

CH402 Chemical Engineering Process Design

Class Notes L3

Pumps

BONUS OP

Chemical Engineering Plebe Open House

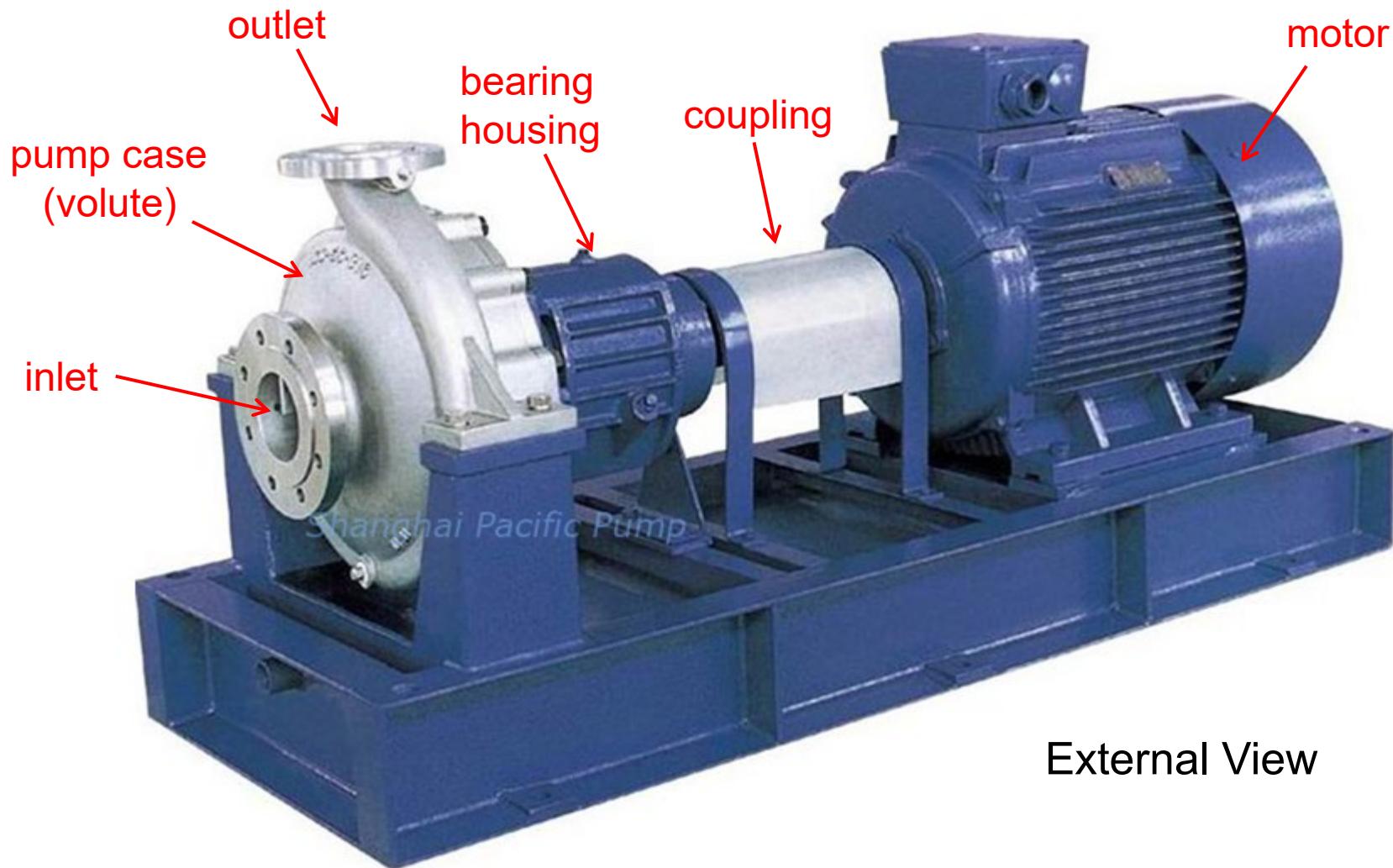
22 JAN 2025 1245 to ~1400
Bartlett Hall Room 150¹

