

NCEES

This document may be printed from the NCEES Web site
for your personal use, but it may not be copied, reproduced,
distributed electronically or in print, or posted online
without the express written permission of NCEES.
Contact permissions@ncees.org for more information.

Reference Handbook

9.3 Version for Computer-Based Testing

Copyright ©2013 by NCEES®. All rights reserved.

All NCEES material is copyrighted under the laws of the United States. No part of this publication may be reproduced, stored in a retrieval system, or transmitted in any form or by any means without the prior written permission of NCEES. Requests for permissions should be addressed in writing to permissions@ncees.org.

PO Box 1686
Clemson, SC 29633
800-250-3196
www.ncees.org

ISBN 978-1-932613-67-4

Printed in the United States of America
Third printing June 2015
Edition 9.3

PREFACE

About the *Handbook*

The Fundamentals of Engineering (FE) exam is computer-based, and the *FE Reference Handbook* is the only resource material you may use during the exam. Reviewing it before exam day will help you become familiar with the charts, formulas, tables, and other reference information provided. You won't be allowed to bring your personal copy of the *Handbook* into the exam room. Instead, the computer-based exam will include a PDF version of the *Handbook* for your use. No printed copies of the *Handbook* will be allowed in the exam room.

The PDF version of the *FE Reference Handbook* that you use on exam day will be very similar to the printed version. Pages not needed to solve exam questions—such as the cover, introductory material, and exam specifications—will not be included in the PDF version. In addition, NCEES will periodically revise and update the *Handbook*, and each FE exam will be administered using the updated version.

The *FE Reference Handbook* does not contain all the information required to answer every question on the exam. Basic theories, conversions, formulas, and definitions examinees are expected to know have not been included. Special material required for the solution of a particular exam question will be included in the question itself.

Updates on exam content and procedures

NCEES.org is our home on the Web. Visit us there for updates on everything exam-related, including specifications, exam-day policies, scoring, and practice tests. A PDF version of the *FE Reference Handbook* similar to the one you will use on exam day is also available there.

Errata

To report errata in this book, send your correction using our chat feature on NCEES.org. We will also post errata on the Web site. Examinees are not penalized for any errors in the *Handbook* that affect an exam question.

CONTENTS

Units	1
Conversion Factors.....	2
Ethics.....	3
Safety.....	5
Mathematics	21
Engineering Probability and Statistics	36
Chemistry	53
Materials Science/Structure of Matter	59
Statics	66
Dynamics.....	71
Mechanics of Materials	79
Thermodynamics.....	86
Fluid Mechanics	102
Heat Transfer	116
Instrumentation, Measurement, and Controls	123
Engineering Economics	130
Chemical Engineering.....	137
Civil Engineering	145
Environmental Engineering	178
Electrical and Computer Engineering	199
Industrial Engineering	219
Mechanical Engineering.....	228
Index.....	241
Appendix: FE Exam Specifications	265

UNITS

The FE exam and this handbook use both the metric system of units and the U.S. Customary System (USCS). In the USCS system of units, both force and mass are called pounds. Therefore, one must distinguish the pound-force (lbf) from the pound-mass (lbm).

The pound-force is that force which accelerates one pound-mass at 32.174 ft/sec². Thus, 1 lbf = 32.174 lbm-ft/sec². The expression 32.174 lbm-ft/(lbf·sec²) is designated as g_c and is used to resolve expressions involving both mass and force expressed as pounds. For instance, in writing Newton's second law, the equation would be written as $F = ma/g_c$, where F is in lbf, m in lbm, and a is in ft/sec².

Similar expressions exist for other quantities. Kinetic Energy, $KE = mv^2/2g_c$, with KE in (ft-lbf); Potential Energy, $PE = mgh/g_c$, with PE in (ft-lbf); Fluid Pressure, $p = \rho gh/g_c$, with p in (lbf/ft²); Specific Weight, $SW = \rho g/g_c$, in (lbf/ft³); Shear Stress, $\tau = (\mu/g_c)(dv/dy)$, with shear stress in (lbf/ft²). In all these examples, g_c should be regarded as a unit conversion factor. It is frequently not written explicitly in engineering equations. However, its use is required to produce a consistent set of units.

Note that the conversion factor g_c [lbm-ft/(lbf·sec²)] should not be confused with the local acceleration of gravity g , which has different units (m/s² or ft/sec²) and may be either its standard value (9.807 m/s² or 32.174 ft/sec²) or some other local value.

If the problem is presented in USCS units, it may be necessary to use the constant g_c in the equation to have a consistent set of units.

METRIC PREFIXES			COMMONLY USED EQUIVALENTS	
Multiple	Prefix	Symbol		
10^{-18}	atto	a		
10^{-15}	femto	f	1 gallon of water weighs	8.34 lbf
10^{-12}	pico	p	1 cubic foot of water weighs	62.4 lbf
10^{-9}	nano	n	1 cubic inch of mercury weighs	0.491 lbf
10^{-6}	micro	μ	The mass of 1 cubic meter of water is	1,000 kilograms
10^{-3}	milli	m	1 mg/L is	8.34 lbf/Mgal
10^{-2}	centi	c		
10^{-1}	deci	d		
10^1	deka	da	TEMPERATURE CONVERSIONS	
10^2	hecto	h	${}^{\circ}\text{F} = 1.8\text{ }({}^{\circ}\text{C}) + 32$	
10^3	kilo	k	${}^{\circ}\text{C} = ({}^{\circ}\text{F} - 32)/1.8$	
10^6	mega	M	${}^{\circ}\text{R} = {}^{\circ}\text{F} + 459.69$	
10^9	giga	G	$\text{K} = {}^{\circ}\text{C} + 273.15$	
10^{12}	tera	T		
10^{15}	peta	P		
10^{18}	exa	E		

IDEAL GAS CONSTANTS

The universal gas constant, designated as \bar{R} in the table below, relates pressure, volume, temperature, and number of moles of an ideal gas. When that universal constant, \bar{R} , is divided by the molecular weight of the gas, the result, often designated as R , has units of energy per degree per unit mass [kJ/(kg·K) or ft-lbf/(lbm·°R)] and becomes characteristic of the particular gas. Some disciplines, notably chemical engineering, often use the symbol R to refer to the universal gas constant \bar{R} .

FUNDAMENTAL CONSTANTS

Quantity	Symbol	Value	Units
electron charge	e	1.6022×10^{-19}	C (coulombs)
Faraday constant	F	96,485	coulombs/(mol)
gas constant	metric \bar{R}	8,314	J/(kmol·K)
gas constant	metric \bar{R}	8.314	kPa·m ³ /(kmol·K)
gas constant	USCS \bar{R}	1,545	ft-lbf/(lb mole·°R)
	\bar{R}	0.08206	L-atm/(mole-K)
gravitation–Newtonian constant	G	6.673×10^{-11}	m ³ /(kg·s ²)
gravitation–Newtonian constant	G	6.673×10^{-11}	N·m ² /kg ²
gravity acceleration (standard)	metric g	9.807	m/s ²
gravity acceleration (standard)	USCS g	32.174	ft/sec ²
molar volume (ideal gas), $T = 273.15\text{ K}$, $p = 101.3\text{ kPa}$	V_m	22,414	L/kmol
speed of light in vacuum	c	299,792,000	m/s
Stefan-Boltzmann constant	σ	5.67×10^{-8}	W/(m ² ·K ⁴)

CONVERSION FACTORS

Multiply	By	To Obtain	Multiply	By	To Obtain
acre	43,560	square feet (ft^2)	joule (J)	9.478×10^{-4}	Btu
ampere-hr (A-hr)	3,600	coulomb (C)	J	0.7376	ft-lbf
ångström (\AA)	1×10^{-10}	meter (m)	J	1	newton•m (N•m)
atmosphere (atm)	76.0	cm, mercury (Hg)	J/s	1	watt (W)
atm, std	29.92	in., mercury (Hg)			
atm, std	14.70	lbf/in ² abs (psia)			
atm, std	33.90	ft, water			
atm, std	1.013×10^5	pascal (Pa)			
bar	1×10^5	Pa			
bar	0.987	atm			
barrels-oil	42	gallons-oil			
Btu	1,055	joule (J)			
Btu	2.928×10^{-4}	kilowatt-hr (kWh)			
Btu	778	ft-lbf			
Btu/hr	3.930×10^{-4}	horsepower (hp)			
Btu/hr	0.293	watt (W)			
Btu/hr	0.216	ft-lbf/sec			
calorie (g-cal)	3.968×10^{-3}	Btu	liter (L)	61.02	in^3
cal	1.560×10^{-6}	hp-hr	L	0.264	gal (U.S. Liq)
cal	4.186	joule (J)	L	10^{-3}	m^3
cal/sec	4.184	watt (W)	L/second (L/s)	2.119	ft^3/min (cfm)
centimeter (cm)	3.281×10^{-2}	foot (ft)	L/s	15.85	gal (U.S.)/min (gpm)
cm	0.394	inch (in)			
centipoise (cP)	0.001	pascal•sec (Pa•s)			
centipoise (cP)	1	g/(m•s)			
centipoise (cP)	2.419	lbm/hr-ft			
centistoke (cSt)	1×10^{-6}	m^2/sec (m^2/s)			
cubic feet/second (cfs)	0.646317	million gallons/day (MGD)			
cubic foot (ft^3)	7.481	gallon			
cubic meters (m^3)	1,000	liters			
electronvolt (eV)	1.602×10^{-19}	joule (J)			
foot (ft)	30.48	cm			
ft	0.3048	meter (m)			
ft-pound (ft-lbf)	1.285×10^{-3}	Btu			
ft-lbf	3.766×10^{-7}	kilowatt-hr (kWh)			
ft-lbf	0.324	calorie (g-cal)			
ft-lbf	1.356	joule (J)			
ft-lbf/sec	1.818×10^{-3}	horsepower (hp)			
gallon (U.S. Liq)	3.785	liter (L)			
gallon (U.S. Liq)	0.134	ft^3			
gallons of water	8.3453	pounds of water			
gamma (γ, Γ)	1×10^{-9}	tesla (T)			
gauss	1×10^{-4}	T			
gram (g)	2.205×10^{-3}	pound (lbm)			
hectare	1×10^4	square meters (m^2)			
hectare	2.47104	acres			
horsepower (hp)	42.4	Btu/min			
hp	745.7	watt (W)			
hp	33,000	(ft-lbf)/min			
hp	550	(ft-lbf)/sec			
hp-hr	2,545	Btu			
hp-hr	1.98×10^6	ft-lbf			
hp-hr	2.68×10^6	joule (J)			
hp-hr	0.746	kWh			
inch (in.)	2.540	centimeter (cm)			
in. of Hg	0.0334	atm			
in. of Hg	13.60	in. of H_2O			
in. of H_2O	0.0361	lbf/in ² (psi)			
in. of H_2O	0.002458	atm			
joule (J)			joule (J)	9.478×10^{-4}	Btu
J			J	0.7376	ft-lbf
J			J	1	newton•m (N•m)
J/s			J/s	1	watt (W)
kilogram (kg)			kilogram (kg)	2.205	pound (lbm)
kgf			kgf	9.8066	newton (N)
kilometer (km)			kilometer (km)	3,281	feet (ft)
km/hr			km/hr	0.621	mph
kilopascal (kPa)			kilopascal (kPa)	0.145	lbf/in ² (psi)
kilowatt (kW)			kilowatt (kW)	1.341	horsepower (hp)
kW			kW	3,413	Btu/hr
kW			kW	737.6	(ft-lbf)/sec
kW-hour (kWh)			kW-hour (kWh)	3,413	Btu
kWh			kWh	1.341	hp-hr
kWh			kWh	3.6×10^6	joule (J)
kip (K)			kip (K)	1,000	lbf
K			K	4,448	newton (N)
liter (L)			liter (L)	61.02	in^3
L			L	0.264	gal (U.S. Liq)
L			L	10^{-3}	m^3
L/second (L/s)			L/second (L/s)	2.119	ft^3/min (cfm)
L/s			L/s	15.85	gal (U.S.)/min (gpm)
meter (m)			meter (m)	3.281	feet (ft)
m			m	1.094	yard
m/second (m/s)			m/second (m/s)	196.8	feet/min (ft/min)
mile (statute)			mile (statute)	5,280	feet (ft)
mile (statute)			mile (statute)	1.609	kilometer (km)
mile/hour (mph)			mile/hour (mph)	88.0	ft/min (fpm)
mph			mph	1.609	km/h
mm of Hg			mm of Hg	1.316×10^{-3}	atm
mm of H_2O			mm of H_2O	9.678×10^{-5}	atm
newton (N)			newton (N)	0.225	lbf
newton (N)			newton (N)	1	$\text{kg}\cdot\text{m}/\text{s}^2$
N•m			N•m	0.7376	ft-lbf
N•m			N•m	1	joule (J)
pascal (Pa)			pascal (Pa)	9.869×10^{-6}	atmosphere (atm)
Pa			Pa	1	newton/m ² (N/m ²)
Pa•sec (Pa•s)			Pa•sec (Pa•s)	10	poise (P)
pound (lbm, avdp)			pound (lbm, avdp)	0.454	kilogram (kg)
lbf			lbf	4.448	N
lbf-ft			lbf-ft	1.356	N•m
lbf/in ² (psi)			lbf/in ² (psi)	0.068	atm
psi			psi	2.307	ft of H_2O
psi			psi	2.036	in. of Hg
psi			psi	6,895	Pa
radian			radian	$180/\pi$	degree
stokes			stokes	1×10^{-4}	m^2/s
therm			therm	1×10^5	Btu
ton (metric)			ton (metric)	1,000	kilogram (kg)
ton (short)			ton (short)	2,000	pound (lb)
watt (W)			watt (W)	3,413	Btu/hr
W			W	1.341×10^{-3}	horsepower (hp)
W			W	1	joule/s (J/s)
weber/m ² (Wb/m ²)			weber/m ² (Wb/m ²)	10,000	gauss

ETHICS

Engineering is considered to be a "profession" rather than an "occupation" because of several important characteristics shared with other recognized learned professions, law, medicine, and theology: special knowledge, special privileges, and special responsibilities. Professions are based on a large knowledge base requiring extensive training. Professional skills are important to the well-being of society. Professions are self-regulating, in that they control the training and evaluation processes that admit new persons to the field. Professionals have autonomy in the workplace; they are expected to utilize their independent judgment in carrying out their professional responsibilities. Finally, professions are regulated by ethical standards. (Harris, C.E., M.S. Pritchard, & M.J. Rabins, *Engineering Ethics: Concepts and Cases*, Wadsworth Publishing company, pages 27–28, 1995.)

The expertise possessed by engineers is vitally important to societal welfare. In order to serve society effectively, engineers must maintain a high level of technical competence. However, a high level of technical expertise without adherence to ethical guidelines is as much a threat to public welfare as is professional incompetence. Therefore, engineers must also be guided by ethical principles.

The ethical principles governing the engineering profession are embodied in codes of ethics. Such codes have been adopted by state boards of registration, professional engineering societies, and even by some private industries. An example of one such code is the NCEES Rules of Professional Conduct, found in Section 240 of the *Model Rules* and presented here. As part of his/her responsibility to the public, an engineer is responsible for knowing and abiding by the code. Additional rules of conduct are also included in the *Model Rules*.

The three major sections of the *Model Rules* address (1) Licensee's Obligation to the Public, (2) Licensee's Obligation to Employers and Clients, and (3) Licensee's Obligation to Other Licensees. The principles amplified in these sections are important guides to appropriate behavior of professional engineers.

Application of the code in many situations is not controversial. However, there may be situations in which applying the code may raise more difficult issues. In particular, there may be circumstances in which terminology in the code is not clearly defined, or in which two sections of the code may be in conflict. For example, what constitutes "valuable consideration" or "adequate" knowledge may be interpreted differently by qualified professionals. These types of questions are called *conceptual issues*, in which definitions of terms may be in dispute. In other situations, *factual issues* may also affect ethical dilemmas. Many decisions regarding engineering design may be based upon interpretation of disputed or incomplete information. In addition, *tradeoffs* revolving around competing issues of risk vs. benefit, or safety vs. economics may require judgments that are not fully addressed simply by application of the code.

No code can give immediate and mechanical answers to all ethical and professional problems that an engineer may face. Creative problem solving is often called for in ethics, just as it is in other areas of engineering.

Model Rules, Section 240.15, Rules of Professional Conduct

To safeguard the health, safety, and welfare of the public and to maintain integrity and high standards of skill and practice in the engineering and surveying professions, the rules of professional conduct provided in this section shall be binding upon every licensee and on all firms authorized to offer or perform engineering or surveying services in this jurisdiction.

A. Licensee's Obligation to the Public

1. Licensees shall be cognizant that their first and foremost responsibility is to safeguard the health, safety, and welfare of the public when performing services for clients and employers.
2. Licensees shall sign and seal only those plans, surveys, and other documents that conform to accepted engineering and surveying standards and that safeguard the health, safety, and welfare of the public.
3. Licensees shall notify their employer or client and such other authority as may be appropriate when their professional judgment is overruled under circumstances in which the health, safety, or welfare of the public is endangered.
4. Licensees shall, to the best of their knowledge, include all relevant and pertinent information in an objective and truthful manner within all professional documents, statements, and testimony.
5. Licensees shall express a professional opinion publicly only when it is founded upon an adequate knowledge of the facts and a competent evaluation of the subject matter.
6. Licensees shall issue no statements, criticisms, or arguments on engineering and surveying matters that are inspired or paid for by interested parties, unless they explicitly identify the interested parties on whose behalf they are speaking and reveal any interest they have in the matters.
7. Licensees shall not partner, practice, or offer to practice with any person or firm that they know is engaged in fraudulent or dishonest business or professional practices.
8. Licensees who have knowledge or reason to believe that any person or firm has violated any rules or laws applying to the practice of engineering or surveying shall report it to the board, may report it to appropriate legal authorities, and shall cooperate with the board and those authorities as may be requested.

9. Licensees shall not knowingly provide false or incomplete information regarding an applicant in obtaining licensure.
 10. Licensees shall comply with the licensing laws and rules governing their professional practice in each of the jurisdictions in which they practice.
- B. Licensee's Obligation to Employer and Clients**
1. Licensees shall undertake assignments only when qualified by education or experience in the specific technical fields of engineering or surveying involved.
 2. Licensees shall not affix their signatures or seals to any plans or documents dealing with subject matter in which they lack competence, nor to any such plan or document not prepared under their responsible charge.
 3. Licensees may accept assignments and assume responsibility for coordination of an entire project, provided that each technical segment is signed and sealed by the licensee responsible for preparation of that technical segment.
 4. Licensees shall not reveal facts, data, or information obtained in a professional capacity without the prior consent of the client, employer, or public body on which they serve except as authorized or required by law or rules.
 5. Licensees shall not solicit or accept gratuities, directly or indirectly, from contractors, their agents, or other parties in connection with work for employers or clients.
 6. Licensees shall disclose to their employers or clients all known or potential conflicts of interest or other circumstances that could influence or appear to influence their judgment or the quality of their professional service or engagement.
 7. Licensees shall not accept compensation, financial or otherwise, from more than one party for services pertaining to the same project, unless the circumstances are fully disclosed and agreed to in writing by all interested parties.
 8. Licensees shall not solicit or accept a professional contract from a governmental body on which a principal or officer of their organization serves as a member. Conversely, licensees serving as members, advisors, or employees of a government body or

department, who are the principals or employees of a private concern, shall not participate in decisions with respect to professional services offered or provided by said concern to the governmental body that they serve. (Section 150, Disciplinary Action, NCEES Model Law)

9. Licensees shall not use confidential information received in the course of their assignments as a means of making personal profit without the consent of the party from whom the information was obtained.

C. Licensee's Obligation to Other Licensees

1. Licensees shall not falsify or permit misrepresentation of their, or their associates', academic or professional qualifications. They shall not misrepresent or exaggerate their degree of responsibility in prior assignments nor the complexity of said assignments. Presentations incidental to the solicitation of employment or business shall not misrepresent pertinent facts concerning employers, employees, associates, joint ventures, or past accomplishments.
2. Licensees shall not offer, give, solicit, or receive, either directly or indirectly, any commission, or gift, or other valuable consideration in order to secure work, and shall not make any political contribution with the intent to influence the award of a contract by public authority.
3. Licensees shall not injure or attempt to injure, maliciously or falsely, directly or indirectly, the professional reputation, prospects, practice, or employment of other licensees, nor indiscriminately criticize other licensees' work.
4. Licensees shall make a reasonable effort to inform another licensee whose work is believed to contain a material discrepancy, error, or omission that may impact the health, safety, or welfare of the public, unless such reporting is legally prohibited.

SAFETY

DEFINITION OF SAFETY

Safety is the condition of protecting people from threats or failures that could harm their physical, emotional, occupational, psychological, or financial well-being. Safety is also the control of known threats to attain an acceptable level of risk.

The United States relies on public codes and standards, engineering designs, and corporate policies to ensure that a structure or place does what it should do to maintain a steady state of safety—that is, long-term stability and reliability. Some *Safety/Regulatory Agencies* that develop codes and standards commonly used in the United States are shown in the table.

Acronym	Name	Jurisdiction
ANSI	American National Standards Institute	Nonprofit standards organization
CGA	Compressed Gas Association	Nonprofit trade association
CSA	Canadian Standards Association	Nonprofit standards organization
FAA	Federal Aviation Administration	Federal regulatory agency
IEC	International Electrotechnical Commission	Nonprofit standards organization
ITSNA	Intertek Testing Services NA (formerly Edison Testing Labs)	Nationally recognized testing laboratory
MSHA	Mine Safety and Health Administration	Federal regulatory agency
NFPA	National Fire Protection Association	Nonprofit trade association
OSHA	Occupational Safety and Health Administration	Federal regulatory agency
UL	Underwriters Laboratories	Nationally recognized testing laboratory
USCG	United States Coast Guard	Federal regulatory agency
USDOT	United States Department of Transportation	Federal regulatory agency
USEPA	United States Environmental Protection Agency	Federal regulatory agency

SAFETY AND PREVENTION

A traditional preventive approach to both accidents and occupational illness involves recognizing, evaluating, and controlling hazards and work conditions that may cause physical or other injuries.

Hazard is the capacity to cause harm. It is an inherent quality of a material or a condition. For example, a rotating saw blade or an uncontrolled high-pressure jet of water has the capability (hazard) to slice through flesh. A toxic chemical or a pathogen has the capability (hazard) to cause illness.

Risk is the chance or probability that a person will experience harm and is not the same as a hazard. Risk always involves both probability and severity elements. The hazard associated with a rotating saw blade or the water jet continues to exist, but the probability of causing harm, and thus the risk, can be reduced by installing a guard or by controlling the jet's path. Risk is expressed by the equation:

$$\text{Risk} = \text{Hazard} \times \text{Probability}$$

When people discuss the hazards of disease-causing agents, the term *exposure* is typically used more than *probability*. If a certain type of chemical has a toxicity hazard, the risk of illness rises with the degree to which that chemical contacts your body or enters your lungs. In that case, the equation becomes:

$$\text{Risk} = \text{Hazard} \times \text{Exposure}$$

Organizations evaluate hazards using multiple techniques and data sources.

Job Safety Analysis

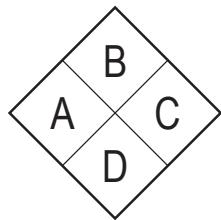
Job safety analysis (JSA) is known by many names, including activity hazard analysis (AHA), or job hazard analysis (JHA). Hazard analysis helps integrate accepted safety and health principles and practices into a specific task. In a JSA, each basic step of the job is reviewed, potential hazards identified, and recommendations documented as to the safest way to do the job. JSA techniques work well when used on a task that the analysts understand well. JSA analysts look for specific types of potential accidents and ask basic questions about each step, such as these:

- Can the employee strike against or otherwise make injurious contact with the object?
- Can the employee be caught in, on, or between objects?
- Can the employee strain muscles by pushing, pulling, or lifting?
- Is exposure to toxic gases, vapors, dust, heat, electrical currents, or radiation possible?

HAZARD ASSESSMENTS

Hazard Assessment

The fire/hazard diamond below summarizes common hazard data available on the Safety Data Sheet (SDS) and is frequently shown on chemical labels.



Position A – Health Hazard (Blue)

0 = normal material

1 = slightly hazardous

2 = hazardous

3 = extreme danger

4 = deadly

Position B – Flammability (Red)

0 = will not burn

1 = will ignite if preheated

2 = will ignite if moderately heated

3 = will ignite at most ambient temperature

4 = burns readily at ambient conditions

Position C – Reactivity (Yellow)

0 = stable and not reactive with water

1 = unstable if heated

2 = violent chemical change

3 = shock short may detonate

4 = may detonate

Position D – (White)

ALKALI = alkali

OXY = oxidizer

ACID = acid

Cor = corrosive

W = use no water

= radiation hazard

GHS

The *Globally Harmonized System of Classification and Labeling of Chemicals*, or GHS, is a system for standardizing and harmonizing the classification and labeling of chemicals. GHS is a comprehensive approach to:

- Defining health, physical, and environmental hazards of chemicals
- Creating classification processes that use available data on chemicals for comparison with the defined hazard criteria
- Communicating hazard information, as well as protective measures, on labels and Safety Data Sheets (SDSs), formerly called Material Safety Data Sheets (MSDSs).

GHS label elements include:

- Precautionary statements and pictograms: Measures to minimize or prevent adverse effects
- Product identifier (ingredient disclosure): Name or number used for a hazardous product on a label or in the SDS
- Supplier identification: The name, address, and telephone number of the supplier
- Supplemental information: nonharmonized information

Other label elements include symbols, signal words, and hazard statements.

GHS LABEL ELEMENTS

*Product Name or Identifier
(Identify Hazardous Ingredients, where appropriate)*



Signal Word

*Physical, Health, Environmental
Hazard Statements*

Supplemental Information

Precautionary Measures and Pictograms



First Aid Statements

Name and Address of Company

Telephone Number

Occupational Safety and Health Administration, *A Guide to The Globally Harmonized System of Classification and Labelling of Chemicals (GHS)*, United States Department of Labor, <https://www.osha.gov/dsg/hazcom/ghs.html#3.2>.

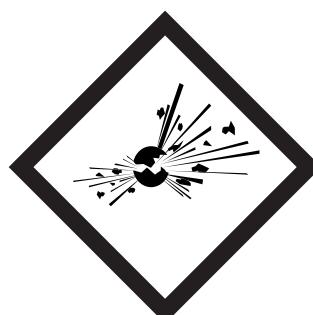
GHS PICTOGRAMS AND HAZARD CLASSES



- OXIDIZERS



- FLAMMABLES
- SELF-REACTIVES
- PYROPHORICS
- SELF-HEATING
- EMITS FLAMMABLE GAS
- ORGANIC PEROXIDES



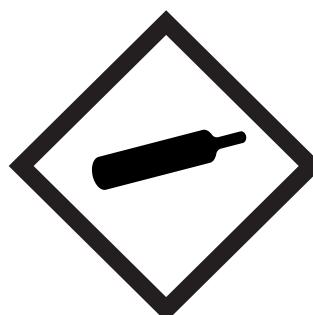
- EXPLOSIVES
- SELF-REACTIVES
- ORGANIC PEROXIDES



- ACUTE TOXICITY (SEVERE)



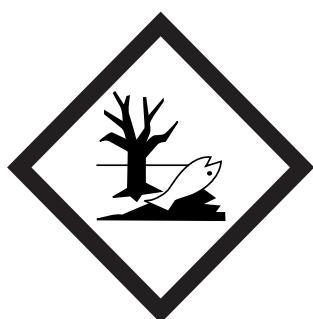
- CORROSIVES



- GASES UNDER PRESSURE



- CARCINOGEN
- RESPIRATORY SENSITIZER
- REPRODUCTIVE TOXICITY
- TARGET ORGAN TOXICITY
- MUTAGENICITY
- ASPIRATION TOXICITY



- ENVIRONMENTAL TOXICITY



- IRRITANT
- DERMAL SENSITIZER
- ACUTE TOXICITY (HARMFUL)
- NARCOTIC EFFECTS
- RESPIRATORY TRACT
- IRRIGATION

TRANSPORT PICTOGRAMS



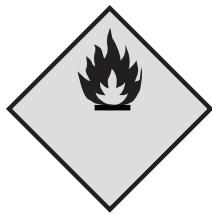
FLAMMABLE LIQUID
FLAMMABLE GAS
FLAMMABLE AEROSOL



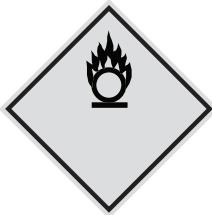
FLAMMABLE SOLID
SELF-REACTIVE
SUBSTANCES



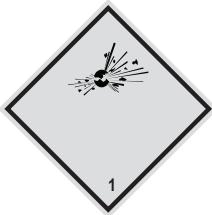
PYROPHORICS (SPONTANEOUSLY
COMBUSTIBLE)
SELF-HEATING SUBSTANCES



SUBSTANCES THAT, IN
CONTACT WITH WATER,
EMIT FLAMMABLE GASES
(DANGEROUS WHEN WET)



OXIDIZING GASES
OXIDIZING LIQUIDS
OXIDIZING SOLIDS



EXPLOSIVE DIVISIONS
1.1, 1.2, 1.3



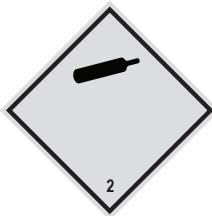
EXPLOSIVE DIVISION 1.4



EXPLOSIVE DIVISION 1.5



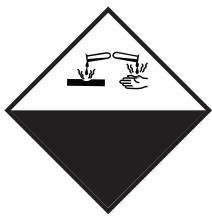
EXPLOSIVE DIVISION 1.6



COMPRESSED GASES



ACUTE TOXICITY (POISON):
ORAL, DERMAL, INHALATION



CORROSIVE



MARINE POLLUTANT



ORGANIC PEROXIDES

ACUTE ORAL TOXICITY					
LD ₅₀	CATEGORY 1 £ 5 mg/kg	CATEGORY 2 > 5 < 50 mg/kg	CATEGORY 3 ³ 50 < 300 mg/kg	CATEGORY 4 ³ 300 < 2,000 mg/kg	CATEGORY 5 ³ 2,000 > 5,000 mg/kg
PICTOGRAM					NO SYMBOL
SIGNAL WORD	DANGER	DANGER	DANGER	WARNING	WARNING
HAZARD STATEMENT	FATAL IF SWALLOWED	FATAL IF SWALLOWED	TOXIC IF SWALLOWED	HARMFUL IF SWALLOWED	MAY BE HARMFUL IF SWALLOWED

♦ Safety Data Sheet (SDS)

The SDS provides comprehensive information for use in workplace chemical management. Employers and workers use the SDS as a source of information about hazards and to obtain advice on safety precautions. The SDS is product related and, usually, is not able to provide information that is specific for any given workplace where the product may be used. However, the SDS information enables the employer to develop an active program of worker protection measures, including training, which is specific to the individual workplace, and to consider any measures that may be necessary to protect the environment. Information in an SDS also provides a source of information for those involved with the transport of dangerous goods, emergency responders, poison centers, those involved with the professional use of pesticides, and consumers.

The GHS and SDS have 16 sections in a set order, and minimum information is prescribed.

♦ The Hazard Communication Standard (HCS) requires chemical manufacturers, distributors, or importers to provide SDSs to communicate the hazards of hazardous chemical products. As of June 1, 2015, the HCS requires new SDSs to be in a uniform format, and include the section numbers, the headings, and associated information under the headings below:

- Section 1, Identification: Includes product identifier; manufacturer or distributor name, address, phone number; emergency phone number; recommended use; restrictions on use
- Section 2, Hazard(s) identification: Includes all hazards regarding the chemical; required label elements
- Section 3, Composition/information on ingredients: Includes information on chemical ingredients; trade secret claims
- Section 4, First-aid measures: Includes important symptoms/effects, acute, delayed; required treatment
- Section 5, Fire-fighting measures: Lists suitable extinguishing techniques, equipment; chemical hazards from fire
- Section 6, Accidental release measures: Lists emergency procedures; protective equipment; proper methods of containment and cleanup
- Section 7, Handling and storage: Lists precautions for safe handling and storage, including incompatibilities
- Section 8, Exposure controls/personal protection: Lists OSHA's Permissible Exposure Limits (PELs); Threshold Limit Values (TLVs); appropriate engineering controls; personal protective equipment (PPE)
- Section 9, Physical and chemical properties: Lists the chemical's characteristics
- Section 10, Stability and reactivity: Lists chemical stability and possibility of hazardous reactions
- Section 11, Toxicological information: Includes routes of exposure; related symptoms, acute and chronic effects; numerical measures of toxicity
- Section 12, Ecological information*
- Section 13, Disposal considerations*
- Section 14, Transport information*
- Section 15, Regulatory information*
- Section 16, Other information: Includes the date of preparation or last revision

*Note: Since other Agencies regulate this information, OSHA will not be enforcing Sections 12 through 15 (29 CFR 1910.1200(g)(2)).

♦ Occupational Safety and Health Administration, *A Guide to The Globally Harmonized System of Classification and Labelling of Chemicals (GHS)*, United States Department of Labor, <https://www.osha.gov/dsg/hazcom/ghs.html#3.2>.

Signal Words

The signal word found on every product's label is based on test results from various oral, dermal, and inhalation toxicity tests, as well as skin and eye corrosion assays in some cases. Signal words are placed on labels to convey a level of care that should be taken (especially personal protection) when handling and using a product, from purchase to disposal of the empty container, as demonstrated by the Pesticide Toxicity Table.

Pesticide Toxicity Categories

Signal Word on Label	Toxicity Category	Acute-Oral LD ₅₀ for Rats	Amount Needed to Kill an Average Size Adult	Notes
Danger—Poison	Highly Toxic	50 or less	Taste to a teaspoon	Skull and crossbones; Keep Out of Reach of Children
Warning	Moderately Toxic	50 to 500	One to six teaspoons	Keep Out of Reach of Children
Caution	Slightly Toxic	500 to 5,000	One ounce to a pint	Keep Out of Reach of Children
Caution	Relatively Nontoxic	>5,000	More than a pint	Keep Out of Reach of Children

LD₅₀ - See Risk Assessment/Toxicology section on page 12.

From *Regulating Pesticides*, U.S. Environmental Protection Agency.

Flammability

Flammable describes any solid, liquid, vapor, or gas that will ignite easily and burn rapidly. A flammable liquid is defined by NFPA and USDOT as a liquid with a flash point below 100°F (38°C). Flammability is further defined with lower and upper limits:

LFL = lower flammability limit (volume % in air)

UFL = upper flammability limit (volume % in air)

A vapor-air mixture will only ignite and burn over the range of concentrations between LFL and UFL. Examples are:

Compound	LFL	UFL
Ethyl alcohol	3.3	19
Ethyl ether	1.9	36
Ethylene	2.7	36
Methane	5	15
Propane	2.1	9.5

♦ Predicting Lower Flammable Limits of Mixtures of Flammable Gases (Le Chatelier's Rule)

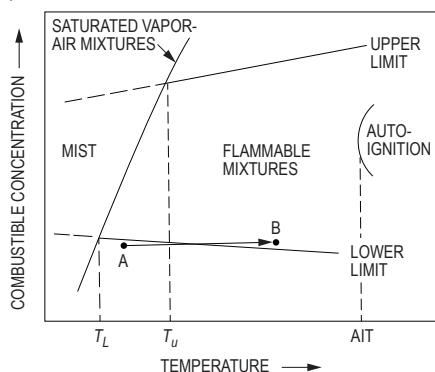
Based on an empirical rule developed by Le Chatelier, the lower flammable limit of mixtures of multiple flammable gases in air can be determined. A generalization of Le Chatelier's rule is

$$\sum_{i=1}^n (C_i / \text{LFL}_i) \geq 1$$

where C_i is the volume percent of fuel gas, i , in the fuel/air mixture and LFL_i is the volume percent of fuel gas, i , at its lower flammable limit in air alone. If the indicated sum is greater than unity, the mixture is above the lower flammable limit. This can be restated in terms of the lower flammable limit concentration of the fuel mixture, LFL_m , as follows:

$$\text{LFL}_m = \frac{100}{\sum_{i=1}^n (C_{fi} / \text{LFL}_i)}$$

where C_{fi} is the volume percent of fuel gas i in the fuel gas mixture.



Granular Storage and Process Safety

Some materials that are not inherently hazardous can become hazardous during storage or processing. An example is the handling of grain in grain bins. Grain bins should not be entered when the grain is being removed since grains flow to the center of the emptying bin and create suffocation hazards. Bridging may occur at the top surface due to condensation and resulting spoilage creating a crust.

Organic vapors and dusts associated with grain handling often contain toxic yeasts or molds and have low oxygen contents. These organic vapors and dusts may also be explosive.

Confined Space Safety

Many workplaces contain spaces that are considered "confined" because their configurations hinder the activities of employees who must enter, work in, and exit them. A confined space has limited or restricted means for entry or exit and is not designed for continuous employee occupancy. Confined spaces include, but are not limited to, underground vaults, tanks, storage bins, manholes, pits, silos, process vessels, and pipelines. OSHA uses the term "permit-required confined spaces" (permit space) to describe a confined space that has one or more of the following characteristics: contains or has the potential to contain a hazardous atmosphere; contains a material that has the potential to engulf an entrant; has walls that converge inward or floors that slope downward and taper into a smaller area that could trap or asphyxiate an entrant; or contains any other recognized safety or health hazard such as unguarded machinery, exposed live wires or heat stress.

OSHA has developed OSHA standards, directives (instructions for compliance officers), standard interpretations (official letters of interpretation of the standards), and national consensus standards related to confined spaces. The following gases are often present in confined spaces:

Ammonia: Irritating at 50 ppm and deadly above 1,000 ppm; sharp, cutting odor

Hydrogen sulfide: Irritating at 10 ppm and deadly at 500 ppm; accumulates at lower levels and in corners where circulation is minimal; rotten egg odor

Methane: Explosive at levels above 50,000 ppm, lighter than air, odorless

Carbon dioxide: Heavier than air, accumulates at lower levels and in corners where circulation is minimal, displaces air leading to asphyxiation

Electrical Safety

Current Level (Milliamperes)	Probable Effect on Human Body
1 mA	Perception level. Slight tingling sensation. Still dangerous under certain conditions.
5 mA	Slight shock felt; not painful but disturbing. Average individual can let go. However, strong involuntary reactions to shocks in this range may lead to injuries.
6 mA–16 mA	Painful shock, begin to lose muscular control. Commonly referred to as the freezing current or "let-go" range.
17 mA–99 mA	Extreme pain, respiratory arrest, severe muscular contractions. Individual cannot let go. Death is possible.
100 mA–2,000 mA	Ventricular fibrillation (uneven, uncoordinated pumping of the heart.) Muscular contraction and nerve damage begins to occur. Death is likely.
> 2,000 mA	Cardiac arrest, internal organ damage, and severe burns. Death is probable.

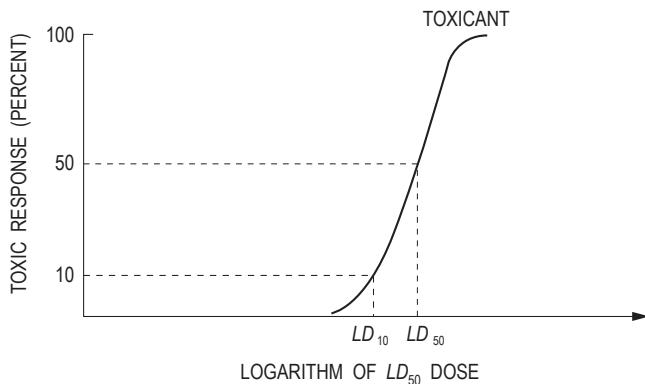
Worker Deaths by Electrocution; A Summary of NIOSH Surveillance and Investigative Findings,
U.S. Health and Human Services, (NIOSH), 1998.

Greenwald E.K., *Electrical Hazards and Accidents—Their Cause and Prevention*, Van Nostrand Reinhold, 1991.

RISK ASSESSMENT/TOXICOLOGY

Dose-Response Curves

The dose-response curve relates toxic response (i.e., percentage of test population exhibiting a specified symptom or dying) to the logarithm of the dosage [i.e., mg/(kg•day) ingested]. A typical dose-response curve is shown below.



LC_{50}

Median lethal concentration in air that, based on laboratory tests, is expected to kill 50% of a group of test animals when administered as a single exposure over 1 or 4 hours.

LD_{50}

Median lethal single dose, based on laboratory tests, expected to kill 50% of a group of test animals, usually by oral or skin exposure.

Similar definitions exist for LC_{10} and LD_{10} , where the corresponding percentages are 10%.

The following table lists the probable effect on the human body of different current levels.



Comparative Acutely Lethal Doses

Actual Ranking No.	LD_{50} (mg/kg)	Toxic Chemical
1	15,000	PCBs
2	10,000	Alcohol (ethanol)
3	4,000	Table salt—sodium chloride
4	1,500	Ferrous sulfate—an iron supplement
5	1,375	Malathion—pesticide
6	900	Morphine
7	150	Phenobarbital—a sedative
8	142	Tylenol (acetaminophen)
9	2	Strychnine—a rat poison
10	1	Nicotine
11	0.5	Curare—an arrow poison
12	0.001	2,3,7,8-TCDD (dioxin)
13	0.00001	Botulinum toxin (food poison)

Selected Chemical Interaction Effects

Effect	Relative toxicity (hypothetical)	Example
Additive	$2 + 3 = 5$	Organophosphate pesticides
Synergistic	$2 + 3 = 20$	Cigarette smoking + asbestos
Antagonistic	$6 + 6 = 8$	Toluene + benzene or caffeine + alcohol

Exposure Limits for Selected Compounds

N	Allowable Workplace Exposure Level (mg/m ³)	Chemical (use)
1	0.1	Iodine
2	5	Aspirin
3	10	Vegetable oil mists (cooking oil)
4	55	1,1,2-Trichloroethane (solvent/degreaser)
5	188	Perchloroethylene (dry-cleaning fluid)
6	170	Toluene (organic solvent)
7	269	Trichloroethylene (solvent/degreaser)
8	590	Tetrahydrofuran (organic solvent)
9	890	Gasoline (fuel)
10	1,590	Naphtha (rubber solvent)
11	1,910	1,1,1-Trichloroethane (solvent/degreaser)

◆ Adapted from Loomis's *Essentials of Toxicology*, 4th ed., Loomis, T.A., and A.W. Hayes, San Diego, Academic Press, 1996.

● Adapted from Williams, P.L., R.C. James, and S.M. Roberts, *Principles of Toxicology: Environmental and Industrial Applications*, 2nd ed., Wiley, 2000.

■ American Conference of Government Industrial Hygienists (ACGIH) 1996.

Carcinogens

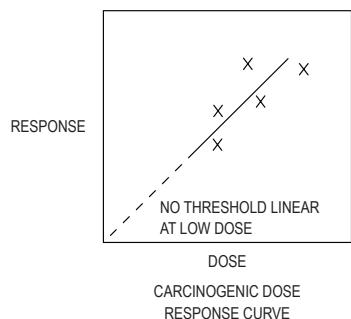
For carcinogens, EPA considers an acceptable risk to be within the range of 10^{-4} to 10^{-6} . The added risk of cancer is calculated as follows:

$$\text{Risk} = \text{dose} \times \text{toxicity} = CDI \times CSF$$

where

CDI = Chronic Daily Intake

CSF = Cancer Slope Factor. Slope of the dose-response curve for carcinogenic materials.



Threshold Limit Value (TLV)

TLV is the highest dose (ppm by volume in the atmosphere) the body is able to detoxify without any detectable effects.

Examples are:

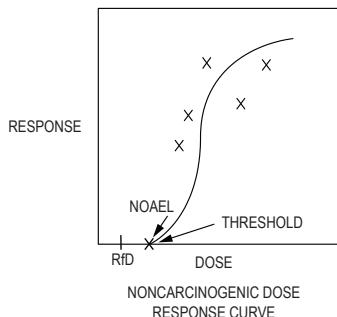
Compound	TLV
Ammonia	25
Chlorine	0.5
Ethyl Chloride	1,000
Ethyl Ether	400

Noncarcinogens

For noncarcinogens, a hazard index (HI) is used to characterize risk from all pathways and exposure routes. EPA considers an $HI > 1.0$ as representing the possibility of an adverse effect occurring.

$$HI = CDI_{\text{noncarcinogen}} / RfD$$

$CDI_{\text{noncarcinogen}}$ = chronic daily intake of noncarcinogenic compound



Dose is expressed

$$\left(\frac{\text{mass of chemical}}{\text{body weight} \cdot \text{exposure time}} \right)$$

$NOAEL$ = No Observable Adverse Effect Level. The dose below which there are no harmful effects

Reference Dose

Reference dose (RfD) is determined from the Noncarcinogenic Dose-Response Curve using $NOAEL$.

RfD = lifetime (i.e., chronic) dose that a healthy person could be exposed to daily without adverse effects

$$RfD = \frac{NOAEL}{UF}$$

and

$$SHD = RfD \times W = \frac{NOAEL \times W}{UF}$$

where

SHD = safe human dose (mg/day)

$NOAEL$ = threshold dose per kg of test animal [mg/(kg•day)] from the dose-response curve

UF = the total uncertainty factor, depending on nature and reliability of the animal test data

W = the weight of the adult male (typically 70 kg)

HAZARDOUS WASTE COMPATIBILITY CHART

Reactivity Group	
No.	Name
1	Acid, Minerals, Non-Oxidizing
2	Acids, Minerals, Oxidizing
3	Acids, Organic
4	Alcohols & Glycols
5	Aldehydes
6	Amides
7	Amines, Aliphatic & Aromatic
8	Azo Compounds, Diazo Comp, Hydrazines
9	Carbamates
10	Caustics
11	Cyanides
12	Dithiocarbamates
13	Esters
14	Ethers
15	Fluorides, Inorganic
16	Hydrocarbons, Aromatic
17	Halogenated Organics
18	Isocyanates
19	Ketones
20	Mercaptans & Other Organic Sulfides
21	Metal, Alkali & Alkaline Earth, Elemental
104	Oxidizing Agents, Strong
105	Reducing Agents, Strong
106	Water & Mixtures Containing Water
107	Water Reactive Substances

KEY

REACTIVITY CODE	CONSEQUENCES
H	HEAT GENERATION
F	FIRE
G	INNOCUOUS & NON-FLAMMABLE GAS
GT	TOXIC GAS GENERATION
GF	FLAMMABLE GAS GENERATION
E	EXPLOSION
P	POLYMERIZATION
S	SOLUBILIZATION OF TOXIC MATERIAL
U	MAY BE HAZARDOUS BUT UNKNOWN

EXAMPLE:

H HEAT GENERATION,
 F FIRE, AND TOXIC GAS
 GT GENERATION

Exposure

Residential Exposure Equations for Various Pathways

Ingestion in drinking water

$$CDI = \frac{(CW)(IR)(EF)(ED)}{(BW)(AT)}$$

Ingestion while swimming

$$CDI = \frac{(CW)(CR)(ET)(EF)(ED)}{(BW)(AT)}$$

Dermal contact with water

$$AD = \frac{(CW)(SA)(PC)(ET)(EF)(ED)(CF)}{(BW)(AT)}$$

Ingestion of chemicals in soil

$$CDI = \frac{(CS)(IR)(CF)(FI)(EF)(ED)}{(BW)(AT)}$$

Dermal contact with soil

$$AD = \frac{(CS)(CF)(SA)(AF)(ABS)(EF)(ED)}{(BW)(AT)}$$

Inhalation of airborne (vapor phase) chemicals

$$CDI = \frac{(CA)(IR)(ET)(EF)(ED)}{(BW)(AT)}$$

Ingestion of contaminated fruits, vegetables, fish and shellfish

$$CDI = \frac{(CF)(IR)(FI)(EF)(ED)}{(BW)(AT)}$$

where ABS = absorption factor for soil contaminant (unitless)

AD = absorbed dose (mg/[kg•day])

AF = soil-to-skin adherence factor (mg/cm²)

AT = averaging time (days)

BW = body weight (kg)

CA = contaminant concentration in air (mg/m³)

CDI = chronic daily intake (mg/[kg•day])

CF = volumetric conversion factor for water

= 1 L/1,000 cm³

= conversion factor for soil = 10⁻⁶ kg/mg

CR = contact rate (L/hr)

CS = chemical concentration in soil (mg/kg)

CW = chemical concentration in water (mg/L)

ED = exposure duration (years)

EF = exposure frequency (days/yr or events/year)

ET = exposure time (hr/day or hr/event)

FI = fraction ingested (unitless)

IR = ingestion rate (L/day or mg soil/day or kg/meal)
= inhalation rate (m³/hr)

PC = chemical-specific dermal permeability constant
(cm/hr)

SA = skin surface area available for contact (cm²)

Risk Assessment Guidance for Superfund. Volume 1, Human Health Evaluation Manual (part A). U.S. Environmental Protection Agency, EPA/540/1-89/002, 1989.

Intake Rates—Variable Values

EPA-Recommended Values for Estimating Intake

Parameter	Standard Value
Average body weight, female adult	65.4 kg
Average body weight, male adult	78 kg
Average body weight, child ^a	
6–11 months	9 kg
1–5 years	16 kg
6–12 years	33 kg
Amount of water ingested, adult	2.3 L/day
Amount of water ingested, child	1.5 L/day
Amount of air breathed, female adult	11.3 m ³ /day
Amount of air breathed, male adult	15.2 m ³ /day
Amount of air breathed, child (3–5 years)	8.3 m ³ /day
Amount of fish consumed, adult	6 g/day
Water swallowing rate, while swimming	50 mL/hr
Inhalation rates	
adult (6-hr day)	0.98 m ³ /hr
adult (2-hr day)	1.47 m ³ /hr
child	0.46 m ³ /hr
Skin surface available, adult male	1.94 m ²
Skin surface available, adult female	1.69 m ²
Skin surface available, child	
3–6 years (average for male and female)	0.720 m ²
6–9 years (average for male and female)	0.925 m ²
9–12 years (average for male and female)	1.16 m ²
12–15 years (average for male and female)	1.49 m ²
15–18 years (female)	1.60 m ²
15–18 years (male)	1.75 m ²
Soil ingestion rate, child 1–6 years	>100 mg/day
Soil ingestion rate, persons > 6 years	50 mg/day
Skin adherence factor, gardener's hands	0.07 mg/cm ²
Skin adherence factor, wet soil	0.2 mg/cm ²
Exposure duration	
Lifetime (carcinogens, for noncarcinogens use actual exposure duration)	75 years
At one residence, 90th percentile	30 years
National median	5 years
Averaging time	(ED)(365 days/year)
Exposure frequency (EF)	
Swimming	7 days/year
Eating fish and shellfish	48 days/year
Oral ingestion	350 days/year
Exposure time (ET)	
Shower, 90th percentile	12 min
Shower, 50th percentile	7 min

^aData in this category taken from: Copeland, T., A. M. Holbrow, J. M. Otan, et al., "Use of probabilistic methods to understand the conservatism in California's approach to assessing health risks posed by air contaminants," *Journal of the Air and Waste Management Association*, vol. 44, pp. 1399-1413, 1994.

Risk Assessment Guidance for Superfund. Volume 1, *Human Health Evaluation Manual* (part A). U.S. Environmental Protection Agency, EPA/540/l-89/002, 1989.

Concentrations of Vaporized Liquids

Vaporization Rate (Q_m , mass/time) from a Liquid Surface

$$Q_m = [MKA_s P^{\text{sat}}/(R_g T_L)]$$

M = molecular weight of volatile substance

K = mass transfer coefficient

A_s = area of liquid surface

P^{sat} = saturation vapor pressure of the pure liquid at T_L

R_g = ideal gas constant

T_L = absolute temperature of the liquid

Mass Flow Rate of Liquid from a Hole in the Wall of a Process Unit

$$Q_m = A_H C_0 (2\rho g_c P_g)^{1/2}$$

A_H = area of hole

C_0 = discharge coefficient

ρ = density of the liquid

g_c = gravitational constant

P_g = gage pressure within the process unit

Concentration (C_{ppm}) of Vaporized Liquid in Ventilated Space

$$C_{\text{ppm}} = [Q_m R_g T \times 10^6 / (k Q_v P M)]$$

T = absolute ambient temperature

k = non-ideal mixing factor

Q_v = ventilation rate

P = absolute ambient pressure

Sweep-Through Concentration Change in a Vessel

$$Q_v t = V \ln[(C_1 - C_0)/(C_2 - C_0)]$$

Q_v = volumetric flow rate

t = time

V = vessel volume

C_0 = inlet concentration

C_1 = initial concentration

C_2 = final concentration

ERGONOMICS

NIOSH Formula

Recommended Weight Limit (RWL)

$$RWL = 51(10/H)(1 - 0.0075|V - 30|)(0.82 + 1.8/D)(1 - 0.0032A)(FM)(CM)$$

where

RWL = recommended weight limit, in pounds

H = horizontal distance of the hand from the midpoint of the line joining the inner ankle bones to a point projected on the floor directly below the load center, in inches

V = vertical distance of the hands from the floor, in inches

D = vertical travel distance of the hands between the origin and destination of the lift, in inches

A = asymmetry angle, in degrees

FM = frequency multiplier (see table)

CM = coupling multiplier (see table)

Frequency Multiplier Table

F, min ⁻¹	≤ 8 hr/day		≤ 2 hr/day		≤ 1 hr/day	
	V < 30 in.	V ≥ 30 in.	V < 30 in.	V ≥ 30 in.	V < 30 in.	V ≥ 30 in.
0.2	0.85		0.95		1.00	
0.5	0.81		0.92		0.97	
1	0.75		0.88		0.94	
2	0.65		0.84		0.91	
3	0.55		0.79		0.88	
4	0.45		0.72		0.84	
5	0.35		0.60		0.80	
6	0.27		0.50		0.75	
7	0.22		0.42		0.70	
8	0.18		0.35		0.60	
9		0.15	0.30		0.52	
10		0.13	0.26		0.45	
11				0.23	0.41	
12				0.21	0.37	
13			0.00			0.34
14						0.31
15						0.28

Waters, Thomas R., Ph.D., et al, *Applications Manual for the Revised NIOSH Lifting Equation*, Table 5, U.S. Department of Health and Human Services (NIOSH), January 1994.

Coupling Multiplier (CM) Table (Function of Coupling of Hands to Load)

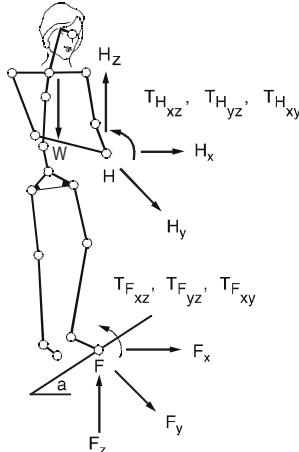
Container		Loose Part / Irreg. Object	
Optimal Design	Not	Comfort Grip	Not
Opt. Handles or Cut-outs	Not	POOR	GOOD
GOOD	Flex Fingers 90 Degrees	Not	POOR
FAIR		POOR	
Coupling		$V < 30 \text{ in. or } 75 \text{ cm}$	$V \geq 30 \text{ in. or } 75 \text{ cm}$
GOOD		1.00	
FAIR		0.95	
POOR		0.90	

Waters, Thomas R., Ph.D., et al, *Applications Manual for the Revised NIOSH Lifting Equation*, Table 7, U.S. Department of Health and Human Services (NIOSH), January 1994.

Biomechanics of the Human Body

Basic Equations

$$\begin{aligned} H_x + F_x &= 0 \\ H_y + F_y &= 0 \\ H_z + W + F_z &= 0 \\ T_{Hxz} + T_{Wxz} + T_{Fxz} &= 0 \\ T_{Hyz} + T_{Wyz} + T_{Fyz} &= 0 \\ T_{Hxy} + T_{Fxy} &= 0 \end{aligned}$$



The coefficient of friction μ and the angle α at which the floor is inclined determine the equations at the foot.

$$F_x = \mu F_z$$

With the slope angle α

$$F_x = \alpha F_z \cos \alpha$$

Of course, when motion must be considered, dynamic conditions come into play according to Newton's Second Law. Force transmitted with the hands is counteracted at the foot. Further, the body must also react with internal forces at all points between the hand and the foot.

Incidence Variable Values

Two concepts can be important when completing OSHA forms. These concepts are *incidence rates* and *severity rates*. On occasion it is necessary to calculate the total injury/illness incident rate of an organization in order to complete OSHA forms. This calculation must include fatalities and all injuries requiring medical treatment beyond mere first aid. The formula for determining the total injury/illness incident rate is as follows:

$$IR = N \times 200,000 \div T$$

IR = Total injury/illness incidence rate

N = Number of injuries, illnesses, and fatalities

T = Total hours worked by all employees during the period in question

The number 200,000 in the formula represents the number of hours 100 employees work in a year ($40 \text{ hours per week} \times 50 \text{ weeks} = 2,000 \text{ hours per year per employee}$). Using the same basic formula with only minor substitutions, safety managers can calculate the following types of incidence rates:

1. Injury rate
2. Illness rate
3. Fatality rate
4. Lost workday cases rate
5. Number of lost workdays rate
6. Specific hazard rate
7. Lost workday injuries rate

NOISE POLLUTION

$$\text{SPL (dB)} = 10 \log_{10} \left(P^2 / P_0^2 \right)$$

$$\text{SPL}_{\text{total}} = 10 \log_{10} \sum 10^{\text{SPL}/10}$$

Point Source Attenuation

$$\Delta \text{SPL (dB)} = 10 \log_{10} (r_1/r_2)^2$$

Line Source Attenuation

$$\Delta \text{SPL (dB)} = 10 \log_{10} (r_1/r_2)$$

where

SPL (dB) = sound pressure level, measured in decibels

P = sound pressure (Pa)

P_0 = reference sound pressure (2×10^{-5} Pa)

$\text{SPL}_{\text{total}}$ = sum of multiple sources

$\Delta \text{SPL (dB)}$ = change in sound pressure level with distance, measured in decibels

r_1 = distance from source to receptor at point 1

r_2 = distance from source to receptor at point 2

PERMISSIBLE NOISE EXPOSURE (OSHA)

Noise dose D should not exceed 100%.

$$D = 100\% \times \sum \frac{C_i}{T_i}$$

where C_i = time spent at specified sound pressure level, SPL, (hours)

T_i = time permitted at SPL (hours)

$$\sum C_i = 8 \text{ (hours)}$$

Noise Level (dBA)	Permissible Time (hr)
80	32
85	16
90	8
95	4
100	2
105	1
110	0.5
115	0.25
120	0.125
125	0.063
130	0.031

If $D > 100\%$, noise abatement required.

If $50\% \leq D \leq 100\%$, hearing conservation program required.

Note: $D = 100\%$ is equivalent to 90 dBA time-weighted average (TWA). $D = 50\%$ equivalent to TWA of 85 dBA.

Hearing conservation program requires: (1) testing employee hearing, (2) providing hearing protection at employee's request, and (3) monitoring noise exposure.

Exposure to impulsive or impact noise should not exceed 140 dB sound pressure level (SPL).

MATHEMATICS

DISCRETE MATH

Symbols

$x \in X$	x is a member of X
$\{\}, \emptyset$	The empty (or null) set
$S \subseteq T$	S is a subset of T
$S \subset T$	S is a proper subset of T
(a,b)	Ordered pair
$P^{(S)}$	Power set of S
(a_1, a_2, \dots, a_n)	n-tuple
$A \times B$	Cartesian product of A and B
$A \cup B$	Union of A and B
$A \cap B$	Intersection of A and B
$\forall x$	Universal qualification for all x; for any x; for each x
$\exists y$	Uniqueness qualification there exists y
A binary relation from A to B is a subset of $A \times B$.	

Matrix of Relation

If $A = \{a_1, a_2, \dots, a_m\}$ and $B = \{b_1, b_2, \dots, b_n\}$ are finite sets containing m and n elements, respectively, then a relation R from A to B can be represented by the $m \times n$ matrix $M_R < [m_{ij}]$, which is defined by:

$$m_{ij} = \begin{cases} 1 & \text{if } (a_i, b_j) \in R \\ 0 & \text{if } (a_i, b_j) \notin R \end{cases}$$

Directed Graphs, or Digraphs, of Relation

A directed graph, or digraph, consists of a set V of vertices (or nodes) together with a set E of ordered pairs of elements of V called edges (or arcs). For edge (a, b), the vertex a is called the initial vertex and vertex b is called the terminal vertex. An edge of form (a, a) is called a loop.

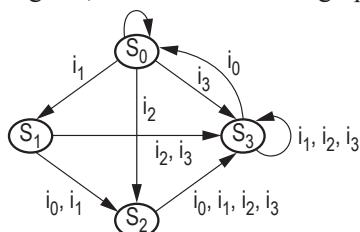
Finite State Machine

A finite state machine consists of a finite set of states $S = \{s_0, s_1, \dots, s_n\}$ and a finite set of inputs I; and a transition function f that assigns to each state and input pair a new state.

A state (or truth) table can be used to represent the finite state machine.

State	Input			
	i_0	i_1	i_2	i_3
s_0	s_0	s_1	s_2	s_3
s_1	s_2	s_2	s_3	s_3
s_2	s_3	s_3	s_3	s_3
s_3	s_0	s_3	s_3	s_3

Another way to represent a finite state machine is to use a state diagram, which is a directed graph with labeled edges.



The characteristic of how a function maps one set (X) to another set (Y) may be described in terms of being either injective, surjective, or bijective.

An injective (one-to-one) relationship exists if, and only if, $\forall x_1, x_2 \in X, \text{ if } f(x_1) = f(x_2), \text{ then } x_1 = x_2$

A surjective (onto) relationship exists when $\forall y \in Y, \exists x \in X$ such that $f(x) = y$

A bijective relationship is both injective (one-to-one) and surjective (onto).

STRAIGHT LINE

The general form of the equation is

$$Ax + By + C = 0$$

The standard form of the equation is

$$y = mx + b,$$

which is also known as the *slope-intercept* form.

The *point-slope* form is $y - y_1 = m(x - x_1)$

Given two points: slope, $m = (y_2 - y_1)/(x_2 - x_1)$

The angle between lines with slopes m_1 and m_2 is

$$\alpha = \arctan [(m_2 - m_1)/(1 + m_2 \cdot m_1)]$$

Two lines are perpendicular if $m_1 = -1/m_2$

The distance between two points is

$$d = \sqrt{(y_2 - y_1)^2 + (x_2 - x_1)^2}$$

QUADRATIC EQUATION

$$ax^2 + bx + c = 0$$

$$x = \text{Roots} = \frac{-b \pm \sqrt{b^2 - 4ac}}{2a}$$

QUADRIC SURFACE (SPHERE)

The standard form of the equation is

$$(x - h)^2 + (y - k)^2 + (z - m)^2 = r^2$$

with center at (h, k, m) .

In a three-dimensional space, the distance between two points is

$$d = \sqrt{(x_2 - x_1)^2 + (y_2 - y_1)^2 + (z_2 - z_1)^2}$$

LOGARITHMS

The logarithm of x to the Base b is defined by

$$\log_b(x) = c, \text{ where } b^c = x$$

Special definitions for $b = e$ or $b = 10$ are:

$$\ln x, \text{ Base } = e$$

$$\log x, \text{ Base } = 10$$

To change from one Base to another:

$$\log_b x = (\log_a x) / (\log_a b)$$

$$\text{e.g., } \ln x = (\log_{10} x) / (\log_{10} e) = 2.302585 (\log_{10} x)$$

Identities

$$\log_b b^n = n$$

$$\log x^c = c \log x; x^c = \text{antilog}(c \log x)$$

$$\log xy = \log x + \log y$$

$$\log_b b = 1; \log 1 = 0$$

$$\log x/y = \log x - \log y$$

ALGEBRA OF COMPLEX NUMBERS

Complex numbers may be designated in rectangular form or polar form. In rectangular form, a complex number is written in terms of its real and imaginary components.

$$z = a + jb, \text{ where}$$

a = the real component,

b = the imaginary component, and

$$j = \sqrt{-1} \text{ (some disciplines use } i = \sqrt{-1})$$

In polar form $z = c \angle \theta$ where

$$c = \sqrt{a^2 + b^2},$$

$$\theta = \tan^{-1}(b/a),$$

$$a = c \cos \theta, \text{ and}$$

$$b = c \sin \theta.$$

Complex numbers can be added and subtracted in rectangular form. If

$$\begin{aligned} z_1 &= a_1 + jb_1 = c_1(\cos \theta_1 + j \sin \theta_1) \\ &= c_1 \angle \theta_1 \text{ and} \end{aligned}$$

$$\begin{aligned} z_2 &= a_2 + jb_2 = c_2(\cos \theta_2 + j \sin \theta_2) \\ &= c_2 \angle \theta_2, \text{ then} \end{aligned}$$

$$z_1 + z_2 = (a_1 + a_2) + j(b_1 + b_2) \text{ and}$$

$$z_1 - z_2 = (a_1 - a_2) + j(b_1 - b_2)$$

While complex numbers can be multiplied or divided in rectangular form, it is more convenient to perform these operations in polar form.

$$z_1 \times z_2 = (c_1 \times c_2) \angle (\theta_1 + \theta_2)$$

$$z_1/z_2 = (c_1/c_2) \angle (\theta_1 - \theta_2)$$

The complex conjugate of a complex number $z_1 = (a_1 + jb_1)$ is defined as $z_1^* = (a_1 - jb_1)$. The product of a complex number and its complex conjugate is $z_1 z_1^* = a_1^2 + b_1^2$.

Polar Coordinate System

$$x = r \cos \theta; y = r \sin \theta; \theta = \arctan(y/x)$$

$$r = |x + jy| = \sqrt{x^2 + y^2}$$

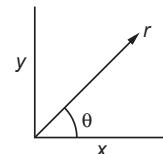
$$x + jy = r(\cos \theta + j \sin \theta) = re^{j\theta}$$

$$[r_1(\cos \theta_1 + j \sin \theta_1)][r_2(\cos \theta_2 + j \sin \theta_2)] = \\ r_1 r_2 [\cos(\theta_1 + \theta_2) + j \sin(\theta_1 + \theta_2)]$$

$$(x + jy)^n = [r(\cos \theta + j \sin \theta)]^n$$

$$= r^n(\cos n\theta + j \sin n\theta)$$

$$\frac{r_1(\cos \theta_1 + j \sin \theta_1)}{r_2(\cos \theta_2 + j \sin \theta_2)} = \frac{r_1}{r_2} [\cos(\theta_1 - \theta_2) + j \sin(\theta_1 - \theta_2)]$$



Euler's Identity

$$e^{j\theta} = \cos \theta + j \sin \theta$$

$$e^{-j\theta} = \cos \theta - j \sin \theta$$

$$\cos \theta = \frac{e^{j\theta} + e^{-j\theta}}{2}, \quad \sin \theta = \frac{e^{j\theta} - e^{-j\theta}}{2j}$$

Roots

If k is any positive integer, any complex number (other than zero) has k distinct roots. The k roots of $r(\cos \theta + j \sin \theta)$ can be found by substituting successively $n = 0, 1, 2, \dots, (k-1)$ in the formula

$$w = k \sqrt{r} \left[\cos\left(\frac{\theta}{k} + n \frac{360^\circ}{k}\right) + j \sin\left(\frac{\theta}{k} + n \frac{360^\circ}{k}\right) \right]$$

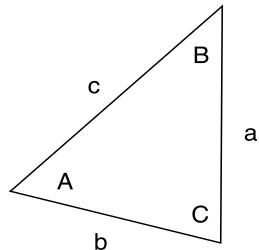
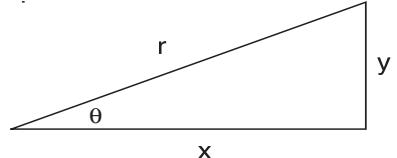
TRIGONOMETRY

Trigonometric functions are defined using a right triangle.

$$\sin \theta = y/r, \cos \theta = x/r$$

$$\tan \theta = y/x, \cot \theta = x/y$$

$$\csc \theta = r/y, \sec \theta = r/x$$



Law of Sines

$$\frac{a}{\sin A} = \frac{b}{\sin B} = \frac{c}{\sin C}$$

Law of Cosines

$$a^2 = b^2 + c^2 - 2bc \cos A$$

$$b^2 = a^2 + c^2 - 2ac \cos B$$

$$c^2 = a^2 + b^2 - 2ab \cos C$$

Brink, R.W., *A First Year of College Mathematics*, D. Appleton-Century Co., Inc., Englewood Cliffs, NJ, 1937.

Identities

$$\cos \theta = \sin(\theta + \pi/2) = -\sin(\theta - \pi/2)$$

$$\sin \theta = \cos(\theta - \pi/2) = -\cos(\theta + \pi/2)$$

$$\csc \theta = 1/\sin \theta$$

$$\sec \theta = 1/\cos \theta$$

$$\tan \theta = \sin \theta / \cos \theta$$

$$\cot \theta = 1/\tan \theta$$

$$\sin^2 \theta + \cos^2 \theta = 1$$

$$\tan^2 \theta + 1 = \sec^2 \theta$$

$$\cot^2 \theta + 1 = \csc^2 \theta$$

$$\sin(\alpha + \beta) = \sin \alpha \cos \beta + \cos \alpha \sin \beta$$

$$\cos(\alpha + \beta) = \cos \alpha \cos \beta - \sin \alpha \sin \beta$$

$$\sin 2\alpha = 2 \sin \alpha \cos \alpha$$

$$\cos 2\alpha = \cos^2 \alpha - \sin^2 \alpha = 1 - 2 \sin^2 \alpha = 2 \cos^2 \alpha - 1$$

$$\tan 2\alpha = (2 \tan \alpha) / (1 - \tan^2 \alpha)$$

$$\cot 2\alpha = (\cot^2 \alpha - 1) / (2 \cot \alpha)$$

$$\tan(\alpha + \beta) = (\tan \alpha + \tan \beta) / (1 - \tan \alpha \tan \beta)$$

$$\cot(\alpha + \beta) = (\cot \alpha \cot \beta - 1) / (\cot \alpha + \cot \beta)$$

$$\sin(\alpha - \beta) = \sin \alpha \cos \beta - \cos \alpha \sin \beta$$

$$\cos(\alpha - \beta) = \cos \alpha \cos \beta + \sin \alpha \sin \beta$$

$$\tan(\alpha - \beta) = (\tan \alpha - \tan \beta) / (1 + \tan \alpha \tan \beta)$$

$$\cot(\alpha - \beta) = (\cot \alpha \cot \beta + 1) / (\cot \beta - \cot \alpha)$$

$$\sin(\alpha/2) = \pm \sqrt{(1 - \cos \alpha)/2}$$

$$\cos(\alpha/2) = \pm \sqrt{(1 + \cos \alpha)/2}$$

$$\tan(\alpha/2) = \pm \sqrt{(1 - \cos \alpha)/(1 + \cos \alpha)}$$

$$\cot(\alpha/2) = \pm \sqrt{(1 + \cos \alpha)/(1 - \cos \alpha)}$$

$$\sin \alpha \sin \beta = (1/2)[\cos(\alpha - \beta) - \cos(\alpha + \beta)]$$

$$\cos \alpha \cos \beta = (1/2)[\cos(\alpha - \beta) + \cos(\alpha + \beta)]$$

$$\sin \alpha \cos \beta = (1/2)[\sin(\alpha + \beta) + \sin(\alpha - \beta)]$$

$$\sin \alpha + \sin \beta = 2 \sin[(1/2)(\alpha + \beta)] \cos[(1/2)(\alpha - \beta)]$$

$$\sin \alpha - \sin \beta = 2 \cos[(1/2)(\alpha + \beta)] \sin[(1/2)(\alpha - \beta)]$$

$$\cos \alpha + \cos \beta = 2 \cos[(1/2)(\alpha + \beta)] \cos[(1/2)(\alpha - \beta)]$$

$$\cos \alpha - \cos \beta = -2 \sin[(1/2)(\alpha + \beta)] \sin[(1/2)(\alpha - \beta)]$$

MENSURATION OF AREAS AND VOLUMES

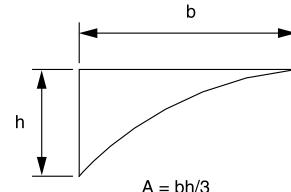
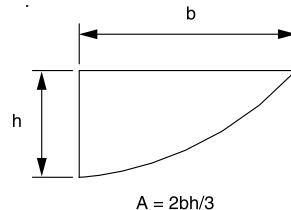
Nomenclature

A = total surface area

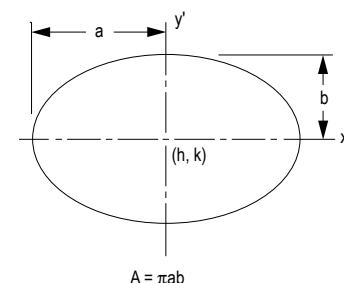
P = perimeter

V = volume

Parabola



Ellipse



$$P_{approx} = 2\pi\sqrt{(a^2 + b^2)/2}$$

$$P = \pi(a+b) \left[1 + (1/2)^2 \lambda^2 + (1/2 \times 1/4)^2 \lambda^4 + (1/2 \times 1/4 \times 3/6)^2 \lambda^6 + (1/2 \times 1/4 \times 3/6 \times 5/8)^2 \lambda^8 + (1/2 \times 1/4 \times 3/6 \times 5/8 \times 7/10)^2 \lambda^{10} + \dots \right],$$

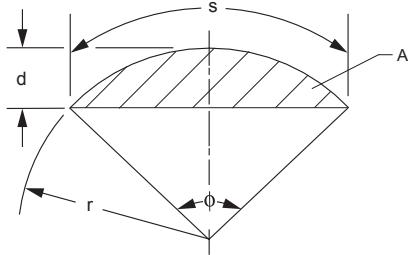
where

$$\lambda = (a - b) / (a + b)$$

◆ Gieck, K., and R. Gieck, *Engineering Formulas*, 6th ed., Gieck Publishing, 1967.

MENSURATION OF AREAS AND VOLUMES (continued)

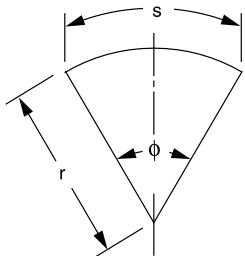
Circular Segment



$$A = [r^2(\phi - \sin \phi)]/2$$

$$\phi = s/r = 2\{\arccos[(r-d)/r]\}$$

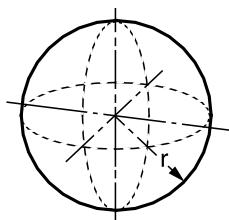
Circular Sector



$$A = \phi r^2/2 = sr/2$$

$$\phi = s/r$$

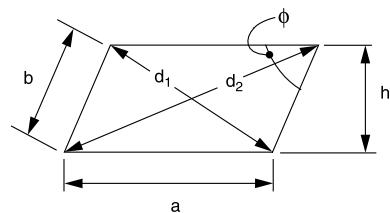
Sphere



$$V = 4\pi r^3/3 = \pi d^3/6$$

$$A = 4\pi r^2 = \pi d^2$$

Parallelogram



$$P = 2(a + b)$$

$$d_1 = \sqrt{a^2 + b^2 - 2ab(\cos \phi)}$$

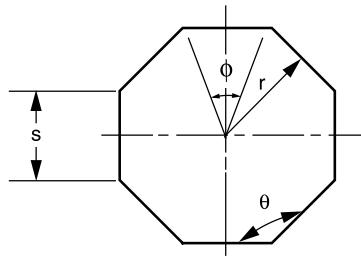
$$d_2 = \sqrt{a^2 + b^2 + 2ab(\cos \phi)}$$

$$d_1^2 + d_2^2 = 2(a^2 + b^2)$$

$$A = ah = ab(\sin \phi)$$

If $a = b$, the parallelogram is a rhombus.

Regular Polygon (n equal sides)



$$\phi = 2\pi/n$$

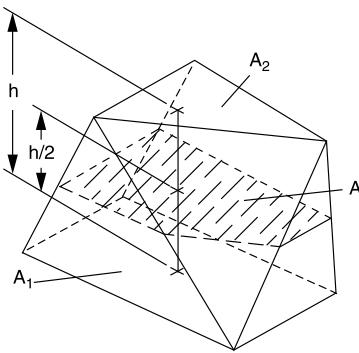
$$\theta = \left[\frac{\pi(n-2)}{n}\right] = \pi\left(1 - \frac{2}{n}\right)$$

$$P = ns$$

$$s = 2r[\tan(\phi/2)]$$

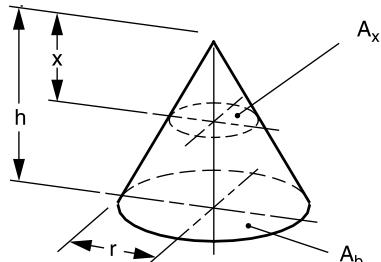
$$A = (nsr)/2$$

Prismoid



$$V = (h/6)(A_1 + A_2 + 4A)$$

Right Circular Cone



$$V = (\pi r^2 h)/3$$

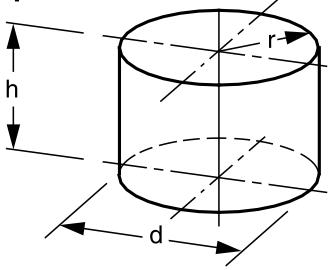
$$A = \text{side area} + \text{base area}$$

$$= \pi r(r + \sqrt{r^2 + h^2})$$

$$A_x : A_b = x^2 : h^2$$

◆ Gieck, K., and R. Gieck, *Engineering Formulas*, 6th ed., Gieck Publishing, 1967.

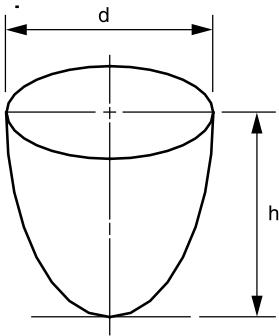
Right Circular Cylinder



$$V = \pi r^2 h = \frac{\pi d^2 h}{4}$$

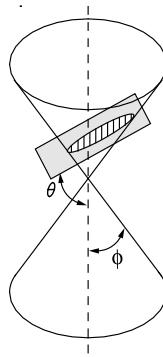
$$A = \text{side area} + \text{end areas} = 2\pi r(h + r)$$

Paraboloid of Revolution



$$V = \frac{\pi d^2 h}{8}$$

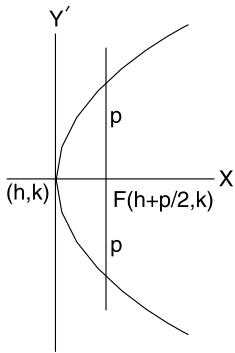
CONIC SECTIONS



$$e = \text{eccentricity} = \cos \theta / (\cos \phi)$$

[Note: X' and Y' , in the following cases, are translated axes.]

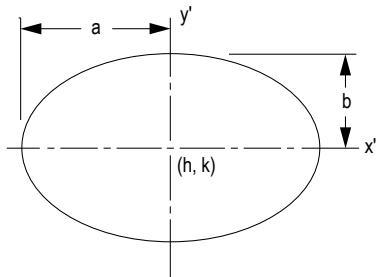
Case 1. Parabola $e = 1$:



$$(y - k)^2 = 2p(x - h); \text{ Center at } (h, k)$$

is the standard form of the equation. When $h = k = 0$,
Focus: $(p/2, 0)$; Directrix: $x = -p/2$

Case 2. Ellipse $e < 1$:



$$\frac{(x - h)^2}{a^2} + \frac{(y - k)^2}{b^2} = 1; \text{ Center at } (h, k)$$

is the standard form of the equation. When $h = k = 0$,

$$\text{Eccentricity: } e = \sqrt{1 - (b^2/a^2)} = c/a$$

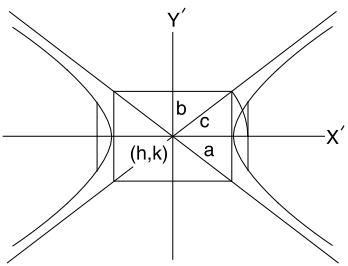
$$b = a\sqrt{1 - e^2};$$

Focus: $(\pm ae, 0)$; Directrix: $x = \pm a/e$

◆ Gieck, K., and R. Gieck, *Engineering Formulas*, 6th ed., Gieck Publishing, 1967.

• Brink, R.W., *A First Year of College Mathematics*, D. Appleton-Century Co., Inc., 1937.

Case 3. Hyperbola $e > 1$:



$$\frac{(x - h)^2}{a^2} - \frac{(y - k)^2}{b^2} = 1; \text{ Center at } (h, k)$$

is the standard form of the equation. When $h = k = 0$,

$$\text{Eccentricity: } e = \sqrt{1 + (b^2/a^2)} = c/a$$

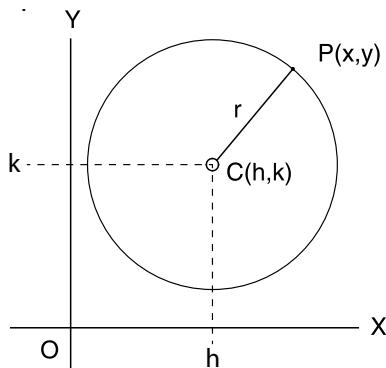
$$b = a\sqrt{e^2 - 1};$$

Focus: $(\pm ae, 0)$; Directrix: $x = \pm a/e$

Case 4. Circle $e = 0$:

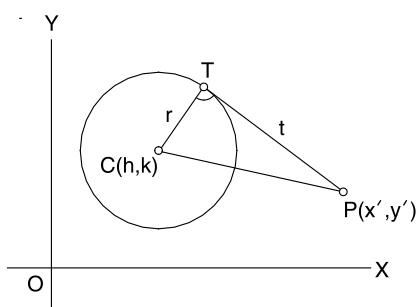
$(x - h)^2 + (y - k)^2 = r^2$, Center at (h, k) is the standard form of the equation with radius

$$r = \sqrt{(x - h)^2 + (y - k)^2}$$



Length of the tangent line from a point on a circle to a point (x', y') :

$$t^2 = (x' - h)^2 + (y' - k)^2 - r^2$$



• Brink, R.W., *A First Year of College Mathematics*, D. Appleton-Century Co., Inc., 1937.

Conic Section Equation

The general form of the conic section equation is

$$Ax^2 + Bxy + Cy^2 + Dx + Ey + F = 0$$

where not both A and C are zero.

If $B^2 - 4AC < 0$, an *ellipse* is defined.

If $B^2 - 4AC > 0$, a *hyperbola* is defined.

If $B^2 - 4AC = 0$, the conic is a *parabola*.

If $A = C$ and $B = 0$, a *circle* is defined.

If $A = B = C = 0$, a *straight line* is defined.

$$x^2 + y^2 + 2ax + 2by + c = 0$$

is the normal form of the conic section equation, if that conic section has a principal axis parallel to a coordinate axis.

$$h = -a; k = -b$$

$$r = \sqrt{a^2 + b^2 - c}$$

If $a^2 + b^2 - c$ is positive, a *circle*, center $(-a, -b)$.

If $a^2 + b^2 - c$ equals zero, a *point* at $(-a, -b)$.

If $a^2 + b^2 - c$ is negative, locus is *imaginary*.

DIFFERENTIAL CALCULUS

The Derivative

For any function $y = f(x)$,

the derivative $= D_x y = dy/dx = y'$

$$y' = \lim_{\Delta x \rightarrow 0} [(\Delta y)/(\Delta x)]$$

$$= \lim_{\Delta x \rightarrow 0} \{[f(x + \Delta x) - f(x)]/(\Delta x)\}$$

y' = the slope of the curve $f(x)$.

Test for a Maximum

$y = f(x)$ is a maximum for

$x = a$, if $f'(a) = 0$ and $f''(a) < 0$.

Test for a Minimum

$y = f(x)$ is a minimum for

$x = a$, if $f'(a) = 0$ and $f''(a) > 0$.

Test for a Point of Inflection

$y = f(x)$ has a point of inflection at $x = a$,

if $f''(a) = 0$, and

if $f''(x)$ changes sign as x increases through

$x = a$.

The Partial Derivative

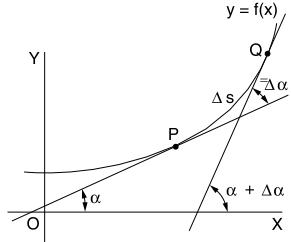
In a function of two independent variables x and y , a derivative with respect to one of the variables may be found if the other variable is *assumed* to remain constant. If y is *kept fixed*, the function

$$z = f(x, y)$$

becomes a function of the *single variable* x , and its derivative (if it exists) can be found. This derivative is called the *partial derivative of z with respect to x*. The partial derivative with respect to x is denoted as follows:

$$\frac{\partial z}{\partial x} = \frac{\partial f(x, y)}{\partial x}$$

The Curvature of Any Curve



The curvature K of a curve at P is the limit of its average curvature for the arc PQ as Q approaches P . This is also expressed as: the curvature of a curve at a given point is the rate-of-change of its inclination with respect to its arc length.

$$K = \lim_{\Delta s \rightarrow 0} \frac{\Delta \alpha}{\Delta s} = \frac{d\alpha}{ds}$$

Curvature in Rectangular Coordinates

$$K = \frac{y'}{\left[1 + (y')^2\right]^{3/2}}$$

When it may be easier to differentiate the function with respect to y rather than x , the notation x' will be used for the derivative.

$$x' = dx/dy$$

$$K = \frac{-x''}{\left[1 + (x')^2\right]^{3/2}}$$

The Radius of Curvature

The *radius of curvature R* at any point on a curve is defined as the absolute value of the reciprocal of the curvature K at that point.

$$R = \frac{1}{|K|} \quad (K \neq 0)$$

$$R = \left| \frac{\left[1 + (y')^2\right]^{3/2}}{|y''|} \right| \quad (y'' \neq 0)$$

L'Hospital's Rule (L'Hôpital's Rule)

If the fractional function $f(x)/g(x)$ assumes one of the indeterminate forms $0/0$ or ∞/∞ (where α is finite or infinite), then

$$\lim_{x \rightarrow \alpha} f(x)/g(x)$$

is equal to the first of the expressions

$$\lim_{x \rightarrow \alpha} \frac{f'(x)}{g'(x)}, \lim_{x \rightarrow \alpha} \frac{f''(x)}{g''(x)}, \lim_{x \rightarrow \alpha} \frac{f'''(x)}{g'''(x)}$$

which is not indeterminate, provided such first indicated limit exists.

INTEGRAL CALCULUS

The definite integral is defined as:

$$\lim_{n \rightarrow \infty} \sum_{i=1}^n f(x_i) \Delta x_i = \int_a^b f(x) dx$$

Also, $\Delta x_i \rightarrow 0$ for all i .

A table of derivatives and integrals is available in the Derivatives and Indefinite Integrals section. The integral equations can be used along with the following methods of integration:

- A. Integration by Parts (integral equation #6),
- B. Integration by Substitution, and
- C. Separation of Rational Fractions into Partial Fractions.

◆ Wade, Thomas L., *Calculus*, Ginn & Company/Simon & Schuster Publishers, 1953.

DERIVATIVES AND INDEFINITE INTEGRALS

In these formulas, u , v , and w represent functions of x . Also, a , c , and n represent constants. All arguments of the trigonometric functions are in radians. A constant of integration should be added to the integrals. To avoid terminology difficulty, the following definitions are followed: $\arcsin u = \sin^{-1} u$, $(\sin u)^{-1} = 1/\sin u$.

1. $dc/dx = 0$
2. $dx/dx = 1$
3. $d(cu)/dx = c du/dx$
4. $d(u + v - w)/dx = du/dx + dv/dx - dw/dx$
5. $d(uv)/dx = u dv/dx + v du/dx$
6. $d(uvw)/dx = uv dw/dx + uw dv/dx + vw du/dx$
7. $\frac{d(u/v)}{dx} = \frac{v du/dx - u dv/dx}{v^2}$
8. $d(u^n)/dx = nu^{n-1} du/dx$
9. $d[f(u)]/dx = \{d[f(u)]/du\} du/dx$
10. $du/dx = 1/(dx/du)$
11. $\frac{d(\log_a u)}{dx} = (\log_a e) \frac{1}{u} \frac{du}{dx}$
12. $\frac{d(\ln u)}{dx} = \frac{1}{u} \frac{du}{dx}$
13. $\frac{d(a^u)}{dx} = (\ln a) a^u \frac{du}{dx}$
14. $d(e^u)/dx = e^u du/dx$
15. $d(u^v)/dx = vu^{v-1} du/dx + (\ln u) u^v dv/dx$
16. $d(\sin u)/dx = \cos u du/dx$
17. $d(\cos u)/dx = -\sin u du/dx$
18. $d(\tan u)/dx = \sec^2 u du/dx$
19. $d(\cot u)/dx = -\csc^2 u du/dx$
20. $d(\sec u)/dx = \sec u \tan u du/dx$
21. $d(\csc u)/dx = -\csc u \cot u du/dx$
22. $\frac{d(\sin^{-1} u)}{dx} = \frac{1}{\sqrt{1-u^2}} \frac{du}{dx} \quad (-\pi/2 \leq \sin^{-1} u \leq \pi/2)$
23. $\frac{d(\cos^{-1} u)}{dx} = -\frac{1}{\sqrt{1-u^2}} \frac{du}{dx} \quad (0 \leq \cos^{-1} u \leq \pi)$
24. $\frac{d(\tan^{-1} u)}{dx} = \frac{1}{1+u^2} \frac{du}{dx} \quad (-\pi/2 < \tan^{-1} u < \pi/2)$
25. $\frac{d(\cot^{-1} u)}{dx} = -\frac{1}{1+u^2} \frac{du}{dx} \quad (0 < \cot^{-1} u < \pi)$
26. $\frac{d(\sec^{-1} u)}{dx} = \frac{1}{u\sqrt{u^2-1}} \frac{du}{dx} \quad (0 < \sec^{-1} u < \pi/2) \quad (-\pi \leq \sec^{-1} u < -\pi/2)$
27. $\frac{d(\csc^{-1} u)}{dx} = -\frac{1}{u\sqrt{u^2-1}} \frac{du}{dx} \quad (0 < \csc^{-1} u \leq \pi/2) \quad (-\pi < \csc^{-1} u \leq -\pi/2)$
1. $\int df(x) = f(x)$
2. $\int dx = x$
3. $\int af(x) dx = a \int f(x) dx$
4. $\int [u(x) \pm v(x)] dx = \int u(x) dx \pm \int v(x) dx$
5. $\int x^m dx = \frac{x^{m+1}}{m+1} \quad (m \neq -1)$
6. $\int u(x) dv(x) = u(x) v(x) - \int v(x) du(x)$
7. $\int \frac{dx}{ax+b} = \frac{1}{a} \ln|ax+b|$
8. $\int \frac{dx}{\sqrt{x}} = 2\sqrt{x}$
9. $\int a^x dx = \frac{a^x}{\ln a}$
10. $\int \sin x dx = -\cos x$
11. $\int \cos x dx = \sin x$
12. $\int \sin^2 x dx = \frac{x}{2} - \frac{\sin 2x}{4}$
13. $\int \cos^2 x dx = \frac{x}{2} + \frac{\sin 2x}{4}$
14. $\int x \sin x dx = \sin x - x \cos x$
15. $\int x \cos x dx = \cos x + x \sin x$
16. $\int \sin x \cos x dx = (\sin^2 x)/2$
17. $\int \sin ax \cos bx dx = -\frac{\cos(a-b)x}{2(a-b)} - \frac{\cos(a+b)x}{2(a+b)} \quad (a^2 \neq b^2)$
18. $\int \tan x dx = -\ln|\cos x| = \ln|\sec x|$
19. $\int \cot x dx = -\ln|\csc x| = \ln|\sin x|$
20. $\int \tan^2 x dx = \tan x - x$
21. $\int \cot^2 x dx = -\cot x - x$
22. $\int e^{ax} dx = (1/a) e^{ax}$
23. $\int x e^{ax} dx = (e^{ax}/a^2)(ax-1)$
24. $\int \ln x dx = x [\ln(x)-1] \quad (x > 0)$
25. $\int \frac{dx}{a^2+x^2} = \frac{1}{a} \tan^{-1} \frac{x}{a} \quad (a \neq 0)$
26. $\int \frac{dx}{ax^2+c} = \frac{1}{\sqrt{ac}} \tan^{-1} \left(x \sqrt{\frac{a}{c}} \right), \quad (a > 0, c > 0)$
- 27a. $\int \frac{dx}{ax^2+bx+c} = \frac{2}{\sqrt{4ac-b^2}} \tan^{-1} \frac{2ax+b}{\sqrt{4ac-b^2}} \quad (4ac-b^2 > 0)$
- 27b. $\int \frac{dx}{ax^2+bx+c} = \frac{1}{\sqrt{b^2-4ac}} \ln \left| \frac{2ax+b-\sqrt{b^2-4ac}}{2ax+b+\sqrt{b^2-4ac}} \right| \quad (b^2-4ac > 0)$
- 27c. $\int \frac{dx}{ax^2+bx+c} = -\frac{2}{2ax+b}, \quad (b^2-4ac = 0)$

CENTROIDS AND MOMENTS OF INERTIA

The *location of the centroid of an area*, bounded by the axes and the function $y = f(x)$, can be found by integration.

$$x_c = \frac{\int x dA}{A}$$

$$y_c = \frac{\int y dA}{A}$$

$$A = \int f(x) dx$$

$$dA = f(x) dx = g(y) dy$$

The *first moment of area* with respect to the y -axis and the x -axis, respectively, are:

$$M_y = \int x dA = x_c A$$

$$M_x = \int y dA = y_c A$$

The *moment of inertia (second moment of area)* with respect to the y -axis and the x -axis, respectively, are:

$$I_y = \int x^2 dA$$

$$I_x = \int y^2 dA$$

The moment of inertia taken with respect to an axis passing through the area's centroid is the *centroidal moment of inertia*. The *parallel axis theorem* for the moment of inertia with respect to another axis parallel with and located d units from the centroidal axis is expressed by

$$I_{\text{parallel axis}} = I_c + Ad^2$$

In a plane, $J = \int r^2 dA = I_x + I_y$

PROGRESSIONS AND SERIES

Arithmetic Progression

To determine whether a given finite sequence of numbers is an arithmetic progression, subtract each number from the following number. If the differences are equal, the series is arithmetic.

1. The first term is a .
2. The common difference is d .
3. The number of terms is n .
4. The last or n th term is l .
5. The sum of n terms is S .

$$l = a + (n - 1)d$$

$$S = n(a + l)/2 = n [2a + (n - 1) d]/2$$

Geometric Progression

To determine whether a given finite sequence is a geometric progression (G.P.), divide each number after the first by the preceding number. If the quotients are equal, the series is geometric:

1. The first term is a .
2. The common ratio is r .
3. The number of terms is n .
4. The last or n th term is l .
5. The sum of n terms is S .

$$l = ar^{n-1}$$

$$S = a (1 - r^n)/(1 - r); r \neq 1$$

$$S = (a - rl)/(1 - r); r \neq 1$$

$$\lim_{n \rightarrow \infty} S_n = a/(1 - r); r < 1$$

A G.P. converges if $|r| < 1$ and it diverges if $|r| > 1$.

Properties of Series

$$\sum_{i=1}^n c = nc; \quad c = \text{constant}$$

$$\sum_{i=1}^n cx_i = c \sum_{i=1}^n x_i$$

$$\sum_{i=1}^n (x_i + y_i - z_i) = \sum_{i=1}^n x_i + \sum_{i=1}^n y_i - \sum_{i=1}^n z_i$$

$$\sum_{x=1}^n x = (n + n^2)/2$$

Power Series

$$\sum_{i=0}^{\infty} a_i (x - a)^i$$

1. A power series, which is convergent in the interval $-R < x < R$, defines a function of x that is continuous for all values of x within the interval and is said to represent the function in that interval.
2. A power series may be differentiated term by term within its interval of convergence. The resulting series has the same interval of convergence as the original series (except possibly at the end points of the series).
3. A power series may be integrated term by term provided the limits of integration are within the interval of convergence of the series.
4. Two power series may be added, subtracted, or multiplied, and the resulting series in each case is convergent, at least, in the interval common to the two series.
5. Using the process of long division (as for polynomials), two power series may be divided one by the other within their common interval of convergence.

Taylor's Series

$$f(x) = f(a) + \frac{f'(a)}{1!}(x - a) + \frac{f''(a)}{2!}(x - a)^2 + \dots + \frac{f^{(n)}(a)}{n!}(x - a)^n + \dots$$

is called *Taylor's series*, and the function $f(x)$ is said to be expanded about the point a in a Taylor's series.

If $a = 0$, the Taylor's series equation becomes a *Maclaurin's series*.

DIFFERENTIAL EQUATIONS

A common class of ordinary linear differential equations is

$$b_n \frac{d^n y(x)}{dx^n} + \dots + b_1 \frac{dy(x)}{dx} + b_0 y(x) = f(x)$$

where $b_n, \dots, b_p, \dots, b_1, b_0$ are constants.

When the equation is a homogeneous differential equation, $f(x) = 0$, the solution is

$$y_h(x) = C_1 e^{r_1 x} + C_2 e^{r_2 x} + \dots + C_i e^{r_i x} + \dots + C_n e^{r_n x}$$

where r_n is the n th distinct root of the characteristic polynomial $P(x)$ with

$$P(r) = b_n r^n + b_{n-1} r^{n-1} + \dots + b_1 r + b_0$$

If the root $r_1 = r_2$, then $C_2 e^{r_2 x}$ is replaced with $C_2 x e^{r_1 x}$.

Higher orders of multiplicity imply higher powers of x . The complete solution for the differential equation is

$$y(x) = y_h(x) + y_p(x),$$

where $y_p(x)$ is any particular solution with $f(x)$ present. If $f(x)$ has $e^{r_n x}$ terms, then resonance is manifested. Furthermore, specific $f(x)$ forms result in specific $y_p(x)$ forms, some of which are:

$f(x)$	$y_p(x)$
A	B
$Ae^{\alpha x}$	$Be^{\alpha x}, \alpha \neq r_n$
$A_1 \sin \omega x + A_2 \cos \omega x$	$B_1 \sin \omega x + B_2 \cos \omega x$

If the independent variable is time t , then transient dynamic solutions are implied.

First-Order Linear Homogeneous Differential Equations with Constant Coefficients

$y' + ay = 0$, where a is a real constant:

Solution, $y = Ce^{-at}$

where C = a constant that satisfies the initial conditions.

First-Order Linear Nonhomogeneous Differential Equations

$$\tau \frac{dy}{dt} + y = Kx(t) \quad x(t) = \begin{cases} A & t < 0 \\ B & t > 0 \end{cases}$$

$$y(0) = KA$$

τ is the time constant

K is the gain

The solution is

$$y(t) = KA + (KB - KA) \left(1 - \exp\left(-\frac{t}{\tau}\right)\right) \text{ or}$$

$$\frac{t}{\tau} = \ln \left[\frac{KB - KA}{KB - y} \right]$$

Second-Order Linear Homogeneous Differential Equations with Constant Coefficients

An equation of the form

$$y'' + ay' + by = 0$$

can be solved by the method of undetermined coefficients where a solution of the form $y = Ce^{rx}$ is sought. Substitution of this solution gives

$$(r^2 + ar + b) Ce^{rx} = 0$$

and since Ce^{rx} cannot be zero, the characteristic equation must vanish or

$$r^2 + ar + b = 0$$

The roots of the characteristic equation are

$$r_{1,2} = \frac{-a \pm \sqrt{a^2 - 4b}}{2}$$

and can be real and distinct for $a^2 > 4b$, real and equal for $a^2 = 4b$, and complex for $a^2 < 4b$.

If $a^2 > 4b$, the solution is of the form (overdamped)

$$y = C_1 e^{r_1 x} + C_2 e^{r_2 x}$$

If $a^2 = 4b$, the solution is of the form (critically damped)

$$y = (C_1 + C_2 x) e^{r x}$$

If $a^2 < 4b$, the solution is of the form (underdamped)

$$y = e^{\alpha x} (C_1 \cos \beta x + C_2 \sin \beta x), \text{ where}$$

$$\alpha = -a/2$$

$$\beta = \frac{\sqrt{4b - a^2}}{2}$$

FOURIER TRANSFORM

The Fourier transform pair, one form of which is

$$F(\omega) = \int_{-\infty}^{\infty} f(t) e^{-j\omega t} dt$$

$$f(t) = [1/(2\pi)] \int_{-\infty}^{\infty} F(\omega) e^{j\omega t} d\omega$$

can be used to characterize a broad class of signal models in terms of their frequency or spectral content. Some useful transform pairs are:

$f(t)$	$F(\omega)$
$\delta(t)$	1
$u(t)$	$\pi\delta(\omega) + 1/j\omega$
$u\left(t + \frac{\tau}{2}\right) - u\left(t - \frac{\tau}{2}\right) = r_{rect} \frac{t}{\tau}$	$\tau \frac{\sin(\omega\tau/2)}{\omega\tau/2}$
$e^{j\omega_o t}$	$2\pi\delta(\omega - \omega_o)$

Some mathematical liberties are required to obtain the second and fourth form. Other Fourier transforms are derivable from the Laplace transform by replacing s with $j\omega$ provided

$$f(t) = 0, t < 0$$

$$\int_0^{\infty} |f(t)| dt < \infty$$

FOURIER SERIES

Every periodic function $f(t)$ which has the period $T = 2\pi/\omega_0$ and has certain continuity conditions can be represented by a series plus a constant

$$f(t) = a_0 + \sum_{n=1}^{\infty} [a_n \cos(n\omega_0 t) + b_n \sin(n\omega_0 t)]$$

The above holds if $f(t)$ has a continuous derivative $f'(t)$ for all t . It should be noted that the various sinusoids present in the series are orthogonal on the interval 0 to T and as a result the coefficients are given by

$$a_0 = (1/T) \int_0^T f(t) dt$$

$$a_n = (2/T) \int_0^T f(t) \cos(n\omega_0 t) dt \quad n = 1, 2, \dots$$

$$b_n = (2/T) \int_0^T f(t) \sin(n\omega_0 t) dt \quad n = 1, 2, \dots$$

The constants a_n and b_n are the *Fourier coefficients* of $f(t)$ for the interval 0 to T and the corresponding series is called the *Fourier series of $f(t)$* over the same interval.

The integrals have the same value when evaluated over any interval of length T .

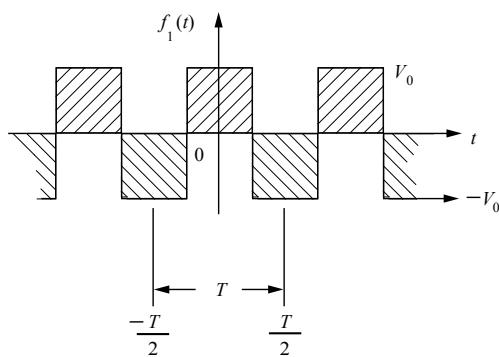
If a Fourier series representing a periodic function is truncated after term $n = N$ the mean square value F_N^2 of the truncated series is given by Parseval's relation. This relation says that the mean-square value is the sum of the mean-square values of the Fourier components, or

$$F_N^2 = a_0^2 + (1/2) \sum_{n=1}^N (a_n^2 + b_n^2)$$

and the RMS value is then defined to be the square root of this quantity or F_N .

Three useful and common Fourier series forms are defined in terms of the following graphs (with $\omega_0 = 2\pi/T$).

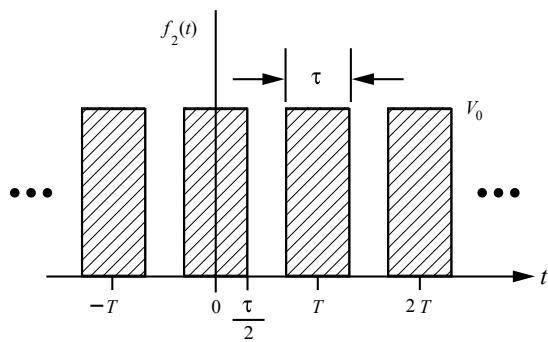
Given:



then

$$f_1(t) = \sum_{\substack{n=1 \\ (n \text{ odd})}}^{\infty} (-1)^{(n-1)/2} (4V_0/n\pi) \cos(n\omega_0 t)$$

Given:

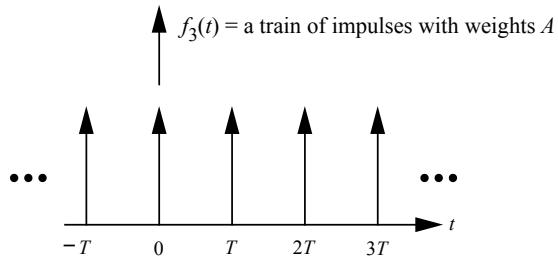


then

$$f_2(t) = \frac{V_0\tau}{T} + \frac{2V_0\tau}{T} \sum_{n=1}^{\infty} \frac{\sin(n\pi\tau/T)}{(n\pi\tau/T)} \cos(n\omega_0 t)$$

$$f_2(t) = \frac{V_0\tau}{T} \sum_{n=-\infty}^{\infty} \frac{\sin(n\pi\tau/T)}{(n\pi\tau/T)} e^{jn\omega_0 t}$$

Given:



then

$$f_3(t) = \sum_{n=-\infty}^{\infty} A\delta(t - nT)$$

$$f_3(t) = (A/T) + (2A/T) \sum_{n=1}^{\infty} \cos(n\omega_0 t)$$

$$f_3(t) = (A/T) \sum_{n=-\infty}^{\infty} e^{jn\omega_0 t}$$

The Fourier Transform and its Inverse

$$X(f) = \int_{-\infty}^{+\infty} x(t) e^{-j2\pi ft} dt$$

$$x(t) = \int_{-\infty}^{+\infty} X(f) e^{j2\pi ft} df$$

We say that $x(t)$ and $X(f)$ form a *Fourier transform pair*:

$$x(t) \leftrightarrow X(f)$$

Fourier Transform Pairs

$x(t)$	$X(f)$
1	$\delta(f)$
$\delta(t)$	1
$u(t)$	$\frac{1}{2}\delta(f) + \frac{1}{j2\pi f}$
$\Pi(t/\tau)$	$\tau \operatorname{sinc}(\tau f)$
$\operatorname{sinc}(Bt)$	$\frac{1}{B}\Pi(f/B)$
$\Lambda(t/\tau)$	$\tau \operatorname{sinc}^2(\tau f)$
$e^{-at}u(t)$	$\frac{1}{a+j2\pi f} \quad a > 0$
$te^{-at}u(t)$	$\frac{1}{(a+j2\pi f)^2} \quad a > 0$
$e^{-a t }$	$\frac{2a}{a^2+(2\pi f)^2} \quad a > 0$
$e^{-(at)^2}$	$\frac{\sqrt{\pi}}{a} e^{-(\pi f/a)^2}$
$\cos(2\pi f_0 t + \theta)$	$\frac{1}{2}[e^{j\theta}\delta(f-f_0) + e^{-j\theta}\delta(f+f_0)]$
$\sin(2\pi f_0 t + \theta)$	$\frac{1}{2j}[e^{j\theta}\delta(f-f_0) - e^{-j\theta}\delta(f+f_0)]$
$\sum_{n=-\infty}^{n=+\infty} \delta(t-nT_s)$	$f_s \sum_{k=-\infty}^{k=+\infty} \delta(f-kf_s) \quad f_s = \frac{1}{T_s}$

Fourier Transform Theorems

Linearity	$ax(t) + by(t)$	$aX(f) + bY(f)$
Scale change	$x(at)$	$\frac{1}{ a }X\left(\frac{f}{a}\right)$
Time reversal	$x(-t)$	$X(-f)$
Duality	$X(t)$	$x(-f)$
Time shift	$x(t-t_0)$	$X(f)e^{-j2\pi f t_0}$
Frequency shift	$x(t)e^{j2\pi f_0 t}$	$X(f-f_0)$
Modulation	$x(t)\cos 2\pi f_0 t$	$\frac{1}{2}X(f-f_0) + \frac{1}{2}X(f+f_0)$
Multiplication	$x(t)y(t)$	$X(f)*Y(f)$
Convolution	$x(t)*y(t)$	$X(f)Y(f)$
Differentiation	$\frac{d^n x(t)}{dt^n}$	$(j2\pi f)^n X(f)$
Integration	$\int_{-\infty}^t x(\lambda)d\lambda$	$\frac{1}{j2\pi f}X(f) + \frac{1}{2}X(0)\delta(f)$

where:

$$\operatorname{sinc}(t) = \frac{\sin(\pi t)}{\pi t}$$

$$\Pi(t) = \begin{cases} 1, & |t| \leq \frac{1}{2} \\ 0, & \text{otherwise} \end{cases}$$

$$\Lambda(t) = \begin{cases} 1 - |t|, & |t| \leq 1 \\ 0, & \text{otherwise} \end{cases}$$

LAPLACE TRANSFORMS

The unilateral Laplace transform pair

$$F(s) = \int_0^\infty f(t)e^{-st} dt$$

$$f(t) = \frac{1}{2\pi j} \int_{\sigma-j\infty}^{\sigma+j\infty} F(s)e^{st} ds$$

$$\text{where } s = \sigma + j\omega$$

represents a powerful tool for the transient and frequency response of linear time invariant systems. Some useful Laplace transform pairs are:

$f(t)$	$F(s)$
$\delta(t)$, Impulse at $t = 0$	1
$u(t)$, Step at $t = 0$	$1/s$
$t[u(t)]$, Ramp at $t = 0$	$1/s^2$
$e^{-\alpha t}$	$1/(s + \alpha)$
$te^{-\alpha t}$	$1/(s + \alpha)^2$
$e^{-\alpha t} \sin \beta t$	$\beta/[(s + \alpha)^2 + \beta^2]$
$e^{-\alpha t} \cos \beta t$	$(s + \alpha)/[(s + \alpha)^2 + \beta^2]$
$\frac{d^n f(t)}{dt^n}$	$s^n F(s) - \sum_{m=0}^{n-1} s^{n-m-1} \frac{d^m f(0)}{dt^m}$
$\int_0^t f(\tau) d\tau$	$(1/s)F(s)$
$\int_0^\infty x(t-\tau)h(\tau)d\tau$	$H(s)X(s)$
$f(t-\tau) u(t-\tau)$	$e^{-\tau s} F(s)$
$\lim_{t \rightarrow \infty} f(t)$	$\lim_{s \rightarrow 0} sF(s)$
$\lim_{t \rightarrow 0} f(t)$	$\lim_{s \rightarrow \infty} sF(s)$

The last two transforms represent the Final Value Theorem (F.V.T.) and Initial Value Theorem (I.V.T.), respectively. It is assumed that the limits exist.

MATRICES

A matrix is an ordered rectangular array of numbers with m rows and n columns. The element a_{ij} refers to row i and column j .

Multiplication of Two Matrices

$$A = \begin{bmatrix} A & B \\ C & D \\ E & F \end{bmatrix} \quad A_{3,2} \text{ is a 3-row, 2-column matrix}$$

$$B = \begin{bmatrix} H & I \\ J & K \end{bmatrix} \quad B_{2,2} \text{ is a 2-row, 2-column matrix}$$

In order for multiplication to be possible, the number of columns in A must equal the number of rows in B.

Multiplying matrix B by matrix A occurs as follows:

$$C = \begin{bmatrix} A & B \\ C & D \\ E & F \end{bmatrix} \cdot \begin{bmatrix} H & I \\ J & K \end{bmatrix}$$

$$C = \begin{bmatrix} (A \cdot H + B \cdot J) & (A \cdot I + B \cdot K) \\ (C \cdot H + D \cdot J) & (C \cdot I + D \cdot K) \\ (E \cdot H + F \cdot J) & (E \cdot I + F \cdot K) \end{bmatrix}$$

Matrix multiplication is not commutative.

Addition

$$\begin{bmatrix} A & B & C \\ D & E & F \end{bmatrix} + \begin{bmatrix} G & H & I \\ J & K & L \end{bmatrix} = \begin{bmatrix} A+G & B+H & C+I \\ D+J & E+K & F+L \end{bmatrix}$$

Identity Matrix

The matrix $I = (a_{ij})$ is a square $n \times n$ matrix with 1's on the diagonal and 0's everywhere else.

Matrix Transpose

Rows become columns. Columns become rows.

$$A = \begin{bmatrix} A & B & C \\ D & E & F \end{bmatrix} \quad A^T = \begin{bmatrix} A & D \\ B & E \\ C & F \end{bmatrix}$$

Inverse []⁻¹

The inverse B of a square $n \times n$ matrix A is

$$B = A^{-1} = \frac{\text{adj}(A)}{|A|}, \text{ where}$$

$\text{adj}(A)$ = adjoint of A (obtained by replacing A^T elements with their cofactors) and $|A|$ = determinant of A .

$$[A][A]^{-1} = [A]^{-1}[A] = [I] \text{ where } I \text{ is the identity matrix.}$$

DETERMINANTS

A determinant of order n consists of n^2 numbers, called the elements of the determinant, arranged in n rows and n columns and enclosed by two vertical lines.

In any determinant, the *minor* of a given element is the determinant that remains after all of the elements are struck out that lie in the same row and in the same column as the given element. Consider an element which lies in the j th column and the i th row. The *cofactor* of this element is the value of the minor of the element (if $i + j$ is even), and it is the negative of the value of the minor of the element (if $i + j$ is odd).

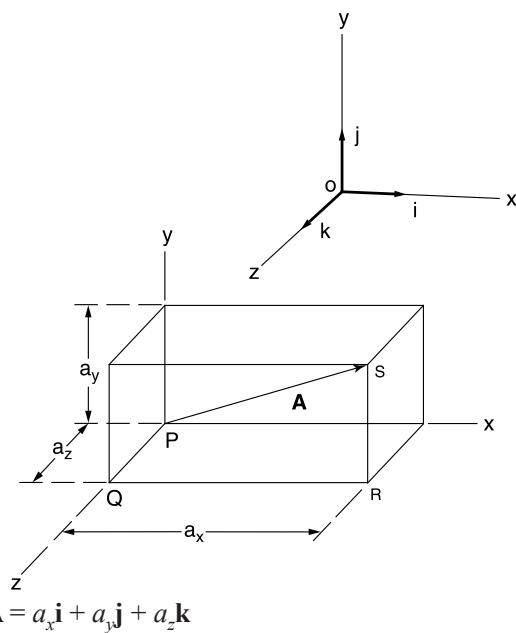
If n is greater than 1, the *value* of a determinant of order n is the sum of the n products formed by multiplying each element of some specified row (or column) by its cofactor. This sum is called the *expansion of the determinant* [according to the elements of the specified row (or column)]. For a second-order determinant:

$$\begin{vmatrix} a_1 & a_2 \\ b_1 & b_2 \end{vmatrix} = a_1 b_2 - a_2 b_1$$

For a third-order determinant:

$$\begin{vmatrix} a_1 & a_2 & a_3 \\ b_1 & b_2 & b_3 \\ c_1 & c_2 & c_3 \end{vmatrix} = a_1 b_2 c_3 + a_2 b_3 c_1 + a_3 b_1 c_2 - a_3 b_2 c_1 - a_2 b_1 c_3 - a_1 b_3 c_2$$

VECTORS



Addition and subtraction:

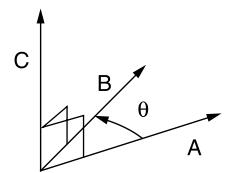
$$\begin{aligned} \mathbf{A} + \mathbf{B} &= (a_x + b_x)\mathbf{i} + (a_y + b_y)\mathbf{j} + (a_z + b_z)\mathbf{k} \\ \mathbf{A} - \mathbf{B} &= (a_x - b_x)\mathbf{i} + (a_y - b_y)\mathbf{j} + (a_z - b_z)\mathbf{k} \end{aligned}$$

The *dot product* is a *scalar product* and represents the projection of \mathbf{B} onto \mathbf{A} times $|\mathbf{A}|$. It is given by

$$\begin{aligned} \mathbf{A} \cdot \mathbf{B} &= a_x b_x + a_y b_y + a_z b_z \\ &= |\mathbf{A}| |\mathbf{B}| \cos \theta = \mathbf{B} \cdot \mathbf{A} \end{aligned}$$

The *cross product* is a *vector product* of magnitude $|\mathbf{B}| |\mathbf{A}| \sin \theta$ which is perpendicular to the plane containing \mathbf{A} and \mathbf{B} . The product is

$$\mathbf{A} \times \mathbf{B} = \begin{vmatrix} \mathbf{i} & \mathbf{j} & \mathbf{k} \\ a_x & a_y & a_z \\ b_x & b_y & b_z \end{vmatrix} = -\mathbf{B} \times \mathbf{A}$$



The sense of $\mathbf{A} \times \mathbf{B}$ is determined by the right-hand rule.

$$\mathbf{A} \times \mathbf{B} = |\mathbf{A}| |\mathbf{B}| \mathbf{n} \sin \theta, \text{ where}$$

\mathbf{n} = unit vector perpendicular to the plane of \mathbf{A} and \mathbf{B} .

Gradient, Divergence, and Curl

$$\nabla \phi = \left(\frac{\partial}{\partial x} \mathbf{i} + \frac{\partial}{\partial y} \mathbf{j} + \frac{\partial}{\partial z} \mathbf{k} \right) \phi$$

$$\nabla \cdot \mathbf{V} = \left(\frac{\partial}{\partial x} \mathbf{i} + \frac{\partial}{\partial y} \mathbf{j} + \frac{\partial}{\partial z} \mathbf{k} \right) \cdot (V_1 \mathbf{i} + V_2 \mathbf{j} + V_3 \mathbf{k})$$

$$\nabla \times \mathbf{V} = \left(\frac{\partial}{\partial x} \mathbf{i} + \frac{\partial}{\partial y} \mathbf{j} + \frac{\partial}{\partial z} \mathbf{k} \right) \times (V_1 \mathbf{i} + V_2 \mathbf{j} + V_3 \mathbf{k})$$

The Laplacian of a scalar function ϕ is

$$\nabla^2 \phi = \frac{\partial^2 \phi}{\partial x^2} + \frac{\partial^2 \phi}{\partial y^2} + \frac{\partial^2 \phi}{\partial z^2}$$

Identities

$$\mathbf{A} \cdot \mathbf{B} = \mathbf{B} \cdot \mathbf{A}; \mathbf{A} \cdot (\mathbf{B} + \mathbf{C}) = \mathbf{A} \cdot \mathbf{B} + \mathbf{A} \cdot \mathbf{C}$$

$$\mathbf{A} \cdot \mathbf{A} = |\mathbf{A}|^2$$

$$\mathbf{i} \cdot \mathbf{i} = \mathbf{j} \cdot \mathbf{j} = \mathbf{k} \cdot \mathbf{k} = 1$$

$$\mathbf{i} \cdot \mathbf{j} = \mathbf{j} \cdot \mathbf{k} = \mathbf{k} \cdot \mathbf{i} = 0$$

If $\mathbf{A} \cdot \mathbf{B} = 0$, then either $\mathbf{A} = 0$, $\mathbf{B} = 0$, or \mathbf{A} is perpendicular to \mathbf{B} .

$$\mathbf{A} \times \mathbf{B} = -\mathbf{B} \times \mathbf{A}$$

$$\mathbf{A} \times (\mathbf{B} + \mathbf{C}) = (\mathbf{A} \times \mathbf{B}) + (\mathbf{A} \times \mathbf{C})$$

$$(\mathbf{B} + \mathbf{C}) \times \mathbf{A} = (\mathbf{B} \times \mathbf{A}) + (\mathbf{C} \times \mathbf{A})$$

$$\mathbf{i} \times \mathbf{i} = \mathbf{j} \times \mathbf{j} = \mathbf{k} \times \mathbf{k} = \mathbf{0}$$

$$\mathbf{i} \times \mathbf{j} = \mathbf{k} = -\mathbf{j} \times \mathbf{i}; \mathbf{j} \times \mathbf{k} = \mathbf{i} = -\mathbf{k} \times \mathbf{j}$$

$$\mathbf{k} \times \mathbf{i} = \mathbf{j} = -\mathbf{i} \times \mathbf{k}$$

If $\mathbf{A} \times \mathbf{B} = \mathbf{0}$, then either $\mathbf{A} = \mathbf{0}$, $\mathbf{B} = \mathbf{0}$, or \mathbf{A} is parallel to \mathbf{B} .

$$\nabla^2 \phi = \nabla \cdot (\nabla \phi) = (\nabla \cdot \nabla) \phi$$

$$\nabla \times \nabla \phi = \mathbf{0}$$

$$\nabla \cdot (\nabla \times \mathbf{A}) = \mathbf{0}$$

$$\nabla \times (\nabla \times \mathbf{A}) = \nabla (\nabla \cdot \mathbf{A}) - \nabla^2 \mathbf{A}$$

DIFFERENCE EQUATIONS

Any system whose input $v(t)$ and output $y(t)$ are defined only at the equally spaced intervals

$$f(t) = y' = \frac{y_{i+1} - y_i}{t_{i+1} - t_i}$$

can be described by a difference equation.

First-Order Linear Difference Equation

$$\Delta t = t_{i+1} - t_i$$

$$y_{i+1} = y_i + y'(\Delta t)$$

NUMERICAL METHODS

Newton's Method for Root Extraction

Given a function $f(x)$ which has a simple root of $f(x) = 0$ at $x = a$ an important computational task would be to find that root. If $f(x)$ has a continuous first derivative then the $(j+1)$ st estimate of the root is

$$a^{j+1} = a^j - \left. \frac{f(x)}{\frac{df(x)}{dx}} \right|_{x=a^j}$$

The initial estimate of the root a^0 must be near enough to the actual root to cause the algorithm to converge to the root.

Newton's Method of Minimization

Given a scalar value function

$$h(\mathbf{x}) = h(x_1, x_2, \dots, x_n)$$

find a vector $\mathbf{x}^* \in R_n$ such that

$$h(\mathbf{x}^*) \leq h(\mathbf{x}) \text{ for all } \mathbf{x}$$

Newton's algorithm is

$$\mathbf{x}_{k+1} = \mathbf{x}_k - \left(\frac{\partial^2 h}{\partial x^2} \Bigg|_{\mathbf{x}=\mathbf{x}_k} \right)^{-1} \frac{\partial h}{\partial x} \Bigg|_{\mathbf{x}=\mathbf{x}_k}, \text{ where}$$

$$\frac{\partial h}{\partial x} = \begin{bmatrix} \frac{\partial h}{\partial x_1} \\ \frac{\partial h}{\partial x_2} \\ \vdots \\ \frac{\partial h}{\partial x_n} \end{bmatrix}$$

and

$$\frac{\partial^2 h}{\partial x^2} = \begin{bmatrix} \frac{\partial^2 h}{\partial x_1^2} & \frac{\partial^2 h}{\partial x_1 \partial x_2} & \cdots & \cdots & \frac{\partial^2 h}{\partial x_1 \partial x_n} \\ \frac{\partial^2 h}{\partial x_1 \partial x_2} & \frac{\partial^2 h}{\partial x_2^2} & \cdots & \cdots & \frac{\partial^2 h}{\partial x_2 \partial x_n} \\ \cdots & \cdots & \cdots & \cdots & \cdots \\ \cdots & \cdots & \cdots & \cdots & \cdots \\ \frac{\partial^2 h}{\partial x_1 \partial x_n} & \frac{\partial^2 h}{\partial x_2 \partial x_n} & \cdots & \cdots & \frac{\partial^2 h}{\partial x_n^2} \end{bmatrix}$$

Numerical Integration

Three of the more common numerical integration algorithms used to evaluate the integral

$$\int_a^b f(x) dx$$

are:

Euler's or Forward Rectangular Rule

$$\int_a^b f(x) dx \approx \Delta x \sum_{k=0}^{n-1} f(a + k\Delta x)$$

Trapezoidal Rule

for $n = 1$

$$\int_a^b f(x) dx \approx \Delta x \left[\frac{f(a) + f(b)}{2} \right]$$

for $n > 1$

$$\int_a^b f(x) dx \approx \frac{\Delta x}{2} \left[f(a) + 2 \sum_{k=1}^{n-1} f(a + k\Delta x) + f(b) \right]$$

Simpson's Rule/Parabolic Rule (n must be an even integer)

for $n = 2$

$$\int_a^b f(x) dx \approx \left(\frac{b-a}{6} \right) \left[f(a) + 4f\left(\frac{a+b}{2}\right) + f(b) \right]$$

for $n \geq 4$

$$\int_a^b f(x) dx \approx \frac{\Delta x}{3} \left[f(a) + 2 \sum_{k=2,4,6,\dots}^{n-2} f(a + k\Delta x) + 4 \sum_{k=1,3,5,\dots}^{n-1} f(a + k\Delta x) + f(b) \right]$$

with $\Delta x = (b-a)/n$

n = number of intervals between data points

Numerical Solution of Ordinary Differential Equations

Euler's Approximation

Given a differential equation

$$dx/dt = f(x, t) \text{ with } x(0) = x_o$$

At some general time $k\Delta t$

$$x[(k+1)\Delta t] \cong x(k\Delta t) + \Delta t f[x(k\Delta t), k\Delta t]$$

which can be used with starting condition x_o to solve recursively for $x(\Delta t), x(2\Delta t), \dots, x(n\Delta t)$.

The method can be extended to n th order differential equations by recasting them as n first-order equations.

In particular, when $dx/dt = f(x)$

$$x[(k+1)\Delta t] \cong x(k\Delta t) + \Delta t f[x(k\Delta t)]$$

which can be expressed as the recursive equation

$$x_{k+1} = x_k + \Delta t (dx_k/dt)$$

$$x_{k+1} = x + \Delta t [f(x(k), t(k))]$$

ENGINEERING PROBABILITY AND STATISTICS

DISPERSION, MEAN, MEDIAN, AND MODE VALUES

If X_1, X_2, \dots, X_n represent the values of a random sample of n items or observations, the *arithmetic mean* of these items or observations, denoted \bar{X} , is defined as

$$\bar{X} = (1/n)(X_1 + X_2 + \dots + X_n) = (1/n) \sum_{i=1}^n X_i$$

$\bar{X} \rightarrow \mu$ for sufficiently large values of n .

The *weighted arithmetic mean* is

$$\bar{X}_w = \frac{\sum w_i X_i}{\sum w_i}, \text{ where}$$

X_i = the value of the i th observation, and

w_i = the weight applied to X_i .

