Hame: -

Gr. No.:-

Design a single-pass cross-flow sieve-tray tower for distillation of 70,000 the (Fmax) of a kindry feed containing 2020 by not. of A. The top & bottom products are almost pure. Reflux ratio is 2.5. Every male of feed causes 0.15 mole of incoming Nop. to condense at the few peute. The proof of the top is 3 plif I deal no. of stages are is 22.

- (a) cal. the internal flow rates of liq. and map. at top & bottom in 12 mol was and 18/8. Tabulate results.
- (b) chose / estimate / cal. the tollowing
- vi) no. of actual stages, by, bottom pr., by at top and bottom
- (ii) plate sporting, hole dia, weir height, $\frac{ah}{aa} = 0.09$, $\frac{ad}{ac} = 0.13$, $\frac{ew}{\phi}$
- (iii) Flooding & design velocities, vol. show rate of rapidin tols, col. chin. at top & bottom
- (c) > Do the tollowing cal. at the bottom only
- (i) using single alia. tower, do the weeping check both too Finin & Finax.

 Finin is 0.65 of Finax.
- (i) cal. the fraction of twees to be blanked off arten weeping check fails.
- (iii) cal. dry plate pr. drop (had) when orifice Coeff. = 0.75.

Perputy

1. Mol. wt.

60 20

2. (m.b.p.) normal boiling pt. (cc) 54 96

3.
$$S_L$$
 at its n.b.p. (Kg/m3) 800 980

4. V_L at its n.b.p. (M/m) 0.018 0.06

 $V_R = 750 \left(\frac{L_M}{S_L l_W}\right)^{2/3}$

---eq. (11.85)

A B

 $V_R = K_1 \sqrt{\frac{S_L - S_R}{S_L}} \dots eq. (11.81)$
 $V_R = \frac{L_M}{S_L} \sqrt{\frac{S_L}{S_L}} \dots eq. (11.81)$
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· (i) area restir cure. factor is 1.0, 0.9 + 0.8 for $\frac{a_0}{a_0} = 0.10, 0.08 + 0.06$ respectively.

(ii) \$2 and \$v in 14/m3; Low and Vo in 14/8; up and in 4 up in m/s; lain m; dh in mm; how & hol in mm H20.

Make any remandle assumptions but state them clearly & justify them.