

# Computer Graphics I

## Lecture 20: Computer animation 4

**Xiaopei LIU**

School of Information Science and Technology  
ShanghaiTech University

# What is a fluid?

- **Definition**

- A substance that continually deforms (flows) under an applied stress



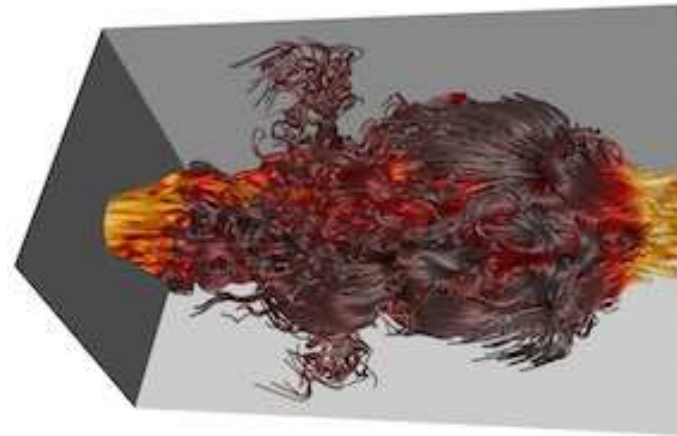
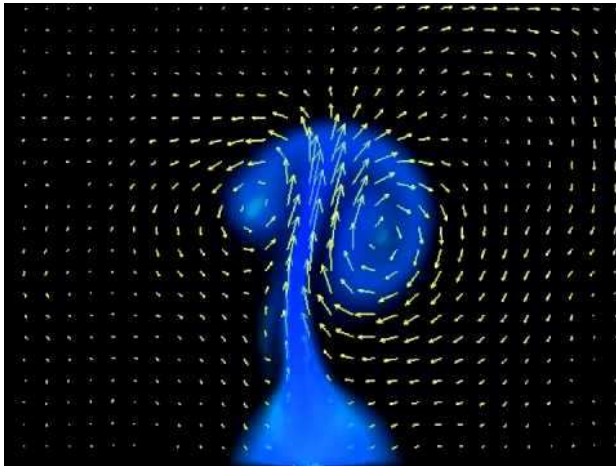
# Fluid simulation

- **Simulate the behavior of fluid flows**
  - Modeling the fluid behavior
  - Solve the fluid equations numerically
  - Rendering the simulation result



# Physical quantities

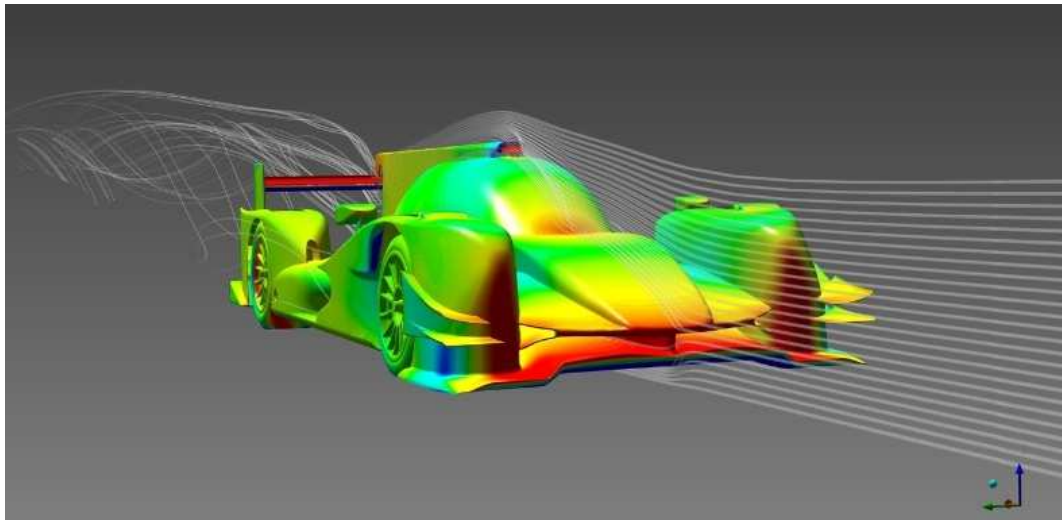
- **Velocity field  $u$** 
  - A spatially and temporally varying vector field of velocity



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# Physical quantities

- Likewise
  - Pressure field  $p$ 
    - A scalar field of pressure
  - Density field  $\rho$ 
    - A scalar field of density
  - Temperature field  $T$ 
    - A scalar field of temperature

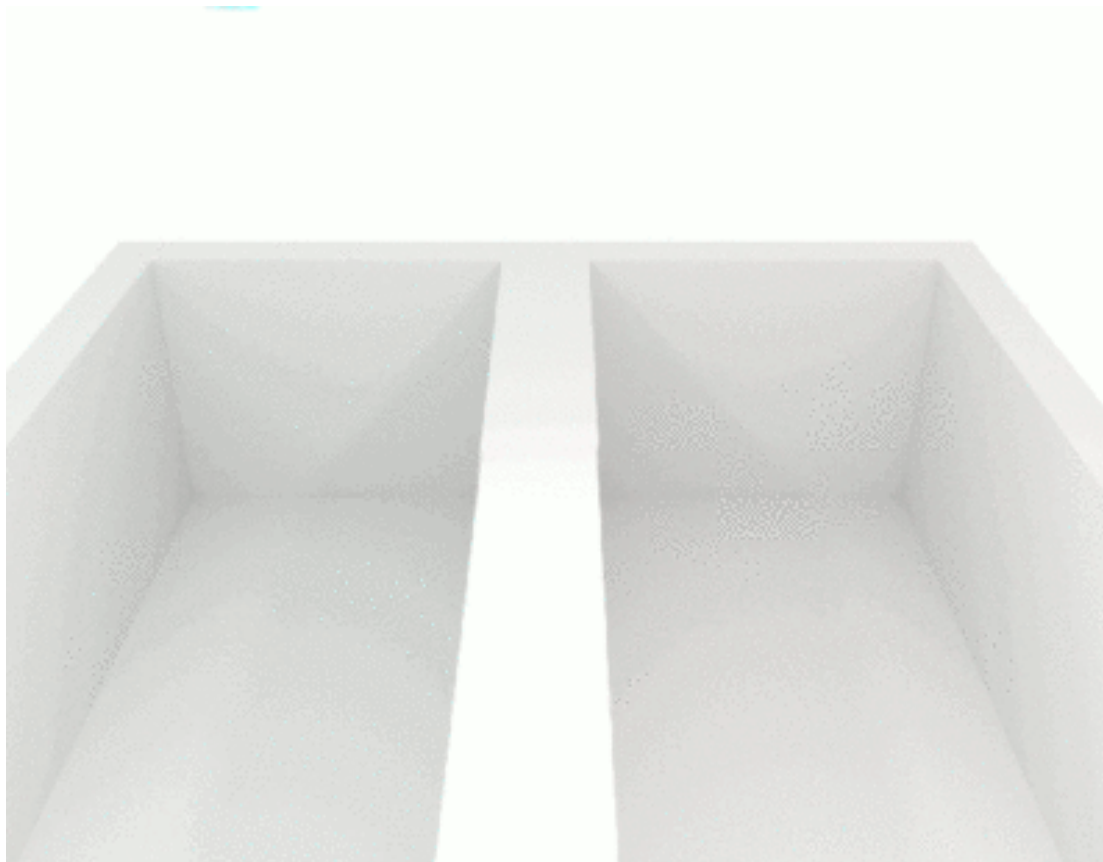


Pressure field on a car surface



# Physical quantities

- **Viscosity  $\nu$** 
  - A measure of its resistance to gradual deformation
  - Small viscosity implies easier (large) deformation



