TABLE A-1

Atomic or Molecular Weights and Critical Properties of Selected Elements and Compounds

Substance	Chemical Formula	<i>M</i> (kg/kmol)	<i>Т</i> <sub>с</sub> (К)	p <sub>c</sub> (bar)	$Z_c = \frac{p_c v_c}{RT_c}$
Acetylene	$ C_2H_2 $ $ - $ $ NH_3 $	26.04	309	62.8	0.274
Air (equivalent)		28.97	133	37.7	0.284
Ammonia		17.03	406	112.8	0.242
Argon	Ar	39.94	151	48.6	0.290
Benzene	C <sub>6</sub> H <sub>6</sub>	78.11	563	49.3	0.274
Butane	C <sub>4</sub> H <sub>10</sub>	58.12	425	38.0	0.274
Carbon	C	12.01	-	-	-
Carbon dioxide	CO <sub>2</sub>	44.01	304	73.9	0.276
Carbon monoxide	CO	28.01	133	35.0	0.294
Copper	Cu	63.54	-	-	-
Ethane	C₂H <sub>6</sub>	30.07	305	48.8	0.285
Ethanol	C₂H₅OH	46.07	516	63.8	0.249
Ethylene	C <sub>2</sub> H <sub>4</sub>	28.05	283	51.2	0.270
Helium	He	4.003	5.2	2.3	0.300
Hydrogen	H <sub>2</sub>	2.016	33.2	13.0	0.304
Methane	CH <sub>4</sub>	16.04	191	46.4	0.290
Methanol	CH <sub>3</sub> OH	32.04	513	79.5	0.220
Nitrogen	N <sub>2</sub>	28.01	126	33.9	0.291
Octane	$     \begin{array}{c}       C_8 H_{18} \\       O_2 \\       C_3 H_8     \end{array} $	114.22	569	24.9	0.258
Oxygen		32.00	154	50.5	0.290
Propane		44.09	370	42.7	0.276
Propylene	$C_3H_6$ $CCl_2F_2$ $CHClF_2$	42.08	365	46.2	0.276
Refrigerant 12		120.92	385	41.2	0.278
Refrigerant 22		86.48	369	49.8	0.267
Refrigerant 134a	CF <sub>3</sub> CH <sub>2</sub> F	102.03	374	40.7	0.260
Sulfur dioxide	SO <sub>2</sub>	64.06	431	78.7	0.268
Water	H <sub>2</sub> O	18.02	647.3	220.9	0.233

Sources: Adapted from International Critical Tables and L. C. Nelson and E. F. Obert, Generalized Compressibility Charts, Chem. Eng., 61: 203 (1954).

Sources for Tables A-2 through A-18.

Tables A-2 through A-6 are extracted from J. H. Keenan, F. G. Keyes, P. G. Hill, and J. G. Moore, *Steam Tables*, Wiley, New York, 1969.

Tables A-7 through A-9 are calculated based on equations from A. Kamei and S. W. Beyerlein, "A Fundamental Equation for Chlorodifluoromethane (R-22)," *Fluid Phase Equilibria*, Vol. 80, No. 11, 1992, pp. 71–86.

Tables A-10 through A-12 are calculated based on equations from D. P. Wilson and R. S. Basu, "Thermodynamic Properties of a New Stratospherically Safe Working Fluid — Refrigerant 134a," *ASHRAE Trans.*, Vol. 94, Pt. 2, 1988, pp. 2095–2118.

Tables A-13 through A-15 are calculated based on equations from L. Haar and J. S. Gallagher, "Thermodynamic Properties of Ammonia," *J. Phys. Chem. Reference Data*, Vol. 7, 1978, pp. 635–792.

Tables A-16 through A-18 are calculated based on B. A. Younglove and J. F. Ely, "Thermophysical Properties of Fluids. II. Methane, Ethane, Propane, Isobutane and Normal Butane," *J. Phys. Chem. Ref. Data*, Vol. 16, No. 4, 1987, pp. 577–598.

