

# CH402 Chemical Engineering Process Design

Class Notes L10

Heat Exchanger Design II  
(Solution of 14-16 with Equation 14-91)

(These slides apply to CC NXT 1.2.0 only)

# WPR 1 – L12– WARNO

Date – 9 February 2026, B&D Hours.

Coverage – Lessons 1-11 (Chapters 12 and 14 and Labs 1-3).

(1) Heat Exchangers – CHEMCAD 3-step method.

- *Simple mode*, including flow rates and exchanger specs.
- *Sizing mode*, including area, number and length of tubes, resistances, Reynolds numbers, and pressure drops.
- *Simulation mode*, including outlet temperatures and exchanger costs.
- Three different exchangers, one for each step.
- Apply equation 14-91 as in problem 14-16.

(2) Pumps and Pipe flow – static and dynamic losses, pump characteristics curve, CHEMCAD pipes, pumps, nodes, and compressors. Be able to explain static and dynamic head.

(3) CHEMCAD and textbook costing tools, especially for heat exchangers, pipes, pumps, compressors.

3 problems, 200 points (80/60/60), 55 minutes

Make sure you understand Problem Sets 1-5 and Labs 1-3.

**Problem 14-16**

Air used in a catalytic oxidation process is to be heated from 15 to 270 °C before entering the oxidation chamber. The heating is accomplished with the use of product gases, which cool from 380 to 200 °C. A steel one-pass shell-and-tube exchanger with cross-flow on the shell side has been proposed. The average absolute pressure on both the tube side and the shell side is 1010 kPa, with the hot gasses being sent through the tubes. The flow rate for the air has been set at 1.9 kg/s. The inside and outside diameters for the tubes are 0.0191 and 0.0254 m, respectively. The tubes will be arranged in line with a square pitch of 0.0381 m. The exchanger operates for 8000 h/yr. The properties of the hot gases can be considered identical to those of air. The cost data for the exchanger are given in Figure 14-19 (p. 682).

Installation costs are 15% of purchased cost, and annual fixed charges including maintenance are 20% of the installed cost. The energy cost is \$0.12/kWh. Under these conditions, determine the most appropriate tube length and purchased cost for the optimum heat exchanger.

# Annual cost of heat exchanger operation

**Important!**

$$C_T = \underbrace{A_0 \cdot K_F \cdot C_{A_0}}_{\text{Fixed annual costs}} + \underbrace{\dot{m}_u \cdot H_y \cdot C_u}_{\text{Utility fluid costs}} + \underbrace{A_0 \cdot E_i \cdot H_y \cdot C_i}_{\text{Tube-side pumping costs}} + \underbrace{A_0 \cdot E_0 \cdot H_y \cdot C_0}_{\text{Shell-side pumping costs}}$$

PTW Eq. 14-91, p. 739

$C_T$  Total annual costs, dollars/yr

$A_0$  Outside tube area,  $m^2$

$K_F$  Annual fixed charges factor (maintenance, etc) as a fraction of installed cost, dimensionless

$C_{A_0}$  Installed cost of the heat exchanger per unit outside tube area, dollars/ $m^2$

$\dot{m}_u$  Mass flow rate of utility fluid, kg/hr

$H_y$  Hours of operation per year

$C_u$  Cost of utility fluid, dollars/kg

$E_i$  Power loss due to fluid flow inside heat exchanger tubes per unit outside tube area,  $N \cdot m/s$  per  $m^2$

$C_i$  Cost of supplying 1  $N \cdot m$  to pump fluid through the inside of the tubes, dollars/ $N \cdot m$

$E_0$  Power loss experienced on the shell side per unit outside tube area,  $N \cdot m/s$  per  $m^2$

$C_0$  Cost of supplying 1  $N \cdot m$  to pump fluid through the shell side, dollars/ $N \cdot m$

This will be explored in detail in Lesson 11. Today – CHEMCAD base “design” case.

The screenshot shows two overlapping windows from a software interface. The 'Engineering Units' window on the left has a 'System Profiles' section where 'Common SI' is highlighted with a red arrow. In the 'Fundamental' section, red arrows point to 'sec' for Time, 'kPa' for Pressure, 'J' for Enthalpy, and 'kJ' for Work. The 'User Profiles' section has 'Chapter14' selected. The 'Select Components' window on the right shows a table of available components. Red arrows point to 'Nitrogen' and 'Oxygen' in the 'Selected Components' list on the right side of this window.

**Engineering Units**

Current Flowsheet Settings: Chapter 14

**System Profiles**

English  
Default Profile

**Common SI**

Formal SI

Metric

**User Profiles**

ALT SI

Research

**Chapter14**

Set Default Delete

**Fundamental**

Time sec

Mole/Mass kg

Temperature C

Pressure kPa

Enthalpy J

Work kJ

**Dimensions**

Length m

Thickness m

Diameter m

Area m<sup>2</sup>

Liquid Volume m<sup>3</sup>

Vapor Volume m<sup>3</sup>

**Pipe Table Selection**

Default pipe table for Pipe, Orifice, and line sizing tool.

ASME (B36.10M-2015, B36.19M-2004)

Help

**Select Components**

Available Components:

ID	Name	CAS ...	For...	Last Modified
1	Hydrogen	1333-74-0	H2	2016/07/01 08:36:47
2	Methane	74-82-8	CH4	2016/07/01 08:36:47
2	Methyl hydride	74-82-8	CH4	2016/07/01 08:36:47
3	Bimethyl	74-84-0	C2H6	2016/07/01 08:36:47
3	Dimethyl	74-84-0	C2H6	2016/07/01 08:36:47
3	Ethane	74-84-0	C2H6	2016/07/01 08:36:47
3	Ethyl hydride	74-84-0	C2H6	2016/07/01 08:36:47
3	Methylmethane	74-84-0	C2H6	2016/07/01 08:36:47
4	Propyl hydride	74-98-6	C3H8	2016/07/01 08:36:47
4	Dimethylmethane	74-98-6	C3H8	2016/07/01 08:36:47
4	Freon 290	74-98-6	C3H8	2016/07/01 08:36:47
4	n-Propane	74-98-6	C3H8	2016/07/01 08:36:47
4	Propane	74-98-6	C3H8	2016/07/01 08:36:47
5	Isobutane	75-28-5	C4H10	2016/07/01 08:36:47

Search:

Options Advanced

**Selected Components**

Top Up Down Bottom

Nitrogen

Oxygen

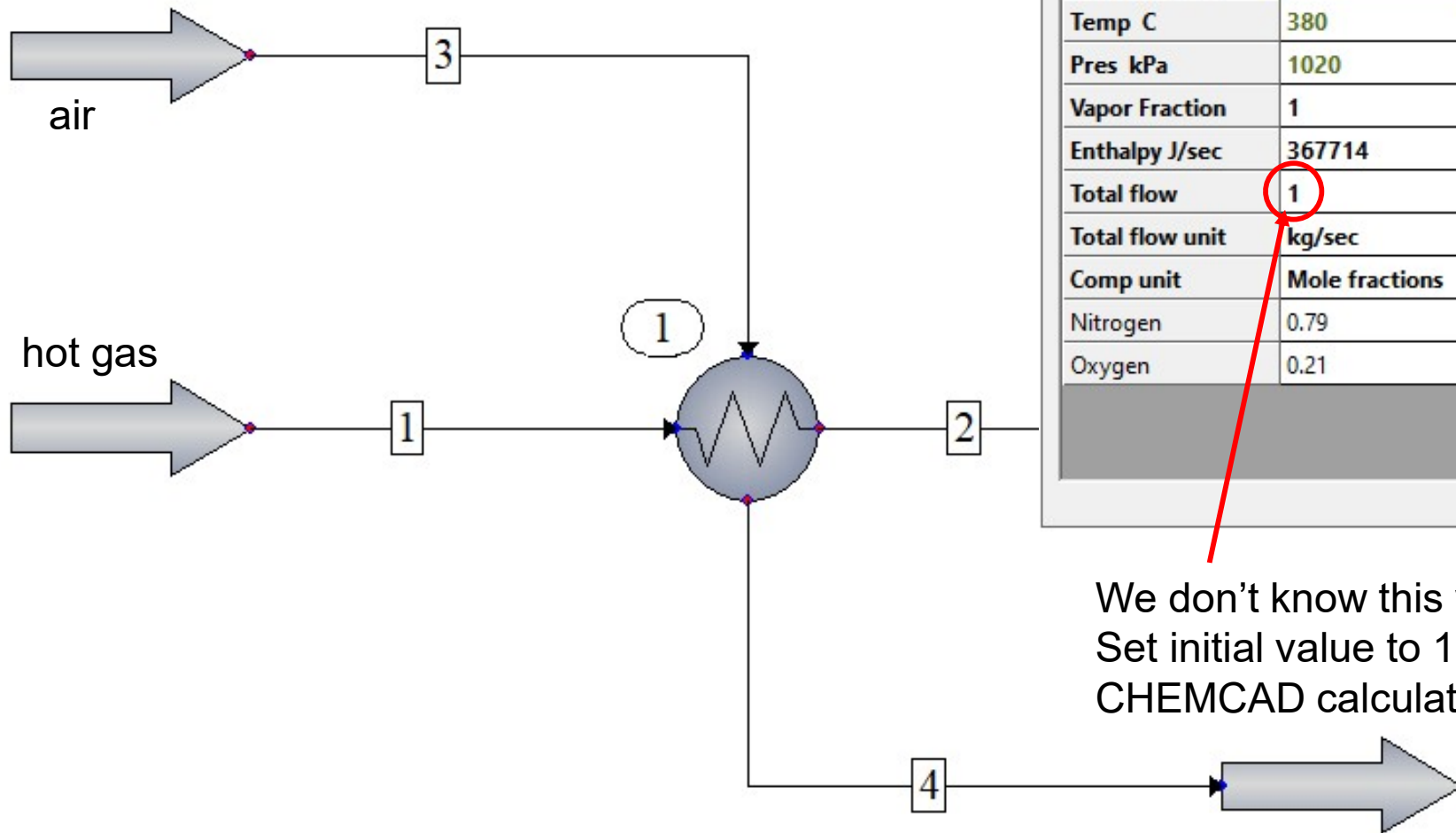
Delete Copy

Format Engineering Units:  
Common SI  
Time – seconds  
Pressure – kPa  
Enthalpy – J  
Work – kJ

Thermophysical Select  
Components:  
Nitrogen and  
Oxygen  
(Do not use “Air”)

Thermodynamics Wizard:  
SRK for K and H

# Level 1 Flowsheet



Edit Streams

Flash Cancel OK

Stream No.	1	3
Stream Name		
Temp C	380	15
Pres kPa	1020	1020
Vapor Fraction	1	1
Enthalpy J/sec	367714	-23977.57
Total flow	1	1.9
Total flow unit	kg/sec	kg/sec
Comp unit	Mole fractions	Mole fractions
Nitrogen	0.79	0.79
Oxygen	0.21	0.21

We don't know this yet.  
Set initial value to 1 kg/s  
CHEMCAD calculates it.

# Level 1 Specs

**Heat Exchanger (HTXR) -**

Specifications | Misc. Settings | Cost Estimations

Simulation mode: 0 Enter specifications (CHEMCAD simulation) ID: 1

Utility option: 3 Calculate flow of stream 1

Pressure drop: (default = 0)

Stream 1 kPa

Stream 3 kPa

Temperature stream 2 200 C

Temperature stream 4 270 C

Vapor fraction stream 2

Vapor fraction stream 4

Subcooling stream 2

Subcooling stream 4

Superheat stream 2

Superheat stream 4

Heat duty (specified) J/sec

Delta temperature specifications:

Minimum delta temperature

Hot outlet - cold inlet

Hot inlet - cold outlet

Stream 2 - stream 4

Stream 2 - stream 1

Stream 4 - stream 3

Heat transfer coefficient and area specification:

Specifying both U and A counts as a single thermal specification.

Heat transfer coefficient (U) W/m<sup>2</sup>-K

Area (per shell) m<sup>2</sup>

Help Cancel OK

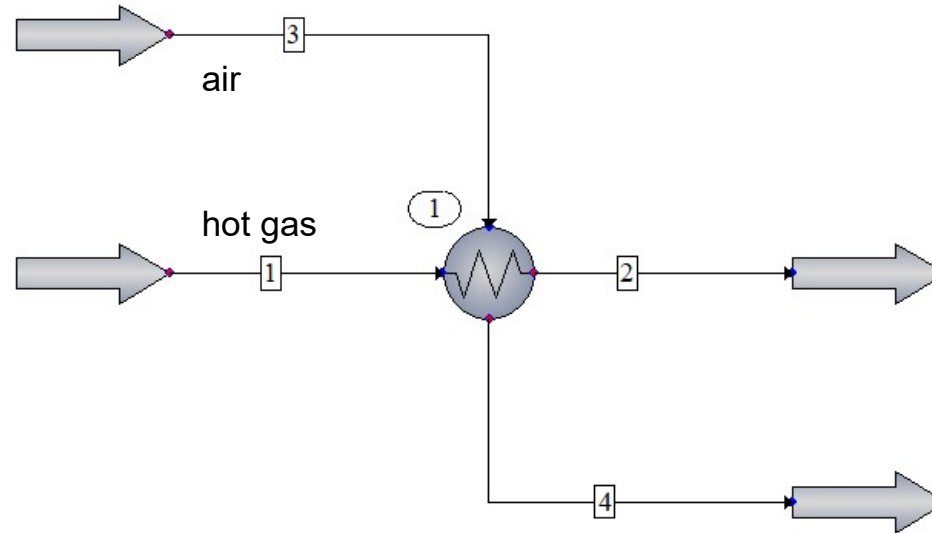
*The flowrate of stream 1 will be recalculated*

Tells CHEMCAD to  
calculate the flow rate of  
hot gases in stream 1

Click "OK" then "Run." Verify that the flow rate of hot gas is 2.6397 kg/s in stream 1. This completes "Level 1" design.

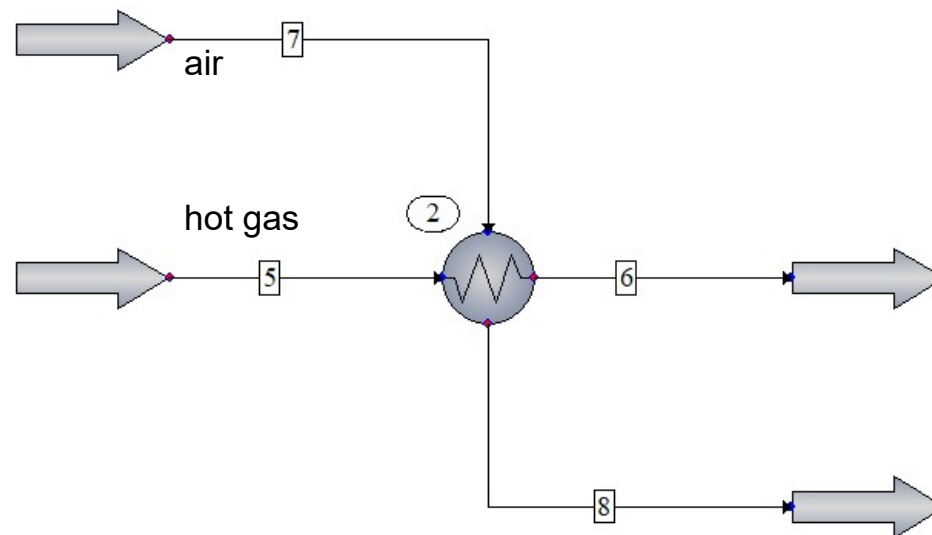
# Level 2 Design

## Step 1



In Step 1, CHEMCAD solved mass and energy balances and determined unknown hot gas flow rate.