# Divergence

- The divergence represents the volume density of the outward flux of a vector field from an infinitesimal volume

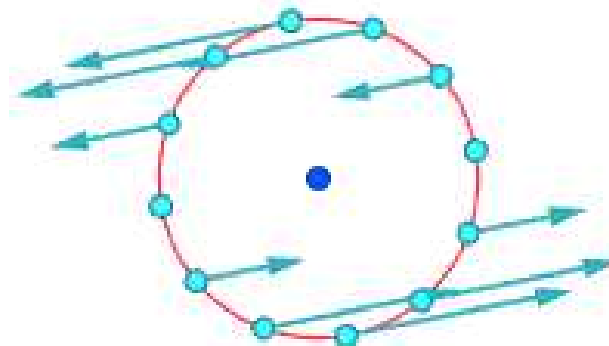
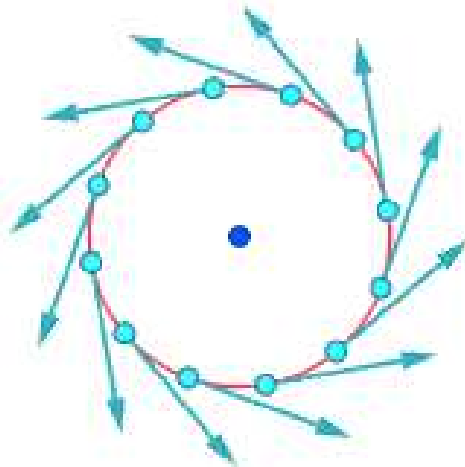
$$\operatorname{div} \mathbf{F}|_p = \lim_{V \rightarrow \{p\}} \iint_{S(V)} \frac{\mathbf{F} \cdot \hat{\mathbf{n}}}{|V|} dS$$

$$\operatorname{div} \mathbf{F} = \nabla \cdot \mathbf{F} = \left( \frac{\partial}{\partial x}, \frac{\partial}{\partial y}, \frac{\partial}{\partial z} \right) \cdot (U, V, W) = \frac{\partial U}{\partial x} + \frac{\partial V}{\partial y} + \frac{\partial W}{\partial z}.$$

# Vorticity

- Describes the local spinning motion

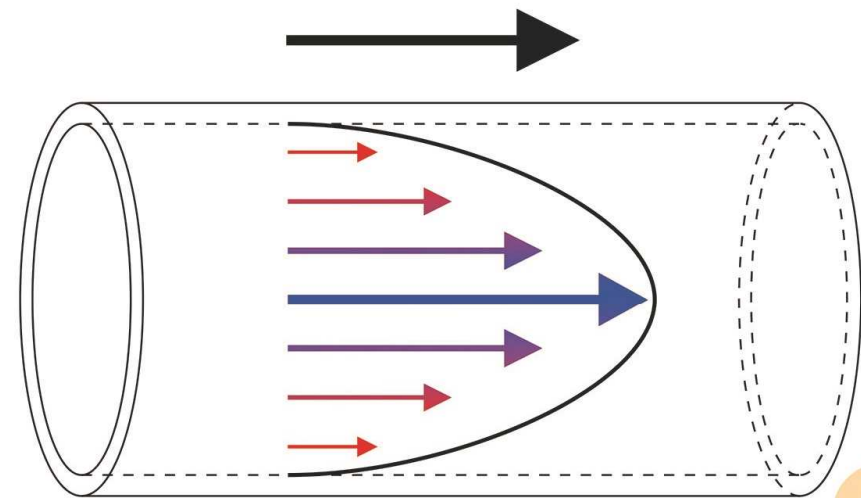
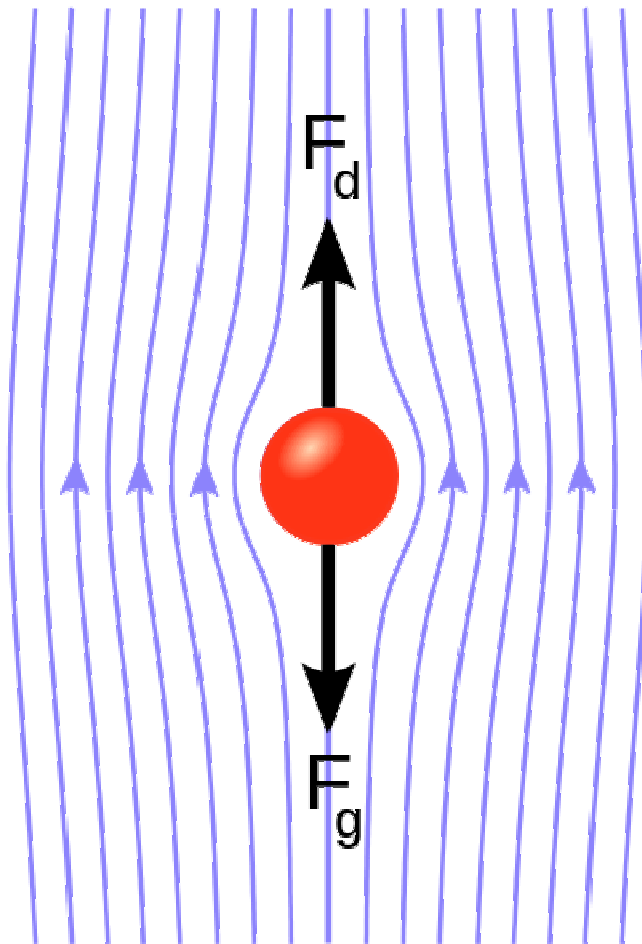
$$\begin{aligned}\vec{\omega} &= \nabla \times \vec{v} = \left( \frac{\partial}{\partial x}, \frac{\partial}{\partial y}, \frac{\partial}{\partial z} \right) \times (v_x, v_y, v_z) \\ &= \left( \frac{\partial v_z}{\partial y} - \frac{\partial v_y}{\partial z}, \frac{\partial v_x}{\partial z} - \frac{\partial v_z}{\partial x}, \frac{\partial v_y}{\partial x} - \frac{\partial v_x}{\partial y} \right)\end{aligned}$$





