# CH402 Chemical Engineering Process Design

Class Notes L15

Cost Components of Capital Investments

A template for today's lesson is found in Canvas Lesson 15

#### L15/16 Learning Objectives

- L15: 1. Use cost components to estimate capital costs for chemical processing facilities.
  - 2. Estimate capital costs using Lang factors.
- L16: 1. Estimate capital costs using scaling factors.
  - 2. Estimate capital costs based on turnover ratio.

## Problem 6-3

The purchase and installation costs of some pieces of equipment are given as a function of weight rather than capacity. An example of this is the installed costs of large tanks. The 1990 cost for an installed aluminum tank weighing 45,000 kg was \$640,000. For a size range from 10,000 to 450,000 kg, the installed cost weight exponent for aluminum tanks is 0.93. If an aluminum tank weighing 300,000 kg is required, what capital investment is needed in the year 2000?

## Problem 6-4

The 1990 cost for an installed 304 stainless steel tank weighing 135,000 kg was \$1,100,000. The installed cost weight exponent for stainless steel tanks is 0.88 for a size range from 100,000 to 300,000 kg. What weight of installed stainless steel tank could have been obtained for the same capital investment as in Problem 6-3?

## Plant Costs - Methods A-G

- A Detailed item estimate
- B Unit cost estimate based on records
- C Percentage of delivered-equipment cost
- D Lang factors
- E Power factors with plant/capacity ratio
- F Cost per unit capacity
- G Turnover ratio

#### Percentage of Delivered-Equipment Cost

#### FE Ref. Manual pages 257

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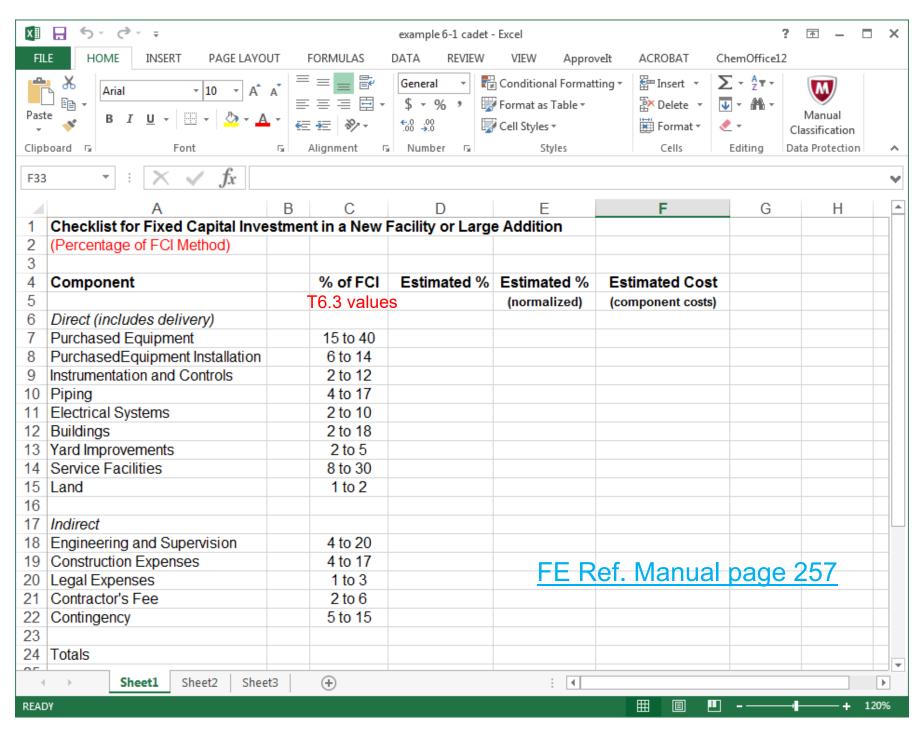
Component	Range
Direct costs  Purchased equipment-delivered (including fabricated equipment and process machinery	100
such as pumps and compressors)	
Purchased-equipment installation	39–47
Instrumentation and controls (installed)	9–18
Piping (installed)	16–66
Electrical (installed)	10–11
Buildings (including services)	18–29
Yard improvements	10–13
Service facilities (installed)	40–70
Land (if purchase is required)	6
Total direct plant cost	264–346
Indirect costs	22 22
Engineering and supervision	32–33
Construction expenses	34–41
Total direct and indirect plant costs	336–420
Contractor's fee (about 5% of direct and indirect plant costs)	17–21
Contingency (about 10% of direct and indirect plant costs)	36–42
Fixed-capital investment	387–483
Working capital (about 15% of total capital investment)	68–86
Total capital investment	455–569