## Step 2 – Copy and Paste



In Step 2, CHEMCAD uses mechanical details to optimize the exchanger in terms of total purchased cost.

Proceed to Sizing -> Shell and Tube, and enter unit 2



# General Specs

In the CCTherm tab, in the Configuration Group, click “General,” and then enter “5” for the stream entering tube side. This opens the General Specs window.

The screenshot shows the 'General Specifications' window with the 'General Information' tab selected. The 'TEMA shell type' is set to 'X - Cross Flow'. A red box labeled 'Cross flow on the shell' has an arrow pointing to this dropdown. Below, the 'Tube Side' and 'Shell Side' sections are visible. In the 'Tube Side' section, the 'Fouling factor' and 'Optional h Coeff.' fields are empty. A red box labeled 'Delete fouling factors' has an arrow pointing to the 'Fouling factor' field. The 'Shell Side' section also has empty 'Fouling factor' and 'Optional h Coeff.' fields. At the bottom, the 'For fouling rating calculation' dropdown is set to 'Delete fouling factors'. The window has 'Help', 'Cancel', and 'OK' buttons at the bottom.

General Specifications

General Information Modeling Methods

TEMA class/ standard TEMA R

Orientation Horizontal

TEMA front end head A - Channel Removable Cover

TEMA shell type X - Cross Flow

TEMA rear end head type L - Fixed Tubesheet (A head)

Tube Side

Stream name

Process type Sensible Flow

Fouling factor m2-K/W

Optional h Coeff. W/m2-K

Shell Side

Stream name

Process type Sensible Flow

Fouling factor m2-K/W

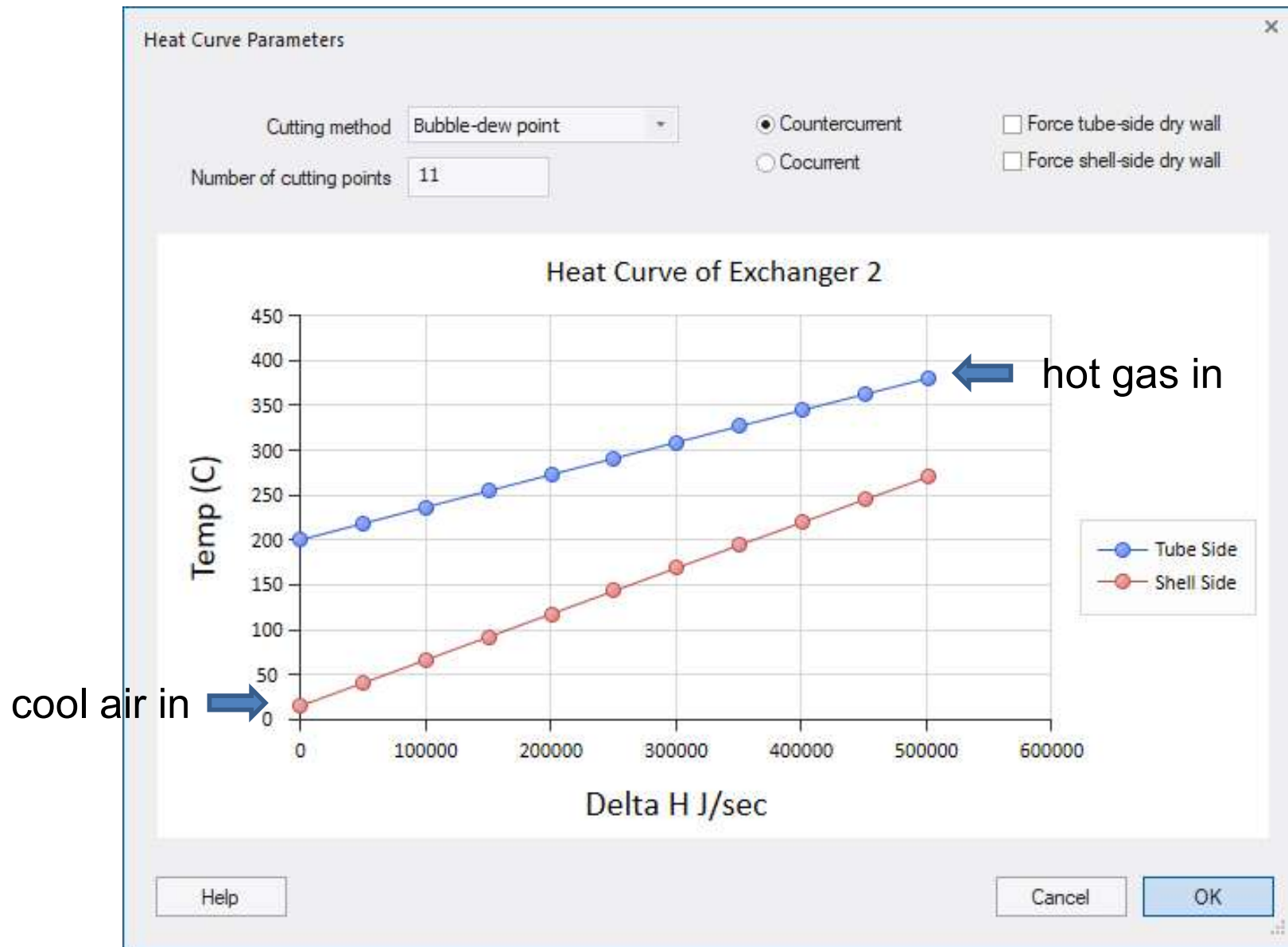
Optional h Coeff. W/m2-K

For fouling rating calculation Delete fouling factors

Help Cancel OK

# Heat Curves

It is a good idea to look at the heating-cooling curves. Proceed to CCTherm Configuration Group -> Heat Curve Specification



# Design Constraints

**Design Constraints**

**Design Criteria**

Allowable tube pressure drop	34.473801	kPa
Allowable shell pressure drop	34.473801	kPa
Allowable tube velocity	76.199997	m/sec
Allowable shell velocity	76.199997	m/sec
Prefer tube length/shell diameter ratio	12	
Minimum excess %		

**Sizing nozzle**

- ☒ Tube, inlet
- ☒ Tube, outlet
- ☒ Shell, inlet
- ☒ Shell, outlet

**Limits of Design Variables**

	Lower Limits	Upper Limits	
Tube Length	0.91439998	20	m
Shell Diameter	0.1524	9	m
Baffle Cut	15	45	Percent of diameter
Baffle Spacing	0.050799999	3.175	m

☐ Optimize number of tube passes

Help Cancel OK

CCTherm Configuration Group -> General Dropdown -> Design Constraints

# Tube Specs

Tube Specifications

Number of tubes *	1396	
Number of tube passes *	1	
Tube outer diameter	.0254	m
Tube wall thickness	.00315	m
Tube length *		m
Roughness factor	1.5748e-06	m
Tube pattern	Square (90)	
Tube pitch	.0381	m
Trufin tube code	Plain tube	
Turbulator	No Turbulator	
Tubesheet thickness	.0254	m
Number of tubesheets	2	

\* Field may be recalculated when design calculation is run

Help Cancel OK

Given in problem statement

Increase tubesheet thickness to 0.0254 m

This is a TEMA spec on tubesheet thickness. Generally, it must match the tube OD.