### TABLE A-2

### Properties of Saturated Water (Liquid-Vapor): Temperature Table

		Entr kJ/kg		Enthalpy kJ/kg			Internal kJ/I	c Volume ³/kg		Pa /	ssure Conv ar = 0.1 MF = 10 <sup>2</sup> kP
Tem	Sat. Vapor	Sat. Liquid	Sat. Vapor	Evap.	Sat. Liquid	Sat. Vapor	Sat. Liquid	Sat. Vapor	Sat. Liquid	Press.	Temp.
°C	<b>S</b> g	Sf	h <sub>g</sub>	<b>h</b> fg	h <sub>f</sub>	u <sub>g</sub>	u <sub>f</sub>	$v_{g}$	$v_{\rm f} \times 10^3$	bar	°C
.01	9.1562	0.0000	2501.4	2501.3	0.01	2375.3	0.00	206.136	1.0002	0.00611	.01
4	9.0514	0.0610	2508.7	2491.9	16.78	2380.9	16.77	157.232	1.0001	0.00813	4
5	9.0257	0.0761	2510.6	2489.6	20.98	2382.3	20.97	147.120	1.0001	0.00872	5
6	9.0003	0.0912	2512.4	2487.2	25.20	2383.6	25.19	137.734	1.0001	0.00935	6
8	8.9501	0.1212	2516.1	2482.5	33.60	2386.4	33.59	120.917	1.0002	0.01072	8
10	8.9008	0.1510	2519.8	2477.7	42.01	2389.2	42.00	106.379	1.0004	0.01228	10
11	8.8765	0.1658	2521.6	2475.4	46.20	2390.5	46.20	99.857	1.0004	0.01312	11
12	8.8524	0.1806	2523.4	2473.0	50.41	2391.9	50.41	93.784	1.0005	0.01402	12
13	8.8285	0.1953	2525.3	2470.7	54.60	2393.3	54.60	88.124	1.0007	0.01497	13
14	8.8048	0.2099	2527.1	2468.3	58.80	2394.7	58.79	82.848	1.0008	0.01598	14
15	8.7814	0.2245	2528.9	2465.9	62.99	2396.1	62.99	77.926	1.0009	0.01705	15
16	8.7582	0.2390	2530.8	2463.6	67.19	2397.4	67.18	73.333	1.0011	0.01818	16
17	8.7351	0.2535	2532.6	2461.2	71.38	2398.8	71.38	69.044	1.0012	0.01938	17
18	8.7123	0.2679	2534.4	2458.8	75.58	2400.2	75.57	65.038	1.0014	0.02064	18
19	8.6897	0.2823	2536.2	2456.5	79.77	2401.6	79.76	61.293	1.0016	0.02198	19
20	8.6672	0.2966	2538.1	2454.1	83.96	2402.9	83.95	57.791	1.0018	0.02339	20
21	8.6450	0.3109	2539.9	2451.8	88.14	2404.3	88.14	54.514	1.0020	0.02487	21
22	8.6229	0.3251	2541.7	2449.4	92.33	2405.7	92.32	51.447	1.0022	0.02645	22
23	8.6011	0.3393	2543.5	2447.0	96.52	2407.0	96.51	48.574	1.0024	0.02810	23
24	8.5794	0.3534	2545.4	2444.7	100.70	2408.4	100.70	45.883	1.0027	0.02985	24
25	8.5580	0.3674	2547.2	2442.3	104.89	2409.8	104.88	43.360	1.0029	0.03169	25
26	8.5367	0.3814	2549.0	2439.9	109.07	2411.1	109.06	40.994	1.0032	0.03363	26
27	8.5156	0.3954	2550.8	2437.6	113.25	2412.5	113.25	38.774	1.0035	0.03567	27
28	8.4946	0.4093	2552.6	2435.2	117.43	2413.9	117.42	36.690	1.0037	0.03782	28
29	8.4739	0.4231	2554.5	2432.8	121.61	2415.2	121.60	34.733	1.0040	0.04008	29
30	8.4533	0.4369	2556.3	2430.5	125.79	2416.6	125.78	32.894	1.0043	0.04246	30
31	8.4329	0.4507	2558.1	2428.1	129.97	2418.0	129.96	31.165	1.0046	0.04496	31
32	8.4127	0.4644	2559.9	2425.7	134.15	2419.3	134.14	29.540	1.0050	0.04759	32
33	8.3927	0.4781	2561.7	2423.4	138.33	2420.7	138.32	28.011	1.0053	0.05034	33
34	8.3728	0.4917	2563.5	2421.0	142.50	2422.0	142.50	26.571	1.0056	0.05324	34
35	8.3531	0.5053	2565.3	2418.6	146.68	2423.4	146.67	25.216	1.0060	0.05628	35
36	8.3336	0.5188	2567.1	2416.2	150.86	2424.7	150.85	23.940	1.0063	0.05947	36
38	8.2950	0.5458	2570.7	2411.5	159.21	2427.4	159.20	21.602	1.0071	0.06632	38
40	8.2570	0.5725	2574.3	2406.7	167.57	2430.1	167.56	19.523	1.0078	0.07384	40
45	8.1648	0.6387	2583.2	2394.8	188.45	2436.8	188.44	15.258	1.0099	0.09593	45

 $v_{\rm f}=$  (table value)/1000

270

280

290

300

320

340

360

374.14

54.99

64.12

74.36

85.81

112.7

145.9

186.5

220.9

# TABLE A-2 (Continued)

**Pressure Conversions:** Enthalpy **Specific Volume Internal Energy** Entropy 1 bar = 0.1 MPa m<sup>3</sup>/kg kJ/kg kJ/kg  $kJ/kg \cdot K$  $= 10^2 \text{ kPa}$ Sat. Sat. Sat. Sat. Sat. Sat. Sat. Sat. Liquid Liquid Liquid Evap. Liquid Temp. Press. Vapor Vapor Vapor Vapor Temp. °C  $v_{\rm f} \times 10^3$ °C bar  $u_{\rm f}$  $u_{\rm g}$  $h_{\rm f}$  $h_{\rm fg}$ hg  $\boldsymbol{s}_{\mathrm{f}}$  $oldsymbol{v}_{\mathsf{g}}$ 209.33 50 .1235 209.32 1.0121 12.032 2443.5 2382.7 2592.1 .7038 8.0763 50 230.23 2370.7 55 .1576 1.0146 9.568 230.21 2450.1 2600.9 .7679 7.9913 55 60 .1994 1.0172 7.671 251.11 2456.6 251.13 2358.5 2609.6 .8312 7.9096 60 65 .2503 1.0199 6.197 272.02 2463.1 272.06 2346.2 2618.3 .8935 7.8310 65 70 .3119 1.0228 5.042 292.95 2469.6 292.98 2333.8 2626.8 .9549 7.7553 70 75 .3858 1.0259 4.131 313.90 2475.9 313.93 2321.4 2635.3 1.0155 7.6824 75 80 .4739 1.0291 3.407 334.86 2482.2 334.91 2308.8 2643.7 1.0753 7.6122 80 85 .5783 1.0325 2.828 355.84 2488.4 355.90 2296.0 2651.9 1.1343 7.5445 85 90 .7014 1.0360 2.361 376.85 2494.5 376.92 2283.2 2660.1 1.1925 7.4791 90 95 .8455 1.0397 1.982 397.88 2500.6 397.96 2270.2 2668.1 1.2500 7.4159 95 100 1.014 1.0435 1.673 418.94 2506.5 419.04 2257.0 2676.1 1.3069 7.3549 100 110 1.433 1.0516 1.210 461.14 2518.1 461.30 2230.2 2691.5 1.4185 7.2387 110 503.50 2202.6 2706.3 120 1.985 1.0603 0.8919 2529.3 503.71 1.5276 7.1296 120 130 2.701 1.0697 0.6685 546.02 2539.9 546.31 2174.2 2720.5 1.6344 7.0269 130 140 0.5089 588.74 589.13 2144.7 2733.9 6.9299 3.613 1.0797 2550.0 1.7391 140 150 4.758 1.0905 0.3928 631.68 2559.5 632.20 2114.3 2746.5 1.8418 6.8379 150 2082.6 160 6.178 1.1020 0.3071 674.86 2568.4 675.55 2758.1 1.9427 6.7502 160 170 7,917 718.33 2576.5 719.21 2049.5 2768.7 2.0419 170 1.1143 0.2428 6.6663 2778.2 180 10.02 1.1274 0.1941 762.09 2583.7 763.22 2015.0 2.1396 6.5857 180 190 12.54 1.1414 0.1565 806.19 2590.0 807.62 1978.8 2786.4 2.2359 6.5079 190 200 15.54 0.1274 850.65 2595.3 852.45 1940.7 2793.2 2.3309 200 1.1565 6.4323 210 19.06 1.1726 0.1044 895.53 2599.5 897.76 1900.7 2798.5 2.4248 210 6.3585 220 23.18 1.1900 0.08619 940.87 2602.4 943.62 1858.5 2802.1 2.5178 6.2861 220 230 27.95 1.2088 0.07158 986.74 2603.9 990.12 1813.8 2804.0 2.6099 6.2146 230 240 33.44 1.2291 0.05976 1033.2 2604.0 1037.3 1766.5 2803.8 2.7015 6.1437 240 250 0.05013 1080.4 2602.4 1085.4 1716.2 2801.5 2.7927 6.0730 39.73 1.2512 250 2.8838 1128.4 2599.0 1134.4 2796.6 6.0019 260 46.88 1.2755 0.04221 1662.5 260

