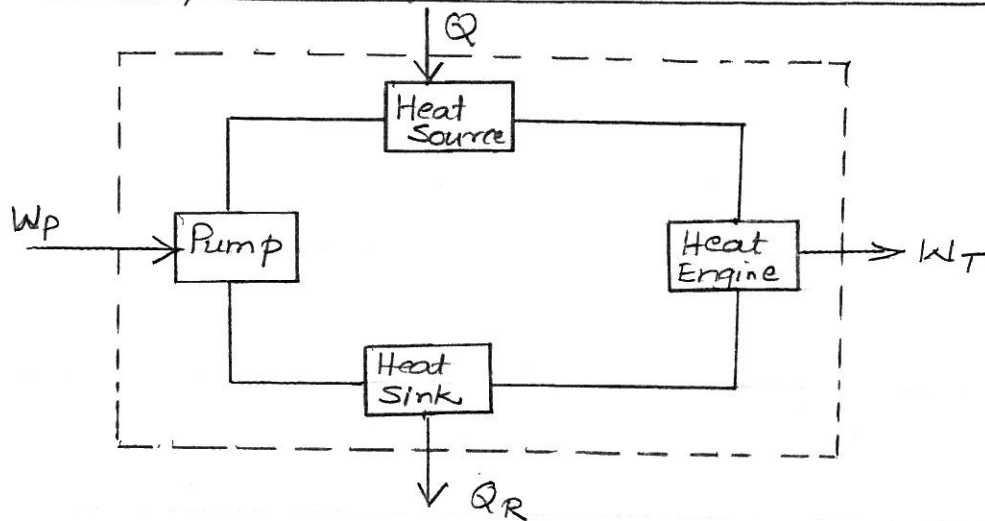


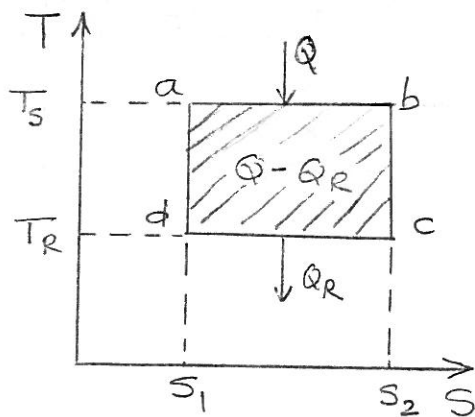
## Thermodynamic Cycles and Their Efficiencies.



• Reactor Power Cycle

$$\begin{aligned} \text{Overall thermal efficiency } \eta &= \frac{\text{Net output Work}}{\text{Input Heat}} = \frac{W_T - W_p}{Q} \\ &= \frac{Q - Q_R}{Q} = 1 - \frac{Q_R}{Q} \end{aligned}$$

### Carnot Cycle :



Efficiency of this cycle abcd

$$\begin{aligned} \eta &= \frac{Q - Q_R}{Q} = \frac{T_s(S_b - S_a) - T_R(S_c - S_d)}{T_s(S_b - S_a)} \\ &= 1 - \frac{T_R}{T_s} \end{aligned}$$

- ① a-b - isothermal heat addition
- ② b-c - isentropic expansion
- ③ c-d - isothermal heat rejection
- ④ d-a isentropic compression

Shaft work of the turbine

$$W_T = h_1 - h_{2s}$$

pumping work  $W_p = h_{4s} - h_3$

$$= \frac{V}{J} (P_1 - P_2)$$

net work per kg of working fluid

$$W_{\text{Net}} = (h_1 - h_{2s}) - (h_{4s} - h_3)$$

$$= (h_1 - h_{2s}) - \frac{V}{J} (P_1 - P_2)$$

Heat input

$$Q = (h_1 - h_{4s}) = (h_1 - h_3) - \frac{V}{J} (P_1 - P_2)$$

Overall thermal efficiency

$$\eta = \frac{W_{\text{Net}}}{Q} = \frac{(h_1 - h_{2s}) - \frac{V}{J} (P_1 - P_2)}{(h_1 - h_3) - \frac{V}{J} (P_1 - P_2)}$$

