

Lab 10: Shell and Tube Heat Exchanger

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1. Figure and Tables

Table 1a. Table presenting the hot-side and cold-side mass flow rate \dot{m} , temperature difference ΔT , overall heat transfer coefficient U, heat transfer rate q, and heat transfer rate percent difference Δq .

	Flow Rate (kg/s)				Temperature (°C)		U_i	Heat Transfer Rate (W)		
Case	\dot{m}_c		\dot{m}_h		ΔT_h	ΔT_c	(W/K m ²)	q_c	q_h	Δq (%)
1a	0.239	(fast)	0.287	(fast)	5.17	6.78		6793.75	6201.73	9.11
1b	0.233	(fast)	0.187	(slow)	7.00	6.78		6615.48	5479.95	18.78
2a	0.201	(slow)	0.325	(fast)	4.00	7.17		6049.23	5426.81	10.85
2b	0.214	(slow)	0.187	(slow)	6.89	7.00		6278.57	5392.23	15.19
							*			

Table 1b. Table presenting the hot-side and cold-side mass flow rate \dot{m} , heat capacity ratio C_r , number of transfer units NTU, and measured, theoretical, and percent difference of effectiveness ε

Case	Flow Rate (kg/s)				Cr	NTU	e		
Case	\dot{m}_c		\dot{m}_h		Cr	NIC	measured	theory	delta_e
1a	0.239	(fast)	0.287	(fast)	0.84	0.086	0.18	0.08	122.78
1b	0.233	(fast)	0.187	(slow)	0.80	0.111	0.20	0.10	94.95
2a	0.201	(slow)	0.325	(fast)	0.62	0.103	0.19	0.09	95.67
2b	0.214	(slow)	0.187	(slow)	0.87	0.111	0.19	0.10	89.85

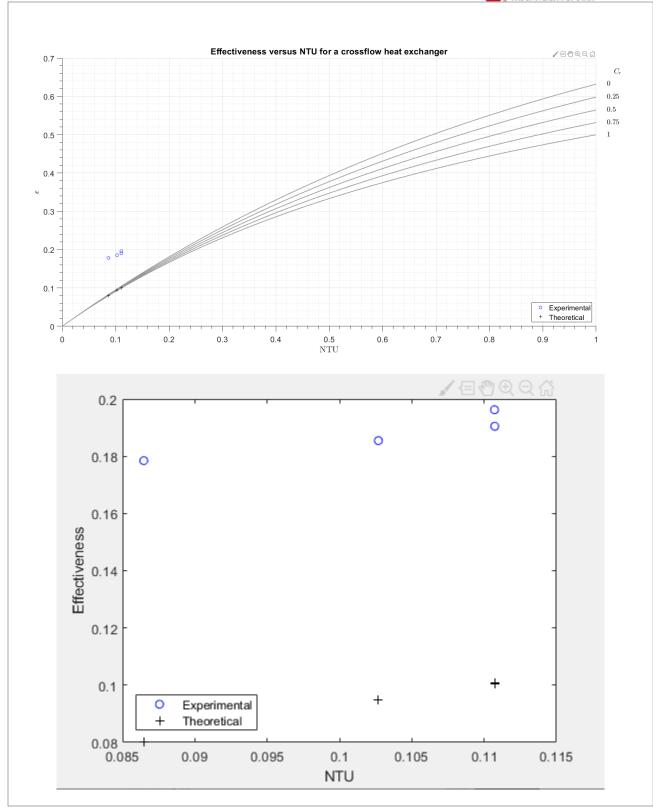


Figure 1c. Plot of the effectiveness ε versus number of transfer units NTU



2. Short Answer Questions

a) Theoretically, we expect qh = qc. However, your measurements will not likely support this. In your analysis, you calculated the percent relative difference, Δq , between qc and qh. State the range of Δq calculated from your measurements. In addition, state the range of percent relative uncertainty in the calculated heat transfer rates: $(\sigma qc/qc) \cdot 100\%$ and $(\sigma qh/qh) \cdot 100\%$. State the extent to which the uncertainty in the measurements helps explain the observed difference between qc and qh? [3–4 sentences]

The range of Δq calculated is from 9.11-18.78%. The range of percent relative uncertainty in the calculated heat transfer rates is 3.84-6.67% and 5.26-6.25% for the hot and cold sides respectively. The uncertainties stated only explain the observed difference between qc and qh to the extent of thermocouple uncertainties and water level reading uncertainties. The uncertainties do not cover fouling or other human errors.

b) State the percent difference in effectiveness values obtained from the measurements compared to theory ($\Delta \varepsilon$ in %). Based on your engineering judgment, does the theory adequately describe the observations? For example, is it possible to use the theory to predict the effectiveness of the present heat exchanger for the following case: mc = 0.3 kg/s and mh = 0.4 kg/s? If yes, explain how. If no, explain why not. [3–5 sentences]

The percent difference of effectiveness values obtained from the measurements are shown in the table below.

delta_e
122.78
94.95
95.67
89.85

In this case, the theory does not adequately describe the observations due to a miscalculation in the code. Since the theory is invalid, it is not possible to use the theory to predict the effectiveness of the present heat exchanger.



c) Estimate the rate of heat transfer from the shell casing to the surroundings due to natural convection (qconv) and radiation (qrad). State the qconv and qrad values in W averaged over all four test cases. Based on your engineering judgment, are these losses important and would you recommend insulating/covering the shell casing to mitigate these losses? Explain why or why not. [3–4 sentences] *Note, be sure to include your calculations for qconv and qrad in your computer code.

```
qconv =
    2.4888    2.6002    2.6502    2.6595
qrad =
    3.1984    3.3502    3.4168    3.4267
```

These values are in Watts. Since they are very small, these losses are not important. Insulation/covering of the shell would not be necessary in this case because of the small values.