 $v_{\rm f} = ({\rm table\ value})/1000$ 

1.3023

1.3321

1.3656

1.4036

1.4988

1.6379

1.8925

3.155

0.03564

0.03017

0.02557

0.02167

0.01549

0.01080

0.006945

0.003155

1177.4

1227.5

1278.9

1332.0

1444.6

1570.3

1725.2

2029.6

2593.7

2586.1

2576.0

2563.0

2525.5

2464.6

2351.5

2029.6

1184.5

1236.0

1289.1

1344.0

1461.5

1594.2

1760.5

2099.3

1605.2

1543.6

1477.1

1404.9

1238.6

1027.9

720.5

0

2789.7

2779.6

2766.2

2749.0

2700.1

2622.0

2481.0

2099.3

2.9751

3.0668

3.1594

3.2534

3.4480

3.6594

3.9147

4.4298

5.9301

5.8571

5.7821

5.7045

5.5362

5.3357

5.0526

4.4298

270

280

290

300

320

340

360

374.14

#### TABLE A-3

# Properties of Saturated Water (Liquid-Vapor): Pressure Table Specific Volume Internal Energy Enthalpy Entropy

ressure Conv	ersions:	Properties o	of Saturated	Water (Liq	uid–Vapo	r): Pressur	e Table				
$bar = 0.1 MF$ $= 10^2 kP$	Pa		Volume /kg		l Energy /kg		Enthalpy kJ/kg			opy g·K	
Press.	Temp.	Sat. Liquid $v_{\rm f}  imes 10^3$	Sat. Vapor $v_{\mathrm{g}}$	Sat. Liquid u <sub>f</sub>	Sat. Vapor u <sub>g</sub>	Sat. Liquid h <sub>f</sub>	Evap.	Sat. Vapor h <sub>g</sub>	Sat. Liquid s <sub>f</sub>	Sat. Vapor s <sub>g</sub>	Press. bar
0.04	28.96	1.0040	34.800	121.45	2415.2	121.46	2432.9	2554.4	0.4226	8.4746	0.04
0.06	36.16	1.0064	23.739	151.53	2425.0	151.53	2415.9	2567.4	0.5210	8.3304	0.06
0.08	41.51	1.0084	18.103	173.87	2432.2	173.88	2403.1	2577.0	0.5926	8.2287	0.08
0.10	45.81	1.0102	14.674	191.82	2437.9	191.83	2392.8	2584.7	0.6493	8.1502	0.10
0.20	60.06	1.0172	7.649	251.38	2456.7	251.40	2358.3	2609.7	0.8320	7.9085	0.20
0.30	69.10	1.0223	5.229	289.20	2468.4	289.23	2336.1	2625.3	0.9439	7.7686	0.30
0.40	75.87	1.0265	3.993	317.53	2477.0	317.58	2319.2	2636.8	1.0259	7.6700	0.40
0.50	81.33	1.0300	3.240	340.44	2483.9	340.49	2305.4	2645.9	1.0910	7.5939	0.50
0.60	85.94	1.0331	2.732	359.79	2489.6	359.86	2293.6	2653.5	1.1453	7.5320	0.60
0.70	89.95	1.0360	2.365	376.63	2494.5	376.70	2283.3	2660.0	1.1919	7.4797	0.70
0.80	93.50	1.0380	2.087	391.58	2498.8	391.66	2274.1	2665.8	1.2329	7.4346	0.80
0.90	96.71	1.0410	1.869	405.06	2502.6	405.15	2265.7	2670.9	1.2695	7.3949	0.90
1.00	99.63	1.0432	1.694	417.36	2506.1	417.46	2258.0	2675.5	1.3026	7.3594	1.00
1.50	111.4	1.0528	1.159	466.94	2519.7	467.11	2226.5	2693.6	1.4336	7.2233	1.50
2.00	120.2	1.0605	0.8857	504.49	2529.5	504.70	2201.9	2706.7	1.5301	7.1271	2.00
2.50	127.4	1.0672	0.7187	535.10	2537.2	535.37	2181.5	2716.9	1.6072	7.0527	2.50
3.00	133.6	1.0732	0.6058	561.15	2543.6	561.47	2163.8	2725.3	1.6718	6.9919	3.00
3.50	138.9	1.0786	0.5243	583.95	2546.9	584.33	2148.1	2732.4	1.7275	6.9405	3.50
4.00	143.6	1.0836	0.4625	604.31	2553.6	604.74	2133.8	2738.6	1.7766	6.8959	4.00
4.50	147.9	1.0882	0.4140	622.25	2557.6	623.25	2120.7	2743.9	1.8207	6.8565	4.50
5.00	151.9	1.0926	0.3749	639.68	2561.2	640.23	2108.5	2748.7	1.8607	6.8212	5.00
6.00	158.9	1.1006	0.3157	669.90	2567.4	670.56	2086.3	2756.8	1.9312	6.7600	6.00
7.00	165.0	1.1080	0.2729	696.44	2572.5	697.22	2066.3	2763.5	1.9922	6.7080	7.00
8.00	170.4	1.1148	0.2404	720.22	2576.8	721.11	2048.0	2769.1	2.0462	6.6628	8.00
9.00	175.4	1.1212	0.2150	741.83	2580.5	742.83	2031.1	2773.9	2.0946	6.6226	9.00
10.0	179.9	1.1273	0.1944	761.68	2583.6	762.81	2015.3	2778.1	2.1387	6.5863	10.0
15.0	198.3	1.1539	0.1318	843.16	2594.5	844.84	1947.3	2792.2	2.3150	6.4448	15.0
20.0	212.4	1.1767	0.09963	906.44	2600.3	908.79	1890.7	2799.5	2.4474	6.3409	20.0
25.0	224.0	1.1973	0.07998	959.11	2603.1	962.11	1841.0	2803.1	2.5547	6.2575	25.0
30.0	233.9	1.2165	0.06668	1004.8	2604.1	1008.4	1795.7	2804.2	2.6457	6.1869	30.0
35.0	242.6	1.2347	0.05707	1045.4	2603.7	1049.8	1753.7	2803.4	2.7253	6.1253	35.0
40.0	250.4	1.2522	0.04978	1082.3	2602.3	1087.3	1714.1	2801.4	2.7964	6.0701	40.0
45.0	257.5	1.2692	0.04406	1116.2	2600.1	1121.9	1676.4	2798.3	2.8610	6.0199	45.0
50.0	264.0	1.2859	0.03944	1147.8	2597.1	1154.2	1640.1	2794.3	2.9202	5.9734	50.0
60.0	275.6	1.3187	0.03244	1205.4	2589.7	1213.4	1571.0	2784.3	3.0267	5.8892	60.0
70.0	285.9	1.3513	0.02737	1257.6	2580.5	1267.0	1505.1	2772.1	3.1211	5.8133	70.0
80.0	295.1	1.3842	0.02352	1305.6	2569.8	1316.6	1441.3	2758.0	3.2068	5.7432	80.0
90.0	303.4	1.4178	0.02048	1350.5	2557.8	1363.3	1378.9	2742.1	3.2858	5.6772	90.0
100.	311.1	1.4524	0.01803	1393.0	2544.4	1407.6	1317.1	2724.7	3.3596	5.6141	100.
110.	318.2	1.4886	0.01599	1433.7	2529.8	1450.1	1255.5	2705.6	3.4295	5.5527	110.

