### ME 266 THERMODYNAMICS 1

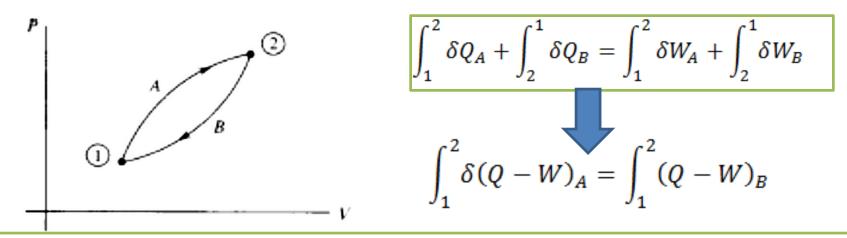
D. A. Quansah

First Law for a Cycle:

$$\sum W = \sum Q \quad \text{or} \quad \oint \delta W = \oint \delta Q$$

- the net heat transfer is equal to the net work done for a system undergoing a cycle.

First Law for a Cycle:



The change in the quantity Q - W from state 1 to state 2 is the same along path A as along path B. Since this change is independent of the path between states 1 and 2 we may write:

$$dQ - dW = dE$$

First Law for a Cycle:

$$dQ - dW = dE$$

The quantity **E** is an extensive property of the system and represents the energy of the system at a particular state. Integration yields:

$$Q_{1-2}-W_{1-2}=E_2-E_1$$

 $Q_{1-2}$  is the heat transferred to the system during the process from state 1 to state 2,  $W_{1-2}$  is the work done by the system on the surroundings during the process, and  $E_2$  and  $E_1$  are the values of the property  $\boldsymbol{E}$ .

The property E represents all of the energy: kinetic energy KE, potential energy PE, and internal energy U.

The first law of then takes the form:

$$Q_{1-2} - W_{1-2} = KE_2 - KE_1 + PE_2 - PE_1 + U_2 - U_1$$
$$= \frac{1}{2}m(V_2^2 - V_1^2) + mg(z_2 - z_1) + U_2 - U_1$$

E is an extensive property with associated intensive property *e*.

### **Enthalpy:**

- In the solution of problems involving systems, certain products or sums of properties occur with regularity.
- One such combination of properties is the Enthalpy, defined as:
- H = U + PV or h = u + Pv on a unit mass basis.
- For a constant-pressure equilibrium process, heat transferred is may be found as:

$$Q_{1-2} = H_2 - H_1$$

#### **SPECIFIC HEAT:**

The heat required to raise the temperature of a unit mass of a substance by 1 °C.

$$Q_{1-2} = \int_1^2 m \, C_n dT$$

where  $C_n$  is the specific heat.

For a constant pressure process:

$$Q_{1-2} = \int_1^2 m \, C_p \, dT$$

For a constant volume process:

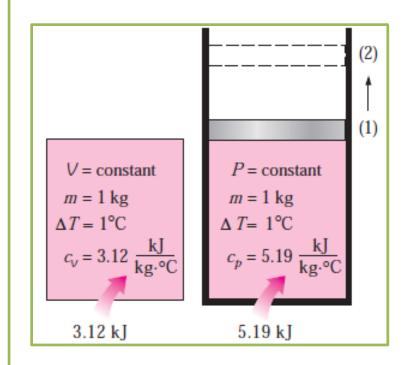
$$Q_{1-2} = \int_1^2 m \, C_v dT$$

# THE FIRST LAW OF THERMODYNAMICS Specific Heats

- Specific Heat: the energy required to raise the temperature of a unit mass of a substance by one degree.
- In general, this energy depends on how the process is executed.
- In thermodynamics, we are interested in two kinds of specific heats:
  - 1. Specific heat at constant volume  $C_{\nu}$
  - 2. Specific heat at constant pressure  $C_p$

# THE FIRST LAW OF THERMODYNAMICS Specific Heats

- Physically, the specific heat at constant volume  $C_v$  can be viewed as the energy required to raise the temperature of the unit mass of a substance by one degree as the volume is maintained constant.
- The energy required to do the same as the pressure is maintained constant is the specific heat at constant pressure  $C_p$ .



