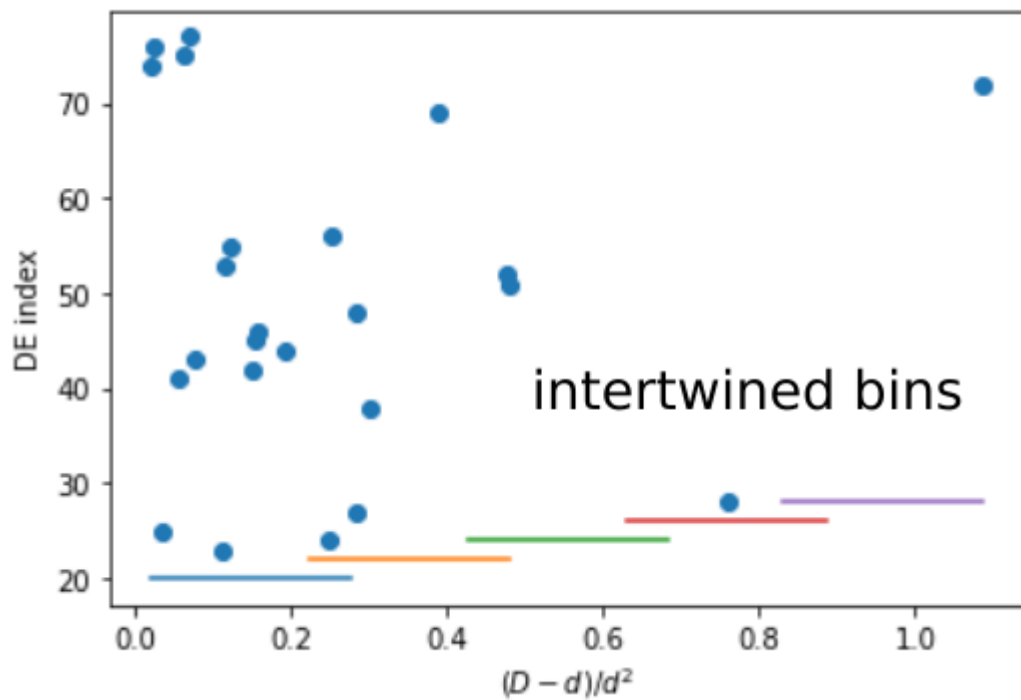
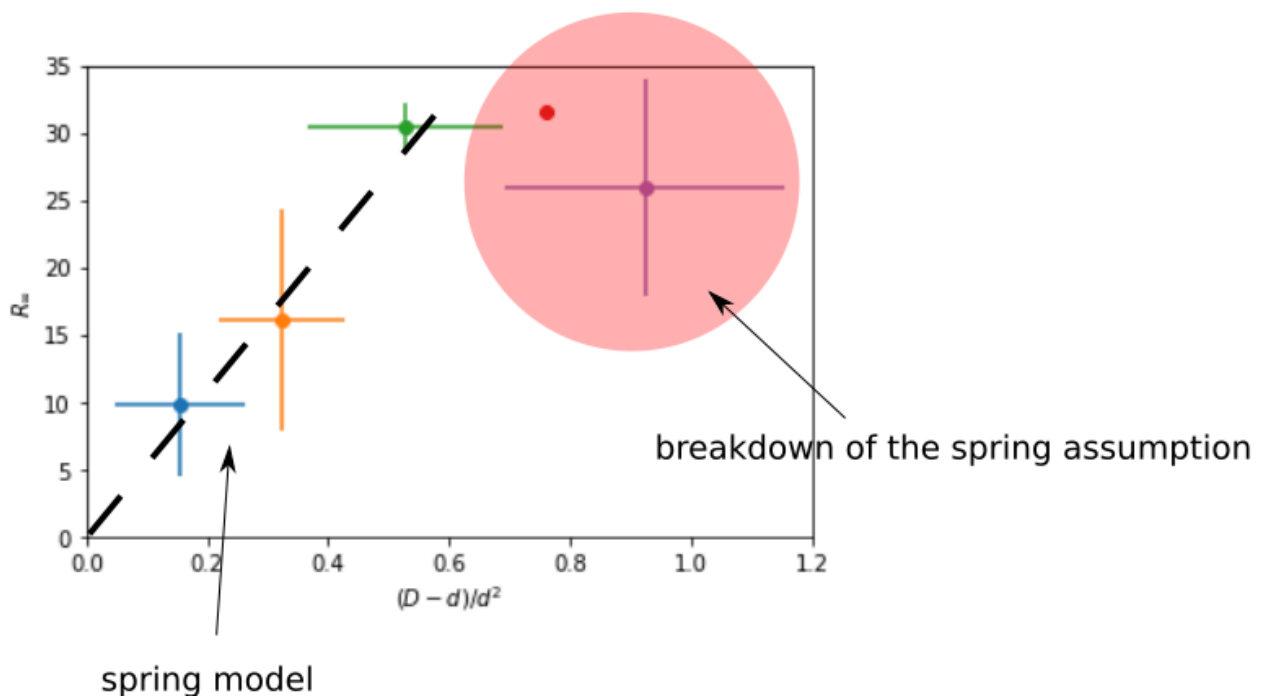