 $v_{\rm f} = \text{(table value)/1000}$ 

sure Conv ur = 0.1 MI = 10 <sup>2</sup> kF	Pa 📗	Specific m <sup>3</sup> ,	Volume /kg		l Energy ′kg	Enthalpy kJ/kg			Entropy kJ/kg·K		
Press.	Temp. °C	Sat. Liquid $v_{ m f}  imes 10^3$	Sat. Vapor $v_{ m g}$	Sat. Liquid <i>u</i> f	Sat. Vapor u <sub>g</sub>	Sat. Liquid <i>h</i> f	Evap. h <sub>fg</sub>	Sat. Vapor h <sub>g</sub>	Sat. Liquid s <sub>f</sub>	Sat. Vapor s <sub>g</sub>	Pres ba
120.	324.8	1.5267	0.01426	1473.0	2513.7	1491.3	1193.6	2684.9	3.4962	5.4924	120
130.	330.9	1.5671	0.01278	1511.1	2496.1	1531.5	1130.7	2662.2	3.5606	5.4323	130
140.	336.8	1.6107	0.01149	1548.6	2476.8	1571.1	1066.5	2637.6	3.6232	5.3717	140
150.	342.2	1.6581	0.01034	1585.6	2455.5	1610.5	1000.0	2610.5	3.6848	5.3098	150
160.	347.4	1.7107	0.009306	1622.7	2431.7	1650.1	930.6	2580.6	3.7461	5.2455	160
170.	352.4	1.7702	0.008364	1660.2	2405.0	1690.3	856.9	2547.2	3.8079	5.1777	170
180.	357.1	1.8397	0.007489	1698.9	2374.3	1732.0	777.1	2509.1	3.8715	5.1044	180
190.	361.5	1.9243	0.006657	1739.9	2338.1	1776.5	688.0	2464.5	3.9388	5.0228	190
200.	365.8	2.036	0.005834	1785.6	2293.0	1826.3	583.4	2409.7	4.0139	4.9269	200
220.9	374.1	3.155	0.003155	2029.6	2029.6	2099.3	0	2099.3	4.4298	4.4298	220