30 minutes = 5 points²
Max 1.0 hours (10 points)

Notes:

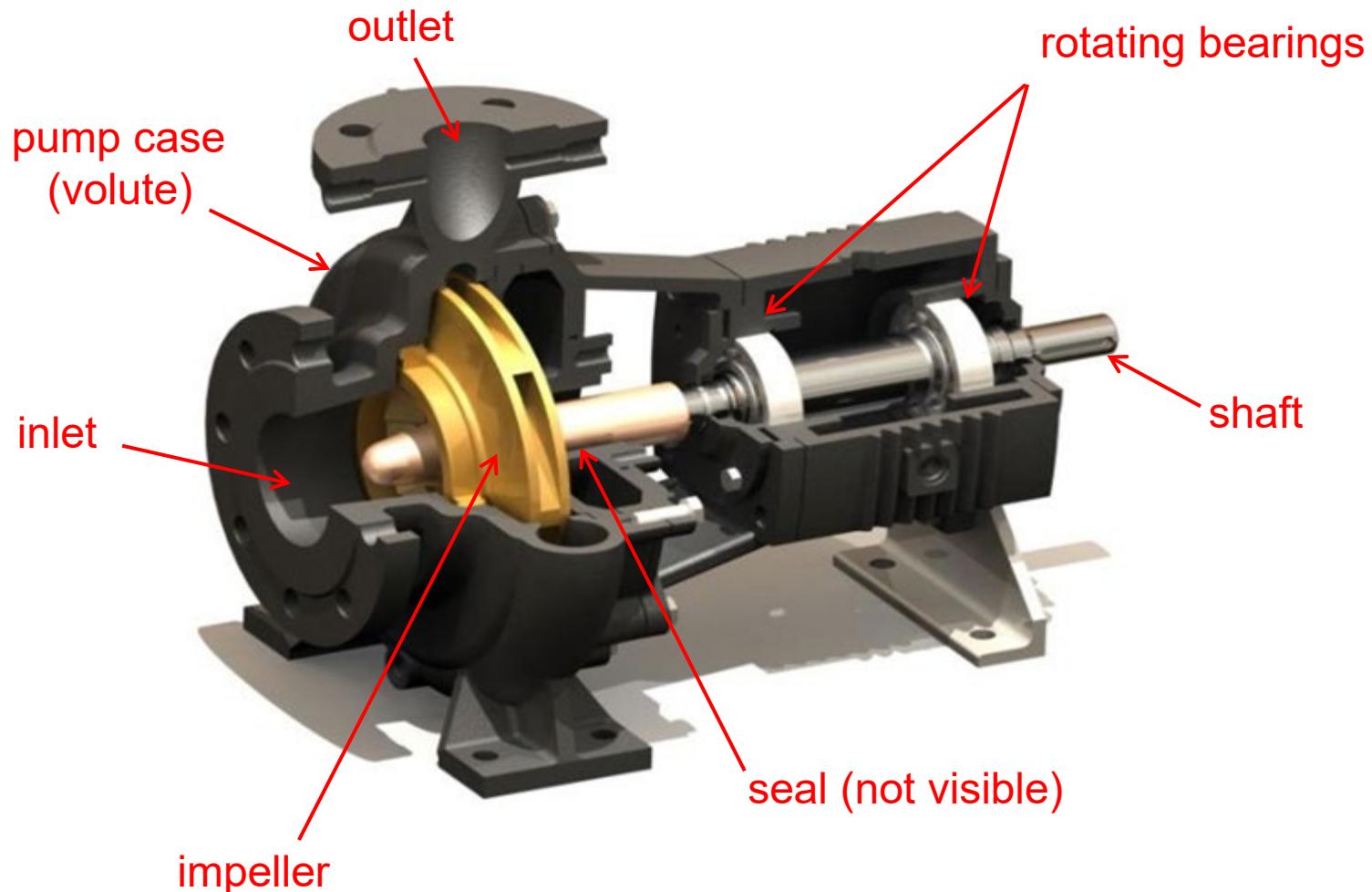
1. If we are moved to a different location, we will still be somewhere near 150.
2. Sign in and out on the provided roster with time in and time out. Interact with prospective cadets. Stay active. Try not to congregate in friend clusters.

