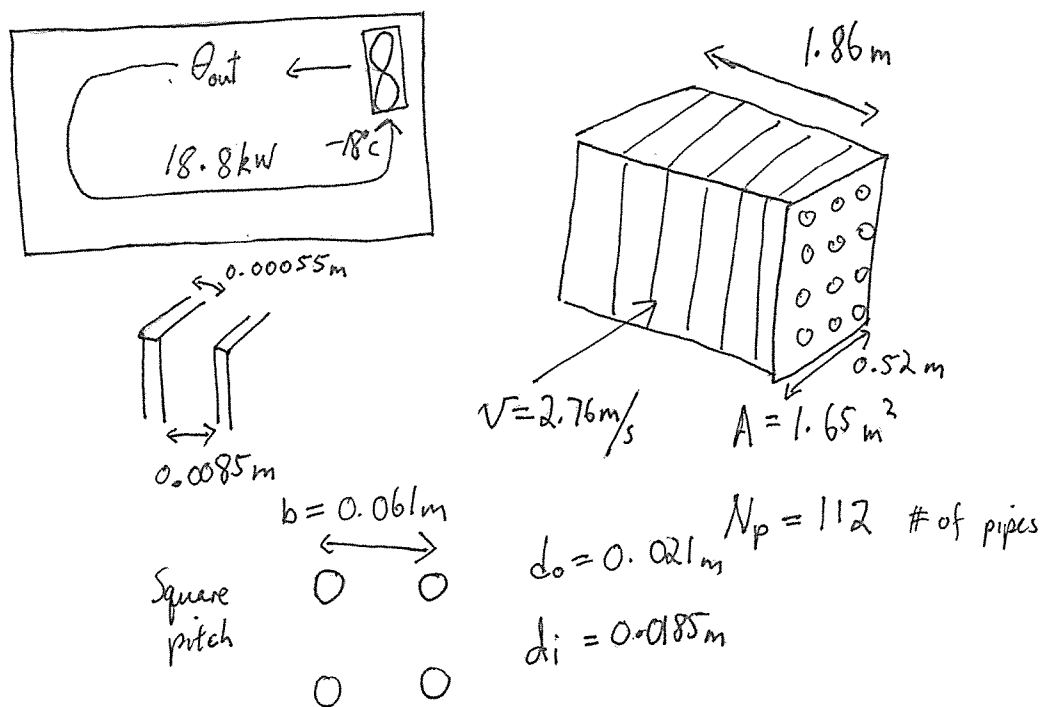


### 3.3 WORKED EXAMPLE – AIR FIN HEAT EXCHANGERS

A coldstore is being built – the expected heat load to be removed is 18.8 kW at an air temperature onto the evaporator of  $-18^{\circ}\text{C}$ . An old air cooling unit is available – it has a face area of  $1.65\text{m}^2$ , and the fan maintains an air flow of  $2.76\text{ m/s}$  off this face. The unit has aluminium fins ( $k = 200\text{ W/mK}$ ) of thickness  $0.55\text{mm}$  and spaced at  $8.5\text{mm}$  centres. The unit length is  $1.86\text{m}$ , and its depth in the direction of air flow  $0.52\text{m}$ . The film heat transfer coefficient in the boiling refrigerant has been estimated as  $265\text{ W/m}^2\text{K}$ , and that in the air flow as  $19\text{ W/m}^2\text{K}$ . There are 112 tubes of outside diameter  $21\text{ mm}$  and inside diameter  $18.5\text{mm}$ , these being placed in square pitch at  $61\text{mm}$  centres. Determine the refrigerant evaporation temperature required if the unit is to accomplish the required heat transfer.

#### 3.3.1 Scenario diagram



#### 3.3.2 Calculate the air off temperature

$$\begin{aligned}\text{Air flow rate} &= 2.76\text{ m/s} \times 1.65\text{ m}^2 \\ &= 4.55\text{ m}^3/\text{s}\end{aligned}$$

$$\begin{aligned}\text{At } -18^{\circ}\text{C } \rho &= 1.38\text{ kg/m}^3 \\ \text{density of air} & \\ \dot{m}_{air} &= 4.55 \times 1.38 \\ &= 6.28\text{ kg/s}\end{aligned}$$

$$\begin{aligned}\phi &= \dot{m} C_p \Delta\theta = \dot{m} C_p (-18 - \theta_{out}) \\ 18.8 &= 6.28 (1.01) (-18 - \theta_{out}) \\ \theta_{out} &= -21^{\circ}\text{C}\end{aligned}$$