## Model the confinement effect

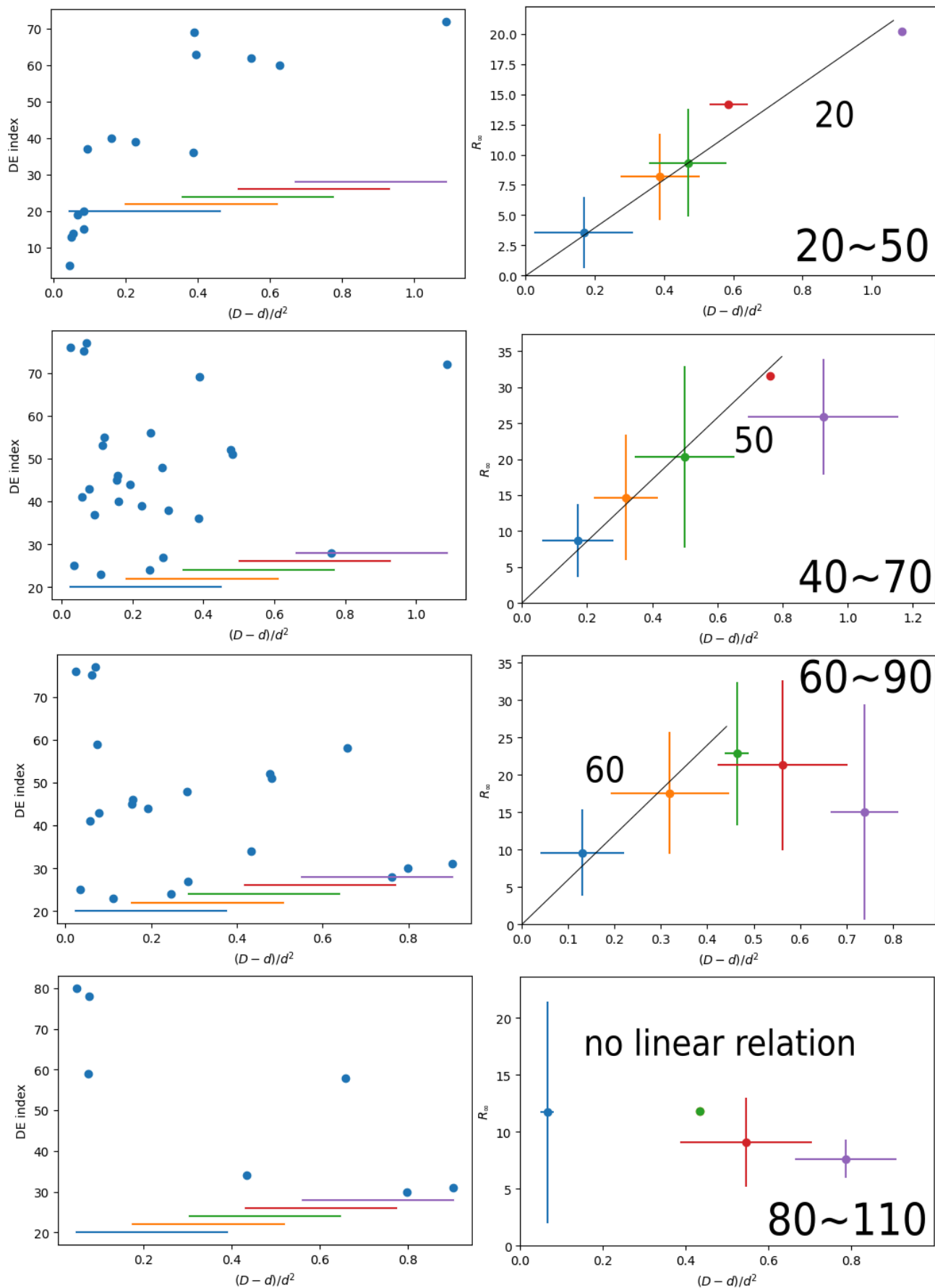
Intertwined bins for  $(D - d)/d^2$  (OD=50~70)



Saturation length  $R_\infty$  vs.  $(D - d)/d^2$



We can also look at data from other concentrations.



