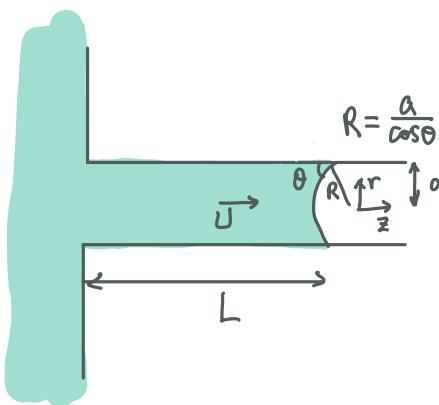


Moving contact lines

Wicking problem (ex. 1999 Ig Nobel prize)

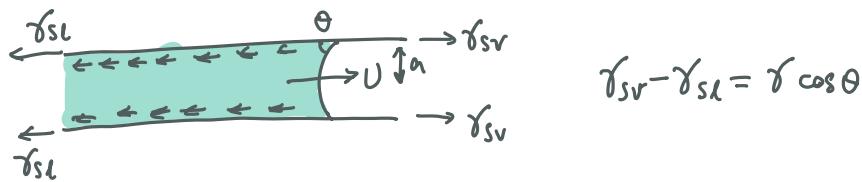
Let us review some basic concepts by working on this interesting question:



How fast does the front grow?

Let's say $B_0 = \frac{\rho g a^2}{\gamma}$, $C_a = \frac{\mu U}{\gamma} \ll 0$ so it is a matter viscosity and Capillarity.

- A scaling argument of force balance



$$\left. \begin{aligned} \text{Viscous force} &\sim \mu \frac{U}{a} \times aL = \mu LU \\ \text{Capillary force} &= \left\{ \begin{array}{l} 2\pi a x \gamma \cos \theta \\ \text{or} \\ \pi a^2 \times 2\gamma/R \end{array} \right. \sim a^2 \gamma \cos \theta \end{aligned} \right\} \rightarrow LU = \frac{1}{2} \frac{d}{dt}(L^2) \sim \frac{a \gamma \cos \theta}{\mu}$$

i.e. $L \sim \left(\frac{a \gamma \cos \theta}{\mu} \right)^{1/2} t^{1/2}$

- A formal analysis assuming fully developed Poiseuille flow ($\frac{\partial u}{\partial z} = 0$)

$$\frac{\partial p}{\partial z} = \mu \nabla^2 u = \mu \frac{1}{r} \frac{\partial}{\partial r} \left(r \frac{\partial u}{\partial r} \right) + \mu \frac{\partial^2 u}{\partial z^2} \xrightarrow{\text{function of } z} \xrightarrow{\text{function of } r}$$

$$\rightarrow \frac{\partial p}{\partial z} = -\frac{2\gamma \cos \theta}{\alpha L}$$

$$\rightarrow U = -\frac{\gamma \cos \theta}{2\mu \alpha L} r^2 + A \ln r + B$$

Use $\frac{\partial U}{\partial r}|_0 = 0$, $U|_{r=a} = 0$ to show

$$U = \frac{\gamma \cos \theta a}{2\mu L} \left(1 - \frac{r^2}{a^2} \right)$$


Finally the flow rate can be calculated

$$Q = 2\pi \int_0^a U r dr = \frac{\pi \gamma \cos \theta a^3}{4\mu L} = \pi a^2 U$$

$$\Rightarrow L(U) = \frac{1}{2} \frac{d}{dt} L^2 = \frac{a \gamma \cos \theta}{4\mu} , \text{ i.e. } L = \left(\frac{a \gamma \cos \theta}{2\mu} \right)^{1/2} t^{1/2}$$

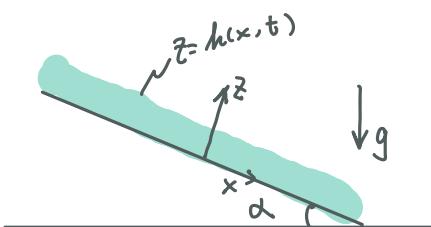
Washburn's equation. (1921)

Front slows down due to increasing viscous dissipation with increasing column length!

Free surface flow down an inclined plane.

