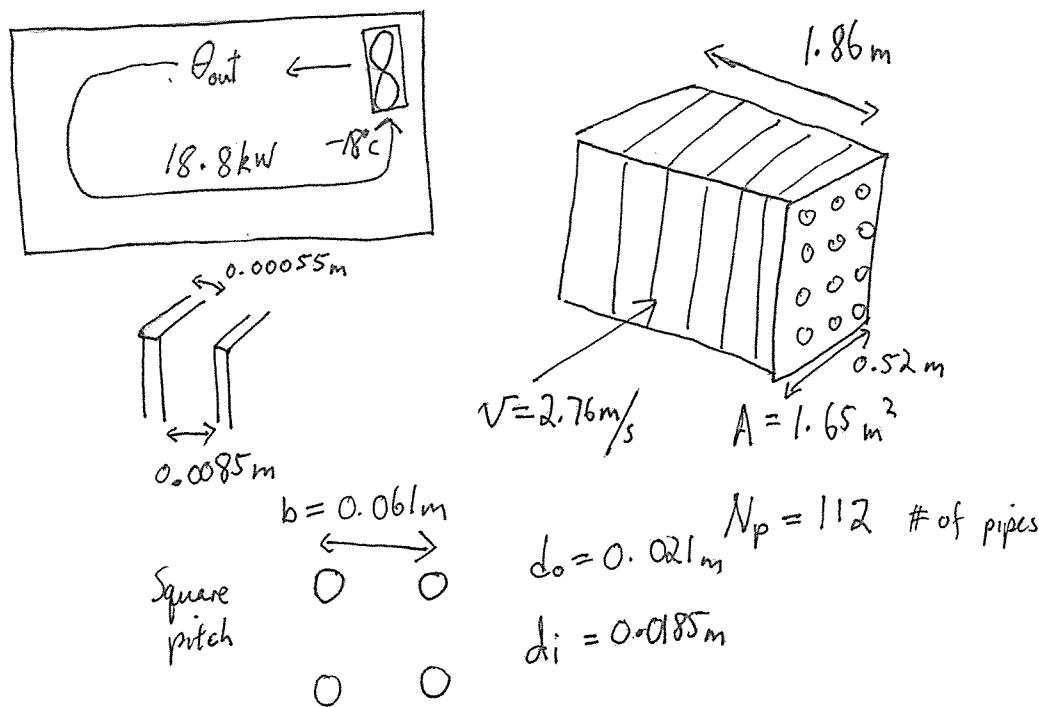


### 3.3 WORKED EXAMPLE – AIR FIN HEAT EXCHANGERS

A coldstore is being built – the expected heat load to be removed is 18.8 kW at an air temperature onto the evaporator of  $-18^{\circ}\text{C}$ . An old air cooling unit is available – it has a face area of  $1.65\text{m}^2$ , and the fan maintains an air flow of  $2.76\text{ m/s}$  off this face. The unit has aluminium fins ( $k = 200\text{ W/mK}$ ) of thickness  $0.55\text{mm}$  and spaced at  $8.5\text{mm}$  centres. The unit length is  $1.86\text{m}$ , and its depth in the direction of air flow  $0.52\text{m}$ . the film heat transfer coefficient in the boiling refrigerant has been estimated as  $265\text{ W/m}^2\text{K}$ , and that in the air flow as  $19\text{ W/m}^2\text{K}$ . There are 112 tubes of outside diameter  $21\text{ mm}$  and inside diameter  $18.5\text{mm}$ , these being placed in square-itch at  $61\text{mm}$  centres. Determine the refrigerant evaporation temperature required if the unit is to accomplish the required heat transfer.

#### 3.3.1 Scenario diagram



#### 3.3.2 Calculate the air off temperature

$$\begin{aligned}\text{Air flow rate} &= 2.76 \text{ m/s} \times 1.65 \text{ m}^2 \\ &= 4.55 \text{ m}^3/\text{s}\end{aligned}$$

$$\begin{aligned}\text{At } -18^{\circ}\text{C} \quad \rho &= 1.38 \frac{\text{kg}}{\text{m}^3} \quad \dot{m}_{\text{air}} = 4.55 \times 1.38 \\ \text{density of air} &\quad = 6.28 \text{ kg/s}\end{aligned}$$

$$\begin{aligned}\phi &= \dot{m} C_p \Delta \theta = \dot{m} C_p (-18 - \theta_{\text{out}}) \\ 18.8 &= 6.28 (1.01) (-18 - \theta_{\text{out}}) \\ 24 &\\ \theta_{\text{out}} &= -21^{\circ}\text{C}\end{aligned}$$