The *variance* of the population is the *arithmetic mean* of the *squared deviations from the population mean*. If μ is the arithmetic mean of a discrete population of size N , the *population variance* is defined by

$$\begin{aligned}\sigma^2 &= (1/N) [(X_1 - \mu)^2 + (X_2 - \mu)^2 + \dots + (X_N - \mu)^2] \\ &= (1/N) \sum_{i=1}^N (X_i - \mu)^2\end{aligned}$$

Standard deviation formulas are

$$\sigma_{\text{population}} = \sqrt{(1/N) \sum (X_i - \mu)^2}$$

$$\sigma_{\text{sum}} = \sqrt{\sigma_1^2 + \sigma_2^2 + \dots + \sigma_n^2}$$

$$\sigma_{\text{series}} = \sigma \sqrt{n}$$

$$\sigma_{\text{mean}} = \frac{\sigma}{\sqrt{n}}$$

$$\sigma_{\text{product}} = \sqrt{A^2 \sigma_b^2 + B^2 \sigma_a^2}$$

The *sample variance* is

$$s^2 = [1/(n-1)] \sum_{i=1}^n (X_i - \bar{X})^2$$

The *sample standard deviation* is

$$s = \sqrt{[1/(n-1)] \sum_{i=1}^n (X_i - \bar{X})^2}$$

The *sample coefficient of variation* = $CV = s/\bar{X}$

The *sample geometric mean* = $\sqrt[n]{X_1 X_2 X_3 \dots X_n}$

The *sample root-mean-square value* = $\sqrt{(1/n) \sum X_i^2}$

When the discrete data are rearranged in increasing order and n is odd, the median is the value of the $(\frac{n+1}{2})^{\text{th}}$ item

When n is even, the median is the average of the

$(\frac{n}{2})^{\text{th}}$ and $(\frac{n}{2} + 1)^{\text{th}}$ items.

The *mode* of a set of data is the value that occurs with greatest frequency.

The *sample range* R is the largest sample value minus the smallest sample value.

PERMUTATIONS AND COMBINATIONS

A *permutation* is a particular sequence of a given set of objects. A *combination* is the set itself without reference to order.

1. The number of different *permutations* of n distinct objects *taken r at a time* is

$$P(n, r) = \frac{n!}{(n-r)!}$$

nPr is an alternative notation for $P(n, r)$

2. The number of different *combinations* of n distinct objects *taken r at a time* is

$$C(n, r) = \frac{P(n, r)}{r!} = \frac{n!}{[r!(n-r)!]}$$

nCr and $\binom{n}{r}$ are alternative notations for $C(n, r)$

3. The number of different *permutations* of n objects *taken n at a time*, given that n_i are of type i , where $i = 1, 2, \dots, k$ and $\sum n_i = n$, is

$$P(n; n_1, n_2, \dots, n_k) = \frac{n!}{n_1! n_2! \dots n_k!}$$

SETS

De Morgan's Law

$$\overline{A \cup B} = \overline{A} \cap \overline{B}$$

$$\overline{A \cap B} = \overline{A} \cup \overline{B}$$

Associative Law

$$A \cup (B \cup C) = (A \cup B) \cup C$$

$$A \cap (B \cap C) = (A \cap B) \cap C$$

Distributive Law

$$A \cup (B \cap C) = (A \cup B) \cap (A \cup C)$$

$$A \cap (B \cup C) = (A \cap B) \cup (A \cap C)$$

LAWS OF PROBABILITY

Property 1. General Character of Probability

The probability $P(E)$ of an event E is a real number in the range of 0 to 1. The probability of an impossible event is 0 and that of an event certain to occur is 1.

Property 2. Law of Total Probability

$$P(A + B) = P(A) + P(B) - P(A, B), \text{ where}$$

$P(A + B)$ = the probability that either A or B occur alone or that both occur together

$P(A)$ = the probability that A occurs

$P(B)$ = the probability that B occurs

$P(A, B)$ = the probability that both A and B occur simultaneously

Property 3. Law of Compound or Joint Probability

If neither $P(A)$ nor $P(B)$ is zero,

$$P(A, B) = P(A)P(B | A) = P(B)P(A | B), \text{ where}$$

$P(B | A)$ = the probability that B occurs given the fact that A has occurred

$P(A | B)$ = the probability that A occurs given the fact that B has occurred

If either $P(A)$ or $P(B)$ is zero, then $P(A, B) = 0$.

Bayes' Theorem

$$P(B_j | A) = \frac{P(B_j)P(A | B_j)}{\sum_{i=1}^n P(A | B_i)P(B_i)}$$

where $P(A_j)$ is the probability of event A_j within the population of A

$P(B_j)$ is the probability of event B_j within the population of B

PROBABILITY FUNCTIONS, DISTRIBUTIONS, AND EXPECTED VALUES

A random variable X has a probability associated with each of its possible values. The probability is termed a discrete probability if X can assume only discrete values, or

$$X = x_1, x_2, x_3, \dots, x_n$$

The *discrete probability* of any single event, $X = x_i$, occurring is defined as $P(x_i)$ while the *probability mass function* of the random variable X is defined by

$$f(x_k) = P(X = x_k), k = 1, 2, \dots, n$$

Probability Density Function

If X is continuous, the *probability density function*, f , is defined such that

$$P(a \leq X \leq b) = \int_a^b f(x) dx$$

Cumulative Distribution Functions

The *cumulative distribution function*, F , of a discrete random variable X that has a probability distribution described by $P(x_i)$ is defined as

$$F(x_m) = \sum_{k=1}^m P(x_k) = P(X \leq x_m), m = 1, 2, \dots, n$$

If X is continuous, the *cumulative distribution function*, F , is defined by

$$F(x) = \int_{-\infty}^x f(t) dt$$

which implies that $F(a)$ is the probability that $X \leq a$.

Expected Values

Let X be a discrete random variable having a probability mass function

$$f(x_k), k = 1, 2, \dots, n$$

The expected value of X is defined as

$$\mu = E[X] = \sum_{k=1}^n x_k f(x_k)$$

The variance of X is defined as

$$\sigma^2 = V[X] = \sum_{k=1}^n (x_k - \mu)^2 f(x_k)$$

Let X be a continuous random variable having a density function $f(X)$ and let $Y = g(X)$ be some general function.

The expected value of Y is:

$$E[Y] = E[g(X)] = \int_{-\infty}^{\infty} g(x) f(x) dx$$

The mean or expected value of the random variable X is now defined as

$$\mu = E[X] = \int_{-\infty}^{\infty} x f(x) dx$$

while the variance is given by

$$\sigma^2 = V[X] = E[(X - \mu)^2] = \int_{-\infty}^{\infty} (x - \mu)^2 f(x) dx$$

The standard deviation is given by

$$\sigma = \sqrt{V[X]}$$

The coefficient of variation is defined as σ/μ .

Combinations of Random Variables

$$Y = a_1 X_1 + a_2 X_2 + \dots + a_n X_n$$

The expected value of Y is:

$$\mu_y = E(Y) = a_1 E(X_1) + a_2 E(X_2) + \dots + a_n E(X_n)$$

If the random variables are statistically *independent*, then the variance of Y is:

$$\begin{aligned} \sigma_y^2 &= V(Y) = a_1^2 V(X_1) + a_2^2 V(X_2) + \dots + a_n^2 V(X_n) \\ &= a_1^2 \sigma_1^2 + a_2^2 \sigma_2^2 + \dots + a_n^2 \sigma_n^2 \end{aligned}$$

Also, the standard deviation of Y is:

$$\sigma_y = \sqrt{\sigma_y^2}$$

When $Y = f(X_1, X_2, \dots, X_n)$ and X_i are independent, the standard deviation of Y is expressed as:

$$\sigma_y = \sqrt{\left(\frac{\partial f}{\partial X_1} \sigma_{X_1}\right)^2 + \left(\frac{\partial f}{\partial X_2} \sigma_{X_2}\right)^2 + \dots + \left(\frac{\partial f}{\partial X_n} \sigma_{X_n}\right)^2}$$

Binomial Distribution

$P(x)$ is the probability that x successes will occur in n trials. If p = probability of success and q = probability of failure = $1 - p$, then

$$P_n(x) = C(n, x) p^x q^{n-x} = \frac{n!}{x!(n-x)!} p^x q^{n-x},$$

where

$x = 0, 1, 2, \dots, n$

$C(n, x)$ = the number of combinations

n, p = parameters

The variance is given by the form:

$$\sigma^2 = npq$$

Normal Distribution (Gaussian Distribution)

This is a unimodal distribution, the mode being $x = \mu$, with two points of inflection (each located at a distance σ to either side of the mode). The averages of n observations tend to become normally distributed as n increases. The variate x is said to be normally distributed if its density function $f(x)$ is given by an expression of the form

$$f(x) = \frac{1}{\sigma\sqrt{2\pi}} e^{-\frac{1}{2}\left(\frac{x-\mu}{\sigma}\right)^2}, \text{ where}$$

μ = the population mean

σ = the standard deviation of the population

$-\infty \leq x \leq \infty$

When $\mu = 0$ and $\sigma^2 = \sigma = 1$, the distribution is called a *standardized* or *unit normal* distribution. Then

$$f(x) = \frac{1}{\sqrt{2\pi}} e^{-\frac{x^2}{2}}, \text{ where } -\infty \leq x \leq \infty.$$

It is noted that $Z = \frac{x-\mu}{\sigma}$ follows a standardized normal distribution function.

A unit normal distribution table is included at the end of this section. In the table, the following notations are utilized:

$F(x)$ = the area under the curve from $-\infty$ to x

$R(x)$ = the area under the curve from x to ∞

$W(x)$ = the area under the curve between $-x$ and x

$F(-x) = 1 - F(x)$

The Central Limit Theorem

Let X_1, X_2, \dots, X_n be a sequence of independent and identically distributed random variables each having mean μ and variance σ^2 . Then for large n , the Central Limit Theorem asserts that the sum

$Y = X_1 + X_2 + \dots + X_n$ is approximately normal.

$$\mu_y = \mu$$

and the standard deviation

$$\sigma_y = \frac{\sigma}{\sqrt{n}}$$

t-Distribution

Student's *t*-distribution has the probability density function given by:

$$f(t) = \frac{\Gamma\left(\frac{v+1}{2}\right)}{\sqrt{v\pi}\Gamma\left(\frac{v}{2}\right)} \left(1 + \frac{t^2}{v}\right)^{-\frac{v+1}{2}}$$

where

v = number of *degrees of freedom*

n = sample size

$v = n - 1$

Γ = gamma function

$$t = \frac{\bar{x} - \mu}{s/\sqrt{n}}$$

$-\infty \leq t \leq \infty$

A table later in this section gives the values of $t_{\alpha, v}$ for values of α and v . Note that, in view of the symmetry of the *t*-distribution, $t_{1-\alpha, v} = -t_{\alpha, v}$

The function for α follows:

$$\alpha = \int_{t_{\alpha, v}}^{\infty} f(t) dt$$

χ^2 - Distribution

If Z_1, Z_2, \dots, Z_n are independent unit normal random variables, then

$$\chi^2 = Z_1^2 + Z_2^2 + \dots + Z_n^2$$

is said to have a chi-square distribution with n degrees of freedom.

A table at the end of this section gives values of $\chi_{\alpha, n}^2$ for selected values of α and n .

Gamma Function

$$\Gamma(n) = \int_0^{\infty} t^{n-1} e^{-t} dt, n > 0$$

PROPAGATION OF ERROR

Measurement Error

$$x = x_{\text{true}} + x_{\text{bias}} + x_{\text{re}}, \text{ where}$$

x = measured value for dimension

x_{true} = true value for dimension

x_{bias} = bias or systematic error in measuring dimension

x_{re} = random error in measuring dimension

$$\mu = \left(\frac{1}{N}\right) \sum_{i=1}^n x_i = \left(\frac{1}{N}\right) \sum_{i=1}^n (x_{\text{true}} + x_{\text{bias}})_i, \text{ where}$$

μ = population or arithmetic mean

N = number of observations of measured values for population

$$\sigma_{\text{population}} = \sigma_{\text{re}} = \sqrt{\left(\frac{1}{N} \sum (x_i - \mu)^2\right)}, \text{ where}$$

σ = standard deviation of uncertainty

Linear Combinations

$$\sigma_{cx} = |c| \sigma_x, \text{ where}$$

c = constant

$$\sigma_{c_1x_1 + \dots + c_nx_n} = \sqrt{c_1^2 \sigma_{x_1}^2 + \dots + c_n^2 \sigma_{x_n}^2}, \text{ where}$$

n = number of observations of measured values for sample

Measurement Uncertainties

$$\sigma_u = \sqrt{\left(\frac{\partial u}{\partial x_1}\right)^2 \sigma_{x_1}^2 + \left(\frac{\partial u}{\partial x_2}\right)^2 \sigma_{x_2}^2 + \dots + \left(\frac{\partial u}{\partial x_n}\right)^2 \sigma_{x_n}^2}$$

$$u(x_1, x_2, \dots, x_n) = f(x_1, x_2, \dots, x_n)$$

where

$f(x_1, x_2, \dots, x_n)$ = the functional relationship between the desired state u and the measured or available states x_i

σ_{x_i} = standard deviation of the state x_i

σ_u = computed standard deviation of u with multiple states x_i

When the state variable x_1 is to be transformed to $u = f(x_1)$ the following relation holds:

$$\sigma_u \approx \left| \frac{du}{dx_1} \right| \sigma_{x_1}$$

LINEAR REGRESSION AND GOODNESS OF FIT

Least Squares

$$y = \hat{a} + \hat{b}x, \text{ where}$$

$$y\text{-intercept, } \hat{a} = \bar{y} - \hat{b}\bar{x}$$

$$\text{and slope, } \hat{b} = S_{xy}/S_{xx}$$

$$S_{xy} = \sum_{i=1}^n x_i y_i - (1/n) \left(\sum_{i=1}^n x_i \right) \left(\sum_{i=1}^n y_i \right)$$

$$S_{xx} = \sum_{i=1}^n x_i^2 - (1/n) \left(\sum_{i=1}^n x_i \right)^2$$

$$\bar{y} = (1/n) \left(\sum_{i=1}^n y_i \right)$$

$$\bar{x} = (1/n) \left(\sum_{i=1}^n x_i \right)$$

where

n = sample size

S_{xx} = sum of squares of x

S_{yy} = sum of squares of y

S_{xy} = sum of x - y products

Standard Error of Estimate (S_e^2):

$$S_e^2 = \frac{S_{xx} S_{yy} - S_{xy}^2}{S_{xx} (n - 2)} = MSE, \text{ where}$$

$$S_{yy} = \sum_{i=1}^n y_i^2 - (1/n) \left(\sum_{i=1}^n y_i \right)^2$$

Confidence Interval for Intercept (\hat{a}):

$$\hat{a} \pm t_{\alpha/2, n-2} \sqrt{\left(\frac{1}{n} + \frac{\bar{x}^2}{S_{xx}} \right) MSE}$$

Confidence Interval for Slope (\hat{b}):

$$\hat{b} \pm t_{\alpha/2, n-2} \sqrt{\frac{MSE}{S_{xx}}}$$

Sample Correlation Coefficient (R) and Coefficient of Determination (R^2):

$$R = \frac{S_{xy}}{\sqrt{S_{xx} S_{yy}}}$$

$$R^2 = \frac{S_{xy}^2}{S_{xx} S_{yy}}$$

HYPOTHESIS TESTING

One-Way Analysis of Variance (ANOVA)

Given independent random samples of size n_i from k populations, then:

$$\begin{aligned} & \sum_{i=1}^k \sum_{j=1}^{n_i} (x_{ij} - \bar{x})^2 \\ &= \sum_{i=1}^k \sum_{j=1}^{n_i} (x_{ij} - \bar{x}_i)^2 + \sum_{i=1}^k n_i (\bar{x}_i - \bar{x})^2 \text{ or} \\ & SS_{\text{total}} = SS_{\text{error}} + SS_{\text{treatments}} \end{aligned}$$

Let T be the grand total of all $N = \sum n_i$ observations and T_i be the total of the n_i observations of the i th sample.

$$C = T^2 / N$$

$$SS_{\text{total}} = \sum_{i=1}^k \sum_{j=1}^{n_i} x_{ij}^2 - C$$

$$SS_{\text{treatments}} = \sum_{i=1}^k (T_i^2 / n_i) - C$$

$$SS_{\text{error}} = SS_{\text{total}} - SS_{\text{treatments}}$$

One-Way ANOVA Table

Source of Variation	Degrees of Freedom	Sum of Squares	Mean Square	F
Between Treatments	$k - 1$	$SS_{\text{treatments}}$	$MST = \frac{SS_{\text{treatments}}}{k - 1}$	$\frac{MST}{MSE}$
Error	$N - k$	SS_{error}	$MSE = \frac{SS_{\text{error}}}{N - k}$	
Total	$N - 1$	SS_{total}		

Two-Way ANOVA Table

Source of Variation	Degrees of Freedom	Sum of Squares	Mean Square	F
Between Treatments	$k - 1$	$SS_{\text{treatments}}$	$MST = \frac{SS_{\text{treatments}}}{k - 1}$	$\frac{MST}{MSE}$
Between Blocks	$n - 1$	SS_{blocks}	$MSB = \frac{SS_{\text{blocks}}}{n - 1}$	$\frac{MSB}{MSE}$
Error	$(k - 1)(n - 1)$	SS_{error}	$MSE = \frac{SS_{\text{error}}}{(k - 1)(n - 1)}$	
Total	$N - 1$	SS_{total}		

Consider an unknown parameter θ of a statistical distribution. Let the null hypothesis be

$$H_0: \mu = \mu_0$$

and let the alternative hypothesis be

$$H_1: \mu \neq \mu_1$$

Rejecting H_0 when it is true is known as a type I error, while accepting H_0 when it is wrong is known as a type II error.

Furthermore, the probabilities of type I and type II errors are usually represented by the symbols α and β , respectively:

α = probability (type I error)

β = probability (type II error)

The probability of a type I error is known as the level of significance of the test.

Table A. Tests on Means of Normal Distribution—Variance Known

Hypothesis	Test Statistic	Criteria for Rejection
$H_0: \mu = \mu_0$		
$H_1: \mu \neq \mu_0$		$ Z_0 > Z_{\alpha/2}$
$H_0: \mu = \mu_0$		
$H_1: \mu < \mu_0$	$Z_0 \equiv \frac{\bar{X} - \mu_0}{\sigma / \sqrt{n}}$	$Z_0 < -Z_\alpha$
$H_0: \mu = \mu_0$		
$H_1: \mu > \mu_0$		$Z_0 > Z_\alpha$
$H_0: \mu_1 - \mu_2 = \gamma$		
$H_1: \mu_1 - \mu_2 \neq \gamma$		$ Z_0 > Z_{\alpha/2}$
$H_0: \mu_1 - \mu_2 = \gamma$		
$H_1: \mu_1 - \mu_2 < \gamma$	$Z_0 \equiv \frac{\bar{X}_1 - \bar{X}_2 - \gamma}{\sqrt{\frac{\sigma_1^2}{n_1} + \frac{\sigma_2^2}{n_2}}}$	$Z_0 < -Z_\alpha$
$H_0: \mu_1 - \mu_2 = \gamma$		
$H_1: \mu_1 - \mu_2 > \gamma$		$Z_0 > Z_\alpha$

Table B. Tests on Means of Normal Distribution—Variance Unknown

Hypothesis	Test Statistic	Criteria for Rejection
$H_0: \mu = \mu_0$		
$H_1: \mu \neq \mu_0$		$ t_0 > t_{\alpha/2, n-1}$
$H_0: \mu = \mu_0$		
$H_1: \mu < \mu_0$	$t_0 = \frac{\bar{X} - \mu_0}{S/\sqrt{n}}$	$t_0 < -t_{\alpha, n-1}$
$H_0: \mu = \mu_0$		
$H_1: \mu > \mu_0$		$t_0 > t_{\alpha, n-1}$
$H_0: \mu_1 - \mu_2 = \gamma$		
$H_1: \mu_1 - \mu_2 \neq \gamma$		

$H_0: \mu_1 - \mu_2 = \gamma$		
$H_1: \mu_1 - \mu_2 < \gamma$		

$H_0: \mu_1 - \mu_2 = \gamma$		
$H_1: \mu_1 - \mu_2 > \gamma$		

$t_0 = \frac{\bar{X}_1 - \bar{X}_2 - \gamma}{S_p \sqrt{\frac{1}{n_1} + \frac{1}{n_2}}}$
 Variances equal
 $v = n_1 + n_2 - 2$

 $t_0 = \frac{\bar{X}_1 - \bar{X}_2 - \gamma}{\sqrt{\frac{S_1^2}{n_1} + \frac{S_2^2}{n_2}}}$
 Variances unequal
 $v = \frac{\left(\frac{S_1^2}{n_1} + \frac{S_2^2}{n_2}\right)^2}{\frac{(S_1^2/n_1)^2}{n_1-1} + \frac{(S_2^2/n_2)^2}{n_2-1}}$

In Table B, $S_p^2 = [(n_1-1)S_1^2 + (n_2-1)S_2^2]/v$

Table C. Tests on Variances of Normal Distribution with Unknown Mean

Hypothesis	Test Statistic	Criteria for Rejection
$H_0: \sigma^2 = \sigma_0^2$		
$H_1: \sigma^2 \neq \sigma_0^2$		$\chi_0^2 > \chi^2_{\alpha/2, n-1}$ or $\chi_0^2 < \chi^2_{1-\alpha/2, n-1}$
$H_0: \sigma^2 = \sigma_0^2$		
$H_1: \sigma^2 < \sigma_0^2$	$\chi_0^2 = \frac{(n-1)S^2}{\sigma_0^2}$	$\chi_0^2 < \chi^2_{1-\alpha, n-1}$
$H_0: \sigma^2 = \sigma_0^2$		
$H_1: \sigma^2 > \sigma_0^2$		$\chi_0^2 > \chi^2_{\alpha, n-1}$
$H_0: \sigma_1^2 = \sigma_2^2$		
$H_1: \sigma_1^2 \neq \sigma_2^2$	$F_0 = \frac{S_1^2}{S_2^2}$	$F_0 > F_{\alpha/2, n_1-1, n_2-1}$ $F_0 < F_{1-\alpha/2, n_1-1, n_2-1}$
$H_0: \sigma_1^2 = \sigma_2^2$		
$H_1: \sigma_1^2 < \sigma_2^2$	$F_0 = \frac{S_2^2}{S_1^2}$	$F_0 > F_{\alpha, n_2-1, n_1-1}$
$H_0: \sigma_1^2 = \sigma_2^2$		
$H_1: \sigma_1^2 > \sigma_2^2$	$F_0 = \frac{S_1^2}{S_2^2}$	$F_0 > F_{\alpha, n_1-1, n_2-1}$

Assume that the values of α and β are given. The sample size can be obtained from the following relationships. In (A) and (B), μ_1 is the value assumed to be the true mean.

$$(A) \quad H_0: \mu = \mu_0; H_1: \mu \neq \mu_0$$

$$\beta = \Phi\left(\frac{\mu_0 - \mu}{\sigma/\sqrt{n}} + Z_{\alpha/2}\right) - \Phi\left(\frac{\mu_0 - \mu}{\sigma/\sqrt{n}} - Z_{\alpha/2}\right)$$

An approximate result is

$$n \simeq \frac{(Z_{\alpha/2} + Z_\beta)^2 \sigma^2}{(\mu_1 - \mu_0)^2}$$

$$(B) \quad H_0: \mu = \mu_0; H_1: \mu > \mu_0$$

$$\beta = \Phi\left(\frac{\mu_0 - \mu}{\sigma/\sqrt{n}} + Z_\alpha\right)$$

$$n = \frac{(Z_\alpha + Z_\beta)^2 \sigma^2}{(\mu_1 - \mu_0)^2}$$

CONFIDENCE INTERVALS, SAMPLE DISTRIBUTIONS AND SAMPLE SIZE

Confidence Interval for the Mean μ of a Normal Distribution

(A) Standard deviation σ is known

$$\bar{X} - Z_{\alpha/2} \frac{\sigma}{\sqrt{n}} \leq \mu \leq \bar{X} + Z_{\alpha/2} \frac{\sigma}{\sqrt{n}}$$

(B) Standard deviation σ is not known

$$\bar{X} - t_{\alpha/2} \frac{s}{\sqrt{n}} \leq \mu \leq \bar{X} + t_{\alpha/2} \frac{s}{\sqrt{n}}$$

where $t_{\alpha/2}$ corresponds to $n - 1$ degrees of freedom.

Confidence Interval for the Difference Between Two Means μ_1 and μ_2

(A) Standard deviations σ_1 and σ_2 known

$$\bar{X}_1 - \bar{X}_2 - Z_{\alpha/2} \sqrt{\frac{\sigma_1^2}{n_1} + \frac{\sigma_2^2}{n_2}} \leq \mu_1 - \mu_2 \leq \bar{X}_1 - \bar{X}_2 + Z_{\alpha/2} \sqrt{\frac{\sigma_1^2}{n_1} + \frac{\sigma_2^2}{n_2}}$$

(B) Standard deviations σ_1 and σ_2 are not known

$$\bar{X}_1 - \bar{X}_2 - t_{\alpha/2} \sqrt{\frac{\left(\frac{1}{n_1} + \frac{1}{n_2}\right)[(n_1 - 1)S_1^2 + (n_2 - 1)S_2^2]}{n_1 + n_2 - 2}} \leq \mu_1 - \mu_2 \leq \bar{X}_1 - \bar{X}_2 + t_{\alpha/2} \sqrt{\frac{\left(\frac{1}{n_1} + \frac{1}{n_2}\right)[(n_1 - 1)S_1^2 + (n_2 - 1)S_2^2]}{n_1 + n_2 - 2}}$$

where $t_{\alpha/2}$ corresponds to $n_1 + n_2 - 2$ degrees of freedom.

Confidence Intervals for the Variance σ^2 of a Normal Distribution

$$\frac{(n - 1)s^2}{x_{\alpha/2, n - 1}^2} \leq \sigma^2 \leq \frac{(n - 1)s^2}{x_{1 - \alpha/2, n - 1}^2}$$

Sample Size

$$z = \frac{\bar{X} - \mu}{\sigma/\sqrt{n}} \quad n = \left[\frac{z_{\alpha/2} \sigma}{\bar{x} - \mu} \right]^2$$

TEST STATISTICS

The following definitions apply.

$$Z_{\text{var}} = \frac{\bar{X} - \mu_0}{\frac{\sigma}{\sqrt{n}}}$$

$$t_{\text{var}} = \frac{\bar{X} - \mu_0}{\frac{s}{\sqrt{n}}}$$

where

Z_{var} is the standard normal Z score

t_{var} is the sample distribution test statistic

σ is known standard deviation

μ_0 is population mean

\bar{X} is hypothesized mean or sample mean

n is sample size

s is computed sample standard deviation

The Z score is applicable when the standard deviation(s) is known. The test statistic is applicable when the standard deviation(s) is computed at time of sampling.

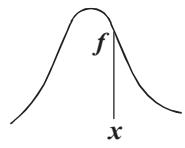
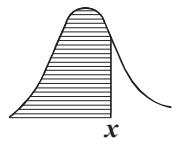
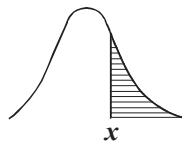
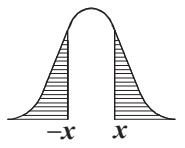
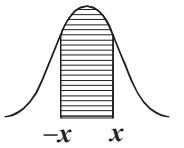
Z_α corresponds to the appropriate probability under the normal probability curve for a given Z_{var} .

$t_{\alpha/2, n-1}$ corresponds to the appropriate probability under the t distribution with $n - 1$ degrees of freedom for a given t_{var} .

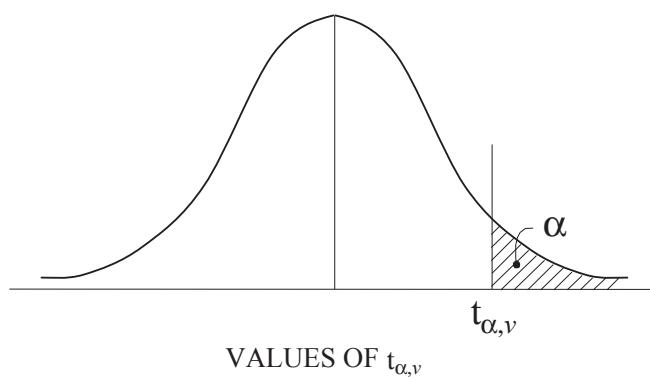
Values of $Z_{\alpha/2}$

Confidence Interval	$Z_{\alpha/2}$
80%	1.2816
90%	1.6449
95%	1.9600
96%	2.0537
98%	2.3263
99%	2.5758

Unit Normal Distribution

					
x	$f(x)$	$F(x)$	$R(x)$	$2R(x)$	$W(x)$
0.0	0.3989	0.5000	0.5000	1.0000	0.0000
0.1	0.3970	0.5398	0.4602	0.9203	0.0797
0.2	0.3910	0.5793	0.4207	0.8415	0.1585
0.3	0.3814	0.6179	0.3821	0.7642	0.2358
0.4	0.3683	0.6554	0.3446	0.6892	0.3108
0.5	0.3521	0.6915	0.3085	0.6171	0.3829
0.6	0.3332	0.7257	0.2743	0.5485	0.4515
0.7	0.3123	0.7580	0.2420	0.4839	0.5161
0.8	0.2897	0.7881	0.2119	0.4237	0.5763
0.9	0.2661	0.8159	0.1841	0.3681	0.6319
1.0	0.2420	0.8413	0.1587	0.3173	0.6827
1.1	0.2179	0.8643	0.1357	0.2713	0.7287
1.2	0.1942	0.8849	0.1151	0.2301	0.7699
1.3	0.1714	0.9032	0.0968	0.1936	0.8064
1.4	0.1497	0.9192	0.0808	0.1615	0.8385
1.5	0.1295	0.9332	0.0668	0.1336	0.8664
1.6	0.1109	0.9452	0.0548	0.1096	0.8904
1.7	0.0940	0.9554	0.0446	0.0891	0.9109
1.8	0.0790	0.9641	0.0359	0.0719	0.9281
1.9	0.0656	0.9713	0.0287	0.0574	0.9426
2.0	0.0540	0.9772	0.0228	0.0455	0.9545
2.1	0.0440	0.9821	0.0179	0.0357	0.9643
2.2	0.0355	0.9861	0.0139	0.0278	0.9722
2.3	0.0283	0.9893	0.0107	0.0214	0.9786
2.4	0.0224	0.9918	0.0082	0.0164	0.9836
2.5	0.0175	0.9938	0.0062	0.0124	0.9876
2.6	0.0136	0.9953	0.0047	0.0093	0.9907
2.7	0.0104	0.9965	0.0035	0.0069	0.9931
2.8	0.0079	0.9974	0.0026	0.0051	0.9949
2.9	0.0060	0.9981	0.0019	0.0037	0.9963
3.0	0.0044	0.9987	0.0013	0.0027	0.9973
Fractiles					
1.2816	0.1755	0.9000	0.1000	0.2000	0.8000
1.6449	0.1031	0.9500	0.0500	0.1000	0.9000
1.9600	0.0584	0.9750	0.0250	0.0500	0.9500
2.0537	0.0484	0.9800	0.0200	0.0400	0.9600
2.3263	0.0267	0.9900	0.0100	0.0200	0.9800
2.5758	0.0145	0.9950	0.0050	0.0100	0.9900

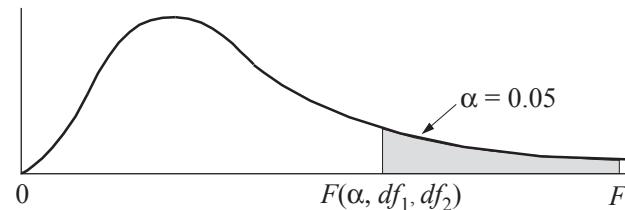
Student's *t*-Distribution



v	α								v
	0.25	0.20	0.15	0.10	0.05	0.025	0.01	0.005	
1	1.000	1.376	1.963	3.078	6.314	12.706	31.821	63.657	1
2	0.816	1.061	1.386	1.886	2.920	4.303	6.965	9.925	2
3	0.765	0.978	1.350	1.638	2.353	3.182	4.541	5.841	3
4	0.741	0.941	1.190	1.533	2.132	2.776	3.747	4.604	4
5	0.727	0.920	1.156	1.476	2.015	2.571	3.365	4.032	5
6	0.718	0.906	1.134	1.440	1.943	2.447	3.143	3.707	6
7	0.711	0.896	1.119	1.415	1.895	2.365	2.998	3.499	7
8	0.706	0.889	1.108	1.397	1.860	2.306	2.896	3.355	8
9	0.703	0.883	1.100	1.383	1.833	2.262	2.821	3.250	9
10	0.700	0.879	1.093	1.372	1.812	2.228	2.764	3.169	10
11	0.697	0.876	1.088	1.363	1.796	2.201	2.718	3.106	11
12	0.695	0.873	1.083	1.356	1.782	2.179	2.681	3.055	12
13	0.694	0.870	1.079	1.350	1.771	2.160	2.650	3.012	13
14	0.692	0.868	1.076	1.345	1.761	2.145	2.624	2.977	14
15	0.691	0.866	1.074	1.341	1.753	2.131	2.602	2.947	15
16	0.690	0.865	1.071	1.337	1.746	2.120	2.583	2.921	16
17	0.689	0.863	1.069	1.333	1.740	2.110	2.567	2.898	17
18	0.688	0.862	1.067	1.330	1.734	2.101	2.552	2.878	18
19	0.688	0.861	1.066	1.328	1.729	2.093	2.539	2.861	19
20	0.687	0.860	1.064	1.325	1.725	2.086	2.528	2.845	20
21	0.686	0.859	1.063	1.323	1.721	2.080	2.518	2.831	21
22	0.686	0.858	1.061	1.321	1.717	2.074	2.508	2.819	22
23	0.685	0.858	1.060	1.319	1.714	2.069	2.500	2.807	23
24	0.685	0.857	1.059	1.318	1.711	2.064	2.492	2.797	24
25	0.684	0.856	1.058	1.316	1.708	2.060	2.485	2.787	25
26	0.684	0.856	1.058	1.315	1.706	2.056	2.479	2.779	26
27	0.684	0.855	1.057	1.314	1.703	2.052	2.473	2.771	27
28	0.683	0.855	1.056	1.313	1.701	2.048	2.467	2.763	28
29	0.683	0.854	1.055	1.311	1.699	2.045	2.462	2.756	29
30	0.683	0.854	1.055	1.310	1.697	2.042	2.457	2.750	30
∞	0.674	0.842	1.036	1.282	1.645	1.960	2.326	2.576	∞

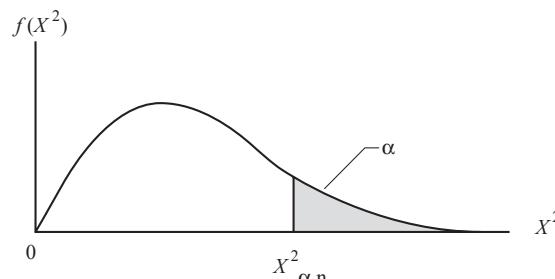
CRITICAL VALUES OF THE F DISTRIBUTION — TABLE

For a particular combination of numerator and denominator degrees of freedom, entry represents the critical values of F corresponding to a specified upper tail area (α).



Denominator df_2	Numerator df_1																		
	1	2	3	4	5	6	7	8	9	10	12	15	20	24	30	40	60	120	∞
1	161.4	199.5	215.7	224.6	230.2	234.0	236.8	238.9	240.5	241.9	243.9	245.9	248.0	249.1	250.1	251.1	252.2	253.3	254.3
2	18.51	19.00	19.16	19.25	19.30	19.33	19.35	19.37	19.38	19.40	19.41	19.43	19.45	19.45	19.46	19.47	19.48	19.49	19.50
3	10.13	9.55	9.28	9.12	9.01	8.94	8.89	8.85	8.81	8.79	8.74	8.70	8.66	8.64	8.62	8.59	8.57	8.55	8.53
4	7.71	6.94	6.59	6.39	6.26	6.16	6.09	6.04	6.00	5.96	5.91	5.86	5.80	5.77	5.75	5.72	5.69	5.66	5.63
5	6.61	5.79	5.41	5.19	5.05	4.95	4.88	4.82	4.77	4.74	4.68	4.62	4.56	4.53	4.50	4.46	4.43	4.40	4.36
6	5.99	5.14	4.76	4.53	4.39	4.28	4.21	4.15	4.10	4.06	4.00	3.94	3.87	3.84	3.81	3.77	3.74	3.70	3.67
7	5.59	4.74	4.35	4.12	3.97	3.87	3.79	3.73	3.68	3.64	3.57	3.51	3.44	3.41	3.38	3.34	3.30	3.27	3.23
8	5.32	4.46	4.07	3.84	3.69	3.58	3.50	3.44	3.39	3.35	3.28	3.22	3.15	3.12	3.08	3.04	3.01	2.97	2.93
9	5.12	4.26	3.86	3.63	3.48	3.37	3.29	3.23	3.18	3.14	3.07	3.01	2.94	2.90	2.86	2.83	2.79	2.75	2.71
10	4.96	4.10	3.71	3.48	3.33	3.22	3.14	3.07	3.02	2.98	2.91	2.85	2.77	2.74	2.70	2.66	2.62	2.58	2.54
11	4.84	3.98	3.59	3.36	3.20	3.09	3.01	2.95	2.90	2.85	2.79	2.72	2.65	2.61	2.57	2.53	2.49	2.45	2.40
12	4.75	3.89	3.49	3.26	3.11	3.00	2.91	2.85	2.80	2.75	2.69	2.62	2.54	2.51	2.47	2.43	2.38	2.34	2.30
13	4.67	3.81	3.41	3.18	3.03	2.92	2.83	2.77	2.71	2.67	2.60	2.53	2.46	2.42	2.38	2.34	2.30	2.25	2.21
14	4.60	3.74	3.34	3.11	2.96	2.85	2.76	2.70	2.65	2.60	2.53	2.46	2.39	2.35	2.31	2.27	2.22	2.18	2.13
15	4.54	3.68	3.29	3.06	2.90	2.79	2.71	2.64	2.59	2.54	2.48	2.40	2.33	2.29	2.25	2.20	2.16	2.11	2.07
16	4.49	3.63	3.24	3.01	2.85	2.74	2.66	2.59	2.54	2.49	2.42	2.35	2.28	2.24	2.19	2.15	2.11	2.06	2.01
17	4.45	3.59	3.20	2.96	2.81	2.70	2.61	2.55	2.49	2.45	2.38	2.31	2.23	2.19	2.15	2.10	2.06	2.01	1.96
18	4.41	3.55	3.16	2.93	2.77	2.66	2.58	2.51	2.46	2.41	2.34	2.27	2.19	2.15	2.11	2.06	2.02	1.97	1.92
19	4.38	3.52	3.13	2.90	2.74	2.63	2.54	2.48	2.42	2.38	2.31	2.23	2.16	2.11	2.07	2.03	1.98	1.93	1.88
20	4.35	3.49	3.10	2.87	2.71	2.60	2.51	2.45	2.39	2.35	2.28	2.20	2.12	2.08	2.04	1.99	1.95	1.90	1.84
21	4.32	3.47	3.07	2.84	2.68	2.57	2.49	2.42	2.37	2.32	2.25	2.18	2.10	2.05	2.01	1.96	1.92	1.87	1.81
22	4.30	3.44	3.05	2.82	2.66	2.55	2.46	2.40	2.34	2.30	2.23	2.15	2.07	2.03	1.98	1.94	1.89	1.84	1.78
23	4.28	3.42	3.03	2.80	2.64	2.53	2.44	2.37	2.32	2.27	2.20	2.13	2.05	2.01	1.96	1.91	1.86	1.81	1.76
24	4.26	3.40	3.01	2.78	2.62	2.51	2.42	2.36	2.30	2.25	2.18	2.11	2.03	1.98	1.94	1.89	1.84	1.79	1.73
25	4.24	3.39	2.99	2.76	2.60	2.49	2.40	2.34	2.28	2.24	2.16	2.09	2.01	1.96	1.92	1.87	1.82	1.77	1.71
26	4.23	3.37	2.98	2.74	2.59	2.47	2.39	2.32	2.27	2.22	2.15	2.07	1.99	1.95	1.90	1.85	1.80	1.75	1.69
27	4.21	3.35	2.96	2.73	2.57	2.46	2.37	2.31	2.25	2.20	2.13	2.06	1.97	1.93	1.88	1.84	1.79	1.73	1.67
28	4.20	3.34	2.95	2.71	2.56	2.45	2.36	2.29	2.24	2.19	2.12	2.04	1.96	1.91	1.87	1.82	1.77	1.71	1.65
29	4.18	3.33	2.93	2.70	2.55	2.43	2.35	2.28	2.22	2.18	2.10	2.03	1.94	1.90	1.85	1.81	1.75	1.70	1.64
30	4.17	3.32	2.92	2.69	2.53	2.42	2.33	2.27	2.21	2.16	2.09	2.01	1.93	1.89	1.84	1.79	1.74	1.68	1.62
40	4.08	3.23	2.84	2.61	2.45	2.34	2.25	2.18	2.12	2.08	2.00	1.92	1.84	1.79	1.74	1.69	1.64	1.58	1.51
60	4.00	3.15	2.76	2.53	2.37	2.25	2.17	2.10	2.04	1.99	1.92	1.84	1.75	1.70	1.65	1.59	1.53	1.47	1.39
120	3.92	3.07	2.68	2.45	2.29	2.17	2.09	2.02	1.96	1.91	1.83	1.75	1.66	1.61	1.55	1.50	1.43	1.35	1.25
∞	3.84	3.00	2.60	2.37	2.21	2.10	2.01	1.94	1.88	1.83	1.75	1.67	1.57	1.52	1.46	1.39	1.32	1.22	1.00

CRITICAL VALUES OF X^2 DISTRIBUTION



Degrees of Freedom	$X^2_{.995}$	$X^2_{.990}$	$X^2_{.975}$	$X^2_{.950}$	$X^2_{.900}$	$X^2_{.100}$	$X^2_{.050}$	$X^2_{.025}$	$X^2_{.010}$	$X^2_{.005}$
1	0.0000393	0.0001571	0.0009821	0.0039321	0.0157908	2.70554	3.84146	5.02389	6.63490	7.87944
2	0.0100251	0.0201007	0.0506356	0.102587	0.210720	4.60517	5.99147	7.37776	9.21034	10.5966
3	0.0717212	0.114832	0.215795	0.351846	0.584375	6.25139	7.81473	9.34840	11.3449	12.8381
4	0.206990	0.297110	0.484419	0.710721	1.063623	7.77944	9.48773	11.1433	13.2767	14.8602
5	0.411740	0.554300	0.831211	1.145476	1.61031	9.23635	11.0705	12.8325	15.0863	16.7496
6	0.675727	0.872085	1.237347	1.63539	2.20413	10.6446	12.5916	14.4494	16.8119	18.5476
7	0.989265	1.239043	1.68987	2.16735	2.83311	12.0170	14.0671	16.0128	18.4753	20.2777
8	1.344419	1.646482	2.17973	2.73264	3.48954	13.3616	15.5073	17.5346	20.0902	21.9550
9	1.734926	2.087912	2.70039	3.32511	4.16816	14.6837	16.9190	19.0228	21.6660	23.5893
10	2.15585	2.55821	3.24697	3.94030	4.86518	15.9871	18.3070	20.4831	23.2093	25.1882
11	2.60321	3.05347	3.81575	4.57481	5.57779	17.2750	19.6751	21.9200	24.7250	26.7569
12	3.07382	3.57056	4.40379	5.22603	6.30380	18.5494	21.0261	23.3367	26.2170	28.2995
13	3.56503	4.10691	5.00874	5.89186	7.04150	19.8119	22.3621	24.7356	27.6883	29.8194
14	4.07468	4.66043	5.62872	6.57063	7.78953	21.0642	23.6848	26.1190	29.1413	31.3193
15	4.60094	5.22935	6.26214	7.26094	8.54675	22.3072	24.9958	27.4884	30.5779	32.8013
16	5.14224	5.81221	6.90766	7.96164	9.31223	23.5418	26.2962	28.8454	31.9999	34.2672
17	5.69724	6.40776	7.56418	8.67176	10.0852	24.7690	27.5871	30.1910	33.4087	35.7185
18	6.26481	7.01491	8.23075	9.39046	10.8649	25.9894	28.8693	31.5264	34.8053	37.1564
19	6.84398	7.63273	8.90655	10.1170	11.6509	27.2036	30.1435	32.8523	36.1908	38.5822
20	7.43386	8.26040	9.59083	10.8508	12.4426	28.4120	31.4104	34.1696	37.5662	39.9968
21	8.03366	8.89720	10.28293	11.5913	13.2396	29.6151	32.6705	35.4789	38.9321	41.4010
22	8.64272	9.54249	10.9823	12.3380	14.0415	30.8133	33.9244	36.7807	40.2894	42.7956
23	9.26042	10.19567	11.6885	13.0905	14.8479	32.0069	35.1725	38.0757	41.6384	44.1813
24	9.88623	10.8564	12.4011	13.8484	15.6587	33.1963	36.4151	39.3641	42.9798	45.5585
25	10.5197	11.5240	13.1197	14.6114	16.4734	34.3816	37.6525	40.6465	44.3141	46.9278
26	11.1603	12.1981	13.8439	15.3791	17.2919	35.5631	38.8852	41.9232	45.6417	48.2899
27	11.8076	12.8786	14.5733	16.1513	18.1138	36.7412	40.1133	43.1944	46.9630	49.6449
28	12.4613	13.5648	15.3079	16.9279	18.9392	37.9159	41.3372	44.4607	48.2782	50.9933
29	13.1211	14.2565	16.0471	17.7083	19.7677	39.0875	42.5569	45.7222	49.5879	52.3356
30	13.7867	14.9535	16.7908	18.4926	20.5992	40.2560	43.7729	46.9792	50.8922	53.6720
40	20.7065	22.1643	24.4331	26.5093	29.0505	51.8050	55.7585	59.3417	63.6907	66.7659
50	27.9907	29.7067	32.3574	34.7642	37.6886	63.1671	67.5048	71.4202	76.1539	79.4900
60	35.5346	37.4848	40.4817	43.1879	46.4589	74.3970	79.0819	83.2976	88.3794	91.9517
70	43.2752	45.4418	48.7576	51.7393	55.3290	85.5271	90.5312	95.0231	100.4225	104.2125
80	51.1720	53.5400	57.1532	60.3915	64.2778	96.5782	101.879	106.629	112.329	116.321
90	59.1963	61.7541	65.6466	69.1260	73.2912	107.565	113.145	118.136	124.116	128.299
100	67.3276	70.0648	74.2219	77.9295	82.3581	118.498	124.342	129.561	135.807	140.169

Source: Thompson, C. M., "Tables of the Percentage Points of the X^2 -Distribution," *Biometrika*, ©1941, 32, 188-189. Reproduced by permission of Oxford University Press.

Cumulative Binomial Probabilities $P(X \leq x)$

		<i>P</i>										
<i>n</i>	<i>x</i>	0.1	0.2	0.3	0.4	0.5	0.6	0.7	0.8	0.9	0.95	0.99
1	0	0.9000	0.8000	0.7000	0.6000	0.5000	0.4000	0.3000	0.2000	0.1000	0.0500	0.0100
2	0	0.8100	0.6400	0.4900	0.3600	0.2500	0.1600	0.0900	0.0400	0.0100	0.0025	0.0001
	1	0.9900	0.9600	0.9100	0.8400	0.7500	0.6400	0.5100	0.3600	0.1900	0.0975	0.0199
3	0	0.7290	0.5120	0.3430	0.2160	0.1250	0.0640	0.0270	0.0080	0.0010	0.0001	0.0000
	1	0.9720	0.8960	0.7840	0.6480	0.5000	0.3520	0.2160	0.1040	0.0280	0.0073	0.0003
	2	0.9990	0.9920	0.9730	0.9360	0.8750	0.7840	0.6570	0.4880	0.2710	0.1426	0.0297
4	0	0.6561	0.4096	0.2401	0.1296	0.0625	0.0256	0.0081	0.0016	0.0001	0.0000	0.0000
	1	0.9477	0.8192	0.6517	0.4752	0.3125	0.1792	0.0837	0.0272	0.0037	0.0005	0.0000
	2	0.9963	0.9728	0.9163	0.8208	0.6875	0.5248	0.3483	0.1808	0.0523	0.0140	0.0006
	3	0.9999	0.9984	0.9919	0.9744	0.9375	0.8704	0.7599	0.5904	0.3439	0.1855	0.0394
5	0	0.5905	0.3277	0.1681	0.0778	0.0313	0.0102	0.0024	0.0003	0.0000	0.0000	0.0000
	1	0.9185	0.7373	0.5282	0.3370	0.1875	0.0870	0.0308	0.0067	0.0005	0.0000	0.0000
	2	0.9914	0.9421	0.8369	0.6826	0.5000	0.3174	0.1631	0.0579	0.0086	0.0012	0.0000
	3	0.9995	0.9933	0.9692	0.9130	0.8125	0.6630	0.4718	0.2627	0.0815	0.0226	0.0010
	4	1.0000	0.9997	0.9976	0.9898	0.6988	0.9222	0.8319	0.6723	0.4095	0.2262	0.0490
6	0	0.5314	0.2621	0.1176	0.0467	0.0156	0.0041	0.0007	0.0001	0.0000	0.0000	0.0000
	1	0.8857	0.6554	0.4202	0.2333	0.1094	0.0410	0.0109	0.0016	0.0001	0.0000	0.0000
	2	0.9842	0.9011	0.7443	0.5443	0.3438	0.1792	0.0705	0.0170	0.0013	0.0001	0.0000
	3	0.9987	0.9830	0.9295	0.8208	0.6563	0.4557	0.2557	0.0989	0.0159	0.0022	0.0000
	4	0.9999	0.9984	0.9891	0.9590	0.9806	0.7667	0.5798	0.3446	0.1143	0.0328	0.0015
	5	1.0000	0.9999	0.9993	0.9959	0.9844	0.9533	0.8824	0.7379	0.4686	0.2649	0.0585
7	0	0.4783	0.2097	0.0824	0.0280	0.0078	0.0106	0.0002	0.0000	0.0000	0.0000	0.0000
	1	0.8503	0.5767	0.3294	0.1586	0.0625	0.0188	0.0038	0.0004	0.0000	0.0000	0.0000
	2	0.9743	0.8520	0.6471	0.4199	0.2266	0.0963	0.0288	0.0047	0.0002	0.0000	0.0000
	3	0.9973	0.9667	0.8740	0.7102	0.5000	0.2898	0.1260	0.0333	0.0027	0.0002	0.0000
	4	0.9998	0.9953	0.9712	0.9037	0.7734	0.5801	0.3529	0.1480	0.0257	0.0038	0.0000
	5	1.0000	0.9996	0.9962	0.9812	0.9375	0.8414	0.6706	0.4233	0.1497	0.0444	0.0020
	6	1.0000	1.0000	0.9998	0.9984	0.9922	0.9720	0.9176	0.7903	0.5217	0.3017	0.0679
8	0	0.4305	0.1678	0.0576	0.0168	0.0039	0.0007	0.0001	0.0000	0.0000	0.0000	0.0000
	1	0.8131	0.5033	0.2553	0.1064	0.0352	0.0085	0.0013	0.0001	0.0000	0.0000	0.0000
	2	0.9619	0.7969	0.5518	0.3154	0.1445	0.0498	0.0113	0.0012	0.0000	0.0000	0.0000
	3	0.9950	0.9437	0.8059	0.5941	0.3633	0.1737	0.0580	0.0104	0.0004	0.0000	0.0000
	4	0.9996	0.9896	0.9420	0.8263	0.6367	0.4059	0.1941	0.0563	0.0050	0.0004	0.0000
	5	1.0000	0.9988	0.9887	0.9502	0.8555	0.6846	0.4482	0.2031	0.0381	0.0058	0.0001
	6	1.0000	0.9999	0.9987	0.9915	0.9648	0.8936	0.7447	0.4967	0.1869	0.0572	0.0027
	7	1.0000	1.0000	0.9999	0.9993	0.9961	0.9832	0.9424	0.8322	0.5695	0.3366	0.0773
9	0	0.3874	0.1342	0.0404	0.0101	0.0020	0.0003	0.0000	0.0000	0.0000	0.0000	0.0000
	1	0.7748	0.4362	0.1960	0.0705	0.0195	0.0038	0.0004	0.0000	0.0000	0.0000	0.0000
	2	0.9470	0.7382	0.4628	0.2318	0.0889	0.0250	0.0043	0.0003	0.0000	0.0000	0.0000
	3	0.9917	0.9144	0.7297	0.4826	0.2539	0.0994	0.0253	0.0031	0.0001	0.0000	0.0000
	4	0.9991	0.9804	0.9012	0.7334	0.5000	0.2666	0.0988	0.0196	0.0009	0.0000	0.0000
	5	0.9999	0.9969	0.9747	0.9006	0.7461	0.5174	0.2703	0.0856	0.0083	0.0006	0.0000
	6	1.0000	0.9997	0.9957	0.9750	0.9102	0.7682	0.5372	0.2618	0.0530	0.0084	0.0001
	7	1.0000	1.0000	0.9996	0.9962	0.9805	0.9295	0.8040	0.5638	0.2252	0.0712	0.0034
	8	1.0000	1.0000	1.0000	0.9997	0.9980	0.9899	0.9596	0.8658	0.6126	0.3698	0.0865

Montgomery, Douglas C., and George C. Runger, *Applied Statistics and Probability for Engineers*, 4th ed. Reproduced by permission of John Wiley & Sons, 2007.

Cumulative Binomial Probabilities $P(X \leq x)$ (continued)

		<i>P</i>										
<i>n</i>	<i>x</i>	0.1	0.2	0.3	0.4	0.5	0.6	0.7	0.8	0.9	0.95	0.99
10	0	0.3487	0.1074	0.0282	0.0060	0.0010	0.0001	0.0000	0.0000	0.0000	0.0000	0.0000
	1	0.7361	0.3758	0.1493	0.0464	0.0107	0.0017	0.0001	0.0000	0.0000	0.0000	0.0000
	2	0.9298	0.6778	0.3828	0.1673	0.0547	0.0123	0.0016	0.0001	0.0000	0.0000	0.0000
	3	0.9872	0.8791	0.6496	0.3823	0.1719	0.0548	0.0106	0.0009	0.0000	0.0000	0.0000
	4	0.9984	0.9672	0.8497	0.6331	0.3770	0.1662	0.0473	0.0064	0.0001	0.0000	0.0000
	5	0.9999	0.9936	0.9527	0.8338	0.6230	0.3669	0.1503	0.0328	0.0016	0.0001	0.0000
	6	1.0000	0.9991	0.9894	0.9452	0.8281	0.6177	0.3504	0.1209	0.0128	0.0010	0.0000
	7	1.0000	0.9999	0.9984	0.9877	0.9453	0.8327	0.6172	0.3222	0.0702	0.0115	0.0001
	8	1.0000	1.0000	0.9999	0.9983	0.9893	0.9536	0.8507	0.6242	0.2639	0.0861	0.0043
	9	1.0000	1.0000	1.0000	0.9999	0.9990	0.9940	0.9718	0.8926	0.6513	0.4013	0.0956
15	0	0.2059	0.0352	0.0047	0.0005	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
	1	0.4590	0.1671	0.0353	0.0052	0.0005	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
	2	0.8159	0.3980	0.1268	0.0271	0.0037	0.0003	0.0000	0.0000	0.0000	0.0000	0.0000
	3	0.9444	0.6482	0.2969	0.0905	0.0176	0.0019	0.0001	0.0000	0.0000	0.0000	0.0000
	4	0.9873	0.8358	0.5155	0.2173	0.0592	0.0093	0.0007	0.0000	0.0000	0.0000	0.0000
	5	0.9978	0.9389	0.7216	0.4032	0.1509	0.0338	0.0037	0.0001	0.0000	0.0000	0.0000
	6	0.9997	0.9819	0.8689	0.6098	0.3036	0.0950	0.0152	0.0008	0.0000	0.0000	0.0000
	7	1.0000	0.9958	0.9500	0.7869	0.5000	0.2131	0.0500	0.0042	0.0000	0.0000	0.0000
	8	1.0000	0.9992	0.9848	0.9050	0.6964	0.3902	0.1311	0.0181	0.0003	0.0000	0.0000
	9	1.0000	0.9999	0.9963	0.9662	0.8491	0.5968	0.2784	0.0611	0.0022	0.0001	0.0000
	10	1.0000	1.0000	0.9993	0.9907	0.9408	0.7827	0.4845	0.1642	0.0127	0.0006	0.0000
	11	1.0000	1.0000	0.9999	0.9981	0.9824	0.9095	0.7031	0.3518	0.0556	0.0055	0.0000
	12	1.0000	1.0000	1.0000	0.9997	0.9963	0.9729	0.8732	0.6020	0.1841	0.0362	0.0004
	13	1.0000	1.0000	1.0000	1.0000	0.9995	0.9948	0.9647	0.8329	0.4510	0.1710	0.0096
	14	1.0000	1.0000	1.0000	1.0000	1.0000	0.9995	0.9953	0.9648	0.7941	0.5367	0.1399
20	0	0.1216	0.0115	0.0008	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
	1	0.3917	0.0692	0.0076	0.0005	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
	2	0.6769	0.2061	0.0355	0.0036	0.0002	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
	3	0.8670	0.4114	0.1071	0.0160	0.0013	0.0000	0.0000	0.0000	0.0000	0.0000	0.0000
	4	0.9568	0.6296	0.2375	0.0510	0.0059	0.0003	0.0000	0.0000	0.0000	0.0000	0.0000
	5	0.9887	0.8042	0.4164	0.1256	0.0207	0.0016	0.0000	0.0000	0.0000	0.0000	0.0000
	6	0.9976	0.9133	0.6080	0.2500	0.0577	0.0065	0.0003	0.0000	0.0000	0.0000	0.0000
	7	0.9996	0.9679	0.7723	0.4159	0.1316	0.0210	0.0013	0.0000	0.0000	0.0000	0.0000
	8	0.9999	0.9900	0.8867	0.5956	0.2517	0.0565	0.0051	0.0001	0.0000	0.0000	0.0000
	9	1.0000	0.9974	0.9520	0.7553	0.4119	0.1275	0.0171	0.0006	0.0000	0.0000	0.0000
	10	1.0000	0.9994	0.9829	0.8725	0.5881	0.2447	0.0480	0.0026	0.0000	0.0000	0.0000
	11	1.0000	0.9999	0.9949	0.9435	0.7483	0.4044	0.1133	0.0100	0.0001	0.0000	0.0000
	12	1.0000	1.0000	0.9987	0.9790	0.8684	0.5841	0.2277	0.0321	0.0004	0.0000	0.0000
	13	1.0000	1.0000	0.9997	0.9935	0.9423	0.7500	0.3920	0.0867	0.0024	0.0000	0.0000
	14	1.0000	1.0000	1.0000	0.9984	0.9793	0.8744	0.5836	0.1958	0.0113	0.0003	0.0000
	15	1.0000	1.0000	1.0000	0.9997	0.9941	0.9490	0.7625	0.3704	0.0432	0.0026	0.0000
	16	1.0000	1.0000	1.0000	1.0000	0.9987	0.9840	0.8929	0.5886	0.1330	0.0159	0.0000
	17	1.0000	1.0000	1.0000	1.0000	0.9998	0.9964	0.9645	0.7939	0.3231	0.0755	0.0010
	18	1.0000	1.0000	1.0000	1.0000	1.0000	0.9995	0.9924	0.9308	0.6083	0.2642	0.0169
	19	1.0000	1.0000	1.0000	1.0000	1.0000	1.0000	0.9992	0.9885	0.8784	0.6415	0.1821

Montgomery, Douglas C., and George C. Runger, *Applied Statistics and Probability for Engineers*, 4th ed. Reproduced by permission of John Wiley & Sons, 2007.

STATISTICAL QUALITY CONTROL

Average and Range Charts

n	A₂	D₃	D₄
2	1.880	0	3.268
3	1.023	0	2.574
4	0.729	0	2.282
5	0.577	0	2.114
6	0.483	0	2.004
7	0.419	0.076	1.924
8	0.373	0.136	1.864
9	0.337	0.184	1.816
10	0.308	0.223	1.777

X_i = an individual observation

n = the sample size of a group

k = the number of groups

R = (range) the difference between the largest and smallest observations in a sample of size n .

$$\bar{X} = \frac{X_1 + X_2 + \dots + X_n}{n}$$

$$\bar{\bar{X}} = \frac{\bar{X}_1 + \bar{X}_2 + \dots + \bar{X}_k}{k}$$

$$\bar{R} = \frac{R_1 + R_2 + \dots + R_k}{k}$$

The R Chart formulas are:

$$CL_R = \bar{R}$$

$$UCL_R = D_4 \bar{R}$$

$$LCL_R = D_3 \bar{R}$$

The \bar{X} Chart formulas are:

$$CL_X = \bar{\bar{X}}$$

$$UCL_X = \bar{\bar{X}} + A_2 \bar{R}$$

$$LCL_X = \bar{\bar{X}} - A_2 \bar{R}$$

Standard Deviation Charts

n	A₃	B₃	B₄
2	2.659	0	3.267
3	1.954	0	2.568
4	1.628	0	2.266
5	1.427	0	2.089
6	1.287	0.030	1.970
7	1.182	0.119	1.882
8	1.099	0.185	1.815
9	1.032	0.239	1.761
10	0.975	0.284	1.716

$$UCL_X = \bar{\bar{X}} + A_3 \bar{S}$$

$$CL_X = \bar{\bar{X}}$$

$$LCL_X = \bar{\bar{X}} - A_3 \bar{S}$$

$$UCL_S = B_4 \bar{S}$$

$$CL_S = \bar{S}$$

$$LCL_S = B_3 \bar{S}$$

Approximations

The following table and equations may be used to generate initial approximations of the items indicated.

n	c₄	d₂	d₃
2	0.7979	1.128	0.853
3	0.8862	1.693	0.888
4	0.9213	2.059	0.880
5	0.9400	2.326	0.864
6	0.9515	2.534	0.848
7	0.9594	2.704	0.833
8	0.9650	2.847	0.820
9	0.9693	2.970	0.808
10	0.9727	3.078	0.797

$$\hat{\sigma} = \bar{R}/d_2$$

$$\hat{\sigma} = \bar{S}/c_4$$

$$\sigma_R = d_3 \hat{\sigma}$$

$$\sigma_S = \hat{\sigma} \sqrt{1 - c_4^2}, \text{ where}$$

$\hat{\sigma}$ = an estimate of σ

σ_R = an estimate of the standard deviation of the ranges of the samples

σ_S = an estimate of the standard deviation of the standard deviations of the samples

Tests for Out of Control

1. A single point falls outside the (three sigma) control limits.
2. Two out of three successive points fall on the same side of and more than two sigma units from the center line.
3. Four out of five successive points fall on the same side of and more than one sigma unit from the center line.
4. Eight successive points fall on the same side of the center line.

Probability and Density Functions: Means and Variances

Variable	Equation	Mean	Variance
Binomial Coefficient	$\binom{n}{x} = \frac{n!}{x!(n-x)!}$		
Binomial	$b(x; n, p) = \binom{n}{x} p^x (1-p)^{n-x}$	np	$np(1-p)$
Hyper Geometric	$h(x; n, r, N) = \binom{r}{x} \binom{N-r}{n-x} / \binom{N}{n}$	$\frac{nr}{N}$	$\frac{r(N-r)n(N-n)}{N^2(N-1)}$
Poisson	$f(x; \lambda) = \frac{\lambda^x e^{-\lambda}}{x!}$	λ	λ
Geometric	$g(x; p) = p (1-p)^{x-1}$	$1/p$	$(1-p)/p^2$
Negative Binomial	$f(y; r, p) = \binom{y+r-1}{r-1} p^r (1-p)^y$	r/p	$r(1-p)/p^2$
Multinomial	$f(x_1, \dots, x_k) = \frac{n!}{x_1! \dots x_k!} p_1^{x_1} \dots p_k^{x_k}$	np_i	$np_i(1-p_i)$
Uniform	$f(x) = 1/(b-a)$	$(a+b)/2$	$(b-a)^2/12$
Gamma	$f(x) = \frac{x^{\alpha-1} e^{-x/\beta}}{\beta^\alpha \Gamma(\alpha)}; \quad \alpha > 0, \beta > 0$	$\alpha\beta$	$\alpha\beta^2$
Exponential	$f(x) = \frac{1}{\beta} e^{-x/\beta}$	β	β^2
Weibull	$f(x) = \frac{\alpha}{\beta} x^{\alpha-1} e^{-x^\alpha/\beta}$	$\beta^{1/\alpha} \Gamma[(\alpha+1)/\alpha]$	$\beta^{2/\alpha} \left[\Gamma\left(\frac{\alpha+1}{\alpha}\right) - \Gamma^2\left(\frac{\alpha+1}{\alpha}\right) \right]$
Normal	$f(x) = \frac{1}{\sigma\sqrt{2\pi}} e^{-\frac{1}{2}\left(\frac{x-\mu}{\sigma}\right)^2}$	μ	σ^2
Triangular	$f(x) = \begin{cases} \frac{2(x-a)}{(b-a)(m-a)} & \text{if } a \leq x \leq m \\ \frac{2(b-x)}{(b-a)(b-m)} & \text{if } m < x \leq b \end{cases}$	$\frac{a+b+m}{3}$	$\frac{a^2 + b^2 + m^2 - ab - am - bm}{18}$

CHEMISTRY

DEFINITIONS

Avogadro's Number – The number of elementary particles in a mol of a substance.

$$1 \text{ mol} = 1 \text{ gram mole}$$

$$1 \text{ mol} = 6.02 \times 10^{23} \text{ particles}$$

Mol – The amount of a substance that contains as many particles as 12 grams of ^{12}C (carbon 12).

Molarity of Solutions – The number of gram moles of a substance dissolved in a liter of solution.

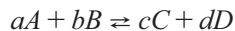
Molality of Solutions – The number of gram moles of a substance per 1,000 grams of solvent.

Normality of Solutions – The product of the molarity of a solution and the number of valence changes taking place in a reaction.

Molar Volume of an Ideal Gas [at 0°C (32°F) and 1 atm (14.7 psia)]; 22.4 L/g mole [$359 \text{ ft}^3/\text{lb mole}$].

Mole Fraction of a Substance – The ratio of the number of moles of a substance to the total moles present in a mixture of substances.

Equilibrium Constant of a Chemical Reaction



$$K_{\text{eq}} = \frac{[C]^c[D]^d}{[A]^a[B]^b}$$

Le Chatelier's Principle for Chemical Equilibrium – When a stress (such as a change in concentration, pressure, or temperature) is applied to a system in equilibrium, the equilibrium shifts in such a way that tends to relieve the stress.

Heats of Reaction, Solution, Formation, and Combustion – Chemical processes generally involve the absorption or evolution of heat. In an endothermic process, heat is absorbed (enthalpy change is positive). In an exothermic process, heat is evolved (enthalpy change is negative).

Solubility Product of a slightly soluble substance AB:



$$\text{Solubility Product Constant} = K_{\text{SP}} = [A^+]^m[B^-]^n$$

Faraday's Law – One gram equivalent weight of matter is chemically altered at each electrode for 96,485 coulombs, or 1 Faraday, of electricity passed through the electrolyte.

Faraday's Equation

$$m = \left(\frac{Q}{F} \right) \left(\frac{M}{z} \right), \text{ where}$$

m = mass (grams) of substance liberated at electrode

Q = total electric charge passed through electrolyte (coulomb or ampere•second)

F = 96,485 coulombs/mol

M = molar mass of the substance (g/mol)

z = valence number

A *catalyst* is a substance that alters the rate of a chemical reaction. The catalyst does not affect the position of equilibrium of a reversible reaction.

The *atomic number* is the number of protons in the atomic nucleus.

Boiling Point Elevation – The presence of a nonvolatile solute in a solvent raises the boiling point of the resulting solution.

Freezing Point Depression – The presence of a solute lowers the freezing point of the resulting solution.

ACIDS, BASES, and pH (aqueous solutions)

$$\text{pH} = \log_{10} \left(\frac{1}{[\text{H}^+]} \right), \text{ where}$$

$[\text{H}^+]$ = molar concentration of hydrogen ion, in gram moles per liter. *Acids* have $\text{pH} < 7$. *Bases* have $\text{pH} > 7$.

Periodic Table of Elements

I														VIII			
1 H 1.0079														2 He 4.0026			
I		II															
3 Li 6.941	4 Be 9.0122																
11 Na 22.990	12 Mg 24.305																
19 K 39.098	20 Ca 40.078	21 Sc 44.956	22 Ti 47.88	23 V 50.941	24 Cr 51.996	25 Mn 54.938	26 Fe 55.847	27 Co 58.933	28 Ni 58.69	29 Cu 63.546	30 Zn 65.39	31 Ga 69.723	32 Ge 72.61	33 As 74.921	34 Se 78.96	35 Br 79.904	36 Kr 83.80
37 Rb 85.468	38 Sr 87.62	39 Y 88.906	40 Zr 91.224	41 Nb 92.906	42 Mo 95.94	43 Tc (98)	44 Ru 101.07	45 Rh 102.91	46 Pd 106.42	47 Ag 107.87	48 Cd 112.41	49 In 114.82	50 Sn 118.71	51 Sb 121.75	52 Te 127.60	53 I 126.90	54 Xe 131.29
55 Cs 132.91	56 Ba 137.33	57* La 138.91	72 Hf 178.49	73 Ta 180.95	74 W 183.85	75 Re 186.21	76 Os 190.2	77 Ir 192.22	78 Pt 195.08	79 Au 196.97	80 Hg 200.59	81 Tl 204.38	82 Pb 207.2	83 Bi 208.98	84 Po (209)	85 At (210)	86 Rn (222)
87 Fr (223)	88 Ra 226.02	89** Ac 227.03	104 Rf (261)	105 Ha (262)													
*Lanthanide Series			58 Ce 140.12	59 Pr 140.91	60 Nd 144.24	61 Pm (145)	62 Sm 150.36	63 Eu 151.96	64 Gd 157.25	65 Tb 158.92	66 Dy 162.50	67 Ho 164.93	68 Er 167.26	69 Tm 168.93	70 Yb 173.04	71 Lu 174.97	
**Actinide Series			90 Th 232.04	91 Pa 231.04	92 U 238.03	93 Np 237.05	94 Pu (244)	95 Am (243)	96 Cm (247)	97 Bk (247)	98 Cf (251)	99 Es (252)	100 Fm (257)	101 Md (258)	102 No (259)	103 Lr (260)	

SELECTED RULES OF NOMENCLATURE IN ORGANIC CHEMISTRY

Alcohols

Three systems of nomenclature are in general use. In the first, the alkyl group attached to the hydroxyl group is named and the separate word *alcohol* is added. In the second system, the higher alcohols are considered as derivatives of the first member of the series, which is called *carbinol*. The third method is the modified Geneva system in which (1) the longest carbon chain containing the hydroxyl group determines the surname, (2) the ending *e* of the corresponding saturated hydrocarbon is replaced by *ol*, (3) the carbon chain is numbered from the end that gives the hydroxyl group the smaller number, and (4) the side chains are named and their positions indicated by the proper number. Alcohols in general are divided into three classes. In *primary* alcohols the hydroxyl group is united to a primary carbon atom, that is, a carbon atom united directly to only one other carbon atom. *Secondary* alcohols have the hydroxyl group united to a secondary carbon atom, that is, one united to two other carbon atoms. *Tertiary* alcohols have the hydroxyl group united to a tertiary carbon atom, that is, one united to three other carbon atoms.

Ethers

Ethers are generally designated by naming the alkyl groups and adding the word *ether*. The group RO is known as an *alkoxyl group*. Ethers may also be named as alkoxy derivatives of hydrocarbons.

Carboxylic Acids

The name of each linear carboxylic acid is unique to the number of carbon atoms it contains. 1: (one carbon atom) Formic. 2: Acetic. 3: Propionic. 4: Butyric. 5: Valeric. 6: Caproic. 7: Enanthic. 8: Caprylic. 9: Pelargonic. 10: Capric.

Aldehydes

The common names of aldehydes are derived from the acids that would be formed on oxidation, that is, the acids having the same number of carbon atoms. In general the *ic acid* is dropped and *aldehyde* added.

Ketones

The common names of ketones are derived from the acid which on pyrolysis would yield the ketone. A second method, especially useful for naming mixed ketones, simply names the alkyl groups and adds the word *ketone*. The name is written as three separate words.

Unsaturated Acyclic Hydrocarbons

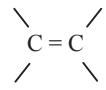
The simplest compounds in this class of hydrocarbon chemicals are olefins or alkenes with a single carbon-carbon double bond, having the general formula of C_nH_{2n} . The simplest example in this category is ethylene, C_2H_4 .

Dienes are acyclic hydrocarbons with two carbon-carbon double bonds, having the general formula of C_nH_{2n-2} ; butadiene (C_4H_6) is an example of such.

Similarly, trienes have three carbon-carbon double bonds with the general formula of C_nH_{2n-4} ; hexatriene (C_6H_8) is such an example.

The simplest alkynes have a single carbon-carbon triple bond with the general formula of C_nH_{2n-2} . This series of compounds begins with acetylene, or C_2H_2 .

Important Families of Organic Compounds

	FAMILY											
	Alkane	Alkene	Alkyne	Arene	Haloalkane	Alcohol	Ether	Amine	Aldehyde	Ketone	Carboxylic Acid	Ester
Specific Example	CH ₃ CH ₃	H ₂ C = CH ₂	HC ≡ CH		CH ₃ CH ₂ Cl	CH ₃ CH ₂ OH	CH ₃ OCH ₃	CH ₃ NH ₂	$\begin{matrix} \text{O} \\ \parallel \\ \text{CH}_3\text{CH} \end{matrix}$	$\begin{matrix} \text{O} \\ \parallel \\ \text{CH}_3\text{CCH}_3 \end{matrix}$	$\begin{matrix} \text{O} \\ \parallel \\ \text{CH}_3\text{COH} \end{matrix}$	$\begin{matrix} \text{O} \\ \parallel \\ \text{CH}_3\text{COCH}_3 \end{matrix}$
IUPAC Name	Ethane	Ethene or Ethylene	Ethyne or Acetylene	Benzene	Chloroethane	Ethanol	Methoxy-methane	Methanamine	Ethanal	Acetone	Ethanoic Acid	Methyl ethanoate
Common Name	Ethane	Ethylene	Acetylene	Benzene	Ethyl chloride	Ethyl alcohol	Dimethyl ether	Methylamine	Acetaldehyde	Dimethyl ketone	Acetic Acid	Methyl acetate
General Formula	RH	RCH = CH ₂ RCH = CHR R ₂ C = CHR R ₂ C = CR ₂	RC ≡ CH RC ≡ CR	ArH	RX	ROH	ROR	RNH ₂ R ₂ NH R ₃ N	$\begin{matrix} \text{O} \\ \parallel \\ \text{RCH} \end{matrix}$	$\begin{matrix} \text{O} \\ \parallel \\ \text{R}_1\text{CR}_2 \end{matrix}$	$\begin{matrix} \text{O} \\ \parallel \\ \text{RCOH} \end{matrix}$	$\begin{matrix} \text{O} \\ \parallel \\ \text{RCOR} \end{matrix}$
Functional Group	C-H and C-C bonds		-C ≡ C -	Aromatic Ring	$\begin{matrix} & \\ -\text{C}-\text{X} \end{matrix}$	$\begin{matrix} & \\ -\text{C}-\text{OH} \end{matrix}$	$\begin{matrix} & \\ -\text{C}-\text{O}-\text{C} \end{matrix}$	$\begin{matrix} & \\ -\text{C}-\text{N}- \end{matrix}$	$\begin{matrix} \text{O} \\ \parallel \\ -\text{C}-\text{H} \end{matrix}$	$\begin{matrix} \text{O} \\ \parallel \\ -\text{C}- \end{matrix}$	$\begin{matrix} \text{O} \\ \parallel \\ -\text{C}-\text{OH} \end{matrix}$	$\begin{matrix} \text{O} \\ \parallel \\ -\text{C}-\text{O}-\text{C}- \end{matrix}$

**Common Names and Molecular Formulas of Some Industrial
(Inorganic and Organic) Chemicals**

Common Name	Chemical Name	Molecular Formula
Muriatic acid	Hydrochloric acid	HCl
Cumene	Isopropyl benzene	C ₆ H ₅ CH(CH ₃) ₂
Styrene	Vinyl benzene	C ₆ H ₅ CH=CH ₂
—	Hypochlorite ion	OCl ⁻¹
—	Chlorite ion	ClO ₂ ⁻¹
—	Chlorate ion	ClO ₃ ⁻¹
—	Perchlorate ion	ClO ₄ ⁻¹
Gypsum	Calcium sulfate	CaSO ₄
Limestone	Calcium carbonate	CaCO ₃
Dolomite	Magnesium carbonate	MgCO ₃
Bauxite	Aluminum oxide	Al ₂ O ₃
Anatase	Titanium dioxide	TiO ₂
Rutile	Titanium dioxide	TiO ₂
—	Vinyl chloride	CH ₂ =CHCl
—	Ethylene oxide	C ₂ H ₄ O
Pyrite	Ferrous sulfide	FeS
Epsom salt	Magnesium sulfate	MgSO ₄
Hydroquinone	p-Dihydroxy benzene	C ₆ H ₄ (OH) ₂
Soda ash	Sodium carbonate	Na ₂ CO ₃
Salt	Sodium chloride	NaCl
Potash	Potassium carbonate	K ₂ CO ₃
Baking soda	Sodium bicarbonate	NaHCO ₃
Lye	Sodium hydroxide	NaOH
Caustic soda	Sodium hydroxide	NaOH
—	Vinyl alcohol	CH ₂ =CHOH
Carbolic acid	Phenol	C ₆ H ₅ OH
Aniline	Aminobenzene	C ₆ H ₅ NH ₂
—	Urea	(NH ₂) ₂ CO
Toluene	Methyl benzene	C ₆ H ₅ CH ₃
Xylene	Dimethyl benzene	C ₆ H ₄ (CH ₃) ₂
—	Silane	SiH ₄
—	Ozone	O ₃
Neopentane	2,2-Dimethylpropane	CH ₃ C(CH ₃) ₂ CH ₃
Magnetite	Ferrous/ferric oxide	Fe ₃ O ₄
Quicksilver	Mercury	Hg
Heavy water	Deuterium oxide	(H ²) ₂ O
—	Borane	BH ₃
Eyewash	Boric acid (solution)	H ₃ BO ₃
—	Deuterium	H ²
—	Tritium	H ³
Laughing gas	Nitrous oxide	N ₂ O
—	Phosgene	COCl ₂
Wolfram	Tungsten	W
—	Permanganate ion	MnO ₄ ⁻¹
—	Dichromate ion	Cr ₂ O ₇ ⁻²
—	Hydronium ion	H ₃ O ⁺¹
Brine	Sodium chloride (solution)	NaCl
Battery acid	Sulfuric acid	H ₂ SO ₄

ELECTROCHEMISTRY

Cathode – The electrode at which reduction occurs.

Anode – The electrode at which oxidation occurs.

Oxidation – The loss of electrons.

Reduction – The gaining of electrons.

Cation – Positive ion

Anion – Negative ion

Standard Oxidation Potentials for Corrosion Reactions*	
Corrosion Reaction	Potential, E_o , Volts vs. Normal Hydrogen Electrode
$\text{Au} \rightarrow \text{Au}^{3+} + 3\text{e}^-$	-1.498
$2\text{H}_2\text{O} \rightarrow \text{O}_2 + 4\text{H}^+ + 4\text{e}^-$	-1.229
$\text{Pt} \rightarrow \text{Pt}^{2+} + 2\text{e}^-$	-1.200
$\text{Pd} \rightarrow \text{Pd}^{2+} + 2\text{e}^-$	-0.987
$\text{Ag} \rightarrow \text{Ag}^+ + \text{e}^-$	-0.799
$2\text{Hg} \rightarrow \text{Hg}_2^{2+} + 2\text{e}^-$	-0.788
$\text{Fe}^{2+} \rightarrow \text{Fe}^{3+} + \text{e}^-$	-0.771
$4(\text{OH})^- \rightarrow \text{O}_2 + 2\text{H}_2\text{O} + 4\text{e}^-$	-0.401
$\text{Cu} \rightarrow \text{Cu}^{2+} + 2\text{e}^-$	-0.337
$\text{Sn}^{2+} \rightarrow \text{Sn}^{4+} + 2\text{e}^-$	-0.150
$\text{H}_2 \rightarrow 2\text{H}^+ + 2\text{e}^-$	0.000
$\text{Pb} \rightarrow \text{Pb}^{2+} + 2\text{e}^-$	+0.126
$\text{Sn} \rightarrow \text{Sn}^{2+} + 2\text{e}^-$	+0.136
$\text{Ni} \rightarrow \text{Ni}^{2+} + 2\text{e}^-$	+0.250
$\text{Co} \rightarrow \text{Co}^{2+} + 2\text{e}^-$	+0.277
$\text{Cd} \rightarrow \text{Cd}^{2+} + 2\text{e}^-$	+0.403
$\text{Fe} \rightarrow \text{Fe}^{2+} + 2\text{e}^-$	+0.440
$\text{Cr} \rightarrow \text{Cr}^{3+} + 3\text{e}^-$	+0.744
$\text{Zn} \rightarrow \text{Zn}^{2+} + 2\text{e}^-$	+0.763
$\text{Al} \rightarrow \text{Al}^{3+} + 3\text{e}^-$	+1.662
$\text{Mg} \rightarrow \text{Mg}^{2+} + 2\text{e}^-$	+2.363
$\text{Na} \rightarrow \text{Na}^+ + \text{e}^-$	+2.714
$\text{K} \rightarrow \text{K}^+ + \text{e}^-$	+2.925

* Measured at 25°C. Reactions are written as anode half-cells.

Arrows are reversed for cathode half-cells.

Flinn, Richard A., and Paul K. Trojan, *Engineering Materials and Their Applications*, 4th ed., Houghton Mifflin Company, 1990.

NOTE: In some chemistry texts, the reactions and the signs of the values (in this table) are reversed; for example, the half-cell potential of zinc is given as -0.763 volt for the reaction $\text{Zn}^{2+} + 2\text{e}^- \rightarrow \text{Zn}$. When the potential E_o is positive, the reaction proceeds spontaneously as written.

MATERIALS SCIENCE/STRUCTURE OF MATTER

ATOMIC BONDING

Primary Bonds

Ionic (e.g., salts, metal oxides)

Covalent (e.g., within polymer molecules)

Metallic (e.g., metals)

CORROSION

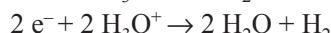
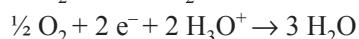
A table listing the standard electromotive potentials of metals is shown on the previous page.

For corrosion to occur, there must be an anode and a cathode in electrical contact in the presence of an electrolyte.

Anode Reaction (Oxidation) of a Typical Metal, M



Possible Cathode Reactions (Reduction)



When dissimilar metals are in contact, the more electropositive one becomes the anode in a corrosion cell. Different regions of carbon steel can also result in a corrosion reaction: e.g., cold-worked regions are anodic to noncold-worked; different oxygen concentrations can cause oxygen-deficient regions to become cathodic to oxygen-rich regions; grain boundary regions are anodic to bulk grain; in multiphase alloys, various phases may not have the same galvanic potential.

DIFFUSION

Diffusion Coefficient

$$D = D_o e^{-Q/(RT)}, \text{ where}$$

D = diffusion coefficient

D_o = proportionality constant

Q = activation energy

R = gas constant [8.314 J/(mol•K)]

T = absolute temperature

THERMAL AND MECHANICAL PROCESSING

Cold working (plastically deforming) a metal increases strength and lowers ductility.

Raising temperature causes (1) recovery (stress relief), (2) recrystallization, and (3) grain growth. *Hot working* allows these processes to occur simultaneously with deformation.

Quenching is rapid cooling from elevated temperature, preventing the formation of equilibrium phases.

In steels, quenching austenite [FCC (γ) iron] can result in martensite instead of equilibrium phases—ferrite [BCC (α) iron] and cementite (iron carbide).

PROPERTIES OF MATERIALS

Electrical

Capacitance: The charge-carrying capacity of an insulating material

Charge held by a capacitor

$$q = CV$$

q = charge

C = capacitance

V = voltage

Capacitance of a parallel plate capacitor

$$C = \frac{\epsilon A}{d}$$

C = capacitance

ϵ = permittivity of material

A = cross-sectional area of the plates

d = distance between the plates

ϵ is also expressed as the product of the dielectric constant (κ) and the permittivity of free space ($\epsilon_0 = 8.85 \times 10^{-12} \text{ F/m}$)

Resistivity: The material property that determines the resistance of a resistor

Resistivity of a material within a resistor

$$\rho = \frac{RA}{L}$$

ρ = resistivity of the material

R = resistance of the resistor

A = cross-sectional area of the resistor

L = length of the resistor

Conductivity is the reciprocal of the resistivity

Photoelectric effect—electrons are emitted from matter (metals and nonmetallic solids, liquids or gases) as a consequence of their absorption of energy from electromagnetic radiation of very short wavelength and high frequency.

Piezoelectric effect—the electromechanical and the electrical state in crystalline materials.

Mechanical

Strain is defined as change in length per unit length; for pure tension the following apply:

Engineering strain

$$\epsilon = \frac{\Delta L}{L_0}$$

ϵ = engineering strain

ΔL = change in length

L_0 = initial length

True strain

$$\epsilon_T = \frac{dL}{L}$$

ϵ_T = true strain

dL = differential change in length

L = initial length

$$\epsilon_T = \ln(1 + \epsilon)$$

Properties of Metals

Metal	Symbol	Atomic Weight	Density ρ (kg/m ³) Water = 1000	Melting Point (°C)	Melting Point (°F)	Specific Heat [J/(kg·K)]	Electrical Resistivity ($10^{-8} \Omega\cdot\text{m}$) at 0°C (273.2 K)	Heat Conductivity λ [W/(m·K)] at 0°C (273.2 K)
Aluminum	Al	26.98	2,698	660	1,220	895.9	2.5	236
Antimony	Sb	121.75	6,692	630	1,166	209.3	39	25.5
Arsenic	As	74.92	5,776	subl. 613	subl. 1,135	347.5	26	—
Barium	Ba	137.33	3,594	710	1,310	284.7	36	—
Beryllium	Be	9.012	1,846	1,285	2,345	2,051.5	2.8	218
Bismuth	Bi	208.98	9,803	271	519	125.6	107	8.2
Cadmium	Cd	112.41	8,647	321	609	234.5	6.8	97
Caesium	Cs	132.91	1,900	29	84	217.7	18.8	36
Calcium	Ca	40.08	1,530	840	1,544	636.4	3.2	—
Cerium	Ce	140.12	6,711	800	1,472	188.4	7.3	11
Chromium	Cr	52	7,194	1,860	3,380	406.5	12.7	96.5
Cobalt	Co	58.93	8,800	1,494	2,721	431.2	5.6	105
Copper	Cu	63.54	8,933	1,084	1,983	389.4	1.55	403
Gallium	Ga	69.72	5,905	30	86	330.7	13.6	41
Gold	Au	196.97	19,281	1,064	1,947	129.8	2.05	319
Indium	In	114.82	7,290	156	312	238.6	8	84
Iridium	Ir	192.22	22,550	2,447	4,436	138.2	4.7	147
Iron	Fe	55.85	7,873	1,540	2,804	456.4	8.9	83.5
Lead	Pb	207.2	11,343	327	620	129.8	19.2	36
Lithium	Li	6.94	533	180	356	4,576.2	8.55	86
Magnesium	Mg	24.31	1,738	650	1,202	1,046.7	3.94	157
Manganese	Mn	54.94	7,473	1,250	2,282	502.4	138	8
Mercury	Hg	200.59	13,547	-39	-38	142.3	94.1	7.8
Molybendum	Mo	95.94	10,222	2,620	4,748	272.1	5	139
Nickel	Ni	58.69	8,907	1,455	2,651	439.6	6.2	94
Niobium	Nb	92.91	8,578	2,425	4,397	267.9	15.2	53
Osmium	Os	190.2	22,580	3,030	5,486	129.8	8.1	88
Palladium	Pd	106.4	11,995	1,554	2,829	230.3	10	72
Platinum	Pt	195.08	21,450	1,772	3,221	134	9.81	72
Potassium	K	39.09	862	63	145	753.6	6.1	104
Rhodium	Rh	102.91	12,420	1,963	3,565	242.8	4.3	151
Rubidium	Rb	85.47	1,533	38.8	102	330.7	11	58
Ruthenium	Ru	101.07	12,360	2,310	4,190	255.4	7.1	117
Silver	Ag	107.87	10,500	961	1,760	234.5	1.47	428
Sodium	Na	22.989	966	97.8	208	1,235.1	4.2	142
Strontium	Sr	87.62	2,583	770	1,418	—	20	—
Tantalum	Ta	180.95	16,670	3,000	5,432	150.7	12.3	57
Thallium	Tl	204.38	11,871	304	579	138.2	10	10
Thorium	Th	232.04	11,725	1,700	3,092	117.2	14.7	54
Tin	Sn	118.69	7,285	232	449	230.3	11.5	68
Titanium	Ti	47.88	4,508	1,670	3,038	527.5	39	22
Tungsten	W	183.85	19,254	3,387	6,128	142.8	4.9	177
Uranium	U	238.03	19,050	1,135	2,075	117.2	28	27
Vanadium	V	50.94	6,090	1,920	3,488	481.5	18.2	31
Zinc	Zn	65.38	7,135	419	786	393.5	5.5	117
Zirconium	Zr	91.22	6,507	1,850	3,362	284.7	40	23

◆ Some Extrinsic, Elemental Semiconductors

Element	Dopant	Periodic table group of dopant	Maximum solid solubility of dopant (atoms/m ³)
Si	B	III A	600×10^{24}
	Al	III A	20×10^{24}
	Ga	III A	40×10^{24}
	P	V A	$1,000 \times 10^{24}$
	As	V A	$2,000 \times 10^{24}$
	Sb	V A	70×10^{24}
	Al	III A	400×10^{24}
	Ga	III A	500×10^{24}
	In	III A	4×10^{24}
Ge	As	V A	80×10^{24}
	Sb	V A	10×10^{24}

◆ Impurity Energy Levels for Extrinsic Semiconductors

Semiconductor	Dopant	$E_g - E_d$ (eV)	E_a (eV)
Si	P	0.044	—
	As	0.049	—
	Sb	0.039	—
	Bi	0.069	—
	B	—	0.045
	Al	—	0.057
	Ga	—	0.065
	In	—	0.160
	Tl	—	0.260
Ge	P	0.012	—
	As	0.013	—
	Sb	0.096	—
	B	—	0.010
	Al	—	0.010
	Ga	—	0.010
	In	—	0.011
	Tl	—	0.01
GaAs	Se	0.005	—
	Te	0.003	—
	Zn	—	0.024
	Cd	—	0.021

Stress is defined as force per unit area; for pure tension the following apply:

Engineering stress

$$\sigma = \frac{F}{A_0}$$

σ = engineering stress

F = applied force

A_0 = initial cross-sectional area

True stress

$$\sigma_T = \frac{F}{A}$$

σ_T = true stress

F = applied force

A = actual cross-sectional area

The elastic modulus (also called modulus, modulus of elasticity, Young's modulus) describes the relationship between engineering stress and engineering strain during elastic loading. Hooke's Law applies in such a case.

$$\sigma = E\epsilon \text{ where } E \text{ is the elastic modulus.}$$

Key mechanical properties obtained from a tensile test curve:

- Elastic modulus
- Ductility (also called percent elongation): Permanent engineering strain after failure
- Ultimate tensile strength (also called tensile strength): Maximum engineering stress
- Yield strength: Engineering stress at which permanent deformation is first observed, calculated by 0.2% offset method.

Other mechanical properties:

- Creep: Time-dependent deformation under load. Usually measured by strain rate. For steady-state creep this is:

$$\frac{d\varepsilon}{dt} = A\sigma^n e^{-\frac{Q}{RT}}$$

A = pre-exponential constant

n = stress sensitivity

Q = activation energy for creep

R = ideal gas law constant

T = absolute temperature

- Fatigue: Time-dependent failure under cyclic load. Fatigue life is the number of cycles to failure. The endurance limit is the stress below which fatigue failure is unlikely.
- Fracture toughness: The combination of applied stress and the crack length in a brittle material. It is the stress intensity when the material will fail.

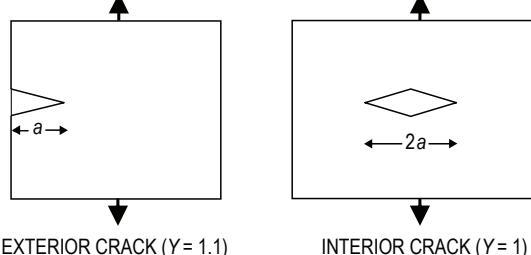
$$K_{IC} = Y\sigma\sqrt{\pi a}$$

K_{IC} = fracture toughness

σ = applied engineering stress

a = crack length

Y = geometrical factor



The critical value of stress intensity at which catastrophic crack propagation occurs, K_{IC} , is a material property.

◆ W.R. Runyan and S.B. Watelski, in *Handbook of Materials and Processes for Electronics*, C.A. Harper, ed., McGraw-Hill, 1970.

Representative Values of Fracture Toughness

Material	K_{Ic} (MPa·m ^{1/2})	K_{Ic} (ksi·in ^{1/2})
A1 2014-T651	24.2	22
A1 2024-T3	44	40
52100 Steel	14.3	13
4340 Steel	46	42
Alumina	4.5	4.1
Silicon Carbide	3.5	3.2

RELATIONSHIP BETWEEN HARDNESS AND TENSILE STRENGTH

For plain carbon steels, there is a general relationship between Brinell hardness and tensile strength as follows:

$$TS(\text{psi}) \approx 500 \text{ BHN}$$

$$TS(\text{MPa}) \approx 3.5 \text{ BHN}$$

ASTM GRAIN SIZE

$$S_V = 2P_L$$

$$N_{(0.0645 \text{ mm}^2)} = 2^{(n - 1)}$$

$$\frac{N_{\text{actual}}}{\text{Actual Area}} = \frac{N}{(0.0645 \text{ mm}^2)}, \text{ where}$$

S_V = grain-boundary surface per unit volume

P_L = number of points of intersection per unit length between the line and the boundaries

N = number of grains observed in a area of 0.0645 mm^2

n = grain size (nearest integer > 1)

COMPOSITE MATERIALS

$$\rho_c = \sum f_i \rho_i$$

$$C_c = \sum f_i c_i$$

$$\left[\sum \frac{f_i}{E_i} \right]^{-1} \leq E_c \leq \sum f_i E_i$$

$$\sigma_c = \sum f_i \sigma_i$$

ρ_c = density of composite

C_c = heat capacity of composite per unit volume

E_c = Young's modulus of composite

f_i = volume fraction of individual material

c_i = heat capacity of individual material per unit volume

E_i = Young's modulus of individual material

σ_c = strength parallel to fiber direction

Also, for axially oriented, long, fiber-reinforced composites, the strains of the two components are equal.

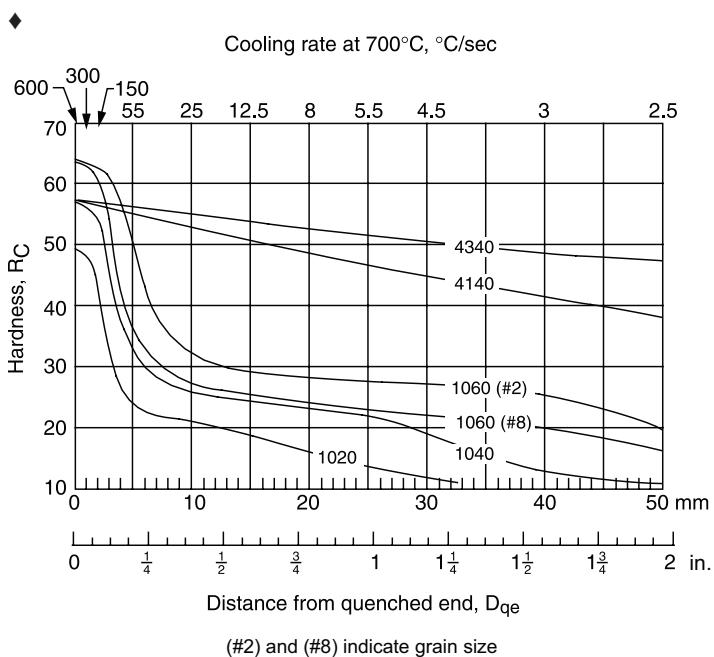
$$(\Delta L/L)_1 = (\Delta L/L)_2$$

ΔL = change in length of the composite

L = original length of the composite

Hardness: Resistance to penetration. Measured by denting a material under known load and measuring the size of the dent.

Hardenability: The "ease" with which hardness can be obtained.



JOMINY HARDENABILITY CURVES FOR SIX STEELS

♦ Van Vlack, L., *Elements of Materials Science & Engineering*, Addison-Wesley, 1989.

The following two graphs show cooling curves for four different positions in the bar.

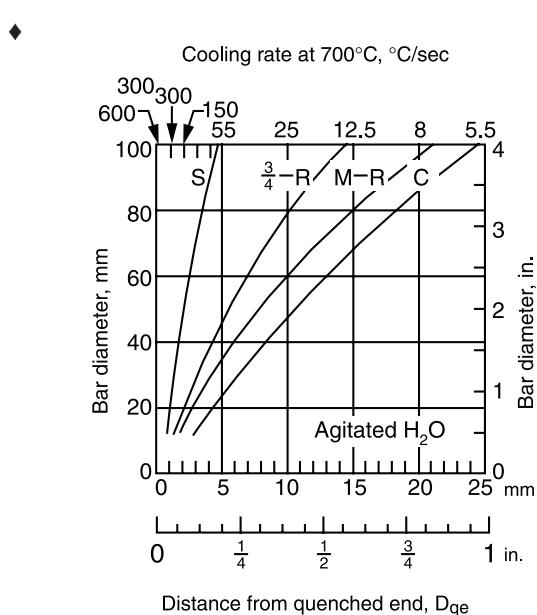
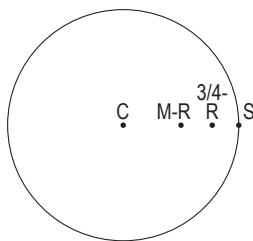
C = Center

M-R = Halfway between center and surface

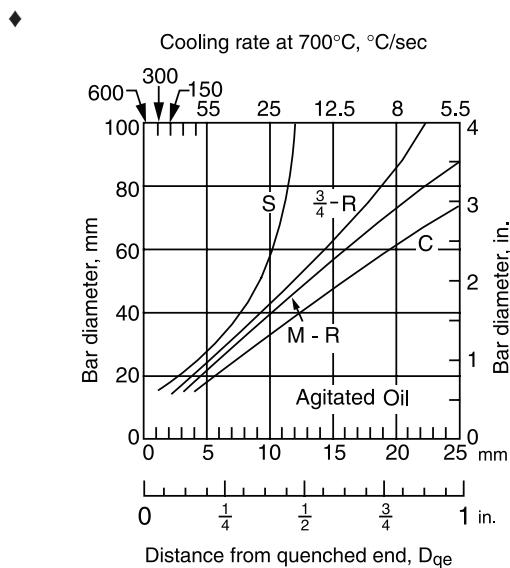
3/4-R = 75% of the distance between the center and the surface

S = Surface

These positions are shown in the following figure.



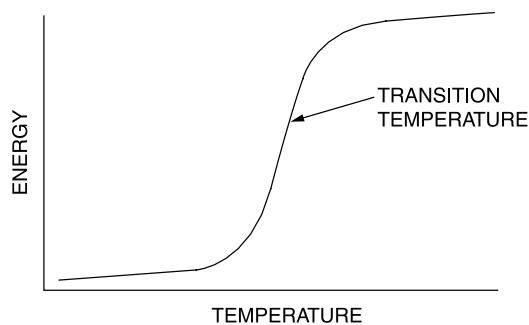
COOLING RATES FOR BARS QUENCHED IN AGITATED WATER



COOLING RATES FOR BARS QUENCHED IN AGITATED OIL

Impact Test

The *Charpy Impact Test* is used to find energy required to fracture and to identify ductile to brittle transition.

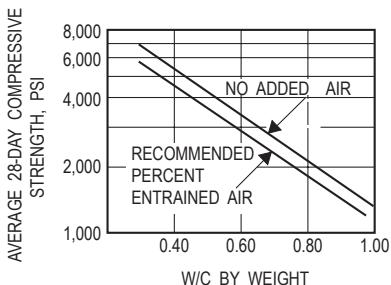


Impact tests determine the amount of energy required to cause failure in standardized test samples. The tests are repeated over a range of temperatures to determine the *ductile to brittle transition temperature*.

◆ Van Vlack, L., *Elements of Materials Science & Engineering*, Addison-Wesley, 1989.

Concrete

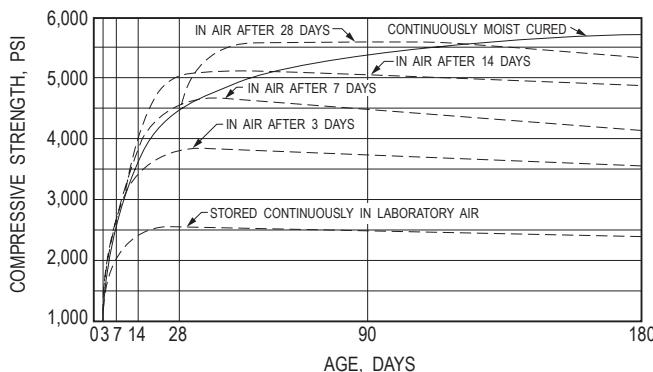
♦



Concrete strength decreases with increases in water-cement ratio for concrete with and without entrained air.

Water-cement (W/C) ratio is the primary factor affecting the strength of concrete. The figure above shows how W/C expressed as a ratio of weight of water and cement by weight of concrete mix affects the compressive strength of both air-entrained and non-air-entrained concrete.

•



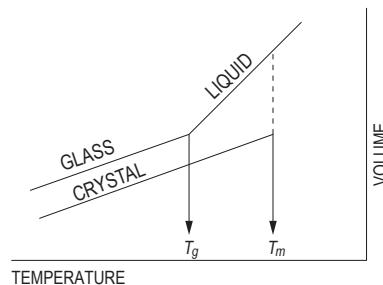
Concrete compressive strength varies with moist-curing conditions. Mixes tested had a water-cement ratio of 0.50, a slump of 3.5 in., cement content of 556 lb/yd³, sand content of 36%, and air content of 4%.

Water content affects workability. However, an increase in water without a corresponding increase in cement reduces the concrete strength. Superplasticizers are the most typical way to increase workability. Air entrainment is used to improve durability.

Amorphous Materials

Amorphous materials such as glass are non-crystalline solids. Thermoplastic polymers are either semicrystalline or amorphous.

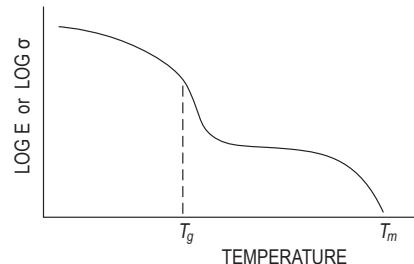
Below the glass transition temperature (T_g) the amorphous material will be a brittle solid.



The volume-temperature curve as shown above is often used to show the difference between amorphous and crystalline solids.

Polymers

Polymers are classified as thermoplastics that can be melted and reformed. Thermosets cannot be melted and reformed.



The above curve shows the temperature dependent strength (σ) or modulus (E) for a thermoplastic polymer.

Polymer Additives

Chemicals and compounds are added to polymers to improve properties for commercial use. These substances, such as plasticizers, improve formability during processing, while others increase strength or durability.

Examples of common additives are:

Plasticizers: vegetable oils, low molecular weight polymers or monomers

Fillers: talc, chopped glass fibers

Flame retardants: halogenated paraffins, zinc borate, chlorinated phosphates

Ultraviolet or visible light resistance: carbon black

Oxidation resistance: phenols, aldehydes

Thermal Properties

The thermal expansion coefficient is the ratio of engineering strain to the change in temperature.

$$\alpha = \frac{\epsilon}{\Delta T}$$

α = thermal expansion coefficient

ϵ = engineering strain

ΔT = change in temperature

Specific heat (also called heat capacity) is the amount of heat required to raise the temperature of something or an amount of something by 1 degree.

At constant pressure the amount of heat (Q) required to increase the temperature of something by ΔT is $C_p \Delta T$, where C_p is the constant pressure heat capacity.

At constant volume the amount of heat (Q) required to increase the temperature of something by ΔT is $C_v \Delta T$, where C_v is the constant volume heat capacity.

An object can have a heat capacity that would be expressed as energy/degree.

The heat capacity of a material can be reported as energy/degree per unit mass or per unit volume.

- ♦ Concrete Manual, 8th ed., U.S. Bureau of Reclamation, 1975.
- Merritt, Frederick S., Standard Handbook for Civil Engineers, 3rd ed., McGraw-Hill, 1983.

BINARY PHASE DIAGRAMS

Allows determination of (1) what phases are present at equilibrium at any temperature and average composition, (2) the compositions of those phases, and (3) the fractions of those phases.

Eutectic reaction (liquid \rightarrow two solid phases)

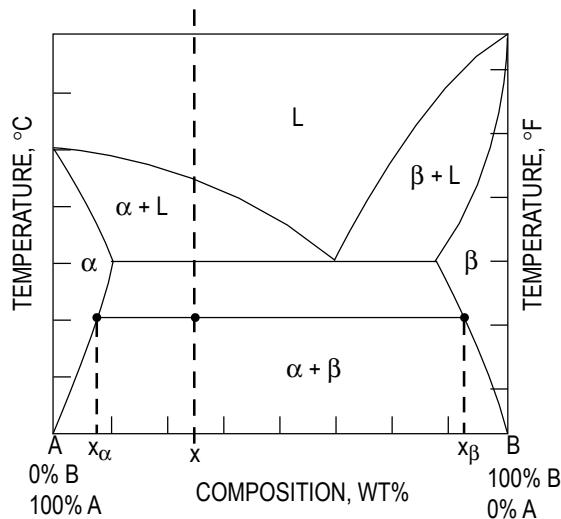
Eutectoid reaction (solid \rightarrow two solid phases)

Peritectic reaction (liquid + solid \rightarrow solid)

Peritectoid reaction (two solid phases \rightarrow solid)

Lever Rule

The following phase diagram and equations illustrate how the weight of each phase in a two-phase system can be determined:

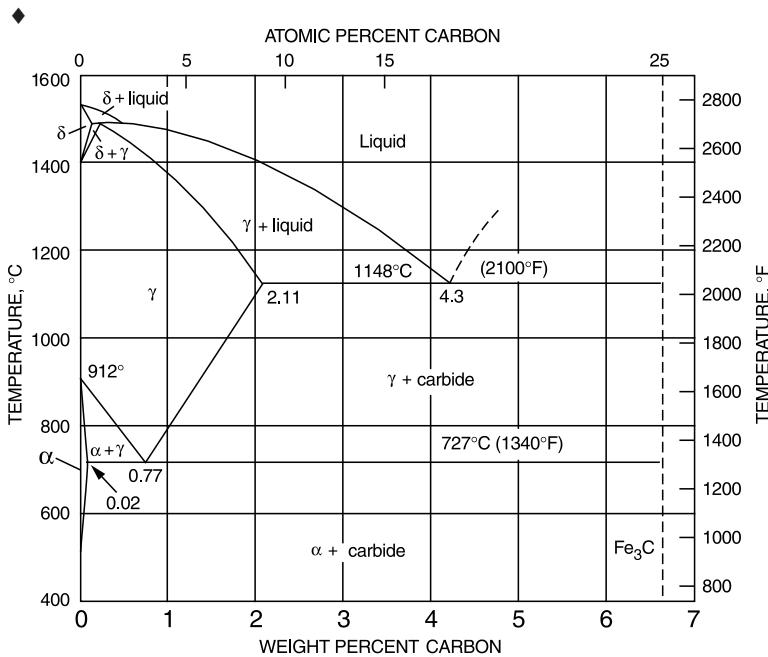


(In diagram, L = liquid.) If x = the average composition at temperature T, then

$$\text{wt\% } \alpha = \frac{x_{\beta} - x}{x_{\beta} - x_{\alpha}} \times 100$$

$$\text{wt\% } \beta = \frac{x - x_{\alpha}}{x_{\beta} - x_{\alpha}} \times 100$$

Iron-Iron Carbide Phase Diagram



♦ Van Vlack, L., *Elements of Materials Science & Engineering*, Addison-Wesley, Boston, 1989.

STATICS

FORCE

A *force* is a *vector* quantity. It is defined when its (1) magnitude, (2) point of application, and (3) direction are known.

The vector form of a force is

$$\mathbf{F} = F_x \mathbf{i} + F_y \mathbf{j}$$

RESULTANT (TWO DIMENSIONS)

The *resultant*, F , of n forces with components $F_{x,i}$ and $F_{y,i}$ has the magnitude of

$$F = \left[\left(\sum_{i=1}^n F_{x,i} \right)^2 + \left(\sum_{i=1}^n F_{y,i} \right)^2 \right]^{1/2}$$

The resultant direction with respect to the x -axis is

$$\theta = \arctan \left(\frac{\sum_{i=1}^n F_{y,i}}{\sum_{i=1}^n F_{x,i}} \right)$$

RESOLUTION OF A FORCE

$$\begin{aligned} F_x &= F \cos \theta_x; & F_y &= F \cos \theta_y; & F_z &= F \cos \theta_z \\ \cos \theta_x &= F_x/F; & \cos \theta_y &= F_y/F; & \cos \theta_z &= F_z/F \end{aligned}$$

Separating a force into components when the geometry of force is known and $R = \sqrt{x^2 + y^2 + z^2}$

$$F_x = (x/R)F; \quad F_y = (y/R)F; \quad F_z = (z/R)F$$

MOMENTS (COUPLES)

A system of two forces that are equal in magnitude, opposite in direction, and parallel to each other is called a *couple*. A *moment* \mathbf{M} is defined as the cross product of the *radius vector* \mathbf{r} and the *force* \mathbf{F} from a point to the line of action of the force.

$$\begin{aligned} \mathbf{M} &= \mathbf{r} \times \mathbf{F}; & M_x &= yF_z - zF_y, \\ & & M_y &= zF_x - xF_z, \text{ and} \\ & & M_z &= xF_y - yF_x. \end{aligned}$$

SYSTEMS OF FORCES

$$\begin{aligned} \mathbf{F} &= \sum \mathbf{F}_n \\ \mathbf{M} &= \sum (\mathbf{r}_n \times \mathbf{F}_n) \end{aligned}$$

Equilibrium Requirements

$$\begin{aligned} \sum \mathbf{F}_n &= 0 \\ \sum \mathbf{M}_n &= 0 \end{aligned}$$

CENTROIDS OF MASSES, AREAS, LENGTHS, AND VOLUMES

The following formulas are for discrete masses, areas, lengths, and volumes:

$$\mathbf{r}_c = \sum m_n \mathbf{r}_n / \sum m_n \text{ where}$$

m_n = the *mass* of each particle making up the system,

\mathbf{r}_n = the *radius vector* to each particle from a selected reference point, and

\mathbf{r}_c = the *radius vector* to the *centroid* of the total mass from the selected reference point.

The *moment of area* (M_a) is defined as

$$M_{ay} = \sum x_n a_n$$

$$M_{ax} = \sum y_n a_n$$

The *centroid of area* is defined as

$$x_{ac} = M_{ay}/A = \sum x_n a_n / A$$

$$y_{ac} = M_{ax}/A = \sum y_n a_n / A$$

where $A = \sum a_n$

MOMENT OF INERTIA

The *moment of inertia*, or the second moment of area, is defined as

$$I_y = \int x^2 dA$$

$$I_x = \int y^2 dA$$

The *polar moment of inertia* J of an area about a point is equal to the sum of the moments of inertia of the area about any two perpendicular axes in the area and passing through the same point.

$$\begin{aligned} I_z &= J = I_y + I_x = \int (x^2 + y^2) dA \\ &= r_p^2 A, \text{ where} \end{aligned}$$

r_p = the *radius of gyration* (as defined on the next page)

Moment of Inertia Parallel Axis Theorem

The moment of inertia of an area about any axis is defined as the moment of inertia of the area about a parallel centroidal axis plus a term equal to the area multiplied by the square of the perpendicular distance d from the centroidal axis to the axis in question.

$$I'_x = I_{x_c} + d_x^2 A$$

$$I'_y = I_{y_c} + d_y^2 A, \text{ where}$$

d_x, d_y = distance between the two axes in question,

I_{x_c}, I_{y_c} = the moment of inertia about the centroidal axis, and

I'_x, I'_y = the moment of inertia about the new axis.

Radius of Gyration

The *radius of gyration* r_p, r_x, r_y is the distance from a reference axis at which all of the area can be considered to be concentrated to produce the moment of inertia.

$$r_x = \sqrt{I_x/A}; \quad r_y = \sqrt{I_y/A}; \quad r_p = \sqrt{J/A}$$

Product of Inertia

The *product of inertia* (I_{xy} , etc.) is defined as:

$I_{xy} = \int xydA$, with respect to the xy -coordinate system,

The *parallel-axis theorem* also applies:

$I'_{xy} = I_{x_c y_c} + d_x d_y A$ for the xy -coordinate system, etc.

where

d_x = x -axis distance between the two axes in question, and

d_y = y -axis distance between the two axes in question.

FRICTION

The largest frictional force is called the *limiting friction*.

Any further increase in applied forces will cause motion.

$$F \leq \mu_s N, \text{ where}$$

F = friction force,

μ_s = coefficient of static friction, and

N = normal force between surfaces in contact.

SCREW THREAD

For a screw-jack, square thread,

$$M = Pr \tan(\alpha \pm \phi), \text{ where}$$

+ is for screw tightening,

- is for screw loosening,

M = external moment applied to axis of screw,

P = load on jack applied along and on the line of the axis,

r = the mean thread radius,

α = the *pitch angle* of the thread, and

$\mu = \tan \phi$ = the appropriate coefficient of friction.

BELT FRICTION

$$F_1 = F_2 e^{\mu \theta}, \text{ where}$$

F_1 = force being applied in the direction of impending motion,

F_2 = force applied to resist impending motion,

μ = coefficient of static friction, and

θ = the total *angle of contact* between the surfaces expressed in radians.

STATICALLY DETERMINATE TRUSS

Plane Truss: Method of Joints

The method consists of solving for the forces in the members by writing the two equilibrium equations for each joint of the truss.

$$\Sigma F = 0 \text{ and } \Sigma M = 0, \text{ where}$$

F = horizontal forces and member components and

F = vertical forces and member components.

Plane Truss: Method of Sections

The method consists of drawing a free-body diagram of a portion of the truss in such a way that the unknown truss member force is exposed as an external force.

CONCURRENT FORCES

A concurrent-force system is one in which the lines of action of the applied forces all meet at one point.

A *two-force* body in static equilibrium has two applied forces that are equal in magnitude, opposite in direction, and collinear.

Figure	Area & Centroid	Area Moment of Inertia	(Radius of Gyration) ²	Product of Inertia
	$A = bh/2$ $x_c = 2b/3$ $y_c = h/3$	$I_{x_c} = bh^3/36$ $I_{y_c} = b^3h/36$ $I_x = bh^3/12$ $I_y = b^3h/4$	$r_{x_c}^2 = h^2/18$ $r_{y_c}^2 = b^2/18$ $r_x^2 = h^2/6$ $r_y^2 = b^2/2$	$I_{x_c y_c} = Abh/36 = b^2h^2/72$ $I_{xy} = Abh/4 = b^2h^2/8$
	$A = bh/2$ $x_c = b/3$ $y_c = h/3$	$I_{x_c} = bh^3/36$ $I_{y_c} = b^3h/36$ $I_x = bh^3/12$ $I_y = b^3h/12$	$r_{x_c}^2 = h^2/18$ $r_{y_c}^2 = b^2/18$ $r_x^2 = h^2/6$ $r_y^2 = b^2/6$	$I_{x_c y_c} = -Abh/36 = -b^2h^2/72$ $I_{xy} = Abh/12 = b^2h^2/24$
	$A = bh/2$ $x_c = (a+b)/3$ $y_c = h/3$	$I_{x_c} = bh^3/36$ $I_{y_c} = [bh(b^2 - ab + a^2)]/36$ $I_x = bh^3/12$ $I_y = [bh(b^2 + ab + a^2)]/12$	$r_{x_c}^2 = h^2/18$ $r_{y_c}^2 = (b^2 - ab + a^2)/18$ $r_x^2 = h^2/6$ $r_y^2 = (b^2 + ab + a^2)/6$	$I_{x_c y_c} = [Ah(2a - b)]/36$ $= [bh^2(2a - b)]/72$ $I_{xy} = [Ah(2a + b)]/12$ $= [bh^2(2a + b)]/24$
	$A = bh$ $x_c = b/2$ $y_c = h/2$	$I_{x_c} = bh^3/12$ $I_{y_c} = b^3h/12$ $I_x = bh^3/3$ $I_y = b^3h/3$ $J = [bh(b^2 + h^2)]/12$	$r_{x_c}^2 = h^2/12$ $r_{y_c}^2 = b^2/12$ $r_x^2 = h^2/3$ $r_y^2 = b^2/3$ $r_p^2 = (b^2 + h^2)/12$	$I_{x_c y_c} = 0$ $I_{xy} = Abh/4 = b^2h^2/4$
	$A = h(a+b)/2$ $y_c = \frac{h(2a+b)}{3(a+b)}$	$I_{x_c} = \frac{h^3(a^2 + 4ab + b^2)}{36(a+b)}$ $I_x = \frac{h^3(3a+b)}{12}$	$r_{x_c}^2 = \frac{h^2(a^2 + 4ab + b^2)}{18(a+b)}$ $r_x^2 = \frac{h^2(3a+b)}{6(a+b)}$	
	$A = ab \sin \theta$ $x_c = (b + a \cos \theta)/2$ $y_c = (a \sin \theta)/2$	$I_{x_c} = (a^3 b \sin^3 \theta)/12$ $I_{y_c} = [ab \sin \theta(b^2 + a^2 \cos^2 \theta)]/12$ $I_x = (a^3 b \sin^3 \theta)/3$ $I_y = [ab \sin \theta(b + a \cos \theta)^2]/3$ $- (a^2 b^2 \sin \theta \cos \theta)/6$	$r_{x_c}^2 = (a \sin \theta)^2/12$ $r_{y_c}^2 = (b^2 + a^2 \cos^2 \theta)/12$ $r_x^2 = (a \sin \theta)^2/3$ $r_y^2 = (b + a \cos \theta)^2/3$ $- (ab \cos \theta)/6$	$I_{x_c y_c} = (a^3 b \sin^2 \theta \cos \theta)/12$

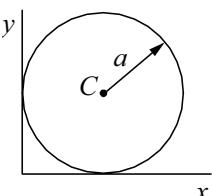
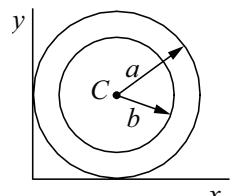
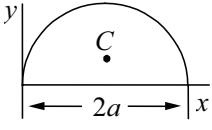
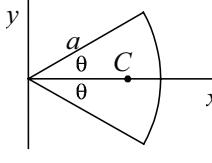
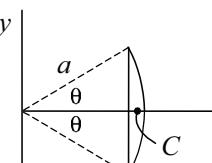
Figure	Area & Centroid	Area Moment of Inertia	(Radius of Gyration) ²	Product of Inertia
	$A = \pi a^2$ $x_c = a$ $y_c = a$	$I_{x_c} = I_{y_c} = \pi a^4 / 4$ $I_x = I_y = 5\pi a^4 / 4$ $J = \pi a^4 / 2$	$r_{x_c}^2 = r_{y_c}^2 = a^2 / 4$ $r_x^2 = r_y^2 = 5a^2 / 4$ $r_p^2 = a^2 / 2$	$I_{x_c y_c} = 0$ $I_{xy} = Aa^2$
	$A = \pi(a^2 - b^2)$ $x_c = a$ $y_c = a$	$I_{x_c} = I_{y_c} = \pi(a^4 - b^4) / 4$ $I_x = I_y = \frac{5\pi a^4}{4} - \pi a^2 b^2 - \frac{\pi b^4}{4}$ $J = \pi(a^4 - b^4) / 2$	$r_{x_c}^2 = r_{y_c}^2 = (a^2 + b^2) / 4$ $r_x^2 = r_y^2 = (5a^2 + b^2) / 4$ $r_p^2 = (a^2 + b^2) / 2$	$I_{x_c y_c} = 0$ $I_{xy} = Ad^2$ $= \pi a^2 (a^2 - b^2)$
	$A = \pi a^2 / 2$ $x_c = a$ $y_c = 4a/(3\pi)$	$I_{x_c} = \frac{a^4(9\pi^2 - 64)}{72\pi}$ $I_{y_c} = \pi a^4 / 8$ $I_x = \pi a^4 / 8$ $I_y = 5\pi a^4 / 8$	$r_{x_c}^2 = \frac{a^2(9\pi^2 - 64)}{36\pi^2}$ $r_{y_c}^2 = a^2 / 4$ $r_x^2 = a^2 / 4$ $r_y^2 = 5a^2 / 4$	$I_{x_c y_c} = 0$ $I_{xy} = 2a^4 / 3$
 CIRCULAR SECTOR	$A = a^2 \theta$ $x_c = \frac{2a \sin \theta}{3 - \theta}$ $y_c = 0$	$I_x = a^4(\theta - \sin \theta \cos \theta) / 4$ $I_y = a^4(\theta + \sin \theta \cos \theta) / 4$	$r_x^2 = \frac{a^2}{4} \frac{(\theta - \sin \theta \cos \theta)}{\theta}$ $r_y^2 = \frac{a^2}{4} \frac{(\theta + \sin \theta \cos \theta)}{\theta}$	$I_{x_c y_c} = 0$ $I_{xy} = 0$
 CIRCULAR SEGMENT	$A = a^2 \left[\theta - \frac{\sin 2\theta}{2} \right]$ $x_c = \frac{2a}{3} \frac{\sin^3 \theta}{\theta - \sin \theta \cos \theta}$ $y_c = 0$	$I_x = \frac{Aa^2}{4} \left[1 - \frac{2\sin^3 \theta \cos \theta}{3\theta - 3\sin \theta \cos \theta} \right]$ $I_y = \frac{Aa^2}{4} \left[1 + \frac{2\sin^3 \theta \cos \theta}{\theta - \sin \theta \cos \theta} \right]$	$r_x^2 = \frac{a^2}{4} \left[1 - \frac{2\sin^3 \theta \cos \theta}{3\theta - 3\sin \theta \cos \theta} \right]$ $r_y^2 = \frac{a^2}{4} \left[1 + \frac{2\sin^3 \theta \cos \theta}{\theta - \sin \theta \cos \theta} \right]$	$I_{x_c y_c} = 0$ $I_{xy} = 0$

Figure	Area & Centroid	Area Moment of Inertia	(Radius of Gyration) ²	Product of Inertia
 PARABOLA	$A = 4ab/3$ $x_c = 3a/5$ $y_c = 0$	$I_{x_c} = I_x = 4ab^3/15$ $I_{y_c} = 16a^3b/175$ $I_y = 4a^3b/7$	$r_{x_c}^2 = r_x^2 = b^2/5$ $r_{y_c}^2 = 12a^2/175$ $r_y^2 = 3a^2/7$	$I_{x_c y_c} = 0$ $I_{xy} = 0$
 HALF A PARABOLA	$A = 2ab/3$ $x_c = 3a/5$ $y_c = 3b/8$	$I_x = 2ab^3/15$ $I_y = 2ba^3/7$	$r_x^2 = b^2/5$ $r_y^2 = 3a^2/7$	$I_{xy} = Aab/4 = a^2b^2$
 n^{th} DEGREE PARABOLA	$A = bh/(n+1)$ $x_c = \frac{n+1}{n+2}b$ $y_c = \frac{h}{2} \frac{n+1}{2n+1}$	$I_x = \frac{bh^3}{3(3n+1)}$ $I_y = \frac{hb^3}{n+3}$	$r_x^2 = \frac{h^2(n+1)}{3(3n+1)}$ $r_y^2 = \frac{n+1}{n+3}b^2$	
 n^{th} DEGREE PARABOLA	$A = \frac{n}{n+1}bh$ $x_c = \frac{n+1}{2n+1}b$ $y_c = \frac{n+1}{2(n+2)}h$	$I_x = \frac{n}{3(n+3)}bh^3$ $I_y = \frac{n}{3n+1}b^3h$	$r_x^2 = \frac{n+1}{3(n+1)}h^2$ $r_y^2 = \frac{n+1}{3n+1}b^2$	

Housner, George W., and Donald E. Hudson, *Applied Mechanics Dynamics*, D. Van Nostrand Company, Inc., Princeton, NJ, 1959. Table reprinted by permission of G.W. Housner & D.E. Hudson.