Let's first consider a problem to 1) include gravity property and 2)

introduce a slip boundary.



$$g = g(\sin \alpha e_x - \cos \alpha e_z)$$

Recall:

$$\frac{\partial h}{\partial t} + \frac{\partial Q}{\partial x} = 0, \quad Q = \int_0^h u dz$$

$$\frac{\partial p}{\partial z} = -\rho g \cos \alpha \rightarrow p = -\gamma h_{xx} + \rho g (h-z) \cos \alpha$$

$$\frac{\partial P}{\partial x} = \mu \frac{\partial^2 u}{\partial z^2} + \rho g \sin \alpha \rightarrow \mu \frac{\partial^2 u}{\partial z^2} = -\underbrace{\gamma h_{xxx} + \rho g \cos \alpha h_x}_{f} - \rho g \sin \alpha$$

$$\rightarrow u = \frac{f}{2\mu} z^2 + C_1 z + C_2$$

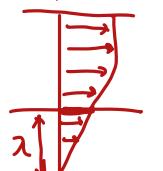
Use boundary conditions

$$\frac{\partial u}{\partial z} = 0 \text{ at } z=h \text{ (No shear)} \rightarrow C_1 = -\frac{f}{2\mu} h$$

$$u = \lambda \frac{\partial u}{\partial z} \text{ at } z=0 \text{ (slip)} \rightarrow C_2 = \lambda C_1$$

$$\rightarrow u = \frac{f}{2\mu} (z^2 - 2hz - 2\lambda h)$$

Interpretation of λ



Slip length.

Now we have the governing equation

$$Q = \int_0^h u dz = -\frac{f}{3\mu} h^3 - \frac{f}{\mu} \lambda h^2$$

$$\frac{\partial h}{\partial t} = -\frac{\partial Q}{\partial x} = \frac{\partial}{\partial x} \left[\left(\frac{1}{3} h^3 + \lambda h^2 \right) (-\gamma h_{xxx} + \rho g \cos \alpha h_x - \rho g \sin \alpha) \right]$$

No-dimensionalization

$$H = h/l, \quad X = x/l, \quad \Lambda = \lambda/l, \quad T = t/t_x, \quad t_x = l/U_0$$

The governing equation can be rewritten as

$$H_T + \left[\frac{1}{Ca} \left(\frac{1}{3} H^3 + \Lambda H^2 \right) (H_{XXX} - B_0 \cos \alpha H_x + B_0 \sin \alpha) \right]_X = 0$$

where

$$B_0 = \frac{\rho g l^2}{\gamma} \quad \text{and} \quad Ca = \frac{\mu U_0}{T}.$$

- Non-zero α and sufficient shallow flows ($h_x \ll \tan \alpha$) with slip BC.

(92)

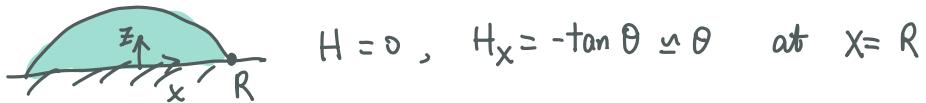
$$H_T + \left[\frac{1}{C_a} \left(\frac{1}{3} H^3 + \Lambda H^2 \right) (H_{xxx} + B_0 \sin \alpha) \right]_x = 0$$

- Zero α (free surface flow on a horizontal plane) with no-slip BC.

$$H_T + \left[\frac{1}{3C_a} H^3 (H_{xxx} - B_0 H_x) \right]_x = 0$$

Spreading: No-slip and slip boundary conditions

How to model the evolution/spreading of a blob of fluid? May simply apply



where R is unknown (to be determined based on mass conservation). However,

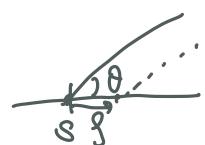
such b.c.s are not compatible with the governing equation — as we show now.

Suppose that the boundary is located at $x = s(t)$. Zoom in on the

interface by setting $x = s(t) + \epsilon$ with ϵ small. Locally we have

$h \sim \theta \epsilon$. Set

$$X = S(t) + \varphi \quad \text{and} \quad H = \theta \varphi + f(\varphi) \quad |\varphi| \ll 1, |f| \ll |\theta \varphi|.$$



Now the governing equation reads (with $\frac{dg}{dt} = \dot{g}$, $\frac{\partial g}{\partial x} = 1$, $H_x = \theta + f_g$)

$$f_T - f_g \dot{s} - \theta \dot{s} + \left[\underbrace{\frac{1}{3Ca} \theta^3 \dot{g}^3}_{\sim f/g} \left(f_{ggg} - B_0 \theta - B_0 f_g \right) \right]_g \sim \dot{g}^2 \sim f$$