### 3.3.3 Calculation of the UA value

$$\frac{1}{UA} = \frac{1}{h_1 A_1} + \frac{x}{KA_{12}} + \frac{1}{h_2(A_p + n_f A_f)}$$

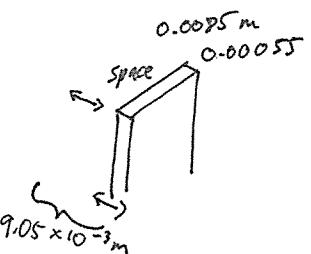
$A_p = \pi d_o N_p (L_p - N_d)$

area  
of plates

$N = \frac{1.86}{9.05 \times 10^{-3}} + 1 = 206 \text{ fins}$

# of fins

$$L_x = \frac{1.65}{1.86} = 0.887 \text{ m}$$



$$A_p = \pi \times 0.021 \times 112 [1.86 - 206 \times 0.00055]$$

$$= 12.91 \text{ m}^2$$

$$A_{f_{ins}} = 2N \left( L_x L_y - N_p \frac{\pi}{4} d_o^2 \right)$$

$$= 2 \times 206 \left( 0.89 \times 0.52 - 112 \frac{\pi}{4} \times 0.021^2 \right)$$

$$= 174.7 \text{ m}^2$$

To find  $n_f$ :  $b = 0.061$

Square pitch tubes

$$H = \left( \frac{1.13b - 0.021}{2} \right) = \frac{1.13 \times 0.061 - 0.021}{2}$$

$$= 0.024 \text{ m}$$

$$Z_1 = H \sqrt{\frac{2h_2}{dk}} = 0.024 \times \sqrt{\frac{2(19)}{0.00055 \times 200}}$$

$$= 0.446$$

$$Z_2 = 1 + \frac{2H}{d_o}$$

from figure 26

$$= 1 + \frac{2 \times 0.024}{0.021} = 3.29$$

$$\therefore n_f = 0.89$$

$$A_1 = N_p \pi \frac{d_i}{2} L$$

inside diameter

$$= 112 \times \pi \times 0.0185 (1.86)$$

$$= 12.1 \text{ m}^2$$

$$A_{12} = 2\pi \left( \frac{\frac{r_2}{2} + r_1}{2} \right) LN$$

$$= 2\pi (9.875 \times 10^{-3}) 1.86 (112)$$

$$= 12.92 \text{ m}^2$$

$$x = \text{pipe thickness} = \frac{1}{2} (0.021 - 0.0185)$$

$$= 0.00125 \text{ m}$$

$$\frac{1}{UA} = \frac{1}{265(12.1)} + \frac{0.00125}{200(12.92)} + \frac{1}{19(12.91 + 0.89 \times 174.7)}$$

$$= 3.1187 \times 10^{-4} + 4.84 \times 10^{-7} + 3.125 \times 10^{-4}$$

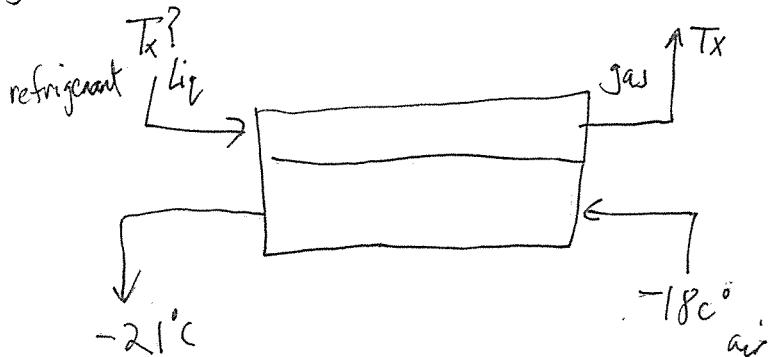
$$UA = 1600 \frac{W}{K}$$

### 3.3.4 Calculate the required evaporation temperature

$$\phi = UA F_t \Delta \theta_{LMD} \quad \text{assume } F_t = 1 \quad (\text{fully counter current})$$

$$-18.8 = 1.6 \Delta \theta_{LMD}$$

negative because  
it is being cooled  
 $\Delta \theta_{LMD} = -11.75^\circ \text{C}$



$$\Delta \theta_{LMD} = -11.75^\circ \text{C}$$

Iterate for  $T_x$

$$\frac{[T_x - (-21)] - [T_x - (-18)]}{\ln \left[ \frac{T_x - (-21)}{T_x - (-18)} \right]} = -11.75^\circ \text{C}$$

$$\underline{T_x = -31.3^\circ \text{C}} \text{ after some iteration.}$$