CH365 Chemical Engineering Thermodynamics

Lesson 11
Application of the 1st Law to Ideal Gases

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Objectives

- 1. Explain why the internal energy of an ideal gas depends on temperature only.
- 2. Explain the relationship between C_P and ΔH and between C_V and ΔU .
- 3. Understand and be able to choose the correct equations for process calculations for an ideal gas.
- 4. Be able to describe and distinguish adiabatic, polytropic, isothermal, and isochoric processes.

General Comments Page 64

- Heat and work necessary for industrial process calculations are calculated using the equations from Chapter 2.
- These equations require enthalpy and internal energy from volume as a function of temperature and pressure.
- These PVT relationships are expressed mathematically as equations of state. The simplest realistic EOS is the ideal gas law, PV = RT.
- First, look at phase rule. L10
- Second, we will describe the general P-V-T behavior of pure fluids. L10
- Third, we will discuss the ideal gas behavior in detail. L11

Hidden Content – Take Notes

 Finally, we will discuss more realistic equations, wrapping up with generalized correlations. L12-L14

Property Relations for the Ideal Gas

Lesson 6, result of the Joule experiment.

In the absence of molecular interactions, enthalpy depends on T only

$$H = U + RT$$

$$\frac{dH}{dT} = \frac{d}{dT} (U + RT)$$

$$= \frac{dU}{dT} + \frac{d(RT)}{dT}$$

$$= \frac{dU}{dT} + R$$

$$C_{V} \equiv \left(\frac{\partial U}{\partial T}\right)_{V} = \frac{dU(T)}{dT} = C_{V}(T) \qquad (3.9) \& (2.15)$$
functions of T only
$$H \equiv U + PV = U + RT = H(T) \qquad (3.10), \text{ from } (2.10) \& (3.7)$$

$$C_{P} \equiv \left(\frac{\partial H}{\partial T}\right)_{P} = \frac{dH(T)}{dT} = C_{P}(T)$$
 (3.11) & (2.19)
Also function of T only

$$C_{P} = \frac{dH}{dT} = \frac{dU}{dT} + R = C_{V} + R$$

$$R = C_P - C_V$$
(3.12)

$$dU = C_V dT$$

$$(3.13a)$$

$$\Delta U = \int_{T_{REF}} C_V dT$$

$$(3.13b)$$

$$dH = C_P dT$$

$$(3.14a)$$

$$\Delta H = \int_{T_{REF}} T C_P dT$$

$$(3.14b)$$

Functions of T only

Q and W Equations for Process Calculations

$$dU = dQ + dW$$
 \Leftrightarrow $dQ = dU - dW$

$$dU = C_V dT \qquad dQ = C_V dT + P dV \qquad dW = -P dV$$

$$(3.15) \qquad dW = -P dV$$

$$(1.3)$$

$$P = \frac{RT}{V} = P(T, V) \qquad dQ = C_V dT + RT \frac{dV}{V} \qquad dW = -RT \frac{dV}{V}$$

$$(3.17)$$

$$V = \frac{RT}{P} = V(T, P) \qquad dQ = C_P dT - RT \frac{dP}{P}$$

$$(3.18) \qquad dW = -R dT + RT \frac{dP}{P}$$

$$(3.19)$$

$$T = \frac{PV}{R} = T(P, V) \qquad dQ = \frac{C_V}{R} V dP + \frac{C_P}{R} P dV \qquad dW = -P dV$$

$$(1.3)$$

Derived on next slide.

Each of these can be derived as shown on next slide.

Where did Slide 4 Come From?

Example (row 3):

Using
$$V = \frac{RT}{P}$$
 show that $dW = -RdT + RT\frac{dP}{P}$ and $dQ = C_PdT - RT\frac{dP}{P}$
(3.18)

$$dV = \left(\frac{\partial V}{\partial P}\right)_{T} dP + \left(\frac{\partial V}{\partial T}\right)_{P} dT$$

$$V = \frac{RT}{P}$$

$$dW = -PdV$$

$$dW = -P\left(-\frac{RT}{P^{2}}dP + \frac{R}{P}dT\right) = \frac{RT}{P}dP - RdT$$

