

# 1D Diagenetic modelling - Porous Media

Arthur Capet, Marilaure Grégoire, Karline Soetaert

October 3, 2019

1. Reaction-Transport Models in 1D

2. Porous Media

3. Reaction-Transport in Porous Media

4. Diagenetic Reaction Processes

5. Case Study : Oxygen diffusion

# Reaction-Transport Models

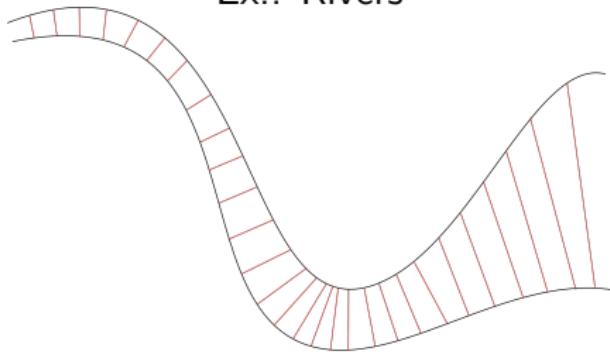
## Transport Reaction Equation

$$\frac{\partial C}{\partial t} = T + R$$

C	Concentration	mass/m <sup>3</sup>
t	Time	time
T	Transport	mass/m <sup>3</sup> /time
R	Reaction	mass/m <sup>3</sup> /time

# 1D spatial contexts

Ex.: Rivers



- ▶  $C : C(x, t)$

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- ▶  $C : C(x, t)$
- ▶  $x$ : main axis of spatial variability

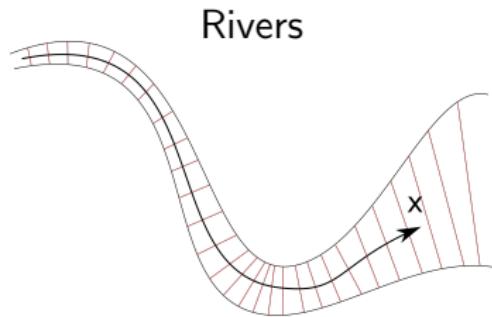
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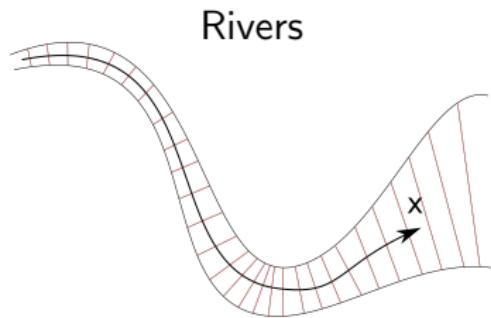


- ▶  $C : C(x, t)$
- ▶  $x$ : main axis of spatial variability
- ▶  $C$  is considered homogeneous along the other dimensions

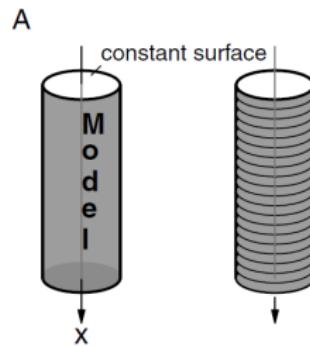
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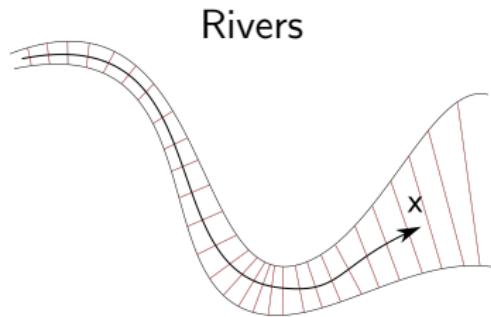
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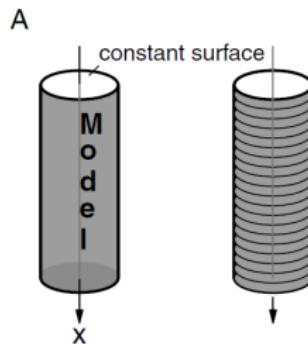
parallel isosurfaces



