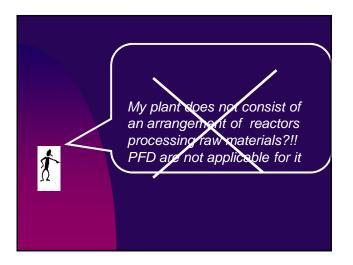
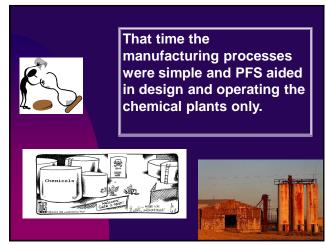


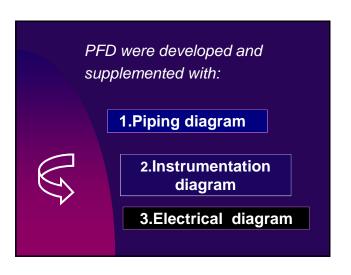
In the early days of the chemical industry Process Flow Sheets were defined as

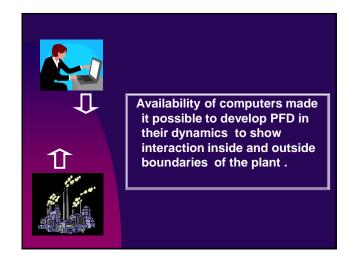
"The schematic representation of the unit operations and reactors involved in manufacturing process at chemical plant "