DYNAMICS

COMMON NOMENCLATURE

t = time
 s = position
 v = velocity
 a = acceleration
 a_n = normal acceleration
 a_t = tangential acceleration
 θ = angle
 ω = angular velocity
 α = angular acceleration
 Ω = angular velocity of x,y,z reference axis
 $\dot{\Omega}$ = angular acceleration of reference axis
 $\mathbf{r}_{A/B}$ = relative position of "A" with respect to "B"
 $\mathbf{v}_{A/B}$ = relative velocity of "A" with respect to "B"
 $\mathbf{a}_{A/B}$ = relative acceleration of "A" with respect to "B"

PARTICLE KINEMATICS

Kinematics is the study of motion without consideration of the mass of, or the forces acting on, a system. For particle motion, let $\mathbf{r}(t)$ be the position vector of the particle in an inertial reference frame. The velocity and acceleration of the particle are defined, respectively, as

$$\mathbf{v} = d\mathbf{r}/dt$$

$$\mathbf{a} = d\mathbf{v}/dt, \text{ where}$$

\mathbf{v} = the instantaneous velocity

\mathbf{a} = the instantaneous acceleration

t = time

Cartesian Coordinates

$$\mathbf{r} = x\mathbf{i} + y\mathbf{j} + z\mathbf{k}$$

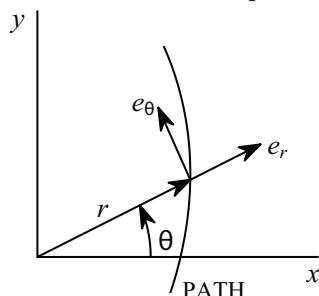
$$\mathbf{v} = \dot{x}\mathbf{i} + \dot{y}\mathbf{j} + \dot{z}\mathbf{k}$$

$$\mathbf{a} = \ddot{x}\mathbf{i} + \ddot{y}\mathbf{j} + \ddot{z}\mathbf{k}, \text{ where}$$

$$\dot{x} = dx/dt = v_x, \text{ etc.}$$

$$\ddot{x} = d^2x/dt^2 = a_x, \text{ etc.}$$

Radial and Transverse Components for Planar Motion



Unit vectors \mathbf{e}_θ and \mathbf{e}_r are, respectively, normal to and collinear with the position vector \mathbf{r} . Thus:

$$\mathbf{r} = r\mathbf{e}_r$$

$$\mathbf{v} = \dot{r}\mathbf{e}_r + r\dot{\theta}\mathbf{e}_\theta$$

$$\mathbf{a} = (\ddot{r} - r\dot{\theta}^2)\mathbf{e}_r + (r\ddot{\theta} + 2\dot{r}\dot{\theta})\mathbf{e}_\theta, \text{ where}$$

r = the radial distance

θ = the angle between the x axis and \mathbf{e}_r

$$\dot{r} = dr/dt, \text{ etc., } \ddot{r} = d^2r/dt^2, \text{ etc.}$$

♦ Particle Rectilinear Motion

<u>Variable a</u>	<u>Constant $a = a_c$</u>
--------------------------------	--------------------------------------

$$a = \frac{dv}{dt} \qquad v = v_0 + a_c t$$

$$v = \frac{ds}{dt} \qquad s = s_0 + v_0 t + \frac{1}{2} a_c t^2$$

$$a ds = v \, dv \qquad v^2 = v_0^2 + 2a_c(s - s_0)$$

♦ Particle Curvilinear Motion

<u>x,y,z Coordinates</u>	<u>r,θ,z Coordinates</u>
$v_x = \dot{x}$	$v_r = \dot{r}$
$v_y = \dot{y}$	$a_r = \ddot{r} - r\dot{\theta}^2$
$v_z = \dot{z}$	$v_\theta = r\dot{\theta}$
$a_x = \ddot{x}$	$a_\theta = r\ddot{\theta} + 2\dot{r}\dot{\theta}$
$a_y = \ddot{y}$	$v_z = \dot{z}$
$a_z = \ddot{z}$	$a_z = \ddot{z}$

n, t, b Coordinates

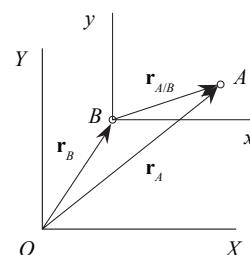
$$v = \dot{s} \quad \left| \begin{array}{l} a_t = \dot{v} = \frac{dv}{dt} \\ a_n = \frac{v^2}{\rho} \quad \rho = \frac{[1 + (dy/dx)^2]^{3/2}}{\left| \frac{d^2y}{dx^2} \right|} \end{array} \right.$$

♦ Relative Motion

$$\mathbf{r}_A = \mathbf{r}_B + \mathbf{r}_{A/B} \quad \mathbf{v}_A = \mathbf{v}_B + \mathbf{v}_{A/B} \quad \mathbf{a}_A = \mathbf{a}_B + \mathbf{a}_{A/B}$$

Translating Axes x-y

The equations that relate the absolute and relative position, velocity, and acceleration vectors of two particles A and B , in plane motion may be written as



$$\mathbf{r}_A = \mathbf{r}_B + \mathbf{r}_{A/B}$$

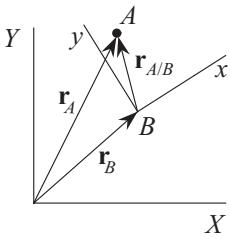
$$\mathbf{v}_A = \mathbf{v}_B + \boldsymbol{\omega} \times \mathbf{r}_{A/B} = \mathbf{v}_B + \mathbf{v}_{A/B}$$

$$\mathbf{a}_A = \mathbf{a}_B + \boldsymbol{\alpha} \times \mathbf{r}_{A/B} + \boldsymbol{\omega} \times (\boldsymbol{\omega} \times \mathbf{r}_{A/B}) = \mathbf{a}_B + \mathbf{a}_{A/B}$$

where $\boldsymbol{\omega}$ and $\boldsymbol{\alpha}$ are the absolute angular velocity and absolute angular acceleration of the relative position vector $\mathbf{r}_{A/B}$, respectively.

♦ Adapted from Hibbeler, R.C., *Engineering Mechanics*, 10th ed., Prentice Hall, 2003.

Rotating Axis



$$\mathbf{r}_A = \mathbf{r}_B + \mathbf{r}_{A/B}$$

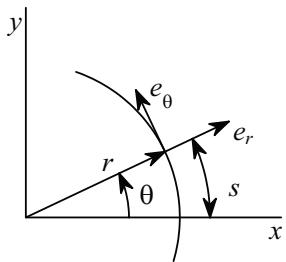
$$\mathbf{v}_A = \mathbf{v}_B + \dot{\Omega} \times \mathbf{r}_{A/B} + \mathbf{v}_{A/B}$$

$$\mathbf{a}_A = \mathbf{a}_B + \ddot{\Omega} \times \mathbf{r}_{A/B} + \dot{\Omega} \times (\Omega \times \mathbf{r}_{A/B}) + 2\Omega \times \mathbf{v}_{A/B} + \mathbf{a}_{A/B}$$

where ω and α are, respectively, the total angular velocity and acceleration of the relative position vector $\mathbf{r}_{A/B}$.

Plane Circular Motion

A special case of transverse and radial components is for constant radius rotation about the origin, or plane circular motion.



Here the vector quantities are defined as

$$\mathbf{r} = r\mathbf{e}_r$$

$$\mathbf{v} = r\omega\mathbf{e}_\theta$$

$$\mathbf{a} = (-r\omega^2)\mathbf{e}_r + r\alpha\mathbf{e}_\theta, \text{ where}$$

r = the radius of the circle

θ = the angle between the x and \mathbf{e}_r axes

The magnitudes of the angular velocity and acceleration, respectively, are defined as

$$\omega = \dot{\theta}$$

$$\alpha = \ddot{\omega} = \ddot{\theta}$$

Arc length, tangential velocity, and tangential acceleration, respectively, are

$$s = r\theta$$

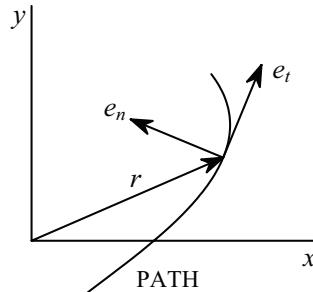
$$v_\theta = r\omega$$

$$a_\theta = r\alpha$$

The normal acceleration is given by

$$a_r = -r\omega^2 \text{ (towards the center of the circle)}$$

Normal and Tangential Components



Unit vectors \mathbf{e}_t and \mathbf{e}_n are, respectively, tangent and normal to the path with \mathbf{e}_n pointing to the center of curvature. Thus

$$\mathbf{v} = v(t)\mathbf{e}_t$$

$$\mathbf{a} = a(t)\mathbf{e}_t + (v_t^2/\rho)\mathbf{e}_n, \text{ where}$$

ρ = instantaneous radius of curvature

Constant Acceleration

The equations for the velocity and displacement when acceleration is a constant are given as

$$a(t) = a_0$$

$$v(t) = a_0(t - t_0) + v_0$$

$$s(t) = a_0(t - t_0)^2/2 + v_0(t - t_0) + s_0, \text{ where}$$

s = distance along the line of travel

s_0 = displacement at time t_0

v = velocity along the direction of travel

v_0 = velocity at time t_0

a_0 = constant acceleration

t = time

t_0 = some initial time

For a free-falling body, $a_0 = -g$ (downward).

An additional equation for velocity as a function of position may be written as

$$v^2 = v_0^2 + 2a_0(s - s_0)$$

For constant angular acceleration, the equations for angular velocity and displacement are

$$\alpha(t) = \alpha_0$$

$$\omega(t) = \alpha_0(t - t_0) + \omega_0$$

$$\theta(t) = \alpha_0(t - t_0)^2/2 + \omega_0(t - t_0) + \theta_0, \text{ where}$$

θ = angular displacement

θ_0 = angular displacement at time t_0

ω = angular velocity

ω_0 = angular velocity at time t_0

α_0 = constant angular acceleration

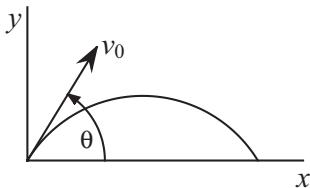
t = time

t_0 = some initial time

An additional equation for angular velocity as a function of angular position may be written as

$$\omega^2 = \omega_0^2 + 2\alpha_0(\theta - \theta_0)$$

Projectile Motion



The equations for common projectile motion may be obtained from the constant acceleration equations as

$$a_x = 0$$

$$v_x = v_0 \cos(\theta)$$

$$x = v_0 \cos(\theta)t + x_0$$

$$a_y = -g$$

$$v_y = -gt + v_0 \sin(\theta)$$

$$y = -gt^2/2 + v_0 \sin(\theta)t + y_0$$

Non-constant Acceleration

When non-constant acceleration, $a(t)$, is considered, the equations for the velocity and displacement may be obtained from

$$v(t) = \int_{t_0}^t a(\tau) d\tau + v_{t_0}$$

$$s(t) = \int_{t_0}^t v(\tau) d\tau + s_{t_0}$$

For variable angular acceleration

$$\omega(t) = \int_{t_0}^t \alpha(\tau) d\tau + \omega_{t_0}$$

$$\theta(t) = \int_{t_0}^t \omega(\tau) d\tau + \theta_{t_0}$$

where τ is the variable of integration

CONCEPT OF WEIGHT

$$W = mg, \text{ where}$$

$$W = \text{weight, N (lbf)}$$

$$m = \text{mass, kg (lbf-sec}^2/\text{ft)}$$

$$g = \text{local acceleration of gravity, m/s}^2 (\text{ft/sec}^2)$$

PARTICLE KINETICS

Newton's second law for a particle is

$$\Sigma F = d(mv)/dt, \text{ where}$$

ΣF = the sum of the applied forces acting on the particle

m = the mass of the particle

v = the velocity of the particle

For constant mass,

$$\Sigma F = m dv/dt = ma$$

One-Dimensional Motion of a Particle (Constant Mass)

When motion exists only in a single dimension then, without loss of generality, it may be assumed to be in the x direction, and

$$a_x = F_x/m, \text{ where}$$

F_x = the resultant of the applied forces, which in general can depend on t , x , and v_x .

If F_x only depends on t , then

$$a_x(t) = F_x(t)/m$$

$$v_x(t) = \int_{t_0}^t a_x(\tau) d\tau + v_{xt_0}$$

$$x(t) = \int_{t_0}^t v_x(\tau) d\tau + x_{t_0}$$

where τ is the variable of integration

If the force is constant (i.e., independent of time, displacement, and velocity) then

$$a_x = F_x/m$$

$$v_x = a_x(t - t_0) + v_{xt_0}$$

$$x = a_x(t - t_0)^2/2 + v_{xt_0}(t - t_0) + x_{t_0}$$

Normal and Tangential Kinetics for Planar Problems

When working with normal and tangential directions, the scalar equations may be written as

$$\Sigma F_t = ma_t = mdv_t/dt \text{ and}$$

$$\Sigma F_n = ma_n = m(v_t^2/\rho)$$

♦ Kinetic Energy

Particle	$T = \frac{1}{2}mv^2$
Rigid Body (Plane Motion)	$T = \frac{1}{2}mv_G^2 + \frac{1}{2}I_G\omega^2$

♦ Potential Energy

$$V = V_g + V_e, \text{ where } V_g = \pm Wy, V_e = +1/2 ks^2$$

The work done by an external agent in the presence of a conservative field is termed the change in potential energy.

Potential Energy in Gravity Field

$$V_g = mgh, \text{ where}$$

h = the elevation above some specified datum.

Elastic Potential Energy

For a linear elastic spring with modulus, stiffness, or spring constant, the force in the spring is

$$F_s = k s, \text{ where}$$

s = the change in length of the spring from the undeformed length of the spring.

In changing the deformation in the spring from position s_1 to s_2 , the change in the potential energy stored in the spring is

$$V_2 - V_1 = k(s_2^2 - s_1^2)/2$$

♦ Adapted from Hibbeler, R.C., *Engineering Mechanics*, 10th ed., Prentice Hall, 2003.

♦ Work

Work U is defined as

$$U = \int \mathbf{F} \cdot d\mathbf{r}$$

$$\text{Variable force } U_F = \int F \cos \theta \, ds$$

$$\text{Constant force } U_F = (F_c \cos \theta) \Delta s$$

$$\text{Weight } U_w = -W \Delta y$$

$$\text{Spring } U_s = -\left(\frac{1}{2} k s_2^2 - \frac{1}{2} k s_1^2\right)$$

where s_1 and s_2 are two different positions of the applied force end of the spring with $|s_2| > |s_1|$.

$$\text{Couple moment } U_M = M \Delta \theta$$

♦ Power and Efficiency

$$P = \frac{dU}{dt} = \mathbf{F} \cdot \mathbf{v} \quad \epsilon = \frac{P_{\text{out}}}{P_{\text{in}}} = \frac{U_{\text{out}}}{U_{\text{in}}}$$

Principle of Work and Energy

If T_i and V_i are, respectively, the kinetic and potential energy of a particle at state i , then for conservative systems (no energy dissipation or gain), the law of conservation of energy is

$$T_2 + V_2 = T_1 + V_1$$

If nonconservative forces are present, then the work done by these forces must be accounted for. Hence

$$T_2 + V_2 = T_1 + V_1 + U_{1 \rightarrow 2}, \text{ where}$$

$U_{1 \rightarrow 2}$ = the work done by the nonconservative forces in moving between state 1 and state 2. Care must be exercised during computations to correctly compute the algebraic sign of the work term. If the forces serve to increase the energy of the system, $U_{1 \rightarrow 2}$ is positive. If the forces, such as friction, serve to dissipate energy, $U_{1 \rightarrow 2}$ is negative.

Impulse and Momentum

Linear

Assuming constant mass, the equation of motion of a particle may be written as

$$md\mathbf{v}/dt = \mathbf{F}$$

$$md\mathbf{v} = \mathbf{F} dt$$

For a system of particles, by integrating and summing over the number of particles, this may be expanded to

$$\sum m_i (\mathbf{v}_i)_{t_2} = \sum m_i (\mathbf{v}_i)_{t_1} + \sum \int_{t_1}^{t_2} \mathbf{F}_i dt$$

The term on the left side of the equation is the linear momentum of a system of particles at time t_2 . The first term on the right side of the equation is the linear momentum of a system of particles at time t_1 . The second term on the right side of the equation is the impulse of the force \mathbf{F} from time t_1 to t_2 . It should be noted that the above equation is a vector equation. Component scalar equations may be obtained by considering the momentum and force in a set of orthogonal directions.

Angular Momentum or Moment of Momentum

The angular momentum or the moment of momentum about point 0 for a particle is defined as

$$\mathbf{H}_0 = \mathbf{r} \times m\mathbf{v}, \text{ or}$$

$$\mathbf{H}_0 = I_0 \omega$$

Taking the time derivative of the above, the equation of motion may be written as

$$\dot{\mathbf{H}}_0 = d(I_0 \omega)/dt = \mathbf{M}, \text{ where}$$

\mathbf{M} is the moment applied to the particle. Now by integrating and summing over a system of any number of particles, this may be expanded to

$$\Sigma (\mathbf{H}_{0i})_{t_2} = \Sigma (\mathbf{H}_{0i})_{t_1} + \sum \int_{t_1}^{t_2} \mathbf{M}_{0i} dt$$

The term on the left side of the equation is the angular momentum of a system of particles at time t_2 . The first term on the right side of the equation is the angular momentum of a system of particles at time t_1 . The second term on the right side of the equation is the angular impulse of the moment \mathbf{M} from time t_1 to t_2 .

Impact

During an impact, momentum is conserved while energy may or may not be conserved. For direct central impact with no external forces

$$m_1 \mathbf{v}_1 + m_2 \mathbf{v}_2 = m_1 \mathbf{v}'_1 + m_2 \mathbf{v}'_2, \text{ where}$$

m_1, m_2 = the masses of the two bodies

$\mathbf{v}_1, \mathbf{v}_2$ = the velocities of the bodies just before impact

$\mathbf{v}'_1, \mathbf{v}'_2$ = the velocities of the bodies just after impact

For impacts, the relative velocity expression is

$$e = \frac{(\mathbf{v}'_2)_n - (\mathbf{v}'_1)_n}{(\mathbf{v}_1)_n - (\mathbf{v}_2)_n}, \text{ where}$$

e = coefficient of restitution

$(\mathbf{v}_i)_n$ = the velocity normal to the plane of impact just **before** impact

$(\mathbf{v}'_i)_n$ = the velocity normal to the plane of impact just **after** impact

The value of e is such that

$0 \leq e \leq 1$, with limiting values

$e = 1$, perfectly elastic (energy conserved)

$e = 0$, perfectly plastic (no rebound)

Knowing the value of e , the velocities after the impact are given as

$$(\mathbf{v}'_1)_n = \frac{m_2 (\mathbf{v}_2)_n (1 + e) + (m_1 - em_2) (\mathbf{v}_1)_n}{m_1 + m_2}$$

$$(\mathbf{v}'_2)_n = \frac{m_1 (\mathbf{v}_1)_n (1 + e) - (em_1 - m_2) (\mathbf{v}_2)_n}{m_1 + m_2}$$

Friction

The Laws of Friction are

1. The total friction force F that can be developed is independent of the area of contact.
2. The total friction force F that can be developed is proportional to the normal force N .
3. For low velocities of sliding, the total frictional force that can be developed is practically independent of the velocity, although experiments show that the force F necessary to initiate slip is greater than that necessary to maintain the motion.

The formula expressing the Laws of Friction is

$$F \leq \mu N, \text{ where}$$

μ = the coefficient of friction.

In general

$$F < \mu_s N, \text{ no slip occurring}$$

$$F = \mu_s N, \text{ at the point of impending slip}$$

$$F = \mu_k N, \text{ when slip is occurring}$$

Here,

μ_s = the coefficient of static friction

μ_k = the coefficient of kinetic friction

PLANE MOTION OF A RIGID BODY

Kinematics of a Rigid Body

Rigid Body Rotation

For rigid body rotation θ

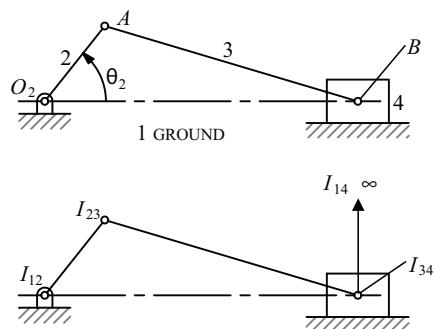
$$\omega = d\theta/dt$$

$$\alpha = d\omega/dt$$

$$\alpha d\theta = \omega d\omega$$

Instantaneous Center of Rotation (Instant Centers)

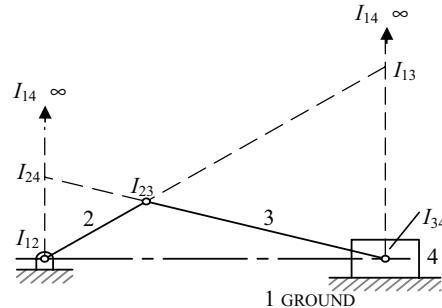
An instantaneous center of rotation (instant center) is a point, common to two bodies, at which each has the same velocity (magnitude and direction) at a given instant. It is also a point in space about which a body rotates, instantaneously.



The figure shows a fourbar slider-crank. Link 2 (the crank) rotates about the fixed center, O_2 . Link 3 couples the crank to the slider (link 4), which slides against ground (link 1). Using the definition of an instant center (IC), we see that the pins at O_2 , A , and B are ICs that are designated I_{12} , I_{23} , and I_{34} . The easily observable IC is I_{14} , which is located at infinity with its direction perpendicular to the interface between links 1 and 4 (the direction of sliding). To locate the remaining two ICs (for a fourbar) we must make use of Kennedy's rule.

Kennedy's Rule: When three bodies move relative to one another they have three instantaneous centers, all of which lie on the same straight line.

To apply this rule to the slider-crank mechanism, consider links 1, 2, and 3 whose ICs are I_{12} , I_{23} , and I_{13} , all of which lie on a straight line. Consider also links 1, 3, and 4 whose ICs are I_{13} , I_{34} , and I_{14} , all of which lie on a straight line. Extending the line through I_{12} and I_{23} and the line through I_{13} and I_{14} to their intersection locates I_{13} , which is common to the two groups of links that were considered.



Similarly, if body groups 1, 2, 4 and 2, 3, 4 are considered, a line drawn through known ICs I_{12} and I_{14} to the intersection of a line drawn through known ICs I_{23} and I_{34} locates I_{24} .

The number of ICs, c , for a given mechanism is related to the number of links, n , by

$$c = \frac{n(n - 1)}{2}$$

Kinetics of a Rigid Body

In general, Newton's second law for a rigid body, with constant mass and mass moment of inertia, in plane motion may be written in vector form as

$$\Sigma F = ma_c$$

$$\Sigma M_c = I_c \alpha$$

$$\Sigma M_p = I_c \alpha + \rho_{pc} \times ma_c, \text{ where}$$

F are forces and a_c is the acceleration of the body's mass center both in the plane of motion, M_c are moments and α is the angular acceleration both about an axis normal to the plane of motion, I_c is the mass moment of inertia about the normal axis through the mass center, and ρ_{pc} is a vector from point p to point c .

♦ **Mass Moment of Inertia** $I = \int r^2 dm$

Parallel-Axis Theorem $I = I_G + md^2$

$$\text{Radius of Gyration } k = \sqrt{\frac{I}{m}}$$

♦ Equations of Motion

<i>Rigid Body</i> <i>(Plane Motion)</i>	$\sum F_x = m(a_G)_x$ $\sum F_y = m(a_G)_y$ $\sum M_G = I_G \alpha \text{ or } \sum M_p = \Sigma (M_k)_p$
--	---

Mass Moment of Inertia

The definitions for the mass moments of inertia are

$$I_x = \int (y^2 + z^2) dm$$

$$I_y = \int (x^2 + z^2) dm$$

$$I_z = \int (x^2 + y^2) dm$$

A table listing moment of inertia formulas for some standard shapes is at the end of this section.

Parallel-Axis Theorem

The mass moments of inertia may be calculated about any axis through the application of the above definitions. However, once the moments of inertia have been determined about an axis passing through a body's mass center, it may be transformed to another parallel axis. The transformation equation is

$$I_{\text{new}} = I_c + md^2, \text{ where}$$

I_{new} = the mass moment of inertia about any specified axis

I_c = the mass moment of inertia about an axis that is parallel to the above specified axis but passes through the body's mass center

m = the mass of the body

d = the normal distance from the body's mass center to the above-specified axis

Mass Radius of Gyration

The mass radius of gyration is defined as

$$r_m = \sqrt{I/m}$$

Without loss of generality, the body may be assumed to be in the x - y plane. The scalar equations of motion may then be written as

$$\sum F_x = ma_{xc}$$

$$\sum F_y = ma_{yc}$$

$$\sum M_{zc} = I_{zc} \alpha, \text{ where}$$

zc indicates the z axis passing through the body's mass center, a_{xc} and a_{yc} are the acceleration of the body's mass center in the x and y directions, respectively, and α is the angular acceleration of the body about the z axis.

Rotation about an Arbitrary Fixed Axis

♦ Rigid Body Motion About a Fixed Axis

<i>Variable α</i> $\alpha = \frac{d\omega}{dt}$ $\omega = \frac{d\theta}{dt}$ $\omega d\omega = \alpha d\theta$	<i>Constant $\alpha = \alpha_c$</i> $\omega = \omega_0 + \alpha_c t$ $\theta = \theta_0 + \omega_0 t + \frac{1}{2} \alpha_c t^2$ $\omega^2 = \omega_0^2 + 2\alpha_c (\theta - \theta_0)$
--	--

For rotation about some arbitrary fixed axis q

$$\sum M_q = I_q \alpha$$

If the applied moment acting about the fixed axis is constant then integrating with respect to time, from $t = 0$ yields

$\alpha = M_q/I_q$ $\omega = \omega_0 + \alpha t$ $\theta = \theta_0 + \omega_0 t + \alpha t^2/2$

where ω_0 and θ_0 are the values of angular velocity and angular displacement at time $t = 0$, respectively.

The change in kinetic energy is the work done in accelerating the rigid body from ω_0 to ω

$$I_q \omega^2/2 = I_q \omega_0^2/2 + \int_{\theta_0}^{\theta} M_q d\theta$$

Kinetic Energy

In general the kinetic energy for a rigid body may be written as

$$T = mv^2/2 + I_c \omega^2/2$$

For motion in the xy plane this reduces to

$$T = m(v_{cx}^2 + v_{cy}^2)/2 + I_c \omega_z^2/2$$

For motion about an instant center,

$$T = I_{IC} \omega^2/2$$

♦ Principle of Angular Impulse and Momentum

<i>Rigid Body</i> <i>(Plane Motion)</i>	$(\mathbf{H}_G)_1 + \sum \int \mathbf{M}_G dt = (\mathbf{H}_G)_2$ where $\mathbf{H}_G = I_G \boldsymbol{\omega}$ $(\mathbf{H}_O)_1 + \sum \int \mathbf{M}_O dt = (\mathbf{H}_O)_2$ where $\mathbf{H}_O = I_O \boldsymbol{\omega}$
--	--

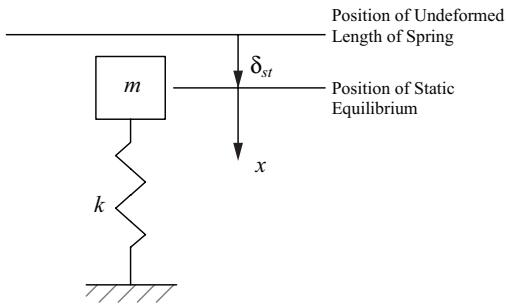
♦ Conservation of Angular Momentum

$$\Sigma(\text{syst. } \mathbf{H})_1 = \Sigma(\text{syst. } \mathbf{H})_2$$

♦ Adapted from Hibbeler, R.C., *Engineering Mechanics*, 10th ed., Prentice Hall, 2003.

Free Vibration

The figure illustrates a single degree-of-freedom system.



The equation of motion may be expressed as

$$m\ddot{x} = mg - k(x + \delta_{st})$$

where m is mass of the system, k is the spring constant of the system, δ_{st} is the static deflection of the system, and x is the displacement of the system from static equilibrium.

From statics it may be shown that

$$mg = k\delta_{st}$$

thus the equation of motion may be written as

$$m\ddot{x} + kx = 0, \text{ or}$$

$$\ddot{x} + (k/m)x = 0$$

The solution of this differential equation is

$$x(t) = C_1 \cos(\omega_n t) + C_2 \sin(\omega_n t)$$

where $\omega_n = \sqrt{k/m}$ is the undamped natural circular frequency and C_1 and C_2 are constants of integration whose values are determined from the initial conditions.

If the initial conditions are denoted as $x(0) = x_0$ and $\dot{x}(0) = v_0$, then

$$x(t) = x_0 \cos(\omega_n t) + (v_0/\omega_n) \sin(\omega_n t)$$

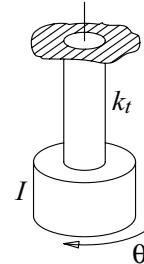
It may also be shown that the undamped natural frequency may be expressed in terms of the static deflection of the system as

$$\omega_n = \sqrt{g/\delta_{st}}$$

The undamped natural period of vibration may now be written as

$$\tau_n = 2\pi/\omega_n = \frac{2\pi}{\sqrt{\frac{k}{m}}} = \frac{2\pi}{\sqrt{\frac{g}{\delta_{st}}}}$$

Torsional Vibration



For torsional free vibrations it may be shown that the differential equation of motion is

$$\ddot{\theta} + (k_t/I)\theta = 0, \text{ where}$$

θ = the angular displacement of the system

k_t = the torsional stiffness of the massless rod

I = the mass moment of inertia of the end mass

The solution may now be written in terms of the initial conditions $\theta(0) = \theta_0$ and $\dot{\theta}(0) = \dot{\theta}_0$ as

$$\theta(t) = \theta_0 \cos(\omega_n t) + (\dot{\theta}_0/\omega_n) \sin(\omega_n t)$$

where the undamped natural circular frequency is given by

$$\omega_n = \sqrt{k_t/I}$$

The torsional stiffness of a solid round rod with associated polar moment-of-inertia J , length L , and shear modulus of elasticity G is given by

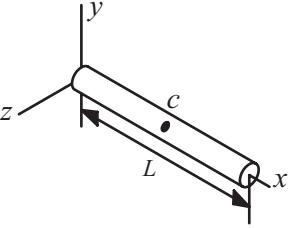
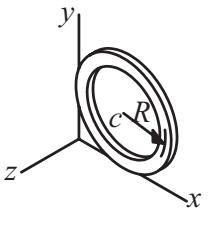
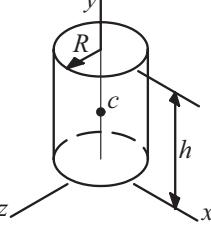
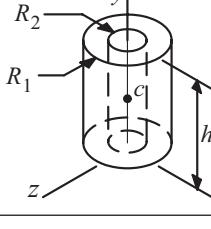
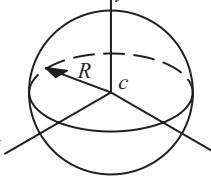
$$k_t = GJ/L$$

Thus the undamped circular natural frequency for a system with a solid round supporting rod may be written as

$$\omega_n = \sqrt{GJ/IL}$$

Similar to the linear vibration problem, the undamped natural period may be written as

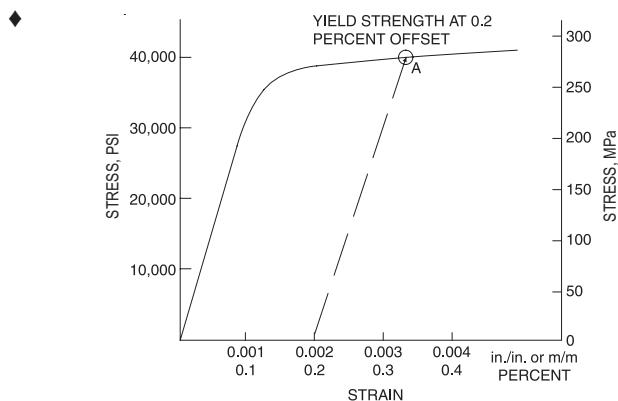
$$\tau_n = 2\pi/\omega_n = \frac{2\pi}{\sqrt{\frac{k_t}{I}}} = \frac{2\pi}{\sqrt{\frac{GJ}{IL}}}$$

Figure	Mass & Centroid	Mass Moment of Inertia	(Radius of Gyration) ²	Product of Inertia
	$M = \rho L A$ $x_c = L/2$ $y_c = 0$ $z_c = 0$ $A = \text{cross-sectional area of rod}$ $\rho = \text{mass/vol.}$	$I_x = I_{x_c} = 0$ $I_{y_c} = I_{z_c} = ML^2/12$ $I_y = I_z = ML^2/3$	$r_x^2 = r_{x_c}^2 = 0$ $r_{y_c}^2 = r_{z_c}^2 = L^2/12$ $r_y^2 = r_z^2 = L^2/3$	$I_{x_c y_c}, \text{ etc.} = 0$ $I_{xy}, \text{ etc.} = 0$
	$M = 2\pi R \rho A$ $x_c = R = \text{mean radius}$ $y_c = R = \text{mean radius}$ $z_c = 0$ $A = \text{cross-sectional area of ring}$ $\rho = \text{mass/vol.}$	$I_{x_c} = I_{y_c} = MR^2/2$ $I_{z_c} = MR^2$ $I_x = I_y = 3MR^2/2$ $I_z = 3MR^2$	$r_{x_c}^2 = r_{y_c}^2 = R^2/2$ $r_{z_c}^2 = R^2$ $r_x^2 = r_y^2 = 3R^2/2$ $r_z^2 = 3R^2$	$I_{x_c y_c}, \text{ etc.} = 0$ $I_{z_c z_c} = MR^2$ $I_{xz} = I_{yz} = 0$
	$M = \pi R^2 \rho h$ $x_c = 0$ $y_c = h/2$ $z_c = 0$ $\rho = \text{mass/vol.}$	$I_{x_c} = I_{z_c} = M(3R^2 + h^2)/12$ $I_{y_c} = I_y = MR^2/2$ $I_x = I_z = M(3R^2 + 4h^2)/12$	$r_{x_c}^2 = r_{z_c}^2 = (3R^2 + h^2)/12$ $r_{y_c}^2 = r_y^2 = R^2/2$ $r_x^2 = r_z^2 = (3R^2 + 4h^2)/12$	$I_{x_c y_c}, \text{ etc.} = 0$ $I_{xy}, \text{ etc.} = 0$
	$M = \pi(R_1^2 - R_2^2)\rho h$ $x_c = 0$ $y_c = h/2$ $z_c = 0$ $\rho = \text{mass/vol.}$	$I_{x_c} = I_{z_c} = M(3R_1^2 + 3R_2^2 + h^2)/12$ $I_{y_c} = I_y = M(R_1^2 + R_2^2)/2$ $I_x = I_z = M(3R_1^2 + 3R_2^2 + 4h^2)/12$	$r_{x_c}^2 = r_{z_c}^2 = (3R_1^2 + 3R_2^2 + h^2)/12$ $r_{y_c}^2 = r_y^2 = (R_1^2 + R_2^2)/2$ $r_x^2 = r_z^2 = (3R_1^2 + 3R_2^2 + 4h^2)/12$	$I_{x_c y_c}, \text{ etc.} = 0$ $I_{xy}, \text{ etc.} = 0$
	$M = \frac{4}{3}\pi R^3 \rho$ $x_c = 0$ $y_c = 0$ $z_c = 0$ $\rho = \text{mass/vol.}$	$I_{x_c} = I_x = 2MR^2/5$ $I_{y_c} = I_y = 2MR^2/5$ $I_{z_c} = I_z = 2MR^2/5$	$r_{x_c}^2 = r_x^2 = 2R^2/5$ $r_{y_c}^2 = r_y^2 = 2R^2/5$ $r_{z_c}^2 = r_z^2 = 2R^2/5$	$I_{x_c y_c}, \text{ etc.} = 0$

MECHANICS OF MATERIALS

UNIAXIAL STRESS-STRAIN

Stress-Strain Curve for Mild Steel



The slope of the linear portion of the curve equals the modulus of elasticity.

DEFINITIONS

Engineering Strain

$$\epsilon = \Delta L/L_o, \text{ where}$$

ϵ = engineering strain (units per unit)

ΔL = change in length (units) of member

L_o = original length (units) of member

Percent Elongation

$$\% \text{ Elongation} = \left(\frac{\Delta L}{L_o} \right) \times 100$$

Percent Reduction in Area (RA)

The % reduction in area from initial area, A_i , to final area, A_f , is:

$$\% RA = \left(\frac{A_i - A_f}{A_i} \right) \times 100$$

Shear Stress-Strain

$$\gamma = \tau/G, \text{ where}$$

γ = shear strain

τ = shear stress

G = shear modulus (constant in linear torsion-rotation relationship)

$$G = \frac{E}{2(1 + \nu)}, \text{ where}$$

E = modulus of elasticity (Young's modulus)

ν = Poisson's ratio

= $-(\text{lateral strain})/(\text{longitudinal strain})$

Uniaxial Loading and Deformation

$$\sigma = P/A, \text{ where}$$

σ = stress on the cross section

P = loading

A = cross-sectional area

$$\epsilon = \delta/L, \text{ where}$$

δ = elastic longitudinal deformation

L = length of member

$$E = \sigma/\epsilon = \frac{P/A}{\delta/L}$$

$$\delta = \frac{PL}{AE}$$

True stress is load divided by actual cross-sectional area whereas engineering stress is load divided by the initial area.

THERMAL DEFORMATIONS

$$\delta_t = \alpha L(T - T_o), \text{ where}$$

δ_t = deformation caused by a change in temperature

α = temperature coefficient of expansion

L = length of member

T = final temperature

T_o = initial temperature

CYLINDRICAL PRESSURE VESSEL

Cylindrical Pressure Vessel

For internal pressure only, the stresses at the inside wall are:

$$\sigma_t = P_i \frac{r_o^2 + r_i^2}{r_o^2 - r_i^2} \quad \text{and} \quad \sigma_r = -P_i$$

For external pressure only, the stresses at the outside wall are:

$$\sigma_t = -P_o \frac{r_o^2 + r_i^2}{r_o^2 - r_i^2} \quad \text{and} \quad \sigma_r = -P_o, \text{ where}$$

σ_t = tangential (hoop) stress

σ_r = radial stress

P_i = internal pressure

P_o = external pressure

r_i = inside radius

r_o = outside radius

For vessels with end caps, the axial stress is:

$$\sigma_a = P_i \frac{r_i^2}{r_o^2 - r_i^2}$$

σ_t , σ_r , and σ_a are principal stresses.

◆ Flinn, Richard A., and Paul K. Trojan, *Engineering Materials & Their Applications*, 4th ed., Houghton Mifflin Co., Boston, 1990.

When the thickness of the cylinder wall is about one-tenth or less of inside radius, the cylinder can be considered as thin-walled. In which case, the internal pressure is resisted by the hoop stress and the axial stress.

$$\sigma_t = \frac{P_i r}{t} \quad \text{and} \quad \sigma_a = \frac{P_i r}{2t}$$

where t = wall thickness and $r = \frac{r_i + r_o}{2}$.

STRESS AND STRAIN

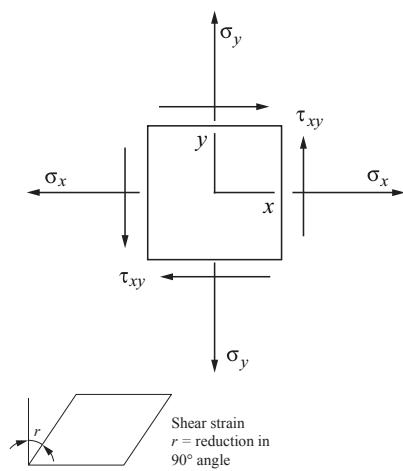
Principal Stresses

For the special case of a *two-dimensional* stress state, the equations for principal stress reduce to

$$\sigma_a, \sigma_b = \frac{\sigma_x + \sigma_y}{2} \pm \sqrt{\left(\frac{\sigma_x - \sigma_y}{2}\right)^2 + \tau_{xy}^2}$$

$$\sigma_c = 0$$

The two nonzero values calculated from this equation are temporarily labeled σ_a and σ_b and the third value σ_c is always zero in this case. Depending on their values, the three roots are then labeled according to the convention:
algebraically largest = σ_1 , *algebraically smallest* = σ_3 ,
other = σ_2 . A typical 2D stress element is shown below with all indicated components shown in their positive sense.



Mohr's Circle – Stress, 2D

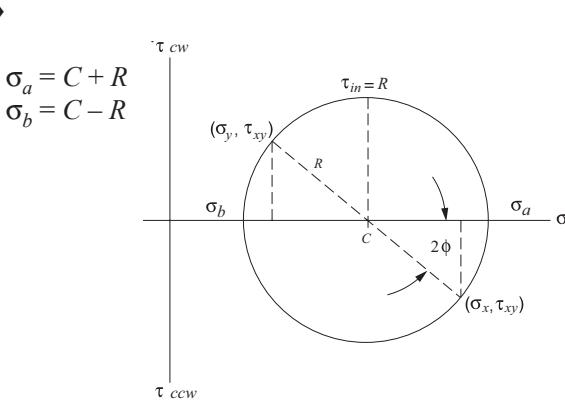
To construct a Mohr's circle, the following sign conventions are used.

1. Tensile normal stress components are plotted on the horizontal axis and are considered positive. Compressive normal stress components are negative.
2. For constructing Mohr's circle only, shearing stresses are plotted above the normal stress axis when the pair of shearing stresses, acting on opposite and parallel faces of an element, forms a clockwise couple. Shearing stresses are plotted below the normal axis when the shear stresses form a counterclockwise couple.

The circle drawn with the center on the normal stress (horizontal) axis with center, C , and radius, R , where

$$C = \frac{\sigma_x + \sigma_y}{2}, \quad R = \sqrt{\left(\frac{\sigma_x - \sigma_y}{2}\right)^2 + \tau_{xy}^2}$$

The two nonzero principal stresses are then:



The maximum *inplane* shear stress is $\tau_{in} = R$. However, the maximum shear stress considering three dimensions is always

$$\tau_{max} = \frac{\sigma_1 - \sigma_3}{2}.$$

Hooke's Law

Three-dimensional case:

$$\begin{aligned} \varepsilon_x &= (1/E)[\sigma_x - v(\sigma_y + \sigma_z)] & \gamma_{xy} &= \tau_{xy}/G \\ \varepsilon_y &= (1/E)[\sigma_y - v(\sigma_z + \sigma_x)] & \gamma_{yz} &= \tau_{yz}/G \\ \varepsilon_z &= (1/E)[\sigma_z - v(\sigma_x + \sigma_y)] & \gamma_{zx} &= \tau_{zx}/G \end{aligned}$$

Plane stress case ($\sigma_z = 0$):

$$\begin{aligned} \varepsilon_x &= (1/E)(\sigma_x - v\sigma_y) & \begin{Bmatrix} \sigma_x \\ \sigma_y \\ \tau_{xy} \end{Bmatrix} &= \frac{E}{1-v^2} \begin{Bmatrix} 1 & v & 0 \\ v & 1 & 0 \\ 0 & 0 & \frac{1-v}{2} \end{Bmatrix} \begin{Bmatrix} \varepsilon_x \\ \varepsilon_y \\ \gamma_{xy} \end{Bmatrix} \end{aligned}$$

Uniaxial case ($\sigma_y = \sigma_z = 0$): $\sigma_x = E\varepsilon_x$ or $\sigma = E\varepsilon$, where $\varepsilon_x, \varepsilon_y, \varepsilon_z$ = normal strain

$\sigma_x, \sigma_y, \sigma_z$ = normal stress

$\gamma_{xy}, \gamma_{yz}, \gamma_{zx}$ = shear strain

$\tau_{xy}, \tau_{yz}, \tau_{zx}$ = shear stress

E = modulus of elasticity

G = shear modulus

v = Poisson's ratio

When there is a temperature change from an initial temperature T_i to a final temperature T_f , there are also thermally-induced normal strains. In this case, $\varepsilon_x, \varepsilon_y$, and ε_z require modification. Thus,

$$\varepsilon_x = \frac{1}{E}[\sigma_x - v(\sigma_y + \sigma_z)] + \alpha(T_f - T_i)$$

and similarly for ε_y and ε_z , where α = coefficient of thermal expansion (CTE).

◆ Crandall, S.H., and N.C. Dahl, *An Introduction to Mechanics of Solids*, McGraw-Hill, New York, 1959.

TORSION

Torsion stress in circular solid or thick-walled ($t > 0.1 r$) shafts:

$$\tau = \frac{Tr}{J}$$

where J = polar moment of inertia

TORSIONAL STRAIN

$$\gamma_{\phi z} = \lim_{\Delta z \rightarrow 0} r(\Delta\phi/\Delta z) = r(d\phi/dz)$$

The shear strain varies in direct proportion to the radius, from zero strain at the center to the greatest strain at the outside of the shaft. $d\phi/dz$ is the twist per unit length or the rate of twist.

$$\tau_{\phi z} = G\gamma_{\phi z} = Gr(d\phi/dz)$$

$$T = G(d\phi/dz) \int_A r^2 dA = GJ(d\phi/dz)$$

$$\phi = \int_0^L \frac{T}{GJ} dz = \frac{TL}{GJ}, \text{ where}$$

ϕ = total angle (radians) of twist

T = torque

L = length of shaft

T/ϕ gives the *twisting moment per radian of twist*. This is called the *torsional stiffness* and is often denoted by the symbol k or c .

For Hollow, Thin-Walled Shafts

$$\tau = \frac{T}{2A_m t}, \text{ where}$$

t = thickness of shaft wall

A_m = the area of a solid shaft of radius equal to the mean radius of the hollow shaft

BEAMS

Shearing Force and Bending Moment Sign Conventions

1. The bending moment is *positive* if it produces bending of the beam *concave upward* (compression in top fibers and tension in bottom fibers).
2. The shearing force is *positive* if the *right portion of the beam tends to shear downward with respect to the left*.



POSITIVE BENDING



NEGATIVE BENDING



POSITIVE SHEAR



NEGATIVE SHEAR



The relationship between the load (w), shear (V), and moment (M) equations are:

$$w(x) = -\frac{dV(x)}{dx}$$

$$V = \frac{dM(x)}{dx}$$

$$V_2 - V_1 = \int_{x_1}^{x_2} [-w(x)] dx$$

$$M_2 - M_1 = \int_{x_1}^{x_2} V(x) dx$$

Stresses in Beams

The normal stress in a beam due to bending:

$$\sigma_x = -My/I, \text{ where}$$

M = the moment at the section

I = the *moment of inertia* of the cross section

y = the distance from the neutral axis to the fiber location above or below the neutral axis

The maximum normal stresses in a beam due to bending:

$$\sigma_x = \pm Mc/I, \text{ where}$$

c = distance from the neutral axis to the outermost fiber of a symmetrical beam section.

$$\sigma_x = -Ms, \text{ where}$$

$s = I/c$: the elastic section modulus of the beam.

Transverse shear stress:

$$\tau_{xy} = VQ/(Ib), \text{ where}$$

V = shear force

$$Q = A'y', \text{ where}$$

A' = area above the layer (or plane) upon which the desired transverse shear stress acts

$$\bar{y}' = \text{distance from neutral axis to area centroid}$$

B = width or thickness or the cross-section

Transverse shear flow:

$$q = VQ/I$$

♦ Timoshenko, S., and Gleason H. MacCullough, *Elements of Strengths of Materials*, K. Van Nostrand Co./Wadsworth Publishing Co., 1949.

Deflection of Beams

Using $1/\rho = M/(EI)$,

$$EI \frac{d^2y}{dx^2} = M, \text{ differential equation of deflection curve}$$

$$EI \frac{d^3y}{dx^3} = dM(x)/dx = V$$

$$EI \frac{d^4y}{dx^4} = dV(x)/dx = -w$$

Determine the deflection curve equation by double integration (apply boundary conditions applicable to the deflection and/or slope).

$$EI (dy/dx) = \int M(x) dx$$

$$EIy = \int [\int M(x) dx] dx$$

The constants of integration can be determined from the physical geometry of the beam.

Composite Sections

The bending stresses in a beam composed of dissimilar materials (material 1 and material 2) where $E_1 > E_2$ are:

$$\sigma_1 = -nMy/I_T$$

$$\sigma_2 = -My/I_T, \text{ where}$$

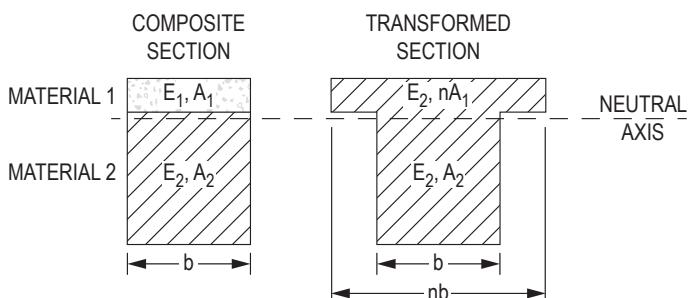
I_T = the moment of inertia of the transformed section

n = the modular ratio E_1/E_2

E_1 = elastic modulus of material 1

E_2 = elastic modulus of material 2

The composite section is transformed into a section composed of a single material. The centroid and then the moment of inertia are found on the *transformed section* for use in the bending stress equations.



COLUMNS

Critical axial load for long column subject to buckling:
Euler's Formula

$$P_{cr} = \frac{\pi^2 EI}{(K\ell)^2}, \text{ where}$$

ℓ = unbraced column length

K = effective-length factor to account for end supports

Theoretical effective-length factors for columns include:

Pinned-pinned, $K = 1.0$

Fixed-fixed, $K = 0.5$

Fixed-pinned, $K = 0.7$

Fixed-free, $K = 2.0$

Critical buckling stress for long columns:

$$\sigma_{cr} = \frac{P_{cr}}{A} = \frac{\pi^2 E}{(K\ell/r)^2}, \text{ where}$$

r = radius of gyration $\sqrt{I/A}$

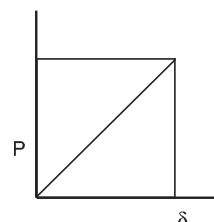
$K\ell/r$ = effective slenderness ratio for the column

ELASTIC STRAIN ENERGY

If the strain remains within the elastic limit, the work done during deflection (extension) of a member will be transformed into potential energy and can be recovered.

If the final load is P and the corresponding elongation of a tension member is δ , then the total energy U stored is equal to the work W done during loading.

$$U = W = P\delta/2$$



The strain energy per unit volume is

$$u = U/AL = \sigma^2/2E \quad (\text{for tension})$$

MATERIAL PROPERTIES

Table 1 - Typical Material Properties
 (Use these values if the specific alloy and temper are not listed on Table 2 below)

Material	Modulus of Elasticity, E [Mpsi (GPa)]	Modulus of Rigidity, G [Mpsi (GPa)]	Poisson's Ratio, ν	Coefficient of Thermal Expansion, α [$10^{-6}/^{\circ}\text{F}$ ($10^{-6}/^{\circ}\text{C}$)]	Density, ρ [lb/in ³ (Mg/m ³)]
Steel	29.0 (200.0)	11.5 (80.0)	0.30	6.5 (11.7)	0.282 (7.8)
Aluminum	10.0 (69.0)	3.8 (26.0)	0.33	13.1 (23.6)	0.098 (2.7)
Cast Iron	14.5 (100.0)	6.0 (41.4)	0.21	6.7 (12.1)	0.246–0.282 (6.8–7.8)
Wood (Fir)	1.6 (11.0)	0.6 (4.1)	0.33	1.7 (3.0)	—
Brass	14.8–18.1 (102–125)	5.8 (40)	0.33	10.4 (18.7)	0.303–0.313 (8.4–8.7)
Copper	17 (117)	6.5 (45)	0.36	9.3 (16.6)	0.322 (8.9)
Bronze	13.9–17.4 (96–120)	6.5 (45)	0.34	10.0 (18.0)	0.278–0.314 (7.7–8.7)
Magnesium	6.5 (45)	2.4 (16.5)	0.35	14 (25)	0.061 (1.7)
Glass	10.2 (70)	—	0.22	5.0 (9.0)	0.090 (2.5)
Polystyrene	0.3 (2)	—	0.34	38.9 (70.0)	0.038 (1.05)
Polyvinyl Chloride (PVC)	<0.6 (<4)	—	—	28.0 (50.4)	0.047 (1.3)
Alumina Fiber	58 (400)	—	—	—	0.141 (3.9)
Aramid Fiber	18.1 (125)	—	—	—	0.047 (1.3)
Boron Fiber	58 (400)	—	—	—	0.083 (2.3)
Beryllium Fiber	43.5 (300)	—	—	—	0.069 (1.9)
BeO Fiber	58 (400)	—	—	—	0.108 (3.0)
Carbon Fiber	101.5 (700)	—	—	—	0.083 (2.3)
Silicon Carbide Fiber	58 (400)	—	—	—	0.116 (3.2)

Table 2 - Average Mechanical Properties of Typical Engineering Materials
 (U.S. Customary Units)

(Use these values for the specific alloys and temperature listed. For all other materials refer to Table 1 above.)

Materials	Specific Weight γ (lb/in ³)	Modulus of Elasticity E (10 ³ ksi)	Modulus of Rigidity G (10 ³ ksi)	Yield Strength (ksi)			Ultimate Strength (ksi)			% Elongation in 2 in. specimen	Poisson's Ratio ν	Coef. of Therm. Expansion α (10^{-6}) $^{\circ}\text{F}$
				Tens.	σ_y	Comp.	Tens.	σ_u	Shear			
Metallic												
Aluminum Wrought Alloys	0.101 0.098	10.6 10.0	3.9 3.7	60 37	60 37	25 19	68 42	68 42	42 27	10 12	0.35 0.35	12.8 13.1
Cast Iron Alloys	0.260 0.263	10.0 25.0	3.9 9.8	— —	— —	— —	26 40	97 83	— —	0.6 5	0.28 0.28	6.70 6.60
Copper Alloys	0.316 0.319	14.6 15.0	5.4 5.6	11.4 50	11.4 50	— —	35 95	35 95	— —	35 20	0.35 0.34	9.80 9.60
Magnesium Alloy	0.066	6.48	2.5	22	22	—	40	40	22	1	0.30	14.3
Steel Alloys	0.284 0.284 0.295	29.0 28.0 29.0	11.0 11.0 11.0	36 30 102	36 30 102	— — —	58 75 116	58 75 116	— — —	30 40 22	0.32 0.27 0.32	6.60 9.60 6.50
Titanium Alloy	0.160	17.4	6.4	134	134	—	145	145	—	16	0.36	5.20
Nonmetallic												
Concrete	0.086 0.086	3.20 4.20	— —	— —	— —	1.8 5.5	— —	— —	— —	— —	0.15 0.15	6.0 6.0
Plastic Reinforced	0.0524 0.0524	19.0 10.5	— —	— —	— —	— —	104 13	70 19	10.2 —	2.8 —	0.34 0.34	— —
Wood Select Structural Grade	0.017 0.130	1.90 1.40	— —	— —	— —	— —	0.30 ^c 0.36 ^c	3.78 ^d 5.18 ^d	0.90 ^d 0.97 ^d	— —	0.29 ^c 0.31 ^c	— —

^a SPECIFIC VALUES MAY VARY FOR A PARTICULAR MATERIAL DUE TO ALLOY OR MINERAL COMPOSITION, MECHANICAL WORKING OF THE SPECIMEN, OR HEAT TREATMENT. FOR A MORE EXACT VALUE REFERENCE BOOKS FOR THE MATERIAL SHOULD BE CONSULTED.

^b THE YIELD AND ULTIMATE STRENGTHS FOR DUCTILE MATERIALS CAN BE ASSUMED EQUAL FOR BOTH TENSION AND COMPRESSION.

^c MEASURED PERPENDICULAR TO THE GRAIN.

^d MEASURED PARALLEL TO THE GRAIN.

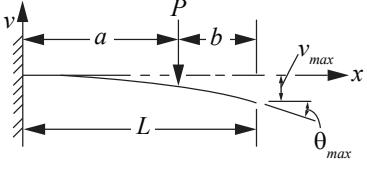
^e DEFORMATION MEASURED PERPENDICULAR TO THE GRAIN WHEN THE LOAD IS APPLIED ALONG THE GRAIN.

Simply Supported Beam Slopes and Deflections

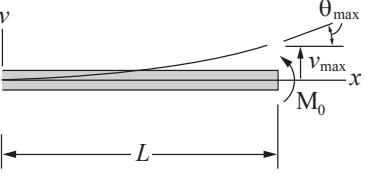
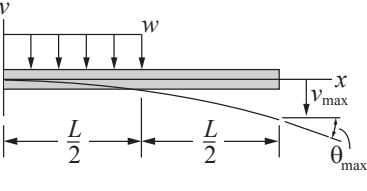
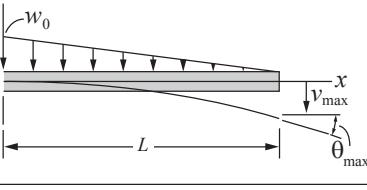
BEAM	SLOPE	DEFLECTION	ELASTIC CURVE
	$\theta_{\max} = \frac{-PL^2}{16EI}$	$v_{\max} = \frac{-PL^3}{48EI}$	$v = \frac{-Px}{48EI}(3L^2 - 4x^2)$ $0 \leq x \leq L/2$
	$\theta_1 = \frac{-Pab(L+b)}{6EIL}$ $\theta_2 = \frac{Pab(L+a)}{6EIL}$	$v _{x=a} = \frac{-Pba}{6EIL}(L^2 - b^2 - a^2)$	$v = \frac{-Pbx}{6EIL}(L^2 - b^2 - x^2)$ $0 \leq x \leq a$
	$\theta_1 = \frac{-M_0L}{3EI}$ $\theta_2 = \frac{M_0L}{6EI}$	$v_{\max} = \frac{-M_0L^2}{\sqrt{243}EI}$	$v = \frac{-M_0x}{6EI}(x^2 - 3Lx + 2L^2)$
	$\theta_{\max} = \frac{-wL^3}{24EI}$	$v_{\max} = \frac{-5wL^4}{384EI}$	$v = \frac{-wx}{24EI}(x^3 - 2Lx^2 + L^3)$
	$\theta_1 = \frac{-3wL^3}{128EI}$ $\theta_2 = \frac{7wL^3}{384EI}$	$v _{x=L/2} = \frac{-5wL^4}{768EI}$ $v_{\max} = -0.006563 \frac{wL^4}{EI}$ at $x = 0.4598L$	$v = \frac{-wx}{384EI}(16x^3 - 24Lx^2 + 9L^3)$ $0 \leq x \leq L/2$ $v = \frac{-wL}{384EI}(8x^3 - 24Lx^2 + 17L^2x - L^3)$ $L/2 \leq x < L$
	$\theta_1 = \frac{-7w_0L^3}{360EI}$ $\theta_2 = \frac{w_0L^3}{45EI}$	$v_{\max} = -0.00652 \frac{w_0L^4}{EI}$ at $x = 0.5193L$	$v = \frac{-w_0x}{360EI}(3x^4 - 10L^2x^2 + 7L^4)$

Adapted from Hibbeler, R.C., *Mechanics of Materials*, 4th ed., Prentice Hall, 2000, p. 800.

Cantilevered Beam Slopes and Deflections

BEAM	SLOPE	DEFLECTION	ELASTIC CURVE
	$\theta_{\max} = \frac{Pa^2}{2EI}$	$v_{\max} = \frac{Pa^2}{6EI} (3L - a)$	$v = \frac{Pa^2}{6EI} (3x - a)$, for $x > a$ $v = \frac{Px^2}{6EI} (-x + 3a)$, for $x \leq a$

Adapted from Crandall, S.H. and N.C. Dahl, *An Introduction to Mechanics of Solids*, McGraw-Hill, New York, 1959.

	$\theta_{\max} = \frac{M_0 L}{EI}$	$v_{\max} = \frac{M_0 L^2}{2EI}$	$v = \frac{M_0 x^2}{2EI}$
	$\theta_{\max} = \frac{-wL^3}{48EI}$	$v_{\max} = \frac{-7wL^4}{384EI}$	$v = \frac{-wx^2}{24EI} \left(x^2 - 2Lx + \frac{3}{2}L^2 \right)$ $L/2 \leq x \leq L$ $v = \frac{-wL^3}{192EI} (4x - L/2)$
	$\theta_{\max} = \frac{-w_0 L^3}{24EI}$	$v_{\max} = \frac{-w_0 L^4}{30EI}$	$v = \frac{-w_0 x^2}{120EI L} (10L^3 - 10L^2 x + 5Lx^2 - x^3)$

Adapted from Hibbeler, R.C., *Mechanics of Materials*, 4th ed., Prentice Hall, 2000, p. 801.

THERMODYNAMICS

PROPERTIES OF SINGLE-COMPONENT SYSTEMS

Nomenclature

1. Intensive properties are independent of mass.
2. Extensive properties are proportional to mass.
3. Specific properties are lowercase (extensive/mass).

State Functions (properties)

Absolute Pressure, P	(lbf/in ² or Pa)
Absolute Temperature, T	(°R or K)
Volume, V	(ft ³ or m ³)
Specific Volume, $v = V/m$	(ft ³ /lbm or m ³ /kg)
Internal Energy, U	(Btu or kJ)
Specific Internal Energy, $u = U/m$	(Btu/lbm or kJ/kg)
Enthalpy, H	(Btu or kJ)
Specific Enthalpy, $h = u + Pv = H/m$	(Btu/lbm or kJ/kg)
Entropy, S	(Btu/°R or kJ/K)
Specific Entropy, $s = S/m$	[Btu/(lbm·°R) or kJ/(kg·K)]
Gibbs Free Energy, $g = h - Ts$	(Btu/lbm or kJ/kg)
Helmholtz Free Energy, $a = u - Ts$	(Btu/lbm or kJ/kg)

For a single-phase pure component, specification of any two intensive, independent properties is sufficient to fix all the rest.

Heat Capacity at Constant Pressure,

$$c_p = \left(\frac{\partial h}{\partial T} \right)_P \quad [\text{Btu/(lbm·°R)} \text{ or } \text{kJ/(kg·K)}]$$

Heat Capacity at Constant Volume,

$$c_v = \left(\frac{\partial u}{\partial T} \right)_v \quad [\text{Btu/(lbm·°R)} \text{ or } \text{kJ/(kg·K)}]$$

The steam tables in this section provide T , P , v , u , h , and s data for saturated and superheated water.

A P - h diagram for refrigerant HFC-134a providing T , P , v , u , h , and s data in a graphical format is included in this section.

Thermal and physical property tables for selected gases, liquids, and solids are included in this section.

Properties for Two-Phase (vapor-liquid) Systems

Quality x (for liquid-vapor systems at saturation) is defined as the mass fraction of the vapor phase:

$$x = m_g / (m_g + m_f), \text{ where}$$

m_g = mass of vapor

m_f = mass of liquid

Specific volume of a two-phase system can be written:

$$v = xv_g + (1-x)v_f \text{ or } v = v_f + xv_{fg}, \text{ where}$$

v_f = specific volume of saturated liquid

v_g = specific volume of saturated vapor

v_{fg} = specific volume change upon vaporization

$$= v_g - v_f$$

Similar expressions exist for u , h , and s :

$$u = xu_g + (1-x)u_f \text{ or } u = u_f + xu_{fg}$$

$$h = xh_g + (1-x)h_f \text{ or } h = h_f + xh_{fg}$$

$$s = xs_g + (1-x)s_f \text{ or } s = s_f + xs_{fg}$$

PVT BEHAVIOR

Ideal Gas

For an ideal gas, $Pv = RT$ or $PV = mRT$, and

$$P_1v_1/T_1 = P_2v_2/T_2, \text{ where}$$

P = pressure

v = specific volume

m = mass of gas

R = gas constant

T = absolute temperature

V = volume

R is specific to each gas but can be found from

$$R = \frac{\bar{R}}{(\text{mol. wt})}, \text{ where}$$

\bar{R} = the universal gas constant

$$= 1,545 \text{ ft-lbf/(lbmol·°R)} = 8,314 \text{ J/(kmol·K)}$$

$$= 8.314 \text{ kPa·m}^3/(\text{kmol·K}) = 0.08206 \text{ L·atm}/(\text{mole·K})$$

For ideal gases, $c_p - c_v = R$

Ideal gas behavior is characterized by:

- no intermolecular interactions
- molecules occupy zero volume

The properties of an ideal gas reflect those of a single molecule and are attributable entirely to the structure of the molecule and the system T .

For ideal gases:

$$\left(\frac{\partial h}{\partial P} \right)_T = 0 \quad \left(\frac{\partial u}{\partial v} \right)_T = 0$$

For cold air standard, heat capacities are assumed to be constant at their room temperature values. In that case, the following are true:

$$\Delta u = c_p \Delta T; \quad \Delta h = c_p \Delta T$$

$$\Delta s = c_p \ln(T_2/T_1) - R \ln(P_2/P_1)$$

$$\Delta s = c_v \ln(T_2/T_1) + R \ln(v_2/v_1)$$

Also, for constant entropy processes:

$$\frac{P_2}{P_1} = \left(\frac{v_1}{v_2} \right)^k; \quad \frac{T_2}{T_1} = \left(\frac{P_2}{P_1} \right)^{\frac{k-1}{k}}$$

$$\frac{T_2}{T_1} = \left(\frac{v_1}{v_2} \right)^{\frac{k-1}{k}}, \text{ where } k = c_p/c_v$$

Ideal Gas Mixtures

$i = 1, 2, \dots, n$ constituents. Each constituent is an ideal gas.

Mole Fraction:

$$x_i = N_i/N; N = \sum N_i; \sum x_i = 1$$

where N_i = number of moles of component i

N = total moles in the mixture

Mass Fraction: $y_i = m_i/m; m = \sum m_i; \sum y_i = 1$

Molecular Weight: $M = m/N = \sum x_i M_i$

To convert *mole fractions* x_i to *mass fractions* y_i :

$$y_i = \frac{x_i M_i}{\sum (x_i M_i)}$$

To convert *mass fractions* to *mole fractions*:

$$x_i = \frac{y_i / M_i}{\sum (y_i / M_i)}$$

Partial Pressures: $P_i = \frac{m_i R_i T}{V}$ and $P = \sum P_i$

Partial Volumes: $V_i = \frac{m_i R_i T}{P}$ and $V = \sum V_i$

where P, V, T = the pressure, volume, and temperature of the mixture and $R_i = R/M_i$

Combining the above generates the following additional expressions for mole fraction.

$$x_i = P_i/P = V_i/V$$

Other Properties:

$$c_p = \sum (y_i c_{p_i})$$

$$c_v = \sum (y_i c_{v_i})$$

$$u = \sum (y_i u_i); h = \sum (y_i h_i); s = \sum (y_i s_i)$$

u_i and h_i are evaluated at T

s_i is evaluated at T and P_i

Real Gas

Most gases exhibit ideal gas behavior when the system pressure is less than 3 atm since the distance between molecules is large enough to produce negligible molecular interactions. The behavior of a real gas deviates from that of an ideal gas at higher pressures due to molecular interactions.

For a real gas, $Pv = ZRT$ where Z = compressibility factor.

$Z = 1$ for an ideal gas; $Z \neq 1$ for a real gas

Equations of State (EOS)

EOS are used to quantify PvT behavior

Ideal Gas EOS (applicable only to ideal gases)

$$P = \left(\frac{RT}{v} \right)$$

Generalized Compressibility EOS (applicable to all systems as gases, liquids, and/or solids)

$$P = \left(\frac{RT}{v} \right) Z$$

Virial EOS (applicable only to gases)

$$P = \left(\frac{RT}{v} \right) \left(1 + \frac{B}{v} + \frac{C}{v^2} + \dots \right) \text{ where } B, C, \dots$$

are virial coefficients obtained from PvT measurements or statistical mechanics.

Cubic EOS (theoretically motivated with intent to predict gas and liquid thermodynamic properties)

$$P = \frac{RT}{v - b} - \frac{a(T)}{(v + c_1 b)(v + c_2 b)}$$

where $a(T)$, b , and c_1 and c_2 are species specific.

An example of a cubic EOS is the Van der Waals equation with constants based on the critical point:

$$\left(P + \frac{a}{v^2} \right) (\bar{v} - b) = \bar{R}T$$

$$\text{where } a = \left(\frac{27}{64} \right) \left(\frac{\bar{R}^2 T_c^2}{P_c} \right), \quad b = \frac{\bar{R} T_c}{8 P_c}$$

where P_c and T_c are the pressure and temperature at the critical point, respectively, and \bar{v} is the molar specific volume.

EOS are used to predict:

- P, v , or T when two of the three are specified
- other thermodynamic properties based on analytic manipulation of the EOS
- mixture properties using appropriate mixing rules to create a pseudo-component that mimics the mixture properties

The Theorem of Corresponding States asserts that all normal fluids have the same value of Z at the same reduced temperature T_r and pressure P_r .

$$T_r = \frac{T}{T_c} \quad P_r = \frac{P}{P_c}$$

where T_c and P_c are the critical temperature and pressure, respectively, expressed in absolute units. This is captured in the Generalized Compressibility Factor chart.

FIRST LAW OF THERMODYNAMICS

The *First Law of Thermodynamics* is a statement of conservation of energy in a thermodynamic system. The net energy crossing the system boundary is equal to the change in energy inside the system.

Heat Q ($q = Q/m$) is *energy transferred* due to temperature difference and is considered positive if it is inward or added to the system.

Work W ($w = W/m$) is considered *positive if it is outward* or *work done* by the system.

Closed Thermodynamic System

No mass crosses system boundary

$$Q - W = \Delta U + \Delta KE + \Delta PE$$

where ΔU = change in internal energy

ΔKE = change in kinetic energy

ΔPE = change in potential energy

Energy can cross the boundary only in the form of heat or work. Work can be boundary work, w_b , or other work forms (electrical work, etc.)

Reversible boundary work is given by $w_b = \int P dv$.

Special Cases of Closed Systems (with no change in kinetic or potential energy)

Constant System Pressure process (**Charles' Law**):

$$w_b = P\Delta v$$

(ideal gas) $T/v = \text{constant}$

Constant Volume process:

$$w_b = 0$$

(ideal gas) $T/P = \text{constant}$

Isentropic process (ideal gas):

$$Pv^k = \text{constant}$$

$$w = (P_2v_2 - P_1v_1)/(1 - k)$$

$$= R(T_2 - T_1)/(1 - k)$$

Constant Temperature process (**Boyle's Law**):

(ideal gas) $Pv = \text{constant}$

$$w_b = RT \ln(v_2/v_1) = RT \ln(P_1/P_2)$$

Polytropic process (ideal gas):

$$Pv^n = \text{constant}$$

$$w = (P_2v_2 - P_1v_1)/(1 - n), n \neq 1$$

Open Thermodynamic System

Mass crosses the system boundary.

There is flow work (Pv) done by mass entering the system.

The reversible flow work is given by:

$$w_{\text{rev}} = - \int v dP + \Delta KE + \Delta PE$$

First Law applies whether or not processes are reversible.

Open System First Law (energy balance)

$$\begin{aligned} \sum \dot{m}_i [h_i + V_i^2/2 + gZ_i] - \sum \dot{m}_e [h_e + V_e^2/2 + gZ_e] \\ + \dot{Q}_{in} - \dot{W}_{net} = d(m_s u_s)/dt, \text{ where} \end{aligned}$$

\dot{W}_{net} = rate of net or shaft work

\dot{m} = mass flow rate (subscripts i and e refer to inlet and exit states of system)

g = acceleration of gravity

Z = elevation

V = velocity

m_s = mass of fluid within the system

u_s = specific internal energy of system

\dot{Q}_{in} = rate of heat transfer (neglecting kinetic and potential energy of the system)

Special Cases of Open Systems (with no change in kinetic or potential energy)

Constant Volume process:

$$w_{\text{rev}} = -v(P_2 - P_1)$$

Constant System Pressure process:

$$w_{\text{rev}} = 0$$

Constant Temperature process:

(ideal gas) $Pv = \text{constant}$

$$w_{\text{rev}} = RT \ln(v_2/v_1) = RT \ln(P_1/P_2)$$

Isentropic process (ideal gas):

$$Pv^k = \text{constant}$$

$$w_{\text{rev}} = k(P_2v_2 - P_1v_1)/(1 - k)$$

$$= kR(T_2 - T_1)/(1 - k)$$

$$w_{\text{rev}} = \frac{k}{k-1} RT_1 \left[1 - \left(\frac{P_2}{P_1} \right)^{(k-1)/k} \right]$$

Polytropic process (ideal gas):

$$Pv^n = \text{constant}$$

$$w_{\text{rev}} = n(P_2v_2 - P_1v_1)/(1 - n)$$

Steady-Flow Systems

The system does not change state with time. This assumption is valid for steady operation of turbines, pumps, compressors, throttling valves, nozzles, and heat exchangers, including boilers and condensers.

$$\sum \dot{m}_i (h_i + V_i^2/2 + gZ_i) - \sum \dot{m}_e (h_e + V_e^2/2 + gZ_e) + \dot{Q}_{in} - \dot{W}_{out} = 0$$

and

$$\sum \dot{m}_i = \sum \dot{m}_e$$

where

\dot{m} = mass flow rate (subscripts i and e refer to inlet and exit states of system)

g = acceleration of gravity

Z = elevation

V = velocity

\dot{Q}_{in} = the net rate of heat transfer into the system

\dot{W}_{out} = the net rate of work out of the system

Special Cases of Steady-Flow Energy Equation

Nozzles, Diffusers: Velocity terms are significant. No elevation change, no heat transfer, and no work. Single mass stream.

$$h_i + \frac{V_i^2}{2} = h_e + \frac{V_e^2}{2}$$

$$\text{Isentropic Efficiency (nozzle)} = \frac{\frac{V_e^2}{2} - \frac{V_i^2}{2}}{2(h_i - h_{es})}, \text{ where}$$

h_{es} = enthalpy at isentropic exit state.

Turbines, Pumps, Compressors: Often considered adiabatic (no heat transfer). Velocity terms usually can be ignored. There are significant work terms and a single mass stream.

$$h_i = h_e + w$$

$$\text{Isentropic Efficiency (turbine)} = \frac{h_i - h_e}{h_i - h_{es}}$$

$$\text{Isentropic Efficiency (compressor, pump)} = \frac{h_{es} - h_i}{h_e - h_i}$$

For pump only, $h_{es} - h_i = v_i(P_e - P_i)$

Throttling Valves and Throttling Processes: No work, no heat transfer, and single-mass stream. Velocity terms are often insignificant.

$$h_i = h_e$$

Boilers, Condensers, Evaporators, One Side in a Heat Exchanger: Heat transfer terms are significant. For a single-mass stream, the following applies:

$$h_i + q = h_e$$

Heat Exchangers: No heat loss to the surroundings or work. Two separate flow rates \dot{m}_1 and \dot{m}_2 :

$$\dot{m}_1(h_{1i} - h_{1e}) = \dot{m}_2(h_{2e} - h_{2i})$$

Mixers, Separators, Open or Closed Feedwater Heaters:

$$\sum \dot{m}_i h_i = \sum \dot{m}_e h_e \quad \text{and}$$

$$\sum \dot{m}_i = \sum \dot{m}_e$$

BASIC CYCLES

Heat engines take in heat Q_H at a high temperature T_H , produce a net amount of work W , and reject heat Q_L at a low temperature T_L . The efficiency η of a heat engine is given by:

$$\eta = W/Q_H = (Q_H - Q_L)/Q_H$$

The most efficient engine possible is the *Carnot Cycle*. Its efficiency is given by:

$$\eta_c = (T_H - T_L)/T_H \text{ where}$$

T_H and T_L = absolute temperatures (Kelvin or Rankine).

The following heat-engine cycles are plotted on $P-v$ and $T-s$ diagrams in this section:

Carnot, Otto, Rankine

Refrigeration cycles are the reverse of heat-engine cycles. Heat is moved from low to high temperature requiring work, W . Cycles can be used either for refrigeration or as heat pumps.

Coefficient of Performance (COP) is defined as:

$$\text{COP} = Q_H/W \text{ for heat pumps, and as}$$

$$\text{COP} = Q_L/W \text{ for refrigerators and air conditioners.}$$

Upper limit of COP is based on reversed Carnot Cycle:

$$\text{COP}_c = T_H/(T_H - T_L) \text{ for heat pumps and}$$

$$\text{COP}_c = T_L/(T_H - T_L) \text{ for refrigeration.}$$

$$1 \text{ ton refrigeration} = 12,000 \text{ Btu/hr} = 3,516 \text{ W}$$

The following refrigeration cycles are plotted on $T-s$ diagrams in this section:

reversed rankine, two-stage refrigeration, air refrigeration

PSYCHROMETRICS

Properties of an air-water vapor mixture at a fixed pressure are given in graphical form on a psychrometric chart as provided in this section. When the system pressure is 1 atm, an ideal-gas mixture is assumed.

The definitions that follow use subscript a for dry air and v for water vapor.

P = pressure of the air-water mixture, normally 1 atm

T = dry-bulb temp (air/water mixture temperature)

P_a = partial pressure of dry air

P_v = partial pressure of water vapor

$$P = P_a + P_v$$

Specific Humidity (absolute humidity, humidity ratio) ω :

$$\omega = m_v/m_a \text{ where}$$

m_v = mass of water vapor

m_a = mass of dry air

$$\omega = 0.622P_v/P_a = 0.622P_v/(P - P_v)$$

Relative Humidity (rh) ϕ :

$$\phi = P_v/P_g, \text{ where}$$

P_g = saturation pressure of water at T .

Enthalpy h : $h = h_a + \omega h_v$

Dew-Point Temperature T_{dp} :

$$T_{dp} = T_{sat} \text{ at } P_g = P_v$$

Wet-bulb temperature T_{wb} is the temperature indicated by a thermometer covered by a wick saturated with liquid water and in contact with moving air.

Humid Volume: Volume of moist air/mass of dry air.

SECOND LAW OF THERMODYNAMICS

Thermal Energy Reservoirs

$$\Delta S_{\text{reservoir}} = Q/T_{\text{reservoir}}, \text{ where}$$

Q is measured with respect to the reservoir.

Kelvin-Planck Statement of Second Law

No heat engine can operate in a cycle while transferring heat with a single heat reservoir.

COROLLARY to Kelvin-Planck: No heat engine can have a higher efficiency than a Carnot Cycle operating between the same reservoirs.

Clausius' Statement of Second Law

No refrigeration or heat pump cycle can operate without a net work input.

COROLLARY: No refrigerator or heat pump can have a higher COP than a Carnot Cycle refrigerator or heat pump.

Entropy

$$ds = (1/T) \delta q_{\text{rev}}$$

$$s_2 - s_1 = \int_1^2 (1/T) \delta q_{\text{rev}}$$

Inequality of Clausius

$$\oint (1/T) \delta q_{\text{rev}} \leq 0$$

$$\int_1^2 (1/T) \delta q \leq s_2 - s_1$$

Isothermal, Reversible Process

$$\Delta s = s_2 - s_1 = q/T$$

Isentropic Process

$$\Delta s = 0; ds = 0$$

A reversible adiabatic process is isentropic.

Adiabatic Process

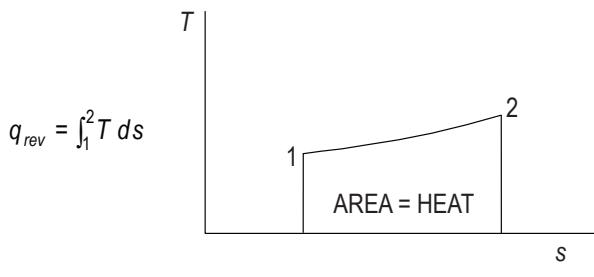
$$\delta q = 0; \Delta s \geq 0$$

Increase of Entropy Principle

$$\Delta s_{\text{total}} = \Delta s_{\text{system}} + \Delta s_{\text{surroundings}} \geq 0$$

$$\Delta s_{\text{total}} = \sum m_{\text{out}} s_{\text{out}} - \sum m_{\text{in}} s_{\text{in}} - \sum (\dot{q}_{\text{external}} / T_{\text{external}}) \geq 0$$

Temperature-Entropy (T - s) Diagram



Entropy Change for Solids and Liquids

$$ds = c (dT/T)$$

$$s_2 - s_1 = \int c (dT/T) = c_{\text{mean}} \ln (T_2/T_1),$$

where c equals the heat capacity of the solid or liquid.

Exergy (Availability)

Exergy (also known as availability) is the maximum possible work that can be obtained from a cycle of a heat engine. The maximum possible work is obtained in a reversible process.

Closed-System Exergy (Availability)

(no chemical reactions)

$$\phi = (u - u_L) - T_L(s - s_L) + p_L(v - v_L)$$

where the subscript L designates environmental conditions and ϕ is availability function.

$$w_{\text{max}} = w_{\text{rev}} = \phi_i - \phi_2$$

Open-System Exergy (Availability)

$$\Psi = (h - h_L) - T_L(s - s_L) + V^2/2 + gZ$$

where V is velocity, g is acceleration of gravity, Z is elevation and Ψ is availability function.

$$w_{\text{max}} = w_{\text{rev}} = \Psi_i - \Psi_2$$

Gibbs Free Energy, ΔG

Energy released or absorbed in a reaction occurring reversibly at constant pressure and temperature.

Helmholtz Free Energy, ΔA

Energy released or absorbed in a reaction occurring reversibly at constant volume and temperature.

Irreversibility, I

$$I = w_{\text{rev}} - w_{\text{actual}} = T_L \Delta s_{\text{total}}$$

HEATS OF REACTION

For a chemical reaction the associated energy can be defined in terms of heats of formation of the individual species ΔH_f° at the standard state

$$(\Delta H_r^\circ) = \sum_{\text{products}} v_i (\Delta H_f^\circ)_i - \sum_{\text{reactants}} v_i (\Delta H_f^\circ)_i$$

v_i = stoichiometric coefficient for species "i"

The standard state is 25°C and 1 bar.

The heat of formation is defined as the enthalpy change associated with the formation of a compound from its atomic species as they normally occur in nature [i.e., O₂(g), H₂(g), C(solid), etc.]

The heat of reaction varies with the temperature as follows:

$$\Delta H_r(T) = \Delta H_r^\circ(T_{\text{ref}}) + \int_{T_{\text{ref}}}^T \Delta c_p dT$$

where T_{ref} is some reference temperature (typically 25°C or 298 K), and:

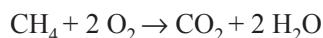
$$\Delta c_p = \sum_{\text{products}} v_i c_{p,i} - \sum_{\text{reactants}} v_i c_{p,i}$$

and $c_{p,i}$ is the molar heat capacity of component i .

The heat of reaction for a combustion process using oxygen is also known as the heat of combustion. The principal products are CO₂(g) and H₂O(l).

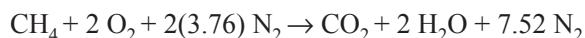
Combustion Processes

First, the combustion equation should be written and balanced. For example, for the stoichiometric combustion of methane in oxygen:



Combustion in Air

For each mole of oxygen, there will be 3.76 moles of nitrogen. For stoichiometric combustion of methane in air:



Combustion in Excess Air

The excess oxygen appears as oxygen on the right side of the combustion equation.

Incomplete Combustion

Some carbon is burned to create carbon monoxide (CO).

$$\text{Molar Air-Fuel Ratio}, \overline{A/F} = \frac{\text{No. of moles of air}}{\text{No. of moles of fuel}}$$

$$\text{Air-Fuel Ratio}, A/F = \frac{\text{Mass of air}}{\text{Mass of fuel}} = \left(\overline{A/F}\right) \left(\frac{M_{\text{air}}}{M_{\text{fuel}}}\right)$$

Stoichiometric (theoretical) air-fuel ratio is the air-fuel ratio calculated from the stoichiometric combustion equation.

$$\text{Percent Theoretical Air} = \frac{(A/F)_{\text{actual}}}{(A/F)_{\text{stoichiometric}}} \times 100$$

$$\text{Percent Excess Air} = \frac{(A/F)_{\text{actual}} - (A/F)_{\text{stoichiometric}}}{(A/F)_{\text{stoichiometric}}} \times 100$$

VAPOR-LIQUID EQUILIBRIUM (VLE)

Henry's Law at Constant Temperature

At equilibrium, the partial pressure of a gas is proportional to its concentration in a liquid. Henry's Law is valid for low concentrations; i.e., $x \approx 0$.

$$P_i = Py_i = hx_p \text{ where}$$

h = Henry's Law constant

P_i = partial pressure of a gas in contact with a liquid

x_i = mol fraction of the gas in the liquid

y_i = mol fraction of the gas in the vapor

P = total pressure

Raoult's Law for Vapor-Liquid Equilibrium

Valid for concentrations near 1; i.e., $x_i \approx 1$ at low pressure (ideal gas behavior)

$$P_i = x_i P_i^*, \text{ where}$$

P_i = partial pressure of component i

x_i = mol fraction of component i in the liquid

P_i^* = vapor pressure of pure component i at the temperature of the mixture

Rigorous Vapor-Liquid Equilibrium

For a multicomponent mixture at equilibrium

$$\hat{f}_i^V = \hat{f}_i^L, \text{ where}$$

\hat{f}_i^V = fugacity of component i in the vapor phase

\hat{f}_i^L = fugacity of component i in the liquid phase

Fugacities of component i in a mixture are commonly calculated in the following ways:

For a liquid $\hat{f}_i^L = x_i \gamma_i f_i^L$, where

x_i = mole fraction of component i

γ_i = activity coefficient of component i

f_i^L = fugacity of pure liquid component i

For a vapor $\hat{f}_i^V = y_i \hat{\Phi}_i P$, where

y_i = mole fraction of component i in the vapor

$\hat{\Phi}_i$ = fugacity coefficient of component i in the vapor

P = system pressure

The activity coefficient γ_i is a correction for liquid phase non-ideality. Many models have been proposed for γ_i such as the Van Laar model:

$$\ln \gamma_1 = A_{12} \left(1 + \frac{A_{12} x_1}{A_{21} x_2}\right)^{-2}$$

$$\ln \gamma_2 = A_{21} \left(1 + \frac{A_{21} x_2}{A_{12} x_1}\right)^{-2}, \text{ where}$$

γ_1 = activity coefficient of component 1 in a two-component system

γ_2 = activity coefficient of component 2 in a two-component system

A_{12}, A_{21} = constants, typically fitted from experimental data

The pure component fugacity is calculated as:

$$f_i^L = \Phi_i^{\text{sat}} P_i^{\text{sat}} \exp\left\{v_i^L (P - P_i^{\text{sat}})/(RT)\right\}, \text{ where}$$

Φ_i^{sat} = fugacity coefficient of pure saturated i

P_i^{sat} = saturation pressure of pure i

v_i^L = specific volume of pure liquid i

R = Ideal Gas Law Constant

T = absolute temperature

Often at system pressures close to atmospheric:

$$f_i^L \approx P_i^{\text{sat}}$$

The fugacity coefficient $\hat{\Phi}_i$ for component i in the vapor is calculated from an equation of state (e.g., Virial).

Sometimes it is approximated by a pure component value from a correlation. Often at pressures close to atmospheric, $\hat{\Phi}_i = 1$. The fugacity coefficient is a correction for vapor phase non-ideality.

For sparingly soluble gases the liquid phase is sometimes represented as:

$$\hat{f}_i^L = x_i k_i$$

where k_i is a constant set by experiment (Henry's constant). Sometimes other concentration units are used besides mole fraction with a corresponding change in k_i .

PHASE RELATIONS

Clapeyron Equation for phase transitions:

$$\left(\frac{dP}{dT}\right)_{sat} = \frac{h_{fg}}{T v_{fg}} = \frac{s_{fg}}{v_{fg}}, \text{ where}$$

h_{fg} = enthalpy change for phase transitions

v_{fg} = volume change

s_{fg} = entropy change

T = absolute temperature

$(dP/dT)_{sat}$ = slope of phase transition (e.g., vapor-liquid) saturation line

Clausius-Clapeyron Equation

This equation results if it is assumed that (1) the volume change (v_{fg}) can be replaced with the vapor volume (v_g), (2) the latter can be replaced with $P/\bar{R}T$ from the ideal gas law, and (3) h_{fg} is independent of the temperature (T).

$$\ln_e\left(\frac{P_2}{P_1}\right) = \frac{h_{fg}}{\bar{R}} \cdot \frac{T_2 - T_1}{T_1 T_2}$$

Gibbs Phase Rule (non-reacting systems)

$P + F = C + 2$, where

P = number of phases making up a system

F = degrees of freedom

C = number of components in a system

CHEMICAL REACTION EQUILIBRIA

Definitions

Conversion – moles reacted/moles fed

Extent – For each species in a reaction, the mole balance may be written:

$$\text{moles}_{i,out} = \text{moles}_{i,in} + v_i \xi \text{ where}$$

ξ is the extent in moles and v_i is the stoichiometric coefficient of the i th species, the sign of which is negative for reactants and positive for products.

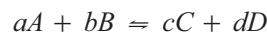
Limiting reactant – Reactant that would be consumed first if the reaction proceeded to completion. Other reactants are excess reactants.

Selectivity – Moles of desired product formed/moles of undesired product formed.

Yield – Moles of desired product formed/moles that would have been formed if there were no side reactions and the limiting reactant had reacted completely.

Chemical Reaction Equilibrium

For the reaction



$$\Delta G^\circ = -RT \ln K_a$$

$$K_a = \frac{(\hat{a}_C^c)(\hat{a}_D^d)}{(\hat{a}_A^a)(\hat{a}_B^b)} = \prod_i (\hat{a}_i)^{v_i}, \text{ where}$$

$$\hat{a}_i = \text{activity of component } i = \frac{\hat{f}_i}{\hat{f}_i^*}$$

\hat{f}_i^* = fugacity of pure i in its standard state at the equilibrium reaction temperature, T

v_i = stoichiometric coefficient of component i

ΔG° = standard Gibbs energy change of reaction

K_a = chemical equilibrium constant

For mixtures of ideal gases:

$$\hat{f}_i^* = \text{unit pressure, often 1 bar}$$

$$\hat{f}_i = y_i P = p_i$$

where p_i = partial pressure of component i .

$$\text{Then } K_a = K_p = \frac{(p_C^c)(p_D^d)}{(p_A^a)(p_B^b)} = P^{c+d-a-b} \frac{(y_C^c)(y_D^d)}{(y_A^a)(y_B^b)}$$

For solids $\hat{a}_i = 1$

For liquids $\hat{a}_i = x_i \gamma_i$

The effect of temperature on the equilibrium constant is

$$\frac{d \ln K}{dT} = \frac{\Delta H^\circ}{RT^2}$$

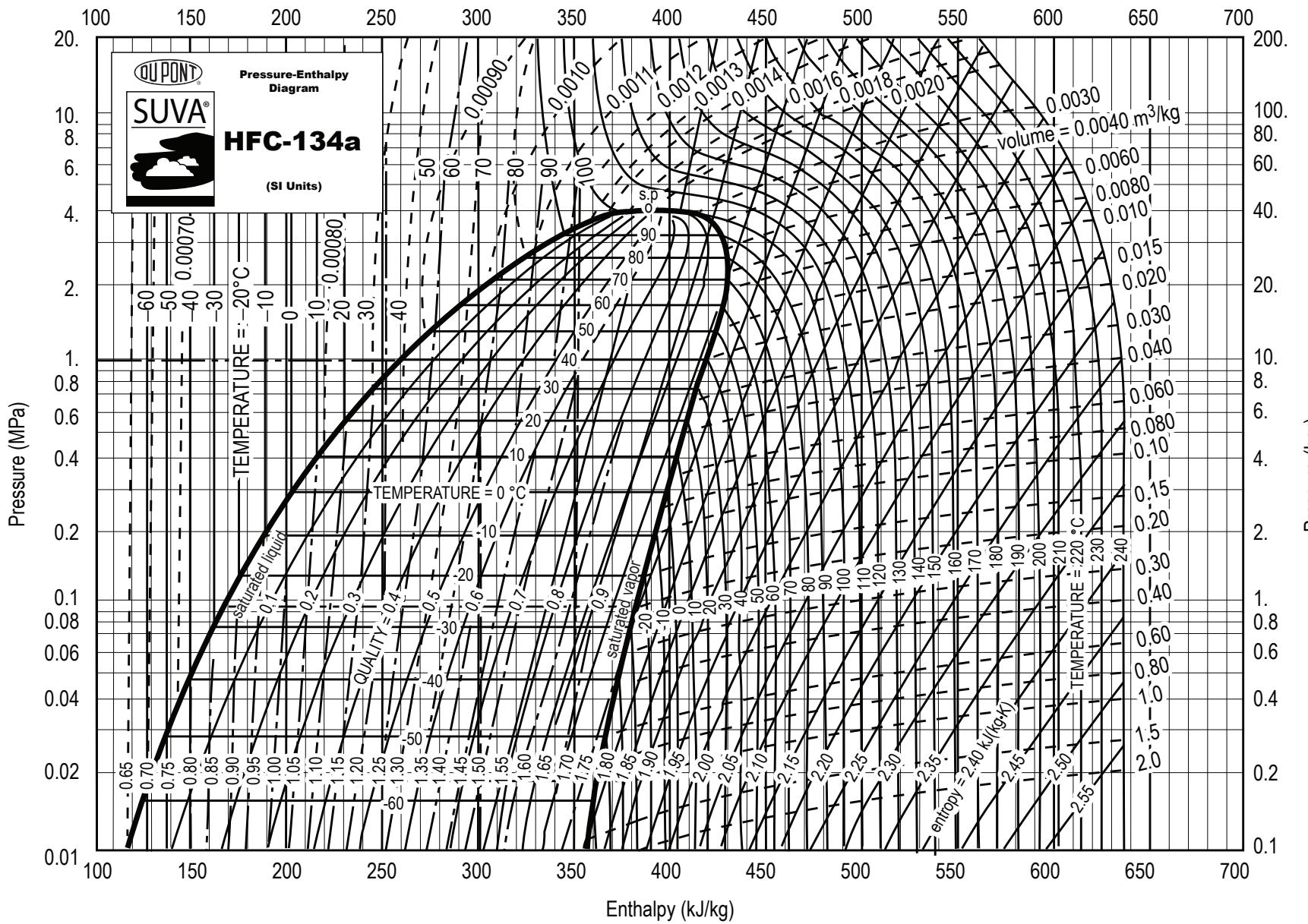
where ΔH° = standard enthalpy change of reaction.

STEAM TABLES
Saturated Water - Temperature Table

Temp. °C <i>T</i>	Sat. Press. kPa <i>P_{sat}</i>	Specific Volume m ³ /kg		Internal Energy kJ/kg			Enthalpy kJ/kg			Entropy kJ/(kg·K)		
		Sat. liquid <i>v_f</i>	Sat. vapor <i>v_g</i>	Sat. liquid <i>u_f</i>	Evap. <i>u_{fg}</i>	Sat. vapor <i>u_g</i>	Sat. liquid <i>h_f</i>	Evap. <i>h_{fg}</i>	Sat. vapor <i>h_g</i>	Sat. liquid <i>s_f</i>	Evap. <i>s_{fg}</i>	Sat. vapor <i>s_g</i>
0.01	0.6113	0.001 000	206.14	0.00	2375.3	2375.3	0.01	2501.3	2501.4	0.0000	9.1562	9.1562
5	0.8721	0.001 000	147.12	20.97	2361.3	2382.3	20.98	2489.6	2510.6	0.0761	8.9496	9.0257
10	1.2276	0.001 000	106.38	42.00	2347.2	2389.2	42.01	2477.7	2519.8	0.1510	8.7498	8.9008
15	1.7051	0.001 001	77.93	62.99	2333.1	2396.1	62.99	2465.9	2528.9	0.2245	8.5569	8.7814
20	2.339	0.001 002	57.79	83.95	2319.0	2402.9	83.96	2454.1	2538.1	0.2966	8.3706	8.6672
25	3.169	0.001 003	43.36	104.88	2304.9	2409.8	104.89	2442.3	2547.2	0.3674	8.1905	8.5580
30	4.246	0.001 004	32.89	125.78	2290.8	2416.6	125.79	2430.5	2556.3	0.4369	8.0164	8.4533
35	5.628	0.001 006	25.22	146.67	2276.7	2423.4	146.68	2418.6	2565.3	0.5053	7.8478	8.3531
40	7.384	0.001 008	19.52	167.56	2262.6	2430.1	167.57	2406.7	2574.3	0.5725	7.6845	8.2570
45	9.593	0.001 010	15.26	188.44	2248.4	2436.8	188.45	2394.8	2583.2	0.6387	7.5261	8.1648
50	12.349	0.001 012	12.03	209.32	2234.2	2443.5	209.33	2382.7	2592.1	0.7038	7.3725	8.0763
55	15.758	0.001 015	9.568	230.21	2219.9	2450.1	230.23	2370.7	2600.9	0.7679	7.2234	7.9913
60	19.940	0.001 017	7.671	251.11	2205.5	2456.6	251.13	2358.5	2609.6	0.8312	7.0784	7.9096
65	25.03	0.001 020	6.197	272.02	2191.1	2463.1	272.06	2346.2	2618.3	0.8935	6.9375	7.8310
70	31.19	0.001 023	5.042	292.95	2176.6	2569.6	292.98	2333.8	2626.8	0.9549	6.8004	7.7553
75	38.58	0.001 026	4.131	313.90	2162.0	2475.9	313.93	2321.4	2635.3	1.0155	6.6669	7.6824
80	47.39	0.001 029	3.407	334.86	2147.4	2482.2	334.91	2308.8	2643.7	1.0753	6.5369	7.6122
85	57.83	0.001 033	2.828	355.84	2132.6	2488.4	355.90	2296.0	2651.9	1.1343	6.4102	7.5445
90	70.14	0.001 036	2.361	376.85	2117.7	2494.5	376.92	2283.2	2660.1	1.1925	6.2866	7.4791
95	84.55	0.001 040	1.982	397.88	2102.7	2500.6	397.96	2270.2	2668.1	1.2500	6.1659	7.4159
		MPa										
100	0.101 35	0.001 044	1.6729	418.94	2087.6	2506.5	419.04	2257.0	2676.1	1.3069	6.0480	7.3549
105	0.120 82	0.001 048	1.4194	440.02	2072.3	2512.4	440.15	2243.7	2683.8	1.3630	5.9328	7.2958
110	0.143 27	0.001 052	1.2102	461.14	2057.0	2518.1	461.30	2230.2	2691.5	1.4185	5.8202	7.2387
115	0.169 06	0.001 056	1.0366	482.30	2041.4	2523.7	482.48	2216.5	2699.0	1.4734	5.7100	7.1833
120	0.198 53	0.001 060	0.8919	503.50	2025.8	2529.3	503.71	2202.6	2706.3	1.5276	5.6020	7.1296
125	0.2321	0.001 065	0.7706	524.74	2009.9	2534.6	524.99	2188.5	2713.5	1.5813	5.4962	7.0775
130	0.2701	0.001 070	0.6685	546.02	1993.9	2539.9	546.31	2174.2	2720.5	1.6344	5.3925	7.0269
135	0.3130	0.001 075	0.5822	567.35	1977.7	2545.0	567.69	2159.6	2727.3	1.6870	5.2907	6.9777
140	0.3613	0.001 080	0.5089	588.74	1961.3	2550.0	589.13	2144.7	2733.9	1.7391	5.1908	6.9299
145	0.4154	0.001 085	0.4463	610.18	1944.7	2554.9	610.63	2129.6	2740.3	1.7907	5.0926	6.8833
150	0.4758	0.001 091	0.3928	631.68	1927.9	2559.5	632.20	2114.3	2746.5	1.8418	4.9960	6.8379
155	0.5431	0.001 096	0.3468	653.24	1910.8	2564.1	653.84	2098.6	2752.4	1.8925	4.9010	6.7935
160	0.6178	0.001 102	0.3071	674.87	1893.5	2568.4	675.55	2082.6	2758.1	1.9427	4.8075	6.7502
165	0.7005	0.001 108	0.2727	696.56	1876.0	2572.5	697.34	2066.2	2763.5	1.9925	4.7153	6.7078
170	0.7917	0.001 114	0.2428	718.33	1858.1	2576.5	719.21	2049.5	2768.7	2.0419	4.6244	6.6663
175	0.8920	0.001 121	0.2168	740.17	1840.0	2580.2	741.17	2032.4	2773.6	2.0909	4.5347	6.6256
180	1.0021	0.001 127	0.194 05	762.09	1821.6	2583.7	763.22	2015.0	2778.2	2.1396	4.4461	6.5857
185	1.1227	0.001 134	0.174 09	784.10	1802.9	2587.0	785.37	1997.1	2782.4	2.1879	4.3586	6.5465
190	1.2544	0.001 141	0.156 54	806.19	1783.8	2590.0	807.62	1978.8	2786.4	2.2359	4.2720	6.5079
195	1.3978	0.001 149	0.141 05	828.37	1764.4	2592.8	829.98	1960.0	2790.0	2.2835	4.1863	6.4698
200	1.5538	0.001 157	0.127 36	850.65	1744.7	2595.3	852.45	1940.7	2793.2	2.3309	4.1014	6.4323
205	1.7230	0.001 164	0.115 21	873.04	1724.5	2597.5	875.04	1921.0	2796.0	2.3780	4.0172	6.3952
210	1.9062	0.001 173	0.104 41	895.53	1703.9	2599.5	897.76	1900.7	2798.5	2.4248	3.9337	6.3585
215	2.104	0.001 181	0.094 79	918.14	1682.9	2601.1	920.62	1879.9	2800.5	2.4714	3.8507	6.3221
220	2.318	0.001 190	0.086 19	940.87	1661.5	2602.4	943.62	1858.5	2802.1	2.5178	3.7683	6.2861
225	2.548	0.001 199	0.078 49	963.73	1643.6	2603.3	966.78	1836.5	2803.3	2.5639	3.6863	6.2503
230	2.795	0.001 209	0.071 58	986.74	1617.2	2603.9	990.12	1813.8	2804.0	2.6099	3.6047	6.2146
235	3.060	0.001 219	0.065 37	1009.89	1594.2	2604.1	1013.62	1790.5	2804.2	2.6558	3.5233	6.1791
240	3.344	0.001 229	0.059 76	1033.21	1570.8	2604.0	1037.32	1766.5	2803.8	2.7015	3.4422	6.1437
245	3.648	0.001 240	0.054 71	1056.71	1546.7	2603.4	1061.23	1741.7	2803.0	2.7472	3.3612	6.1083
250	3.973	0.001 251	0.050 13	1080.39	1522.0	2602.4	1085.36	1716.2	2801.5	2.7927	3.2802	6.0730
255	4.319	0.001 263	0.045 98	1104.28	1506.7	2600.9	1109.73	1689.8	2799.5	2.8383	3.1992	6.0375
260	4.688	0.001 276	0.042 21	1128.39	1470.6	2599.0	1134.37	1662.5	2796.9	2.8838	3.1181	6.0019
265	5.081	0.001 289	0.038 77	1152.74	1443.9	2596.6	1159.28	1634.4	2793.6	2.9294	3.0368	5.9662
270	5.499	0.001 302	0.035 64	1177.36	1416.3	2593.7	1184.51	1605.2	2789.7	2.9751	2.9551	5.9301
275	5.942	0.001 317	0.032 79	1202.25	1387.9	2590.2	1210.07	1574.9	2785.0	3.0208	2.8730	5.8938
280	6.412	0.001 332	0.030 17	1227.46	1358.7	2586.1	1235.99	1543.6	2779.6	3.0668	2.7903	5.8571
285	6.909	0.001 348	0.027 77	1253.00	1328.4	2581.4	1262.31	1511.0	2773.3	3.1130	2.7070	5.8199
290	7.436	0.001 366	0.025 57	1278.92	1297.1	2576.0	1289.07	1477.1	2766.2	3.1594	2.6227	5.7821
295	7.993	0.001 384	0.023 54	1305.2	1264.7	2569.9	1316.3	1441.8	2758.1	3.2062	2.5375	5.7437
300	8.581	0.001 404	0.021 67	1332.0	1231.0	2563.0	1344.0	1404.9	2749.0	3.2534	2.4511	5.7045
305	9.202	0.001 425	0.019 948	1359.3	1195.9	2555.2	1372.4	1366.4	2738.7	3.3010	2.3633	5.6643
310	9.856	0.001 447	0.018 350	1387.1	1159.4	2546.4	1401.3	1326.0	2727.3	3.3493	2.2737	5.6230
315	10.547	0.001 472	0.016 867	1415.5	1121.1	2536.6	1431.0	1283.5	2714.5	3.3982	2.1821	5.5804
320	11.274	0.001 499	0.015 488	1444.6	1080.9	2525.5	1461.5	1238.6	2700.1			

Superheated Water Tables								
T Temp. °C	v m³/kg	u kJ/kg	h kJ/kg	s kJ/(kg·K)	v m³/kg	u kJ/kg	h kJ/kg	
	p = 0.01 MPa (45.81°C)				p = 0.05 MPa (81.33°C)			
Sat.	14.674	2437.9	2584.7	8.1502	3.240	2483.9	2645.9	7.5939
50	14.869	2443.9	2592.6	8.1749	3.418	2511.6	2682.5	7.6947
100	17.196	2515.5	2687.5	8.4479	3.889	2585.6	2780.1	7.9401
150	19.512	2587.9	2783.0	8.6882	4.356	2659.9	2877.7	8.1580
200	21.825	2661.3	2879.5	8.9038	4.820	2735.0	2976.0	8.3556
250	24.136	2736.0	2977.3	9.1002	5.284	2811.3	3075.5	8.5373
300	26.445	2812.1	3076.5	9.2813	6.209	2968.5	3278.9	8.8642
400	31.063	2968.9	3279.6	9.6077	7.134	3132.0	3488.7	9.1546
500	35.679	3132.3	3489.1	9.8978	8.057	3302.2	3705.1	9.4178
600	40.295	3302.5	3705.4	10.1608	8.981	3479.4	3928.5	9.6599
700	44.911	3479.6	3928.7	10.4028	9.904	3663.6	4158.9	9.8852
800	49.526	3663.8	4159.0	10.6281	10.828	3854.9	4396.3	10.0967
900	54.141	3855.0	4396.4	10.8396	11.751	4052.9	4640.5	10.2964
1000	58.757	4053.0	4640.6	11.0393	12.674	4257.4	4891.1	10.4859
1100	63.372	4257.5	4891.2	11.2287	13.597	4467.8	5147.7	10.6662
1200	67.987	4467.9	5147.8	11.4091	14.521	4683.6	5409.6	10.8382
1300	72.602	4683.7	5409.7	11.5811	p = 0.10 MPa (99.63°C)			
Sat.	1.6940	2506.1	2675.5	7.3594	0.8857	2529.5	2706.7	7.1272
100	1.6958	2506.7	2676.2	7.3614	0.9596	2576.9	2768.8	7.2795
150	1.9364	2582.8	2776.4	7.6134	1.0803	2654.4	2870.5	7.5066
200	2.172	2658.1	2875.3	7.8343	1.1988	2731.2	2971.0	7.7086
250	2.406	2733.7	2974.3	8.0333	1.3162	2808.6	3071.8	7.8926
300	2.639	2810.4	3074.3	8.2158	1.5493	2966.7	3276.6	8.2218
400	3.103	2967.9	3278.2	8.5435	1.7814	3130.8	3487.1	8.5133
500	3.565	3131.6	3488.1	8.8342	2.013	3301.4	3704.0	8.7770
600	4.028	3301.9	3704.4	9.0976	2.244	3478.8	3927.6	9.0194
700	4.490	3479.2	3928.2	9.3398	2.475	3663.1	4158.2	9.2449
800	4.952	3663.5	4158.6	9.5652	2.705	3854.5	4395.8	9.4566
900	5.414	3854.8	4396.1	9.7767	2.937	4052.5	4640.0	9.6563
1000	5.875	4052.8	4640.3	9.9764	3.168	4257.0	4890.7	9.8458
1100	6.337	4257.3	4891.0	10.1659	3.399	4467.5	5147.5	10.0262
1200	6.799	4467.7	5147.6	10.3463	3.630	4683.2	5409.3	10.1982
1300	7.260	4683.5	5409.5	10.5183	p = 0.40 MPa (143.63°C)			
Sat.	0.4625	2553.6	2738.6	6.8959	0.3157	2567.4	2756.8	6.7600
150	0.4708	2564.5	2752.8	6.9299	0.3520	2638.9	2850.1	6.9665
200	0.5342	2646.8	2860.5	7.1706	0.3938	2720.9	2957.2	7.1816
250	0.5951	2726.1	2964.2	7.3789	0.4344	2801.0	3061.6	7.3724
300	0.6548	2804.8	3066.8	7.5662	0.4742	2881.2	3165.7	7.5464
350	0.7137	2884.6	3170.1	7.7324	0.5137	2962.1	3270.3	7.7079
400	0.7726	2964.4	3273.4	7.8985	0.5920	3127.6	3482.8	8.0021
500	0.8893	3129.2	3484.9	8.1913	0.6697	3299.1	3700.9	8.2674
600	1.0055	3300.2	3702.4	8.4558	0.7472	3477.0	3925.3	8.5107
700	1.1215	3477.9	3926.5	8.6987	0.8245	3661.8	4156.5	8.7367
800	1.2372	3662.4	4157.3	8.9244	0.9017	3853.4	4394.4	8.9486
900	1.3529	3853.9	4395.1	9.1362	0.9788	4051.5	4638.8	9.1485
1000	1.4685	4052.0	4639.4	9.3360	1.0559	4256.1	4889.6	9.3381
1100	1.5840	4256.5	4890.2	9.5256	1.1330	4466.5	5146.3	9.5185
1200	1.6996	4467.0	5146.8	9.7060	1.2101	4682.3	5408.3	9.6906
1300	1.8151	4682.8	5408.8	9.8780	p = 0.80 MPa (170.43°C)			
Sat.	0.2404	2576.8	2769.1	6.6628	0.194 44	2583.6	2778.1	6.5865
200	0.2608	2630.6	2839.3	6.8158	0.2060	2621.9	2827.9	6.6940
250	0.2931	2715.5	2950.0	7.0384	0.2327	2709.9	2942.6	6.9247
300	0.3241	2797.2	3056.5	7.2328	0.2579	2793.2	3051.2	7.1229
350	0.3544	2878.2	3161.7	7.4089	0.2825	2875.2	3157.7	7.3011
400	0.3843	2959.7	3267.1	7.5716	0.3066	2957.3	3263.9	7.4651
500	0.4433	3126.0	3480.6	7.8673	0.3541	3124.4	3478.5	7.7622
600	0.5018	3297.9	3699.4	8.1333	0.4011	3296.8	3697.9	8.0290
700	0.5601	3476.2	3924.2	8.3770	0.4478	3475.3	3923.1	8.2731
800	0.6181	3661.1	4155.6	8.6033	0.4943	3660.4	4154.7	8.4996
900	0.6761	3852.8	4393.7	8.8153	0.5407	3852.2	4392.9	8.7118
1000	0.7340	4051.0	4638.2	9.0153	0.5871	4050.5	4637.6	8.9119
1100	0.7919	4255.6	4889.1	9.2050	0.6335	4255.1	4888.6	9.1017
1200	0.8497	4466.1	5145.9	9.3855	0.6798	4465.6	5145.4	9.2822
1300	0.9076	4681.8	5407.9	9.5575	0.7261	4681.3	5407.4	9.4543

P-h Diagram for Refrigerant HFC-134a
(metric units)

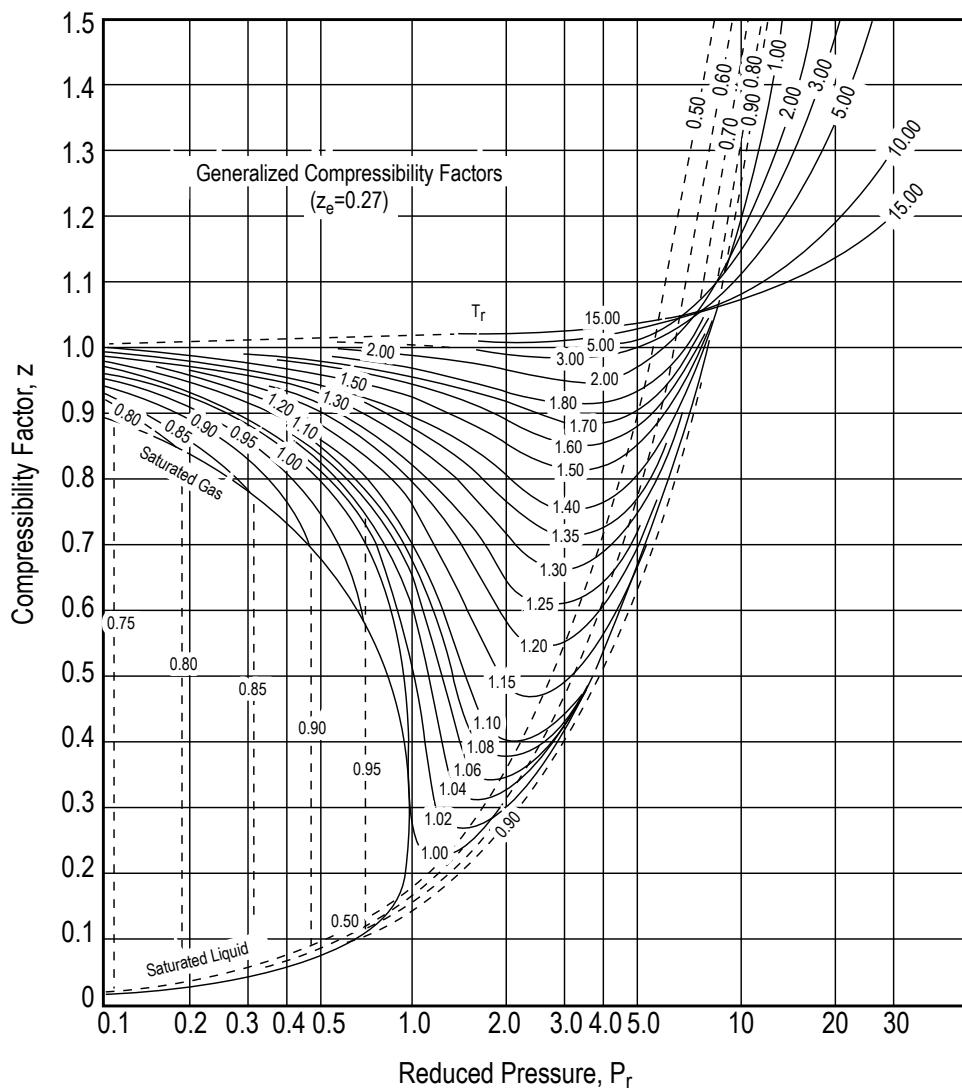


Data provided by DuPont Refrigerants, a division of E.I. duPont de Nemours and Co., Inc.

Thermal and Physical Property Tables
(at room temperature)

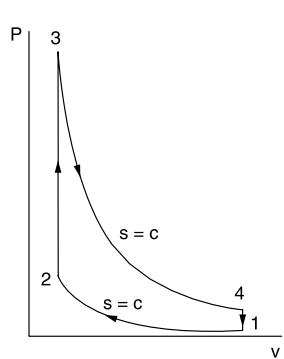
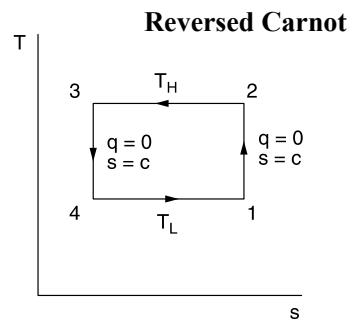
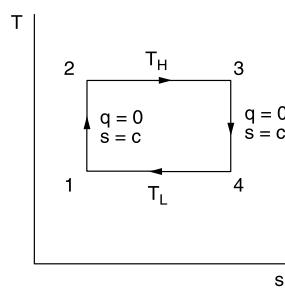
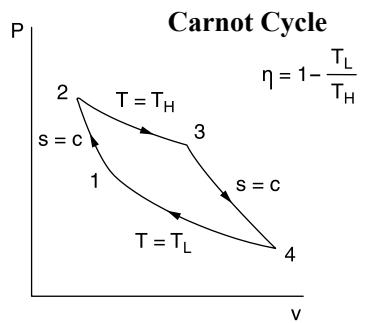
GASES							
Substance	Mol wt	<i>c_p</i>		<i>c_v</i>		<i>k</i>	R
		kJ/(kg·K)	Btu/(lbm- °R)	kJ/(kg·K)	Btu/(lbm- °R)		kJ/(kg·K)
Gases							
Air	29	1.00	0.240	0.718	0.171	1.40	0.2870
Argon	40	0.520	0.125	0.312	0.0756	1.67	0.2081
Butane	58	1.72	0.415	1.57	0.381	1.09	0.1430
Carbon dioxide	44	0.846	0.203	0.657	0.158	1.29	0.1889
Carbon monoxide	28	1.04	0.249	0.744	0.178	1.40	0.2968
Ethane	30	1.77	0.427	1.49	0.361	1.18	0.2765
Helium	4	5.19	1.25	3.12	0.753	1.67	2.0769
Hydrogen	2	14.3	3.43	10.2	2.44	1.40	4.1240
Methane	16	2.25	0.532	1.74	0.403	1.30	0.5182
Neon	20	1.03	0.246	0.618	0.148	1.67	0.4119
Nitrogen	28	1.04	0.248	0.743	0.177	1.40	0.2968
Octane vapor	114	1.71	0.409	1.64	0.392	1.04	0.0729
Oxygen	32	0.918	0.219	0.658	0.157	1.40	0.2598
Propane	44	1.68	0.407	1.49	0.362	1.12	0.1885
Steam	18	1.87	0.445	1.41	0.335	1.33	0.4615

SELECTED LIQUIDS AND SOLIDS				
Substance	<i>c_p</i>		Density	
	kJ/(kg·K)	Btu/(lbm- °R)	kg/m ³	lbm/ft ³
Liquids				
Ammonia	4.80	1.146	602	38
Mercury	0.139	0.033	13,560	847
Water	4.18	1.000	997	62.4
Solids				
Aluminum	0.900	0.215	2,700	170
Copper	0.386	0.092	8,900	555
Ice (0°C; 32°F)	2.11	0.502	917	57.2
Iron	0.450	0.107	7,840	490
Lead	0.128	0.030	11,310	705

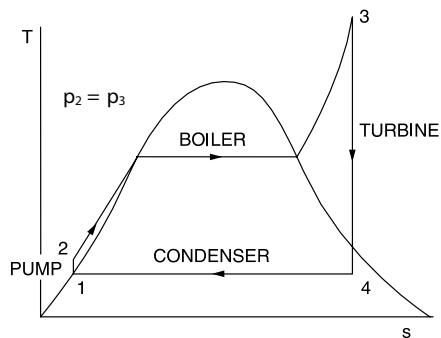
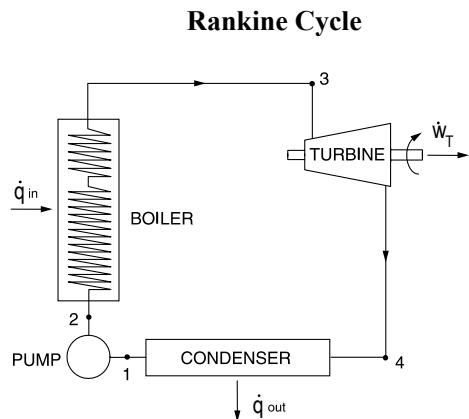
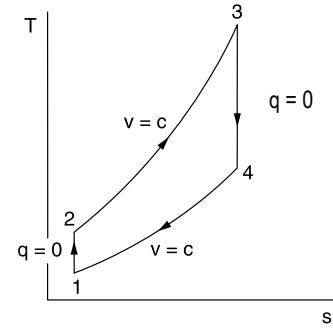


de Nevers, Noel, *Physical and Chemical Equilibrium for Chemical Engineers*, 2nd ed., Wiley, p. 308, © 2012.

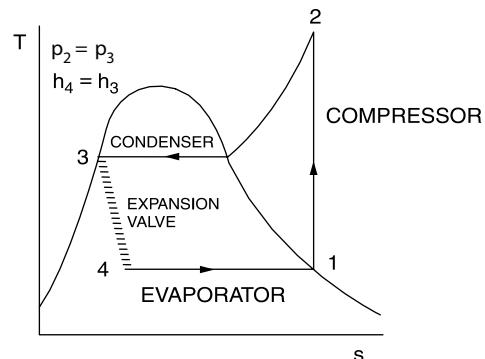
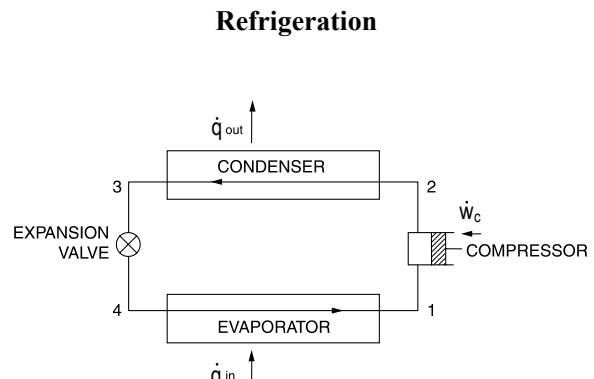
COMMON THERMODYNAMIC CYCLES



**Otto Cycle
(Gasoline Engine)**



$$\eta = \frac{(h_3 - h_4) - (h_2 - h_1)}{h_3 - h_2}$$



$$COP_{ref} = \frac{h_1 - h_4}{h_2 - h_1}$$

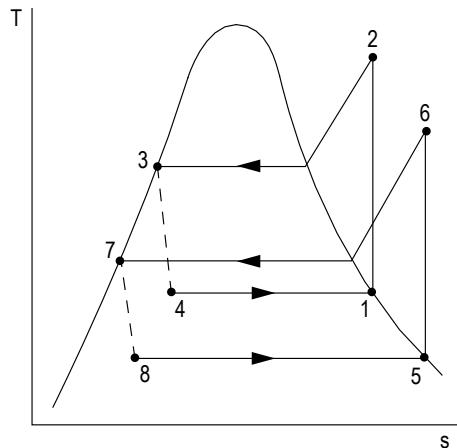
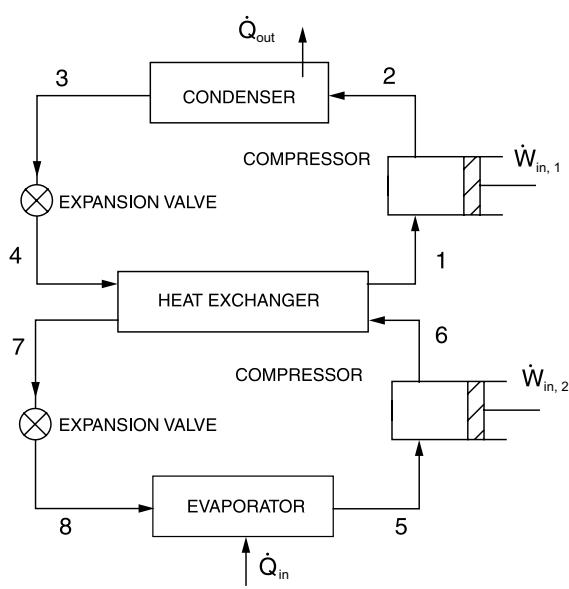
$$COP_{HP} = \frac{h_2 - h_3}{h_2 - h_1}$$

REFRIGERATION AND HVAC

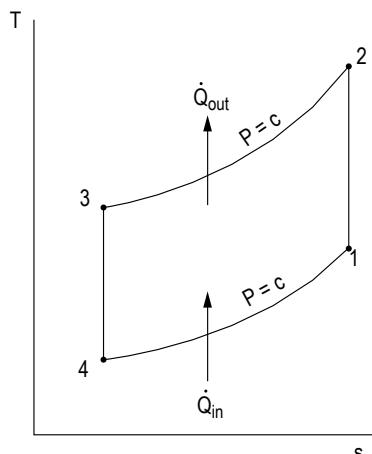
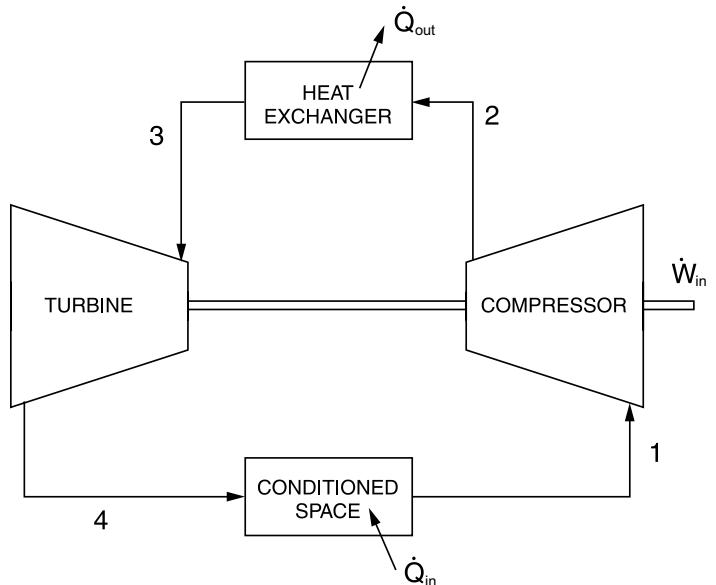
Cycles

Refrigeration and HVAC

Two-Stage Cycle



Air Refrigeration Cycle



$$COP_{ref} = \frac{\dot{Q}_{in}}{\dot{W}_{in,1} + \dot{W}_{in,2}} = \frac{h_1 - h_4}{(h_2 - h_1) - (h_3 - h_4)}$$

$$COP_{HP} = \frac{\dot{Q}_{out}}{\dot{W}_{in,1} + \dot{W}_{in,2}} = \frac{h_2 - h_3}{(h_2 - h_1) - (h_3 - h_4)}$$

The following equations are valid if the mass flows are the same in each stage.

$$COP_{ref} = \frac{\dot{Q}_{in}}{\dot{W}_{in,1} + \dot{W}_{in,2}} = \frac{h_1 - h_4}{h_2 - h_1 + h_6 - h_5}$$

$$COP_{HP} = \frac{\dot{Q}_{out}}{\dot{W}_{in,1} + \dot{W}_{in,2}} = \frac{h_2 - h_3}{h_2 - h_1 + h_6 - h_5}$$



ASHRAE PSYCHROMETRIC CHART NO.1

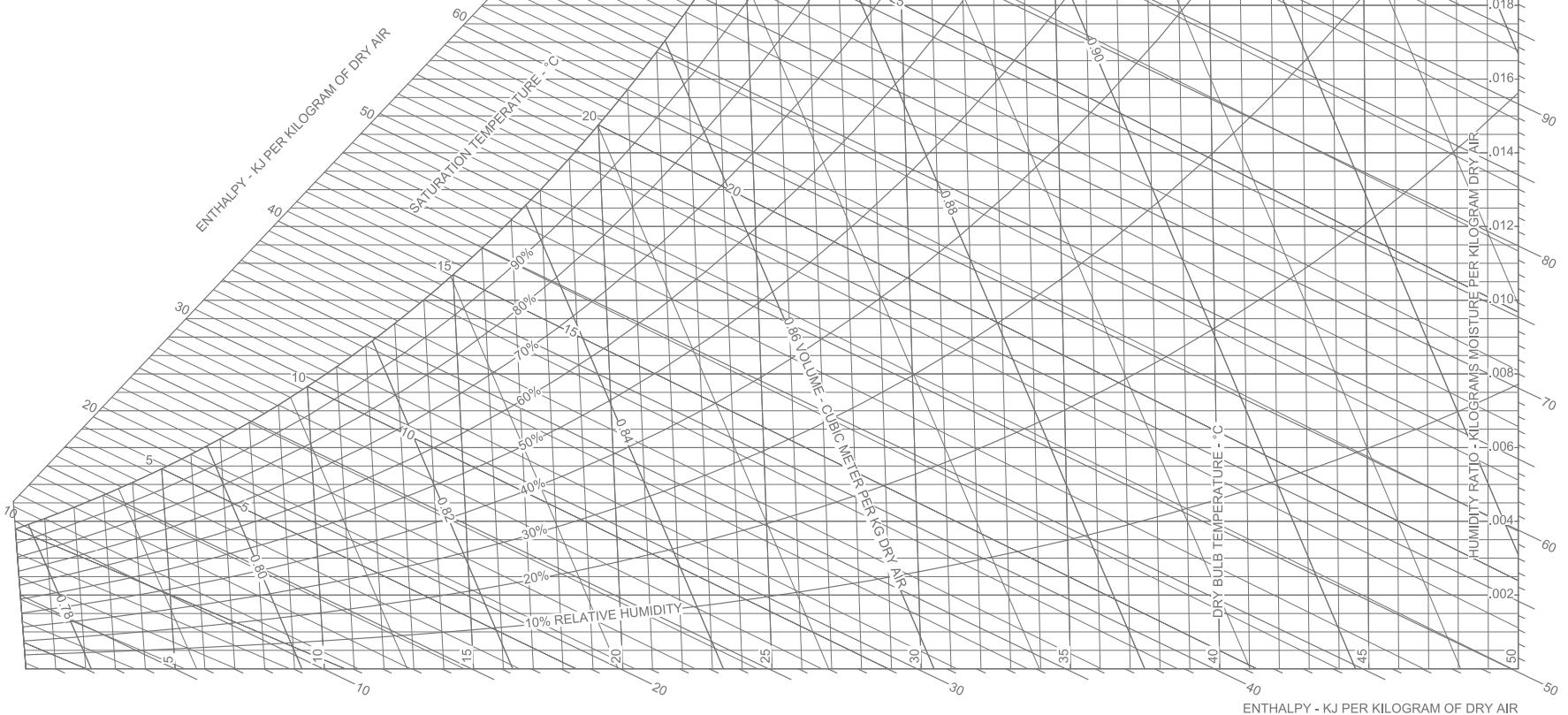
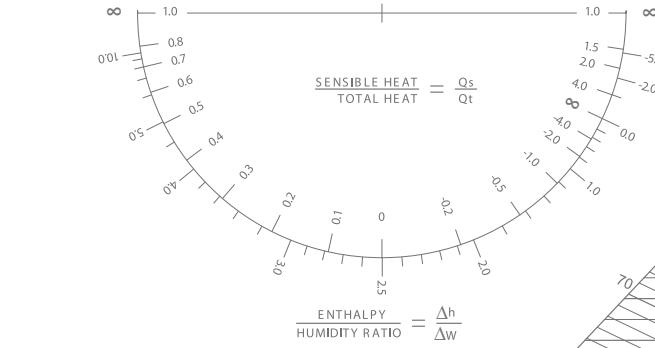
NORMAL TEMPERATURE

BAROMETRIC PRESSURE: 101.325 kPa

Copyright 1992

AMERICAN SOCIETY OF HEATING, REFRIGERATING AND AIR-CONDITIONING ENGINEERS, INC.

