

CADET \_\_\_\_\_ SECTION \_\_\_\_\_ TIME OF DEPARTURE \_\_\_\_\_

DEPARTMENT OF CHEMISTRY & LIFE SCIENCE

CH365 2022-2023

WRITTEN PARTIAL REVIEW III

17 November 2022, A-Hour

TEXT: Smith, Van Ness, & Abbott

SCOPE: Lessons 22-32

TIME: 55 Minutes

References Permitted: Open notes, book, internet, CHEMCAD, Mathematica, Excel.

**INSTRUCTIONS**

1. Do not mark this exam or open it until “begin work” is given.
2. You have 55 minutes to complete the exam.
3. Solve the problems in the space provided. Show all work to receive full credit.
4. There are 3 problems on 3 pages in this exam (not including the cover page). Write your name on the top of each sheet.
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6. Save all electronic work to your SharePoint directory.
7. Write the file name and file location on the exam.

(TOTAL WEIGHT: 200 POINTS)

DO NOT WRITE IN THIS SPACE

PROBLEM	VALUE	CUT
A	40	
B	100	
C	60	
TOTAL CUT		
TOTAL GRADE	200	

Problem:    Weight:  
A                    40

Use Table C.1 on page 669 of the textbook with gas constant  $R=8.314 \text{ J}/(\text{mol}\cdot\text{K})$  to calculate  $\Delta H^{\text{ig}}$  and  $\Delta S^{\text{ig}}$  for *ideal* gas-phase n-butane being compressed and heated from 298.15 K and 1 bar to 900 K and 30 bar. Report your answers for  $\Delta H^{\text{ig}}$  and  $\Delta S^{\text{ig}}$  in J/mol and J/(mol·K), respectively.

**Solution:**

$$p = 30.00; (*\text{bar}*)$$

$$t = 900.; (*\text{K}*)$$

$$R = 8.314;$$

$$a = 1.935;$$

$$b = 36.915 * 10^{-3};$$

$$c = -11.402 * 10^{-6};$$

$$C_p = a + b * T + c * T^2;$$

$$(*\text{enthalpy}*)$$

$$H_{\text{ig}} = R * \int_{298.15}^t C_p dT (*\text{eq 2.21}*)$$

$$(*\text{entropy}*)$$

$$S_{\text{ig}} = R * \left( \int_{298.15}^t \frac{C_p}{T} dT - \text{Log} \left[ \frac{p}{1} \right] \right) (*\text{eq 5.10}*)$$

$$\text{Out}[8] = \frac{98142.1944246}{\text{ANS, } \Delta H_{\text{ig}}} \text{ J/mol}$$

$$\text{Out}[9] = \frac{140.031463151}{\text{ANS, } \Delta S_{\text{ig}}} \text{ J}/(\text{mol}\cdot\text{K})$$

<u>Problem:</u>	<u>Weight:</u>
B	100

Use the Peng-Robinson equation of state to calculate the compressibility, residual enthalpy, and residual entropy ( $Z$ ,  $H^R$ , and  $S^R$ ) for n-butane at 900 K and 30 bar.

Use Table B.1 on page 663 of the textbook for critical constants and acentric factor. Use gas constant  $R=8.314 \text{ J}/(\text{mol}\cdot\text{K})$ . Report your answers for  $H^R$  and  $S^R$  in  $\text{J}/\text{mol}$  and  $\text{J}/(\text{mol}\cdot\text{K})$ , respectively.

**Solution:**

```

In[21]:= (*Table B.1, p.663*)
tc = 425.1; (*K*)
pc = 37.96; (*bar*)
ω = 0.200;

(*Reduced t and p*)
tr = t / tc; pr = p / pc;

(*Table 3.1 page 100*)
ε = 1 - √2; σ = 1 + √2; Ω = 0.07780; Ψ = 0.45724;
α[x_] = (1 + (0.37464 + 1.54226 * ω - 0.26992 * ω^2) * (1 - √x))^2;

β = Ω * pr / tr; (*eq 3.50*)
q[x_] =  $\frac{\Psi * \alpha[x]}{\Omega * x}$ ; (*eq 3.51*)

eq1 = Z == 1 + β - q[tr] * β *  $\frac{Z - \beta}{(Z + \epsilon * \beta) * (Z + \sigma * \beta)}$ ; (*eq 3.48*)
ans = Quiet[Solve[eq1, Z, Reals]];
Z1 = Z /. ans[[1]];
I =  $\frac{1}{\sigma - \epsilon} * \text{Log}\left[\frac{Z1 + \sigma * \beta}{Z1 + \epsilon * \beta}\right]$ ; (*eq 13.72*)
Hr[x_] = (Z1 - 1 + x * ∂xq[x] * I) * R * t; (*13.75*)
Sr[x_] = (Log[Z1 - β] + (q[x] + x * ∂xq[x]) * I) * R; (*13.76*)