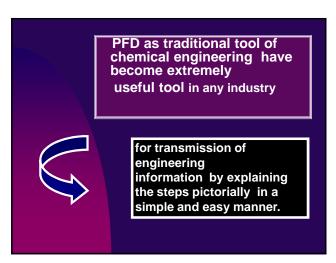


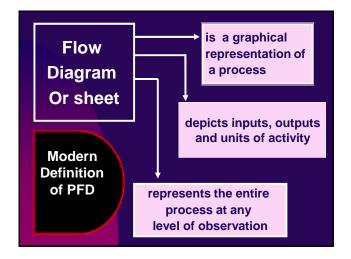


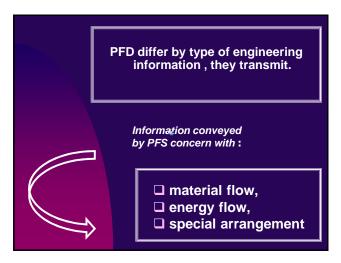


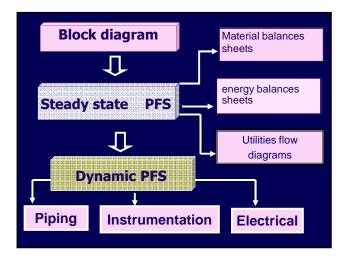


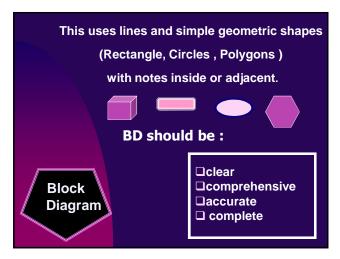


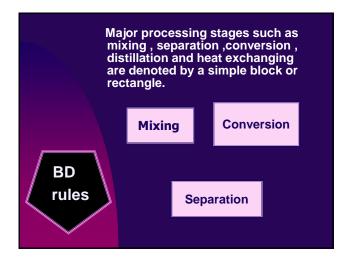


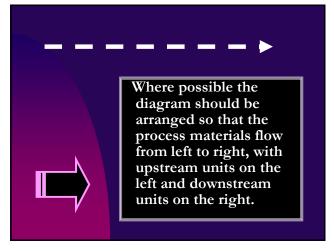


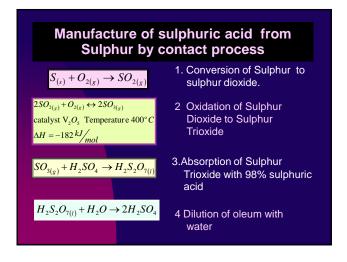


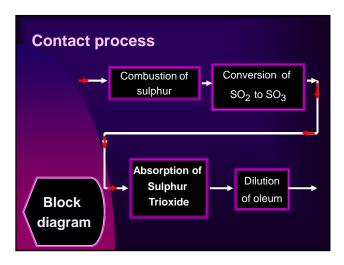


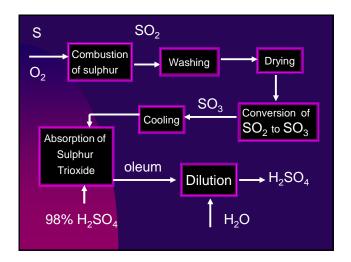


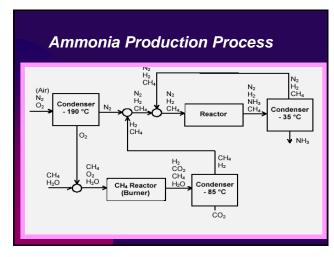


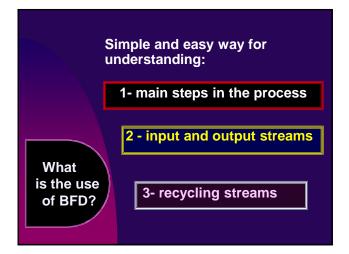


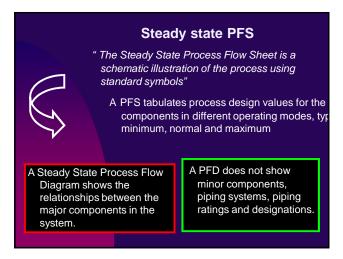


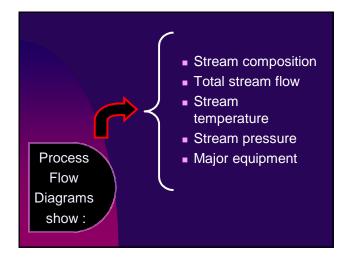


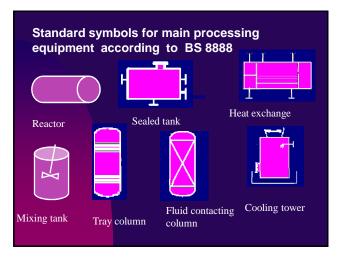


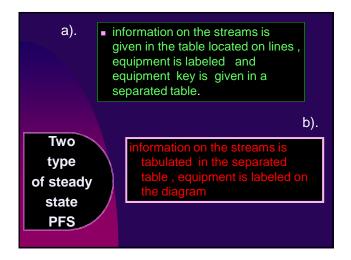


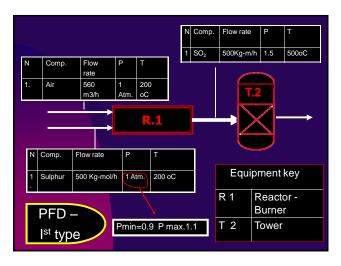