SEA LEVEL



ASHRAE Psychrometric Chart No. 1

(English units)

© 2013 ASHRAE Psychrometric Chart No. 1

ASHRAE PSYCHROMETRIC CHART NO.1

NORMAL TEMPERATURE

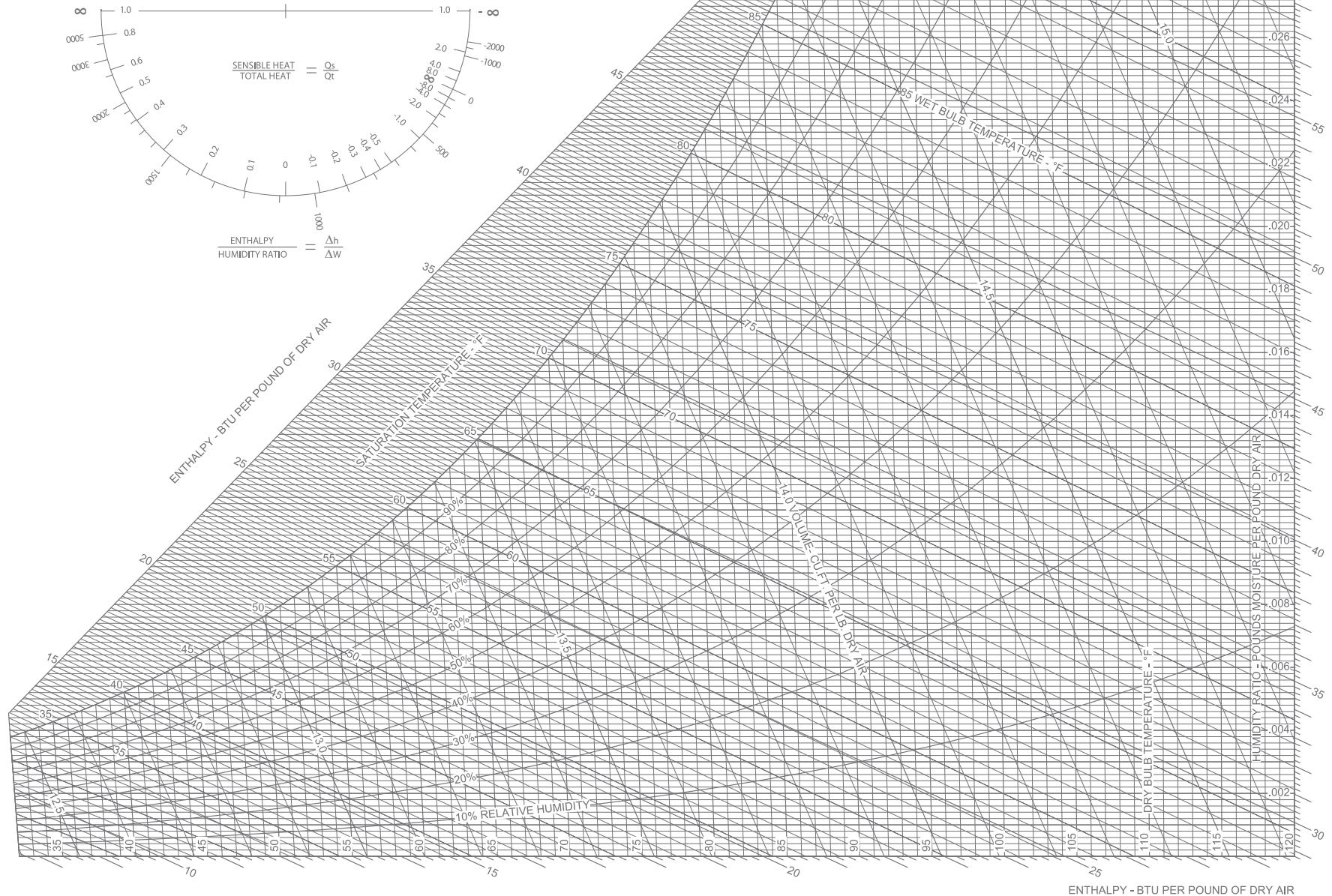
BAROMETRIC PRESSURE: 29.921 INCHES OF MERCURY

Copyright 1992

AMERICAN SOCIETY OF HEATING, REFRIGERATING AND AIR-CONDITIONING ENGINEERS, INC.



SEA LEVEL



FLUID MECHANICS

DEFINITIONS

Density, Specific Volume, Specific Weight, and Specific Gravity

The definitions of density, specific weight, and specific gravity follow:

$$\rho = \lim_{\Delta V \rightarrow 0} \frac{\Delta m}{\Delta V}$$

$$\gamma = \lim_{\Delta V \rightarrow 0} \frac{\Delta W}{\Delta V}$$

$$\gamma = \lim_{\Delta V \rightarrow 0} g \cdot \Delta m / \Delta V = \rho g$$

also $SG = \gamma/\gamma_w = \rho/\rho_w$, where

ρ = density (also called *mass density*)

Δm = mass of infinitesimal volume

ΔV = volume of infinitesimal object considered

γ = specific weight

$$= \rho g$$

ΔW = weight of an infinitesimal volume

SG = specific gravity

ρ_w = density of water at standard conditions
= 1,000 kg/m³ (62.4 lbm/ft³)

γ_w = specific weight of water at standard conditions
= 9,810 N/m³ (62.4 lbf/ft³)
= 9,810 kg/(m²•s²)

Stress, Pressure, and Viscosity

Stress is defined as

$$\tau(1) = \lim_{\Delta A \rightarrow 0} \frac{\Delta F}{\Delta A}, \text{ where}$$

$\tau(1)$ = surface stress vector at point 1

ΔF = force acting on infinitesimal area ΔA

ΔA = infinitesimal area at point 1

$$\tau_n = -P$$

$\tau_t = \mu(dv/dy)$ (one-dimensional; i.e., y), where

τ_n and τ_t = normal and tangential stress components at point 1, respectively

P = pressure at point 1

μ = absolute dynamic viscosity of the fluid
N•s/m² [lbm/(ft•sec)]

dv = differential velocity

dy = differential distance, normal to boundary

v = velocity at boundary condition

y = normal distance, measured from boundary

ν = kinematic viscosity; m²/s (ft²/sec)

$$\text{where } \nu = \mu/\rho$$

For a thin Newtonian fluid film and a linear velocity profile,

$$v(y) = vy/\delta; dv/dy = v/\delta, \text{ where}$$

v = velocity of plate on film

δ = thickness of fluid film

For a power law (non-Newtonian) fluid

$$\tau_t = K (dv/dy)^n, \text{ where}$$

K = consistency index

n = power law index

$n < 1 \equiv$ pseudo plastic

$n > 1 \equiv$ dilatant

Surface Tension and Capillarity

Surface tension σ is the force per unit contact length

$$\sigma = F/L, \text{ where}$$

σ = surface tension, force/length

F = surface force at the interface

L = length of interface

The capillary rise h is approximated by

$$h = (4\sigma \cos \beta)/(\gamma d), \text{ where}$$

h = height of the liquid in the vertical tube

σ = surface tension

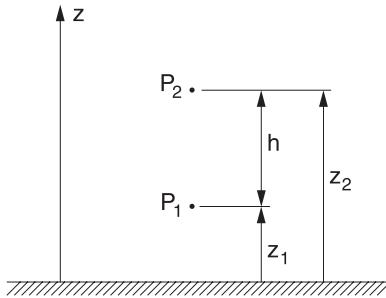
β = angle made by the liquid with the wetted tube wall

γ = specific weight of the liquid

d = the diameter of the capillary tube

CHARACTERISTICS OF A STATIC LIQUID

The Pressure Field in a Static Liquid



The difference in pressure between two different points is

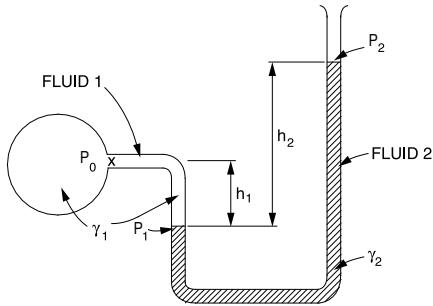
$$P_2 - P_1 = -\gamma(z_2 - z_1) = -\gammah = -\rho gh$$

Absolute pressure = atmospheric pressure + gage pressure reading

Absolute pressure = atmospheric pressure - vacuum gage pressure reading

◆ Bober, W., and R.A. Kenyon, *Fluid Mechanics*, Wiley, 1980. Diagrams reprinted by permission of William Bober and Richard A. Kenyon.

Manometers



For a simple manometer,

$$P_0 = P_2 + \gamma_2 h_2 - \gamma_1 h_1 = P_2 + g (\rho_2 h_2 - \rho_1 h_1)$$

$$\text{If } h_1 = h_2 = h$$

$$P_0 = P_2 + (\gamma_2 - \gamma_1)h = P_2 + (\rho_2 - \rho_1)gh$$

Note that the difference between the two densities is used.

P = pressure

γ = specific weight of fluid

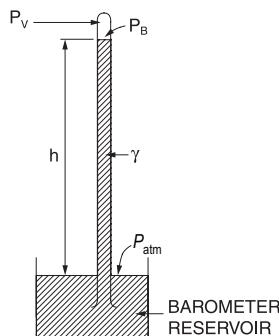
h = height

g = acceleration of gravity

ρ = fluid density

Another device that works on the same principle as the manometer is the simple barometer.

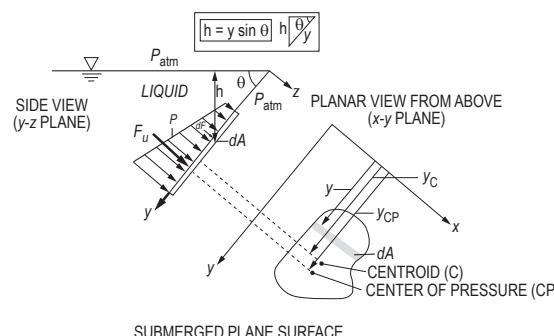
$$P_{\text{atm}} = P_A = P_v + \gamma h = P_B + \gamma h = P_B + \rho gh$$



P_v = vapor pressure of the barometer fluid

Forces on Submerged Surfaces and the Center of Pressure

•



The pressure on a point at a vertical distance h below the surface is:

$$P = P_{\text{atm}} + \rho gh, \text{ for } h \geq 0$$

- ◆ Bober, W., and R.A. Kenyon, *Fluid Mechanics*, Wiley, 1980. Diagrams reprinted by permission of William Bober and Richard A. Kenyon.
- Elger, Donald F., et al, *Engineering Fluid Mechanics*, 10th ed., 2012. Reproduced with permission of John Wiley & Sons, Inc.

P = pressure

P_{atm} = atmospheric pressure

P_C = pressure at the centroid of area

P_{CP} = pressure at center of pressure

y_C = slant distance from liquid surface to the centroid of area

$y_C = h_C / \sin \theta$

h_C = vertical distance from liquid surface to centroid of area

y_{CP} = slant distance from liquid surface to center of pressure

h_{CP} = vertical distance from liquid surface to center of pressure

θ = angle between liquid surface and edge of submerged surface

I_{x_C} = moment of inertia about the centroidal x-axis

If atmospheric pressure acts above the liquid surface and on the non-wetted side of the submerged surface:

$$y_{\text{CP}} = y_C + I_{x_C} / y_C A$$

$$y_{\text{CP}} = y_C + \rho g \sin \theta I_{x_C} / P_C A$$

$$\text{Wetted side: } F_R = (P_{\text{atm}} + \rho g y_C \sin \theta) A$$

$$P_{\text{atm}} \text{ acting both sides: } F_{R_{\text{net}}} = (\rho g y_C \sin \theta) A$$

Archimedes Principle and Buoyancy

1. The buoyant force exerted on a submerged or floating body is equal to the weight of the fluid displaced by the body.

2. A floating body displaces a weight of fluid equal to its own weight; i.e., a floating body is in equilibrium.

The *center of buoyancy* is located at the centroid of the displaced fluid volume.

In the case of a body lying at the *interface of two immiscible fluids*, the buoyant force equals the sum of the weights of the fluids displaced by the body.

PRINCIPLES OF ONE-DIMENSIONAL FLUID FLOW

The Continuity Equation

So long as the flow Q is continuous, the *continuity equation*, as applied to one-dimensional flows, states that the flow passing two points (1 and 2) in a stream is equal at each point, $A_1 v_1 = A_2 v_2$.

$$Q = Av$$

$$\dot{m} = \rho Q = \rho Av, \text{ where}$$

Q = volumetric flow rate

\dot{m} = mass flow rate

A = cross-sectional area of flow

v = average flow velocity

ρ = the fluid density

For steady, one-dimensional flow, \dot{m} is a constant. If, in addition, the density is constant, then Q is constant.

The Energy Equation

The energy equation for steady incompressible flow with no shaft device is

$$\frac{P_1}{\gamma} + z_1 + \frac{v_1^2}{2g} = \frac{P_2}{\gamma} + z_2 + \frac{v_2^2}{2g} + h_f \text{ or}$$

$$\frac{P_1}{\rho g} + z_1 + \frac{v_1^2}{2g} = \frac{P_2}{\rho g} + z_2 + \frac{v_2^2}{2g} + h_f$$

h_f = the head loss, considered a friction effect, and all remaining terms are defined above.

If the cross-sectional area and the elevation of the pipe are the same at both sections (1 and 2), then $z_1 = z_2$ and $v_1 = v_2$.

The pressure drop $P_1 - P_2$ is given by the following:

$$P_1 - P_2 = \gamma h_f = \rho g h_f$$

The Field Equation

The field equation is derived when the energy equation is applied to one-dimensional flows. Assuming no friction losses and that no pump or turbine exists between sections 1 and 2 in the system,

$$\frac{P_2}{\gamma} + \frac{v_2^2}{2g} + z_2 = \frac{P_1}{\gamma} + \frac{v_1^2}{2g} + z_1 \text{ or}$$

$$\frac{P_2}{\rho} + \frac{v_2^2}{2} + z_2 g = \frac{P_1}{\rho} + \frac{v_1^2}{2} + z_1 g, \text{ where}$$

P_1, P_2 = pressure at sections 1 and 2

v_1, v_2 = average velocity of the fluid at the sections

z_1, z_2 = the vertical distance from a datum to the sections (the potential energy)

γ = the specific weight of the fluid (ρg)

g = the acceleration of gravity

ρ = fluid density

Hydraulic Gradient (Grade Line)

Hydraulic grade line is the line connecting the sum of pressure and elevation heads at different points in conveyance systems. If a row of piezometers were placed at intervals along the pipe, the grade line would join the water levels in the piezometer water columns.

Energy Line (Bernoulli Equation)

The Bernoulli equation states that the sum of the pressure, velocity, and elevation heads is constant. The energy line is this sum or the "total head line" above a horizontal datum. The difference between the hydraulic grade line and the energy line is the $v^2/2g$ term.

FLUID FLOW CHARACTERIZATION

Reynolds Number

$$Re = vD\rho/\mu = vD/\nu$$

$$Re' = \frac{v^{(2-n)} D^n \rho}{K \left(\frac{3n+1}{4n}\right)^n 8^{(n-1)}}, \text{ where}$$

ρ = the mass density

D = the diameter of the pipe, dimension of the fluid streamline, or characteristic length

μ = the dynamic viscosity

ν = the kinematic viscosity

Re = the Reynolds number (Newtonian fluid)

Re' = the Reynolds number (Power law fluid)

K and n are defined in the Stress, Pressure, and Viscosity section.

The critical Reynolds number (Re_c) is defined to be the minimum Reynolds number at which a flow will turn turbulent.

Flow through a pipe is generally characterized as laminar for $Re < 2,100$ and fully turbulent for $Re > 10,000$, and transitional flow for $2,100 < Re < 10,000$.

The velocity distribution for *laminar flow* in circular tubes or between planes is

$$v(r) = v_{max} \left[1 - \left(\frac{r}{R} \right)^2 \right], \text{ where}$$

r = the distance (m) from the centerline

R = the radius (m) of the tube or half the distance between the parallel planes

v = the local velocity (m/s) at r

v_{max} = the velocity (m/s) at the centerline of the duct

$v_{max} = 1.18 \bar{v}$, for fully turbulent flow

$v_{max} = 2\bar{v}$, for circular tubes in laminar flow and

$v_{max} = 1.5\bar{v}$, for parallel planes in laminar flow, where

\bar{v} = the average velocity (m/s) in the duct

The shear stress distribution is

$$\frac{\tau}{\tau_w} = \frac{r}{R}, \text{ where}$$

τ and τ_w are the shear stresses at radii r and R respectively.

CONSEQUENCES OF FLUID FLOW

Head Loss Due to Flow

The Darcy-Weisbach equation is

$$h_f = f \frac{L}{D} \frac{v^2}{2g}, \text{ where}$$

f = $f(\text{Re}, \epsilon/D)$, the Moody, Darcy, or Stanton friction factor

D = diameter of the pipe

L = length over which the pressure drop occurs

ϵ = roughness factor for the pipe, and other symbols are defined as before

An alternative formulation employed by chemical engineers is

$$h_f = (4f_{\text{Fanning}}) \frac{Lv^2}{D2g} = \frac{2f_{\text{Fanning}} Lv^2}{Dg}$$

$$\text{Fanning friction factor, } f_{\text{Fanning}} = \frac{f}{4}$$

A chart that gives f versus Re for various values of ϵ/D , known as a *Moody, Darcy, or Stanton diagram*, is available in this section.

Minor Losses in Pipe Fittings, Contractions, and Expansions

Head losses also occur as the fluid flows through pipe fittings (i.e., elbows, valves, couplings, etc.) and sudden pipe contractions and expansions.

$$\frac{P_1}{\gamma} + z_1 + \frac{v_1^2}{2g} = \frac{P_2}{\gamma} + z_2 + \frac{v_2^2}{2g} + h_f + h_{f, \text{fitting}}$$

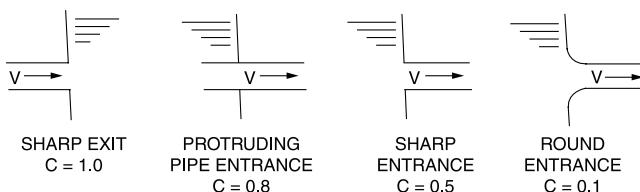
$$\frac{P_1}{\rho g} + z_1 + \frac{v_1^2}{2g} = \frac{P_2}{\rho g} + z_2 + \frac{v_2^2}{2g} + h_f + h_{f, \text{fitting}}, \text{ where}$$

$$h_{f, \text{fitting}} = C \frac{v^2}{2g}, \text{ and } \frac{v^2}{2g} = 1 \text{ velocity head}$$

Specific fittings have characteristic values of C , which will be provided in the problem statement. A generally accepted *nominal value* for head loss in *well-streamlined gradual contractions* is

$$h_{f, \text{fitting}} = 0.04 v^2 / 2g$$

The *head loss* at either an *entrance* or *exit* of a pipe from or to a reservoir is also given by the $h_{f, \text{fitting}}$ equation. Values for C for various cases are shown as follows.



Bober, W., and R.A. Kenyon, *Fluid Mechanics*, Wiley, 1980. Diagrams reprinted by permission of William Bober and Richard A. Kenyon.

Pressure Drop for Laminar Flow

The equation for Q in terms of the pressure drop ΔP_f is the Hagen-Poiseuille equation. This relation is valid only for flow in the laminar region.

$$Q = \frac{\pi R^4 \Delta P_f}{8 \mu L} = \frac{\pi D^4 \Delta P_f}{128 \mu L}$$

Flow in Noncircular Conduits

Analysis of flow in conduits having a noncircular cross section uses the *hydraulic radius* R_H , or the *hydraulic diameter* D_H , as follows:

$$R_H = \frac{\text{cross-sectional area}}{\text{wetted perimeter}} = \frac{D_H}{4}$$

Drag Force

The *drag force* F_D on objects immersed in a large body of flowing fluid or objects moving through a stagnant fluid is

$$F_D = \frac{C_D \rho v^2 A}{2}, \text{ where}$$

C_D = the *drag coefficient*,

v = the velocity (m/s) of the flowing fluid or moving object, and

A = the *projected area* (m^2) of blunt objects such as spheres, ellipsoids, disks, and plates, cylinders, ellipses, and air foils with axes perpendicular to the flow.

ρ = fluid density

For flat plates placed parallel with the flow:

$$C_D = 1.33/\text{Re}^{0.5} (10^4 < \text{Re} < 5 \times 10^5)$$

$$C_D = 0.031/\text{Re}^{1/7} (10^6 < \text{Re} < 10^9)$$

The characteristic length in the Reynolds Number (Re) is the length of the plate parallel with the flow. For blunt objects, the characteristic length is the largest linear dimension (diameter of cylinder, sphere, disk, etc.) that is perpendicular to the flow.

CHARACTERISTICS OF SELECTED FLOW CONFIGURATIONS

Open-Channel Flow and/or Pipe Flow of Water

Manning's Equation

$$v = (K/n) R_H^{2/3} S^{1/2}, \text{ where}$$

v = velocity (m/s, ft/sec)

K = 1.0 for SI units, 1.486 for USCS units

n = roughness coefficient

R_H = hydraulic radius (m, ft)

S = slope of energy grade line (m/m, ft/ft)

Hazen-Williams Equation

$$v = k_1 C R_H^{0.63} S^{0.54}, \text{ where}$$

k_1 = 0.849 for SI units, 1.318 for USCS units

C = roughness coefficient, as tabulated in the Civil Engineering section. Other symbols are defined as before.

Flow Through a Packed Bed

A porous, fixed bed of solid particles can be characterized by

L = length of particle bed (m)

D_p = average particle diameter (m)

Φ_s = sphericity of particles, dimensionless (0–1)

ε = porosity or void fraction of the particle bed, dimensionless (0–1)

The Ergun equation can be used to estimate pressure loss through a packed bed under laminar and turbulent flow conditions.

$$\frac{\Delta P}{L} = \frac{150v_o\mu(1-\varepsilon)^2}{\Phi_s^2 D_p^2 \varepsilon^3} + \frac{1.75\rho v_o^2(1-\varepsilon)}{\Phi_s D_p \varepsilon^3}$$

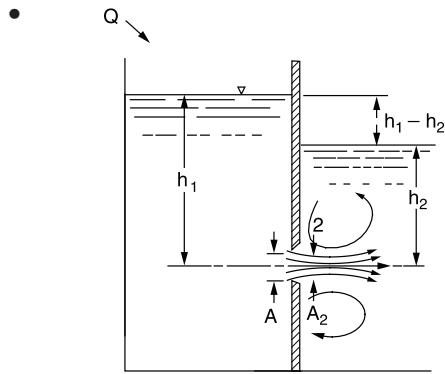
ΔP = pressure loss across packed bed (Pa)

v_o = superficial (flow through empty vessel) fluid velocity (m/s)

ρ = fluid density (kg/m^3)

μ = fluid viscosity [$\text{kg}/(\text{m}\cdot\text{s})$]

Submerged Orifice operating under steady-flow conditions:



$$Q = A_2 v_2 = C_c C_v A \sqrt{2g(h_1 - h_2)}$$

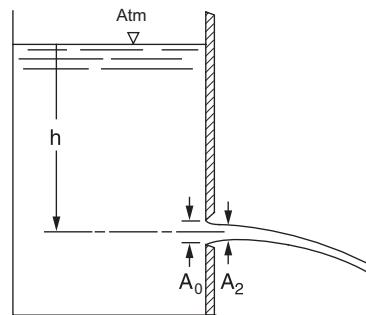
$$= CA \sqrt{2g(h_1 - h_2)}$$

in which the product of C_c and C_v is defined as the *coefficient of discharge* of the orifice.

v_2 = velocity of fluid exiting orifice

Orifice Discharging Freely into Atmosphere

-



$$Q = CA_0 \sqrt{2gh}$$

in which h is measured from the liquid surface to the centroid of the orifice opening.

Q = volumetric flow

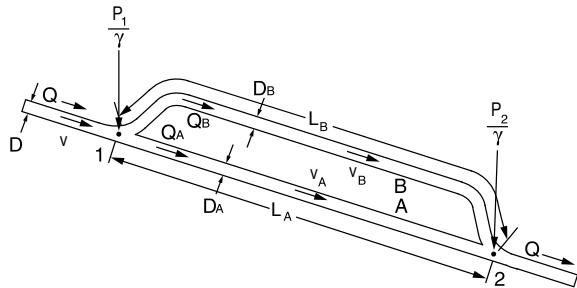
A_0 = cross-sectional area of flow

g = acceleration of gravity

h = height of fluid above orifice

Multipath Pipeline Problems

-



For pipes in parallel, the head loss is the same in each pipe.

$$h_L = f_A \frac{L_A}{D_A} \frac{v_A^2}{2g} = f_B \frac{L_B}{D_B} \frac{v_B^2}{2g}$$

$$(\pi D^2/4)v = (\pi D_A^2/4)v_A + (\pi D_B^2/4)v_B$$

The total flow rate Q is the sum of the flow rates in the parallel pipes.

THE IMPULSE-MOMENTUM PRINCIPLE

The resultant force in a given direction acting on the fluid equals the rate of change of momentum of the fluid.

$$\Sigma F = \Sigma Q_2 \rho_2 v_2 - \Sigma Q_1 \rho_1 v_1, \text{ where}$$

ΣF = the resultant of all external forces acting on the control volume

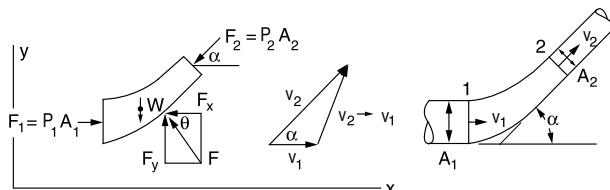
$\Sigma Q_1 \rho_1 v_1$ = the rate of momentum of the fluid flow entering the control volume in the same direction of the force

$\Sigma Q_2 \rho_2 v_2$ = the rate of momentum of the fluid flow leaving the control volume in the same direction of the force

- Vennard, J.K., *Elementary Fluid Mechanics*, 6th ed., J.K. Vennard, 1954.

Pipe Bends, Enlargements, and Contractions

The force exerted by a flowing fluid on a bend, enlargement, or contraction in a pipeline may be computed using the impulse-momentum principle.



$$P_1 A_1 - P_2 A_2 \cos \alpha - F_x = Q \rho (v_2 \cos \alpha - v_1)$$

$$F_y - W - P_2 A_2 \sin \alpha = Q \rho (v_2 \sin \alpha - 0), \text{ where}$$

F = the force exerted by the bend on the fluid (the force exerted by the fluid on the bend is equal in magnitude and opposite in sign), F_x and F_y are the x -component and y -component of the force $F = \sqrt{F_x^2 + F_y^2}$ and
 $\theta = \tan^{-1}\left(\frac{F_y}{F_x}\right)$.

P = the internal pressure in the pipe line

A = the cross-sectional area of the pipe line

W = the weight of the fluid

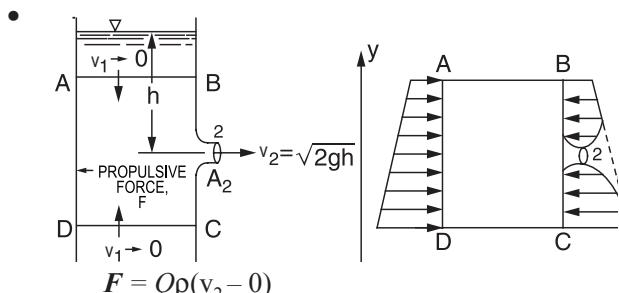
v = the velocity of the fluid flow

α = the angle the pipe bend makes with the horizontal

ρ = the density of the fluid

Q = the quantity of fluid flow

Jet Propulsion



$$F = 2\gamma h A_2, \text{ where}$$

F = the propulsive force

γ = the specific weight of the fluid

h = the height of the fluid above the outlet

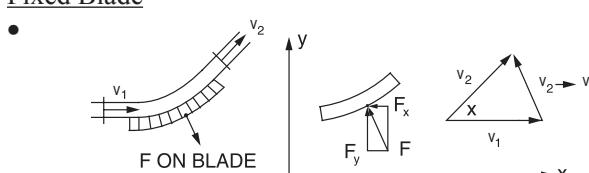
A_2 = the area of the nozzle tip

$$Q = A_2 \sqrt{2gh}$$

$$v_2 = \sqrt{2gh}$$

Deflectors and Blades

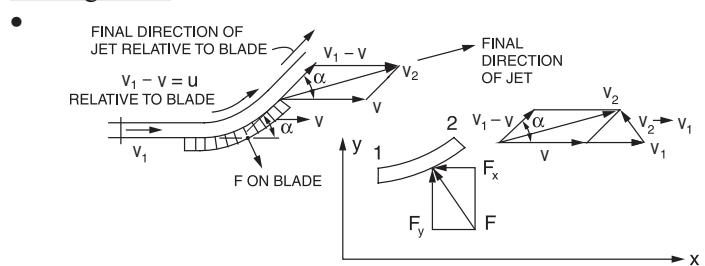
Fixed Blade



$$-F_x = Q\rho(v_2 \cos \alpha - v_1)$$

$$F_y = Q\rho(v_2 \sin \alpha - 0)$$

Moving Blade

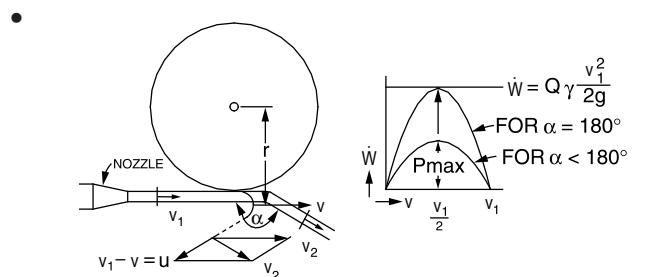


$$-F_x = Q\rho(v_{2x} - v_{1x}) \\ = -Q\rho(v_1 - v)(1 - \cos \alpha)$$

$$F_y = Q\rho(v_{2y} - v_{1y}) \\ = +Q\rho(v_1 - v) \sin \alpha, \text{ where}$$

v = the velocity of the blade.

Impulse Turbine



$$\dot{W} = Q\rho(v_1 - v)(1 - \cos \alpha)v, \text{ where}$$

\dot{W} = power of the turbine.

$$\dot{W}_{\max} = Q\rho(v_1^2/4)(1 - \cos \alpha)$$

When $\alpha = 180^\circ$,

$$\dot{W}_{\max} = (Q\rho v_1^2)/2 = (Q\gamma v_1^2)/2g$$

COMPRESSIBLE FLOW

Mach Number

The local speed of sound in an ideal gas is given by:

$$c = \sqrt{kRT}, \text{ where}$$

c = local speed of sound

$$k = \text{ratio of specific heats} = \frac{c_p}{c_v}$$

$$R = \text{specific gas constant} = \bar{R}/(\text{molecular weight})$$

$$T = \text{absolute temperature}$$

This shows that the acoustic velocity in an ideal gas depends only on its temperature. The *Mach number* (Ma) is the ratio of the fluid velocity to the speed of sound.

$$\text{Ma} \equiv \frac{V}{c}$$

V = mean fluid velocity

• Vennard, J.K., *Elementary Fluid Mechanics*, 6th ed., J.K. Vennard, 1954.

Isentropic Flow Relationships

In an ideal gas for an isentropic process, the following relationships exist between static properties at any two points in the flow.

$$\frac{P_2}{P_1} = \left(\frac{T_2}{T_1} \right)^{\frac{k}{(k-1)}} = \left(\frac{\rho_2}{\rho_1} \right)^k$$

The stagnation temperature, T_0 , at a point in the flow is related to the static temperature as follows:

$$T_0 = T + \frac{V^2}{2 \cdot c_p}$$

Energy relation between two points:

$$h_1 + \frac{V_1^2}{2} = h_2 + \frac{V_2^2}{2}$$

The relationship between the static and stagnation properties (T_0 , P_0 , and ρ_0) at any point in the flow can be expressed as a function of the Mach number as follows:

$$\frac{T_0}{T} = 1 + \frac{k-1}{2} \cdot Ma^2$$

$$\frac{P_0}{P} = \left(\frac{T_0}{T} \right)^{\frac{k}{(k-1)}} = \left(1 + \frac{k-1}{2} \cdot Ma^2 \right)^{\frac{k}{(k-1)}}$$

$$\frac{\rho_0}{\rho} = \left(\frac{T_0}{T} \right)^{\frac{1}{(k-1)}} = \left(1 + \frac{k-1}{2} \cdot Ma^2 \right)^{\frac{1}{(k-1)}}$$

Compressible flows are often accelerated or decelerated through a nozzle or diffuser. For subsonic flows, the velocity decreases as the flow cross-sectional area increases and vice versa. For supersonic flows, the velocity increases as the flow cross-sectional area increases and decreases as the flow cross-sectional area decreases. The point at which the Mach number is sonic is called the throat and its area is represented by the variable, A^* . The following area ratio holds for any Mach number.

$$\frac{A}{A^*} = \frac{1}{Ma} \left[\frac{1 + \frac{1}{2}(k-1)Ma^2}{\frac{1}{2}(k+1)} \right]^{\frac{(k+1)}{2(k-1)}}$$

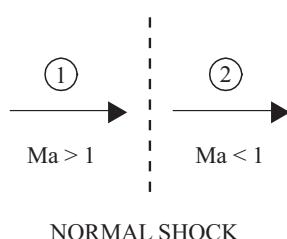
where

$$A \equiv \text{area [length}^2]$$

$$A^* \equiv \text{area at the sonic point (Ma = 1.0)}$$

Normal Shock Relationships

A normal shock wave is a physical mechanism that slows a flow from supersonic to subsonic. It occurs over an infinitesimal distance. The flow upstream of a normal shock wave is always supersonic and the flow downstream is always subsonic as depicted in the figure.



The following equations relate downstream flow conditions to upstream flow conditions for a normal shock wave.

$$Ma_2 = \sqrt{\frac{(k-1)Ma_1^2 + 2}{2k Ma_1^2 - (k-1)}}$$

$$\frac{T_2}{T_1} = \left[2 + (k-1)Ma_1^2 \right] \frac{2k Ma_1^2 - (k-1)}{(k+1)^2 Ma_1^2}$$

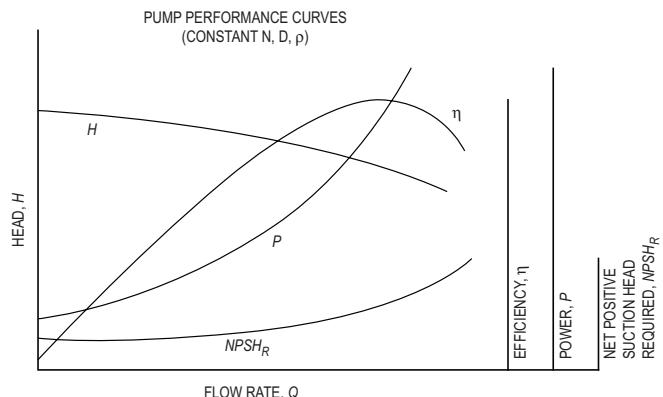
$$\frac{P_2}{P_1} = \frac{1}{k+1} \left[2k Ma_1^2 - (k-1) \right]$$

$$\frac{\rho_2}{\rho_1} = \frac{V_1}{V_2} = \frac{(k+1)Ma_1^2}{(k-1)Ma_1^2 + 2}$$

$$T_{01} = T_{02}$$

FLUID FLOW MACHINERY

Centrifugal Pump Characteristics



Net Positive Suction Head Available ($NPSH_A$)

$$NPSH_A = H_{pa} + H_s - \sum h_L - H_{vp} = \frac{P_{inlet}}{\rho g} + \frac{v_{inlet}^2}{2g} - \frac{P_{vapor}}{\rho g}$$

where,

H_{pa} = the atmospheric pressure head on the surface of the liquid in the sump (ft or m)

H_s = static suction head of liquid. This is height of the surface of the liquid above the centerline of the pump impeller (ft or m)

$\sum h_L$ = total friction losses in the suction line (ft or m)

H_{vp} = the vapor pressure head of the liquid at the operating temperature (ft or m)

v = fluid velocity at pump inlet

P_{vapor} = fluid vapor pressure at pump inlet

ρ = fluid density

g = gravitational constant

Fluid power $\dot{W}_{fluid} = \rho g H Q$

Pump (brake) power $\dot{W} = \frac{\rho g H Q}{\eta_{pump}}$

Purchased power $\dot{W}_{purchased} = \frac{\dot{W}}{\eta_{motor}}$

η_{pump} = pump efficiency (0 to 1)

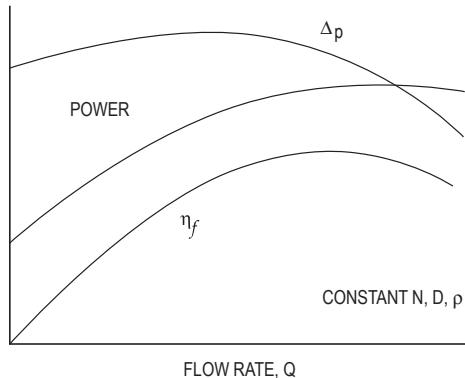
η_{motor} = motor efficiency (0 to 1)

H = head increase provided by pump

Pump Power Equation

- $\dot{W} = Q\gamma h/\eta_t = Qogh/\eta_t$, where
 Q = volumetric flow (m^3/s or cfs)
 h = head (m or ft) the fluid has to be lifted
 η_t = total efficiency ($\eta_{\text{pump}} \times \eta_{\text{motor}}$)
 \dot{W} = power ($\text{kg}\cdot\text{m}^2/\text{sec}^3$ or ft-lbf/sec)

Fan Characteristics



Typical Backward Curved Fans

$$\dot{W} = \frac{\Delta P Q}{\eta_f}, \text{ where}$$

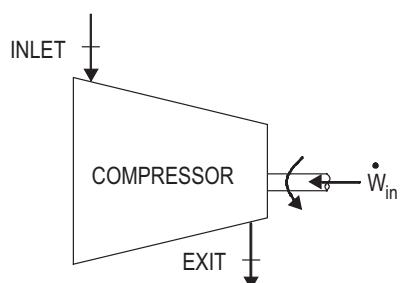
\dot{W} = fan power

ΔP = pressure rise

η_f = fan efficiency

Compressors

Compressors consume power to add energy to the working fluid. This energy addition results in an increase in fluid pressure (head).



For an adiabatic compressor with $\Delta PE = 0$ and negligible ΔKE :

$$\dot{W}_{\text{comp}} = -\dot{m}(h_e - h_i)$$

For an ideal gas with constant specific heats:

$$\dot{W}_{\text{comp}} = -\dot{m}c_p(T_e - T_i)$$

Per unit mass:

$$w_{\text{comp}} = -c_p(T_e - T_i)$$

Compressor Isentropic Efficiency

$$\eta_c = \frac{w_s}{w_a} = \frac{T_{es} - T_i}{T_e - T_i} \text{ where,}$$

w_a ≡ actual compressor work per unit mass

w_s ≡ isentropic compressor work per unit mass

T_{es} ≡ isentropic exit temperature

For a compressor where ΔKE is included:

$$\begin{aligned} \dot{W}_{\text{comp}} &= -\dot{m} \left(h_e - h_i + \frac{V_e^2 - V_i^2}{2} \right) \\ &= -\dot{m} \left(c_p(T_e - T_i) + \frac{V_e^2 - V_i^2}{2} \right) \end{aligned}$$

Adiabatic Compression

$$\dot{W}_{\text{comp}} = \frac{\dot{m} P_i k}{(k - 1)\rho_i \eta_c} \left[\left(\frac{P_e}{P_i} \right)^{1 - 1/k} - 1 \right]$$

\dot{W}_{comp} = fluid or gas power (W)

P_i = inlet or suction pressure (N/m^2)

P_e = exit or discharge pressure (N/m^2)

k = ratio of specific heats = c_p/c_v

ρ_i = inlet gas density (kg/m^3)

η_c = isentropic compressor efficiency

Isothermal Compression

$$\dot{W}_{\text{comp}} = \frac{\bar{R}T_i}{M\eta_c} \ln \frac{P_e}{P_i} (\dot{m})$$

\dot{W}_{comp} , P_i , P_e , and η_c as defined for adiabatic compression

\bar{R} = universal gas constant

T_i = inlet temperature of gas (K)

M = molecular weight of gas (kg/kmol)

♦ Blowers

$$P_w = \frac{WRT_1}{Cne} \left[\left(\frac{P_2}{P_1} \right)^{0.283} - 1 \right]$$

C = 29.7 (constant for SI unit conversion)

= 550 ft-lb/(sec-hp) (U.S. Customary Units)

P_w = power requirement (hp)

W = weight of flow of air (lb/sec)

R = engineering gas constant for air = 53.3 ft-lb/(lb air-°R)

T_1 = absolute inlet temperature (°R)

P_1 = absolute inlet pressure (lbf/in²)

P_2 = absolute outlet pressure (lbf/in²)

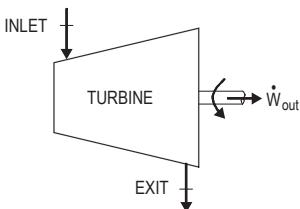
n = $(k - 1)/k = 0.283$ for air

e = efficiency (usually $0.70 < e < 0.90$)

♦ Metcalf and Eddy, *Wastewater Engineering: Treatment, Disposal, and Reuse*, 3rd ed., McGraw-Hill, 1991.

Turbines

Turbines produce power by extracting energy from a working fluid. The energy loss shows up as a decrease in fluid pressure (head).



For an adiabatic turbine with $\Delta PE = 0$ and negligible ΔKE :

$$\dot{W}_{\text{turb}} = \dot{m}(h_i - h_e)$$

For an ideal gas with constant specific heats:

$$\dot{W}_{\text{turb}} = \dot{m}c_p(T_i - T_e)$$

Per unit mass:

$$w_{\text{turb}} = c_p(T_i - T_e)$$

Turbine Isentropic Efficiency

$$\eta_T = \frac{w_a}{w_s} = \frac{T_i - T_e}{T_i - T_{es}}$$

For a turbine where ΔKE is included:

$$\begin{aligned}\dot{W}_{\text{turb}} &= \dot{m}\left(h_e - h_i + \frac{V_e^2 - V_i^2}{2}\right) \\ &= \dot{m}\left(c_p(T_e - T_i) + \frac{V_e^2 - V_i^2}{2}\right)\end{aligned}$$

Performance of Components

Fans, Pumps, and Compressors

Scaling Laws; Affinity Laws

$$\begin{aligned}\left(\frac{\mathcal{Q}}{ND^3}\right)_2 &= \left(\frac{\mathcal{Q}}{ND^3}\right)_1 \\ \left(\frac{\dot{m}}{\rho ND^3}\right)_2 &= \left(\frac{\dot{m}}{\rho ND^3}\right)_1 \\ \left(\frac{H}{N^2 D^2}\right)_2 &= \left(\frac{H}{N^2 D^2}\right)_1 \\ \left(\frac{P}{\rho N^2 D^2}\right)_2 &= \left(\frac{P}{\rho N^2 D^2}\right)_1 \\ \left(\frac{\dot{W}}{\rho N^3 D^5}\right)_2 &= \left(\frac{\dot{W}}{\rho N^3 D^5}\right)_1\end{aligned}$$

where

\mathcal{Q} = volumetric flow rate

\dot{m} = mass flow rate

H = head

P = pressure rise

\dot{W} = power

ρ = fluid density

N = rotational speed

D = impeller diameter

Subscripts 1 and 2 refer to different but similar machines or to different operating conditions of the same machine.

FLUID FLOW MEASUREMENT

The Pitot Tube – From the stagnation pressure equation for an *incompressible fluid*,

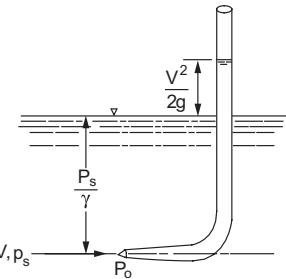
$$v = \sqrt{(2/\rho)(P_0 - P_s)} = \sqrt{2g(P_0 - P_s)/\gamma}, \text{ where}$$

v = the velocity of the fluid

P_0 = the stagnation pressure

P_s = the static pressure of the fluid at the elevation where the measurement is taken

-



For a *compressible fluid*, use the above incompressible fluid equation if the Mach number ≤ 0.3 .

Venturi Meters

$$Q = \frac{C_v A_2}{\sqrt{1 - (A_2/A_1)^2}} \sqrt{2g\left(\frac{P_1}{\gamma} + z_1 - \frac{P_2}{\gamma} - z_2\right)}, \text{ where}$$

Q = volumetric flow rate

C_v = the coefficient of velocity

A = cross-sectional area of flow

P = pressure

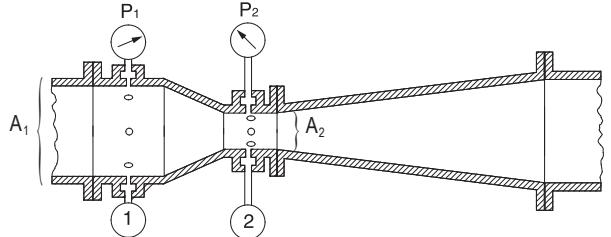
γ = ρg

z_1 = elevation of venturi entrance

z_2 = elevation of venturi throat

The above equation is for *incompressible fluids*.

-

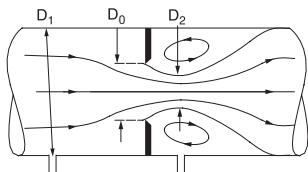


- Vennard, J.K., *Elementary Fluid Mechanics*, 6th ed., J.K. Vennard, 1954.

Orifices

The cross-sectional area at the vena contracta A_2 is characterized by a *coefficient of contraction* C_c and given by $C_c A$.

-



$$Q = C A_0 \sqrt{2g \left(\frac{P_1}{\gamma} + z_1 - \frac{P_2}{\gamma} - z_2 \right)}$$

where C , the *coefficient of the meter (orifice coefficient)*, is given by

$$C = \frac{C_v C_c}{\sqrt{1 - C_c^2 (A_0/A_1)^2}}$$

- ♦

ORIFICES AND THEIR NOMINAL COEFFICIENTS				
	SHARP EDGED	ROUNDED	SHORT TUBE	BORDA
C	0.61	0.98	0.80	0.51
C_c	0.62	1.00	1.00	0.52
C_v	0.98	0.98	0.80	0.98

For incompressible flow through a horizontal orifice meter installation

$$Q = C A_0 \sqrt{\frac{2}{\rho} (P_1 - P_2)}$$

DIMENSIONAL HOMOGENEITY

Dimensional Analysis

A dimensionally homogeneous equation has the same dimensions on the left and right sides of the equation. Dimensional analysis involves the development of equations that relate dimensionless groups of variables to describe physical phenomena.

Buckingham Pi Theorem: The *number of independent dimensionless groups* that may be employed to describe a phenomenon known to involve n variables is equal to the number $(n - r)$, where r is the number of basic dimensions (e.g., M, L, T) needed to express the variables dimensionally.

Similitude

In order to use a model to simulate the conditions of the prototype, the model must be *geometrically, kinematically, and dynamically similar* to the prototype system.

To obtain dynamic similarity between two flow pictures, all independent force ratios that can be written must be the same in both the model and the prototype. Thus, dynamic similarity between two flow pictures (when all possible forces are acting) is expressed in the five simultaneous equations below.

$$\left[\frac{F_I}{F_P} \right]_p = \left[\frac{F_I}{F_P} \right]_m = \left[\frac{\rho v^2}{P} \right]_p = \left[\frac{\rho v^2}{P} \right]_m$$

$$\left[\frac{F_I}{F_V} \right]_p = \left[\frac{F_I}{F_V} \right]_m = \left[\frac{v l \rho}{\mu} \right]_p = \left[\frac{v l \rho}{\mu} \right]_m = [Re]_p = [Re]_m$$

$$\left[\frac{F_I}{F_G} \right]_p = \left[\frac{F_I}{F_G} \right]_m = \left[\frac{v^2}{l g} \right]_p = \left[\frac{v^2}{l g} \right]_m = [Fr]_p = [Fr]_m$$

$$\left[\frac{F_I}{F_E} \right]_p = \left[\frac{F_I}{F_E} \right]_m = \left[\frac{\rho v^2}{E_v} \right]_p = \left[\frac{\rho v^2}{E_v} \right]_m = [Ca]_p = [Ca]_m$$

$$\left[\frac{F_I}{F_T} \right]_p = \left[\frac{F_I}{F_T} \right]_m = \left[\frac{\rho l v^2}{\sigma} \right]_p = \left[\frac{\rho l v^2}{\sigma} \right]_m = [We]_p = [We]_m$$

where the subscripts p and m stand for *prototype* and *model* respectively, and

F_I = inertia force

F_P = pressure force

F_V = viscous force

F_G = gravity force

F_E = elastic force

F_T = surface tension force

Re = Reynolds number

We = Weber number

Ca = Cauchy number

Fr = Froude number

l = characteristic length

v = velocity

ρ = density

σ = surface tension

E_v = bulk modulus

μ = dynamic viscosity

P = pressure

g = acceleration of gravity

♦ Bober, W., and R.A. Kenyon, *Fluid Mechanics*, Wiley, 1980. Diagrams reprinted by permission of William Bober and Richard A. Kenyon.

• Vennard, J.K., *Elementary Fluid Mechanics*, 6th ed., J.K. Vennard, 1954.

AERODYNAMICS

Airfoil Theory

The lift force on an airfoil, F_L , is given by

$$F_L = \frac{C_L \rho v^2 A_p}{2}$$

C_L = the lift coefficient

ρ = fluid density

v = velocity (m/s) of the undisturbed fluid and

A_p = the projected area of the airfoil as seen from above (plan area). This same area is used in defining the drag coefficient for an airfoil.

The lift coefficient, C_L , can be approximated by the equation

$C_L = 2\pi k_1 \sin(\alpha + \beta)$, which is valid for small values of α and β

k_1 = a constant of proportionality

α = angle of attack (angle between chord of airfoil and direction of flow)

β = negative of angle of attack for zero lift

The drag coefficient, C_D , may be approximated by

$$C_D = C_{D\infty} + \frac{C_L^2}{\pi AR}$$

$C_{D\infty}$ = infinite span drag coefficient

The aspect ratio, AR , is defined

$$AR = \frac{b^2}{A_p} = \frac{A_p}{c^2}$$

b = span length

A_p = plan area

c = chord length

The aerodynamic moment, M , is given by

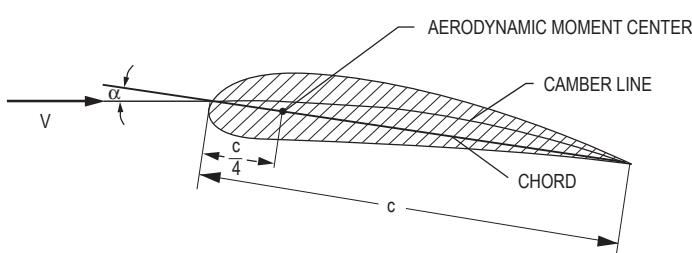
$$M = \frac{C_M \rho v^2 A_p c}{2}$$

where the moment is taken about the front quarter point of the airfoil.

C_M = moment coefficient

ρ = fluid density

v = velocity



♦ Properties of Water^f (SI Metric Units)

Temperature (°C)	Specific Weight ^a γ (kN/m ³)	Density ^a ρ (kg/m ³)	Absolute Dynamic Viscosity ^a μ (Pa•s)	Kinematic Viscosity ^a ν (m ² /s)	Vapor Pressure ^e P_v (kPa)
0	9.805	999.8	0.001781	0.000001785	0.61
5	9.807	1000.0	0.001518	0.000001518	0.87
10	9.804	999.7	0.001307	0.000001306	1.23
15	9.798	999.1	0.001139	0.000001139	1.70
20	9.789	998.2	0.001002	0.000001003	2.34
25	9.777	997.0	0.000890	0.000000893	3.17
30	9.764	995.7	0.000798	0.000000800	4.24
40	9.730	992.2	0.000653	0.000000658	7.38
50	9.689	988.0	0.000547	0.000000553	12.33
60	9.642	983.2	0.000466	0.000000474	19.92
70	9.589	977.8	0.000404	0.000000413	31.16
80	9.530	971.8	0.000354	0.000000364	47.34
90	9.466	965.3	0.000315	0.000000326	70.10
100	9.399	958.4	0.000282	0.000000294	101.33

♦ Properties of Water (English Units)

Temperature (°F)	Specific Weight γ (lbf/ft ³)	Mass Density ρ (lbf•sec ² /ft ⁴)	Absolute Dynamic Viscosity μ ($\times 10^{-5}$ lbf•sec/ft ²)	Kinematic Viscosity ν ($\times 10^{-5}$ ft ² /sec)	Vapor Pressure P_v (psi)
32	62.42	1.940	3.746	1.931	0.09
40	62.43	1.940	3.229	1.664	0.12
50	62.41	1.940	2.735	1.410	0.18
60	62.37	1.938	2.359	1.217	0.26
70	62.30	1.936	2.050	1.059	0.36
80	62.22	1.934	1.799	0.930	0.51
90	62.11	1.931	1.595	0.826	0.70
100	62.00	1.927	1.424	0.739	0.95
110	61.86	1.923	1.284	0.667	1.24
120	61.71	1.918	1.168	0.609	1.69
130	61.55	1.913	1.069	0.558	2.22
140	61.38	1.908	0.981	0.514	2.89
150	61.20	1.902	0.905	0.476	3.72
160	61.00	1.896	0.838	0.442	4.74
170	60.80	1.890	0.780	0.413	5.99
180	60.58	1.883	0.726	0.385	7.51
190	60.36	1.876	0.678	0.362	9.34
200	60.12	1.868	0.637	0.341	11.52
212	59.83	1.860	0.593	0.319	14.70

♦^aFrom "Hydraulic Models," ASCE Manual of Engineering Practice, No. 25, ASCE, 1942.

^bFrom J.H. Keenan and F.G. Keyes, *Thermodynamic Properties of Steam*, John Wiley & Sons, 1936.

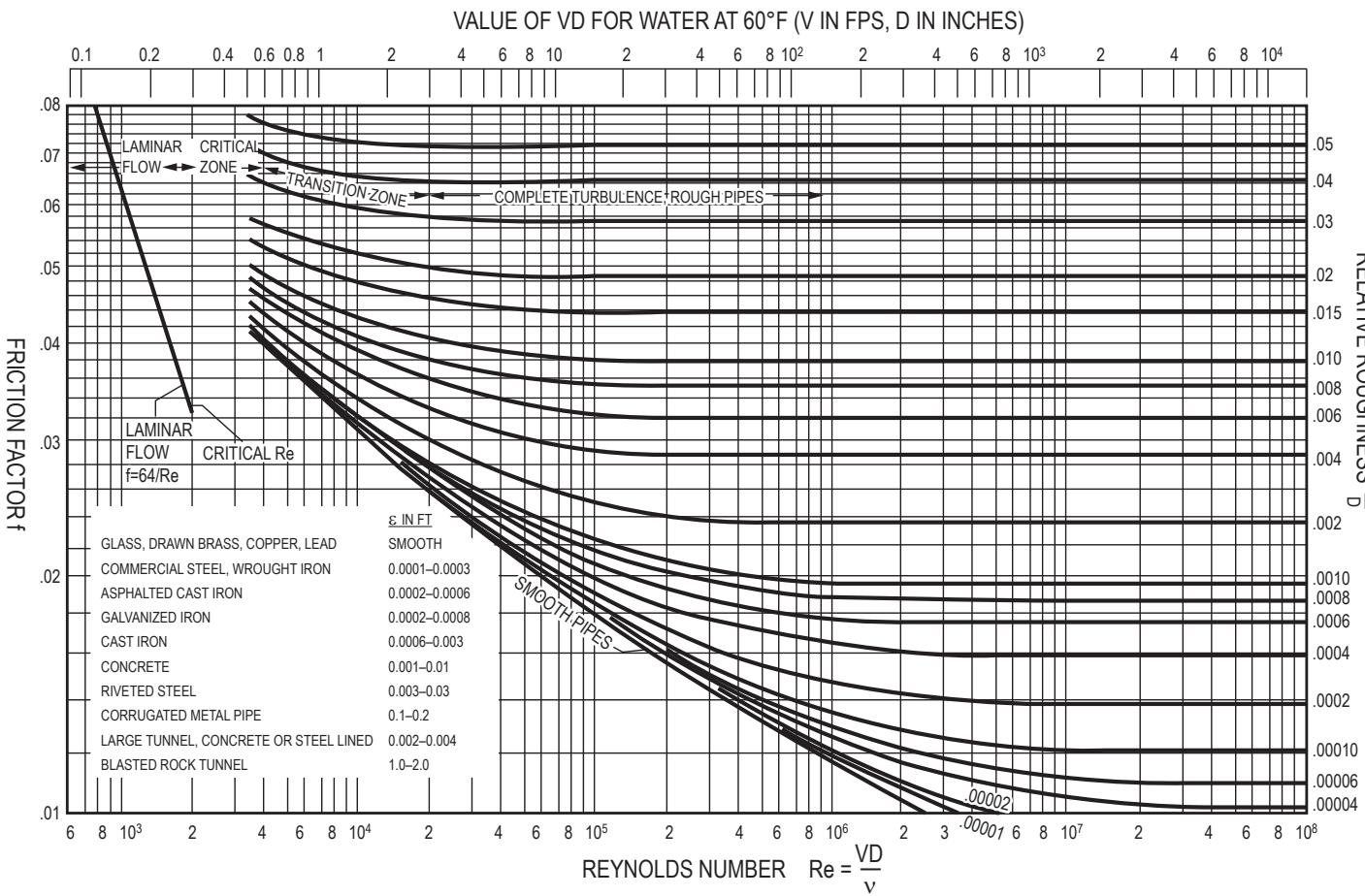
^cCompiled from many sources including those indicated: *Handbook of Chemistry and Physics*, 54th ed.,

The CRC Press, 1973, and *Handbook of Tables for Applied Engineering Science*, The Chemical Rubber Co., 1970.

Vennard, J.K. and Robert L. Street, *Elementary Fluid Mechanics*, 6th ed., 1982. Reproduced with permission of John Wiley & Sons.

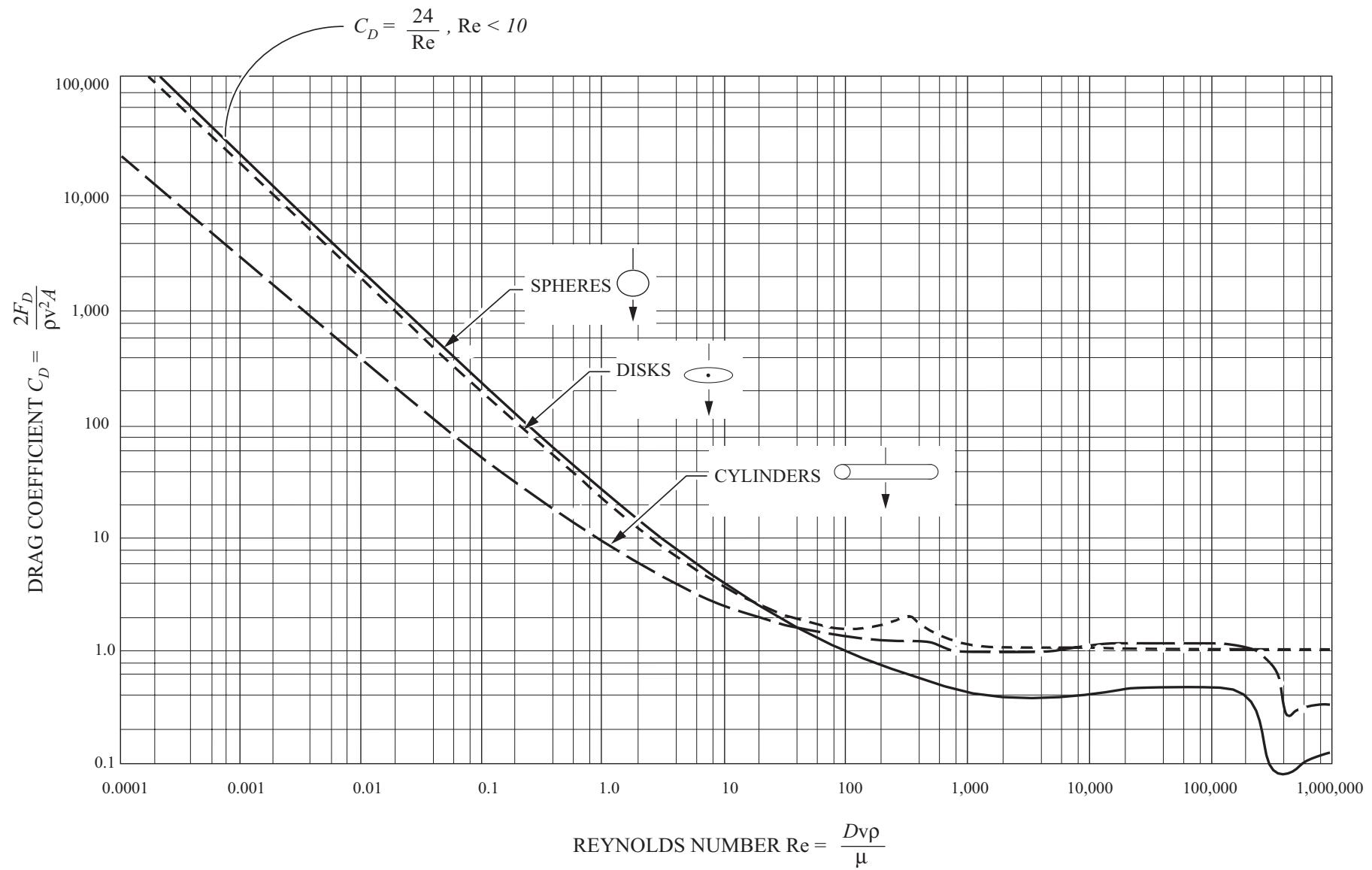
Moody (Stanton) Diagram

FLOW IN CLOSED CONDUITS



Chow, Ven Te, *Handbook of Applied Hydrology*, McGraw-Hill, 1964.

Drag Coefficient for Spheres, Disks, and Cylinders



HEAT TRANSFER

There are three modes of heat transfer: conduction, convection, and radiation.

BASIC HEAT TRANSFER RATE EQUATIONS

Conduction

Fourier's Law of Conduction

$$\dot{Q} = -kA \frac{dT}{dx}, \text{ where}$$

\dot{Q} = rate of heat transfer (W)

k = the thermal conductivity [W/(m•K)]

A = the surface area perpendicular to direction of heat transfer (m^2)

Convection

Newton's Law of Cooling

$$\dot{Q} = hA(T_w - T_\infty), \text{ where}$$

h = the convection heat transfer coefficient of the fluid [W/(m²•K)]

A = the convection surface area (m^2)

T_w = the wall surface temperature (K)

T_∞ = the bulk fluid temperature (K)

Radiation

The radiation emitted by a body is given by

$$\dot{Q} = \varepsilon\sigma AT^4, \text{ where}$$

ε = the emissivity of the body

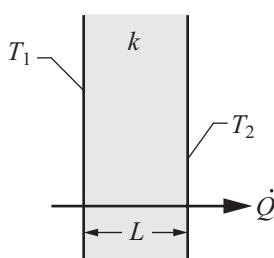
σ = the Stefan-Boltzmann constant
= $5.67 \times 10^{-8} \text{ W}/(\text{m}^2 \cdot \text{K}^4)$

A = the body surface area (m^2)

T = the absolute temperature (K)

CONDUCTION

Conduction Through a Plane Wall



$$\dot{Q} = \frac{-kA(T_2 - T_1)}{L}, \text{ where}$$

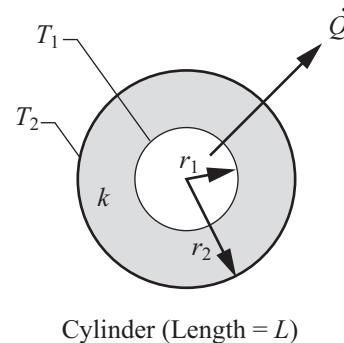
A = wall surface area normal to heat flow (m^2)

L = wall thickness (m)

T_1 = temperature of one surface of the wall (K)

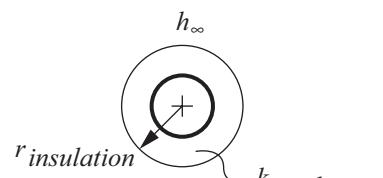
T_2 = temperature of the other surface of the wall (K)

Conduction Through a Cylindrical Wall



Critical Insulation Radius

$$r_{cr} = \frac{k_{insulation}}{h_\infty}$$



Thermal Resistance (R)

$$\dot{Q} = \frac{\Delta T}{R_{total}}$$

Resistances in series are added: $R_{total} = \sum R$, where

Plane Wall Conduction Resistance (K/W): $R = \frac{L}{kA}$, where

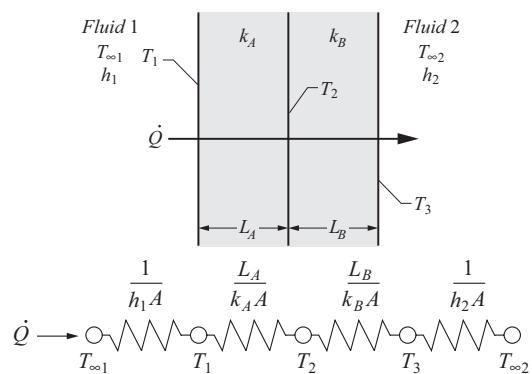
L = wall thickness

Cylindrical Wall Conduction Resistance (K/W): $R = \frac{\ln(\frac{r_2}{r_1})}{2\pi kL}$, where

L = cylinder length

Convection Resistance (K/W) : $R = \frac{1}{hA}$

Composite Plane Wall



To evaluate surface or intermediate temperatures:

$$\dot{Q} = \frac{T_1 - T_2}{R_A} = \frac{T_2 - T_3}{R_B}$$

Transient Conduction Using the Lumped Capacitance Model

The lumped capacitance model is valid if

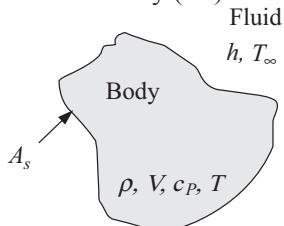
$$\text{Biot number, Bi} = \frac{hV}{kA_s} \ll 1, \text{ where}$$

h = the convection heat transfer coefficient of the fluid [W/(m²•K)]

V = the volume of the body (m³)

k = thermal conductivity of the body [W/(m•K)]

A_s = the surface area of the body (m²)



Constant Fluid Temperature

If the temperature may be considered uniform within the body at any time, the heat transfer rate at the body surface is given by

$$\dot{Q} = hA_s(T - T_\infty) = -\rho V(c_P) \left(\frac{dT}{dt} \right), \text{ where}$$

T = the body temperature (K)

T_∞ = the fluid temperature (K)

ρ = the density of the body (kg/m³)

c_P = the heat capacity of the body [J/(kg•K)]

t = time (s)

The temperature variation of the body with time is

$$T - T_\infty = (T_i - T_\infty) e^{-\beta t}, \text{ where}$$

$$\beta = \frac{hA_s}{\rho V c_P} \quad \text{where } \beta = \frac{1}{\tau} \text{ and} \\ \tau = \text{time constant (s)}$$

The total heat transferred (\dot{Q}_{total}) up to time t is

$$\dot{Q}_{total} = \rho V c_P (T_i - T), \text{ where}$$

T_i = initial body temperature (K)

Fins

For a straight fin with uniform cross section (assuming negligible heat transfer from tip),

$$\dot{Q} = \sqrt{hP k A_c} (T_b - T_\infty) \tanh(mL_c), \text{ where}$$

h = the convection heat transfer coefficient of the fluid [W/(m²•K)]

P = perimeter of exposed fin cross section (m)

k = fin thermal conductivity [W/(m•K)]

A_c = fin cross-sectional area (m²)

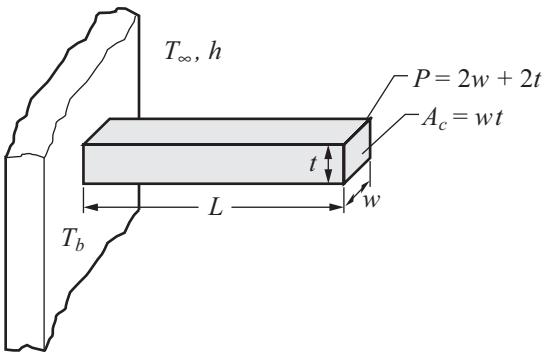
T_b = temperature at base of fin (K)

T_∞ = fluid temperature (K)

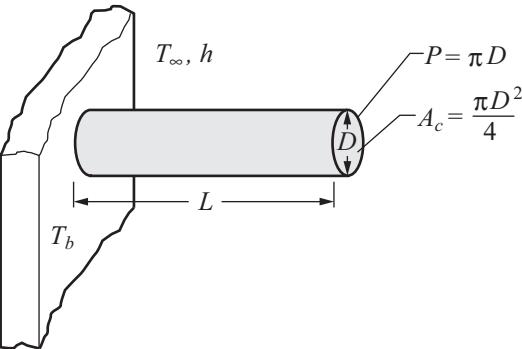
$$m = \sqrt{\frac{hP}{kA_c}}$$

$L_c = L + \frac{A_c}{P}$, corrected length of fin (m)

Rectangular Fin



Pin Fin



CONVECTION

Terms

D = diameter (m)

\bar{h} = average convection heat transfer coefficient of the fluid [W/(m²•K)]

L = length (m)

\overline{Nu} = average Nusselt number

Pr = Prandtl number = $\frac{c_P \mu}{k}$

u_m = mean velocity of fluid (m/s)

u_∞ = free stream velocity of fluid (m/s)

μ = dynamic viscosity of fluid [kg/(s•m)]

ρ = density of fluid (kg/m³)

External Flow

In all cases, evaluate fluid properties at average temperature between that of the body and that of the flowing fluid.

Flat Plate of Length L in Parallel Flow

$$Re_L = \frac{\rho u_\infty L}{\mu}$$

$$\overline{Nu}_L = \frac{\bar{h}L}{k} = 0.6640 Re_L^{1/2} Pr^{1/3} \quad (Re_L < 10^5)$$

$$\overline{Nu}_L = \frac{\bar{h}L}{k} = 0.0366 Re_L^{0.8} Pr^{1/3} \quad (Re_L > 10^5)$$

Cylinder of Diameter D in Cross Flow

$$Re_D = \frac{\rho u_\infty D}{\mu}$$

$$\overline{Nu}_D = \frac{\bar{h}D}{k} = C Re_D^n Pr^{1/3}, \text{ where}$$

Re_D	C	n
1 – 4	0.989	0.330
4 – 40	0.911	0.385
40 – 4,000	0.683	0.466
4,000 – 40,000	0.193	0.618
40,000 – 250,000	0.0266	0.805

Flow Over a Sphere of Diameter, D

$$\overline{Nu}_D = \frac{\bar{h}D}{k} = 2.0 + 0.60 Re_D^{1/2} Pr^{1/3},$$

($1 < Re_D < 70,000$; $0.6 < Pr < 400$)

Internal Flow

$$Re_D = \frac{\rho u_m D}{\mu}$$

Laminar Flow in Circular Tubes

For laminar flow ($Re_D < 2300$), fully developed conditions

$$Nu_D = 4.36 \quad (\text{uniform heat flux})$$

$$Nu_D = 3.66 \quad (\text{constant surface temperature})$$

For laminar flow ($Re_D < 2300$), combined entry length with constant surface temperature

$$Nu_D = 1.86 \left(\frac{Re_D Pr}{L/D} \right)^{1/3} \left(\frac{\mu_b}{\mu_s} \right)^{0.14}, \text{ where}$$

L = length of tube (m)

D = tube diameter (m)

μ_b = dynamic viscosity of fluid [$\text{kg}/(\text{s}\cdot\text{m})$] at bulk temperature of fluid, T_b

μ_s = dynamic viscosity of fluid [$\text{kg}/(\text{s}\cdot\text{m})$] at inside surface temperature of the tube, T_s

Turbulent Flow in Circular Tubes

For turbulent flow ($Re_D > 10^4$, $Pr > 0.7$) for either uniform surface temperature or uniform heat flux condition, Sieder-Tate equation offers good approximation:

$$Nu_D = 0.023 Re_D^{0.8} Pr^{1/3} \left(\frac{\mu_b}{\mu_s} \right)^{0.14}$$

Noncircular Ducts

In place of the diameter, D , use the equivalent (hydraulic) diameter (D_H) defined as

$$D_H = \frac{4 \times \text{cross-sectional area}}{\text{wetted perimeter}}$$

Circular Annulus ($D_o \geq D_i$)

In place of the diameter, D , use the equivalent (hydraulic) diameter (D_H) defined as

$$D_H = D_o - D_i$$

Liquid Metals ($0.003 < Pr < 0.05$)

$$Nu_D = 6.3 + 0.0167 Re_D^{0.85} Pr^{0.93} \quad (\text{uniform heat flux})$$

$$Nu_D = 7.0 + 0.025 Re_D^{0.8} Pr^{0.8} \quad (\text{constant wall temperature})$$

Boiling

Evaporation occurring at a solid-liquid interface when $T_{\text{solid}} > T_{\text{sat, liquid}}$

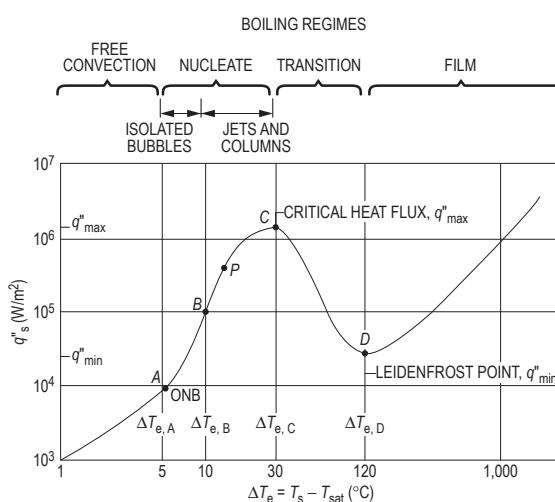
$$q'' = h(T_s - T_{\text{sat}}) = h\Delta T_e, \text{ where } \Delta T_e = \text{excess temperature}$$

Pool Boiling – Liquid is quiescent; motion near solid surface is due to free convection and mixing induced by bubble growth and detachment.

Forced Convection Boiling – Fluid motion is induced by external means in addition to free convection and bubble-induced mixing.

Sub-Cooled Boiling – Temperature of liquid is below saturation temperature; bubbles forming at surface may condense in the liquid.

Saturated Boiling – Liquid temperature slightly exceeds the saturation temperature; bubbles forming at the surface are propelled through liquid by buoyancy forces.



Typical boiling curve for water at one atmosphere: surface heat flux q''_s as a function of excess temperature, $\Delta T_e = T_s - T_{\text{sat}}$

Free Convection Boiling – Insufficient vapor is in contact with the liquid phase to cause boiling at the saturation temperature.

Nucleate Boiling – Isolated bubbles form at nucleation sites and separate from surface; vapor escapes as jets or columns.

◆ Incropera, Frank P. and David P. DeWitt, *Fundamentals of Heat and Mass Transfer*, 3rd ed., Wiley, 1990. Reproduced with permission of John Wiley & Sons, Inc.

- ◆ For nucleate boiling a widely used correlation was proposed in 1952 by Rohsenow:

$$\dot{q}_{\text{nucleate}} = \mu_l h_{fg} \left[\frac{g(\rho_l - \rho_v)}{\sigma} \right]^{1/2} \left[\frac{c_{pl}(T_s - T_{\text{sat}})}{C_{sf} h_{fg} \text{Pr}_l^n} \right]^3$$

$\dot{q}_{\text{nucleate}}$	= nucleate boiling heat flux, W/m ²
μ_l	= viscosity of the liquid, kg/(m•s)
h_{fg}	= enthalpy of vaporization, J/kg
g	= gravitational acceleration, m/s ²
ρ_l	= density of the liquid, kg/m ³
ρ_v	= density of the vapor, kg/m ³
σ	= surface tension of liquid–vapor interface, N/m
c_{pl}	= specific heat of the liquid, J/(kg•°C)
T_s	= surface temperature of the heater, °C
T_{sat}	= saturation temperature of the fluid, °C
C_{sf}	= experimental constant that depends on surface–fluid combination
Pr_l	= Prandtl number of the liquid
n	= experimental constant that depends on the fluid

◆ Peak Heat Flux

The maximum (or critical) heat flux (CHF) in nucleate pool boiling:

$$\dot{q}_{\text{max}} = C_{cr} h_{fg} \left[\sigma g \rho_v^2 (\rho_l - \rho_v) \right]^{1/4}$$

C_{cr} is a constant whose value depends on the heater geometry, but generally is about 0.15.

The CHF is independent of the fluid–heating surface combination, as well as the viscosity, thermal conductivity, and specific heat of the liquid.

The CHF increases with pressure up to about one-third of the critical pressure, and then starts to decrease and becomes zero at the critical pressure.

The CHF is proportional to h_{fg} , and large maximum heat fluxes can be obtained using fluids with a large enthalpy of vaporization, such as water.

◆

Values of the coefficient C_{cr} for maximum heat flux (dimensionless parameter $L^* = L[g(\rho_l - \rho_v)/\sigma]^{1/2}$)

Heater Geometry	C_{cr}	Charac. Dimension of Heater, L	Range of L^*
Large horizontal flat heater	0.149	Width or diameter	$L^* > 27$
Small horizontal flat heater ¹	$18.9 K_1$	Width or diameter	$9 < L^* < 20$
Large horizontal cyclinder	0.12	Radius	$L^* > 1.2$
Small horizontal cyclinder	$0.12 L^{*-0.25}$	Radius	$0.15 < L^* < 1.2$
Large sphere	0.11	Radius	$L^* > 4.26$
Small sphere	$0.227 L^{*-0.5}$	Radius	$0.15 < L^* < 4.26$

¹ $K_1 = \sigma/[g(\rho_l - \rho_v)A_{\text{heater}}]$

◆ Minimum Heat Flux

Minimum heat flux, which occurs at the Leidenfrost point, is of practical interest since it represents the lower limit for the heat flux in the film boiling regime.

Zuber derived the following expression for the minimum heat flux for a large horizontal plate

$$\dot{q}_{\min} = 0.09 \rho_v h_{fg} \left[\frac{\sigma g (\rho_l - \rho_v)}{(\rho_l + \rho_v)^2} \right]^{1/4}$$

The relation above can be in error by 50% or more.

Transition Boiling – Rapid bubble formation results in vapor film on surface and oscillation between film and nucleate boiling.

Film Boiling – Surface completely covered by vapor blanket; includes significant radiation through vapor film.

◆ Film Boiling

The heat flux for film boiling on a horizontal cylinder or sphere of diameter D is given by

$$\dot{q}_{\text{film}} = C_{\text{film}} \left[\frac{g k_v^3 \rho_v (\rho_l - \rho_v) [h_{fg} + 0.4 c_{pv} (T_s - T_{\text{sat}})]}{\mu_v D (T_s - T_{\text{sat}})} \right]^{1/4} (T_s - T_{\text{sat}})$$

$$C_{\text{film}} = \begin{cases} 0.62 & \text{for horizontal cylinders} \\ 0.67 & \text{for spheres} \end{cases}$$

Film Condensation of a Pure Vapor On a Vertical Surface

$$\overline{Nu}_L = \frac{\overline{h}L}{k_l} = 0.943 \left[\frac{\rho_l^2 g h_{fg} L^3}{\mu_l k_l (T_{\text{sat}} - T_s)} \right]^{0.25}, \text{ where}$$

ρ_l = density of liquid phase of fluid (kg/m³)

g = gravitational acceleration (9.81 m/s²)

h_{fg} = latent heat of vaporization [J/kg]

L = length of surface [m]

μ_l = dynamic viscosity of liquid phase of fluid [kg/(s•m)]

k_l = thermal conductivity of liquid phase of fluid [W/(m•K)]

T_{sat} = saturation temperature of fluid [K]

T_s = temperature of vertical surface [K]

Note: Evaluate all liquid properties at the average temperature between the saturated temperature, T_{sat} , and the surface temperature, T_s .

Outside Horizontal Tubes

$$\overline{Nu}_D = \frac{\overline{h}D}{k} = 0.729 \left[\frac{\rho_l^2 g h_{fg} D^3}{\mu_l k_l (T_{\text{sat}} - T_s)} \right]^{0.25}, \text{ where}$$

D = tube outside diameter (m)

Note: Evaluate all liquid properties at the average temperature between the saturated temperature, T_{sat} , and the surface temperature, T_s .

◆ Cengel, Yunus A., and Afshin J. Ghajar, *Heat and Mass Transfer*, 4th ed., McGraw-Hill, 2011.

Natural (Free) Convection

Vertical Flat Plate in Large Body of Stationary Fluid

Equation also can apply to vertical cylinder of sufficiently large diameter in large body of stationary fluid.

$$\bar{h} = C \left(\frac{k}{L} \right) Ra_L^n, \text{ where}$$

L = the length of the plate (cylinder) in the vertical direction

$$Ra_L = \text{Rayleigh Number} = \frac{g\beta(T_s - T_\infty)L^3}{\nu^2} \Pr$$

T_s = surface temperature (K)

T_∞ = fluid temperature (K)

β = coefficient of thermal expansion (1/K)

(For an ideal gas: $\beta = \frac{2}{T_s + T_\infty}$ with T in absolute temperature)

ν = kinematic viscosity (m^2/s)

Range of Ra_L	C	n
$10^4 - 10^9$	0.59	1/4
$10^9 - 10^{13}$	0.10	1/3

Long Horizontal Cylinder in Large Body of Stationary Fluid

$$\bar{h} = C \left(\frac{k}{D} \right) Ra_D^n, \text{ where}$$

$$Ra_D = \frac{g\beta(T_s - T_\infty)D^3}{\nu^2} \Pr$$

Ra_D	C	n
$10^{-3} - 10^2$	1.02	0.148
$10^2 - 10^4$	0.850	0.188
$10^4 - 10^7$	0.480	0.250
$10^7 - 10^{12}$	0.125	0.333

Heat Exchangers

The rate of heat transfer in a heat exchanger is

$$\dot{Q} = UAF\Delta T_{lm}, \text{ where}$$

A = any convenient reference area (m^2)

F = correction factor for log mean temperature difference for more complex heat exchangers (shell and tube arrangements with several tube or shell passes or cross-flow exchangers with mixed and unmixed flow); otherwise $F = 1$.

U = overall heat transfer coefficient based on area A and the log mean temperature difference [$\text{W}/(\text{m}^2 \cdot \text{K})$]

ΔT_{lm} = log mean temperature difference (K)

Overall Heat Transfer Coefficient for Concentric Tube and Shell-and-Tube Heat Exchangers

$\frac{1}{UA} = \frac{1}{h_i A_i} + \frac{R_{fi}}{A_i} + \frac{\ln\left(\frac{D_o}{D_i}\right)}{2\pi k L} + \frac{R_{fo}}{A_o} + \frac{1}{h_o A_o}$, where
A_i = inside area of tubes (m^2)
A_o = outside area of tubes (m^2)
D_i = inside diameter of tubes (m)
D_o = outside diameter of tubes (m)
h_i = convection heat transfer coefficient for inside of tubes [$\text{W}/(\text{m}^2 \cdot \text{K})$]
h_o = convection heat transfer coefficient for outside of tubes [$\text{W}/(\text{m}^2 \cdot \text{K})$]
k = thermal conductivity of tube material [$\text{W}/(\text{m} \cdot \text{K})$]
R_{fi} = fouling factor for inside of tube [$(\text{m}^2 \cdot \text{K})/\text{W}$]
R_{fo} = fouling factor for outside of tube [$(\text{m}^2 \cdot \text{K})/\text{W}$]

Log Mean Temperature Difference (LMTD)

For *counterflow* in tubular heat exchangers

$$\Delta T_{lm} = \frac{(T_{Ho} - T_{Ci}) - (T_{Hi} - T_{Co})}{\ln\left(\frac{T_{Ho} - T_{Ci}}{T_{Hi} - T_{Co}}\right)}$$

For *parallel flow* in tubular heat exchangers

$$\Delta T_{lm} = \frac{(T_{Ho} - T_{Co}) - (T_{Hi} - T_{Ci})}{\ln\left(\frac{T_{Ho} - T_{Co}}{T_{Hi} - T_{Ci}}\right)}, \text{ where}$$

ΔT_{lm} = log mean temperature difference (K)

T_{Hi} = inlet temperature of the hot fluid (K)

T_{Ho} = outlet temperature of the hot fluid (K)

T_{Ci} = inlet temperature of the cold fluid (K)

T_{Co} = outlet temperature of the cold fluid (K)

Heat Exchanger Effectiveness, ε

$$\varepsilon = \frac{\dot{Q}}{\dot{Q}_{max}} = \frac{\text{actual heat transfer rate}}{\text{maximum possible heat transfer rate}}$$

$$\varepsilon = \frac{C_H (T_{Hi} - T_{Ho})}{C_{min} (T_{Hi} - T_{Ci})} \quad \text{or} \quad \varepsilon = \frac{C_C (T_{Co} - T_{Ci})}{C_{min} (T_{Hi} - T_{Ci})}$$

where

$C = mc_p$ = heat capacity rate (W/K)

C_{min} = smaller of C_C or C_H

Number of Transfer Units (NTU)

$$NTU = \frac{UA}{C_{\min}}$$

Effectiveness-NTU Relations

$$C_r = \frac{C_{\min}}{C_{\max}} = \text{heat capacity ratio}$$

For *parallel flow concentric tube* heat exchanger

$$\varepsilon = \frac{1 - \exp[-NTU(1 + C_r)]}{1 + C_r}$$

$$NTU = -\frac{\ln[1 - \varepsilon(1 + C_r)]}{1 + C_r}$$

For *counterflow concentric tube* heat exchanger

$$\varepsilon = \frac{1 - \exp[-NTU(1 - C_r)]}{1 - C_r \exp[-NTU(1 - C_r)]} \quad (C_r < 1)$$

$$\varepsilon = \frac{NTU}{1 + NTU} \quad (C_r = 1)$$

$$NTU = \frac{1}{C_r - 1} \ln\left(\frac{\varepsilon - 1}{\varepsilon C_r - 1}\right) \quad (C_r < 1)$$

$$NTU = \frac{\varepsilon}{1 - \varepsilon} \quad (C_r = 1)$$

RADIATION

Types of Bodies

Any Body

For any body, $\alpha + \rho + \tau = 1$, where

α = absorptivity (ratio of energy absorbed to incident energy)

ρ = reflectivity (ratio of energy reflected to incident energy)

τ = transmissivity (ratio of energy transmitted to incident energy)

Opaque Body

For an opaque body: $\alpha + \rho = 1$

Gray Body

A gray body is one for which

$$\alpha = \varepsilon, (0 < \alpha < 1; 0 < \varepsilon < 1), \text{ where}$$

ε = the emissivity of the body

For a gray body: $\varepsilon + \rho = 1$

Real bodies are frequently approximated as gray bodies.

Black body

A black body is defined as one that absorbs all energy incident upon it. It also emits radiation at the maximum rate for a body of a particular size at a particular temperature. For such a body

$$\alpha = \varepsilon = 1$$

Shape Factor (View Factor, Configuration Factor)

Relations

Reciprocity Relations

$$A_i F_{ij} = A_j F_{ji}, \text{ where}$$

A_i = surface area (m^2) of surface i

F_{ij} = shape factor (view factor, configuration factor); fraction of the radiation leaving surface i that is intercepted by surface j ; $0 \leq F_{ij} \leq 1$

Summation Rule for N Surfaces

$$\sum_{j=1}^N F_{ij} = 1$$

Net Energy Exchange by Radiation between Two Bodies

Body Small Compared to its Surroundings

$$\dot{Q}_{12} = \varepsilon \sigma A (T_1^4 - T_2^4), \text{ where}$$

\dot{Q}_{12} = the net heat transfer rate from the body (W)

ε = the emissivity of the body

σ = the Stefan-Boltzmann constant

$$[\sigma = 5.67 \times 10^{-8} \text{ W}/(\text{m}^2 \cdot \text{K}^4)]$$

A = the body surface area (m^2)

T_1 = the absolute temperature (K) of the body surface

T_2 = the absolute temperature (K) of the surroundings

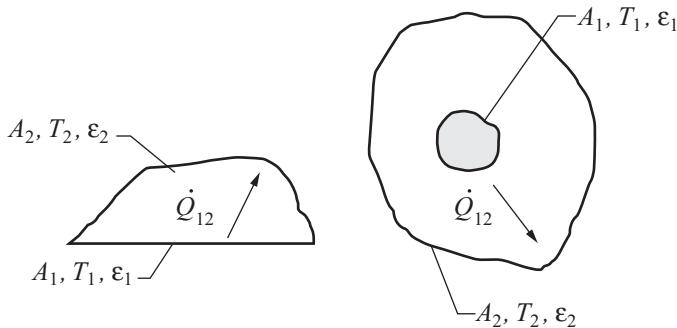
Net Energy Exchange by Radiation between Two Black Bodies

The net energy exchange by radiation between two black bodies that see each other is given by

$$\dot{Q}_{12} = A_1 F_{12} \sigma (T_1^4 - T_2^4)$$

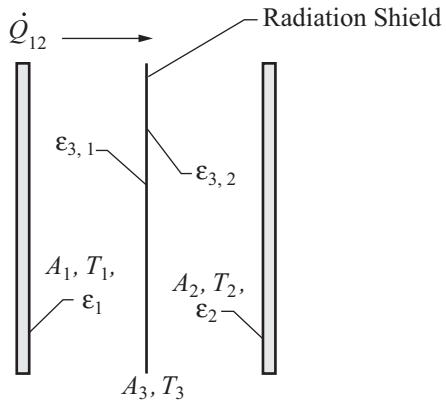
Net Energy Exchange by Radiation between Two Diffuse-Gray Surfaces that Form an Enclosure

Generalized Cases



$$\dot{Q}_{12} = \frac{\sigma(T_1^4 - T_2^4)}{\frac{1-\varepsilon_1}{\varepsilon_1 A_1} + \frac{1}{A_1 F_{12}} + \frac{1-\varepsilon_2}{\varepsilon_2 A_2}}$$

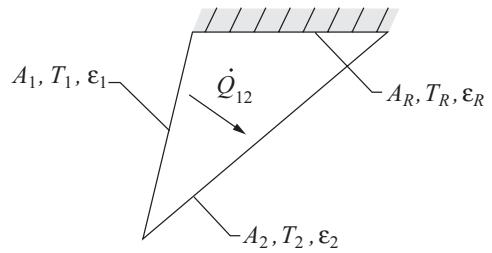
One-Dimensional Geometry with Thin Low-Emissivity Shield Inserted between Two Parallel Plates



$$\dot{Q}_{12} = \frac{\sigma(T_1^4 - T_2^4)}{\frac{1-\varepsilon_1}{\varepsilon_1 A_1} + \frac{1}{A_1 F_{13}} + \frac{1-\varepsilon_{3,1}}{\varepsilon_{3,1} A_3} + \frac{1-\varepsilon_{3,2}}{\varepsilon_{3,2} A_3} + \frac{1}{A_3 F_{32}} + \frac{1-\varepsilon_2}{\varepsilon_2 A_2}}$$

Reradiating Surface

Reradiating Surfaces are considered to be insulated or adiabatic ($\dot{Q}_R = 0$).



$$\dot{Q}_{12} = \frac{\sigma(T_1^4 - T_2^4)}{\frac{1-\varepsilon_1}{\varepsilon_1 A_1} + \frac{1}{A_1 F_{12} + \left[\left(\frac{1}{A_1 F_{1R}} \right) + \left(\frac{1}{A_2 F_{2R}} \right) \right]^{-1}} + \frac{1-\varepsilon_2}{\varepsilon_2 A_2}}$$

INSTRUMENTATION, MEASUREMENT, AND CONTROLS

MEASUREMENT

Definitions

Transducer – a device used to convert a physical parameter such as temperature, pressure, flow, light intensity, etc. into an electrical signal (also called a *sensor*).

Transducer sensitivity – the ratio of change in electrical signal magnitude to the change in magnitude of the physical parameter being measured.

Resistance Temperature Detector (RTD) – a device used to relate change in resistance to change in temperature. Typically made from platinum, the controlling equation for an RTD is given by:

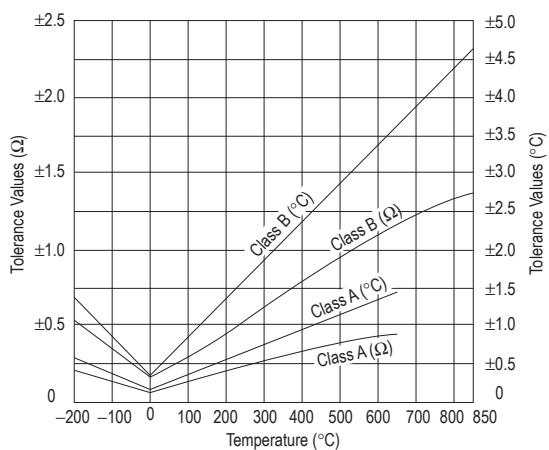
$$R_T = R_0 [1 + \alpha(T - T_0)], \text{ where}$$

R_T = resistance of the RTD at temperature T (in °C)

R_0 = resistance of the RTD at the reference temperature T_0 (usually 0°C)

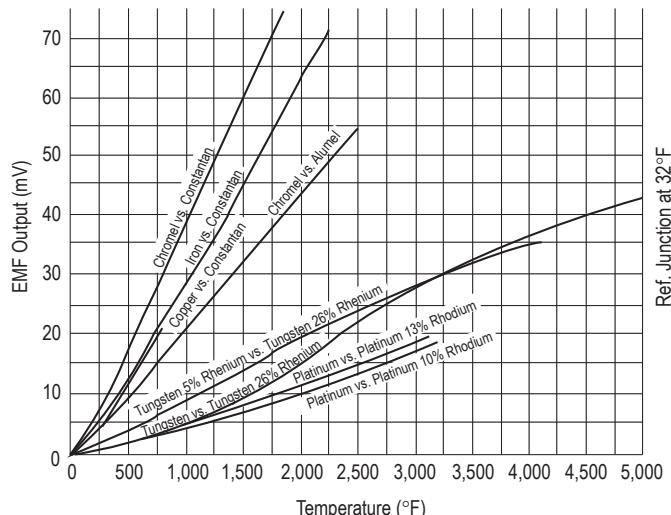
α = temperature coefficient of the RTD

The following graph shows tolerance values as a function of temperature for 100-Ω RTDs.

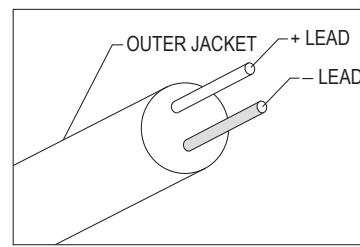


From Tempco Manufactured Products, as posted on www.tempco.com, July 2013.

Thermocouple (TC) – a device used to relate change in voltage to change in temperature. A thermocouple consists of two dissimilar conductors in contact, which produce a voltage when heated.



From Convectronics Inc., as posted on www.convectronics.com, July 2013.



Typical Thermocouple (TC) Cable

From Convectronics Inc., as posted on www.convectronics.com, July 2013.

ANSI Code	Alloy Combination and Color		Outer Jacket Color		Maximum Thermocouple Temperature Range	Environment
	+ Lead	- Lead	Thermocouple Leads	Extension Cable		
J	IRON Fe (magnetic) White	CONSTANTAN COPPER-NICKEL Cu-Ni Red	Brown	Black	-346 to 2,193°F -210 to 1,200°C	Reducing, Vacuum, Inert. Limited use in Oxidizing at High Temperatures. Not Recommended for Low Temperatures
K	NICKELCHROMIUM Ni-Cr Yellow	NICEL-ALUMINUM Ni-Al (magnetic) Red	Brown	Yellow	-454 to 2,501°F -270 to 1,372°C	Clean Oxidizing and Inert. Limited Use in Vacuum or Reducing.
T	COPPER Cu Blue	CONSTANTAN COPPER-NICKEL Cu-Ni Red	Brown	Blue	-454 to 752°F -270 to 400°C	Mild Oxidizing, Reducing Vacuum or Inert. Good where moisture is present.
E	NICKELCHROMIUM Ni-Cr Purple	CONSTANTAN COPPER-NICKEL Cu-Ni Red	Brown	Purple	-454 to 1,832°F -270 to 1,000°C	Oxidizing or Inert. Limited Use in Vacuum or Reducing.

From Omega Engineering, as posted on www.omega.com, July 2013.

Strain Gage – a device whose electrical resistance varies in proportion to the amount of strain in the device.

Gage factor (GF) – the ratio of fractional change in electrical resistance to the fractional change in length (strain):

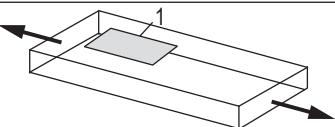
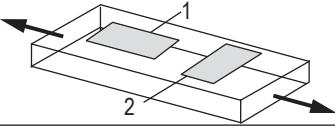
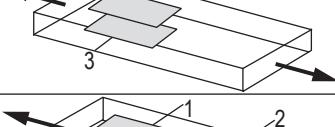
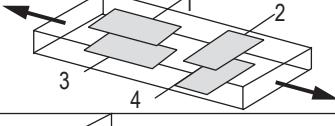
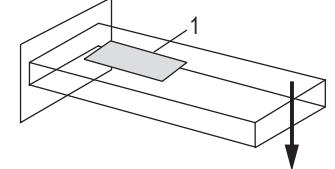
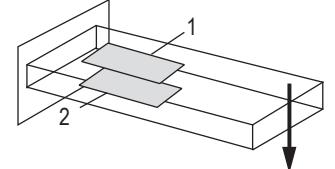
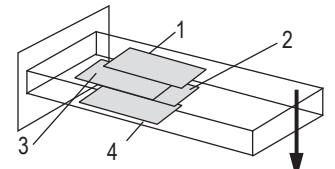
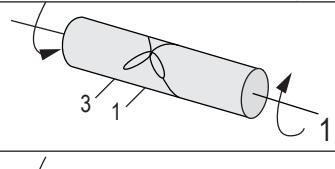
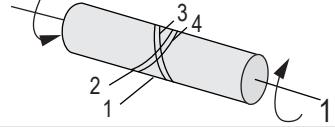
$$GF = \frac{\Delta R/R}{\Delta L/L} = \frac{\Delta R/R}{\varepsilon}, \text{ where}$$

R = nominal resistance of the strain gage at nominal length L

ΔR = change in resistance due the change in length ΔL

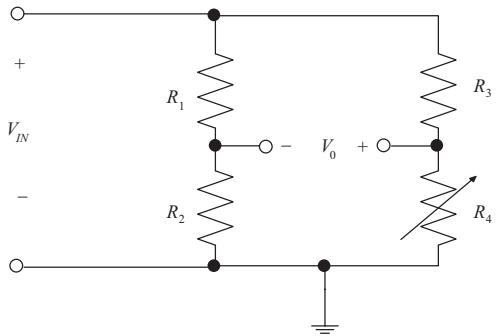
ε = normal strain sensed by the gage

The gage factor for metallic strain gages is typically around 2.

Strain	Gage Setup	Bridge Type	Sensitivity mV/V @ 100 $\mu\varepsilon$	Details
Axial		1/4	0.5	Good: Simplest to implement, but must use a dummy gage if compensating for temperature. Also responds to bending strain.
		1/2	0.65	Better: Temperature compensated, but it is sensitive to bending strain.
		1/2	1.0	Better: Rejects bending strain, but not temperature. Must use dummy gages if compensating for temperature
		Full	1.3	Best: More sensitive and compensates for both temperature and bending strain.
Bending		1/4	0.5	Good: Simplest to implement, but must use a dummy gage if compensating for temperature. Responds equally to axial strain.
		1/2	1.0	Better: Rejects axial strain and is temperature compensated.
		Full	2.0	Best: Rejects axial strain and is temperature compensated. Most sensitive to bending strain.
Torsional and Shear		1/2	1.0	Good: Gages must be mounted at 45 degrees from centerline.
		Full	2.0	Best: Most sensitive full-bridge version of previous setup. Rejects both axial and bending strains.

From National Instruments Corporation, as posted on www.ni.com, July 2013.

Wheatstone Bridge – an electrical circuit used to measure changes in resistance.



WHEATSTONE BRIDGE

If $\frac{R_1}{R_2} = \frac{R_3}{R_4}$ then $V_0 = 0$ V and the bridge is said to be *balanced*.

If $R_1 = R_2 = R_3 = R$ and $R_4 = R + \Delta R$, where $\Delta R \ll R$, then

$$V_0 \approx \frac{\Delta R}{4R} \cdot V_{IN}.$$

◆ *Pressure sensors* – can alternatively be called pressure transducers, pressure transmitters, pressure senders, pressure indicators, piezometers, and manometers.

◆

Pressure Relative Measurement Types	Comparison
Absolute	Relative to 0 Pa, the pressure in a vacuum
Gage	Relative to local atmospheric pressure
Vacuum	Relative to either absolute vacuum (0 Pa) or local atmospheric pressure
Differential	Relative to another pressurized container
Sealed	Relative to sea level pressure

• *pH sensor* – a typical pH meter consists of a special measuring probe connected to an electronic meter that measures and displays the pH reading.

$$E_{el} = E^0 - S(pH_a - pH_i)$$

E_{el} = electrode potential

E^0 = zero potential

S = slope (mV per pH unit)

pH_a = pH value of the measured solution

pH_i = pH value of the internal buffer

◆ From National Instruments Corporation, as posted on www.ni.com, July 2013.

• From Alliance Technical Sales, Inc., as posted on www.alliancets.com, July 2013.

Examples of Common Chemical Sensors

Sensor Type	Principle	Materials	Analyte
Semiconducting oxide sensor	Conductivity impedance	SnO_2 , TiO_2 , ZnO_2 , WO_3 , polymers	O_2 , H_2 , CO, SO_x , NO_x , combustible hydrocarbons, alcohol, H_2S , NH_3
Electrochemical sensor (liquid electrolyte)	Amperometric	composite Pt, Au catalyst	H_2 , O_2 , O_3 , CO, H_2S , SO_2 , NO_x , NH_3 , glucose, hydrazine
Ion-selective electrode (ISE)	Potentiometric	glass, LaF_3 , CaF_2	pH, K^+ , Na^+ , Cl^- , Ca^{2+} , Mg^{2+} , F^- , Ag^+
Solid electrode sensor	Amperometric Potentiometric	YSZ, H^+ -conductor YSZ, β -alumina, Nasicon, Nafion	O_2 , H_2 , CO, combustible hydrocarbons, O_2 , H_2 , CO_2 , CO, NO_x , SO_x , H_2S , Cl_2 , H_2O , combustible hydrocarbons
Piezoelectric sensor	Mechanical w/ polymer film	quartz	combustible hydrocarbons, VOCs
Catalytic combustion sensor	Calorimetric	$\text{Pt}/\text{Al}_2\text{O}_3$, Pt-wire	H_2 , CO, combustible hydrocarbons
Pyroelectric sensor	Calorimetric	Pyroelectric + film	Vapors
Optical sensors	Colorimetric fluorescence	optical fiber/indicator dye	Acids, bases, combustible hydrocarbons, biologicals

Reprinted with permission from *Journal of The Electrochemical Society*, 150 (2), ©2003, The Electrochemical Society.

SAMPLING

When a continuous-time or analog signal is sampled using a discrete-time method, certain basic concepts should be considered. The sampling rate or frequency is given by

$$f_s = \frac{1}{\Delta t}$$

Nyquist's (Shannon's) sampling theorem states that in order to accurately reconstruct the analog signal from the discrete sample points, the sample rate must be larger than twice the highest frequency contained in the measured signal. Denoting this frequency, which is called the Nyquist frequency, as f_N , the sampling theorem requires that

$$f_s > 2f_N$$

When the above condition is not met, the higher frequencies in the measured signal will not be accurately represented and will appear as lower frequencies in the sampled data. These are known as alias frequencies.

Analog-to-Digital Conversion

When converting an analog signal to digital form, the resolution of the conversion is an important factor. For a measured analog signal over the nominal range $[V_L, V_H]$, where V_L is the low end of the voltage range and V_H is the nominal high end of the voltage range, the voltage resolution is given by

$$\varepsilon_V = \frac{V_H - V_L}{2^n}$$

where n is the number of conversion bits of the A/D converter with typical values of 4, 8, 10, 12, or 16. This number is a key design parameter. After converting an analog signal, the A/D converter produces an integer number of n bits. Call this number N . Note that the range of N is $[0, 2^n - 1]$. When calculating the discrete voltage, V , using the reading, N , from the A/D converter the following equation is used.

$$V = \varepsilon_V N + V_L$$

Note that with this strategy, the highest measurable voltage is one voltage resolution less than V_H , or $V_H - \varepsilon_V$.

Signal Conditioning

Signal conditioning of the measured analog signal is often required to prevent alias frequencies from being measured, and to reduce measurement errors.

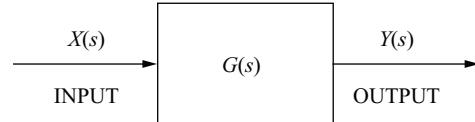
MEASUREMENT UNCERTAINTY

Suppose that a calculated result R depends on measurements whose values are $x_1 \pm w_1, x_2 \pm w_2, x_3 \pm w_3$, etc., where $R = f(x_1, x_2, x_3, \dots, x_n)$, x_i is the measured value, and w_i is the uncertainty in that value. The uncertainty in R , w_R , can be estimated using the Kline-McClintock equation:

$$w_R = \sqrt{\left(w_1 \frac{\partial f}{\partial x_1}\right)^2 + \left(w_2 \frac{\partial f}{\partial x_2}\right)^2 + \dots + \left(w_n \frac{\partial f}{\partial x_n}\right)^2}$$

CONTROL SYSTEMS

The linear time-invariant transfer function model represented by the block diagram

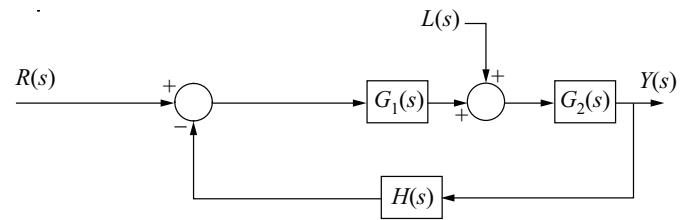


can be expressed as the ratio of two polynomials in the form

$$\frac{Y(s)}{X(s)} = G(s) = \frac{N(s)}{D(s)} = K \frac{\prod_{m=1}^M (s - z_m)}{\prod_{n=1}^N (s - p_n)}$$

where the M zeros, z_m , and the N poles, p_n , are the roots of the numerator polynomial, $N(s)$, and the denominator polynomial, $D(s)$, respectively.

One classical negative feedback control system model block diagram is



where $G_1(s)$ is a controller or compensator, $G_2(s)$ represents a plant model, and $H(s)$ represents the measurement dynamics. $Y(s)$ represents the controlled variable, $R(s)$ represents the reference input, and $L(s)$ represents a disturbance. $Y(s)$ is related to $R(s)$ and $L(s)$ by

$$Y(s) = \frac{G_1(s) G_2(s)}{1 + G_1(s) G_2(s) H(s)} R(s) + \frac{G_2(s)}{1 + G_1(s) G_2(s) H(s)} L(s)$$

$G_1(s) G_2(s) H(s)$ is the open-loop transfer function. The closed-loop characteristic equation is

$$1 + G_1(s) G_2(s) H(s) = 0$$

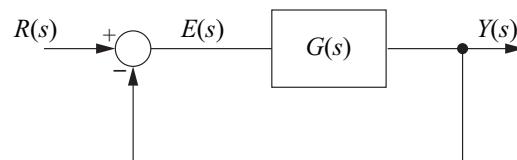
System performance studies normally include

1. Steady-state analysis using constant inputs based on the Final Value Theorem. If all poles of a $G(s)$ function have negative real parts, then

$$\text{dc gain} = \lim_{s \rightarrow 0} G(s)$$

Note that $G(s)$ could refer to either an open-loop or a closed-loop transfer function.

For the unity feedback control system model



with the open-loop transfer function defined by

$$G(s) = \frac{K_B}{s^T} \times \frac{\prod_{m=1}^M (1 + s/\omega_m)}{\prod_{n=1}^N (1 + s/\omega_n)}$$

The following steady-state error analysis table can be constructed where T denotes the type of system, i.e., type 0, type 1, etc.

Steady-State Error e_{ss}				
Input \ Type	$T = 0$	$T = 1$	$T = 2$	
Unit Step	$1/(K_B + 1)$	0	0	
Ramp	∞	$1/K_B$	0	
Acceleration	∞	∞	$1/K_B$	

2. Frequency response evaluations to determine dynamic performance and stability. For example, relative stability can be quantified in terms of

a. Gain margin (GM), which is the additional gain required to produce instability in the unity gain feedback control system. If at $\omega = \omega_{180}$,

$$\angle G(j\omega_{180}) = -180^\circ; \text{ then}$$

$$GM = -20\log_{10}(|G(j\omega_{180})|)$$

b. Phase margin (PM), which is the additional phase required to produce instability. Thus,

$$PM = 180^\circ + \angle G(j\omega_{0dB})$$

where ω_{0dB} is the ω that satisfies $|G(j\omega)| = 1$.

3. Transient responses are obtained by using Laplace transforms or computer solutions with numerical integration.

Common Compensator/Controller forms are

$$\text{PID Controller } G_C(s) = K \left(1 + \frac{1}{T_I s} + T_D s \right)$$

Lag or Lead Compensator $G_C(s) = K \left(\frac{1 + sT_1}{1 + sT_2} \right)$ depending on the ratio of T_1/T_2 .

Routh Test

For the characteristic equation

$$a_n s^n + a_{n-1} s^{n-1} + a_{n-2} s^{n-2} + \dots + a_0 = 0$$

the coefficients are arranged into the first two rows of an array. Additional rows are computed. The array and coefficient computations are defined by:

$$\begin{array}{ccccccc} a_n & a_{n-2} & a_{n-4} & \dots & \dots & \dots \\ a_{n-1} & a_{n-3} & a_{n-5} & \dots & \dots & \dots \\ b_1 & b_2 & b_3 & \dots & \dots & \dots \\ c_1 & c_2 & c_3 & \dots & \dots & \dots \end{array}$$

where

$$b_1 = \frac{a_{n-1}a_{n-2} - a_n a_{n-3}}{a_{n-1}} \quad c_1 = \frac{a_{n-3}b_1 - a_{n-1}b_2}{b_1}$$

$$b_2 = \frac{a_{n-1}a_{n-4} - a_n a_{n-5}}{a_{n-1}} \quad c_2 = \frac{a_{n-5}b_1 - a_{n-1}b_3}{b_1}$$

The necessary and sufficient conditions for all the roots of the equation to have negative real parts is that all the elements in the first column be of the same sign and nonzero.

First-Order Control System Models

The transfer function model for a first-order system is

$$\frac{Y(s)}{R(s)} = \frac{K}{\tau s + 1}, \text{ where}$$

K = steady-state gain

τ = time constant

The step response of a first-order system to a step input of magnitude M is

$$y(t) = y_0 e^{-t/\tau} + KM(1 - e^{-t/\tau})$$

In the chemical process industry, y_0 is typically taken to be zero, and $y(t)$ is referred to as a deviation variable.

For systems with time delay (dead time or transport lag) θ , the transfer function is

$$\frac{Y(s)}{R(s)} = \frac{Ke^{-\theta s}}{\tau s + 1}$$

The step response for $t \geq \theta$ to a step of magnitude M is

$$y(t) = [y_0 e^{-(t-\theta)/\tau} + KM(1 - e^{-(t-\theta)/\tau})] u(t - \theta), \text{ where } u(t) \text{ is the unit step function.}$$

Second-Order Control System Models

One standard second-order control system model is

$$\frac{Y(s)}{R(s)} = \frac{K\omega_n^2}{s^2 + 2\zeta\omega_n s + \omega_n^2}, \text{ where}$$

K = steady-state gain

ζ = the damping ratio

ω_n = the undamped natural ($\zeta = 0$) frequency

$\omega_d = \omega_n \sqrt{1 - \zeta^2}$, the damped natural frequency

$\omega_r = \omega_n \sqrt{1 - 2\zeta^2}$, the damped resonant frequency

If the damping ratio ζ is less than unity, the system is said to be underdamped; if ζ is equal to unity, it is said to be critically damped; and if ζ is greater than unity, the system is said to be overdamped.

For a unit step input to a normalized underdamped second-order control system, the time required to reach a peak value t_p and the value of that peak M_p are given by

$$t_p = \pi / (\omega_n \sqrt{1 - \zeta^2})$$

$$M_p = 1 + e^{-\pi\zeta/\sqrt{1 - \zeta^2}}$$

The percent overshoot (% OS) of the response is given by

$$\% \text{ OS} = 100e^{-\pi\zeta/\sqrt{1 - \zeta^2}}$$

For an underdamped second-order system, the logarithmic decrement is

$$\delta = \frac{1}{m} \ln \left(\frac{x_k}{x_{k+m}} \right) = \frac{2\pi\zeta}{\sqrt{1 - \zeta^2}}$$

where x_k and x_{k+m} are the amplitudes of oscillation at cycles k and $k+m$, respectively. The period of oscillation τ is related to ω_d by

$$\omega_d \tau = 2\pi$$

The time required for the output of a second-order system to settle to within 2% of its final value (2% settling time) is defined to be

$$T_s = \frac{4}{\zeta\omega_n}$$

An alternative form commonly employed in the chemical process industry is

$$\frac{Y(s)}{R(s)} = \frac{K}{\tau^2 s^2 + 2\zeta\tau s + 1}, \text{ where}$$

K = steady-state gain

ζ = the damping ratio

τ = the inverse natural frequency

Root Locus

The root locus is the locus of points in the complex s -plane satisfying

$$1 + K \frac{(s - z_1)(s - z_2) \dots (s - z_m)}{(s - p_1)(s - p_2) \dots (s - p_n)} = 0 \quad m \leq n$$

as K is varied. The p_i and z_j are the open-loop poles and zeros, respectively. When K is increased from zero, the locus has the following properties.

1. Locus branches exist on the real axis to the left of an odd number of open-loop poles and/or zeros.
2. The locus originates at the open-loop poles p_1, \dots, p_n and terminates at the zeros z_1, \dots, z_m . If $m < n$ then $(n - m)$ branches terminate at infinity at asymptote angles

$$\alpha = \frac{(2k + 1)180^\circ}{n - m} \quad k = 0, \pm 1, \pm 2, \pm 3, \dots$$

with the real axis.

3. The intersection of the real axis with the asymptotes is called the asymptote centroid and is given by

$$\sigma_A = \frac{\sum_{i=1}^n \operatorname{Re}(p_i) - \sum_{i=1}^m \operatorname{Re}(z_i)}{n - m}$$

4. If the locus crosses the imaginary (ω) axis, the values of K and ω are given by letting $s = j\omega$ in the defining equation.

State-Variable Control System Models

One common state-variable model for dynamic systems has the form

$$\begin{aligned} \dot{\mathbf{x}}(t) &= \mathbf{A}\mathbf{x}(t) + \mathbf{B}\mathbf{u}(t) && \text{(state equation)} \\ \mathbf{y}(t) &= \mathbf{C}\mathbf{x}(t) + \mathbf{D}\mathbf{u}(t) && \text{(output equation)} \end{aligned}$$

where

$\mathbf{x}(t)$ = N by 1 state vector (N state variables)

$\mathbf{u}(t)$ = R by 1 input vector (R inputs)

$\mathbf{y}(t)$ = M by 1 output vector (M outputs)

A = system matrix

B = input distribution matrix

C = output matrix

D = feed-through matrix

The orders of the matrices are defined via variable definitions.

State-variable models are used to handle multiple inputs and multiple outputs. Furthermore, state-variable models can be formulated for open-loop system components or the complete closed-loop system.

The Laplace transform of the time-invariant state equation is

$$s\mathbf{X}(s) - \mathbf{x}(0) = \mathbf{AX}(s) + \mathbf{BU}(s)$$

from which

$$\mathbf{X}(s) = \Phi(s) \mathbf{x}(0) + \Phi(s) \mathbf{BU}(s)$$

where the Laplace transform of the state transition matrix is

$$\Phi(s) = [s\mathbf{I} - \mathbf{A}]^{-1}.$$

The state-transition matrix

$$\Phi(t) = L^{-1}\{\Phi(s)\}$$

(also defined as $e^{\mathbf{A}t}$) can be used to write

$$\mathbf{x}(t) = \Phi(t) \mathbf{x}(0) + \int_0^t \Phi(t-\tau) \mathbf{B}\mathbf{u}(\tau) d\tau$$

The output can be obtained with the output equation; e.g., the Laplace transform output is

$$\mathbf{Y}(s) = \{\mathbf{C}\Phi(s) \mathbf{B} + \mathbf{D}\}\mathbf{U}(s) + \mathbf{C}\Phi(s) \mathbf{x}(0)$$

The latter term represents the output(s) due to initial conditions, whereas the former term represents the output(s) due to the $\mathbf{U}(s)$ inputs and gives rise to transfer function definitions.

ENGINEERING ECONOMICS

Factor Name	Converts	Symbol	Formula
Single Payment Compound Amount	to F given P	$(F/P, i\%, n)$	$(1 + i)^n$
Single Payment Present Worth	to P given F	$(P/F, i\%, n)$	$(1 + i)^{-n}$
Uniform Series Sinking Fund	to A given F	$(A/F, i\%, n)$	$\frac{i}{(1 + i)^n - 1}$
Capital Recovery	to A given P	$(A/P, i\%, n)$	$\frac{i(1 + i)^n}{(1 + i)^n - 1}$
Uniform Series Compound Amount	to F given A	$(F/A, i\%, n)$	$\frac{(1 + i)^n - 1}{i}$
Uniform Series Present Worth	to P given A	$(P/A, i\%, n)$	$\frac{(1 + i)^n - 1}{i(1 + i)^n}$
Uniform Gradient Present Worth	to P given G	$(P/G, i\%, n)$	$\frac{(1 + i)^n - 1}{i^2(1 + i)^n} - \frac{n}{i(1 + i)^n}$
Uniform Gradient † Future Worth	to F given G	$(F/G, i\%, n)$	$\frac{(1 + i)^n - 1}{i^2} - \frac{n}{i}$
Uniform Gradient Uniform Series	to A given G	$(A/G, i\%, n)$	$\frac{1}{i} - \frac{n}{(1 + i)^n - 1}$

NOMENCLATURE AND DEFINITIONS

- A Uniform amount per interest period
 B Benefit
 BV Book value
 C Cost
 d Inflation adjusted interest rate per interest period
 D_j Depreciation in year j
 F Future worth, value, or amount
 f General inflation rate per interest period
 G Uniform gradient amount per interest period
 i Interest rate per interest period
 i_e Annual effective interest rate
 m Number of compounding periods per year
 n Number of compounding periods; or the expected life of an asset
 P Present worth, value, or amount
 r Nominal annual interest rate
 S_n Expected salvage value in year n

Subscripts

- j at time j
 n at time n
 \dagger $F/G = (F/A - n)/i = (F/A) \times (A/G)$

Risk

Risk is the chance of an outcome other than what is planned to occur or expected in the analysis.

NON-ANNUAL COMPOUNDING

$$i_e = \left(1 + \frac{r}{m}\right)^m - 1$$

BREAK-EVEN ANALYSIS

By altering the value of any one of the variables in a situation, holding all of the other values constant, it is possible to find a value for that variable that makes the two alternatives equally economical. This value is the break-even point.

Break-even analysis is used to describe the percentage of capacity of operation for a manufacturing plant at which income will just cover expenses.

The payback period is the period of time required for the profit or other benefits of an investment to equal the cost of the investment.

INFLATION

To account for inflation, the dollars are deflated by the general inflation rate per interest period f , and then they are shifted over the time scale using the interest rate per interest period i . Use an inflation adjusted interest rate per interest period d for computing present worth values P .

The formula for d is $d = i + f + (i \times f)$

DEPRECIATION

Straight Line

$$D_j = \frac{C - S_n}{n}$$

Modified Accelerated Cost Recovery System (MACRS)

$$D_j = (\text{factor}) C$$

A table of MACRS factors is provided below.

BOOK VALUE

$$BV = \text{initial cost} - \sum D_j$$

TAXATION

Income taxes are paid at a specific rate on taxable income. Taxable income is total income less depreciation and ordinary expenses. Expenses do not include capital items, which should be depreciated.

CAPITALIZED COSTS

Capitalized costs are present worth values using an assumed perpetual period of time.

$$\text{Capitalized Costs} = P = \frac{A}{i}$$

BONDS

Bond value equals the present worth of the payments the purchaser (or holder of the bond) receives during the life of the bond at some interest rate i .

Bond yield equals the computed interest rate of the bond value when compared with the bond cost.

RATE-OF-RETURN

The minimum acceptable rate-of-return (MARR) is that interest rate that one is willing to accept, or the rate one desires to earn on investments. The rate-of-return on an investment is the interest rate that makes the benefits and costs equal.