As expected, at low concentrations, the displacements of inner droplets are so small, so

that the Langevin equation takes the following form

$$\dot{x} = \eta(t) + \gamma x,$$

where  $\eta(t)$  is assumed to be an exponentially correlated noise, satisfying  $\langle \eta(t)\eta(t') \rangle = Ae^{-\nu|t-t'|}$ . It can be shown that this equation predicts the following MSD saturation value  $R_\infty$  and transition time  $\tau^*$ :

$$R_\infty = \frac{A}{\gamma(\nu + \gamma)},$$

$$\tau^* = \frac{1}{\gamma} = \frac{\Gamma}{k},$$

where  $\Gamma = 6\pi\eta r_i$  is the drag coefficient and  $k = m^*g/(r_o - r_i)$  is the effective spring constant. Notice that  $m^*$  is the buoyant mass of the oil droplet in water, and can be computed as  $m^* = \rho^*\frac{4}{3}\pi r_i^3$ . Taken together,  $\tau^*$  can be expressed as

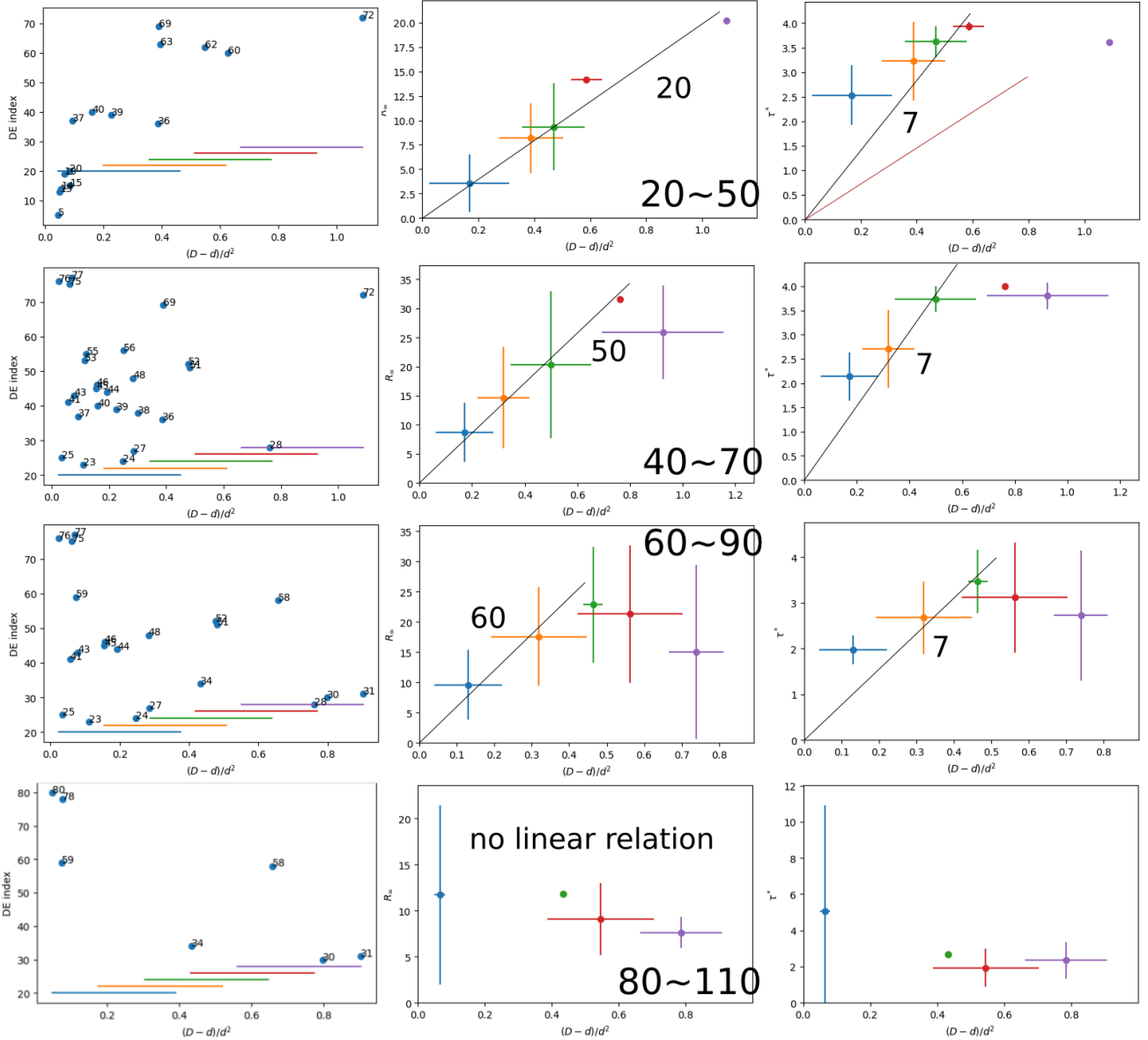
$$\tau^* = \frac{9\eta}{2\rho^*g} \frac{r_o - r_i}{r_i^2}.$$

