Experimental investigation of forced convective heat transfer in cylindical pipe flow

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Index Terms—Forced convective heat transfer, Nusselt number, Wall friction, Laminar, Turblent, Cylindical pipe flow

I. INTRODUCTION

In recent years, forced convective heat transfer in cylindical pipe flow plays an important role in many technical cooling systems. Considering heat transfer issues, heat transfer coefficient is one of the most important numbers.

$$h = \frac{Nu \cdot K}{L} \tag{1}$$

From general dimensional analysis, Nusselt number represents function of Reynolds number (Re) times Prandlt number (Pr) as following equation.

$$Nu = \alpha \cdot Re^{\pi_{\beta}} \cdot Pr^{\pi_{\gamma}} \tag{2}$$

Here, factors α , β and γ are constant value depend on flow regime and calculated from experimental result. By using above (1), we can easily find out heat transfer coefficient from (2).

Many studies have pointed out that heat transfer coefficient vary depending on the type of flow: laminar, transition and turblent. For laminar flow...

$$Nu_{lam} = \sqrt[3]{Nu_1^3 + b^3 + (Nu_2 - b)^3 + Nu_3^3}$$
 (3)

For turblent flow...

$$Nu_{turb} = \frac{\frac{\xi}{8} \cdot Re \cdot Pr}{1 + 12.7 \cdot \frac{\xi}{8})^{0.5} \cdot (Pr^{\frac{2}{3}} - 1)} \cdot (1 + (\frac{d_h}{l})^{\frac{2}{3}}) \quad (4)$$

$$\xi = (1.8\log 10Re - 1.5)^{-2} \tag{5}$$

Bertsche et al,[Bertsche2015] focused on reliable prediction of heat transfer coefficient for transitional flows. In their study, Bertsche et al, showed experimental heat transfer coefficients for Reynolds number 500 < Re < 23000 and Prandtl number 7 < Pr < 41.

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$$a + b = \gamma \tag{6}$$

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