

CH365 Chemical Engineering Thermodynamics

Lesson 7

Enthalpy, Heat Capacity, and Open Systems – Part 2

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Measures of Flow

$$\dot{m} = \text{mass flow rate} \left(\frac{\text{kg}}{\text{s}}, \frac{\text{lb}_m}{\text{hr}}, \text{etc.} \right)$$

$$\dot{n} = \text{molar flow rate} \left(\frac{\text{mol}}{\text{s}}, \frac{\text{lbmol}}{\text{s}}, \text{etc.} \right)$$

$$\dot{q} = \text{volumetric flow rate} \left(\frac{\text{m}^3}{\text{s}}, \frac{\text{ft}^3}{\text{min}}, \text{etc.} \right)$$

$$u = \text{velocity} \left(\frac{\text{ft}}{\text{hr}}, \frac{\text{m}}{\text{s}}, \text{etc.} \right)$$

$$\dot{m} = M\dot{n}$$

M = molar mass

$$\text{e.g., } \frac{\text{kg}}{\text{s}} = \frac{\text{kg}}{\text{kmol}} \cdot \frac{\text{kmol}}{\text{s}}$$

$$\dot{m} = uA\rho \quad A = \text{cross-sectional area} = \frac{\pi D^2}{4} \quad \rho = \text{density} = \frac{1}{V} [=] \frac{\text{kg}}{\text{m}^3}$$

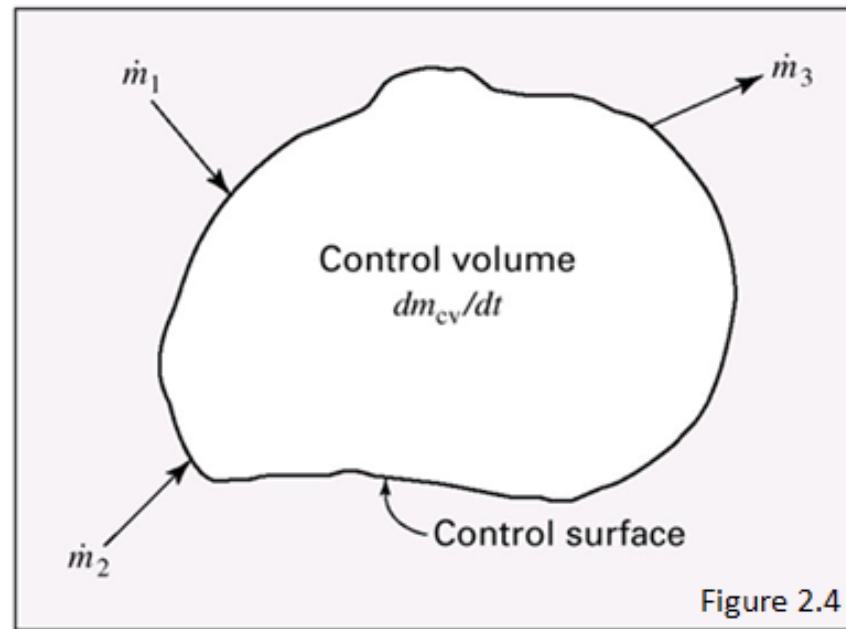
2.23a

$$\dot{n} = uA\rho \cdot \frac{1}{M}$$

$$\text{e.g., } \frac{\text{lb}_m}{\text{sec}} = \frac{\text{ft}}{\text{sec}} \cdot \text{ft}^2 \cdot \frac{\text{lb}_m}{\text{ft}^3}$$