Actual Ideal Rankine Cycle:

$$\text{pump (compressor)} \quad \eta_p = \frac{h_{4s} - h_3}{h_4 - h_3}$$

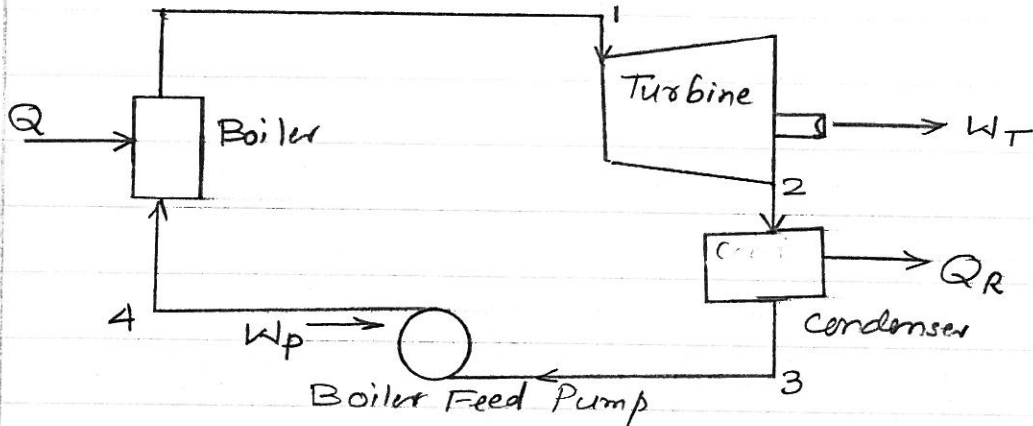
$$\text{turbine (expansion)} \quad \eta_t = \frac{h_1 - h_2}{h_1 - h_{2s}}$$

$$\therefore W_{\text{Net}} = \eta_t (h_1 - h_2) - \frac{V \Delta P}{\eta_p J}$$

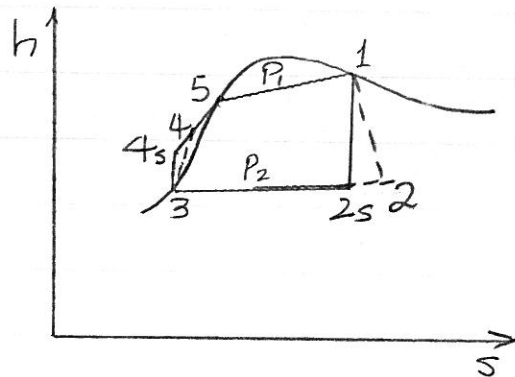
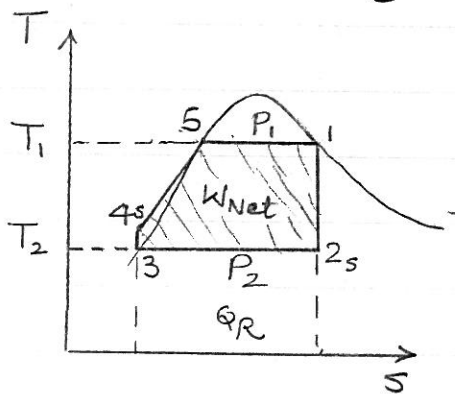
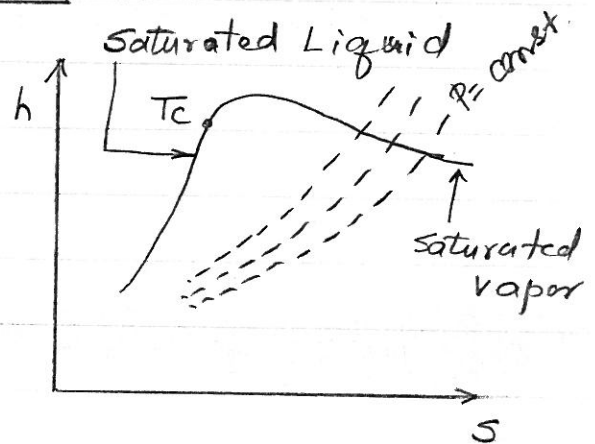
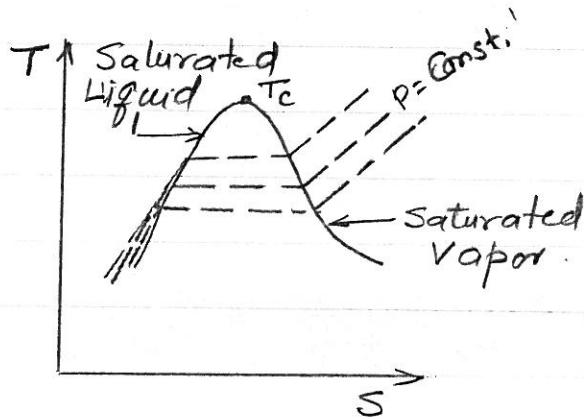
$$Q = (h_1 - h_4) = (h_1 - h_3) - \frac{V \Delta P}{\eta_p J}$$

$$\therefore \eta = \frac{\eta_t (h_1 - h_{2s}) - \frac{V \Delta P}{J \eta_p}}{(h_1 - h_3) - \frac{V \Delta P}{J \eta_p}}$$

