# **Design Problem 1 – Pump and Piping Design**

- 1. Objectives
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# **Objectives**

The objectives of Design Problem 1 are to: (1) update the cost index in CHEMCAD, (2) use CHEMCAD to perform an optimized design and pricing of a section of pipeline, and (3) determine the purchased price and power requirements for a pump.

#### **Problem Statement**

Your assignment is to use CHEMCAD to design the piping and pump to deliver feed liquid to a distillation process. The feed temperature, pressure, and component flow rates are given in Table 1, and you will determine the size and cost of the pump and pipeline needed to deliver the feed to the column. You will also determine the size and cost of fittings and valves, the cost of paint for the pipe, and the energy requirements for one year of operation. Finally, this type of system must be *optimized* for peak economic efficiency, and you will discuss why your solution is considered to be optimized. Your design will be subject to the constraints and specifications described below.

Table 1. Feed Component Flow Rates (298 K and 202.650 kPa)

| Component                     | Feed Rate, lb-mol/h |
|-------------------------------|---------------------|
| Toluene                       | 91.50               |
| Naphthalene                   | 299.81              |
| Biphenyl                      | 3156.56             |
| Diphenylenemethane (Fluorene) | 192.94              |
| Phenanthrene                  | 144.19              |
| M-Terphenyl                   | <u>359.81</u>       |
| _ Total                       | 4244.81             |

### **Constraints and Additional Information**

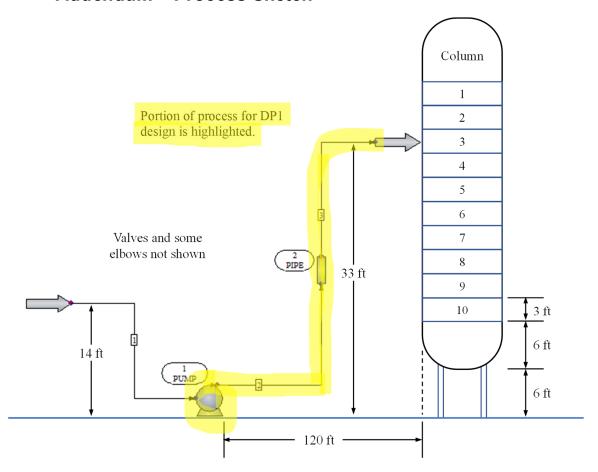
- You are designing the pump and the pipe connecting the pump to the column. You will *not* be designing the distillation column or column internals (trays, shell, condenser, reboiler). This has already been designed by another group.
- Pump constraints and specs:
  - The pump and motor costs must be calculated in CHEMCAD. The pump is centrifugal, one stage, 3550 rpm vertical split casing (VSC), cast steel, and explosion proof, and the pump motor is 1200 rpm, and installed costs are 2.8 times the purchased equipment cost.
  - CHEMCAD cost information must be updated to January 2024 by entering the current Chemical Engineering Plant Cost Indices. Values can be viewed in "Tools," then "Edit Cost Index."

- Energy cost based on one year of operation (365d=1yr) at \$0.0646 per kWh and the pump is 79% efficient.
  - (energy costs found at https://www.eia.gov/electricity/monthly/epm table grapher.php?t=epmt 5 6 a)
- Piping constraints and specs:
  - Pipe, valve, and fitting costs cannot be calculated in CHEMCAD. Pipe costs can be found in the PTW textbook. Any cost data taken from the textbook is referenced to January 2002.
  - Fittings costs are not in the 2002 edition of the textbook. They can be found in the "1979 Pipe & Fitting Prices" document found in your SharePoint (Fig. 13-4, PTW, 3<sup>rd</sup> ed., p. 529). This data is referenced to January 1979.
  - Installed costs are 2.8 times the purchased equipment cost.
  - The pipe diameter is determined in CHEMCAD. Fluid flow in the pipeline is single-phase, and the pipe sizing option in CHEMCAD is "1 Design, single-phase flow."
  - All pipe and fittings are Sch. 40 welded commercial (carbon) steel and must be painted.
  - The length of the pipeline is 153 feet with a net elevation change of 19 feet.
  - The pipeline has 12 90° standard elbows, two gate valves, three globe valves, and one sudden expansion where the fluid emerges into the column. The diameter ratio for the expansion can be taken as 0.001.
  - The feed must enter the column at 298 K and 353.5 kPa.

