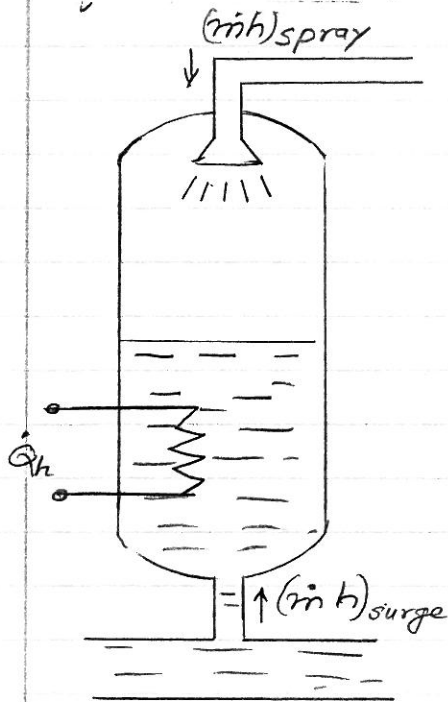


# PRESSURIZER

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Equilibrium Single-Region.

Mass balance:

$$\frac{d}{dt} m = \dot{m}_{surge} + \dot{m}_{spray} \quad (1)$$

Energy balance:

$$\frac{d}{dt} (m u) = \dot{m}_{surge} h_{surge} + \dot{m}_{spray} h_{spray} + \dot{Q}_h - p \frac{d}{dt} (m v) \quad (2)$$

$$m = m_v + m_l$$

$$\dot{m} = \dot{m}_v + \dot{m}_l$$

$$\dot{m}_v = \dot{m}_v v_v + \dot{m}_l v_l$$

$$\frac{d}{dt} (m v) = \frac{d}{dt} (m_v v_v + m_l v_l) = 0 \quad (3)$$

(Constant volume)

Prescribed inputs:  $\dot{m}_{spray}$ ,  $h_{spray}$ ,  $\dot{m}_{surge}$ ,  $h_{surge}$ , &  $\dot{Q}$

Unknown:  $p$ ,  $m_v$ ,  $m_l$ ,  $u_v$ ,  $v_v$ ,  $u_l$ , and  $v_l$

Equation of state:

$$\left. \begin{aligned} u_v &= u_g = f(p) \\ u_l &= u_f = f(p) \\ v_v &= v_g = f(p) \\ v_l &= v_f = f(p) \end{aligned} \right\} \text{Saturation Condition.}$$

Final Pressure:

Initial state:

$$(V_{f1})_{outsurge} \quad (V_{g1})_{insurge}$$

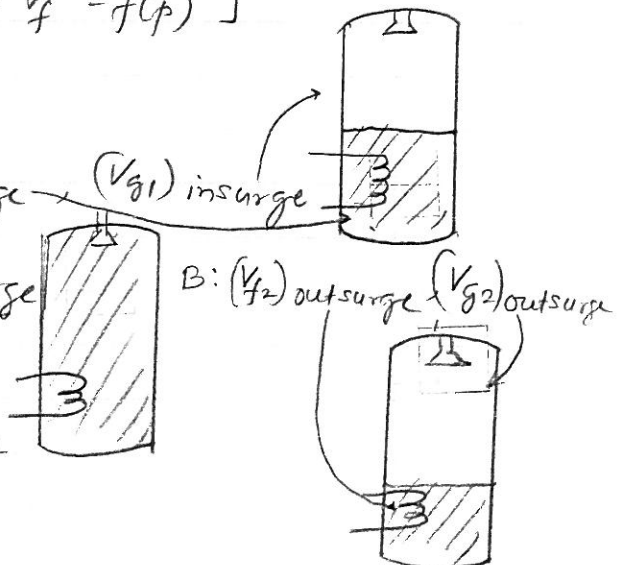
Final state:

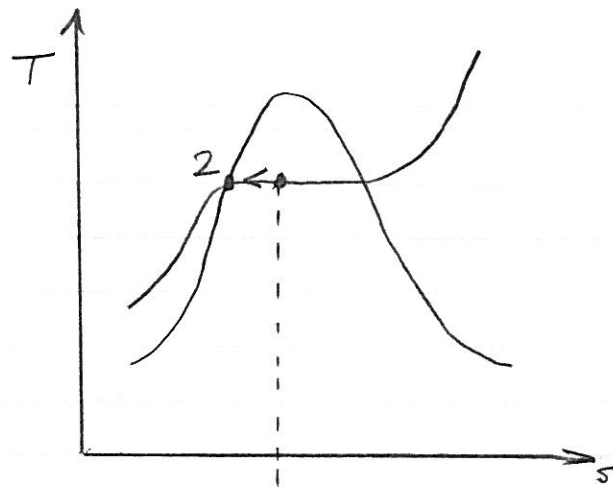
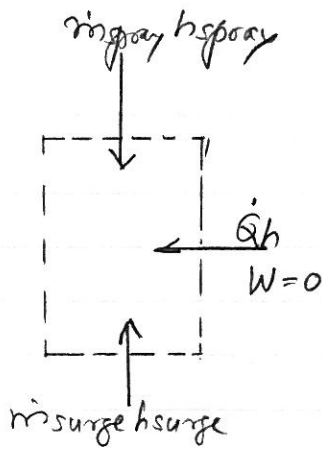
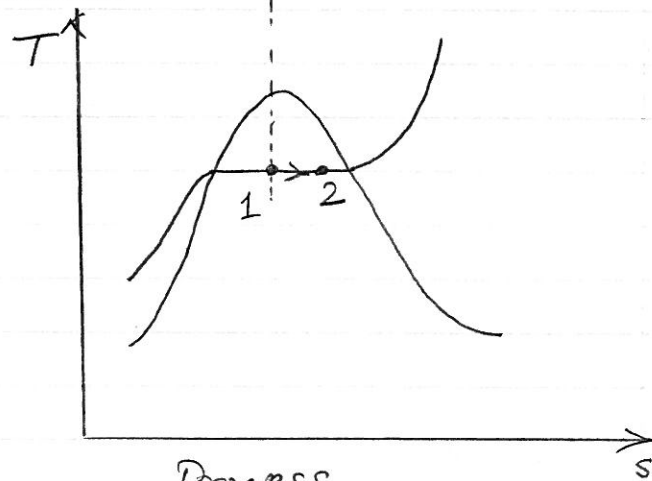
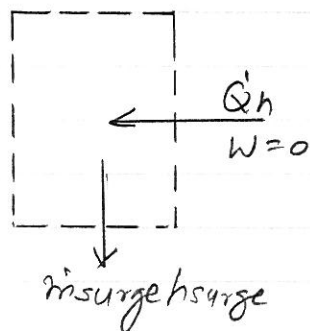
$$A: (V_{f2})_{insurge} \quad B: (V_{f2})_{outsurge} \quad (V_{g2})_{outsurge}$$

$$V_T = (V_{g1})_{insurge} + (V_{f1})_{outsurge}$$

Unknown:  $m_l$ ,  $m_v$ ,  $\dot{Q}$

Inputs:  $\dot{m}_{spray}$ ,  $h_{spray}$ ,  $\dot{m}_{surge}$ ,  $h_{surge}$  &  $p$ .



INSURGEOUTSURGE

Control Volume

Process.

Integrate equations ①-③ between initial (1) and final states (2)

$$m_2 - m_1 = m_{\text{surge}} + m_{\text{spray}}$$

$$m_2 u_2 - m_1 u_1 = m_{\text{surge}} h_{\text{surge}} + m_{\text{spray}} h_{\text{spray}} + Q_h$$

$$m_2 v_2 = m_1 v_1$$

For insurge: final state is saturated water at initial pressure

$$m_{\text{fw}} + m_{\text{f}} + m_{\text{surge}} + m_{\text{spray}} = m_2$$

$$m_{\text{fw}} = m_{\text{surge}} (1 + f) + m_{\text{f}} + m_{\text{spray}} \quad \text{--- ④}$$

$$f m_{\text{surge}} = m_{\text{spray}}$$

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$$m_2 u_2 = m_{\text{surge}} (h_{\text{surge}} + f h_{\text{spray}}) + m_g u_g + m_f u_f + Q_h \quad (5)$$

$$m_2 v_2 = m_g v_g + m_f v_f \quad (6)$$

State (1) & (2) are saturated at same pressure.