BENEFIT-COST ANALYSIS

In a benefit-cost analysis, the benefits B of a project should exceed the estimated costs C .

$$B - C \geq 0, \text{ or } B/C \geq 1$$

MACRS FACTORS				
Year	Recovery Period (Years)			
	3	5	7	10
1	33.33	20.00	14.29	10.00
2	44.45	32.00	24.49	18.00
3	14.81	19.20	17.49	14.40
4	7.41	11.52	12.49	11.52
5		11.52	8.93	9.22
6		5.76	8.92	7.37
7			8.93	6.55
8			4.46	6.55
9				6.56
10				6.55
11				3.28

Interest Rate Tables
Factor Table - $i = 0.50\%$

n	P/F	P/A	P/G	F/P	F/A	A/P	A/F	A/G
1	0.9950	0.9950	0.0000	1.0050	1.0000	1.0050	1.0000	0.0000
2	0.9901	1.9851	0.9901	1.0100	2.0050	0.5038	0.4988	0.4988
3	0.9851	2.9702	2.9604	1.0151	3.0150	0.3367	0.3317	0.9967
4	0.9802	3.9505	5.9011	1.0202	4.0301	0.2531	0.2481	1.4938
5	0.9754	4.9259	9.8026	1.0253	5.0503	0.2030	0.1980	1.9900
6	0.9705	5.8964	14.6552	1.0304	6.0755	0.1696	0.1646	2.4855
7	0.9657	6.8621	20.4493	1.0355	7.1059	0.1457	0.1407	2.9801
8	0.9609	7.8230	27.1755	1.0407	8.1414	0.1278	0.1228	3.4738
9	0.9561	8.7791	34.8244	1.0459	9.1821	0.1139	0.1089	3.9668
10	0.9513	9.7304	43.3865	1.0511	10.2280	0.1028	0.0978	4.4589
11	0.9466	10.6770	52.8526	1.0564	11.2792	0.0937	0.0887	4.9501
12	0.9419	11.6189	63.2136	1.0617	12.3356	0.0861	0.0811	5.4406
13	0.9372	12.5562	74.4602	1.0670	13.3972	0.0796	0.0746	5.9302
14	0.9326	13.4887	86.5835	1.0723	14.4642	0.0741	0.0691	6.4190
15	0.9279	14.4166	99.5743	1.0777	15.5365	0.0694	0.0644	6.9069
16	0.9233	15.3399	113.4238	1.0831	16.6142	0.0652	0.0602	7.3940
17	0.9187	16.2586	128.1231	1.0885	17.6973	0.0615	0.0565	7.8803
18	0.9141	17.1728	143.6634	1.0939	18.7858	0.0582	0.0532	8.3658
19	0.9096	18.0824	160.0360	1.0994	19.8797	0.0553	0.0503	8.8504
20	0.9051	18.9874	177.2322	1.1049	20.9791	0.0527	0.0477	9.3342
21	0.9006	19.8880	195.2434	1.1104	22.0840	0.0503	0.0453	9.8172
22	0.8961	20.7841	214.0611	1.1160	23.1944	0.0481	0.0431	10.2993
23	0.8916	21.6757	233.6768	1.1216	24.3104	0.0461	0.0411	10.7806
24	0.8872	22.5629	254.0820	1.1272	25.4320	0.0443	0.0393	11.2611
25	0.8828	23.4456	275.2686	1.1328	26.5591	0.0427	0.0377	11.7407
30	0.8610	27.7941	392.6324	1.1614	32.2800	0.0360	0.0310	14.1265
40	0.8191	36.1722	681.3347	1.2208	44.1588	0.0276	0.0226	18.8359
50	0.7793	44.1428	1,035.6966	1.2832	56.6452	0.0227	0.0177	23.4624
60	0.7414	51.7256	1,448.6458	1.3489	69.7700	0.0193	0.0143	28.0064
100	0.6073	78.5426	3,562.7934	1.6467	129.3337	0.0127	0.0077	45.3613

Factor Table - $i = 1.00\%$

n	P/F	P/A	P/G	F/P	F/A	A/P	A/F	A/G
1	0.9901	0.9901	0.0000	1.0100	1.0000	1.0100	1.0000	0.0000
2	0.9803	1.9704	0.9803	1.0201	2.0100	0.5075	0.4975	0.4975
3	0.9706	2.9410	2.9215	1.0303	3.0301	0.3400	0.3300	0.9934
4	0.9610	3.9020	5.8044	1.0406	4.0604	0.2563	0.2463	1.4876
5	0.9515	4.8534	9.6103	1.0510	5.1010	0.2060	0.1960	1.9801
6	0.9420	5.7955	14.3205	1.0615	6.1520	0.1725	0.1625	2.4710
7	0.9327	6.7282	19.9168	1.0721	7.2135	0.1486	0.1386	2.9602
8	0.9235	7.6517	26.3812	1.0829	8.2857	0.1307	0.1207	3.4478
9	0.9143	8.5650	33.6959	1.0937	9.3685	0.1167	0.1067	3.9337
10	0.9053	9.4713	41.8435	1.1046	10.4622	0.1056	0.0956	4.4179
11	0.8963	10.3676	50.8067	1.1157	11.5668	0.0965	0.0865	4.9005
12	0.8874	11.2551	60.5687	1.1268	12.6825	0.0888	0.0788	5.3815
13	0.8787	12.1337	71.1126	1.1381	13.8093	0.0824	0.0724	5.8607
14	0.8700	13.0037	82.4221	1.1495	14.9474	0.0769	0.0669	6.3384
15	0.8613	13.8651	94.4810	1.1610	16.0969	0.0721	0.0621	6.8143
16	0.8528	14.7179	107.2734	1.1726	17.2579	0.0679	0.0579	7.2886
17	0.8444	15.5623	120.7834	1.1843	18.4304	0.0643	0.0543	7.7613
18	0.8360	16.3983	134.9957	1.1961	19.6147	0.0610	0.0510	8.2323
19	0.8277	17.2260	149.8950	1.2081	20.8109	0.0581	0.0481	8.7017
20	0.8195	18.0456	165.4664	1.2202	22.0190	0.0554	0.0454	9.1694
21	0.8114	18.8570	181.6950	1.2324	23.2392	0.0530	0.0430	9.6354
22	0.8034	19.6604	198.5663	1.2447	24.4716	0.0509	0.0409	10.0998
23	0.7954	20.4558	216.0660	1.2572	25.7163	0.0489	0.0389	10.5626
24	0.7876	21.2434	234.1800	1.2697	26.9735	0.0471	0.0371	11.0237
25	0.7798	22.0232	252.8945	1.2824	28.2432	0.0454	0.0354	11.4831
30	0.7419	25.8077	355.0021	1.3478	34.7849	0.0387	0.0277	13.7557
40	0.6717	32.8347	596.8561	1.4889	48.8864	0.0305	0.0205	18.1776
50	0.6080	39.1961	879.4176	1.6446	64.4632	0.0255	0.0155	22.4363
60	0.5504	44.9550	1,192.8061	1.8167	81.6697	0.0222	0.0122	26.5333
100	0.3697	63.0289	2,605.7758	2.7048	170.4814	0.0159	0.0059	41.3426

Interest Rate Tables
Factor Table - $i = 1.50\%$

<i>n</i>	P/F	P/A	P/G	F/P	F/A	A/P	A/F	A/G
1	0.9852	0.9852	0.0000	1.0150	1.0000	1.0150	1.0000	0.0000
2	0.9707	1.9559	0.9707	1.0302	2.0150	0.5113	0.4963	0.4963
3	0.9563	2.9122	2.8833	1.0457	3.0452	0.3434	0.3284	0.9901
4	0.9422	3.8544	5.7098	1.0614	4.0909	0.2594	0.2444	1.4814
5	0.9283	4.7826	9.4229	1.0773	5.1523	0.2091	0.1941	1.9702
6	0.9145	5.6972	13.9956	1.0934	6.2296	0.1755	0.1605	2.4566
7	0.9010	6.5982	19.4018	1.1098	7.3230	0.1516	0.1366	2.9405
8	0.8877	7.4859	26.6157	1.1265	8.4328	0.1336	0.1186	3.4219
9	0.8746	8.3605	32.6125	1.1434	9.5593	0.1196	0.1046	3.9008
10	0.8617	9.2222	40.3675	1.1605	10.7027	0.1084	0.0934	4.3772
11	0.8489	10.0711	48.8568	1.1779	11.8633	0.0993	0.0843	4.8512
12	0.8364	10.9075	58.0571	1.1956	13.0412	0.0917	0.0767	5.3227
13	0.8240	11.7315	67.9454	1.2136	14.2368	0.0852	0.0702	5.7917
14	0.8118	12.5434	78.4994	1.2318	15.4504	0.0797	0.0647	6.2582
15	0.7999	13.3432	89.6974	1.2502	16.6821	0.0749	0.0599	6.7223
16	0.7880	14.1313	101.5178	1.2690	17.9324	0.0708	0.0558	7.1839
17	0.7764	14.9076	113.9400	1.2880	19.2014	0.0671	0.0521	7.6431
18	0.7649	15.6726	126.9435	1.3073	20.4894	0.0638	0.0488	8.0997
19	0.7536	16.4262	140.5084	1.3270	21.7967	0.0609	0.0459	8.5539
20	0.7425	17.1686	154.6154	1.3469	23.1237	0.0582	0.0432	9.0057
21	0.7315	17.9001	169.2453	1.3671	24.4705	0.0559	0.0409	9.4550
22	0.7207	18.6208	184.3798	1.3876	25.8376	0.0537	0.0387	9.9018
23	0.7100	19.3309	200.0006	1.4084	27.2251	0.0517	0.0367	10.3462
24	0.6995	20.0304	216.0901	1.4295	28.6335	0.0499	0.0349	10.7881
25	0.6892	20.7196	232.6310	1.4509	30.0630	0.0483	0.0333	11.2276
30	0.6398	24.0158	321.5310	1.5631	37.5387	0.0416	0.0266	13.3883
40	0.5513	29.9158	524.3568	1.8140	54.2679	0.0334	0.0184	17.5277
50	0.4750	34.9997	749.9636	2.1052	73.6828	0.0286	0.0136	21.4277
60	0.4093	39.3803	988.1674	2.4432	96.2147	0.0254	0.0104	25.0930
100	0.2256	51.6247	1,937.4506	4.4320	228.8030	0.0194	0.0044	37.5295

Factor Table - $i = 2.00\%$

<i>n</i>	P/F	P/A	P/G	F/P	F/A	A/P	A/F	A/G
1	0.9804	0.9804	0.0000	1.0200	1.0000	1.0200	1.0000	0.0000
2	0.9612	1.9416	0.9612	1.0404	2.0200	0.5150	0.4950	0.4950
3	0.9423	2.8839	2.8458	1.0612	3.0604	0.3468	0.3268	0.9868
4	0.9238	3.8077	5.6173	1.0824	4.1216	0.2626	0.2426	1.4752
5	0.9057	4.7135	9.2403	1.1041	5.2040	0.2122	0.1922	1.9604
6	0.8880	5.6014	13.6801	1.1262	6.3081	0.1785	0.1585	2.4423
7	0.8706	6.4720	18.9035	1.1487	7.4343	0.1545	0.1345	2.9208
8	0.8535	7.3255	24.8779	1.1717	8.5830	0.1365	0.1165	3.3961
9	0.8368	8.1622	31.5720	1.1951	9.7546	0.1225	0.1025	3.8681
10	0.8203	8.9826	38.9551	1.2190	10.9497	0.1113	0.0913	4.3367
11	0.8043	9.7868	46.9977	1.2434	12.1687	0.1022	0.0822	4.8021
12	0.7885	10.5753	55.6712	1.2682	13.4121	0.0946	0.0746	5.2642
13	0.7730	11.3484	64.9475	1.2936	14.6803	0.0881	0.0681	5.7231
14	0.7579	12.1062	74.7999	1.3195	15.9739	0.0826	0.0626	6.1786
15	0.7430	12.8493	85.2021	1.3459	17.2934	0.0778	0.0578	6.6309
16	0.7284	13.5777	96.1288	1.3728	18.6393	0.0737	0.0537	7.0799
17	0.7142	14.2919	107.5554	1.4002	20.0121	0.0700	0.0500	7.5256
18	0.7002	14.9920	119.4581	1.4282	21.4123	0.0667	0.0467	7.9681
19	0.6864	15.6785	131.8139	1.4568	22.8406	0.0638	0.0438	8.4073
20	0.6730	16.3514	144.6003	1.4859	24.2974	0.0612	0.0412	8.8433
21	0.6598	17.0112	157.7959	1.5157	25.7833	0.0588	0.0388	9.2760
22	0.6468	17.6580	171.3795	1.5460	27.2990	0.0566	0.0366	9.7055
23	0.6342	18.2922	185.3309	1.5769	28.8450	0.0547	0.0347	10.1317
24	0.6217	18.9139	199.6305	1.6084	30.4219	0.0529	0.0329	10.5547
25	0.6095	19.5235	214.2592	1.6406	32.0303	0.0512	0.0312	10.9745
30	0.5521	22.3965	291.7164	1.8114	40.5681	0.0446	0.0246	13.0251
40	0.4529	27.3555	461.9931	2.2080	60.4020	0.0366	0.0166	16.8885
50	0.3715	31.4236	642.3606	2.6916	84.5794	0.0318	0.0118	20.4420
60	0.3048	34.7609	823.6975	3.2810	114.0515	0.0288	0.0088	23.6961
100	0.1380	43.0984	1,464.7527	7.2446	312.2323	0.0232	0.0032	33.9863

Interest Rate Tables
Factor Table - $i = 4.00\%$

n	P/F	P/A	P/G	F/P	F/A	A/P	A/F	A/G
1	0.9615	0.9615	0.0000	1.0400	1.0000	1.0400	1.0000	0.0000
2	0.9246	1.8861	0.9246	1.0816	2.0400	0.5302	0.4902	0.4902
3	0.8890	2.7751	2.7025	1.1249	3.1216	0.3603	0.3203	0.9739
4	0.8548	3.6299	5.2670	1.1699	4.2465	0.2755	0.2355	1.4510
5	0.8219	4.4518	8.5547	1.2167	5.4163	0.2246	0.1846	1.9216
6	0.7903	5.2421	12.5062	1.2653	6.6330	0.1908	0.1508	2.3857
7	0.7599	6.0021	17.0657	1.3159	7.8983	0.1666	0.1266	2.8433
8	0.7307	6.7327	22.1806	1.3686	9.2142	0.1485	0.1085	3.2944
9	0.7026	7.4353	27.8013	1.4233	10.5828	0.1345	0.0945	3.7391
10	0.6756	8.1109	33.8814	1.4802	12.0061	0.1233	0.0833	4.1773
11	0.6496	8.7605	40.3772	1.5395	13.4864	0.1141	0.0741	4.6090
12	0.6246	9.3851	47.2477	1.6010	15.0258	0.1066	0.0666	5.0343
13	0.6006	9.9856	54.4546	1.6651	16.6268	0.1001	0.0601	5.4533
14	0.5775	10.5631	61.9618	1.7317	18.2919	0.0947	0.0547	5.8659
15	0.5553	11.1184	69.7355	1.8009	20.0236	0.0899	0.0499	6.2721
16	0.5339	11.6523	77.7441	1.8730	21.8245	0.0858	0.0458	6.6720
17	0.5134	12.1657	85.9581	1.9479	23.6975	0.0822	0.0422	7.0656
18	0.4936	12.6593	94.3498	2.0258	25.6454	0.0790	0.0390	7.4530
19	0.4746	13.1339	102.8933	2.1068	27.6712	0.0761	0.0361	7.8342
20	0.4564	13.5903	111.5647	2.1911	29.7781	0.0736	0.0336	8.2091
21	0.4388	14.0292	120.3414	2.2788	31.9692	0.0713	0.0313	8.5779
22	0.4220	14.4511	129.2024	2.3699	34.2480	0.0692	0.0292	8.9407
23	0.4057	14.8568	138.1284	2.4647	36.6179	0.0673	0.0273	9.2973
24	0.3901	15.2470	147.1012	2.5633	39.0826	0.0656	0.0256	9.6479
25	0.3751	15.6221	156.1040	2.6658	41.6459	0.0640	0.0240	9.9925
30	0.3083	17.2920	201.0618	3.2434	56.0849	0.0578	0.0178	11.6274
40	0.2083	19.7928	286.5303	4.8010	95.0255	0.0505	0.0105	14.4765
50	0.1407	21.4822	361.1638	7.1067	152.6671	0.0466	0.0066	16.8122
60	0.0951	22.6235	422.9966	10.5196	237.9907	0.0442	0.0042	18.6972
100	0.0198	24.5050	563.1249	50.5049	1,237.6237	0.0408	0.0008	22.9800

Factor Table - $i = 6.00\%$

n	P/F	P/A	P/G	F/P	F/A	A/P	A/F	A/G
1	0.9434	0.9434	0.0000	1.0600	1.0000	1.0600	1.0000	0.0000
2	0.8900	1.8334	0.8900	1.1236	2.0600	0.5454	0.4854	0.4854
3	0.8396	2.6730	2.5692	1.1910	3.1836	0.3741	0.3141	0.9612
4	0.7921	3.4651	4.9455	1.2625	4.3746	0.2886	0.2286	1.4272
5	0.7473	4.2124	7.9345	1.3382	5.6371	0.2374	0.1774	1.8836
6	0.7050	4.9173	11.4594	1.4185	6.9753	0.2034	0.1434	2.3304
7	0.6651	5.5824	15.4497	1.5036	8.3938	0.1791	0.1191	2.7676
8	0.6274	6.2098	19.8416	1.5938	9.8975	0.1610	0.1010	3.1952
9	0.5919	6.8017	24.5768	1.6895	11.4913	0.1470	0.0870	3.6133
10	0.5584	7.3601	29.6023	1.7908	13.1808	0.1359	0.0759	4.0220
11	0.5268	7.8869	34.8702	1.8983	14.9716	0.1268	0.0668	4.4213
12	0.4970	8.3838	40.3369	2.0122	16.8699	0.1193	0.0593	4.8113
13	0.4688	8.8527	45.9629	2.1329	18.8821	0.1130	0.0530	5.1920
14	0.4423	9.2950	51.7128	2.2609	21.0151	0.1076	0.0476	5.5635
15	0.4173	9.7122	57.5546	2.3966	23.2760	0.1030	0.0430	5.9260
16	0.3936	10.1059	63.4592	2.5404	25.6725	0.0990	0.0390	6.2794
17	0.3714	10.4773	69.4011	2.6928	28.2129	0.0954	0.0354	6.6240
18	0.3505	10.8276	75.3569	2.8543	30.9057	0.0924	0.0324	6.9597
19	0.3305	11.1581	81.3062	3.0256	33.7600	0.0896	0.0296	7.2867
20	0.3118	11.4699	87.2304	3.2071	36.7856	0.0872	0.0272	7.6051
21	0.2942	11.7641	93.1136	3.3996	39.9927	0.0850	0.0250	7.9151
22	0.2775	12.0416	98.9412	3.6035	43.3923	0.0830	0.0230	8.2166
23	0.2618	12.3034	104.7007	3.8197	46.9958	0.0813	0.0213	8.5099
24	0.2470	12.5504	110.3812	4.0489	50.8156	0.0797	0.0197	8.7951
25	0.2330	12.7834	115.9732	4.2919	54.8645	0.0782	0.0182	9.0722
30	0.1741	13.7648	142.3588	5.7435	79.0582	0.0726	0.0126	10.3422
40	0.0972	15.0463	185.9568	10.2857	154.7620	0.0665	0.0065	12.3590
50	0.0543	15.7619	217.4574	18.4202	290.3359	0.0634	0.0034	13.7964
60	0.0303	16.1614	239.0428	32.9877	533.1282	0.0619	0.0019	14.7909
100	0.0029	16.6175	272.0471	339.3021	5,638.3681	0.0602	0.0002	16.3711

Interest Rate Tables
Factor Table - $i = 8.00\%$

<i>n</i>	<i>P/F</i>	<i>P/A</i>	<i>P/G</i>	<i>F/P</i>	<i>F/A</i>	<i>A/P</i>	<i>A/F</i>	<i>A/G</i>
1	0.9259	0.9259	0.0000	1.0800	1.0000	1.0800	1.0000	0.0000
2	0.8573	1.7833	0.8573	1.1664	2.0800	0.5608	0.4808	0.4808
3	0.7938	2.5771	2.4450	1.2597	3.2464	0.3880	0.3080	0.9487
4	0.7350	3.3121	4.6501	1.3605	4.5061	0.3019	0.2219	1.4040
5	0.6806	3.9927	7.3724	1.4693	5.8666	0.2505	0.1705	1.8465
6	0.6302	4.6229	10.5233	1.5869	7.3359	0.2163	0.1363	2.2763
7	0.5835	5.2064	14.0242	1.7138	8.9228	0.1921	0.1121	2.6937
8	0.5403	5.7466	17.8061	1.8509	10.6366	0.1740	0.0940	3.0985
9	0.5002	6.2469	21.8081	1.9990	12.4876	0.1601	0.0801	3.4910
10	0.4632	6.7101	25.9768	2.1589	14.4866	0.1490	0.0690	3.8713
11	0.4289	7.1390	30.2657	2.3316	16.6455	0.1401	0.0601	4.2395
12	0.3971	7.5361	34.6339	2.5182	18.9771	0.1327	0.0527	4.5957
13	0.3677	7.9038	39.0463	2.7196	21.4953	0.1265	0.0465	4.9402
14	0.3405	8.2442	43.4723	2.9372	24.2149	0.1213	0.0413	5.2731
15	0.3152	8.5595	47.8857	3.1722	27.1521	0.1168	0.0368	5.5945
16	0.2919	8.8514	52.2640	3.4259	30.3243	0.1130	0.0330	5.9046
17	0.2703	9.1216	56.5883	3.7000	33.7502	0.1096	0.0296	6.2037
18	0.2502	9.3719	60.8426	3.9960	37.4502	0.1067	0.0267	6.4920
19	0.2317	9.6036	65.0134	4.3157	41.4463	0.1041	0.0241	6.7697
20	0.2145	9.8181	69.0898	4.6610	45.7620	0.1019	0.0219	7.0369
21	0.1987	10.0168	73.0629	5.0338	50.4229	0.0998	0.0198	7.2940
22	0.1839	10.2007	76.9257	5.4365	55.4568	0.0980	0.0180	7.5412
23	0.1703	10.3711	80.6726	5.8715	60.8933	0.0964	0.0164	7.7786
24	0.1577	10.5288	84.2997	6.3412	66.7648	0.0950	0.0150	8.0066
25	0.1460	10.6748	87.8041	6.8485	73.1059	0.0937	0.0137	8.2254
30	0.0994	11.2578	103.4558	10.0627	113.2832	0.0888	0.0088	9.1897
40	0.0460	11.9246	126.0422	21.7245	259.0565	0.0839	0.0039	10.5699
50	0.0213	12.2335	139.5928	46.9016	573.7702	0.0817	0.0017	11.4107
60	0.0099	12.3766	147.3000	101.2571	1,253.2133	0.0808	0.0008	11.9015
100	0.0005	12.4943	155.6107	2,199.7613	27,484.5157	0.0800		12.4545

Factor Table - $i = 10.00\%$

<i>n</i>	<i>P/F</i>	<i>P/A</i>	<i>P/G</i>	<i>F/P</i>	<i>F/A</i>	<i>A/P</i>	<i>A/F</i>	<i>A/G</i>
1	0.9091	0.9091	0.0000	1.1000	1.0000	1.1000	1.0000	0.0000
2	0.8264	1.7355	0.8264	1.2100	2.1000	0.5762	0.4762	0.4762
3	0.7513	2.4869	2.3291	1.3310	3.3100	0.4021	0.3021	0.9366
4	0.6830	3.1699	4.3781	1.4641	4.6410	0.3155	0.2155	1.3812
5	0.6209	3.7908	6.8618	1.6105	6.1051	0.2638	0.1638	1.8101
6	0.5645	4.3553	9.6842	1.7716	7.7156	0.2296	0.1296	2.2236
7	0.5132	4.8684	12.7631	1.9487	9.4872	0.2054	0.1054	2.6216
8	0.4665	5.3349	16.0287	2.1436	11.4359	0.1874	0.0874	3.0045
9	0.4241	5.7590	19.4215	2.3579	13.5735	0.1736	0.0736	3.3724
10	0.3855	6.1446	22.8913	2.5937	15.9374	0.1627	0.0627	3.7255
11	0.3505	6.4951	26.3962	2.8531	18.5312	0.1540	0.0540	4.0641
12	0.3186	6.8137	29.9012	3.1384	21.3843	0.1468	0.0468	4.3884
13	0.2897	7.1034	33.3772	3.4523	24.5227	0.1408	0.0408	4.6988
14	0.2633	7.3667	36.8005	3.7975	27.9750	0.1357	0.0357	4.9955
15	0.2394	7.6061	40.1520	4.1772	31.7725	0.1315	0.0315	5.2789
16	0.2176	7.8237	43.4164	4.5950	35.9497	0.1278	0.0278	5.5493
17	0.1978	8.0216	46.5819	5.0545	40.5447	0.1247	0.0247	5.8071
18	0.1799	8.2014	49.6395	5.5599	45.5992	0.1219	0.0219	6.0526
19	0.1635	8.3649	52.5827	6.1159	51.1591	0.1195	0.0195	6.2861
20	0.1486	8.5136	55.4069	6.7275	57.2750	0.1175	0.0175	6.5081
21	0.1351	8.6487	58.1095	7.4002	64.0025	0.1156	0.0156	6.7189
22	0.1228	8.7715	60.6893	8.1403	71.4027	0.1140	0.0140	6.9189
23	0.1117	8.8832	63.1462	8.9543	79.5430	0.1126	0.0126	7.1085
24	0.1015	8.9847	65.4813	9.8497	88.4973	0.1113	0.0113	7.2881
25	0.0923	9.0770	67.6964	10.8347	98.3471	0.1102	0.0102	7.4580
30	0.0573	9.4269	77.0766	17.4494	164.4940	0.1061	0.0061	8.1762
40	0.0221	9.7791	88.9525	45.2593	442.5926	0.1023	0.0023	9.0962
50	0.0085	9.9148	94.8889	117.3909	1,163.9085	0.1009	0.0009	9.5704
60	0.0033	9.9672	97.7010	304.4816	3,034.8164	0.1003	0.0003	9.8023
100	0.0001	9.9993	99.9202	13,780.6123	137,796.1234	0.1000		9.9927

Interest Rate Tables
Factor Table - $i = 12.00\%$

n	P/F	P/A	P/G	F/P	F/A	A/P	A/F	A/G
1	0.8929	0.8929	0.0000	1.1200	1.0000	1.1200	1.0000	0.0000
2	0.7972	1.6901	0.7972	1.2544	2.1200	0.5917	0.4717	0.4717
3	0.7118	2.4018	2.2208	1.4049	3.3744	0.4163	0.2963	0.9246
4	0.6355	3.0373	4.1273	1.5735	4.7793	0.3292	0.2092	1.3589
5	0.5674	3.6048	6.3970	1.7623	6.3528	0.2774	0.1574	1.7746
6	0.5066	4.1114	8.9302	1.9738	8.1152	0.2432	0.1232	2.1720
7	0.4523	4.5638	11.6443	2.2107	10.0890	0.2191	0.0991	2.5515
8	0.4039	4.9676	14.4714	2.4760	12.2997	0.2013	0.0813	2.9131
9	0.3606	5.3282	17.3563	2.7731	14.7757	0.1877	0.0677	3.2574
10	0.3220	5.6502	20.2541	3.1058	17.5487	0.1770	0.0570	3.5847
11	0.2875	5.9377	23.1288	3.4785	20.6546	0.1684	0.0484	3.8953
12	0.2567	6.1944	25.9523	3.8960	24.1331	0.1614	0.0414	4.1897
13	0.2292	6.4235	28.7024	4.3635	28.0291	0.1557	0.0357	4.4683
14	0.2046	6.6282	31.3624	4.8871	32.3926	0.1509	0.0309	4.7317
15	0.1827	6.8109	33.9202	5.4736	37.2797	0.1468	0.0268	4.9803
16	0.1631	6.9740	36.3670	6.1304	42.7533	0.1434	0.0234	5.2147
17	0.1456	7.1196	38.6973	6.8660	48.8837	0.1405	0.0205	5.4353
18	0.1300	7.2497	40.9080	7.6900	55.7497	0.1379	0.0179	5.6427
19	0.1161	7.3658	42.9979	8.6128	63.4397	0.1358	0.0158	5.8375
20	0.1037	7.4694	44.9676	9.6463	72.0524	0.1339	0.0139	6.0202
21	0.0926	7.5620	46.8188	10.8038	81.6987	0.1322	0.0122	6.1913
22	0.0826	7.6446	48.5543	12.1003	92.5026	0.1308	0.0108	6.3514
23	0.0738	7.7184	50.1776	13.5523	104.6029	0.1296	0.0096	6.5010
24	0.0659	7.7843	51.6929	15.1786	118.1552	0.1285	0.0085	6.6406
25	0.0588	7.8431	53.1046	17.0001	133.3339	0.1275	0.0075	6.7708
30	0.0334	8.0552	58.7821	29.9599	241.3327	0.1241	0.0041	7.2974
40	0.0107	8.2438	65.1159	93.0510	767.0914	0.1213	0.0013	7.8988
50	0.0035	8.3045	67.7624	289.0022	2,400.0182	0.1204	0.0004	8.1597
60	0.0011	8.3240	68.8100	897.5969	7,471.6411	0.1201	0.0001	8.2664
100	8.3332	69.4336		83,522.2657	696,010.5477	0.1200		8.3321

Factor Table - $i = 18.00\%$

n	P/F	P/A	P/G	F/P	F/A	A/P	A/F	A/G
1	0.8475	0.8475	0.0000	1.1800	1.0000	1.1800	1.0000	0.0000
2	0.7182	1.5656	0.7182	1.3924	2.1800	0.6387	0.4587	0.4587
3	0.6086	2.1743	1.9354	1.6430	3.5724	0.4599	0.2799	0.8902
4	0.5158	2.6901	3.4828	1.9388	5.2154	0.3717	0.1917	1.2947
5	0.4371	3.1272	5.2312	2.2878	7.1542	0.3198	0.1398	1.6728
6	0.3704	3.4976	7.0834	2.6996	9.4423	0.2859	0.1059	2.0252
7	0.3139	3.8115	8.9670	3.1855	12.1415	0.2624	0.0824	2.3526
8	0.2660	4.0776	10.8292	3.7589	15.3270	0.2452	0.0652	2.6558
9	0.2255	4.3030	12.6329	4.4355	19.0859	0.2324	0.0524	2.9358
10	0.1911	4.4941	14.3525	5.2338	23.5213	0.2225	0.0425	3.1936
11	0.1619	4.6560	15.9716	6.1759	28.7551	0.2148	0.0348	3.4303
12	0.1372	4.7932	17.4811	7.2876	34.9311	0.2086	0.0286	3.6470
13	0.1163	4.9095	18.8765	8.5994	42.2187	0.2037	0.0237	3.8449
14	0.0985	5.0081	20.1576	10.1472	50.8180	0.1997	0.0197	4.0250
15	0.0835	5.0916	21.3269	11.9737	60.9653	0.1964	0.0164	4.1887
16	0.0708	5.1624	22.3885	14.1290	72.9390	0.1937	0.0137	4.3369
17	0.0600	5.2223	23.3482	16.6722	87.0680	0.1915	0.0115	4.4708
18	0.0508	5.2732	24.2123	19.6731	103.7403	0.1896	0.0096	4.5916
19	0.0431	5.3162	24.9877	23.2144	123.4135	0.1881	0.0081	4.7003
20	0.0365	5.3527	25.6813	27.3930	146.6280	0.1868	0.0068	4.7978
21	0.0309	5.3837	26.3000	32.3238	174.0210	0.1857	0.0057	4.8851
22	0.0262	5.4099	26.8506	38.1421	206.3448	0.1848	0.0048	4.9632
23	0.0222	5.4321	27.3394	45.0076	244.4868	0.1841	0.0041	5.0329
24	0.0188	5.4509	27.7725	53.1090	289.4944	0.1835	0.0035	5.0950
25	0.0159	5.4669	28.1555	62.6686	342.6035	0.1829	0.0029	5.1502
30	0.0070	5.5168	29.4864	143.3706	790.9480	0.1813	0.0013	5.3448
40	0.0013	5.5482	30.5269	750.3783	4,163.2130	0.1802	0.0002	5.5022
50	0.0003	5.5541	30.7856	3,927.3569	21,813.0937	0.1800		5.5428
60	0.0001	5.5553	30.8465	20,555.1400	114,189.6665	0.1800		5.5526
100	5.5556	30.8642		15,424,131.91	85,689,616.17	0.1800		5.5555

CHEMICAL ENGINEERING

CHEMICAL REACTION ENGINEERING

Nomenclature

A chemical reaction may be expressed by the general equation



The rate of reaction of any component is defined as the moles of that component formed per unit time per unit volume.

$$-r_A = -\frac{1}{V} \frac{dN_A}{dt} \quad (\text{negative because A disappears})$$

$$-r_A = \frac{-dC_A}{dt} \quad \text{if } V \text{ is constant}$$

The rate of reaction is frequently expressed by

$$-r_A = kf_r(C_A, C_B, \dots), \text{ where}$$

k = reaction rate constant

C_I = concentration of component I

In the conversion of A , the fractional conversion X_A is defined as the moles of A reacted per mole of A fed.

$$X_A = (C_{A0} - C_A)/C_{A0} \quad \text{if } V \text{ is constant}$$

The Arrhenius equation gives the dependence of k on temperature

$$k = Ae^{-E_a/\bar{R}T}, \text{ where}$$

A = pre-exponential or frequency factor

E_a = activation energy (J/mol, cal/mol)

T = temperature (K)

\bar{R} = gas law constant = 8.314 J/(mol•K)

For values of rate constant (k_i) at two temperatures (T_i),

$$E_a = \frac{RT_1 T_2}{(T_1 - T_2)} \ln\left(\frac{k_1}{k_2}\right)$$

Reaction Order

If $-r_A = kC_A^x C_B^y$

the reaction is x order with respect to reactant A and y order with respect to reactant B . The overall order is

$$n = x + y$$

Batch Reactor, Constant Volume

For a well-mixed, constant-volume batch reactor

$$-r_A = -dC_A/dt$$

$$t = -C_{A0} \int_0^{X_A} dX_A / (-r_A)$$

Zero-Order Irreversible Reaction

$$\begin{aligned} -r_A &= kC_A^0 = k(1) \\ -dC_A/dt &= k && \text{or} \\ C_A &= C_{A0} - kt \\ dX_A/dt &= k/C_{A0} && \text{or} \\ C_{A0}X_A &= kt \end{aligned}$$

First-Order Irreversible Reaction

$$\begin{aligned} -r_A &= kC_A \\ -dC_A/dt &= kC_A && \text{or} \\ \ln(C_A/C_{A0}) &= -kt \\ dX_A/dt &= k(1 - X_A) && \text{or} \\ \ln(1 - X_A) &= -kt \end{aligned}$$

Second-Order Irreversible Reaction

$$\begin{aligned} -r_A &= kC_A^2 \\ -dC_A/dt &= kC_A^2 && \text{or} \\ 1/C_A - 1/C_{A0} &= kt \\ dX_A/dt &= kC_{A0}(1 - X_A)^2 && \text{or} \\ X_A/[C_{A0}(1 - X_A)] &= kt \end{aligned}$$

First-Order Reversible Reactions

$$\begin{aligned} A &\xrightleftharpoons[k_2]{k_1} R \\ -r_A &= -\frac{dC_A}{dt} = k_1 C_A - k_2 C_R \\ K_c &= k_1/k_2 = \hat{C}_R/\hat{C}_A \\ M &= C_{R0}/C_{A0} \\ \frac{d\hat{X}_A}{dt} &= \frac{k_1(M+1)}{M+\hat{X}_A} (\hat{X}_A - X_A) \\ -\ln\left(1 - \frac{X_A}{\hat{X}_A}\right) &= -\ln \frac{C_A - \hat{C}_A}{C_{A0} - \hat{C}_A} \\ &= \frac{(M+1)}{(M+\hat{X}_A)} k_1 t \end{aligned}$$

Reactions of Shifting Order

$$-r_A = \frac{k_1 C_A}{1 + k_2 C_A}$$

$$\ln\left(\frac{C_{A_0}}{C_A}\right) + k_2(C_{A_0} - C_A) = k_1 t$$

$$\frac{\ln(C_{A_0}/C_A)}{C_{A_0} - C_A} = -k_2 + \frac{k_1 t}{C_{A_0} - C_A}$$

This form of the rate equation is used for elementary enzyme-catalyzed reactions and for elementary surface-catalyzed reactions.

Batch Reactor, Variable Volume

If the volume of the reacting mass varies with the conversion (such as a variable-volume batch reactor) according to

$$V = V_{X_A=0}(1 + \varepsilon_A X_A)$$

(i.e., at constant pressure), where

$$\varepsilon_A = \frac{V_{X_A=1} - V_{X_A=0}}{V_{X_A=0}} = \frac{\Delta V}{V_{X_A=0}}$$

then at any time

$$C_A = C_{A0} \left[\frac{1 - X_A}{1 + \varepsilon_A X_A} \right]$$

and

$$t = -C_{A0} \int_0^{X_A} dX_A / [(1 + \varepsilon_A X_A)(-r_A)]$$

For a first-order irreversible reaction,

$$kt = -\ln(1 - X_A) = -\ln\left(1 - \frac{\Delta V}{\varepsilon_A V_{X_A=0}}\right)$$

Flow Reactors, Steady State

Space-time τ is defined as the reactor volume divided by the inlet volumetric feed rate. Space-velocity SV is the reciprocal of space-time, $SV = 1/\tau$.

Plug-Flow Reactor (PFR)

$$\tau = \frac{C_{A0} V_{PFR}}{F_{A0}} = C_{A0} \int_0^{X_A} \frac{dX_A}{(-r_A)}, \text{ where}$$

F_{A0} = moles of A fed per unit time.

Continuous-Stirred Tank Reactor (CSTR)

For a constant volume, well-mixed CSTR

$$\frac{\tau}{C_{A0}} = \frac{V_{CSTR}}{F_{A0}} = \frac{X_A}{-r_A}, \text{ where}$$

$-r_A$ is evaluated at exit stream conditions.

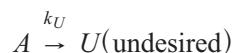
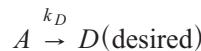
Continuous-Stirred Tank Reactors in Series

With a first-order reaction $A \rightarrow R$, no change in volume.

$$\begin{aligned} \tau_{N\text{-reactors}} &= N\tau_{\text{individual}} \\ &= \frac{N}{k} \left[\left(\frac{C_{A0}}{C_{AN}} \right)^{1/N} - 1 \right], \text{ where} \end{aligned}$$

N = number of CSTRs (equal volume) in series, and C_{AN} = concentration of A leaving the N th CSTR.

Two Irreversible Reactions in Parallel



$$-r_A = -dc_A/dt = k_D C_A^x + k_U C_A^y$$

$$r_D = dc_D/dt = k_D C_A^x$$

$$r_U = dc_U/dt = k_U C_A^y$$

Y_D = instantaneous fractional yield of D

$$= dC_D/(-dC_A)$$

\bar{Y}_D = overall fractional yield of D

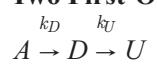
$$= N_{D_f}/(N_{A_0} - N_{A_f})$$

where N_{A_f} and N_{D_f} are measured at the outlet of the flow reactor.

\bar{S}_{DU} = overall selectivity to D

$$= N_{D_f}/N_{U_f}$$

Two First-Order Irreversible Reactions in Series



$$r_A = -dC_A/dt = k_D C_A$$

$$r_D = dC_D/dt = k_D C_A - k_U C_D$$

$$r_U = dC_U/dt = k_U C_D$$

Yield and selectivity definitions are identical to those for two irreversible reactions in parallel. The optimal yield of D in a PFR is

$$\frac{C_{D,\max}}{C_{A0}} = \left(\frac{k_D}{k_U} \right)^{k_U/(k_U - k_D)}$$

at time

$$\tau_{\max} = \frac{1}{k_{\log \text{mean}}} = \frac{\ln(k_U/k_D)}{(k_U - k_D)}$$

The optimal yield of D in a CSTR is

$$\frac{C_{D,\max}}{C_{A0}} = \frac{1}{\left[(k_U/k_D)^{1/2} + 1 \right]^2}$$

at time

$$\tau_{\max} = 1/\sqrt{k_D k_U}$$

MASS TRANSFER

Diffusion

Molecular Diffusion

$$\text{Gas: } N_A = \frac{p_A}{P} (N_A + N_B) - \frac{D_m}{RT} \frac{\partial p_A}{\partial z}$$

$$\text{Liquid: } N_A = x_A (N_A + N_B) - CD_m \frac{\partial x_A}{\partial z}$$

where,

N_i = molar flux of component i

P = pressure

p_i = partial pressure of component i

D_m = mass diffusivity

\bar{R} = universal gas constant

T = temperature

z = length

Unidirectional Diffusion of a Gas A Through a Second Stagnant Gas B ($N_b = 0$)

$$N_A = \frac{D_m P}{\bar{R} T (p_B)_{lm}} \times \frac{(p_{A2} - p_{A1})}{z_2 - z_1}$$

in which $(p_B)_{lm}$ is the log mean of p_{B2} and p_{B1}

$$(p_{BM})_{lm} = \frac{p_{B2} - p_{B1}}{\ln \left(\frac{p_{B2}}{p_{B1}} \right)}$$

N_i = diffusive flux [mole/(time × area)] of component i through area A , in z direction

D_m = mass diffusivity

p_I = partial pressure of species I

C = concentration (mole/volume)

$(z_2 - z_1)$ = diffusion flow path length

Equimolar Counter-Diffusion (Gases)

$$(N_B = -N_A)$$

$$N_A = D_m / (RT) \times [(p_{A1} - p_{A2}) / (\Delta z)]$$

$$N_A = D_m (C_{A1} - C_{A2}) / \Delta z$$

Convection

Two-Film Theory (for Equimolar Counter-Diffusion)

$$\begin{aligned} N_A &= k'_G (p_{AG} - p_{Ai}) \\ &= k'_L (C_{Ai} - C_{AL}) \\ &= K'_G (p_{AG} - p_A^*) \\ &= K'_L (C_A^* - C_{AL}) \end{aligned}$$

where,

N_A = molar flux of component A

k'_G = gas phase mass transfer coefficient

k'_L = liquid phase mass transfer coefficient

K'_G = overall gas phase mass transfer coefficient

K'_L = overall liquid phase mass transfer coefficient

p_{AG} = partial pressure in component A in the bulk gas phase

p_{Ai} = partial pressure at component A at the gas-liquid interface

C_{Ai} = concentration (mole/volume) of component A in the liquid phase at the gas-liquid interface

C_{AL} = concentration of component A in the bulk liquid phase

p_A^* = partial pressure of component A in equilibrium with C_{AL}

C_A^* = concentration of component A in equilibrium with the bulk gas vapor composition of A

Overall Coefficients

$$1/K'_G = 1/k'_G + H/k'_L$$

$$1/K'_L = 1/Hk'_G + 1/k'_L$$

H = Henry's Law constant where $p_A^* = H C_{AL}$ and $C_A^* = p_{AG}/H$

Dimensionless Group Equation (Sherwood)

For the turbulent flow inside a tube the Sherwood number

$$Sh = \left(\frac{k_m D}{D_m} \right) = 0.023 \left(\frac{DV\rho}{\mu} \right)^{0.8} \left(\frac{\mu}{\rho D_m} \right)^{1/3}$$

where,

D = inside diameter

D_m = diffusion coefficient

V = average velocity in the tube

ρ = fluid density

μ = fluid viscosity

k_m = mass transfer coefficient

Distillation

Definitions:

α = relative volatility

B = molar bottoms-product rate

D = molar overhead-product rate

F = molar feed rate

L = molar liquid downflow rate

R_D = ratio of reflux to overhead product

V = molar vapor upflow rate

W = total moles in still pot

x = mole fraction of the more volatile component in the liquid phase

y = mole fraction of the more volatile component in the vapor phase

Subscripts:

B = bottoms product

D = overhead product

F = feed

m = any plate in stripping section of column

$m+1$ = plate below plate m

n = any plate in rectifying section of column

$n+1$ = plate below plate n

o = original charge in still pot

Flash (or equilibrium) Distillation

Component material balance:

$$Fz_F = yV + xL$$

Overall material balance:

$$F = V + L$$

Differential (Simple or Rayleigh) Distillation

$$\ln\left(\frac{W}{W_o}\right) = \int_{x_o}^x \frac{dx}{y - x}$$

When the relative volatility α is constant,

$$y = \alpha x / [1 + (\alpha - 1)x]$$

can be substituted to give

$$\ln\left(\frac{W}{W_o}\right) = \frac{1}{(\alpha - 1)} \ln\left[\frac{x(1 - x_o)}{x_o(1 - x)}\right] + \ln\left[\frac{1 - x_o}{1 - x}\right]$$

For binary system following Raoult's Law

$$\alpha = (y/x)_a / (y/x)_b = p_a / p_b, \text{ where}$$

p_i = partial pressure of component i .

Continuous Distillation (Binary System)

Constant molal overflow is assumed.

Equilibrium stages numbered from top.

Overall Material Balances

Total Material:

$$F = D + B$$

Component A :

$$Fz_F = Dx_D + Bx_B$$

Operating Lines

Rectifying section

Total Material:

$$V_{n+1} = L_n + D$$

Component A :

$$V_{n+1}y_{n+1} = L_n x_n + D x_D$$

$$y_{n+1} = [L_n / (L_n + D)] x_n + D x_D / (L_n + D)$$

Stripping section

Total Material:

$$L_m = V_{m+1} + B$$

Component A :

$$L_m x_m = V_{m+1} y_{m+1} + B x_B$$

$$y_{m+1} = [L_m / (L_m - B)] x_m - B x_B / (L_m - B)$$

Reflux ratio

Ratio of reflux to overhead product

$$R_D = L_R / D = (V_R - D) / D$$

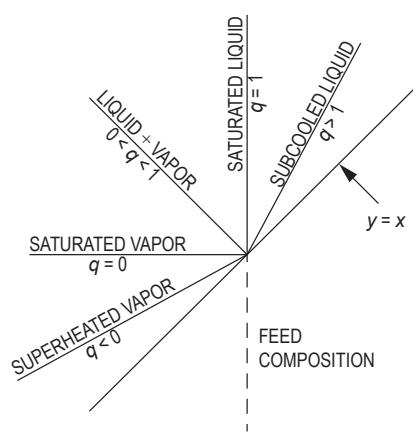
Minimum reflux ratio is defined as that value which results in an infinite number of contact stages. For a binary system the equation of the operating line is

$$y = \frac{R_{\min}}{R_{\min} + 1} x + \frac{x_D}{R_{\min} + 1}$$

Feed condition line

slope = $q/(q - 1)$, where

$$q = \frac{\text{heat to convert one mol of feed to saturated vapor}}{\text{molar heat of vaporization}}$$

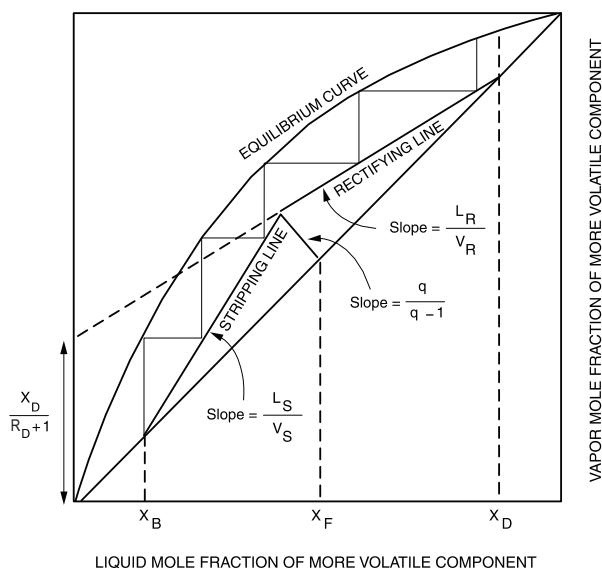
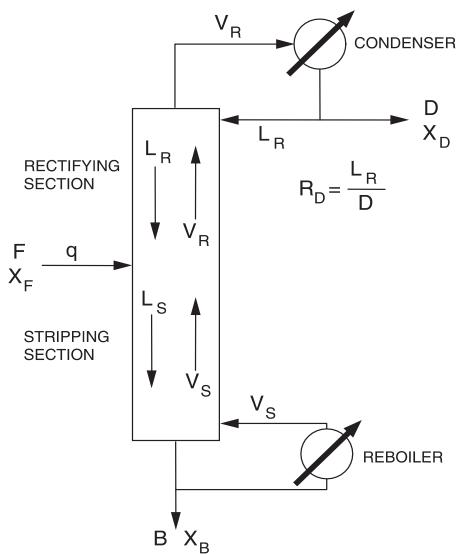


q -LINE SLOPES

Murphree plate efficiency

$$E_{ME} = (y_n - y_{n+1}) / (y_n^* - y_{n+1}), \text{ where}$$

y_n = concentration of vapor above equilibrium stage n
 y_{n+1} = concentration of vapor entering from equilibrium stage below n
 y_n^* = concentration of vapor in equilibrium with liquid leaving equilibrium stage n



Absorption (packed columns)

Continuous Contact Columns

$$Z = NTU_G \cdot HTU_G = NTU_L \cdot HTU_L = N_{EQ} \cdot HETP$$

Z = column height

NTU_G = number of transfer units (gas phase)

NTU_L = number of transfer units (liquid phase)

N_{EQ} = number of equilibrium stages

HTU_G = height of transfer unit (gas phase)

HTU_L = height of transfer unit (liquid phase)

$HETP$ = height equivalent to theoretical plate (stage)

$$HTU_G = \frac{G}{K'_G a} \quad HTU_L = \frac{L}{K'_L a}$$

G = gas phase mass velocity (mass or moles/flow area • time)

L = liquid phase mass velocity (mass or moles/flow area • time)

K'_G = overall gas phase mass transfer coefficient (mass or moles/mass transfer area • time)

K'_L = overall liquid phase mass transfer coefficient (mass or moles/mass transfer area • time)

a = mass transfer area/volume of column (length^{-1})

$$NTU_G = \int_{y_1}^{y_2} \frac{dy}{(y - y^*)} \quad NTU_L = \int_{x_1}^{x_2} \frac{dx}{(x^* - x)}$$

y = gas phase solute mole fraction

x = liquid phase solute mole fraction

y^* = $K \cdot x$, where K = equilibrium constant

x^* = y/K , where K = equilibrium constant

y_2, x_2 = mole fractions at the lean end of column

y_1, x_1 = mole fractions at the rich end of column

For dilute solutions (constant G/L and constant K value for entire column):

$$NTU_G = \frac{y_1 - y_2}{(y - y^*)_{LM}}$$

$$(y - y^*)_{LM} = \frac{(y_1 - y_1^*) - (y_2 - y_2^*)}{\ln \left(\frac{y_1 - y_1^*}{y_2 - y_2^*} \right)}$$

For a chemically reacting system—absorbed solute reacts in the liquid phase—the preceding relation simplifies to:

$$NTU_G = \ln \left(\frac{y_1}{y_2} \right)$$

TRANSPORT PHENOMENA—MOMENTUM, HEAT, AND MASS TRANSFER ANALOGY

For the equations which apply to *turbulent flow in circular tubes*, the following definitions apply:

$$\text{Nu} = \text{Nusselt Number} \left[\frac{hD}{k} \right]$$

$$\text{Pr} = \text{Prandtl Number} (c_p \mu / k)$$

$$\text{Re} = \text{Reynolds Number} (DV\rho/\mu)$$

$$\text{Sc} = \text{Schmidt Number} [\mu/(\rho D_m)]$$

$$\text{Sh} = \text{Sherwood Number} (k_m D/D_m)$$

$$\text{St} = \text{Stanton Number} [h/(c_p G)]$$

$$c_m = \text{concentration (mol/m}^3\text{)}$$

$$c_p = \text{heat capacity of fluid [J/(kg}\cdot\text{K}]\text{)}$$

$$D = \text{tube inside diameter (m)}$$

$$D_m = \text{diffusion coefficient (m}^2/\text{s)}$$

$$(dc_m/dy)_w = \text{concentration gradient at the wall (mol/m}^4\text{)}$$

$$(dT/dy)_w = \text{temperature gradient at the wall (K/m)}$$

$$(dv/dy)_w = \text{velocity gradient at the wall (s}^{-1}\text{)}$$

$$f = \text{Moody friction factor}$$

$$G = \text{mass velocity [kg/(m}^2\cdot\text{s}]\text{)}$$

$$h = \text{heat-transfer coefficient at the wall [W/(m}^2\cdot\text{K}]\text{)}$$

$$k = \text{thermal conductivity of fluid [W/(m}\cdot\text{K}]\text{)}$$

$$k_m = \text{mass-transfer coefficient (m/s)}$$

$$L = \text{length over which pressure drop occurs (m)}$$

$$(N/A)_w = \text{inward mass-transfer flux at the wall [mol/(m}^2\cdot\text{s}]\text{)}$$

$$(\dot{Q}/A)_w = \text{inward heat-transfer flux at the wall (W/m}^2\text{)}$$

$$y = \text{distance measured from inner wall toward centerline (m)}$$

$$\Delta c_m = \text{concentration difference between wall and bulk fluid (mol/m}^3\text{)}$$

$$\Delta T = \text{temperature difference between wall and bulk fluid (K)}$$

$$\mu = \text{absolute dynamic viscosity (N}\cdot\text{s/m}^2\text{)}$$

$$\tau_w = \text{shear stress (momentum flux) at the tube wall (N/m}^2\text{)}$$

Definitions already introduced also apply.

Rate of Transfer as a Function of Gradients at the Wall

Momentum Transfer:

$$\tau_w = -\mu \left(\frac{dv}{dy} \right)_w = -\frac{f_0 V^2}{8} = \left(\frac{D}{4} \right) \left(-\frac{\Delta p}{L} \right)_f$$

Heat Transfer

$$\left(\frac{\dot{Q}}{A} \right)_w = -k \left(\frac{dT}{dy} \right)_w$$

Mass Transfer in Dilute Solutions

$$\left(\frac{N}{A} \right)_w = -D_m \left(\frac{dc_m}{dy} \right)_w$$

Rate of Transfer in Terms of Coefficients

Momentum Transfer

$$\tau_w = \frac{f_0 V^2}{8}$$

Heat Transfer

$$\left(\frac{\dot{Q}}{A} \right)_w = h \Delta T$$

Mass Transfer

$$\left(\frac{N}{A} \right)_w = k_m \Delta c_m$$

Use of Friction Factor (*f*) to Predict Heat-Transfer and Mass Transfer Coefficients (Turbulent Flow)

Heat Transfer

$$j_H = \left(\frac{\text{Nu}}{\text{RePr}} \right) \text{Pr}^{2/3} = \frac{f}{8}$$

Mass Transfer

$$j_M = \left(\frac{\text{Sh}}{\text{ReSc}} \right) \text{Sc}^{2/3} = \frac{f}{8}$$

COST ESTIMATION

Cost Indexes

Cost indexes are used to update historical cost data to the present. If a purchase cost is available for an item of equipment in year M , the equivalent current cost would be found by:

$$\text{Current \$} = (\text{Cost in year } M) \left(\frac{\text{Current Index}}{\text{Index in year } M} \right)$$

Component	Range
<i>Direct costs</i>	
Purchased equipment-delivered (including fabricated equipment and process machinery such as pumps and compressors)	100
Purchased-equipment installation	39–47
Instrumentation and controls (installed)	9–18
Piping (installed)	16–66
Electrical (installed)	10–11
Buildings (including services)	18–29
Yard improvements	10–13
Service facilities (installed)	40–70
Land (if purchase is required)	6
Total direct plant cost	264–346
<i>Indirect costs</i>	
Engineering and supervision	32–33
Construction expenses	34–41
Total direct and indirect plant costs	336–420
Contractor's fee (about 5% of direct and indirect plant costs)	17–21
Contingency (about 10% of direct and indirect plant costs)	36–42
Fixed-capital investment	387–483
Working capital (about 15% of total capital investment)	68–86
Total capital investment	455–569

Scaling of Equipment Costs

The cost of Unit A at one capacity related to the cost of a similar Unit B with X times the capacity of Unit A is approximately X^n times the cost of Unit B.

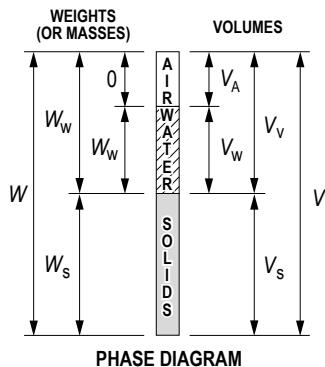
$$\text{Cost of Unit A} = \text{cost of Unit B} \left(\frac{\text{capacity of Unit A}}{\text{capacity of Unit B}} \right)^n$$

Typical Exponents (*n*) for Equipment Cost vs. Capacity

Equipment	Size range	Exponent
Dryer, drum, single vacuum	10 to 10^2 ft ²	0.76
Dryer, drum, single atmospheric	10 to 10^2 ft ²	0.40
Fan, centrifugal	10^3 to 10^4 ft ³ /min	0.44
Fan, centrifugal	2×10^4 to 7×10^4 ft ³ /min	1.17
Heat exchanger, shell and tube, floating head, c.s.	100 to 400 ft ²	0.60
Heat exchanger, shell and tube, fixed sheet, c.s.	100 to 400 ft ²	0.44
Motor, squirrel cage, induction, 440 volts, explosion proof	5 to 20 hp	0.69
Motor, squirrel cage, induction, 440 volts, explosion proof	20 to 200 hp	0.99
Tray, bubble cup, c.s.	3- to 10-ft diameter	1.20
Tray, sieve, c.s.	3- to 10-ft diameter	0.86

CIVIL ENGINEERING

GEOTECHNICAL Phase Relationships



Volume of voids

$$V_v = V_A + V_W$$

Total unit weight

$$\gamma = W/V$$

Saturated unit weight

$$\gamma_{\text{sat}} = (G_s + e) \gamma_w / (1 + e)$$

$$\gamma_w = 62.4 \text{ lb/ft}^3 \text{ or } 9.81 \text{ kN/m}^3$$

Effective (submerged) unit weight

$$\gamma' = \gamma_{\text{sat}} - \gamma_w$$

Unit weight of solids

$$\gamma_s = W_s/V_s$$

Dry unit weight

$$\gamma_d = W_s/V$$

Water content (%)

$$\omega = (W_w/W_s) \times 100$$

Specific gravity of soil solids

$$G_s = (W_s/V_s)/\gamma_w$$

Void ratio

$$e = V_v/V_s$$

Porosity

$$n = V_v/V = e/(1+e)$$

Degree of saturation (%)

$$S = (V_w/V_v) \times 100$$

$$S = \omega G_s/e$$

Relative density

$$D_r = [(e_{\max} - e)/(e_{\max} - e_{\min})] \times 100$$

$$= [(\gamma_{D \text{ field}} - \gamma_{D \text{ min}})/(\gamma_{D \text{ max}} - \gamma_{D \text{ min}})][\gamma_{D \text{ max}}/\gamma_{D \text{ field}}] \times 100$$

Relative compaction (%)

$$RC = (\gamma_{D \text{ field}}/\gamma_{D \text{ max}}) \times 100$$

Plasticity index

$$PI = LL - PL$$

LL = liquid limit

PL = Plastic limit

Coefficient of uniformity

$$C_u = D_{60}/D_{10}$$

Coefficient of concavity (or curvature)

$$C_c = (D_{30})^2/(D_{10} \times D_{60})$$

Hydraulic conductivity (also coefficient of permeability)

From constant head test: $k = Q/(iAt_e)$

$$i = dh/dL$$

Q = total quantity of water

From falling head test: $k = 2.303[(aL)/(At_e)]\log_{10}(h_1/h_2)$

A = cross-sectional area of test specimen perpendicular to flow

a = cross-sectional area of reservoir tube

t_e = elapsed time

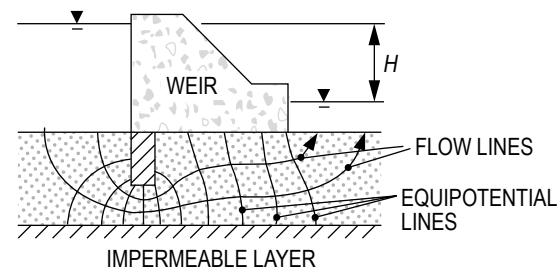
h_1 = head at time $t = 0$

h_2 = head at time $t = t_e$

L = length of soil column

Discharge velocity, $v = ki$

Flow Nets



$$Q = kH(N_f/N_d), \text{ where}$$

Q = flow per unit time

N_f = number of flow channels

N_d = number of equipotential drops

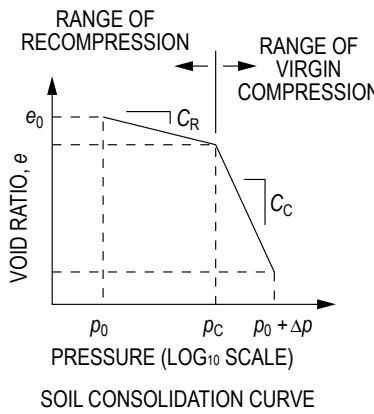
H = total hydraulic head differential

Factor of safety against seepage liquefaction

$$FS_s = i_c/i_e$$

$$i_c = (\gamma_{\text{sat}} - \gamma_w)/\gamma_w$$

i_e = seepage exit gradient



e_0 = initial void ratio (prior to consolidation)

Δe = change in void ratio

p_0 = initial effective consolidation stress, σ'_0

p_c = past maximum consolidation stress, σ'_c

Δp = induced change in consolidation stress at center of consolidating stratum

$\Delta p = I q_s$

I = Stress influence value at center of consolidating stratum

q_s = applied surface stress causing consolidation

$$\text{If } (p_0 \text{ and } p_0 + \Delta p) < p_c, \text{ then } \Delta H = \frac{H_0}{1 + e_0} \left[C_R \log \frac{p_0 + \Delta p}{p_0} \right]$$

$$\text{If } (p_0 \text{ and } p_0 + \Delta p) > p_c, \text{ then } \Delta H = \frac{H_0}{1 + e_0} \left[C_C \log \frac{p_0 + \Delta p}{p_0} \right]$$

$$\text{If } p_0 < p_c < (p_0 + \Delta p), \text{ then } \Delta H = \frac{H_0}{1 + e_0} \left[C_R \log \frac{p_c}{p_0} + C_C \log \frac{p_0 + \Delta p}{p_c} \right]$$

where: ΔH = change in thickness of soil layer

Compression index

In virgin compression range: $C_C = \Delta e / \Delta \log p$

By correlation to liquid limit: $C_C = 0.009 (\text{LL} - 10)$

Recompression index

In recompression range: $C_R = \Delta e / \Delta \log p$

By correlation to compression index, C_C : $C_R = C_C / 6$

Ultimate consolidation settlement in soil layer

$$S_{\text{ULT}} = \varepsilon_v H_s$$

H_s = thickness of soil layer

$$\varepsilon_v = \Delta e_{\text{TOT}} / (1 + e_0)$$

Δe_{TOT} = total change in void ratio due to recompression and virgin compression

Approximate settlement (at time $t = t_c$)

$$S_t = U_{\text{AV}} S_{\text{ULT}}$$

U_{AV} = average degree of consolidation

t_c = elapsed time since application of consolidation load

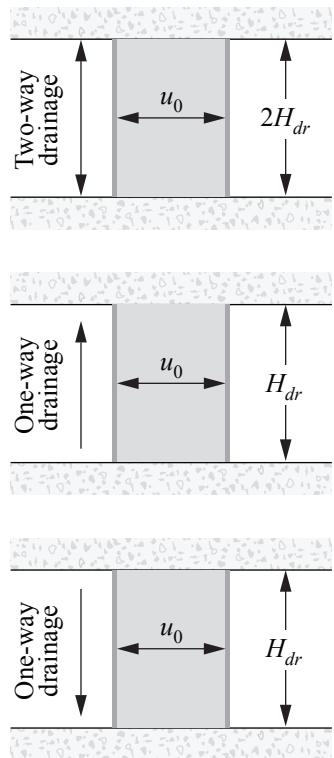
Variation of time factor with degree of consolidation*

<i>U (%)</i>	<i>T_v</i>	<i>U (%)</i>	<i>T_v</i>	<i>U (%)</i>	<i>T_v</i>
0	0	34	0.0907	68	0.377
1	0.00008	35	0.0962	69	0.390
2	0.0003	36	0.102	70	0.403
3	0.00071	37	0.107	71	0.417
4	0.00126	38	0.113	72	0.431
5	0.00196	39	0.119	73	0.446
6	0.00283	40	0.126	74	0.461
7	0.00385	41	0.132	75	0.477
8	0.00502	42	0.138	76	0.493
9	0.00636	43	0.145	77	0.511
10	0.00785	44	0.152	78	0.529
11	0.0095	45	0.159	79	0.547
12	0.0113	46	0.166	80	0.567
13	0.0133	47	0.173	81	0.588
14	0.0154	48	0.181	82	0.610
15	0.0177	49	0.188	83	0.633
16	0.0201	50	0.197	84	0.658
17	0.0227	51	0.204	85	0.684
18	0.0254	52	0.212	86	0.712
19	0.0283	53	0.221	87	0.742
20	0.0314	54	0.230	88	0.774
21	0.0346	55	0.239	89	0.809
22	0.0380	56	0.248	90	0.848
23	0.0415	57	0.257	91	0.891
24	0.0452	58	0.267	92	0.938
25	0.0491	59	0.276	93	0.993
26	0.0531	60	0.286	94	1.055
27	0.0572	61	0.297	95	1.129
28	0.0615	62	0.307	96	1.219
29	0.0660	63	0.318	97	1.336
30	0.0707	64	0.329	98	1.500
31	0.0754	65	0.340	99	1.781
32	0.0803	66	0.352	100	∞
33	0.0855	67	0.364		

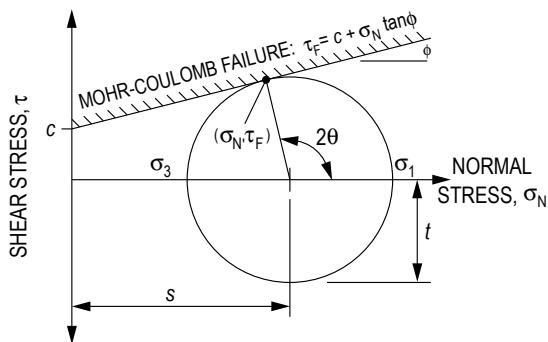
**u₀* constant with depth.

where time factor is $T_v = \frac{c_v t}{H_{dr}^2}$

Das, Braja M., *Fundamentals of Geotechnical Engineering*, Cengage Learning (formerly Brooks/Cole), 2000, p. 179.



Different types of drainage
with *u₀* constant



s = mean normal stress

t = maximum shear stress

σ_1 = major principal stress

σ_3 = minor principal stress

θ = orientation angle between plane of existing normal stress and plane of major principal stress

Total normal stress

$$\sigma_N = P/A$$

P = normal force

A = cross-sectional area over which force acts

Effective stress

$$\sigma' = \sigma - u$$

$$u = h_u \gamma_w$$

h_u = uplift or pressure head

Shear stress

$$\tau = T/A$$

T = shearing force

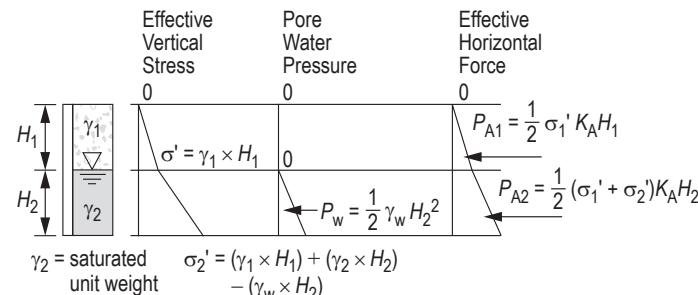
Shear stress at failure

$$\tau_F = c + \sigma_N \tan \phi$$

c = cohesion

ϕ = angle of internal friction

Horizontal Stress Profiles and Forces



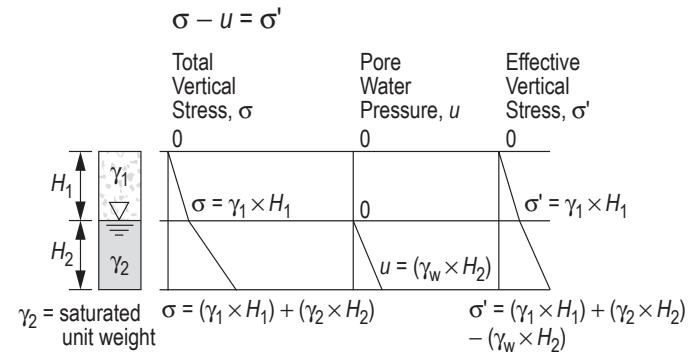
Active forces on retaining wall per unit wall length (as shown):

K_A = Rankine active earth pressure coefficient (smooth wall, $c = 0$, level backfill) = $\tan^2(45^\circ - \phi/2)$

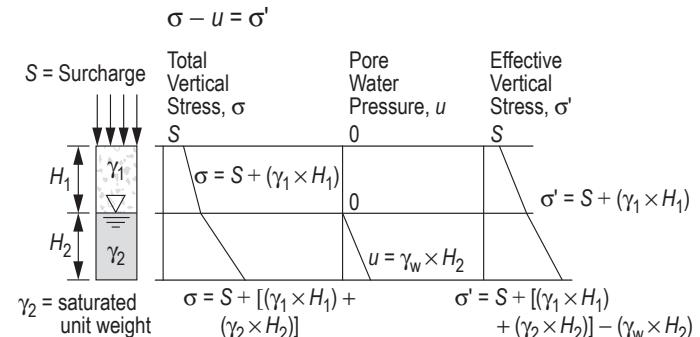
Passive forces on retaining wall per unit wall length (similar to the active forces shown):

K_p = Rankine passive earth pressure coefficient (smooth wall, $c = 0$, level backfill) = $\tan^2(45^\circ + \phi/2)$

Vertical Stress Profiles



Vertical Stress Profiles with Surcharge



Ultimate Bearing Capacity

$$q_{ULT} = c N_c + \gamma' D_f N_q + \frac{1}{2} \gamma' B N_\gamma$$

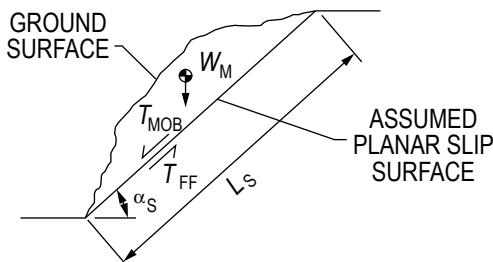
N_c = bearing capacity factor for cohesion

N_q = bearing capacity factor for depth

N_γ = bearing capacity factor for unit weight

D_f = depth of footing below ground surface

B = width of strip footing



SLOPE FAILURE ALONG PLANAR SURFACE

- FS = factor of safety against slope instability
 = T_{FF}/T_{MOB}
 T_{FF} = available shearing resistance along slip surface
 = $cL_S + W_M \cos\alpha_S \tan\phi$
 T_{MOB} = mobilized shear force along slip surface
 = $W_M \sin\alpha_S$
 L_S = length of assumed planar slip surface
 W_M = weight of soil above slip surface
 α_S = angle of assumed slip surface with respect to horizontal

◆

AASHTO Soil Classification

GENERAL CLASSIFICATION		GRANULAR MATERIALS (35% OR LESS PASSING 0.075 SIEVE)						SILT-CLAY MATERIALS (MORE THAN 35% PASSING 0.075 SIEVE)				
GROUP CLASSIFICATION		A-1		A-3	A-2				A-4	A-5	A-6	A-7-5 A-7-6
		A-1-a	A-1-b		A-2-4	A-2-5	A-2-6	A-2-7				
SIEVE ANALYSIS, PERCENT PASSING:												
2.00 mm (No. 10)	≤ 50	—		—	—	—	—	—	—	—	—	—
0.425 mm (No. 40)	≤ 30	≤ 50		≥ 51	—	—	—	—	—	—	—	—
0.075 mm (No. 200)	≤ 15	≤ 25		≤ 10	≤ 35	≤ 35	≤ 35	≤ 35	≥ 36	≥ 36	≥ 36	≥ 36
CHARACTERISTICS OF FRACTION PASSING 0.425 SIEVE (No. 40):												
LIQUID LIMIT	—				≤ 40	≥ 41	≤ 40	≥ 41	≤ 40	≥ 41	≤ 40	≥ 41
PLASTICITY INDEX *	6 max				NP	≤ 10	≤ 10	≥ 11	≥ 11	≤ 10	≤ 10	≥ 11
USUAL TYPES OF CONSTITUENT MATERIALS	STONE FRAGM'TS, GRAVEL, SAND	FINE SAND	SILTY OR CLAYEY GRAVEL AND SAND				SILTY SOILS		CLAYEY SOILS			
GENERAL RATING AS A SUBGRADE	EXCELLENT TO GOOD						FAIR TO POOR					

*Plasticity index of A-7-5 subgroup is equal to or less than LL – 30. Plasticity index of A-7-6 subgroup is greater than LL – 30.

NP = Non-plastic (use "0"). Symbol "—" means that the particular sieve analysis is not considered for that classification.

If the soil classification is A4-A7, then calculate the group index (GI) as shown below and report with classification. The higher the GI, the less suitable the soil. Example: A-6 with GI = 15 is less suitable than A-6 with GI = 10.

$$GI = (F - 35) [0.2 + 0.005 (LL - 40)] + 0.01 (F - 15) (PI - 10)$$

where: F = Percent passing No. 200 sieve, expressed as a whole number. This percentage is based only on the material passing the No. 200 sieve.

LL = Liquid limit

PI = Plasticity index

If the computed value of GI < 0, then use GI = 0.

◆ Adapted from AASHTO Standard Specification M145-91, Standard Specification for Classification of Soils and Soil-Aggregate Mixtures for Highway Construction Purposes, 2004.

ASTM D2487-11 Standard Practice for Classification of Soils for Engineering Purposes (Unified Soil Classification System)

Criteria for Assigning Group Symbols and Group Names Using Laboratory Tests ^A			Soil Classification	
			Group Symbol	Group Name ^B
COARSE-GRAINED SOILS More than 50% retained on No. 200 sieve	Gravels (more than 50% of coarse fraction retained on No. 4 sieve)	Clean Gravels (Less than 5% fines ^C)	$Cu \geq 4$ and $1 \leq Cc \leq 3^D$	GW Well-graded gravel ^E
			$Cu < 4$ and/or $[Cc < 1 \text{ or } Cc > 3]^D$	GP Poorly graded gravel ^E
		Gravels with Fines (More than 12% fines ^C)	Fines classify as ML or MH	GM Silty gravel ^{E, F, G}
	Sands (50% or more of coarse fraction passes No. 4 sieve)		Fines classify as CL or CH	GC Clayey gravel ^{E, F, G}
		Clean Sands (Less than 5% fines ^H)	$Cu \geq 6$ and $1 \leq Cc \leq 3^D$	SW Well-graded sand ^I
			$Cu < 6$ and/or $[Cc < 1 \text{ or } Cc > 3]^D$	SP Poorly graded sand ^I
		Sands with Fines (More than 12% fines ^H)	Fines classify as ML or MH	SM Silty sand ^{F, G, I}
			Fines classify as CL or CH	SC Clayey sand ^{F, G, I}
FINE-GRAINED SOILS 50% or more passes the No. 200 sieve	Silts and Clays Liquid limit less than 50	inorganic	PI > 7 and plots on or above "A" line ^J	CL Lean clay ^{K, L, M}
			PI < 4 or plots below "A" line ^J	ML Silt ^{K, L, M}
		organic	Liquid limit - oven dried/Liquid ^{&#10} < 0.75	OL Organic clay ^{K, L, M, N} Organic silt ^{K, L, M, O}
	Silts and Clays Liquid limit 50 or more	inorganic	PI plots on or above "A" line	CH Fat clay ^{K, L, M}
			PI plots below "A" line	MH Elastic silt ^{K, L, M}
		organic	Liquid limit - oven dried/Liquid ^{&#10} < 0.75	OH Organic clay ^{K, L, M, P} Organic silt ^{K, L, M, Q}
HIGHLY ORGANIC SOILS		Primarily organic matter, dark in color, and organic odor	PT	Peat

^ABased on the material passing the 3-in. (75-mm) sieve.

^BIf field sample contained cobbles or boulders, or both, add "with cobbles or boulders, or both" to group name.

^CGravels with 5 to 12% fines require dual symbols:

GW-GM well-graded gravel with silt

GW-GC well-graded gravel with clay

GP-GM poorly graded gravel with silt

GP-GC poorly graded gravel with clay

$$^D Cu = \frac{(D_{30})^2}{D_{60}/D_{10}} \quad Cc = \frac{(D_{30})^2}{D_{10} \times D_{60}}$$

^EIf soil contains $\geq 15\%$ sand, add "with sand" to group name.

^FIf fines classify as CL-ML, use dual symbol GC-GM, or SC-SM.

^GIf fines are organic, add "with organic fines" to group name.

^HSands with 5 to 12% fines require dual symbols:

SW-SM well-graded sand with silt

SW-SC well-graded sand with clay

SP-SM poorly graded sand with silt

SP-SC poorly graded sand with clay

^IIf soil contains $\geq 15\%$ gravel, add "with gravel" to group name.

^JIf Atterberg limits plot in hatched area, soil is a CL-ML, silty clay.

^KIf soil contains 15 to 30% plus No. 200, add "with sand" or "with gravel", whichever is predominant.

^LIf soil contains $\geq 30\%$ plus No. 200, predominantly sand, add "sandy" to group name.

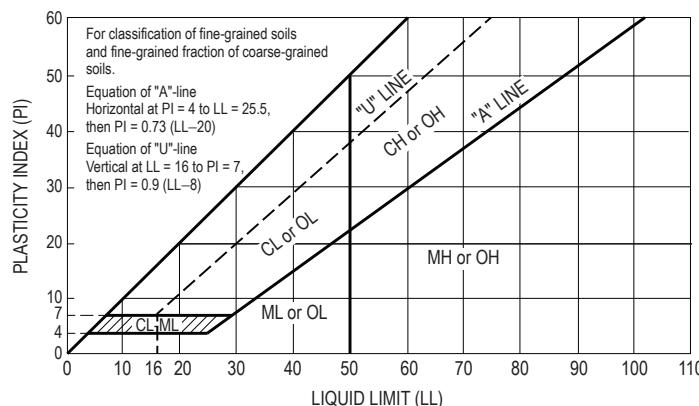
^MIf soil contains $\geq 30\%$ plus No. 200, predominantly gravel, add "gravelly" to group name.

^NPI ≥ 4 and plots on or above "A" line.

^OPI < 4 or plots below "A" line.

^PPI plots on or above "A" line.

^QPI plots below "A" line.

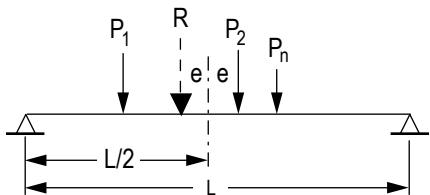


STRUCTURAL ANALYSIS

Influence Lines for Beams and Trusses

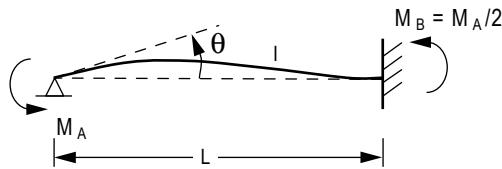
An influence line shows the variation of an effect (reaction, shear and moment in beams, bar force in a truss) caused by moving a unit load across the structure. An influence line is used to determine the position of a moveable set of loads that causes the maximum value of the effect.

Moving Concentrated Load Sets



The **absolute maximum moment** produced in a beam by a set of "n" moving loads occurs when the resultant "R" of the load set and an adjacent load are equal distance from the centerline of the beam. In general, two possible load set positions must be considered, one for each adjacent load.

Beam Stiffness and Moment Carryover



$$\theta = \frac{M L}{4 EI} \rightarrow M = \left(\frac{4 EI}{L} \right) \theta = k_{AB} \theta$$

k_{AB} = stiffness

$M_B = M_A/2$ = carryover

Truss Deflection by Unit Load Method

The displacement of a truss joint caused by external effects (truss loads, member temperature change, member misfit) is found by applying a unit load at the point that corresponds to the desired displacement.

$$\Delta_{\text{joint}} = \sum_{i=1}^{\text{members}} f_i (\Delta L)_i$$

where: Δ_{joint} = joint displacement at point of application of unit load (+ in direction of unit load)

f_i = force in member "i" caused by unit load (+ tension)

$(\Delta L)_i$ = change in length caused by external effect (+ for increase in member length):

= $\left(\frac{FL}{AE} \right)_i$ for bar force F caused by external load

= $\alpha L_i (\Delta T)_i$ for temperature change in member (α = coefficient of thermal expansion)

= member misfit

L, A = member length and cross-sectional area

E = member elastic modulus

Frame Deflection by Unit Load Method

The displacement of any point on a frame caused by external loads is found by applying a unit load at that point that corresponds to the desired displacement:

$$\Delta = \sum_{i=1}^{\text{members}} \int_x^x \frac{L_i m_i M_i}{EI_i} dx$$

where: Δ = displacement at point of application of unit load (+ in direction of unit load)

m_i = moment equation in member "i" caused by the unit load

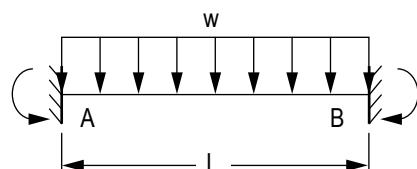
M_i = moment equation in member "i" caused by loads applied to frame

L_i = length of member "i"

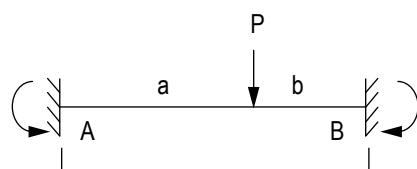
I_i = moment of inertia of member "i"

If either the real loads or the unit load cause no moment in a member, that member can be omitted from the summation.

Member Fixed-End Moments (Magnitudes)



$$FEM_{AB} = FEM_{BA} = \frac{wl^2}{12}$$



$$FEM_{AB} = \frac{Pab^2}{L^2} \quad FEM_{BA} = \frac{Pa^2b}{L^2}$$

STABILITY, DETERMINACY, AND CLASSIFICATION OF STRUCTURES

m = number of members

r = number of independent reaction components

j = number of joints

c = number of condition equations based on known internal moments or forces, such as internal moment of zero at a hinge

Plane Truss

Static Analysis	Classification
-----------------	----------------

$m + r < 2j$	Unstable
--------------	----------

$m + r = 2j$	Stable and statically determinate
--------------	-----------------------------------

$m + r > 2j$	Stable and statically indeterminate
--------------	-------------------------------------

Plane Frame

Static Analysis	Classification
-----------------	----------------

$3m + r < 3j + c$	Unstable
-------------------	----------

$3m + r = 3j + c$	Stable and statically determinate
-------------------	-----------------------------------

$3m + r > 3j + c$	Stable and statically indeterminate
-------------------	-------------------------------------

Stability also requires an appropriate arrangement of members and reaction components.

Load Combinations using Strength Design (LRFD, USD)

Nominal loads used in following combinations:

D = dead loads

E = earthquake loads

L = live loads (floor)

L_r = live loads (roof)

R = rain load

S = snow load

W = wind load

Load factors λ : λ_D (dead load), λ_L (live load), etc.

Basic combinations $L_r/S/R = \text{largest of } L_r, S, R$

L or $0.8W = \text{larger of } L, 0.8W$

$1.4D$

$1.2D + 1.6L + 0.5(L_r/S/R)$

$1.2D + 1.6(L_r/S/R) + (L \text{ or } 0.8W)$

$1.2D + 1.6W + L + 0.5(L_r/S/R)$

$1.2D + 1.0E + L + 0.2S$

$0.9D + 1.6W$

$0.9D + 1.0E$

STRUCTURAL DESIGN

Live Load Reduction

The effect on a building member of nominal occupancy live loads may often be reduced based on the loaded floor area supported by the member. A typical model used for computing reduced live load (as found in ASCE 7 and many building codes) is:

$$L_{\text{reduced}} = L_{\text{nominal}} \left(0.25 + \frac{15}{\sqrt{K_{LL}A_T}} \right) \geq 0.4L_{\text{nominal}}$$

where: L_{nominal} = nominal live load given in ASCE 7 or a building code

A_T = the cumulative floor tributary area supported by the member

$K_{LL}A_T$ = area of influence supported by the member

K_{LL} = ratio of area of influence to the tributary area supported by the member:

$K_{LL} = 4$ (typical columns)

$K_{LL} = 2$ (typical beams and girders)

DESIGN OF REINFORCED CONCRETE COMPONENTS (ACI 318-11)

U.S. Customary units

Definitions

- a = depth of equivalent rectangular stress block, in.
- A_g = gross area of column, in²
- A_s = area of tension reinforcement, in²
- A_{st} = total area of longitudinal reinforcement, in²
- A_v = area of shear reinforcement within a distance s , in.
- b = width of compression face of member, in.
- β_1 = ratio of depth of rectangular stress block, a , to depth to neutral axis, c

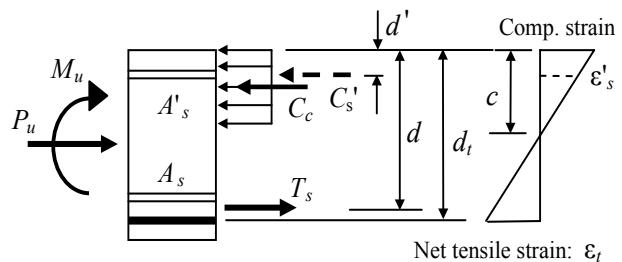
$$= 0.85 \geq 0.85 - 0.05 \left(\frac{f'_c - 4,000}{1,000} \right) \geq 0.65$$
- c = distance from extreme compression fiber to neutral axis, in.
- d = distance from extreme compression fiber to centroid of nonprestressed tension reinforcement, in.
- d_t = distance from extreme compression fiber to extreme tension steel, in.
- E_c = modulus of elasticity = $33w_c^{1.5} \sqrt{f'_c}$, psi
- ϵ_t = net tensile strain in extreme tension steel at nominal strength
- f'_c = compressive strength of concrete, psi
- f_y = yield strength of steel reinforcement, psi
- M_n = nominal moment strength at section, in.-lb
- ϕM_n = design moment strength at section, in.-lb
- M_u = factored moment at section, in.-lb
- P_n = nominal axial load strength at given eccentricity, lb
- ϕP_n = design axial load strength at given eccentricity, lb
- P_u = factored axial force at section, lb
- ρ_g = ratio of total reinforcement area to cross-sectional area of column = A_{st}/A_g
- s = spacing of shear ties measured along longitudinal axis of member, in.
- V_c = nominal shear strength provided by concrete, lb
- V_n = nominal shear strength at section, lb
- ϕV_n = design shear strength at section, lb
- V_s = nominal shear strength provided by reinforcement, lb
- V_u = factored shear force at section, lb

ASTM STANDARD REINFORCING BARS

BAR SIZE	DIAMETER, IN.	AREA, IN ²	WEIGHT, LB/FT
#3	0.375	0.11	0.376
#4	0.500	0.20	0.668
#5	0.625	0.31	1.043
#6	0.750	0.44	1.502
#7	0.875	0.60	2.044
#8	1.000	0.79	2.670
#9	1.128	1.00	3.400
#10	1.270	1.27	4.303
#11	1.410	1.56	5.313
#14	1.693	2.25	7.650
#18	2.257	4.00	13.60

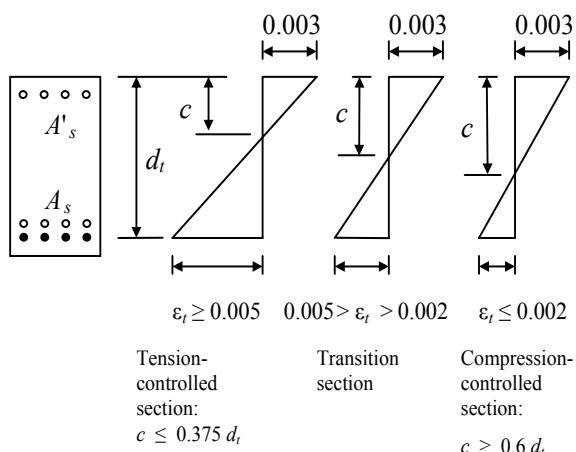
UNIFIED DESIGN PROVISIONS

Internal Forces and Strains



Net tensile strain: ϵ_t

Strain Conditions



Tension-controlled section:
 $c \leq 0.375 d_t$

Transition section

Compression-controlled section:
 $c \geq 0.6 d_t$

RESISTANCE FACTORS, ϕ

Tension-controlled sections ($\epsilon_t \geq 0.005$): $\phi = 0.9$

Compression-controlled sections ($\epsilon_t \leq 0.002$):

Members with tied reinforcement $\phi = 0.65$

Transition sections ($0.002 < \epsilon_t < 0.005$):

Members with tied reinforcement $\phi = 0.48 + 83\epsilon_t$

Shear and torsion $\phi = 0.75$

Bearing on concrete $\phi = 0.65$

BEAMS—FLEXURE

$$\phi M_n \geq M_u$$

For All Beams

Net tensile strain: $a = \beta_1 c$

$$\varepsilon_t = \frac{0.003(d_t - c)}{c} = \frac{0.003(\beta_1 d_t - a)}{a}$$

Design moment strength: ϕM_n

where: $\phi = 0.9 [\varepsilon_t \geq 0.005]$

$\phi = 0.48 + 83\varepsilon_t [0.002 \leq \varepsilon_t < 0.005]$

$\phi = 0.65 [\varepsilon_t < 0.002]$

Singly-Reinforced Beams

$$a = \frac{A_s f_y}{0.85 f_c b}$$

$$M_n = 0.85 f_c a b \left(d - \frac{a}{2} \right) = A_s f_y \left(d - \frac{a}{2} \right)$$

BEAMS—SHEAR

$$\phi V_n \geq V_u$$

Nominal shear strength:

$$V_n = V_c + V_s$$

$$V_c = 2 b_w d \sqrt{f_c}$$

$$V_s = \frac{A_v f_y d}{s} \text{ (may not exceed } 8 b_w d \sqrt{f_c})$$

Required and maximum-permitted stirrup spacing, s

$$V_u \leq \frac{\phi V_c}{2}: \text{No stirrups required}$$

$$V_u > \frac{\phi V_c}{2}: \text{Use the following table (} A_v \text{ given)}$$

	$\frac{\phi V_c}{2} < V_u \leq \phi V_c$	$V_u > \phi V_c$
Required spacing	<p>Smaller of:</p> $s = \frac{A_v f_y}{50 b_w}$ $s = \frac{A_v f_y}{0.75 b_w \sqrt{f_c}}$	$V_s = \frac{V_u}{\phi} - V_c$ $s = \frac{A_v f_y d}{V_s}$
Maximum permitted spacing	<p>Smaller of:</p> $s = \frac{d}{2}$ <p>OR</p> $s = 24"$	$V_s \leq 4 b_w d \sqrt{f_c}$ <p>Smaller of:</p> $s = \frac{d}{2} \quad \text{OR}$ $s = 24"$ $V_s > 4 b_w d \sqrt{f_c}$ <p>Smaller of:</p> $s = \frac{d}{4}$ $s = 12"$

SHORT COLUMNS

Limits for Main Reinforcements

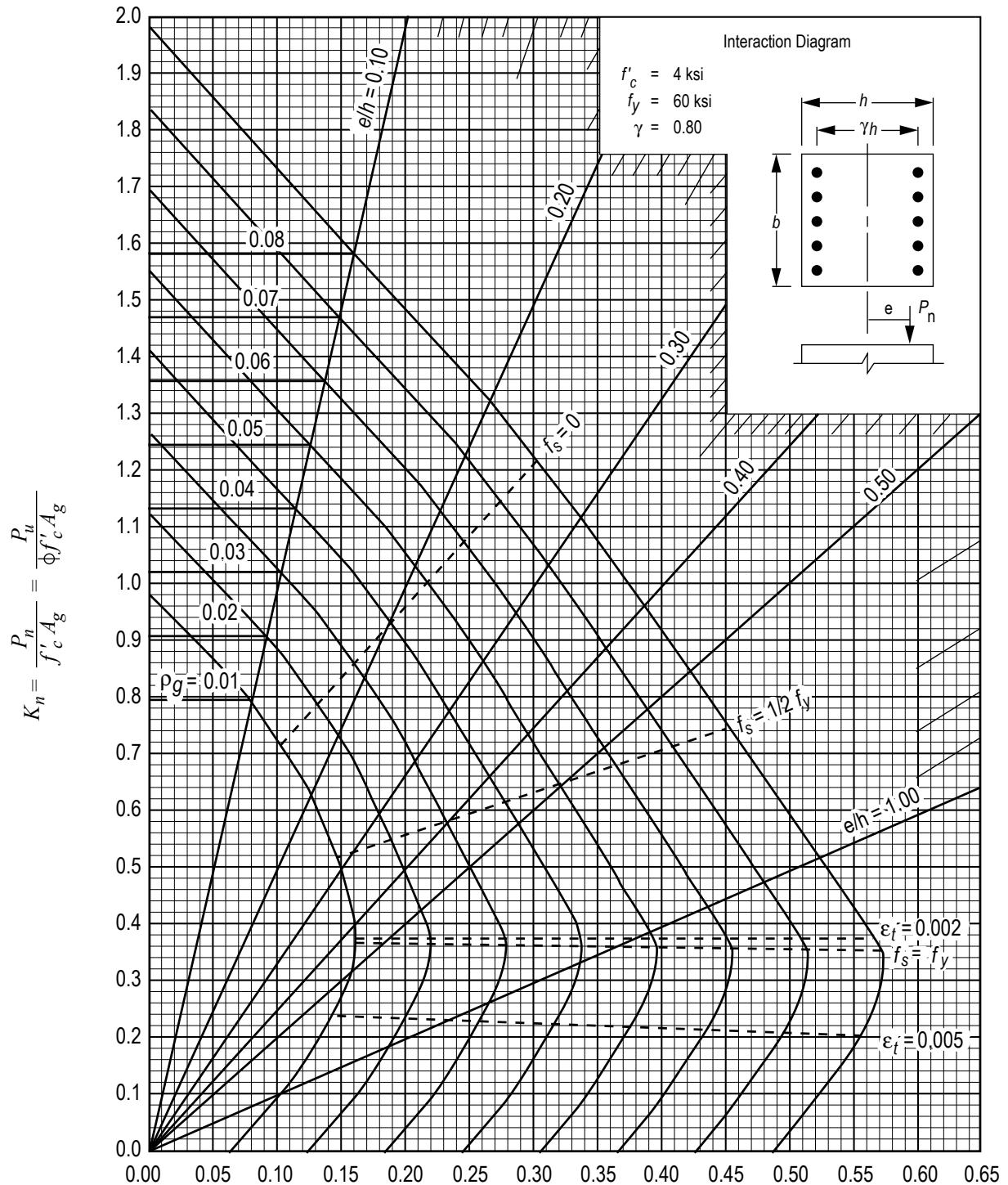
$$\rho_g = \frac{A_{st}}{A_g}$$

$$0.01 \leq \rho_g \leq 0.08$$

Design Column Strength, Tied Columns

$$\phi = 0.65$$

$$\phi P_n = 0.80\phi [0.85 f_c (A_g - A_{st}) + A_{st} f_y]$$



$$R_n = \frac{P_n e}{f'_c A_g h} = \frac{P_u e}{\phi f'_c A_g h}$$

GRAPH A.11

Column strength interaction diagram for rectangular section with bars on end faces and $\gamma = 0.80$ (for instructional use only).

Nilson, Arthur H., David Darwin, and Charles W. Dolan, *Design of Concrete Structures*, 13th ed., McGraw-Hill, 2004.

DESIGN OF STEEL COMPONENTS

(ANSI/AISC 360-10)

LRFD, $E = 29,000$ ksi

BEAMS

For doubly symmetric compact I-shaped members bent about their major axis, the *design flexural strength* $\phi_b M_n$ is determined with $\phi_b = 0.90$ as follows:

Yielding

$$M_n = M_p = F_y Z_x$$

where

F_y = specified minimum yield stress

Z_x = plastic section modulus about the x-axis

Lateral-Torsional Buckling

Based on bracing where L_b is the length between points that are either braced against lateral displacement of the compression flange or braced against twist of the cross section with respect to the length limits L_p and L_r :

When $L_b \leq L_p$, the limit state of lateral-torsional buckling does not apply.

When $L_p < L_b \leq L_r$,

$$M_n = C_b \left[M_p - (M_p - 0.7 F_y S_x) \left(\frac{L_b - L_p}{L_r - L_p} \right) \right] \leq M_p$$

where

$$C_b = \frac{12.5 M_{\max}}{2.5 M_{\max} + 3 M_A + 4 M_B + 3 M_C}$$

M_{\max} = absolute value of maximum moment in the unbraced segment

M_A = absolute value of maximum moment at quarter point of the unbraced segment

M_B = absolute value of maximum moment at centerline of the unbraced segment

M_C = absolute value of maximum moment at three-quarter of the unbraced segment

Shear

The *design shear strength* $\phi_v V_n$ is determined with

$\phi_v = 1.00$ for webs of rolled I-shaped members and is

determined as follows:

$$V_n = 0.6 F_y (d t_w)$$

COLUMNS

The *design compressive strength* $\phi_c P_n$ is determined with $\phi_c = 0.90$ for flexural buckling of members without slender elements and is determined as follows:

$$P_n = F_{cr} A_g$$

where the critical stress F_{cr} is determined as follows:

$$(a) \text{ When } \frac{KL}{r} \leq 4.71 \sqrt{\frac{E}{F_y}}, F_{cr} = \left[0.658 \frac{F_e}{F_y} \right] F_y$$

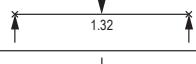
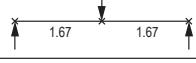
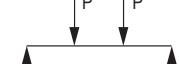
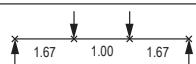
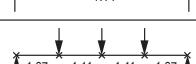
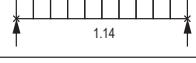
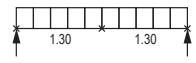
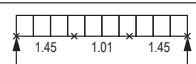
$$(b) \text{ When } \frac{KL}{r} > 4.71 \sqrt{\frac{E}{F_y}}, F_{cr} = 0.877 F_e$$

where

KL/r is the effective slenderness ratio based on the column effective length (KL) and radius of gyration (r)

KL is determined from AISC Table C-A-7.1 or AISC Figures C-A-7.1 and C-A-7.2 on p. 158.

F_e is the elastic buckling stress = $\pi^2 E / (KL/r)^2$

VALUES OF C_b FOR SIMPLY SUPPORTED BEAMS		
LOAD	LATERAL BRACING ALONG SPAN	C_b
	NONE LOAD AT MIDPOINT	
	AT LOAD POINT	
	NONE LOADS AT THIRD POINTS	
	AT LOAD POINTS LOADS SYMMETRICALLY PLACED	
	NONE LOADS AT QUARTER POINTS	
	AT LOAD POINTS LOADS AT QUARTER POINTS	
	NONE	
	AT MIDPOINT	
	AT THIRD POINTS	
	AT QUARTER POINTS	
	AT FIFTH POINTS	

NOTE: LATERAL BRACING MUST ALWAYS BE PROVIDED AT POINTS OF SUPPORT PER AISC SPECIFICATION CHAPTER F.

Adapted from *Steel Construction Manual*, 14th ed., AISC, 2011.

TENSION MEMBERS

Flat bars or angles, bolted or welded

Definitions

Bolt diameter: d_b

Nominal hole diameter: $d_h = d_b + 1/16"$

Gross width of member: b_g

Member thickness: t

Connection eccentricity: \bar{x}

Gross area: $A_g = b_g t$ (use tabulated areas for angles)

Net area (parallel holes): $A_n = \left[b_g - \sum \left(d_h + \frac{1}{16} \right) \right] t$

Net area (staggered holes):

$$A_n = \left[b_g - \sum \left(d_h + \frac{1}{16} \right) + \sum \frac{s^2}{4g} \right] t$$

s = longitudinal spacing of consecutive holes

g = transverse spacing between lines of holes

Effective area (bolted members):

$$A_e = UA_n \quad \begin{cases} \text{Flat bars: } U = 1.0 \\ \text{Angles: } U = 1 - \bar{x}/L \end{cases}$$

Effective area (welded members):

$$A_e = UA_n \quad \left\{ \begin{array}{l} \text{Flat bars or angles with transverse} \\ \text{welds: } U = 1.0 \\ \\ \text{Flat bars of width "w", longitudinal} \\ \text{welds of length "L" only:} \\ \quad U = 1.0 \ (L \geq 2w) \\ \quad U = 0.87 \ (2w > L \geq 1.5w) \\ \quad U = 0.75 \ (1.5w > L > w) \\ \\ \text{Angles with longitudinal welds} \\ \text{only} \\ \quad U = 1 - \bar{x}/L \end{array} \right.$$

Limit States and Available Strengths

Yielding:

$$\begin{aligned} \phi_y &= 0.90 \\ \phi T_n &= \phi_y F_y A_g \end{aligned}$$

Fracture:

$$\begin{aligned} \phi_f &= 0.75 \\ \phi T_n &= \phi_f F_u A_e \end{aligned}$$

Block shear:

$$\phi = 0.75$$

$U_{bs} = 1.0$ (flat bars and angles)

A_{gv} = gross area for shear

A_{nv} = net area for shear

A_{nt} = net area for tension

$$\phi T_n = \begin{cases} 0.75 F_u [0.6A_{nv} + U_{bs} A_{nt}] \\ 0.75 [0.6F_y A_{gv} + U_{bs} F_u A_{nt}] \end{cases} \text{ smaller}$$

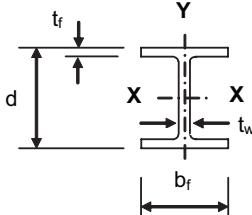


Table 1-1: W Shapes Dimensions and Properties

Shape	Area	Depth	Web	Flange		Axis X-X				Axis Y-Y	
	A	d	t _w	b _f	t _f	I	S	r	Z	I	r
	In. ²	In.	In.	In.	In.	In. ⁴	In. ³	In.	In. ³	In. ⁴	In.
W24X68	20.1	23.7	0.415	8.97	0.585	1830	154	9.55	177	70.4	1.87
W24X62	18.2	23.7	0.430	7.04	0.590	1550	131	9.23	153	34.5	1.38
W24X55	16.3	23.6	0.395	7.01	0.505	1350	114	9.11	134	29.1	1.34
W21X73	21.5	21.2	0.455	8.30	0.740	1600	151	8.64	172	70.6	1.81
W21X68	20.0	21.1	0.430	8.27	0.685	1480	140	8.60	160	64.7	1.80
W21X62	18.3	21.0	0.400	8.24	0.615	1330	127	8.54	144	57.5	1.77
W21X55	16.2	20.8	0.375	8.22	0.522	1140	110	8.40	126	48.4	1.73
W21X57	16.7	21.1	0.405	6.56	0.650	1170	111	8.36	129	30.6	1.35
W21X50	14.7	20.8	0.380	6.53	0.535	984	94.5	8.18	110	24.9	1.30
W21X48	14.1	20.6	0.350	8.14	0.430	959	93.0	8.24	107	38.7	1.66
W21X44	13.0	20.7	0.350	6.50	0.450	843	81.6	8.06	95.4	20.7	1.26
W18X71	20.8	18.5	0.495	7.64	0.810	1170	127	7.50	146	60.3	1.70
W18X65	19.1	18.4	0.450	7.59	0.750	1070	117	7.49	133	54.8	1.69
W18X60	17.6	18.2	0.415	7.56	0.695	984	108	7.47	123	50.1	1.68
W18X55	16.2	18.1	0.390	7.53	0.630	890	98.3	7.41	112	44.9	1.67
W18X50	14.7	18.0	0.355	7.50	0.570	800	88.9	7.38	101	40.1	1.65
W18X46	13.5	18.1	0.360	6.06	0.605	712	78.8	7.25	90.7	22.5	1.29
W18X40	11.8	17.9	0.315	6.02	0.525	612	68.4	7.21	78.4	19.1	1.27
W16X67	19.7	16.3	0.395	10.2	0.67	954	117	6.96	130	119	2.46
W16X57	16.8	16.4	0.430	7.12	0.715	758	92.2	6.72	105	43.1	1.60
W16X50	14.7	16.3	0.380	7.07	0.630	659	81.0	6.68	92.0	37.2	1.59
W16X45	13.3	16.1	0.345	7.04	0.565	586	72.7	6.65	82.3	32.8	1.57
W16X40	11.8	16.0	0.305	7.00	0.505	518	64.7	6.63	73.0	28.9	1.57
W16X36	10.6	15.9	0.295	6.99	0.430	448	56.5	6.51	64.0	24.5	1.52
W14X74	21.8	14.2	0.450	10.1	0.785	795	112	6.04	126	134	2.48
W14X68	20.0	14.0	0.415	10.0	0.720	722	103	6.01	115	121	2.46
W14X61	17.9	13.9	0.375	9.99	0.645	640	92.1	5.98	102	107	2.45
W14X53	15.6	13.9	0.370	8.06	0.660	541	77.8	5.89	87.1	57.7	1.92
W14X48	14.1	13.8	0.340	8.03	0.595	484	70.2	5.85	78.4	51.4	1.91
W12X79	23.2	12.4	0.470	12.1	0.735	662	107	5.34	119	216	3.05
W12X72	21.1	12.3	0.430	12.0	0.670	597	97.4	5.31	108	195	3.04
W12X65	19.1	12.1	0.390	12.0	0.605	533	87.9	5.28	96.8	174	3.02
W12X58	17.0	12.2	0.360	10.0	0.640	475	78.0	5.28	86.4	107	2.51
W12X53	15.6	12.1	0.345	9.99	0.575	425	70.6	5.23	77.9	95.8	2.48
W12X50	14.6	12.2	0.370	8.08	0.640	391	64.2	5.18	71.9	56.3	1.96
W12X45	13.1	12.1	0.335	8.05	0.575	348	57.7	5.15	64.2	50.0	1.95
W12X40	11.7	11.9	0.295	8.01	0.515	307	51.5	5.13	57.0	44.1	1.94
W10x60	17.6	10.2	0.420	10.1	0.680	341	66.7	4.39	74.6	116	2.57
W10x54	15.8	10.1	0.370	10.0	0.615	303	60.0	4.37	66.6	103	2.56
W10x49	14.4	10.0	0.340	10.0	0.560	272	54.6	4.35	60.4	93.4	2.54
W10x45	13.3	10.1	0.350	8.02	0.620	248	49.1	4.32	54.9	53.4	2.01
W10x39	11.5	9.92	0.315	7.99	0.530	209	42.1	4.27	46.8	45.0	1.98

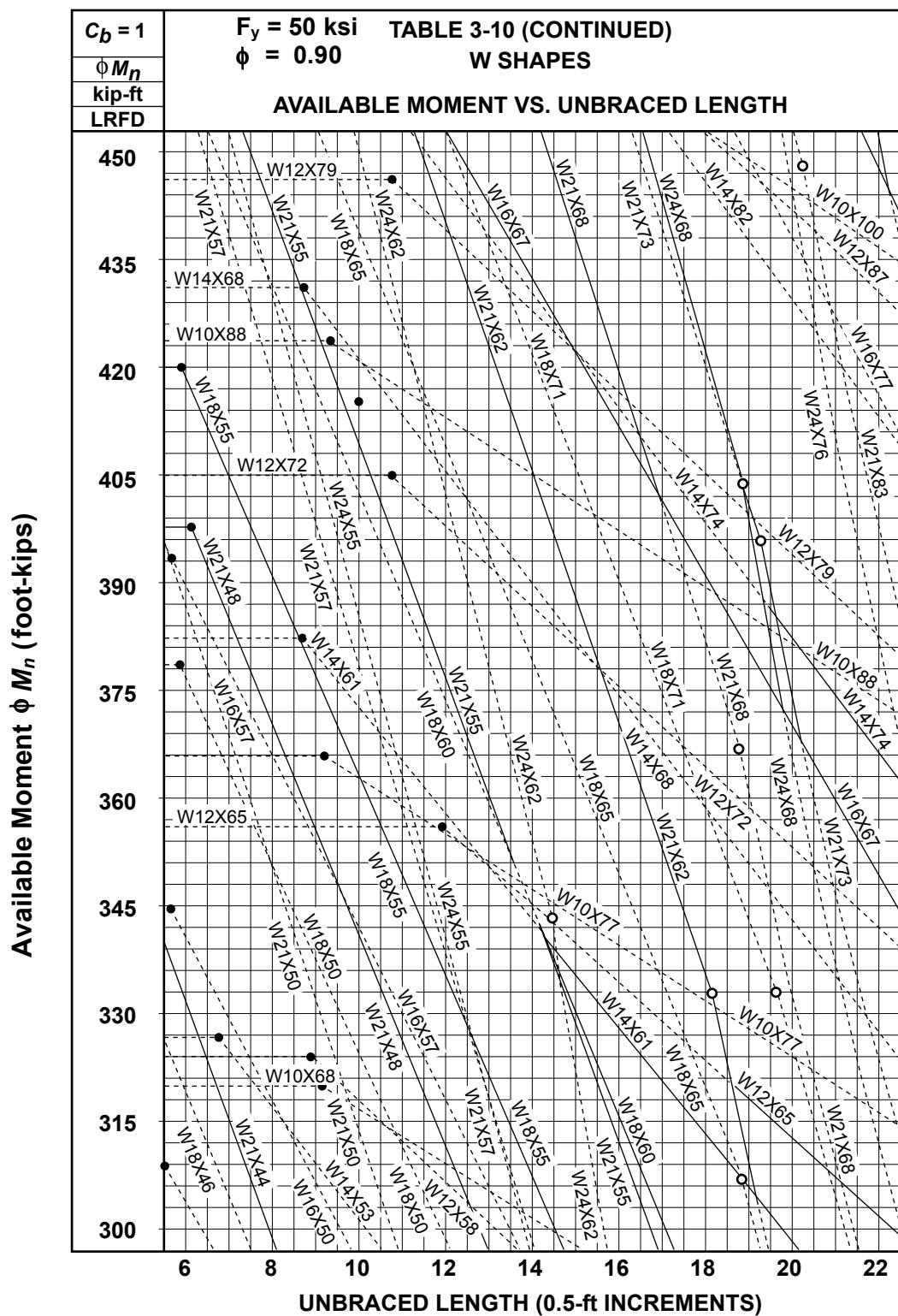
Adapted from *Steel Construction Manual*, 14th ed., AISC, 2011.

AISC Table 3-2 W Shapes – Selection by Z_x								
	Z_x							
Shape	Z_x in. ³	$\phi_b M_{px}$ kip-ft	$\phi_b M_{rx}$ kip-ft	$\phi_b BF$ kips	L_p ft.	L_r ft.	I_x in. ⁴	$\phi_v V_{nx}$ kips
W24 x 55	134	503	299	22.2	4.73	13.9	1350	251
W18 x 65	133	499	307	14.9	5.97	18.8	1070	248
W12 x 87	132	495	310	5.76	10.8	43.0	740	194
W16 x 67	130	488	307	10.4	8.69	26.1	954	194
W10 x 100	130	488	294	4.01	9.36	57.7	623	226
W21 x 57	129	484	291	20.1	4.77	14.3	1170	256
W21 x 55	126	473	289	16.3	6.11	17.4	1140	234
W14 x 74	126	473	294	8.03	8.76	31.0	795	191
W18 x 60	123	461	284	14.5	5.93	18.2	984	227
W12 x 79	119	446	281	5.67	10.8	39.9	662	175
W14 x 68	115	431	270	7.81	8.69	29.3	722	175
W10 x 88	113	424	259	3.95	9.29	51.1	534	197
W18 x 55	112	420	258	13.9	5.90	17.5	890	212
W21 x 50	110	413	248	18.3	4.59	13.6	984	237
W12 x 72	108	405	256	5.59	10.7	37.4	597	158
W21 x 48	107	398	244	14.7	6.09	16.6	959	217
W16 x 57	105	394	242	12.0	5.56	18.3	758	212
W14 x 61	102	383	242	7.46	8.65	27.5	640	156
W18 x 50	101	379	233	13.1	5.83	17.0	800	192
W10 x 77	97.6	366	225	3.90	9.18	45.2	455	169
W12 x 65	96.8	356	231	5.41	11.9	35.1	533	142
W21 x 44	95.4	358	214	16.8	4.45	13.0	843	217
W16 x 50	92.0	345	213	11.4	5.62	17.2	659	185
W18 x 46	90.7	340	207	14.6	4.56	13.7	712	195
W14 x 53	87.1	327	204	7.93	6.78	22.2	541	155
W12 x 58	86.4	324	205	5.66	8.87	29.9	475	132
W10 x 68	85.3	320	199	3.86	9.15	40.6	394	147
W16 x 45	82.3	309	191	10.8	5.55	16.5	586	167
W18 x 40	78.4	294	180	13.3	4.49	13.1	612	169
W14 x 48	78.4	294	184	7.66	6.75	21.1	484	141
W12 x 53	77.9	292	185	5.48	8.76	28.2	425	125
W10 x 60	74.6	280	175	3.80	9.08	36.6	341	129
W16 x 40	73.0	274	170	10.1	5.55	15.9	518	146
W12 x 50	71.9	270	169	5.97	6.92	23.9	391	135
W8 x 67	70.1	263	159	2.60	7.49	47.7	272	154
W14 x 43	69.6	261	164	7.24	6.68	20.0	428	125
W10 x 54	66.6	250	158	3.74	9.04	33.7	303	112
W18 x 35	66.5	249	151	12.3	4.31	12.4	510	159
W12 x 45	64.2	241	151	5.75	6.89	22.4	348	121
W16 x 36	64.0	240	148	9.31	5.37	15.2	448	140
W14 x 38	61.5	231	143	8.10	5.47	16.2	385	131
W10 x 49	60.4	227	143	3.67	8.97	31.6	272	102
W8 x 58	59.8	224	137	2.56	7.42	41.7	228	134
W12 x 40	57.0	214	135	5.50	6.85	21.1	307	106
W10 x 45	54.9	206	129	3.89	7.10	26.9	248	106

$$M_{rx} = (0.7F_y)S_x$$

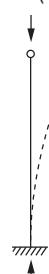
$$BF = \frac{M_{px} - M_{rx}}{L_r - L_p}$$

Adapted from *Steel Construction Manual*, 14th ed., AISC, 2011.



Steel Construction Manual, 14th ed., AISC, 2011.

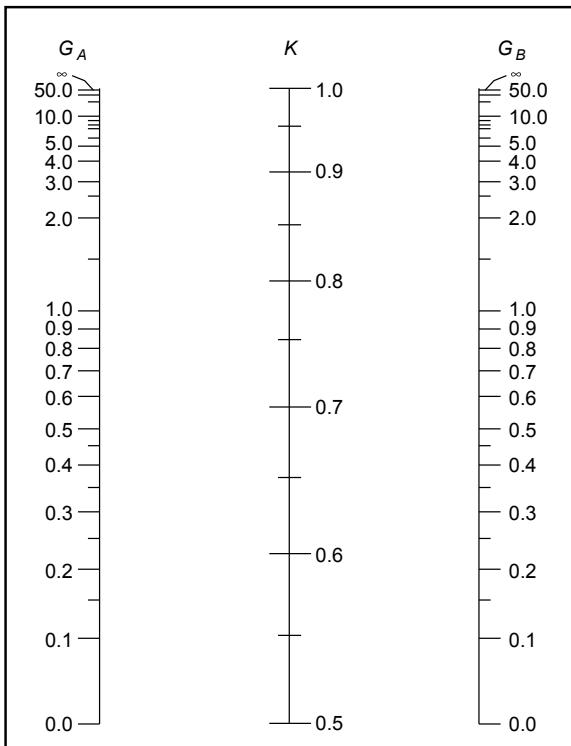
TABLE C-A-7.1
APPROXIMATE VALUES OF EFFECTIVE LENGTH FACTOR, K

BUCKLED SHAPE OF COLUMN IS SHOWN BY DASHED LINE.	(a)	(b)	(c)	(d)	(e)	(f)
						
THEORETICAL K VALUE	0.5	0.7	1.0	1.0	2.0	2.0
RECOMMENDED DESIGN VALUE WHEN IDEAL CONDITIONS ARE APPROXIMATED	0.65	0.80	1.2	1.0	2.10	2.0
END CONDITION CODE						
	 ROTATION FIXED AND TRANSLATION FIXED					
	 ROTATION FREE AND TRANSLATION FIXED					
	 ROTATION FIXED AND TRANSLATION FREE					
	 ROTATION FREE AND TRANSLATION FREE					

FOR COLUMN ENDS SUPPORTED BY, BUT NOT RIGIDLY CONNECTED TO, A FOOTING OR FOUNDATION, G IS THEORETICALLY INFINITY BUT UNLESS DESIGNED AS A TRUE FRICTION-FREE PIN, MAY BE TAKEN AS 10 FOR PRACTICAL DESIGNS. IF THE COLUMN END IS RIGIDLY ATTACHED TO A PROPERLY DESIGNED FOOTING, G MAY BE TAKEN AS 1.0. SMALLER VALUES MAY BE USED IF JUSTIFIED BY ANALYSIS.

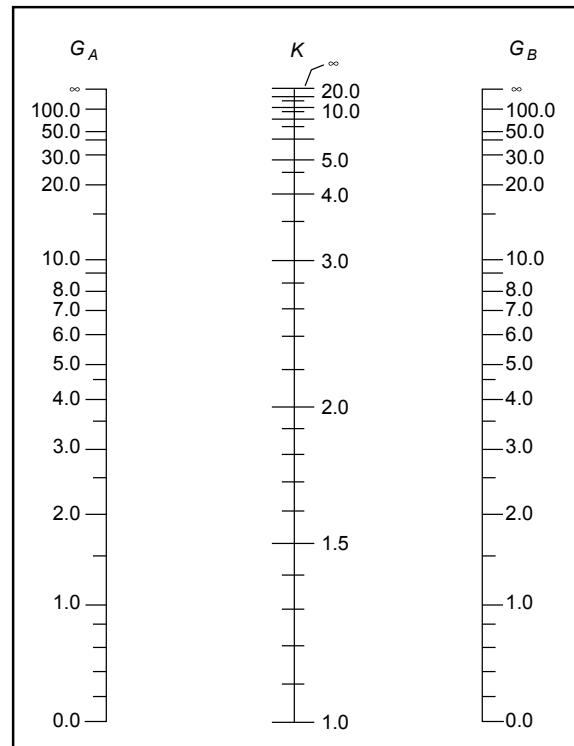
AISC Figure C-A-7.1

Alignment chart, sidesway inhibited (braced frame)



AISC Figure C-A-7.2

Alignment chart, sidesway uninhibited (moment frame)



AISC Table 4-22
 Available Critical Stress $\phi_c F_{cr}$ for Compression Members
 $F_y = 50$ ksi $\phi_c = 0.90$

$\frac{KL}{r}$	ϕF_{cr} ksi								
1	45.0	41	39.8	81	27.9	121	15.4	161	8.72
2	45.0	42	39.5	82	27.5	122	15.2	162	8.61
3	45.0	43	39.3	83	27.2	123	14.9	163	8.50
4	44.9	44	39.1	84	26.9	124	14.7	164	8.40
5	44.9	45	38.8	85	26.5	125	14.5	165	8.30
6	44.9	46	38.5	86	26.2	126	14.2	166	8.20
7	44.8	47	38.3	87	25.9	127	14.0	167	8.10
8	44.8	48	38.0	88	25.5	128	13.8	168	8.00
9	44.7	49	37.7	89	25.2	129	13.6	169	7.89
10	44.7	50	37.5	90	24.9	130	13.4	170	7.82
11	44.6	51	37.2	91	24.6	131	13.2	171	7.73
12	44.5	52	36.9	92	24.2	132	13.0	172	7.64
13	44.4	53	36.7	93	23.9	133	12.8	173	7.55
14	44.4	54	36.4	94	23.6	134	12.6	174	7.46
15	44.3	55	36.1	95	23.3	135	12.4	175	7.38
16	44.2	56	35.8	96	22.9	136	12.2	176	7.29
17	44.1	57	35.5	97	22.6	137	12.0	177	7.21
18	43.9	58	35.2	98	22.3	138	11.9	178	7.13
19	43.8	59	34.9	99	22.0	139	11.7	179	7.05
20	43.7	60	34.6	100	21.7	140	11.5	180	6.97
21	43.6	61	34.3	101	21.3	141	11.4	181	6.90
22	43.4	62	34.0	102	21.0	142	11.2	182	6.82
23	43.3	63	33.7	103	20.7	143	11.0	183	6.75
24	43.1	64	33.4	104	20.4	144	10.9	184	6.67
25	43.0	65	33.0	105	20.1	145	10.7	185	6.60
26	42.8	66	32.7	106	19.8	146	10.6	186	6.53
27	42.7	67	32.4	107	19.5	147	10.5	187	6.46
28	42.5	68	32.1	108	19.2	148	10.3	188	6.39
29	42.3	69	31.8	109	18.9	149	10.2	189	6.32
30	42.1	70	31.4	110	18.6	150	10.0	190	6.26
31	41.9	71	31.1	111	18.3	151	9.91	191	6.19
32	41.8	72	30.8	112	18.0	152	9.78	192	6.13
33	41.6	73	30.5	113	17.7	153	9.65	193	6.06
34	41.4	74	30.2	114	17.4	154	9.53	194	6.00
35	41.2	75	29.8	115	17.1	155	9.40	195	5.94
36	40.9	76	29.5	116	16.8	156	9.28	196	5.88
37	40.7	77	29.2	117	16.5	157	9.17	197	5.82
38	40.5	78	28.8	118	16.2	158	9.05	198	5.76
39	40.3	79	28.5	119	16.0	159	8.94	199	5.70
40	40.0	80	28.2	120	15.7	160	8.82	200	5.65

Adapted from *Steel Construction Manual*, 14th ed., AISC, 2011.

		AISC Table 4-1 Available Strength in Axial Compression, kips—W shapes LRFD: ϕP_n												$F_y = 50 \text{ ksi}$ $\phi c = 0.90$		
Shape wt/ft		W14					W12					W10				
		74	68	61	53	48	58	53	50	45	40	60	54	49	45	39
Effective length KL (ft) with respect to least radius of gyration r_y	0	980	899	806	702	636	767	701	657	590	526	794	712	649	597	516
	6	922	844	757	633	573	722	659	595	534	475	750	672	612	543	469
	7	901	826	740	610	552	707	644	574	516	458	734	658	599	525	452
	8	878	804	721	585	529	689	628	551	495	439	717	643	585	505	435
	9	853	781	700	557	504	670	610	526	472	419	698	625	569	483	415
	10	826	755	677	528	477	649	590	499	448	397	677	607	551	460	395
	11	797	728	652	497	449	627	569	471	422	375	655	586	533	435	373
	12	766	700	626	465	420	603	547	443	396	351	631	565	513	410	351
	13	734	670	599	433	391	578	525	413	370	328	606	543	493	384	328
	14	701	639	572	401	361	553	501	384	343	304	581	520	471	358	305
	15	667	608	543	369	332	527	477	354	317	280	555	496	450	332	282
	16	632	576	515	338	304	500	452	326	291	257	528	472	428	306	260
	17	598	544	486	308	276	473	427	297	265	234	501	448	405	281	238
	18	563	512	457	278	250	446	402	270	241	212	474	423	383	256	216
	19	528	480	428	250	224	420	378	244	217	191	447	399	360	233	195
	20	494	448	400	226	202	393	353	220	196	172	420	375	338	210	176
	22	428	387	345	186	167	342	306	182	162	142	367	327	295	174	146
	24	365	329	293	157	140	293	261	153	136	120	317	282	254	146	122
	26	311	281	250	133	120	249	222	130	116	102	270	241	216	124	104
	28	268	242	215	115	103	215	192	112	99.8	88.0	233	208	186	107	90.0
	30	234	211	187	100	89.9	187	167	97.7	87.0	76.6	203	181	162	93.4	78.4
	32	205	185	165	88.1		165	147	82.9	76.4	67.3	179	159	143	82.1	68.9
	34	182	164	146			146	130				158	141	126		
	36	162	146	130			130	116				141	126	113		
	38	146	131	117			117	104				127	113	101		
	40	131	119	105			105	93.9				114	102	91.3		

Heavy line indicates KL/r equal to or greater than 200Adapted from *Steel Construction Manual*, 14th ed., AISC, 2011

HYDROLOGY/WATER RESOURCES

NRCS (SCS) Rainfall-Runoff

$$Q = \frac{(P - 0.2S)^2}{P + 0.8S}$$

$$S = \frac{1,000}{CN} - 10$$

$$CN = \frac{1,000}{S + 10}$$

P = precipitation (inches)

S = maximum basin retention (inches)

Q = runoff (inches)

CN = curve number

Rational Formula

$$Q = CIA, \text{ where}$$

A = watershed area (acres)

C = runoff coefficient

I = rainfall intensity (in./hr)

Q = peak discharge (cfs)

Darcy's Law

$$Q = -KA(dh/dx), \text{ where}$$

Q = discharge rate (ft^3/sec or m^3/s)

K = hydraulic conductivity (ft/sec or m/s)

h = hydraulic head (ft or m)

A = cross-sectional area of flow (ft^2 or m^2)

$$q = -K(dh/dx)$$

q = specific discharge (also called Darcy velocity or superficial velocity)

$$v = q/n = -K/n(dh/dx)$$

v = average seepage velocity

n = effective porosity

Unit hydrograph: The direct runoff hydrograph that would result from one unit of runoff occurring uniformly in space and time over a specified period of time.

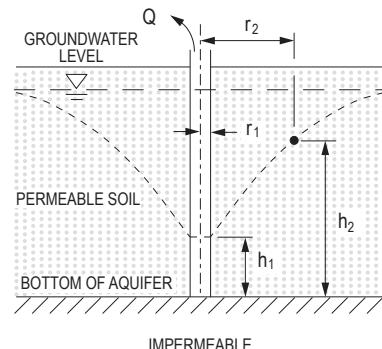
Transmissivity, T : The product of hydraulic conductivity and thickness, b , of the aquifer ($L^2 T^{-1}$).

Storage coefficient of an aquifer, S :

The volume of water taken into or released from storage per unit surface area per unit change in potentiometric (piezometric) head.