 $v_{\rm f}=$  (table value)/1000  $^{\rm L}$ 

Pressure Conversions: 1 bar = 0.1 MPa = 10<sup>2</sup> kPa

## TABLE A-4

	<b>Properties</b>	of Su	perheated	Water	Vapor
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Piop	erties or	Superne	ated wat	ei vapoi				
T	$\boldsymbol{v}$	и	h	S	v	и	h	S
°C	m <sup>3</sup> /kg	kJ/kg	kJ/kg	kJ/kg · K	m³/kg	kJ/kg	kJ/kg	kJ/kg · K
	p		r = <b>0.006</b>	MPa	р		r = 0.035	MPa
		$(T_{\rm sat} =$	36.16°C)			$(T_{\rm sat} =$	72.69°C)	,
Sat.	23.739	2425.0	2567.4	8.3304	4.526	2473.0	2631.4	7.7158
80	27.132	2487.3	2650.1	8.5804	4.625	2483.7	2645.6	7.7564
120	30.219	2544.7	2726.0	8.7840	5.163	2542.4	2723.1	7.9644
160	22.202	2602.7	2002 5	0.0603	F (0)	2604.2	2000 (	0.4540
160	33.302	2602.7	2802.5	8.9693	5.696	2601.2	2800.6	8.1519
200	36.383	2661.4	2879.7	9.1398	6.228	2660.4	2878.4	8.3237
240	39.462	2721.0	2957.8	9.2982	6.758	2720.3	2956.8	8.4828
280	42.540	2781.5	3036.8	9.4464	7.287	2780.9	3036.0	8.6314
320	45.618	2843.0	3116.7	9.5859	7.815	2842.5	3116.1	8.7712
360	48.696	2905.5	3197.7	9.7180	8.344	2905.1	3197.1	8.9034
400	F4 77/	20/0.0	2270.6	0.0425	0.072	2060.6	2270.2	0.0204
400	51.774	2969.0	3279.6	9.8435	8.872	2968.6	3279.2	9.0291
440	54.851	3033.5	3362.6	9.9633	9.400	3033.2	3362.2	9.1490
500	59.467	3132.3	3489.1	10.1336	10.192	3132.1	3488.8	9.3194
		•	bar = $0.07$ 89.95°C)	MPa	p :		= 0.10 MPa 99.63°C)	3
			r					
Sat.	2.365	2494.5	2660.0	7.4797	1.694	2506.1	2675.5	7.3594
100	2.434	2509.7	2680.0	7.5341	1.696	2506.7	2676.2	7.3614
120	2.571	2539.7	2719.6	7.6375	1.793	2537.3	2716.6	7.4668
160	2.841	2599.4	2798.2	7.8279	1.984	2597.8	2796.2	7.6597
200	3.108	2659.1	2876.7	8.0012	2.172	2658.1	2875.3	7.8343
240	3.374	2719.3	2955.5	8.1611	2.359	2718.5	2954.5	7.9949
200	2 ( ( 0	2700.0	2025.0	0.2462	25//	2770 (	2027.2	0.4//5
280	3.640	2780.2	3035.0	8.3162	2.546	2779.6	3034.2	8.1445
320	3.905	2842.0	3115.3	8.4504	2.732	2841.5	3114.6	8.2849
360	4.170	2904.6	3196.5	8.5828	2.917	2904.2	3195.9	8.4175
400	4.434	2968.2	3278.6	8.7086	3.103	2967.9	3278.2	8.5435
440	4.698	3032.9	3361.8	8.8286	3.288	3032.6	3361.4	8.6636
500	5.095	3131.8	3488.5	8.9991	3.565	3131.6	3488.1	8.8342
		•		'				'
	•••••	p = 1.5 l	bar = 0.15	MPa	<i>p</i> =	= 3.0 bar :	= 0.30 MP	a
		$(T_{\rm sat} =$	111.37°C)			$(T_{\rm sat} =$	133.55°C)	
Sat.	1.159	2519.7	2693.6	7.2233	0.606	2543.6	2725.3	6.9919
120	1.188	2533.3	2711.4	7.2693				
160	1.317	2595.2	2792.8	7.4665	0.651	2587.1	2782.3	7.1276
200	1.444	2656.2	2872.9	7.6433	0.716	2650.7	2865.5	7.3115
240	1.570	2717.2	2952.7	7.8052	0.781	2713.1	2947.3	7.4774
280	1.695	2778.6	3032.8	7.9555	0.844	2775.4	3028.6	7.6299
320	1.819	2840.6	3113.5	8.0964	0.907	2838.1	3110.1	7.7722
360	1.943	2903.5	3195.0	8.2293	0.969	2901.4	3192.2	7.9061
400	2.067	2967.3	3277.4	8.3555	1.032	2965.6	3275.0	8.0330
440	2.191	3032.1	3360.7	8.4757	1.094	3030.6	3358.7	8.1538
500	2.376	3131.2	3487.6	8.6466	1.187	3130.0	3486.0	8.3251
600	2.685	3301.7	3704.3	8.9101	1.341	3300.8	3703.2	8.5892

Pressure Conversions: 1 bar = 0.1 MPa = 10<sup>2</sup> kPa

#### TABLE A-4

#### (Continued)

(COIII	unueu)				 			
<i>T</i> °C	$\frac{v}{m^3/kg}$	u kJ/kg	<i>h</i> kJ/kg	s kJ/kg · K	$\frac{v}{m^3/kg}$	u kJ/kg	<i>h</i> kJ/kg	s kJ/kg · K
•••••		5.0 ba	r = <b>0.50</b> M		 	7.0 ba	r = 0.70 M	
		( <i>T</i> <sub>sat</sub> =	151.86°C)			( <i>T</i> <sub>sat</sub> =	164.97°C)	
Sat.	0.3749	2561.2	2748.7	6.8213	0.2729	2572.5	2763.5	6.7080
180 200	0.4045 0.4249	2609.7 2642.9	2812.0	6.9656	0.2847 0.2999	2599.8 2634.8	2799.1	6.7880
200		2042.9	2855.4	7.0592	0.2999	2034.6	2844.8	6.8865
240	0.4646	2707.6	2939.9	7.2307	0.3292	2701.8	2932.2	7.0641
280 320	0.5034 0.5416	2771.2 2834.7	3022.9 3105.6	7.3865 7.5308	0.3574 0.3852	2766.9 2831.3	3017.1 3100.9	7.2233 7.3697
360 400	0.5796 0.6173	2898.7 2963.2	3188.4 3271.9	7.6660 7.7938	0.4126 0.4397	2895.8 2960.9	3184.7 3268.7	7.5063 7.6350
440	0.6548	3028.6	3356.0	7.9152	0.4667	3026.6	3353.3	7.7571
500	0.7109	3128.4	3483.9	8.0873	0.5070	3126.8	3481.7	7.9299
600	0.8041	3299.6	3701.7	8.3522	0.5738	3298.5	3700.2	8.1956
700	0.8969	3477.5	3925.9	8.5952	0.6403	3476.6	3924.8	8.4391
	p	o = 10.0 ba	ar = 1.0 M	Pa		p = 15.0 b	ar = 1.5 M	Pa
		( <b>7</b> <sub>sat</sub> =	179.91°C)			( <i>T</i> <sub>sat</sub> =	198.32°C)	
Sat.	0.1944	2583.6	2778.1	6.5865	0.1318	2594.5	2792.2	6.4448
200	0.2060	2621.9	2827.9	6.6940	0.1325	2598.1	2796.8	6.4546
240	0.2275	2692.9	2920.4	6.8817	0.1483	2676.9	2899.3	6.6628
280	0.2480	2760.2	3008.2	7.0465	0.1627	2748.6	2992.7	6.8381
320 360	0.2678 0.2873	2826.1 2891.6	3093.9 3178.9	7.1962 7.3349	0.1765 0.1899	2817.1 2884.4	3081.9 3169.2	6.9938 7.1363
400 440	0.3066 0.3257	2957.3 3023.6	3263.9 3349.3	7.4651 7.5883	0.2030 0.2160	2951.3 3018.5	3255.8 3342.5	7.2690 7.3940
500	0.3541	3124.4	3478.5	7.7622	0.2352	3120.3	3473.1	7.5698
540	0.3729	3192.6	3565.6	7.8720	0.2478	3189.1	3560.9	7.6805
600	0.4011	3296.8	3697.9	8.0290	0.2668	3293.9	3694.0	7.8385
640	0.4198	3367.4	3787.2	8.1290	0.2793	3364.8	3783.8	7.9391
	p		ar = 2.0 M	Pa			ar = 3.0 N	
		$(T_{\rm sat} = 1)$	212.42°C)			( <i>T</i> <sub>sat</sub> =	233.90°C)	
Sat.	0.0996	2600.3	2799.5	6.3409	0.0667	2604.1	2804.2	6.1869
240	0.1085	2659.6	2876.5	6.4952	0.0682	2619.7	2824.3	6.2265
280	0.1200	2736.4	2976.4	6.6828	0.0771	2709.9	2941.3	6.4462
320	0.1308	2807.9	3069.5	6.8452	0.0850	2788.4	3043.4	6.6245
360 400	0.1411 0.1512	2877.0 2945.2	3159.3 3247.6	6.9917 7.1271	0.0923 0.0994	2861.7 2932.8	3138.7 3230.9	6.7801 6.9212
440 500	0.1611 0.1757	3013.4 3116.2	3335.5 3467.6	7.2540 7.4317	0.1062 0.1162	3002.9 3108.0	3321.5 3456.5	7.0520 7.2338
540	0.1757	3185.6	3556.1	7.5434	0.1102	3178.4	3546.6	7.2336
600	0.1996	3290.9	3690.1	7.7024	0.1324		3682.3	
640	0.1996	3362.2	3780.4	7.7024	0.1324	3285.0 3357.0	3682.3	7.5085 7.6106
700	0.2232	3470.9	3917.4	7.9487	0.1484	3466.5	3911.7	7.7571