- Attempt to neglect the higher spatial derivatives

$$-f_g \dot{s} = \theta \dot{s} \quad \text{with } f=0 \text{ at } g=0$$

$$\rightarrow f = -\theta \dot{g} \quad (\text{Not compatible with } H \ll |\theta \dot{g}|) \quad X$$

- To include higher spatial derivatives

$$\left(\frac{1}{3Ca} \theta^3 \dot{g}^3 f_{ggg} \right)_g \sim \theta \dot{s}$$

$$\rightarrow f_{ggg} \sim \frac{3Ca \dot{s}}{\theta^2 \dot{g}^2}$$

$$\rightarrow f \sim \frac{3Ca \dot{s}}{\theta^2} \left(\dot{g} \log \dot{g} - \frac{1}{2} \dot{g}^2 \right) \not\sim \theta \dot{g} \quad X \quad \text{Check here?}$$

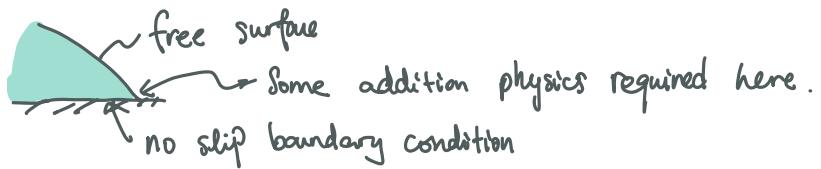
Incompatible again

- To include gravity term

$$\rightarrow f_g \sim -\frac{\theta \dot{s} g \times 3Ca}{B_0 \theta^3 \dot{g}^3} = -\frac{3Ca \dot{s}}{B_0 \theta^2 \dot{g}^2} \quad (\text{More singular}) \quad X$$

CANNOT find a consistent solution local to the moving contact line! The difficulty

does not lie in the use of thin-film equation or inadequate mathematics – it is a fundamental physical difficulty



An hypothesis for the physics required to treat the moving contact line is to

allow a small amount of slip between the substrate and the fluid: $u = 2 \frac{\partial u}{\partial z} \Big|_{z=0}$.

The thin film equation becomes

$$H_T + \left[\frac{1}{Ca} \left(\frac{1}{3} H^3 + \Lambda H^2 \right) (H_{XXX} - B_0 H_X) \right]_X = 0.$$

Use $X = S + \xi$ and $H = \theta \xi + f$ so that

$$f_T - \theta \dot{S} - f_{\xi} \dot{S} + \left[\frac{1}{Ca} \left(\frac{1}{3} \theta^3 \xi^3 + \Lambda \theta^2 \xi^2 \right) (f_{\xi\xxi\xxi} - B_0 f_{\xi} - B_0 \theta) \right]_{\xi} = 0$$

The leading-order balance gives

$$\Lambda \theta^2 \xi^2 f_{\xi\xxi\xxi} \sim Ca \theta \dot{S} \xi$$

$$\rightarrow f_{\xi\xxi} \sim \frac{Ca \dot{S}}{\theta \Lambda} \log \xi$$

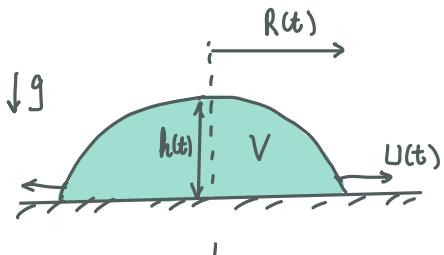
$$\rightarrow f \sim \frac{Ca \dot{S}}{\theta \Lambda} \xi^2 \log \xi \ll \theta \xi \quad \checkmark$$

So that it is possible to impose a contact angle θ with slip bcs.