# 1D spatial contexts

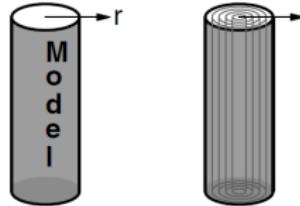


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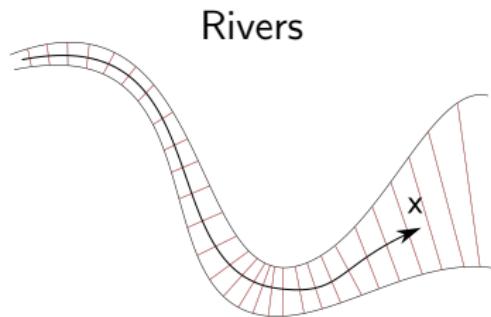


cylindrical isosurfaces

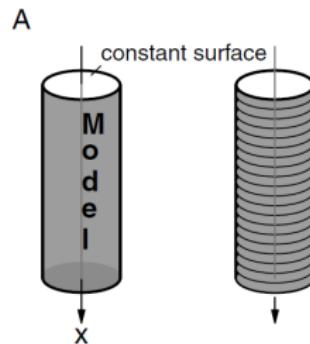
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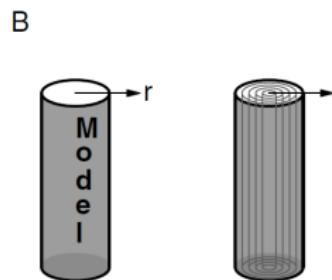
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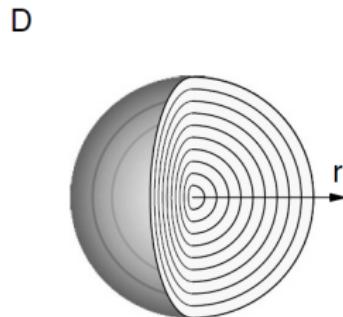
parallel isosurfaces



cylindrical isosurfaces



spherical isosurfaces

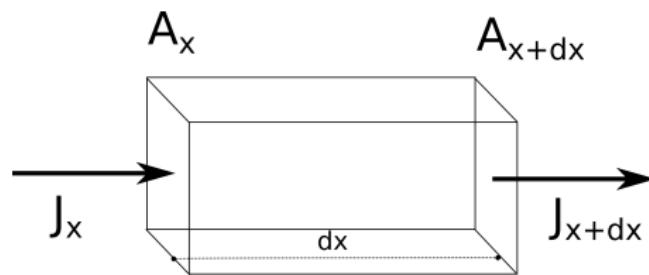


# Reaction-Transport Models in 1D

## Transport Reaction Equation in 1D

$$\frac{\partial C}{\partial t} = - \underbrace{\frac{1}{A_x} \frac{\partial (A_x \cdot J)}{\partial x}}_{\text{Transport}} + R$$

C	Concentration	mass/m <sup>3</sup>
t	Time	time
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A <sub>x</sub>	Surface	m <sup>2</sup>
J	Flux	mass/m <sup>2</sup> /time



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J	Flux	mass/m <sup>2</sup> /time

## General flux expression

$$J = \underbrace{-D \frac{\partial C}{\partial x}}_{\text{Diffusion}} + \underbrace{vC}_{\text{Advection}}$$

D	Diffusion Coefficient	m <sup>2</sup> /time
v	Advection rate	m/time

# Reaction-Transport Models in 1D

$$\frac{\partial C}{\partial t} = -\frac{1}{A_x} \frac{\partial(A_x \cdot J)}{\partial x} + R \quad (1)$$

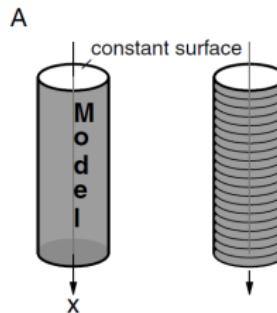
$$J = -D \frac{\partial C}{\partial x} + vC \quad (2)$$

Spatial context

Horizontal homogeneity

- ▶ Depth as the main axis → Constant surface  $A_x = A$

parallel isosurfaces



(1) + (2) → General 1D Diffusion-Advection-Reaction equation

$$\frac{\partial C}{\partial t} = \frac{\partial}{\partial x} \left[ D \frac{\partial C}{\partial x} - vC \right] + R$$