## Rankine Cycle (Liquid-vapor cycle)



### Simple Rankine Cycle.



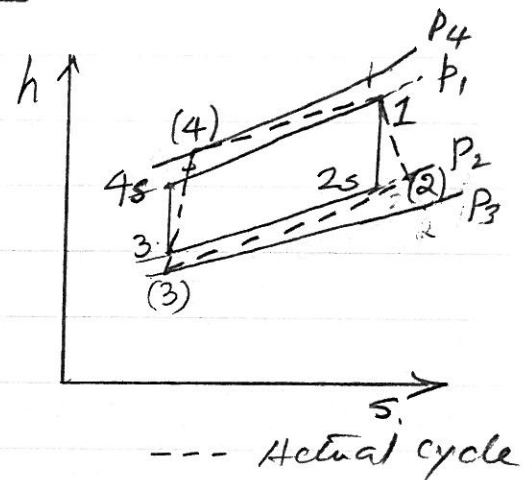
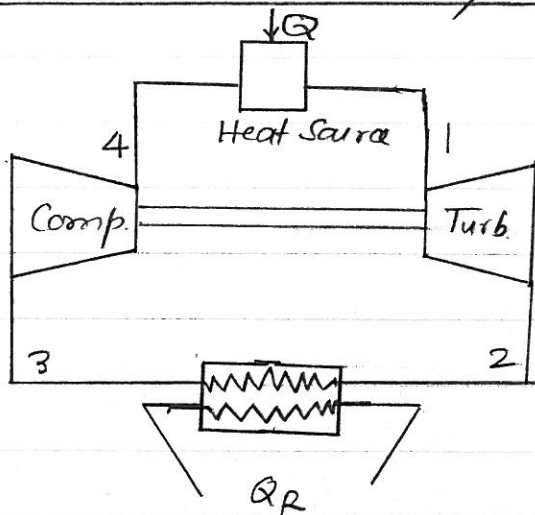
### Ideal Rankine Cycle.

1  $\rightarrow$  2<sub>s</sub> isentropic expansion, 2<sub>s</sub>  $\rightarrow$  3, steam condensation

3  $\rightarrow$  4<sub>s</sub> - isentropic compression  $P_2 \rightarrow P_1$  with pump.  
(boiler pressure)

4<sub>s</sub>  $\rightarrow$  5 - 1 - high pressure liquid emerges as steam ..  
at 1.

## Gas Turbine or Brayton Cycles.



1 → 2s - adiabatic & isentropic expansion. (turbine)

2s - 3 - heat removed at constant p.

3 → 4s - adiabatic & isentropic compression (compressor)

4s → 1 - heated at constant p.

Turbine:  $W_{Ts} = h_1 - h_{2s}$

Comp.  $W_{Cs} = h_{4s} - h_3$

heat added  $Q = h_1 - h_{4s}$

For ideal Brayton Cycle:

$$\eta = \frac{W_{net}}{Q} = \frac{(h_1 - h_{2s}) - (h_{4s} - h_3)}{h_1 - h_{4s}}$$

Actual Brayton Cycle:

compressor efficiency  $\eta_c = \frac{\text{Ideal Work}}{\text{Actual Work}} = \frac{h_{4s} - h_3}{h_4 - h_3}$

turbine efficiency  $\eta_t = \frac{\text{Actual Work}}{\text{Ideal Work}} = \frac{h_1 - h_2}{h_1 - h_{2s}}$

$$\eta = \frac{(h_1 - h_2) - (h_4 - h_3)}{h_1 - h_4} = \frac{\eta_t(h_1 - h_{2s}) - (h_{4s} - h_3)/\eta_c}{h_1 - h_3 - \frac{h_{4s} - h_3}{\eta_c}}$$

## Thermodynamic Analysis of Nuclear Power Plants

Rankine and Brayton Cycles.

Constant pressure heat addition and rejection for steady flow operation.

Thermodynamic efficiency (or effectiveness)  $\eta$   

$$\equiv \frac{\dot{W}_{u, \text{actual}}}{\dot{W}_{u, \text{max}}}$$

$$\dot{W}_{u, \text{max}} = \frac{\partial(U - T_0 S)}{\partial t} + \sum_{i=1}^I \dot{m}_i (h - T_0 s_i) + \left(1 - \frac{T_0}{T_s}\right) \dot{Q}$$

isentropic efficiency  $\eta_s = \left( \frac{\dot{W}_{u, \text{actual}}}{\dot{W}_{u, \text{max}}} \right)_{\dot{Q}=0}$

For adiabatic control volume,  $\eta = \eta_s$ .

