# How To Use Free-Surface Flows in OpenFOAM v2012

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Training level: Intermediate

Session type: Lecture with examples

Software stack: OpenFOAM v2012

https://unicfd.ru

# Plan of training course

- 1. Introduction
- 2. Key points of training course
- 3. interFoam solver: how it works
  - Governing equations
  - Volume of Fluid method
  - Solution process
  - Boundary conditions
- 4. Basic case: Spillway tutorial
  - Problem statement
  - Physical properties setup
  - Mesh generation

- Boundary conditions setup
- Numerical schemes and time advancement settings.
   Running.
- Results
- 5. Additional case: RT tutorial
  - Problem statement
  - Settings in OpenFOAM. Running.
  - Results. Comparison with linear theory.
- 6. Conclusions and discussion

#### Introduction

#### **Applicability**

- printing;
- engines;
- ecological cases;
- dams, spillways;
- etc.



Ladybower Reservoir, England

#### Complexities

- large deformations of the interface;
- creation of different subregions (droplets, bubbles...);
- solution should:
  - be stable:
  - have small diffusivity in the interface region;
  - satisfy to conservation laws;
  - be correct in different scales;
  - require not so much resources for computations.

# Key points of training course

- Look inside the standard solver for free-surface flows
- Study how to set boundary conditions in different versions of OpenFOAM
- Look to all stages of modelling of free-surface flows in OpenFOAM v2012: from mesh generation to post-processing

Boundary conditions are critically important in the successful modelling. There are strong differences between OpenFOAM 2.2.x and 2.3.0+.

The main tool: an interFoam solver in OF v2012. We will study it with Spillway tutorial: the turbulent flow of fluid

# Part I Theoretical part

interFoam: how it works

# Structure of theoretical part

- 1. Governing equations
- 2. Volume of Fluid method
- 3. Block scheme of interFoam
- 4. Pressure-velocity coupling
- 5. Boundary conditions (most common types):
  - walls and inlets:
  - outlets and open boundaries;
  - planes of symmetry.

# Governing equations for incompressible flow

Continuity equation:

$$\nabla \cdot \mathbf{U} = 0;$$

• Navier — Stokes equations:

$$\frac{\partial(\rho \mathbf{U})}{\partial t} + \nabla \cdot (\rho \mathbf{U} \otimes \mathbf{U}) = -\nabla p + \nabla \cdot \hat{\tau} + \rho \mathbf{g},$$

where  $\hat{\tau} = \mu(\nabla \mathbf{U}^T + \nabla \mathbf{U})$  is the viscous stress tensor;

• boundary conditions on the interface:

$$[-p\mathbf{I} + \hat{\tau}] \cdot \mathbf{n} = \sigma \kappa \mathbf{n}, \quad [\mathbf{U}] = 0;$$

• initial and boundary conditions on the flow region boundaries (different types — walls, inlets, outlets, open boundaries and other).

#### Volume of Fluid method

Add a volume fraction function:

$$\alpha_1 = \begin{cases} 1 \text{ if cell full of liquid;} \\ 0 \text{ if cell full of gas;} \\ (0;1) \text{ if cell is placed on the interface;} \end{cases}$$

0	0	0	0	0	0
0	0	0	0	0	0
0	0	0	0	0	0
0.8	0.9	0.5	0	0	0
1	1	1	0.2	0	0
1	1	1	<b>0</b> .2	0	0

For two phases

$$\alpha_1 + \alpha_2 = 1.$$

Solve a transport equation for this function:

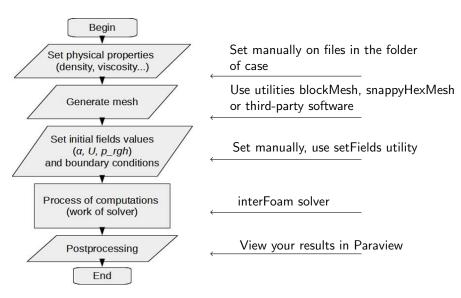
$$\frac{\partial \alpha_1}{\partial t} + \nabla \cdot (\mathbf{U}\alpha_1) + \nabla \cdot (\mathbf{U}_R \alpha_1 \alpha_2) = 0,$$

where  $\mathbf{U} = \alpha_1 \mathbf{U}_1 + \alpha_2 \mathbf{U}_2$  — velocity of mixture;

 $\mathbf{U}_R = \mathbf{U}_1 - \mathbf{U}_2$  — velocity field suitable to compress the interface.