from (5) and (6)

$$m_g = \frac{v_f [m_{\text{surge}} (h_{\text{surge}} + f h_{\text{spray}}) + Q_h]}{v_g u_f - v_f u_g} \quad (7)$$

and from (4) and (5)

$$m_g = \frac{f h (1 + f) v_f}{v_g - v_f} \quad (8)$$

From (7) & (8)

$$(Q_h)_{\text{insurge}} = \frac{m_{\text{surge}} (1 + f) [v_g u_f - v_f u_g]}{v_g - v_f} - m_{\text{surge}} (h_{\text{surge}} + f h_{\text{spray}}) \quad \leftarrow$$

$$\text{Steam volume } (V_g)_{\text{insurge}} = m_g v_g \quad \leftarrow$$

For outsurge case,

$$\text{mass balance: } m_2 + m_g - m_1 - m_f = -m_{\text{surge}}$$

energy balance:

$$m_2 u_2 + m_g u_g - m_1 u_1 - m_f u_f = -m_{\text{surge}} h_{\text{surge}} + Q_h$$

$$\text{Volume constraint: } v_2 + m_g v_g = v_1 + m_f v_f$$

$$v_2 = v_1 + \frac{f h v_g}{v_g - v_f} \quad \text{and}$$

$$v_2 = v_1 + \frac{Q_h - m_{\text{surge}} h_{\text{surge}}}{\frac{v_f}{v_g} u_g - u_f}$$

$$(Q_h)_{\text{outsurge}} = m_{\text{surge}} h_{\text{surge}} - \left( u_f - \frac{v_f}{v_g} u_g \right) \left( m_{\text{surge}} \frac{v_g}{v_g - v_f} \right) \quad \leftarrow$$

$$(V_f)_{\text{outsurge}} = m_{f1} v_f$$

total volume:  $V_T = (V_g)_{\text{insurge}} + (V_f)_{\text{outsurge}}$

### Example: Pressurizer Sizing

Determine size of the pressurizer that can accommodate a maximum outsurge of 14,000 kg and hot leg insurge of 9500 kg for the conditions of Table

**Table 7-3 Conditions for pressurizer design problem**

Saturation pressure	15.5 MPa	(2250 psia)
Saturation temperature	618.3°K	(652.9°F)
Saturation properties		
$u_f$	$1.60 \times 10^6 \text{ J/kg}$	(689.9 B/lb)
$u_g$	$2.44 \times 10^6 \text{ J/kg}$	(1050.6 B/lb)
$v_f$	$1.68 \times 10^{-3} \text{ m}^3/\text{kg}$	(0.02698 ft <sup>3</sup> /lb)
$v_g$	$9.81 \times 10^{-3} \text{ m}^3/\text{kg}$	(0.15692 ft <sup>3</sup> /lb)
Mass of maximum outsurge	14,000 kg	
Mass of maximum insurge	9,500 kg	
Hot leg insurge enthalpy	$1.43 \times 10^6 \text{ J/kg}$	(612.8 B/lb)
Cold leg spray enthalpy	$1.27 \times 10^6 \text{ J/kg}$	(546.8 B/lb)
Cold leg spray expressed as a fraction of hot leg insurge (f)	0.03	
Outsurge enthalpy	$1.63 \times 10^6 \text{ J/kg}$	(701.1 B/lb)
Mass of liquid water necessary to cover the heaters (requires an assumption about the pressurizer configuration)	1827 kg	

Solution:

$$(Q_h)_{\text{insurge}} = \frac{m_{\text{insurge}}(1+f)[v_g u_f - v_f u_g]}{v_g - v_f} = 1.06 \times 10^7 \text{ J}$$

$$m_{g1} = \frac{m_{\text{insurge}}(1+f)v_f}{v_g - v_f} = 2022 \text{ kg}$$

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$$(V_{g1})_{in surge} = m_{g1} v_{g1} = 19.24 \text{ m}^3$$

$$\begin{aligned} (Q_h)_{out surge} &= m_{surge} h_{surge} - \left(u_f - \frac{v_f}{v_g} u_g\right) \left(m_{surge} \frac{v_g}{v_g - v_f}\right) \\ &= 2.851 \times 10^9 \text{ J} \end{aligned}$$

$$m_{f1} = m_{f2} + m_{surge} \frac{v_g}{v_g - v_f} = 1.872 \times 10^4 \text{ kg}$$

$$(V_{f1})_{out surge} = m_{f1} v_{f1} = 31.45 \text{ m}^3$$

$$\text{Total volume} = V_T = (V_{g1})_{in surge} + (V_{f1})_{out surge} = 51.29 \text{ m}^3$$

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