# Shell Specs

Shell Specifications

Shell diameter \* 0.99059999 m Calculate tube count

Number of exchangers in parallel 1

Number of exchangers in series 1

Untubed area/OTL area of tube sheet

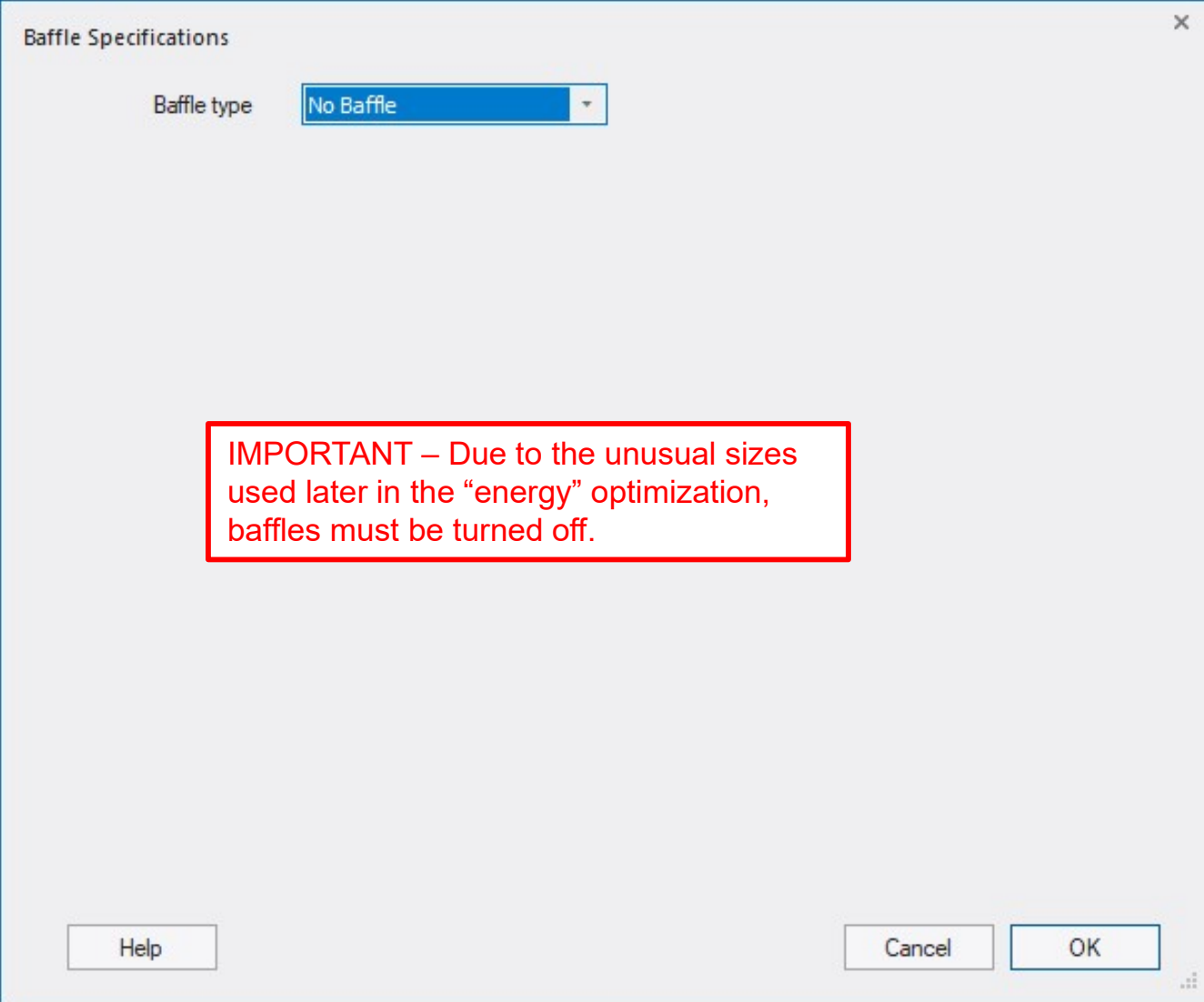
Impingement protection Use impingement plates

Accept all defaults here. We will change these later.

\* Field may be recalculated when design calculation is run

Help Cancel OK

# Baffle Specs



A screenshot of a software dialog box titled "Baffle Specifications". The dialog has a light gray background and a blue border. At the top left is the title "Baffle Specifications" and a close button (X) at the top right. Below the title is a label "Baffle type" followed by a dropdown menu showing "No Baffle". In the center of the dialog, there is a red-bordered box containing red text. At the bottom, there are three buttons: "Help" on the left, and "Cancel" and "OK" on the right. A small icon of three dots is visible in the bottom right corner of the dialog area.

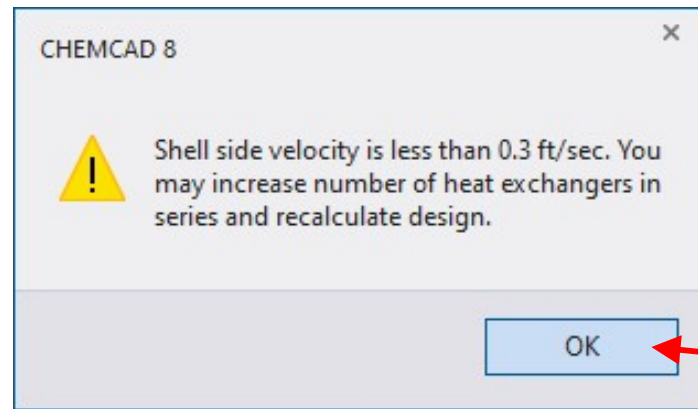
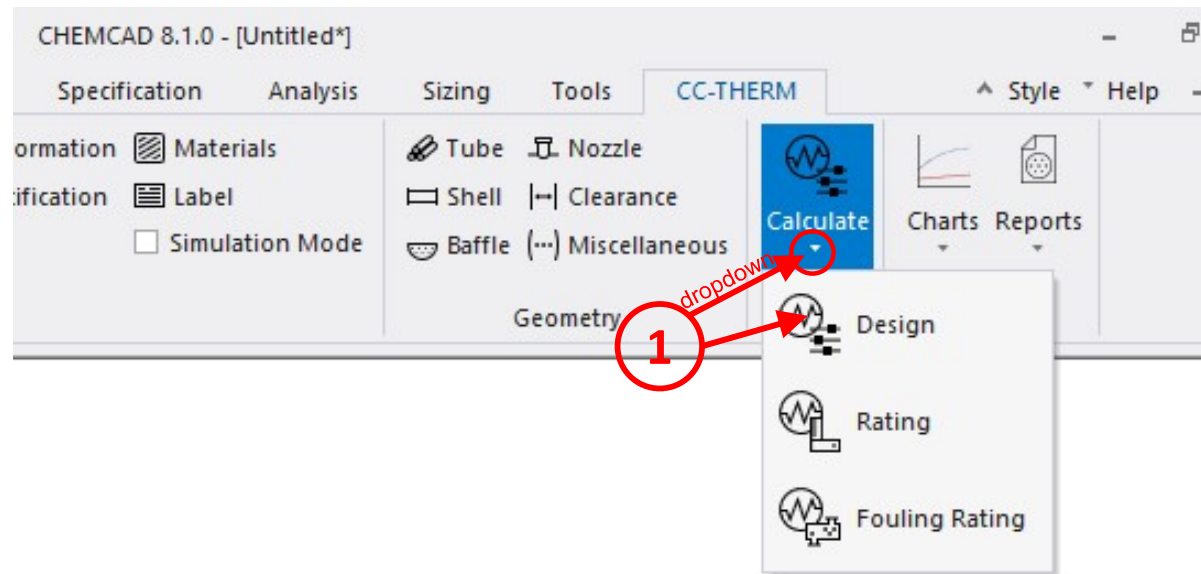
Baffle Specifications

Baffle type No Baffle

IMPORTANT – Due to the unusual sizes used later in the “energy” optimization, baffles must be turned off.

