of state for property calculations.

## **Implement Reactor Modeling**

Employ a convergent reactor system to ensure precise control over temperature and pressure during the reaction process.

## **Utilize Distillation Modeling**

Apply a rigorous stage-by-stage method in distillation columns for efficient separation of components.

## **Analyze Process Performance**

Study the impact of operating conditions like temperature, pressure, and feed composition on conversion, selectivity, and yield.

## **Evaluate Energy Consumption**

Summarize energy consumption for major unit operations including compression, heating, reactor operation, and distillation.



## RESULTS: PROCESS PERFORMANCE ANALYSIS

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**85%**

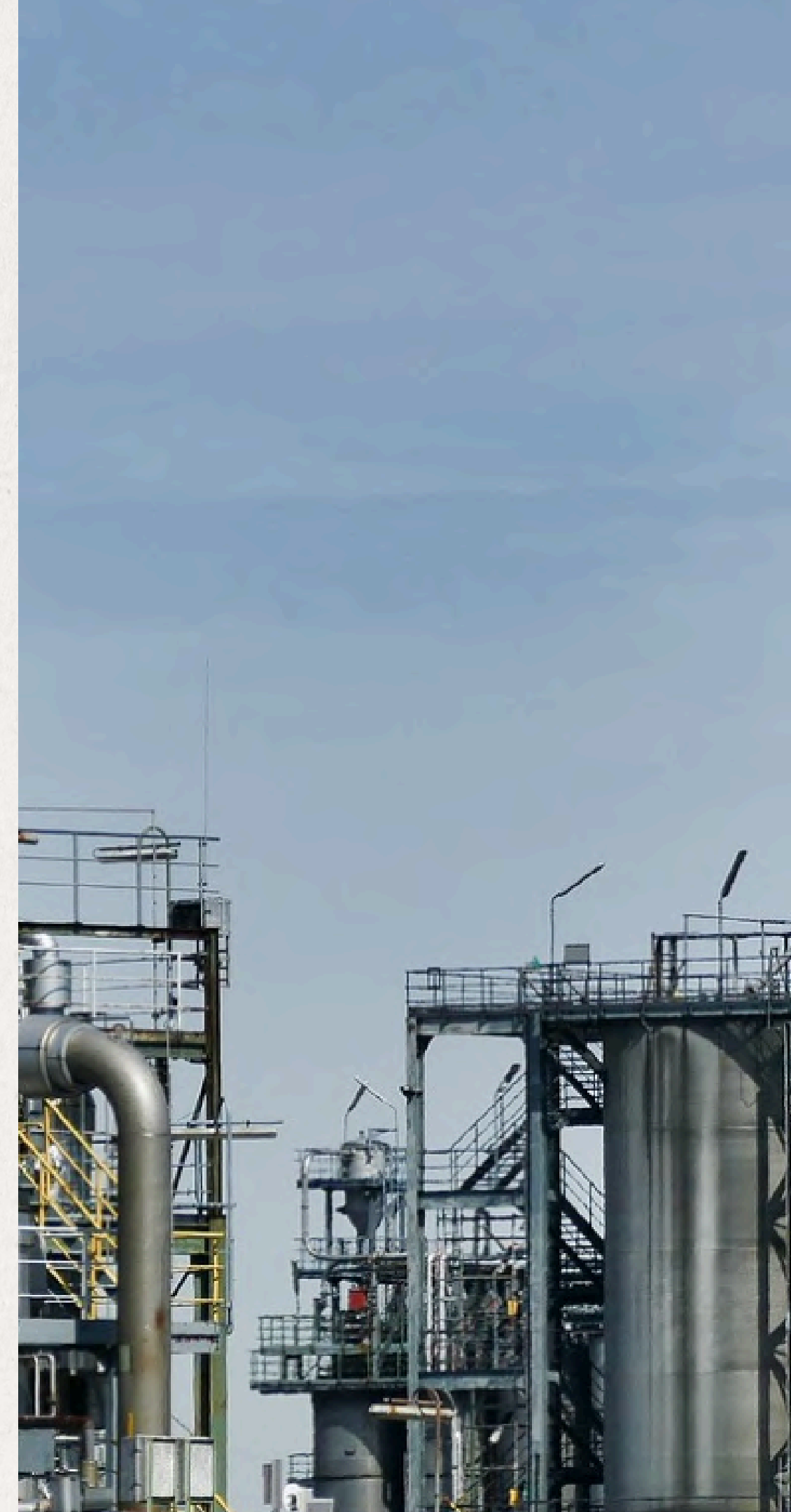
**Ethylbenzene Selectivity**

Process Performance Analysis

**100%**

**Di-ethylbenzene Recycle**

Process Performance Analysis





## CONCLUSION AND KEY FINDINGS

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**45 kWh**

### Total Energy Consumption

The total energy consumed during the process.