1. Reaction-Transport Models in 1D

2. Porous Media

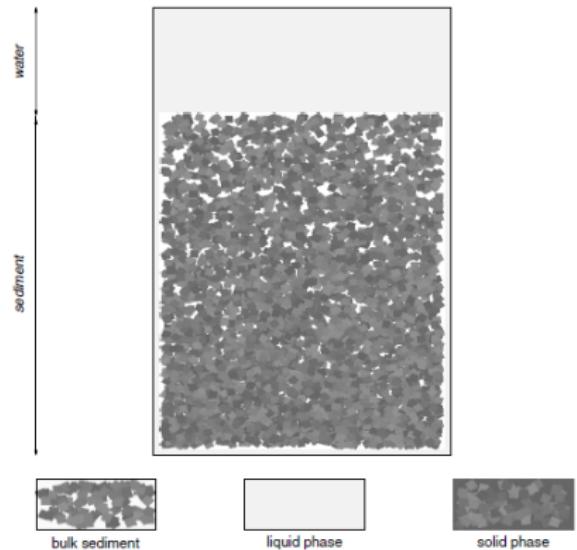
3. Reaction-Transport in Porous Media

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# Multiple phases

Bulk Sediments = Solid + Liquid



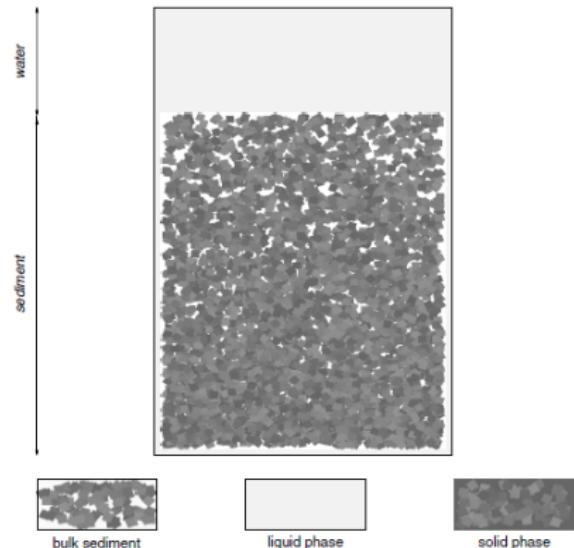
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Until now :

- ▶ Concentrations

Mass / Vol. of Bulk Sediments



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Different transport processes

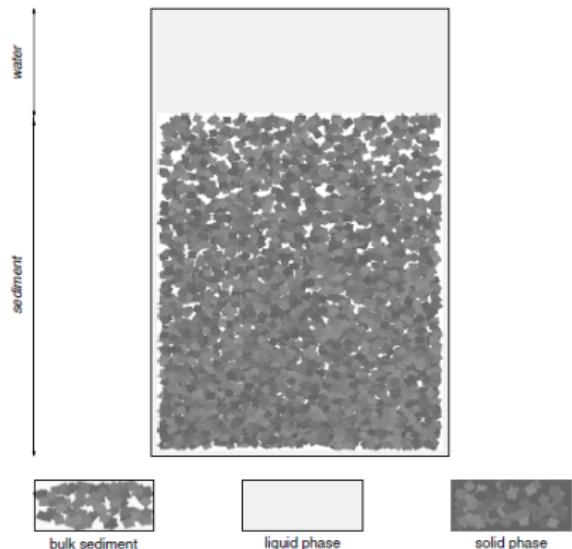
→ need to express different phases.

- ▶ for Solutes

Mass / Vol. of liquid

- ▶ for Solids

Mass / Vol. of solid



# Multiple phases

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Until now :

- ▶ Concentrations

Mass / Vol. of Bulk Sediments

Different transport processes

→ need to express different phases.

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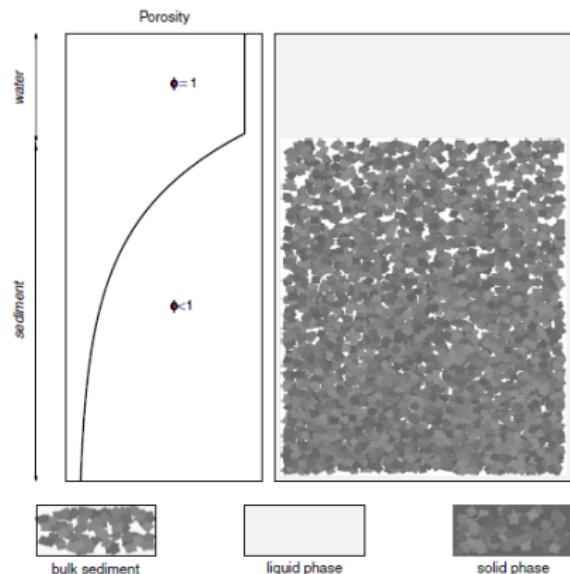
- ▶ for Solids

Mass / Vol. of solid

Useful for conversion: Porosity ( $\phi$ )