Help Cancel OK

# Calculate: Design





## TABULATED ANALYSIS

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## Overall Data:

Area Total	m2	224.15	% Excess		2.72
Area Required	m2	217.08	U Calc.	W/m2-K	19.61
Area Effective	m2	222.98	U Service	W/m2-K	19.09
Area Per Shell	m2	222.98	Heat Duty	J/sec	5.01E+05
Weight LMTD C	144.27	LMTD CORR Factor	0.8154	CORR LMTD C	117.63

## Shell-side Data:

Film Coef.	W/m2-K	24.55	Reynolds No.		1502
Allow Press. Drop	kPa	34.47	Calc. Press. Drop	kPa	16.32
Inlet Nozzle Size	m	0.13	Press. Drop/In Nozzle	kPa	1.82
Outlet Nozzle Size	m	0.09	Press. Drop/Out Nozzle	kPa	2.63
			Mean Temperature	C	142.50
Rho V2 IN	kg/m-sec2	1760.30	Press. Drop (Dirty)	kPa	27.74

Low Reynolds Number.

## Tube-side Data:

Film Coef.	W/m2-K	130.72	Reynolds No.		20904
Allow Press. Drop	kPa	34.47	Calc. Press. Drop	kPa	13.94
Inlet Nozzle Size	m	0.13	Press. Drop/In Nozzle	kPa	3.72
Outlet Nozzle Size	m	0.10	Press. Drop/Out Nozzle	kPa	2.87
Interm. Nozzle Size	m	0.00			
Velocity	m/sec	5.06			

## Resistances:

Shell-side Film	m2-K/W	0.04073
Shell-side Fouling	m2-K/W	0.00000
Tube Wall	m2-K/W	0.00008
Tube-side Fouling	m2-K/W	0.00000
Tube-side Film	m2-K/W	0.00765
Reference Factor (Total outside area/inside area based on tube ID)		1.330

## Pressure Drop Distribution:

Tube Side		Shell Side			
Inlet Nozzle	kPa	3.7201	Inlet Nozzle	kPa	1.8239
Tube Entrance	kPa	0.0389	Impingement	kPa	1.1442
Tube	kPa	1.0672	Bundle	kPa	0.0136
Tube Exit	kPa	0.0686	Outlet Nozzle	kPa	2.6325
End	kPa	0.0000	Total Fric.	kPa	4.4700
Outlet Nozzle	kPa	2.8731	Total Grav.	kPa	-0.0713
Total Fric.	kPa	7.7678	Total Mome.	kPa	11.9172
Total Grav.	kPa	0.0559	Total	kPa	16.3159
Total Mome.	kPa	6.1167			
Total	kPa	13.9405			

## Shell:

Shell O.D.	m	0.81
Shell I.D.	m	0.79
Bonnet I.D.	m	0.79
Type		AXL
Imping. Plate	Impingement Plate	

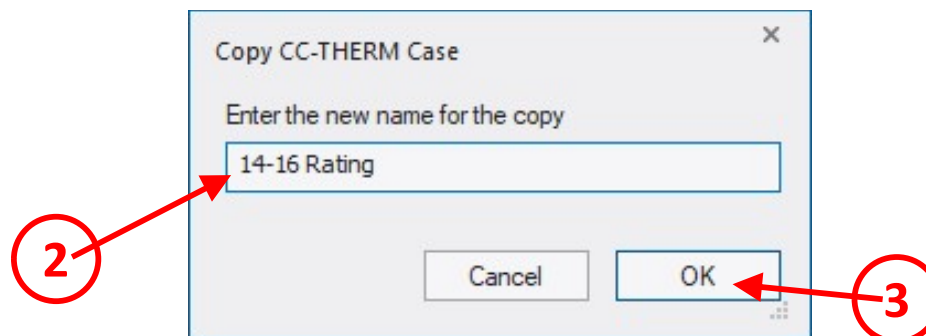
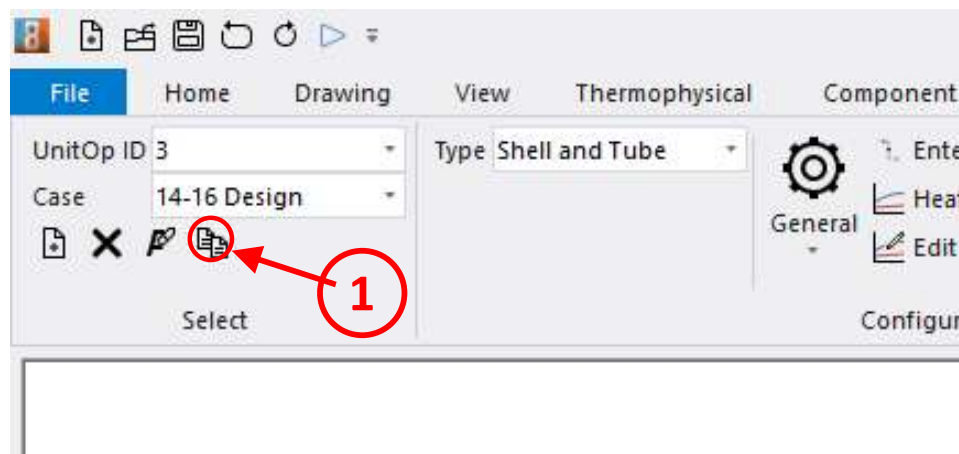
## Tubes:

Number		288
Length	m	9.75
Tube O.D.	m	0.025
Tube I.D.	m	0.019
Tube Wall Thk.	m	0.003
No. Tube Pass		1
Inner Roughness	m	0.0000016
Number of tubesheets		2



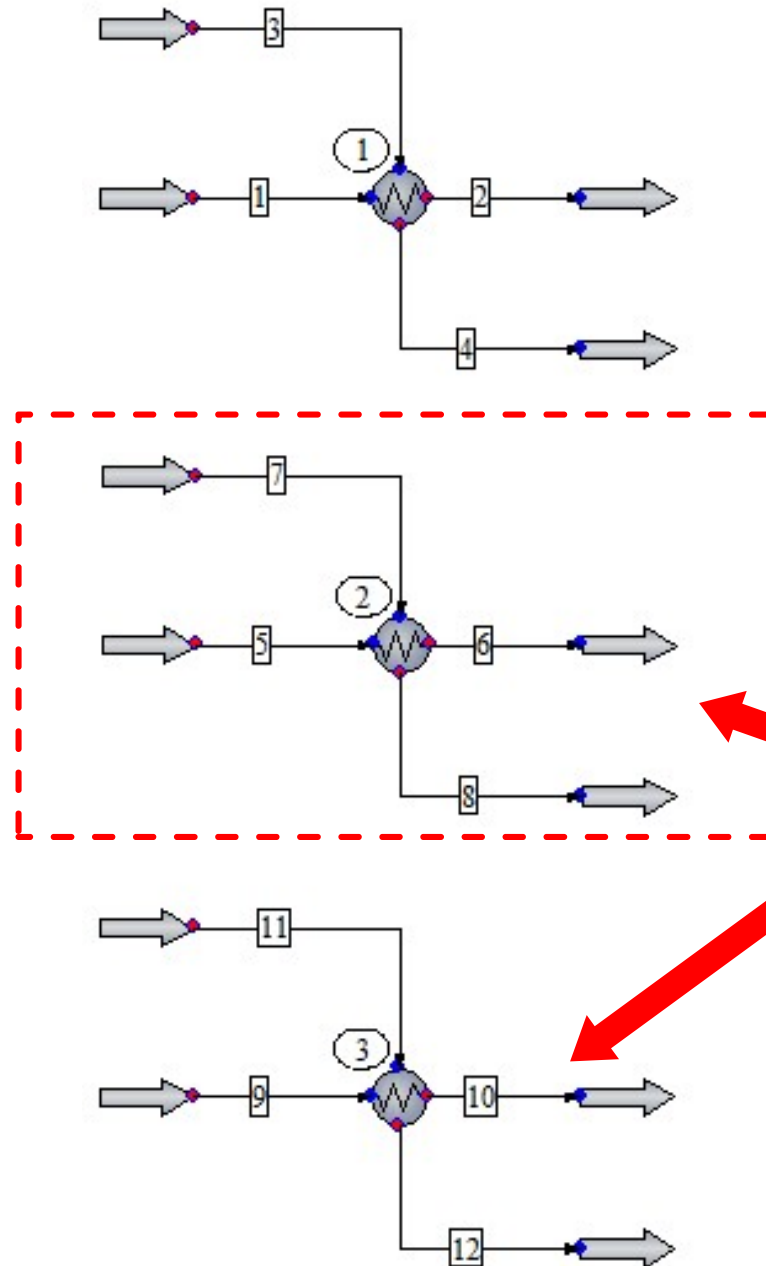
# Create a Copy of Your CCTherm Design

Create a copy of your CCTherm design. This guards against losing your work through mistakes. In the CCTherm “Select” Group -> Click “Copy CCTherm Case”



