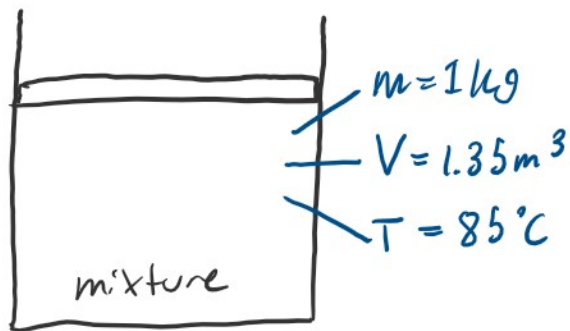
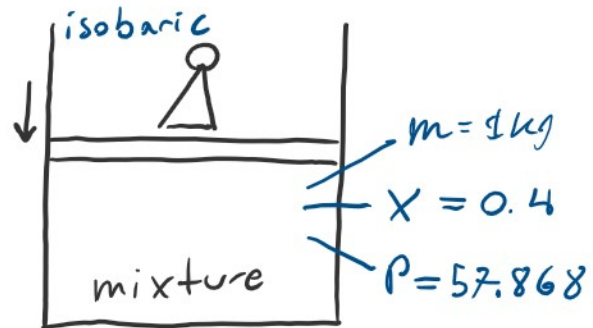


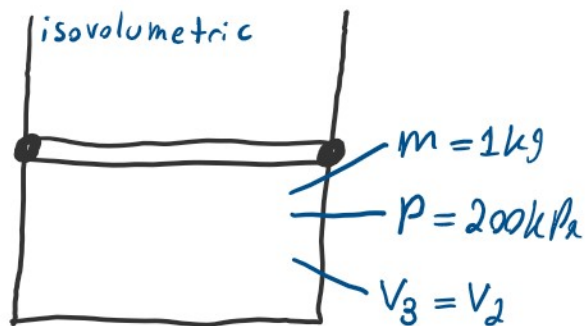
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STATE 1



STATE 2



STATE 3

a) Assume: $V_1 = 1.35 \text{ m}^3/\text{kg}$, $T_1 = 85^\circ\text{C}$

$V_f < V_1 < V_g$ @ T_1 \therefore mixture

$P_1 = P_{\text{sat}} @ T_1 = 57.868 \text{ kPa}$

b) Assume: $P_2 = P_1 = 57.868 \text{ kPa}$, $X = 0.4$

* since $P_2 = P_1$ & state = mixture, $\therefore T_2 = T_1 = 85^\circ\text{C}$

find $V_g @ P_2$ & $V_f @ P_2$

$$\frac{2.2172 - 3.2403}{75 - 50} = \frac{V_g - 3.2403}{57.868 - 50}$$

$$V_g @ P_2 = 2.9183 \text{ m}^3/\text{kg}$$

$$\frac{0.001037 - 0.001030}{75 - 50} = \frac{V_f - 0.001030}{57.868 - 50}$$

$$V_f @ P_2 = 0.001032 \text{ m}^3/\text{kg}$$

$$0.4 = \frac{V_2 - V_f}{V_g - V_f} = \frac{V_2 - 0.001032}{2.9183 - 0.001032}$$

$$\underline{V_2 = 1.16794 \text{ m}^3/\text{kg}}$$

State 3

$$V_3 = V_2 = 1.16794 \text{ m}^3/\text{kg}$$

$$P_3 = 200 \text{ kPa}$$

$$V_3 > V_g @ 200 \text{ kPa} \quad \therefore \underline{\text{superheated}} \\ \underline{\text{vapour}}$$

interpolate for U_3

$$\frac{1.1989 - 1.0805}{2731.4 - 2654.6} = \frac{\overbrace{1.16794}^{V_3} - 1.0805}{U_3 - 2654.6}$$

