

Detailed Solution of Quiz 2 2020-2021 Regular

Regular Stream 2020/21

QUIZ 2, 2020-2021 ME 365 THERMODYNAMICS II

PROPERTIES OF GASES AND GAS MIXTURES

GAS STATE EQUATIONS

1. According to Avogadro's law, volume of a g mol of all gases at the pressure of _____ and temperature of _____ is same.

- a) 760 mm Hg, 100 degree Celsius
- b) 760 mm Hg, 0 degree Celsius
- c) 750 mm Hg, 100 degree Celsius
- d) 750 mm Hg, 0 degree Celsius

Fact

$$n = m / M \quad \checkmark \text{ (i)}$$

2. Which of the following statements is true?

- a) number of kg moles of a gas = mass / molecular weight \checkmark
- b) molar volume = total volume of the gas / number of kg moles \checkmark
- c) both of the mentioned \checkmark
- d) none of the mentioned \times

Facts

$$\tilde{V} = \frac{V}{n} \quad \checkmark \text{ (ii)}$$

3. For which of the following gases, does the product (pv) when plotted against p gives depends only on temperature?

- a) nitrogen \checkmark
- b) hydrogen \checkmark
- c) air and oxygen \checkmark
- d) all of the mentioned \times

All ideal gases

IDEAL GAS - 1

4. Which of the following statement is true?

- a) characteristic gas constant is given by dividing the universal gas constant by the molecular weight \checkmark
- b) Avogadro's number (A) = 6.023×10^{26} molecules/kgmol \checkmark
- c) Boltzmann constant (K) = 1.38×10^{-23} J/molecule K \checkmark
- d) all of the mentioned \times

Facts

$$(i) R = \frac{R_u}{M} \quad \checkmark$$

$$(ii) A = 6.023 \times 10^{26} \frac{\text{molecules}}{\text{kg mol}} \quad \checkmark$$

$$(iii) K = 1.38 \times 10^{-23} \frac{\text{J}}{\text{mole K}} \quad \checkmark$$

5. For real gases,

- a) specific heats vary appreciably with temperature \checkmark
- b) specific heats vary little with pressure \checkmark
- c) both of the mentioned \checkmark
- d) none of the mentioned \times

6. Which of the following statement is true? (c is the specific heat at constant volume)

- a) the equation $du=c*dT$ holds good for an ideal gas for any process
- b) for gases other than ideal ones, the equation holds true for a constant volume process only
- c) for an ideal gas c is constant and hence $\Delta u=c*\Delta T$
- d) all of the mentioned

7. Characteristic gas constant is given by (here cp =specific heat at constant pressure and cv is the specific heat at constant volume)

- a) $R=cv - cp$
- b) $R=cp + cv$
- c) $R=cp - cv$
- d) none of the mentioned

fact

IDEAL GAS – 2

8. Which of the following statement is true?

- a) value of γ for monoatomic gases is $5/3$
- b) value of γ for diatomic gases is $7/5$
- c) for polyatomic gases, the value of γ is approximately taken as $4/3$
- d) all of the mentioned

9. Which of the following equation can be used to compute the entropy change between any two states of an ideal gas?

- a) $s_2-s_1 = c_v * \ln(T_2/T_1) + R * \ln(v_2/v_1)$ ✓
- b) $s_2-s_1 = cp * \ln(T_2/T_1) - R * \ln(p_2/p_1)$ ✓
- c) $s_2-s_1 = cp * \ln(v_2/v_1) + c_v * \ln(p_2/p_1)$ ✓
- d) all of the mentioned ✓

10. Which of the following is true for a polytropic process?

- a) $p(v^n)$ is used to describe the process ✓
- b) it is not adiabatic ✓
- c) it can be reversible ✓
- d) all of the mentioned ✓

11. Which of the following is true?

- a) for $n>\gamma$, there will be positive heat transfer and gain in entropy ✓
- b) for $n<\gamma$, there will be negative heat transfer and decrease in entropy ✓
- c) both of the mentioned
- d) none of the mentioned

for polytropic process

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$$s_2-s_1 = C_v \left(\frac{n-\gamma}{n-1} \right) \ln \left(\frac{T_2}{T_1} \right)$$

IDEAL GAS – 3

12. Which of the following values of n are correct?

 - a) for isobaric process, $n=0$
 - b) for isothermal process, $n=1$
 - c) for isentropic process, $n=\gamma$
 - d) all of the mentioned

$$\tilde{M}_{N_2} = 28 \text{ kg/kmol}$$

$$R_{N_2} = 0.2969 \frac{\text{KJ}}{\text{kg K}}$$

13. A rigid tank of 1 m^3 contains nitrogen gas at 600 kPa and 400 K . If 0.5 kg of gas flows out then what is the final pressure given the final temperature is 375 K ?