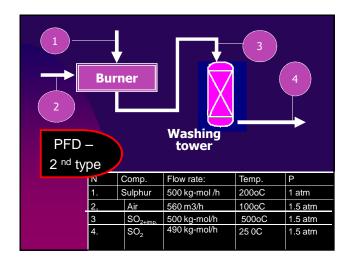


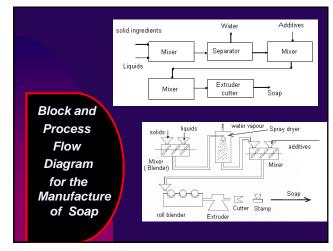


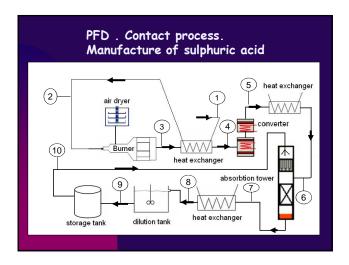


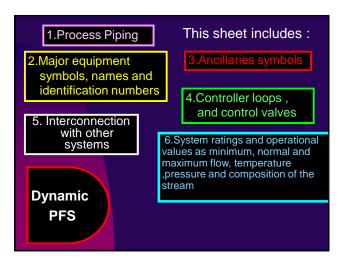


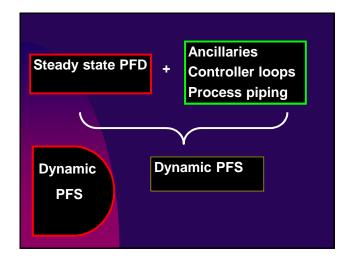


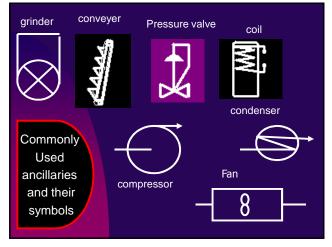


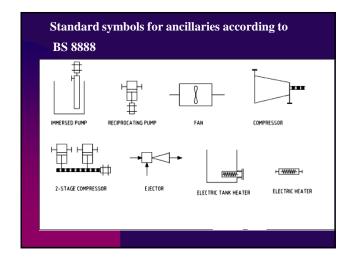


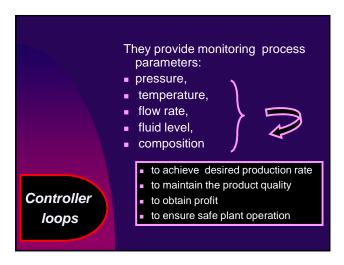


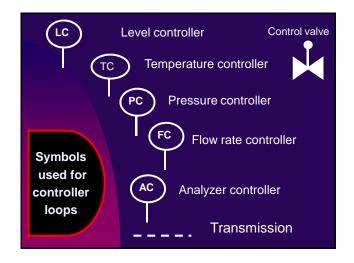


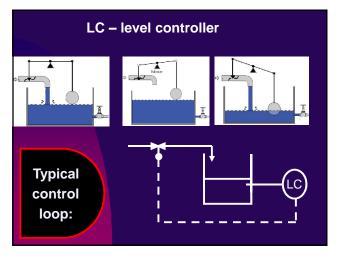


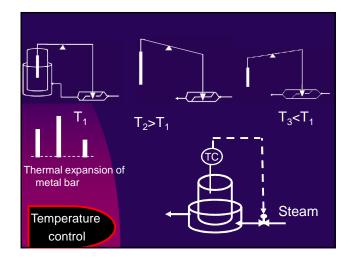


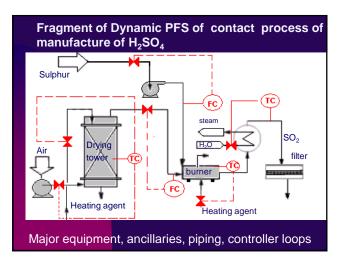


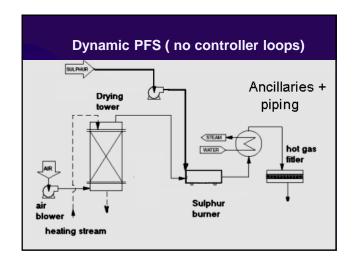


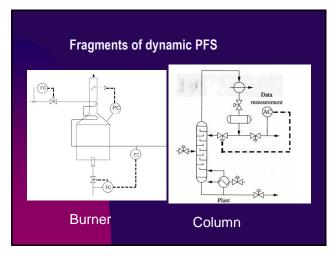


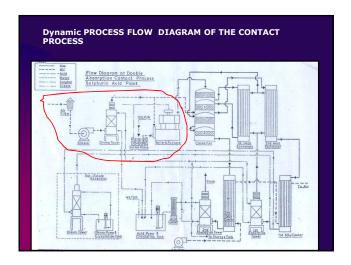


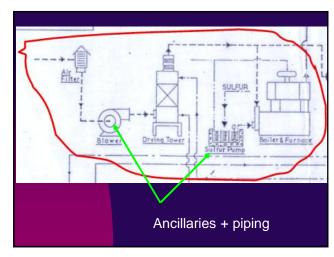


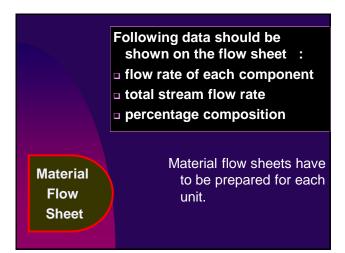


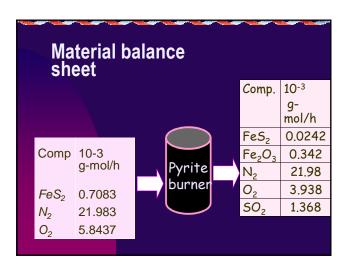


