

# CH402 Chemical Engineering Process Design

Class Notes L3

Pumps

# BONUS OP

Chemical Engineering Plebe Open House

22 JAN 2025 1245 to ~1400

Bartlett Hall Room 150<sup>1</sup>

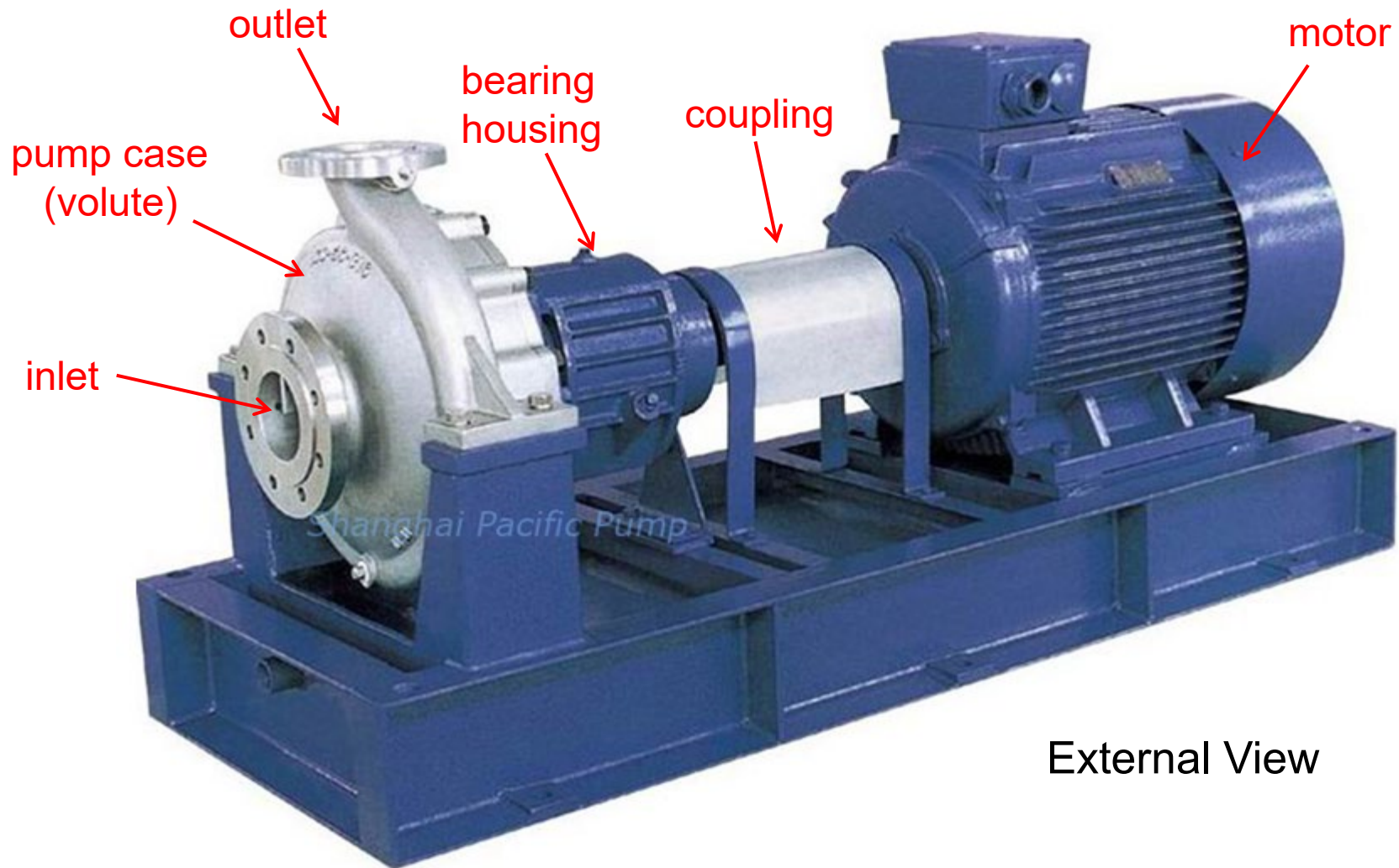
30 minutes = 5 points<sup>2</sup>

Max 1.0 hours (10 points)

