# CH402 Chemical Engineering Process Design

Class Notes L3

Pumps

## **BONUS OP**

Chemical Engineering Plebe Open House

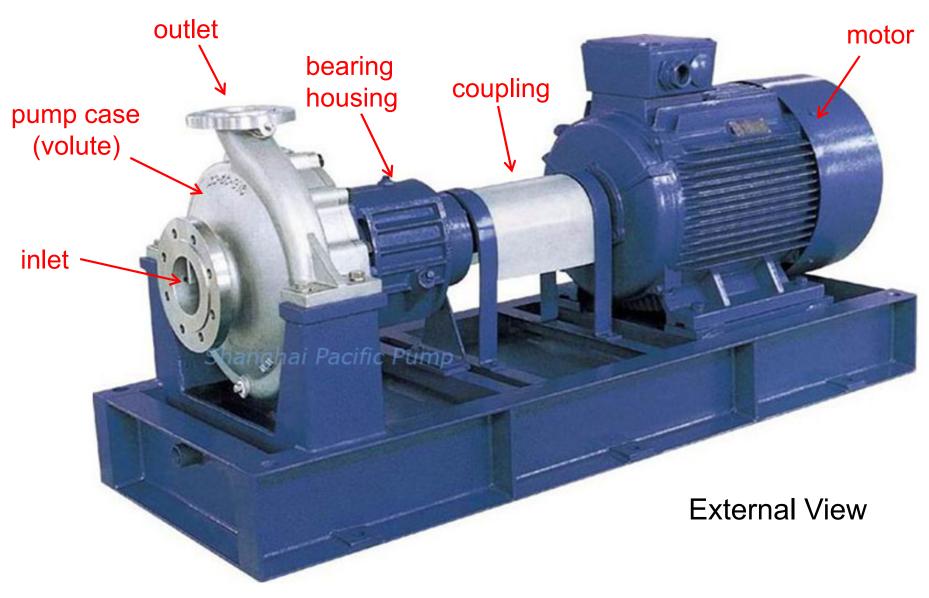
18 JAN 2023 1245 to ~1400 Bartlett Hall Room 150<sup>1</sup>

 $30 \text{ minutes} = 5 \text{ points}^2$ Max 1.5 hours (15 points)

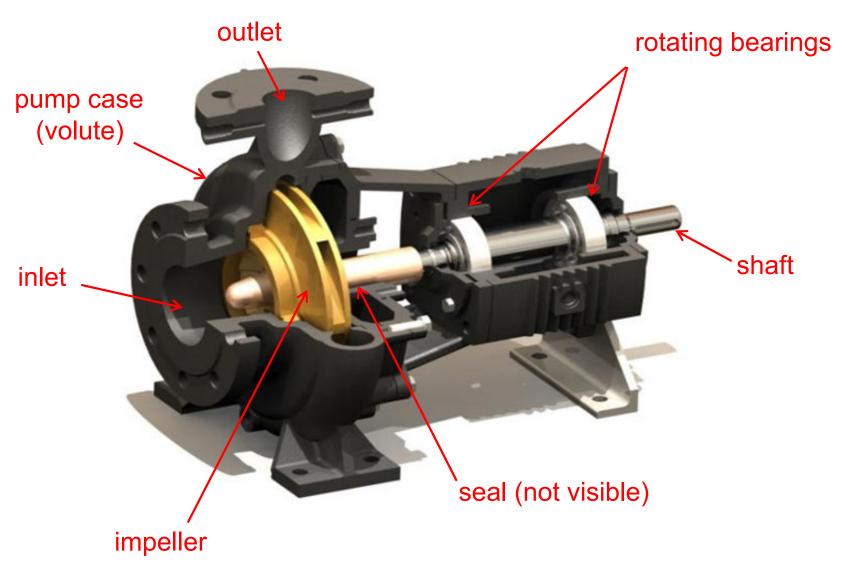
#### Notes:

- 1. If we are moved to a different location, we will still be somewhere near 150.
- 2. Sign in and out on the provided roster with time in and time out. Interact with prospective cadets. Stay active. Try not to congregate in friend clusters.

## Pump Design Basics

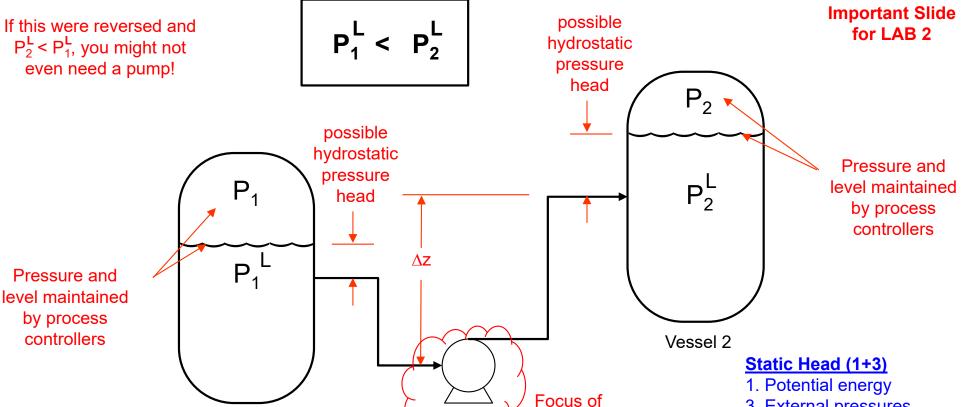


## Pump Design Basics



**Internal View** 

# Pump Overview (Purpose)



$$W_o = g\Delta z + \Delta \left(\frac{V^2}{2\alpha}\right) + \frac{\Delta p}{\rho} + \sum F$$