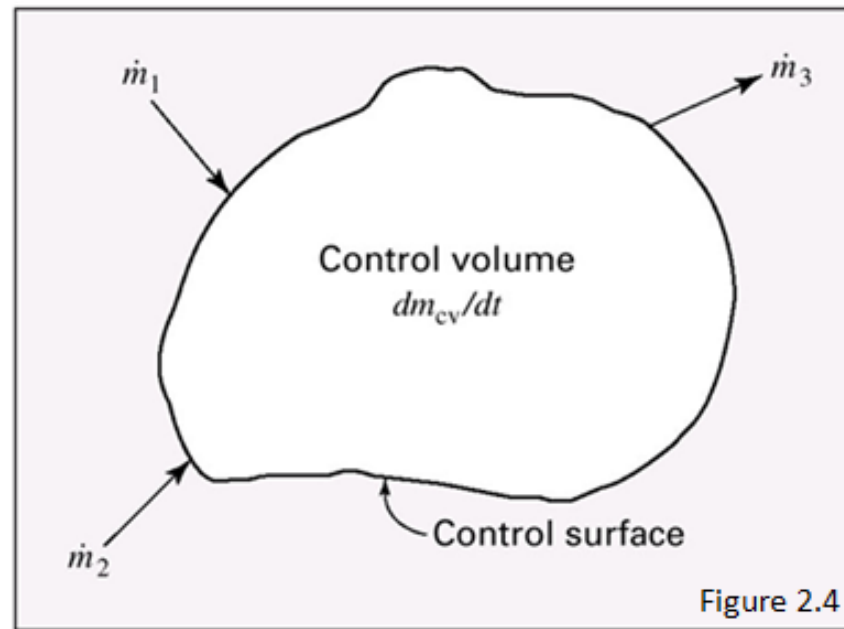
2.23b – M is missing on p. 47

Equation of Continuity



This diagram changes in Figure 2.5 in a very important way.

Mass Balance for Open Systems

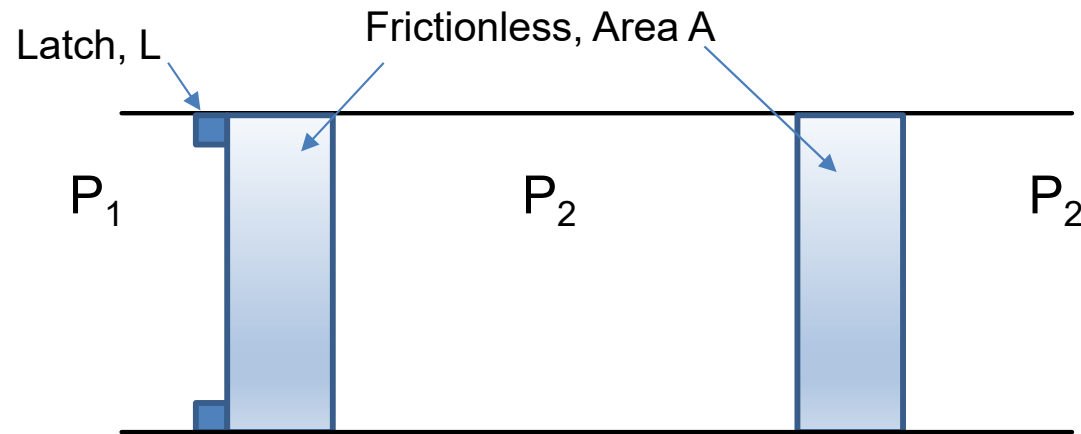


This diagram changes in Figure 2.5 in a very important way with the addition of frictionless pistons, but there is no explanation of this in the textbook.

Frictionless “Double Piston”

Slide 5

Understanding the “pistons” in figure 2.5
Initially at rest, how does the system respond to a push?



