

# CH365 Chemical Engineering Thermodynamics

## Lesson 14

### Generalized Correlations for Gases and Liquids

# Generalized Correlations for Gases Slide 2

## Lee-Kesler Method

Byung Ik Lee and Michael Kesler,  
AIChE Journal, 1975, 21(3), 511-527

### Pitzer Correlation (L13)

$$Z = Z^0 + \omega Z^1 \quad (\text{Eq. 3.53})$$

simple fluids

deviation from  
simple fluids:

$$\omega Z^1 = Z - Z^0$$

$$Z^0 = 1 + B^0 \frac{P_r}{T_r} \quad Z^1 = B^1 \cdot \frac{P_r}{T_r} \quad (\text{Eq. 3.60})$$

Lesson 13, Slide 5  
formulas for  $B^0$  and  $B^1$   
eqns. 3.61 and 3.62

### Lee-Kesler Modification

$Z^{(r)}$ : calculated for n-octane

$$Z = Z^0 + \frac{\omega}{\omega^{(r)}} (Z^{(r)} - Z^0) \quad \text{where} \quad Z^1 = \frac{(Z^{(r)} - Z^0)}{\omega^{(r)}}$$

Lee and Kesler used a modified Benedict-Webb-Rubin EOS:

$$Z = 1 + \frac{B}{V_r} + \frac{C}{V_r^2} + \frac{D}{V_r^5} + \frac{c_4}{T_r^3 V_r^2} \left( \beta + \frac{\gamma}{V_r^2} \right) \exp \left( -\frac{\gamma}{V_r^2} \right)$$

$B, C, D$  are functions of  $T_r$   
(published in the paper)  
 $\beta, \gamma, c_4$ , etc. are constants

$Z$  calculated twice:

$Z^0$ : calculated for simple fluids

$Z^{(r)}$ : calculated for n-octane

Tables: Appendix – Tables D.1-D.4, pp. 676-692

Example: Find Z for n-octane at  $P_r=0.4$ ,  $T_r=0.9$

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Table D.1: Values of  $Z^0$  Page 677

$P_r =$	0.0100	0.0500	0.1000	0.2000	0.4000	0.6000	0.8000	1.0000
$T_r$								
0.30	0.0029	0.0145	0.0290	0.0579	0.1158	0.1737	0.2315	0.2892
0.35	0.0026	0.0130	0.0261	0.0522	0.1043	0.1564	0.2084	0.2604
0.40	0.0024	0.0119	0.0239	0.0477	0.0953	0.1429	0.1904	0.2379
0.45	0.0022	0.0110	0.0221	0.0442	0.0882	0.1322	0.1762	0.2200
0.50	0.0021	0.0103	0.0207	0.0413	0.0825	0.1236	0.1647	0.2056
0.55	0.9804	0.0098	0.0195	0.0390	0.0778	0.1166	0.1553	0.1939
0.60	0.9849	0.0093	0.0186	0.0371	0.0741	0.1109	0.1476	0.1842
0.65	0.9881	0.9377	0.0178	0.0356	0.0710	0.1063	0.1415	0.1765
0.70	0.9904	0.9504	0.8958	0.0344	0.0687	0.1027	0.1366	0.1703
0.75	0.9922	0.9598	0.9165	0.0336	0.0670	0.1001	0.1330	0.1656
0.80	0.9935	0.9669	0.9319	0.8539	0.0661	0.0985	0.1307	0.1626
0.85	0.9946	0.9725	0.9436	0.8810	0.0661	0.0983	0.1301	0.1614
0.90	0.9954	0.9768	0.9528	0.9015	0.7800	0.1006	0.1321	0.1630
0.93	0.9959	0.9790	0.9573	0.9115	0.8059	0.6635	0.1359	0.1664
0.95	0.9961	0.9803	0.9600	0.9174	0.8206	0.6967	0.1410	0.1705
0.97	0.9963	0.9815	0.9625	0.9227	0.8338	0.7240	0.5580	0.1779
0.98	0.9965	0.9821	0.9637	0.9253	0.8398	0.7360	0.5887	0.1844
0.99								
1.00								
1.01								
1.02								
1.05								
1.10								
1.15								
1.20								
1.30								
1.40								
1.50								
1.60								
1.70								
1.80								
1.90								
2.00								
2.20								
2.40								
2.60								
2.80								
3.00								
3.50								
4.00								

