

# CH365 Chemical Engineering Thermodynamics

## Lesson 34

### Chemical Potential and Partial Properties

Block 6 – Solution Thermodynamics

# Example 10.1

The partial molar volume is defined as

$$\bar{V}_i \equiv \left[ \frac{\partial(nV)}{\partial n_i} \right]_{P,T,n_j} \quad (\text{A, page 362})$$

What physical interpretation can be given to this equation?

It is the volume of “i” as it exists in solution.

Consider the total volume of an equimolar solution of alcohol and water:

$$nV (= V^{\text{TOT}}) \quad \text{at } T \text{ and } P$$

Add pure water also at T and P containing  $\Delta n_w$ .

Allow it to mix thoroughly and re-equilibrate.

What is the change in total volume?

$$\Delta(nV) \stackrel{?}{=} V_w \Delta n_w \quad \text{experiments show this is not true}$$

$$\Delta(nV) = \bar{V}_w \Delta n_w \quad \text{we need to change the molar property}$$



effective molar volume of water in solution

# Overview

Theoretical foundations for the study of gas mixtures and liquid solutions

- Relevant to mixing, separations, and chemical reactions
- Along with T and P, compositions are essential variables

Fundamental property relationship was developed earlier.

$$dG = VdP - SdT$$

(L27 slide 8, eq. 6.11 p. 212  
and PS10 problem 6.1b)

needs to be more  
comprehensive

- Extend to open systems with variable composition
- Define *chemical potential*
  - Phase equilibria and chemical equilibria
- Define *partial molar properties* (derived this lesson)
  - Not the same as molar properties of pure components.
  - Properties of individual species as they exist in solution
  - Composition-dependent.
  - Used to build equations for solution properties
- Define *fugacity*
  - Improvement over models based on chemical potential
- Define *excess properties*
  - Concept of *ideal solution model* as a reference, like ideal gases
  - The *excess Gibbs energy* is the basis for activity and activity coefficients

## Review from Lesson 27 (derivation of fundamental relations and Maxwell's equations):

(Eq. 2.6, 1<sup>st</sup> Law, closed system, reversible)

$$d(nU) = dQ + dW$$

$dQ_{\text{rev}} = TdS^t$   
(Eq. 5.1)

$dQ_{\text{rev}} = Td(nS)$

$dW_{\text{rev}} = -Pd(nV)$

$dW_{\text{rev}} = -PdV^t$   
(Eq. 1.3)

$$d(nU) = Td(nS) - Pd(nV) \quad (\text{Eq. 6.1})$$

$$dU = TdS - PdV$$

n=1 or const. comp. (Eq. 6.7)

- Not restricted to reversible processes
- **System must be closed, and**
- **Change must be between equilibrium states.**

- Includes primary properties: U, S, T, P, and V

Additional properties arise by definition:

Enthalpy:  $H \equiv U + PV$  (Eq. 2.10 and 6.2)

Helmholtz Energy:  $A \equiv U - TS$  (Eq. 6.3)

Gibbs Energy:  $G \equiv H - TS$  (Eq. 6.4)

# Fundamental Property Relations

**General equations for a homogenous fluid of constant composition.**

$dU = TdS - PdV$ <p>(Eq.6.8)</p>	$dH = TdS + VdP$ <p>(Eq. 6.9)</p>
$dA = -PdV - SdT$ <p>(Eq. 6.10)</p>	$dG = VdP - SdT$ <p>(Eq. 6.11)</p>

Lesson 27, Slide 8

Instructor derived 6.8 and 6.9

Cadets derived 6.10 and 6.11  
in problem 6.1 of PS10

$$d(nG) = (nV)dP - (nS)dT$$

(Eq. 6.7, page 216)

(Eq.6.7, page 216)

$$\therefore nV \equiv \left( \frac{\partial(nG)}{\partial P} \right)_{T,n} \quad \text{and} \quad \therefore nS \equiv - \left( \frac{\partial(nG)}{\partial T} \right)_{P,n}$$

$$\left(\frac{\partial V}{\partial T}\right)_P = -\left(\frac{\partial S}{\partial P}\right)_T$$