- a) 501.9 kPa
b) 503.9 kPa
c) 506.8 kPa ✓
d) none of the mentioned

$$m = \frac{PV}{RT} = \frac{600 \times 1}{0.2969 \times 300} = 5.052 \text{ Kg}$$

$$\therefore m_2 = m - 0.5 = 5.052 - 0.5 = 4.552 \text{ kg}$$

$$P = (m_2 RT) / V = 4.552 \times 0.2969 \times 375 / 1 = 506.8$$

14. A hollow metal sphere having an inside diameter of 150-mm is weighed first when evacuated and then after being filled to 875 kPa with an unknown gas. If the difference in mass is 0.0025 kg, and the temperature is 25 °C, find the gas.

- a) helium ✓
b) argon
c) hydrogen
d) nitrogen

$$\therefore \tilde{M} = \frac{\frac{m R_u T}{P V}}{PV} = \frac{m}{\tilde{M}} = \frac{0.0025 \times 8.3144 \times 298.15}{875 \times 0.001767}$$

15. A piston cylinder contains air at 600 kPa, 290 K and a volume of 0.01m³. A constant pressure process gives 54 kJ of work out. Find the final temperature of the air.

$$P_1 = P_2 \quad \text{ideal gas } PV = mRT \quad |W| = P\Delta V \Rightarrow \Delta V = \frac{|W|}{P} \quad \text{which is Helium}$$

a) 2700 K $PV = mRT_1$
 b) 2800 K
 c) 2900 K $P_2V_2 = mRT_2$ $V_2 = V_1 + \Delta V = 0.01 + 0.09 = 0.1 \text{ m}^3$ 600 kN/m^2
 d) 3000 K

GAS COMPRESSION

$$\frac{P_2V_2}{P_1V_1} = \frac{T_2}{T_1} \Rightarrow T_2 = \frac{P_2V_2T_1}{P_1V_1} = \frac{V_2}{V_1} \times T_1 = \frac{0.1}{0.01} \times 290$$

16. For $\gamma > n > 1$ and for the same pressure ratio p_2/p_1 , the maximum work is needed for

- a) isothermal compression X
 - b) adiabatic compression ✓
 - c) polytropic compression X
 - d) all need same work X

$$T_2 = 2900 \text{ K}$$

17. For minimum work the intermediate pressure is the _____ of the suction and discharge pressures.

- a) arithmetic mean
- b) geometric mean
- c) sum
- d) difference

18. Heat rejected in the intercooler is given by (here c_p is the specific heat at constant pressure)

- a) $c_p * (T_3 - T_2)$
- b) $c_p * (T_3 + T_2)$
- c) $c_p * (T_2 - T_3)$
- d) none of the mentioned

19. The isothermal efficiency of a compressor is given by

- a) $p_1 * v_1 / \text{total work of compression}$
- b) $p_1 * v_1 * \ln(p_2/p_1) / \text{total work of compression}$
- c) $\text{total work of compression} / p_1 * v_1 * \ln(p_2/p_1)$
- d) $\text{total work of compression} / p_1 * v_1$

20. The volumetric efficiency is given by

- a) $1 - C + C(p_2/p_1)^{1/n}$ X
- b) $1 + C - C(p_2/p_1)^{1/n}$ ✓
- c) $1 + C + C(p_2/p_1)^{1/n}$ X
- d) $1 - C - C(p_2/p_1)^{1/n}$ X

Fad

PSYCHOMETRICS

PROPERTIES OF ATMOSPHERIC AIR

21. Complete dry air exists in nature.

- a) true
- b) false

22. In a mixture of dry air and water vapour,

- a) mole fraction of dry air = p_a/p
- b) mole fraction of water vapour = p_w/p
- c) both of the mentioned
- d) none of the mentioned

23. When the partial pressure of water (p_w) is very small,

- a) saturation temperature of water vapour at p_w is less than atmospheric temperature
- b) water vapour in air exists in superheated state
- c) air is said to be in unsaturated state
- d) all of the mentioned

24. If water is injected into a container which has unsaturated air,

- a) water will evaporate
- b) moisture content of air will decrease
- c) p_w will decrease
- d) all of the mentioned

25. The degree of saturation is the ratio of

- a) (saturated specific humidity / actual specific humidity)²
- b) 1/(saturated specific humidity * actual specific humidity)
- c) saturated specific humidity / actual specific humidity
- d) actual specific humidity / saturated specific humidity

26. The wet bulb temperature is the _____ temperature recorded by moistened bulb.

- a) lowest
- b) highest
- c) atmospheric
- d) none of the mentioned

27. At any dry bulb temperature, the _____ the difference of the wet bulb temperature reading below the dry bulb temperature, the _____ is the amount of water vapour held in mixture.