# Submission Requirements

- 1. Download, complete and upload the CHEMCAD template found in Canvas.
- 2. Download, complete and upload the Excel template found in Canvas, including:
  - a. Diameter, purchased and installed costs in January 2024 for pipe, elbows, valves, and paint.
  - c. Purchased and installed cost of pump and motor in January 2024.
  - d. Pump NPSH, power, energy, and energy cost for 1 year of operation.
  - d. Total cost of installed equipment and energy for one year of operation.
  - e. Print the bordered areas from the Excel template as a pdf, attach a cover sheet, and submit the combined pdf to Canvas.
- 3. Discuss how the design has been *optimized*. Answer this question in the space provided in Excel.
- 4. All three electronic files (CHEMCAD, Excel, and PDF) must be uploaded to Canvas.

## Addendum - Process Sketch





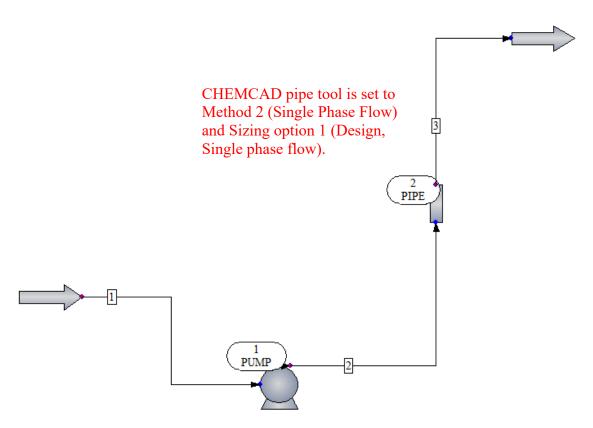
Vertical split-case pump (VSC), https://www.statesupply.com/bell-andgossett/pump/series-vsx. Casing split is perpendicular to motor shaft axis.



Horizontal split-case pump (HSC), https://www.ruhrpumpen.com/en/products/ between-bearing-pumps/hsc-pump. Casing split is parallel to motor shaft axis.

## Solution

The CHEMCAD flowsheet is shown below. Pump  $\Delta P$  is adjusted until the pressure in stream 3 is on spec. The resulting stream and unit ops reports are shown on the following pages for 2.5-inch nominal pipe size. The calculation of the NPSH and the resulting value are shown in the unit ops report for the pump on page 5. The cost and optimization information are shown in the Excel spreadsheet on pages 7 and 8 of this document.



CHEMCAD pump is set to "Specify pressure increase" mode. A value of 296.18 kPa puts stream 3 on spec.