4<sup>th</sup> Maxwell Relation  
Slide 12 L27 or p. 218

$$d(nG) = \left( \frac{\partial(nG)}{\partial P} \right)_{T,n} dP + \left( \frac{\partial(nG)}{\partial T} \right)_{P,n} dT + \left( \frac{\partial(nG)}{\partial n_1} \right)_{P,T,n_{i \neq 1}} dn_1 + \left( \frac{\partial(nG)}{\partial n_2} \right)_{P,T,n_{i \neq 2}} dn_2 + \dots$$

$$\mu_i \equiv \left( \frac{\partial(nG)}{\partial n_i} \right)_{P,T,n_{j \neq i}} \quad (\text{Eq. 10.1, page 359})$$

# Fundamental Property Relation

## Modified to Include Chemical Potentials

$$d(nG) = (nV)dP - (nS)dT \quad (\text{Eq. 6.7, page 216})$$

$$d(nG) = (nV)dP - (nS)dT + \sum_i \mu_i dn_i \quad (\text{Eq. 10.2, page 359})$$

Special Case:  $n = 1$  mole of solution,  $n_i = x_i$

$$d(G) = V dP - S dT + \sum_i \mu_i dx_i \quad (\text{Eq. 10.3, page 359})$$

$$nG = g(T, P, x_1, x_2, \dots, x_i, \dots)$$

“Canonical” variables for  $G$  have changed. They are now  $T$ ,  $P$ , and  $x_i$ .

$$\left( \frac{\partial G}{\partial P} \right)_{T,x} = V$$

(Eq. 10.4)

$$-\left( \frac{\partial G}{\partial T} \right)_{P,x} = S$$

(Eq. 10.5)

$$\left( \frac{\partial G}{\partial x_i} \right)_{T,P} = \mu_i$$

(Eq. 10.1)

# Phase Equilibria

(Closed System)

$$d(nG) = (nV) dP - (nS) dT + \sum_i \mu_i dn_i \quad (\text{Eq. 10.2, page 359})$$

$$\text{Phase } \alpha: \quad d(nG)^\alpha = (nV)^\alpha dP - (nS)^\alpha dT + \sum_i \mu_i^\alpha dn_i^\alpha$$

$$\text{Phase } \beta: \quad d(nG)^\beta = (nV)^\beta dP - (nS)^\beta dT + \sum_i \mu_i^\beta dn_i^\beta$$

$$\text{Sum:} \quad d(nG) = (nV) dP - (nS) dT + \sum_i \mu_i^\alpha dn_i^\alpha + \sum_i \mu_i^\beta dn_i^\beta$$

$$d(nG) = (nV) dP - (nS) dT$$

(Eq. 6.1, page 216, still valid for closed system)

$$\text{Subtract:} \quad \sum_i \mu_i^\alpha dn_i^\alpha + \sum_i \mu_i^\beta dn_i^\beta = 0$$

$$dn_i^\alpha = -dn_i^\beta \quad \Rightarrow \quad \sum_i (\mu_i^\alpha - \mu_i^\beta) dn_i^\alpha = 0 \quad \Rightarrow \quad \therefore \mu_i^\alpha - \mu_i^\beta = 0$$

“Equilibrium Condition”

$$\therefore \mu_i^\alpha = \mu_i^\beta$$

(Eq. 10.6, page 361)

Very Important!