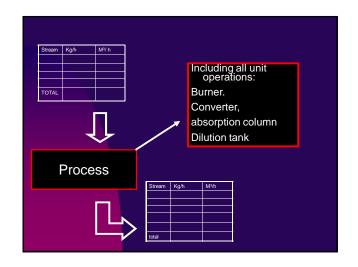


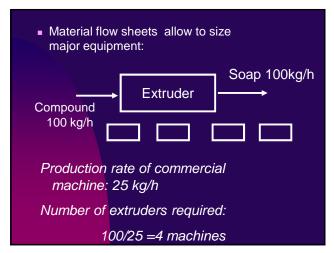


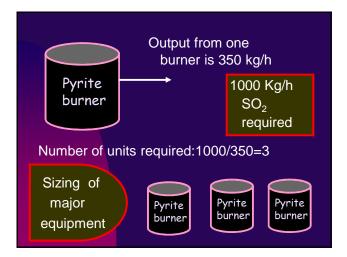


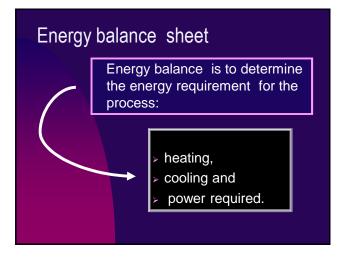


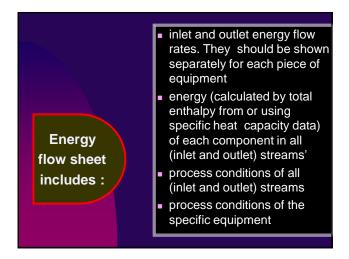


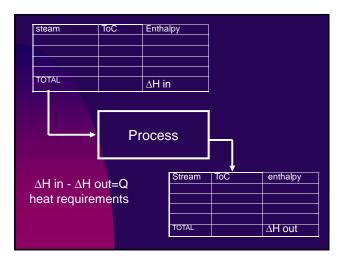


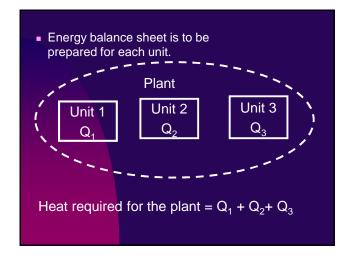


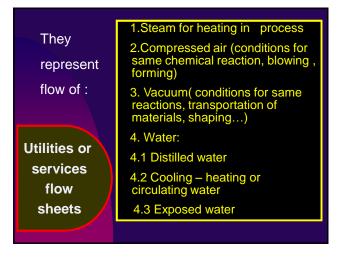


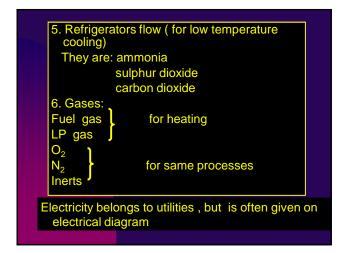


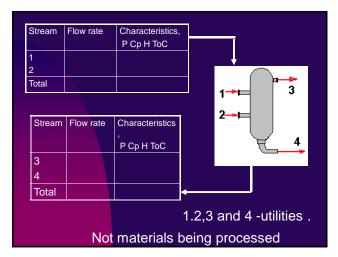


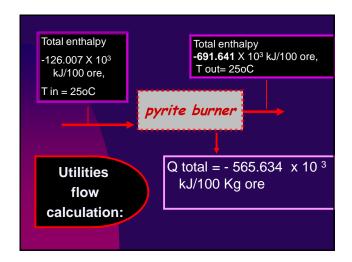


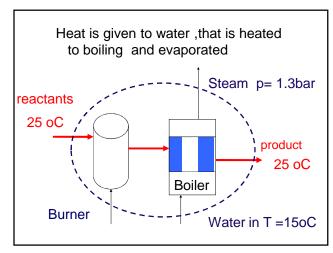


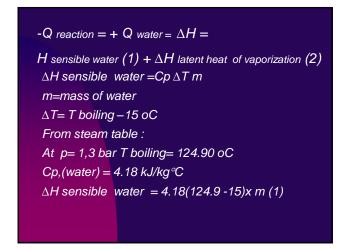








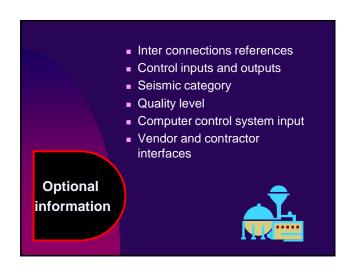


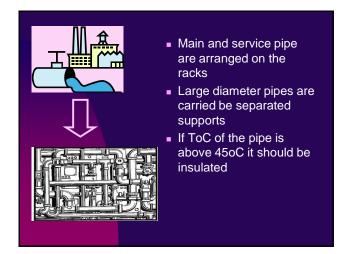


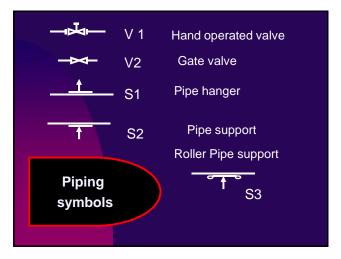
			kJ/kg	volume
1.3	130.0	124.90	2713.3	0.773

