# CH365 Chemical Engineering Thermodynamics

Lesson 40 Review and Wrap-up

### Lesson 40 Agenda

- Online Canvas surveys
- Paper ABET end-of-semester surveys

TEE exam review

#### Term-End Exam

#### Room 331

- 14 December 0730-1100 Thursday
- 18 December 0730-1100 Monday
- 500 points, 5 problems, 100 points each
- Calculating properties of mixtures of ideal gases (V<sub>ig</sub>, S<sub>ig</sub>, and H<sub>ig</sub>).
- Properties of mixtures; calculate  $C_P$ ,  $T_{pc}$ ,  $P_{pc}$ , and  $\omega$  for a mixture.
- Residual properties  $V_R$ ,  $S_R$ , and  $H_R$ . Calculating  $\phi$  and residual properties from the Lee-Kesler tables and cubic equations of state.
- Calculating V and Z from cubic equations of state (Peng-Robinson, SRK, RK, etc.).
- Combining residuals and ideal properties to get real properties.
- Applications of Raoult's Law and Rachford-Rice method to VLE and solutions with and without activity.

#### Term-End Exam Review

- Pure components Z, V, H, S, G, and φ (or f)
  - Ideal gases  $Z = \frac{PV}{RT} = 1$  and  $\phi = 1$  (ideal gas)

## Calculating Properties

$$H = H_0^{ig} + R \cdot \int_{T_0}^{T} \left( C_{P_{298}}^{ig} / R \right) dT + H^R \qquad S = S_0^{ig} + R \cdot \left( \int_{T_0}^{T} \left( \frac{C_{P_{298}}^{ig} / R}{T} \right) dT - In \left( \frac{P}{P_0} \right) \right) + S^R$$
(eq 6.50)

Real gas Z, V, and number of phases from cubic EOS

$$Z = \frac{PV}{RT} \neq 1$$
  $Z = 1 + \beta - q\beta \frac{Z - \beta}{(Z + \epsilon\beta)(Z + \sigma\beta)}$  (eq 3.52, real gas)

- Residual properties from EOS or Lee-Kessler
  - Cubic EOS Lesson 28, 29, Problem 6.141, WPR3

$$\frac{H^{R}}{RT} = Z - 1 + T_{r} \left(\frac{dq}{dT_{r}}\right) \cdot I \qquad \frac{S^{R}}{R} = ln(Z - \beta) + \left(q + T_{r} \frac{dq}{dT_{r}}\right) \cdot I \qquad I = \frac{1}{\sigma - \epsilon} ln\left(\frac{Z + \sigma\beta}{Z + \epsilon\beta}\right)$$
• Lee-Kessler tables – Lesson 30 (eq 13.72)

- Real combine ideal and residuals
- Fugacity Lesson 35, Slides 10-13, computing slides 12-13

$$\ln \phi_{i} = Z_{i} - 1 - \ln(Z_{i} - \beta_{i}) - q_{i}I_{i} \qquad \beta_{i} = \Omega \frac{P_{r_{i}}}{T_{r}} \qquad \text{(eq 3.50)} \qquad q_{i} = \frac{\Psi \alpha}{\Omega T_{r_{i}}} \qquad \text{(eq 3.51)}$$

- Mixtures use average ω, T<sub>C</sub>, P<sub>C</sub>, C<sub>P</sub>
  - Weighted averages with y<sub>i</sub>
  - Ideal gas entropy of mixing

adds to entropy 
$$R \sum_{i=1}^{3} y_i \ln \frac{1}{y_i}$$

#### Term-End Exam Review

Flash and activity coefficients – modified Raoult's Law

#### Calculating **Properties**

$$y_i P = x_i P_i^{sat}$$
  $K_i = \frac{y_i}{x_i} = \frac{P_i^{sat}}{P}$ 

Raoult's Law K-values (simple solution, id vapor phase)

$$K_{i} = \frac{y_{i}}{x_{i}} = \frac{\gamma_{i} P_{i}^{sat}}{P}$$

Modified Raoult's Law K-values (real liquid phase, id vapor phase)

$$K_i = \frac{y_i}{x_i} = \frac{\gamma_i f_i^{sat}}{f}$$

Modified Raoult's Law K-values with fugacity (real liquid phase, real vapor phase)

- Rachford-Rice algorithm Prob. 13.1
- Fugacity and fugacity coefficients
- Practical applications CHEMCAD, pipeline diameters Prob. 6.83

## Issues

Conceptual • What does it mean? Be able to define:

- Simple fluids
- Acentric factor
- Enthalpy
- Entropy
- Gibbs Energy
- Partial molar property
   Chemical potential
- Chemical potential

- Pitzer correlation
- Residual property
- Excess property
- Gibbs Energy
- Partial molar property
- Pitzer correlation

- Fugacity
- Bip
- Activity coefficient
- Ideal solution
- Ideal gas
- Phase equilibrium
- Clapeyron's equation