```

```
In[34]:= Z1
         Hr[tr]
         Sr[tr]
```

Out[34]= 0.99314832986  
ANS, Z

Out[35]= -736.617362747 J/mol  
ANS. H<sup>R</sup>

Out[36]= -0.749348425478 J/(mol·K)  
ANS, S<sup>R</sup>

Problem: Weight:  
C 60

- (a) Using your results from Problems A and B and Table C.4 on page 671 of the textbook, calculate the total real-gas enthalpy and entropy for n-butane at 900 K and 30 bar. Report your answers for H and S in J/mol and J/(mol·K), respectively.
- (b) Use CHEMCAD and the CHEMCAD file in your SharePoint directory calculate the enthalpy and entropy for n-butane at 900 K and 30 (same conditions as in Problem C.a).
- (c) Give three reasons for the difference between the answers in C.a and C.b.

**Solution, part (a):**

$$\Delta H_{fo} = -125\,790;$$

$$\Delta G_{fo} = -16\,570;$$

$$\Delta S_{fo} = \frac{\Delta H_{fo} - \Delta G_{fo}}{298.15};$$

$$H = \Delta H_{fo} + H_{ig} + H_r[\text{tr}] \quad (*6.50*)$$

$$S = \Delta S_{fo} + S_{ig} + S_r[\text{tr}] \quad (*6.51*)$$

$$\text{Out[29]} = -28\,384.4229382 \quad \text{J/mol //ANS}$$

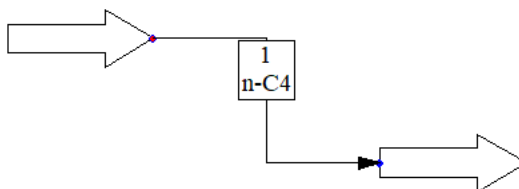
ANS, H

$$\text{Out[30]} = -227.04356027 \quad \text{J/(mol·K) //ANS}$$

ANS, S

**Solution, part (b):**

Stream No.	1
Name	n-C4
-- Overall --	
Temp K	900.0000
Pres bar	30.0000
Enth J/sec	-27152. //ANS
Molar flow mol/sec	1.0000
Entropy J/K/sec	-224.6 //ANS



**Solution, part (c):**

The answers are different because of the following: (1) different heat capacity polynomial, (2) different  $T_c$ ,  $P_c$ , and  $\omega$ , and (3) different standard-state enthalpy and entropy of formation. //ANS

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PROBLEM	VALUE	CUT
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TOTAL CUT		
TOTAL GRADE	200	

Problem:    Weight:  
A                    40

Use Table C.1 on page 669 of the textbook with gas constant  $R=8.314 \text{ J/(mol}\cdot\text{K)}$  to calculate  $\Delta H^{\text{ig}}$  and  $\Delta S^{\text{ig}}$  for *ideal* gas-phase n-pentane being compressed and heated from 298.15 K and 1 bar to 800 K and 40 bar. Report your answers in J/mol and J/(mol·K).

**Solution:**

$$p = 40.00; \text{ (*bar*)}$$

$$t = 800.; \text{ (*K*)}$$

$$R = 8.314;$$

$$a = 2.464;$$

$$b = 45.351 \times 10^{-3};$$

$$c = -14.111 \times 10^{-6};$$

$$C_p = a + b \cdot T + c \cdot T^2;$$

$$\text{(*enthalpy*)}$$

$$H_{\text{ig}} = R \cdot \int_{298.15}^t C_p \, dT \text{ (*eq 2.21*)}$$

$$\text{(*entropy*)}$$

$$S_{\text{ig}} = R \cdot \left( \int_{298.15}^t \frac{C_p}{T} \, dT - \text{Log} \left[ \frac{p}{1} \right] \right) \text{ (*eq 5.10*)}$$

$$\text{Out[8]} = \underline{\underline{95191.6604796}} \text{ J/mol}$$

ANS,  $\Delta H_{\text{ig}}$

$$\text{Out[9]} = \underline{\underline{146.444395848}} \text{ J/(mol}\cdot\text{K)}$$

ANS,  $\Delta S_{\text{ig}}$

Problem: Weight:  
B 100

Use the Peng-Robinson equation of state to calculate the compressibility, residual enthalpy, and residual entropy ( $Z$ ,  $H^R$ , and  $S^R$ ) for n-pentane at 800 K and 40 bar.