$$(2)$$

Pump

attention in L3

• Pump power must be sufficient to overcome changes in elevation, kinetic energy changes, external pressure difference, and frictional losses.

Vessel 1

 Pump cost depends on pump power and pump flow rate, then materials & design details.

3. External pressures

(Static pump head is the sum of the potential energy and external pressure difference terms and does not depend on flow rate.)

#### **Dynamic Head (2+4)**

- 2. Frictional losses
- 4. Kinetic energy

Dynamic head is the sum of the kinetic energy and frictional loss terms and depends on the flow rate)

### Pump Performance

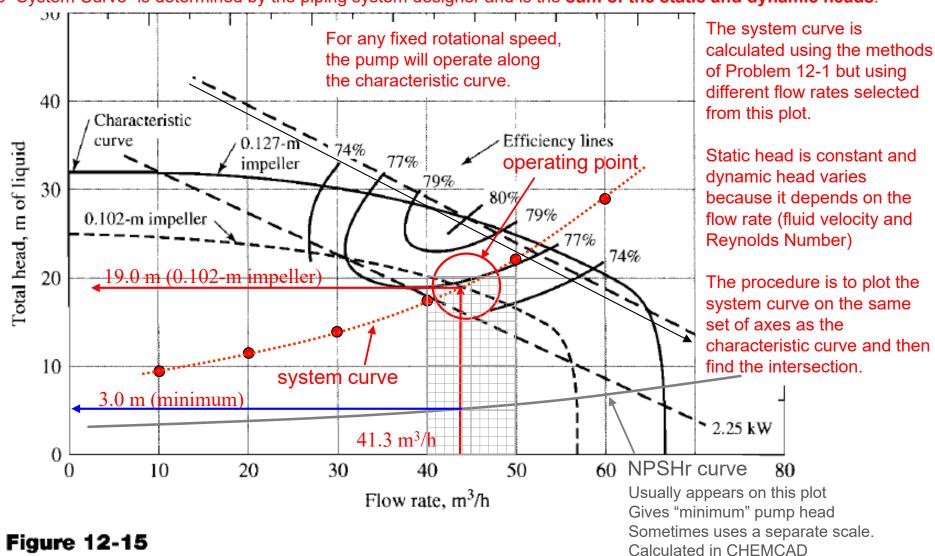
**Important Slide** for LAB 2

#### Depends primarily on the "Characteristic Curves"

The characteristic curve is determined by the manufacturer and is a plot of pump head versus flow rate.

Pump head is a combination of input power and friction, internal leakage and recirculation losses.

The "System Curve" is determined by the piping system designer and is the **sum of the static and dynamic heads**.



Characteristic curve of a centrifugal pump operating at a constant speed of 3450 r/min

NPSH (Net Positive Suction Head) is the "available" pressure present in the liquid at the entrance to the pump.

## NPSHa Example Calculation

Conditions taken from feed stream in DP2

50/50 mol% mixture of toluene and ethylbenzene

T = 20 deg C (293 K)P = 101325 Pa

In[13]:= 
$$Pa * \frac{\frac{N}{m^2}}{Pa} * \frac{\frac{kg*m}{s^2}}{N}$$

Out[13]=  $\frac{kg}{m s^2}$ 
 $(*\rho*g*h*)$ 

In[15]:=  $\frac{\frac{N}{m^2} * \frac{\frac{kg*m}{s^2}}{N}}{\frac{kg}{m^3} * \frac{m}{s^2}}$ 

Out[15]=  $m$ 

In[20]:=  $\frac{101325 - P[293.]}{868.1519*9.8}$ 

Out[20]=  $11.68337623$ 

"available" suction head NPSHa

## Design Procedure for Pumps

Mechanical Energy Balance – Equation 12-12 – Excel, Mathematica, CAD, By-hand (same as we used in problem set 1)

Total pressure developed by pump

$$\frac{\mathbf{m}}{\mathbf{s}^2} \cdot \mathbf{m} = \frac{\mathbf{m}^2}{\mathbf{s}^2}$$

$$\frac{m^2}{s^2} \cdot \frac{kg}{s} = \frac{kg \cdot m^2}{s^3} = Watts$$

Total pressure developed by pump 
$$\frac{m}{s^2} \cdot m = \frac{m^2}{s^2} \qquad \frac{m^2}{s^2} \cdot \frac{kg}{s} = \frac{kg \cdot m^2}{s^3} = \text{Watts} \qquad w_0 = \frac{\Delta p}{\rho} = g \cdot H \text{ specific work; from eq 12-12}$$

pump work equations on page 515

in eq 12-20a, H in units of Nm/kg

$$\frac{\mathbf{N} \cdot \mathbf{m}}{\mathbf{kg}} = \frac{\mathbf{kg} \cdot \mathbf{m}}{\mathbf{s}^2} \cdot \frac{\mathbf{m}}{\mathbf{kg}} = \frac{\mathbf{m}^2}{\mathbf{s}^2}$$