Pump Design Basics



External View

Pump Design Basics



Internal View

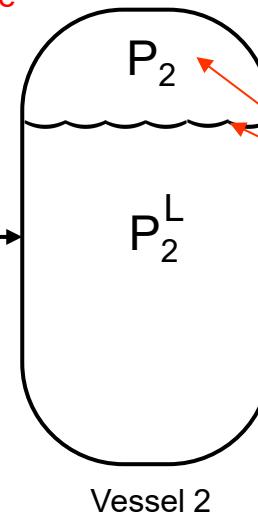
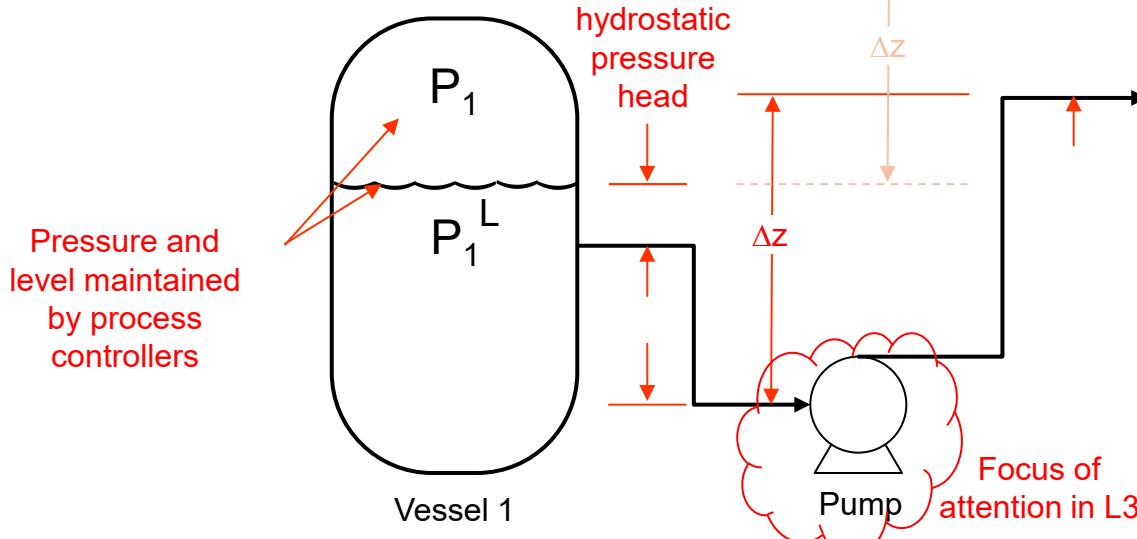
Pump Overview (Purpose)

If this were reversed and $P_2^L < P_1^L$, you might not even need a pump!

$$P_1^L < P_2^L$$

possible hydrostatic pressure head

Important Slide for LAB 2



Pressure and level maintained by process controllers

- Pump power can be expressed power (W), pressure (Pa), or static pressure equivalent ("total head" or "meters of head")

$$W_o = g\Delta z + \Delta\left(\frac{V^2}{2\alpha}\right) + \frac{\Delta p}{\rho} + \sum F$$

① ② ③ ④

- Pump power must be sufficient to overcome changes in elevation, kinetic energy changes, external pressure difference, and frictional losses.
- Pump cost depends on pump power and pump flow rate, then materials & design details.

Static Head (1+3)

- Potential energy
 - External pressures
- (Static pump head is the sum of the potential energy and external pressure difference terms and does not depend on flow rate.)