# Laminar flow

- **When a fluid flows in parallel layers**
  - No disruption between the layers

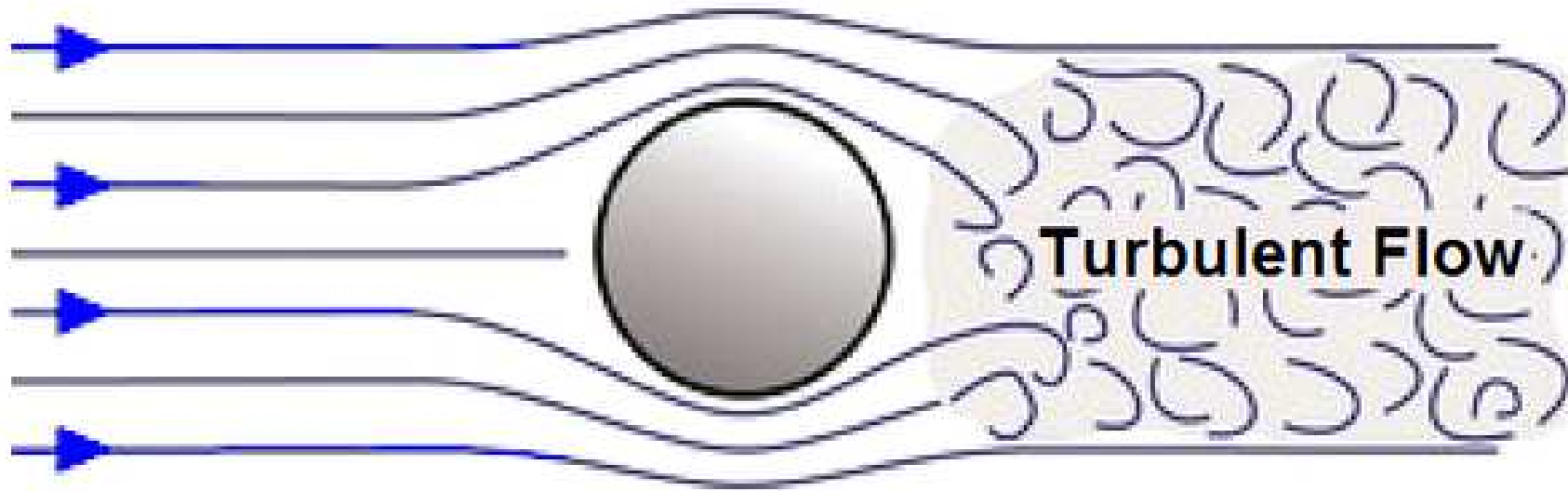


**Laminar flow**



# Turbulence flow

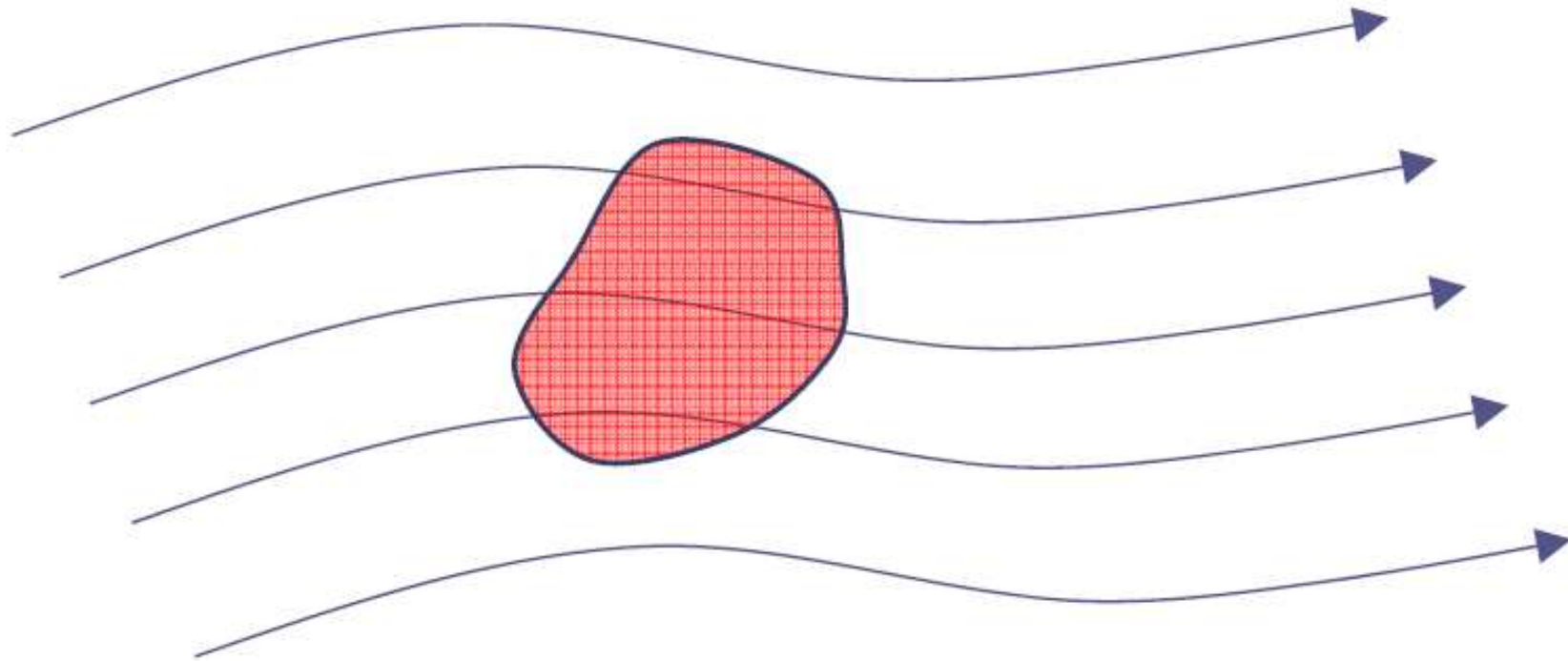
- A flow in chaotic behavior



# **1. Modeling for Fluids**

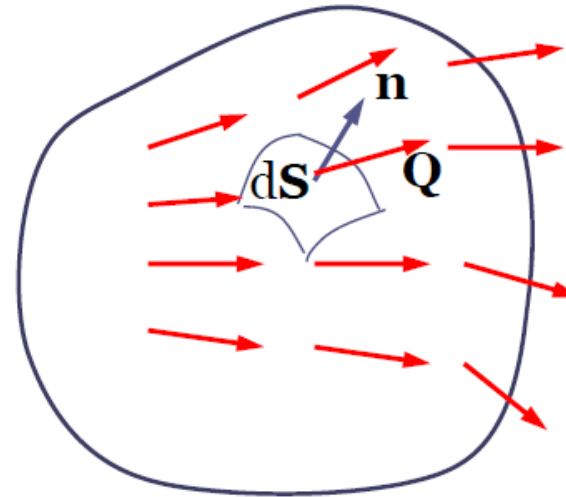
# Control volume

- An enclosed volume with arbitrary shape

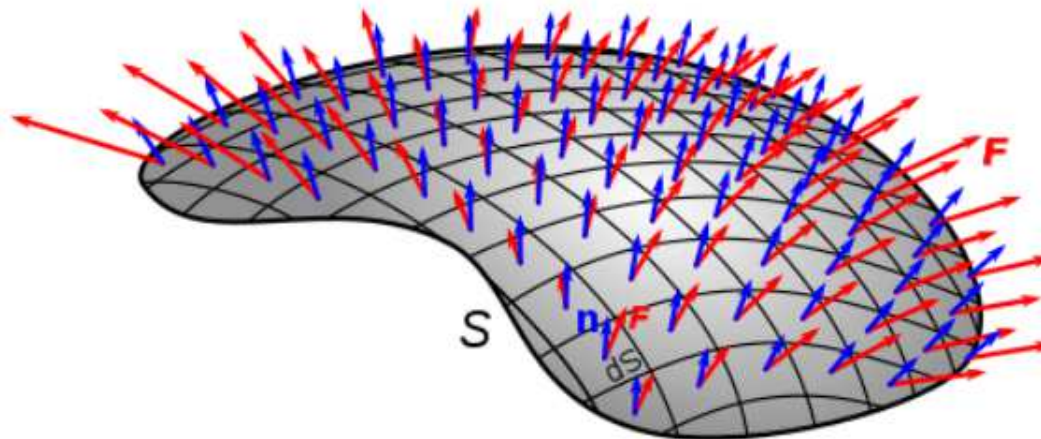


# Flux

- Any effect that passes through a surface or substance



$$\phi = \oint_S \mathbf{Q} \cdot d\mathbf{s}$$



# Fluid dynamics

- **Conservation laws**
  - **Conservation of mass**
    - The rate of change of mass = mass flux rate
  - **Conservation of momentum**
    - The rate of change of momentum = internal + external force