### 3.3.3 Calculation of the UA value

$$\frac{1}{UA} = \frac{1}{h_1 A_1} + \frac{x}{KA_{12}} + \frac{1}{h_2(A_p + n_f A_f)}$$

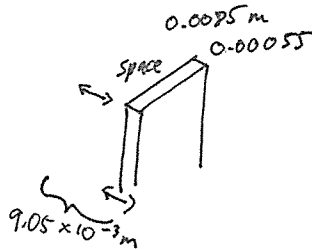
$$A_p = \pi d_o N_p (L_p - Nd)$$

area of plates

$$N = \frac{1.86}{9.05 \times 10^{-3}} + 1 = 206 \text{ fins}$$

# of fins

$$L_x = \frac{1.65}{1.86} = 0.887 \text{ m}$$



$$A_p = \pi \times 0.021 \times 112 [1.86 - 206 \times 0.00055]$$

$$= 12.91 \text{ m}^2$$

$$A_{f_{ins}} = 2N (L_x L_y - N_p \frac{\pi}{4} d_o^2)$$

$$= 2 \times 206 (0.89 \times 0.52 - 112 \frac{\pi}{4} \times 0.021^2)$$

$$= 174.7 \text{ m}^2$$

To find  $n_f$ :

Square pitch tubes

$$b = 0.061$$

$$H = \left( \frac{1.13b - 0.021}{2} \right) = \frac{1.13 \times 0.061 - 0.021}{2}$$

$$= 0.024 \text{ m}$$

$$Z_1 = H \sqrt{\frac{2h_2}{dk}} = 0.024 \times \sqrt{\frac{2(19)}{0.00055 \times 200}}$$

$$= 0.446$$

$$Z_2 = 1 + \frac{2H}{d_o}$$

$$= 1 + \frac{2 \times 0.024}{0.021} = 3.29$$

25

from figure 26

$$\therefore n_f = 0.89$$

$$A_1 = N_p \pi d_i L$$

$$= 112 \times \pi \times 0.0185 (1.86)$$

$$= 12.1 \text{ m}^2$$

$$A_{12} = 2\pi \left( \frac{r_2 + r_1}{2} \right) L N$$

$$= 2\pi (9.875 \times 10^{-3}) 1.86 (112)$$

$$= 12.92 \text{ m}^2$$

$$x = \text{pipe thickness} = \frac{1}{2} (0.021 - 0.0185)$$

$$= 0.00125 \text{ m}$$

$$\frac{1}{UA} = \frac{1}{265(12.1)} + \frac{0.00125}{200(12.92)} + \frac{1}{19(12.91 + 0.89 \times 174.7)}$$

$$= 3.1187 \times 10^{-4} + 4.84 \times 10^{-7} + 3.125 \times 10^{-4}$$

$$UA = 1600 \frac{\text{W}}{\text{K}}$$

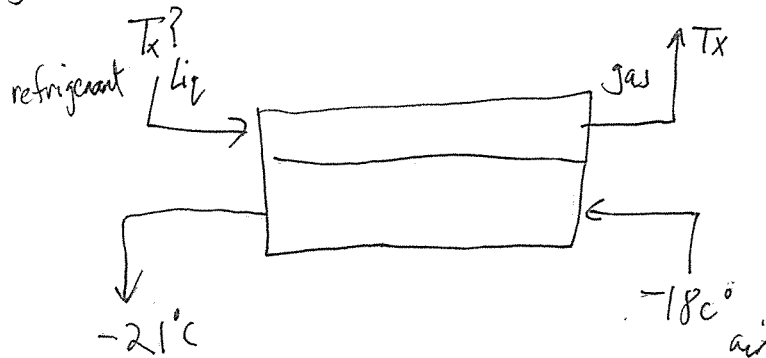
3.3.4 Calculate the required evaporation temperature

$$\phi = UA F_t \theta_{\text{LMTD}} \quad \text{assume } F_t = 1 \text{ (fully counter current)}$$

$$-18.8 = 1.6 \Delta \theta_{\text{LMTD}}$$

$$\Delta \theta_{\text{LMTD}} = -11.75^\circ \text{C}$$

negative because it is being cooled



$$\Delta \theta_{\text{LMTD}} = -11.75^\circ \text{C}$$

Iterate for  $T_x$

$$\frac{[T_x - (-21)] - [T_x - (-18)]}{\ln \left[ \frac{T_x - (-21)}{T_x - (-18)} \right]} = -11.75^\circ \text{C}$$

$$T_x = \underline{\underline{-31.3^\circ \text{C}}} \text{ after some iterations.}$$