# THE FIRST LAW OF THERMODYNAMICS Specific Heats

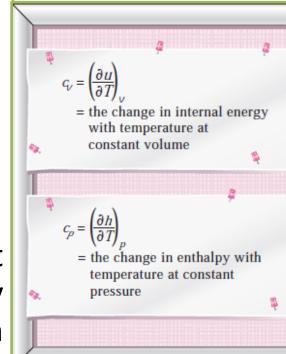
• In a constant-volume process, the amount of energy added may be expressed as:

$$\delta e_{\rm in} - \delta e_{\rm out} = du$$

$$c_v dT = du$$

$$c_{\rm v} = \left(\frac{\partial u}{\partial T}\right)_{\rm v}$$

• an expression for the specific heat at constant pressure  $c_p$  can be obtained by considering a constant-pressure expansion or compression process.  $c_p = \left(\frac{\partial h}{\partial T}\right)_n$ 



• Units:

kJ/kg · °C or kJ/kg · K

kJ/kmol · °C or kJ/kmol · K

Internal Energy, Enthalpy, and Specific Heats of Ideal Gases

Ideal gases by definition obey the equation:

$$Pv = RT$$

 It has been demonstrated (mathematically and experimentally) that for an ideal gas the internal energy is a function of the temperature only. That is:

$$u = u(T)$$

• From the definitions above:  $\begin{vmatrix} h = u + Pv \\ Pv = RT \end{vmatrix}$  h = u + RT

• Since **R** is constant and  $\mathbf{u} = \mathbf{u}(\mathbf{T})$ , it follows that enthalpy is a function of temperature only: h = h(T)

Internal Energy, Enthalpy, and Specific Heats of Ideal Gases

• For ideal gases u, h,  $C_v$ , and  $C_p$  are functions of temperature alone:

$$\Delta u = u_2 - u_1 = \int_1^2 c_v(T) dT \cong c_{v,avg}(T_2 - T_1)$$

$$\Delta h = h_2 - h_1 = \int_1^2 c_p(T) dT \cong c_{p,avg}(T_2 - T_1)$$

• For ideal gases,  $C_v$  and  $C_p$  are related by:

$$c_p = c_v + R$$
 (kJ/kg·K)

 For incompressible substances (liquids and solids), both the constant-pressure and constant-volume specific heats are identical and denoted by c:

$$c_p = c_v = c$$
 (kJ/kg·K)

Ratio of specific heats: 1.667 for monoatomic gases and 1.4 for diatomic gases

#### **Constant-Temperature Process**

$$Q - W = \Delta U$$

• the internal energy depends only on the temperature and thus  $\Delta U = 0$  for an isothermal process; for such a process:

$$Q = W$$

$$W = \int_{V_1}^{V_2} P dV$$

$$= mRT \int_{V_1}^{V_2} \frac{dV}{V} = mRTIn \frac{V_2}{V_1} = mRTIn \frac{P_1}{P_2}$$

$$P_1V_1 = P_2V_2$$

From previous lessons, this should be easy to do. Be careful to use the proper form of R.

### **Constant-Volume Process**

• Since dV is zero, work PdV is zero and the first law becomes:  $Q = \Delta U$ 

For an ideal gas with constant C<sub>v</sub>:

$$Q = mC_v(T_2 - T_1)$$
 or  $q = c_v(T_2 - T_1)$ 

## THE FIRST LAW OF THERMODYNAMICS Constant-Pressure Process

For a constant pressure process:

$$Q = \Delta H$$

$$Q = m \int_{T_1}^{T_2} C_p dT$$

$$Q = mC_p(T_2 - T_1)$$

### **Adiabatic Process**

- For an adiabatic process:
- Q=0
- $-\delta W = du$
- du + Pdv = 0
- For an ideal gas:  $C_v dT + \frac{RT}{r^2} dv = 0$