# Conservation of mass

- **Continuity equation**

- Integral form

$$\frac{\partial}{\partial t} \oint_V \rho dV = - \oint_s \rho \mathbf{u} \cdot d\mathbf{s}$$

- Differential form

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{u}) = 0$$



# Conservation of momentum

- **Momentum equation**

- Apply Newton's second law
- Integral form

$$\frac{\partial}{\partial t} \oint_V \rho \mathbf{u} dV + \oint_s (\rho \mathbf{u} \cdot d\mathbf{s}) \mathbf{u} = - \oint_s p d\mathbf{s} + \oint_s \boldsymbol{\tau}_{shear} \cdot d\mathbf{s} + \oint_V \rho \mathbf{g} dV$$

- Differential form

$$\frac{\partial \rho \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla (\rho \mathbf{u}) = -\nabla p + \nabla \cdot \boldsymbol{\tau}_{shear} + \rho \mathbf{g}$$

# Governing equations

- Integral form

$$\frac{\partial}{\partial t} \oint_V \rho dV = - \oint_s \rho \mathbf{u} \cdot d\mathbf{s}$$

$$\frac{\partial}{\partial t} \oint_V \rho \mathbf{u} dV + \oint_s (\rho \mathbf{u} \cdot d\mathbf{s}) \mathbf{u} = - \oint_s p d\mathbf{s} + \oint_s \boldsymbol{\tau}_{shear} \cdot d\mathbf{s} + \oint_V \rho \mathbf{g} dV$$

# Governing equations

- Differential form

$$\frac{\partial \rho}{\partial t} + \nabla \cdot (\rho \mathbf{u}) = 0$$

$$\frac{\partial \rho \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla (\rho \mathbf{u}) = -\nabla p + \nabla \cdot \boldsymbol{\tau}_{shear} + \rho \mathbf{g}$$

# Incompressible fluids

- **The volume and density do not change**
  - Differential form (constant density)

$$\nabla \cdot \mathbf{u} = 0$$

$$\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} = -\frac{1}{\rho} \nabla p + \frac{1}{\rho} \nabla \cdot \boldsymbol{\tau}_{shear} + \mathbf{g}$$

# Newtonian fluids

- Linear shear-stress relation

$$\boldsymbol{\tau}_{shear} = -\nu' \rho (\nabla \cdot \mathbf{u}) \mathbf{I} + 2\rho \nu \mathbf{S}$$

- Strain rate (deformation rate)

$$\mathbf{S} = \frac{1}{2} \left( \nabla \mathbf{u} + (\nabla \mathbf{u})^T \right)$$

# Incompressible Navier-Stokes equations

- Apply Newtonian fluid relation in incompressible governing equations

$$\nabla \cdot \mathbf{u} = 0$$

$$\frac{\partial \mathbf{u}}{\partial t} + \mathbf{u} \cdot \nabla \mathbf{u} = -\frac{1}{\rho} \nabla p + \nu \nabla^2 \mathbf{u} + \mathbf{g}$$

# Incompressible Navier-Stokes equations

- **Fluid equations in computer graphics**
  - Navier-Stokes equations in isothermal case

$$\frac{\partial \vec{u}}{\partial t} + \vec{u} \cdot \nabla \vec{u} + \frac{1}{\rho} \nabla p = \vec{g} + \nu \nabla \cdot \nabla \vec{u}$$
$$\nabla \cdot \vec{u} = 0$$

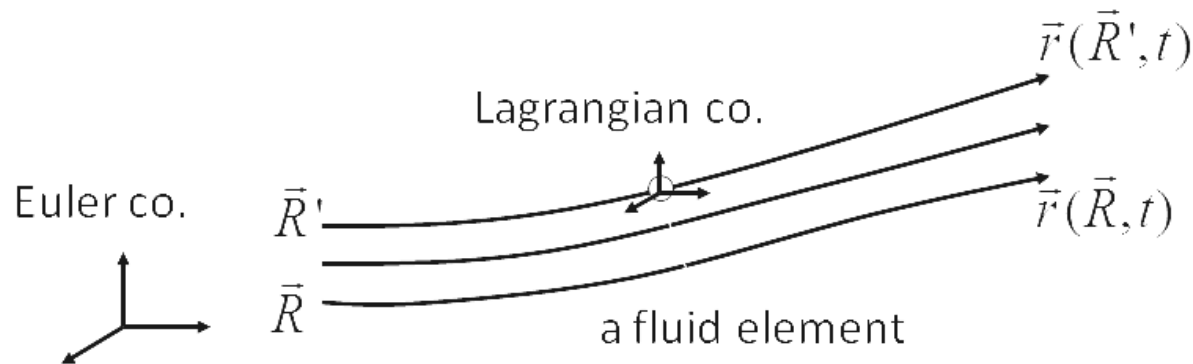
Incompressibility constraint





# Governing equations

- **Lagrangian view**
  - Coordinate is moving with fluid



$$\frac{\partial \vec{u}}{\partial t} + \vec{u} \cdot \nabla \vec{u} + \frac{1}{\rho} \nabla p = \vec{g} + \nu \nabla \cdot \nabla \vec{u}$$



$$\frac{D\vec{u}}{Dt} + \frac{1}{\rho} \nabla p = \vec{g} + \nu \nabla \cdot \nabla \vec{u}$$

# Governing equations

- **Pressure equation**

- Taking divergence of the momentum equation

$$\nabla \cdot \frac{\partial \vec{u}}{\partial t} + \nabla \cdot (\vec{u} \cdot \nabla \vec{u}) + \nabla \cdot \frac{1}{\rho} \nabla p = \nabla \cdot (\vec{g} + \nu \nabla \cdot \nabla \vec{u})$$

- Remove zero terms

$$\nabla \cdot \vec{u} = 0 \quad \longrightarrow \quad \nabla \cdot \frac{1}{\rho} \nabla p = \nabla \cdot (-\vec{u} \cdot \nabla \vec{u} + \vec{g} + \nu \nabla \cdot \nabla \vec{u})$$

# Governing equations

- **Ideal inviscid flows**
  - No viscosity or very small viscosity
  - Drop the viscosity term

$$\frac{D\vec{u}}{Dt} + \frac{1}{\rho}\nabla p = \vec{g}$$
$$\nabla \cdot \vec{u} = 0$$