$$1.3$$

$$dU = dQ + dW \implies dQ = dU - dW \implies dQ = C_V dT + RdT - \frac{RT}{P} dP$$

$$dQ = (C_V + R) dT - \frac{RT}{P} dP$$

$$(3.13a) \qquad C_P = C_V + R$$

$$(3.12) \qquad dQ = C_P dT - RT \frac{dP}{P} \checkmark$$

Isothermal Process

(Q, W, Δ H, and Δ U with no change in temperature)

$$\Delta U = \Delta H = 0$$

(3.13b) & (3.14b)

$$Q = RT \ln \left(\frac{V_2}{V_1}\right) = -RT \ln \left(\frac{P_2}{P_1}\right)$$
 (3.20), from (3.16) & (3.18) (rows 2 and 3)

 $C_V dT = 0$

molar heat (energy per mole)

From 2.3 with $\Delta U=0$ Q = -W

$$W = -RT \ln \left(\frac{V_2}{V_1}\right) = RT \ln \left(\frac{P_2}{P_1}\right)$$
 (3.20), from (3.17) & (3.19) RdT = 0 (rows 2 and 3)

molar work (energy per mole)

$$Q = -W = RTIn\left(\frac{V_2}{V_1}\right) = -RTIn\left(\frac{P_2}{P_1}\right)$$
 (Constant T) (3.20)

Isobaric Process

(No change in pressure)

$$\Delta U = \int C_V dT \qquad \text{and} \qquad \Delta H = \int C_P dT \qquad \begin{array}{c} C_P \text{ and } C_V \text{ in} \\ \text{Appendix C or} \\ \text{assumed constant} \end{array}$$

$$dP = 0 \qquad dP = 0 \qquad dP = 0 \qquad dP = 0 \qquad dP = 0 \qquad (3.18) \text{ and } (3.19) \\ Q = \int C_P dT \qquad \text{and} \qquad W = -R(T_2 - T_1)$$

$$Q = \Delta H = \int C_P dT$$
 (Constant P)
(3.21)

Isochoric Process

(No change in volume)

$$\Delta U = \int C_V dT \quad \text{and} \quad \Delta H = \int C_P dT \qquad (3.13b) \text{ and } (3.14b)$$

$$dQ = C_V dT + RT \frac{dV}{V} \quad \text{and} \quad W = -\int P dV = 0 \qquad (3.16) \text{ and } (1.2)$$

$$Q = \int C_V dT$$

$$Q = \Delta U = \int C_V dT$$
 (Constant V) (3.22)

Adiabatic Process

$$dQ = 0$$

C_V, C_P assumed constant

(any of the dQ equations from slide 4)

Mechanically reversible adiabatic expansion or compression

$$0 = C_V dT + RT \frac{dV}{V} \qquad \Longrightarrow \qquad \frac{dT}{T} = -\frac{R}{C_V} \frac{dV}{V} \qquad \Longrightarrow$$

$$\frac{dT}{T} = -\frac{R}{C_V} \frac{dV}{V}$$

$$\frac{\mathsf{T}_2}{\mathsf{T}_1} = \left(\frac{\mathsf{V}_1}{\mathsf{V}_2}\right)^{\mathsf{N}}$$

$$0 = C_{P}dT - RT\frac{dP}{P} \qquad \Longrightarrow \qquad \frac{dT}{T} = \frac{R}{C_{P}}\frac{dP}{P} \qquad \Longrightarrow \qquad \frac{T_{2}}{T_{1}} = \left(\frac{P_{2}}{P_{1}}\right)^{R/C_{P}}$$

$$\frac{dT}{T} = \frac{R}{C_{D}} \frac{dF}{P}$$

$$\Rightarrow$$

$$\frac{T_2}{T_1} = \left(\frac{P_2}{P_1}\right)^{1/(O_1)}$$

$$0 = \frac{C_{V}}{R}VdP + \frac{C_{P}}{R}PdV \implies \frac{dP}{P} = -\frac{C_{P}}{C_{V}}\frac{dV}{V} \implies \frac{P_{2}}{P_{1}} = \left(\frac{V_{1}}{V_{2}}\right)^{C_{P}/C_{V}}$$

$$\Rightarrow$$

$$\frac{dP}{P} = -\frac{C_P}{C_V} \frac{dV}{V}$$

$$\Rightarrow$$

$$\frac{P_2}{P_1} = \left(\frac{V_1}{V_2}\right)^{C_P/C_V}$$

$$TV^{\gamma-1} = constant$$

$$TP^{(1-\gamma)/\gamma} = constant$$
(3.23b)