Pressure Conversions: 1 bar = 0.1 MPa  $= 10^2 \text{ kPa}$ 

#### TABLE A-4

	٠.	_							- 1	'n
•	7		n	n	TI	'n	"	o	п	а

(Con	tinued)							
<i>T</i> °C	<i>v</i> m³/kg	u kJ/kg	h	S Id / lange 17	<i>v</i>	U	h	S
			kJ/kg = 4.0 MPa	kJ/kg·K	m <sup>3</sup> /kg	kJ/kg n = 60 ha	kJ/kg r = 6.0 M	kJ/kg·K
	P	$(T_{\rm sat} = 2$					275.64°C)	ı a
Sat.	0.04978	2602.3	2801.4	6.0701	0.03244	2589.7	2784.3	5.8892
280	0.05546	2680.0	2901.8	6.2568	0.03317	2605.2	2804.2	5.9252
320	0.06199	2767.4	3015.4	6.4553	0.03876	2720.0	2952.6	6.1846
360	0.06788	2845.7	3117.2	6.6215	0.04331	2811.2	3071.1	6.3782
400 440	0.07341 0.07872	2919.9	3213.6 3307.1	6.7690	0.04739	2892.9	3177.2	6.5408
		2992.2		6.9041	0.05122	2970.0	3277.3	6.6853
500	0.08643	3099.5	3445.3 3536.9	7.0901	0.05665	3082.2	3422.2	6.8803
540 600	0.09145 0.09885	3171.1 3279.1	3674.4	7.2056 7.3688	0.06015 0.06525	3156.1 3266.9	3517.0 3658.4	6.9999 7.1677
640			3766.6					
700	0.1037 0.1110	3351.8 3462.1	3905.9	7.4720 7.6198	0.06859 0.07352	3341.0 3453.1	3752.6 3894.1	7.2731 7.4234
740	0.1157	3536.6	3999.6	7.7141	0.07677	3528.3	3989.2	7.5190
	p	0 = 80  bar $(T_{\text{sat}} = 2)$	= 8.0 MP 95.06°C)	a	р		r = 10.0 M 311.06°C)	Pa
Sat.	0.02352	2569.8	2758.0	5.7432	0.01803	2544.4	2724.7	5.6141
320	0.02682	2662.7	2877.2	5.9489	0.01925	2588.8	2781.3	5.7103
360	0.03089	2772.7	3019.8	6.1819	0.02331	2729.1	2962.1	6.0060
400	0.03432	2863.8	3138.3	6.3634	0.02641	2832.4	3096.5	6.2120
440	0.03742	2946.7	3246.1	6.5190	0.02911	2922.1	3213.2	6.3805
480	0.04034	3025.7	3348.4	6.6586	0.03160	3005.4	3321.4	6.5282
520	0.04313	3102.7	3447.7	6.7871	0.03394	3085.6	3425.1	6.6622
560 600	0.04582 0.04845	3178.7 3254.4	3545.3 3642.0	6.9072 7.0206	0.03619 0.03837	3164.1 3241.7	3526.0 3625.3	6.7864 6.9029
640 700	0.05102 0.05481	3330.1 3443.9	3738.3 3882.4	7.1283 7.2812	0.04048 0.04358	3318.9 3434.7	3723.7 3870.5	7.0131 7.1687
740	0.05729	3520.4	3978.7	7.3782	0.04560	3512.1	3968.1	7.1667
	p	= 120  bar $(T_{\text{sat}} = 3)$	= 12.0 MI 24.75°C)	Pa	р		r = 14.0 M 336.75°C)	Pa
Sat.	0.01426	2513.7	2684.9	5.4924	0.01149	2476.8	2637.6	5.3717
	0.01420	2678.4		5.8361	0.01422		2816.5	5.6602
400	0.02108	2798.3	3051.3	6.0747	0.01722	2760.9	3001.9	5.9448
440	0.02355	2896.1	3178.7	6.2586	0.01954	2868.6	3142.2	6.1474
480	0.02576	2984.4	3293.5	6.4154	0.02157	2962.5	3264.5	6.3143
520	0.02781	3068.0	3401.8	6.5555	0.02343	3049.8	3377.8	6.4610
560	0.02977	3149.0	3506.2	6.6840	0.02517	3133.6	3486.0	6.5941
600	0.03164	3228.7	3608.3	6.8037	0.02683	3215.4	3591.1	6.7172
640	0.03345	3307.5	3709.0	6.9164	0.02843	3296.0	3694.1	6.8326
700	0.03610	3425.2	3858.4	7.0749	0.03075	3415.7	3846.2	6.9939
740	0.03781	3503.7	3957.4	7.1746	0.03225	3495.2	3946.7	7.0952