| Pump Summary from CHEMCAD           |                        |                                      |
|-------------------------------------|------------------------|--------------------------------------|
| Pressure increase kPa               | <mark>296.</mark> 1800 | Pump spec set by cadets. Pressure    |
| Efficiency                          | 0.7900                 | ·                                    |
| Calculated power kJ/sec             | 30.5755                | increase is iterated, and efficiency |
| Calculated Pout kPa                 | 498.8300               | was given.                           |
| Head m                              | 28.9756                |                                      |
| Vol. flow rate m3/h                 | 293.4264               |                                      |
| Mass flow rate lb/sec               | 187.2978               |                                      |
| NPSH available m                    | 19.8175                |                                      |
| Cost estimation flag                | 1                      |                                      |
| Material                            | 1                      |                                      |
| Motor type                          | 2                      |                                      |
| Motor RPM                           | 2                      |                                      |
| Install factor                      | 2.8000                 | Given in problem statement.          |
| Basic pump cost \$                  | 18 <mark>139.73</mark> | 1                                    |
| Basic motor cost \$                 | 9849.54                | Pump costs carried forward to        |
| Total purchase cost \$              | 2 <mark>7989.28</mark> | •                                    |
| Total installed cost \$             | 78369.97               | spreadsheet.                         |
| ,                                   |                        |                                      |
| Pipe / Line Sizing Summary          |                        |                                      |
| Method                              | 2                      |                                      |
| Pipe schedule<br>Nominal size DN mm | 40<br>200              | Calculated by CHEMCAD using          |
| Nominal size NPS in                 | 8                      | •                                    |
| Calculated ID m                     | 0.2027                 | design mode (optimal economic pipe   |
| Wall thickness m                    | 0.0082                 | diameter.                            |
| Pipe length m                       | 46.6344                | Total length of pipe = 153 feet      |
|                                     | .5720e-005             | Townsongon of paper 100 1000         |
| Elevation change m                  | 5.7912                 | Must subtract feed pipe height from  |
| Sizing option                       | 1                      | pipe outlet height at column:        |
| Pressure drop kPa                   | 145.3295               | 33 ft - 14 ft = 19 ft = 5.7912 m     |
| <del>-</del>                        | 52945.4219             | 33 II - 14 II - 19 II - 3.7912 III   |
| Fric factor liq                     | 0.0179                 |                                      |
| Avg density kg/m3                   | 1042.3170              |                                      |
| Calc. velocity m/sec                | 2.5254                 |                                      |
| Min. velocity m/sec                 | 0.9847                 |                                      |
| DP friction kPa                     | 86.1339                |                                      |
| DP elevation kPa                    | 59.1954                |                                      |
| Output press. kPa                   | 353.5005               | Constraint. System must              |
| DP/100ft, psi                       | 1.2993                 | deliver this pressure to             |
| Liquid flow lb/sec                  | 187.2978               | column.                              |
| Liquid density kg/m3                | 1042.3170              |                                      |
| Liq viscosity N-s/m2                | 0.0035                 |                                      |
| Surface tension N/m                 | 0.0418                 |                                      |
| EL. fittings m                      | 246.4270               |                                      |
| Total ELength m                     | 293.0614               |                                      |
| Gate valve                          | 2                      |                                      |
| Glb seat flatBevelPlug              | 3                      |                                      |
| Standard elbow 90 deg. 12           | 1                      |                                      |
| Friction fac. model                 | 1<br>1                 |                                      |
| Incl. expansion fac.                | 51.2818                |                                      |
| Pipe wall cond. W/m-K               | 7.1336                 |                                      |
| Inclination angle                   | 1.1330                 |                                      |

|                                    | •       |           | •••                              |
|------------------------------------|---------|-----------|----------------------------------|
| nominal size                       | in      | 8"        | 200 mm                           |
| pipe inside diameter, actual       | m       | 0.2027    | ID, inches, page 962             |
| pipe length                        | m       | 46.63     | ib, inches, page 302             |
| pipe price per length, 2002        | \$/m    | 40.03     | Fig 12-4, page 503               |
| pipe price, total, 2002            | \$      | 2285      | Fig 12-4, page 303               |
| pipe price, total, JAN 2024        | \$      | 5257      |                                  |
| pipe installed price               | \$      | 14719     |                                  |
| pipe installed price               | J       | 14/13     |                                  |
| number of elbows                   |         | 12        |                                  |
| elbow price each, 1979             | \$ each | 40        | See "1979 Pipe & Fitting Prices" |
| elbow price, total, 1979           | \$      | 480       | Found in Lesson 2 on Website     |
| elbow price, total, JAN 2024       | \$      | 2044      | Fig 13-4, PTW 3rd Ed., p. 529    |
| elbow installed price              | \$      | 5723      | 3 11 1/1 11 11 11 11 11          |
|                                    |         |           |                                  |
| number of gate valves              |         | 2         |                                  |
| gate valve price each, 2002        | \$ each | 700       | Fig 12-8, page 505               |
| gate valve price, total, 2002      | \$      | 1400      |                                  |
| gate valve price, total, JAN 2024  | \$      | 3221      |                                  |
| gate valve installed price         | \$      | 9019      |                                  |
|                                    |         |           |                                  |
| number of globe valves             |         | 3         |                                  |
| globe valve price, each, 2002      | \$ each | 900       | Fig 12-8, page 505               |
| globe valve price, total, 2002     | \$      | 2700      |                                  |
| globe valve price, total, JAN 2024 | 1\$     | 6212      |                                  |
| globe valve installed price        |         | 17393     |                                  |
|                                    |         |           |                                  |
| paint price, 2002                  | \$/m    | 1.6       | Fig 12-12, page 507              |
| paint price, total, 2002           | \$      | 75        |                                  |
| paint, total, JAN 2024             | \$      | 172       |                                  |
|                                    |         | 40.00     |                                  |
| pump NPSH                          | m       | 19.82     |                                  |
| pump ΔP                            | kPa     | 296.18    |                                  |
| pump cost, JAN 2024                | \$      | 18140     | CHEMCAD                          |
| motor cost, JAN 2024               | \$      | 9850      | CHEMCAD                          |
| total price, pump+motor            | \$      | 27990     |                                  |
| pump+motor installed price         | \$      | 78372     |                                  |
| Electrical Power                   |         |           |                                  |
| pump efficiency                    | 0.79    |           |                                  |
| pump input power                   | kW      | 22.019    | CHEMCAD                          |
| operating time                     | h       | 8760      | OTTENIO/ ID                      |
| pump power                         | kWh     | 267841    |                                  |
| power cost per unit                | \$/kWh  | 0.0646    |                                  |
| power cost per unit                | \$      | 17303     |                                  |
| 201101 0000                        | •       | 17000     |                                  |
| Total cost                         | \$      | \$142,699 |                                  |