Well Drawdown

Unconfined aquifer



Dupuit's Formula

$$Q = \frac{\pi K(h_2^2 - h_1^2)}{\ln\left(\frac{r_2}{r_1}\right)}, \text{ where}$$

Q = flow rate of water drawn from well (cfs)

K = coefficient of permeability of soil

= hydraulic conductivity (ft/sec)

h_1 = height of water surface above bottom of aquifer at perimeter of well (ft)

h_2 = height of water surface above bottom of aquifer at distance r_2 from well centerline (ft)

r_1 = radius to water surface at perimeter of well, i.e., radius of well (ft)

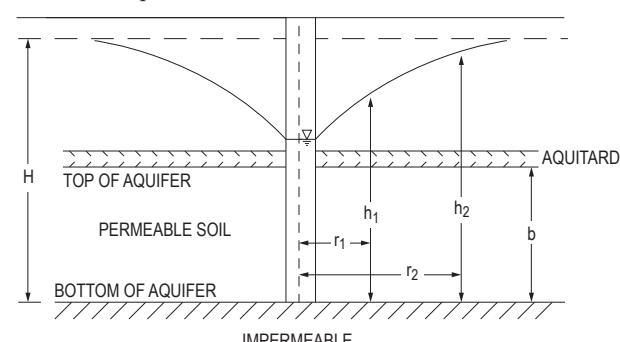
r_2 = radius to water surface whose height is h_2 above bottom of aquifer (ft)

\ln = natural logarithm

Q/D_w = specific capacity

D_w = well drawdown (ft)

Confined aquifer:



Theim Equation

$$Q = \frac{2\pi T(h_2 - h_1)}{\ln\left(\frac{r_2}{r_1}\right)}, \text{ where}$$

T = Kb = transmissivity (ft^2/sec)

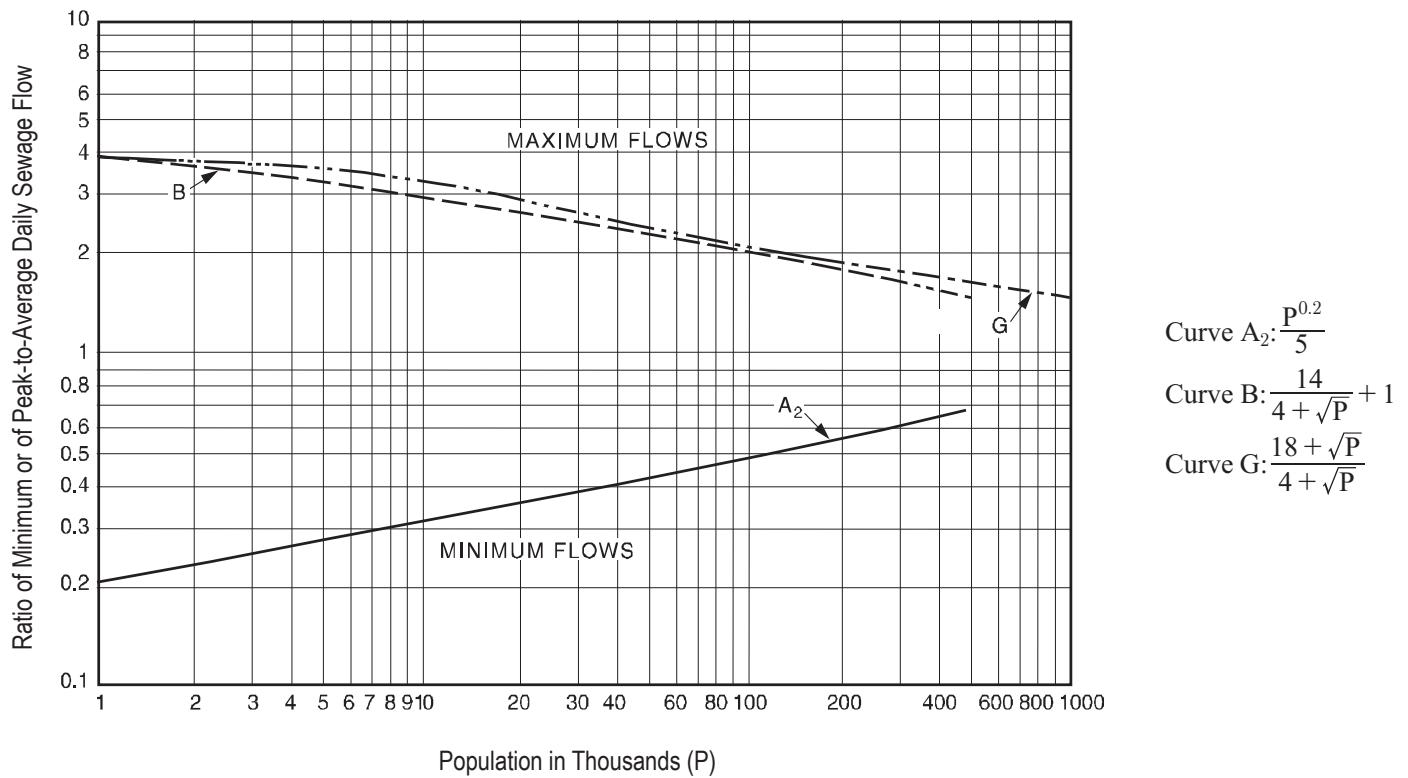
b = thickness of confined aquifer (ft)

h_1, h_2 = heights of piezometric surface above bottom of aquifer (ft)

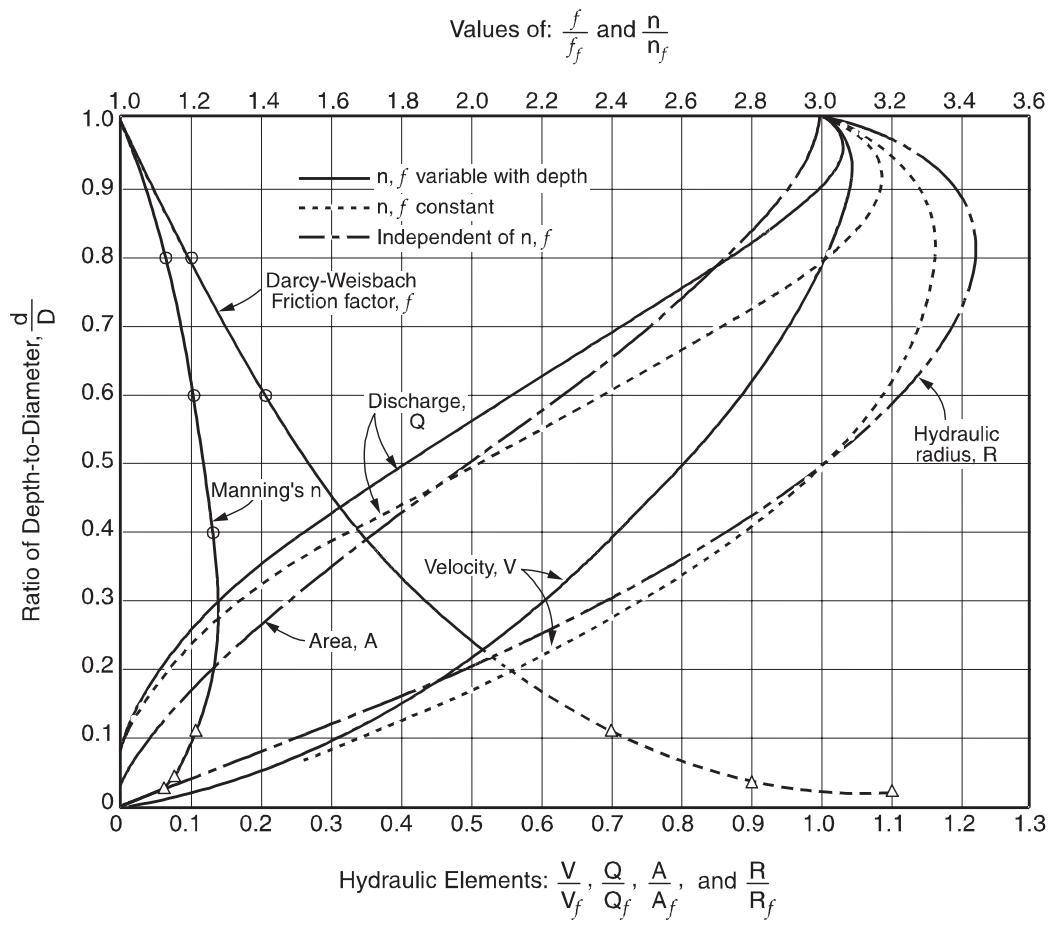
r_1, r_2 = radii from pumping well (ft)

\ln = natural logarithm

◆ Sewage Flow Ratio Curves



◆ Hydraulic-Elements Graph for Circular Sewers



◆ Design and Construction of Sanitary and Storm Sewers, Water Pollution Control Federation and American Society of Civil Engineers, 1970. Reprinted with permission from ASCE. This material may be downloaded from ncees.org for personal use only. Any other use requires prior permission of ASCE.

Open-Channel Flow

Specific Energy

$$E = \alpha \frac{V^2}{2g} + y = \frac{\alpha Q^2}{2gA^2} + y, \text{ where}$$

E = specific energy

Q = discharge

V = velocity

y = depth of flow

A = cross-sectional area of flow

α = kinetic energy correction factor, usually 1.0

Critical Depth = that depth in a channel at minimum specific energy

$$\frac{Q^2}{g} = \frac{A^3}{T}$$

where Q and A are as defined above,

g = acceleration due to gravity

T = width of the water surface

For rectangular channels

$$y_c = \left(\frac{q^2}{g} \right)^{1/3}, \text{ where}$$

y_c = critical depth

q = unit discharge = Q/B

B = channel width

g = acceleration due to gravity

Froude Number = ratio of inertial forces to gravity forces

$$Fr = \frac{V}{\sqrt{gy_h}} = \sqrt{\frac{Q^2 T}{g A^3}}, \text{ where}$$

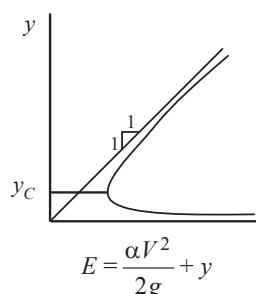
y_h = hydraulic depth = A/T

Supercritical flow: $Fr > 1$

Subcritical flow: $Fr < 1$

Critical flow: $Fr = 1$

Specific Energy Diagram

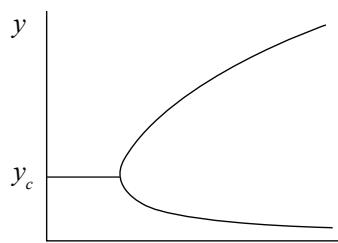


$$E = \frac{\alpha V^2}{2g} + y$$

Alternate depths: depths with the same specific energy

Uniform flow: a flow condition where depth and velocity do not change along a channel

Momentum Depth Diagram



$$M = \frac{Q^2}{gA} + Ah_c, \text{ where}$$

h_c = vertical distance from liquid surface to centroid of area
Sequent (conjugate) depths: depths with the same momentum

Hydraulic Jump

$$y_2 = \frac{y_1}{2} \left(-1 + \sqrt{1 + 8 Fr_1^2} \right), \text{ where}$$

y_1 = flow depth at upstream supercritical flow location

y_2 = flow depth at downstream subcritical flow location

Fr_1 = Froude number at upstream supercritical flow location

Manning's Equation

$$Q = \frac{K}{n} A R_H^{2/3} S^{1/2}$$

Q = discharge (ft^3/sec or m^3/s)

K = 1.0 for SI units, 1.486 for USCS units

A = cross-sectional area of flow (ft^2 or m^2)

R_H = hydraulic radius = A/P (ft or m)

P = wetted perimeter (ft or m)

S = slope of hydraulic surface (ft/ft or m/m)

n = Manning's roughness coefficient

Weir Formulas

Rectangular

Free discharge suppressed

$$Q = CLH^{3/2}$$

Free discharge contracted

$$Q = C(L - 0.2H)H^{3/2}$$

V-Notch

$$Q = CH^{5/2}, \text{ where}$$

Q = discharge (cfs or m^3/s)

C = 3.33 for rectangular weir (USCS units)

C = 1.84 for rectangular weir (SI units)

C = 2.54 for 90° V-notch weir (USCS units)

C = 1.40 for 90° V-notch weir (SI units)

L = weir length (ft or m)

H = head (depth of discharge over weir) ft or m

Hazen-Williams Equation

$$V = k_1 C R_H^{0.63} S^{0.54}, \text{ where}$$

C = roughness coefficient

k_1 = 0.849 for SI units

k_1 = 1.318 for USCS units

R_H = hydraulic radius (ft or m)

S = slope of energy grade line

$$= h_f/L \text{ (ft/ft or m/m)}$$

V = velocity (ft/sec or m/s)

Circular Pipe Head Loss Equation (Head Loss Expressed in Feet)

$$h_f = \frac{4.73 L}{C^{1.852} D^{4.87}} Q^{1.852}, \text{ where}$$

h_f = head loss (ft)

L = pipe length (ft)

D = pipe diameter (ft)

Q = flow (cfs)

C = Hazen-Williams coefficient

Circular Pipe Head Loss Equation (Head Loss Expressed as Pressure)

U.S. Customary Units

$$P = \frac{4.52 Q^{1.85}}{C^{1.85} D^{4.87}}, \text{ where}$$

P = pressure loss (psi per foot of pipe)

Q = flow (gpm)

D = pipe diameter (inches)

C = Hazen-Williams coefficient

SI Units

$$P = \frac{6.05 Q^{1.85}}{C^{1.85} D^{4.87}} \times 10^5, \text{ where}$$

P = pressure loss (bars per meter of pipe)

Q = flow (liters/minute)

D = pipe diameter (mm)

Values of Hazen-Williams Coefficient C

Pipe Material	C
Ductile iron	140
Concrete (regardless of age)	130
Cast iron:	
New	130
5 yr old	120
20 yr old	100
Welded steel, new	120
Wood stave (regardless of age)	120
Vitrified clay	110
Riveted steel, new	110
Brick sewers	100
Asbestos-cement	140
Plastic	150

♦ Formula for Calculating Rated Capacity at 20 psi from Fire Hydrant

$$Q_R = Q_F \times (H_R/H_F)^{0.54}, \text{ where}$$

Q_R = rated capacity (gpm) at 20 psi

Q_F = total test flow

H_R = $P_S - 20$ psi

H_F = $P_S - P_R$

P_S = static pressure

P_R = residual pressure

♦ Fire Hydrant Discharging to Atmosphere

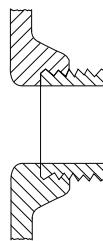
$$Q = 29.8 D^2 C_d P^{1/2}, \text{ where}$$

Q = discharge (gpm)

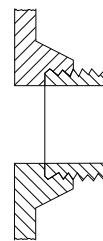
D = outlet diameter (in.)

P = pressure detected by pitot gage (psi)

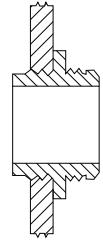
C_d = hydrant coefficient based on hydrant outlet geometry



OUTLET SMOOTH
AND WELL-ROUNDED
COEF. 0.90



OUTLET SQUARE
AND SHARP
COEF. 0.80



OUTLET SQUARE AND
PROJECTING INTO BARREL
COEF. 0.70

• Fire Sprinkler Discharge

$$Q = K P^{1/2}, \text{ where}$$

Q = flow (gpm)

K = measure of the ease of getting water out of the orifice, related to size and shape of the orifice in units of gpm per (psi)^{1/2}

P = pressure (psi)

Sprinkler K Factors

Orifice Size	Name	K Factor
1/2"	Standard	5.6
17/32"	Large	8.0
5/8"	Extra large	11.2

♦ NFPA Standard 291, *Recommended Practice for Fire Flow Testing and Marking of Hydrants*, Section 4.10.1.2

• Isman, Kenneth E., P.E., 2001, "Which Sprinkler to Choose?", *Fire Protection Engineering*, Winter 2001 (9), Society of Fire Protection Engineers, p. 28.

TRANSPORTATION

U.S. Customary Units

a	= deceleration rate (ft/sec^2)
A	= absolute value of algebraic difference in grades (%)
e	= superelevation (%)
f	= side friction factor
$\pm G$	= percent grade divided by 100 (uphill grade "+")
h_1	= height of driver's eyes above the roadway surface (ft)
h_2	= height of object above the roadway surface (ft)
L	= length of curve (ft)
L_s	= spiral transition length (ft)
R	= radius of curve (ft)
SSD	= stopping sight distance (ft)
t	= driver reaction time (sec)
V	= design speed (mph)
v	= vehicle approach speed (fps)
W	= width of intersection, curb-to-curb (ft)
l	= length of vehicle (ft)
y	= length of yellow interval to nearest 0.1 sec (sec)
r	= length of red clearance interval to nearest 0.1 sec (sec)

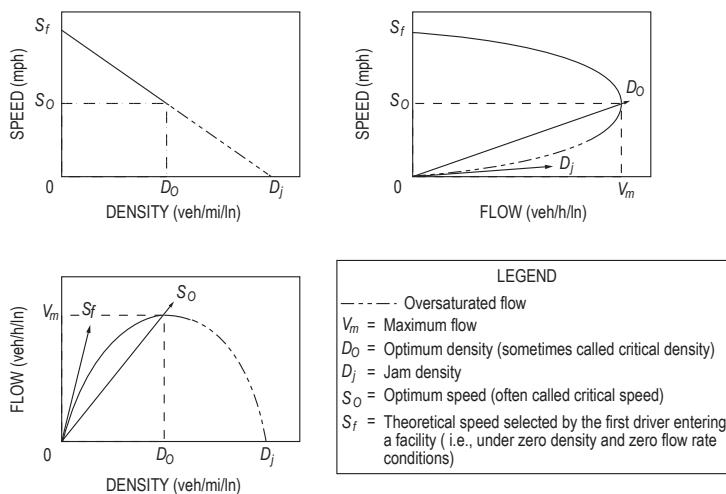
Vehicle Signal Change Interval

$$y = t + \frac{v}{2a \pm 64.4G}$$
$$r = \frac{W + l}{v}$$

Stopping Sight Distance

$$SSD = 1.47Vt + \frac{V^2}{30\left(\left(\frac{a}{32.2}\right) \pm G\right)}$$

Traffic Flow Relationships



Vertical Curves: Sight Distance Related to Curve Length

	$S \leq L$	$S > L$
Crest Vertical Curve General equation:	$L = \frac{AS^2}{100(\sqrt{2h_1} + \sqrt{2h_2})^2}$	$L = 2S - \frac{200(\sqrt{h_1} + \sqrt{h_2})^2}{A}$
Standard Criteria: $h_1 = 3.50$ ft and $h_2 = 2.0$ ft:	$L = \frac{AS^2}{2,158}$	$L = 2S - \frac{2,158}{A}$
Sag Vertical Curve (based on standard headlight criteria)	$L = \frac{AS^2}{400 + 3.5S}$	$L = 2S - \left(\frac{400 + 3.5S}{A} \right)$
Sag Vertical Curve (based on riding comfort)		$L = \frac{AV^2}{46.5}$
Sag Vertical Curve (based on adequate sight distance under an overhead structure to see an object beyond a sag vertical curve)	$L = \frac{AS^2}{800 \left(C - \frac{h_1 + h_2}{2} \right)}$	$L = 2S - \frac{800}{A} \left(C - \frac{h_1 + h_2}{2} \right)$
$C = \text{vertical clearance for overhead structure (overpass) located within 200 feet of the midpoint of the curve}$		

Horizontal Curves	
Side friction factor (based on superelevation)	$0.01e + f = \frac{V^2}{15R}$
Spiral Transition Length	$L_s = \frac{3.15V^3}{RC}$ $C = \text{rate of increase of lateral acceleration [use } 1 \text{ ft/sec}^3 \text{ unless otherwise stated]}$
Sight Distance (to see around obstruction)	$\text{HSO} = R \left[1 - \cos \left(\frac{28.65S}{R} \right) \right]$ HSO = Horizontal sight line offset

◆ AASHTO, *A Policy on Geometric Design of Highways and Streets*, 6th ed., 2011. Used by permission.

• Compiled from AASHTO, *A Policy on Geometric Design of Highways and Streets*, 6th ed., 2011.

Horizontal Curve Formulas

- D = Degree of Curve, Arc Definition
 PC = Point of Curve (also called BC)
 PT = Point of Tangent (also called EC)
 PI = Point of Intersection
 I = Intersection Angle (also called Δ)
 Angle Between Two Tangents
 L = Length of Curve, from PC to PT
 T = Tangent Distance
 E = External Distance
 R = Radius
 LC = Length of Long Chord
 M = Length of Middle Ordinate
 c = Length of Sub-Chord
 d = Angle of Sub-Chord
 l = Curve Length for Sub-Chord

$$R = \frac{5729.58}{D}$$

$$R = \frac{LC}{2 \sin(I/2)}$$

$$T = R \tan(I/2) = \frac{LC}{2 \cos(I/2)}$$

$$L = RI \frac{\pi}{180} = \frac{I}{D} 100$$

$$M = R[1 - \cos(I/2)]$$

$$\frac{R}{E + R} = \cos(I/2)$$

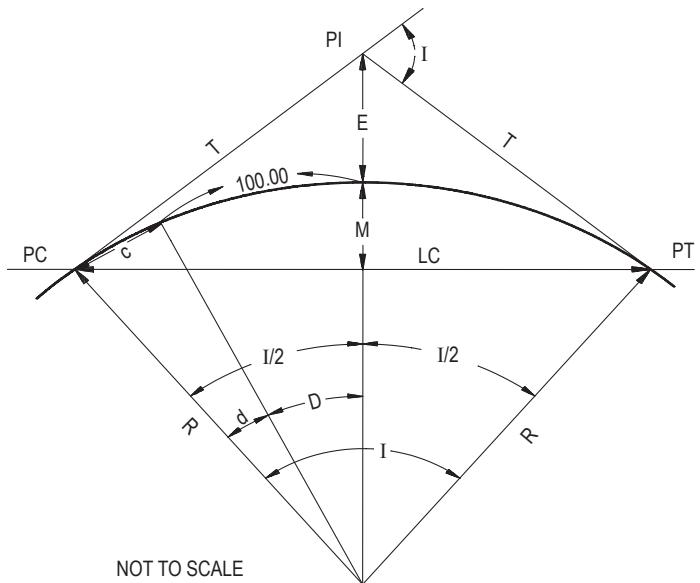
$$\frac{R - M}{R} = \cos(I/2)$$

$$c = 2R \sin(d/2)$$

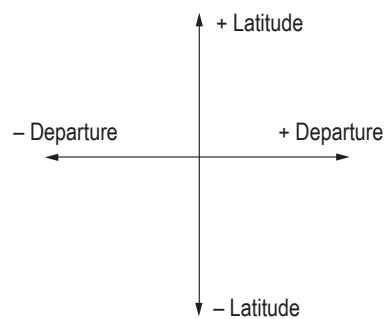
$$l = Rd \left(\frac{\pi}{180} \right)$$

$$E = R \left[\frac{1}{\cos(I/2)} - 1 \right]$$

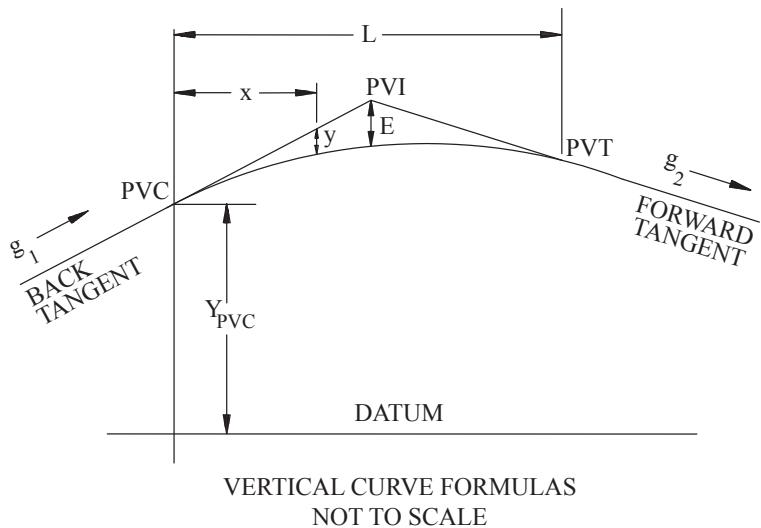
Deflection angle per 100 feet of arc length equals $D/2$



LATITUDES AND DEPARTURES



Vertical Curve Formulas



L = Length of curve

PVC = Point of vertical curvature

PVI = Point of vertical intersection

PVT = Point of vertical tangency

g_1 = Grade of back tangent

x = Horizontal distance from PVC to point on curve

g_2 = Grade of forward tangent

a = Parabola constant

y = Tangent offset

E = Tangent offset at $PVI = AL/800$

r = Rate of change of grade

K = Rate of vertical curvature

$$x_m = \text{Horizontal distance to min/max elevation on curve} = -\frac{g_1}{2a} = \frac{g_1 L}{g_1 - g_2}$$

$$\text{Tangent elevation} = Y_{PVC} + g_1 x \text{ and } = Y_{PVI} + g_2(x - L/2)$$

$$\text{Curve elevation} = Y_{PVC} + g_1 x + ax^2 = Y_{PVC} + g_1 x + [(g_2 - g_1)/(2L)]x^2$$

$$y = ax^2 \quad a = \frac{g_2 - g_1}{2L} \quad E = a\left(\frac{L}{2}\right)^2 \quad r = \frac{g_2 - g_1}{L} \quad K = \frac{L}{A}$$

EARTHWORK FORMULAS

Average End Area Formula, $V = L(A_1 + A_2)/2$

Prismoidal Formula, $V = L(A_1 + 4A_m + A_2)/6$

where A_m = area of mid-section

L = distance between A_1 and A_2

Pyramid or Cone, $V = h (\text{Area of Base})/3$

AREA FORMULAS

Area by Coordinates: Area = $[X_A(Y_B - Y_N) + X_B(Y_C - Y_A) + X_C(Y_D - Y_B) + \dots + X_N(Y_A - Y_{N-1})]/2$

Trapezoidal Rule: Area = $w\left(\frac{h_1 + h_n}{2} + h_2 + h_3 + h_4 + \dots + h_{n-1}\right)$

w = common interval

Simpson's 1/3 Rule: Area = $w\left[h_1 + 2\left(\sum_{k=3,5,\dots}^{n-2} h_k\right) + 4\left(\sum_{k=2,4,\dots}^{n-1} h_k\right) + h_n\right]/3$

n must be odd number of measurements
(only for Simpson's 1/3 Rule)

Highway Pavement Design

AASHTO Structural Number Equation
$SN = a_1D_1 + a_2D_2 + \dots + a_nD_n$, where
SN = structural number for the pavement
a_i = layer coefficient and D_i = thickness of layer (inches).

Gross Axle Load		Load Equivalency Factors		Gross Axle Load		Load Equivalency Factors	
kN	lb	Single Axles	Tandem Axles	kN	lb	Single Axles	Tandem Axles
4.45	1,000	0.00002		187.0	42,000	25.64	2.51
8.9	2,000	0.00018		195.7	44,000	31.00	3.00
17.8	4,000	0.00209		200.0	45,000	34.00	3.27
22.25	5,000	0.00500		204.5	46,000	37.24	3.55
26.7	6,000	0.01043		213.5	48,000	44.50	4.17
35.6	8,000	0.0343		222.4	50,000	52.88	4.86
44.5	10,000	0.0877	0.00688	231.3	52,000		5.63
53.4	12,000	0.189	0.0144	240.2	54,000		6.47
62.3	14,000	0.360	0.0270	244.6	55,000		6.93
66.7	15,000	0.478	0.0360	249.0	56,000		7.41
71.2	16,000	0.623	0.0472	258.0	58,000		8.45
80.0	18,000	1.000	0.0773	267.0	60,000		9.59
89.0	20,000	1.51	0.1206	275.8	62,000		10.84
97.8	22,000	2.18	0.180	284.5	64,000		12.22
106.8	24,000	3.03	0.260	289.0	65,000		12.96
111.2	25,000	3.53	0.308	293.5	66,000		13.73
115.6	26,000	4.09	0.364	302.5	68,000		15.38
124.5	28,000	5.39	0.495	311.5	70,000		17.19
133.5	30,000	6.97	0.658	320.0	72,000		19.16
142.3	32,000	8.88	0.857	329.0	74,000		21.32
151.2	34,000	11.18	1.095	333.5	75,000		22.47
155.7	35,000	12.50	1.23	338.0	76,000		23.66
160.0	36,000	13.93	1.38	347.0	78,000		26.22
169.0	38,000	17.20	1.70	356.0	80,000		28.99
178.0	40,000	21.08	2.08				

Note: kN converted to lb are within 0.1 percent of lb shown

Superpave

PERFORMANCE-GRADED (PG) BINDER GRADING SYSTEM

PERFORMANCE GRADE	PG 52							PG 58					PG 64																
	-10	-16	-22	-28	-34	-40	-46	-16	-22	-28	-34	-40	-16	-22	-28	-34	-40												
AVERAGE 7-DAY MAXIMUM PAVEMENT DESIGN TEMPERATURE, °C ^a	<52							<58					<64																
MINIMUM PAVEMENT DESIGN TEMPERATURE, °C ^a	>-10	>-16	>-22	>-28	>-34	>-40	>-46	>-16	>-22	>-28	>-34	>-40	>-16	>-22	>-28	>-34	>-40												
ORIGINAL BINDER																													
FLASH POINT TEMP, T48: MINIMUM °C	230																												
VISCOSITY, ASTM D 4402: ^b MAXIMUM, 3 Pa·s (3,000 cP), TEST TEMP, °C	135																												
DYNAMIC SHEAR, TP5: ^c G'/sin δ , MINIMUM, 1.00 kPa TEST TEMPERATURE @ 10 rad/sec., °C	52					58					64																		
ROLLING THIN FILM OVEN (T240) OR THIN FILM OVEN (T179) RESIDUE																													
MASS LOSS, MAXIMUM, %	1.00																												
DYNAMIC SHEAR, TP5: G'/sin δ , MINIMUM, 2.20 kPa TEST TEMP @ 10 rad/sec. °C	52					58					64																		
PRESSURE AGING VESSEL RESIDUE (PP1)																													
PAV AGING TEMPERATURE, °C ^d	90							100					100																
DYNAMIC SHEAR, TP5: G'/sin δ , MAXIMUM, 5,000 kPa TEST TEMP @ 10 rad/sec. °C	25	22	19	16	13	10	7	25	22	19	16	13	28	25	22	19	16												
PHYSICAL HARDENING ^e	REPORT																												
CREEP STIFFNESS, TP1: ^f S, MAXIMUM, 300 MPa M-VALUE, MINIMUM, 0.300 TEST TEMP, @ 60 sec., °C	0	-6	-12	-18	-24	-30	-36	-6	-12	-18	-24	-30	-6	-12	-18	-24	-30												
DIRECT TENSION, TP3: ^f FAILURE STRAIN, MINIMUM, 1.0% TEST TEMP @ 1.0 mm/min, °C	0	-6	-12	-18	-24	-30	-36	-6	-12	-18	-24	-30	-6	-12	-18	-24	-30												

Federal Highway Administration Report FHWA-SA-95-03, "Background of Superpave Asphalt Mixture Design and Analysis," Nov. 1994.

Superpave Mixture Design: Compaction Requirements

TRAFFIC, MILLION ESALs	SUPERPAVE GYRATORY COMPACTION EFFORT											
	AVERAGE DESIGN HIGH AIR TEMPERATURE											
	< 39°C			39° – 40°C			41° – 42°C			42° – 43°C		
	N _{int}	N _{des}	N _{max}	N _{int}	N _{des}	N _{max}	N _{int}	N _{des}	N _{max}	N _{int}	N _{des}	N _{max}
< 0.3	7	68	104	7	74	114	7	78	121	7	82	127
< 1	7	76	117	7	83	129	7	88	138	8	93	146
< 3	7	86	134	8	95	150	8	100	158	8	105	167
< 10	8	96	152	8	106	169	8	113	181	9	119	192
< 30	8	109	174	9	121	195	9	128	208	9	135	220
< 100	9	126	204	9	139	228	9	146	240	10	153	253
≥ 100	9	142	233	10	158	262	10	165	275	10	177	288

VFA REQUIREMENTS @ 4% AIR VOIDS	
TRAFFIC, MILLION ESALs	DESIGN VFA (%)
< 0.3	70 – 80
< 1	65 – 78
< 3	65 – 78
< 10	65 – 75
< 30	65 – 75
< 100	65 – 75
≥ 100	65 – 75

VMA REQUIREMENTS @ 4% AIR VOIDS					
NOMINAL MAXIMUM AGGREGATE SIZE (mm)	9.5	12.5	19.0	25.0	37.5
MINIMUM VMA (%)	15	14	13	12	11

COMPACTON KEY			
SUPERPAVE GYRATORY COMPACTION	N _{int}	N _{des}	N _{max}
PERCENT OF Gmm	≤ 89%	96%	≤ 98%

Federal Highway Administration Report FHWA-SA-95-03, "Background of Superpave Asphalt Mixture Design and Analysis," Nov. 1994.

Gravity Model

$$T_{ij} = P_i \left[\frac{A_j F_{ij} K_{ij}}{\sum_j A_j F_{ij} K_{ij}} \right]$$

where

T_{ij} = number of trips that are produced in zone i and attracted to zone j

P_i = total number of trips produced in zone i

A_j = number of trips attracted to zone j

F_{ij} = a friction factor that is an inverse function of travel time between zones i and j

K_{ij} = socioeconomic adjustment factor for interchange ij

Logit Models

$$U_x = \sum_{i=1}^n a_i X_i$$

where

U_x = utility of mode x

n = number of attributes

X_i = attribute value (time, cost, and so forth)

a_i = coefficient value for attributes i (negative, since the values are disutilities)

If two modes, auto (A) and transit (T), are being considered, the probability of selecting the auto mode A can be written as

$$P(A) = \frac{e^{U_A}}{e^{U_A} + e^{U_T}} \quad P(x) = \frac{e^{U_x}}{\sum_{e=1}^n e^{U_{xi}}}$$

Traffic Safety Equations

Crash Rates at Intersections

$$RMEV = \frac{A \times 1,000,000}{V}$$

where

$RMEV$ = crash rate per million entering vehicles

A = number of crashes, total or by type occurring in a single year at the location

V = $ADT \times 365$

ADT = average daily traffic entering intersection

Crash Rates for Roadway Segments

$$RMVM = \frac{A \times 100,000,000}{VMT}$$

where

$RMVM$ = crash rate per hundred million vehicle miles

A = number of crashes, total or by type at the study location, during a given period

VMT = vehicle miles of travel during the given period

= $ADT \times (\text{number of days in study period}) \times (\text{length of road})$

ADT = average daily traffic on the roadway segment

Crash Reduction

$$\text{Crashes prevented} = N \times CR \frac{(\text{ADT after improvement})}{(\text{ADT before improvement})}$$

where

N = expected number of crashes if countermeasure is not implemented and if the traffic volume remains the same

CR = $CR_1 + (1 - CR_1)CR_2 + (1 - CR_1)(1 - CR_2)CR_3 + \dots + (1 - CR_1)\dots(1 - CR_{m-1})CR_m$

= overall crash reduction factor for multiple mutually exclusive improvements at a single site

CR_i = crash reduction factor for a specific countermeasure i

m = number of countermeasures at the site

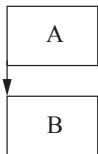
Garber, Nicholas J., and Lester A. Hoel, *Traffic and Highway Engineering*, 4th ed., Cengage Learning, 2009.

CONSTRUCTION

Construction project scheduling and analysis questions may be based on either the activity-on-node method or the activity-on-arrow method.

CPM PRECEDENCE RELATIONSHIPS

ACTIVITY-ON-NODE



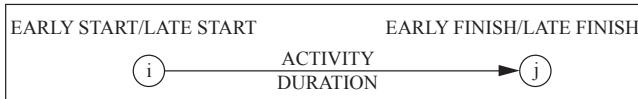
START-TO-START: START OF B
DEPENDS ON THE START OF A

FINISH-TO-FINISH: FINISH OF B
DEPENDS ON THE FINISH OF A

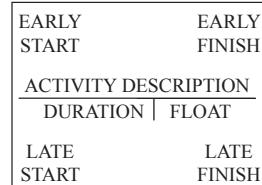


FINISH-TO-START: START OF B
DEPENDS ON THE FINISH OF A

ACTIVITY-ON-ARROW ANNOTATION



ACTIVITY-ON-NODE ANNOTATION



Nomenclature

ES = Early start = Latest EF of predecessors

EF = Early finish = ES + duration

LS = Late start = LF - duration

LF = Late finish = Earliest LS of successors

D = Duration

Float = LS - ES or LF - EF

Determining the Project Size Modifier

Square Foot Base Size							
Building Type	Median Cost per S.F.	Typical Size Gross S.F.	Typical Range Gross S.F.	Building Type	Median Cost per S.F.	Typical Size Gross S.F.	Typical Range Gross S.F.
Apartments, Low Rise	\$ 54.05	21,000	9,700–37,200	Jails	\$ 165.00	13,700	7,500–28,000
Apartments, Mid Rise	68.25	50,000	32,000–100,000	Libraries	97.30	12,000	7,000–31,000
Apartments, High Rise	78.30	310,000	100,000–650,000	Medical Clinics	93.15	7,200	4,200–15,700
Auditoriums	90.35	25,000	7,600–39,000	Medical Offices	87.50	6,000	4,000–15,000
Auto Sales	55.90	20,000	10,800–28,600	Motels	67.00	27,000	15,800–51,000
Banks	121.00	4,200	2,500–7,500	Nursing Homes	89.95	23,000	15,000–37,000
Churches	81.60	9,000	5,300–13,200	Offices, Low Rise	73.00	8,600	4,700–19,000
Clubs, Country	81.40	6,500	4,500–15,000	Offices, Mid Rise	76.65	52,000	31,300–83,100
Clubs, Social	79.15	10,000	6,000–13,500	Offices, High Rise	98.05	260,000	151,000–468,000
Clubs, YMCA	81.60	28,300	12,800–39,400	Police Stations	122.00	10,500	4,000–19,000
Colleges (Class)	107.00	50,000	23,500–98,500	Post Offices	90.40	12,400	6,800–30,000
Colleges (Science Lab)	156.00	45,600	16,600–80,000	Power Plants	678.00	7,500	1,000–20,000
College (Student Union)	119.00	33,400	16,000–85,000	Religious Education	74.85	9,000	6,000–12,000
Community Center	85.05	9,400	5,300–16,700	Research	127.00	19,000	6,300–45,000
Court Houses	116.00	32,400	17,800–106,000	Restaurants	110.00	4,400	2,800–6,000
Dept. Stores	50.50	90,000	44,000–122,000	Retail Stores	53.70	7,200	4,000–17,600
Dormitories, Low Rise	87.20	24,500	13,400–40,000	Schools, Elementary	78.20	41,000	24,500–55,000
Dormitories, Mid Rise	113.00	55,600	36,100–90,000	Schools, Jr. High	79.65	92,000	52,000–119,000
Factories	48.95	26,400	12,900–50,000	Schools, Sr. High	79.65	101,000	50,500–175,000
Fire Stations	85.45	5,800	4,000–8,700	Schools, Vocational	79.35	37,000	20,500–82,000
Fraternity Houses	84.10	12,500	8,200–14,800	Sports Arenas	66.45	15,000	5,000–40,000
Funeral Homes	94.00	7,800	4,500–11,000	Supermarkets	53.85	20,000	12,000–30,000
Garages, Commercial	59.70	9,300	5,000–13,600	Swimming Pools	125.00	13,000	7,800–22,000
Garages, Municipal	76.40	8,300	4,500–12,600	Telephone Exchange	145.00	4,500	1,200–10,600
Garages, Parking	31.30	163,000	76,400–225,300	Theaters	79.70	10,500	8,800–17,500
Gymnasiums	78.95	19,200	11,600–41,000	Town Halls	87.65	10,800	4,800–23,400
Hospitals	149.00	55,000	27,200–125,000	Warehouses	36.15	25,000	8,000–72,000
House (Elderly)	73.90	37,000	21,000–66,000	Warehouse and Office	41.75	25,000	8,000–72,000
Housing (Public)	68.45	36,000	14,400–74,400				
Ice Rinks	76.00	29,000	27,200–33,600				

From RS Means Assemblies Cost Data, 2000, ©RSMeans, Norwell, MA, 781-422-5000. All rights reserved.

Earned-Value Analysis

BCWS = Budgeted cost of work scheduled (Planned)

ACWP = Actual cost of work performed (Actual)

BCWP = Budgeted cost of work performed (Earned)

Variances

CV = BCWP – ACWP (Cost variance = Earned – Actual)

SV = BCWP – BCWS (Schedule variance = Earned – Planned)

Indices

$$CPI = \frac{BCWP}{ACWP} \quad \left(\text{Cost Performance Index} = \frac{\text{Earned}}{\text{Actual}} \right)$$

$$SPI = \frac{BCWP}{BCWS} \quad \left(\text{Schedule Performance Index} = \frac{\text{Earned}}{\text{Planned}} \right)$$

Forecasting

BAC = Original project estimate (Budget at completion)

$$ETC = \frac{BAC - BCWP}{CPI} \quad (\text{Estimate to complete})$$

$$EAC = (ACWP + ETC) \quad (\text{Estimate to complete})$$

ENVIRONMENTAL ENGINEERING

AIR POLLUTION

Nomenclature

$$\frac{\mu\text{g}}{\text{m}^3} = \text{ppb} \times \frac{P(\text{MW})}{RT}$$

ppb = parts per billion

P = pressure (atm)

R = ideal gas law constant
 $= 0.0821 \text{ L}\cdot\text{atm}/(\text{mole}\cdot\text{K})$

T = absolute temperature, K = $273.15 + ^\circ\text{C}$

MW = molecular weight (g/mole)

Atmospheric Dispersion Modeling (Gaussian)

σ_y and σ_z as a function of downwind distance and stability class, see following figures.

$$C = \frac{Q}{2\pi u \sigma_y \sigma_z} \exp\left(-\frac{1}{2} \frac{y^2}{\sigma_y^2}\right) \left[\exp\left(-\frac{1}{2} \frac{(z - H)^2}{\sigma_z^2}\right) + \exp\left(-\frac{1}{2} \frac{(z + H)^2}{\sigma_z^2}\right) \right]$$

where

C = steady-state concentration at a point (x, y, z) ($\mu\text{g}/\text{m}^3$)

Q = emissions rate ($\mu\text{g}/\text{s}$)

σ_y = horizontal dispersion parameter (m)

σ_z = vertical dispersion parameter (m)

u = average wind speed at stack height (m/s)

y = horizontal distance from plume centerline (m)

z = vertical distance from ground level (m)

H = effective stack height (m) = $h + \Delta h$

where h = physical stack height

Δh = plume rise

x = downwind distance along plume centerline (m)

Maximum concentration at ground level and directly downwind from an elevated source.

$$C_{\max} = \frac{Q}{\pi u \sigma_y \sigma_z} \exp\left(-\frac{1}{2} \frac{(H^2)}{\sigma_z^2}\right)$$

where variables are as above except

C_{\max} = maximum ground-level concentration

$\sigma_z = \frac{H}{\sqrt{2}}$ for neutral atmospheric conditions

Selected Properties of Air

Nitrogen (N ₂) by volume	78.09%
Oxygen (O ₂) by volume	20.94%
Argon (Ar) by volume	0.93%
Molecular weight of air	28.966 g/mol
Absolute viscosity, μ	
at 80°F	0.045 lbm/(hr-ft)
at 100°F	0.047 lbm/(hr-ft)
Density	
at 80°F	0.0734 lbm/ft ³
at 100°F	0.0708 lbm/ft ³

The dry adiabatic lapse rate Γ_{AD} is 0.98°C per 100 m (5.4°F per 1,000 ft). This is the rate at which dry air cools adiabatically with altitude. The actual (environmental) lapse rate Γ is compared to Γ_{AD} to determine stability as follows:

Lapse Rate	Stability Condition
$\Gamma > \Gamma_{AD}$	Unstable
$\Gamma = \Gamma_{AD}$	Neutral
$\Gamma < \Gamma_{AD}$	Stable

Atmospheric Stability Under Various Conditions

Surface Wind Speed ^a (m/s)	Day			Night	
	Solar Insolation			Cloudiness ^e	
	Strong ^b	Moderate ^c	Slight ^d	Cloudy (≥4/8)	Clear (≤3/8)
<2	A	A–B ^f	B	E	F
2–3	A–B	B	C	E	F
3–5	B	B–C	C	D	E
5–6	C	C–D	D	D	D
>6	C	D	D	D	D

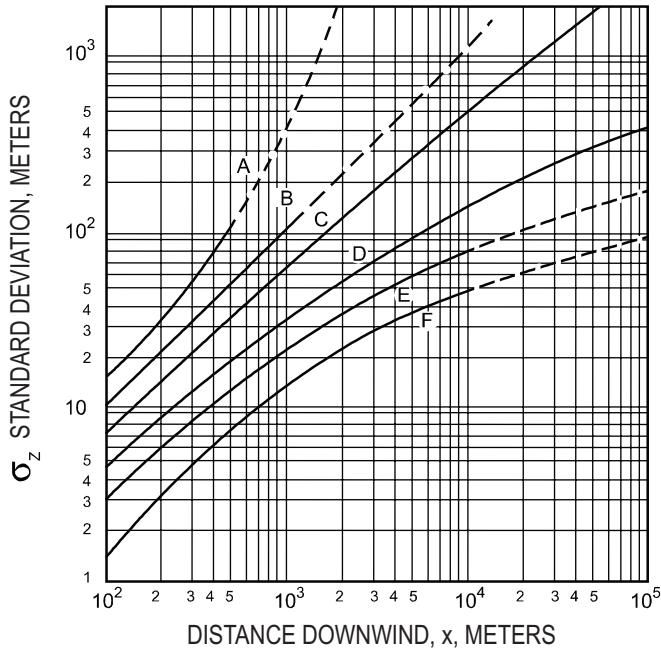
Notes:

- a. Surface wind speed is measured at 10 m above the ground.
- b. Corresponds to clear summer day with sun higher than 60° above the horizon.
- c. Corresponds to a summer day with a few broken clouds, or a clear day with sun 35-60° above the horizon.
- d. Corresponds to a fall afternoon, or a cloudy summer day, or clear summer day with the sun 15-35°.
- e. Cloudiness is defined as the fraction of sky covered by the clouds.
- f. For A–B, B–C, or C–D conditions, average the values obtained for each.

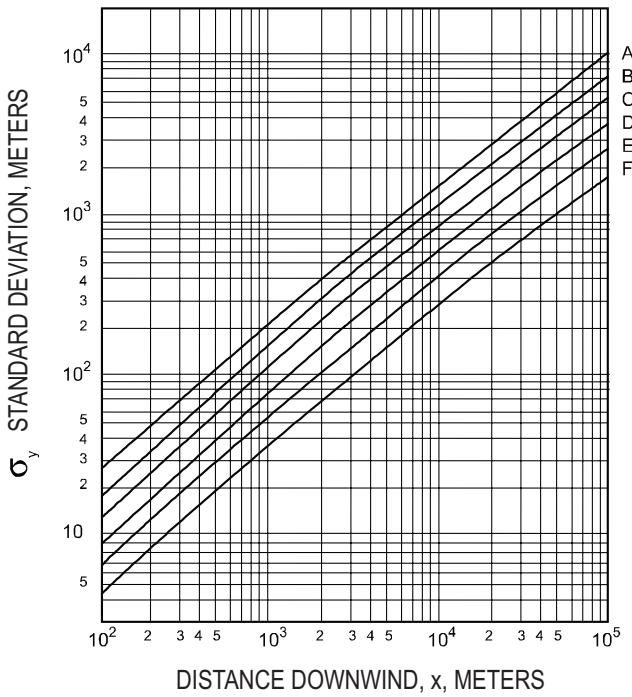
* A = Very unstable D = Neutral
 B = Moderately unstable E = Slightly stable
 C = Slightly unstable F = Stable

Regardless of wind speed, Class D should be assumed for overcast conditions, day or night.

Turner, D.B., "Workbook of Atmospheric Dispersion Estimates: An Introduction to Dispersion Modeling," 2nd ed., Lewis Publishing/CRC Press, Florida, 1994.



VERTICAL STANDARD DEVIATIONS OF A PLUME

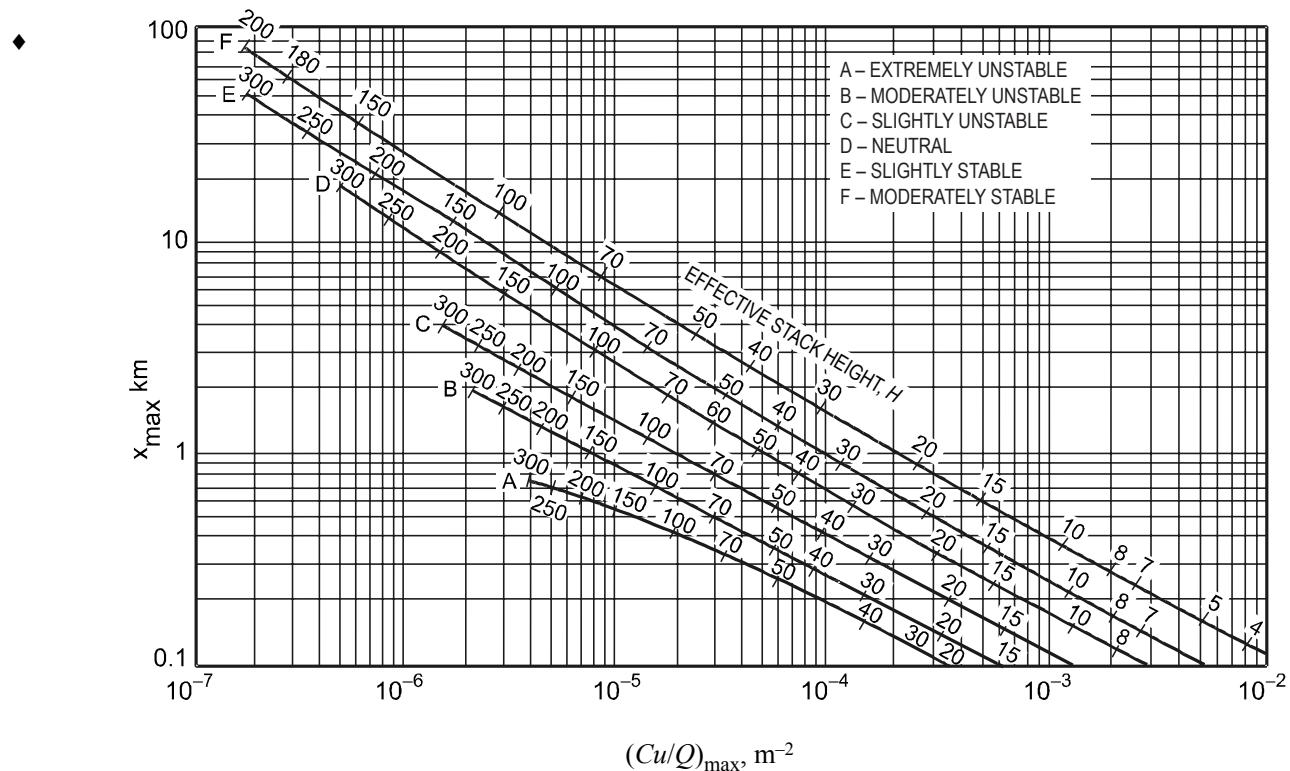


HORIZONTAL STANDARD DEVIATIONS OF A PLUME

- A – EXTREMELY UNSTABLE
- B – MODERATELY UNSTABLE
- C – SLIGHTLY UNSTABLE
- D – NEUTRAL
- E – SLIGHTLY STABLE
- F – MODERATELY STABLE

◆ Turner, D.B., "Workbook of Atmospheric Dispersion Estimates," U.S. Department of Health, Education, and Welfare, Washington, DC, 1970.

Downwind distance where the maximum concentration occurs, x_{\max} , versus $(Cu/Q)_{\max}$ as a function of stability class



NOTES: Effective stack height shown on curves numerically.

x_{\max} = distance along plume centerline to the point of maximum concentration

$$(Cu/Q)_{\max} = e^{[a + b \ln H + c (\ln H)^2 + d(\ln H)^3]}$$

H = effective stack height, stack height + plume rise, m

◆ Values of Curve-Fit Constants for Estimating $(Cu/Q)_{\max}$ from H as a Function of Atmospheric Stability

Stability	Constants			
	a	b	c	d
A	-1.0563	-2.7153	0.1261	0
B	-1.8060	-2.1912	0.0389	0
C	-1.9748	-1.9980	0	0
D	-2.5302	-1.5610	-0.0934	0
E	-1.4496	-2.5910	0.2181	-0.0343
F	-1.0488	-3.2252	0.4977	-0.0765

Adapted from Ranchoux, R.J.P., 1976.

◆ Turner, D.B., "Workbook of Atmospheric Dispersion Estimates: An Introduction to Dispersion Modeling," 2nd ed., Lewis Publishing/CRC Press, Florida, 1994.

Cyclone

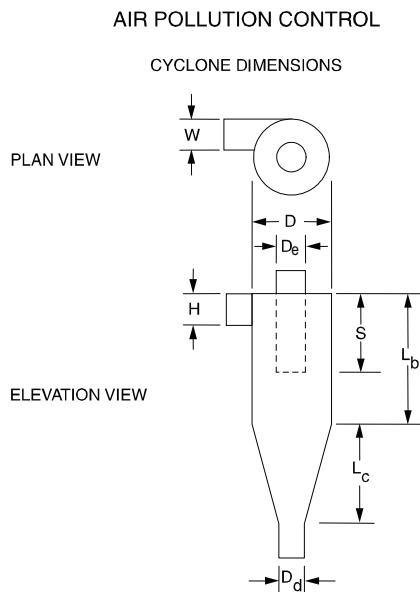
Cyclone Collection (Particle Removal) Efficiency

$$\eta = \frac{1}{1 + (d_{pc}/d_p)^2}, \text{ where}$$

d_{pc} = diameter of particle collected with 50% efficiency

d_p = diameter of particle of interest

η = fractional particle collection efficiency



Cyclone 50% Collection Efficiency for Particle Diameter

$$d_{pc} = \left[\frac{9\mu W}{2\pi N_e V_i (\rho_p - \rho_g)} \right]^{0.5}, \text{ where}$$

d_{pc} = diameter of particle that is collected with 50% efficiency (m)

μ = dynamic viscosity of gas (kg/m·s)

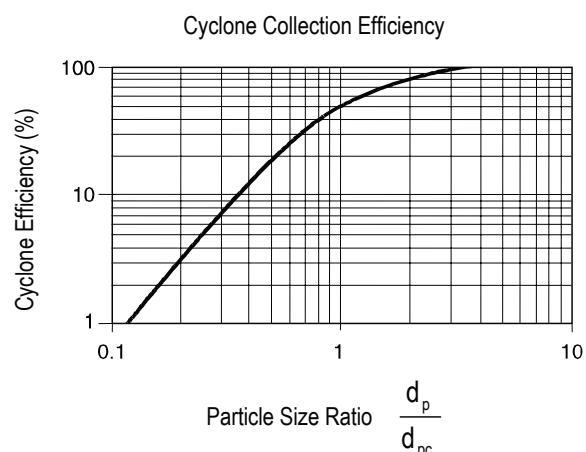
W = inlet width of cyclone (m)

N_e = number of effective turns gas makes in cyclone

V_i = inlet velocity into cyclone (m/s)

ρ_p = density of particle (kg/m³)

ρ_g = density of gas (kg/m³)



Cyclone Effective Number of Turns Approximation

$$N_e = \frac{1}{H} \left[L_b + \frac{L_c}{2} \right], \text{ where}$$

N_e = number of effective turns gas makes in cyclone

H = inlet height of cyclone (m)

L_b = length of body cyclone (m)

L_c = length of cone of cyclone (m)

Cyclone Ratio of Dimensions to Body Diameter

Dimension	High Efficiency	Conventional	High Throughput
Inlet height, H	0.44	0.50	0.80
Inlet width, W	0.21	0.25	0.35
Body length, L_b	1.40	1.75	1.70
Cone length, L_c	2.50	2.00	2.00
Vortex finder length, S	0.50	0.60	0.85
Gas exit diameter, D_e	0.40	0.50	0.75
Dust outlet diameter, D_d	0.40	0.40	0.40

* Adapted from Cooper, David C., and F.C. Alley, *Air Pollution Control: A Design Approach*, 2nd ed., Waveland Press, Illinois, 1986.

Baghouse

Air-to-Cloth Ratio for Baghouses

Dust	Shaker/Woven Reverse Air/Woven [m ³ /(min•m ²)]	Pulse Jet/Felt [m ³ /(min•m ²)]
alumina	0.8	2.4
asbestos	0.9	3.0
bauxite	0.8	2.4
carbon black	0.5	1.5
coal	0.8	2.4
cocoa	0.8	3.7
clay	0.8	2.7
cement	0.6	2.4
cosmetics	0.5	3.0
enamel frit	0.8	2.7
feeds, grain	1.1	4.3
feldspar	0.7	2.7
fertilizer	0.9	2.4
flour	0.9	3.7
fly ash	0.8	1.5
graphite	0.6	1.5
gypsum	0.6	3.0
iron ore	0.9	3.4
iron oxide	0.8	2.1
iron sulfate	0.6	1.8
lead oxide	0.6	1.8
leather dust	1.1	3.7
lime	0.8	3.0
limestone	0.8	2.4
mica	0.8	2.7
paint pigments	0.8	2.1
paper	1.1	3.0
plastics	0.8	2.1
quartz	0.9	2.7
rock dust	0.9	2.7
sand	0.8	3.0
sawdust (wood)	1.1	3.7
silica	0.8	2.1
slate	1.1	3.7
soap detergents	0.6	1.5
spices	0.8	3.0
starch	0.9	2.4
sugar	0.6	2.1
talc	0.8	3.0
tobacco	1.1	4.0

U.S. EPA OAQPS Control Cost Manual, 4th ed., EPA 450/3-90-006 (NTIS PB 90-169954), January 1990.

Electrostatic Precipitator Efficiency

Deutsch-Anderson equation:

$$\eta = 1 - e^{(-WA/Q)}$$

where

η = fractional collection efficiency

W = terminal drift velocity

A = total collection area

Q = volumetric gas flow rate

Note that any consistent set of units can be used for W , A , and Q (for example, ft/min, ft², and ft³/min).

Incineration

$$DRE = \frac{W_{in} - W_{out}}{W_{in}} \times 100\%$$

where

DRE = destruction and removal efficiency (%)

W_{in} = mass feed rate of a particular POHC (kg/h or lb/h)

W_{out} = mass emission rate of the same POHC (kg/h or lb/h)

POHC = principal organic hazardous contaminant

$$CE = \frac{CO_2}{CO_2 + CO} \times 100\%$$

CO_2 = volume concentration (dry) of CO_2
(parts per million, volume, ppm_v)

CO = volume concentration (dry) of CO (ppm_v)

CE = combustion efficiency

Kiln Formula

$$t = \frac{2.28 L/D}{SN}$$

where

t = mean residence time, min

L/D = internal length-to-diameter ratio

S = kiln rake slope, in./ft of length

N = rotational speed, rev/min

Energy Content of Waste

Typical Waste Values	Moisture, %	Energy, Btu/lb
Food Waste	70	2,000
Paper	6	7,200
Cardboard	5	7,000
Plastics	2	14,000
Wood	20	8,000
Glass	2	60
Bi-metallic Cans	3	300

FATE AND TRANSPORT

Mass Calculations

Mass balance: $\text{Mass}_{\text{in}} = \text{Mass}_{\text{out}}$

$$M = CQ = CV$$

Continuity equation = $Q = vA$

M = mass

C = concentration

Q = flow rate

V = volume

v = velocity

A = cross-sectional area of flow

$$M (\text{lb/day}) = C (\text{mg/L}) \times Q (\text{MGD}) \times 8.34 [\text{lb-L}/(\text{mg-MG})]$$

where:

MGD = million gallons per day

MG = million gallons

Microbial Kinetics

BOD Exertion

$$y_t = L(1 - e^{-kt})$$

where

k = BOD decay rate constant (base e, days⁻¹)

L = ultimate BOD (mg/L)

t = time (days)

y_t = the amount of BOD exerted at time t (mg/L)

Stream Modeling

Streeter Phelps

$$D = \frac{k_1 L_0}{k_2 - k_1} [\exp(-k_1 t) - \exp(-k_2 t)] + D_0 \exp(-k_2 t)$$

$$t_c = \frac{1}{k_2 - k_1} \ln \left[\frac{k_2}{k_1} \left(1 - D_0 \frac{(k_2 - k_1)}{k_1 L_0} \right) \right]$$

$$DO = DO_{\text{sat}} - D$$

where

D = dissolved oxygen deficit (mg/L)

DO = dissolved oxygen concentration (mg/L)

D_0 = initial dissolved oxygen deficit in mixing zone (mg/L)

DO_{sat} = saturated dissolved oxygen concentration (mg/L)

k_1 = deoxygenation rate constant, base e (days⁻¹)

k_2 = reaeration rate constant, base e (days⁻¹)

L_0 = initial BOD ultimate in mixing zone (mg/L)

t = time (days)

t_c = time at which minimum dissolved oxygen occurs (days)

Monod Kinetics—Substrate Limited Growth

Continuous flow systems where growth is limited by one substrate (chemostat):

$$\mu = \frac{Yk_m S}{K_s + S} - k_d = \mu_{\max} \frac{S}{K_s + S} - k_d$$

Multiple Limiting Substrates

$$\frac{\mu}{\mu_{\max}} = [\mu_1(S_1)][\mu_2(S_2)][\mu_3(S_3)] \dots [\mu_n(S_n)]$$

$$\text{where } \mu_i = \frac{S_i}{K_{s_i} + S_i} \text{ for } i = 1 \text{ to } n$$

Non-steady State Continuous Flow

$$\frac{dx}{dt} = Dx_0 + (\mu - k_d - D)x$$

Steady State Continuous Flow

$$\mu = D \text{ with } k_d \ll \mu$$

Product production at steady state, single substrate limiting

$$X_l = Y_{P/S}(S_0 - S_i)$$

k_d = microbial death rate or endogenous decay rate constant (time⁻¹)

k_m = maximum growth rate constant (time⁻¹)

K_s = saturation constant or half-velocity constant [= concentration at $\mu_{\max}/2$]

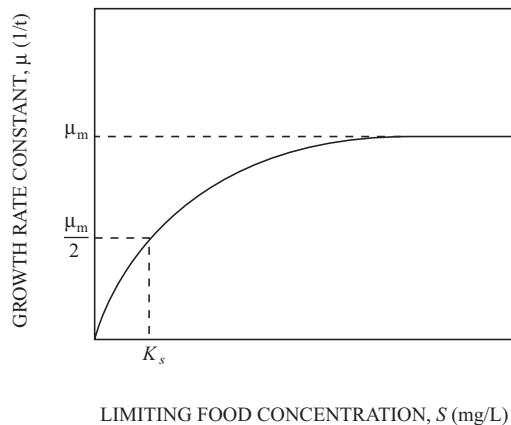
S = concentration of substrate in solution (mass/unit volume)

Y = yield coefficient [(mass/L product)/(mass/L food used)]

μ = specific growth rate (time⁻¹)

μ_{\max} = maximum specific growth rate (time⁻¹) = Yk_m

- ♦ Monod growth rate constant as a function of limiting food concentration.



- X_1 = product (mg/L)
 V_r = volume (L)
 D = dilution rate (flow f /reactor volume V_r ; hr $^{-1}$)
 f = flow rate (L/hr)
 μ_i = growth rate with one or multiple limiting substrates (hr $^{-1}$)
 S_i = substrate i concentration (mass/unit volume)
 S_0 = initial substrate concentration (mass/unit volume)
 $Y_{P/S}$ = product yield per unit of substrate (mass/mass)
 p = product concentration (mass/unit volume)
 x = cell concentration (mass/unit volume)
 x_0 = initial cell concentration (mass/unit volume)
 t = time (time)

Kinetic Temperature Corrections

$k_T = k_{20} (\Theta)^{T-20}$	
Activated sludge:	$\Theta = 1.136$ ($T > 20^\circ\text{C}$)
	$\Theta = 1.056$ ($T < 20^\circ\text{C}$)
Reaeration	$\Theta = 1.024$
Biotowers	$\Theta = 1.035$
Trickling Filters	$\Theta = 1.072$

♦ Davis, M.L., and D. Cornwell, *Introduction to Environmental Engineering*, 3rd ed., McGraw-Hill, 1998.

Partition Coefficients

Bioconcentration Factor BCF

The amount of a chemical to accumulate in aquatic organisms.

$$BCF = C_{\text{org}}/C$$

where

C_{org} = equilibrium concentration in organism (mg/kg or ppm)
 C = concentration in water (ppm)

Octanol-Water Partition Coefficient

The ratio of a chemical's concentration in the octanol phase to its concentration in the aqueous phase of a two-phase octanol-water system.

$$K_{ow} = C_o/C_w$$

where

C_o = concentration of chemical in octanol phase (mg/L or $\mu\text{g}/\text{L}$)

C_w = concentration of chemical in aqueous phase (mg/L or $\mu\text{g}/\text{L}$)

Organic Carbon Partition Coefficient K_{oc}

$$K_{oc} = C_{\text{soil}}/C_{\text{water}}$$

where

C_{soil} = concentration of chemical in organic carbon component of soil ($\mu\text{g adsorbed}/\text{kg organic } C$, or ppb)

C_{water} = concentration of chemical in water (ppb or $\mu\text{g}/\text{kg}$)

Retardation Factor R

$$R = 1 + (\rho/\eta)K_d$$

where

ρ = bulk density

η = porosity

K_d = distribution coefficient

Soil - Water Partition Coefficient $K_{sw} = K_\rho$

$$K_{sw} = X/C$$

where

X = concentration of chemical in soil (ppb or $\mu\text{g}/\text{kg}$)

C = concentration of chemical in water (ppb or $\mu\text{g}/\text{kg}$)

$$K_{sw} = K_{oc}f_{oc}$$

f_{oc} = fraction of organic carbon in the soil (dimensionless)

♦ Steady-State Reactor Parameters (Constant Density Systems)

Comparison of Steady-State Retention Times (θ) for Decay Reactions of Different Order^a

Reaction Order	r	Equations for Mean Retention Times (θ)		
		Ideal Batch	Ideal Plug Flow	Ideal CMFR
Zero ^b	-k	$\frac{(C_o - C_t)}{k}$	$\frac{(C_o - C_t)}{k}$	$\frac{(C_o - C_t)}{k}$
First	-kC	$\frac{\ln(C_o/C_t)}{k}$	$\frac{\ln(C_o/C_t)}{k}$	$\frac{(C_o/C_t) - 1}{k}$
Second	-kC ²	$\frac{(C_o/C_t) - 1}{kC_o}$	$\frac{(C_o/C_t) - 1}{kC_o}$	$\frac{(C_o/C_t) - 1}{kC_t}$

^aC_o = initial concentration or influent concentration; C_t = final condition or effluent concentration.

^bExpressions are valid for kθ ≤ C_o; otherwise C_t = 0.

Comparison of Steady-State Performance for Decay Reactions of Different Order^a

Reaction Order	r	Equations for C _t		
		Ideal Batch	Ideal Plug Flow	Ideal CMFR
Zero ^b t ≤ C _o /k t > C _o /k	-k	C _o - kt 0	C _o - kθ	C _o - kθ
	-kC	C _o [exp(-kt)]	C _o [exp(-kθ)]	$\frac{C_o}{1 + k\theta}$
Second	-kC ²	$\frac{C_o}{1 + ktC_o}$	$\frac{C_o}{1 + k\theta C_o}$	$\frac{(4k\theta C_o + 1)^{1/2} - 1}{2k\theta}$

^aC_o = initial concentration or influent concentration; C_t = final condition or effluent concentration.

^bTime conditions are for ideal batch reactor only.

♦ Davis, M.L., and S.J. Masten, *Principles of Environmental Engineering and Science*, 2nd ed., McGraw-Hill, 2004.

LANDFILL

Break-Through Time for Leachate to Penetrate a Clay Liner

$$t = \frac{d^2 \eta}{K(d + h)}$$

where

t = breakthrough time (yr)

d = thickness of clay liner (ft)

η = porosity

K = hydraulic conductivity (ft/yr)

h = hydraulic head (ft)

Typical porosity values for clays with a coefficient of permeability in the range of 10^{-6} to 10^{-8} cm/s vary from 0.1 to 0.3.

Effect of Overburden Pressure

$$SW_p = SW_i + \frac{p}{a + bp}$$

where

SW_p = specific weight of the waste material at pressure

p (lb/yd³) (typical 1,750 to 2,150)

SW_i = initial compacted specific weight of waste
(lb/yd³) (typical 1,000)

p = overburden pressure (lb/in²)

a = empirical constant (yd³/in²)

b = empirical constant (yd³/lb)

Gas Flux

$$N_A = \frac{D\eta^{4/3} (C_{A_{atm}} - C_{A_{fill}})}{L}$$

where

N_A = gas flux of compound A , [g/(cm² • s)][lb • mol/(ft² • d)]

$C_{A_{atm}}$ = concentration of compound A at the surface of the landfill cover, g/cm³ (lb • mol/ft³)

$C_{A_{fill}}$ = concentration of compound A at the bottom of the landfill cover, g/cm³ (lb • mol/ft³)

L = depth of the landfill cover, cm (ft)

Typical values for the coefficient of diffusion for methane and carbon dioxide are 0.20 cm²/s (18.6 ft²/d) and 0.13 cm²/s (12.1 ft²/d), respectively.

D = diffusion coefficient, cm²/s (ft²/d)

η_{gas} = gas-filled porosity, cm³/cm³ (ft³/ft³)

η = porosity, cm³/cm³ (ft³/ft³)

Soil Landfill Cover Water Balance

$$\Delta S_{LC} = P - R - ET - PER_{sw}$$

where

ΔS_{LC} = change in the amount of water held in storage in a unit volume of landfill cover (in.)

P = amount of precipitation per unit area (in.)

R = amount of runoff per unit area (in.)

ET = amount of water lost through evapotranspiration per unit area (in.)

PER_{sw} = amount of water percolating through the unit area of landfill cover into compacted solid waste (in.)

POPULATION MODELING

Population Projection Equations

Linear Projection = Algebraic Projection

$$P_t = P_0 + k\Delta t$$

where

P_t = population at time t

P_0 = population at time zero

k = growth rate

Δt = elapsed time in years relative to time zero

Log Growth = Exponential Growth = Geometric Growth

$$P_t = P_0 e^{kt}$$

$$\ln P_t = \ln P_0 + kt$$

where

P_t = population at time t

P_0 = population at time zero

k = growth rate

Δt = elapsed time in years relative to time zero

Percent Growth

$$P_t = P_0 (1 + k)^n$$

where

P_t = population at time t

P_0 = population at time zero

k = growth rate

n = number of periods

Ratio and Correlation Growth

$$\frac{P_2}{P_{2R}} = \frac{P_1}{P_{1R}} = k$$

where

P_2 = projected population

P_{2R} = projected population of a larger region

P_1 = population at last census

P_{1R} = population of larger region at last census

k = growth ratio constant

Decreasing-Rate-of-Increase Growth

$$P_t = P_0 + (S - P_0)(1 - e^{-k(t-t_0)})$$

where

P_t = population at time t

P_0 = population at time zero

k = growth rate constant

S = saturation population

t, t_0 = future time, initial time

RADIATION

Effective Half-Life

Effective half-life, τ_e , is the combined radioactive and biological half-life.

$$\frac{1}{\tau_e} = \frac{1}{\tau_r} + \frac{1}{\tau_b}$$

where

τ_r = radioactive half-life

τ_b = biological half-life

Half-Life

$$N = N_0 e^{-0.693 t/\tau}$$

where

N_0 = original number of atoms

N = final number of atoms

t = time

τ = half-life

Flux at distance 2 = (Flux at distance 1) $(r_1/r_2)^2$

where r_1 and r_2 are distances from source.

The half-life of a biologically degraded contaminant assuming a first-order rate constant is given by:

$$t_{1/2} = \frac{0.693}{k}$$

k = rate constant (time⁻¹)

$t_{1/2}$ = half-life (time)

SAMPLING AND MONITORING

Data Quality Objectives (DQO) for Sampling Soils and Solids

Investigation Type	Confidence Level (1- α) (%)	Power (1- β) (%)	Minimum Detectable Relative Difference (%)
Preliminary site investigation	70–80	90–95	10–30
Emergency clean-up	80–90	90–95	10–20
Planned removal and remedial response operations	90–95	90–95	10–20

Confidence level: 1 – (Probability of a Type I error) = 1 – α = size probability of not making a Type I error.

Power = 1 – (Probability of a Type II error) = 1 – β = probability of not making a Type II error.

EPA Document "EPA/600/8-89/046" *Soil Sampling Quality Assurance User's Guide*, Chapter 7.

$$CV = (100 * s)/\bar{x}$$

CV = coefficient of variation

s = standard deviation of sample

\bar{x} = sample average

Minimum Detectable Relative Difference = Relative increase over background $[100 (\mu_s - \mu_B)/\mu_B]$ to be detectable with a probability $(1-\beta)$

Daughter Product Activity

$$N_2 = \frac{\lambda_l N_{10}}{\lambda_2 - \lambda_l} (e^{-\lambda_l t} - e^{-\lambda_2 t})$$

where $\lambda_{1,2}$ = decay constants (time⁻¹)

N_{10} = initial activity (curies) of parent nuclei

t = time

Daughter Product Maximum Activity Time

$$t' = \frac{\ln \lambda_2 - \ln \lambda_l}{\lambda_2 - \lambda_l}$$

Inverse Square Law

$$\frac{I_1}{I_2} = \frac{(R_2)^2}{(R_1)^2}$$

where $I_{1,2}$ = Radiation intensity at locations 1 and 2

$R_{1,2}$ = Distance from the source at locations 1 and 2

Number of Samples Required in a One-Sided One-Sample t-Test to Achieve a Minimum Detectable Relative Difference at Confidence Level ($1-\alpha$) and Power ($1-\beta$)

Coefficient of Variation (%)	Power (%)	Confidence Level (%)	Minimum Detectable Relative Difference (%)				
			5	10	20	30	40
15	95	99	145	39	12	7	5
		95	99	26	8	5	3
		90	78	21	6	3	3
		80	57	15	4	2	2
	90	99	120	32	11	6	5
		95	79	21	7	4	3
		90	60	16	5	3	2
		80	41	11	3	2	1
	80	99	94	26	9	6	5
		95	58	16	5	3	3
		90	42	11	4	2	2
		80	26	7	2	2	1
25	95	99	397	102	28	14	9
		95	272	69	19	9	6
		90	216	55	15	7	5
		80	155	40	11	5	3
	90	99	329	85	24	12	8
		95	272	70	19	9	6
		90	166	42	12	6	4
		80	114	29	8	4	3
	80	99	254	66	19	10	7
		95	156	41	12	6	4
		90	114	30	8	4	3
		80	72	19	5	3	2
35	95	99	775	196	42	25	15
		95	532	134	35	17	10
		90	421	106	28	13	8
		80	304	77	20	9	6
	90	99	641	163	43	21	13
		95	421	107	28	14	8
		90	323	82	21	10	6
		80	222	56	15	7	4
	80	99	495	126	34	17	11
		95	305	78	21	10	7
		90	222	57	15	7	5
		80	140	36	10	5	3

WASTEWATER TREATMENT AND TECHNOLOGIES

Activated Sludge

$$X_A = \frac{\theta_c Y(S_0 - S_e)}{\theta(1 + k_d \theta_c)}$$

Steady State Mass Balance around Secondary Clarifier:

$$(Q_0 + Q_R)X_A = Q_e X_e + Q_R X_r + Q_w X_w$$

$$\theta_c = \text{Solids residence time} = \frac{V(X_A)}{Q_w X_w + Q_e X_e}$$

$$\text{Sludge volume/day: } Q_s = \frac{M(100)}{\rho_s (\% \text{ solids})}$$

$$\text{SVI} = \frac{\text{Sludge volume after settling (mL/L)} * 1,000}{\text{MLSS (mg/L)}}$$

k_d = microbial death ratio; kinetic constant; day⁻¹; typical range 0.1–0.01, typical domestic wastewater value = 0.05 day⁻¹

S_e = effluent BOD or COD concentration (kg/m³)

S_0 = influent BOD or COD concentration (kg/m³)

X_A = biomass concentration in aeration tank (MLSS or MLVSS kg/m³)

Y = yield coefficient (kg biomass/kg BOD or COD consumed); range 0.4–1.2

θ = hydraulic residence time = V/Q

Solids loading rate = $Q X_A$

For activated sludge secondary clarifier $Q = Q_0 + Q_R$

Organic loading rate (volumetric) = $Q_0 S_0 / Vol$

Organic loading rate (F:M) = $Q_0 S_0 / (Vol X_A)$

Organic loading rate (surface area) = $Q_0 S_0 / A_M$

ρ_s = density of solids

A = surface area of unit

A_M = surface area of media in fixed-film reactor

A_x = cross-sectional area of channel

M = sludge production rate (dry weight basis)

Q_0 = influent flow rate

Q_e = effluent flow rate

Q_w = waste sludge flow rate

ρ_s = wet sludge density

R = recycle ratio = Q_R/Q_0

Q_R = recycle flow rate = $Q_0 R$

X_e = effluent suspended solids concentration

X_w = waste sludge suspended solids concentration

V = aeration basin volume

Q = flow rate

X_r = recycled sludge suspended solids concentration

Design and Operational Parameters for Activated-Sludge Treatment of Municipal Wastewater

Type of Process	Mean cell residence time (θ_c , d)	Food-to-mass ratio [(kg BOD ₅ /day·kg MLSS)]	Volumetric loading (kg BOD ₅ /m ³)	Hydraulic residence time in aeration basin (θ , h)	Mixed liquor suspended solids (MLSS, mg/L)	Recycle ratio (Q_r/Q)	Flow regime*	BOD ₅ removal efficiency (%)	Air supplied (m ³ /kg BOD ₅)
Tapered aeration	5–15	0.2–0.4	0.3–0.6	4–8	1,500–3,000	0.25–0.5	PF	85–95	45–90
Conventional	4–15	0.2–0.4	0.3–0.6	4–8	1,500–3,000	0.25–0.5	PF	85–95	45–90
Step aeration	4–15	0.2–0.4	0.6–1.0	3–5	2,000–3,500	0.25–0.75	PF	85–95	45–90
Completely mixed	4–15	0.2–0.4	0.8–2.0	3–5	3,000–6,000	0.25–1.0	CM	85–95	45–90
Contact stabilization	4–15	0.2–0.6	1.0–1.2			0.25–1.0			45–90
Contact basin				0.5–1.0	1,000–3,000		PF	80–90	
Stabilization basin				4–6	4,000–10,000		PF		
High-rate aeration	4–15	0.4–1.5	1.6–16	0.5–2.0	4,000–10,000	1.0–5.0	CM	75–90	25–45
Pure oxygen	8–20	0.2–1.0	1.6–4	1–3	6,000–8,000	0.25–0.5	CM	85–95	
Extended aeration	20–30	0.05–0.15	0.16–0.40	18–24	3,000–6,000	0.75–1.50	CM	75–90	90–125

*PF = plug flow, CM = completely mixed.

Metcalf and Eddy, *Wastewater Engineering: Treatment, Disposal, and Reuse*, 3rd ed., McGraw-Hill, 1991.

Facultative Pond

BOD Loading Total System \leq 35 pounds $BOD_5/(acre \cdot day)$

Minimum = 3 ponds

Depth = 3–8 ft

Minimum $t = 90\text{--}120$ days

Biotower

Fixed-Film Equation without Recycle

$$\frac{S_e}{S_0} = e^{-kD/q^n}$$

Fixed-Film Equation with Recycle

$$\frac{S_e}{S_a} = \frac{e^{-kD/q^n}}{(1+R) - R(e^{-kD/q^n})}$$

where

S_e = effluent BOD_5 (mg/L)

S_0 = influent BOD_5 (mg/L)

R = recycle ratio = Q_R/Q_0

Q_R = recycle flow rate

$$S_a = \frac{S_0 + RS_e}{1+R}$$

D = depth of biotower media (m)

q = hydraulic loading [$m^3/(m^2 \cdot min)$]

$$= (Q_0 + RQ_0)/A_{plan} \text{ (with recycle)}$$

k = treatability constant; functions of wastewater and medium (min^{-1}); range 0.01–0.1; for municipal wastewater and modular plastic media $0.06\ min^{-1}$ @ $20^\circ C$

$$k_T = k_{20}(1.035)^{T-20}$$

n = coefficient relating to media characteristics; modular plastic, $n = 0.5$

◆ Aerobic Digestion

Design criteria for aerobic digesters^a

Parameter	Value
Sludge retention time, d	
At $20^\circ C$	40
At $15^\circ C$	60
Solids loading, lb volatile solids/ $ft^3 \cdot d$	0.1–0.3
Oxygen requirements, lb O_2 /lb solids destroyed	
Cell tissue	~2.3
BOD_5 in primary sludge	1.6–1.9
Energy requirements for mixing	
Mechanical aerators, $hp/10^3\ ft^3$	0.7–1.50
Diffused-air mixing, $ft^3/10^3\ ft^3 \cdot min$	20–40
Dissolved-oxygen residual in liquid, mg/L	1–2
Reduction in volatile suspended solids, %	40–50

Tank Volume

$$V = \frac{Q_i(X_i + FS_i)}{X_d(k_d P_v + 1/\theta_c)}$$

where

V = volume of aerobic digester (ft^3)

Q_i = influent average flowrate to digester (ft^3/d)

X_i = influent suspended solids (mg/L)

F = fraction of the influent BOD_5 consisting of raw primary sludge (expressed as a decimal)

S_i = influent BOD_5 (mg/L)

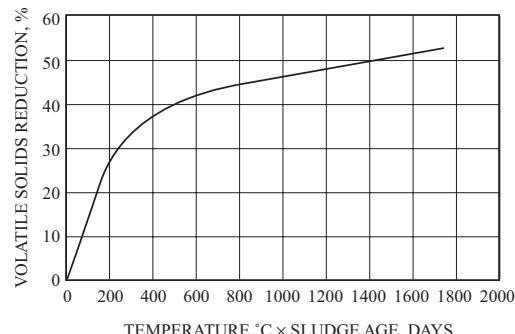
X_d = digester suspended solids (mg/L); typically $X_d = (0.7)X_i$

k_d = reaction-rate constant (d^{-1})

P_v = volatile fraction of digester suspended solids (expressed as a decimal)

θ_c = solids residence time (sludge age) (d)

FS_i can be neglected if primary sludge is not included on the sludge flow to the digester.



VOLATILE SOLIDS REDUCTION IN AN AEROBIC DIGESTER AS A FUNCTION OF DIGESTER LIQUID TEMPERATURE AND DIGESTER SLUDGE AGE

• Anaerobic Digestion

Design parameters for anaerobic digesters

Parameter	Standard-rate	High-rate
Solids residence time, d	30–90	10–20
Volatile solids loading, kg/m ³ /d	0.5–1.6	1.6–6.4
Digested solids concentration, %	4–6	4–6
Volatile solids reduction, %	35–50	45–55
Gas production (m ³ /kg VSS added)	0.5–0.55	0.6–0.65
Methane content, %	65	65

Standard Rate

$$\text{Reactor Volume} = \frac{V_1 + V_2}{2} t_r + V_2 t_s$$

High Rate

First stage

$$\text{Reactor Volume} = V_1 t_r$$

Second Stage

$$\text{Reactor Volume} = \frac{V_1 + V_2}{2} t_t + V_2 t_s$$

where

V_1 = raw sludge input (volume/day)

V_2 = digested sludge accumulation (volume/day)

t_r = time to react in a high-rate digester = time to react and thicken in a standard-rate digester

t_t = time to thicken in a high-rate digester

t_s = storage time

◆ Tchobanoglou, G., and Metcalf and Eddy, *Wastewater Engineering: Treatment, Disposal, and Reuse*, 4th ed., McGraw-Hill, 2003.

• Peavy, HS, D.R. Rowe, and G. Tchobanoglou, *Environmental Engineering*, McGraw-Hill, 1985.

WATER TREATMENT TECHNOLOGIES

Activated Carbon Adsorption

Freundlich Isotherm

$$\frac{x}{m} = X = KC_e^{1/n}$$

where

x = mass of solute adsorbed

m = mass of adsorbent

X = mass ratio of the solid phase—that is, the mass of adsorbed solute per mass of adsorbent

C_e = equilibrium concentration of solute, mass/volume

K, n = experimental constants

Linearized Form

$$\ln \frac{x}{m} = \frac{1}{n} \ln C_e + \ln K$$

For linear isotherm, $n = 1$

Langmuir Isotherm

$$\frac{x}{m} = X = \frac{aKC_e}{1 + KC_e}$$

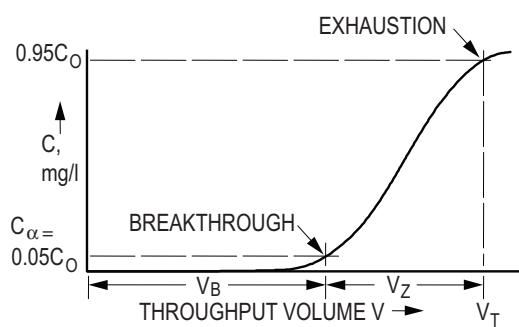
where

a = mass of adsorbed solute required to saturate completely a unit mass of adsorbent

K = experimental constant

Linearized Form

$$\frac{m}{x} = \frac{1}{a} + \frac{1}{aK} \frac{1}{C_e}$$



Depth of Sorption Zone

$$Z_s = Z \left[\frac{V_Z}{V_T - 0.5V_Z} \right]$$

where

$V_Z = V_T - V_B$

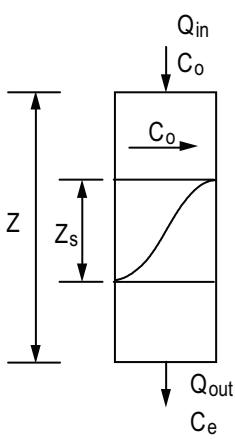
Z_s = depth of sorption zone

Z = total carbon depth

V_T = total volume treated at exhaustion ($C = 0.95 C_0$)

V_B = total volume at breakthrough ($C = C_\alpha = 0.05 C_0$)

C_0 = concentration of contaminant in influent



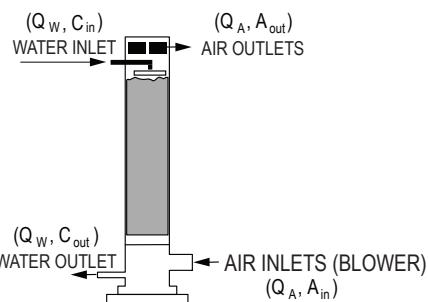
Air Stripping

$P_i = HC_i$ = Henry's Law

P_i = partial pressure of component i , atm

H = Henry's Law constant, atm·m³/kmol

C_i = concentration of component i in solvent, kmol/m³



$$A_{out} = HC_{in}$$

$$Q_W \cdot C_{in} = Q_A H C_{in}$$

$$Q_W = Q_A H$$

$$H (Q_A / Q_W) = 1$$

where

A_{out} = concentration in the effluent air (kmol/m³); in this formulation of the equation A_{in} and C_{out} are assumed to be negligible for simplicity.

Q_W = water flow rate (m³/s)

Q_A = air flow rate (m³/s)

A_{in} = concentration of contaminant in air (kmol/m³)

C_{out} = concentration of contaminants in effluent water (kmol/m³)

C_{in} = concentration of contaminants in influent water (kmol/m³)

Stripper Packing Height = Z

$$Z = HTU \times NTU$$

Assuming rapid equilibrium:

$$NTU = \left(\frac{R_S}{R_S - 1} \right) \ln \left(\frac{(C_{in}/C_{out})(R_S - 1) + 1}{R_S} \right)$$

where

NTU = number of transfer units

H = Henry's Law constant

H' = H/RT = dimensionless Henry's Law constant

T = temperature in units consistent with K

R = universal gas constant, atm·m³/(kmol·K)

R_S = stripping factor $H'(Q_A/Q_W)$

C_{in} = concentration in the influent water (kmol/m³)

C_{out} = concentration in the effluent water (kmol/m³)

HTU = Height of Transfer Units = $\frac{L}{M_w K_L a}$, where

L = liquid molar loading rate [kmol/(s·m²)]

M_w = molar density of water (55.6 kmol/m³) = 3.47 lbmol/ft³

$K_L a$ = overall transfer rate constant (s⁻¹)

Clarifier

Overflow rate = Hydraulic loading rate = $v_o = Q/A_{\text{surface}}$

v_o = critical settling velocity

= terminal settling velocity of smallest particle that is 100% removed

Weir loading = weir overflow rate, WOR = $Q/\text{Weir Length}$

Horizontal velocity = approach velocity = v_h

$$= Q/A_{\text{cross-section}} = Q/A_x$$

Hydraulic residence time = $V/Q = \theta$

where

Q = flow rate

A_x = cross-sectional area

A = surface area, plan view

V = tank volume

Typical Primary Clarifier Efficiency Percent Removal

	Overflow rates			
	1,200 (gpd/ft ²)	1,000 (gpd/ft ²)	800 (gpd/ft ²)	600 (gpd/ft ²)
	48.9 (m/d)	40.7 (m/d)	32.6 (m/d)	24.4 (m/d)
	54%	58%	64%	68%
	BOD ₅	30%	32%	34%
Suspended Solids				
BOD ₅				

Weir Loadings

- Water Treatment—weir overflow rates should not exceed 20,000 gpd/ft
- Wastewater Treatment
 - Flow ≤ 1 MGD: weir overflow rates should not exceed 10,000 gpd/ft
 - Flow > 1 MGD: weir overflow rates should not exceed 15,000 gpd/ft

Horizontal Velocities

- Water Treatment—horizontal velocities should not exceed 0.5 fpm
- Wastewater Treatment—no specific requirements (use the same criteria as for water)

Dimensions

- Rectangular Tanks
 - Length:Width ratio = 3:1 to 5:1
 - Basin width is determined by the scraper width (or multiples of the scraper width)
 - Bottom slope is set at 1%
- Circular Tanks
 - Diameters up to 200 ft
 - Diameters must match the dimensions of the sludge scraping mechanism
 - Bottom slope is less than 8%

Settling Equations

Design Criteria for Sedimentation Basins

Type of Basin	Overflow Rate				Solids Loading Rate				Hydraulic Residence Time (hr)	Depth (ft)
	Average (gpd/ft ²)	(m ³ /m ² •d)	Peak (gpd/ft ²)	(m ³ /m ² •d)	Average (lb/ft ² •d)	(kg/m ² •h)	Peak (lb/ft ² •h)	(kg/m ² •h)		
Water Treatment										
Clarification following coagulation and flocculation:										
Alum coagulation	350–550	14–22							4–8	12–16
Ferric coagulation	550–700	22–28							4–8	12–16
Upflow clarifiers										
Groundwater	1,500–2,200	61–90							1	
Surface water	1,000–1,500	41–61							4	
Clarification following lime-soda softening										
Conventional	550–1,000	22–41							2–4	
Upflow clarifiers										
Groundwater	1,000–2,500	41–102							1	
Surface water	1,000–1,800	41–73							4	
Wastewater Treatment										
Primary clarifiers	800–1,200	32–49	1,200–2,000	50–80					2	10–12
Settling basins following fixed film reactors	400–800	16–33							2	
Settling basins following air-activated sludge reactors										
All configurations EXCEPT extended aeration	400–700	16–28							2	12–15
Extended aeration	200–400	8–16	1,000–1,200	40–64	19–29	4–6	38	8	2	12–15
Settling basins following chemical flocculation reactors	800–1,200		600–800	24–32	5–24	1–5	34	7	2	

General Spherical

$$v_t = \sqrt{\frac{4g(\rho_p - \rho_f)d}{3C_D\rho_f}}$$

where

C_D = drag coefficient

= $24/\text{Re}$ (Laminar; $\text{Re} \leq 1.0$)

= $24/\text{Re} + 3/(\text{Re}^{1/2}) + 0.34$ (Transitional)

= 0.4 (Turbulent; $\text{Re} \geq 10^4$)

Re = Reynolds number $\frac{v_t \rho d}{\mu}$

g = gravitational constant

ρ_p and ρ_f = density of particle and fluid respectively

d = diameter of sphere

μ = bulk viscosity of liquid = absolute viscosity

v_t = terminal settling velocity

Stokes' Law

$$v_t = \frac{g(\rho_p - \rho_f)d^2}{18\mu} = \frac{g \rho_f(S.G. - 1)d^2}{18\mu}$$

Approach velocity = horizontal velocity = Q/A_x

Hydraulic loading rate = Q/A

Hydraulic residence time = $V/Q = \theta$

where

Q = flow rate

A_x = cross-sectional area

A = surface area, plan view

V = tank volume

ρ_f = fluid mass density

$S.G.$ = specific gravity

Filtration Equations

Filter bay length:width ratio = 1.2:1 to 1.5:1

Effective size = d_{10}

Uniformity coefficient = d_{60}/d_{10}

d_x = diameter of particle class for which $x\%$ of sample is less than (units meters or feet)

Filter equations can be used with any consistent set of units.

Head Loss Through Clean Bed

Rose Equation

Monosized Media

$$h_f = \frac{1.067(v_s)^2 L C_D}{g \eta^4 d}$$

Multisized Media

$$h_f = \frac{1.067(v_s)^2 L}{g \eta^4} \sum \frac{C_{Dij} x_{ij}}{d_{ij}}$$

Carmen-Kozeny Equation

Monosized Media

$$h_f = \frac{f' L (1 - \eta) v_s^2}{\eta^3 g d}$$

Multisized Media

$$h_f = \frac{L (1 - \eta) v_s^2}{\eta^3 g} \sum \frac{f'_{ij} x_{ij}}{d_{ij}}$$

$$f' = \text{friction factor} = 150 \left(\frac{1 - \eta}{\text{Re}} \right) + 1.75$$

where

h_f = head loss through the clean bed (m of H₂O)

L = depth of filter media (m)

η = porosity of bed = void volume/total volume

v_s = filtration rate = empty bed approach velocity

$$= Q/A_{\text{plan}} (\text{m/s})$$

g = gravitational acceleration (m/s²)

$$\text{Re} = \text{Reynolds number} = \frac{v_s \rho d}{\mu}$$

d_{ij}, d = diameter of filter media particles; arithmetic average of adjacent screen openings (m)

i = filter media (sand, anthracite, garnet)

j = filter media particle size

x_{ij} = mass fraction of media retained between adjacent sieves

f'_{ij} = friction factors for each media fraction

C_D = drag coefficient as defined in settling velocity equations

Bed Expansion

Monosized

Multisized

$$L_f = \frac{L_o(1 - \eta_o)}{1 - \left(\frac{v_B}{v_t} \right)^{0.22}} \quad L_f = L_o(1 - \eta_o) \sum \frac{x_{ij}}{1 - \left(\frac{v_B}{v_{t,ij}} \right)^{0.22}}$$

$$\eta_f = \left(\frac{v_B}{v_t} \right)^{0.22}$$

where

L_f = depth of fluidized filter media (m)

v_B = backwash velocity (m/s), Q_B/A_{plan}

Q_B = backwash flowrate

v_t = terminal setting velocity

η_f = porosity of fluidized bed

L_o = initial bed depth

η_o = initial bed porosity

Lime-Soda Softening Equations

1. Carbon dioxide removal
 $\text{CO}_2 + \text{Ca}(\text{OH})_2 \rightarrow \text{CaCO}_3(\text{s}) + \text{H}_2\text{O}$
2. Calcium carbonate hardness removal
 $\text{Ca}(\text{HCO}_3)_2 + \text{Ca}(\text{OH})_2 \rightarrow 2\text{CaCO}_3(\text{s}) + 2\text{H}_2\text{O}$
3. Calcium non-carbonate hardness removal
 $\text{CaSO}_4 + \text{Na}_2\text{CO}_3 \rightarrow \text{CaCO}_3(\text{s}) + 2\text{Na}^+ + \text{SO}_4^{2-}$
4. Magnesium carbonate hardness removal
 $\text{Mg}(\text{HCO}_3)_2 + 2\text{Ca}(\text{OH})_2 \rightarrow 2\text{CaCO}_3(\text{s}) + \text{Mg}(\text{OH})_2(\text{s}) + 2\text{H}_2\text{O}$
5. Magnesium non-carbonate hardness removal
 $\text{MgSO}_4 + \text{Ca}(\text{OH})_2 + \text{Na}_2\text{CO}_3 \rightarrow \text{CaCO}_3(\text{s}) + \text{Mg}(\text{OH})_2(\text{s}) + 2\text{Na}^+ + \text{SO}_4^{2-}$
6. Destruction of excess alkalinity
 $2\text{HCO}_3^- + \text{Ca}(\text{OH})_2 \rightarrow \text{CaCO}_3(\text{s}) + \text{CO}_3^{2-} + 2\text{H}_2\text{O}$
7. Recarbonation
 $\text{Ca}^{2+} + 2\text{OH}^- + \text{CO}_2 \rightarrow \text{CaCO}_3(\text{s}) + \text{H}_2\text{O}$

Molecular Formulas	Molecular Weight	<i>n</i> # Equiv per mole	Equivalent Weight
CO_3^{2-}	60.0	2	30.0
CO_2	44.0	2	22.0
$\text{Ca}(\text{OH})_2$	74.1	2	37.1
CaCO_3	100.1	2	50.0
$\text{Ca}(\text{HCO}_3)_2$	162.1	2	81.1
CaSO_4	136.1	2	68.1
Ca^{2+}	40.1	2	20.0
H^+	1.0	1	1.0
HCO_3^-	61.0	1	61.0
$\text{Mg}(\text{HCO}_3)_2$	146.3	2	73.2
$\text{Mg}(\text{OH})_2$	58.3	2	29.2
MgSO_4	120.4	2	60.2
Mg^{2+}	24.3	2	12.2
Na^+	23.0	1	23.0
Na_2CO_3	106.0	2	53.0
OH^-	17.0	1	17.0
SO_4^{2-}	96.1	2	48.0

Rapid Mix and Flocculator Design

$$G = \sqrt{\frac{P}{\mu V}} = \sqrt{\frac{\gamma H_L}{t \mu}}$$

$Gt = 10^4$ to 10^5

where

G = root mean square velocity gradient (mixing intensity)
 $[\text{ft}/(\text{sec}\cdot\text{ft}) \text{ or } \text{m}/(\text{s}\cdot\text{m})]$

P = power to the fluid ($\text{ft}\cdot\text{lb}/\text{sec}$ or $\text{N}\cdot\text{m}/\text{s}$)

V = volume (ft^3 or m^3)

μ = dynamic viscosity [$\text{lb}/(\text{ft}\cdot\text{sec})$ or $\text{Pa}\cdot\text{s}$]

g = specific weight of water (lb/ft^3 or N/m^3)

H_L = head loss (ft or m)

t = time (sec or s)

Reel and Paddle

$$P = \frac{C_D A_p \rho_f v_r^3}{2}$$

where

C_D = drag coefficient = 1.8 for flat blade with a L:W > 20:1

A_p = area of blade (m^2) perpendicular to the direction of travel through the water

ρ_f = density of H_2O (kg/m^3)

v_p = velocity of paddle (m/s)

v_r = relative or effective paddle velocity

= $v_p \cdot$ slip coefficient

slip coefficient = 0.5 to 0.75

Turbulent Flow Impeller Mixer

$$P = K_T (n)^3 (D_i)^5 \rho_f$$

where

K_T = impeller constant (see table)

n = rotational speed (rev/sec)

D_i = impeller diameter (m)

Values of the Impeller Constant K_T (Assume Turbulent Flow)

Type of Impeller	K_T
Propeller, pitch of 1, 3 blades	0.32
Propeller, pitch of 2, 3 blades	1.00
Turbine, 6 flat blades, vaned disc	6.30
Turbine, 6 curved blades	4.80
Fan turbine, 6 blades at 45°	1.65
Shrouded turbine, 6 curved blades	1.08
Shrouded turbine, with stator, no baffles	1.12

Note: Constant assumes baffled tanks having four baffles at the tank wall with a width equal to 10% of the tank diameter.

Reprinted with permission from *Industrial & Engineering Chemistry*, "Mixing of Liquids in Chemical Processing," J. Henry Rushton, 1952, v. 44, no. 12. p. 2934, American Chemical Society.

Reverse Osmosis

Osmotic Pressure of Solutions of Electrolytes

$$\Pi = \phi v \frac{n}{V} RT$$

where

Π = osmotic pressure, Pa

ϕ = osmotic coefficient

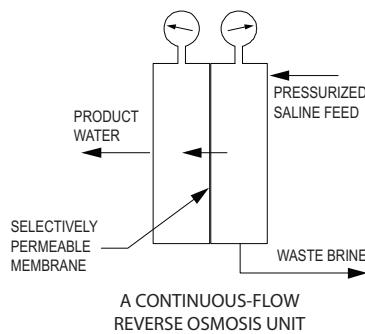
v = number of ions formed from one molecule of electrolyte

n = number of moles of electrolyte

V = specific volume of solvent, m³/kmol

R = universal gas constant, Pa • m³/(kmol • K)

T = absolute temperature, K



Salt Flux through the Membrane

$$J_s = (D_s K_s / \Delta Z)(C_{in} - C_{out})$$

where

J_s = salt flux through the membrane [kmol/(m² • s)]

D_s = diffusivity of the solute in the membrane (m²/s)

K_s = solute distribution coefficient (dimensionless)

C = concentration (kmol/m³)

ΔZ = membrane thickness (m)

$$J_s = K_p (C_{in} - C_{out})$$

K_p = membrane solute mass transfer coefficient

$$= \frac{D_s K_s}{\Delta Z} (L/t, m/s)$$

Water Flux

$$J_w = W_p (\Delta P - \Delta \pi)$$

where

J_w = water flux through the membrane [kmol/(m² • s)]

W_p = coefficient of water permeation, a characteristic of the particular membrane [kmol/(m² • s • Pa)]

ΔP = pressure differential across membrane = $P_{in} - P_{out}$ (Pa)

$\Delta \pi$ = osmotic pressure differential across membrane

$$\pi_{in} - \pi_{out} (Pa)$$

Ultrafiltration

$$J_w = \frac{\varepsilon r^2 \int \Delta P}{8\mu\delta}$$

where

ε = membrane porosity

r = membrane pore size

ΔP = net transmembrane pressure

μ = viscosity

δ = membrane thickness

J_w = volumetric flux (m/s)

♦ Disinfection

Chlorine contact chamber length:width ratio = 20:1 to 50:1

$$T = TDT \times BF$$

T = time that the water is in contact with the disinfectant (min)

TDT = theoretical detention time (min)

$$TDT (\text{min-mg/L}) = C \times T$$

BF = baffling factor

C = residual disinfectant concentration measured during peak hourly flow (mg/L)



Baffling Factors

Baffling Condition	Baffling Factor	Baffling Description
Unbaffled (mixed flow)	0.1	None, agitated basin, very low length to width ratio, high inlet and outlet flow velocities.
Poor	0.3	Single or multiple unbaffled inlets and outlets, no intra-basin baffles.
Average	0.5	Baffled inlet or outlet with some intra-basin baffles.
Superior	0.7	Perforated inlet baffle, serpentine or perforated intra-basin baffles, outlet weir or perforated launders.
Perfect (plug flow)	1.0	Very high length to width ratio (pipeline flow), perforated inlet, outlet, and intra-basin baffles.

♦ *Guidance Manual LTIESWTR Disinfection Profiling and Benchmarking*, U.S. Environmental Protection Agency, 2003.

♦ Removal and Inactivation Requirements

Microorganism	Required Log Reduction	Treatment
<i>Giardia</i>	3-log (99.9%)	Removal and/or inactivation
Viruses	4-log (99.99%)	Removal and/or inactivation
<i>Cryptosporidium</i>	2-log (99%)	Removal

♦ Typical Removal Credits and Inactivation Requirements for Various Treatment Technologies

Process	Typical Log Removal Credits		Resulting Disinfection Log Inactivation Requirements	
	<i>Giardia</i>	Viruses	<i>Giardia</i>	Viruses
Conventional Treatment	2.5	2.0	0.5	2.0
Direct Filtration	2.0	1.0	1.0	3.0
Slow Sand Filtration	2.0	2.0	1.0	2.0
Diatomaceous Earth Filtration	2.0	1.0	1.0	3.0
Unfiltered	0	0	3.0	4.0

♦ *Guidance Manual LTIESWTR Disinfection Profiling and Benchmarking*, U.S. Environmental Protection Agency, 2003.

**CT Values* For 3-LOG Inactivation
Of *Giardia* Cysts By Free Chlorine**

Chlorine Concentration (mg/L)	Temperature <= 0.5°C									Temperature = 5°C									Temperature = 10°C									
	pH									pH									pH									
	<=6.0	6.5	7.0	7.5	8.0	8.5	9.0	<=6.0	6.5	7.0	7.5	8.0	8.5	9.0	<=6.0	6.5	7.0	7.5	8.0	8.5	9.0	<=6.0	6.5	7.0	7.5	8.0	8.5	9.0
<=0.4	137	163	195	237	277	329	390	97	117	139	166	198	236	279	73	88	104	125	149	177	209	137	163	195	227	253	281	309
0.6	141	168	200	239	286	342	407	100	120	143	171	204	244	291	75	90	107	128	153	183	218	141	168	195	227	253	281	309
0.8	145	172	205	246	295	354	422	103	122	146	175	210	252	301	78	92	110	131	158	189	226	145	172	205	234	261	289	309
1.0	148	176	210	253	304	365	437	105	125	149	179	216	260	312	79	94	112	134	162	195	234	148	176	210	243	271	309	309
1.2	152	180	215	259	313	376	451	107	127	152	183	221	267	320	80	95	114	137	166	200	240	152	180	215	243	271	309	309
1.4	155	184	221	266	321	387	464	109	130	155	187	227	274	329	82	98	116	140	170	206	247	155	184	221	253	281	309	309
1.6	157	189	226	273	329	397	477	111	132	158	192	232	281	337	83	99	119	144	174	211	253	157	189	226	253	281	309	309
1.8	162	193	231	279	338	407	489	114	135	162	196	238	287	345	86	101	122	147	179	215	259	162	193	231	265	293	309	309
2.0	165	197	236	286	346	417	500	116	138	165	200	243	294	353	87	104	124	150	182	221	265	165	197	236	265	293	309	309
2.2	169	201	242	297	353	426	511	118	140	169	204	248	300	361	89	105	127	153	186	225	271	169	201	242	271	300	309	309
2.4	172	205	247	298	361	435	522	120	143	172	209	253	306	368	90	107	129	157	190	230	276	172	205	247	276	300	309	309
2.6	175	209	252	304	368	444	533	122	146	175	213	258	312	375	92	110	131	160	194	234	281	175	209	252	281	300	309	309
2.8	178	213	257	310	375	452	543	124	148	178	217	263	318	382	93	111	134	163	197	239	287	178	213	257	287	300	309	309
3.0	181	217	261	316	382	460	552	126	151	182	221	268	324	389	95	113	137	166	201	243	292	181	217	261	292	300	309	309
Chlorine Concentration (mg/L)	Temperature = 15°C									Temperature = 20°C									Temperature = 25°C									
	pH									pH									pH									
	<=6.0	6.5	7.0	7.5	8.0	8.5	9.0	<=6.0	6.5	7.0	7.5	8.0	8.5	9.0	<=6.0	6.5	7.0	7.5	8.0	8.5	9.0	<=6.0	6.5	7.0	7.5	8.0	8.5	9.0
<=0.4	49	59	70	83	99	118	140	36	44	52	62	74	89	105	24	29	35	42	50	59	70	49	59	70	83	99	118	140
0.6	50	60	72	86	102	122	146	38	45	54	64	77	92	109	25	30	36	43	51	61	73	50	60	72	86	102	122	146
0.8	52	61	73	88	105	126	151	39	46	55	66	79	95	113	26	31	37	44	53	63	75	52	61	73	88	105	126	151
1.0	53	63	75	90	108	130	156	39	47	56	67	81	98	117	26	31	37	45	54	65	78	53	63	75	90	108	130	156
1.2	54	64	76	92	111	134	160	40	48	57	69	83	100	120	27	32	38	46	55	67	80	54	64	76	92	111	134	160
1.4	55	65	78	94	114	137	165	41	49	58	70	85	103	123	27	33	39	47	57	69	82	55	65	78	94	114	137	165
1.6	56	66	79	96	116	141	169	42	50	59	72	87	105	126	28	33	40	48	58	70	84	56	66	79	96	116	141	169
1.8	57	68	81	98	119	144	173	43	51	61	74	89	106	129	29	34	41	49	60	72	86	57	68	81	98	119	144	173
2.0	58	69	83	100	122	147	177	44	52	62	75	91	110	132	29	35	41	50	61	74	88	58	69	83	100	122	147	177
2.2	59	70	85	102	124	150	181	44	53	63	77	93	113	135	30	35	42	51	62	75	90	59	70	85	102	124	150	181
2.4	60	72	86	105	127	153	184	45	54	65	78	95	115	138	30	36	43	52	63	77	92	60	72	86	105	127	153	184
2.6	61	73	88	107	129	156	188	46	55	66	80	97	117	141	31	37	44	53	65	78	94	61	73	88	107	129	156	188
2.8	62	74	89	109	132	159	191	47	56	67	81	99	119	143	31	37	45	54	66	80	96	62	74	89	109	132	159	191
3.0	63	76	91	111	134	162	195	47	57	68	83	101	122	146	32	38	46	55	67	81	97	63	76	91	111	134	162	195

*Although units did not appear in the original tables, units are min-mg/L

**CT VALUES* FOR
4-LOG INACTIVATION OF VIRUSES BY FREE CHLORINE**

<u>Temperature (°C)</u>	pH	
	6–9	10
0.5	12	90
5	8	60
10	6	45
15	4	30
20	3	22
25	2	15

*Although units did not appear in the original tables, units are min-mg/L

♦ *Guidance Manual LTIESWTR Disinfection Profiling and Benchmarking*, U.S. Environmental Protection Agency, 2003.

ELECTRICAL AND COMPUTER ENGINEERING

UNITS

The basic electrical units are coulombs for charge, volts for voltage, amperes for current, and ohms for resistance and impedance.

ELECTROSTATICS

$$\mathbf{F}_2 = \frac{Q_1 Q_2}{4\pi\epsilon r^2} \mathbf{a}_{r12}, \text{ where}$$

\mathbf{F}_2 = the force on charge 2 due to charge 1

Q_i = the i th point charge

r = the distance between charges 1 and 2

\mathbf{a}_{r12} = a unit vector directed from 1 to 2

ϵ = the permittivity of the medium

For free space or air:

$$\epsilon = \epsilon_0 = 8.85 \times 10^{-12} \text{ farads/meter}$$

Electrostatic Fields

Electric field intensity \mathbf{E} (volts/meter) at point 2 due to a point charge Q_1 at point 1 is

$$\mathbf{E} = \frac{Q_1}{4\pi\epsilon r^2} \mathbf{a}_{r12}$$

For a line charge of density ρ_L coulombs/meter on the z -axis, the radial electric field is

$$\mathbf{E}_L = \frac{\rho_L}{2\pi\epsilon r} \mathbf{a}_r$$

For a sheet charge of density ρ_s coulombs/meter² in the x - y plane:

$$\mathbf{E}_s = \frac{\rho_s}{2\epsilon} \mathbf{a}_z, z > 0$$

Gauss' law states that the integral of the electric flux density $\mathbf{D} = \epsilon\mathbf{E}$ over a closed surface is equal to the charge enclosed or

$$Q_{encl} = \oint_S \epsilon \mathbf{E} \cdot d\mathbf{S}$$

The force on a point charge Q in an electric field with intensity \mathbf{E} is $\mathbf{F} = Q\mathbf{E}$.

The work done by an external agent in moving a charge Q in an electric field from point p_1 to point p_2 is

$$W = -Q \int_{p_1}^{p_2} \mathbf{E} \cdot d\mathbf{l}$$

The energy W_E stored in an electric field \mathbf{E} is

$$W_E = (1/2) \iiint_V \epsilon |\mathbf{E}|^2 dV$$

Voltage

The potential difference V between two points is the work per unit charge required to move the charge between the points.

For two parallel plates with potential difference V , separated by distance d , the strength of the E field between the plates is

$$E = \frac{V}{d}$$

directed from the + plate to the - plate.

Current

Electric current $i(t)$ through a surface is defined as the rate of charge transport through that surface or

$$i(t) = dq(t)/dt, \text{ which is a function of time } t$$

since $q(t)$ denotes instantaneous charge.

A constant current $i(t)$ is written as I , and the vector current density in amperes/m² is defined as \mathbf{J} .

Magnetic Fields

For a current-carrying wire on the z -axis

$$\mathbf{H} = \frac{\mathbf{B}}{\mu} = \frac{I\mathbf{a}_\phi}{2\pi r}, \text{ where}$$

\mathbf{H} = the magnetic field strength (amperes/meter)

\mathbf{B} = the magnetic flux density (tesla)

\mathbf{a}_ϕ = the unit vector in positive ϕ direction in cylindrical coordinates

I = the current

μ = the permeability of the medium

$$\text{For air: } \mu = \mu_0 = 4\pi \times 10^{-7} \text{ H/m}$$

Force on a current-carrying conductor in a uniform magnetic field is

$$\mathbf{F} = I\mathbf{L} \times \mathbf{B}, \text{ where}$$

\mathbf{L} = the length vector of a conductor

The energy stored W_H in a magnetic field \mathbf{H} is

$$W_H = (1/2) \iiint_V \mu |\mathbf{H}|^2 dV$$

Induced Voltage

Faraday's Law states for a coil of N turns enclosing flux ϕ :

$$v = -N d\phi/dt, \text{ where}$$

v = the induced voltage

ϕ = the average flux (webers) enclosed by each turn

$$\phi = \int_S \mathbf{B} \cdot d\mathbf{S}$$

Resistivity

For a conductor of length L , electrical resistivity ρ , and cross-sectional area A , the resistance is

$$R = \frac{\rho L}{A}$$

For metallic conductors, the resistivity and resistance vary linearly with changes in temperature according to the following relationships:

$$\rho = \rho_0 [1 + \alpha(T - T_0)], \text{ and}$$

$$R = R_0 [1 + \alpha(T - T_0)], \text{ where}$$

ρ_0 = resistivity at T_0

R_0 = resistance at T_0

α = temperature coefficient

Ohm's Law: $V = IR; v(t) = i(t) R$

Resistors in Series and Parallel

For series connections, the current in all resistors is the same and the equivalent resistance for n resistors in series is

$$R_S = R_1 + R_2 + \dots + R_n$$

For parallel connections of resistors, the voltage drop across each resistor is the same and the equivalent resistance for n resistors in parallel is

$$R_P = 1/(1/R_1 + 1/R_2 + \dots + 1/R_n)$$

For two resistors R_1 and R_2 in parallel

$$R_P = \frac{R_1 R_2}{R_1 + R_2}$$

Power Absorbed by a Resistive Element

$$P = VI = \frac{V^2}{R} = I^2 R$$

Kirchhoff's Laws

Kirchhoff's voltage law for a closed path is expressed by

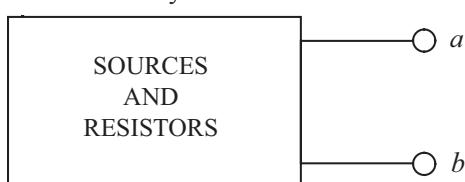
$$\sum V_{\text{rises}} = \sum V_{\text{drops}}$$

Kirchhoff's current law for a closed surface is

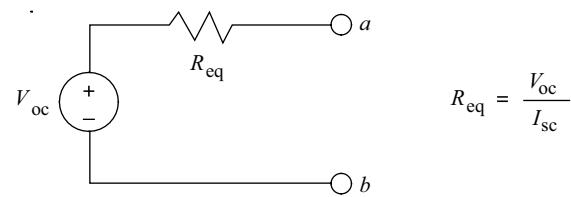
$$\sum I_{\text{in}} = \sum I_{\text{out}}$$

SOURCE EQUIVALENTS

For an arbitrary circuit



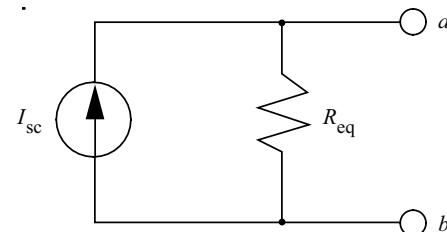
The Thévenin equivalent is



$$R_{\text{eq}} = \frac{V_{\text{oc}}}{I_{\text{sc}}}$$

The open circuit voltage V_{oc} is $V_a - V_b$, and the short circuit current is I_{sc} from a to b .

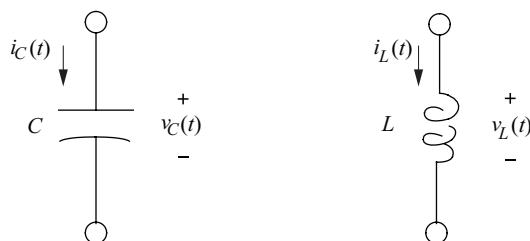
The Norton equivalent circuit is



where I_{sc} and R_{eq} are defined above.

A load resistor R_L connected across terminals a and b will draw maximum power when $R_L = R_{\text{eq}}$.

CAPACITORS AND INDUCTORS



The charge $q_C(t)$ and voltage $v_C(t)$ relationship for a capacitor C in farads is

$$C = q_C(t)/v_C(t) \quad \text{or} \quad q_C(t) = Cv_C(t)$$

A parallel plate capacitor of area A with plates separated a distance d by an insulator with a permittivity ϵ has a capacitance

$$C = \frac{\epsilon A}{d}$$

ϵ is often given as $\epsilon = \epsilon_r (\epsilon_0)$ where ϵ_r is the relative permittivity or dielectric constant and $\epsilon_0 = 8.85 \times 10^{-12} \text{ F/m}$.

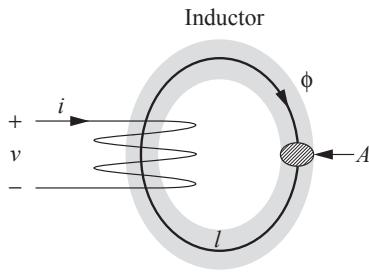
The current-voltage relationships for a capacitor are

$$v_C(t) = v_C(0) + \frac{1}{C} \int_0^t i_C(\tau) d\tau$$

and $i_C(t) = C(dv_C/dt)$

The energy stored in a capacitor is expressed in joules and given by

$$\text{Energy} = Cv_C^2/2 = q_C^2/2C = q_C v_C/2$$



The inductance L (henrys) of a coil of N turns wound on a core with cross-sectional area A (m^2), permeability μ and flux ϕ with a mean path of l (m) is given as:

$$L = N^2 \mu A / l$$

$$N\phi = Li$$

and using Faraday's law, the voltage-current relations for an inductor are

$$v_L(t) = L (di_L/dt)$$

$$i_L(t) = i_L(0) + \frac{1}{L} \int_0^t v_L(\tau) d\tau, \text{ where}$$

v_L = inductor voltage

L = inductance (henrys)

i_L = inductor current (amperes)

The energy stored in an inductor is expressed in joules and given by

$$\text{Energy} = Li_L^2/2$$

Capacitors and Inductors in Parallel and Series

Capacitors in Parallel

$$C_P = C_1 + C_2 + \dots + C_n$$

Capacitors in Series

$$C_S = \frac{1}{1/C_1 + 1/C_2 + \dots + 1/C_n}$$

Inductors in Parallel

$$L_P = \frac{1}{1/L_1 + 1/L_2 + \dots + 1/L_n}$$

Inductors in Series

$$L_S = L_1 + L_2 + \dots + L_n$$

AC CIRCUITS

For a sinusoidal voltage or current of frequency f (Hz) and period T (seconds),

$$f = 1/T = \omega/(2\pi), \text{ where}$$

ω = the angular frequency in radians/s

Average Value

For a periodic waveform (either voltage or current) with period T ,

$$X_{\text{ave}} = (1/T) \int_0^T x(t) dt$$

The average value of a full-wave rectified sinusoid is

$$X_{\text{ave}} = (2X_{\text{max}})/\pi$$

and half this for half-wave rectification, where

X_{max} = the peak amplitude of the sinusoid.

Effective or RMS Values

For a periodic waveform with period T , the rms or effective value is

$$X_{\text{eff}} = X_{\text{rms}} = \left[(1/T) \int_0^T x^2(t) dt \right]^{1/2}$$

For a sinusoidal waveform and full-wave rectified sine wave,

$$X_{\text{eff}} = X_{\text{rms}} = X_{\text{max}}/\sqrt{2}$$

For a half-wave rectified sine wave,

$$X_{\text{eff}} = X_{\text{rms}} = X_{\text{max}}/2$$

For a periodic signal,

$$X_{\text{rms}} = \sqrt{X_{\text{dc}}^2 + \sum_{n=1}^{\infty} X_n^2} \quad \text{where}$$

X_{dc} is the dc component of $x(t)$

X_n is the rms value of the n th harmonic

Sine-Cosine Relations and Trigonometric Identities

$$\cos(\omega t) = \sin(\omega t + \pi/2) = -\sin(\omega t - \pi/2)$$

$$\sin(\omega t) = \cos(\omega t - \pi/2) = -\cos(\omega t + \pi/2)$$

Other trigonometric identities for sinusoids are given in the section on Trigonometry.

Phasor Transforms of Sinusoids

$$P[V_{\text{max}} \cos(\omega t + \phi)] = V_{\text{rms}} \angle \phi = \mathbf{V}$$

$$P[I_{\text{max}} \cos(\omega t + \theta)] = I_{\text{rms}} \angle \theta = \mathbf{I}$$

For a circuit element, the impedance is defined as the ratio of phasor voltage to phasor current.

$$\mathbf{Z} = \mathbf{V}/\mathbf{I}$$

For a resistor, $\mathbf{Z}_R = R$

$$\text{For a capacitor, } \mathbf{Z}_C = \frac{1}{j\omega C} = jX_C$$

For an inductor,

$$\mathbf{Z}_L = j\omega L = jX_L, \text{ where}$$

X_C and X_L are the capacitive and inductive reactances respectively defined as

$$X_C = -\frac{1}{\omega C} \text{ and } X_L = \omega L$$

Impedances in series combine additively while those in parallel combine according to the reciprocal rule just as in the case of resistors.

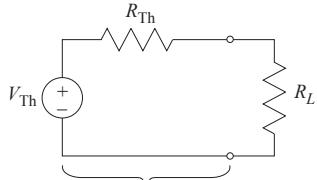
Maximum Power-Transfer Theorem

DC Circuits

Maximum power transfer to the load R_L occurs when $R_L = R_{Th}$

$$P_{\max} = \frac{V_{Th}^2}{4 R_{Th}}$$

$$\text{Efficiency: } \eta = \frac{P_L}{P_S} = \frac{R_L}{R_L + R_{Th}}$$

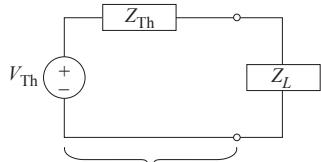


Thevenin Equivalent Circuit

AC Circuits

In an ac circuit maximum power transfer to the load impedance Z_L occurs when the load impedance equals the complex conjugate of the Thevenin equivalent impedance:

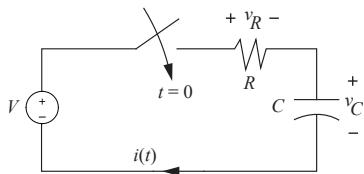
$$Z_L = Z_{Th}^*$$



Thevenin Equivalent Circuit

*If the load is purely resistive (R_L) then for maximum power transfer $R_L = |Z_{Th}|$

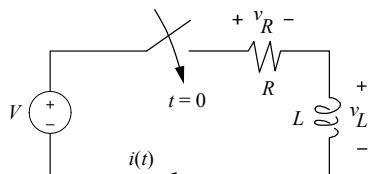
RC AND RL TRANSIENTS



$$t \geq 0; v_C(t) = v_C(0)e^{-t/RC} + V(1 - e^{-t/RC})$$

$$i(t) = \{[V - v_C(0)]/R\}e^{-t/RC}$$

$$v_R(t) = i(t)R = [V - v_C(0)]e^{-t/RC}$$



$$t \geq 0; i(t) = i(0)e^{-Rt/L} + \frac{V}{R}(1 - e^{-Rt/L})$$

$$v_R(t) = i(t)R = i(0)Re^{-Rt/L} + V(1 - e^{-Rt/L})$$

$$v_L(t) = L(di/dt) = -i(0)Re^{-Rt/L} + Ve^{-Rt/L}$$

where $v(0)$ and $i(0)$ denote the initial conditions and the parameters RC and L/R are termed the respective circuit time constants.

RESONANCE

The radian resonant frequency for both parallel and series resonance situations is

$$\omega_0 = \frac{1}{\sqrt{LC}} = 2\pi f_0 \text{ rad/s}$$

Series Resonance

$$\omega_0 L = \frac{1}{\omega_0 C}$$

$Z = R$ at resonance

$$Q = \frac{\omega_0 L}{R} = \frac{1}{\omega_0 CR}$$

$$BW = \frac{\omega_0}{Q} \text{ rad/s}$$

Parallel Resonance

$$\omega_0 C = \frac{1}{\omega_0 R}$$

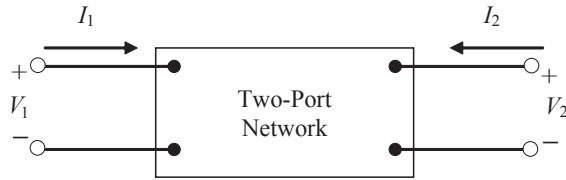
$Z = R$ at resonance

$$Q = \omega_0 RC = \frac{1}{\omega_0 L}$$

$$BW = \frac{\omega_0}{Q} \text{ rad/s}$$

TWO-PORT PARAMETERS

A two-port network consists of two input and two output terminals as shown.



A two-port network may be represented by an equivalent circuit using a set of two-port parameters. Three commonly used sets of parameters are impedance, admittance, and hybrid parameters. The following table describes the equations used for each of these sets of parameters.

Parameter Type	Equations	Definitions
Impedance (z)	$V_1 = z_{11}I_1 + z_{12}I_2$ $V_2 = z_{21}I_1 + z_{22}I_2$	$z_{11} = \frac{V_1}{I_1} \Big _{I_2=0}$ $z_{12} = \frac{V_1}{I_2} \Big _{I_1=0}$ $z_{21} = \frac{V_2}{I_1} \Big _{I_2=0}$ $z_{22} = \frac{V_2}{I_2} \Big _{I_1=0}$
Admittance (y)	$I_1 = y_{11}V_1 + y_{12}V_2$ $I_2 = y_{21}V_1 + y_{22}V_2$	$y_{11} = \frac{I_1}{V_1} \Big _{V_2=0}$ $y_{12} = \frac{I_1}{V_2} \Big _{V_1=0}$ $y_{21} = \frac{I_2}{V_1} \Big _{V_2=0}$ $y_{22} = \frac{I_2}{V_2} \Big _{V_1=0}$
Hybrid (h)	$V_1 = h_{11}I_1 + h_{12}V_2$ $I_2 = h_{21}I_1 + h_{22}V_2$	$h_{11} = \frac{V_1}{I_1} \Big _{V_2=0}$ $h_{12} = \frac{V_1}{V_2} \Big _{I_1=0}$ $h_{21} = \frac{I_2}{V_1} \Big _{V_2=0}$ $h_{22} = \frac{I_2}{V_2} \Big _{I_1=0}$

AC POWER

Complex Power

Real power P (watts) is defined by

$$P = (\frac{1}{2})V_{\text{max}}I_{\text{max}}\cos\theta \\ = V_{\text{rms}}I_{\text{rms}}\cos\theta$$

where θ is the angle measured from \mathbf{V} to \mathbf{I} . If \mathbf{I} leads (lags) \mathbf{V} , then the power factor (pf),

$$pf = \cos\theta$$

is said to be a leading (lagging) pf .

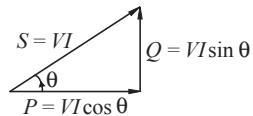
Reactive power Q (vars) is defined by

$$Q = (\frac{1}{2})V_{\text{max}}I_{\text{max}}\sin\theta \\ = V_{\text{rms}}I_{\text{rms}}\sin\theta$$

Complex power \mathbf{S} (volt-amperes) is defined by

$$\mathbf{S} = \mathbf{VI}^* = P + jQ,$$

where \mathbf{I}^* is the complex conjugate of the phasor current.



Complex Power Triangle (Inductive Load)

For resistors, $\theta = 0$, so the real power is

$$P = V_{\text{rms}}I_{\text{rms}} = V_{\text{rms}}^2/R = I_{\text{rms}}^2R$$

Balanced Three-Phase (3-φ) Systems

The 3-φ line-phase relations are

for a delta

$$V_L = V_P$$

$$I_L = \sqrt{3}I_P$$

for a wye

$$V_L = \sqrt{3}V_P = \sqrt{3}V_{LN}$$

$$I_L = I_P$$

where subscripts L and P denote line and phase respectively.