Reversible

$$P_2 > P_1$$

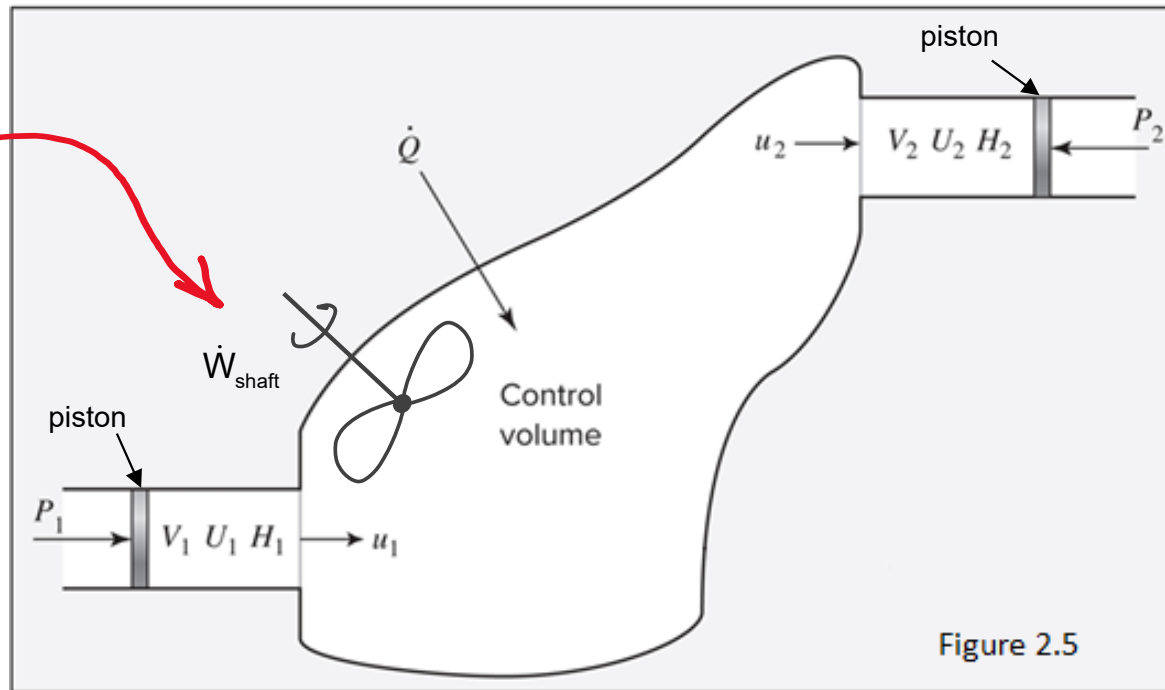
Static equilibrium
(all forces balanced)

General Energy Balance

Slide 6

Shaft work is not illustrated in Figure 2.5 but is used in the equations.

Question: How does the system respond to a “push” on the left-hand piston?



Steady-State Systems

$$\Delta \left[\left(H + \frac{u^2}{2} + gz \right) \dot{m} \right]_{fs} = \dot{Q} + \dot{W}_s$$

2.29

general open system steady-state energy balance

$$\Delta \left(H + \frac{u^2}{2} + gz \right) \dot{m} = \dot{Q} + \dot{W}_s$$

2.30

constant flow open system energy balance (constant density) with one inlet and one outlet.

SI units:
$$\Delta H + \frac{\Delta(u^2)}{2} + g\Delta z = Q + W_s$$

2.31

First law of thermodynamics for steady-state, steady flow, constant density process with one inlet and one outlet

English units:
$$\Delta H + \frac{\Delta(u^2)}{2g_c} + \frac{g}{g_c} \Delta z = Q + W_s$$

all properties are energy per mass

$$\frac{\dot{Q}}{\dot{m}} = Q \quad \frac{\dot{W}_s}{\dot{m}} = W_s$$

$$\Delta H = Q + W_s$$

2.32

Ignoring kinetic and potential energy changes

Problem 2.38

Carbon dioxide gas enters a water-cooled compressor at conditions $P_1 = 15$ (psia) and $T_1 = 50$ (degF), and is discharged at conditions $P_2 = 520$ (psia) and $T_2 = 200$ (degF). The entering CO_2 flows through a 4-inch-diameter pipe with a velocity of 20 (ft) (s)^{-1} , and is discharged through a 1-inch-diameter pipe. The shaft work supplied to the compressor is $5,360 \text{ (Btu) (lb mol)}^{-1}$. What is the heat-transfer rate from the compressor in (Btu) (hr)^{-1} ?

Additional Information:

$$H_1 = 307 \text{ (Btu) (lb}_m\text{)}^{-1} \text{ and } V_1 = 9.25 \text{ (ft)}^3 \text{ (lb}_m\text{)}^{-1}$$