$$\underline{U_3 = 2711.3178 \text{ kJ/kg}}$$

$$U_1 = U_2 x_1 + (1 - x_1) U_F$$

$$x_1 = \frac{1.35 - 0.001032}{2.8261 - 0.001032} = \underline{0.4775}$$

$$U_1 = (2487.8)(0.4775) + (1 - 0.4775)(355.96)$$

$$\underline{U_1 = 1373.91 \text{ kJ/kg}}$$

$$\Delta U_{31} = 2711.3178 - 1373.91 = \underline{1337.4 \text{ kJ/kg}}$$

constant pressure
↓

← constant volume

$$W_T = W_{21} + W_{32}$$

$$W_T = W_{21} + 0$$

$$W_T = 57.868(1.1679 - 1.35)$$

$$\underline{W_T = -10.538 \text{ kJ/kg}}$$

$$w_T = w_{21} + w_{12}$$

$$w_T = 57.868(1.1679 - 1.35)$$

$$w_T = -10.538 \text{ kJ/kg}$$

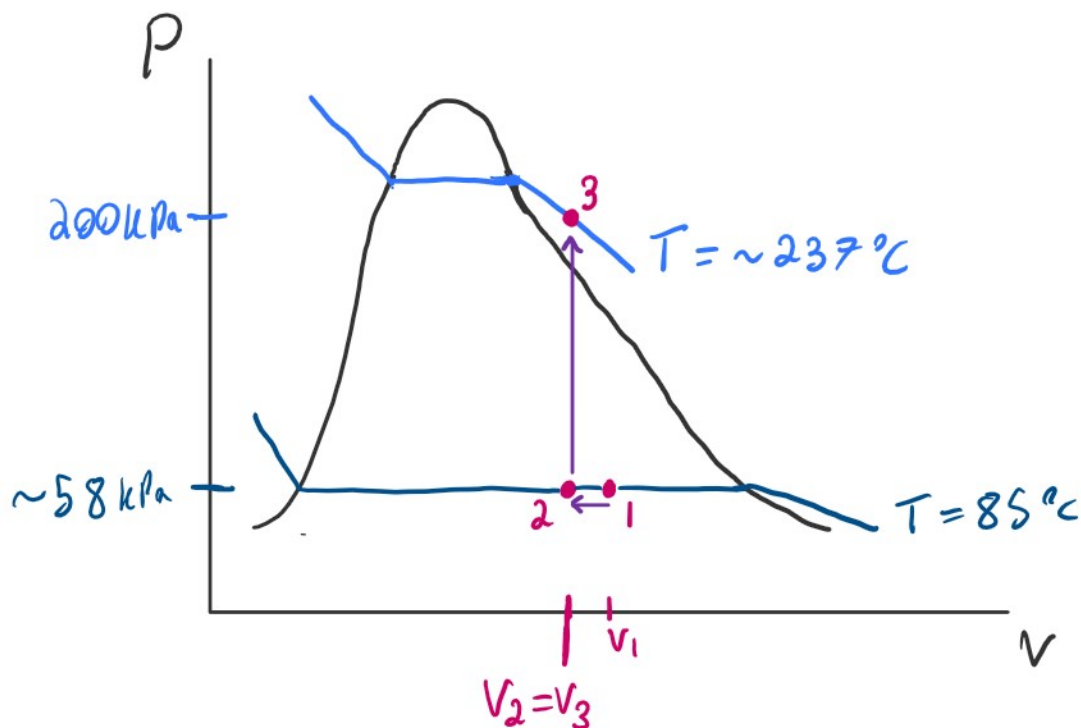
For diagram: interpolate for state 3 temperature

$$\frac{v_{@250^\circ\text{C}} - v_{@200^\circ\text{C}}}{250 - 200} = \frac{v_3 - v_{@200^\circ\text{C}}}{T_3 - 200^\circ\text{C}}$$

$$\frac{1.1989 - 1.0805}{250 - 200} = \frac{1.16794 - 1.0805}{T_3 - 200}$$

$$T_3 = 236.926^\circ\text{C}$$

Diagrams



$$V_2 = V_3$$

V

