## Applied Mechanics Department, I Semester 2006-07 AML773 Modelling and Analysis (Fluids) 3-0-0, Majar Test

29-11-06

Time 2 hours, Marks 80

- Derive the von Karman momentum integral equation valid for 2-D incompressible steady Marks laminar/ turbulent boundary layer on flat plate.
  - <71/2>

Obtain Blasius solution, and hence determine the values of u/U,  $\tau_w/\rho U^2$ ,  $\delta/x$ ,  $\delta_1/x$ ,  $\delta_2/x$ .

- <7½>
- Obtain the turbulent boundary layer equations for incompressible steady 2-D flow over a flat <71/2>
  - <71/2>
  - Determine the values of  $\tau_w/\rho U^2$ ,  $\delta/x$ ,  $\delta_1/x$ ,  $\delta_2/x$  for  $1/7^{th}$  power law velocity profile in a 2-D steady incompressible turbulent boundary layer flow.
  - The Reynolds number of a flat plate at zero incidence is  $5 \times 10^6$ . Transition on each surface occurs at 0.4c. The velocity distribution in the laminar part of the boundary layer is given by  $u/U = \sin[(\pi/2).(y/\delta)]$ , whilst in the turbulent part of the layer it fits a power law  $u/U = (y/\delta)^n$  of index n = 1/2. Find the drag eoefficient of the plate (taking both surfaces in to account).
    - Consider fully developed turbulent flow through a smooth pipe. Adopt the notations: distance from the wall  $y = r_o - r$ , diameter  $D = 2r_o$ , friction velocity  $u^* = \sqrt{r_o/\rho}$ , non-dimensional time mean velocity  $u^+ = u/u^*$  and non-dimensional y distance  $y^+ = yu^*/v$ . Flow region consists of viseous sub-layer, buffer-layer and log-law region. The log-law due to von Karman is  $u^+ = \frac{1}{k} \ln y^+ + B$ , where k = 0.41, B = 5.2. The friction law for smooth pipe is expressed in terms of friction factor f given by  $f = \frac{\Delta p D}{\frac{1}{2} \rho \overline{u}^2 L}$ . Assuming that the log law holds on the pipe

axis, and relation  $\frac{u^*}{ii} = \sqrt{\frac{f}{g}}$  holds. Let Re is Reynolds number based on space average velocity.

 $\frac{1}{\sqrt{f}} = 1.99 \log_{10}(\text{Re}\sqrt{f}) - 0.95$ . Obtain the friction law

<13>

A circular orifice of diamete: 80 mm is designed to be fitted at the bottom of a cylindrical tank which is placed with its axis vertical. Water flows in to the tank at a uniform rate and is discharged through the crifice. It is found that it takes 107 s for the water height in the tank to rise from 0.60 m to 0.75 m, and 120 x for it to rise from 1.2 m to 1.28 m. Assume a coefficient of discharge of 0.62 for the orifice.

<10>

Find the rate of inflow and the cross-sectional area of the tank.

a) Derive Euler's equations of motion for an ideal flow.

<5>

b) Derive Euler's equations of motion for an ideal flow along a streamline.

<5>

Air ( $\rho = 1.23 \text{ kg/m}^3$  and  $\nu = 1.5 \times 10^{-5} \text{ m}^2/\text{s}$ ) is flowing over a flat plate. The free stream speed is 15 m/s.

At a distance 1 m from the leading edge, calculate the values of  $\delta(x)$  and  $\tau(x)$  for

a) Completely laminar flow, and

b) Completely turbulent flow for a 1/7th power law velocity profile.

<5> <5>