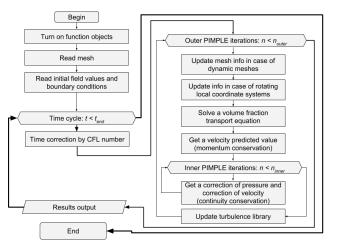
Approximation: Finite Volume Method

# Solution process



#### interFoam solver

#### Block scheme



see alphaEqn.H¹ ≤ see UEqn.H

see pEqn.H

Location: OpenFoam-v2012/applications/solvers/multiphase/VoF

<sup>&</sup>lt;sup>1</sup>see slide 8

#### interFoam solver

Modified Navier — Stokes equations

Surface tension forces are approximated as an additional term  $\mathbf{F}_{\sigma}$  in Navier — Stokes equation<sup>2</sup>:

$$\frac{\partial(\rho\mathbf{U})}{\partial t} + \nabla \cdot (\rho\mathbf{U} \otimes \mathbf{U}) = -\nabla p + \nabla \cdot \hat{\tau} + \rho \mathbf{g} + \mathbf{F}_{\sigma}.$$

Use modified pressure:

$$p^* = p - \rho(\mathbf{g} \cdot \mathbf{r}).$$

Its gradient:

$$\nabla p^* = \nabla p - (\nabla \rho)(\mathbf{g} \cdot \mathbf{r}) - \rho \mathbf{g}.$$

Approximation of surface tension forces — by volume fraction gradient:

$$\mathbf{F}_{\sigma} \approx \sigma \kappa \nabla \alpha_1$$
.

<sup>&</sup>lt;sup>2</sup>see slide 7

## interFoam solver I

#### Pressure-velocity coupling

Use velocity as sum of prediction and correction parts:

$$\mathbf{U} = \mathbf{U}^* + \mathbf{U}'. \tag{1}$$

Semi-discrete form of momentum equation:

$$A\mathbf{U} = H - \nabla p^* - (\nabla \rho)(\mathbf{g} \cdot \mathbf{r}) + \mathbf{F}_{\sigma}.$$

Here A is the diagonal part of initial matrix system,

H is the non-diagonal part of matrix + r.h.s. without diagonal part of initial matrix system, pressure gradient and terms for gravity and surface tension.

We can write comparing with the velocity splitting (1):

$$\mathbf{U}^* = A^{-1}H;$$

$$\mathbf{U}' = -A^{-1}\nabla p^* - A^{-1}(\nabla \rho)(\mathbf{g} \cdot \mathbf{r}) + A^{-1}\mathbf{F}_{\sigma}.$$

## interFoam solver II

#### Pressure-velocity coupling

Continuity equation in the discrete form:

$$\int_{V} \nabla \cdot \mathbf{U} \, dV = \int_{S} \mathbf{U} \cdot \mathbf{n} \, dS \approx \sum_{f} \underbrace{\mathbf{U}_{f} \cdot \mathbf{S}_{f}}_{\varphi_{f}} = 0, \tag{2}$$

consequently,

$$\sum_{f} \varphi_f = 0. \tag{3}$$

Let's calculate fluxes through one face f:

$$\underbrace{\mathbf{U}_{f} \cdot \mathbf{S}_{f}}_{\varphi} = \underbrace{\mathbf{U}_{f}^{*} \cdot \mathbf{S}_{f}}_{\varphi_{H/A}} - \underbrace{(A^{-1})_{f}}_{D_{p}} (\nabla p^{*})_{f} \cdot \mathbf{S}_{f} - \underbrace{(A^{-1}(\nabla \rho)(\mathbf{g} \cdot \mathbf{r}))_{f} \cdot \mathbf{S}_{f} + (A^{-1}\mathbf{F}_{\sigma})_{f}}_{\varphi_{g}}. \quad (4)$$