A balanced 3-φ, delta-connected load impedance can be converted to an equivalent wye-connected load impedance using the following relationship

$$\mathbf{Z}_\Delta = 3\mathbf{Z}_Y$$

The following formulas can be used to determine 3-φ power for balanced systems.

$$\mathbf{S} = P + jQ$$

$$|\mathbf{S}| = 3V_PI_P = \sqrt{3}V_LI_L$$

$$\mathbf{S} = 3V_P\mathbf{I}_P^* = \sqrt{3}V_LI_L(\cos\theta_P + j\sin\theta_P)$$

For balanced 3-φ, wye- and delta-connected loads

$$\mathbf{S} = \frac{V_L^2}{Z_Y} \quad \mathbf{S} = 3\frac{V_L^2}{Z_\Delta}$$

where

- S = total 3- ϕ complex power (VA)
- $|S|$ = total 3- ϕ apparent power (VA)
- P = total 3- ϕ real power (W)
- Q = total 3- ϕ reactive power (var)
- θ_P = power factor angle of each phase
- V_L = rms value of the line-to-line voltage
- V_{LN} = rms value of the line-to-neutral voltage
- I_L = rms value of the line current
- I_P = rms value of the phase current

For a 3- ϕ , wye-connected source or load with line-to-neutral voltages and a positive phase sequence

$$\mathbf{V}_{an} = V_p \angle 0^\circ$$

$$\mathbf{V}_{bn} = V_p \angle -120^\circ$$

$$\mathbf{V}_{cn} = V_p \angle 120^\circ$$

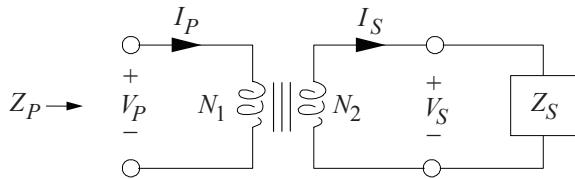
The corresponding line-to-line voltages are

$$\mathbf{V}_{ab} = \sqrt{3} V_p \angle 30^\circ$$

$$\mathbf{V}_{bc} = \sqrt{3} V_p \angle -90^\circ$$

$$\mathbf{V}_{ca} = \sqrt{3} V_p \angle 150^\circ$$

Transformers (Ideal)



Turns Ratio

$$a = N_1 / N_2$$

$$a = \left| \frac{\mathbf{V}_P}{\mathbf{V}_S} \right| = \left| \frac{\mathbf{I}_S}{\mathbf{I}_P} \right|$$

The impedance seen at the input is

$$\mathbf{Z}_P = a^2 \mathbf{Z}_S$$

AC Machines

The synchronous speed n_s for ac motors is given by

$$n_s = 120f/p, \text{ where}$$

f = the line voltage frequency (Hz)

p = the number of poles

The slip for an induction motor is

$$\text{slip} = (n_s - n)/n_s, \text{ where}$$

n = the rotational speed (rpm)

DC Machines

The armature circuit of a dc machine is approximated by a series connection of the armature resistance R_a , the armature inductance L_a , and a dependent voltage source of value

$$V_a = K_a n \phi \text{ volts, where}$$

K_a = constant depending on the design

n = armature speed (rpm)

ϕ = the magnetic flux generated by the field

The field circuit is approximated by the field resistance R_f in series with the field inductance L_f . Neglecting saturation, the magnetic flux generated by the field current I_f is

$$\phi = K_f I_f \text{ webers}$$

The mechanical power generated by the armature is

$$P_m = V_a I_a \text{ watts}$$

where I_a is the armature current. The mechanical torque produced is

$$T_m = (60/2\pi) K_a \phi I_a \text{ newton-meters.}$$

Servomotors and Generators

Servomotors are electrical motors tied to a feedback system to obtain precise control. Smaller servomotors typically are dc motors.

A permanent magnet dc generator can be used to convert mechanical energy to electrical energy, as in a tachometer.

DC motor suppliers may provide data sheets with speed torque curves, motor torque constants (K_T), and motor voltage constants (K_E). An idealized dc motor at steady state exhibits the following relationships:

$$\begin{aligned} V &= I R + K_E \omega \\ T &= K_T I \end{aligned}$$

where

V = voltage at the motor terminals

I = current through the motor

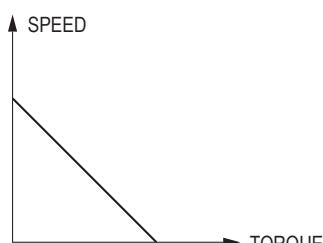
T = torque applied by the motor

R = resistance of the windings

ω = rotational speed

When using consistent SI units [N•m/A and V/(rad/s)], $K_T = K_E$.

An ideal speed-torque curve for a servomotor, with constant V , would look like this:



ELECTROMAGNETIC DYNAMIC FIELDS

The integral and point form of Maxwell's equations are

$$\begin{aligned}\oint \mathbf{E} \cdot d\ell &= -\iint_S (\partial \mathbf{B} / \partial t) \cdot d\mathbf{S} \\ \oint \mathbf{H} \cdot d\ell &= I_{\text{enc}} + \iint_S (\partial \mathbf{D} / \partial t) \cdot d\mathbf{S} \\ \iint_{S_V} \mathbf{D} \cdot d\mathbf{S} &= \iiint_V \rho dV \\ \iint_{S_V} \mathbf{B} \cdot d\mathbf{S} &= 0 \\ \nabla \times \mathbf{E} &= -\partial \mathbf{B} / \partial t \\ \nabla \times \mathbf{H} &= \mathbf{J} + \partial \mathbf{D} / \partial t \\ \nabla \cdot \mathbf{D} &= \rho \\ \nabla \cdot \mathbf{B} &= 0\end{aligned}$$

LOSSLESS TRANSMISSION LINES

The wavelength, λ , of a sinusoidal signal is defined as the distance the signal will travel in one period.

$$\lambda = \frac{U}{f}$$

where U is the velocity of propagation and f is the frequency of the sinusoid.

The characteristic impedance, Z_0 , of a transmission line is the input impedance of an infinite length of the line and is given by

$$Z_0 = \sqrt{L/C}$$

where L and C are the per unit length inductance and capacitance of the line.

The reflection coefficient at the load is defined as

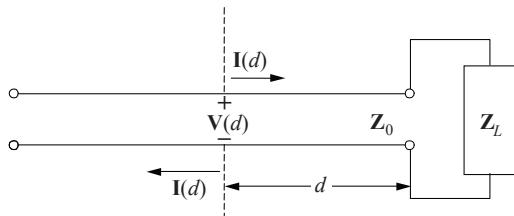
$$\Gamma = \frac{Z_L - Z_0}{Z_L + Z_0}$$

and the standing wave ratio SWR is

$$\text{SWR} = \frac{1 + |\Gamma|}{1 - |\Gamma|}$$

$$\beta = \text{Propagation constant} = \frac{2\pi}{\lambda}$$

For sinusoidal voltages and currents:



Voltage across the transmission line:

$$\mathbf{V}(d) = \mathbf{V}^+ e^{j\beta d} + \mathbf{V}^- e^{-j\beta d}$$

Current along the transmission line:

$$\mathbf{I}(d) = \mathbf{I}^+ e^{j\beta d} + \mathbf{I}^- e^{-j\beta d}$$

where $\mathbf{I}^+ = \mathbf{V}^+ / Z_0$ and $\mathbf{I}^- = -\mathbf{V}^- / Z_0$

Input impedance at d

$$Z_{\text{in}}(d) = Z_0 \frac{\mathbf{Z}_L + j\mathbf{Z}_0 \tan(\beta d)}{\mathbf{Z}_0 + j\mathbf{Z}_L \tan(\beta d)}$$

DIFFERENCE EQUATIONS

Difference equations are used to model discrete systems.

Systems which can be described by difference equations include computer program variables iteratively evaluated in a loop, sequential circuits, cash flows, recursive processes, systems with time-delay components, etc. Any system whose input $x(t)$ and output $y(t)$ are defined only at the equally spaced intervals $t = kT$ can be described by a difference equation.

First-Order Linear Difference Equation

A first-order difference equation is

$$y[k] + a_1 y[k-1] = x[k]$$

Second-Order Linear Difference Equation

A second-order difference equation is

$$y[k] + a_1 y[k-1] + a_2 y[k-2] = x[k]$$

z -Transforms

The transform definition is

$$F(z) = \sum_{k=0}^{\infty} f[k] z^{-k}$$

The inverse transform is given by the contour integral

$$f[k] = \frac{1}{2\pi j} \oint F(z) z^{k-1} dz$$

and it represents a powerful tool for solving linear shift-invariant difference equations. A limited unilateral list of z -transform pairs follows:

$f[k]$	$F(z)$
$\delta[k]$, Impulse at $k = 0$	1
$u[k]$, Step at $k = 0$	$1/(1 - z^{-1})$
β^k	$1/(1 - \beta z^{-1})$
$y[k-1]$	$z^{-1} Y(z)$
$y[k-2]$	$z^{-2} Y(z)$
$y[k+1]$	$z Y(z) - z y[0]$
$y[k+2]$	$z^2 Y(z) - z^2 y[0] - z y[1]$
$\sum_{m=0}^{\infty} x[k-m] h[m]$	$H(z) X(z)$
$\lim_{k \rightarrow 0} f[k]$	$\lim_{z \rightarrow \infty} F(z)$
$\lim_{k \rightarrow \infty} f[k]$	$\lim_{z \rightarrow 1} (1 - z^{-1}) F(z)$

[Note: The last two transform pairs represent the Initial Value Theorem (I.V.T.) and the Final Value Theorem (F.V.T.) respectively.]

CONVOLUTION

Continuous-time convolution:

$$v(t) = x(t) * y(t) = \int_{-\infty}^{\infty} x(\tau)y(t - \tau)d\tau$$

Discrete-time convolution:

$$v[n] = x[n] * y[n] = \sum_{k=-\infty}^{\infty} x[k]y[n-k]$$

DIGITAL SIGNAL PROCESSING

A discrete-time, linear, time-invariant (DTLTI) system with a single input $x[n]$ and a single output $y[n]$ can be described by a linear difference equation with constant coefficients of the form

$$y[n] + \sum_{i=1}^k b_i y[n-i] = \sum_{i=0}^l a_i x[n-i]$$

If all initial conditions are zero, taking a z -transform yields a transfer function

$$H(z) = \frac{Y(z)}{X(z)} = \frac{\sum_{i=0}^l a_i z^{-i}}{1 + \sum_{i=1}^k b_i z^{-i}}$$

Two common discrete inputs are the unit-step function $u[n]$ and the unit impulse function $\delta[n]$, where

$$u[n] = \begin{cases} 0 & n < 0 \\ 1 & n \geq 0 \end{cases} \text{ and } \delta[n] = \begin{cases} 1 & n = 0 \\ 0 & n \neq 0 \end{cases}$$

The impulse response $h[n]$ is the response of a discrete-time system to $x[n] = \delta[n]$.

A finite impulse response (FIR) filter is one in which the impulse response $h[n]$ is limited to a finite number of points:

$$h[n] = \sum_{i=0}^k a_i \delta[n-i]$$

The corresponding transfer function is given by

$$H(z) = \sum_{i=0}^k a_i z^{-i}$$

where k is the order of the filter.

An infinite impulse response (IIR) filter is one in which the impulse response $h[n]$ has an infinite number of points:

$$h[n] = \sum_{i=0}^{\infty} a_i \delta[n-i]$$

COMMUNICATION THEORY AND CONCEPTS

The following concepts and definitions are useful for communications systems analysis.

Functions

Unit step, $u(t)$	$u(t) = \begin{cases} 0 & t < 0 \\ 1 & t \geq 0 \end{cases}$
Rectangular pulse, $\Pi(t/\tau)$	$\Pi(t/\tau) = \begin{cases} 1 & t/\tau < \frac{1}{2} \\ 0 & t/\tau > \frac{1}{2} \end{cases}$
Triangular pulse, $\Lambda(t/\tau)$	$\Lambda(t/\tau) = \begin{cases} 1 - t/\tau & t/\tau < 1 \\ 0 & t/\tau \geq 1 \end{cases}$
Sinc, $\text{sinc}(at)$	$\text{sinc}(at) = \frac{\sin(a\pi t)}{a\pi t}$
Unit impulse, $\delta(t)$	$\int_{-\infty}^{+\infty} x(t+t_0)\delta(t)dt = x(t_0)$ for every $x(t)$ defined and continuous at $t = t_0$. This is equivalent to $\int_{-\infty}^{+\infty} x(t)\delta(t-t_0)dt = x(t_0)$

$$\begin{aligned} x(t) * h(t) &= \int_{-\infty}^{+\infty} x(\lambda)h(t-\lambda)d\lambda \\ &= h(t) * x(t) = \int_{-\infty}^{+\infty} h(\lambda)x(t-\lambda)d\lambda \end{aligned}$$

In particular,

$$x(t) * \delta(t-t_0) = x(t-t_0)$$

The Fourier Transform and its Inverse

$$X(f) = \int_{-\infty}^{+\infty} x(t)e^{-j2\pi ft}dt$$

$$x(t) = \int_{-\infty}^{+\infty} X(f)e^{j2\pi ft}df$$

$x(t)$ and $X(f)$ form a *Fourier transform pair*:

$$x(t) \leftrightarrow X(f)$$

Frequency Response and Impulse Response

The *frequency response* $H(f)$ of a system with input $x(t)$ and output $y(t)$ is given by

$$H(f) = \frac{Y(f)}{X(f)}$$

This gives

$$Y(f) = H(f)X(f)$$

The response $h(t)$ of a linear time-invariant system to a unit-impulse input $\delta(t)$ is called the *impulse response* of the system. The response $y(t)$ of the system to any input $x(t)$ is the convolution of the input $x(t)$ with the impulse response $h(t)$:

$$\begin{aligned} y(t) &= x(t) * h(t) = \int_{-\infty}^{+\infty} x(\lambda)h(t - \lambda)d\lambda \\ &= h(t) * x(t) = \int_{-\infty}^{+\infty} h(\lambda)x(t - \lambda)d\lambda \end{aligned}$$

Therefore, the impulse response $h(t)$ and frequency response $H(f)$ form a Fourier transform pair:

$$h(t) \leftrightarrow H(f)$$

Parseval's Theorem

The total energy in an energy signal (finite energy) $x(t)$ is given by

$$E = \int_{-\infty}^{+\infty} |x(t)|^2 dt = \int_{-\infty}^{+\infty} |X(f)|^2 df$$

Parseval's Theorem for Fourier Series

A periodic signal $x(t)$ with period T_0 and fundamental frequency $f_0 = 1/T_0 = \omega_0/2\pi$ can be represented by a complex-exponential Fourier series

$$x(t) = \sum_{n=-\infty}^{n=+\infty} X_n e^{jn2\pi f_0 t}$$

The average power in the dc component and the first N harmonics is

$$P = \sum_{n=-N}^{n=+N} |X_n|^2 = X_0^2 + 2 \sum_{n=0}^{n=N} |X_n|^2$$

The total average power in the periodic signal $x(t)$ is given by

Parseval's theorem:

$$P = \frac{1}{T_0} \int_{t_0}^{t_0+T_0} |x(t)|^2 dt = \sum_{n=-\infty}^{n=+\infty} |X_n|^2$$

Decibels and Bode Plots

Decibels is a technique to measure the ratio of two powers:

$$dB = 10\log_{10} (P_2/P_1)$$

The definition can be modified to measure the ratio of two voltages:

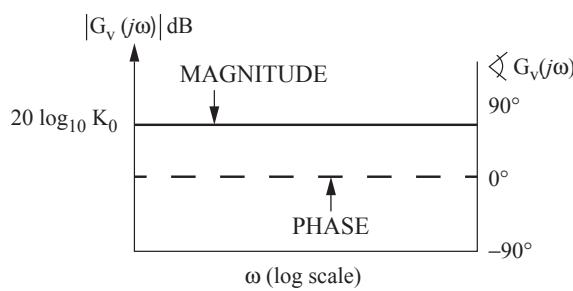
$$dB = 20\log_{10} (V_2/V_1)$$

Bode plots use a logarithmic scale for the frequency when plotting magnitude and phase response, where the magnitude is plotted in dB using a straight-line (asymptotic) approximation.

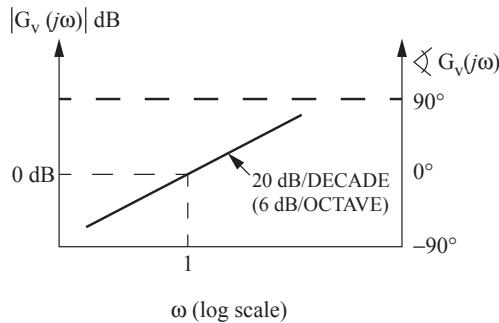
The information below summarizes Bode plots for several terms commonly encountered when determining voltage gain, $G_v(j\omega)$. Since logarithms are used to convert gain to decibels, the decibel response when these various terms are multiplied together can be added to determine the overall response.

Term	Magnitude Response $ G_v(j\omega) _{dB}$	Phase Response $\angle G_v(j\omega)$	Plot
K_0	$20\log_{10}(K_0)$	0°	a
$(j\omega)^{\pm 1}$	$\pm 20\log_{10}(\omega)$	$\pm 90^\circ$	b & c
$(1 + j\omega/\omega_c)^{\pm 1}$	0 for $\omega \ll \omega_c$ ± 3 dB for $\omega = \omega_c$ $\pm 20\log_{10}(\omega)$ for $\omega \gg \omega_c$	0° for $\omega \ll \omega_c$ $\pm 45^\circ$ for $\omega = \omega_c$ $\pm 90^\circ$ for $\omega \gg \omega_c$	d & e

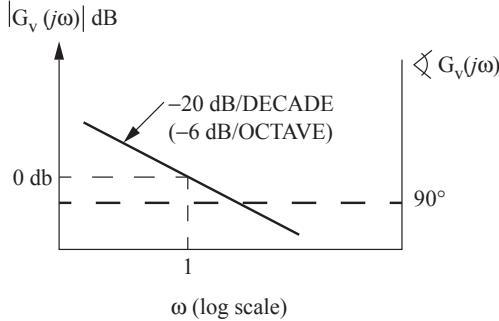
(a) K_0



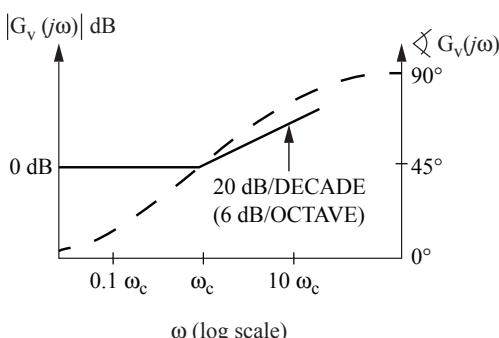
(b) $|G_v(j\omega)|$



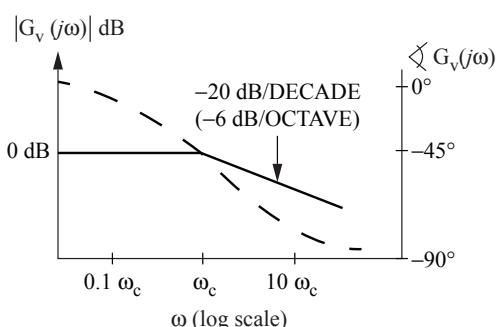
(c) $(j\omega)^{-1}$



(d) $(1 + j\omega/\omega_c)$



(e) $(1 + j\omega/\omega_c)^{-1}$



Amplitude Modulation (AM)

$$x_{AM}(t) = A_c [A + m(t)] \cos(2\pi f_c t)$$

$$= A'_c [1 + am_n(t)] \cos(2\pi f_c t)$$

The *modulation index* is a , and the normalized message is

$$m_n(t) = \frac{m(t)}{\max|m(t)|}$$

The *efficiency* η is the percent of the total transmitted power that contains the message.

$$\eta = \frac{a^2 \langle m_n^2(t) \rangle}{1 + a^2 \langle m_n^2(t) \rangle} \times 100 \text{ percent}$$

where the mean-squared value or normalized average power in $m_n(t)$ is

$$\langle m_n^2(t) \rangle = \lim_{T \rightarrow \infty} \frac{1}{2T} \int_{-T}^{+T} |m_n(t)|^2 dt$$

If $M(f) = 0$ for $|f| > W$, then the *bandwidth* of $x_{AM}(t)$ is $2W$. AM signals can be demodulated with an envelope detector or a synchronous demodulator.

Double-Sideband Modulation (DSB)

$$x_{DSB}(t) = A_c m(t) \cos(2\pi f_c t)$$

If $M(f) = 0$ for $|f| > W$, then the bandwidth of $m(t)$ is W and the bandwidth of $x_{DSB}(t)$ is $2W$. DSB signals must be demodulated with a synchronous demodulator. A Costas loop is often used.

Single-Sideband Modulation (SSB)

Lower Sideband:

$$x_{LSB}(t) \longleftrightarrow X_{LSB}(f) = X_{DSB}(f) \Pi\left(\frac{f}{2f_c}\right)$$

Upper Sideband:

$$x_{USB}(t) \longleftrightarrow X_{USB}(f) = X_{DSB}(f) \left[1 - \Pi\left(\frac{f}{2f_c}\right)\right]$$

In either case, if $M(f) = 0$ for $|f| > W$, then the bandwidth of $x_{LSB}(t)$ or of $x_{USB}(t)$ is W . SSB signals can be demodulated with a synchronous demodulator or by carrier reinsertion and envelope detection.

Angle Modulation

$$x_{Ang}(t) = A_c \cos[2\pi f_c t + \phi(t)]$$

The *phase deviation* $\phi(t)$ is a function of the message $m(t)$.

The *instantaneous phase* is

$$\phi_i(t) = 2\pi f_c t + \phi(t) \text{ rad}$$

The *instantaneous frequency* is

$$\omega_i(t) = \frac{d}{dt} \phi_i(t) = 2\pi f_c + \frac{d}{dt} \phi(t) \text{ rad/s}$$

The *frequency deviation* is

$$\Delta\omega(t) = \frac{d}{dt} \phi(t) \text{ rad/s}$$

The *phase deviation* is

$$\phi(t) = k_p m(t) \text{ rad}$$

The *complete bandwidth* of an angle-modulated signal is infinite.

A discriminator or a phase-lock loop can demodulate angle-modulated signals.

Frequency Modulation (FM)

The *phase deviation* is

$$\phi(t) = k_F \int_{-\infty}^t m(\lambda) d\lambda \text{ rad}$$

The *frequency-deviation ratio* is

$$D = \frac{k_F \max|m(t)|}{2\pi W}$$

where W is the message bandwidth. If $D \ll 1$ (narrowband FM), the 98% power bandwidth B is

$$B \approx 2W$$

If $D > 1$, (wideband FM) the 98% power bandwidth B is given by *Carson's rule*:

$$B \approx 2(D + 1)W$$

Sampled Messages

A low-pass message $m(t)$ can be exactly reconstructed from uniformly spaced samples taken at a sampling frequency of $f_s = 1/T_s$

$$f_s > 2W \text{ where } M(f) = 0 \text{ for } f > W$$

The frequency $2W$ is called the *Nyquist frequency*. Sampled messages are typically transmitted by some form of pulse modulation. The minimum bandwidth B required for transmission of the modulated message is inversely proportional to the pulse length τ .

$$B \propto \frac{1}{\tau}$$

Frequently, for approximate analysis

$$B \approx \frac{1}{2\tau}$$

is used as the *minimum bandwidth* of a pulse of length τ .

Ideal-Impulse Sampling

$$\begin{aligned} x_\delta(t) &= m(t) \sum_{n=-\infty}^{n=+\infty} \delta(t - nT_s) = \sum_{n=-\infty}^{n=+\infty} m(nT_s) \delta(t - nT_s) \\ X_\delta(f) &= M(f) * \left[f_s \sum_{k=-\infty}^{k=+\infty} \delta(f - kf_s) \right] \\ &= f_s \sum_{k=-\infty}^{k=+\infty} M(f - kf_s) \end{aligned}$$

The message $m(t)$ can be recovered from $x_\delta(t)$ with an ideal low-pass filter of bandwidth W if $f_s > 2W$.

(PAM) Pulse-Amplitude Modulation—Natural Sampling

A PAM signal can be generated by multiplying a message by a pulse train with pulses having duration τ and period $T_s = 1/f_s$

$$\begin{aligned} x_N(t) &= m(t) \sum_{n=-\infty}^{n=+\infty} \Pi\left[\frac{t - nT_s}{\tau}\right] = \sum_{n=-\infty}^{n=+\infty} m(t) \Pi\left[\frac{t - nT_s}{\tau}\right] \\ X_N(f) &= \tau f_s \sum_{k=-\infty}^{k=+\infty} \text{sinc}(k\tau f_s) M(f - kf_s) \end{aligned}$$

The message $m(t)$ can be recovered from $x_N(t)$ with an ideal low-pass filter of bandwidth W .

Pulse-Code Modulation (PCM)

PCM is formed by sampling a message $m(t)$ and digitizing the sample values with an A/D converter. For an n -bit binary word length, transmission of a pulse-code-modulated low-pass message $m(t)$, with $M(f) = 0$ for $f \geq W$, requires the transmission of at least $2nW$ binary pulses per second. A binary word of length n bits can represent q quantization levels:

$$q = 2^n$$

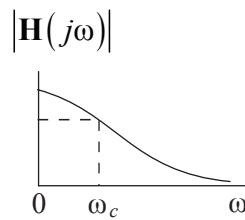
The minimum bandwidth required to transmit the PCM message will be

$$B \approx 2nW = 2W \log_2 q$$

ANALOG FILTER CIRCUITS

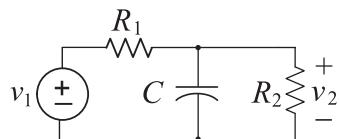
Analog filters are used to separate signals with different frequency content. The following circuits represent simple analog filters used in communications and signal processing.

First-Order Low-Pass Filters



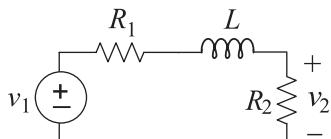
$$|H(j\omega_c)| = \frac{1}{\sqrt{2}} |H(0)|$$

Frequency Response



$$H(s) = \frac{V_2}{V_1} = \frac{R_P}{R_1} \cdot \frac{1}{1 + sR_P C}$$

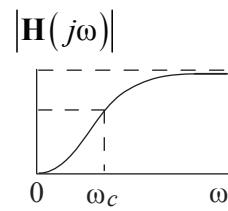
$$R_P = \frac{R_1 R_2}{R_1 + R_2} \quad \omega_c = \frac{1}{R_P C}$$



$$H(s) = \frac{V_2}{V_1} = \frac{R_2}{R_S} \cdot \frac{1}{1 + sL/R_S}$$

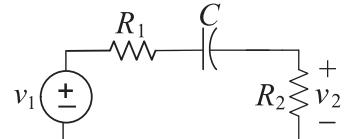
$$R_S = R_1 + R_2 \quad \omega_c = \frac{R_S}{L}$$

First-Order High-Pass Filters



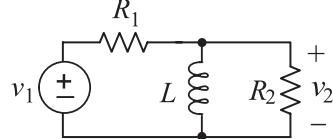
$$|H(j\omega_c)| = \frac{1}{\sqrt{2}} |H(j\infty)|$$

Frequency Response



$$H(s) = \frac{V_2}{V_1} = \frac{R_2}{R_S} \cdot \frac{sR_S C}{1 + sR_S C}$$

$$R_S = R_1 + R_2 \quad \omega_c = \frac{1}{R_S C}$$

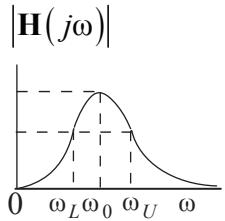


$$H(s) = \frac{V_2}{V_1} = \frac{R_P}{R_1} \cdot \frac{sL/R_P}{1 + sL/R_P}$$

$$R_P = \frac{R_1 R_2}{R_1 + R_2} \quad \omega_c = \frac{R_P}{L}$$

Band-Pass Filters

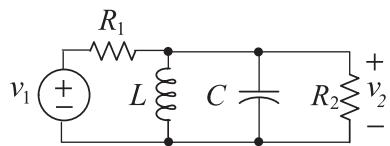
Band-Reject Filters



$$|H(j\omega_L)| = |H(j\omega_U)| = \frac{1}{\sqrt{2}} |H(j\omega_0)|$$

3-dB Bandwidth = $BW = \omega_U - \omega_L$

Frequency Response

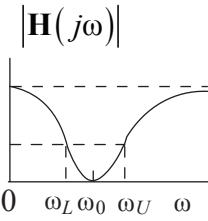


$$H(s) = \frac{V_2}{V_1} = \frac{1}{R_1 C} \cdot \frac{s}{s^2 + s/R_P C + 1/LC}$$

$$R_P = \frac{R_1 R_2}{R_1 + R_2}$$

$$\omega_0 = \frac{1}{\sqrt{LC}}$$

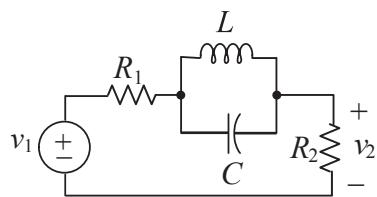
$$|H(j\omega_0)| = \frac{R_2}{R_1 + R_2} = \frac{R_P}{R_1} \quad BW = \frac{1}{R_P C}$$



$$|H(j\omega_L)| = |H(j\omega_U)| = \left[1 - \frac{1}{\sqrt{2}}\right] |H(0)|$$

3-dB Bandwidth = $BW = \omega_U - \omega_L$

Frequency Response

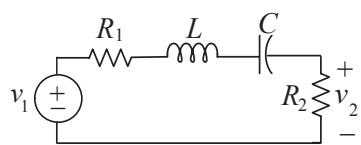


$$H(s) = \frac{V_2}{V_1} = \frac{R_2}{R_S} \cdot \frac{s^2 + 1/LC}{s^2 + s/R_S C + 1/LC}$$

$$R_S = R_1 + R_2$$

$$\omega_0 = \frac{1}{\sqrt{LC}}$$

$$|H(0)| = \frac{R_2}{R_1 + R_2} = \frac{R_2}{R_S} \quad BW = \frac{1}{R_S C}$$

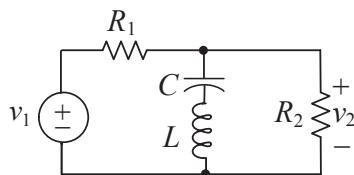


$$H(s) = \frac{V_2}{V_1} = \frac{R_2}{L} \cdot \frac{s}{s^2 + sR_S/L + 1/LC}$$

$$R_S = R_1 + R_2$$

$$\omega_0 = \frac{1}{\sqrt{LC}}$$

$$|H(j\omega_0)| = \frac{R_2}{R_1 + R_2} = \frac{R_2}{R_S} \quad BW = \frac{R_S}{L}$$



$$H(s) = \frac{V_2}{V_1} = \frac{R_P}{R_1} \cdot \frac{s^2 + 1/LC}{s^2 + sR_P/L + 1/LC}$$

$$R_P = \frac{R_1 R_2}{R_1 + R_2}$$

$$\omega_0 = \frac{1}{\sqrt{LC}}$$

$$|H(0)| = \frac{R_2}{R_1 + R_2} = \frac{R_P}{R_1} \quad BW = \frac{R_P}{L}$$

OPERATIONAL AMPLIFIERS

Ideal

$$v_0 = A(v_1 - v_2)$$

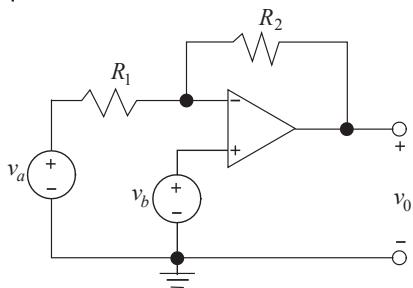
where

A is large ($> 10^4$), and

$v_1 - v_2$ is small enough so as not to saturate the amplifier.

For the ideal operational amplifier, assume that the input currents are zero and that the gain A is infinite so when operating linearly $v_2 - v_1 = 0$.

For the two-source configuration with an ideal operational amplifier,



$$v_0 = -\frac{R_2}{R_1} v_a + \left(1 + \frac{R_2}{R_1}\right) v_b$$

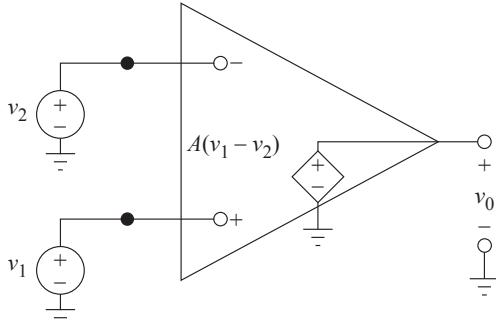
If $v_a = 0$, we have a non-inverting amplifier with

$$v_0 = \left(1 + \frac{R_2}{R_1}\right) v_b$$

If $v_b = 0$, we have an inverting amplifier with

$$v_0 = -\frac{R_2}{R_1} v_a$$

Common Mode Rejection Ratio (CMRR)



Equivalent Circuit of an Ideal Op Amp

In the op amp circuit shown the differential input is defined as:

$$v_{id} = v_1 - v_2$$

The common-mode input voltage is defined as:

$$v_{icm} = (v_1 + v_2)/2$$

The output voltage is given by:

$$v_o = Av_{id} + A_{cm}v_{icm}$$

In an ideal op amp $A_{cm} = 0$. In a non-ideal op amp the CMRR is used to measure the relative degree of rejection between the differential gain and common-mode gain.

$$CMRR = \frac{|A|}{|A_{cm}|}$$

CMRR is usually expressed in decibels as:

$$CMRR = 20 \log_{10} \left[\frac{|A|}{|A_{cm}|} \right]$$

SOLID-STATE ELECTRONICS AND DEVICES

Conductivity of a semiconductor material:

$$\sigma = q(n\mu_n + p\mu_p), \text{ where}$$

μ_n ≡ electron mobility

μ_p ≡ hole mobility

n ≡ electron concentration

p ≡ hole concentration

q ≡ charge on an electron ($1.6 \times 10^{-19} \text{ C}$)

Doped material:

p -type material; $p_p \approx N_a$

n -type material; $n_n \approx N_d$

Carrier concentrations at equilibrium

$$(p)(n) = n_i^2, \text{ where}$$

n_i ≡ intrinsic concentration.

Built-in potential (contact potential) of a p - n junction:

$$V_0 = \frac{kT}{q} \ln \frac{N_a N_d}{n_i^2}$$

Thermal voltage

$$V_T = \frac{kT}{q} \approx 0.026 \text{ V at } 300\text{K}$$

N_a = acceptor concentration

N_d = donor concentration

T = temperature (K)

k = Boltzmann's Constant = $1.38 \times 10^{-23} \text{ J/K}$

Capacitance of abrupt p - n junction diode

$$C(V) = C_0 / \sqrt{1 - V/V_{bi}}, \text{ where:}$$

C_0 = junction capacitance at $V=0$

V = potential of anode with respect to cathode

V_{bi} = junction contact potential

Resistance of a diffused layer is

$$R = R_s(L/W), \text{ where:}$$

R_s = sheet resistance = ρ/d in ohms per square

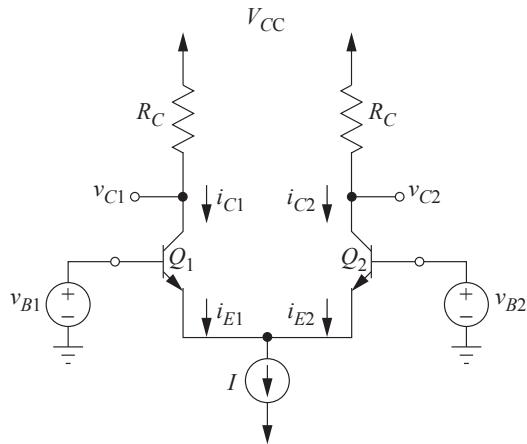
ρ = resistivity

d = thickness

L = length of diffusion

W = width of diffusion

◆ Differential Amplifier



A Basic BJT Differential Amplifier

A basic BJT differential amplifier consists of two matched transistors whose emitters are connected and that are biased by a constant-current source. The following equations govern the operation of the circuit given that neither transistor is operating in the saturation region.

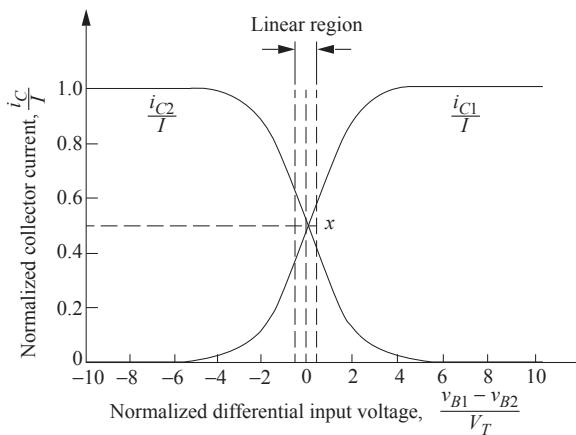
$$\frac{i_{E1}}{i_{E2}} = e^{(v_{B1} - v_{B2})/V_T}$$

$$i_{E1} + i_{E2} = I$$

$$i_{E1} = \frac{I}{1 + e^{(v_{B2} - v_{B1})/V_T}} \quad i_{E2} = \frac{I}{1 + e^{(v_{B1} - v_{B2})/V_T}}$$

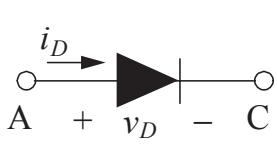
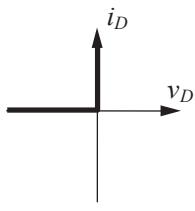
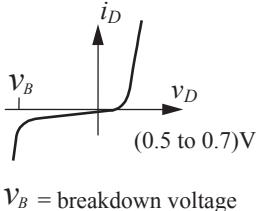
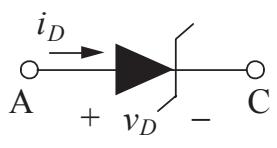
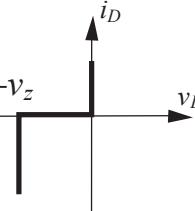
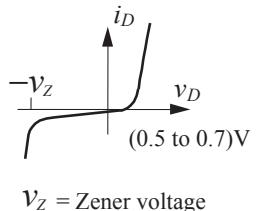
$$i_{C1} = \alpha I_{E1} \quad i_{C2} = \alpha I_{E2}$$

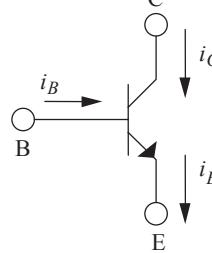
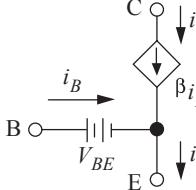
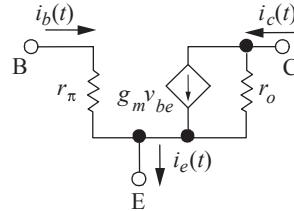
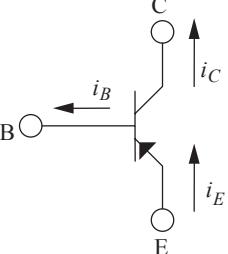
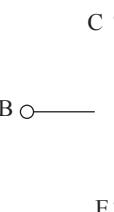
The following figure shows a plot of two normalized collector currents versus normalized differential input voltage for a circuit using transistors with $\alpha \approx 1$.

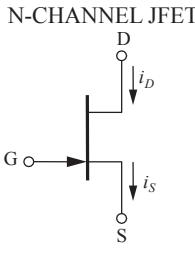
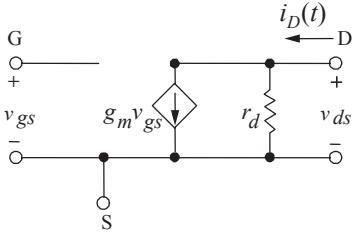
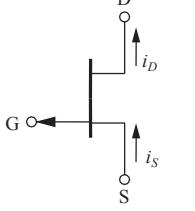
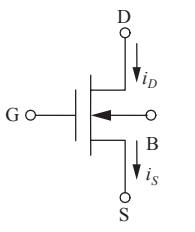
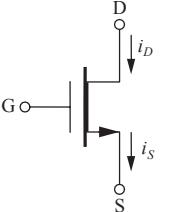
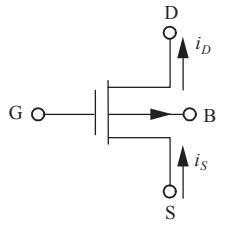
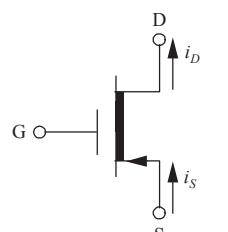


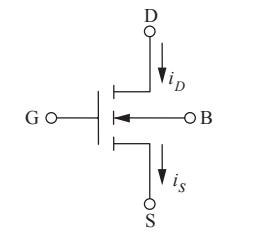
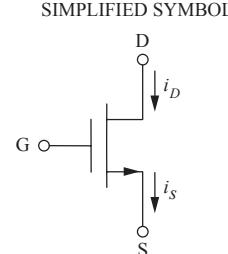
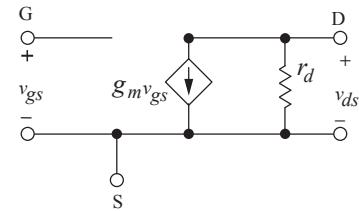
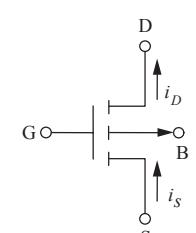
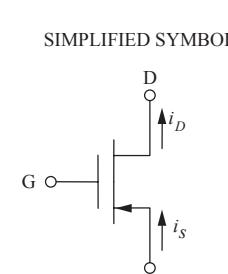
Transfer characteristics of the BJT differential amplifier with $\alpha \approx 1$

◆ Sedra, Adel, and Kenneth Smith, *Microelectronic Circuits*, 3rd ed., ©1991, pp. 408 and 412, by permission of Oxford University Press.

DIODES			
Device and Schematic Symbol	Ideal $I - V$ Relationship	Piecewise-Linear Approximation of the $I - V$ Relationship	Mathematical $I - V$ Relationship
(Junction Diode) 		 V_B = breakdown voltage (0.5 to 0.7)V	Shockley Equation $i_D \approx I_s [e^{(v_D/\eta V_T)} - 1]$ where I_s = saturation current η = emission coefficient, typically 1 for Si V_T = thermal voltage = $\frac{kT}{q}$
(Zener Diode) 		 V_Z = Zener voltage (0.5 to 0.7)V	Same as above.

NPN Bipolar Junction Transistor (BJT)			
Schematic Symbol	Mathematical Relationships	Large-Signal (DC) Equivalent Circuit	Low-Frequency Small-Signal (AC) Equivalent Circuit
 NPN – Transistor	$i_E = i_B + i_C$ $i_C = \beta i_B$ $i_E = \alpha i_E$ $\alpha = \beta / (\beta + 1)$ $i_C \approx I_S e^{(V_{BE}/V_T)}$ I_S = emitter saturation current V_T = thermal voltage Note: These relationships are valid in the active mode of operation.	<u>Active Region:</u> base emitter junction forward biased; base collector junction reverse biased 	<u>Low Frequency:</u> $g_m \approx I_{CQ}/V_T$ $r_\pi \approx \beta/g_m$, $r_o = \left[\frac{\partial v_{CE}}{\partial i_c} \right]_{Q_{point}} \approx \frac{V_A}{I_{CQ}}$ where I_{CQ} = dc collector current at the Q_{point} V_A = Early voltage 
 PNP – Transistor	Same as for NPN with current directions and voltage polarities reversed.	<u>Cutoff Region:</u> both junctions reverse biased 	Same as for NPN.
		Same as NPN with current directions and voltage polarities reversed	

N-Channel Junction Field Effect Transistors (JFETs) and Depletion MOSFETs (Low and Medium Frequency)		
Schematic Symbol	Mathematical Relationships	Small-Signal (AC) Equivalent Circuit
N-CHANNEL JFET 	<p><u>Cutoff Region:</u> $v_{GS} < V_p$ $i_D = 0$</p> <p><u>Triode Region:</u> $v_{GS} > V_p$ and $v_{GD} > V_p$ $i_D = (I_{DSS}/V_p^2)[2v_{DS}(v_{GS} - V_p) - v_{DS}^2]$</p> <p><u>Saturation Region:</u> $v_{GS} > V_p$ and $v_{GD} < V_p$ $i_D = I_{DSS}(1 - v_{GS}/V_p)^2$</p> <p>where I_{DSS} = drain current with $v_{GS} = 0$ (in the saturation region) $= KV_p^2$, K = conductivity factor, and V_p = pinch-off voltage.</p>	$g_m = \frac{2\sqrt{I_{DSS}I_D}}{ V_p } \quad \text{in saturation region}$  <p>where</p> $r_d = \left \frac{\partial v_{ds}}{\partial i_d} \right _{Q_{point}}$
P-CHANNEL JFET 		
N-CHANNEL DEPLETION MOSFET (NMOS) 		
SIMPLIFIED SYMBOL 		
P-CHANNEL DEPLETION MOSFET (PMOS) 	Same as for N-Channel with current directions and voltage polarities reversed.	Same as for N-Channel.
SIMPLIFIED SYMBOL 		

Enhancement MOSFET (Low and Medium Frequency)		
Schematic Symbol	Mathematical Relationships	Small-Signal (AC) Equivalent Circuit
 N-CHANNEL ENHANCEMENT MOSFET (NMOS)  SIMPLIFIED SYMBOL	<p><u>Cutoff Region:</u> $v_{GS} < V_t$ $i_D = 0$</p> <p><u>Triode Region:</u> $v_{GS} > V_t$ and $v_{GD} > V_t$ $i_D = K [2v_{DS} (v_{GS} - V_t) - v_{DS}^2]$</p> <p><u>Saturation Region:</u> $v_{GS} > V_t$ and $v_{GD} < V_t$ $i_D = K (v_{GS} - V_t)^2$ where K = conductivity factor V_t = threshold voltage</p>	$g_m = 2K(v_{GS} - V_t)$ in saturation region  where $r_d = \left \frac{\partial v_{ds}}{\partial i_d} \right _{Q_{\text{point}}}$
 P-CHANNEL ENHANCEMENT MOSFET (PMOS)  SIMPLIFIED SYMBOL	Same as for N-channel with current directions and voltage polarities reversed.	Same as for N-channel.

NUMBER SYSTEMS AND CODES

An unsigned number of base- r has a decimal equivalent D defined by

$$D = \sum_{k=0}^n a_k r^k + \sum_{i=1}^m a_i r^{-i}, \text{ where}$$

a_k = the $(k+1)$ digit to the left of the radix point and
 a_i = the i th digit to the right of the radix point.

Binary Number System

In digital computers, the base-2, or binary, number system is normally used. Thus the decimal equivalent, D , of a binary number is given by

$$D = a_k 2^k + a_{k-1} 2^{k-1} + \dots + a_0 + a_{-1} 2^{-1} + \dots$$

Since this number system is so widely used in the design of digital systems, we use a short-hand notation for some powers of two:

$2^{10} = 1,024$ is abbreviated "k" or "kilo"

$2^{20} = 1,048,576$ is abbreviated "M" or "mega"

Signed numbers of base- r are often represented by the radix complement operation. If M is an N -digit value of base- r , the radix complement $R(M)$ is defined by

$$R(M) = r^N - M$$

The 2's complement of an N -bit binary integer can be written

$$\text{2's Complement } (M) = 2^N - M$$

This operation is equivalent to taking the 1's complement (inverting each bit of M) and adding one.

The following table contains equivalent codes for a four-bit binary value.

Binary Base-2	Decimal Base-10	Hexa-decimal Base-16	Octal Base-8	BCD Code	Gray Code
0000	0	0	0	0	0000
0001	1	1	1	1	0001
0010	2	2	2	2	0011
0011	3	3	3	3	0010
0100	4	4	4	4	0110
0101	5	5	5	5	0111
0110	6	6	6	6	0101
0111	7	7	7	7	0100
1000	8	8	10	8	1100
1001	9	9	11	9	1101
1010	10	A	12	---	1111
1011	11	B	13	---	1110
1100	12	C	14	---	1010
1101	13	D	15	---	1011
1110	14	E	16	---	1001
1111	15	F	17	---	1000

LOGIC OPERATIONS AND BOOLEAN ALGEBRA

Three basic logic operations are the "AND (\bullet)," "OR (+)," and "Exclusive-OR \oplus " functions. The definition of each function, its logic symbol, and its Boolean expression are given in the following table.

Function	AND	OR	XOR
Inputs	A B	A B	A B
	$C = A \bullet B$	$C = A + B$	$C = A \oplus B$
0 0	0	0	0
0 1	0	1	1
1 0	0	1	1
1 1	1	1	0

As commonly used, A AND B is often written AB or $A \bullet B$.

The not operator inverts the sense of a binary value
 $(0 \rightarrow 1, 1 \rightarrow 0)$

NOT OPERATOR	
Input	Output
A	$C = \bar{A}$
0	1
1	0

LOGIC SYMBOL

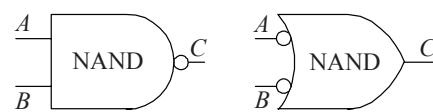
De Morgan's Theorems

$$\text{first theorem: } \overline{A + B} = \overline{A} \cdot \overline{B}$$

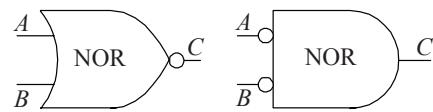
$$\text{second theorem: } \overline{A \bullet B} = \overline{A} + \overline{B}$$

These theorems define the NAND gate and the NOR gate. Logic symbols for these gates are shown below.

$$\text{NAND Gates: } \overline{A \bullet B} = \overline{A} + \overline{B}$$

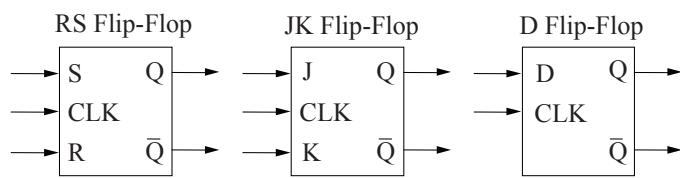


$$\text{NOR Gates: } \overline{A + B} = \overline{A} \bullet \overline{B}$$



FLIP-FLOPS

A flip-flop is a device whose output can be placed in one of two states, 0 or 1. The flip-flop output is synchronized with a clock (CLK) signal. Q_n represents the value of the flip-flop output before CLK is applied, and Q_{n+1} represents the output after CLK has been applied. Three basic flip-flops are described below.



SR	Q_{n+1}	JK	Q_{n+1}	D	Q_{n+1}
00	Q_n no change	00	Q_n no change	0	
01	0	01	0		
10	1	10	1		
11	x invalid	11	\bar{Q}_n toggle		

Composite Flip-Flop State Transition						
Q_n	Q_{n+1}	S	R	J	K	D
0	0	0	x	0	x	0
0	1	1	0	1	x	1
1	0	0	1	x	1	0
1	1	x	0	x	0	1

Switching Function Terminology

Minterm, m_i – A product term which contains an occurrence of every variable in the function.

Maxterm, M_j – A sum term which contains an occurrence of every variable in the function.

Implicant – A Boolean algebra term, either in sum or product form, which contains one or more minterms or maxterms of a function.

Prime Implicant – An implicant which is not entirely contained in any other implicant.

Essential Prime Implicant – A prime implicant which contains a minterm or maxterm which is not contained in any other prime implicant.

A function can be described as a sum of minterms using the notation

$$\begin{aligned} F(ABCD) &= \sum m(h, i, j, \dots) \\ &= m_h + m_i + m_j + \dots \end{aligned}$$

A function can be described as a product of maxterms using the notation

$$\begin{aligned} G(ABCD) &= \prod M(h, i, j, \dots) \\ &= M_h \cdot M_i \cdot M_j \cdot \dots \end{aligned}$$

A function represented as a sum of minterms only is said to be in *canonical sum of products* (SOP) form. A function represented as a product of maxterms only is said to be in *canonical product of sums* (POS) form. A function in canonical SOP form is often represented as a *minterm list*, while a function in canonical POS form is often represented as a *maxterm list*.

A *Karnaugh Map* (K-Map) is a graphical technique used to represent a truth table. Each square in the K-Map represents one minterm, and the squares of the K-Map are arranged so that the adjacent squares differ by a change in exactly one variable. A four-variable K-Map with its corresponding minterms is shown below. K-Maps are used to simplify switching functions by visually identifying all essential prime implicants.

		CD	00	01	11	10
AB		00	m_0	m_1	m_3	m_2
		01	m_4	m_5	m_7	m_6
		11	m_{12}	m_{13}	m_{15}	m_{14}
		10	m_8	m_9	m_{11}	m_{10}

INDUSTRIAL ENGINEERING

LINEAR PROGRAMMING

The general linear programming (LP) problem is:

$$\text{Maximize } Z = c_1x_1 + c_2x_2 + \dots + c_nx_n$$

Subject to:

$$a_{11}x_1 + a_{12}x_2 + \dots + a_{1n}x_n \leq b_1$$

$$a_{21}x_1 + a_{22}x_2 + \dots + a_{2n}x_n \leq b_2$$

⋮

$$a_{m1}x_1 + a_{m2}x_2 + \dots + a_{mn}x_n \leq b_m$$

$$x_1, \dots, x_n \geq 0$$

An LP problem is frequently reformulated by inserting non-negative slack and surplus variables. Although these variables usually have zero costs (depending on the application), they can have non-zero cost coefficients in the objective function. A slack variable is used with a "less than" inequality and transforms it into an equality. For example, the inequality $5x_1 + 3x_2 + 2x_3 \leq 5$ could be changed to $5x_1 + 3x_2 + 2x_3 + s_1 = 5$ if s_1 were chosen as a slack variable. The inequality $3x_1 + x_2 - 4x_3 \geq 10$ might be transformed into $3x_1 + x_2 - 4x_3 - s_2 = 10$ by the addition of the surplus variable s_2 . Computer printouts of the results of processing an LP usually include values for all slack and surplus variables, the dual prices, and the reduced costs for each variable.

Dual Linear Program

Associated with the above linear programming problem is another problem called the dual linear programming problem. If we take the previous problem and call it the primal problem, then in matrix form the primal and dual problems are respectively:

Primal

$$\text{Maximize } Z = \mathbf{c}\mathbf{x}$$

$$\text{Subject to: } \mathbf{A}\mathbf{x} \leq \mathbf{b}$$

$$\mathbf{x} \geq 0$$

Dual

$$\text{Minimize } W = \mathbf{y}\mathbf{b}$$

$$\text{Subject to: } \mathbf{y}\mathbf{A} \geq \mathbf{c}$$

$$\mathbf{y} \geq 0$$

It is assumed that if \mathbf{A} is a matrix of size $[m \times n]$, then \mathbf{y} is a $[1 \times m]$ vector, \mathbf{c} is a $[1 \times n]$ vector, \mathbf{b} is an $[m \times 1]$ vector, and \mathbf{x} is an $[n \times 1]$ vector.

Network Optimization

Assume we have a graph $G(N, A)$ with a finite set of nodes N and a finite set of arcs A . Furthermore, let

$$N = \{1, 2, \dots, n\}$$

x_{ij} = flow from node i to node j

c_{ij} = cost per unit flow from i to j

u_{ij} = capacity of arc (i, j)

b_i = net flow generated at node i

We wish to minimize the total cost of sending the available supply through the network to satisfy the given demand. The minimal cost flow model is formulated as follows:

$$\text{Minimize } Z = \sum_{i=1}^n \sum_{j=1}^n c_{ij}x_{ij}$$

subject to

$$\sum_{j=1}^n x_{ij} - \sum_{j=1}^n x_{ji} = b_i \text{ for each node } i \in N$$

and

$$0 \leq x_{ij} \leq u_{ij} \text{ for each arc } (i, j) \in A$$

The constraints on the nodes represent a conservation of flow relationship. The first summation represents total flow out of node i , and the second summation represents total flow into node i . The net difference generated at node i is equal to b_i .

Many models, such as shortest-path, maximal-flow, assignment and transportation models, can be reformulated as minimal-cost network flow models.

PROCESS CAPABILITY

Actual Capability

$$PCR_k = C_{pk} = \min\left(\frac{\mu - LSL}{3\sigma}, \frac{USL - \mu}{3\sigma}\right)$$

Potential Capability (i.e., Centered Process)

$$PCR = C_p = \frac{USL - LSL}{6\sigma}, \text{ where}$$

μ and σ are the process mean and standard deviation, respectively, and LSL and USL are the lower and upper specification limits, respectively.

QUEUEING MODELS

Definitions

P_n = probability of n units in system

L = expected number of units in the system

L_q = expected number of units in the queue

W = expected waiting time in system

W_q = expected waiting time in queue

λ = mean arrival rate (constant)

$\tilde{\lambda}$ = effective arrival rate

μ = mean service rate (constant)

ρ = server utilization factor

s = number of servers

Kendall notation for describing a queueing system:

$A / B / s / M$

A = the arrival process

B = the service time distribution

s = the number of servers

M = the total number of customers including those in service

Fundamental Relationships

$$L = \lambda W$$

$$L_q = \lambda W_q$$

$$W = W_q + 1/\mu$$

$$\rho = \lambda/(s\mu)$$

Single Server Models ($s = 1$)

Poisson Input—Exponential Service Time: $M = \infty$

$$P_0 = 1 - \lambda/\mu = 1 - \rho$$

$$P_n = (1 - \rho)\rho^n = P_0\rho^n$$

$$L = \rho/(1 - \rho) = \lambda/(\mu - \lambda)$$

$$L_q = \lambda^2/[\mu(\mu - \lambda)]$$

$$W = 1/[\mu(1 - \rho)] = 1/(\mu - \lambda)$$

$$W_q = W - 1/\mu = \lambda/[\mu(\mu - \lambda)]$$

Finite queue: $M < \infty$

$$\tilde{\lambda} = \lambda(1 - P_m)$$

$$P_0 = (1 - \rho)/(1 - \rho^{M+1})$$

$$P_n = [(1 - \rho)/(1 - \rho^{M+1})]\rho^n$$

$$L = \rho/(1 - \rho) - (M + 1)\rho^{M+1}/(1 - \rho^{M+1})$$

$$L_q = L - (1 - P_0)$$

$$W = L/\tilde{\lambda}$$

$$W = W_q + 1/\mu$$

Poisson Input—Arbitrary Service Time

Variance σ^2 is known. For constant service time, $\sigma^2 = 0$.

$$P_0 = 1 - \rho$$

$$L_q = (\lambda^2\sigma^2 + \rho^2)/[2(1 - \rho)]$$

$$L = \rho + L_q$$

$$W_q = L_q / \lambda$$

$$W = W_q + 1/\mu$$

Poisson Input—Erlang Service Times, $\sigma^2 = 1/(k\mu^2)$

$$L_q = [(1 + k)/(2k)][(\lambda^2)/(\mu(\mu - \lambda))]$$

$$= [\lambda^2/(k\mu^2) + \rho^2]/[2(1 - \rho)]$$

$$W_q = [(1 + k)/(2k)]\{\lambda/[\mu(\mu - \lambda)]\}$$

$$W = W_q + 1/\mu$$

Multiple Server Model ($s > 1$)

Poisson Input—Exponential Service Times

$$P_0 = \left[\sum_{n=0}^{s-1} \frac{\left(\frac{\lambda}{\mu}\right)^n}{n!} + \frac{\left(\frac{\lambda}{\mu}\right)^s}{s!} \left(\frac{1}{1 - \frac{\lambda}{s\mu}} \right) \right]^{-1}$$

$$= 1 / \left[\sum_{n=0}^{s-1} \frac{(s\rho)^n}{n!} + \frac{(s\rho)^s}{s!(1 - \rho)} \right]$$

$$L_q = \frac{P_0 \left(\frac{\lambda}{\mu}\right)^s \rho}{s! (1 - \rho)^2}$$

$$= \frac{P_0 s^s \rho^{s+1}}{s! (1 - \rho)^2}$$

$$P_n = P_0 (\lambda/\mu)^n / n! \quad 0 \leq n \leq s$$

$$P_n = P_0 (\lambda/\mu)^n / (s! s^{n-s}) \quad n \geq s$$

$$W_q = L_q / \lambda$$

$$W = W_q + 1/\mu$$

$$L = L_q + \lambda/\mu$$

Calculations for P_0 and L_q can be time consuming; however, the following table gives formulas for 1, 2, and 3 servers.

s	P_0	L_q
1	$1 - \rho$	$\rho^2/(1 - \rho)$
2	$(1 - \rho)/(1 + \rho)$	$2\rho^3/(1 - \rho^2)$
3	$\frac{2(1 - \rho)}{2 + 4\rho + 3\rho^2}$	$\frac{9\rho^4}{2 + 2\rho - \rho^2 - 3\rho^3}$

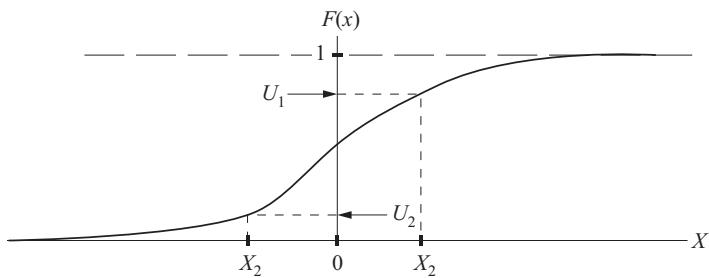
SIMULATION

1. Random Variate Generation

The linear congruential method of generating pseudo-random numbers U_i between 0 and 1 is obtained using $Z_n = (aZ_{n-1} + C) \pmod{m}$ where a , C , m , and Z_0 are given nonnegative integers and where $U_i = Z_i/m$. Two integers are equal $(\pmod m)$ if their remainders are the same when divided by m .

2. Inverse Transform Method

If X is a continuous random variable with cumulative distribution function $F(x)$, and U_i is a random number between 0 and 1, then the value of X_i corresponding to U_i can be calculated by solving $U_i = F(x_i)$ for x_i . The solution obtained is $x_i = F^{-1}(U_i)$, where F^{-1} is the inverse function of $F(x)$.



Inverse Transform Method for Continuous Random Variables

FORECASTING

Moving Average

$$\hat{d}_t = \frac{\sum_{i=1}^n d_{t-i}}{n}, \text{ where}$$

\hat{d}_t = forecasted demand for period t

d_{t-i} = actual demand for i th period preceding t

n = number of time periods to include in the moving average

Exponentially Weighted Moving Average

$$\hat{d}_t = \alpha d_{t-1} + (1 - \alpha) \hat{d}_{t-1}, \text{ where}$$

\hat{d}_t = forecasted demand for t

α = smoothing constant, $0 \leq \alpha \leq 1$

RANDOMIZED BLOCK DESIGN

The experimental material is divided into n randomized blocks. One observation is taken at random for every treatment within the same block. The total number of observations is $N = nk$. The total value of these observations is equal to T . The total value of observations for treatment i is T_i . The total value of observations in block j is B_j .

$$C = T^2/N$$

$$SS_{\text{total}} = \sum_{i=1}^k \sum_{j=1}^n x_{ij}^2 - C$$

$$SS_{\text{blocks}} = \sum_{j=1}^n (B_j^2/k) - C$$

$$SS_{\text{treatments}} = \sum_{i=1}^k (T_i^2/n) - C$$

$$SS_{\text{error}} = SS_{\text{total}} - SS_{\text{blocks}} - SS_{\text{treatments}}$$

2ⁿ FACTORIAL EXPERIMENTS

Factors: X_1, X_2, \dots, X_n

Levels of each factor: 1, 2 (sometimes these levels are represented by the symbols – and +, respectively)

r = number of observations for each experimental condition (treatment)

E_i = estimate of the effect of factor X_i , $i = 1, 2, \dots, n$

E_{ij} = estimate of the effect of the interaction between factors X_i and X_j

\bar{Y}_{ik} = average response value for all $r2^{n-1}$ observations having X_i set at level k , $k = 1, 2$

\bar{Y}_{ij}^{km} = average response value for all $r2^{n-2}$ observations having X_i set at level k , $k = 1, 2$, and X_j set at level m , $m = 1, 2$.

$$E_i = \bar{Y}_{i2} - \bar{Y}_{i1}$$

$$E_{ij} = \frac{(\bar{Y}_{ij}^{22} - \bar{Y}_{ij}^{21}) - (\bar{Y}_{ij}^{12} - \bar{Y}_{ij}^{11})}{2}$$

ANALYSIS OF VARIANCE FOR 2ⁿ FACTORIAL DESIGNS

Main Effects

Let E be the estimate of the effect of a given factor, let L be the orthogonal contrast belonging to this effect. It can be proved that

$$E = \frac{L}{2^{n-1}}$$

$$L = \sum_{c=1}^m a_{(c)} \bar{Y}_{(c)}$$

$$SS_L = \frac{rL^2}{2^n}, \text{ where}$$

m = number of experimental conditions
($m = 2^n$ for n factors)

$a_{(c)}$ = -1 if the factor is set at its low level (level 1) in experimental condition c

$a_{(c)}$ = +1 if the factor is set at its high level (level 2) in experimental condition c

r = number of replications for each experimental condition

$\bar{Y}_{(c)}$ = average response value for experimental condition c

SS_L = sum of squares associated with the factor

Interaction Effects

Consider any group of two or more factors.

$a_{(c)} = +1$ if there is an even number (or zero) of factors in the group set at the low level (level 1) in experimental condition $c = 1, 2, \dots, m$

$a_{(c)} = -1$ if there is an odd number of factors in the group set at the low level (level 1) in experimental condition $c = 1, 2, \dots, m$

It can be proved that the interaction effect E for the factors in the group and the corresponding sum of squares SS_L can be determined as follows:

$$E = \frac{L}{2^{n-1}}$$

$$L = \sum_{c=1}^m a_{(c)} \bar{Y}_{(c)}$$

$$SS_L = \frac{rL^2}{2^n}$$

Sum of Squares of Random Error

The sum of the squares due to the random error can be computed as

$$SS_{\text{error}} = SS_{\text{total}} - \sum_i SS_i - \sum_j SS_{ij} - \dots - SS_{12\dots n}$$

where SS_i is the sum of squares due to factor X_i , SS_{ij} is the sum of squares due to the interaction of factors X_i and X_j , and so on. The total sum of squares is equal to

$$SS_{\text{total}} = \sum_{c=1}^m \sum_{k=1}^r Y_{ck}^2 - \frac{T^2}{N}$$

where Y_{ck} is the k th observation taken for the c th experimental condition, $m = 2^n$, T is the grand total of all observations, and $N = r2^n$.

RELIABILITY

If P_i is the probability that component i is functioning, a reliability function $R(P_1, P_2, \dots, P_n)$ represents the probability that a system consisting of n components will work.

For n independent components connected in series,

$$R(P_1, P_2, \dots, P_n) = \prod_{i=1}^n P_i$$

For n independent components connected in parallel,

$$R(P_1, P_2, \dots, P_n) = 1 - \prod_{i=1}^n (1 - P_i)$$

LEARNING CURVES

The time to do the repetition N of a task is given by

$$T_N = KN^s, \text{ where}$$

K = constant

s = ln (learning rate, as a decimal)/ln 2; or, learning rate = 2^s

If N units are to be produced, the average time per unit is given by

$$T_{\text{avg}} = \frac{K}{N(1+s)} [(N+0.5)^{(1+s)} - 0.5^{(1+s)}]$$

INVENTORY MODELS

For instantaneous replenishment (with constant demand rate, known holding and ordering costs, and an infinite stockout cost), the economic order quantity is given by

$$EOQ = \sqrt{\frac{2AD}{h}}, \text{ where}$$

A = cost to place one order

D = number of units used per year

h = holding cost per unit per year

Under the same conditions as above with a finite replenishment rate, the economic manufacturing quantity is given by

$$EMQ = \sqrt{\frac{2AD}{h(1-D/R)}}, \text{ where}$$

R = the replenishment rate

FACILITY PLANNING

Equipment Requirements

$$M_j = \sum_{i=1}^n \frac{P_{ij} T_{ij}}{C_{ij}} \text{ where}$$

M_j = number of machines of type j required per production period

P_{ij} = desired production rate for product i on machine j , measured in pieces per production period

T_{ij} = production time for product i on machine j , measured in hours per piece

C_{ij} = number of hours in the production period available for the production of product i on machine j

n = number of products

People Requirements

$$A_j = \sum_{i=1}^n \frac{P_{ij}T_{ij}}{C_{ij}}, \text{ where}$$

A_j = number of crews required for assembly operation j

P_{ij} = desired production rate for product i and assembly operation j (pieces per day)

T_{ij} = standard time to perform operation j on product i (minutes per piece)

C_{ij} = number of minutes available per day for assembly operation j on product i

n = number of products

Standard Time Determination

$$ST = NT \times AF$$

where

NT = normal time

AF = allowance factor

Case 1: Allowances are based on the *job time*.

$$AF_{\text{job}} = 1 + A_{\text{job}}$$

A_{job} = allowance fraction (percentage/100) based on *job time*.

Case 2: Allowances are based on *workday*.

$$AF_{\text{time}} = 1/(1 - A_{\text{day}})$$

A_{day} = allowance fraction (percentage/100) based on *workday*.

- ◆ Predetermined time systems are useful in cases where either (1) the task does not yet exist or (2) changes to a task are being designed and normal times have not yet been established for all elements of the new task or changed task. In such cases no opportunity exists to measure the element time. Unfortunately, there is no scientific basis for predicting element times without breaking them down into motion-level parts. A task consists of elements. An organization may develop its own database of normal element durations, and normal times for new or changed tasks may be predicted if the tasks consist entirely of elements whose normal times are already in the database. But new elements can be decomposed into motions, for which scientifically predetermined times exist in databases called MTM-1, MTM-2, and MTM-3. These databases and software to manipulate them are commercially available. To use one of them effectively requires about 50 hours of training.

◆ Kennedy, W.J., and Daniel P. Rogers, *Review for the Professional Engineers' Examination in Industrial Engineering*, 2012.

Plant Location

The following is one formulation of a discrete plant location problem.

Minimize

$$z = \sum_{i=1}^m \sum_{j=1}^n c_{ij}y_{ij} + \sum_{j=1}^n f_j x_j$$

subject to

$$\sum_{i=1}^m y_{ij} \leq mx_j, \quad j = 1, \dots, n$$

$$\sum_{j=1}^n y_{ij} = 1, \quad i = 1, \dots, m$$

$$y_{ij} \geq 0, \text{ for all } i, j$$

$$x_j = (0, 1), \text{ for all } j, \text{ where}$$

m = number of customers

n = number of possible plant sites

y_{ij} = fraction or proportion of the demand of customer i which is satisfied by a plant located at site j ; $i = 1, \dots, m$; $j = 1, \dots, n$

$x_j = 1$, if a plant is located at site j

$x_j = 0$, otherwise

c_{ij} = cost of supplying the entire demand of customer i from a plant located at site j

f_j = fixed cost resulting from locating a plant at site j

Material Handling

Distances between two points (x_1, y_1) and (x_2, y_2) under different metrics:

Euclidean:

$$D = \sqrt{(x_1 - x_2)^2 + (y_1 - y_2)^2}$$

Rectilinear (or Manhattan):

$$D = |x_1 - x_2| + |y_1 - y_2|$$

Chebyshev (simultaneous x and y movement):

$$D = \max(|x_1 - x_2|, |y_1 - y_2|)$$

Line Balancing

$$N_{\min} = \left(OR \times \sum_i t_i / OT \right)$$

= theoretical minimum number of stations

Idle Time/Station = $CT - ST$

Idle Time/Cycle = $\Sigma (CT - ST)$

Percent Idle Time = $\frac{\text{Idle Time/Cycle}}{N_{\text{actual}} \times CT} \times 100$, where

CT = cycle time (time between units)

OT = operating time/period

OR = output rate/period

ST = station time (time to complete task at each station)

t_i = individual task times

N = number of stations

Job Sequencing

Two Work Centers—Johnson's Rule

1. Select the job with the shortest time, from the list of jobs, and its time at each work center.
2. If the shortest job time is the time at the first work center, schedule it first, otherwise schedule it last. Break ties arbitrarily.
3. Eliminate that job from consideration.
4. Repeat 1, 2, and 3 until all jobs have been scheduled.

CRITICAL PATH METHOD (CPM)

d_{ij} = duration of activity (i, j)

CP = critical path (longest path)

T = duration of project

$$T = \sum_{(i,j) \in CP} d_{ij}$$

PERT

(a_{ij}, b_{ij}, c_{ij}) = (optimistic, most likely, pessimistic) durations for activity (i, j)

μ_{ij} = mean duration of activity (i, j)

σ_{ij} = standard deviation of the duration of activity (i, j)

μ = project mean duration

σ = standard deviation of project duration

$$\mu_{ij} = \frac{a_{ij} + 4b_{ij} + c_{ij}}{6}$$

$$\sigma_{ij} = \frac{c_{ij} - a_{ij}}{6}$$

$$\mu = \sum_{(i,j) \in CP} \mu_{ij}$$

$$\sigma^2 = \sum_{(i,j) \in CP} \sigma_{ij}^2$$

TAYLOR TOOL LIFE FORMULA

$$VT^n = C, \text{ where}$$

V = speed in surface feet per minute

T = tool life in minutes

C, n = constants that depend on the material and on the tool

WORK SAMPLING FORMULAS

$$D = Z_{\alpha/2} \sqrt{\frac{p(1-p)}{n}} \text{ and } R = Z_{\alpha/2} \sqrt{\frac{1-p}{pn}}, \text{ where}$$

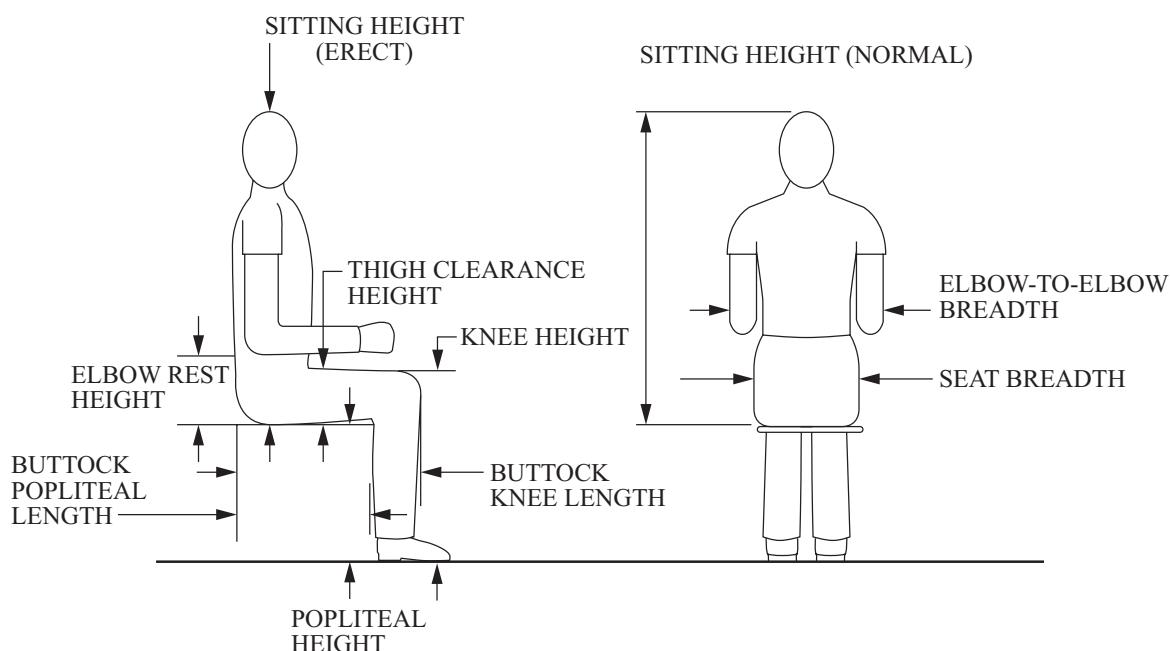
p = proportion of observed time in an activity

D = absolute error

R = relative error ($R = D/p$)

n = sample size

ANTHROPOMETRIC MEASUREMENTS

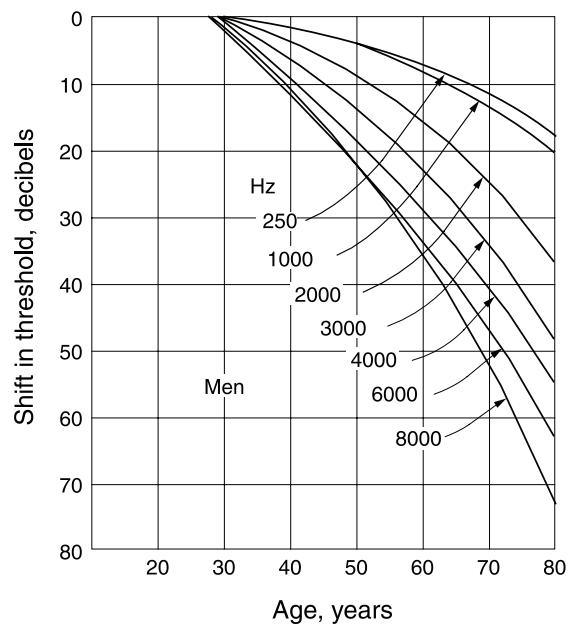
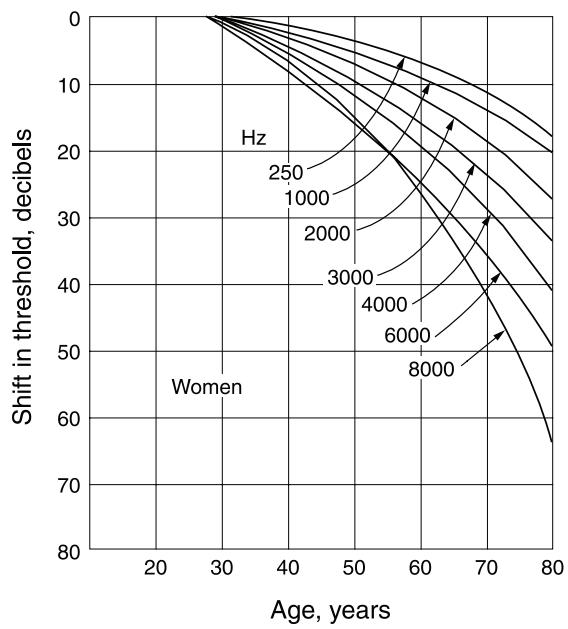


After Sanders and McCormick, *Human Factors In Design*, McGraw-Hill, 1987.

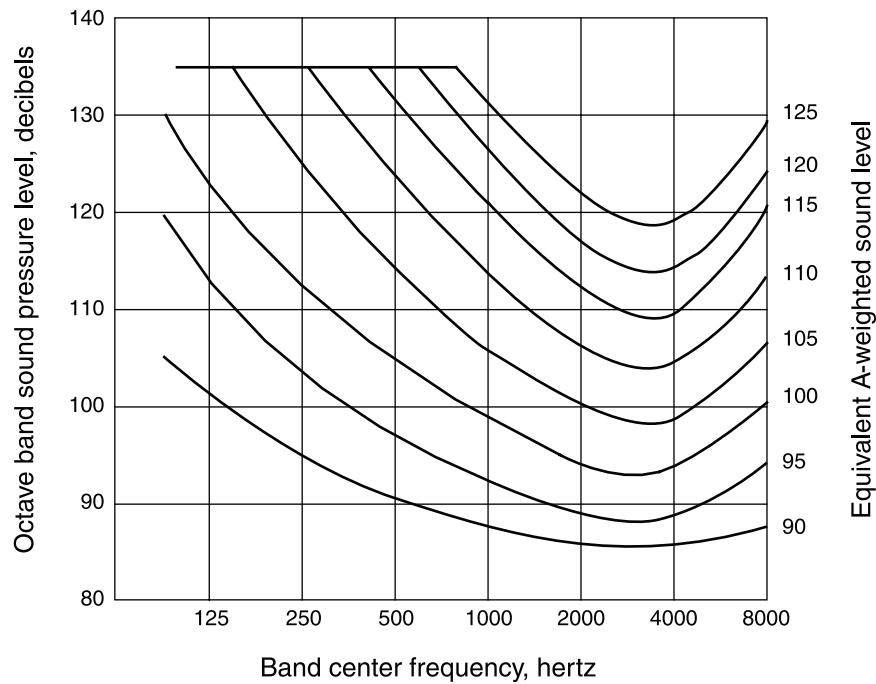
U.S. Civilian Body Dimensions, Female/Male, for Ages 20 to 60 Years (Centimeters)				
(See Anthropometric Measurements Figure)	Percentiles			
	5th	50th	95th	Std. Dev.
HEIGHTS				
Stature (height)	149.5 / 161.8	160.5 / 173.6	171.3 / 184.4	6.6 / 6.9
Eye height	138.3 / 151.1	148.9 / 162.4	159.3 / 172.7	6.4 / 6.6
Shoulder (acromion) height	121.1 / 132.3	131.1 / 142.8	141.9 / 152.4	6.1 / 6.1
Elbow height	93.6 / 100.0	101.2 / 109.9	108.8 / 119.0	4.6 / 5.8
Knuckle height	64.3 / 69.8	70.2 / 75.4	75.9 / 80.4	3.5 / 3.2
Height, sitting (erect)	78.6 / 84.2	85.0 / 90.6	90.7 / 96.7	3.5 / 3.7
Eye height, sitting	67.5 / 72.6	73.3 / 78.6	78.5 / 84.4	3.3 / 3.6
Shoulder height, sitting	49.2 / 52.7	55.7 / 59.4	61.7 / 65.8	3.8 / 4.0
Elbow rest height, sitting	18.1 / 19.0	23.3 / 24.3	28.1 / 29.4	2.9 / 3.0
Knee height, sitting	45.2 / 49.3	49.8 / 54.3	54.5 / 59.3	2.7 / 2.9
Popliteal height, sitting	35.5 / 39.2	39.8 / 44.2	44.3 / 48.8	2.6 / 2.8
Thigh clearance height	10.6 / 11.4	13.7 / 14.4	17.5 / 17.7	1.8 / 1.7
DEPTHES				
Chest depth	21.4 / 21.4	24.2 / 24.2	29.7 / 27.6	2.5 / 1.9
Elbow-fingertip distance	38.5 / 44.1	42.1 / 47.9	46.0 / 51.4	2.2 / 2.2
Buttock-knee length, sitting	51.8 / 54.0	56.9 / 59.4	62.5 / 64.2	3.1 / 3.0
Buttock-popliteal length, sitting	43.0 / 44.2	48.1 / 49.5	53.5 / 54.8	3.1 / 3.0
Forward reach, functional	64.0 / 76.3	71.0 / 82.5	79.0 / 88.3	4.5 / 5.0
BREADTHS				
Elbow-to-elbow breadth	31.5 / 35.0	38.4 / 41.7	49.1 / 50.6	5.4 / 4.6
Seat (hip) breadth, sitting	31.2 / 30.8	36.4 / 35.4	43.7 / 40.6	3.7 / 2.8
HEAD DIMENSIONS				
Head breadth	13.6 / 14.4	14.54 / 15.42	15.5 / 16.4	0.57 / 0.59
Head circumference	52.3 / 53.8	54.9 / 56.8	57.7 / 59.3	1.63 / 1.68
Interpupillary distance	5.1 / 5.5	5.83 / 6.20	6.5 / 6.8	0.4 / 0.39
HAND DIMENSIONS				
Hand length	16.4 / 17.6	17.95 / 19.05	19.8 / 20.6	1.04 / 0.93
Breadth, metacarpal	7.0 / 8.2	7.66 / 8.88	8.4 / 9.8	0.41 / 0.47
Circumference, metacarpal	16.9 / 19.9	18.36 / 21.55	19.9 / 23.5	0.89 / 1.09
Thickness, metacarpal III	2.5 / 2.4	2.77 / 2.76	3.1 / 3.1	0.18 / 0.21
Digit 1				
Breadth, interphalangeal	1.7 / 2.1	1.98 / 2.29	2.1 / 2.5	0.12 / 0.13
Crotch-tip length	4.7 / 5.1	5.36 / 5.88	6.1 / 6.6	0.44 / 0.45
Digit 2				
Breadth, distal joint	1.4 / 1.7	1.55 / 1.85	1.7 / 2.0	0.10 / 0.12
Crotch-tip length	6.1 / 6.8	6.88 / 7.52	7.8 / 8.2	0.52 / 0.46
Digit 3				
Breadth, distal joint	1.4 / 1.7	1.53 / 1.85	1.7 / 2.0	0.09 / 0.12
Crotch-tip length	7.0 / 7.8	7.77 / 8.53	8.7 / 9.5	0.51 / 0.51
Digit 4				
Breadth, distal joint	1.3 / 1.6	1.42 / 1.70	1.6 / 1.9	0.09 / 0.11
Crotch-tip length	6.5 / 7.4	7.29 / 7.99	8.2 / 8.9	0.53 / 0.47
Digit 5				
Breadth, distal joint	1.2 / 1.4	1.32 / 1.57	1.5 / 1.8	0.09 / 0.12
Crotch-tip length	4.8 / 5.4	5.44 / 6.08	6.2 / 6.99	0.44 / 0.47
FOOT DIMENSIONS				
Foot length	22.3 / 24.8	24.1 / 26.9	26.2 / 29.0	1.19 / 1.28
Foot breadth	8.1 / 9.0	8.84 / 9.79	9.7 / 10.7	0.50 / 0.53
Lateral malleolus height	5.8 / 6.2	6.78 / 7.03	7.8 / 8.0	0.59 / 0.54
Weight (kg)	46.2 / 56.2	61.1 / 74.0	89.9 / 97.1	13.8 / 12.6

ERGONOMICS—HEARING

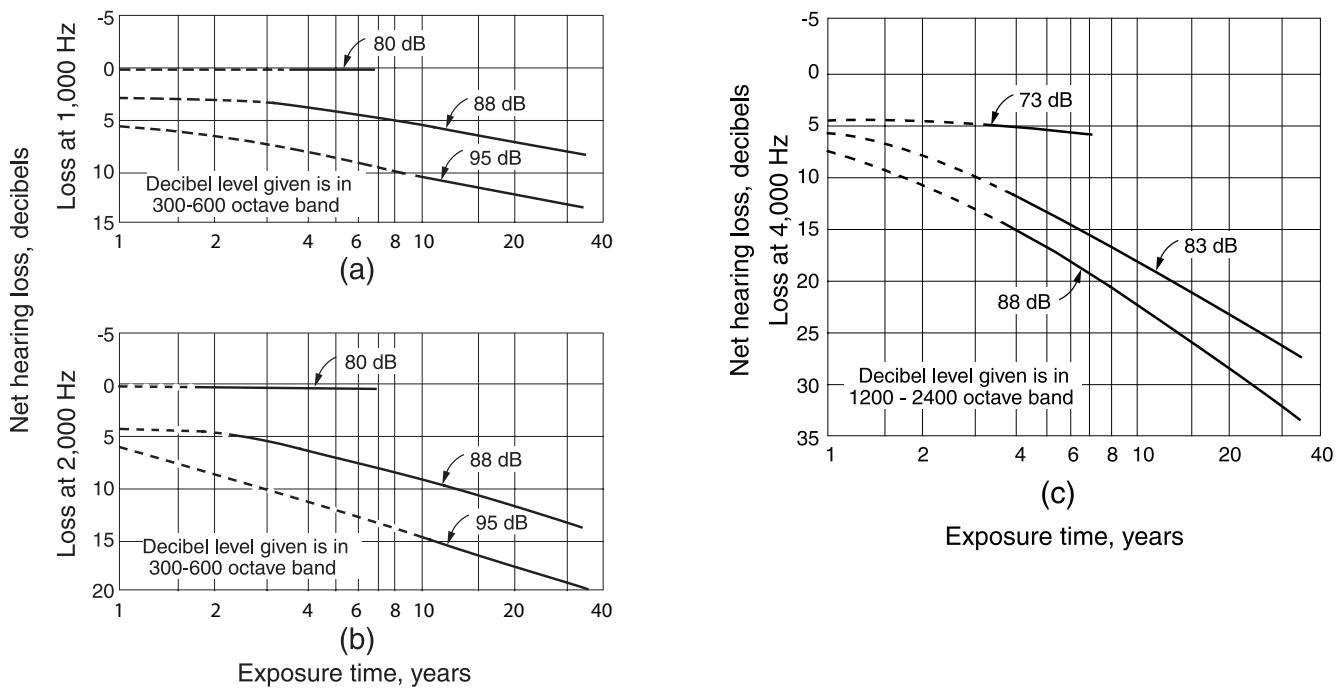
The average shifts with age of the threshold of hearing for pure tones of persons with "normal" hearing, using a 25-year-old group as a reference group.



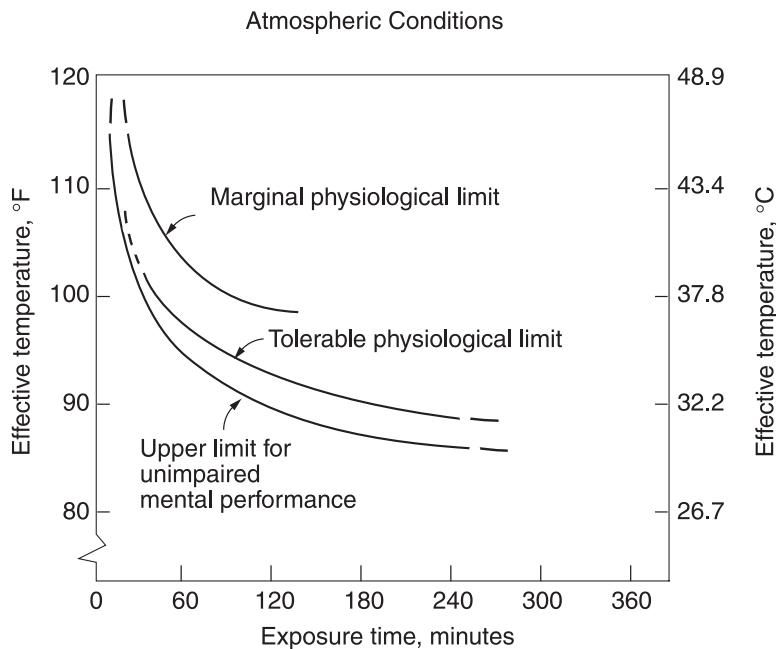
Equivalent sound-level contours used in determining the A-weighted sound level on the basis of an octave-band analysis. The curve at the point of the highest penetration of the noise spectrum reflects the A-weighted sound level.



Estimated average trend curves for net hearing loss at 1,000, 2,000, and 4,000 Hz after continuous exposure to steady noise. Data are corrected for age, but not for temporary threshold shift. Dotted portions of curves represent extrapolation from available data.



Tentative upper limit of effective temperature (ET) for unimpaired mental performance as related to exposure time; data are based on an analysis of 15 studies. Comparative curves of tolerable and marginal physiological limits are also given.



Effective temperature (ET) is the dry bulb temperature at 50% relative humidity, which results in the same physiological effect as the present conditions.

MECHANICAL ENGINEERING

MECHANICAL DESIGN AND ANALYSIS

Springs

Mechanical Springs

Helical Linear Springs: The shear stress in a helical linear spring is

$$\tau = K_s \frac{8FD}{\pi d^3}, \text{ where}$$

d = wire diameter

F = applied force

D = mean spring diameter

$$K_s = (2C + 1)/(2C)$$

$$C = D/d$$

The deflection and force are related by $F = kx$ where the spring rate (spring constant) k is given by

$$k = \frac{d^4 G}{8D^3 N}$$

where G is the shear modulus of elasticity and N is the number of active coils.

Spring Material: The minimum tensile strength of common spring steels may be determined from

$$S_{ut} = A/d^m$$

where S_{ut} is the tensile strength in MPa, d is the wire diameter in millimeters, and A and m are listed in the following table:

Material	ASTM	m	A
Music wire	A228	0.163	2060
Oil-tempered wire	A229	0.193	1610
Hard-drawn wire	A227	0.201	1510
Chrome vanadium	A232	0.155	1790
Chrome silicon	A401	0.091	1960

Maximum allowable torsional stress for static applications may be approximated as

$$S_{sy} = \tau = 0.45S_{ut} \text{ cold-drawn carbon steel} \\ (\text{A227, A228, A229})$$

$$S_{sy} = \tau = 0.50S_{ut} \text{ hardened and tempered carbon and low-alloy steels} (\text{A232, A401})$$

Compression Spring Dimensions

Type of Spring Ends		
Term	Plain	Plain and Ground
End coils, N_e	0	1
Total coils, N_t	N	$N + 1$
Free length, L_0	$pN + d$	$p(N + 1)$
Solid length, L_s	$d(N_t + 1)$	dN_t
Pitch, p	$(L_0 - d)/N$	$L_0/(N + 1)$

Term	Squared or Closed	Squared and Ground
End coils, N_e	2	2
Total coils, N_t	$N + 2$	$N + 2$
Free length, L_0	$pN + 3d$	$pN + 2d$
Solid length, L_s	$d(N_t + 1)$	dN_t
Pitch, p	$(L_0 - 3d)/N$	$(L_0 - 2d)/N$

Helical Torsion Springs: The bending stress is given as

$$\sigma = K_i [32Fr/(\pi d^3)]$$

where F is the applied load and r is the radius from the center of the coil to the load.

K_i = correction factor

$$= (4C^2 - C - 1) / [4C(C - 1)]$$

$$C = D/d$$

The deflection θ and moment Fr are related by

$$Fr = k\theta$$

where the spring rate k is given by

$$k = \frac{d^4 E}{64DN}$$

where k has units of N•m/rad and θ is in radians.

Spring Material: The strength of the spring wire may be found as shown in the section on linear springs. The allowable stress σ is then given by

$$S_y = \sigma = 0.78S_{ut} \text{ cold-drawn carbon steel} \\ (\text{A227, A228, A229})$$

$$S_y = \sigma = 0.87S_{ut} \text{ hardened and tempered carbon and low-alloy steel} (\text{A232, A401})$$

Bearings

Ball/Roller Bearing Selection

The minimum required *basic load rating* (load for which 90% of the bearings from a given population will survive 1 million revolutions) is given by

$$C = PL^{1/a}, \text{ where}$$

C = minimum required basic load rating

P = design radial load

L = design life (in millions of revolutions)

a = 3 for ball bearings, 10/3 for roller bearings

When a ball bearing is subjected to both radial and axial loads, an equivalent radial load must be used in the equation above.

The equivalent radial load is

$$P_{eq} = XVF_r + YF_a, \text{ where}$$

P_{eq} = equivalent radial load

F_r = applied constant radial load

F_a = applied constant axial (thrust) load

For radial contact, deep-groove ball bearings:

V = 1 if inner ring rotating, 1.2 if outer ring rotating,

If $F_a/(VF_r) > e$,

$$X = 0.56, \text{ and } Y = 0.840 \left(\frac{F_a}{C_0} \right)^{-0.247}$$

$$\text{where } e = 0.513 \left(\frac{F_a}{C_0} \right)^{0.236}$$

C_0 = basic static load rating from bearing catalog

If $F_a/(VF_r) \leq e$, $X = 1$ and $Y = 0$.

Power Screws

Square Thread Power Screws: The torque required to raise, T_R , or to lower, T_L , a load is given by

$$T_R = \frac{Fd_m}{2} \left(\frac{l + \pi \mu d_m}{\pi d_m - \mu l} \right) + \frac{F \mu_c d_c}{2}$$

$$T_L = \frac{Fd_m}{2} \left(\frac{\pi \mu d_m - l}{\pi d_m + \mu l} \right) + \frac{F \mu_c d_c}{2}, \text{ where}$$

d_c = mean collar diameter

d_m = mean thread diameter

l = lead

F = load

μ = coefficient of friction for thread

μ_c = coefficient of friction for collar

The efficiency of a power screw may be expressed as

$$\eta = Fl/(2\pi T)$$

Power Transmission

Shafts and Axles

Static Loading: The maximum shear stress and the von Mises stress may be calculated in terms of the loads from

$$\tau_{max} = \frac{2}{\pi d^3} [(8M + Fd)^2 + (8T)^2]^{1/2},$$

$$\sigma' = \frac{4}{\pi d^3} [(8M + Fd)^2 + 48T^2]^{1/2}, \text{ where}$$

M = the bending moment

F = the axial load

T = the torque

d = the diameter

Fatigue Loading: Using the maximum-shear-stress theory combined with the Soderberg line for fatigue, the diameter and safety factor are related by

$$\frac{\pi d^3}{32} = n \left[\left(\frac{M_m}{S_y} + \frac{K_f M_a}{S_e} \right)^2 + \left(\frac{T_m}{S_y} + \frac{K_{fs} T_a}{S_e} \right)^2 \right]^{1/2}$$

where

d = diameter

n = safety factor

M_a = alternating moment

M_m = mean moment

T_a = alternating torque

T_m = mean torque

S_e = fatigue limit

S_y = yield strength

K_f = fatigue strength reduction factor

K_{fs} = fatigue strength reduction factor for shear

Gearing

Involute Gear Tooth Nomenclature

Circular pitch $p_c = \pi d/N$

Base pitch $p_b = p_c \cos \phi$

Module $m = d/N$

Center distance $C = (d_1 + d_2)/2$

where

N = number of teeth on pinion or gear

d = pitch circle diameter

ϕ = pressure angle

Gear Trains: Velocity ratio, m_v , is the ratio of the output velocity to the input velocity. Thus, $m_v = \omega_{out}/\omega_{in}$. For a two-gear train, $m_v = -N_{in}/N_{out}$ where N_{in} is the number of teeth on the input gear and N_{out} is the number of teeth on the output gear. The negative sign indicates that the output gear rotates in the opposite sense with respect to the input gear. In a *compound gear train*, at least one shaft carries more than one gear (rotating at the same speed). The velocity ratio for a compound train is:

$$m_v = \pm \frac{\text{product of number of teeth on driver gears}}{\text{product of number of teeth on driven gears}}$$

A simple planetary gearset has a sun gear, an arm that rotates about the sun gear axis, one or more gears (planets) that rotate about a point on the arm, and a ring (internal) gear that is concentric with the sun gear. The planet gear(s) mesh with the sun gear on one side and with the ring gear on the other. A planetary gearset has two independent inputs and one output (or two outputs and one input, as in a differential gearset).

Often one of the inputs is zero, which is achieved by grounding either the sun or the ring gear. The velocities in a planetary set are related by

$$\frac{\omega_L - \omega_{\text{arm}}}{\omega_f - \omega_{\text{arm}}} = \pm m_v, \text{ where}$$

ω_f = speed of the first gear in the train

ω_L = speed of the last gear in the train

ω_{arm} = speed of the arm

Neither the first nor the last gear can be one that has planetary motion. In determining m_v , it is helpful to invert the mechanism by grounding the arm and releasing any gears that are grounded.

Dynamics of Mechanisms

Gearing

Loading on Straight Spur Gears: The load, W , on straight spur gears is transmitted along a plane that, in edge view, is called the *line of action*. This line makes an angle with a tangent line to the pitch circle that is called the *pressure angle* ϕ . Thus, the contact force has two components: one in the tangential direction, W_t , and one in the radial direction, W_r . These components are related to the pressure angle by

$$W_r = W_t \tan(\phi).$$

Only the tangential component W_t transmits torque from one gear to another. Neglecting friction, the transmitted force may be found if either the transmitted torque or power is known:

$$W_t = \frac{2T}{d} = \frac{2T}{mN},$$

$$W_t = \frac{2H}{d\omega} = \frac{2H}{mN\omega}, \text{ where}$$

W_t = transmitted force (newtons)

T = torque on the gear (newton-mm)

d = pitch diameter of the gear (mm)

N = number of teeth on the gear

m = gear module (mm) (same for both gears in mesh)

H = power (kW)

ω = speed of gear (rad/s)

Stresses in Spur Gears: Spur gears can fail in either bending (as a cantilever beam, near the root) or by surface fatigue due to contact stresses near the pitch circle. AGMA Standard 2001 gives equations for bending stress and surface stress. They are:

$$\sigma_b = \frac{W_t}{FmJ} \frac{K_a K_m}{K_v} K_S K_B K_I, \text{ bending and}$$

$$\sigma_c = C_p \sqrt{\frac{W_t}{FId} \frac{C_a C_m}{C_v} C_s C_f}, \text{ surface stress, where}$$

σ_b = bending stress

σ_c = surface stress

W_t = transmitted load

F = face width

m = module

J = bending strength geometry factor

K_a = application factor

K_B = rim thickness factor

K_I = idler factor

K_m = load distribution factor

K_s = size factor

K_v = dynamic factor

C_p = elastic coefficient

I = surface geometry factor

d = pitch diameter of gear being analyzed

C_f = surface finish factor

C_a , C_m , C_s , and C_v are the same as K_a , K_m , K_s , and K_v , respectively.

Joining Methods

Threaded Fasteners: The load carried by a bolt in a threaded connection is given by

$$F_b = CP + F_i \quad F_m < 0$$

while the load carried by the members is

$$F_m = (1 - C) P - F_i \quad F_m < 0, \text{ where}$$

C = joint coefficient

$$= k_b/(k_b + k_m)$$

F_b = total bolt load

F_i = bolt preload

F_m = total material load

P = externally applied load

k_b = effective stiffness of the bolt or fastener in the grip

k_m = effective stiffness of the members in the grip

Bolt stiffness may be calculated from

$$k_b = \frac{A_d A E}{A_d l_t + A_l l_d}, \text{ where}$$

A_d = major-diameter area

A_t = tensile-stress area

E = modulus of elasticity

l_d = length of unthreaded shank

l_t = length of threaded shank contained within the grip

If all members within the grip are of the same material, member stiffness may be obtained from

$$k_m = d E A e^{b(d/l)}, \text{ where}$$

d = bolt diameter

E = modulus of elasticity of members

l = grip length

Coefficients A and b are given in the table below for various joint member materials.

Material	A	b
Steel	0.78715	0.62873
Aluminum	0.79670	0.63816
Copper	0.79568	0.63553
Gray cast iron	0.77871	0.61616

The approximate tightening torque required for a given preload F_i and for a steel bolt in a steel member is given by $T = 0.2 F_i d$.

Threaded Fasteners – Design Factors: The bolt load factor is

$$n_b = (S_p A_t - F_i) / CP, \text{ where}$$

S_p = proof strength

The factor of safety guarding against joint separation is

$$n_s = F_i / [P(1 - C)]$$

Threaded Fasteners – Fatigue Loading: If the externally applied load varies between zero and P , the alternating stress is

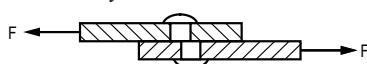
$$\sigma_a = CP/(2A_t)$$

and the mean stress is

$$\sigma_m = \sigma_a + F_i/A_t$$

Bolted and Riveted Joints Loaded in Shear:

Failure by Pure Shear

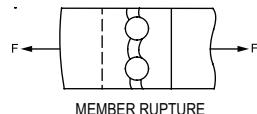


$$\tau = F/A, \text{ where}$$

F = shear load

A = cross-sectional area of bolt or rivet

Failure by Rupture



$$\sigma = F/A, \text{ where}$$

F = load

A = net cross-sectional area of thinnest member

Failure by Crushing of Rivet or Member

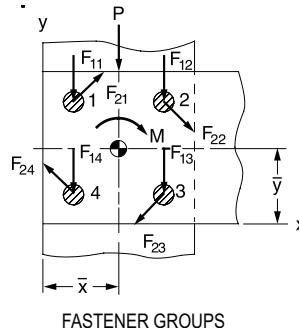


$$\sigma = F/A, \text{ where}$$

F = load

A = projected area of a single rivet

Fastener Groups in Shear



The location of the centroid of a fastener group with respect to any convenient coordinate frame is:

$$\bar{x} = \frac{\sum_{i=1}^n A_i x_i}{\sum_{i=1}^n A_i}, \quad \bar{y} = \frac{\sum_{i=1}^n A_i y_i}{\sum_{i=1}^n A_i}, \text{ where}$$

n = total number of fasteners

i = the index number of a particular fastener

A_i = cross-sectional area of the i th fastener

x_i = x -coordinate of the center of the i th fastener

y_i = y -coordinate of the center of the i th fastener

The total shear force on a fastener is the **vector** sum of the force due to direct shear P and the force due to the moment M acting on the group at its centroid.

The magnitude of the direct shear force due to P is

$$|F_{1i}| = \frac{P}{n}.$$

This force acts in the same direction as P .

The magnitude of the shear force due to M is

$$|F_{2i}| = \frac{M r_i}{\sum_{i=1}^n r_i^2}.$$

This force acts perpendicular to a line drawn from the group centroid to the center of a particular fastener. Its sense is such that its moment is in the same direction (CW or CCW) as M .

Press/Shrink Fits

The interface pressure induced by a press/shrink fit is

$$p = \frac{0.5\delta}{\frac{r}{E_o} \left(\frac{r_o^2 + r^2}{r_o^2 - r^2} + v_o \right) + \frac{r}{E_i} \left(\frac{r^2 + r_i^2}{r^2 - r_i^2} - v_i \right)}$$

where the subscripts i and o stand for the inner and outer member, respectively, and

p = inside pressure on the outer member and outside pressure on the inner member

δ = the diametral interference

r = nominal interference radius

r_i = inside radius of inner member

r_o = outside radius of outer member

E = Young's modulus of respective member

v = Poisson's ratio of respective member

The *maximum torque* that can be transmitted by a press fit joint is approximately

$$T = 2\pi r^2 \mu p l,$$

where r and p are defined above,

T = torque capacity of the joint

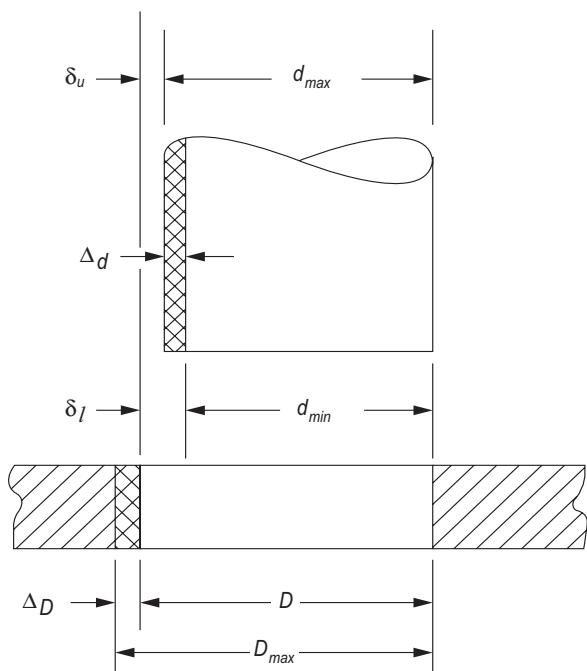
μ = coefficient of friction at the interface

l = length of hub engagement

MANUFACTURABILITY

Limits and Fits

The designer is free to adopt any geometry of fit for shafts and holes that will ensure intended function. Over time, sufficient experience with common situations has resulted in the development of a standard. The metric version of the standard is newer and will be presented. The standard specifies that uppercase letters always refer to the hole, while lowercase letters always refer to the shaft.



Definitions

Basic Size or *nominal size*, D or d , is the size to which the limits or deviations are applied. It is the same for both components.

Deviation is the algebraic difference between the actual size and the corresponding basic size.

Upper Deviation, δ_u , is the algebraic difference between the maximum limit and the corresponding basic size.

Lower Deviation, δ_l , is the algebraic difference between the minimum limit and the corresponding basic size.

Fundamental Deviation, δ_F , is the upper or lower deviation, depending on which is closer to the basic size.

Tolerance, Δ_D or Δ_d , is the difference between the maximum and minimum size limits of a part.

International tolerance (IT) grade numbers designate groups of tolerances such that the tolerance for a particular IT number will have the same relative accuracy for a basic size.

Hole basis represents a system of fits corresponding to a basic hole size. The fundamental deviation is H.

Some Preferred Fits

Clearance	
<i>Free running fit</i> : not used where accuracy is essential but good for large temperature variations, high running speeds, or heavy journal loads.	H9/d9
<i>Sliding fit</i> : where parts are not intended to run freely but must move and turn freely and locate accurately.	H7/g6
<i>Locational clearance fit</i> : provides snug fit for location of stationary parts, but can be freely assembled and disassembled.	H7/h6
<i>Loose running fit</i> : for wide commercial tolerances or allowances on external members	H11/c11
<i>Close running fit</i> : for running on accurate machines and for accurate location at moderate speeds and journal pressures	H8/f7
Transition	
<i>Locational transition fit</i> : for accurate location, a compromise between clearance and interference	H7/k6
<i>Locational transition fit</i> : for more accurate location where greater interface is permissible	H7/n6
Interference	
<i>Location interference fit</i> : for parts requiring rigidity and alignment with prime accuracy of location but without special bore pressure requirements.	H7/p6
<i>Medium drive fit</i> : for ordinary steel parts or shrink fits on light sections. The tightest fit usable on cast iron.	H7/s6
<i>Force fit</i> : suitable for parts which can be highly stressed or for shrink fits where the heavy pressing forces required are impractical.	H7/u6

For the hole

$$D_{\max} = D + \Delta_D$$

$$D_{\min} = D$$

For a shaft with clearance fits *d, g, h, c, or f*

$$d_{\max} = d + \delta_F$$

$$d_{\min} = d_{\max} - \Delta_d$$

For a shaft with transition or interference fits *k, p, s, u, or n*

$$d_{\min} = d + \delta_F$$

$$d_{\max} = d_{\min} + \Delta_d$$

where

D = basic size of hole

d = basic size of shaft

δ_u = upper deviation

δ_l = lower deviation

δ_F = fundamental deviation

Δ_D = tolerance grade for hole

Δ_d = tolerance grade for shaft

International Tolerance (IT) Grades

Lower limit < Basic Size ≤ Upper Limit
All values in mm

Basic Size	Tolerance Grade, (Δ_D or Δ_d)		
	IT6	IT7	IT9
0–3	0.006	0.010	0.025
3–6	0.008	0.012	0.030
6–10	0.009	0.015	0.036
10–18	0.011	0.018	0.043
18–30	0.013	0.021	0.052
30–50	0.016	0.025	0.062

Source: Preferred Metric Limits and Fits, ANSI B4.2-1978

Deviations for shafts

Lower limit < Basic Size ≤ Upper Limit
All values in mm

Basic Size	Upper Deviation Letter, (δ_u)					Lower Deviation Letter, (δ_l)				
	c	d	f	g	h	k	n	p	s	u
0–3	-0.060	-0.020	-0.006	-0.002	0	0	+0.004	+0.006	+0.014	+0.018
3–6	-0.070	-0.030	-0.010	-0.004	0	+0.001	+0.008	+0.012	+0.019	+0.023
6–10	-0.080	-0.040	-0.013	-0.005	0	+0.001	+0.010	+0.015	+0.023	+0.028
10–14	-0.095	-0.050	-0.016	-0.006	0	+0.001	+0.012	+0.018	+0.028	+0.033
14–18	-0.095	-0.050	-0.016	-0.006	0	+0.001	+0.012	+0.018	+0.028	+0.033
18–24	-0.110	-0.065	-0.020	-0.007	0	+0.002	+0.015	+0.022	+0.035	+0.041
24–30	-0.110	-0.065	-0.020	-0.007	0	+0.002	+0.015	+0.022	+0.035	+0.048
30–40	-0.120	-0.080	-0.025	-0.009	0	+0.002	+0.017	+0.026	+0.043	+0.060
40–50	-0.130	-0.080	-0.025	-0.009	0	+0.002	+0.017	+0.026	+0.043	+0.070

Source: ASME B4.2:2009

As an example, 34H7/s6 denotes a basic size of $D = d = 34$ mm , an IT class of 7 for the hole, and an IT class of 6 and an "s" fit class for the shaft.

Maximum Material Condition (MMC)

The maximum material condition defines the dimension of a part such that the part weighs the most. The MMC of a shaft is at the maximum size of the shaft while the MMC of a hole is at the minimum size of the hole.

Least Material Condition (LMC)

The least material condition or minimum material condition defines the dimensions of a part such that the part weighs the least. The LMC of a shaft is the minimum size of the shaft while the LMC of a hole is at the maximum size of the hole.

Intermediate- and Long-Length Columns

For both intermediate and long columns, the effective column length depends on the end conditions. The AISC recommended design values for the effective lengths of columns are, for: rounded-rounded or pinned-pinned ends, $l_{eff} = l$; fixed-free, $l_{eff} = 2.1l$; fixed-pinned, $l_{eff} = 0.80l$; fixed-fixed, $l_{eff} = 0.65l$. The effective column length should be used when calculating the slenderness ratio.

The slenderness ratio of a column is $S_r = l/r$, where l is the length of the column and r is the radius of gyration. The radius of gyration of a column cross-section is, $r = \sqrt{I/A}$ where I is the area moment of inertia and A is the cross-sectional area of the column. A column is considered to be intermediate if its slenderness ratio is less than or equal to $(S_r)_D$, where

$$(S_r)_D = \pi \sqrt{\frac{2E}{S_y}}, \text{ and}$$

E = Young's modulus of respective member

S_y = yield strength of the column material

For intermediate columns, the critical load is

$$P_{cr} = A \left[S_y - \frac{1}{E} \left(\frac{S_y S_r}{2\pi} \right)^2 \right], \text{ where}$$

P_{cr} = critical buckling load

A = cross-sectional area of the column

S_y = yield strength of the column material

E = Young's modulus of respective member

S_r = slenderness ratio

For long columns, the critical load is

$$P_{cr} = \frac{\pi^2 EA}{S_r^2}$$

where the variables are as defined above.

STATIC LOADING FAILURE THEORIES

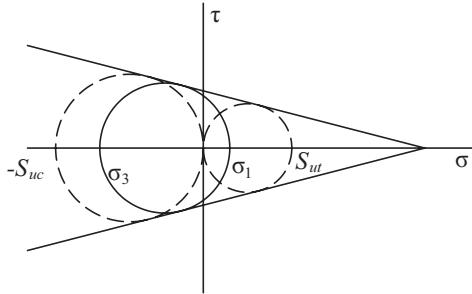
Brittle Materials

Maximum-Normal-Stress Theory

The maximum-normal-stress theory states that failure occurs when one of the three principal stresses equals the strength of the material. If $\sigma_1 \geq \sigma_2 \geq \sigma_3$, then the theory predicts that failure occurs whenever $\sigma_1 \geq S_{ut}$ or $\sigma_3 \leq -S_{uc}$ where S_{ut} and S_{uc} are the tensile and compressive strengths, respectively.

Coulomb-Mohr Theory

The Coulomb-Mohr theory is based upon the results of tensile and compression tests. On the σ, τ coordinate system, one circle is plotted for S_{ut} and one for S_{uc} . As shown in the figure, lines are then drawn tangent to these circles. The Coulomb-Mohr theory then states that fracture will occur for any stress situation that produces a circle that is either tangent to or crosses the envelope defined by the lines tangent to the S_{ut} and S_{uc} circles.



If $\sigma_1 \geq \sigma_2 \geq \sigma_3$ and $\sigma_3 < 0$, then the theory predicts that yielding will occur whenever

$$\frac{\sigma_1}{S_{ut}} - \frac{\sigma_3}{S_{uc}} \geq 1$$

Ductile Materials

Maximum-Shear-Stress Theory

The maximum-shear-stress theory states that yielding begins when the maximum shear stress equals the maximum shear stress in a tension-test specimen of the same material when that specimen begins to yield. If $\sigma_1 \geq \sigma_2 \geq \sigma_3$, then the theory predicts that yielding will occur whenever $\tau_{max} \geq S_y/2$ where S_y is the yield strength.

$$\tau_{max} = \frac{\sigma_1 - \sigma_3}{2}.$$

Distortion-Energy Theory

The distortion-energy theory states that yielding begins whenever the distortion energy in a unit volume equals the distortion energy in the same volume when uniaxially stressed to the yield strength. The theory predicts that yielding will occur whenever

$$\left[\frac{(\sigma_1 - \sigma_2)^2 + (\sigma_2 - \sigma_3)^2 + (\sigma_1 - \sigma_3)^2}{2} \right]^{1/2} \geq S_y$$

The term on the left side of the inequality is known as the effective or Von Mises stress. For a biaxial stress state the effective stress becomes

$$\sigma' = (\sigma_A^2 - \sigma_A \sigma_B + \sigma_B^2)^{1/2}$$

or

$$\sigma' = (\sigma_x^2 - \sigma_x \sigma_y + \sigma_y^2 + 3\tau_{xy}^2)^{1/2}$$

where σ_A and σ_B are the two nonzero principal stresses and σ_x , σ_y , and τ_{xy} are the stresses in orthogonal directions.

VARIABLE LOADING FAILURE THEORIES

Modified Goodman Theory: The modified Goodman criterion states that a fatigue failure will occur whenever

$$\frac{\sigma_a}{S_e} + \frac{\sigma_m}{S_{ut}} \geq 1 \quad \text{or} \quad \frac{\sigma_{max}}{S_y} \geq 1, \quad \sigma_m \geq 0,$$

where

S_e = fatigue strength

S_{ut} = ultimate strength

S_y = yield strength

σ_a = alternating stress

σ_m = mean stress

$\sigma_{max} = \sigma_m + \sigma_a$

Soderberg Theory: The Soderberg theory states that a fatigue failure will occur whenever

$$\frac{\sigma_a}{S_e} + \frac{\sigma_m}{S_y} \geq 1 \quad \sigma_m \geq 0$$

Endurance Limit for Steels: When test data is unavailable, the endurance limit for steels may be estimated as

$$S'_e = \begin{cases} 0.5 S_{ut}, S_{ut} \leq 1,400 \text{ MPa} \\ 700 \text{ MPa}, S_{ut} > 1,400 \text{ MPa} \end{cases}$$

Endurance Limit Modifying Factors: Endurance limit modifying factors are used to account for the differences between the endurance limit as determined from a rotating beam test, S'_e , and that which would result in the real part, S_e .

$$S_e = k_a k_b k_c k_d k_e S'_e$$

where

$$\text{Surface Factor, } k_a = a S_{ut}^b$$

Surface Finish	Factor <i>a</i>		Exponent <i>b</i>
	kpsi	MPa	
Ground	1.34	1.58	-0.085
Machined or CD	2.70	4.51	-0.265
Hot rolled	14.4	57.7	-0.718
As forged	39.9	272.0	-0.995

Size Factor, k_b :

For bending and torsion:

$$d \leq 8 \text{ mm}; \quad k_b = 1$$

$$8 \text{ mm} \leq d \leq 250 \text{ mm}; \quad k_b = 1.189d^{-0.097}$$

$$d > 250 \text{ mm}; \quad 0.6 \leq k_b \leq 0.75$$

For axial loading:

$$k_b = 1$$

Load Factor, k_c :

$$k_c = 0.923$$

axial loading, $S_{ut} \leq 1,520 \text{ MPa}$

$$k_c = 1$$

axial loading, $S_{ut} > 1,520 \text{ MPa}$

$$k_c = 1$$

bending

$$k_c = 0.577$$

torsion

Temperature Factor, k_d :

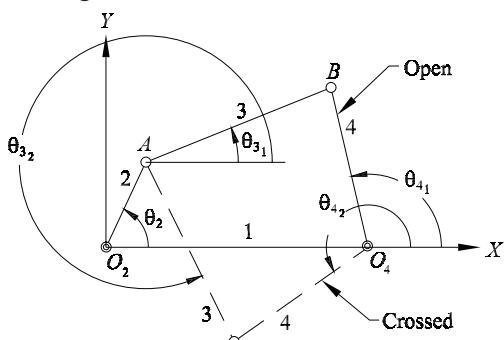
$$\text{for } T \leq 450^\circ\text{C}, k_d = 1$$

Miscellaneous Effects Factor, k_e : Used to account for strength reduction effects such as corrosion, plating, and residual stresses. In the absence of known effects, use $k_e = 1$.

KINEMATICS, DYNAMICS, AND VIBRATIONS

Kinematics of Mechanisms

Four-Bar Linkage



The four-bar linkage shown above consists of a reference (usually grounded) link (1), a crank (input) link (2), a coupler link (3), and an output link (4). Links 2 and 4 rotate about the fixed pivots O_2 and O_4 , respectively. Link 3 is joined to link 2 at the moving pivot A and to link 4 at the moving pivot B . The lengths of links 2, 3, 4, and 1 are a , b , c , and d , respectively.

Taking link 1 (ground) as the reference (X -axis), the angles that links 2, 3, and 4 make with the axis are θ_2 , θ_3 , and θ_4 , respectively. It is possible to assemble a four-bar in two different configurations for a given position of the input link (2). These are known as the "open" and "crossed" positions or circuits.

Position Analysis. Given a , b , c , and d , and θ_2

$$\theta_{4_{1,2}} = 2 \arctan \left(\frac{-B \pm \sqrt{B^2 - 4AC}}{2A} \right)$$

$$\text{where } A = \cos \theta_2 - K_1 - K_2 \cos \theta_2 + K_3$$

$$B = -2 \sin \theta_2$$

$$C = K_1 - (K_2 + 1) \cos \theta_2 + K_3$$

$$K_1 = \frac{d}{a}, K_2 = \frac{d}{c}, K_3 = \frac{a^2 - b^2 + c^2 + d^2}{2ac}$$

In the equation for θ_4 , using the minus sign in front of the radical yields the open solution. Using the plus sign yields the crossed solution.

$$\theta_{3_{1,2}} = 2 \arctan \left(\frac{-E \pm \sqrt{E^2 - 4DF}}{2D} \right)$$

$$\text{where } D = \cos \theta_2 - K_1 + K_4 \cos \theta_2 + K_5$$

$$E = -2 \sin \theta_2$$

$$F = K_1 + (K_4 - 1) \cos \theta_2 + K_5$$

$$K_4 = \frac{d}{b}, K_5 = \frac{c^2 - d^2 - a^2 - b^2}{2ab}$$

In the equation for θ_3 , using the minus sign in front of the radical yields the open solution. Using the plus sign yields the crossed solution.