# Level 3 – Shell and Tube Simulation

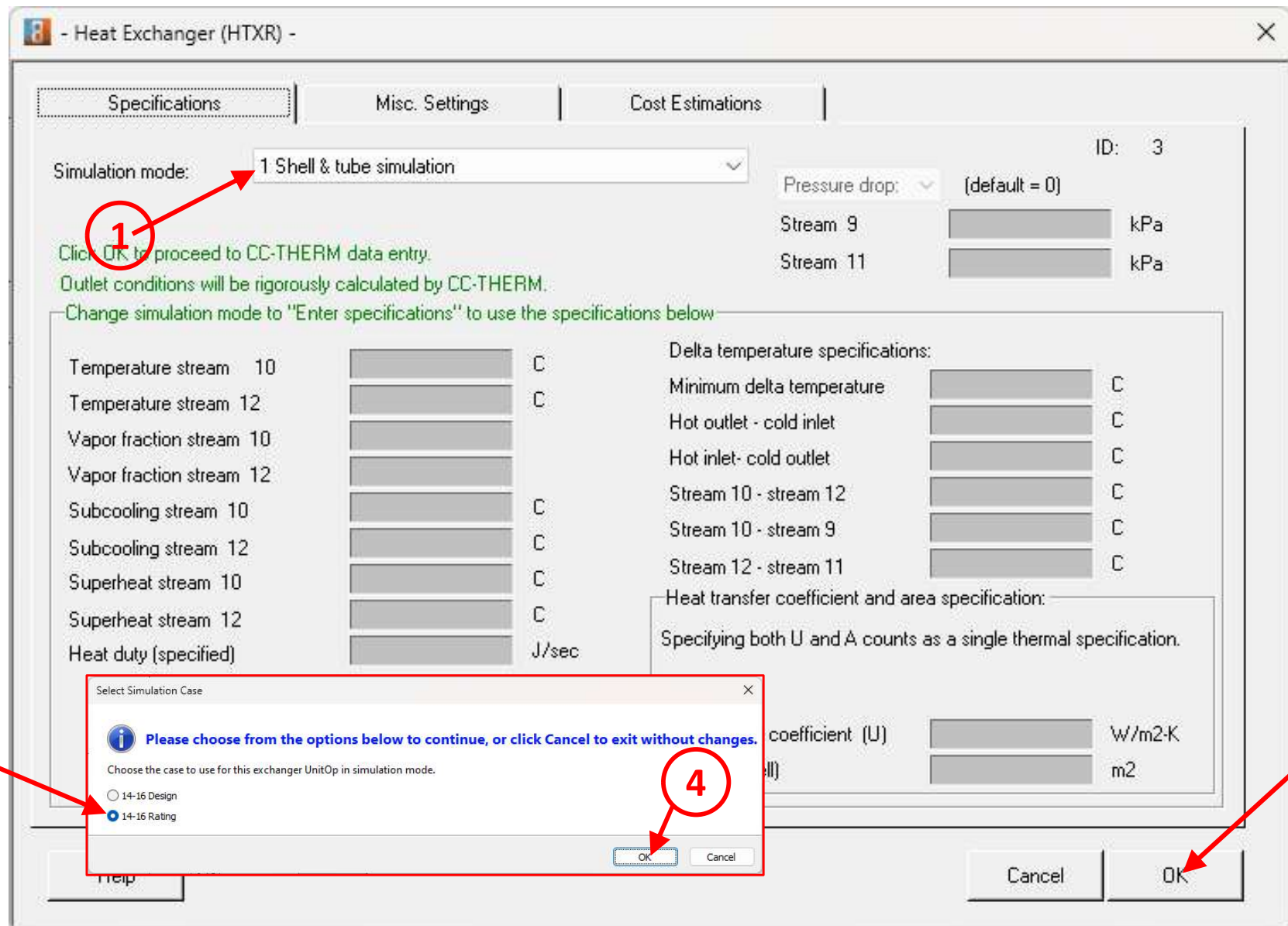
Copy and Paste Exchanger 2 (creating exchanger 3)



Copy this exchanger and past it here.

# Change Mode to Simulation

Copy and Paste Exchanger 2 (creating exchanger 3), double-click the exchanger, and change simulation mode to “1 Shell & tube simulation”

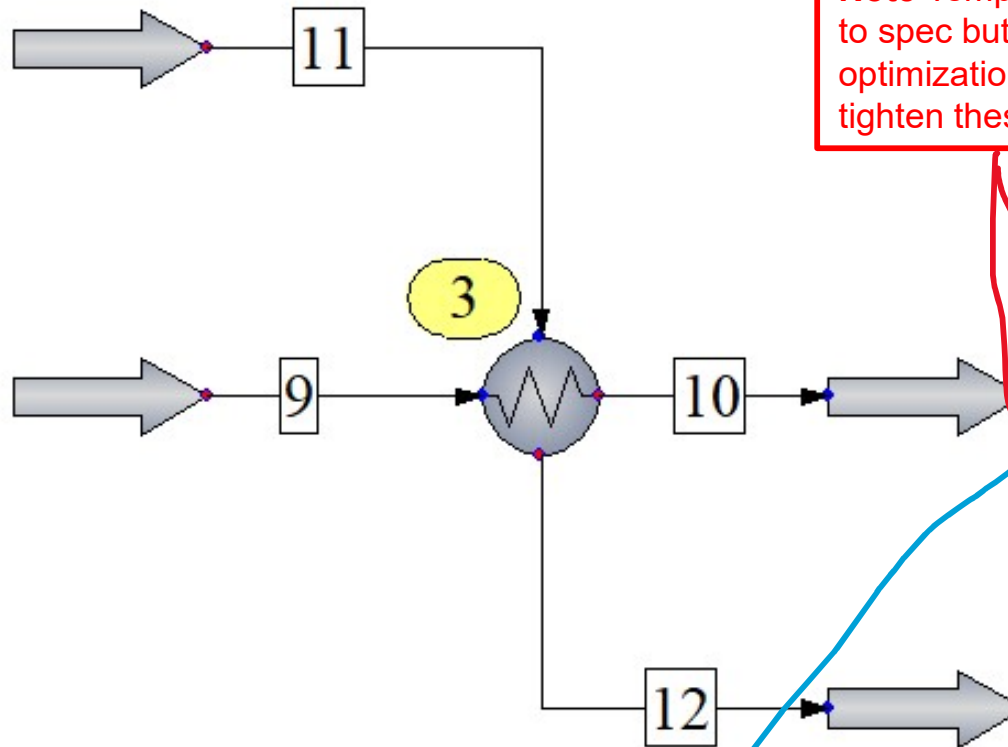


# Run the Simulation

Checking results shows that outlet streams are slightly off spec based on percent excess safety factor.