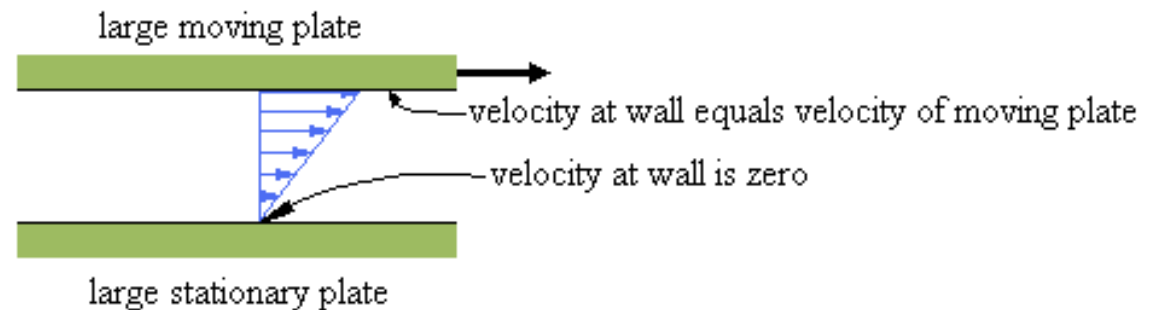
# Boundary conditions

- **Solid wall boundary**
  - The flow cannot penetrate
    - Slip boundary

$$\vec{u} \cdot \hat{n} = \vec{u}_{\text{solid}} \cdot \hat{n}$$

- No-slip (Neumann) boundary

$$\vec{u} = \vec{u}_{\text{solid}}$$



## **2. Unconditionally stable semi-Lagrangian method**

# Finite difference method

- **Derivative approximation**

- First derivative

- Taylor expansion

$$u(x + \Delta x) = u(x) + \Delta x \frac{\partial u(x)}{\partial x} + \frac{(\Delta x)^2}{2} \frac{\partial^2 u(x)}{\partial x^2} + \frac{(\Delta x)^3}{3!} \frac{\partial^3 u(x)}{\partial x^3} + \dots$$

- First order approximation

$$\frac{u(x + \Delta x) - u(x)}{\Delta x} = \frac{\partial u(x)}{\partial x} + \frac{\Delta x}{2} \frac{\partial^2 u(x)}{\partial x^2} + \dots = \frac{\partial u(x)}{\partial x} + O(\Delta x)$$

# Finite difference method

- **Derivative approximation**
  - First derivative
    - Second order approximation

$$u_{i+1} = u_i + \Delta x \left( \frac{\partial u}{\partial x} \right)_i + \frac{\Delta x^2}{2} \left( \frac{\partial^2 u}{\partial x^2} \right)_i + \frac{\Delta x^3}{3!} \left( \frac{\partial^3 u}{\partial x^3} \right)_i + \frac{\Delta x^4}{4!} \left( \frac{\partial^4 u}{\partial x^4} \right)_i + \dots$$

$$u_{i-1} = u_i - \Delta x \left( \frac{\partial u}{\partial x} \right)_i + \frac{\Delta x^2}{2} \left( \frac{\partial^2 u}{\partial x^2} \right)_i - \frac{\Delta x^3}{3!} \left( \frac{\partial^3 u}{\partial x^3} \right)_i + \frac{\Delta x^4}{4!} \left( \frac{\partial^4 u}{\partial x^4} \right)_i + \dots$$



$$\left( \frac{\partial u}{\partial x} \right)_i = \frac{u_{i+1} - u_{i-1}}{2\Delta x} + O(\Delta x^2)$$



# Splitting

- **How to solve the fluid equations?**
  - Split the complex equations into simpler ones
- **Splitting in general PDE**

$$\frac{dq}{dt} = f(q) + g(q)$$



$$\begin{aligned}\tilde{q} &= q^n + \Delta t f(q^n) \\ q^{n+1} &= \tilde{q} + \Delta t g(\tilde{q})\end{aligned}$$

# Splitting

- **Splitting in general PDE**

- Is splitting with the same order as original? Yes!

$$\begin{aligned}q^{n+1} &= (q^n + \Delta t f(q^n)) + \Delta t g(q^n + \Delta t f(q^n)) \\&= q^n + \Delta t f(q^n) + \Delta t (g(q^n) + O(\Delta t)) \\&= q^n + \Delta t (f(q^n) + g(q^n)) + O(\Delta t^2) \\&= q^n + \frac{dq}{dt} \Delta t + O(\Delta t^2)\end{aligned}$$

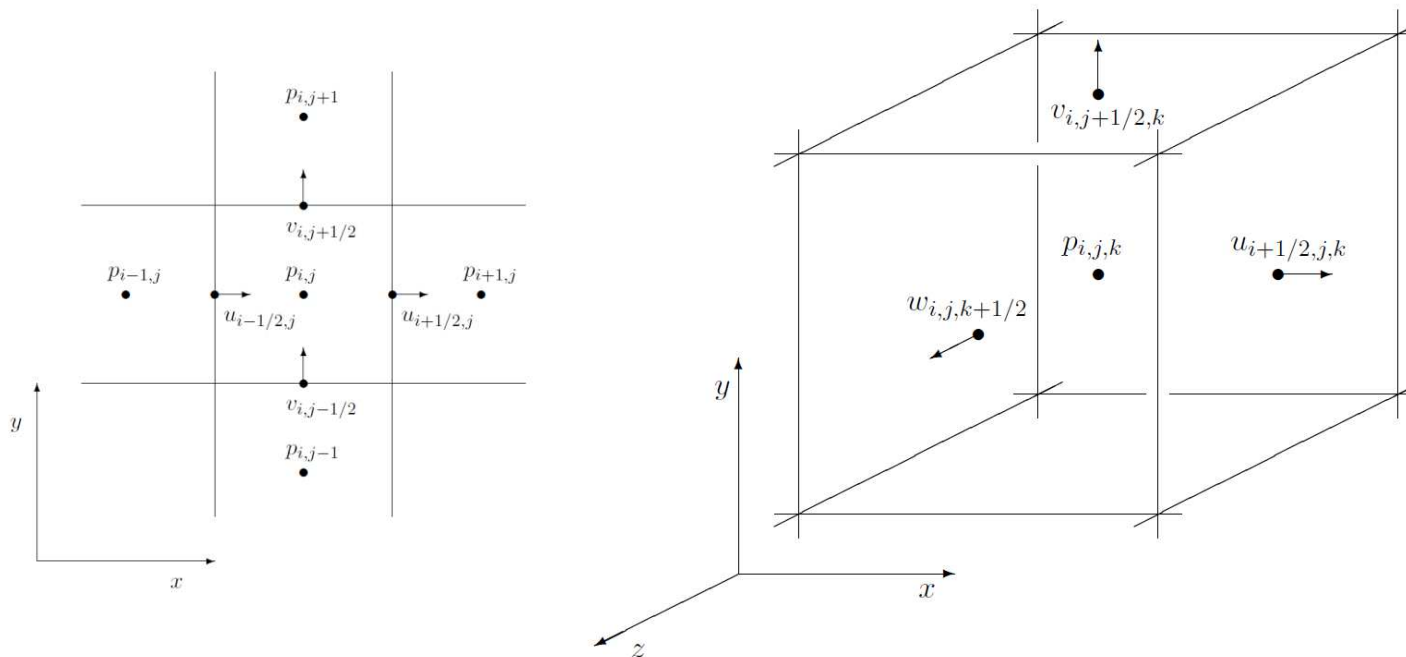
- **Splitting for Navier-Stokes equations**

$$\mathbf{w}_0(\mathbf{x}) \xrightarrow{\text{add force}} \mathbf{w}_1(\mathbf{x}) \xrightarrow{\text{advect}} \mathbf{w}_2(\mathbf{x}) \xrightarrow{\text{diffuse}} \mathbf{w}_3(\mathbf{x}) \xrightarrow{\text{project}} \mathbf{w}_4(\mathbf{x})$$