Dynamic Head (2+4)

- Frictional losses
 - Kinetic energy
- Dynamic head is the sum of the kinetic energy and frictional loss terms and depends on the flow rate)

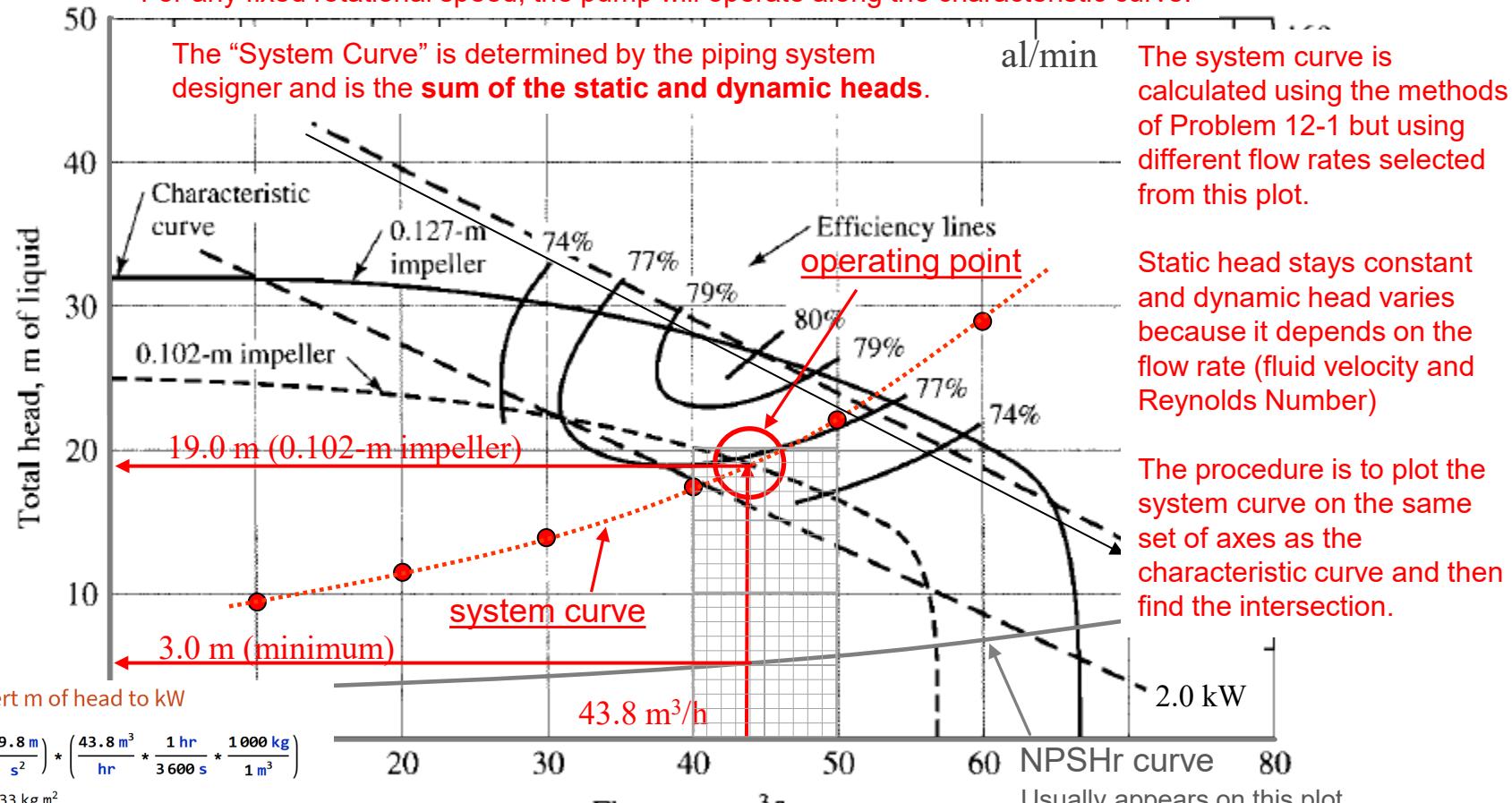
Pump Performance

Depends primarily on the “Characteristic Curves”

The characteristic curve is determined by the manufacturer and is a plot of pump head versus flow rate.

Pump head is a combination of input power and friction, internal leakage and recirculation losses.

For any fixed rotational speed, the pump will operate along the characteristic curve.



of a centrifugal pump operating at a constant speed of 3450 r/min

NPSH (Net Positive Suction Head) is the “available” pressure present in the liquid at the entrance to the pump.