 $PV^{\gamma} = constant$

(3.23c)

$$\gamma \equiv \frac{\mathsf{C}_{\mathsf{P}}}{\mathsf{C}_{\mathsf{V}}}$$

$$P_2 = P_1 \cdot \left(\frac{V_1}{V_2}\right)^r$$

Adiabatic Process - Work

$$dW = dU = C_V dT$$

$$W = \Delta U = C_V \Delta T$$
(3.25)

$$\gamma \equiv \frac{C_{P}}{C_{V}} = \frac{C_{V} + R}{C_{V}} = 1 + \frac{R}{C_{V}} \qquad \text{or} \qquad C_{V} = \frac{R}{\gamma - 1}$$

$$W = C_{V} \Delta T = \frac{R \Delta T}{\gamma - 1}$$

For ideal gas with constant heat capacities in a closed, adiabatic system:

$$W = \frac{P_2V_2 - P_1V_1}{\gamma - 1}$$
 (or) $W = \frac{R(T_2 - T_1)}{\gamma - 1}$ (3.26, both equations)

For ideal gas with constant heat capacities in a closed, adiabatic, reversible system:

$$W = \frac{P_1 V_1}{\gamma - 1} \left[\left(\frac{P_2}{P_1} \right)^{(\gamma - 1)/\gamma} - 1 \right] = \frac{R T_1}{\gamma - 1} \left[\left(\frac{P_2}{P_1} \right)^{(\gamma - 1)/\gamma} - 1 \right]$$
(3.27)

Polytropic Process

"many ways" or "many paths"

$$PV^{\delta} = constant$$
 (3.23c)

$$\mathsf{TV}^{\delta-1} = \mathsf{constant}$$
 (3.23a)

$$TP^{(1-\delta)/\delta} = constant$$
 (3.23b)

δ is the "polytropic constant"

(3.23c and integral of -PdV)

$$W = \frac{RT_1}{\delta - 1} \left[\left(\frac{P_2}{P_1} \right)^{(\delta - 1)/\delta} - 1 \right]$$
 (3.27)

$$Q = \frac{(\delta - \gamma)RT_1}{(\delta - 1)(\gamma - 1)} \left[\left(\frac{P_2}{P_1} \right)^{(\delta - 1)/\delta} - 1 \right]$$
(3.37)

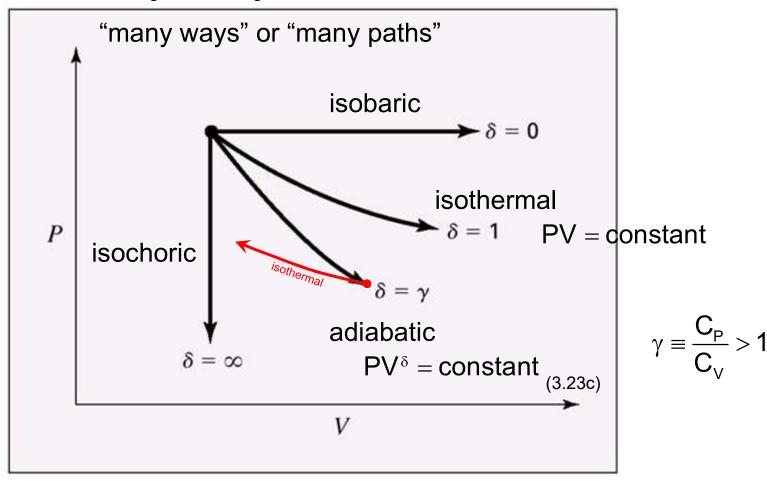
(same as 3.34 with γ replaced by δ)

$$K \equiv \frac{dQ}{dW}$$
$$\delta = (1 - \gamma)K + \gamma$$

(derivation not shown)

- Write 1st Law with definition of K
- Use differential form of ideal gas law

Polytropic Process



Paths of polytropic processes characterized by specific values of δ .