- a) smaller, smaller
- b) greater, greater
- c) greater, smaller
- d) smaller, greater

PSYCHROMETRIC CHART AND PROCESSES

28. Which of the following statements is true relating to the Psychrometric chart?

- a) the chart is plotted for pressure equal to 760mm Hg
- b) the constant wet bulb temperature line represents adiabatic saturation process
- c) the constant wet bulb temperature line coincides with constant enthalpy line
- d) all of the mentioned

29. When humidity ratio of air _____ the air is said to be dehumidified.

- a) increases
- b) decreases
- c) remains constant
- d) none of the mentioned

30. Cooling and dehumidification of air is done in summer air conditioning.

- a) true
- b) false

31. When air passes through silica gel,

- a) it absorbs water vapour molecules
- b) latent heat of condensation is released
- c) dry bulb temperature of air increases
- d) all of the mentioned

32. In adiabatic evaporative cooling, heat transfer between the chamber and its surroundings is

- a) zero
- b) high
- c) low
- d) none of the mentioned

COMBUSTION OF FUELS

33. The process of burning fuels in the presence of oxygen is called _____

- a) Induction
- b) Ignition
- c) Condensation
- d) Combustion

34. The substance which helps in combustion of fuels is called _____

- a) Igniter
- b) Flammables
- c) Supporter
- d) Inflammables

35. $C + O_2 \rightarrow$ _____

- a) CO
- b) CO_2
- c) CO_3
- d) 2CO

FUELS AND COMBUSTION

36. Which are the main constituents of fuel from given options?

- a) Carbon and Nitrogen
- b) Oxygen and Hydrogen
- c) Carbon and Hydrogen
- d) Helium and Oxygen

37. On what basis is the coal classified?

- a) Period of formation
- b) Depending on capacity to burn
- c) Region/area where it formed
- d) Physical and chemical composition

CALORIFIC VALUES OF FUEL - 1

38. The amount of heat liberated by complete combustion of unit quantity of fuel is known as

- a) Agitation
- b) Combustion
- c) Calorific value
- d) Thermogenesis

39. Which gas has the highest calorific value among given option?

- a) Oxygen
- b) Helium
- c) Hydrogen
- d) Nitrogen

40. Which calorimeter is used to find calorific values of solid and liquid fuels?

- a) Boy's calorimeter
- b) Bomb calorimeter
- c) Junker's calorimeter
- d) Calvet-type calorimeter

41. What value of a substance, usually a fuel or food is the amount of heat released during the combustion?

- a) Energy value
- b) Flash point value
- c) Fire point value
- d) Auto ignition

42. What is the factor on which, difference between the two heating values of fuel depends on?

- a) Physical properties
- b) Reactants
- c) Chemical composition
- d) Products

CALORIFIC VALUES OF FUEL – 2

43. Which is the common method to relate higher calorific value to lower calorific value?

- a) $HCV = LCV + Hv(n_{H_2O, out} / n_{fuel, in})$
- b) $LCV = HCV + Hv(n_{H_2O, out} / n_{fuel, in})$
- c) $HCV = LCV + Hv(n_{fuel, in} / n_{H_2O, out})$
- d) $LCV = HCV + Hv(n_{fuel, in} / n_{H_2O, out})$

44. Which value is determined by bringing all products of combustion back to original pre-combustion temperature?

- a) Higher calorific value
- b) Low calorific value
- c) Flash point value
- d) Fire point value

45. Which formula is used to determine higher calorific value of fuel?

- a) Rayleigh's formula
- b) Lamme's equation
- c) Dulong's formula
- d) Cauchy's formula

Fact.

46. Which fuel has higher calorific value among given fuels?

- a) Natural gas
- b) Gasoline
- c) Diesel
- d) Fuel oil

ADDITIONAL QUESTIONS ON REFRIGERATION

47. In a vapour compression refrigeration system, a throttle valve is used in place of expander because

- a) It considerably reduces the system weight
- b) It improves the COP, as the condenser is small
- c) The positive work involved in the isentropic expansion of liquid is very small
- d) It leads to significant cost reduction

48. Consider the following statements:

Moisture should be removed from refrigerants in order to avoid:

- | | |
|-------------------------------|------------------------------------|
| 1. Compressor seal failure | 2. Freezing at the expansion valve |
| 3. Restriction to refrigerant | 4. Corrosion steel parts |

On these statements

- a) 1, 2, 3 and 4 are correct
- b) 2, 3 and 4 are correct
- c) 1 and 2 are correct
- d) 1, 3 and 4 are correct

49. The refrigerant used for absorption refrigerators working on the heat from solar collectors is a mixture of water and

- a) Carbon dioxide
- b) Sulphur dioxide
- c) Lithium bromide
- d) Freon-12.

