

Levelset-mixing of Navier-Stokes equations with Boussinesq: Incompressible multiphase flow

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November 4, 2014

1 Introduction

This report addresses the volume force added by the Boussinesq approximation to the incompressible Navier Stokes equations when we solve a multiphase flow. Such flow is characterized by the presence of at least two immiscible fluids.

The same situation is encountered when treating for instance the SMACS benchmark case before the onset of solidification, where we have two distinct fluids: air and liquid metal. The flow at this stage is driven by thermal convection using side exchangers: one is cooler than the liquid metal, while the other is hotter. Since for now solidification is not accounted for, there will no mention of the Darcy interfacial terms. They will be discussed later.

2 Monophase flow: momentum conservation

In the case of a single phase fluid flow, the incompressible Navier Stokes equations, with the only external volume force applied to the fluid being its body weight, are written as:

$$\rho \left(\frac{\partial \vec{v}}{\partial t} + (\nabla \vec{v}) \vec{v} \right) = \vec{\nabla} \cdot \sigma + \rho \vec{g} \quad (1)$$

$$\nabla \cdot \vec{v} = 0 \quad (2)$$

where ρ , v , σ and \vec{g} are respectively the fluid's density, fluid's velocity, stress tensor and the gravity vector. Now, suppose that density is subject to thermal variations, then the Boussinesq holds a good approximation if these variations remain small (order of magnitude given later). The approximation is introduced by a temperature-dependent density, $\tilde{\rho}$, in the weight force:

$$\tilde{\rho} = \rho_0 (1 - \beta_T (T - T_{\text{ref}})) \quad (3)$$

while the inertial term is kept at reference density $\rho_0 = \tilde{\rho}(T_{\text{ref}})$. This is acceptable as long as the coefficient β_T satisfies the relation $\beta_T (T - T_{\text{ref}}) \ll 1$.

the only reference that states this fact is FLUENT's reference guide. I should search for more formal sources

In these conditions, (1) is written with the variable force term:

$$\rho_0 \left(\frac{\partial \vec{v}}{\partial t} + (\nabla \vec{v}) \vec{v} \right) = \vec{\nabla} \cdot \sigma + \tilde{\rho} \vec{g} \quad (4)$$

$$\nabla \cdot \vec{v} = 0 \quad (5)$$

3 Multiphase flow: momentum conservation

The monolithic Eulerian approaches are very interesting in the computational fluid field as they rely on a fixed mesh where all fluids are treated as a single one. This fluid's thermophysical and mechanical properties are obtained by a mixture of those fluids properties. The level set is one of the most suited approaches for multiphase flows.

3.1 Levelset formulation

Introducing the levelset function α (signed distance function) helps tracking implicitly the interface between two fluids, F_1 and F_2 . The distance between any point in space, x , and the interface, Γ , also denoted $d_\Gamma(x)$, is used to track the interface as follows:

$$\alpha(x) = \begin{cases} d_\Gamma(x) & \text{if } x \in F_1 \\ -d_\Gamma(x) & \text{if } x \in F_2 \\ 0 & \text{if } x \in \Gamma_{F_1, F_2} \end{cases} \quad (6)$$

However, the previous function gives only the distance information, thus useless to mix the fluids properties. The solution is to process the levelset to extract a presence function or the *Heaviside* function, for each fluid. In the literature, many definitions exist, depending on the function's steepness, continuity or differentiability. In our case, we consider the smoothed Heaviside based on a sinusoidal function, given by:

$$H(\alpha(x)) = \begin{cases} 1 & \text{if } \alpha(x) < -\epsilon \\ 0 & \text{if } \alpha(x) > \epsilon \\ \frac{1}{2} \left(1 + \frac{\alpha(x)}{\epsilon} + \frac{1}{\epsilon} \sin\left(\frac{\pi\alpha(x)}{\epsilon}\right) \right) & \text{if } -\epsilon \leq \alpha(x) \leq \epsilon \end{cases} \quad (7)$$