## interFoam solver III

#### Pressure-velocity coupling

Create a pressure equation which is derived from continuity equation (3):

$$\sum_{f} (\varphi_{H/A} + \varphi_g) = \sum_{f} D_p(\nabla p^*)_f \cdot \mathbf{S}_f.$$

Pressure gradient:

$$(\nabla p^*)_f = \frac{\varphi_{H/A} + \varphi_g - \varphi}{D_p \cdot \mathbf{S}_f}.$$
 (5)

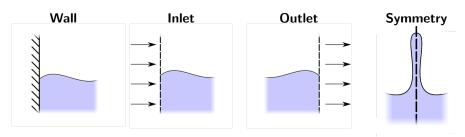
In the source code:

phiHbyA = phiHbyA + phig;

 $snGrad(p_rgh) = (phiHbyA - phi) / (rAUf * Sf).$ 

#### interFoam solver

#### Types of boundary conditions



#### Note

For incompressible fluids it is important to calculate correctly the pressure gradient. Absolute value of pressure is calculated up to a constant. So, it is enough to know the pressure reference value only in one point.

Location: OpenFoam-4.1/src/finiteVolume/fields/fvPatchFields

## interFoam solver I

#### Walls & inlets

Boundary condition for volume fraction:

$$\alpha=0$$
 or  $\alpha=1$  (fixedValue) — for inlets; 
$$\nabla \alpha=0 \ ({\tt zeroGradient}) \ -- \ {\tt for walls}.$$

Boundary condition for velocity:

$$\mathbf{U} = \{U_x; U_y; U_z\}$$
 (fixedValue).

#### Note

Capillary effects are neglected; to account for these effects — special boundary conditions for volume fraction must be imposed.

Boundary conditions for **pressure** are critically important here. Let's consider the correct boundary condition and changes in OpenFOAM v.2.3.0+.

## interFoam solver II

#### Walls & inlets

On boundaries for walls and inlets:

$$\mathbf{U} = \{U_x; U_y; U_z\}, \quad \mathbf{U}^* = \{U_x; U_y; U_z\} \Rightarrow \mathbf{U}' = \{0; 0; 0\}.$$

According to BC for volume fraction:

$$\mathbf{F}_{\sigma} \approx \sigma \kappa \nabla \alpha_1 = 0$$
 on the boundary.

So, according to expression for volumetric flux (4):

$$-D_p(\nabla p^*)_f \cdot \mathbf{S}_f - (A^{-1}(\nabla \rho)(\mathbf{g} \cdot \mathbf{r}))_f \cdot \mathbf{S}_f) = 0,$$

and, therefore, we can derive boundary condition for pressure:

$$\nabla p^*_f = -((\nabla \rho)(\mathbf{g} \cdot \mathbf{r}))_f.$$

## interFoam solver III

Walls & inlets

#### Implementation in OpenFOAM

In OpenFOAM v.2.2.x — buoyantPressure: this expression is in the source code of boundary condition.

In OpenFOAM v.2.3.0+ — fixedFluxPressure: boundary condition is satisfied automatically by pressure gradient (5), calculating in the solver's source code.

# interFoam solver I

#### Outlets

Boundary condition for volume fraction:

$$\nabla \alpha = 0$$
 (zeroGradient).

Boundary condition for velocity:

$$\nabla \mathbf{U} = 0$$
 (zeroGradient).

Boundary condition for pressure:

• reference level of pressure — if there are no pressure boundary conditions in any another boundary (typically means "atmosphere"):

$$p_p^* = p_0 - \frac{U^2}{2}$$
 (totalPressure),

where  $p_0$  — total pressure, U — velocity magnitude.

## interFoam solver II

#### Outlets

In the source code we use:

$$p = p0 - 0.5*(1 - pos(phi))*magSqr(U).$$

Here pos() is the boolean function which equals to 1 when the flux phi>0.

• zeroGradient — if you have some another boundary with derived reference level of pressure.

