## **Department of Chemical Engineering**

## **Major Test in CHL221**

## **Answer all Questions:**

1. The reaction  $2A \rightleftharpoons B+C$  is occurring on a catalyst. The initial rates were measured by conducting the experiments at different pressures. Test whether the data satisfies the surface chemical reaction as the rate controlling step or not.

$$\pi \Rightarrow 1 \quad 1.8 \quad 2.5 \quad 4.0 \quad 7.0 \quad 10.0$$
 $(-\gamma_A) \Rightarrow 1 \quad 1.65 \quad 2.07 \quad 2.56 \quad 3.06 \quad 3.30$ 
(6)

2. The gas phase reaction  $A \rightarrow 4R$  is conducted in a packed bed catalytic reactor. Experiments are conducted with pure A at 25 lit/hr. 3 atm pressure, 120°C with varying amounts of catalyst. From the results given below determine the rate equation. Assume the reaction to be first order. (8)

Expt. No. - 1 2 3 4 5 Cat. Wt (Kg) - 0.025 0.05 0.1 0.15 0.2 
$$C_A(\text{exit})$$
 (mol/lit) - 0.075 0.06 0.045 0.035 0.03

3. Fe $_3$ O $_4$  is reduced to metallic iron by heating with pure H $_2$  at 600°C and 1 atm pressure. The particle dia is 1 cm. Assuming shrinking core model with chemical reaction as rate controlling step determine the time required for 50% conversion of the solid and 50% penetration of the unreacted core.

## Data:

Density of the solid reactant is 4.6gm/cc and molecular weight of Iron is 56.

Frequency factor is 
$$1.95 \times 10^5$$
 cm/s  
Activation energy is 24000 cal/mole. (6)

4.  $CaCO_3$  decomposition is conducted in a TGA and due to power failure only two data points could be obtained. Determine the reaction rate constant from the data given.

dp = 0.74 cm, wt = 0.384 gm  
Heating medium 
$$CO_2 + N_2$$
 mixture having 5%  $CO_2$ . T = 760°C,  
P = 1 atm  
Eq. Partial pressure of  $CO_2$  is given by  
 $Log_{10}p_e = (-8792.3/T) + 10.4022$   
 $p_e = mmHg$ , T = °K  
t (Sec)  $\longrightarrow$  100 - 240  
wt of pellet (gm)  $\longrightarrow$  0.3714 - 0.3515 (6)

5. Lime stone is calcined in a vertical moving bed reactor. The residence time of the solids is 8 min. The particle size distribution in the feed and the time for complete conversion of the particles are,

$$dp(\mu) \rightarrow 100 \quad 200 \quad 400$$
  
 $wt(\%) \rightarrow 40 \quad 30 \quad 30$   
 $t(\min) \rightarrow 5 \quad 10 \quad 20$ 

Determine the conversion of the feed at the exit of the reactor. (6)

6. The following date is obtained from the wicke – kallen bach apparatus.

ZnO pellet weight = 0.75 gm Pellet Dia = 0.78 cm Pellet Thickness = 0.74 cm Density of pure ZnO = 5.42 gm/c.c. Exit flow rate of gas mixture on  $H_2$  gas side = 10.65cc/s Exit flow rate of gas mixture on  $N_2$  gas side = 5.2 c.c./s Partial pressure of  $H_2$  gas on  $N_2$  gas side = 27 mm  $H_2$ Partial pressure of  $H_2$  gas on  $H_2$  gas side = 755 mm  $H_2$ 

Total pressure = 1 atm, Temperature = 
$$25^{\circ}$$
C  $D_{H2-N2}$  =  $0.76 \text{ cm}^2/\text{s}$ 

(i) Determine tortuosity factor (ii) What is the value of the tortuosity factor if equimotal counter current diffusion in the pellet is assumed.

Derive the relevant equations separately. (8)