## Notes:

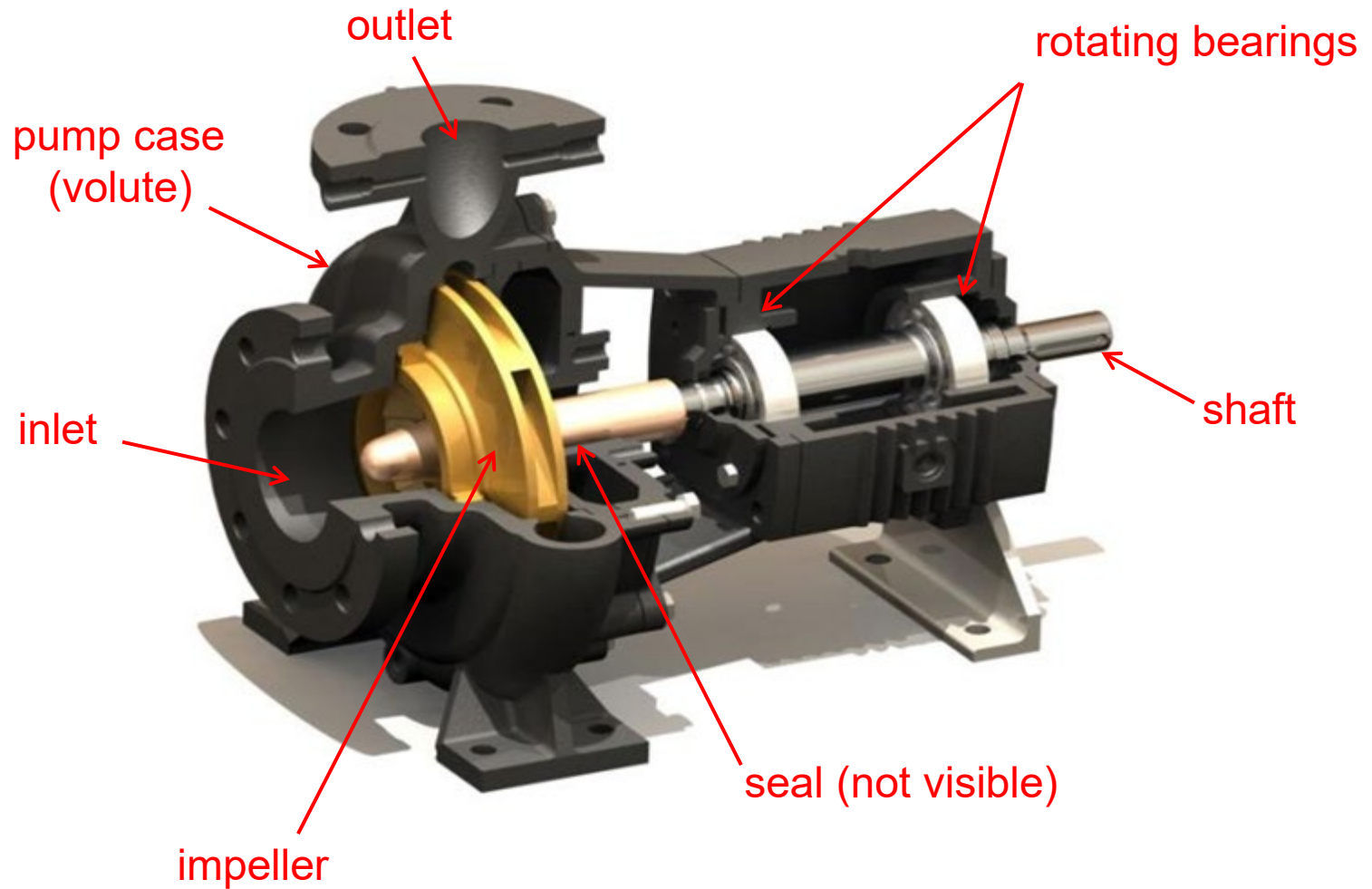
1. If we are moved to a different location, we will still be somewhere near 150.
2. Sign in and out on the provided roster with time in and time out. Interact with prospective cadets. Stay active. Try not to congregate in friend clusters.

