

Problem 14-15

The overhead vapor from the C₂ splitter in Fig. 3-13 is partially condensed in E-601. The process conditions for the vapor entering the condenser are:

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|-------------------------------|---|
| Temperature | -30.1°C (sat.) |
| Pressure | 1945.8 kPa (sat.) (changed from 2944 kPa) |
| Flow rate into condenser | |
| CH ₄ | 3×10^{-3} kg/s |
| C ₂ H ₄ | 64.52 kg/s |
| C ₂ H ₆ | 6.26×10^{-2} kg/s |

A shell-and-tube exchanger has been selected for this heat transfer process to condense 73.5% of the overhead vapor. Use an appropriate software package (based on TEMA guidelines) to obtain the overall heat-transfer coefficient and the area required for the condensation if the tubes have an outside diameter of 0.0127 m and an inside diameter of 0.0094 m. Assuming that the maximum length of the tubes is 3.05 m, how many tubes will be required and what shell diameter is recommended? Propylene at -46 °C serves as the coolant for the condensation process. Additional Questions: Identify the largest resistance to heat transfer in the exchanger and determine the total purchase cost of the exchanger in Feb 2026.

Important Note: There are two typos. First, the original problem statement has -30.1 °C and 2944 kPa. At these conditions the overhead vapor is completely condensed, not feasible for overhead vapor leaving a distillation column. To fix this in CHEMCAD, flash the stream at -30.1 °C with the vapor fraction set to 1, giving the correct pressure of 1945.8 kPa. Second, the temperature in Fig. 3-13 is wrong. The correct value is -30.1 °C as stated in the problem, not -46 °C.

Problem 14-16

Air used in a catalytic oxidation process is to be heated from 15 to 270 °C before entering the oxidation chamber. The heating is accomplished with the use of product gases, which cool from 380 to 200 °C. A steel one-pass shell-and-tube heat exchanger with cross-flow on the shell side has been proposed. The average absolute pressure on both the tube side and the shell side is 1010 kPa, with the hot gases being sent through the tubes. The flow rate for the air has been set at 1.9 kg/s. The inside and outside diameters for the tubes are 0.0191 and 0.0254 m, respectively. The tubes will be arranged in line with a square pitch of 0.0381 m. The exchanger operates for 8000 h/yr. The properties of the hot gases can be considered identical to those of air. The cost data for the exchanger are given in Fig. 14-19.

Installation costs are 15 percent of the purchased cost, and annual fixed charges including maintenance are 20 percent of the installed cost. The cost for power delivered is \$0.12/kWh. Under these conditions, determine the most appropriate tube length and the purchased cost for the optimum heat exchanger.