NPSHa Example Calculation

Conditions taken from feed stream in DP2

50/50 mol% mixture of toluene and ethylbenzene

T = 20 deg C (293 K)

P = 101325 Pa

```
In[1]:= a = {76.945, 89.063};
b = {-6729.8, -7733.7};
c = {-8.179, -9.917};
d = {5.3017 * 10-6, 5.986 * 10-6};
e = {2, 2};
```

```
In[6]:= (*modified Antoine eqn from CHEMCAD*)
```

$$P_{sat}[T] = \text{Exp} \left[a + \frac{b}{T} + c * \text{Log}[T] + d * T^e \right];$$

```
In[7]:= x = {.5, .5};
```

```
In[8]:= P[T_] = Plus @@ (x * Psat[T]);
```

$$P[293.] \quad (*\text{Pa}*)$$

```
Out[9]= 1924.14
```

$$\text{In[10]:= } \frac{\text{Pa} * \frac{\text{N}}{\text{m}^2} * \frac{\text{kg} * \text{m}}{\text{s}^2}}{\text{Pa} * \frac{\text{N}}{\text{m}}} \quad \frac{\text{kg}}{\text{m s}^2}$$

$$(*\Delta P = \rho * g * h \rightarrow h = \Delta P / \rho * g*)$$

$$\text{In[11]:= } \frac{\frac{\text{Pa} * \frac{\text{N}}{\text{m}^2} * \frac{\text{kg} * \text{m}}{\text{s}^2}}{\text{Pa} * \frac{\text{N}}{\text{m}}}}{\frac{\text{kg}}{\text{m}^3} * \frac{\text{m}}{\text{s}^2}}$$

```
Out[11]= m
```

$$\text{In[12]:= } \frac{101325 - P[293.]}{868.1519 * 9.8}$$

```
Out[12]= 11.6834
```

“available” suction head
NPSHa

Design Procedure for Pumps

Mechanical Energy Balance – Equation 12-12 – Excel, Mathematica, CAD, By-hand
(same as we used in problem set 1)

Total pressure developed by pump

$$\frac{m}{s^2} \cdot m = \frac{m^2}{s^2}$$

$$\frac{m^2}{s^2} \cdot \frac{kg}{s} = \frac{kg \cdot m^2}{s^3} = \text{Watts}$$

$$w_0 = \frac{\Delta p}{\rho} = g \cdot H$$

Total pressure expressed in meters of liquid
specific work; from eq 12-12

pump work equations on page 515

in eq 12-20a,

H in units of Nm/kg

$$\frac{N \cdot m}{kg} = \frac{kg \cdot m}{s^2} \cdot \frac{m}{kg} = \frac{m^2}{s^2}$$

$$w_0 = \frac{H \cdot \dot{m}_v \cdot \rho}{10^3}$$

$$\frac{\frac{N \cdot m}{kg} \cdot \frac{m^3}{s} \cdot \frac{kg}{m^3}}{10^3} = \frac{kg \cdot m}{s^2} \cdot \frac{m}{kg} \cdot \frac{m^3}{s} \cdot \frac{kg}{m^3} = \frac{kg \cdot m^2}{s^3} = \text{Watts}$$

$\underbrace{1N = 1 \frac{kg \cdot m}{s^2}}$

In eq 12-20b,

H in units of N/m²

Pascals

$$w_0 = \frac{H \cdot \dot{m}_v}{10^3}$$

$$\frac{N \cdot m^3}{m^2 \cdot s} = \frac{N \cdot m}{s} = \frac{J}{s} = \text{Watts}$$

Cavitation

$$NPSH = \frac{1}{g} \cdot \left(\frac{p_{\text{reference}} - p_{\text{vapor}}}{\rho} - h_f \right) - Z_{\text{ref}}$$

Frictional losses

Typically 2-5 m for small pumps
And up to 15 m for large pumps
See McCabe, et al, page 204

Efficiency

$$\eta = \frac{w_0}{w}$$

Use Fig. 12-17, page 516

Cost

Use Figs 12-19 through 12-24, pages 517-520; PTW website; CHEMCAD

Pump Video Links - Watch

multistage
(1st two minutes)

centrifugal
explained

pump internals

cavitation
sound

simple piston

pump curve
(Jacques Chaurette, #2)

cavitation

cavitation
explained

centrifugal force
(fantastic demo)

Questions