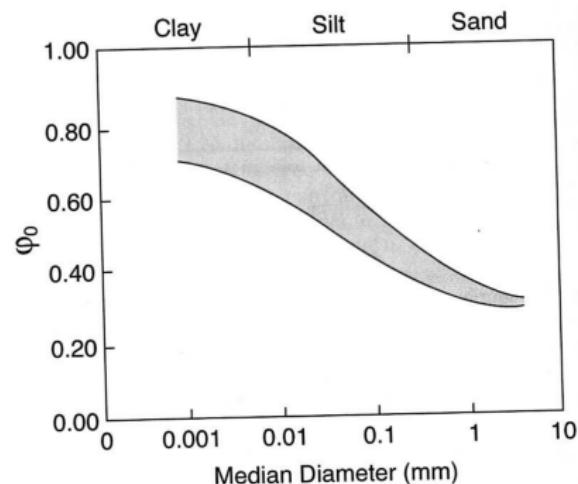
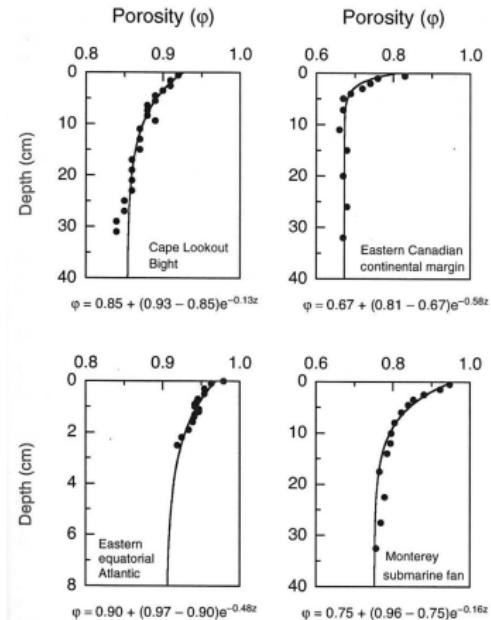
- ▶  $\phi = \text{Vol. Liquid} / \text{Vol. Bulk}$

- ▶  $1 - \phi = \text{Vol. Solid} / \text{Vol. Bulk}$



# Multiple phases : porosity

Porosity :  $\phi = \frac{\text{volume of pore waters}}{\text{volume sediments}}$



**Figure 2:** Upper porosity and grain size

**Figure 1:** Examples of porosity profiles

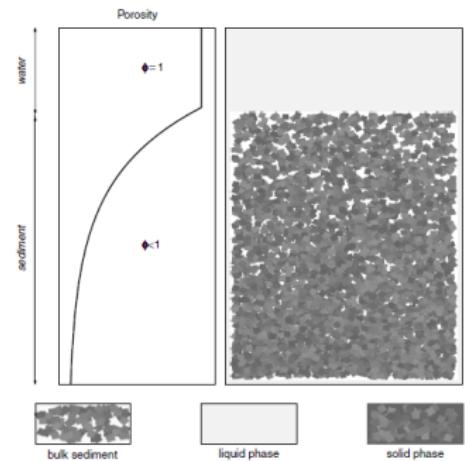
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Example : Solid Dissolution



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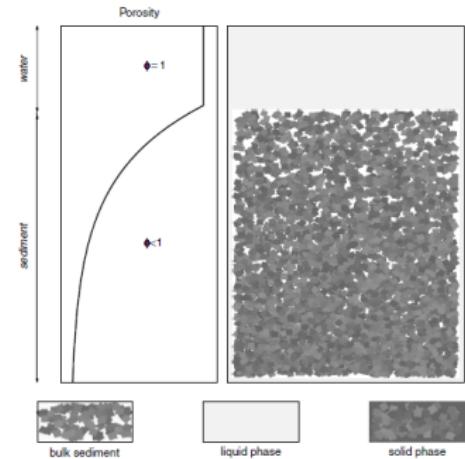


$$\frac{\partial S}{\partial t} = -\gamma S \quad (\text{No Transport})$$

---

$S$	Conc. in solid	$\text{mmol m}^{-3}_{solid}$
$\gamma$	diss. rate	$\text{d}^{-1}$
$C$	Conc. in liquid	$\text{mmol m}^{-3}_{liquid}$

---



# Multiple phases : porosity

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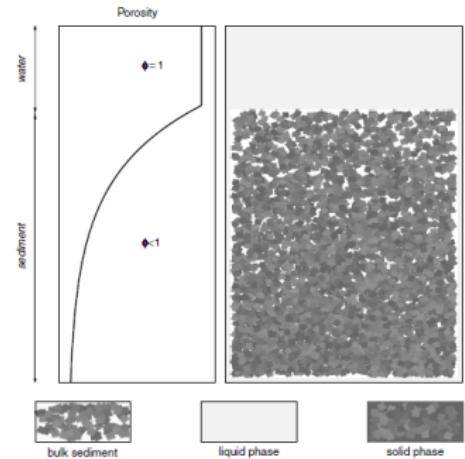


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$C$	Conc. in liquid	$\text{mmol m}_{\text{liquid}}^{-3}$

---



The effect on liquid phase will be :

$$\frac{\partial C}{\partial t} = \gamma S \cdot \frac{1-\phi}{\phi}$$

# Multiple phases : Different transport processes

## Liquids

- ▶ Diffusion is due to molecular diffusion
- ▶ Advection is due to liquid flow with respect to the SWI.

