

NATIONAL INSTITUTE OF TECHNOLOGY CALICUT

Test 2 – October 2014

B.Tech Chemical Engineering V Semester

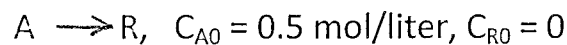
CH3003/CHU312 CHEMICAL REACTION ENGINEERING

Any missing data maybe suitably assumed

Time: 1 hour

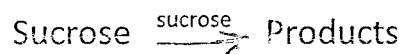
Maxi. Mark : 20

1. The first order reversible liquid reaction (4)



takes place in a batch reactor. After 8 minutes, conversion of A is 33.3% while equilibrium conversion is 66.7%. Find the rate equation for this reaction.

2. At room temperature sucrose is hydrolyzed by the catalytic action of the enzyme sucrose as follows: (5)



Starting with a sucrose concentration  $C_{A0} = 1.0$  millimol/liter and an enzyme concentration  $C_{E0} = 0.01$  millimol/liter, the following kinetic data are obtained in a batch reactor

$C_A$ , millimol/liter	0.84	0.68	0.53	0.38	0.27	0.16	0.09	0.04	0.018	0.006	0.0025
t, hr	1	2	3	4	5	6	7	8	9	10	11

Determine whether these data can be reasonably fitted by a kinetic equation of the Michaelis – Menten type, or

$$-r_A = \frac{k_3 C_A C_{E0}}{C_A + C_M} \quad \text{Where } C_M = \text{Michaelis constant}$$

If the fit is reasonable, evaluate the constants  $k_3$  and  $C_M$ . Solve by the integral method.

3. The following data are obtained at 0°C in a constant-volume batch reactor using pure gaseous A: (5)

Time, min	0	2	4	6	8	10	12	14	$\infty$
Partial Pressure of A, mm	760	600	475	390	320	275	240	215	150

The stoichiometry of the decomposition is  $A \rightarrow 2R$ . Find a rate equation which satisfactorily represents this decomposition. Use differential method of analysis

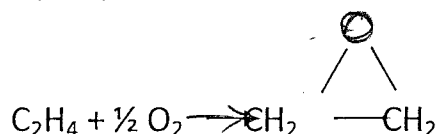
4. Set up a stoichiometry table (column 1: particular species, column 2: number of moles of each species initially present, column 3: the change in number of moles due to reaction, column 4: the number of moles remaining in the system at time t) for each of the following reactions and express the concentration of each species in the reaction as a function of conversion. (Evaluating all constants  $\epsilon$  and  $M$ ,) (6)

(a) The gas-phase pyrolysis



Pure ethane enters the flow reactor at 6 atm and 1100 K.

(b) The catalytic gas – phase oxidation



The feed enters at 6 atm and 260°C and is a stoichiometric mixture of air and Ethylene.

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