# MAC grid

- **Staggered grid**

- Staggered arrangement of velocity and pressure
- Face center: velocity samples
- Cell center: pressure samples
- Avoid high frequency artifacts



# Advection

- **What is an advection?**
  - Transport of a substance

$$Dq/Dt = 0$$

- Numerical solver
  - The simple discretization: explicit Euler

$$\frac{\partial q}{\partial t} + u \frac{\partial q}{\partial x} = 0 \quad \longrightarrow \quad \frac{q_i^{n+1} - q_i^n}{\Delta t} + u_i^n \frac{q_{i+1}^n - q_{i-1}^n}{2\Delta x} = 0$$

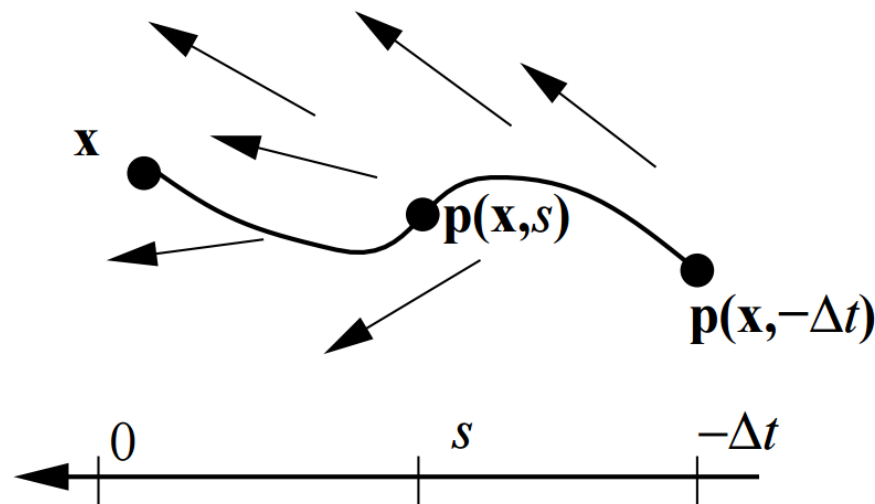


Unconditionally unstable!  $\longrightarrow$   $q_i^{n+1} = q_i^n - \Delta t u_i^n \frac{q_{i+1}^n - q_{i-1}^n}{2\Delta x}$

# Semi-Lagrangian advection

- **How to make stable solution?**
  - Implicit formulation?
    - Difficult to solve; hard for non-linear advection
- **Unconditionally stable yet simple solution?**
  - Semi-Lagrangian scheme
    - Jos Stam, Stable Fluids, SIGGRAPH 1999

$$\frac{d\vec{x}}{dt} = \vec{u}$$



# Unconditionally stable simulation

- **Helmholtz-Hodge Decomposition**

- Any vector field can be uniquely decomposed into
  - Divergence free field
  - Divergent field

$$\mathbf{w} = \mathbf{u} + \nabla q \quad \nabla \cdot \mathbf{u} = 0$$

- **How can this be applied to fluid equations?**

- Define an operator  $\mathbf{P}$ : project any vector field  $\mathbf{w}$  onto its divergence free part  $\mathbf{u}$

$$\nabla \cdot \mathbf{w} = \nabla^2 q \quad \longrightarrow \quad \mathbf{u} = \mathbf{P}\mathbf{w} = \mathbf{w} - \nabla q$$

# Unconditionally stable simulation

- **Apply to Navier-Stokes equation**
  - Apply to both sides of momentum equation

$$\frac{\partial \mathbf{u}}{\partial t} = -(\mathbf{u} \cdot \nabla) \mathbf{u} - \frac{1}{\rho} \nabla p + \nu \nabla^2 \mathbf{u} + \mathbf{f}$$

$$\mathbf{P} \mathbf{u} = \mathbf{u} \quad \mathbf{P} \nabla p = 0 \quad \downarrow \quad \mathbf{P}$$

$$\frac{\partial \mathbf{u}}{\partial t} = \mathbf{P} \left( -(\mathbf{u} \cdot \nabla) \mathbf{u} + \nu \nabla^2 \mathbf{u} + \mathbf{f} \right)$$

$$\mathbf{w}_0(\mathbf{x}) \xrightarrow{\text{add force}} \mathbf{w}_1(\mathbf{x}) \xrightarrow{\text{advect}} \mathbf{w}_2(\mathbf{x}) \xrightarrow{\text{diffuse}} \mathbf{w}_3(\mathbf{x}) \xrightarrow{\text{project}} \mathbf{w}_4(\mathbf{x})$$



# Unconditionally stable simulation

$$\frac{\partial \mathbf{u}}{\partial t} = \mathbf{P} \left( -(\mathbf{u} \cdot \nabla) \mathbf{u} + \nu \nabla^2 \mathbf{u} + \mathbf{f} \right)$$

- **Add force**  $\mathbf{w}_1(\mathbf{x}) = \mathbf{w}_0(\mathbf{x}) + \Delta t \mathbf{f}(\mathbf{x}, t)$
- **Advect**  $\mathbf{w}_2(\mathbf{x}) = \mathbf{w}_1(\mathbf{p}(\mathbf{x}, -\Delta t))$
- **Diffuse**  $(\mathbf{I} - \nu \Delta t \nabla^2) \mathbf{w}_3(\mathbf{x}) = \mathbf{w}_2(\mathbf{x})$
- **Project**  $\nabla^2 q = \nabla \cdot \mathbf{w}_3 \quad \mathbf{w}_4 = \mathbf{w}_3 - \nabla q$

# Vorticity confinement

- **Compensate for numerical diffusion**

- Add a “vorticity confinement” force
- Disturb the flow from current vorticity
- Definition of vorticity

- **Find vortices**  $\vec{\omega} = \nabla \times \vec{u}$

- The local axes of vorticity  $\vec{N} = \frac{\nabla |\vec{\omega}|}{\|\nabla |\vec{\omega}|\|}$

- **Construct disturbing force**

$$f_{\text{conf}} = \epsilon \Delta x (\vec{N} \times \vec{\omega})$$

# Vorticity confinement

- **Implementation**

- Computation of vorticity

$$\vec{\omega}_{i,j,k} = \left( \frac{w_{i,j+1,k} - w_{i,j-1,k}}{2\Delta x} - \frac{v_{i,j,k+1} - v_{i,j,k-1}}{2\Delta x}, \right. \\ \left. \frac{u_{i,j,k+1} - u_{i,j,k-1}}{2\Delta x} - \frac{w_{i+1,j,k} - w_{i-1,j,k}}{2\Delta x}, \right. \\ \left. \frac{v_{i+1,j,k} - v_{i-1,j,k}}{2\Delta x} - \frac{u_{i,j+1,k} - u_{i,j-1,k}}{2\Delta x} \right)$$

- Computation of vorticity gradient

$$\nabla |\vec{\omega}|_{i,j,k} = \left( \frac{|\vec{\omega}|_{i+1,j,k} - |\vec{\omega}|_{i-1,j,k}}{2\Delta x}, \frac{|\vec{\omega}|_{i,j+1,k} - |\vec{\omega}|_{i,j-1,k}}{2\Delta x}, \frac{|\vec{\omega}|_{i,j,k+1} - |\vec{\omega}|_{i,j,k-1}}{2\Delta x} \right)$$

- Normalize this to get N

$$\vec{N}_{i,j,k} = \frac{\nabla |\vec{\omega}|_{i,j,k}}{\|\nabla |\vec{\omega}|_{i,j,k}\| + 10^{-20}}$$