Velocity Analysis. Given a , b , c , and d , θ_2 , θ_3 , θ_4 , and ω_2

$$\omega_3 = \frac{a\omega_2}{b} \frac{\sin(\theta_4 - \theta_2)}{\sin(\theta_3 - \theta_4)}$$

$$\omega_4 = \frac{a\omega_2}{c} \frac{\sin(\theta_2 - \theta_3)}{\sin(\theta_4 - \theta_3)}$$

$$V_{Ax} = -a\omega_2 \sin \theta_2, \quad V_{Ay} = a\omega_2 \cos \theta_2$$

$$V_{BAx} = -b\omega_3 \sin \theta_3, \quad V_{BAy} = b\omega_3 \cos \theta_3$$

$$V_{Bx} = -c\omega_4 \sin \theta_4, \quad V_{By} = c\omega_4 \cos \theta_4$$

Acceleration Analysis. Given a , b , c , and d , θ_2 , θ_3 , θ_4 , and ω_2 , ω_3 , ω_4 , and α_2

$$\alpha_3 = \frac{CD - AF}{AE - BD}, \quad \alpha_4 = \frac{CE - BF}{AE - BD}, \text{ where}$$

$$A = c\sin \theta_4, B = b\sin \theta_3$$

$$C = a\alpha_2 \sin \theta_2 + a\omega_2^2 \cos \theta_2 + b\omega_3^2 \cos \theta_3 - c\omega_4^2 \cos \theta_4$$

$$D = c\cos \theta_4, E = b\cos \theta_3$$

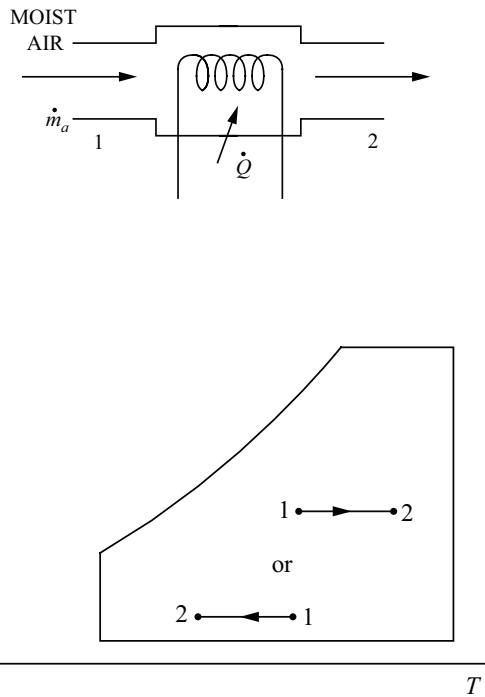
$$F = a\alpha_2 \cos \theta_2 - a\omega_2^2 \sin \theta_2 - b\omega_3^2 \sin \theta_3 + c\omega_4^2 \sin \theta_4$$

HVAC

Nomenclature

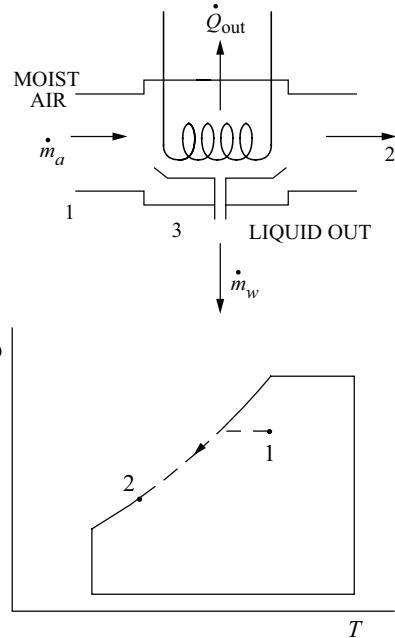
- h = specific enthalpy
- h_f = specific enthalpy of saturated liquid
- \dot{m}_a = mass flow rate of dry air
- \dot{m}_w = mass flow rate of water
- \dot{Q} = rate of heat transfer
- T_{wb} = wet bulb temperature
- ω = specific humidity (absolute humidity, humidity ratio)

HVAC—Pure Heating and Cooling



$$\dot{Q} = \dot{m}_a(h_2 - h_1)$$

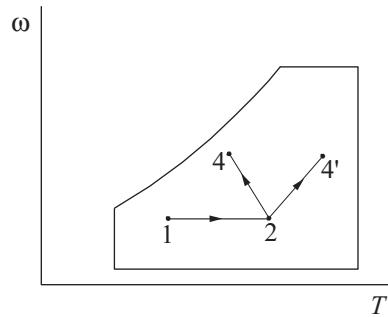
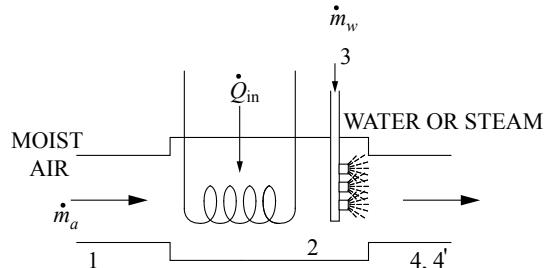
Cooling and Dehumidification



$$\dot{Q}_{out} = \dot{m}_a[(h_l - h_2) - h_{f3}(\omega_l - \omega_2)]$$

$$\dot{m}_w = \dot{m}_a(\omega_l - \omega_2)$$

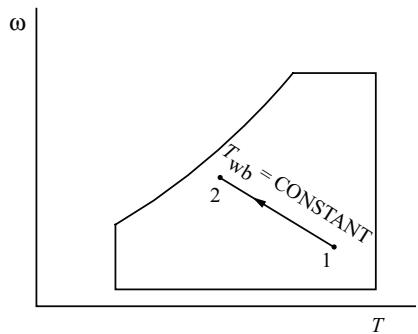
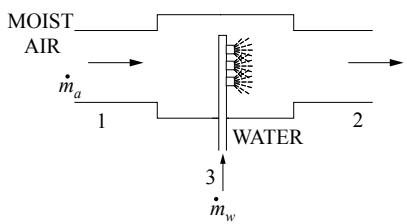
Heating and Humidification



$$\dot{Q}_{in} = \dot{m}_a(h_2 - h_1)$$

$$\dot{m}_w = \dot{m}_a(\omega_4 - \omega_2) \text{ or } \dot{m}_w = \dot{m}_a(\omega_4 - \omega_2)$$

Adiabatic Humidification (evaporative cooling)

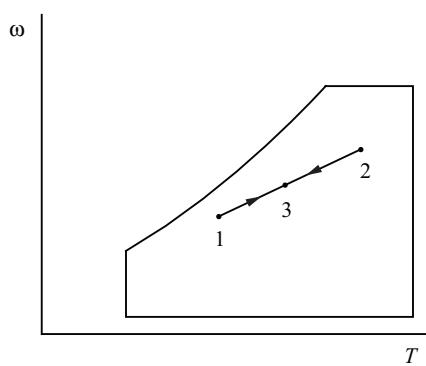
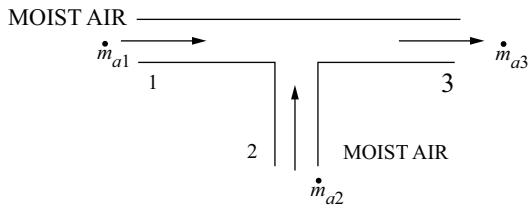


$$h_2 = h_1 + h_3(\omega_2 - \omega_1)$$

$$m_w = \dot{m}_a(\omega_2 - \omega_1)$$

$$h_3 = h_f \text{ at } T_{wb}$$

Adiabatic Mixing



$$\dot{m}_{a3} = \dot{m}_{a1} + \dot{m}_{a2}$$

$$h_3 = \frac{\dot{m}_{a1}h_1 + \dot{m}_{a2}h_2}{\dot{m}_{a3}}$$

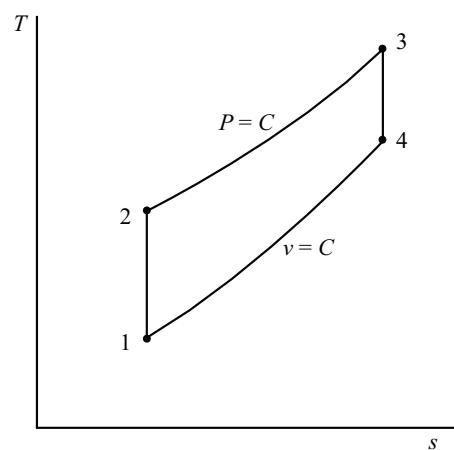
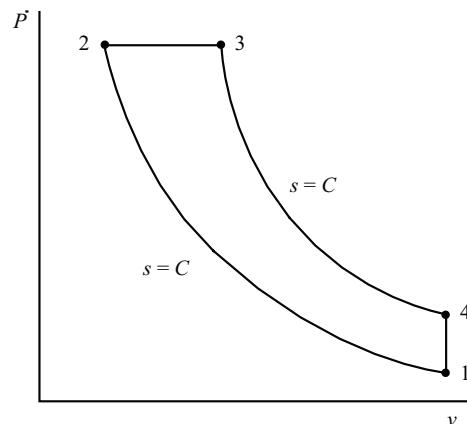
$$\omega_3 = \frac{\dot{m}_{a1}\omega_1 + \dot{m}_{a2}\omega_2}{\dot{m}_{a3}}$$

distance $\overline{13} = \frac{\dot{m}_{a2}}{\dot{m}_{a3}} \times \text{distance } \overline{12}$ measured on
psychrometric chart

Cycles and Processes

Internal Combustion Engines

Diesel Cycle



$$r = V_1/V_2$$

$$r_c = V_3/V_2$$

$$\eta = 1 - \frac{1}{r^{k-1}} \left[\frac{r_c^k - 1}{k(r_c - 1)} \right]$$

$$k = c_p/c_v$$

Brake Power

$$\dot{W}_b = 2\pi TN = 2\pi FRN, \text{ where}$$

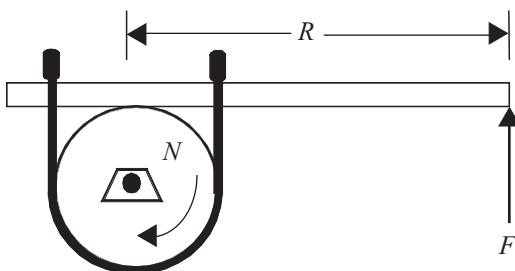
\dot{W}_b = brake power (W)

T = torque (N•m)

N = rotation speed (rev/s)

F = force at end of brake arm (N)

R = length of brake arm (m)



Indicated Power

$$\dot{W}_i = \dot{W}_b + \dot{W}_f, \text{ where}$$

\dot{W}_i = indicated power (W)

\dot{W}_f = friction power (W)

Brake Thermal Efficiency

$$\eta_b = \frac{\dot{W}_b}{\dot{m}_f(HV)}, \text{ where}$$

η_b = brake thermal efficiency

\dot{m}_f = fuel consumption rate (kg/s)

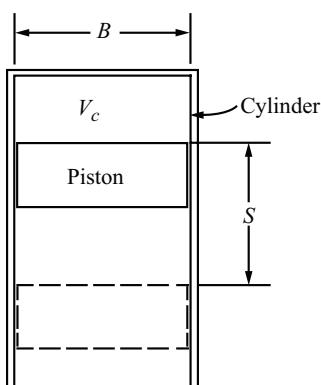
HV = heating value of fuel (J/kg)

Indicated Thermal Efficiency

$$\eta_i = \frac{\dot{W}_i}{\dot{m}_f(HV)}$$

Mechanical Efficiency

$$\eta_l = \frac{\dot{W}_b}{\dot{W}_i} = \frac{\eta_b}{\eta_i}$$



Displacement Volume

$$V_d = \frac{\pi B^2 S}{4}, \text{ m}^3 \text{ for each cylinder}$$

Total volume = $V_t = V_d + V_c$ (m³)

V_c = clearance volume (m³)

Compression Ratio

$$r_c = V_t/V_c$$

Mean Effective Pressure (mep)

$$mep = \frac{\dot{W}_n s}{V_d n_c N}, \text{ where}$$

n_s = number of crank revolutions per power stroke

n_c = number of cylinders

V_d = displacement volume per cylinder

mep can be based on brake power (*bmepl*), indicated power (*imepl*), or friction power (*fmepl*).

Volumetric Efficiency

$$\eta_v = \frac{2\dot{m}_a}{\rho_a V_d n_c N} \quad (\text{four-stroke cycles only})$$

where

\dot{m}_a = mass flow rate of air into engine (kg/s)

ρ_a = density of air (kg/m³)

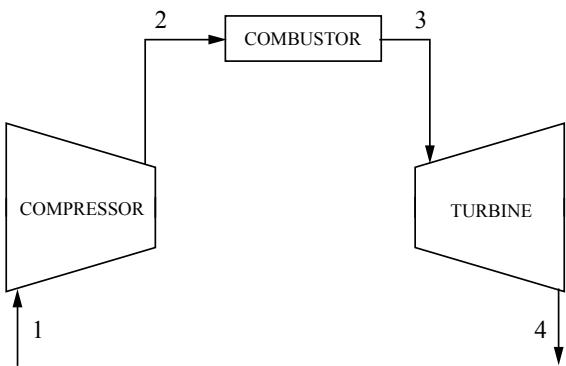
Specific Fuel Consumption (SFC)

$$sfc = \frac{\dot{m}_f}{\dot{W}} = \frac{1}{\eta H V}, \text{ kg/J}$$

Use η_b and \dot{W}_b for *bsfc* and η_i and \dot{W}_i for *isfc*.

Gas Turbines

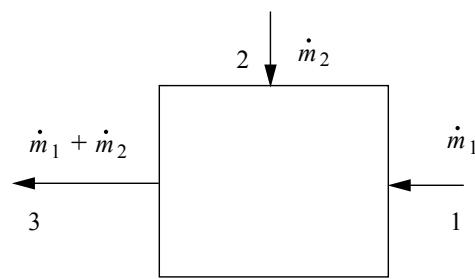
Brayton Cycle (Steady-Flow Cycle)



Steam Power Plants

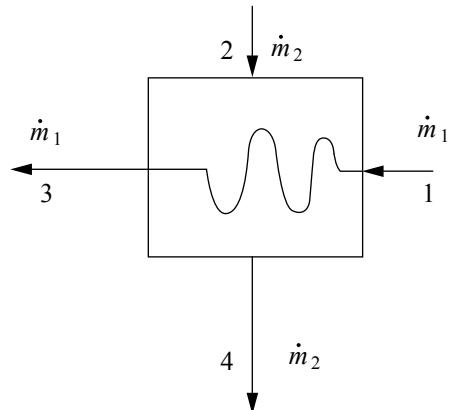
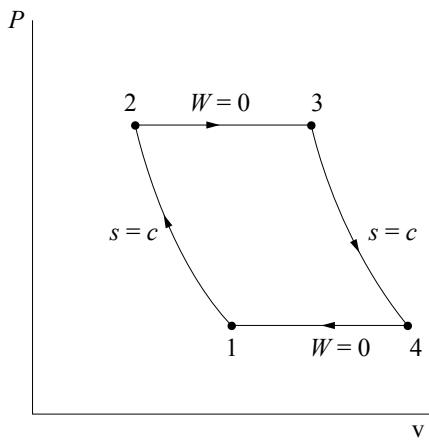
Feedwater Heaters

- Open (mixing)

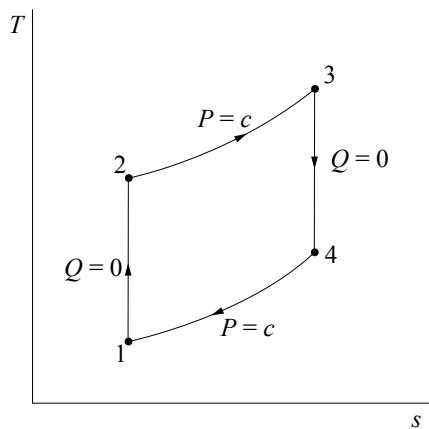


$$\dot{m}_1 h_1 + \dot{m}_2 h_2 = h_3 (\dot{m}_1 + \dot{m}_2)$$

- Closed (no mixing)

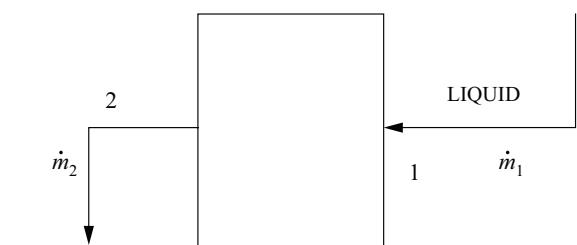


$$\dot{m}_1 h_1 + \dot{m}_2 h_2 = \dot{m}_1 h_3 + \dot{m}_2 h_4$$



Steam Trap

A steam trap removes condensate from steam piping or a heat exchanger.



$$h_2 = h_1 \text{ (if adiabatic)}$$

$$w_{12} = h_1 - h_2 = c_p (T_1 - T_2)$$

$$w_{34} = h_3 - h_4 = c_p (T_3 - T_4)$$

$$w_{\text{net}} = w_{12} + w_{34}$$

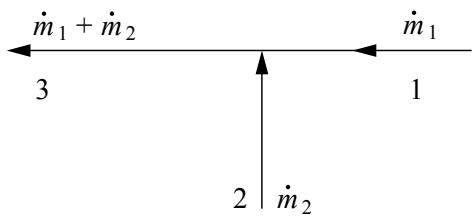
$$q_{23} = h_3 - h_2 = c_p (T_3 - T_2)$$

$$q_{41} = h_1 - h_4 = c_p (T_1 - T_4)$$

$$q_{\text{net}} = q_{23} + q_{41}$$

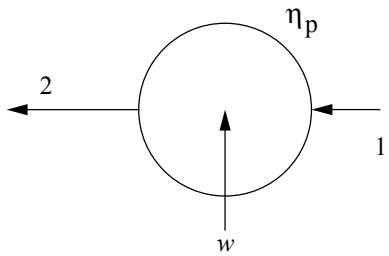
$$\eta = w_{\text{net}} / q_{23}$$

Junction



$$\dot{m}_1 h_1 + \dot{m}_2 h_2 = h_3 (\dot{m}_1 + \dot{m}_2)$$

Pump



$$w = h_1 - h_2 = (h_1 - h_{2S})/\eta_p$$

$$h_{2S} - h_1 = v(P_2 - P_1)$$

$$w = -\frac{v(P_2 - P_1)}{\eta_p}$$

INDEX

A

AASHTO soil classification (table) 149
 AASHTO structural number equation 172
 absolute angular acceleration 71
 absolute angular velocity 71
 absolute dynamic viscosity 102
 absolute humidity 89
 absolute maximum moment 151
 absolute pressure 102
 absorption 141
 absorptivity 121
 acceleration 71, 72, 73
 acceleration due to gravity 166
 acceleration of gravity 88, 103, 104, 106, 111
 acceleration, non-constant 73
 acceleration, normal 71, 72
 acceleration, tangential 71, 72
 acceleration, variable angular 73
 ac circuits 201, 202
 acetylene 55
 acids 53
 acids, carboxylic 55
 ac machines 204
 ac power 203–204
 activated carbon adsorption 192
 activated sludge 190
 activated-sludge treatment (table) 190
 activation energy 59, 61, 137
 activity coefficient 91
 activity, daughter product 188
 acutely lethal doses, comparative (table) 12
 acyclic hydrocarbons, unsaturated 55
 A/D converter 126
 addition, matrix 33
 additives 64
 additives, polymer 64
 adiabatic 90, 122
 adiabatic compression 109
 adiabatic humidification 237
 adiabatic lapse rate, dry 178
 adiabatic mixing 237
 adiabatic process 90
 adiabatic turbine 110
 adsorption, activated carbon 192
 aeration basin volume 190
 aeration tank 190
 aerobic digestion 191
 aerodynamics 112
 affinity laws 110
 agitated oil (graph) 63
 agitated water (graph) 63
 air-entrained concrete 64
 air entrainment 64
 airfoil 112
 air-fuel ratio 91
 air pollution 178–183
 air, properties of 178

air refrigeration cycle (diagrams) 99
 air stripping 192
 air-to-cloth ratio for baghouses (table) 183
 aldehyde 55, 64
 algebra, Boolean 217
 algebra of complex numbers 22
 algebraic projection 187
 alignment charts 161
 alternate depths 166
 AM, amplitude modulation 208
 amorphous materials 64
 amplifier, differential 213
 amplifiers, operational 212
 amplitude modulation (AM) 208
 anaerobic digestion 191
 analog filter circuits 210–211
 analog-to-digital conversion 126
 analysis, earned-value 177
 analysis, job safety 5
 analysis, steady-state 126
 analysis of variance 222
 analysis of variance, one-way 39
 angle-modulated signal 209
 angle modulation 208
 angular acceleration, absolute 71
 angular impulse and momentum 76
 angular velocity, absolute 71
 anion 58
 annual effective interest rate 130
 annulus, circular 118
 anode 58
 anode reaction (oxidation) 59
 ANOVA 39
 ANOVA tables 40
 anthropometric measurements (figure) 224
 anthropometric measurements (table) 225
 applied engineering stress 61
 applied force 61
 approximate values of effective length factor (table) 161
 approximations, statistical (table) 51
 aqueous solutions 53
 aquifer 164
 arbitrary fixed axis, rotation about an 76
 arc definition 170
 Archimedes principle 103
 arc length 72
 area formulas 171
 area, net 157
 area, watershed 164
 arithmetic mean 36
 arithmetic progression 29
 Arrhenius equation 137
 aspect ratio 112
 assemblies cost data 176
 assessment, hazard 6
 associative law 36

- ASTM standard practice for classification of soils for engineering purposes (unified soil classification system) (table) 150
asymptotes 128
atmosphere, orifice discharging freely into 106
atmospheric dispersion 178–181
atmospheric pressure 102, 103, 108
atmospheric stability (tables) 179, 181
atomic bonding 59
atomic number 53
austenite 59
availability 90
available moment (table) 160
available, net positive suction head 108
available strengths 157, 163 (table)
average end area formula 171
average flow velocity 103
average particle diameter 106
average shifts with age of the threshold of hearing for pure tones of persons with "normal" hearing (graphs) 226
average velocity 104
Avogadro's number 53
axial compression (table) 163
axially oriented 62
axis, rigid body motion about a fixed 76
axis, rotation about an arbitrary fixed 76
axle load, gross (table) 172
axles 229
- B**
- backward curved fans 109
baffling factors (table) 196
baghouse 183
baghouses, air-to-cloth ratio for (table) 183
balanced three-phase (3- φ) systems 203
ball/roller bearing 229
band-pass filters (diagram) 211
band-reject filters (diagram) 211
bandwidth, complete 209
barometer, simple 103
bars quenched (graphs) 63
bases 53
basic cycles 89
basic load rating 229
basin retention 164
basins, sedimentation (table) 193
batch reactor 137–138
Bayes' theorem 37
beam 81–82, 84 (table), 85 (table), 151, 154, 156
beams, deflection of 82
beam slopes and deflections, cantilevered (table) 85
beam slopes and deflections, simply supported (table) 84
beams, shear 154
beams, simply supported (table) 156
beams, singly-reinforced 154
beam stiffness 151
bearing, ball/roller 229
bearing capacity, ultimate 148
belt friction 67
bending moment 81
bending stresses 82
benefit-cost analysis 131
Bernoulli equation 104
binary number system 217
binary phase diagrams 65
binder grading system (table) 173
binomial distribution 38
binomial probabilities, cumulative (table) 49–50
biological half-life 188
biomass concentration 190
biomechanics of the human body 19
biotower 191
bipolar junction transistor (BJT), NPN (table) 214
BJT differential amplifier 213
BJT, NPN bipolar junction transistor (table) 214
black body 121, 122
blades, fixed and moving 107
block shear 157
blowers 109
bode plots 207
body, black 121
body dimensions, female/male, for ages 20 to 60 years, U.S. civilian (table) 225
body, gray 121
body, opaque 121
body temperature 117
boiler 89, 98 (diagrams)
boiling 118–119
bolt diameter 157
bolted and riveted joints loaded in shear 231
bolted members 157
bolt stiffness 231
bonds 131
bonds, primary 59
book value 130, 131
Boolean algebra 217
Boyle's law 88
braced frame (chart) 161
bracing, lateral (table) 156
brake power 238
brake power, pump 108
brake thermal efficiency 238
Brayton cycle 239
break-even analysis 130
break-through time 187
Brinell hardness 62
brittle materials 234
Buckingham Pi theorem 111
buckled shape (table) 161
buckling 82
buckling, flexural 156
buckling, lateral-torsional 156
buckling stress 82
buckling stress, elastic 156
bulk fluid temperature 116
bulk modulus 111
buoyancy 103

C

calculus 26–27
 canonical product of sums (POS) 218
 canonical sum of products (SOP) 218
 cantilevered beam slopes and deflections (table) 85
 capability, process 219
 capacitance 59
 capacities, heat 62, 64, 86, 117
 capacitor 59, 200–202
 capacitor, parallel plate 59, 200
 capacitors and inductors in parallel and series 201
 capillarity 102
 capillary 102
 capillary rise 102
 capitalized costs 131
 capital recovery (table) 130
 carbide 59
 carbide phase diagram, iron-iron 65
 carbon black 64
 carboxylic acid 55
 carcinogens 7 (GHS pictogram), 13
 Carnot cycle 89, 98 (diagram)
 Cartesian coordinates 71
 catalyst 53
 catastrophic crack propagation 61
 cathode 58
 cathode reactions (reduction) 59
 cation 58
 Cauchy number 111
 cement 64
 center of buoyancy 103
 center of curvature 72
 center of pressure 103
 central limit theorem 38
 centrifugal pump 108
 centroid 29, 66, 68–70 (tables), 78 (table), 82, 103, 106
 centroidal axis 67
 centroidal x-axis 103
 centroid of area 66, 103
 centroid, asymptote 128
 centroid of the total mass 66
 channels, rectangular 166
 Charles' law 88
 Charpy impact test 63
 chemical engineering 137–144
 chemical equilibrium constant 92
 chemical equilibrium, Le Chatelier's principle for 53
 chemical interaction effects, selected (table) 12
 chemical process industry 127, 128
 chemical reaction 137
 chemical reaction equilibrium 92
 chemical reaction, equilibrium constant of a 53
 chemical sensors (table) 125
 chemicals, industrial (table) 57
 chemistry 53–58
 chemostat 184
 chlorinated phosphates 64

circle 26
 circuits, ac 201, 202
 circuits, analog filter 210–211
 circular annulus 118
 circular cone, right 24
 circular cylinder, right 25
 circular motion, plane 72
 circular pipe head loss equation 167
 circular sector 24
 circular segment 24
 circular sewers (graph) 165
 civil engineering 145–177
 Clapeyron equation 92
 clarifier 193
 classification of structures 152
 Clausius-Clapeyron equation 92
 Clausius, inequality of 90
 Clausius' statement of second law 90
 corollary to Clausius 90
 closed-loop characteristic equation 126
 closed-system exergy 90
 closed thermodynamic system 88
 coefficient
 concavity 145
 contraction 111
 convection heat transfer 116, 117, 120
 determination 39
 diffusion 59, 139, 187
 discharge 106
 drag 105, 112, 115 (graph)
 friction 67, 75
 fugacity 91
 Hazen-Williams 167
 heat transfer 120
 kinetic friction 75
 lift 112
 Manning's roughness 166
 meter 111
 octanol-water partition 185
 organic carbon partition 185
 orifice 111
 overall 139
 partition 185
 performance (COP) 89
 permeability 145, 187
 permeability of soil 164
 Rankine earth pressure 148
 restitution 74
 roughness 105, 166
 runoff 164
 sample correlation 39
 soil-water partition 185
 static friction 67, 75
 stoichiometric 92
 storage 164
 thermal expansion 64, 80, 120
 uniformity 145
 variation 37

- velocity 110
yield 184, 190
cold working 59
columns 82, 154, 156
columns, intermediate- and long-length 233
column strength interaction 155
combinations 36
combustion in air 91
combustion efficiency 183
combustion equation 91
combustion, heats of reaction, solution, formation, and 53
combustion, incomplete 91
combustion processes 91
common mode rejection ratio (CMRR) 212
communication theory 206–209
comparison of steady-state performance for decay reactions of different order (table) 186
comparison of steady-state retention times for decay reactions of different order (table) 186
compatibility chart 14
compensator, lag or lead 127
complete bandwidth 209
complex numbers, algebra of 22
complex power 203
components, steel 156
composite materials 62
composite plane wall 116
composite sections 82
composites, fiber-reinforced 62
compound amount (table) 130
compounding, non-annual 130
compounds 64
compounds, families of organic (table) 56
compressibility factors (graph) 97
compressible flow 107–108
compressible fluid 110
compression, axial (table) 163
compression, isothermal 109
compression members (table) 162
compression ratio 238
compression spring dimensions (tables) 228
compressive normal stress components 80
compressive strength, design 156
compressive strength (graphs) 64
compressor 98 (diagram), 99 (diagram), 109, 110
compressor, adiabatic 109
compressor efficiency, isentropic 109
compressor isentropic efficiency 109
computer engineering, electrical and 199–218
concavity coefficient 145
concentration change in a vessel, sweep-through 17
concentration of vaporized liquid 17
concept of weight 73
concrete 64
concrete, air-entrained 64
concrete, non-air-entrained 64
concrete, reinforced 153
ASTM standard reinforcing bars (table) 153
concrete strength 64
concurrent forces 67
concurrent-force system 67
condensation of a pure vapor, film 119
condenser (diagrams) 98, 99
condensers 89
conditioning, signal 126
conduction 116–117
conduction, Fourier's law of 116
conduction resistance, cylindrical wall 116
conduction resistance, plane wall 116
conduction through a cylindrical wall 116
conduction, transient 117
conductivity 59, 212
conductivity, hydraulic 145, 164, 187
conductivity impedance (table) 125
conductivity, thermal 116, 117, 119
conduct, professional 3–4
cone 171
cone, right circular 24
confidence interval 43, 44
confidence interval for intercept 39
configuration factor 121
configurations, flow 105
confined aquifer 164
confined space safety 11
conic section equation 26
conic sections 25–26
connection eccentricity 157
consecutive holes 157
conservation of angular momentum 76
conservation of energy, law of 74
consistency index 102
consolidation, degree of 147
constant acceleration 72
constant acceleration equations 73
constant angular acceleration 72
constant, Stefan-Boltzmann's 116, 121, 212
constant of a chemical reaction, equilibrium 53
constant, curve-fit (table) 181
constant density systems 186
constant entropy 86
constant fluid temperature 117
constant, gas 1, 59, 86, 107
constant, Henry's law 139, 192
constant, ideal gas law 61
constant, impeller (table) 195
constant, kinetic 190
constant mass 73
constant, monod growth rate 185
constant, pre-exponential 61
constant pressure heat capacity 64
constant, proportionality 59
constant system pressure 88
constant temperature 88
constant, universal gas 109, 139
constant volume 64, 86, 88
constant volume heat capacity 64

- construction 176–177
 continuity equation 103
 continuous distillation (binary system) 140
 continuous-stirred tank reactor (CSTR) 138
 continuous-time convolution 206
 contraction, coefficient of 111
 contractions 105, 107
 controller, PID 127
 controls 123
 control, statistical quality 51
 control system models 127–128
 control system negative feedback 126
 control systems 126–129
 control, tests for out of 51
 control volume 106
 convection 116, 117–121, 139
 convection heat transfer coefficient 116, 117, 120
 convection, natural (free) 120
 convection resistance 116
 convection surface area 116
 conversion 92
 conversion, analog-to-digital 126
 conversion factors (table) 2
 conversions, temperature (table) 1
 conveyance systems 104
 convolution 206
 cooling 236
 cooling, evaporative 237
 cooling, Newton's law of 116
 cooling rate 62, 63 (graphs)
 cooling rates for bars quenched in agitated oil (graph) 63
 cooling rates for bars quenched in agitated water (graph) 63
 coordinates, Cartesian, 71
 coordinate system, polar 22
 copper 83, 123, 231
 corollary to Clausius 90
 corollary to Kelvin-Planck 90
 correction factor, kinetic energy 166
 corrections, kinetic temperature 185
 correlation coefficient, sample 39
 corrosion 59
 corrosion reactions (table) 58
 corrosives (GHS pictograms) 7, 8
 cosines 22
 cost 130
 cost estimation 143–144
 cost indexes 143
 Coulomb-Mohr theory 234
 counterflow 120
 counterflow concentric tube heat exchanger 121
 couples 66
 coupling multiplier (table) 19
 CPM precedence 176
 crack length 61
 crack propagation, catastrophic 61
 crash rates at intersections 175
 crash rates for roadway segments 175
 crash reduction 175
 creep 61
 criteria for rejection (tables) 41, 42
 critical axial load 82
 critical depth 166
 critical heat flux 119
 critical insulation radius 116
 critical path method (CPM) 224
 critical pressure 119
 critical stress 156, 162 (table)
 critical values of the F distribution (table) 47
 critical values of χ^2 distribution (table) 48
 cross flow 118
 crystalline materials 59
 crystalline solids 64
 CT values (tables) 198
 cubic EOS 87
 cumulative binomial probabilities (table) 49–50
 cumulative distribution functions 37
 curl, vectors, gradient, divergence, and 34
 current 199
 curvature 27
 curvature in rectangular coordinates 27
 curve-fit constants as a function of atmospheric stability (table) 181
 curve formulas, horizontal 170
 curve formulas, vertical 171
 curve number 164
 curves, horizontal (table) 169
 curves, vertical (table) 169
 curvilinear motion, particle 71
 cycle, air refrigeration (diagrams) 99
 cycle, Brayton 239
 cycle, Carnot 89, 98 (diagram)
 reversed Carnot 89, 98 (diagram)
 cycle, diesel 237
 cycle, Otto 89, 98 (diagram)
 cycle, Rankine 89, 98 (diagram)
 cycles, basic 89
 cycle, steady-flow 239
 cycles, thermodynamic (diagrams) 98
 cyclic load 61
 cyclone 182
 cylinder, right circular 25
 cylindrical pressure vessel 79
 cylindrical wall, conduction through a 116

D

- Darcy's law 164
 Darcy-Weisbach equation 105
 data quality objectives (DQO) for sampling soils and solids (table) 188
 daughter product activity 188
 dc machines 204
 decay reactions (table) 186
 decibels 207
 deflection angle 170
 deflection of beams 82
 deflections, cantilevered beam slopes and (table) 85

- deflections, simply supported beam slopes and (table) 84
 deformation 61, 79
 deforming, plastically 59
 degree of consolidation 147
 degree-of-freedom, single 77
 dehumidification 236
 De Morgan's law 36
 De Morgan's theorems 217
 density functions: means and variances, probability and (table) 52
 density systems, constant 186
 depreciation 130, 131
 modified accelerated cost recovery system (MACRS) 131
 straight line 131
 depth, critical 166
 depth of sorption zone 192
 derivative 26
 derivatives and indefinite integrals 28
 design and operational parameters for activated-sludge treatment
 of municipal wastewater (table) 190
 design compressive strength 156
 design criteria for sedimentation basins (table) 193
 design flexural strength 156
 design moment strength 154
 design provisions 153
 design shear strength 156
 design, superpave mixture (table) 173
 destruction and removal efficiency 183
 determinacy 152
 determinants 34
 determining the project size modifier (table) 176
 Deutsch-Anderson equation 183
 deviations for shafts (table) 233
 deviation, standard 36, 51 (charts)
 dew-point temperature 89
 dielectric constant 59
 diesel cycle 237
 difference between two means, confidence interval for the 43
 difference equations 35, 205
 differential amplifier 213
 differential calculus 26–27
 differential distance 102
 differential equation 30, 77
 differential equations, numerical solution of ordinary 35
 differential gearset 230
 differential (simple or Rayleigh) distillation 140
 differential velocity 102
 diffuse-gray surfaces 122
 diffusion coefficient 59, 139, 1873
 diffusion of a gas A through a second stagnant gas,
 unidirectional 139
 digital signal processing 206
 digraphs of relation 21
 dilatant 102
 dimensional analysis 111
 dimensional homogeneity 111
 dimensionless 106
 dimensionless group equation (Sherwood) 139
 diodes (table) 214
 direct costs (table) 143
 directed graphs 21
 discharge, coefficient of 106
 discharge, fire sprinkler 167
 discharge pressure 109
 discharging freely into atmosphere, orifice 106
 discrete math 21
 discrete-time convolution 206
 discriminator 209
 disinfection 196
 dispersion 36
 displaced fluid volume 103
 displacement 72, 73
 displacement, lateral 156
 displacement volume 238
 distance, sight (tables) 169
 distance, stopping sight 168
 distillation 140–141
 distortion-energy theory 234
 distribution 37, 38
 distribution, binomial 38
 distribution, Gaussian 38
 distribution, normal 38, 41 (table), 42 (tables), 45 (table)
 distribution, student's t- (table) 46
 distributive law 36
 dose-response curves 12
 double-sideband modulation (DSB) 204
 downwind distance as a function of stability class
 (graph) 181
 drag coefficient 105, 112, 115 (graph)
 drag force 105
 drainage 147
 drift velocity, terminal 183
 dry adiabatic lapse rate 178
 DSB, double-sideband modulation 208
 dual linear program 219
 ductile to brittle transition 63
 ductile materials 234
 ductility 59, 61
 ducts, noncircular 118
 Dupuit's formula 164
 durability 64
 dynamic fields, electromagnetic 205
 dynamics 71–78, 235
 dynamics of mechanisms 230
 dynamic similarity 111
 dynamic viscosity 104, 111, 117, 118, 119
 dynamic viscosity, absolute 102, 113 (tables)

E

- earned-value analysis 177
 earthwork formulas 171
 eccentricity, connection 157
 economics, engineering 130–136
 economics factors (table) 130
 effective area 157
 effective half-life 188
 effective length (table) 163

- effective length factor (table) 161
 effectiveness, heat exchanger 120
 effective porosity 164
 effective slenderness ratio 156
 efficiency, brake thermal 238
 efficiency, compressor isentropic 109
 efficiency, cyclone collection (particle removal) 182
 efficiency, destruction and removal 183
 efficiency, electrostatic precipitator 183
 efficiency, indicated thermal 238
 efficiency, isentropic compressor, 109
 efficiency, mechanical 238
 efficiency, power and 74
 efficiency, turbine isentropic 110
 effluent flow rate 190
 effluent suspended solids concentration 190
 elastic buckling stress 156
 elastic curve (tables) 84, 85
 elastic force 111
 elasticity, modulus of 61, 79, 80, 83 (tables)
 elastic loading 61
 elastic longitudinal deformation 79
 elastic modulus 61, 82
 elastic potential energy 73
 elastic spring 73
 elastic strain energy 82
 electrical 59
 electrical and computer engineering 199–218
 electrical safety (table) 11
 electrical units 199
 electrochemistry 58
 electrode 58
 electrolytes 196
 electromagnetic dynamic fields 205
 electronics, solid-state 212–216
 electrons 58
 electrostatic fields 199
 electrostatic precipitator efficiency 183
 electrostatics 199
 elemental semiconductors, extrinsic (table) 61
 elements, hydraulic (graph) 165
 elevation 88
 elevation heads 104
 ellipse 23, 25
 elongation 79, 83 (table)
 elongation, percent 61
 emissivity 116, 121
 empirical constant 187
 endogenous decay rate constant 184
 endurance limit 234
 energy 74
 energy, activation 59, 61, 137
 energy content of waste (table) 183
 energy, elastic potential 73
 energy, elastic strain 82
 energy equation 104
 energy exchange 121, 122
 energy, kinetic 73, 74, 76
 energy, law of conservation of 74
 energy levels, impurity (table) 61
 energy line 104
 energy, potential 73, 104
 energy, principle of work and 74
 energy, specific 166
 energy, specific internal 86
 engineering economics 130–136
 engineering economics factors (table) 130
 engineering strain 61, 64, 79
 engineering stress 61
 engineering stress, applied 61
 engines, internal combustion 237
 enhancement MOSFET (low and medium frequency) (table) 216
 enlargements 107
 enthalpy 86, 89, 90, 93 (table), 119, 236
 enthalpy change for phase transitions 92
 enthalpy change of reaction, standard 92
 enthalpy, pressure (diagram) 95
 enthalpy, specific 86
 entropy 86, 90, 93 (table)
 entropy change 92
 entropy change for solids and liquids 90
 entropy, constant 86
 entropy principle, increase of 90
 entropy, specific 86
 environmental engineering 178–198
 equation
 AASHTO structural number 172
 Arrhenius 137
 Bernoulli 104
 circular pipe head loss 167
 Clapeyron 92
 Clausius-Clapeyron 92
 closed-loop characteristic 126
 conic section 26
 continuity 103
 Deutsch-Anderson 183
 difference 35, 205
 differential 30, 77
 energy 104
 Ergun 106
 Faraday's 53
 field 104
 filtration 194
 first-order linear difference 35
 fixed-film 191
 Hagen-Poiseuille 105
 Hazen-Williams 105, 167
 heat transfer 120
 heat transfer rate 116
 Kline-McClintock 126
 lime-soda softening 195
 linear difference 205
 Manning's 105, 166
 of motion 76
 population projection 187

- pump power 109
 residential exposure 15
 Rose 194
 settling 194
 of state (EOS) 87
 straight line 21
 Theim 164
 traffic safety 175
 equilibrium 103
 equilibrium constant 92
 equilibrium constant of a chemical reaction 53
 equilibrium curve 141
 equilibrium phases 59
 equilibrium requirements 66
 equilibrium (VLE), vapor-liquid 91–92
 equimolar counter-diffusion 139
 equivalent codes for a four-bit binary value (table) 217
 equivalent, Norton 200
 ergonomics 18–20
 ergonomics, hearing 226–227
 Ergun equation 106
 error analysis, steady-state 127
 error, propagation of 38
 essential prime implicant 218
 estimate, standard error of 39
 ether 55
 ethics 3–4
 Model Rules of Professional Conduct 3–4
 Euler's approximation 35
 Euler's formula 82
 Euler's identity 22
 eutectic reaction 65
 eutectoid reaction 65
 evaporation 118
 evaporative cooling 237
 evaporator 89, 98 (diagram), 99 (diagram)
 exchangers, heat 89, 99 (diagrams), 120, 239
 exergy 90
 expansions 105
 expansion valve (diagrams) 98, 99
 expected values 37–38
 experimental constant 119
 exponential growth 187
 exponentially weighted moving average 221
 exposure limits for selected compounds (table) 12
 exposure, noise 20
 exposure pathways (residential) 15
 external flow 117
 external moment 67
 extrinsic, elemental semiconductors (table) 61
 extrinsic semiconductors 61
- F**
 facility planning 222–224
 facultative pond 191
 failure by crushing of rivet or member 231
 failure, fatigue 61
 failure by rupture 231
 failure theories 234–235
 families of organic compounds (table), 56
 fan 109, 110
 Fanning friction factor 105
 Faraday's equation 53
 Faraday's law 53, 199, 201
 fastener groups in shear 231
 fasteners, threaded 230, 231
 fate 184
 fatigue 61
 fatigue failure 61
 fatigue loading 229
 F distribution, critical values of the (table) 47
 feedback control system model 126
 feedwater heaters 239
 ferrite 59
 fiber-reinforced composites 62
 field effect transistors (JFETs) and depletion MOSFETs (low and medium frequency), N-channel junction (table) 215
 field equation 104
 field, pressure 102
 fields, electromagnetic dynamic 205
 fields, electrostatic 199
 fields, magnetic 199
 fillers 64
 film boiling 119
 film condensation of a pure vapor 119
 filter circuits, analog 210–211
 filters, band-pass (diagram) 211
 filters, band-reject (diagram) 211
 filters, first-order high-pass (diagram) 210
 filters, first-order low-pass (diagram) 210
 filtration equations 194
 final value theorem 126
 finite state machine 21
 fin, pin 117
 fin, rectangular 117
 fins 117
 fire hazard diamond 6
 fire hydrant discharging to atmosphere 167
 fire hydrant, formula for calculating rated capacity 167
 fire sprinkler discharge 167
 fire sprinkler K factors (table) 167
 first law of thermodynamics 87–89
 first-order control system models 127
 first-order high-pass filters (diagram) 210
 first-order irreversible reaction 137
 first-order linear difference equation 35
 first-order low-pass filters (diagram) 210
 first-order rate constant 188
 first-order reversible reactions 137
 fit, goodness of 39
 fits 232
 fits, preferred (table) 232
 fits, press/shrink 232
 fixed axis, rigid body motion about a 76

- fixed axis, rotation about an arbitrary 76
 fixed blade 107
 fixed-film equation 191
 flame retardants 64
 flammability 6–8, 10
 flammable limits 10
 flammables (GHS pictogram) 7
 flash (or equilibrium) distillation 140
 flat bars 157
 flexural buckling 156
 flexural strength, design 156
 flip-flops 218
 floating body 103
 flocculator 195
 flow
 compressible 107–108
 configurations 105
 cross-sectional area of 103, 106, 110, 164, 167
 external 117
 fluid 104–105, 106
 internal 118
 isentropic 108
 laminar 104, 105, 106, 118
 machinery, fluid flow 108–110
 measurement, fluid flow 110
 nets 145
 noncircular conduits 105
 one-dimensional fluid flow 103–104
 open-channel 105, 166
 over a sphere 118
 pipe 105
 rate, mass 88, 103, 110
 ratio curves, sewage (graph) 165
 reactors, steady state 138
 relationships, traffic 169
 subsonic 108
 supersonic 108
 steady incompressible 104
 through a packed bed 106
 turbulent 104, 106, 118
 uniform 166
 volumetric 103, 106, 109, 110
 fluid density 103, 104, 105, 106, 108, 110, 112
 fluid flow 104–105, 106
 fluid flow machinery 108–110
 fluid flow measurement 110
 fluid flow, one-dimensional 103–104
 fluid mechanics 102–115
 fluid power 108
 fluid, power law (non-Newtonian) 102
 fluid pressure (head) 110
 fluid streamline 104
 fluid temperature 117
 fluid vapor pressure 108
 fluid velocity 107, 108
 fluid viscosity 106
 flux 188
 flux, critical heat 119
 flux density, magnetic 199
 flux, gas 187
 flux, heat 118, 119
 flux, minimum heat 119
 flux, peak heat 119
 flux, salt 196
 flux, water 196
 FM, frequency modulation 209
 force 66
 concurrent 67
 convection boiling 118
 resolution of a 66
 shearing 81
 and strains (diagram) 153
 on submerged surfaces 103
 surface 102
 systems of 66
 forecasting 221
 formability 64
 formation, and combustion, heats of reaction, solution 53
 formula
 area 171
 average end area 171
 Dupuit's 164
 earthwork 171
 horizontal curve 170
 kiln 183
 NIOSH 18
 prismoidal 171
 rational 164
 Taylor tool life 224
 vertical curve 171
 weir 166
 work sampling 224
 fouling factor 120
 four-bar linkage 235
 Fourier series 31, 207
 Fourier's law of conduction 116
 Fourier transform 30, 206
 Fourier transform, inverse of 32
 Fourier transform pairs (table) 32
 Fourier transform theorems (table) 32
 4-LOG inactivation (table) 198
 fraction, mole 87, 91
 fraction of a substance, mole 53
 fracture 157
 fracture toughness 61, 62 (table)
 frame, braced (chart) 161
 frame deflection 151
 frame, moment (chart) 161
 frame, plane 152
 free convection boiling 118
 free discharge 166
 free energy, Gibbs 86, 90
 free energy, Helmholtz 86, 90
 free-falling body 72

- free stream velocity 117
 free vibration 77
 freezing point depression 53
 frequency deviation 208
 frequency-deviation ratio 209
 frequency modulation (FM) 209
 frequency multiplier (table) 18
 frequency, Nyquist 126, 209
 frequency response 127, 207 (diagram), 210 (diagram), 211 (diagram)
 frequency, undamped natural 77, 128
 Freundlich isotherm 192
 friction 67, 75
 friction, belt 67
 friction, coefficient of 75
 friction, coefficient of kinetic 75
 friction, coefficient of static 75
 friction effect 104
 friction factor 105
 Darcy 105
 Fanning 105
 Moody 105, 142
 Stanton 105
 friction force 67, 75
 friction, laws of 75
 friction, limiting 67
 friction losses 108
 Froude number 111, 166
 fugacity coefficient 91
 fugacity, pure component 91
 function, gamma 38
 function, open-loop transfer 126, 127
 function, probability density 37
 functions, cumulative distribution 37
 fundamental constants 1
 future worth 130
- G**
- gage factor (GF) 124
 gage pressure 102
 gage setup (table) 124
 gages, metallic strain 124
 gage, strain 124
 gain margin (GM) 127
 gamma function 38
 gas constant 1, 59, 86, 107
 gas constant, universal 109, 139
 gas-filled porosity 187
 gas flux 187
 gas, ideal 86, 88, 92, 107, 109, 110, 120
 gas law constant, ideal 61, 91
 gas mixtures, ideal 87
 gasoline engine (diagram) 98
 gas phase mass transfer coefficient 139, 141
 gas phase mass velocity 141
 gas phase solute mole fraction 141
 gas turbines 239
 gate, NAND 217
 gate, NOR 217
 Gaussian 178
 Gaussian distribution 38
 Gauss' law 199
 gearing 230
 gearset, differential 230
 gearset, planetary 230
 gear trains 229
 general character of probability 36
 general inflation rate 130
 generalized compressibility EOS 87
 generalized compressibility factors (graph) 97
 generators 204
 geometrical factor 61
 geometric growth 187
 geometric progression 29
 geotechnical 145–150
 GHS (Globally Harmonized System of Classification and Labelling of Chemicals) 6
 label elements 6
 pictograms and hazard classes 7
 transport pictograms 8
 giardia cysts (table) 198
 Gibbs energy change of reaction 92
 Gibbs free energy 86, 90
 Gibbs phase rule 92
 glass fibers, chopped 64
 glass transition temperature 64
 Globally Harmonized System of Classification and Labelling of Chemicals (GHS) 6
 Goodman theory, modified 234
 goodness of fit 39
 grade line 104
 grades, algebraic difference in 168
 gradient, divergence, and curl, vectors 34
 gradient, hydraulic 104
 grading system, binder (table) 173
 grain-boundary surface 62
 grain growth 59
 grain size 62
 granular storage 11
 gravitational acceleration 119
 gravitational constant 108
 gravity, acceleration due to 166
 gravity, acceleration of 88, 103, 104, 106, 111
 gravity field 73
 gravity force 111, 166
 gravity, local acceleration of 73
 gravity model 174
 gray body 121
 gray surfaces, diffuse- 122
 gross area 157
 gross width of member 157
 growth, exponential 187
 growth, geometric 187
 growth, log 187
 gyration, least radius of (table) 163

- gyration, mass radius of 76
 gyration, radius of 67, 68–70 (tables), 78 (table), 82
 gyratory compaction effort, superpave (table) 174
- H**
- Hagen-Poiseuille equation 105
 half-life 188
 hardenability curves, Jominy (graph) 62
 hardness, Brinell 62
 hazard assessment 6
 hazard communication standard (HCS) 9
 hazardous waste compatibility chart 14
 Hazen-Williams coefficient 167
 Hazen-Williams equation 105, 167
 HCS (hazard communication standard) 9
 head 110
 head loss 104, 105, 106
 head loss due to flow 105
 head loss equation, circular pipe 167
 hearing, ergonomics 226–227
 hearing loss (graphs) 227
 heat 87, 142
 heat capacity 62, 64, 86, 117
 heat of combustion 90–91
 heaters, feedwater 239
 heat exchanger 89, 99 (diagrams), 120, 239
 heat exchanger, counterflow concentric tube 121
 heat exchanger effectiveness 120
 heat exchanger, parallel flow concentric tube 121
 heat flux 118, 119
 heating 236
 heats of reaction 90–91
 heats of reaction, solution, formation, and combustion 53
 heat, specific 64, 109, 119
 heat transfer 116–122, 142, 236
 heat transfer coefficient 120
 heat transfer coefficient, convection 116, 117, 120
 heat transfer rate equations 116
 helical springs 228
 Helmholtz free energy 86, 90
 Henry's constant 92
 Henry's law constant 139, 192
 Henry's law at constant temperature 91
 HFC-134a (diagram) 95
 high-pass filters (diagram) 210
 highway curves 169–171
 highway pavement design 172
 highway pavement design, load equivalency factors for (table) 172
 homogeneity, dimensional 111
 Hooke's law 61, 80
 horizontal curve formulas 170
 horizontal curves (table) 169
 horizontal orifice meter 111
 horizontal sight line offset (table) 169
 horizontal standard deviations of a plume (graph) 180
 horizontal stress 148
 hot working 59
- human body, biomechanics of the 19
 humidification 236
 humidification, adiabatic 237
 humidity 89
 HVAC 99, 236–240
 HVAC two-stage cycle, refrigeration and (diagrams) 99
 hydrant, fire 167
 hydraulic conductivity 145, 164, 187
 hydraulic depth 166
 hydraulic diameter 105
 hydraulic-elements graph for circular sewers 165
 hydraulic grade line 104
 hydraulic gradient 104
 hydraulic head 164, 187
 hydraulic jump 166
 hydraulic radius 105, 166
 hydraulic residence time 190
 hydrocarbons, unsaturated acyclic 55
 hydrology 164–167
 hyperbola 26
 hypothesis (tables) 41, 42
 hypothesis testing 39–43
- I**
- ideal gas 86, 88, 92, 107, 109, 110, 120
 ideal gas EOS 87
 ideal gas law constant 61, 91
 ideal gas mixtures 87
 ideal-impulse sampling 209
 identities, trigonometric 23
 identities, vectors 34
 identity matrix 33
 immiscible fluids 103
 impact 74
 impact test, Charpy 63
 impeller constant (table) 195
 impeller diameter 110
 impermeable layer (diagram) 145
 implicant 218
 impulse and momentum 74
 impulse-momentum principle 106–107
 impulse response 207
 impulse turbine 107
 impurity energy levels for extrinsic semiconductors (table) 61
 inactivation requirements, removal and (table) 197
 incidence rates 20
 incineration 183
 incomplete combustion 91
 incompressible flow 111
 incompressible flow, steady 104
 incompressible fluid 110
 increase of entropy principle 90
 indefinite integrals, derivatives and 28
 indicated power 238
 indicated thermal efficiency 238
 induced voltage 199
 inductors 200–202
 industrial chemicals (table) 57

- industrial engineering 219–227
 inequality of Clausius 90
 inertia force 111
 inertial forces 166
 inertia, mass moment of 76, 77, 78 (table)
 inertia, moment of 29, 66–67, 68–70 (table), 81, 82, 103
 inertia parallel axis theorem, moment of 67
 inertia, product of 67, 68–70 (tables), 78 (table)
 inflation 131
 influence lines 151
 influent flow rate 190
 inlet gas density 109
 inplane shear stress 80
 instantaneous center of rotation 75
 instantaneous frequency 208
 instantaneous phase 208
 instantaneous radius of curvature 72
 instant center 75
 instrumentation, measurement, and controls 123–129
 intake, EPA recommended values for estimating (table) 16
 integral calculus 27
 interaction diagram 155
 interest rate 130
 interest rate factor tables 132–136
 intermediate- and long-length columns 233
 internal combustion engines 237
 internal energy 86, 93 (table)
 internal flow 118
 internal pressure 107
 international tolerance (IT) grades (table) 233
 intersection angle 170
 inventory models 222
 inverse of Fourier transform 32
 inverse, matrix 33
 inverse natural frequency 128
 inverse square law 188
 inverse transform method 221
 iron-iron carbide phase diagram 65
 irreversibility 90
 isentropic 88, 89, 90
 isentropic compressor 109
 isentropic efficiency 89
 isentropic efficiency, turbine 110
 isentropic exit temperature 109
 isentropic flow 108
 isentropic process 88, 90, 108
 isothermal compression 109
- J**
 jet propulsion 107
 JFETs and depletion MOSFETs (low and medium frequency),
 N-channel junction field effect transistors (table) 215
 job safety analysis 5
 job sequencing 224
 Johnson's rule 22
 joining methods 230–232
 Jominy hardenability curves for six steels (graph) 62
- junction 240
- K**
 Karnaugh map (K-map) 218
 Kelvin-Planck statement of second law 90
 corollary to Kelvin-Planck 90
 Kendall notation 219
 Kennedy's rule 75
 ketone 55
 kiln formula 183
 kinematics 71, 235
 kinematics of mechanisms 235
 kinematics, particle 71–73
 kinematics of a rigid body 75
 kinematic viscosity 102, 104
 kinetic constant 190
 kinetic energy 73, 74, 76
 kinetic energy correction factor 166
 kinetic friction, coefficient of 75
 kinetics, microbial 184
 kinetics, monod 184
 kinetics, particle 73–75
 kinetics for planar problems, normal and tangential 73
 kinetics of a rigid body 75–76
 kinetic temperature corrections 185
 Kirchhoff's laws 200
 Kline-McClintock equation 126
- L**
 lag or lead compensator 127
 laminar flow 104, 105, 106, 118
 landfill 187
 Langmuir isotherm 192
 Laplace transform 33, 127, 129
 Laplace transform pairs 33
 latent heat 119
 lateral-torsional buckling 156
 law
 associative 36
 Charles' 88
 compound or joint probability 37
 conservation of energy 74
 ideal gas constant 61, 91
 Darcy's 164
 De Morgan's 36
 distributive 36
 Faraday's 53, 199, 201
 friction 75
 Gauss' 199
 Henry's 192
 Hooke's 61, 80
 inverse square 188
 Kirchhoff's 200
 probability 36–37
 Stokes' 194
 thermodynamics, first 87–89
 thermodynamics, second 90
 total probability 36

- leachate 187
 lead compensator, lag or 127
 learning curves 222
 least material condition (LMC) 233
 least squares 39
 Le Chatelier's principle for chemical equilibrium 53
 Le Chatelier's rule 10
 Leidenfrost point 119
 length, arc 72
 length, column effective 156
 length, crack 61
 lethal doses, comparative acutely (table) 12
 Lever rule 65
 L'Hospital's Rule 27
 lift coefficient 112
 lift force 112
 lime-soda softening equations 195
 limiting friction 67
 limiting reactant 92
 limits 232
 limit states 157
 linear combinations 39
 linear difference equation 205
 linear programming 219
 linear projection 187
 linear regression 39
 linear velocity profile 102
 line balancing 223
 linkage, four-bar 235
 liquid, mass flow rate of 17
 liquid, mass of 86
 liquid metals 118
 liquid phase 119
 liquid phase mass transfer coefficient 139
 liquid phase mass velocity 141
 liquid, static 102
 liquid surface 103, 106
 liquids, vaporized 17
 liquid-vapor interface 119
 live load reduction 152
 load combinations 152
 load, critical axial 82
 load equivalency factors for highway pavement design
 (table) 172
 loading and deformation, uniaxial 79
 loading failure theories, static 234
 loading failure theories, variable 234–235
 loading, fatigue 229
 loading, static 229
 loading on straight spur gears 230
 loadings, Weir 193
 local acceleration of gravity 73
 local velocity 104
 locus branches 128
 locus, root 128
 logarithm, natural 164
 logarithms 22
 log growth 186
 logic operations 217
 logit models 174
 log mean temperature difference 120
 long chord 170
 longitudinal deformation, elastic 79
 longitudinal spacing 157
 longitudinal welds 157
 long-length columns, intermediate- and 233
 lossless transmission lines 205
 low-emissivity shield 122
 low molecular weight polymers 64
 low-pass filters (diagram) 210
 low-pass message 209
 lumped capacitance model 117
- M**
- machinery, fluid flow 108–110
 Mach number 107, 108, 110
 MACRS, modified accelerated cost recovery system 131
 magnetic fields 199
 magnetic flux density 199
 magnitude 66
 magnitude response 207
 Manning's equation 105, 166
 Manning's roughness coefficient 166
 manometers 103, 125
 manufacturability 232–233
 marine pollutant 8
 MARR, minimum acceptable rate-of-return 131
 mass 66
 mass balance, steady state 190
 mass density 104
 mass diffusivity 139
 mass flow rate 88, 103, 110
 mass flow rate of liquid 17
 mass of fluid within the system 88
 mass fraction 87
 mass of gas 86
 massless rod 77
 mass of liquid 86
 mass moment of inertia 76, 77
 mass radius of gyration 76
 mass transfer 139–141
 mass of vapor 86
 material condition (LMC), least 233
 material condition (MMC), maximum 233
 material handling 223
 material properties (table) 83
 materials, brittle 234
 materials, crystalline 59
 materials, ductile 234
 materials, mechanics of 79–85
 materials, properties of 59
 materials science 59–65
 mathematics 21–35
 matrices 33

- matrix of relation 21
 matrix transpose 33
 matter, structure of 59–65
 maximum material condition (MMC) 233
 maximum-normal-stress theory 234
 maximum power-transfer theorem 202
 maximum-shear-stress theory 234
 maxterm 218
 mean 36
 mean effective pressure (mep) 238
 mean temperature difference, log 120
 mean velocity 117
 measurement and controls, instrumentation 123–129
 measurement error 38
 measurement uncertainty 39, 126
 mechanical design 228–232
 mechanical efficiency 238
 mechanical engineering 228–240
 mechanical processing 59
 mechanical properties 61
 mechanical properties of typical engineering materials
 (table) 83
 mechanical springs 228
 mechanics of materials 79–85
 mechanisms, dynamics of 230
 median 36
 member fixed-end moments 151
 member, gross width of 157
 members, bolted 157
 member stiffness 231
 members, welded 157
 member thickness 157
 mensuration of areas and volumes 23–25
 message, low-pass 209
 messages, sampled 209
 metals, liquid 118
 metals, properties of (table) 60
 meter, coefficient of the 111
 meters, venturi 110
 method, inverse transform 221
 method joints, plane truss 67
 method sections, plane truss 67
 methods, numerical 35
 metric prefixes (table) 1
 microbial death rate 184
 microbial death ratio 190
 microbial kinetics 184
 middle ordinate 170
 mild steel, stress-strain curve for 79
 minimization, Newton's method of 35
 minimum acceptable rate-of-return (MARR) 131
 minimum detectable relative difference 188, 189 (table)
 minimum heat flux 119
 minterm 218
 mode 36
 model, gravity 174
 modeling, atmospheric dispersion 178
 modeling, population 187
 model, lumped capacitance 117
 Model Rules 3–4
 models, logit 174
 models, queueing 219–220
 modified accelerated cost recovery system (MACRS) 131
 modified Goodman theory 234
 modifier, project size (table) 176
 modular ratio 82
 modulation (AM), amplitude 208
 modulation, angle 208
 modulation (DSB), double-sideband 208
 modulation (FM), frequency 209
 modulation index 208
 modulation, (PAM) pulse-amplitude 209
 modulation (PCM), pulse-code 209
 modulation (SSB), single-sideband 208
 modulus 61, 64
 modulus, bulk 111
 modulus of elasticity 61, 79, 80, 83 (tables)
 modulus, shear 79, 80
 modulus, Young's 61, 62, 79, 232, 233
 Mohr's circle 80
 mol 53
 molality of solutions 53
 molar air-fuel ratio 91
 molar flux 139
 molar heat capacity 90
 molarity of solutions 53
 molar volume of an ideal gas 53
 molecular diffusion 139
 molecular formulas with molecular weight (table) 195
 molecular weight 87, 109, 178
 mole fraction 87, 91
 mole fraction of a substance 53
 moment, absolute maximum 151
 moment, aerodynamic 112
 moment of area 66
 moment, available (table) 160
 moment, bending 81
 moment carryover 151
 moment coefficient 112
 moment frame (chart) 161
 moment of inertia 29, 66–67, 68–70 (table), 81, 82, 103
 moment of inertia formulas for some standard shapes
 (table) 78
 moment of inertia, mass 76, 77, 78 (table)
 moment of inertia parallel axis theorem 67
 moment of momentum 74
 moments 66
 moments, member fixed-end 151
 moment strength, design 154
 momentum 76 106, 142
 momentum, angular 74
 momentum, angular impulse and 76
 momentum, conservation of angular 76
 momentum depth diagram (figure) 166

momentum, impulse and 74
 momentum, moment of 74
 momentum principle, impulse- 106–107
 momentum transfer 142
 monitoring 188–189
 monod growth rate constant 185
 monod kinetics 184
 monomers 64
 Moody diagram 105
 Moody friction factor 105, 142
 Moody (Stanton) diagram 114
 MOSFET, enhancement (table) 216
 motion about a fixed axis, rigid body 76
 motion about an instant center 76
 motion, equations of 76
 motion, particle curvilinear 71
 motion of a particle, one-dimensional 73
 motion, particle rectilinear 71
 motion, planar 71
 motion, plane circular 72
 motion, projectile 73
 motion, relative 71
 motion of a rigid body, plane 75
 motor efficiency 108
 moving average 221
 moving average, exponentially weighted 221
 moving blade 107
 multipath pipeline 106
 multiplication of two matrices 33
 municipal wastewater (table) 190
 Murphree plate efficiency 141
 music wire (table) 228

N

NAND gate 217
 natural (free) convection 120
 natural logarithm 164
 N-channel junction field effect transistors (JFETs) and depletion
 MOSFETs (low and medium frequency) (table) 215
 negative feedback control system 126
 negative ion 58
 net area 157
 net positive suction head available 108
 network equations, two-port (table) 203
 network optimization 219
 network, two-port 203
 Newtonian fluid 104
 Newtonian fluid film 102
 Newton's law of cooling 116
 Newton's method of minimization 35
 Newton's method for root extraction 35
 Newton's second law 19, 73, 75
 NIOSH formula 18
 noise exposure 20
 noise pollution 20
 nominal annual interest rate 130
 nominal hole diameter 157

nominal resistance 124
 nominal shear strength 154
 nominal value for head loss 105
 noncarcinogens 13
 non-Newtonian fluid, power law 102
 nonzero principal stresses 80
 NOR gate 217
 normal acceleration 71, 72
 normal distribution 38, 41 (table), 42 (table), 45 (table)
 normal distribution, confidence interval 43
 normality of solutions 53
 normal shock relationships 108
 normal and tangential components 72
 normal and tangential kinetics for planar problems 73
 Norton equivalent 200
 NPN bipolar junction transistor (BJT) (table) 214
 nucleate boiling 118, 119
 number
 atomic 53, 54 (table)
 binary number system 217
 Cauchy 111
 curve number 164
 Froude 111, 166
 Mach 107, 108, 110
 Nusselt 117, 142
 Prandtl 117, 119, 142
 Rayleigh 120
 Reynolds 104, 105, 111, 114 (table), 115 (graph), 142
 Schmidt 142
 Sherwood 139, 142
 Stanton 142
 system, binary number 217
 systems and codes, number 217
 Weber 111
 numerical integration 35
 numerical methods 35
 numerical solution of ordinary differential equations 35
 Nusselt number 117, 142
 Nyquist frequency 126, 209
 Nyquist's (Shannon's) sampling theorem 126

O

one-dimensional fluid flow 103–104
 one-dimensional motion of a particle 73
 one-way analysis of variance 39
 one-way ANOVA table 40
 opaque body 121
 open-channel flow 105, 166
 open-loop transfer function 126, 127
 open-system exergy 90
 open systems, special cases of 88
 open thermodynamic system 88
 operational amplifiers 212
 ordinary differential equations, numerical solution of 35
 organic carbon partition coefficient 185
 organic chemicals (table) 57
 organic chemistry 55–57

- organic compounds, families of (table) 56
 orifice coefficient 111
 orifice discharging freely into atmosphere 106
 orifice opening 106
 orifices 111
 orifice, submerged 106
 OSHA 5, 9, 20
 osmosis, reverse 196
 osmotic pressure 196
 Otto cycle 89, 98 (diagram)
 overall coefficients 139
 overburden pressure 187
 oxidation, anode reaction 59
 oxidation potentials (table) 58
- P**
- packed bed 106
 pairs, Fourier transform (table) 32
 pairs, Laplace transform (table) 33
 (PAM) pulse-amplitude modulation 209
 parabola 23, 25
 parabola constant 171
 paraboloid of revolution 25
 parallel-axis theorem 67, 76
 parallel centroidal axis 67
 parallel flow 120
 parallel flow concentric tube heat exchanger 121
 parallelogram 24
 parallel plate capacitor 59, 200
 parallel, resistors in series and 200
 parallel resonance 202
 parallel and series, capacitors and inductors in 201
 parameters, two-port 203
 Parseval's theorem 207
 particle bed 106
 particle curvilinear motion 71
 particle kinematics 71–73
 particle kinetics 73–75
 particle rectilinear motion 71
 partition coefficient 185
 pavement design, highway 172
 payback period 130
 PCM, pulse-code modulation 209
 peak discharge 164
 peak heat flux 119
 performance-graded (PG) binder grading system (table) 173
 perimeter, wetted 166
 periodic table of elements 54
 period of vibration, undamped natural 77
 peritectic reaction 65
 peritectoid reaction 65
 permeability, coefficient of 145, 164, 187
 permittivity 59
 permutations 36
 pert 224
 pesticide toxicity categories (table) 10
- pH 53
 phase
 binary 65
 deviation 208
 equilibrium 59
 margin (PM) 127
 relations 92
 relationships 145
 response 207
 phase-lock loop 209
 phase transitions 92
 phasor transforms of sinusoids 201
 P-h diagram for refrigerant HFC-134a 95
 phenomena, transport 142
 photoelectric effect 59
 pH sensor 125
 pictograms, GHS and transport 7, 8
 PID controller 127
 piezoelectric effect 59
 piezometers 104, 125
 piezometer water columns 104
 pin fin 117
 pipe bends 107
 pipe fittings 105
 pipe flow 105
 pipeline, multipath 106
 pitch angle 67
 Pitot tube 110
 planar motion 71
 planar problems, normal and tangential kinetics for 73
 planar slip (diagram) 149
 plane circular motion 72
 plane frame 152
 plane motion of a rigid body 75–77
 plane stress 80
 planetary gearset 230
 plane truss 152
 plane truss: method of joints 67
 plane truss: method of sections 67
 plane wall conduction resistance 116
 plastically deforming 59
 plasticity index 145
 plasticizers 64
 plug-flow reactor (PFR) 138
 POHC, principal organic hazardous contaminant 183
 point of application 66
 Poisson input 220
 Poisson's ratio 79, 80, 83 (tables), 232
 polar coordinate system 22
 polar moment of inertia 66, 77
 pollution, air 178–183
 pollution, noise 20
 polygon, regular 24
 polymers 64
 polytropic process 88
 pool boiling 118

- population modeling 187
 population projection equations 187
 porosity 106, 1873
 porosity, effective 164
 position vector 71
 positive ion 58
 positive suction head available, net 108
 potential energy 73, 74, 104
 power 109, 110
 power, ac 203–204
 power, brake 238
 power, complex 203
 power and efficiency 74
 power, indicated 238
 Power law fluid 104
 power law index 102
 power law (non-Newtonian) fluid 102
 power plants, steam 239
 power, pump (brake) 108
 power screws 229
 power series 29
 power-transfer theorem, maximum 202
 power transmission 229–230
 power of the turbine 107
 Prandtl number 117, 119, 142
 precedence, CPM 176
 precipitation 164
 precipitator efficiency, electrostatic 183
 pre-exponential constant 61
 preferred fits (table) 232
 present worth (table) 130
 press/shrink fits 232
 pressure 86, 95 (diagram), 102, 103, 104, 110, 111, 139
 absolute 86, 102
 atmospheric 102, 103, 108
 center of 103
 drop 104, 105
 enthalpy diagram 95
 field 102
 force 111
 indicators 125
 loss 106
 overburden 187
 partial 87, 139
 rise 109, 110
 senders 125
 sensors 125
 transducers 125
 transmitters 125
 vapor 103
 vessel, cylindrical 79
 prevention, safety and 5
 primary bonds 59
 prime implicant 218
 principal organic hazardous contaminant (POHC) 183
 principal stresses 80
 principle, impulse-momentum 106–107
 principle of work and energy 74
 prismoid 24
 prismoidal formula 171
 probabilities, cumulative binomial (table) 49–50
 probability density function 37
 probability and density functions: means and variances (table) 52
 probability functions 37–38
 probability, general character of 36
 probability, law of compound or joint 37
 probability, laws of 36–37
 probability and statistics, engineering 36–52
 process capability 219
 processes 237
 processing, digital signal 206
 processing, mechanical 59
 processing, thermal 59
 process, isentropic 88, 90, 108
 process safety 11
 product activity, daughter 188
 product of inertia 67
 professional conduct 3–4
 progression, arithmetic 29
 progression, geometric 29
 projected area 105
 projectile motion 73
 projection, algebraic 187
 projection, linear 187
 project size modifier (table) 176
 propagation, catastrophic crack 61
 propagation of error 38, 39
 properties, mechanical 61
 properties of air 178
 properties of gases (table) 96
 properties of liquids (table) 96
 properties of materials 59
 properties of metals (table) 60
 properties of series 29
 properties, thermal 64
 properties of water (English units) (table) 113
 properties of water (SI metric units) (table) 113
 proportionality constant 59
 propulsion, jet 107
 propulsive force 107
 prototype system 111
 pseudo plastic 102
 psychrometric chart, ASHRAE (English units) 101
 psychrometric chart, ASHRAE (metric units) 100
 psychrometrics 89
 pulse-code modulation (PCM) 209
 pump 110, 240
 pump (brake) power 108
 pump, centrifugal 108
 pump efficiency 108
 pump inlet 108
 pump power equation 109
 purchased power 108

pure component fugacity 91
PVT behavior 86–87

Q

quadratic equation 21
quadric surface (sphere) 21
quality control, statistical 51
quenching 59
queueing models 219–220
queueing system 219

R

radial and transverse components 71
radiation 116, 121–122, 188
radiation intensity 188
radioactive half-life 188
radius 27
radius, critical insulation 116
radius of gyration 67
radius of gyration, least (table) 163
radius of gyration, mass 76
radius, hydraulic 167
radius vector 67
rainfall intensity 164
rainfall-runoff 164
random error, sum of squares of 222
randomized block design 221
random variables 37
random variate generation 221
Rankine 89
Rankine earth pressure coefficient 148
Rankine cycle 89, 98 (diagram)
range charts, statistical average and 51
Raoult's law for vapor-liquid equilibrium 91
rapid mix 195
rate heat transfer 88
rate of reaction 137
rate-of-return 131
rate work 88
ratio, compression 238
ratio, effective slenderness 156
ratio, humidity 89
ratio, microbial death 190
rational formula 164
ratio, sewage flow (graph) 165
ratio, turns 204
ratio, water-cement (W/C) 64
Rayleigh number 120
RC and RL transients 202
reactant, limiting 92
reaction, eutectic 65
reaction, eutectoid 65
reaction, first-order irreversible 137
reaction, heats of 90–91
reaction order 137
reaction peritectic, 65
reaction peritectoid, 65
reactions in parallel 138

reactions in series 138
reactions of shifting order 138
reactor, parameters, steady-state 186
real gas 87
reciprocity relations 121
recovery (stress relief) 59
recrystallization 59
rectangular channels 166
rectangular fin 117
rectified sine wave 201
rectifying line 141
rectilinear motion, particle 71
recycled sludge suspended solids concentration 190
recycle flow rate 190
recycle ratio 190
reduction in area 79
reduction, cathode reactions 59
reduction, live load 152
reel and paddle 195
reference dose 13
reflectivity 121
reflux ratio 140
refrigerant 86
refrigerant (diagram) 95
refrigerant HFC-134a 95
refrigeration 98 (diagram), 99
refrigeration cycles 89
regulatory agencies, safety (table) 5
reinforced concrete 152
ASTM standard reinforcing bars (table) 153
reinforcements 154
reinforcing bars, ASTM standard (table) 153
relative acceleration 71
relative compaction 145
relative density 145
relative humidity 89
relative motion 71
relative position 71
relative velocity 71
relative volatility 140
reliability 222
reradiating surface 122
residential exposure equations 15
resistance 59, 123
resistance factors 153
resistance, oxidation 64
resistance temperature detector (RTD) 123
resistance, thermal 116
resistive element 200
resistivity 59, 200
resistor 59
resistors in series and parallel 200
resolution of a force 66
resonance 202
restitution, coefficient of 74
resultant 66
retardation factor 185

retention, basin 164
 retention times, steady-state (table) 186
 reversed Carnot cycle (diagram) 98
 reverse osmosis 196
 revolution, paraboloid of 25
 Reynolds number 104, 105, 111, 114 (table), 115 (graph), 142
 right circular cone 24
 right circular cylinder 25
 rigid body, kinematics of a 75
 rigid body, kinetics of a 75
 rigid body, plane motion of a 75–77
 rigorous vapor-liquid equilibrium 91
 risk 130
 risk assessment/toxicology 12–13
 riveted joints loaded in shear, bolted and 231
 roller bearing, ball/ 229
 root locus 128
 roots 22
 Rose equation 194
 rotating axis 72
 rotation about an arbitrary fixed axis 76
 rotational speed 110
 rotation, instantaneous center of 75
 roughness coefficient 105, 166
 roughness coefficient, Manning's 166
 roughness factor 105
 Routh test 127
 runoff 164

S

safety 5–20
 confined space safety 11
 definition of 5
 electrical safety (table) 11
 fire/hazard diamond 5
 labeling of chemicals 6–10
 prevention 5
 safety/regulatory agencies (table) 5
 safety data sheets (SDS) 6, 9
 safety equations, traffic 175
 salt flux 196
 salvage value 130
 sample coefficient of variation 36
 sample correlation coefficient 39
 sample distributions 43
 sampled messages 209
 sample geometric mean 36
 sample root-mean-square value 36
 sample size 43
 sample standard deviation 36
 sample variance 36
 sampling 126, 188–189
 sampling frequency 126
 sampling rate 126
 sampling soils and solids, data quality objectives (DQO) for (table) 188
 sampling theorem, Nyquist's (Shannon's) 126

saturated boiling 118
 saturated liquid, specific volume of 86
 saturated temperature 119
 saturated vapor, specific volume of 86
 saturation line, phase transition 92
 saturation pressure 91
 saturation temperature 119
 scalar equations 73
 scaling laws 110
 Schmidt number 142
 screw thread 67
 SDS (safety data sheets) 6, 9
 second law of thermodynamics 90
 second moment of area 66
 second-order control system models 128
 second-order irreversible reaction 137
 sections, conic 25
 sedimentation basins (table) 193
 seepage velocity 164
 selectivity 92
 semiconductors, extrinsic (table) 61
 semicrystalline 64
 sensors, pressure 125
 series resonance 202
 servomotors 204
 settling equations 194
 severity rates 20
 sewage flow ratio curves (graph) 165
 sewers, circular (graph) 165
 shafts 229
 shape factor 121
 shapes dimensions and properties, W- (table) 158
 shapes, W 159 (AISC table), 160 (table)
 shear 156, 157
 shear modulus 79, 80
 shear modulus of elasticity 77
 shear strain 79, 80, 81
 shear strength, design 156
 shear strength, nominal 154
 shear stress 79, 80, 148 (diagram), 228
 shear stress at failure 148
 shear stresses 104
 shear stress, inplane 80
 shear stress-strain 79
 shear stress, transverse 81
 Sherwood number 139, 142
 shield, low-emissivity 122
 short columns 154
 shrink fits, press/ 232
 sidesway inhibited (chart) 161
 sidesway uninhibited (chart) 161
 sight distance related to curve length, vertical curves and horizontal curves (tables) 169
 signal change interval, vehicle 168
 signal conditioning 126
 signal processing, digital 206
 signal words on product labels 10

- similitude 111
 simple barometer 103
 simple or Rayleigh distillation, differential 140
 simply supported beam slopes and deflections (table) 84
 simply supported beams (table) 156
 Simpson's 1/3 rule 171
 simulation 221
 sine-cosine relations 201
 sines 22
 single degree-of-freedom 77
 single payment (table) 130
 single-sideband modulation (SSB) 208
 singly-reinforced beams 154
 sinusoidal voltage 201
 sinusoidal waveform 201
 sinusoids, phasor transforms of 201
 slant distance 103
 slenderness ratio 82
 slenderness ratio, effective 156
 slope (tables) 84, 85
 slope of energy grade line 105
 slope failure (diagram) 149
 slopes and deflections, cantilevered beam (table) 85
 slopes and deflections, simply supported beam (table) 84
 sludge, activated 190
 sludge production rate 190
 socioeconomic adjustment factor 174
 Soderberg theory 234
 soil classification, AASHTO (table) 149
 soil classification system (table) 150
 soil consolidation curve (graph) 146
 soil landfill cover water balance 187
 soils and solids, data quality objectives (DQO) for sampling (table) 188
 soil-water partition coefficient 185
 solid-liquid interface 118
 solids loading rate 190
 solid-state electronics 212–216
 solubility product 53
 sorption zone, depth of 192
 sound, speed of 107
 spacing, longitudinal 157
 spacing, stirrup (table) 154
 spacing, transverse 157
 span drag coefficient 112
 special cases of open systems 88
 special cases of steady-flow energy equation 89
 specific capacity 164
 specific discharge 164
 specific energy 166
 specific enthalpy 86
 specific entropy 86
 specific gravity 102
 specific gravity of soil solids 145
 specific heat 64, 109, 119
 specific humidity 89, 236
 specific internal energy 86
 specific internal energy of system 88
 specific volume 86, 91, 93 (table), 102
 specific volume change upon vaporization 86
 specific volume of saturated liquid 86
 specific volume of saturated vapor 86
 specific volume of a two-phase system 86
 specific weight 102
 specific weight of water at standard conditions 102
 speed, design 168
 speed of sound 107
 speed-torque curve 204
 speed, vehicle approach 168
 sphere 24
 sphere, quadric surface 21
 spiral transition length 168
 spring material (table) 228
 springs 228
 sprinkler discharge, fire 167
 sprinkler K factors 167
 square thread power screws 229
 SSB, single-sideband modulation 208
 stability 152
 stability, atmospheric (tables) 179, 181
 stability class (graph) 181
 stagnation pressure 110
 stagnation temperature 108
 standard deviation 36, 44, 51 (charts)
 standard deviations of a plume, horizontal (graph) 180
 standard deviations of a plume, vertical (graph) 180
 standard enthalpy change of reaction 92
 standard error of estimate 39
 standard time determination 223
 Stanton diagram 105
 Stanton friction factor 105
 Stanton number 142
 state diagram 21
 state, equations of (EOS) 87
 state functions 86
 states, limit 157
 state-variable control system models 128
 statically determinate truss 67
 static equilibrium 77
 static friction, coefficient of 67, 75
 static liquid 102–103
 static loading 229
 static loading failure theories 234
 static pressure 110
 statics 66–70
 static suction head 108
 static temperature 108
 statistical approximations (table) 51
 statistical average and range charts 51
 statistical quality control 51
 statistics, engineering probability and 36–52
 statistics, test 41 (table), 42 (table), 44
 steady-flow cycle 239
 steady-flow systems 88
 steady incompressible flow 104
 steady-state analysis 126

- steady-state error analysis 127
 steady-state gain 127, 128
 steady state mass balance 190
 steady-state reactor parameters 186
 steady-state retention times (table) 186
 steam power plants 239
 steam tables 93, 94
 steam trap 239
 steel components 156–163
 Stefan-Boltzmann constant 1, 116, 121, 212
 stiffness, bolt 231
 stiffness, creep (table) 173
 stiffness, member 231
 stirrup spacing (table) 154
 stoichiometric coefficient 92
 stoichiometric combustion 91
 stoichiometric (theoretical) air-fuel ratio 91
 Stokes' law 194
 stopping sight distance 168
 storage coefficient 164
 storativity 164
 straight line depreciation 131
 straight line equation 21
 strain 59
 strain conditions (diagram) 153
 strain energy, elastic 82
 strain, engineering 59, 64, 79
 strain gage 124
 strain, shear 79, 80, 81
 strain, stress and 80
 strain, tensile 154
 strain, torsional 81
 strain, true 59
 strain, uniaxial stress- 79
 stream modeling 184
 Streeter Phelps 184
 strength, column 155
 strength, concrete 64
 strength design 152
 strength, design compressive 156
 strength, design flexural 156
 strength, design shear 156
 strength interaction diagram, column 155
 strength, nominal shear 154
 strength, temperature dependent 64
 strength, tensile 61, 62
 strength, yield 61, 83 (table)
 stress 61, 102, 104
 stress, applied engineering 61
 stress, critical 156, 162 (table)
 stress, elastic buckling 156
 stress, engineering 61
 stresses in beams 81
 stresses in spur gears 230
 stresses, nonzero principal 80
 stress intensity 61
 stress profiles and forces, horizontal 148
 stress profiles, vertical 148
 stress relief, recovery 59
 stress sensitivity 61
 stress, shear 79, 80 (diagram), 148 (diagram), 228
 stress and strain 80
 stress-strain curve for mild steel 79
 stress-strain, shear 79
 stress-strain, uniaxial 79
 stress, torsion 81
 stress, true 61
 stripping, air 192
 stripping line 141
 structural analysis 151
 structural design 152
 structural number equation, AASHTO 172
 structure of matter 59–65
 structures, classification of 152
 student's t-distribution (table) 46
 sub-chord 170
 sub-cooled boiling 118
 subcritical flow location 166
 submerged orifice 106
 submerged surfaces 103
 subsonic flows 108
 suction head available, net positive 108
 suction head, static 108
 suction pressure 109
 summation rule 121
 sum of squares of random error 222
 supercritical flow location 166
 superelevation 168
 superficial fluid velocity 106
 superficial velocity 164
 superpave 173
 superpave mixture design: compaction requirements (table) 174
 superplasticizers 64
 supersonic flows 108
 surface area 116, 117, 121
 surface area, convection 116
 surface force 102
 surface, reradiating 122
 surfaces, submerged 103
 surface stress vector 102
 surface temperature 119
 surface tension 102, 111, 119
 surface tension force 111
 sustainability 4
 sweep-through concentration change in a vessel 17
 switching function 218
 symbols, mathematic 21
 system pressure 91
- T**
- tangent distance 170
 tangential 73
 tangential acceleration 71, 72
 tangential components, normal and 72
 tangential kinetics for planar problems, normal and 73
 tangential stress components 102

- tangential velocity 72
 tangent offset 171
 taxation 131
 Taylor's series 29
 Taylor tool life formula 224
 t-distribution 38
 t-distribution, student's (table) 46
 temperature 139
 absolute 59, 61, 86, 89, 91, 92, 107, 116, 120, 121
 bulk fluid 116
 change in 64
 coefficient 123
 coefficient of expansion 79
 constant fluid 117
 conversions (table) 1
 corrections, kinetic 185
 curve, volume 64
 dependent strength 64
 dew-point 89
 entropy 89
 glass transition 64
 saturated water (table) 93
 saturation 119
 stagnation 108
 static 108
 variation 117
 wall surface 116
 wet bulb 89, 236
 tensile normal stress components 80
 tensile strain 154
 tensile strength 61, 62
 tensile test curve 61
 tension 59, 157
 tension members 157
 tension, surface 102, 111, 119
 terminal drift velocity 183
 test, Charpy impact 63
 test, impact 63
 test, Routh 127
 tests for out of control 51
 test statistics 41 (table), 42 (table), 44
 Theim equation 164
 theorem
 Bayes' 37
 Buckingham Pi 111
 central limit 38
 of corresponding states 87
 De Morgan's 217
 final value 126
 Fourier transform (table) 32
 maximum power-transfer 202
 moment of inertia parallel axis 67
 Nyquist's (Shannon's) sampling 126
 parallel-axis 67, 76
 Parseval's 207
 sampling 126
 thermal conductivity 116, 117, 119
 thermal deformations 79
 thermal efficiency, brake 238
 thermal efficiency, indicated 238
 thermal expansion coefficient 64
 thermal expansion, coefficient of 80, 83 (tables), 120
 thermal and physical property tables 96
 thermal processing 59
 thermal properties 64
 thermal resistance 116
 thermal voltage 212
 thermocouple (TC) 123
 thermodynamic cycles (diagrams) 98
 thermodynamics 86–101
 thermodynamics, first law of 87–89
 thermodynamics, second law of 90
 thermodynamic system 88
 thermoplastic polymer 64
 thermoplastics 64
 thermosets 64
 Thévenin equivalent 200
 thickness of fluid film 102
 thickness, member 157
 threaded fasteners 230, 231
 thread, screw 67
 3-LOG inactivation (table) 198
 threshold limit value (TLV) 13
 throttling processes 89
 throttling valves 89
 tied columns 154
 time, break-through 187
 time constant 127
 time factor, variation of 147
 TLV, threshold limit value 13
 tolerance values 123
 torque curve, speed- 204
 torsion 81
 torsional buckling, lateral- 156
 torsional stiffness 77
 torsional strain 81
 torsional vibration 77
 torsion stress 81
 total efficiency 109
 total head line 104
 toughness, fracture 61, 62 (table)
 toxicology, risk assessment 12–13
 traffic flow relationships 169
 traffic safety equations 175
 transducer 123
 transducer sensitivity 123
 transducers, pressure 125
 transfer coefficient, heat 120
 transfer function, open-loop 126, 127
 transfer, heat 116–122, 142, 236
 transfer, mass 139–141
 transfer units 121
 transformed section 82
 transformers (ideal) 204

transform, Fourier 30, 206
 transform pairs, Laplace (table) 33
 transforms, Laplace 33, 127, 129
 transient conduction 117
 transients, RC and RL 202
 transistor (BJT), NPN bipolar junction (table) 214
 transitional flow 104
 transition boiling 119
 transition length, spiral 168
 transitions, phase 92
 transition temperature 63
 transition temperature, glass 64
 transmission lines, lossless 205
 transmission, power 229–230
 transmissivity 121
 transmitters, pressure 125
 transport 184
 transportation 168–175
 transport phenomena 142
 transport pictograms 8
 transpose, matrix 33
 transverse components, radial and 71
 transverse shear stress 81
 transverse spacing 157
 transverse welds 157
 trapezoidal rule 171
 trap, steam (diagram) 239
 treatment, wastewater 190–191
 treatment, water 192–198
 trigonometric identities 23, 201
 trigonometry 22–23
 true strain 59
 true stress 61
 truss deflection 151
 trusses 151
 truss, plane 152
 truss, plane: method of joints 67
 truss, plane: method of sections 67
 truss, statically determinate 67
 turbine (diagrams) 98, 99
 turbine, adiabatic 110
 turbine, impulse 107
 turbine isentropic efficiency 110
 turbines 110
 turbines, gas 239
 turbulent flow 104, 106, 118
 turbulent flow impeller mixer 195
 turns ratio 204
 two-film theory 139
 two-force body in static equilibrium 67
 2^n factorial experiments 221
 two-phase (vapor-liquid) systems 86
 two-port network 203
 two-stage cycle, refrigeration and HVAC 99
 two-way ANOVA table 40

U

ultimate bearing capacity 148
 ultimate tensile strength 61
 ultrafiltration 196
 ultraviolet or visible light resistance 64
 unbraced segment 156
 uncertainty, measurement 126
 unconfined aquifer 164
 undamped natural frequency 77, 128
 uniaxial case 80
 uniaxial loading and deformation 79
 unidirectional diffusion of a gas A through a second
 stagnant gas B 139
 uniform flow 166
 uniform series (table) 130
 unimpaired mental performance (graph) 227
 unit hydrograph 164
 unit load method 150
 unit normal distribution (table) 45
 units of measure 1
 unit vectors 71
 universal gas constant 109, 139
 unsaturated acyclic hydrocarbons 55
 U.S. civilian body dimensions, female/male, for ages 20 to 60
 years (table) 225

V

vacuum gage 102
 vapor, film condensation of a pure 119
 vaporization 119
 vaporization rate 17
 vaporization, specific volume change upon 86
 vaporized liquid, concentration of 17
 vapor-liquid equilibrium (VLE) 91–92
 vapor, mass of 86
 vapor pressure 103, 113 (tables)
 variable angular acceleration 73
 variable loading failure theories 234–235
 variables, random 37
 variation of time factor with degree of consolidation (table) 147
 vector 34, 66
 vector quantities 72
 vehicle approach speed 168
 vehicle signal change interval 168
 velocity 71, 72, 88, 89, 104, 105, 106, 111, 112
 velocity at boundary condition 102
 velocity, coefficient of 110
 velocity, Darcy 164
 velocity, free stream 117
 velocity as a function of position 72
 velocity of plate on film 102
 velocity ratio 229
 velocity, seepage 164
 velocity, superficial 164
 velocity, tangential 72
 venturi meters 110

vertical curve formulas 171
 vertical curves (table) 169
 vertical distance 103, 104
 vertical standard deviations of a plume (graph) 180
 vertical stress 148
 vibration, free 77
 vibrations 235
 vibration, torsional 77
 vibration, undamped natural period of 77
 view factor 121
 virial EOS 87
 viruses (table) 197, 198
 viscosity 102, 104, 119
 viscosity, absolute 178
 viscosity, absolute dynamic 102
 viscosity, dynamic 104, 111, 117, 119
 viscous force 111
 visible light resistance, ultraviolet or 64
 V-notch 166
 void fraction 106
 voltage 59, 123, 199
 voltage, induced 199
 voltage, sinusoidal 201
 volume 86
 volume change 92
 volume, displacement 238
 volume fraction 62
 volume, humid 89
 volume, specific 86, 91, 102
 volume temperature curve 64
 volumetric flow 106, 109
 volumetric flow rate 103, 111
 volumetric gas flow rate 183

W

wall surface area 116
 wall surface temperature 116
 wall thickness 116
 waste sludge flow rate 190
 waste sludge suspended solids concentration 190
 wastewater, municipal (table) 190
 wastewater treatment 190–191
 water balance, soil landfill cover 187
 water-cement (W/C) ratio 64
 water flux 196
 water resources 164–167
 watershed area 164
 water treatment 192–198
 waveform, sinusoidal 201
 Weber number 111
 weight, concept of 73
 weighted arithmetic mean 36
 weight limit 18
 weight, molecular 87, 109, 178
 weight, specific 102, 103, 104, 107, 187
 weir formulas 145, 166
 weir loadings 193
 welded 157

welded members 157
 well drawdown 164
 wet bulb temperature 89, 236
 wet sludge density 190
 wetted perimeter 166
 wetted side 103
 Wheatstone bridge 125
 work 74, 87
 work energy 74
 work and energy, principle of 74
 working, cold 59
 working, hot 59
 work sampling formulas 224
 W shapes, AISI table 159
 W shapes available moment vs. unbraced length (table) 160
 W shapes, available strength in axial compression, kips (table) 163
 W-shapes dimensions and properties (table) 158

X

χ^2 - distribution 38
 χ^2 distribution, critical values of (table) 48

Y

yield 92
 yield coefficient 190
 yielding 157
 yield strength 61
 Young's modulus 61, 62, 79, 232, 233

Z

Zener diode 214
 zero lift 112
 zero-order irreversible reaction 137
 z-transforms 205

APPENDIX FE EXAM SPECIFICATIONS

Chemical	266
Civil.....	269
Electrical and Computer.....	273
Environmental	276
Industrial	279
Mechanical	282
Other Disciplines.....	286

**Fundamentals of Engineering (FE)
CHEMICAL CBT Exam Specifications**

Effective Beginning with the January 2014 Examinations

- The FE exam is a computer-based test (CBT). It is closed book with an electronic reference.
- Examinees have 6 hours to complete the exam, which contains 110 multiple-choice questions. The 6-hour time also includes a tutorial and an optional scheduled break.
- The FE exam uses both the International System of Units (SI) and the US Customary System (USCS).

Knowledge	Number of Questions
1. Mathematics A. Analytic geometry B. Roots of equations C. Calculus D. Differential equations	8–12
2. Probability and Statistics A. Probability distributions (e.g., discrete, continuous, normal, binomial) B. Expected value (weighted average) in decision making C. Hypothesis testing D. Measures of central tendencies and dispersions (e.g., mean, mode, standard deviation) E. Estimation for a single mean (e.g., point, confidence intervals) F. Regression and curve fitting	4–6
3. Engineering Sciences A. Applications of vector analysis (e.g., statics) B. Basic dynamics (e.g., friction, force, mass, acceleration, momentum) C. Work, energy, and power (as applied to particles or rigid bodies) D. Electricity and current and voltage laws (e.g., charge, energy, current, voltage, power, Kirchhoff, Ohm)	4–6
4. Computational Tools A. Numerical methods and concepts (e.g., convergence, tolerance) B. Spreadsheets for chemical engineering calculations C. Simulators	4–6
5. Materials Science A. Chemical, electrical, mechanical, and physical properties (e.g., effect of temperature, pressure, stress, strain) B. Material types and compatibilities (e.g., engineered materials, ferrous and nonferrous metals) C. Corrosion mechanisms and control	4–6

6. Chemistry	8-12
A. Inorganic chemistry (e.g., molarity, normality, molality, acids, bases, redox reactions, valence, solubility product, pH, pK, electrochemistry, periodic table)	
B. Organic chemistry (e.g., nomenclature, structure, qualitative and quantitative analyses, balanced equations, reactions, synthesis, basic biochemistry)	
7. Fluid Mechanics/Dynamics	8-12
A. Fluid properties	
B. Dimensionless numbers (e.g., Reynolds number)	
C. Mechanical energy balance (e.g., pipes, valves, fittings, pressure losses across packed beds, pipe networks)	
D. Bernoulli equation (hydrostatic pressure, velocity head)	
E. Laminar and turbulent flow	
F. Flow measurement (e.g., orifices, Venturi meters)	
G. Pumps, turbines, and compressors	
H. Compressible flow and non-Newtonian fluids	
8. Thermodynamics	8-12
A. Thermodynamic properties (e.g. specific volume, internal energy, enthalpy, entropy, free energy)	
B. Properties data and phase diagrams (e.g. steam tables, psychrometric charts, T-s, P-h, x-y, T-x-y)	
C. Thermodynamic laws (e.g., 1st law, 2nd law)	
D. Thermodynamic processes (e.g., isothermal, adiabatic, isentropic)	
E. Cyclic processes and efficiency (e.g., power, refrigeration, heat pump)	
F. Phase equilibrium (e.g., fugacity, activity coefficient)	
G. Chemical equilibrium	
H. Heats of reaction and mixing	
9. Material/Energy Balances	8-12
A. Mass balance (steady and unsteady state)	
B. Energy balance (steady and unsteady state)	
C. Recycle/bypass processes	
D. Reactive systems (e.g., combustion)	
10. Heat Transfer	8-12
A. Conductive heat transfer	
B. Convective heat transfer (natural and forced)	
C. Radiation heat transfer	
D. Heat transfer coefficients (e.g., overall, local, fouling)	
E. Heat transfer equipment, operation, and design (e.g., double pipe, shell and tube, fouling, number of transfer units, log-mean temperature difference, flow configuration)	
11. Mass Transfer and Separation	8-12
A. Molecular diffusion (e.g., steady and unsteady state, physical property estimation)	
B. Convective mass transfer (e.g., mass transfer coefficient, eddy diffusion)	
C. Separation systems (e.g., distillation, absorption, extraction, membrane processes)	

- D. Equilibrium stage methods (e.g., graphical methods, McCabe-Thiele, efficiency)
- E. Continuous contact methods (e.g., number of transfer units, height equivalent to a theoretical plate, height of transfer unit, number of theoretical plates)
- F. Humidification and drying

12. Chemical Reaction Engineering 8–12

- A. Reaction rates and order
- B. Rate constant (e.g., Arrhenius function)
- C. Conversion, yield, and selectivity
- D. Type of reactions (e.g., series, parallel, forward, reverse, homogeneous, heterogeneous, catalysis, biocatalysis)
- E. Reactor types (e.g., batch, semibatch, continuous stirred tank, plug flow, gas phase, liquid phase)

13. Process Design and Economics 8–12

- A. Process flow diagrams and piping and instrumentation diagrams
- B. Equipment selection (e.g., sizing and scale-up)
- C. Cost estimation
- D. Comparison of economic alternatives (e.g., net present value, discounted cash flow, rate of return, expected value and risk)
- E. Process design and optimization (e.g., sustainability, efficiency, green engineering, inherently safer design, evaluation of specifications)

14. Process Control 5–8

- A. Dynamics (e.g., time constants and 2nd order, underdamped, and transfer functions)
- B. Control strategies (e.g., feedback, feed-forward, cascade, ratio, and PID)
- C. Control loop design and hardware (e.g., matching measured and manipulated variables, sensors, control valves, and conceptual process control)

15. Safety, Health, and Environment 5–8

- A. Hazardous properties of materials (e.g., corrosivity, flammability, toxicity, reactivity, handling and storage), including MSDS
- B. Industrial hygiene (e.g., noise, PPE, ergonomics)
- C. Process safety and hazard analysis [e.g., layer of protection analysis, hazard and operability studies (HazOps), fault-tree analysis or event tree]
- D. Overpressure and underpressure protection (e.g., relief, redundant control, intrinsically safe)
- E. Waste minimization, waste treatment, and regulation (e.g., air, water, solids, RCRA, CWA, EPA, OSHA)

16. Ethics and Professional Practice 2–3

- A. Codes of ethics (professional and technical societies)
- B. Agreements and contracts
- C. Ethical and legal considerations
- D. Professional liability
- E. Public protection issues (e.g., licensing boards)

Fundamentals of Engineering (FE)
CIVIL CBT Exam Specifications

Effective Beginning with the January 2014 Examinations

- The FE exam is a computer-based test (CBT). It is closed book with an electronic reference.
- Examinees have 6 hours to complete the exam, which contains 110 multiple-choice questions. The 6-hour time also includes a tutorial and an optional scheduled break.
- The FE exam uses both the International System of Units (SI) and the US Customary System (USCS).

Knowledge	Number of Questions
1. Mathematics	7–11
A. Analytic geometry	
B. Calculus	
C. Roots of equations	
D. Vector analysis	
2. Probability and Statistics	4–6
A. Measures of central tendencies and dispersions (e.g., mean, mode, standard deviation)	
B. Estimation for a single mean (e.g., point, confidence intervals)	
C. Regression and curve fitting	
D. Expected value (weighted average) in decision making	
3. Computational Tools	4–6
A. Spreadsheet computations	
B. Structured programming (e.g., if-then, loops, macros)	
4. Ethics and Professional Practice	4–6
A. Codes of ethics (professional and technical societies)	
B. Professional liability	
C. Licensure	
D. Sustainability and sustainable design	
E. Professional skills (e.g., public policy, management, and business)	
F. Contracts and contract law	
5. Engineering Economics	4–6
A. Discounted cash flow (e.g., equivalence, PW, equivalent annual worth, FW, rate of return)	
B. Cost (e.g., incremental, average, sunk, estimating)	
C. Analyses (e.g., breakeven, benefit-cost, life cycle)	
D. Uncertainty (e.g., expected value and risk)	
6. Statics	7–11
A. Resultants of force systems	
B. Equivalent force systems	
C. Equilibrium of rigid bodies	
D. Frames and trusses	

- E. Centroid of area
- F. Area moments of inertia
- G. Static friction

7. Dynamics

4-6

- A. Kinematics (e.g., particles and rigid bodies)
- B. Mass moments of inertia
- C. Force acceleration (e.g., particles and rigid bodies)
- D. Impulse momentum (e.g., particles and rigid bodies)
- E. Work, energy, and power (e.g., particles and rigid bodies)

8. Mechanics of Materials

7-11

- A. Shear and moment diagrams
- B. Stresses and strains (e.g., axial, torsion, bending, shear, thermal)
- C. Deformations (e.g., axial, torsion, bending, thermal)
- D. Combined stresses
- E. Principal stresses
- F. Mohr's circle
- G. Column analysis (e.g., buckling, boundary conditions)
- H. Composite sections
- I. Elastic and plastic deformations
- J. Stress-strain diagrams

9. Materials

4-6

- A. Mix design (e.g., concrete and asphalt)
- B. Test methods and specifications (e.g., steel, concrete, aggregates, asphalt, wood)
- C. Physical and mechanical properties of concrete, ferrous and nonferrous metals, masonry, wood, engineered materials (e.g., FRP, laminated lumber, wood/plastic composites), and asphalt

10. Fluid Mechanics

4-6

- A. Flow measurement
- B. Fluid properties
- C. Fluid statics
- D. Energy, impulse, and momentum equations

11. Hydraulics and Hydrologic Systems

8-12

- A. Basic hydrology (e.g., infiltration, rainfall, runoff, detention, flood flows, watersheds)
- B. Basic hydraulics (e.g., Manning equation, Bernoulli theorem, open-channel flow, pipe flow)
- C. Pumping systems (water and wastewater)
- D. Water distribution systems
- E. Reservoirs (e.g., dams, routing, spillways)
- F. Groundwater (e.g., flow, wells, drawdown)
- G. Storm sewer collection systems

12. Structural Analysis

6-9

- A. Analysis of forces in statically determinant beams, trusses, and frames
- B. Deflection of statically determinant beams, trusses, and frames
- C. Structural determinacy and stability analysis of beams, trusses, and frames

- D. Loads and load paths (e.g., dead, live, lateral, influence lines and moving loads, tributary areas)
- E. Elementary statically indeterminate structures

13. Structural Design 6–9

- A. Design of steel components (e.g., codes and design philosophies, beams, columns, beam-columns, tension members, connections)
- B. Design of reinforced concrete components (e.g., codes and design philosophies, beams, slabs, columns, walls, footings)

14. Geotechnical Engineering 9–14

- A. Geology
- B. Index properties and soil classifications
- C. Phase relations (air-water-solid)
- D. Laboratory and field tests
- E. Effective stress (buoyancy)
- F. Stability of retaining walls (e.g., active pressure/pассив pressure)
- G. Shear strength
- H. Bearing capacity (cohesive and noncohesive)
- I. Foundation types (e.g., spread footings, deep foundations, wall footings, mats)
- J. Consolidation and differential settlement
- K. Seepage/flow nets
- L. Slope stability (e.g., fills, embankments, cuts, dams)
- M. Soil stabilization (e.g., chemical additives, geosynthetics)
- N. Drainage systems
- O. Erosion control

15. Transportation Engineering 8–12

- A. Geometric design of streets and highways
- B. Geometric design of intersections
- C. Pavement system design (e.g., thickness, subgrade, drainage, rehabilitation)
- D. Traffic safety
- E. Traffic capacity
- F. Traffic flow theory
- G. Traffic control devices
- H. Transportation planning (e.g., travel forecast modeling)

16. Environmental Engineering 6–9

- A. Water quality (ground and surface)
- B. Basic tests (e.g., water, wastewater, air)
- C. Environmental regulations
- D. Water supply and treatment
- E. Wastewater collection and treatment

17. Construction	4–6
A. Construction documents	
B. Procurement methods (e.g., competitive bid, qualifications-based)	
C. Project delivery methods (e.g., design-bid-build, design build, construction management, multiple prime)	
D. Construction operations and methods (e.g., lifting, rigging, dewatering and pumping, equipment production, productivity analysis and improvement, temporary erosion control)	
E. Project scheduling (e.g., CPM, allocation of resources)	
F. Project management (e.g., owner/contractor/client relations)	
G. Construction safety	
H. Construction estimating	
18. Surveying	4–6
A. Angles, distances, and trigonometry	
B. Area computations	
C. Earthwork and volume computations	
D. Closure	
E. Coordinate systems (e.g., state plane, latitude/longitude)	
F. Leveling (e.g., differential, elevations, percent grades)	

**Fundamentals of Engineering (FE)
ELECTRICAL AND COMPUTER CBT Exam Specifications**

Effective Beginning with the January 2014 Examinations

- The FE exam is a computer-based test (CBT). It is closed book with an electronic reference.
- Examinees have 6 hours to complete the exam, which contains 110 multiple-choice questions. The 6-hour time also includes a tutorial and an optional scheduled break.
- The FE exam uses both the International System of Units (SI) and the US Customary System (USCS).

Knowledge	Number of Questions
1. Mathematics	11–17
A. Algebra and trigonometry B. Complex numbers C. Discrete mathematics D. Analytic geometry E. Calculus F. Differential equations G. Linear algebra H. Vector analysis	
2. Probability and Statistics	4–6
A. Measures of central tendencies and dispersions (e.g., mean, mode, standard deviation) B. Probability distributions (e.g., discrete, continuous, normal, binomial) C. Expected value (weighted average) in decision making D. Estimation for a single mean (e.g., point, confidence intervals, conditional probability)	
3. Ethics and Professional Practice	3–5
A. Codes of ethics (professional and technical societies) B. NCEES Model Law and Model Rules C. Intellectual property (e.g., copyright, trade secrets, patents)	
4. Engineering Economics	3–5
A. Time value of money (e.g., present value, future value, annuities) B. Cost estimation C. Risk identification D. Analysis (e.g., cost-benefit, trade-off, breakeven)	
5. Properties of Electrical Materials	4–6
A. Chemical (e.g., corrosion, ions, diffusion) B. Electrical (e.g., conductivity, resistivity, permittivity, magnetic permeability) C. Mechanical (e.g., piezoelectric, strength) D. Thermal (e.g., conductivity, expansion)	

6. Engineering Sciences	6–9
A. Work, energy, power, heat	
B. Charge, energy, current, voltage, power	
C. Forces (e.g., between charges, on conductors)	
D. Work done in moving a charge in an electric field (relationship between voltage and work)	
E. Capacitance	
F. Inductance	
7. Circuit Analysis (DC and AC Steady State)	10–15
A. KCL, KVL	
B. Series/parallel equivalent circuits	
C. Thevenin and Norton theorems	
D. Node and loop analysis	
E. Waveform analysis (e.g., RMS, average, frequency, phase, wavelength)	
F. Phasors	
G. Impedance	
8. Linear Systems	5–8
A. Frequency/transient response	
B. Resonance	
C. Laplace transforms	
D. Transfer functions	
E. 2-port theory	
9. Signal Processing	5–8
A. Convolution (continuous and discrete)	
B. Difference equations	
C. Z-transforms	
D. Sampling (e.g., aliasing, Nyquist theorem)	
E. Analog filters	
F. Digital filters	
10. Electronics	7–11
A. Solid-state fundamentals (e.g., tunneling, diffusion/drift current, energy bands, doping bands, p-n theory)	
B. Discrete devices (diodes, transistors, BJT, CMOS) and models and their performance	
C. Bias circuits	
D. Amplifiers (e.g., single-stage/common emitter, differential)	
E. Operational amplifiers (ideal, non-ideal)	
F. Instrumentation (e.g., measurements, data acquisition, transducers)	
G. Power electronics	
11. Power	8–12
A. Single phase and three phase	
B. Transmission and distribution	
C. Voltage regulation	
D. Transformers	
E. Motors and generators	
F. Power factor (pf)	

12. Electromagnetics	5–8
A. Maxwell equations	
B. Electrostatics/magnetostatics (e.g., measurement of spatial relationships, vector analysis)	
C. Wave propagation	
D. Transmission lines (high frequency)	
E. Electromagnetic compatibility	
13. Control Systems	6–9
A. Block diagrams (feed-forward, feedback)	
B. Bode plots	
C. Closed-loop and open-loop response	
D. Controller performance (gain, PID), steady-state errors	
E. Root locus	
F. Stability	
G. State variables	
14. Communications	5–8
A. Basic modulation/demodulation concepts (e.g., AM, FM, PCM)	
B. Fourier transforms/Fourier series	
C. Multiplexing (e.g., time division, frequency division)	
D. Digital communications	
15. Computer Networks	3–5
A. Routing and switching	
B. Network topologies/frameworks/models	
C. Local area networks	
16. Digital Systems	7–11
A. Number systems	
B. Boolean logic	
C. Logic gates and circuits	
D. Logic minimization (e.g., SOP, POS, Karnaugh maps)	
E. Flip-flops and counters	
F. Programmable logic devices and gate arrays	
G. State machine design	
H. Data path/controller design	
I. Timing (diagrams, asynchronous inputs, races, hazards)	
17. Computer Systems	4–6
A. Architecture (e.g., pipelining, cache memory)	
B. Microprocessors	
C. Memory technology and systems	
D. Interfacing	
18. Software Development	4–6
A. Algorithms	
B. Data structures	
C. Software design methods (structured, object-oriented)	
D. Software implementation (e.g., procedural, scripting languages)	
E. Software testing	

**Fundamentals of Engineering (FE)
ENVIRONMENTAL CBT Exam Specifications**

Effective Beginning with the January 2014 Examinations

- The FE exam is a computer-based test (CBT). It is closed book with an electronic reference.
- Examinees have 6 hours to complete the exam, which contains 110 multiple-choice questions. The 6-hour time also includes a tutorial and an optional scheduled break.
- The FE exam uses both the International System of Units (SI) and the US Customary System (USCS).

Knowledge	Number of Questions
1. Mathematics	4–6
A. Analytic geometry B. Numerical methods C. Roots of equations D. Calculus E. Differential equations	
2. Probability and Statistics	3–5
A. Measures of central tendencies and dispersions (e.g., mean, mode, standard deviation) B. Probability distributions (e.g., discrete, continuous, normal, binomial) C. Estimation (point, confidence intervals) for a single mean D. Regression and curve fitting E. Expected value (weighted average) in decision making F. Hypothesis testing	
3. Ethics and Professional Practice	5–8
A. Codes of ethics (professional and technical societies) B. Agreements and contracts C. Ethical and legal considerations D. Professional liability E. Public protection issues (e.g., licensing boards) F. Regulations (e.g., water, wastewater, air, solid/hazardous waste, groundwater/soils)	
4. Engineering Economics	4–6
A. Discounted cash flow (e.g., life cycle, equivalence, PW, equivalent annual worth, FW, rate of return) B. Cost (e.g., incremental, average, sunk, estimating) C. Analyses (e.g., breakeven, benefit-cost) D. Uncertainty (expected value and risk)	
5. Materials Science	3–5
A. Properties (e.g., chemical, electrical, mechanical, physical) B. Corrosion mechanisms and controls C. Material selection and compatibility	

6. Environmental Science and Chemistry	11–17
A. Reactions (e.g., equilibrium, acid base, oxidation-reduction, precipitation)	
B. Stoichiometry	
C. Kinetics (chemical, microbiological)	
D. Organic chemistry (e.g., nomenclature, functional group reactions)	
E. Ecology (e.g., Streeter-Phelps, fluviology, limnology, eutrophication)	
F. Multimedia equilibrium partitioning (e.g., Henry's law, octanol partitioning coefficient)	
7. Risk Assessment	5–8
A. Dose-response toxicity (carcinogen, noncarcinogen)	
B. Exposure routes	
8. Fluid Mechanics	9–14
A. Fluid statics	
B. Closed conduits (e.g., Darcy-Weisbach, Hazen-Williams, Moody)	
C. Open channel (Manning)	
D. Pumps (e.g., power, operating point, parallel and series)	
E. Flow measurement (e.g., weirs, orifices, flowmeters)	
F. Blowers (e.g., power, operating point, parallel, and series)	
9. Thermodynamics	3–5
A. Thermodynamic laws (e.g., 1st law, 2nd law)	
B. Energy, heat, and work	
C. Ideal gases	
D. Mixture of nonreacting gases	
E. Heat transfer	
10. Water Resources	10–15
A. Demand calculations	
B. Population estimations	
C. Runoff calculations (e.g., land use, land cover, time of concentration, duration, intensity, frequency)	
D. Reservoir sizing	
E. Routing (e.g., channel, reservoir)	
F. Water quality and modeling (e.g., erosion, channel stability, stormwater quality management)	
11. Water and Wastewater	14–21
A. Water and wastewater characteristics	
B. Mass and energy balances	
C. Conventional water treatment processes (e.g., clarification, disinfection, filtration, flocculation, softening, rapid mix)	
D. Conventional wastewater treatment processes (e.g., activated sludge, decentralized wastewater systems, fixed-film system, disinfection, flow equalization, headworks, lagoons)	
E. Alternative treatment process (e.g., conservation and reuse, membranes, nutrient removal, ion exchange, activated carbon, air stripping)	
F. Sludge treatment and handling (e.g., land application, sludge digestion, sludge dewatering)	

12. Air Quality	10–15
A. Chemical principles (e.g., ideal gas, mole fractions, stoichiometry, Henry's law)	
B. Mass balances	
C. Emissions (factors, rates)	
D. Atmospheric sciences (e.g., stability classes, dispersion modeling, lapse rates)	
E. Gas handling and treatment technologies (e.g., hoods, ducts, coolers, biofiltration, scrubbers, adsorbers, incineration)	
F. Particle handling and treatment technologies (e.g., baghouses, cyclones, electrostatic precipitators, settling velocity)	
13. Solid and Hazardous Waste	10–15
A. Composting	
B. Mass balances	
C. Compatibility	
D. Landfilling (e.g., siting, design, leachate, material and energy recovery)	
E. Site characterization and remediation	
F. Hazardous waste treatment (e.g., physical, chemical, thermal)	
G. Radioactive waste treatment and disposal	
14. Groundwater and Soils	9–14
A. Basic hydrogeology (e.g., aquifers, permeability, water table, hydraulic conductivity, saturation, soil characteristics)	
B. Drawdown (e.g., Jacob, Theis, Thiem)	
C. Groundwater flow (e.g., Darcy's law, specific capacity, velocity, gradient)	
D. Soil and groundwater remediation	

**Fundamentals of Engineering (FE)
INDUSTRIAL CBT Exam Specifications**

Effective Beginning with the January 2014 Examinations

- The FE exam is a computer-based test (CBT). It is closed book with an electronic reference.
- Examinees have 6 hours to complete the exam, which contains 110 multiple-choice questions. The 6-hour time also includes a tutorial and an optional scheduled break.
- The FE exam uses both the International System of Units (SI) and the US Customary System (USCS).

Knowledge	Number of Questions
1. Mathematics	6–9
A. Analytic geometry B. Calculus C. Matrix operations D. Vector analysis E. Linear algebra	
2. Engineering Sciences	5–8
A. Work, energy, and power B. Material properties and selection C. Charge, energy, current, voltage, and power	
3. Ethics and Professional Practice	5–8
A. Codes of ethics and licensure B. Agreements and contracts C. Professional, ethical, and legal responsibility D. Public protection and regulatory issues	
4. Engineering Economics	10–15
A. Discounted cash flows (PW, EAC, FW, IRR, amortization) B. Types and breakdown of costs (e.g., fixed, variable, direct and indirect labor) C. Cost analyses (e.g., benefit-cost, breakeven, minimum cost, overhead) D. Accounting (financial statements and overhead cost allocation) E. Cost estimation F. Depreciation and taxes G. Capital budgeting	
5. Probability and Statistics	10–15
A. Combinatorics (e.g., combinations, permutations) B. Probability distributions (e.g., normal, binomial, empirical) C. Conditional probabilities D. Sampling distributions, sample sizes, and statistics (e.g., central tendency, dispersion) E. Estimation (e.g., point, confidence intervals) F. Hypothesis testing G. Regression (linear, multiple)	

- H. System reliability (e.g., single components, parallel and series systems)
- I. Design of experiments (e.g., ANOVA, factorial designs)

6. Modeling and Computations 8–12

- A. Algorithm and logic development (e.g., flow charts, pseudocode)
- B. Databases (e.g., types, information content, relational)
- C. Decision theory (e.g., uncertainty, risk, utility, decision trees)
- D. Optimization modeling (e.g., decision variables, objective functions, and constraints)
- E. Linear programming (e.g., formulation, primal, dual, graphical solutions)
- F. Mathematical programming (e.g., network, integer, dynamic, transportation, assignment)
- G. Stochastic models (e.g., queuing, Markov, reliability)
- H. Simulation

7. Industrial Management 8–12

- A. Principles (e.g., planning, organizing, motivational theory)
- B. Tools of management (e.g., MBO, reengineering, organizational structure)
- C. Project management (e.g., scheduling, PERT, CPM)
- D. Productivity measures

8. Manufacturing, Production, and Service Systems 8–12

- A. Manufacturing processes
- B. Manufacturing systems (e.g., cellular, group technology, flexible)
- C. Process design (e.g., resources, equipment selection, line balancing)
- D. Inventory analysis (e.g., EOQ, safety stock)
- E. Forecasting
- F. Scheduling (e.g., sequencing, cycle time, material control)
- G. Aggregate planning
- H. Production planning (e.g., JIT, MRP, ERP)
- I. Lean enterprises
- J. Automation concepts (e.g., robotics, CIM)
- K. Sustainable manufacturing (e.g., energy efficiency, waste reduction)
- L. Value engineering

9. Facilities and Logistics 8–12

- A. Flow measurements and analysis (e.g., from/to charts, flow planning)
- B. Layouts (e.g., types, distance metrics, planning, evaluation)
- C. Location analysis (e.g., single- and multiple-facility location, warehouses)
- D. Process capacity analysis (e.g., number of machines and people, trade-offs)
- E. Material handling capacity analysis
- F. Supply chain management and design

10. Human Factors, Ergonomics, and Safety 8–12

- A. Hazard identification and risk assessment
- B. Environmental stress assessment (e.g., noise, vibrations, heat)
- C. Industrial hygiene
- D. Design for usability (e.g., tasks, tools, displays, controls, user interfaces)
- E. Anthropometry
- F. Biomechanics
- G. Cumulative trauma disorders (e.g., low back injuries, carpal tunnel syndrome)

- H. Systems safety
- I. Cognitive engineering (e.g., information processing, situation awareness, human error, mental models)

11. Work Design 8-12

- A. Methods analysis (e.g., charting, workstation design, motion economy)
- B. Time study (e.g., time standards, allowances)
- C. Predetermined time standard systems (e.g., MOST, MTM)
- D. Work sampling
- E. Learning curves

12. Quality 8-12

- A. Six sigma
- B. Management and planning tools (e.g., fishbone, Pareto, QFD, TQM)
- C. Control charts
- D. Process capability and specifications
- E. Sampling plans
- F. Design of experiments for quality improvement
- G. Reliability engineering

13. Systems Engineering 8-12

- A. Requirements analysis
- B. System design
- C. Human systems integration
- D. Functional analysis and allocation
- E. Configuration management
- F. Risk management
- G. Verification and assurance
- H. System life-cycle engineering

**Fundamentals of Engineering (FE)
MECHANICAL CBT Exam Specifications**

Effective Beginning with the January 2014 Examinations

- The FE exam is a computer-based test (CBT). It is closed book with an electronic reference.
- Examinees have 6 hours to complete the exam, which contains 110 multiple-choice questions. The 6-hour time also includes a tutorial and an optional scheduled break.
- The FE exam uses both the International System of Units (SI) and the US Customary System (USCS).

Knowledge	Number of Questions
1. Mathematics	6–9
A. Analytic geometry B. Calculus C. Linear algebra D. Vector analysis E. Differential equations F. Numerical methods	
2. Probability and Statistics	4–6
A. Probability distributions B. Regression and curve fitting	
3. Computational Tools	3–5
A. Spreadsheets B. Flow charts	
4. Ethics and Professional Practice	3–5
A. Codes of ethics B. Agreements and contracts C. Ethical and legal considerations D. Professional liability E. Public health, safety, and welfare	
5. Engineering Economics	3–5
A. Time value of money B. Cost, including incremental, average, sunk, and estimating C. Economic analyses D. Depreciation	
6. Electricity and Magnetism	3–5
A. Charge, current, voltage, power, and energy B. Current and voltage laws (Kirchhoff, Ohm) C. Equivalent circuits (series, parallel) D. AC circuits E. Motors and generators	

7. Statics	8–12
A. Resultants of force systems	
B. Concurrent force systems	
C. Equilibrium of rigid bodies	
D. Frames and trusses	
E. Centroids	
F. Moments of inertia	
G. Static friction	
8. Dynamics, Kinematics, and Vibrations	9–14
A. Kinematics of particles	
B. Kinetic friction	
C. Newton's second law for particles	
D. Work-energy of particles	
E. Impulse-momentum of particles	
F. Kinematics of rigid bodies	
G. Kinematics of mechanisms	
H. Newton's second law for rigid bodies	
I. Work-energy of rigid bodies	
J. Impulse-momentum of rigid bodies	
K. Free and forced vibrations	
9. Mechanics of Materials	8–12
A. Shear and moment diagrams	
B. Stress types (axial, bending, torsion, shear)	
C. Stress transformations	
D. Mohr's circle	
E. Stress and strain caused by axial loads	
F. Stress and strain caused by bending loads	
G. Stress and strain caused by torsion	
H. Stress and strain caused by shear	
I. Combined loading	
J. Deformations	
K. Columns	
10. Material Properties and Processing	8–12
A. Properties, including chemical, electrical, mechanical, physical, and thermal	
B. Stress-strain diagrams	
C. Engineered materials	
D. Ferrous metals	
E. Nonferrous metals	
F. Manufacturing processes	
G. Phase diagrams	
H. Phase transformation, equilibrium, and heat treating	
I. Materials selection	
J. Surface conditions	
K. Corrosion mechanisms and control	
L. Thermal failure	

- M. Ductile or brittle behavior
- N. Fatigue
- O. Crack propagation

11. Fluid Mechanics	9–14
A. Fluid properties	
B. Fluid statics	
C. Energy, impulse, and momentum	
D. Internal flow	
E. External flow	
F. Incompressible flow	
G. Compressible flow	
H. Power and efficiency	
I. Performance curves	
J. Scaling laws for fans, pumps, and compressors	
12. Thermodynamics	13–20
A. Properties of ideal gases and pure substances	
B. Energy transfers	
C. Laws of thermodynamics	
D. Processes	
E. Performance of components	
F. Power cycles, thermal efficiency, and enhancements	
G. Refrigeration and heat pump cycles and coefficients of performance	
H. Nonreacting mixtures of gases	
I. Psychrometrics	
J. Heating, ventilating, and air-conditioning (HVAC) processes	
K. Combustion and combustion products	
13. Heat Transfer	9–14
A. Conduction	
B. Convection	
C. Radiation	
D. Thermal resistance	
E. Transient processes	
F. Heat exchangers	
G. Boiling and condensation	
14. Measurements, Instrumentation, and Controls	5–8
A. Sensors	
B. Block diagrams	
C. System response	
D. Measurement uncertainty	
15. Mechanical Design and Analysis	9–14
A. Stress analysis of machine elements	
B. Failure theories and analysis	
C. Deformation and stiffness	
D. Springs	
E. Pressure vessels	
F. Beams	
G. Piping	

- H. Bearings
- I. Power screws
- J. Power transmission
- K. Joining methods
- L. Manufacturability
- M. Quality and reliability
- N. Hydraulic components
- O. Pneumatic components
- P. Electromechanical components

**Fundamentals of Engineering (FE)
OTHER DISCIPLINES CBT Exam Specifications**

Effective Beginning with the January 2014 Examinations

- The FE exam is a computer-based test (CBT). It is closed book with an electronic reference.
- Examinees have 6 hours to complete the exam, which contains 110 multiple-choice questions. The 6-hour time also includes a tutorial and an optional scheduled break.
- The FE exam uses both the International System of Units (SI) and the US Customary System (USCS).

Knowledge	Number of Questions
1. Mathematics and Advanced Engineering Mathematics	12–18
A. Analytic geometry and trigonometry	
B. Calculus	
C. Differential equations (e.g., homogeneous, nonhomogeneous, Laplace transforms)	
D. Numerical methods (e.g., algebraic equations, roots of equations, approximations, precision limits)	
E. Linear algebra (e.g., matrix operations)	
2. Probability and Statistics	6–9
A. Measures of central tendencies and dispersions (e.g., mean, mode, variance, standard deviation)	
B. Probability distributions (e.g., discrete, continuous, normal, binomial)	
C. Estimation (e.g., point, confidence intervals)	
D. Expected value (weighted average) in decision making	
E. Sample distributions and sizes	
F. Goodness of fit (e.g., correlation coefficient, least squares)	
3. Chemistry	7–11
A. Periodic table (e.g., nomenclature, metals and nonmetals, atomic structure of matter)	
B. Oxidation and reduction	
C. Acids and bases	
D. Equations (e.g., stoichiometry, equilibrium)	
E. Gas laws (e.g., Boyle's and Charles' Laws, molar volume)	
4. Instrumentation and Data Acquisition	4–6
A. Sensors (e.g., temperature, pressure, motion, pH, chemical constituents)	
B. Data acquisition (e.g., logging, sampling rate, sampling range, filtering, amplification, signal interface)	
C. Data processing (e.g., flow charts, loops, branches)	
5. Ethics and Professional Practice	3–5
A. Codes of ethics	
B. NCEES <i>Model Law</i>	
C. Public protection issues (e.g., licensing boards)	

6. Safety, Health, and Environment	4–6
A. Industrial hygiene (e.g., carcinogens, toxicology, MSDS, lower exposure limits)	
B. Basic safety equipment (e.g., pressure relief valves, emergency shut-offs, fire prevention and control, personal protective equipment)	
C. Gas detection and monitoring (e.g., O ₂ , CO, CO ₂ , CH ₄ , H ₂ S, Radon)	
D. Electrical safety	
7. Engineering Economics	7–11
A. Time value of money (e.g., present worth, annual worth, future worth, rate of return)	
B. Cost (e.g., incremental, average, sunk, estimating)	
C. Economic analyses (e.g., breakeven, benefit-cost, optimal economic life)	
D. Uncertainty (e.g., expected value and risk)	
E. Project selection (e.g., comparison of unequal life projects, lease/buy/make, depreciation, discounted cash flow)	
8. Statics	8–12
A. Resultants of force systems and vector analysis	
B. Concurrent force systems	
C. Force couple systems	
D. Equilibrium of rigid bodies	
E. Frames and trusses	
F. Area properties (e.g., centroids, moments of inertia, radius of gyration)	
G. Static friction	
9. Dynamics	7–11
A. Kinematics	
B. Linear motion (e.g., force, mass, acceleration)	
C. Angular motion (e.g., torque, inertia, acceleration)	
D. Mass moment of inertia	
E. Impulse and momentum (linear and angular)	
F. Work, energy, and power	
G. Dynamic friction	
H. Vibrations	
10. Strength of Materials	8–12
A. Stress types (e.g., normal, shear, bending, torsion)	
B. Combined stresses	
C. Stress and strain caused by axial loads, bending loads, torsion, or shear	
D. Shear and moment diagrams	
E. Analysis of beams, trusses, frames, and columns	
F. Deflection and deformations (e.g., axial, bending, torsion)	
G. Elastic and plastic deformation	
H. Failure theory and analysis (e.g., static/dynamic, creep, fatigue, fracture, buckling)	

11. Materials Science	6–9
A. Physical, mechanical, chemical, and electrical properties of ferrous metals	
B. Physical, mechanical, chemical, and electrical properties of nonferrous metals	
C. Physical, mechanical, chemical, and electrical properties of engineered materials (e.g., polymers, concrete, composites)	
D. Corrosion mechanisms and control	
12. Fluid Mechanics and Dynamics of Liquids	8–12
A. Fluid properties (e.g., Newtonian, non-Newtonian)	
B. Dimensionless numbers (e.g., Reynolds number, Froude number)	
C. Laminar and turbulent flow	
D. Fluid statics	
E. Energy, impulse, and momentum equations (e.g., Bernoulli equation)	
F. Pipe flow and friction losses (e.g., pipes, valves, fittings, Darcy-Weisbach equation, Hazen-Williams equation)	
G. Open-channel flow (e.g., Manning equation, drag)	
H. Fluid transport systems (e.g., series and parallel operations)	
I. Flow measurement	
J. Turbomachinery (e.g., pumps, turbines)	
13. Fluid Mechanics and Dynamics of Gases	4–6
A. Fluid properties (e.g., ideal and non-ideal gases)	
B. Dimensionless numbers (e.g., Reynolds number, Mach number)	
C. Laminar and turbulent flow	
D. Fluid statics	
E. Energy, impulse, and momentum equations	
F. Duct and pipe flow and friction losses	
G. Fluid transport systems (e.g., series and parallel operations)	
H. Flow measurement	
I. Turbomachinery (e.g., fans, compressors, turbines)	
14. Electricity, Power, and Magnetism	7–11
A. Electrical fundamentals (e.g., charge, current, voltage, resistance, power, energy)	
B. Current and voltage laws (Kirchhoff, Ohm)	
C. DC circuits	
D. Equivalent circuits (series, parallel, Norton's theorem, Thevenin's theorem)	
E. Capacitance and inductance	
F. AC circuits (e.g., real and imaginary components, complex numbers, power factor, reactance and impedance)	
G. Measuring devices (e.g., voltmeter, ammeter, wattmeter)	

15. Heat, Mass, and Energy Transfer**9–14**

- A. Energy, heat, and work
- B. Thermodynamic laws (e.g., 1st law, 2nd law)
- C. Thermodynamic equilibrium
- D. Thermodynamic properties (e.g., entropy, enthalpy, heat capacity)
- E. Thermodynamic processes (e.g., isothermal, adiabatic, reversible, irreversible)
- F. Mixtures of nonreactive gases
- G. Heat transfer (e.g., conduction, convection, and radiation)
- H. Mass and energy balances
- I. Property and phase diagrams (e.g., T-s, P-h)
- J. Phase equilibrium and phase change
- K. Combustion and combustion products (e.g., CO, CO₂, NO_x, ash, particulates)
- L. Psychrometrics (e.g., relative humidity, wet-bulb)