# Partial Molar Properties

Molar properties of individual species as they exist in solution

$$\bar{M}_i \equiv \left[ \frac{\partial(nM)}{\partial n_i} \right]_{P,T,n_{j \neq i}} \quad (\text{Eq. 10.7, page 361})$$

Response function – response of “nM” to addition of “dn<sub>i</sub>”

Total solution properties	M	V, U, H, S, G
Partial molar properties	$\bar{M}_i$	$\bar{V}_i, \bar{U}_i, \bar{H}_i, \bar{S}_i, \bar{G}_i$
Pure-species properties	$M_i$	$V_i, U_i, H_i, S_i, G_i$

Definition 10.7 gives partial molar properties from total molar property

We can reverse this and get total molar properties from partial molar properties (Problem 10.53b)

Partial molar Gibbs energy is the chemical potential:

$$\mu_i \equiv \left[ \frac{\partial(nG)}{\partial n_i} \right]_{P,T,n_{j \neq i}} \quad \longleftrightarrow \quad \bar{G}_i \equiv \mu_i$$

(Eq. 10.1, p. 359)  (Eq. 10.8, p. 362)

# Partial Molar Properties

Start with function “nM”

$$nM = nM(T, P, n_1, n_2, \dots, n_i, \dots) = \text{func}(T, P, n_1, n_2, \dots, n_i, \dots)$$

$$d(nM) = \left( \frac{\partial(nM)}{\partial P} \right)_{T,n} dP + \left( \frac{\partial(nM)}{\partial T} \right)_{P,n} dT + \sum_i \left( \frac{\partial(nM)}{\partial n_i} \right)_{T,P,n_{j \neq i}} dn_i$$

inserting equation 10.7 and assuming constant n yields:

$$\bar{M}_i \equiv \left[ \frac{\partial(nM)}{\partial n_i} \right]_{P,T,n_{j \neq i}} \quad (\text{Eq. 10.7})$$

$$d(nM) = n \left( \frac{\partial M}{\partial P} \right)_{T,x} dP + n \left( \frac{\partial M}{\partial T} \right)_{P,x} dT + \sum_i \bar{M}_i dn_i \quad (\text{Eq. 10.9, page 364})$$

$$d(nM) \xrightarrow{\text{product rule}}$$

$$d(nM) = n dM + M dn$$

$$n_i = x_i n \xrightarrow{\text{product rule}}$$

$$dn_i = d(x_i n) = x_i dn + n dx_i$$

$$n dM + M dn = n \left( \frac{\partial M}{\partial P} \right)_{T,x} dP + n \left( \frac{\partial M}{\partial T} \right)_{P,x} dT + \sum_i \bar{M}_i (x_i dn + n dx_i)$$

$$\sum_i \bar{M}_i (x_i dn + n dx_i) = dn \sum_i \bar{M}_i x_i + n \sum_i \bar{M}_i dx_i$$

collect terms  
by n and dn:

$$\left[ dM - \left( \frac{\partial M}{\partial P} \right)_{T,x} dP - \left( \frac{\partial M}{\partial T} \right)_{P,x} dT - \sum_i \bar{M}_i dx_i \right] n + \left[ M - \sum_i \bar{M}_i x_i \right] dn = 0$$

Terms in brackets must each be zero.

# Partial Molar Properties – Gibbs/Duhem

(1<sup>st</sup> term in brackets)

$$dM - \left( \frac{\partial M}{\partial P} \right)_{T,x} dP - \left( \frac{\partial M}{\partial T} \right)_{P,x} dT - \sum_i \bar{M}_i dx_i = 0 \quad \Rightarrow \quad dM = \left( \frac{\partial M}{\partial T} \right)_{P,x} dT + \left( \frac{\partial M}{\partial P} \right)_{T,x} dP + \sum_i \bar{M}_i dx_i \quad (A)$$

(Eq. 10.10, page 364)

(2<sup>nd</sup> term in brackets)

$$M - \sum_i \bar{M}_i x_i = 0$$

(homework and slide 12)

$$M = \sum_i x_i \bar{M}_i \quad (\text{Eq. 10.11})$$

$$\text{or } nM = \sum_i n_i \bar{M}_i \quad (\text{Eq. 10.12})$$

subtract  
(A) – (B)

take derivative  
using product rule

$$dM = \sum_i x_i d\bar{M}_i + \sum_i \bar{M}_i dx_i \quad (B)$$

$$dM = \left( \frac{\partial M}{\partial T} \right)_{P,x} dT + \left( \frac{\partial M}{\partial P} \right)_{T,x} dP + \sum_i \bar{M}_i dx_i \quad (A)$$

$$- \quad dM = \sum_i x_i d\bar{M}_i + \sum_i \bar{M}_i dx_i \quad (B)$$

(homework and slide 12)