50. The desirable combination of properties for a refrigerant includes:

- (a) High specific heat and high specific volume of refrigerant vapour
- (b) High heat transfer coefficient and low latent heat
- c) High thermal conductivity and low freezing point
- (d) High latent heat of vaporisation and low specific volume of refrigerant vapour

51. Match items in List I (A -D) with those in List II (1-4) and List III (6-10) and then select the correct answer using the codes given below the Lists:

List I

- A. Reversed Carnot engine
- B. Sub-cooling
- C. Super heating
- D. Constant enthalpy

List II

- 1. Condenser
- 2. Evaporator
- 3. Vortex refrigerator
- 4. Throttling
- 5. Heat pump

List III

- 6. Generator
- 7. Increase in refrigerating effect
- 8. Highest COP
- 9. Adiabatic
- 10. Dry compression

Codes:

- A. A B C D
3, 10 1, 7 2, 9 4, 6
- B. A B C D
5, 8 1, 7 2, 10 4, 9
- C. A B C D
4, 10 3, 8 3, 10 1, 6
- D. A B C D
2, 7 5, 8 4, 6 1, 9

52. When the discharge pressure is too high in a refrigerators system, high pressure control is installed to

- a) Stop the cooling fan
- b) Stop the water circulating pump
- c) Regulate the flow cooling water
- d) Stop the compressor

53. Consider the following statements:

In the case the vapour compression machine, if the condensing temperature of the refrigerant is closer to the critical temperature, then there will be

- 1. Excessive power consumption
- 2. High compression
- 3. Large volume flow

Of these statements

- a) 1, 2 and 3 are correct
- b) 1 and 2 are correct
- c) 2 and 3 are correct
- d) 1 and 3 are correct

54. A single stage vapour compression refrigeration system cannot be used to produce ultra low temperature because

- a) refrigerants for ultra-low temperature are not available
- b) Lubricants for ultra-low temperature are not available
- c) Volumetric efficiency will decrease considerably
- d) Heat leakage into the system will be excessive

55. Vapour absorption refrigeration system works using

- a) ability of a substance to get easily condensed
- b) Ability of a vapour to get compressed or expanded
- c) Affinity of a substance of another substance
- d) Absorptivity of a substance

56. Which one of the following statements regarding ammonia absorption refrigeration system is correct?

The solubility of ammonia in water is

- a) a function of the temperature and pressure of solution
- b) A function of the pressure of the solution irrespective of the temperature
- c) A function of temperature of the solution alone
- d) Independent of the temperature and pressure of the solution

57. The flash chamber in single-stage simple vapour compression cycle

- a) Increases the refrigerating effect
- b) Decreases the refrigerating effect
- c) Increases the work of compression
- d) has no effect on refrigerating effect

58. Consider the following statements:

In a vapour compression system, a thermometer placed in the liquid line can indicate whether the

- 1. Refrigerant flow is too low
- 3. Condenser is fouled

Of these statements:

- a) 1, 2 and 3 are correct
- c) 1, 3 and 4 are correct

- 2. Water circulation is adequate
- 4. Pump is functioning properly

- b) 1, 2 and 4 are correct
- d) 2, 3 and 4 are correct

59. Match List I (A-D) with List II (1-4) and then select the correct answer using the codes given below the Lists:

Lists I

- A. Bell Coleman refrigerator
- B. Simple vapour-compression refrigerator
- C. Absorption refrigerator
- D. Jet refrigerator

List II

- 1. Compressor
- 2. Generator
- 3. Flash Chamber
- 4. Expansion cylinder

Codes:

a) A B C D

1 4 3 2

b) A B C D

4 1 3 2

c) A B C D

1 4 2 3

d) A B C D

4 1 2 3

$$W_{12} = h_2 - h_1 = 279.37 - 251.88 = 27.49 \text{ kJ/kg}$$

CALCULATIONS ON HEAT PUMP, GAS REFRIGERATION, MIXTURES,
PSYCHROMETRY, AIR CONDITIONING AND COMBUSTION OF FUELS

$$Q_1 = h_2 - h_3 \quad 60$$

$$H = 279.37 - 117.77$$

$$P_{12}^q = 161.16$$

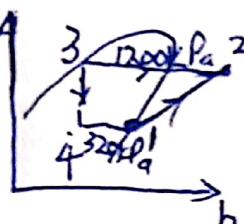
$$P_1 = 320 \text{ kPa}$$

$$S_1 = 0.9306$$

$$h_1 = 251.88 \text{ kJ/kg}$$

Consider a heat pump that operates on the ideal vapour compression refrigeration cycle with R-134a as the working fluid between the pressure limits of 0.32 and 1.2 MPa. The coefficient of performance of this heat pump is approximately:

- (a) 0.17
- (b) 1.2
- (c) 3.1
- (d) 4.9
- (e) 5.9



$$\begin{aligned} P_2 &= 1200 \text{ kPa} \quad h_2 = 279.37 + \frac{(0.9306 - 0.9267)}{279.37 - 251.88} (251.88) \\ S_1 &= S_2 = 0.9306 \quad (0.9306 - 0.9267) \\ h_3 &= h_1 = 251.88 \text{ kJ/kg} \quad COP = \frac{161.16}{27.49} \\ P_{12}^q &= 117.77 \text{ kPa} = h_4 = h_1 \end{aligned}$$

$$61 \quad \text{Refrigeration Cycle}$$

$$T_1 = T_2 = 279.37 \text{ K}$$

$$\begin{array}{l} T_3 = 308 \text{ K} \\ T_4 = T_1 = T_2 = 279.37 \text{ K} \\ P_1 = P_2 = P_3 = P_4 \end{array}$$