Reaarrange and integrate between states 1 and 2, assuming constant  $C_v$ 

$$\frac{C_v}{R} In \frac{T_2}{T_1} = -In \frac{v_2}{v_1}$$

this can be put in several forms:

$$\frac{T_2}{T_1} = \left(\frac{v_1}{v_2}\right)^{\frac{k}{C_v}} = \left(\frac{v_1}{v_2}\right)^{k-1} = \left(\frac{P_2}{P_1}\right)^{\frac{k-1}{k}} \quad and \quad \frac{P_2}{P_1} = \left(\frac{v_1}{v_2}\right)^{k}$$

# FIRST LAW APPLIED TO CONTROL VOLUMES Conservation of Mass - Continuity

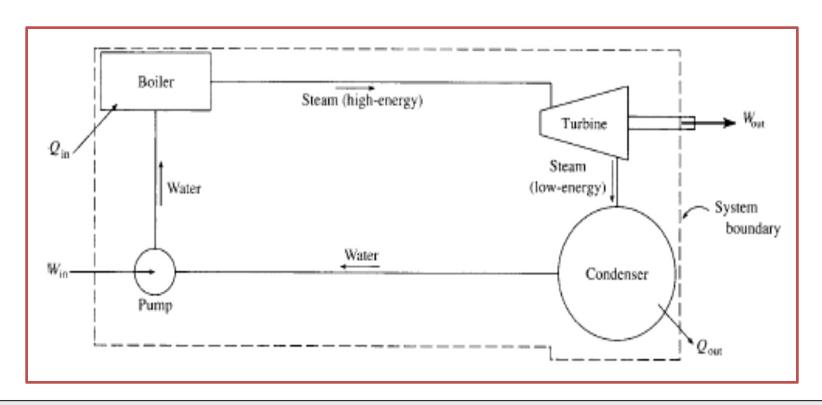
 In a steady flow mode, the amount of mass that enters a control volume can be expressed

as: 
$$\Delta m_1 = volume \times density = area \times length \times density$$
  
=  $area \times (velocity \times time) \times density$   
=  $A_1V_1\Delta t \rho_1$ 

- Similarly, the mass leaving the control volume can be expressed as:  $\Delta m_2 = A_2 V_2 \Delta t \rho_2$
- For steady flow,  $\Delta m_1 = \Delta m_2$  $\rho_1 A_1 V_1 = \rho_2 A_2 V_2$

Also note that Volumetric Flow, Q  $(m^3/s) = A*V$ 

### Schematic of a Power Plant



For an analysis of this system, we must relate  $W_{in}$ ,  $Q_{in}$ ,  $W_{out}$ , and  $Q_{out}$  to the pressure and temperature changes for the pump, boiler, turbine, and condenser, respectively.

 The first law for a steady-state device can be stated as:

$$Q - W = E_{sys}(t + \Delta t) - E_{sys}(t)$$

$$Q - W = \rho_2 A_2 V_2 \Delta t \left( u_2 + \frac{1}{2} V_2^2 + g z_2 \right) - \rho_1 A_1 V_1 \Delta t \left( u_1 + \frac{1}{2} V_1^2 + g z_1 \right)$$

- The work W is composed of two parts:
  - 1. the work, sometimes called **flow work**, due to the pressure needed to move the fluid into and from the device.
  - 2. and the work that results from a shaft that is usually rotating, called shaft work  $W_s$ , that operates inside the device.

$$W = P_2 A_2 V_2 \Delta t - P_1 A_1 V_1 \Delta t + W_s$$

• Substitute the expression for work *W*:

into

$$W = P_2 A_2 V_2 \Delta t - P_1 A_1 V_1 \Delta t + W_s$$

 $Q - W = \rho_2 A_2 V_2 \Delta t \left( u_2 + \frac{1}{2} V_2^2 + g z_2 \right) - \rho_1 A_1 V_1 \Delta t \left( u_1 + \frac{1}{2} V_1^2 + g z_1 \right)$ 