Calculations are embedded in the spreadsheet. The optimization of the pipeline diameter was conducted using the "Sizing" tool in CHEMCAD, resulting in 8-inch nominal pipe.

| CE Plant Cost Indices                          |        |
|--|--------|
| Pipe, Valves, and Fittings, 1979               | 300.3  |
| Pipe, Valves, and Fittings, 2002               | 555.8  |
| Pipe, Valves, and Fittings, JAN 2024           | 1278.7 |
| Pipes, Valves and Fittings, 2002 to JAN 2024   | 2.301  |
| Pipes, Valves and Fittings, 1979 to JAN 2024   | 4.258  |
| Installation Factors                           |        |
| Install factor for pumps                       | 2.8    |
| Install factor for pipes, valves, and fittings | 2.8    |

CE Plant Cost Index values are found in the "CE Plant Cost Index" linked to the main course web page and are used in the spreadsheet to update prices from 1979 or 2002 to 2024.

How has the design been optimized? (Answer in the space below.

CHEMCAD computes pipe diamter using optimum diamter equations discussed in Lesson 1 in "How to Find the Pipe Diameter." The pipe diamter can be changed in CHEMCAD to prove this. For example, the total cost of the system for 6-inch pipe is \$157,393, for 8-inch it is \$142,697, and for 10-inch it is \$167,074, showing a minimum at 8 inches. Additional results are shown below.

|                                    |          |           | •                                |
|------------------------------------|----------|-----------|----------------------------------|
| nominal size                       | in       | 6"        | 200 mm                           |
| pipe inside diameter, actual       | m        | 0.1541    | ID, inches, page 962             |
| pipe length                        | m        | 46.63     | ib, liiclies, page 902           |
|                                    | \$/m     | 32        | Fig 12-4, page 503               |
| pipe price per length, 2002        | •        |           | Fig 12-4, page 505               |
| pipe price, total, 2002            | \$       | 1492      |                                  |
| pipe price, total, JAN 2024        | \$<br>\$ | 3433      |                                  |
| pipe installed price               | <b>3</b> | 9612      |                                  |
| number of elbows                   |          | 12        |                                  |
|                                    | ¢ ooch   | 24        | See "1979 Pipe & Fitting Prices" |
| elbow price each, 1979             | \$ each  |           |                                  |
| elbow price, total, 1979           | \$       | 288       | Found in Lesson 2 on Website     |
| elbow price, total, JAN 2024       | \$<br>\$ | 1226      | Fig 13-4, PTW 3rd Ed., p. 529    |
| elbow installed price              | <b>D</b> | 3434      |                                  |
| number of gate valves              |          | 2         |                                  |
| gate valve price each, 2002        | \$ each  | 420       | Fig 12-8, page 505               |
| gate valve price, total, 2002      | \$       | 840       | 11g 12-0, page 505               |
| gate valve price, total, JAN 2024  |          | 1933      |                                  |
| gate valve installed price         | \$       | 5411      |                                  |
| gate valve mstalled price          | <b>J</b> | 3411      |                                  |
| number of globe valves             |          | 3         |                                  |
| globe valve price, each, 2002      | \$ each  | 550       | Fig 12-8, page 505               |
| globe valve price, total, 2002     | \$       | 1650      | 1.ig 12.0, page 000              |
| globe valve price, total, JAN 2024 | -        | 3796      |                                  |
| globe valve installed price        | 10       | 10629     |                                  |
| gross varvo motanoa prico          |          | 70020     |                                  |
| paint price, 2002                  | \$/m     | 1.5       | Fig 12-12, page 507              |
| paint price, total, 2002           | \$       | 70        | 7, 0                             |
| paint, total, JAN 2024             | \$       | 161       |                                  |
|                                    |          |           |                                  |
| pump NPSH                          | m        | 19.82     |                                  |
| pump ∆P                            | kPa      | 492.58    |                                  |
| pump cost, JAN 2024                | \$       | 20038     | CHEMCAD                          |
| motor cost, JAN 2024               | \$       | 15451     | CHEMCAD                          |
| total price, pump+motor            | \$       | 35489     |                                  |
| pump+motor installed price         | \$       | 99369     |                                  |
|                                    |          |           |                                  |
| Electrical Power                   |          |           |                                  |
| pump efficiency                    | 0.79     |           |                                  |
| pump input power                   | kW       | 50.850    | CHEMCAD                          |
| operating time                     | h        | 8760      |                                  |
| pump power                         | kWh      | 445446    |                                  |
| power cost per unit                | \$/kWh   | 0.0646    |                                  |
| power cost                         | \$       | 28776     |                                  |
|                                    | •        | A457.000  |                                  |
| Total cost                         | \$       | \$157,392 |                                  |