$$\gamma_{\text{air}} = 1.4$$

An ideal gas refrigeration cycle using air as the working fluid operates between the pressure limits of 80 and 280 kPa. Air is cooled to 35 °C before entering the turbine. The lowest temperature of this cycle is approximately:

$$T_3 = 308 \text{ K}$$

- (a) -57.7 °C
- (b) -26.1 °C
- (c) 5.1 °C
- (d) 11.2 °C
- (e) 24.1 °C

$$\frac{T_4}{T_3} = \left(\frac{P_4}{P_3} \right)^{1/1.4} \Rightarrow T_4 = T_3 \left(\frac{80}{280} \right)^{0.4/1.4} = 308 \left(\frac{80}{280} \right)^{0.4/1.4}$$

$$T_4 = 215.3 \text{ K} (-57.7^\circ \text{C})$$

$$62$$

Consider an ideal gas refrigeration cycle using helium as the working fluid. Helium enters the compressor at 100 kPa and 17 °C and compressed to 400 kPa. Helium is then cooled to 20 °C before it enters the turbine. For a mass flow rate of 0.2 kg/s, the net power input required is approximately:

$$C_p = 5.1926 \text{ kJ/kg}$$

$$\gamma_{He} = 1.667$$

$$T_1 = 290 \text{ K}$$

$$T_2 = 293 \text{ K}$$

$$T_3 = 290 \text{ K}$$

$$W_{\text{net,in}} = 93.77 \text{ kW} \quad W_{\text{net,in}} = m C_p [(T_2 - T_1) - (T_3 - T_4)]$$

$$(a) 28.3 \text{ kW} \quad (b) 40.5 \text{ kW} \quad (c) 64.7 \text{ kW} \quad (d) 93.8 \text{ kW} \quad (e) 113 \text{ kW}$$

$$T_2 = T_1 \left(\frac{400}{100} \right)^{0.667/1.667} = 290 \left(\frac{400}{100} \right)^{0.667/1.667} = 505 \text{ K}$$

$$W_{\text{net,in}} = 0.2 \times 5.1926 \left[\left(\frac{505 - 290}{293 - 290} \right) \right] = 293 \left(\frac{100}{400} \right)^{0.667/1.667} = 168.3 \text{ kW}$$

An absorption air-conditioning system is to remove heat from the conditioned space at 20 °C at a rate of 150 kJ/s while operating in an environment at 35 °C. Heat is to be supplied from a geothermal source at 140 °C. The minimum rate of heat supply is approximately:

$$T_E = 35^\circ \text{C} (308 \text{ K})$$

$$(a) 86.2 \text{ kJ/s}$$

$$T_G = 140^\circ \text{C} (413 \text{ K})$$

$$(b) 21.2 \text{ kJ/s}$$

$$T_L = 20^\circ \text{C} (293 \text{ K})$$

$$(c) 30.2 \text{ kJ/s}$$

$$Q_L = 150 \text{ kJ/s}$$

$$(d) 61.2 \text{ kJ/s}$$

$$Q_G = Q_L$$

$$(e) 150 \text{ kJ/s}$$

$$COP_{\text{max}, ABRS} = \left(1 - \frac{T_E}{T_G} \right) \left(\frac{T_L}{T_E - T_L} \right) = \left(1 - \frac{308}{413} \right) \left(\frac{293}{308 - 293} \right) = 4.966$$

$$Q_{G,\min} = \frac{Q_L}{COP_{\text{max}}} = \frac{150 \text{ kJ/s}}{4.966} = 30.2 \text{ kJ/s.}$$

- 64 An ideal-gas mixture consists of 3 kg of Ar and 6 kg of CO₂ gases. The mixture is now heated at constant volume from 250 K to 350 K. The amount of heat transfer is approximately:

- (a) 374.1 kJ
- (b) 435.6 kJ
- (c) 487.9 kJ ✓
- (d) 524.7 kJ
- (e) 663.9 kJ

$$m_{Ar} = 3 \text{ kg}; C_{V,Ar} = 0.3122 \text{ kJ/kgK} \quad (\text{Lecture Material})$$

$$m_{CO_2} = 6 \text{ kg}; C_{V,CO_2} = 0.657 \text{ kJ/kgK} \quad (\text{Lecture Material})$$

$$T_{in} = T_1 = 250 \text{ K} \quad T_{final} = T_2 = 350 \text{ K}$$

$$Q = 487.89 \text{ kJ} \quad \text{or} \quad Q = (m_{Ar} C_{V,Ar} + m_{CO_2} C_{V,CO_2})(T_2 - T_1) = (3 \times 0.3122 + 6 \times 0.657)(350 - 250)$$

- 65 An ideal-gas mixture consists of 60 percent helium and 40 percent argon gases by mass. The mixture is now expanded isentropically in a turbine from 400 °C and 1.2 MPa to a pressure of 200 kPa. The mixture temperature at turbine exit is approximately:

- (a) 55.6 °C ✓
- (b) 194.5 °C
- (c) 129.9 °C
- (d) 112.1 °C
- (e) 400.1 °C

$$\gamma_{He} = 1.667; \gamma_{Ar} = 1.667; \therefore \gamma_{mix} = 1.667$$

$$T_1 = 400^\circ\text{C} (673 \text{ K}); T_2 = T_1 \left(\frac{P_f}{P_i} \right)^{\frac{1}{\gamma-1}} - 273$$

$$= 673 \left(\frac{200}{1200} \right)^{0.667/1.667} - 273 = 55.59^\circ\text{C}$$

$$\leq 55.6^\circ\text{C}$$

$$C_V = 10.183 \text{ kJ/kgK}$$

~~insulated tank~~ $\sim Q = 0$

$$m = nM$$

$$\bar{m} = 2 \text{ kg/kmol}$$

$$\bar{M} = 44 \text{ kg/kmol}$$

$$C_V = 0.657 \text{ kJ/kgK}$$

$$\bar{m}_{He} = 4 \text{ kg/kmol}$$

He = Argon

H = Helium

$$\bar{M} = 3 \times 4 = 12 \text{ kg}$$

$$\bar{M} = 7 \times 35.95$$

$$\bar{m}_{Ar} = 279.65 \text{ kg}$$

$$\bar{m} = 35.95 \text{ kg/kmol}$$

Ar

$$(a) 25.6^\circ\text{C}$$

$$(b) 29.6^\circ\text{C}$$

$$(c) 22.6^\circ\text{C}$$

$$(d) 32.6^\circ\text{C}$$

$$(e) 34.6^\circ\text{C}$$

$$m_{He} = 5 \times 2 = 10 \text{ kg}; m_{CO_2} = 2 \times 44 = 88 \text{ kg}$$

$$T_1 = 35^\circ\text{C} (308 \text{ K})$$

$$T_1 = 20^\circ\text{C} (293 \text{ K})$$

$$Q = m_{He} C_{V,He} (T_2 - T_1) + m_{CO_2} C_{V,CO_2} (T_2 - T_1)$$

$$T_2 = 29.56^\circ\text{C} \quad \text{or} \quad 29.6^\circ\text{C}$$

A piston-cylinder device contains an ideal-gas mixture of 3 kmol of He gas and 7 kmol of Ar gas at 50 °C and 400 kPa. Now the gas expands at constant pressure until its volume doubles. The amount of heat transfer to the gas mixture is approximately:

$$T_f = 50^\circ\text{C} (323 \text{ K})$$

$$(a) 6.2 \text{ MJ}$$

$$(b) 4.2 \text{ MJ}$$

$$(c) 27 \text{ MJ}$$

$$(d) 10.1 \text{ MJ}$$

$$(e) 67.1 \text{ MJ}$$

$$Q = n_1 C_p (T_f - T_i) + n_2 C_p (T_f - T_i)$$

why: gas expand at constant pressure and volume double

$$= 279.65 \times 0.5203 (646 - 323) + 12 \times 5.1926 (646 - 323)$$

$$Q = 67.123 \text{ MJ} \quad \text{or} \quad 67.1 \text{ MJ}$$

$$C_p = 0.5203 \text{ kJ/kgK}$$

$$C_p = 5.1926 \text{ kJ/kgK}$$

From Table in lecture material on page 83

For the turbine

$$T_f = T_{in} \left(\frac{P_f}{P_{in}} \right)^{\gamma-1/8} = 1500 \left(\frac{100}{1000} \right)^{0.667/1.667} = 597 K$$

68

An ideal-gas mixture of helium and argon gases with identical mass fractions enters a turbine at 1500 K and 1 MPa at a rate of 0.12 kg/s, and expands isentropically to 100 kPa. The power output of the turbine is approximately: $\chi_{mix} = 1.667$

$$\begin{aligned} 1 &= \text{Argon} \\ 2 &= \text{Helium} \\ C_p &= 0.5203 \text{ kJ/kg K} \\ C_p &= 5.1926 \text{ kJ/kg K} \end{aligned}$$

- (a) 252.8 kW
- (b) 309.6 kW ✓
- (c) 340.8 kW
- (d) 462.9 kW
- (e) 550 kW

$$C_{p_{mix}} = m_1 C_{p_1} + m_2 C_{p_2} = 0.5 \times 0.5203 + 0.5 \times 5.1926$$

$$C_{p_{mix}} = 2.8475 \text{ kJ/kg K}$$

$$m_i = \text{mass fraction} \quad |W_e| = 309.55 \text{ kW}$$

69

A room is filled with saturated moist air at 25 °C and a total pressure of 100 kPa. If the mass of dry air in the room is 100 kg, the mass of water vapour is approximately:

- (a) 0.52 kg
- (b) 1.97 kg
- (c) 2.96 kg
- (d) 2.04 kg ✓
- (e) 3.17 kg

$$\begin{aligned} P_{atm} &= 100 \text{ kPa} & T_i &= 25^\circ C, P_g &= 3.1698 \text{ kPa} & \text{Table A4} \\ M_{air} &= 100 \text{ kg} & \text{and } \phi = 100\% & P_v = P_g \\ w_i &= \frac{0.622 P_v}{P_i - P_v} & = \frac{0.622 \times 3.1698}{100 - 3.1698} & = 0.0204 \frac{\text{kg H}_2\text{O}}{\text{kg dry air}} \end{aligned}$$

$$M_v = w M_{air} = 0.0204 \times 100 = 2.04 \text{ kg}$$

70

A room contains 65 kg of dry air and 0.6 kg of water vapour at 25 °C and 90 kPa total pressure. The relative humidity of air in the room is approximately:

- (a) 3.5 %
- (b) 41.5 % ✓
- (c) 55.2 %
- (d) 60.9 %
- (e) 73.0 %

A 40-m³ room contains air at 30 °C and a total pressure of 90 kPa with a relative humidity of 75 percent. The mass of dry air in the room is approximately:

- (a) 24.7 kg
- (b) 29.9 kg
- (c) 39.9 kg ✓
- (d) 41.4 kg
- (e) 52.3 kg

$$T_i = 30^\circ C (303 K) \quad P_g = 4.2469 \text{ kPa Table A4}$$

$$RH = 0.75 \Rightarrow P_v = 0.75 \times 4.2469 = 3.1852 \text{ kPa}$$

$$w = \frac{0.622 \times P_v}{P_i - P_v} = \frac{0.622 \times 3.1852}{90 - 3.1852} = 0.0228 \frac{\text{kg H}_2\text{O}}{\text{kg dry air}}$$

$$\text{For air } P_a V = m R T_i$$

$$\begin{aligned} P_a &= P_i - P_v \\ &= 90 - 3.1852 \\ &= 86.8148 \text{ kPa} \end{aligned}$$

$$m = \frac{P_a V}{R T_i} = \frac{86.8148 \times 40}{0.287 \times 303}$$

P_a = partial pressure of dry air

$$m = 39.93 \text{ kg} \approx 39.9 \text{ kg}$$

72

A room contains air at 30 °C and a total pressure of 96.0 kPa with a relative humidity of 75 percent. The partial pressure of dry air is approximately:

$$\begin{aligned} P_t &= 96 \text{ kPa} \\ RH &= \phi = 0.75 \\ P_d &=? \end{aligned}$$

- (a) 82.0 kPa
- (b) 85.8 kPa
- (c) 92.8 kPa ✓
- (d) 90.6 kPa
- (e) 72.0 kPa

Note: $w = \frac{0.622 P_v}{P_a}$

$$T_i = 30^\circ\text{C}, P_g = 42469 \text{ kPa}$$

$$P_v = \phi \times P_g = 0.75 \times 42469 = 31852 \text{ kPa}$$

$$P_d = P_t - P_v = 96 - 31852 = 92.8148 \text{ kPa}$$

Table A4

73

The air in a house is at 25 °C and 65 percent relative humidity. Now the air is cooled at constant pressure. The temperature at which the moisture in the air will start condensing is approximately:

$$T_i = 25^\circ\text{C} \Rightarrow P_g = 31698 \text{ kPa} \quad \text{Table A4}$$

$$P_d @ 25^\circ\text{C} = P_g$$

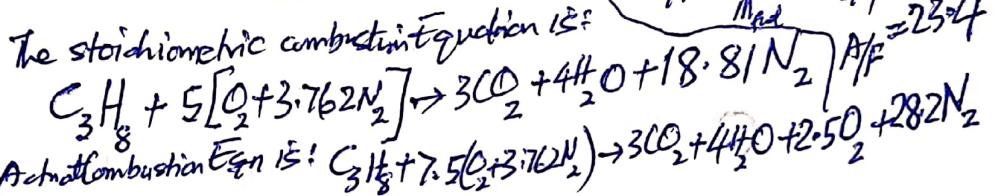
- (a) 7.4 °C
- (b) 16.3 °C
- (c) 18.0 °C ✓
- (d) 11.3 °C
- (e) 20.2 °C

$$T_d = T_{sat} @ P_d = 15 + \frac{(2.0604 - 1.7057)(5)}{(2.3392 - 1.7057)} = 17.99^\circ\text{C}$$

$$\approx 18^\circ\text{C}$$

Propane (C_3H_8) is burned with 150 percent theoretical air. The air-fuel mass ratio for this combustion process is approximately: $\lambda = 1.5$