where the interval $[-\epsilon; \epsilon]$ is an artificial interface thickness around the zero distance. The advantage of a sinusoidal-based Heaviside is that it's continuously differentiable in $[-\epsilon; \epsilon]$. It is clear from the definition above, that the sum of the Heaviside functions for all the fluids is equal to 1 in any point of the mesh. Bearing in mind that $H^{F_2} = 1 - H^{F_1}$, the properties ψ^{F_1} and ψ^{F_2} are mixed using the Heaviside functions of both fluids:

$$\hat{\psi} = H^{F_1} \psi^{F_1} + H^{F_2} \psi^{F_2} \quad (8)$$

3.2 Mixed Navier Stokes equations

In the case of 2 incompressible fluids, the Navier Stokes system writes:

$$\hat{\rho} \left(\frac{\partial \vec{v}}{\partial t} + (\underline{\nabla} \vec{v}) \vec{v} \right) = \underline{\nabla} \cdot \hat{\sigma} + \hat{\rho} \vec{g} \quad (9)$$

$$\underline{\nabla} \cdot \vec{v} = 0 \quad (10)$$

where the density and the stress tensor are mixed using the Heaviside defined in the previous section. Assuming that both fluids densities may vary with temperature, the momentum conservation equation (9) can be written with the Boussinesq approximation:

$$\hat{\rho}_0 \left(\frac{\partial \vec{v}}{\partial t} + (\underline{\nabla} \vec{v}) \vec{v} \right) = \underline{\nabla} \cdot \hat{\sigma} + \hat{\rho} \vec{g} \quad (11)$$

$$\underline{\nabla} \cdot \vec{v} = 0 \quad (12)$$

The term $\widehat{\rho}$ represents a mixture of two densities, each of which may vary with temperature independently from the other, as follows:

$$\widehat{\rho} = H^{F_1} \widetilde{\rho}^{F_1} + H^{F_2} \widetilde{\rho}^{F_2} \quad (13)$$

$$= H^{F_1} \rho_0^{F_1} \theta^{F_1} + H^{F_2} \rho_0^{F_2} \theta^{F_2} \quad (14)$$

$$= H^{F_1} \rho_0^{F_1} \left(1 - \beta_T^{F_1} (T - T_{\text{ref}}^{F_1})\right) + H^{F_2} \rho_0^{F_2} \left(1 - \beta_T^{F_2} (T - T_{\text{ref}}^{F_2})\right) \quad (15)$$

Cimlib Implementation

The previous set of incompressible momentum equations with boussinesq approximation mixed with a level set for two fluids is solved using the NavierStokesVMS solver in CimLib. Apart from the classic input parameters that are passed to the solver (e.g. time step, initial and boundary conditions ...), the latter takes also the mixed reference density, $\widehat{\rho}_0$, the mixed viscosity, $\widehat{\mu}$, and the gravity vector, \vec{g} . The weight force is automatically computed inside the solver by P1-P1 multiplication of the inertial density and the gravity vector. The user should consequently multiply the mixed Boussinesq coefficient θ by \vec{g} in a way to form the final volume force: $\widehat{\rho}_0 \widehat{\theta} \vec{g}$. However, in the current context, this term is wrong, as it infers a redundancy in the Heaviside multiplication:

$$\widehat{\rho} \vec{g} = \widehat{\rho}_0 \widehat{\theta} \vec{g} \quad (16)$$

$$= \left(H^{F_1} \rho_0^{F_1} + H^{F_2} \rho_0^{F_2} \right) \left(H^{F_1} \theta^{F_1} + H^{F_2} \theta^{F_2} \right) \vec{g} \quad (17)$$

The correct handling of the Boussinesq force in a monolithic approach is given by:

$$\widehat{\rho} \vec{g} = \widehat{\rho}_0 \widehat{\theta} \vec{g} \quad (18)$$

$$= \left(H^{F_1} \theta^{F_1} \rho_0^{F_1} + H^{F_2} \theta^{F_2} \rho_0^{F_2} \right) \vec{g} \quad (19)$$