**99%**

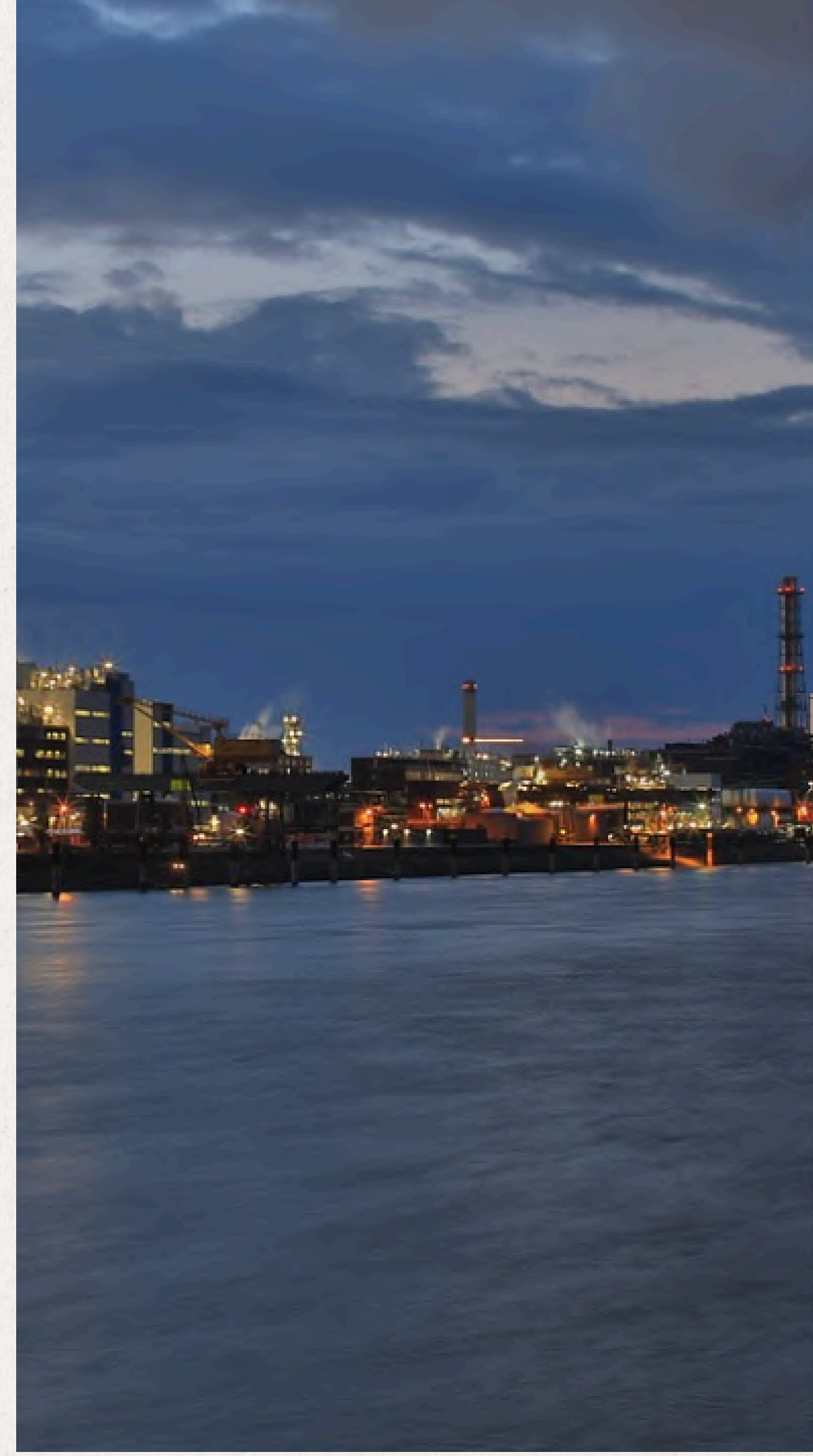
### Maximum Ethylbenzene Yield

The highest yield of ethylbenzene achieved.

**Achieved**

### By-Product Minimization

Successful minimization of by-products in the process.





# REFERENCES AND CITATIONS

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William L. Luyben  
AIChE Journal  
[Link to article](#)





Thank  
you! ✨



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