$Z^0=0.780$

$Z^1=-0.1118$

$\omega=0.400$

$$Z = Z^0 + \omega Z^1$$

$$= 0.780 + (0.400) \cdot (-0.1118)$$

$$= .7353$$

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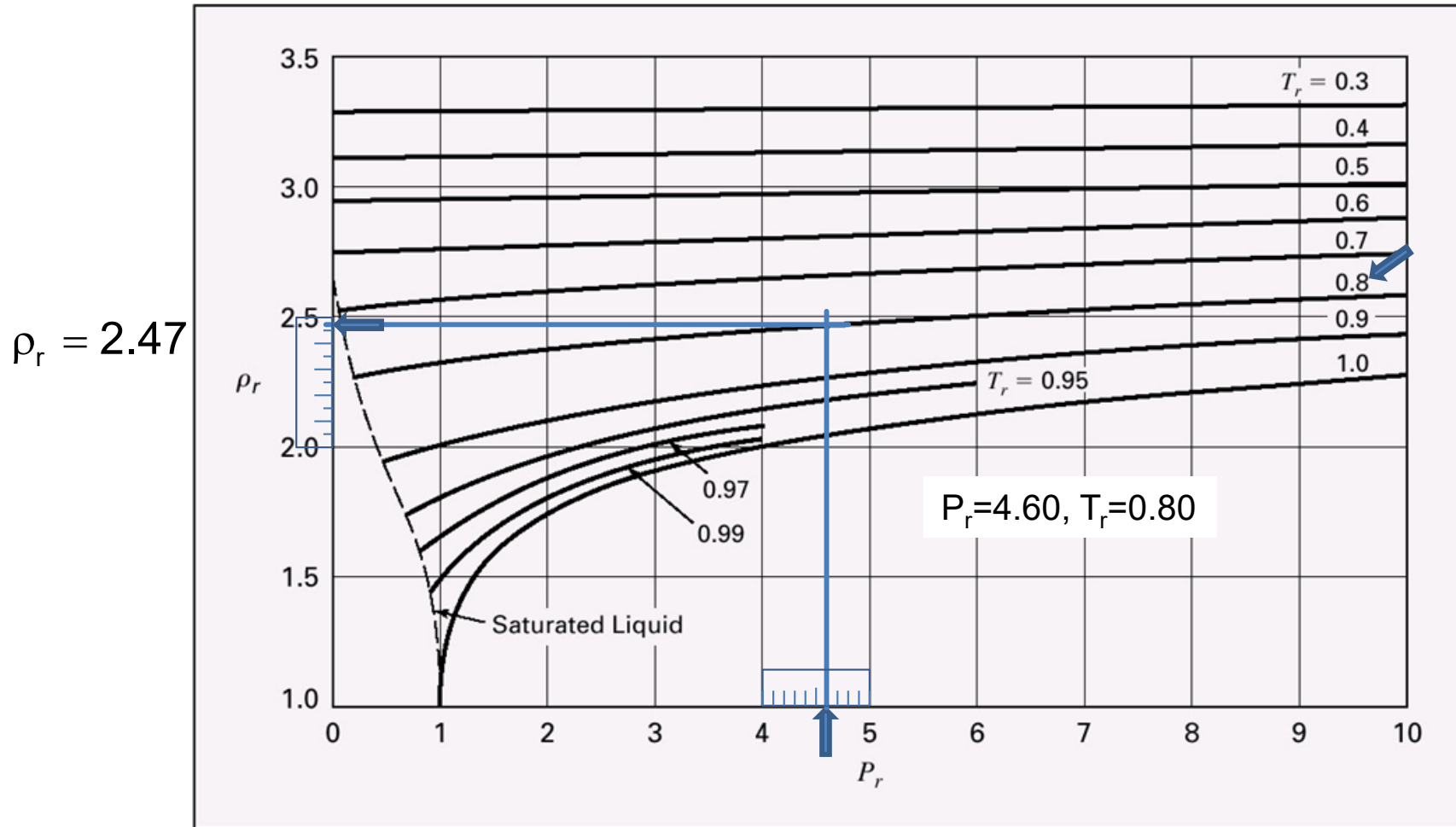
Table D.2: Values of  $Z^1$  Page 678