• and express the **flow work** term as  $\rho AV(P/\rho) \Delta t$ . The first law is then arranged as

$$Q - W_s = \rho_2 A_2 V_2 \left( \frac{V_2^2}{2} + g z_2 + u_2 + \frac{P_2}{\rho_2} \right) \Delta t - \rho_1 A_1 V_1 \left( \frac{V_1^2}{2} + g z_1 + u_1 + \frac{P_1}{\rho_1} \right) \Delta t$$

• Dividing through by  $\Delta t$ , we obtain:

$$\dot{Q} - \dot{W_S} = \dot{m} \left( \frac{V_2^2 - V_1^2}{2} + g(z_2 - z_1) + u_2 - u_1 + \frac{P_2}{\rho_2} - \frac{P_1}{\rho_1} \right)$$

• Where:

$$\dot{m} = \dot{m_1} = \dot{m_2}$$

And:

$$\dot{Q}=rac{Q}{\Delta t}$$
 ,  $\dot{W_{S}}=rac{W_{S}}{\Delta t}$  ,  $\dot{m}=
ho AV$ 

 For many devices in Thermodynamics, KE and PE changes are negligible, hence we may

$$\dot{Q} - \dot{W}_s = \dot{m}(h_2 - h_1)$$

$$\dot{Q} - \dot{W}_{\scriptscriptstyle S} = \dot{m}(h_2 - h_1)$$

since 
$$h = u + Pv = u + P/\rho$$

On a unit mass basis:

$$q - w_s = h_2 - h_1$$

For a steady flow with  $\rho_2 = \rho_1 = \rho$ , neglecting heat transfer and changes in internal energy, the energy equation takes the form:

$$\dot{W}_{s} = \dot{m} \left[ \frac{P_{2} - P_{1}}{\rho} + \frac{V_{2}^{2} - V_{1}^{2}}{2} + g(z_{2} - z_{1}) \right]$$

This form of the Energy Equation is useful for the analysis on pumps and hydro turbines.

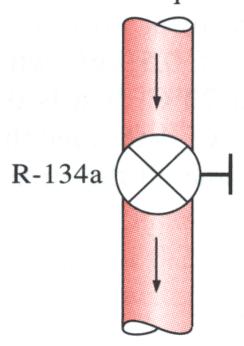
### **Throttling Devices**

A throttling device involves a steady-flow adiabatic process that provides a pressure drop with no significant potential energy changes, kinetic energy changes, heat transfer, or work.

The Energy Equation then becomes:

$$h_2 = h_1$$

 $P_1 = 700 \text{ kPa}$ Sat. liquid



 $P_2 = 160 \text{ kPa}$ 

Throttling valves find major application in refrigeration and air-conditioning

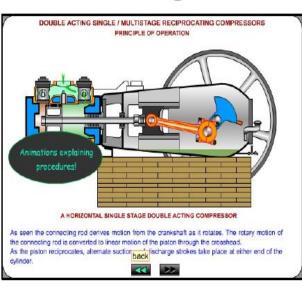
### COMPRESSORS, PUMPS, AND TURBINES

Pump are devices that transfer energy to a liquid (incompressible fluid), result in pressure increase.

A compressor is a machine for raising a gas - a compressible fluid - to a higher level of pressure

A turbine, on the other hand, is a device in which work is done by the fluid on a set of rotating blades.