- (a) 5.3
- (b) 10.5
- (c) 15.7
- (d) 23.4 ✓
- (e) 39.3



74

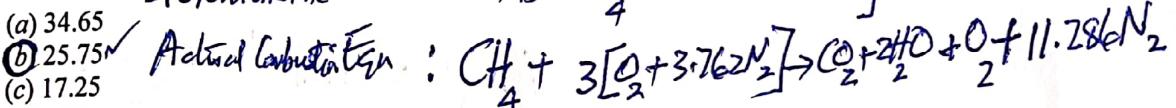
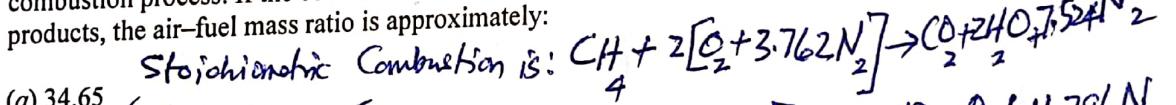
One kmol of methane (CH_4) is burned with an unknown amount of air during a combustion process. If the combustion is complete and there are 1 kmol of free O_2 in the products, the air-fuel mass ratio is approximately:

$$\begin{aligned} M &= 3 \times 12 + 1 \times 8 \\ f &= 44 \text{ kg} \end{aligned}$$

Stoichiometric
2 O_2 molecules
A fuel needs 1 O_2
extra 1 kmol of O_2
so O_2 kmol is become

- (a) 34.65
- (b) 25.75 ✓
- (c) 17.25
- (d) 14.35
- (e) 11.95

Stoichiometric Combustion is:



$$M_{fuel} = 1 \times 12 + 1 \times 4 = 16 \text{ kg}$$

$$M_{air} = 3 \times 32 + 11.286 \times 28 = 412.008 \text{ kg}$$

$$A/F = \frac{M_{air}}{M_{fuel}} = \frac{412.008}{16} = 25.75$$

$$P_{CO_2} = \frac{\tilde{R}_u}{\tilde{M}_{CO_2}} = \frac{83144}{44} = 0.1889 \text{ kJ/kg K}$$

Cp_{CO₂} = 0.846 kJ/kg K
Page 83 Lecture material

- 76** An equimolar mixture of carbon dioxide and water vapour at 1 atm and 60 °C enter a dehumidifying section where the entire water vapour is condensed and removed from the mixture, and the carbon dioxide leaves at 1 atm and 60 °C. The entropy change of carbon dioxide in the dehumidifying section is approximately:

y_i = mole fraction
of a
constituent

$$P_{H_2O} = 0.5 \text{ atm}$$

$$P_{CO_2} = 1 \text{ atm.}$$

- (a) -2.8 kJ/kg·K
- (b)** -0.131 kJ/kg·K ✓
- (c) 0
- (d) 0.131 kJ/kg·K
- (e) 2.8 kJ/kg·K

$$y_{i, CO_2} = 0.5 \quad y_i = 0.5 \text{ equimolar mixture.}$$

$$\Delta S_{CO_2} = -0.1889 \ln\left(\frac{1}{0.5}\right) = -0.131 \text{ kJ/kg K}$$

$$\bar{T}_r = 60^\circ\text{C} (333\text{K})$$

$$\frac{\bar{T}_2}{\bar{T}_1} = \frac{1}{2} \quad \Delta S = C_p \ln\left(\frac{\bar{T}_2}{\bar{T}_1}\right) - R_{CO_2} \ln\left(\frac{P_{CO_2}}{P_{CO_2}}\right)$$

- 77** Methane (CH₄) (HH V=55.56 MJ/kg, LHV=50.05 MJ/kg) is burned completely with 80 percent excess air during a steady-flow combustion process. If both the reactants and the products are maintained at 25 °C and 1 atm and the water in the products exists in the liquid form, the heat transfer from the combustion chamber per unit mass of methane, correct to the nearest integer, is:

- (a) 62.5 MJ/kg
- (b)** 132 MJ/kg
- (c) 70 MJ/kg
- (d)** 56 MJ/kg
- (e) 50 MJ/kg

$$Q_f = HHV \text{ of } CH_4 \cdot T_{reactants} = 25^\circ\text{C} = T_{ref.}$$

$$\approx 56 \text{ MJ/kg. } T_{products} = 25^\circ\text{C} = T_{ref.}$$

- 78** The higher heating value of a hydrocarbon fuel C_nH_m with m= 8 is given to be 1560 MJ/kmol of fuel. Then its lower heating value is approximately:

- (a)** 1384 MJ/kmol
- (b) 1208 MJ/kmol
- (c) 1402 MJ/kmol
- (d) 1514 MJ/kmol
- (e) 1551 MJ/kmol

Notes: h_{fg} of water @ 25°C = 2.443 MJ/kg

$$m/2 = 4$$

$$\text{mass of H}_2\text{O formed per kmol fuel} = 4 \times 18 \text{ kg/kmol}$$

F.K. FORSON

R. OPOKU

$$\text{LHV} = HHV - \frac{m \times h_{fg}}{n_{fuel}}$$

$$= 1560 \frac{\text{MJ}}{\text{kmol fuel}} = \frac{72 \times 2.443 \text{ MJ}}{\text{kmol fuel}}$$

$$= 1560 \frac{\text{MJ}}{\text{kmol fuel}} = 176 \frac{\text{MJ}}{\text{kmol fuel}}$$

$$= 1384 \frac{\text{MJ}}{\text{kmol fuel}}$$