To be consistent with my diameter representation,

$$\tau^* = \frac{9\eta}{\rho^*g} \frac{D - d}{d^2}.$$

Use water viscosity  $\eta = 0.001$  Pa s, we can compute the theoretical coefficient  $K = 9\eta/\rho^*g = 3.9 \mu\text{m s}$ .  $\tau^*$  is plotted against  $(D - d)/d^2$  as below:

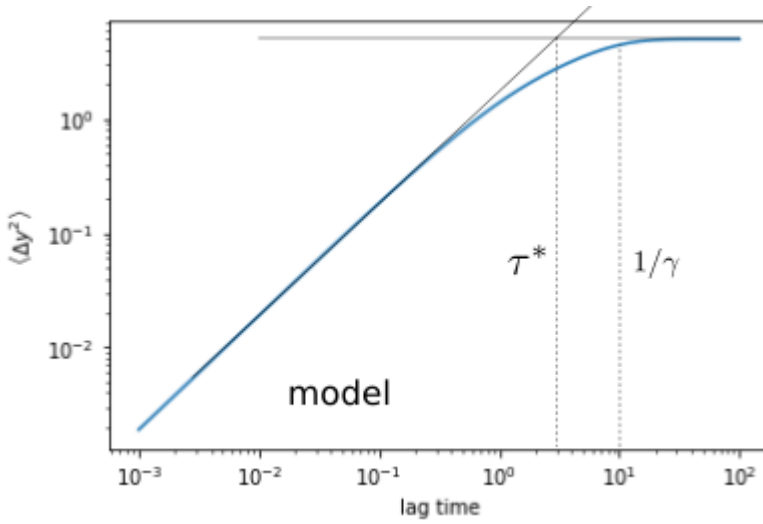
# $R_\infty$ and $\tau^*$ scaling



The nice linear relation observed at low OD's in the  $R_\infty$  vs.  $(D-d)/d^2$  plots is not observed in the  $\tau^*$  plots. If we force a linear fitting to the data points, we obtain a constant slope  $\approx 7 \mu\text{m s}$  for OD up to 90. Although the linear relation is not very pronounced, the value of the prefactor  $\approx 7 \mu\text{m s}$  is quite close to the theoretical prediction  $3.9 \mu\text{m s}$ .

## Difference between $\tau^*$ and $1/\gamma$

Note that although we stated  $\tau^* = 1/\gamma$ , it is actually not exact. The figure below plots a typical MSD predicted by the Langevin model, with the definitions of both  $\tau^*$  and  $1/\gamma$  illustrated.



If we use the  $1/\gamma$  definition to measure the time scale  $\tau^*$ , the  $\tau^*$  curves will shift up and deviate more from the theoretical prediction.

### Discuss the theoretical saturation value $R_\infty$

In the previous section, I show that the time scale  $\tau^*$  (or  $1/\gamma$ ) scales linearly with  $(D - d)/d^2$ . The Langevin model predicts that

$$R_\infty = \frac{A}{\gamma(\nu + \gamma)}$$

where  $\nu = 1/\tau > 1$  is roughly a constant according to current data. Since  $\gamma \ll 1$  holds true in most scenarios, we can assume  $\nu \gg \gamma$ . The saturation value  $R_\infty$  can be approximated as  $A\tau\tau^*$ . It is also assumed that  $A$ , the activity of the active bath, is only a function of the bacterial concentration OD, and does not depend on the confinement. Therefore, at a fixed OD, we expect

$$R_\infty \approx A\tau\tau^* \propto \tau^* \propto \frac{D - d}{d^2}$$

Look at the  $R_\infty$  vs.  $(D - d)/d^2$  plots, this is indeed a good prediction for the low OD and large inner size regime. More interestingly, although we derive how  $R_\infty$  depends on the confinement through  $\tau^*$ ,  $R_\infty$  actually shows better linear relations than  $\tau^*$ . This has brought new questions:

**Why does  $R_\infty$  show better linear relation with  $(D - d)/d^2$  than  $\tau^*$ ? Is it because our  $\tau^*$  is not exactly the  $1/\gamma$  in the model? Or  $A\tau$  is not a constant, but also depends on the confinement? Or more simply, the model is wrong?**

**How to understand the limit where the spring assumption breaks down?**