## Example 6-1

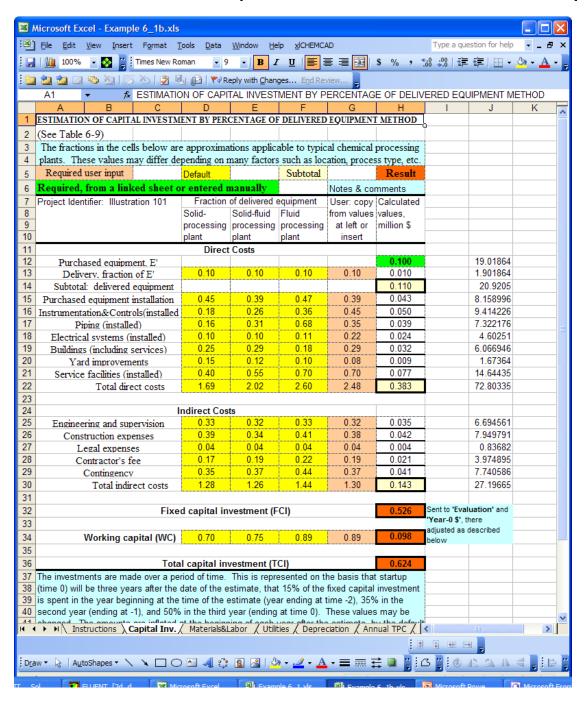
p. 240

Estimate the fixed capital investment for a process plant if the purchased-equipment cost is \$100,000. Use the ranges of process-plant component cost outlined in Table 6-3, for a process plant handling both solids and fluids, with a high degree of automatic controls, and essentially outdoor operation. Do not include land.

Very Important Example – Needed for PS8 Problem 6-8



Use cost & evaluation spreadsheet from course webpage.



## FE Ref. Manual pages 257 Lang Factors

#### Method D

PTW, Page 254

Table 6-10. Revised Lang factors for estimation of fixedcapital investment (FCI) or total capital investment (TCI)

Factor × delivered-equipment cost = FCI or TCI				
	Lang factors			
Type of Plant	FCI	TCI		
Solid	4.0	4.7		
Solid-fluid	4.3	5.0		
Fluid	5.0	6.0		

H.J. Lang, Chem. Eng., 54 (10) 1947, page 117; H.J. Lang, Chem. Eng., 55 (6) 1948, page 112

Example 1: Delivered equipment cost (DEC) for a fluid processing plant is \$100,000

$$FCI = 5.0 \times \$100,000 = \$500,000$$
 and  $TCI = 6.0 \times \$100,000 = \$600,000$ 

Example 2: Purchased equipment cost for a fluid processing plant is \$100,000

DEC = 
$$$100,000 + .1 \times $100,000 = $110,000$$
 (delivery = 10% of PEC, slide 10)

$$FCI = 5.0 \times \$110,000 = \$550,000$$
 and  $TCI = 6.0 \times \$110,000 = \$660,000$ 

#### Problem 6-8.

The purchased-equipment cost for a plant which produces pentaerythritol (solid-fluid processing plant) is \$300,000. The plant is to be an addition to an existing formaldehyde plant. The major part of the building cost will be for indoor construction. The contractor's fee will be 7% of the direct plant cost. All other costs are close to the average values found for typical chemical plants. On the basis of this information, estimate the total direct plant cost, the fixed capital investment, and the total capital investment.