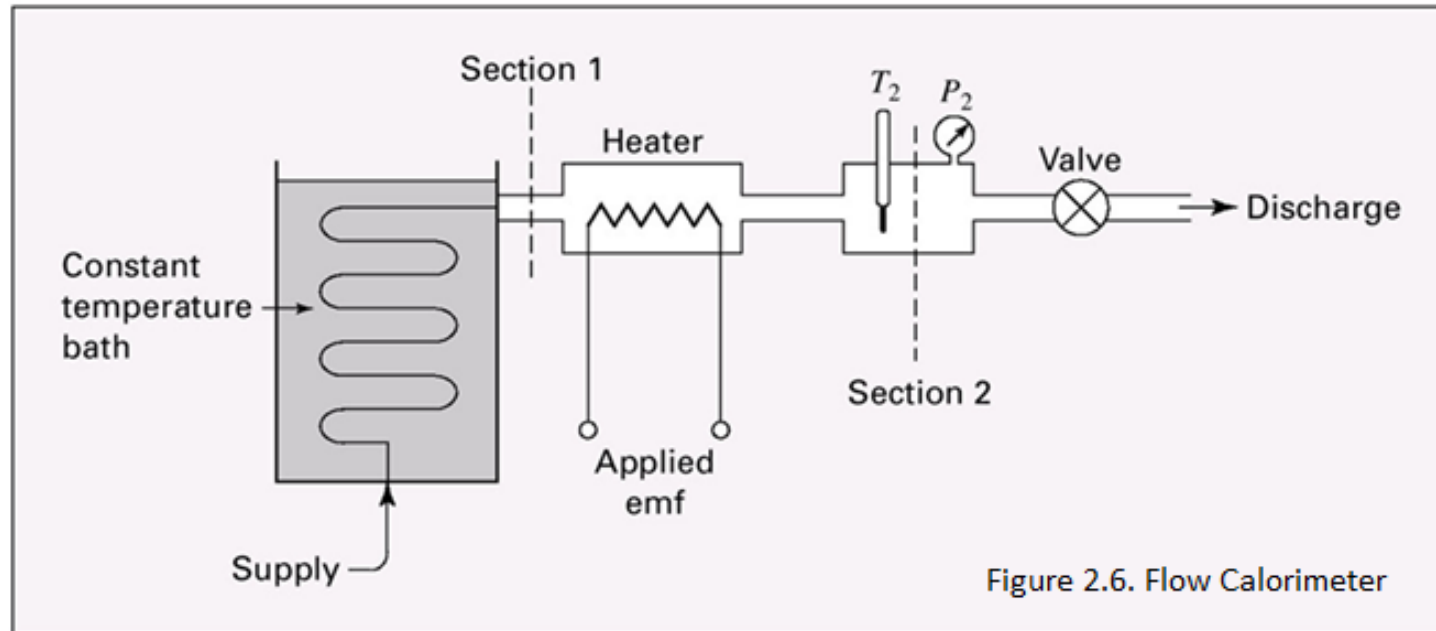
$$H_2 = 330 \text{ (Btu) (lb}_m\text{)}^{-1} \text{ and } V_2 = 0.28 \text{ (ft)}^3 \text{ (lb}_m\text{)}^{-1}$$

Problem 2.28

Nitrogen flows at steady state through a horizontal, insulated pipe with inside diameter of 1.5 (in). A pressure drop results from flow through a partially opened valve. Just upstream from the valve the pressure is 100 (psia), the temperature is 120 (degF), and the average velocity is 20 (ft)(s)^{-1} . If the pressure just downstream from the valve is 20 (psia), what is the temperature? Assume for nitrogen that PV/T is constant, $C_v = (5/2)R$, and $C_p = (7/2)R$. (Values of R are given in App. A.)

Old Slides – Not Used

Flow Calorimeter



Designed for minimum velocity and elevation changes from 1 to 2.

$$\Delta H + \cancel{\frac{\Delta u^2}{2}} + \cancel{g\Delta z} = Q + W_s$$

$$\Delta H = H_2 - H_1 = Q$$

$$\Delta H = H_2 - H_1 = Q$$

$$H_2 = H_1 + Q = 0 + Q$$

Used to generate steam tables.

Example 2.12

For the flow calorimeter in Figure 2.6, the following data are taken with water as the test fluid:

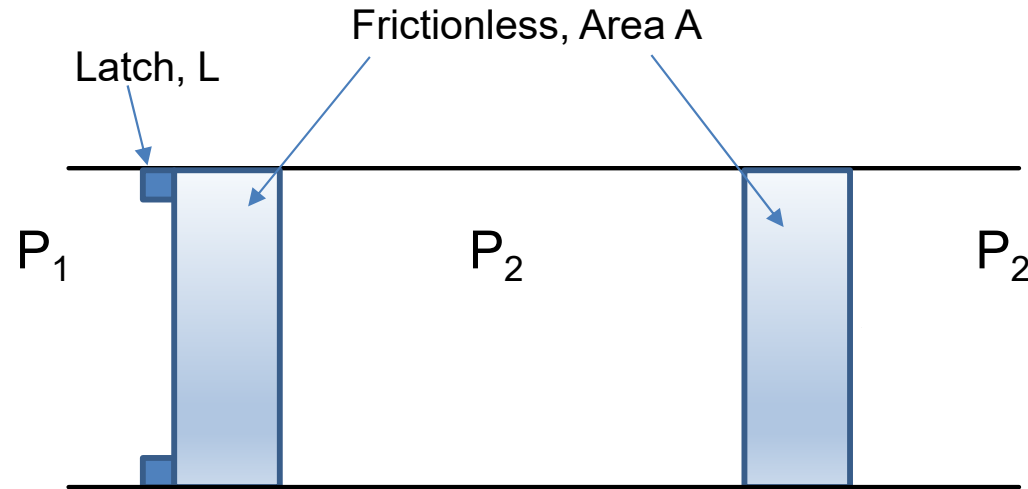
Flow rate = 4.15 g s^{-1} $T_1 = 0 \text{ }^\circ\text{C}$ $T_2 = 300 \text{ }^\circ\text{C}$ $P_2 = 3 \text{ bar}$

Rate of heat addition from resistance heater = $12,740 \text{ W}$.

The water is completely vaporized in the process. Calculate the enthalpy of the steam at $300 \text{ }^\circ\text{C}$ and 3 bar based on $H=0$ for liquid water at $0 \text{ }^\circ\text{C}$.

Frictionless “Double Piston”

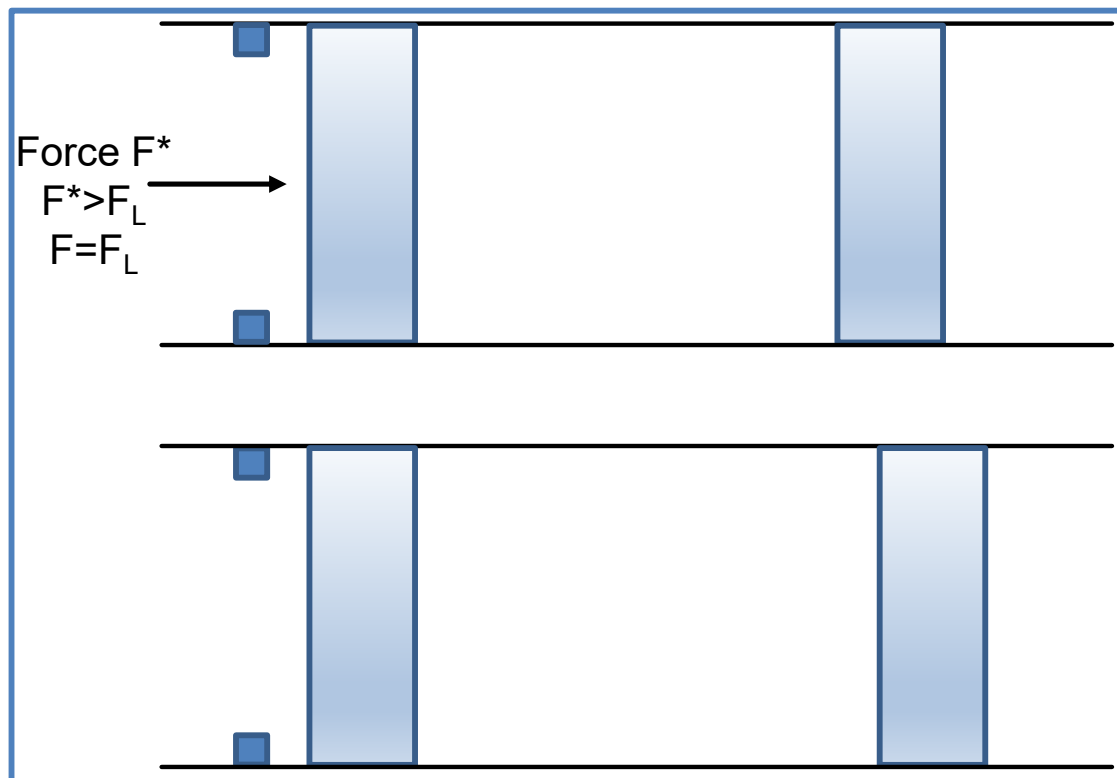
Slide 14



Reversible

$$P_2 > P_1$$

Static equilibrium
(all forces balanced)



General Energy Balance

Slide 15