$P_r =$	0.0100	0.0500	0.1000	0.2000	0.4000	0.6000	0.8000	1.0000
$T_r$								
0.30	-0.0008	-0.0040	-0.0081	-0.0161	-0.0323	-0.0484	-0.0645	-0.0806
0.35	-0.0009	-0.0046	-0.0093	-0.0185	-0.0370	-0.0554	-0.0738	-0.0921
0.40	-0.0010	-0.0048	-0.0095	-0.0190	-0.0380	-0.0570	-0.0758	-0.0946
0.45	-0.0009	-0.0047	-0.0094	-0.0187	-0.0374	-0.0560	-0.0745	-0.0929
0.50	-0.0009	-0.0045	-0.0090	-0.0181	-0.0360	-0.0539	-0.0716	-0.0893
0.55	-0.0314	-0.0043	-0.0086	-0.0172	-0.0343	-0.0513	-0.0682	-0.0849
0.60	-0.0205	-0.0041	-0.0082	-0.0164	-0.0326	-0.0487	-0.0646	-0.0803
0.65	-0.0137	-0.0072	-0.0078	-0.0156	-0.0309	-0.0461	-0.0611	-0.0759
0.70	-0.0093	-0.0507	-0.1161	-0.0148	-0.0294	-0.0438	-0.0579	-0.0718
0.75	-0.0064	-0.0339	-0.0744	-0.0143	-0.0282	-0.0417	-0.0550	-0.0681
0.80	-0.0044	-0.0228	-0.0487	-0.1160	-0.0272	-0.0401	-0.0526	-0.0648
0.85	-0.0029	-0.0152	-0.0319	-0.0715	-0.0268	-0.0391	-0.0509	-0.0622
0.90	-0.0019	-0.0099	-0.0205	-0.0442	-0.1118	-0.0396	-0.0503	-0.0604
0.93	-0.0015	-0.0075	-0.0154	-0.0326	-0.0763	-0.1662	-0.0514	-0.0602
0.95	-0.0012	-0.0062	-0.0126	-0.0262	-0.0589	-0.1110	-0.0540	-0.0607
0.97	-0.0010	-0.0050	-0.0101	-0.0208	-0.0450	-0.0770	-0.1647	-0.0623
0.98	-0.0009	-0.0044	-0.0090	-0.0184	-0.0390	-0.0641	-0.1100	-0.0641
0.99	-0.0008	-0.0039	-0.0079	-0.0161	-0.0335	-0.0531	-0.0796	-0.0680
1.00	-0.0007	-0.0034	-0.0069	-0.0140	-0.0285	-0.0435	-0.0588	-0.0879
1.01	-0.0006	-0.0030	-0.0060	-0.0120	-0.0240	-0.0351	-0.0429	-0.0223
1.02	-0.0005	-0.0026	-0.0051	-0.0102	-0.0198	-0.0277	-0.0303	-0.0062
1.05	-0.0003	-0.0015	-0.0029	-0.0054	-0.0092	-0.0097	-0.0032	0.0220
1.10	0.0000	0.0000	0.0001	0.0007	0.0038	0.0106	0.0236	0.0476
1.15	0.0002	0.0011	0.0023	0.0052	0.0127	0.0237	0.0396	0.0625
1.20	0.0004	0.0019	0.0039	0.0084	0.0190	0.0326	0.0499	0.0719
1.30	0.0006	0.0030	0.0061	0.0125	0.0267	0.0429	0.0612	0.0819
1.40	0.0007	0.0036	0.0072	0.0147	0.0306	0.0477	0.0661	0.0857
1.50	0.0008	0.0039	0.0078	0.0158	0.0323	0.0497	0.0677	0.0864
1.60	0.0008	0.0040	0.0080	0.0162	0.0330	0.0501	0.0677	0.0855
1.70	0.0008	0.0040	0.0081	0.0163	0.0329	0.0497	0.0667	0.0838
1.80	0.0008	0.0040	0.0081	0.0162	0.0325	0.0488	0.0652	0.0814
1.90	0.0008	0.0040	0.0079	0.0159	0.0318	0.0477	0.0635	0.0792
2.00	0.0008	0.0039	0.0078	0.0155	0.0310	0.0464	0.0617	0.0767
2.20	0.0007	0.0037	0.0074	0.0147	0.0293	0.0437	0.0579	0.0719
2.40	0.0007	0.0035	0.0070	0.0139	0.0276	0.0411	0.0544	0.0675
2.60	0.0007	0.0033	0.0066	0.0131	0.0260	0.0387	0.0512	0.0634
2.80	0.0006	0.0031	0.0062	0.0124	0.0245	0.0365	0.0483	0.0598
3.00	0.0006	0.0029	0.0059	0.0117	0.0232	0.0345	0.0456	0.0565
3.50	0.0005	0.0026	0.0052	0.0103	0.0204	0.0303	0.0401	0.0497
4.00	0.0005	0.0023	0.0046	0.0091	0.0182	0.0270	0.0357	0.0443