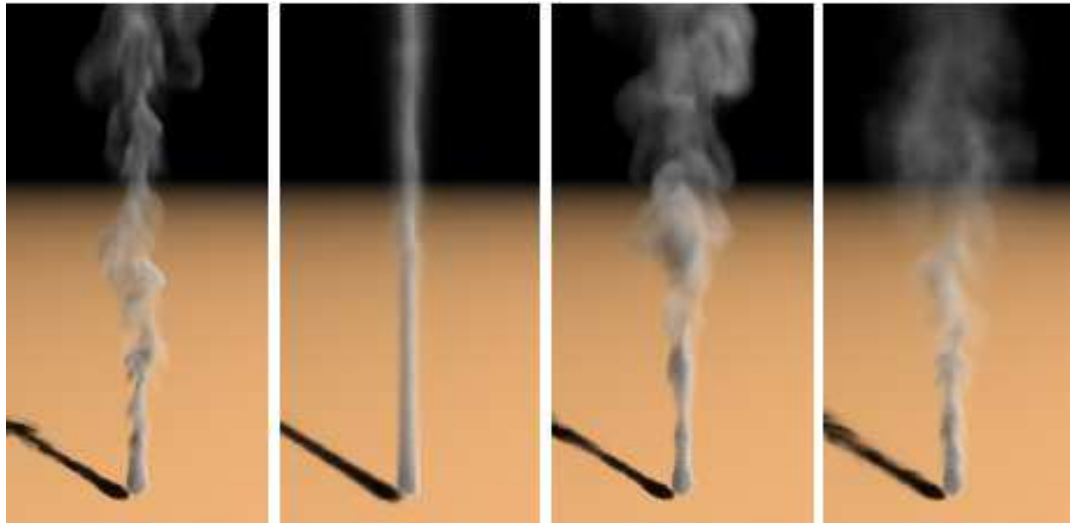
# Smoke simulation

- **Evolve additional quantities**

- Temperature  $T$  and smoke concentration  $s$

$$\frac{DT}{Dt} = 0 \quad \frac{Ds}{Dt} = 0$$

- Buoyancy force  $f_{\text{buoy}} = (0, -\alpha s + \beta(T - T_{\text{amb}}), 0)$



# An Advection-Reflection Solver for Detail-Preserving Fluid Simulation

Jonas Zehnder  
Université de Montréal

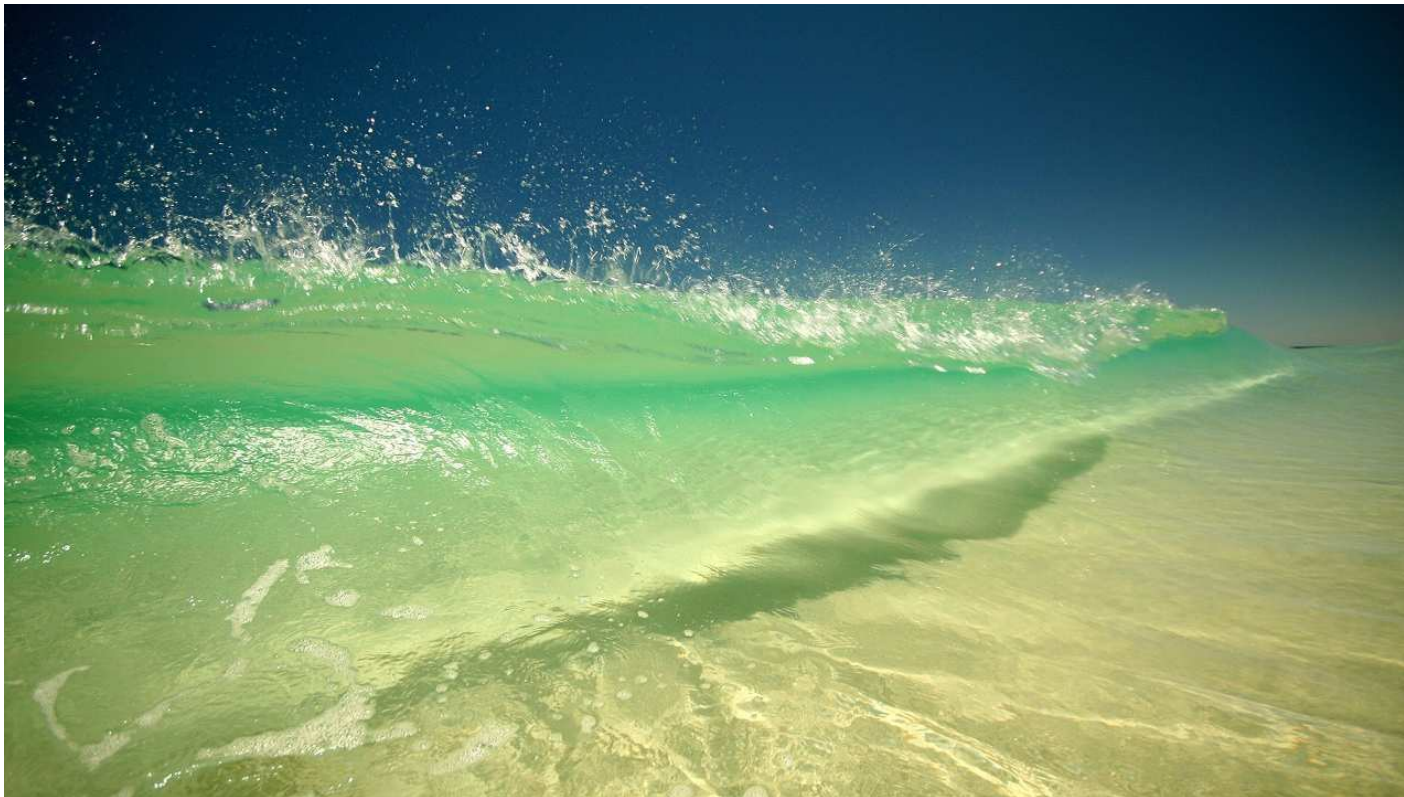
Rahul Narain  
Indian Institute of Technology Delhi  
University of Minnesota

Bernhard Thomaszewski  
Université de Montréal

## 4. Liquid Simulation

# Liquid simulation

- **Characteristics of liquids**
  - Interface dynamics
  - Tracking the motion of interface



# Liquid simulation

- **Implicit surface & level set**

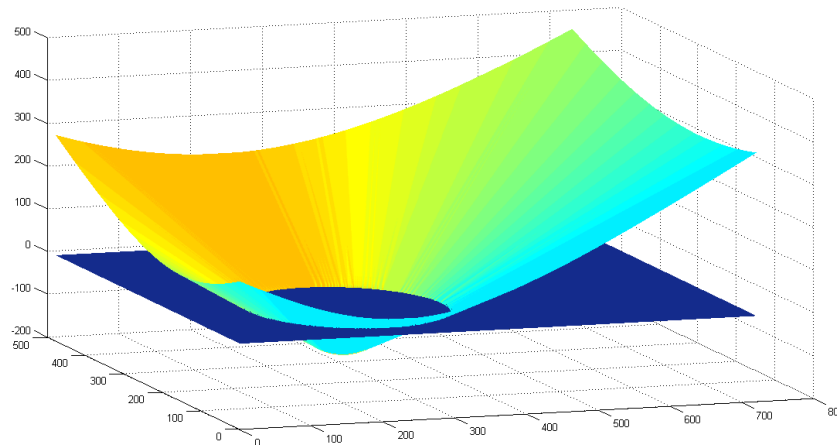
- Implicit surface

- A surface in Euclidean space defined by an equation

$$F(x, y, z) = 0.$$

- Why? Easy for complex surfaces

- Level set surface





# Liquid simulation

- **Interface representation**

- Implicit surface
- liquid volume as one side of an isocontour of an implicit function

$$\phi \leq 0$$

- Interface
  - Isosurface (isocontuour)