Precursor film and Tanner's law

Let us first check how a drop spreads via a scaling argument.

$$\bullet B_0 = \frac{\rho g R^2}{\gamma} \gg 1, \quad Re \ll 1$$



Driven by gravity, resisted by viscosity

$$\frac{\partial P}{\partial r} = \mu \frac{\partial^2 u}{\partial z^2} \rightarrow \frac{\rho g h}{R} \sim \mu \frac{U}{h^2} \sim \mu \frac{R}{h^2 t}$$

$$\text{Continuity } \pi R^2 h \sim V \rightarrow h \sim \frac{V}{R^2}$$

$$\Rightarrow R \sim \left(\frac{\rho g V^3}{\mu} \right)^{1/8} t^{1/8}$$

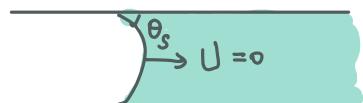
$$\bullet B_0 = \frac{\rho g R^2}{\gamma} \ll 1, \quad Re \ll 1 \quad (\text{Note that gravity becomes progressively more important as } R \uparrow)$$

$$\gamma \frac{h}{R^3} \sim \mu \frac{U}{h^2} \sim \mu \frac{R}{h^2 t} \Rightarrow \gamma \frac{h^3}{R^4} \sim \frac{\mu}{t} \Rightarrow R \sim \left(\frac{\gamma V^3}{\mu} \right)^{1/10} t^{1/10}$$

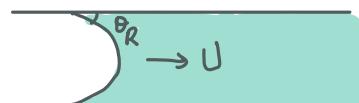
How to figure out the prefactor? To be discussed in next lecture.

① Advancing and receding angle (A regularization mechanism like slip)

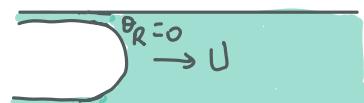
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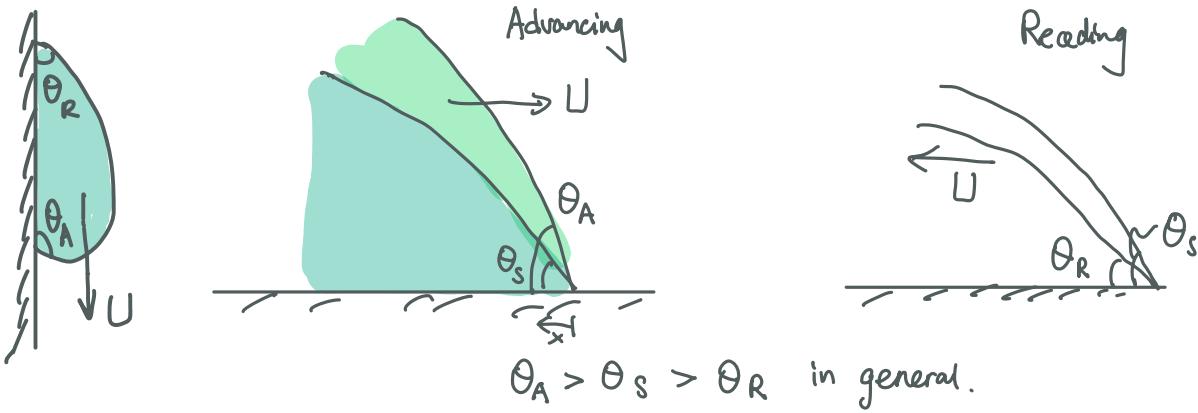


$C_a \ll 1$



$C_a \uparrow$





For the spreading problem, let's see what is going on near the advancing front.

- Geometry. For $\theta_s < \theta_A \ll 1$, $\tan \theta_A \approx \frac{h}{x} \approx \theta_A$, $h \approx \theta_A x$
- Velocity gradient. $\frac{\partial U}{\partial z} \sim \frac{U}{h} = \frac{U}{\theta_A x}$
- Force balance. Driving force $F = \gamma_{sv} - \gamma_{sl} - \gamma \cos \theta_A$
 $= \gamma (\cos \theta_s - \cos \theta_A) > 0$ since $\theta_s < \theta_A$
- Revisiting the scaling argument

$$\underbrace{\mu \frac{U}{h}}_{\text{Viscous stress}} \times \pi R^2 \sim \underbrace{\gamma (\cos \theta_s - \cos \theta_A)}_{\text{Line force}} \times 2\pi R$$

$$\Rightarrow \mu \frac{dR}{dt} \times \frac{R^2}{V} \times R^2 \sim \gamma (\cos \theta_s - \cos \theta_A) R \rightarrow R \sim \left(\frac{\gamma V}{\mu} \right)^{1/4} + t^{1/4}$$

Not what has been observed. why? $\theta_A \text{inf}(U)$

② Physical picture of precursor film (complete wetting)

