

**Time : 120 minutes**

**Max. Marks 80**

**(to be scaled down to 40)**

**Note: 1. Use of Steam Tables permitted.**

**2. Draw neat sketch(es), wherever necessary to explain your point.**

**3. Make suitable assumption(s) if necessary, and state the same clearly.**

- 1.(a) (i) Discuss briefly, Principle of Corresponding States: two parameter model.  
(ii) What is acentric factor,  $\omega$ ? What is its relevance?

- (b) Determine vapour pressure of water at 179.82°C and compare the same with the reported value of 10.00 bar at 179.88°C.

For water,  $T_c = 647.1 \text{ K}$   $P_c = 220.55 \text{ bar}$   $\omega = 0.345$

For argon,	$T_c = 150.9 \text{ K}$	$P_c = 48.98 \text{ bar}$	$\omega = 0.0$
$T, \text{K}$	72.65	82.55	87.55
$P^{\text{sat}}, \text{bar}$	0.1333	0.5333	1.0133
			48.98

- (c) Using any method of your choice, determine fugacity of saturated steam at 179.88°C. {(5+5) + 10 + 5)}

2. A tank of 4-m<sup>3</sup> capacity contains 1500 kg water (liquid + vapour in equilibrium with each other) at 250°C. A quantity of 1000 kg of liquid water at 50°C is pumped into the tank. How much heat must be added during this process if the temperature in the tank is not to change? (15)

- 3.(a) Discuss briefly the concept of (i) Carnot Heat Engine and (ii) Carnot refrigerator.

- (b) A Carnot engine is coupled to a Carnot refrigerator so that all of the work produced by the engine is used by the refrigerator in extraction of heat from a heat reservoir at 273.15 K (0°C) at the rate of 35 kW. The source of energy for the Carnot engine is a heat reservoir at 523.15 K (250°C). If both devices discard heat to the surroundings at 298.15 K (25°C), how much heat does the engine absorb from its heat-source reservoir. {(5+5)+5)}

4. (a) Benzene (1) and toluene (2) form ideal solution with each other, such that Raoult's law holds good. Their vapour pressures at a given temperature  $T$  are  $P_1^{\text{sat}}$  and  $P_2^{\text{sat}}$  respectively, and the total pressure is  $P_t$ . Show that

$$x_1 = \frac{P_t - P_2^{\text{sat}}}{P_1^{\text{sat}} - P_2^{\text{sat}}}$$

$$P_t = \frac{1}{\frac{y_1}{P_1^{\text{sat}}} + \frac{y_2}{P_2^{\text{sat}}}}$$

- (b) A binary system of species 1 and 2 consists of vapour and liquid phases in equilibrium at temperature  $T$ , for which

$$\ln \gamma_1 = 1.8 x_2^2 \text{ and } \ln \gamma_2 = 1.8 x_1^2$$

$$P_1^{\text{sat}} = 1.24 \text{ bar}, P_2^{\text{sat}} = 0.89 \text{ bar}$$

- (i) For what range of values of overall mole fraction  $Z_1$  can this two-phase system exist with a liquid phase mole fraction  $x_1 = 0.65$ ?

- (ii) What is the pressure  $P_t$  and vapour mole fraction  $y_1$  within this range?

- (iii) What are the pressure and composition of the azeotrope at temperature  $T$ ?

{(5+(5+5)+5)}