# Pump Design Basics



External View

# Pump Design Basics



## Internal View

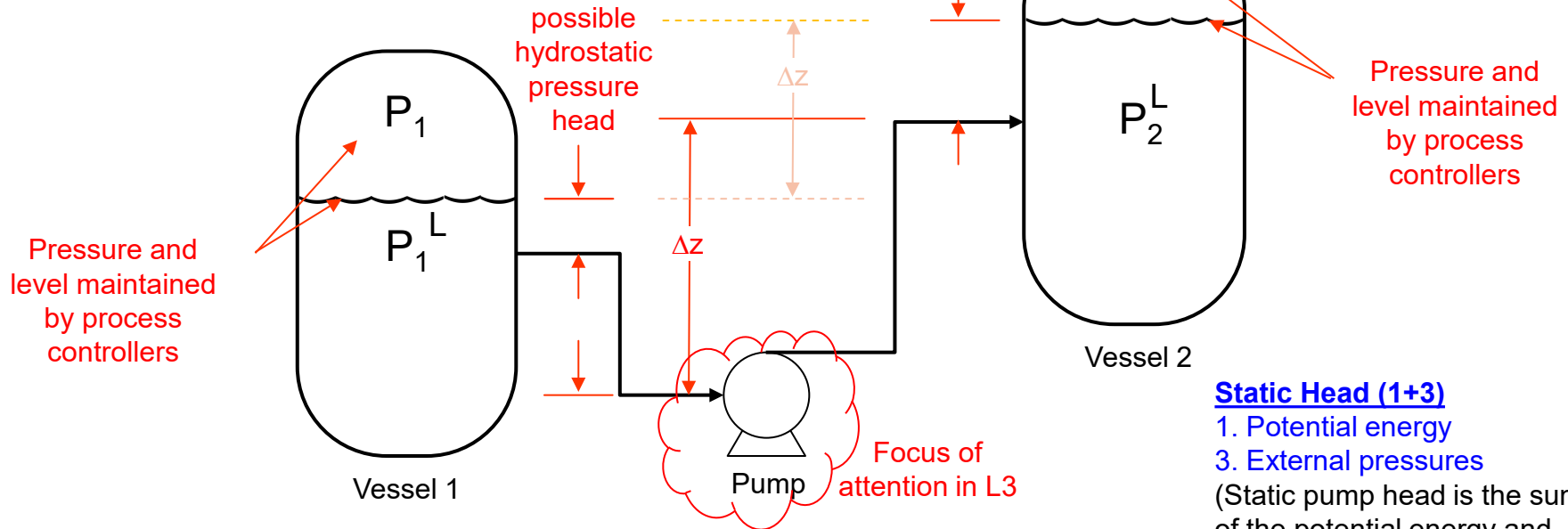
# Pump Overview (Purpose)

Slide 5

If this were reversed and  $P_2^L < P_1^L$ , you might not even need a pump!

$$P_1^L < P_2^L$$

Important Slide for LAB 2



## Static Head (1+3)

1. Potential energy
3. External pressures

(Static pump head is the sum of the potential energy and external pressure difference terms and does not depend on flow rate.)

## Dynamic Head (2+4)

2. Frictional losses
4. Kinetic energy

Dynamic head is the sum of the kinetic energy and frictional loss terms and depends on the flow rate)

- Pump power can be expressed power (W), pressure (Pa), or static pressure equivalent (“total head” or “meters of head”)

$$W_o = \underbrace{g\Delta z}_{(1)} + \underbrace{\Delta\left(\frac{V^2}{2\alpha}\right)}_{(2)} + \underbrace{\frac{\Delta p}{\rho}}_{(3)} + \underbrace{\sum F}_{(4)}$$

- Pump power must be sufficient to overcome changes in elevation, kinetic energy changes, external pressure difference, and frictional losses.
- Pump cost depends on pump power and pump flow rate, then materials & design details.