### COMPRESSORS, PUMPS, AND TURBINES

#### **ANALYSIS**

- ·Heat transfer is usually negligible
- •Kinetic and Potential Energy changes are also usually very small and are often ignored

Therefore at steady-state the energy equation for these devices becomes:

$$-\dot{W}_s = \dot{m}(h_2 - h_1)$$
 or  $-w_s = h_2 - h_1$ 

For liquids, such as water, the energy equation neglecting kinetic and potential energy changes, becomes:

$$-\dot{W}_{s} = \dot{m} \frac{P_2 - P_1}{\rho}$$



Please note the direction of Work done in all these devices

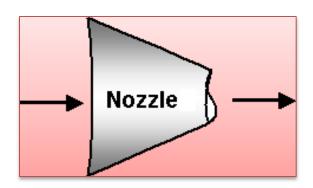
#### **Nozzles and Diffusers**

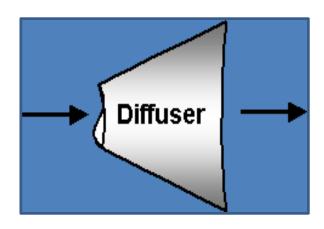
A nozzle is a device that increases the velocity of a fluid at the expense of pressure.

The chief use of nozzle is to produce a jet of steam (or gas) of high velocity to produce thrust for the propulsion of rocket motors and jet engines and to drive steam or gas turbines

A diffuser is a device that slows down a fluid by increasing the pressure.

Diffusers are used in compressors, combustion chambers etc.





#### **Nozzles and Diffusers**

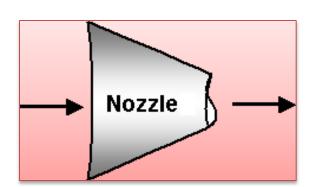
#### **ANALYSIS**

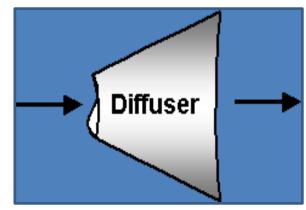
There is no work input and heat transfer is usually negligible.

With additional assumptions of negligible internal energy and potential energy changes, the energy equation takes the form:

$$0 = \frac{V_2^2 - V_1^2}{2} + h_2 - h_1$$

Three equations may be used for nozzle and diffuser flow: energy, continuity, and a process equation, such as for an adiabatic quasi-equilibrium flow





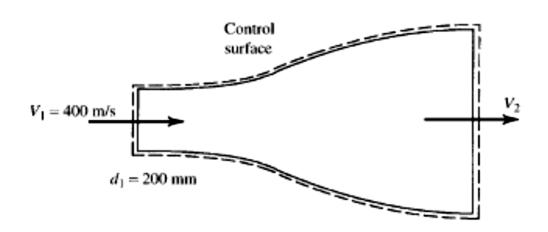
$$\dot{Q} - \dot{W}_s = \dot{m} \left( \frac{V_2^2 - V_1^2}{2} + g(z_2 - z_1) + u_2 - u_1 + \frac{P_2}{\rho_2} - \frac{P_1}{\rho_1} \right)$$

## **Worked Example**

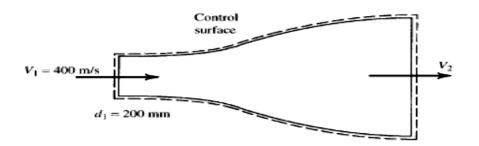
Air flows through the supersonic nozzle shown. The inlet conditions are **7 kPa** and **420 °C**. The nozzle exit diameter is adjusted such that the exiting velocity is **700 m/s**. Calculate (a) the exit temperature,

- (b) the mass flow rate, and
- (c) the exit diameter.

Assume an adiabatic quasi-equilibrium flow.



## Second Law of Thermodynamics



#### **Solution**

(a)To find the exit temperature the energy equation is used. Noting that:  $\Delta h = C_p \Delta T$ 

The energy equation becomes:  $\frac{V_1^2}{2} + C_p T_1 = \frac{V_2^2}{2} + C_p T_2$ 

using  $C_p = 1000 \text{ J/kg.K}$   $T_2 = \frac{V_1^2 - V_2^2}{2C_n} + T_1 = \frac{400^2 - 700^2}{2 \times 1000} + 420 = 255 \text{ °C}$ 

(b) To find the mass flow rate we must find the density at the entrance