First, relate the driving force F to the local velocity by

$$FU \sim \phi$$

where ϕ is Viscous dissipation in the corner. Locally, we have

$$\phi \sim \int_A \mu \left(\frac{\partial U}{\partial z} \right)^2 dA \sim \int_0^\infty dz \int_0^{h=\theta_A z} \mu \left(\frac{U^2}{\theta_A z} \right) dz$$

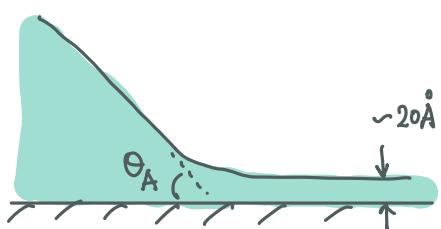
$$\sim \frac{\mu U^2}{\theta_A} \int_a^{R \approx} \frac{1}{z} dz$$

Drop size
Molecular size

$$\phi \sim \frac{3\mu U^2 l_D}{\theta_A}, \quad l_D \sim \int_a^R \frac{1}{z} dz = \ln R/a$$

De Gennes' approximation, $15 < l_D < 20$ in experiments

Then calculate F assuming a thin film covering the substrate (in the presence of precursor film).



$$F = \gamma + \gamma_{SL} - \gamma \cos \theta_A - \gamma_{SE}$$

$$\simeq \frac{1}{2} \gamma \theta_A^2$$

(May use this to revisit the scaling above and obtain the same result)

$$\mu \frac{U}{h} R^2 \sim \gamma \theta_A^2 R \quad \& \quad h \sim R \theta_A$$

$$FU \sim \phi \rightarrow \frac{1}{2} \gamma \theta_A^2 U \sim \frac{3\mu U^2 l_D}{\theta_A} \rightarrow U \sim \frac{\gamma l_D}{\mu} \theta_A^3 \rightarrow \theta_A^3 \propto Ca \quad (\text{Tanner's law}).$$

Finally, use the conservation of mass $V \sim R^3 \theta_A$ to obtain

$$\frac{1}{\theta_A} \frac{d\theta_A}{dt} \sim - \frac{1}{R} \frac{dR}{dt} \sim - \frac{\gamma}{\mu R} \theta_A^3 \sim - \frac{\gamma}{\mu V^{1/3}} \theta_A^{10/3}$$

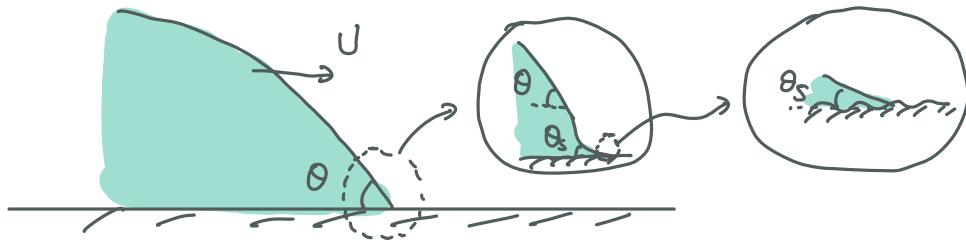
$$\rightarrow \theta_A \sim \left(\frac{\mu V^{1/3}}{\gamma t} \right)^{3/10}, \quad R \sim \left(\frac{V}{\theta_A} \right)^{1/3} \sim \left(\frac{\gamma V^3}{\mu} \right)^{1/10} t^{1/10}$$

$$\theta = \theta_A R^2 \frac{dR}{dt} + \frac{d\theta_A}{dt} \cdot R^3$$

(consistent with the thin-film behavior)

③ Cox-Voinov Law

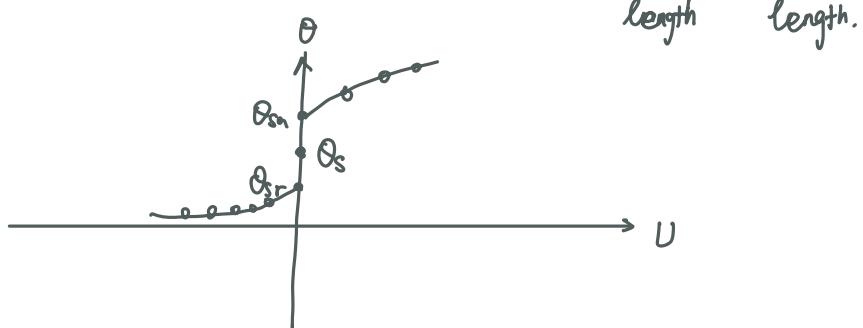
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Matching of solutions at different scales gives rise to

$$|U| = \begin{cases} K(\theta^3 - \theta_{sa}^3) \\ -K(\theta^3 - \theta_{sr}^3) \end{cases}, \quad K = \frac{\gamma}{q \mu h_0 (\alpha h_0 / l_i)} \quad \text{Depends on details of micro/macro solutions}$$

Outer length Inner length.