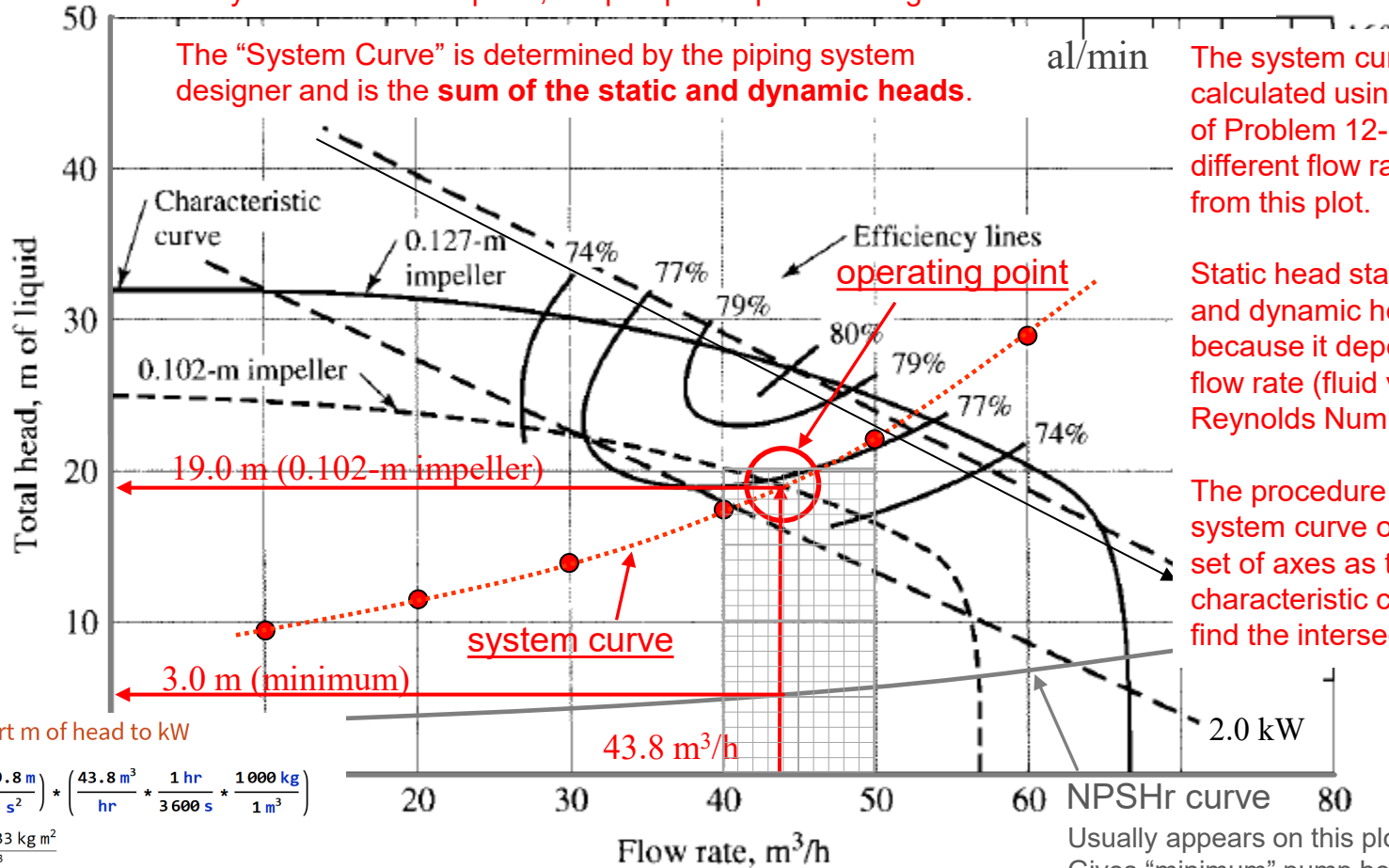
# Pump Performance

## Depends primarily on the “Characteristic Curves”

The characteristic curve is determined by the manufacturer and is a plot of pump head versus flow rate.

Pump head is a combination of input power and friction, internal leakage and recirculation losses.

For any fixed rotational speed, the pump will operate along the characteristic curve.



of a centrifugal pump operating at a constant speed of 3450 r/min

NPSH (Net Positive Suction Head) is the “available” pressure present in the liquid at the entrance to the pump.

# NPSHa Example Calculation

Conditions taken from feed stream in DP2  
 50/50 mol% mixture of toluene and ethylbenzene  
 T = 20 deg C (293 K)  
 P = 101325 Pa

```
In[1]:= a = {76.945, 89.063};
        b = {-6729.8, -7733.7};
        c = {-8.179, -9.917};
        d = {5.3017 * 10-6, 5.986 * 10-6};
        e = {2, 2};
```

```
In[6]:= (*modified Antoine eqn from CHEMCAD*)
```

$$\text{Psat}[T\_] = \text{Exp}\left[a + \frac{b}{T} + c * \text{Log}[T] + d * T^e\right];$$

```
In[7]:= x = {.5, .5};
```

```
In[8]:= P[T_] = Plus @@ (x * Psat[T]);
```

```
P[293.] (*Pa*)
```

```
Out[9]= 1924.14
```