The importance of the polytropic constant δ is that is shows the general shape of the PV curve under different conditions

Irreversible Processes

For an ideal gas

Any equation for dU, Δ U, dH, or Δ H is valid regardless of the process Q and W are subject to the conditions of the derivations.

Work of an irreversible process:

- •Step 1: Determine reversible work
- •Step 2: Multiply or divide by an efficiency that gives the irreversible work

Example 3.3

Air is compressed from an initial state of 1 bar and 25 °C to a final state of 3 bar and 25 °C by three different mechanically reversible processes in a closed system:

- (a) Heating at constant volume followed by cooling at constant pressure
- (b) Isothermal compression
- (c) Adiabatic compression followed by cooling at constant volume.

Assume air to be an ideal gas with constant heat capacities, $C_V = (5/2)R$ and $C_P = (7/2)R$. Calculate the work required, heat transferred, and the changes in internal energy and enthalpy of the air for each process.

Solution: The system is one mole of air.

Additional givens:

$$R = 8.314 \text{ J mol}^{-1} \text{ K}^{-1}$$

$$V_1 = 0.02479 \text{ m}^3$$

In all cases:
$$\Delta H = \Delta U = 0$$

$$C_V = 20.785 \text{ J mol}^{-1} \text{ K}^{-1}$$

$$V_2 = 0.004948 \text{ m}^3$$

$$C_P = 29.100 \text{ J mol}^{-1} \text{ K}^{-1}$$

Example 3.3, part (a)

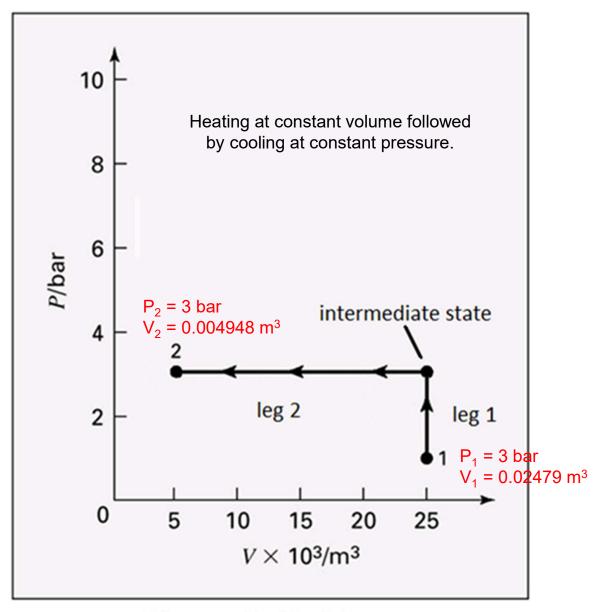


Diagram for Ex. 3.3.a

Example 3.3, part (a), cont.

Air is compressed from an initial state of 1 bar and 25 °C to a final state of 5 bar and 25 °C by three different mechanically reversible processes in a closed system:

(a) Heating at constant volume followed by cooling at constant pressure

$$\Delta H_{\text{overall}} = \Delta U_{\text{overall}} = 0$$

T is constant (25 °C)

$$\frac{P_1 \cancel{V_1}}{T_1} = \frac{P_{int} V_{int}}{T_{int}} = \frac{P_2 \cancel{V_1}}{T_{int}} \qquad T_{int \, ermediate} = T_1 \frac{P_2}{P_1} = 298.15 \cdot \left(\frac{3}{1}\right) = 894.45 \, \text{K}$$

$$Q_{leq1} = \Delta U = C_V \Delta T = (20.785)(894.45 - 298.15) = 12,394 J$$

$$Q_{leg2} = \Delta H = C_p \Delta T = (29.10)(298.15 - 894.45) = -17,352J$$

Ex. 2.7a

$$Q_{overall} = 12,391 - 17,352 = -4,958 J$$

$$\Delta U_{\text{overall}} = 0 = Q_{\text{overall}} + W_{\text{overall}} \implies W_{\text{overall}} = -Q_{\text{overall}} = 4,958 \, J$$

Example 3.3, part (b)