In case of **symmetry** just use slip boundary condition for all variables.

#### Note

Calculations of patch boundary field on the symmetry planes are performed using the Householder projection on the patch.

# Part II Practical part

Basic case: Spillway tutorial

# Stages of solution

- 1. Geometry: make STL-surface to draw the dam (in SALOME).
- 2. Liquid/gas properties: write density, kinematic viscosity . . .
- 3. Mesh generation:
  - blockMesh: create a basic mesh box;
  - snappyHexMesh: refine mesh near the dam surface:
  - extrudeMesh: make a 2D-mesh for fast calculations.
- 4. Boundary conditions: describe it in files in 0.org folder.

- 5. Set fields: set initial liquid phase volume fraction.
- 6. Numerical settings:
  - describe interpolation of terms;
  - describe solvers for SLAE;
  - setup turbulence models.
- 7. Time settings: set the end time, CFL-number . . .
- 8. Running: interFoam command.
- 9. Post-processing: open file spillway.foam in Paraview.
- 10. Enjoy!

#### Problem statement

## Input data

Water:

 $\textbf{density} \colon 1000 \text{ kg/m}^3;$ 

dynamic viscosity:

 $10^{-3} \ \mathrm{Pa} \cdot \mathrm{s}.$ 

Air:

 $\textbf{density}{:}\ 1\ \text{kg/m}^3;$ 

dynamic viscosity:

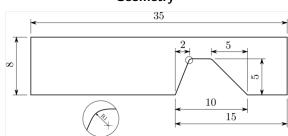
 $1.48 \cdot 10^{-5} \text{ Pa} \cdot \text{s}.$ 

Surface tension

coefficient: 0.07 N/m.

Inlet velocity: 0.6 m/s.

#### Geometry



#### Scheme



# Physical properties I

See: folder \constant

#### File transportProperties:

Set phases:

```
phases (water air);
```

• Set density and kinematic viscosity for each phase:

# Physical properties II

Set surface tension:

```
sigma sigma [ 1 0 -2 0 0 0 0 ] 0.07;
```

File g: set the value and direction of gravity

```
dimensions [0 1 -2 0 0 0 0];
value (0 0 -9.81);
```

File turbulenceProperties: set the turbulence model

```
simulationType RAS;

RAS
{
    RASModel     kOmegaSST;
    turbulence     on;
    printCoeffs     on;
}
```

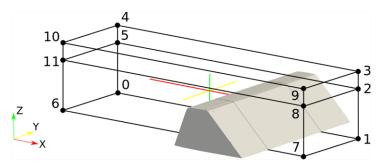
Turbulent intensity:  $\approx 2\%$ .

#### blockMesh I

Create basic coarse mesh in the flow region and mark the boundaries.

See: constant/polyMesh/blockMeshDict

Command: blockMesh



Exercise: inspect results in Paraview.

You should see the rectangular region with the coarse mesh

## blockMesh II

Set scale:

```
convertToMeters 1;
```

Set vertices:

```
vertices (
    (-20 - 0.45 \ 0) // 0
    ( 15 -0.45 0 ) // 1
    ( 15 -0.45 6 ) // 2
    ( 15 -0.45 8 ) // 3
    (-20 - 0.45 8) // 4
    (-20 - 0.45 6) // 5
    (-20 - 0.55 \ 0) // 6
    ( 15 -0.55 0 ) // 7
    ( 15 -0.55 6 ) // 8
    ( 15 -0.55 8 ) // 9
    (-20 - 0.55 8) // 10
    (-20 - 0.55 6) // 11
);
```

## blockMesh III

Create two boxes:

```
blocks
(
    hex (0 1 2 5 6 7 8 11) (70 12 1)
        simpleGrading (1 1 1)
    hex (5 2 3 4 11 8 9 10) (70 4 1)
        simpleGrading (1 1 1)
);
```

Describe boundaries:

```
boundary
(
    outlet
    {
        type patch;
        faces ( (1 2 8 7) (2 3 9 8) );
}
```