## Liquids

$$J_{Liq.} = -D_{sed} \frac{\partial C}{\partial x} + v_L C$$

## Tortuosity

$$D_{sed} = \frac{D_{sea \text{ water}}}{1 - \ln(\phi^2)}$$

Boudreau, 1996

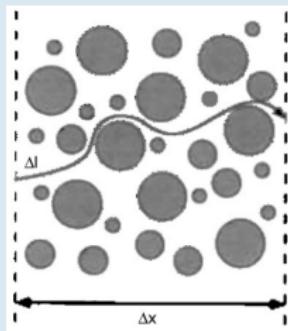


Fig. 1. Convolute diffusion path in a sediment from Boudreau (1996).

# Multiple phases : Different transport processes

## Liquids

- ▶ Diffusion is due to molecular diffusion
- ▶ Advection is due to liquid flow with respect to the SWI.
  - ▶ Sedimentation
  - ▶ Compaction
  - ▶ Biological activity
  - ▶ Pressure gradients in permeable sediments.

## Liquids

$$J_{Liq.} = -D_{sed} \frac{\partial C}{\partial x} + v_L C$$

# Multiple phases : Different transport processes

## Liquids

- ▶ Diffusion is due to molecular diffusion
- ▶ Advection is due to liquid flow with respect to the SWI.

## Solid

- ▶ Diffusion is due to bioturbation
- ▶ Advection is due to solid advection with respect to the SWI  
(sedimentation or compression)

### Liquids

$$J_{Liq.} = -D_{sed} \frac{\partial C}{\partial x} + v_L C$$

### Solids

$$J_{Sol.} = -D_b \frac{\partial S}{\partial x} + v_S S$$

# Bioirrigation

Flushing of burrows with overlying waters

Allows diffusive exchanges between bottom waters and porewaters at depth, through burrow walls

→ 3D(2D) context.

However, Boudreau (1984) showed the equivalence of

- ▶ 3D set-up with cylindrical burrows
- ▶ 1D vertical set-up with non-local exchange of pore waters

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# Reactive Transport in Porous Media

## Solutes

$$\frac{\partial \phi_x C}{\partial t} = -\frac{\partial}{\partial x} [\phi_x J_L] + \phi_x R_L$$

## Solids

$$\frac{\partial (1 - \phi_x) S}{\partial t} = -\frac{\partial}{\partial x} [(1 - \phi_x) J_S] + (1 - \phi_x) R_S$$

# Reactive Transport in Porous Media

## Solutes

$$\frac{\partial \phi_x C}{\partial t} = \frac{\partial}{\partial x} \left[ \phi_x (D_{\text{sed}} \frac{\partial C}{\partial x} - v_L C) \right] + \phi_x R_L$$

## Solids

$$\frac{\partial (1 - \phi_x) S}{\partial t} = \frac{\partial}{\partial x} \left[ (1 - \phi_x) (D_b \frac{\partial S}{\partial x} - v_S S) \right] + (1 - \phi_x) R_S$$

# Reactive Transport in Porous Media

## Solutes

$$\frac{\partial C}{\partial t} = \frac{1}{\phi_x} \frac{\partial}{\partial x} \left[ \phi_x (D_{\text{sed}} \frac{\partial C}{\partial x} - v_L C) \right] + R_L$$

## Solids

$$\frac{\partial S}{\partial t} = \frac{1}{1 - \phi_x} \frac{\partial}{\partial x} \left[ (1 - \phi_x) (D_b \frac{\partial S}{\partial x} - v_S S) \right] + R_S$$

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## Boundary Conditions (usual)

Solutes

Solids

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## Boundary Conditions (usual)

### Solutes

@ Upper boundary ( $x = 0$ )  
Imposed conc. ( $C_{\text{bot. waters}}$ ).

### Solids

@ Upper boundary ( $x = 0$ )  
Imposed flux (sedimentation).

