CH365 Chemical Engineering Thermodynamics

Lesson 40 Review and Wrap-up

Professor Andrew Biaglow 9 December 2022

Lesson 40 Agenda

- Online Canvas surveys
- Paper ABET end-of-semester surveys

TEE exam review

Lesson 40 Agenda

Online Canvas Surveys

Lesson 40 Agenda

ABET end-of-semester surveys

Term-End Exam

Room 331

- 14 December 0730-1100 Thursday
- 18 December 0730-1100 Monday
- 500 points, 5 problems, 100 points each
- Calculating properties of mixtures of ideal gases (V_{ig}, S_{ig}, and H_{ig}).
- Properties of mixtures; calculate C_P , T_{pc} , P_{pc} , and ω for a mixture.
- Residual properties V_R , S_R , and H_R . Calculating ϕ and residual properties from the Lee-Kesler tables and cubic equations of state.
- Calculating V and Z from cubic equations of state (Peng-Robinson, SRK, RK, etc.).
- Combining residuals and ideal properties to get real properties.
- Applications of Raoult's Law and Rachford-Rice method to VLE and solutions with and without activity.

Term-End Exam Review

- Pure components Z, V, H, S, G, and φ (or f)
 - Ideal gases $Z = \frac{PV}{RT} = 1$ and $\phi = 1$ (ideal gas)

Calculating Properties

$$H = H_0^{ig} + R \cdot \int_{T_0}^{T} \left(C_{P_{298}}^{ig} / R \right) dT + H^R \qquad S = S_0^{ig} + R \cdot \left(\int_{T_0}^{T} \left(\frac{C_{P_{298}}^{ig} / R}{T} \right) dT - In \left(\frac{P}{P_0} \right) \right) + S^R$$
(eq 6.50)

Real gas Z, V, and number of phases from cubic EOS

$$Z = \frac{PV}{RT} \neq 1$$

$$Z = 1 + \beta - q\beta \frac{Z - \beta}{(Z + \epsilon\beta)(Z + \sigma\beta)}$$
 (eq 3.52, real gas)

- Residual properties from EOS or Lee-Kessler
 - Cubic EOS Lesson 28, 29, Problem 6.141, WPR3

$$\frac{H^{R}}{RT} = Z - 1 + T_{r} \left(\frac{dq}{dT_{r}}\right) \cdot I \qquad \frac{S^{R}}{R} = ln(Z - \beta) + \left(q + T_{r} \frac{dq}{dT_{r}}\right) \cdot I \qquad I = \frac{1}{\sigma - \epsilon} ln\left(\frac{Z + \sigma\beta}{Z + \epsilon\beta}\right)$$
• Lee-Kessler tables – Lesson 30 (eq 13.72)

- Real combine ideal and residuals
- Fugacity Lesson 35, Slides 12-13

$$\ln \phi_{i} = Z_{i} - 1 - \ln(Z_{i} - \beta_{i}) - q_{i}I_{i} \qquad \qquad \beta_{i} = \Omega \frac{P_{r_{i}}}{T_{r_{i}}} \qquad \text{(eq 3.50)} \qquad q_{i} = \frac{\Psi \alpha}{\Omega T_{r_{i}}} \qquad \text{(eq 3.51)}$$

- Mixtures use average ω, T_C, P_C, C_P
 - Weighted averages with y_i
 - Ideal gas entropy of mixing

$$\text{adds to entropy} \quad R \sum_{i=1}^{3} y_i \ln \frac{1}{y_i}$$

Term-End Exam Review

Flash and activity coefficients – modified Raoult's Law

Calculating **Properties**

$$y_i P = x_i P_i^{sat}$$
 $K_i = \frac{y_i}{x_i} = \frac{P_i^{sat}}{P}$

Raoult's Law K-values (simple solution, id vapor phase)

$$K_i = \frac{V_i}{X_i} = \frac{\gamma_i P_i^{\text{sat}}}{P}$$

Modified Raoult's Law K-values (real liquid phase, id vapor phase)

$$K_{i} = \frac{y_{i}}{x_{i}} = \frac{\gamma_{i} f_{i}^{sat}}{f}$$

Modified Raoult's Law K-values with fugacity (real liquid phase, real vapor phase)

- Rachford-Rice algorithm
- Fugacity and fugacity coefficients

$$f_{i} = \phi_{i}^{sat} P_{i}^{sat} exp \left| \frac{V_{i}^{I} \left(P - P_{i}^{sat} \right)}{RT} \right| \qquad (eq 10.44) \qquad \phi \equiv \frac{f}{P} \qquad (eq 10.34)$$

$$\phi \equiv \frac{1}{P}$$

- Practical applications CHEMCAD, pipeline diameters Prob. 6.83
- Conceptual Issues
- What does it mean? Be able to define:
 - EnthalpyFugacity

 - Chemical potential
- Entropy
 Activity and activity coefficient
- Gibbs Energy
 Ideal solution (IMFs)
 - Phase equilibrium (condition)

Questions?