## blockMesh IV

```
inletAir
   type patch;
   faces ( (4 5 11 10) );
inletWater
   type patch;
   faces ( (5 0 6 11) );
atmosphere
   type patch;
   faces ( (3 4 10 9) );
```

### blockMesh V

```
bottomWall
   type wall;
    faces ( (0 1 7 6) );
front
   type empty;
    faces ( (1 0 5 2) (2 5 4 3) );
back
   type empty;
    faces ( (6 7 8 11) (11 8 9 10) );
```

# snappyHexMesh I

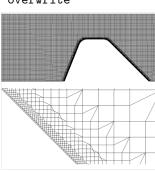
**See**: constant/system/snappyHexMeshDict Command: snappyHexMesh -overwrite

**Stage 1.** Refine mesh near the surface of dam. Three stages of meshing:

- refinement (see CastellatedMeshControl section);
- smoothing (see SnapControls section);
- set of layers (see addLayersControls section).

Use STL-surface (from constant/triSurface):

```
dam.stl {
    type triSurfaceMesh;
    name dam:
```



# snappyHexMesh II

**Stage 2.** Add two refinement regions where the surface of water will flow. Use two boxes and plane to do it:

```
surface
{
   type searchableBox;
   min ( -15 -1 4.5);
   max ( 4 0 7 );
aroundDam
         searchablePlane;
   type
   planeType pointAndNormal;
   pointAndNormalDict {
       basePoint (7.5 -0.5 2.5):
      normalVector (1 0 1);
   };
```

# snappyHexMesh III

```
outlet
{
    type searchableBox;
    min ( 10 -1 0 );
    max ( 15 0 1 );
}
```

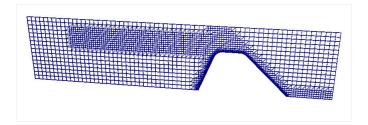
**Exercise**: try to run snappyHexMesh with different studies of remeshing. Watch differences.



#### extrudeMesh

See: constant/system/extrudeMeshDict
Command: extrudeMesh

blockMesh and snappyHexMesh construct 3D-mesh. extrudeMesh creates a 2D-mesh based one the planar surface (in our case — from patch).



**Exercise**: run checkMesh utility before running extrudeMesh and after that. Compare numbers of cells.

# Boundary conditions

See: folder 0.org/. Change needed files and copy it to folder 0/.

Name	α	k	$\omega$	$p^*$	U
inletAir	fixedValue 0	fixedValue 2.16e-4	fixedValue 0.1470	fixedFlux Pressure	fixedValue (0 0 0)
inletWater	fixedValue 1	fixedValue 2.16e-4	fixedValue 0.1470	fixedFlux Pressure	fixedValue (0.6 0 0)
outlet	zero Gradient	zero Gradient	zero Gradient	fixedFlux Pressure	zero Gradient
walls	kqRWall Function	omegaWall Function	zero Gradient	fixedFlux Pressure	fixedValue (0 0 0)
atmosphere	inletOutlet	inletOutlet 2.16e-4	inletOutlet 0.1470	total Pressure	pressure Inlet Outlet Velocity
front,back, defaultFaces	empty	empty	empty	empty	empty

#### setFields

Set an initial distribution of fields (alpha.water) in regions.

Files in 0/ folder will be modified.

```
defaultFieldValues (
    volScalarFieldValue alpha.water 0
);

regions (
    boxToCell {
        box (-20 -1 0) (3 1 5);
        fieldValues (
            volScalarFieldValue alpha.water 1
        );
    }
):
```



# Numerical schemes and time settings. Running

See system/controlDict to create time settings:

- time interval,
- CFL number.
- write interval,
- time precision.

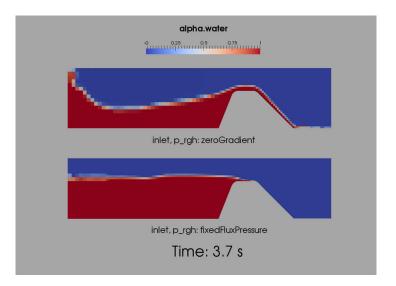
Settings for numerical schemes (use default settings): see system/fvSchemes and system/fvSolution.