Constant T and P:

$$\sum_i x_i d\bar{M}_i = 0$$

(Eq. 10.14 p.365)

(homework)

$$0 = \left( \frac{\partial M}{\partial P} \right)_{T,x} dP + \left( \frac{\partial M}{\partial T} \right)_{P,x} dT - \sum_i x_i d\bar{M}_i \quad (\text{Eq. 10.13, page 365})$$

Gibbs-Duhem Equation  
(famous)

# Special Case – Binary Systems

Slide 12

Eq. 10.11 (slide 11) for 2 components  $M = x_1 \bar{M}_1 + x_2 \bar{M}_2$

Differentiate using the product rule

$$dM = x_1 d\bar{M}_1 + \bar{M}_1 dx_1 + x_2 d\bar{M}_2 + \bar{M}_2 dx_2$$

Eq 10.14, (slide 11) for 2 components:

$$x_1 d\bar{M}_1 + x_2 d\bar{M}_2 = 0$$

Rearrange

$$dM = (\bar{M}_1 dx_1 + \bar{M}_2 dx_2) + (x_1 d\bar{M}_1 + x_2 d\bar{M}_2)$$

sum of mole fractions

$$x_1 + x_2 = 1$$

$$x_2 = 1 - x_1$$

$$dx_2 = -dx_1$$

$$dM = \bar{M}_1 dx_1 - \bar{M}_2 dx_1$$

$$dM = (\bar{M}_1 - \bar{M}_2) dx_1$$

$$\frac{dM}{dx_1} = \bar{M}_1 - \bar{M}_2$$

$$x_1 = 1 - x_2$$

$$M = x_1 \bar{M}_1 + x_2 \bar{M}_2 = (1 - x_2) \bar{M}_1 + x_2 \bar{M}_2 = \bar{M}_1 + x_2 (\bar{M}_2 - \bar{M}_1) = \bar{M}_1 - x_2 \left( \frac{dM}{dx_1} \right)$$

$$\bar{M}_1 = M + x_2 \left( \frac{dM}{dx_1} \right) \quad (\text{Eq. 10.15})$$

(homework)

$$M = x_1 \bar{M}_1 + x_2 \bar{M}_2 = x_1 \bar{M}_1 + (1 - x_1) \bar{M}_2 = \bar{M}_2 + x_1 (\bar{M}_1 - \bar{M}_2) = \bar{M}_2 + x_1 \left( \frac{dM}{dx_1} \right)$$

$$\bar{M}_2 = M - x_1 \left( \frac{dM}{dx_1} \right) \quad (\text{Eq. 10.16})$$

(homework)

# Summary of Equations Needed for Homework

(Eq. 10.11)

$$M = \sum_i x_i \bar{M}_i$$

(Eq. 10.14)

$$\sum_i x_i d\bar{M}_i = 0$$

Gibbs-Duhem Equation  
at constant T and P:

(Eq. 10.15)

$$\bar{M}_1 = M + x_2 \left( \frac{dM}{dx_1} \right)$$

(Eq. 10.16)

$$\bar{M}_2 = M - x_1 \left( \frac{dM}{dx_1} \right)$$

# Questions?

# Problem 10.53

The molar volume ( $\text{cm}^3 \text{mol}^{-1}$ ) of a binary liquid mixture at T and P is given by:

$$V = 120x_1 + 70x_2 + (15x_1 + 8x_2)x_1x_2$$

- (a) Find expressions for the partial molar volumes of species 1 and 2 in terms of  $x_1$ .
- (b) Show that the given equation for V is recovered when these expressions are combined using Eq. 10.11.
- (c) Show that these expressions satisfy Eq. 10.14.
- (d) Show that  $\left(d\bar{V}_1 / dx_1\right)_{x_1=1} = \left(d\bar{V}_2 / dx_1\right)_{x_1=0} = 0$ .
- (e) Make a plot of  $V$ ,  $\bar{V}_1$ , and  $\bar{V}_2$  versus  $x_1$ .
- (f) Label points  $V_1$ ,  $V_2$ ,  $\bar{V}_1^{x_1 \rightarrow 0}$  and  $\bar{V}_2^{x_2 \rightarrow 0}$ , and show their values.

Use file “PlotExampleCadet.nb” in Canvas for part (f).

# Homework

## Manipulation of $d\bar{M}_i$ in Equation 10.14

$$\sum_i x_i d\bar{M}_i = 0 \quad (\text{Eq. 10.14})$$

Gibbs-Duhem Equation  
at constant T and P:

$$d\bar{M}_i = ?$$

$$\bar{V}_1 = 128 - 2x_1 - 20x_1^2 + 14x_1^3$$

$$d\bar{V}_1 = d(128 - 2x_1 - 20x_1^2 + 14x_1^3)$$

$$d\bar{V}_1 = d(128) - d(2x_1) - d(20x_1^2) + d(14x_1^3)$$

$$d\bar{V}_1 = d(128) - 2dx_1 - (20)(2)x_1dx_1 + (14)(3)x_1^2dx_1$$

$$d\bar{V}_1 = (-2 - (20)(2)x_1 + (14)(3)x_1^2)dx_1 = \bar{V}_1'dx_1$$

$$d\bar{V}_2 = (2x_1 + (14)(3)x_1^2)dx_1 = \bar{V}_2'dx_1$$

$$x_1 d\bar{V}_1 + x_2 d\bar{V}_2 = 0$$

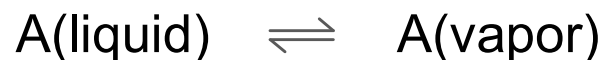
$$x_1 \cancel{\bar{V}_1'} dx_1 + x_2 \cancel{\bar{V}_2'} dx_1 = 0$$

$$x_1 \bar{V}_1' + x_2 \bar{V}_2' = 0$$



# Supplemental Slides

# Review of Lesson 32 – Phase Equilibria



$$K = \frac{\text{“activity” of products}}{\text{“activity” of reactants}}$$

In general chemistry, “activity” was molar concentration:

$$A(\text{aq}) \rightleftharpoons B(\text{aq})$$

$$K = \frac{[A(\text{aq})]}{[B(\text{aq})]}$$

Square brackets denote molar concentration in moles per L.

This is an “ideal solution.”

$$\Delta G = -RT \ln(K)$$

“Van’t Hoff Isotherm Equation”

Derivations:

[Link 1](#) [Link 2](#)

$\Delta G < 0$  “product side” favored

$\Delta G > 0$  “reactant side” favored

$\Delta G = 0$  “equilibrium”

$$G_{\text{vapor}} = G_{\text{liquid}}$$

$$dG = \cancel{VdP} - \cancel{SdT} \quad \begin{matrix} 0, \text{ const } P \\ 0, \text{ const } T \end{matrix}$$

(Eq. 6.11)

“Clapeyron” and “Clausius-Clapeyron” equations

Clausius-Clapeyron

$$\frac{dP^{\text{sat}}}{dT} = \frac{\Delta S^{\text{lv}}}{\Delta V^{\text{lv}}} = \frac{\Delta H^{\text{lv}}}{T \Delta V^{\text{lv}}} \quad \begin{matrix} \text{Clapeyron} \\ \text{(Eq. 6.85)} \end{matrix}$$

$$\Delta H^{\text{lv}} = -R \frac{d \ln(P^{\text{sat}})}{d(1/T)}$$