**Pressure Conversions:** 1 bar = 0.1 MPa  $= 10^2 \text{ kPa}$ 

#### TABLE A-4

#### (Continued)

(Con	tinuea)							
<i>T</i> °C	$\frac{v}{{ m m}^3/{ m kg}}$	u kJ/kg	<i>h</i> kJ/kg	s kJ/kg · K	$rac{v}{m^3/kg}$	<i>u</i> kJ/kg	<i>h</i> kJ/kg	s kJ/kg · K
•••••		= 160 bar	= 16.0 MF			p = 180 ba	r = 18.0 A	
			47.44°C)				357.06°C)	1
Sat.	0.00931	2431.7	2580.6	5.2455	0.00749	2374.3	2509.1	5.1044
360	0.01105	2539.0	2715.8	5.4614	0.00809		2564.5	5.1922
400	0.01426	2719.4	2947.6	5.8175	0.01190	2672.8	2887.0	5.6887
440	0.01652	2839.4	3103.7	6.0429	0.01414	2808.2	3062.8	5.9428
480	0.01842	2939.7	3234.4	6.2215	0.01596	2915.9	3203.2	6.1345
520	0.02013	3031.1	3353.3	6.3752	0.01757	3011.8	3378.0	6.2960
560	0.02172	3117.8	3465.4	6.5132	0.01904	3101.7	3444.4	6.4392
600	0.02323	3201.8	3573.5	6.6399	0.02042	3188.0	3555.6	6.5696
640	0.02467	3284.2	3678.9	6.7580	0.02174	3272.3	3663.6	6.6905
700	0.02674	3406.0	3833.9	6.9224	0.02362	3396.3	3821.5	6.8580
740	0.02808	3486.7	3935.9	7.0251	0.02483	3478.0	3925.0	6.9623
	a	= 200 bar	= 20.0 M	Pa		o = 240 ba	r = 24.0 N	IPa
		$(T_{\rm sat}=3)$			,			
Sat.	0.00583	2293.0	2409.7	4.9269	***************************************			
400	0.00994	2619.3	2818.1	5.5540	0.00673	2477.8	2639.4	5.2393
440	0.01222	2774.9	3019.4	5.8450	0.00929	2700.6	2923.4	5.6506
480	0.01399	2891.2	3170.8	6.0518	0.01100	2838.3	3102.3	5.8950
520	0.01551	2992.0	3302.2	6.2218	0.01241	2950.5	3248.5	6.0842
560	0.01689	3085.2	3423.0	6.3705	0.01366	3051.1	3379.0	6.2448
600	0.01818	3174.0	3537.6	6.5048	0.01481	3145.2	3500.7	6.3875
640	0.01940	3260.2	3648.1	6.6286	0.01588	3235.5	3616.7	6.5174
700	0.02113	3386.4	3809.0	6.7993	0.01739	3366.4	3783.8	6.6947
740	0.02224	2460.2	2016.1	6.0052	0.01035	2/517	2002.1	6 9029
740 800	0.02224 0.02385	3469.3 3592.7	3914.1 4069.7	6.9052 7.0544	0.01835 0.01974	3451.7 3578.0	3892.1 4051.6	6.8038 6.9567
000	0.02505	3372.1	4007.7	7.0544	0.01774	7570.0	4051.0	0.7507
		200 haw	_ 20 0 14			- 220 ha	- 22 0 N	
		= 280 bar				) = 320 ba	·····	1
400	0.00383	2223.5	2330.7	4.7494	0.00236	1980.4	2055.9	4.3239
440 480	0.00712 0.00885	2613.2 2780.8	2812.6 3028.5	5.4494	0.00544 0.00722	2509.0 2718.1	2683.0 2949.2	5.2327 5.5968
400	0.00665	2/60.6	3026.3	5.7446	0.00722		2949.2	3.3900
520	0.01020	2906.8	3192.3	5.9566	0.00853	2860.7	3133.7	5.8357
560	0.01136	3015.7	3333.7	6.1307	0.00963	2979.0	3287.2	6.0246
600	0.01241	3115.6	3463.0	6.2823	0.01061	3085.3	3424.6	6.1858
640	0.01338	3210.3	3584.8	6.4187	0.01150	3184.5	3552.5	6.3290
700	0.01473	3346.1	3758.4	6.6029	0.01273	3325.4	3732.8	6.5203
740	0.01558	3433.9	3870.0	6.7153	0.01350	3415.9	3847.8	6.6361
800	0.01680	3563.1	4033.4	6.8720	0.01460	3548.0	4015.1	6.7966
900	0.01873	3774.3	4298.8	7.1084	0.01633	3762.7	4285.1	7.0372