Start application by interFoam command.

## Scripts

Sequence of all commands is placed in the script file ./Allrun. Clean results: ./Allclean.

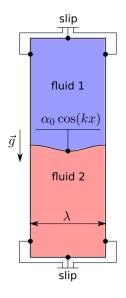
## Results



## Part II **Practical part**

Additional case: Rayleigh — Taylor instability

#### Problem statement



## Input data

Fluid 1:

**density**:  $1.255 \text{ kg/m}^3$ ;

dynamic viscosity:  $3.13 \cdot 10^{-3}$  Pa·s.

Fluid 2:

**density**:  $0.032 \text{ kg/m}^3$ ;

dynamic viscosity:  $3.13 \cdot 10^{-3}$  Pa·s.

Surface tension coefficient: 0.01 N/m.

Interface form:  $\alpha_0 = 0.05$  m,  $k = 2\pi$ .

Wave length:  $\lambda = 1$  m.

# Linear theory

## Instability conditions

- 1. Initial perturbation:  $\alpha > 0$ ,  $\alpha \ll \lambda$ .
- 2. Surface tension coefficient:  $\sigma < \sigma_c, \sigma_c = \frac{\Delta \rho g}{k^2}$ .
- 3. Dynamic viscosities:  $\mu_1 = \mu_2 = \mu$ .

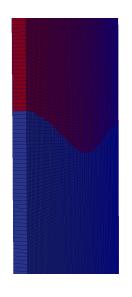
## Law for growth of amplitude instabitily

$$\alpha(t) = \alpha_0 \cosh(\Gamma t),$$

where  $\Gamma$  — growth rate (1/s), A — Atwood number (non-dimensional):

$$\Gamma = \sqrt{kg\left(A - \frac{k^2\sigma}{g(\rho_1 + \rho_2)}\right)}; \quad A = \frac{\rho_2 - \rho_1}{\rho_2 + \rho_1}.$$

# OpenFOAM case



#### General settings

**Mesh**: one block, uniform mesh, no refinement.

**Boundary conditions**: slip for all variables.

**Transport properties**: set density and kinematic viscosity for two fluids.

Turbulence properties: laminar flow.

Numerical settings: standard interFoam settings.

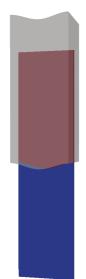
## How to set up the interface

Different ways to set up the initial perturbation:

- use STL surface in standard setFields utility;
- use funkySetFields utility from swak4Foam library.

# OpenFOAM case

setFields

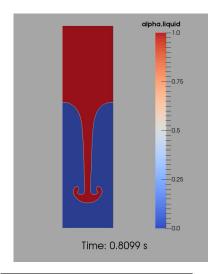


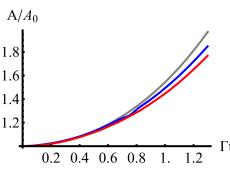
#### Source code for STL in setFields

```
regions (
  surfaceToCell {
                   "liquid.stl";
   file
   useSurfaceOrientation false;
   outsidePoints ((1e-4 0 -1.04));
   includeCut
                 true:
       includeInside true;
       includeOutside false;
       nearDistance -1;
       curvature
                      -100;
   fieldValues (
      volScalarFieldValue alpha.liquid 1
      volVectorFieldValue U
                                (0\ 0\ 0)
```

STL surface should be placed in the case folder.

## Results





Gray color — linear theory Blue color — Gerris<sup>3</sup> Red color — OpenFOAM

<sup>&</sup>lt;sup>3</sup>open-source code for free-surface flows, see http://gfs.sourceforge.net/wiki/index.php/Main\_Page

# Summary

- We looked how interFoam works (look in the source code).
- We learned how to set boundary conditions for free-surface flows.
- We studied how to solve cases for free-surface flows step-by-step on the basic example — Spillway tutorial.
- We get the first experience in linear theory of hydrodynamic instabilities and run the additional case — RT instability

Let's talk about training track. Some questions?