ID	11
T	15.00 C
P	1020.00 kPa
W	1.90 kg/sec

ID	9
T	380.00 C
P	1020.00 kPa
W	2.64 kg/sec



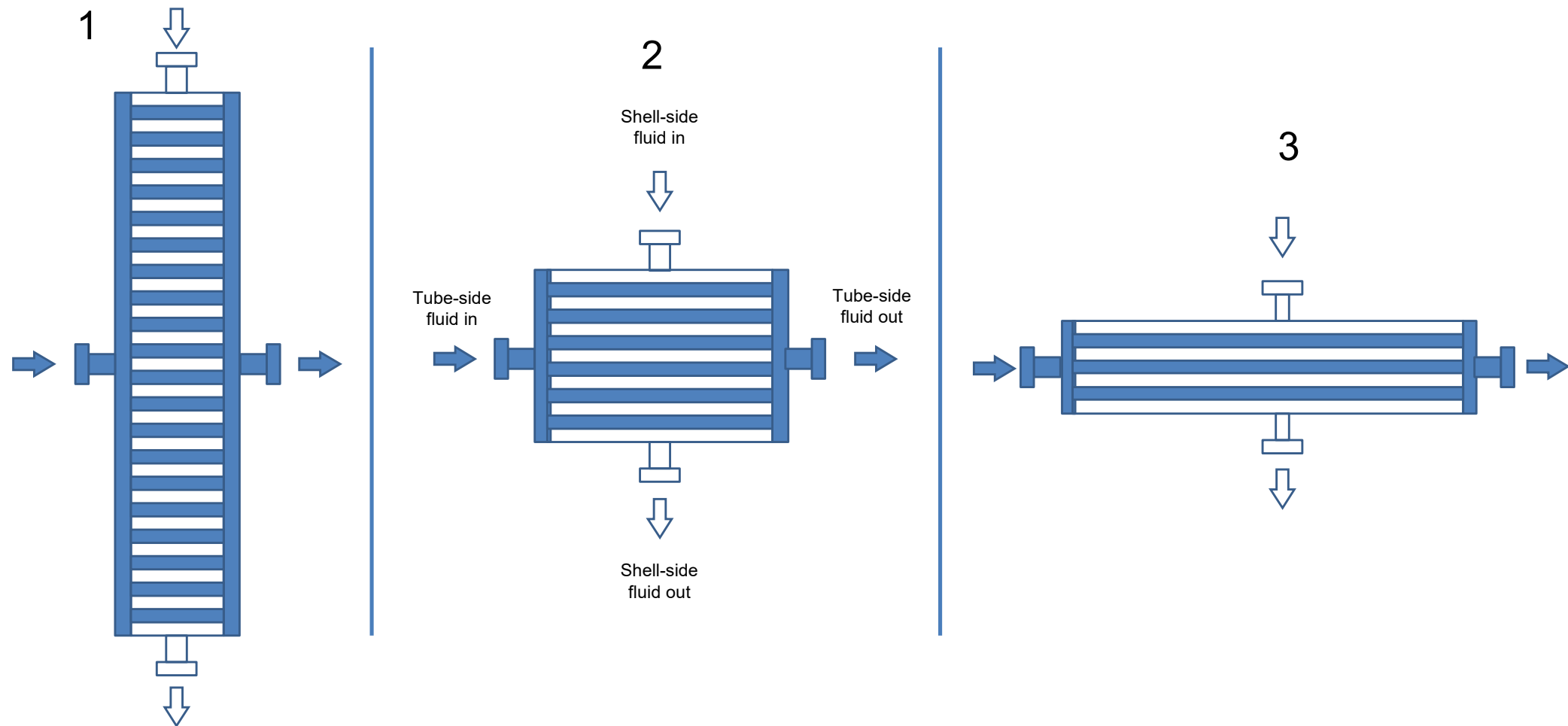
**Note** Temperatures are close to spec but for more precise optimization, we will need to tighten these up.

ID	10
T	198.54 C
P	1006.06 kPa
W	2.64 kg/sec

ID	12
T	272.00 C
P	1003.23 kPa
W	1.90 kg/sec

**Note** Outlet pressures give average pressure close to spec. Recall from problem statement that the average absolute pressure on both the tube side and the shell side is 1010 kPa.

# What happens to P-drop when we go from 1 to 2 to 3?



This affects cost to push fluids.

# Update Cost Index and Run Costing

Heat Exchanger (HTXR) -

Specifications | Misc. Settings | Cost Estimations

ID: 3

☒ Run the costing report after running the unit

Cost model: Shell and tube

Exchanger type: Fixed head

Evaporator type: Forced circulation

Design pressure: kPa

Install factor: 1.15

Material factor: 1

Pressure factor: 1.15813

Type factor: 0.655386

Material selection for this model: Shell and tube, Carbon steel

Calculated Results:

- Basic cost
- Total purchase cost
- Total installed cost
- Utility Cost
- Purchase Cost

Chemical Engineering Plant Cost Index

Year/Month Selection for the Cost Index

Year: 2026, Month: February, Source: Database

Type: Cost Index

CE Index	830.50
Equipment	1045.80
Heat exchangers and tanks	815.70
Process machinery	1057.50
	1410.40
	620.50
Pumps and compressors	1677.10
Electrical equipment	917.90
Structural supports and misc.	1142.00
Construction labor	390.30
Buildings	835.10
Engineering and supervision	313.20

Help

Cancel OK

Activate the costing tool.

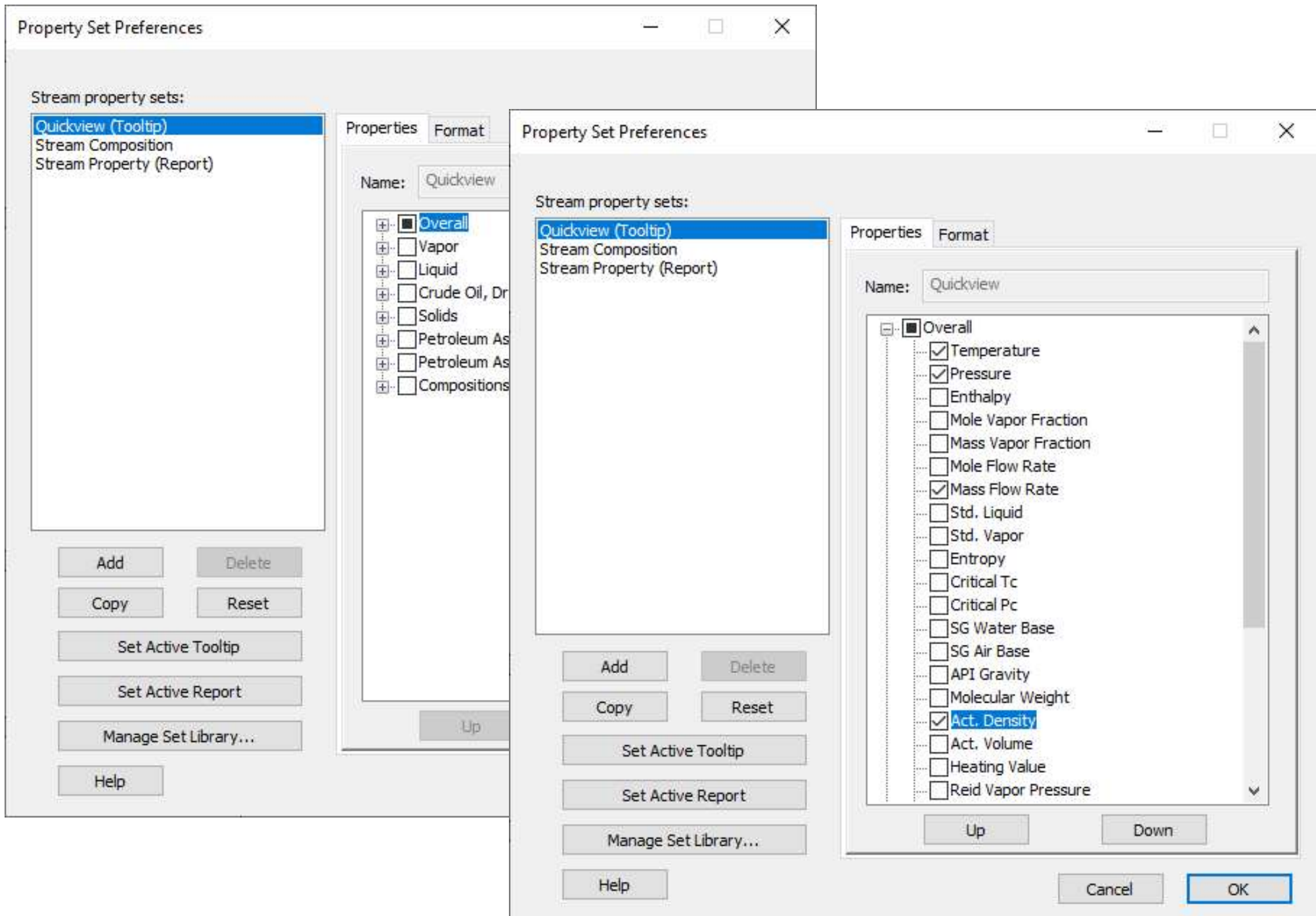
Make sure month and year are correct..