In Summary, the "singularity" of moving contact line can be "regularized"

by "slip", "precursor film", "C-V law" and other multiscale modelling.

• Quasistatic evolution with $Ca \ll 1$, $Bo \ll 1$

Using C-V law in full-time dependent problem often still requires some slip to

avoid a contact line singularity. However, there is a natural velocity scale

in C-V law and if it is slow ($Ca = \frac{U k}{\sigma} \ll 1$), the fluid moves quasi-statically.

We solve the static version of

$$H_T + \left[\frac{1}{Ca} \left(\frac{1}{3} H^3 + \Lambda H^2 \right) (H_{XXX} - B_0 H_X) \right]_X = 0.$$

The contact line moves with a speed determined by the contact angle. We don't have to include slip in this case (no stress singularity). Let us focus

on a 2D example

$$Ca = \frac{\mu k}{\gamma} \ll 1, \quad B_0 \ll 1, \quad \Lambda_0 = K, \quad l = A^{1/2}$$

The thin film equation is now

$$\left(H^3 H_{XXX} \right)_X = 0$$

subject to

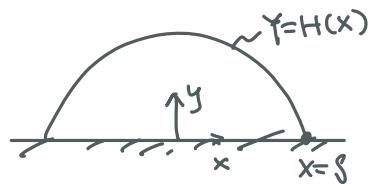
$$H_x(0) = 0$$

and

$$H_x(S) = -\theta$$

$$H(S) = 0$$

$$\dot{S} = \theta^3 - \theta_{SA}^3$$



at the contact line $X=S(t)$, together with a global mass balance equation

$$\int_0^S H dx = \frac{1}{2}$$

We find that

$$H = \frac{\theta}{2S} (S^2 - X^2)$$

Imposing the total mass constraint gives

$$\frac{2}{3} \theta S^2 = 1$$

Using GV law gives the evolution equation S as

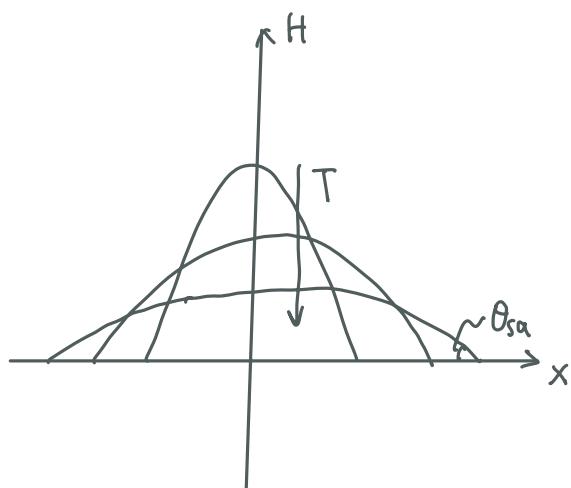
$$\frac{dS}{dT} = \frac{27}{8} \frac{1}{S^6} - \theta_{sa} .$$

This is an ODE for $S(t)$ with $S(0) = S_0$.

- For $\theta_{sa} \ll 1$, $S^7 - S_0^7 \sim T$

$$\rightarrow \frac{R}{A^{4/3}} \sim \left(\frac{t}{A^{4/3}/(\tau/\mu)} \right)^{1/7}$$

$$R \sim \left(\frac{\gamma A^3}{\mu} \right)^{1/7} t^{1/7} \text{ for 2D case.}$$



- Eventually, $S \rightarrow S_\infty$ as $T \rightarrow \infty$ when $t_{\infty} = -\theta_{sa}$.

(Note that for the axisymmetric case, the mass conservation becomes $\theta S^3 \sim 1$, which

will lead $\frac{dS}{dt} \sim \frac{1}{S^9}$ or $S^{10} - S_0^{10} \sim T$)