Pressure Conversions: 1 bar = 0.1 MPa = 10<sup>2</sup> kPa

TABLE A-5										
Prope	erties of C	Compresse	d Liquid V	<b>V</b> ater						
<i>T</i> °C	$v \times 10^3$ m <sup>3</sup> /kg	u kJ/kg	<i>h</i> kJ/kg	s kJ/kg·K	$v \times 10^3$ m <sup>3</sup> /kg	u kJ/kg	<i>h</i> kJ/kg	s kJ/kg·K		
	III / Kg		r = 2.5  MPa		III / Kg		r = 5.0 MPa			
		•	23.99°C)				263.99°C)	•		
20	1.0006	83.80	86.30	.2961	.9995	83.65	88.65	.2956		
40	1.0067	167.25	169.77	.5715	1.0056	166.95	171.97	.5705		
80	1.0280	334.29	336.86	1.0737	1.0268	333.72	338.85	1.0720		
100	1.0423	418.24	420.85	1.3050	1.0410	417.52	422.72	1.3030		
140	1.0784	587.82	590.52	1.7369	1.0768	586.76	592.15	1.7343		
180	1.1261	761.16	763.97	2.1375	1.1240	759.63	765.25	2.1341		
200	1.1555	849.9	852.8	2.3294	1.1530	848.1	853.9	2.3255		
220	1.1898	940.7	943.7	2.5174	1.1866	938.4	944.4	2.5128		
Sat.	1.1973	959.1	962.1	2.5546	1.2859	1147.8	1154.2	2.9202		
	***************************************	p = 75 bai	r = 7.5 MPa	•••••		p = 100 ba	r = 10.0 MP	'a		
	***************************************	$(T_{\rm sat}=2)$	90.59°C)			( <i>T</i> <sub>sat</sub> = 1	311.06°C)	r		
20	.9984	83.50	90.99	.2950	.9972	83.36	93.33	.2945		
40	1.0045	166.64	174.18	.5696	1.0034	166.35	176.38	.5686		
80	1.0256	333.15	340.84	1.0704	1.0245	332.59	342.83	1.0688		
100	1.0397	416.81	424.62	1.3011	1.0385	416.12	426.50	1.2992		
140	1.0752	585.72	593.78	1.7317	1.0737	584.68	595.42	1.7292		
180	1.1219	758.13	766.55	2.1308	1.1199	756.65	767.84	2.1275		
220	1.1835	936.2	945.1	2.5083	1.1805	934.1	945.9	2.5039		
260 Sat.	1.2696 1.3677	1124.4 1282.0	1134.0 1292.2	2.8763 3.1649	1.2645 1.4524	1121.1 1393.0	1133.7 1407.6	2.8699 3.3596		
Jat.	1.50//	1202.0	1292.2	5.1049	1.4324	1393.0	1407.0	3.3390		
		p = 150  bar		a	ı		r = 20.0 MF	Pa		
		r	42.24°C)				365.81°C)			
20 40	.9950 1.0013	83.06 165.76	97.99 180.78	.2934 .5666	.9928 .9992	82.77 165.17	102.62 185.16	.2923		
80	1.0222	331.48	346.81	1.0656	1.0199	330.40	350.80	1.0624		
100 140	1.0361 1.0707	414.74 582.66	430.28 598.72	1.2955 1.7242	1.0337 1.0678	413.39 580.69	434.06 602.04	1.2917 1.7193		
180	1.1159	753.76	770.50	2.1210	1.1120	750.95	773.20	2.1147		
220	1.1748	929.9	947.5	2.4953	1.1693	925.9	949.3	2.4870		
260	1.2550	1114.6	1133.4	2.8576	1.2462	1108.6	1133.5	2.8459		
300	1.3770	1316.6	1337.3	3.2260	1.3596	1306.1	1333.3	3.2071		
Sat.	1.6581	1585.6	1610.5	3.6848	2.036	1785.6	1826.3	4.0139		
	•••••	n - 250 hs	nr = 25 MPa			n – 300 ha	r = 30.0 MF	 Da		
20	0007	p = 250  Ba	• • • • • • • • • • • • • • • • • • • •							
20 40	.9907 .9971	164.60	107.24 189.52	.2911 .5626	.9886 .9951	82.17 164.04	111.84 193.89	.2899		
100	1.0313	412.08	437.85	1.2881	1.0290	410.78	441.66	1.2844		
200	1.1344	834.5	862.8	2.2961	1.1302	831.4	865.3	2.2893		
300	1.1344	1296.6	1330.2	3.1900	1.3304	1287.9	1327.8	3.1741		
							- 11-			
v = (ta)	ble value)/1	1000		$oldsymbol{v}$	= (table value)/	1000				

TABLE A-6		9			ŀ							
Pressure Conversions: 1 bar = 0.1 MPa = 10 <sup>2</sup> kPa	sions:	Properties of Saturated Volume m <sup>3</sup> /kg		Mater (Sourd-Vapor); Temperature Table Internal Energy KJ/kg	ory: Temperatu Internal Energy kJ/kg	ire lable		Enthalpy kJ/kg			Entropy kJ/kg·K	
Temp.	Pressure kPa	Sat. Solid $v_1 \times 10^3$	Sat. Vapor <sub>Vg</sub>	Sat. Solid u <sub>i</sub>	Subl.	Sat. Vapor u <sub>e</sub>	Sat. Solid h	Subl.	Sat. Vapor h <sub>e</sub>	Sat. Solid Si	Subl. Sig	Sat. Vapor Sg
.01	.6113 .6108 .5176	1.0908 1.0908 1.0904	206.1 206.3 241.7	-333.40 -333.43 -337.62	2708.7 2708.8 2710.2	2375.3 2375.3 2372.6	-333.40 -333.43 -337.62	2834.8 2834.8 2835.3	2501.4 2501.3 2497.7	-1.221 -1.221 -1.237	10.378 10.378 10.456	9.156 9.157 9.219
4 – 6 8 – 8	.4375 .3689 .3102	1.0901 1.0898 1.0894	283.8 334.2 394.4	-341.78 -345.91 -350.02	2711.6 2712.9 2714.2	2369.8 2367.0 2364.2	-341.78 -345.91 -350.02	2835.7 2836.2 2836.6	2494.0 2490.3 2486.6	-1.253 -1.268 -1.284	10.536 10.616 10.698	9.283 9.348 9.414
-10 -12 -14	.2602 .2176 .1815	1.0891 1.0888 1.0884	466.7 553.7 658.8	-354.09 -358.14 -362.15	2715.5 2716.8 2718.0	2361.4 2358.7 2355.9	-354.09 -358.14 -362.15	2837.0 2837.3 2837.6	2482.9 2479.2 2475.5	-1.299 -1.315 -1.331	10.781 10.865 10.950	9.481 9.550 9.619
-16 -18 -20	.1510 .1252 .1035	1.0881 1.0878 1.0874	786.0 940.5 1128.6	-366.14 -370.10 -374.03	2719.2 2720.4 2721.6	2353.1 2350.3 2347.5	-366.14 -370.10 -374.03	2837.9 2838.2 2838.4	2471.8 2468.1 2464.3	-1.346 -1.362 -1.377	11.036 11.123 11.212	9.690 9.762 9.835
-22 -24 -26	.0853	1.0871 1.0868 1.0864	1358.4 1640.1 1986.4	-377.93 -381.80 -385.64	2722.7 2723.7 2724.8	2344.7 2342.0 2339.2	-377.93 -381.80 -385.64	2838.6 2838.7 2838.9	2460.6 2456.9 2453.2	-1.393 -1.408 -1.424	11.302 11.394 11.486	9.909 9.985 10.062
-28 -30 -32	.0469 .0381 .0309	1.0861 1.0858 1.0854	2413.7 2943 3600	-389.45 -393.23 -396.98	2725.8 2726.8 2727.8	2336.4 2333.6 2330.8	-389.45 -393.23 -396.98	2839.0 2839.0 2839.1	2449.5 2445.8 2442.1	-1.439 -1.455 -1.471	11.580 11.676 11.773	10.141 10.221 10.303
-34 -36 -38 -40	.0250 .0201 .0161	1.0851 1.0848 1.0844 1.0841	4419 5444 6731 8354	-400.71 -404.40 -408.06 -411.70	2728.7 2729.6 2730.5 2731.3	2328.0 2325.2 2322.4 2319.6	-400.71 -404.40 -408.06 -411.70	2839.1 2839.1 2839.0 2838.9	2438.4 2434.7 2430.9 2427.2	-1.486 -1.501 -1.517 -1.532	11.872 11.972 12.073 12.176	10.386 10.470 10.556 10.644

v = (table value)/1000