# Reactive Transport in Porous Media

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## Boundary Conditions (usual)

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- ① Upper boundary ( $x = 0$ )  
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- ② Lower boundary ( $x = \infty$ )  
Zero Gradient

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# Organic Matter Lability I

Large chain generally replaced by one step reaction  $Part. OrgC \xrightarrow{R_G} DIC$

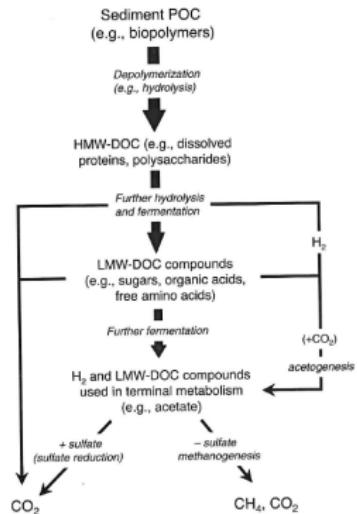
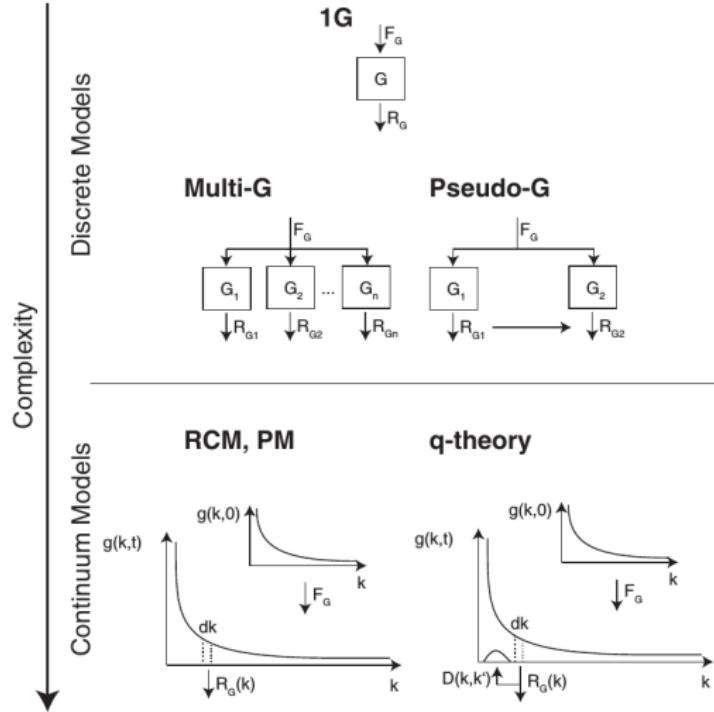


Figure 3: Example of Org. C degradation

$G$	Organic Matter
$R_G$	Degradation rate,
$k$	max degradation rate,
$i$	metabolic pathways,
$F_{TEM,i}$	Temperature effect
$F_{BIO,i}$	Microbial biomasses
$F_{TEA,i}$	Terminal electron acceptor
$F_{IN,i}$	Inhibition by other TEA
$F_{T,i}$	bioenergetic limitation (Gibbs energy)