# Generalized Correlations for Liquids Slide 4

Rackett:  $V^{\text{sat}} = V_C Z_C^{(1-T_r)^{2/7}}$  (Eq. 3.68)

$$Z^{\text{sat}} = \frac{P_r}{T_r} Z_C^{[1+(1-T_r)^{2/7}]} \quad (\text{Eq. 3.69})$$



**Figure 3.15:** Generalized density correlation for liquids.

Lydersen, Greenkorn, and Hougen:  $\rho_r \equiv \frac{\rho}{\rho_C} = \frac{V_C}{V}$  (Eq. 3.70)

# Example 3.14

For ammonia at 310 K, estimate the molar volume ~~density~~ of (a) the saturated liquid and (b) the liquid at 100 bar.

## (Liquids)

## Example 3.14 , part b, continued

Rackett:  $V^{\text{sat}} = V_C Z_C^{(1-T_r)^{2/7}}$  (Eq. 3.68)  $Z^{\text{sat}} = \frac{P_r}{T_r} Z_C^{[1+(1-T_r)^{2/7}]}$  (Eq. 3.69)

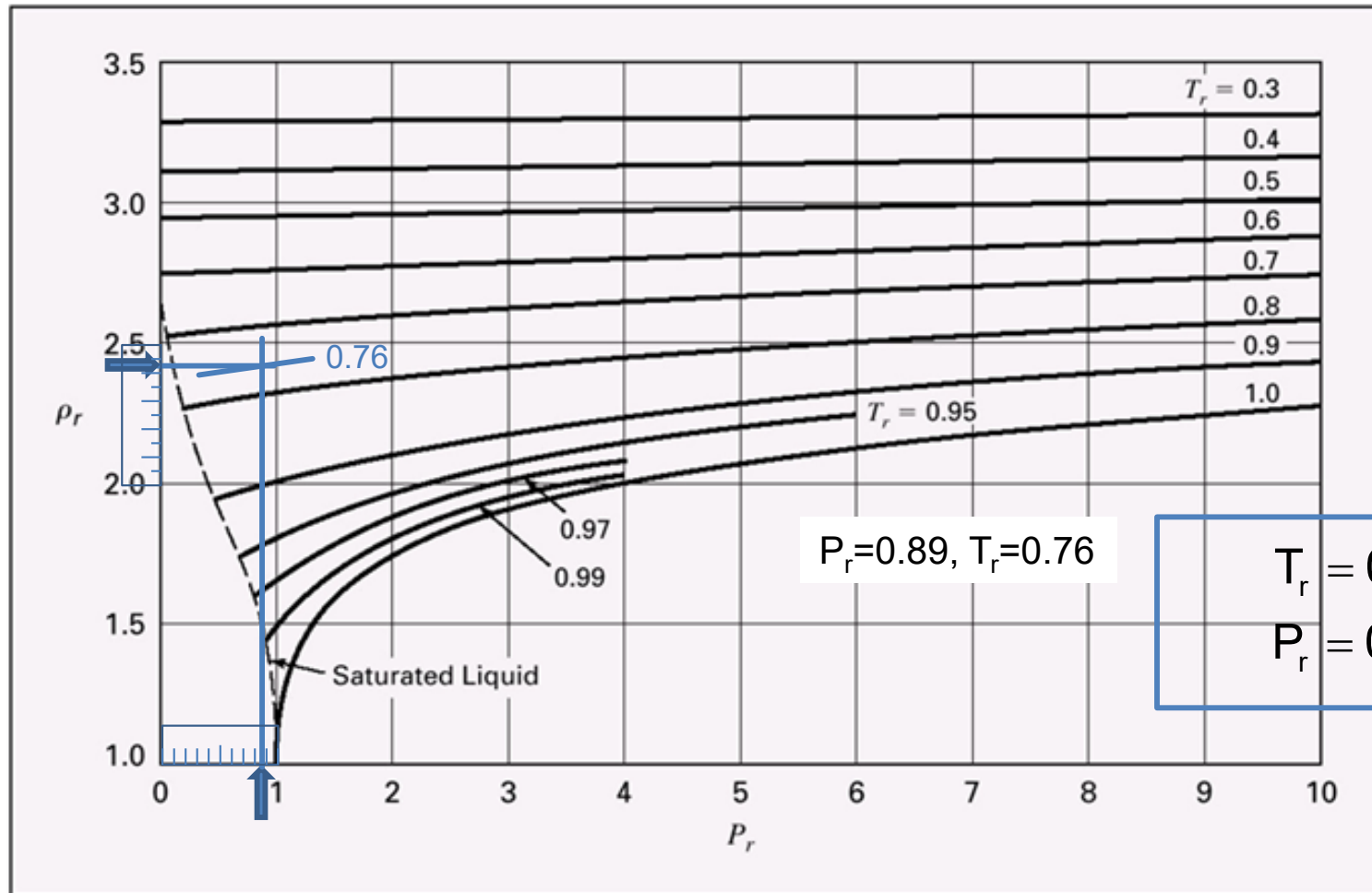


Figure 3.15. Generalized density correlation for liquids.

Lydersen, Greenkorn, and Hougen:  $\rho_r \equiv \frac{\rho}{\rho_C} = \frac{V_C}{V}$  (Eq. 3.70)

$$\rho_r = 2.43$$

solution deviates  
from book;  
authors read  
reduced density  
as 2.38 on p. 117

$$P_r = 0.89, T_r = 0.76$$

$$T_r = 0.7641$$

$$P_r = 0.8865$$

## Example 3.14, continued

For ammonia at 310 K, estimate the molar volume ~~density~~ of (a) the saturated liquid and (b) the liquid at 100 bar.

# Homework



# Problem 3.58

To a good approximation, what is the molar volume of ethanol vapor at 480 deg C and 6000 kPa? How does this result compare with the ideal gas?

Answer the problem in four parts:

(a) Lee-Kesler method.

(b) SRK equation.

(c) Ideal gas equation.

For comparison: Compare LK and SRK to IG. If either is less than IG, explain why using knowledge of IG behavior.

Online Interpolator Tool for Lee-Kesler Tables:

[https://www.ajdesigner.com/phpinterpolation/bilinear\\_interpolation\\_equation.php](https://www.ajdesigner.com/phpinterpolation/bilinear_interpolation_equation.php)