| nominal size                       | in      | 10"       | 200 mm                           |
|------------------------------------|---------|-----------|----------------------------------|
| pipe inside diameter, actual       | m       | 0.2545    | ID, inches, page 962             |
| pipe length                        | m       | 46.63     | ib, meres, page 302              |
| pipe price per length, 2002        | \$/m    | 65        | Fig 12-4, page 503               |
| pipe price, total, 2002            | \$      | 3031      | 1 ig 12-4, page 500              |
| pipe price, total, JAN 2024        | \$      | 6973      |                                  |
| pipe installed price               | \$      | 19525     |                                  |
| proc matanoa prioc                 | •       | 70020     |                                  |
| number of elbows                   |         | 12        |                                  |
| elbow price each, 1979             | \$ each | 70        | See "1979 Pipe & Fitting Prices" |
| elbow price, total, 1979           | \$      | 840       | Found in Lesson 2 on Website     |
| elbow price, total, JAN 2024       | \$      | 3577      | Fig 13-4, PTW 3rd Ed., p. 529    |
| elbow installed price              | \$      | 10015     |                                  |
| number of gate valves              |         | 2         |                                  |
| gate valve price each, 2002        | \$ each | 1100      | Fig 12-8, page 505               |
| gate valve price, total, 2002      | \$      | 2200      |                                  |
| gate valve price, total, JAN 2024  | \$      | 5061      |                                  |
| gate valve installed price         | \$      | 14172     |                                  |
| number of globe valves             |         | 3         |                                  |
| globe valve price, each, 2002      | \$ each | 1900      | Fig 12-8, page 505               |
| globe valve price, total, 2002     | \$      | 5700      |                                  |
| globe valve price, total, JAN 2024 | 1\$     | 13114     |                                  |
| globe valve installed price        |         | 36718     |                                  |
| paint price, 2002                  | \$/m    | 1.8       | Fig 12-12, page 507              |
| paint price, total, 2002           | \$      | 84        |                                  |
| paint, total, JAN 2024             | \$      | 193       |                                  |
| pump NPSH                          | m       | 19.82     |                                  |
| pump ΔP                            | kPa     | 242.56    |                                  |
| pump cost, JAN 2024                | \$      | 17477     | CHEMCAD                          |
| motor cost, JAN 2024               | \$      | 8338      | CHEMCAD                          |
| total price, pump+motor            | \$      | 25815     |                                  |
| pump+motor installed price         | \$      | 72282     |                                  |
| Electrical Power                   |         |           |                                  |
| pump efficiency                    | 0.79    |           |                                  |
| pump input power                   | kW      | 25.040    | CHEMCAD                          |
| operating time                     | h       | 8760      |                                  |
| pump power                         | kWh     | 219350    |                                  |
| power cost per unit                | \$/kWh  | 0.0646    |                                  |
| power cost                         | \$      | 14170     |                                  |
| Total cost                         | \$      | \$167,075 |                                  |