According to complexity, several factors are empirically included in  $k$

# Organic Matter Lability II



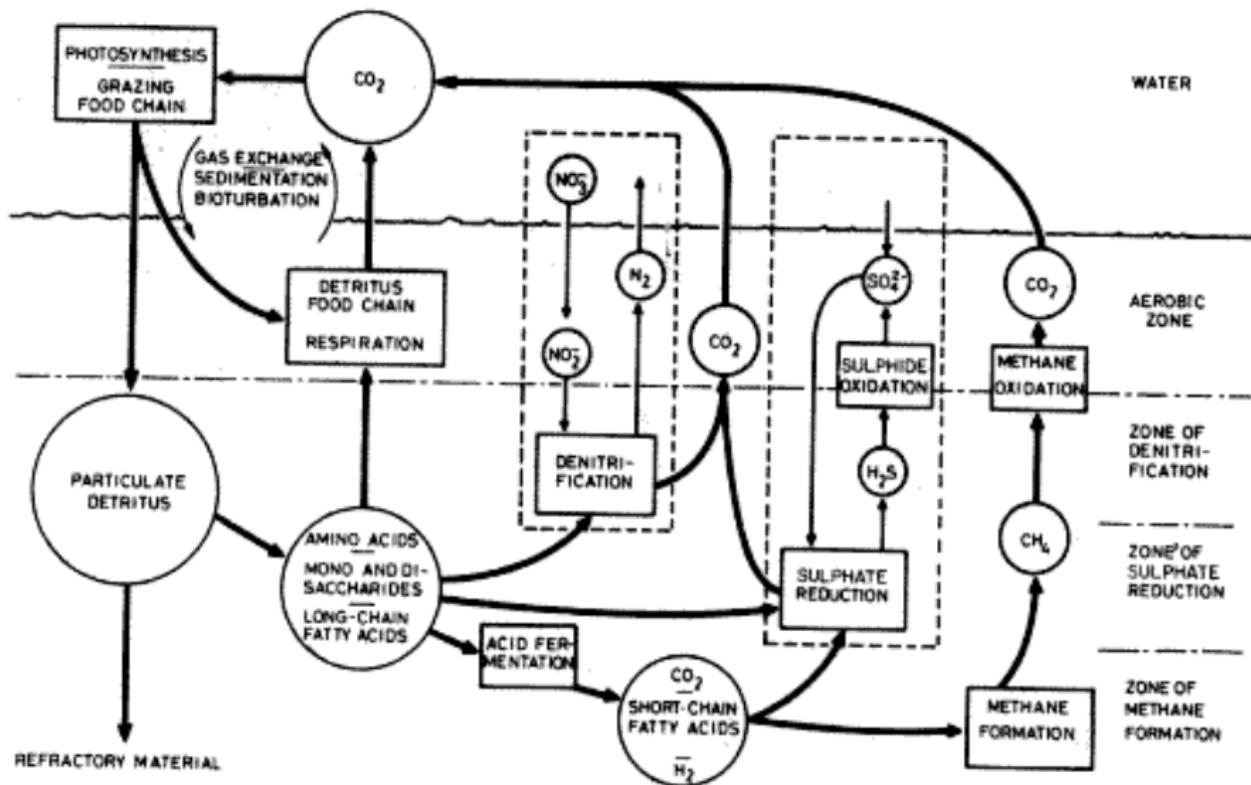
Single G neglects

- ▶ Various organic compounds in OM source :
- ▶ Refractory OM formed during bacterial remin.

Arndt, 2013 (review) :

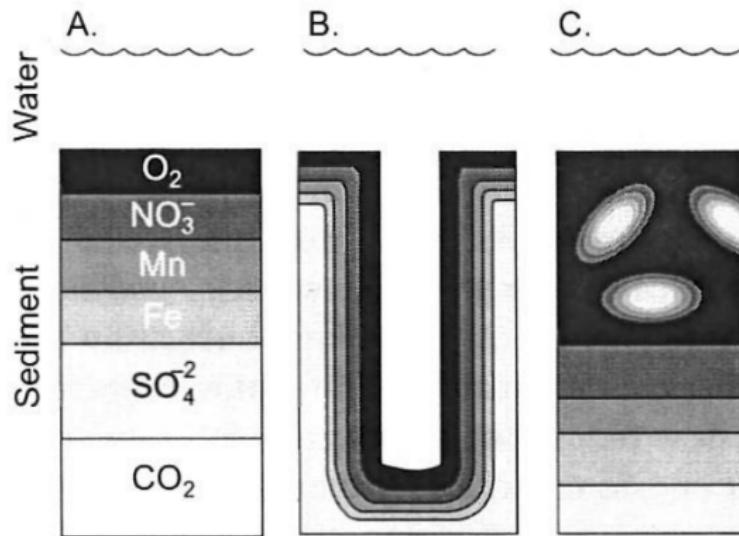
- ▶ Multi-G model  
 $R_G = \sum_i k_i G_i$
- ▶ Continuous lability spectrum models  
$$R_G = - \int_0^{\infty} kg(k) dk$$
- ▶ OM degradation explicitly driven by ecosystem dynamics (incl. bact.)