In eq 12-20b,

H in units of N/m<sup>2</sup>

$$\mathbf{w}_0 = \frac{\mathbf{H} \cdot \dot{\mathbf{m}}_{\mathbf{v}} \cdot \mathbf{p}}{10^3}$$

$$\mathbf{w}_0 = \frac{\mathbf{H} \cdot \dot{\mathbf{m}}_{\mathbf{v}}}{10^3}$$

$$\mathbf{w}_{0} = \frac{\mathbf{H} \cdot \dot{\mathbf{m}}_{v} \cdot \boldsymbol{\rho}}{10^{3}} \qquad \underbrace{\frac{N \cdot \mathbf{m}}{kg} \cdot \frac{m^{3}}{s} \cdot \frac{kg}{m^{3}}}_{1N = 1} = \underbrace{\frac{kg \cdot \mathbf{m}}{s^{2}} \cdot \frac{m}{kg}}_{1N = 1} \cdot \underbrace{\frac{kg \cdot \mathbf{m}}{s^{2}} \cdot \frac{kg}{m^{3}}}_{1N = 1} = \underbrace{\frac{kg \cdot \mathbf{m}}{s^{2}}}_{1N = 1} \cdot \underbrace{\frac{kg \cdot \mathbf{m}}{s^{2}}}_{1N = 1} = \underbrace{\frac{k$$

$$\mathbf{W}_0 = \frac{\mathbf{H} \cdot \mathbf{m}_{v}}{10^3} \qquad \frac{\mathbf{N}}{\mathbf{m}^2} \cdot \frac{\mathbf{m}^3}{\mathbf{s}} = \frac{\mathbf{N} \cdot \mathbf{m}}{\mathbf{s}} = \frac{\mathbf{J}}{\mathbf{s}} = \text{Watts}$$

Cavitation

$$NPSH = \frac{1}{g} \cdot \left( \frac{p_{reference} - p_{vapor}}{\rho} - h_f \right) - Z_{ref}$$
 Typically 2-5 m for small pumps And up to 15 m for large pumps See McCabe, et al, page 204

Frictional losses

Efficiency

$$\eta = \frac{W_0}{W}$$

Use Fig. 12-17, page 516

Cost

Use Figs 12-19 through 12-24, pages 517-520; PTW website; CHEMCAD

## Pump Video Links - Watch

multistage (1st two minutes)

centrifugal explained

pump internals

cavitation sound

simple piston

pump curve
(Jacques Chaurette, #2)

cavitation

cavitation explained

centrifugal force (fantastic demo)

## **Homework**

#### PROBLEM SET 2

#### Problem 12-6

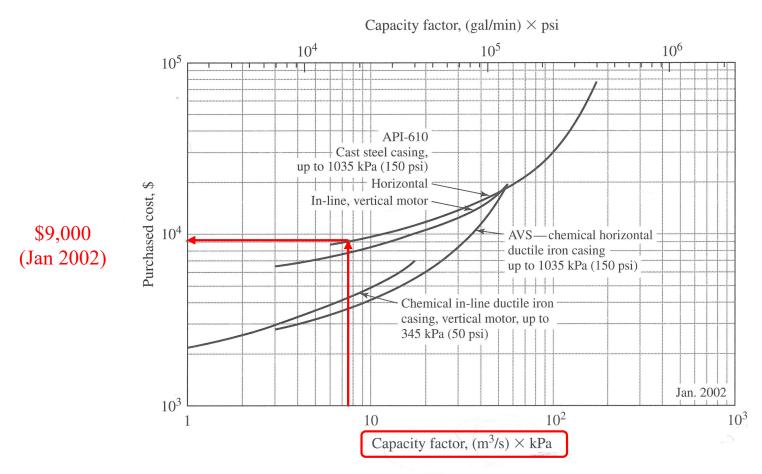
A preliminary estimate of the total cost for a completely installed pumping system is required for a certain design project. In this system, 15.75 kg/s of cooling water at 15.5 °C is to be provided using 305-m pipeline. It has been estimated that the theoretical power requirements for the pump will be 7.5 kW. Using the following data, estimate the total cost of the pumping system:

Material of construction – carbon steel Insulation (85% magnesia) – 0.038 m

Number of fittings (equivalent to tees) – 40 Pump – centrifugal

Number of valves (gate) – 4 Motor – AC, enclosed, 3-phase, 1800 r/min

COST MUST BE PURCHASED INSTALLED COST IN JANUARY 2024



**Figure 12-20**Purchased cost of centrifugal pumps. Price includes electric motor.

## Questions