$$\dot{W}_{u, \text{max}}|_{\dot{Q}=0} = - \left[ \frac{\partial U}{\partial t} \right]_{\text{cv}} + \sum_{i=1}^I \dot{m}_i h_{is}$$

steady state

$$\dot{W}_{u, \text{max}}|_{\dot{Q}=0} = \sum_{i=1}^I \dot{m}_i h_{is}$$

$$\dot{W}_{u, \text{act}} = \sum_{i=1}^I \dot{m}_i h_i$$

$$\therefore \eta_s = \frac{\sum_{i=1}^I \dot{m}_i h_i}{\sum_{i=1}^I \dot{m}_i h_{is}}$$

Thermal efficiency.

$$\eta_{th} = \frac{\dot{W}_{u, \text{act}}}{\dot{Q}_{in}}$$

Simplified PWR System:

$$\sum_{k=1}^I (\dot{m}h)_{in,k} - \sum_{k=1}^I (\dot{m}h)_{out,k} = \dot{W}_{shaft} - \dot{Q}$$

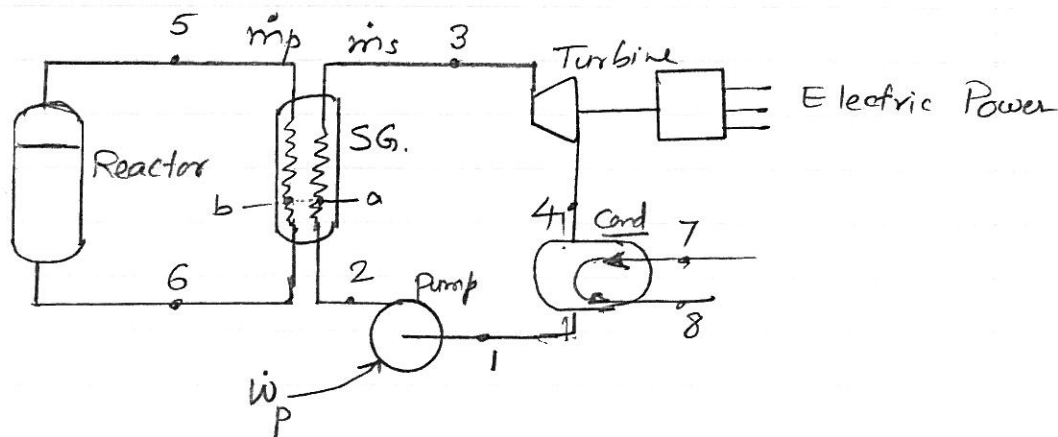
steady state  $\dot{m} = \sum_{k=1}^I \dot{m}_{in,k} = \sum_{k=1}^I \dot{m}_{out,k}$

$$\eta_T = \frac{h_{in} - h_{out}}{h_{in} - h_{out,s}} \quad \text{--- turbine}$$

$$\eta_p = \frac{h_{in} - h_{out,s}}{h_{in} - h_{out}} \quad - \text{pump}$$

$$\frac{m_p}{m_s} = \frac{(h_{out} - h_{in})_s}{(h_{in} - h_{out})_p}$$

p- primary  
s- secondary



$$\frac{\dot{m}_p}{\dot{m}_s} = \frac{h_3 - h_a}{\bar{c}_p [T_5 - (T_a + \Delta T_p)]} = \frac{h_a - h_2}{\bar{c}_p [(T_a + \Delta T_p) - T_6]}$$

$$\begin{aligned} \dot{W}_{u, \text{actual}} &= \dot{W}_T + \dot{W}_p = [\dot{m}_s (h_{in} - h_{out})]_T + [\dot{m}_s (h_{in} - h_{out})]_p \\ &= [\eta_T \dot{m}_s (h_{in} - h_{out, s})]_T + \left[ \frac{\dot{m}_s}{\eta_p} (h_{in} - h_{out, s}) \right]_p \end{aligned}$$

for pump  $h_{in} < h_{out, s}$ ,  $\cup$  for turbine  $h_{in} > h_{out, s}$

$$\begin{aligned} \dot{W}_{u, \text{max}} &= \dot{m}_p (h_{out} - h_{in})_R = \dot{m}_p (h_5 - h_6) \\ &= \dot{m}_p (h_5 - h_6) = \dot{m}_s (h_3 - h_2) \end{aligned}$$

$$\xi = \frac{[\dot{m}_s (h_{in} - h_{out})]_T + [\dot{m}_s (h_{in} - h_{out})]_p}{[\dot{m}_s (h_{out} - h_{in})]_{SGs.}}$$

$$= \frac{h_3 - h_4 + h_1 - h_2}{h_3 - h_2}$$