Air is compressed from an initial state of 1 bar and 25 °C to a final state of 3 bar and 25 °C by three different mechanically reversible processes in a closed system:

(b) Isothermal compression

$$\Delta H_{\text{overall}} = \Delta U_{\text{overall}} = 0$$

T is constant (25 °C)

Use equation 3.2 for Q and W (slide 7):

Q = -W = RT ln
$$\left(\frac{P_1}{P_2}\right)$$

= (8.314)(298.15)ln $\left(\frac{1}{3}\right)$
= -2,723.26 J

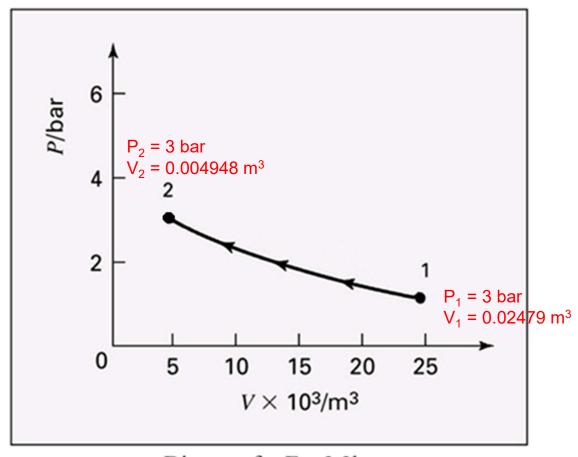


Diagram for Ex. 3.3b

Example 3.3, part (c)

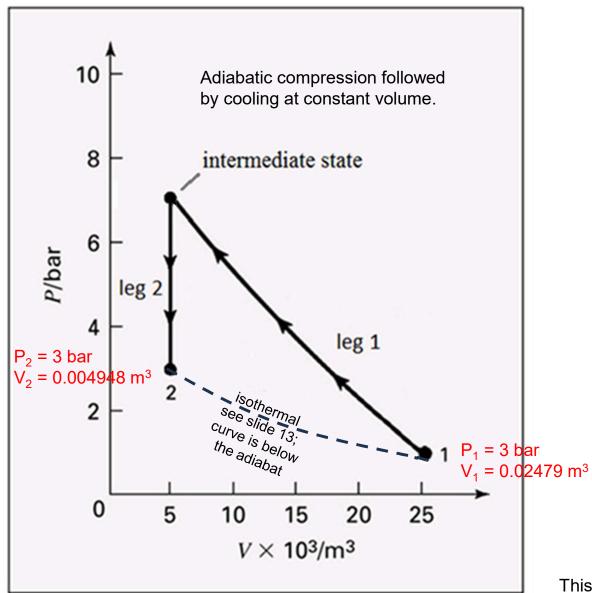


Diagram for Ex. 3. 3c

This is a sketch. Values are approximate.

Example 3.3, part (c), cont.

Air is compressed from an initial state of 1 bar and 25 °C to a final state of 3 bar and 25 °C by three different mechanically reversible processes in a closed system:

(c) Adiabatic compression followed by cooling at constant volume.

Adiabatic compression step (leg 1):

$$\gamma - 1 = \frac{C_P}{C_V} - 1 = \frac{7}{2} - 1 = 0.4$$

Use equation 3.30a:

$$T_{\text{intermediate}} = T_1 \left(\frac{V_1}{V_2} \right)^{\gamma - 1} = (298.15) \cdot \left(\frac{0.02479}{0.004958} \right)^{0.4} = 462.69 \text{ K}$$

Then use equation 3.32 (Recall first Law: Q + W = Δ U, Q = 0, and Δ U=C_v Δ T):

$$W_{\text{leg1}} = C_{\text{V}} \Delta T = (20.785)(462.69 - 298.15) = 3,419 \, \text{J} \qquad \text{and} \quad Q_{\text{leq1}} = 0$$

Constant volume step (leg 2):

$$Q_{leg2} = \Delta U = C_V \Delta T = (20.785)(298.15 - 462.69) = -3,419 J$$
 and $W_{leg 2} = 0$

Overall:
$$W_{\text{overall}} = 3,419 + 0 = 3,419 J$$
 and $Q_{\text{overall}} = 0 - 3,419 = -3,419 J$

Questions?