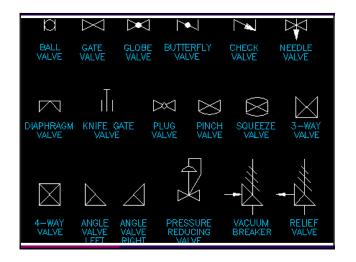
 ΔH latent heat of vaporization = mass x H' H' – specific latent heat of vaporization. From steam table: H' =2713.3 kJ/kg ΔH latent heat of vaporization = 2713.3 x m(2) $\Delta H = 4.18(124.9 - 15)x m + 2713.3 x m$ $Q \ water = - Q \ from \ process = \\ - (-565.634 \ x \ 10^{3}) \ kJ/100 \ kg \ ore$ $From \ where :$ $Mass \ of \ cooling \ water = 565.634 \ x \ 10^{3}/\\ 4.18(124.9 - 15) + 2713 = \\ 200 \ kg \ water /100 \ kg \ ore$ This is a schematic illustration of piping, and instrumentation.
 This diagram shows all piping including the physical sequence of branches, reducers, valves.
 They are used to operate the process system.
 Instrumentation Diagram

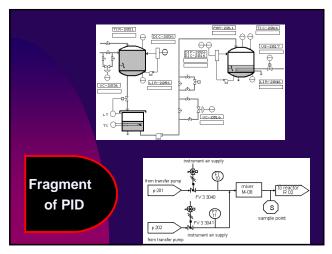
Instrumentation and designations All valves and their identifications Process piping, sizes and Piping and identification Instrumentation Miscellaneous - vents, drains, special fittings, sampling lines, Diagram reducers, increasers should Permanent start-up and flush lines include Flow directions

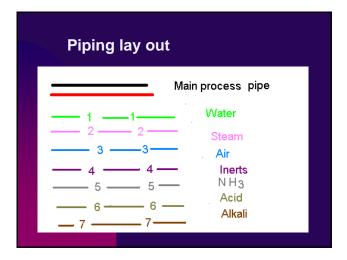


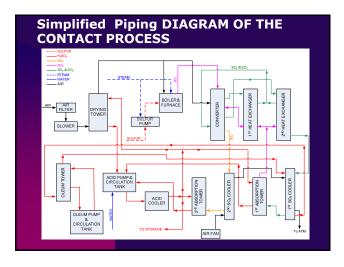


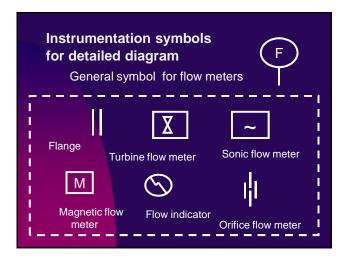


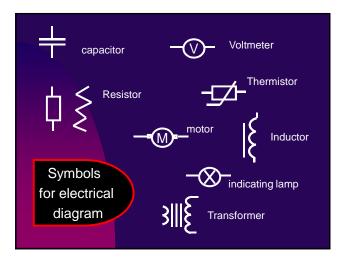


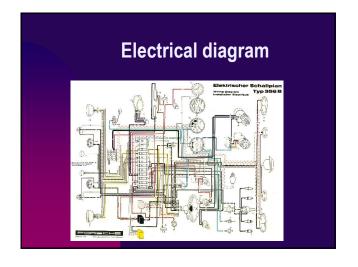


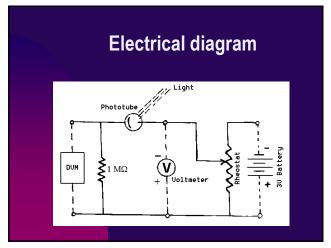


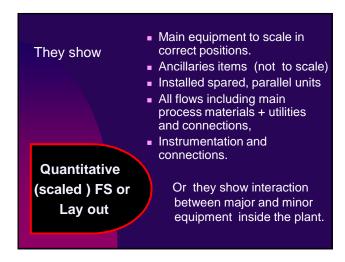


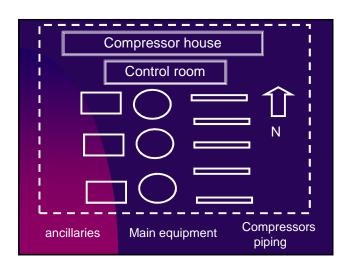












Plot plan or lay out should be drawn to scale, clearly indicating direction North.
 Layout should show the facilities/operations as they exist on the floor.
 The locations of various utilities (e.g., boiler house), laboratories, canteens, administrative blocks, storage areas (especially of hazardous substances) should be clearly indicated.

Areas that are marked for future expansion should also be shown.
 The compound wall should be indicated, clearly showing the entry and exit gates.
 Special thematic forms of layout can also be prepared to show water supply lines, steam lines, cabling, effluent drains, storm water channels etc

materials

Normally plants are arrange such a

way to give economical flow of