$$\text{In[10]} := \frac{\text{Pa} * \frac{\frac{\text{N}}{\text{m}^2}}{\text{Pa}} * \frac{\frac{\text{kg} * \text{m}}{\text{s}^2}}{\text{N}}}$$

$$\text{Out[10]} = \frac{\text{kg}}{\text{m s}^2}$$

$$(*\Delta P = \rho * g * h \rightarrow h = \Delta P / (\rho * g*)$$

$$\text{In[11]} := \frac{\frac{\text{Pa} * \frac{\frac{\text{N}}{\text{m}^2}}{\text{Pa}} * \frac{\frac{\text{kg} * \text{m}}{\text{s}^2}}{\text{N}}}{\frac{\text{kg}}{\text{m}^3} * \frac{\text{m}}{\text{s}^2}}}$$

```
Out[11]= m
```

$$\text{In[12]} := \frac{101325 - P[293.]}{868.1519 * 9.8}$$

```
Out[12]= 11.6834
```

“available” suction head  
 NPSHa

# Design Procedure for Pumps

Mechanical Energy Balance – Equation 12-12 – Excel, Mathematica, CAD, By-hand  
(same as we used in problem set 1)

Total pressure developed by pump

Total pressure expressed in meters of liquid

$$\frac{\text{m}}{\text{s}^2} \cdot \text{m} = \frac{\text{m}^2}{\text{s}^2}$$

$$\frac{\text{m}^2}{\text{s}^2} \cdot \frac{\text{kg}}{\text{s}} = \frac{\text{kg} \cdot \text{m}^2}{\text{s}^3} = \text{Watts}$$

$$w_0 = \frac{\Delta p}{\rho} = g \cdot H$$

specific work; from eq 12-12

pump work equations on page 515

in eq 12-20a, H in units of Nm/kg

$$\frac{\text{N} \cdot \text{m}}{\text{kg}} = \frac{\text{kg} \cdot \text{m}}{\text{s}^2} \cdot \frac{\text{m}}{\text{kg}} = \frac{\text{m}^2}{\text{s}^2}$$

$$w_0 = \frac{H \cdot \dot{m}_v \cdot \rho}{10^3}$$

$$\underbrace{\frac{\text{N} \cdot \text{m}}{\text{kg}} \cdot \frac{\text{m}^3}{\text{s}} \cdot \frac{\text{kg}}{\text{m}^3}}_{1\text{N} = 1 \frac{\text{kg} \cdot \text{m}}{\text{s}^2}} = \underbrace{\frac{\text{kg} \cdot \text{m}}{\text{s}^2} \cdot \frac{\text{m}}{\text{kg}} \cdot \frac{\text{m}^3}{\text{s}} \cdot \frac{\text{kg}}{\text{m}^3}}_{\text{m}^2/\text{s}^2} = \frac{\text{kg} \cdot \text{m}^2}{\text{s}^3} = \text{Watts}$$

In eq 12-20b, H in units of N/m<sup>2</sup>

Pascals

$$w_0 = \frac{H \cdot \dot{m}_v}{10^3}$$

$$\frac{\text{N}}{\text{m}^2} \cdot \frac{\text{m}^3}{\text{s}} = \frac{\text{N} \cdot \text{m}}{\text{s}} = \frac{\text{J}}{\text{s}} = \text{Watts}$$

Cavitation

$$\text{NPSH} = \frac{1}{g} \cdot \left( \frac{p_{\text{reference}} - p_{\text{vapor}}}{\rho} - h_f \right) - Z_{\text{ref}}$$

Frictional losses

Typically 2-5 m for small pumps  
And up to 15 m for large pumps  
See McCabe, et al, page 204

Efficiency

$$\eta = \frac{w_0}{w}$$

Use Fig. 12-17, page 516

Cost

Use Figs 12-19 through 12-24, pages 517-520; PTW website; CHEMCAD

# Pump Video Links - Watch

multistage  
(1<sup>st</sup> two minutes)

centrifugal  
explained

pump internals

cavitation  
sound

simple piston

pump curve  
(Jacques Chaurette, #2)

cavitation

cavitation  
explained

centrifugal force  
(fantastic demo)

# Questions