Use Cost and Evaluation Worksheet (colorful worksheet).

#### New Definitions - Important Grass-Roots Plant

- A complete plant including infrastructure erected on a new area or site.
- Investment includes all costs of land, site development, battery-limit facilities, and auxiliary facilities.

#### **Battery Limit**

- The design of most process units includes a pipe rack on one side of the unit that contains all the piping entering and exiting the unit. The battery limit is where the piping crosses the defined boundary between the unit and the area outside of the unit.
- Battery limits typically exclude storage facilities, administrative buildings, utilities, or auxiliary facilities unless otherwise specified.
- The operational principle is primarily safety but is commonly applied in process design as well. In preparing for major maintenance of a unit, it is cleared of hazardous materials and isolated from the rest of the refinery. A chief operator can go to the battery limits and determine whether all the necessary blinds have been properly installed. He or she signs off on a blind list confirming full unit isolation before work begins.

## Plant Costs - Methods A-G

- A Detailed item estimate
- B Unit cost estimate based on records
- C Percentage of delivered-equipment cost ✓
- D Lang factors ✓
- E Power factors with plant/capacity ratio
- F Cost per unit capacity
- G Turnover ratio

#### Method G: Turnover Ratio

- Use existing data to calculate turnover ratio.
- Assume turnover ratio is constant.

$$Turnover Ratio = \frac{gross \ annual \ sales}{fixed \ capital \ investment}$$

Eq. 6-11, p. 258

 $0.2 \text{ to } 4 \text{ y}^{-1}$ 

± 30 % accuracy.

Use in PS8, problem 6-9

#### Problem 6-9.

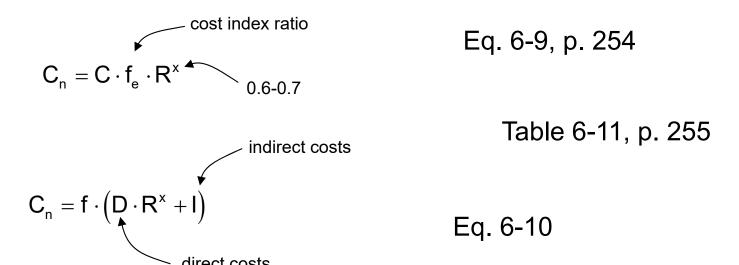
Estimate by the turnover ratio method the fixed-capital investment required in 2000 for a proposed sulfuric acid plant (battery-limit) which has an annual capacity of 1.3×10<sup>8</sup> kg/yr of 100% sulfuric acid (contact catalytic process), using the data from Table 6-11, when the selling price of sulfuric acid is \$86 per metric ton. The plant will operate 325 days/year. Repeat the calculation, using the cost capacity exponent (scaling) method with data from Table 6-11

#### Problem 6-9.

Estimate by the turnover ratio method the fixed-capital investment required in 2000 for a proposed sulfuric acid plant (battery-limit) which has an annual capacity of 1.3×10<sup>8</sup> kg/yr of 100% sulfuric acid (contact catalytic process), using the data from Table 6-11, when the selling price of sulfuric acid is \$86 per metric ton. The plant will operate 325 days/year. Repeat the calculation, using the cost capacity exponent (scaling) method with data from Table 6-11

### Method E: Power Factors and Plant Capacity Ratio

Similar to what we have been doing for single pieces of equipment.



± 20 % accuracy.

Cost of Plant A = Cost of Plant B 
$$\cdot \left(\frac{\text{Capacity of Plant A}}{\text{Capacity of Plant B}}\right)^n$$

#### Problem 6-10.

The total capital investment for a chemical plant is \$1 million, and the working capital is \$100,000. If the plant can produce an average of 8000 kg of final product per day during a 365-day year, what selling price in dollars per kilogram of product would be necessary to give a turnover ratio of 1.0?

## Questions?