Heat exchanger index from course web site.

Add "costing\_data" to CHEMCAD directory.

In the Home tab, in the Results Group, click  (property sets)

Slide 23





mass flow rate has units of  $\text{kg/s}$   
and is volumetric flow rate  
multiplied by density

$$\frac{\text{m}^3}{\text{s}} \cdot \frac{\text{kg}}{\text{m}^3} = \frac{\text{kg}}{\text{s}}$$

power in watts

$$\frac{\text{kg} \cdot \text{m}^2}{\text{s}^3}$$

meters of head

$\text{m}$

gravitational acceleration  
 $g = 9.8 \text{ m/s}^2$

$$\frac{\text{kg}}{\text{m} \cdot \text{s}^2} \cdot \frac{\text{m} \cdot \text{s}^2}{\text{kg}} = \text{m}$$

$$\text{m} \cdot \frac{\text{m}}{\text{s}^2} \cdot \frac{\text{kg}}{\text{s}} = \frac{\text{kg} \cdot \text{m}^2}{\text{s}^3}$$

$$\frac{\text{m}^2}{\text{s}^2}$$

$$\frac{\text{kg}}{\text{s}}$$

$$\frac{\text{kg}}{\text{m}^3}$$

density  $\rho$  has  
units of  $\text{kg/m}^3$

$$\frac{\text{kg}}{\text{m} \cdot \text{s}^2}$$

pressure in pascals

$$\frac{\text{kg}}{\text{m} \cdot \text{s}^2} \cdot \frac{\text{m}^3}{\text{kg}} = \text{m}^2$$

$$\frac{\text{kg} \cdot \text{m}^2}{\text{s}^3}$$



**Problem 14-16. Cadet Template****"sizing" checks are required**

Optimal Heat Exchanger Design

Yellow - obtained from CHEMCAD simulations

Light Blue - Values are derived from specs and do not change.

White - excel calculations - verified with "checks" (results from CC design)

Spreadsheet for evaluating Equation 14-91				"sizing" checks
Number of tubes	$N_t$	dimensionless	288	
Length of tubes	$L$	m	9.750	
Installed cost, CC	$C$	\$	\$82,011	
Tube outer diameter	$D_o$	m	0.0254	
Tube inner diameter	$D_i$	m	0.0191	
Tube wall thickness	$x$	m	0.00315	
Outside area of tubes	$A_o$	$m^2$	224.1	
Installed cost per area	$C_{Ao}$	$\$/m^2$	\$366	
Tube-side (hot gas) flow rate, CC	$m_i$	kg/s	2.6397	
Tube-side inlet fluid density, CC	$r_{ti}$	$kg/m^3$	5.3956	
Tube-side outlet fluid density, CC	$r_{to}$	$kg/m^3$	7.3697	
Tube-side pressure drop, CC	$Dp_i$	kPa	13.9405	
Tube-side average density	$r_t$	$kg/m^3$	6.3803	
Tube-side power loss per area	$E_i$	Nm/s per $m^2$	25.7402	
Shell-side (air) flow rate	$m_o$	kg/s	1.9000	
Shell-side inlet fluid density, CC	$r_{si}$	$kg/m^3$	12.3104	
Shell-side outlet fluid density, CC	$r_{so}$	$kg/m^3$	6.3576	
Shell-side pressure drop, CC	$Dp_o$	kPa	16.7692	
Shell-side average density	$r_s$	$kg/m^3$	9.3340	
Shell-side power loss per area	$E_o$	Nm/s per $m^2$	15.2341	
Hours of operation per year	$H_y$	h/y	8000	
Cost of pumping power	$C_i$	$\$/kWh$	0.12	
Annual fixed charges factor	$K_F$	dimensionless	0.2	
Fixed charges		$\$/y$	\$16,402	
Tube-side pumping costs		$\$/y$	\$5,537	
Shell-side pumping costs		$\$/y$	\$3,277	
<b>Total annual cost</b>	<b><math>C_T</math></b>	<b><math>\\$/y</math></b>	<b>\$25,216</b>	

Complete this portion of the template.

Values in column D are checks to confirm your work.

Blue rows are specs or calculated from the specs from the problem and are typed in as is. These numbers do not change.

Yellow rows (red font) come from CHEMCAD exchanger 3. These numbers will change in the optimization, but not yet.

White rows are formula entries. Calculation of cells E21 and E21 (power losses) are calculated from the methods in slide 24.

Formulas are shown in slide 26.

Problem 14-16. Cadet Template			"sizing" checks are required	
Optimal Heat Exchanger Design				
Yellow - obtained from CHEMCAD simulations				
Light Blue - Values are derived from specs and do not change.				
White - excel calculations - verified with "checks" (results from CC design)				
			"sizing"	
Spreadsheet for evaluating Equation 14-91			checks	
Number of tubes	$N_t$	dimensionless	288	288
Length of tubes	$L$	m	9.750	9.750
Installed cost, CC	$C$	\$	\$82,011	\$82,011
Tube outer diameter	$D_o$	m	0.0254	0.0254
Tube inner diameter	$D_i$	m	0.0191	0.0191
Tube wall thickness	$x$	m	0.00315	= $(E11-E12)/2$
Outside area of tubes	$A_o$	$m^2$	224.1	= $PI()*E11*E8*E9$
Installed cost per area	$C_{A_o}$	$\$/m^2$	\$366	= $E10/E14$
Tube-side (hot gas) flow rate, CC	$m_i$	kg/s	2.6397	2.6397
Tube-side inlet fluid density, CC	$r_{ti}$	$kg/m^3$	5.3956	5.3956
Tube-side outlet fluid density, CC	$r_{to}$	$kg/m^3$	7.3697	7.3697
Tube-side pressure drop, CC	$Dp_i$	kPa	13.9405	13.9405
Tube-side average density	$r_t$	$kg/m^3$	6.3803	= $AVERAGE(E17:E18)$
Tube-side power loss per area	$E_i$	Nm/s per $m^2$	25.7402	= $1000*E19*E16/E20/E14$
Shell-side (air) flow rate	$m_o$	kg/s	1.9000	1.9000
Shell-side inlet fluid density, CC	$r_{si}$	$kg/m^3$	12.3104	12.3104
Shell-side outlet fluid density, CC	$r_{so}$	$kg/m^3$	6.3576	6.3576
Shell-side pressure drop, CC	$Dp_o$	kPa	16.7692	16.7692
Shell-side average density	$r_s$	$kg/m^3$	9.3340	= $AVERAGE(E23:E24)$
Shell-side power loss per area	$E_o$	Nm/s per $m^2$	15.2341	= $1000*E25*E22/E26/E14$
Hours of operation per year	$H_y$	h/y	8000	8000
Cost of pumping power	$C_i$	$\$/kWh$	0.12	0.12
Annual fixed charges factor	$K_F$	dimensionless	0.2	0.2
Fixed charges		$\$/y$	\$16,402	= $E30*E15*E14$
Tube-side pumping costs		$\$/y$	\$5,537	= $E21*E14*E28*E29/1000$
Shell-side pumping costs		$\$/y$	\$3,277	= $E27*E14*E28*E29/1000$
Total annual cost	$C_T$	$\$/y$	\$25,216	= $SUM(E32:E34)$

**Good Luck!**