# Redox zonation I



# Redox zonation II

## Microscales



# N cycling

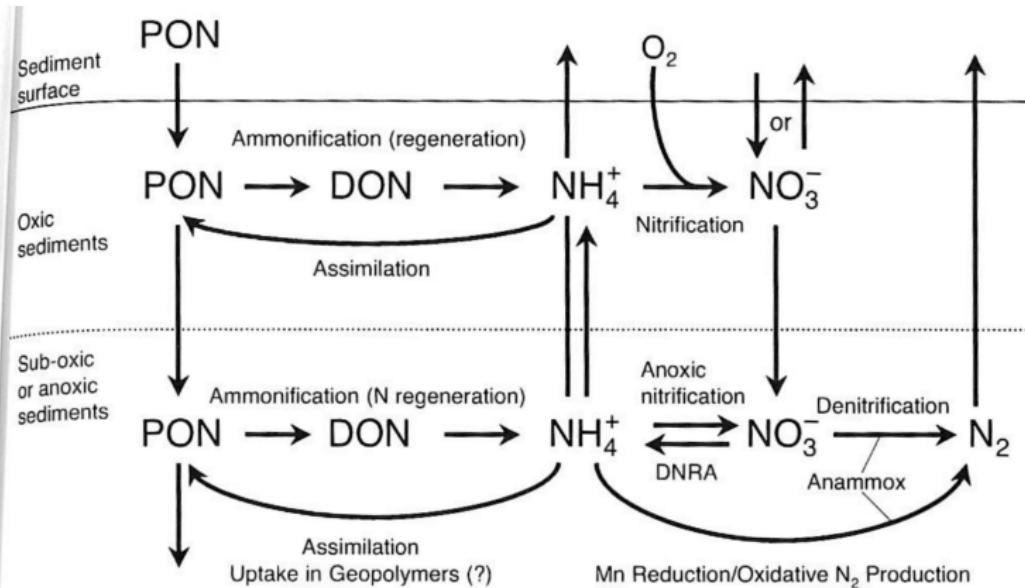
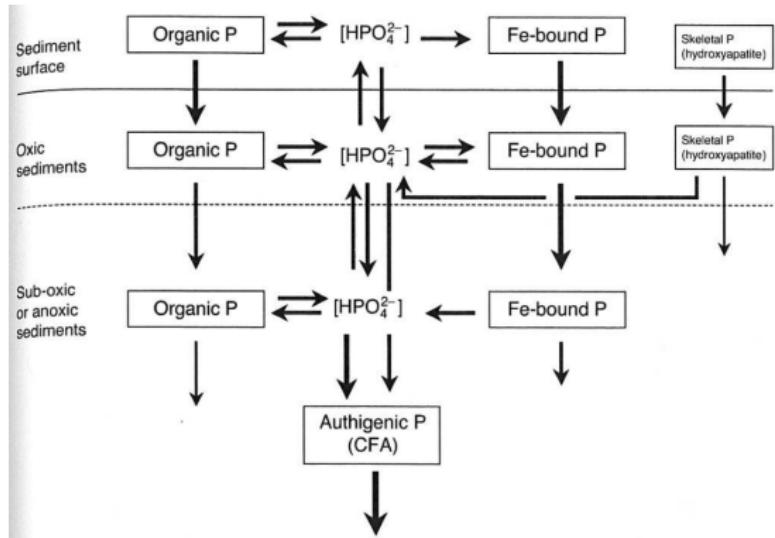


Figure 16.2 A conceptual model illustrating the processes associated with nitrogen cycling in marine sediments (based on information from several sources).

# Phosphorus cycling I



Slomp et al, 2007

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5. Case Study : Oxygen diffusion

## Case Study : Oxygen diffusion

- ▶ We consider dissolved Oxygen (only liquid phase).
- ▶ Non-permeable sediments → No liquid flow, no advection.
- ▶ Constant oxygen consumption rate above a certain depth, 0 below.

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$$\gamma(z) = \gamma_0 \cdot \frac{O_2(z)}{O_2(z) + k_s} \quad (3)$$

- Boundary conditions:  
 $O_2|_{z=0} = O_2 \text{ b.w.}; \frac{\partial O_2}{\partial z}|_{z=\infty} = 0$
- Steady-state solution :  $\frac{\partial O_2}{\partial t} = 0$

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- |                           |  |                    |                         |
|---------------------------|--|--------------------|-------------------------|
| ► Boundary conditions:    | $O_2 _{z=0} = O_2 \text{ b.w.}; \frac{\partial O_2}{\partial z} _{z=\infty} = 0$ | $\phi$             | Porosity                |
| ► Steady-state solution : | $\frac{\partial O_2}{\partial t} = 0$  | $D$                | Diffusion coefficient   |
|                           |  | $\gamma_0$         | Respiration rate        |
|                           |  | $k_s$              | "Oxygen Limitation"     |
|                           |  | $O_2 \text{ b.w.}$ | [ $O_2$ ] bottom waters |

## Case Study : Oxygen diffusion

- ▶ Describe model implementation in R (using the Reactran framework)
- ▶ Compare with oxygen profile from the mud sediment core
- ▶ Infer diffusive flux at the Sediment-Water interface
- ▶ Extend the model :
  - ▶ Include Solid phase for organic carbon
  - ▶ Include Bioirrigation
  - ▶ Include Nitrogen Cycle

# Why do we consider cohesive sediments ?

Sands

- Permeability
- Needs to resolve flows through the sediment matrix
- Needs higher dimensional context.