Use Table B.1 on page 663 of the textbook for critical constants and acentric factor. Use gas constant  $R=8.314$  J/(mol·K). Report your answers for  $H^R$  and  $S^R$  in J/mol and J/(mol·K), respectively.

**Solution:**

```

In[10]:= (*Table B.1, p.663*)
tc = 469.7; (*K*)
pc = 33.70; (*bar*)
ω = 0.252;

(*Reduced t and p*)
tr = t / tc; pr = p / pc;

(*Table 3.1 page 100*)
ε = 1 - √2; σ = 1 + √2; Ω = 0.07780; Ψ = 0.45724;
α[x_] = (1 + (0.37464 + 1.54226 * ω - 0.26992 * ω²) * (1 - √x))²;

β = Ω * pr / tr; (*eq 3.50*)
q[x_] = (Ψ * α[x]) / (Ω * x); (*eq 3.51*)

eq1 = Z == 1 + β - q[tr] * β * (Z - β) / ((Z + ε * β) * (Z + σ * β)); (*eq 3.48*)
ans = Quiet[Solve[eq1, Z, Reals]];
Z1 = Z /. ans[[1]];

I = (1 / (σ - ε)) * Log[(Z1 + σ * β) / (Z1 + ε * β)]; (*eq 13.72*)

Hr[x_] = (Z1 - 1 + x * ∂x q[x] * I) * R * t; (*13.75*)
Sr[x_] = (Log[Z1 - β] + (q[x] + x * ∂x q[x]) * I) * R; (*13.76*)

In[23]:= Z1
Hr[tr]
Sr[tr]

Out[23]= 0.954934272789
          ANS, Z
Out[24]= -1965.92751277 J/mol
          ANS, HR
Out[25]= -2.03083124078 J/(mol·K)
          ANS, SR

```

Problem: Weight:  
C 60

- (a) Using your results from Problems A and B and Table C.4 on page 671 of the textbook, calculate the total real-gas enthalpy and entropy for n-pentane at 800 K and 40 bar. Report your answers for H and S in J/mol and J/(mol·K), respectively.
- (b) Use CHEMCAD and the CHEMCAD file in your SharePoint directory calculate the enthalpy and entropy for n-pentane at 800 K and 40 bar (same conditions as in C.a).
- (c) Give three reasons for the difference between the answers in C.a and C.b.

**Solution, part (a):**

In[26]:= (\*Table C.4, p.671\*)

$$\Delta H_{fo} = -146\,760;$$

$$\Delta G_{fo} = -8650;$$

$$\Delta S_{fo} = \frac{\Delta H_{fo} - \Delta G_{fo}}{298.15};$$

$$H = \Delta H_{fo} + H_{ig} + H_r[\text{tr}] \quad (*6.50*)$$

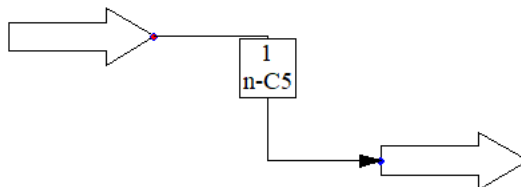
$$S = \Delta S_{fo} + S_{ig} + S_r[\text{tr}] \quad (*6.51*)$$

Out[29]= -53 534.2670332 J/mol //ANS  
ANS, H

Out[30]= -318.809645187 J/(mol·K) //ANS  
ANS, S

**Solution, part (b):**

Stream No.	1
Name	n-C5
-- Overall --	
Temp K	800.0000
Pres bar	40.0000
Enth J/sec	-52242. //ANS
Molar flow mol/sec	1.0000
Entropy J/K/sec	-316.2 //ANS



**Solution, part (c):**

The answers are different because of the following: (1) different heat capacity polynomial, (2) different  $T_c$ ,  $P_c$ , and  $\omega$ , and (3) different standard-state enthalpy and entropy of formation. //ANS