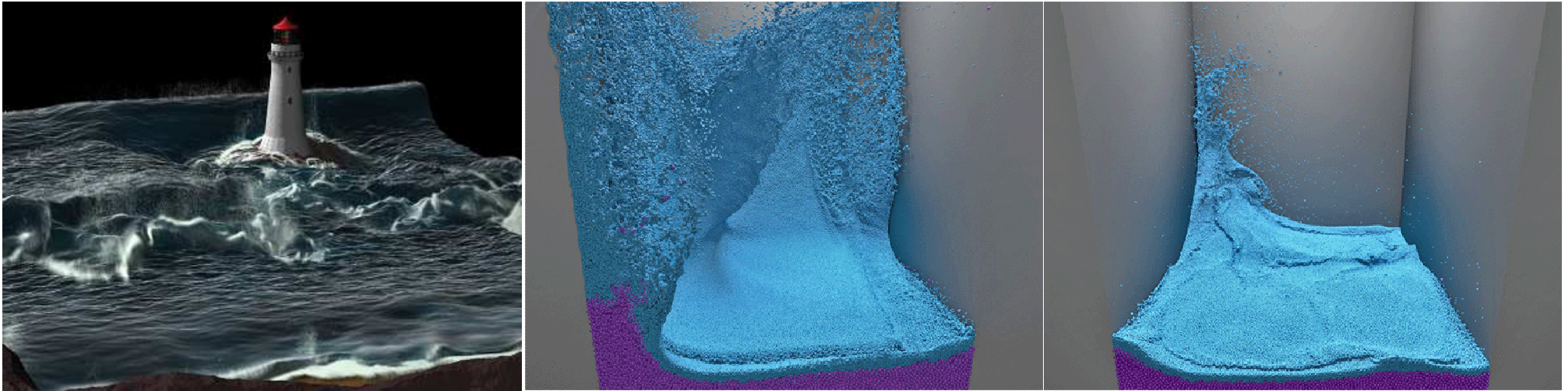
$$\phi = 0$$

- Interface advection
  - Level set equation

$$\phi_t + \vec{u} \cdot \nabla \phi = 0$$

# Problem with mesh-based method

- **How to simulate complex free surface?**
  - Complex free boundary condition
  - Water splashes

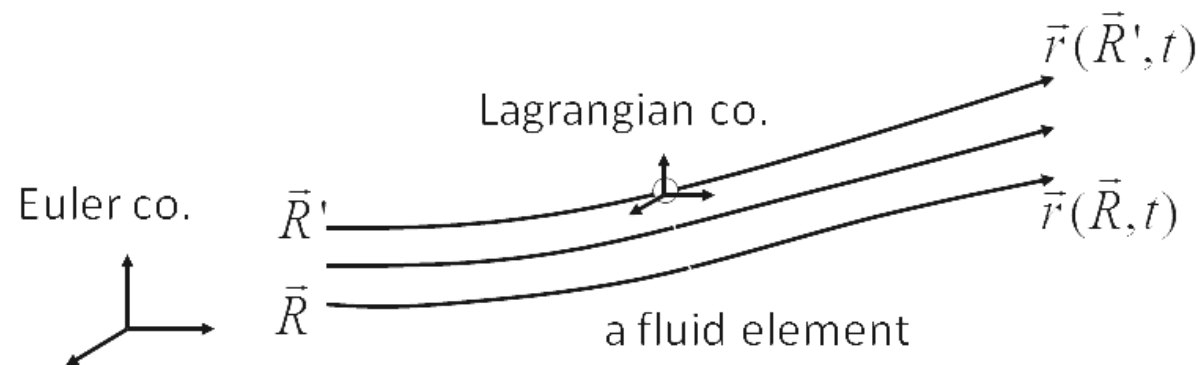


- Particle methods are preferred

# **5. Smoothed Particle Hydrodynamics**

# Lagrangian solver for fluids

- Coordinate is moving with fluid



$$\boxed{\frac{\partial \vec{u}}{\partial t} + \vec{u} \cdot \nabla \vec{u}} + \frac{1}{\rho} \nabla p = \vec{g} + \nu \nabla \cdot \nabla \vec{u}$$



$$\boxed{\frac{D \vec{u}}{Dt}} + \frac{1}{\rho} \nabla p = \vec{g} + \nu \nabla \cdot \nabla \vec{u}$$



# Smoothed-particle hydrodynamics

- **Function approximation with SPH**

- Problem setting

- Reconstructing an (unknown) function  $f$  from a set of irregular samples  $f_i = f(\mathbf{x}_i)$
    - Using the Dirac-delta function, we can rewrite  $f(\mathbf{x})$  as a convolution

$$f(\mathbf{x}) = \int_{\mathbf{x}'} f(\mathbf{x}') \delta(\|\mathbf{x} - \mathbf{x}'\|) dV$$

- Replace delta function with a kernel function  $w_h$

$$\tilde{f}(\mathbf{x}) = \int_{\mathbf{x}'} f(\mathbf{x}') \omega_h(\|\mathbf{x} - \mathbf{x}'\|) dV \quad \int \omega_h = 1$$

# Smoothed-particle hydrodynamics

- **Function approximation with SPH**

- Discretize the integral into a sum over all sample points to obtain the SPH approximation

$$\tilde{f}(\mathbf{x}) = \int_{\mathbf{x}'} f(\mathbf{x}') \omega_h(\|\mathbf{x} - \mathbf{x}'\|) dV \quad \rightarrow \quad \langle f \rangle(\mathbf{x}) = \sum_i f_i \omega_h(\|\mathbf{x}_i - \mathbf{x}\|) V_i$$

- How to compute volume  $V_i$  for each sample?
  - Associate with mass  $m_i$

$$V_i = \frac{m_i}{\rho_i}$$

# Smoothed-particle hydrodynamics

- **Function approximation with SPH**
  - How to compute density estimation?

$$\rho_i = \langle \rho \rangle (\mathbf{x}_i) = \sum_j \omega_h(\|\mathbf{x}_i - \mathbf{x}_j\|) \rho_j V_j \quad + \quad V_i = \frac{m_i}{\rho_i}$$



$$\begin{aligned} \rho_i = \langle \rho \rangle (\mathbf{x}_i) &= \sum_j \omega_h(\|\mathbf{x}_i - \mathbf{x}_j\|) \rho_j V_j \\ &= \sum_j \omega_h(\|\mathbf{x}_i - \mathbf{x}_j\|) \rho_j \frac{m_j}{\rho_j} \\ &= \sum_j \omega_h(\|\mathbf{x}_i - \mathbf{x}_j\|) m_j \end{aligned}$$

# Smoothed-particle hydrodynamics

- **Kernel functions**

- Admissible kernel functions: they must be normalized

$$\int_{\mathbf{x}} \omega_h(\|\mathbf{x}\|) dV = 1$$

- Smoothing parameter  $h$

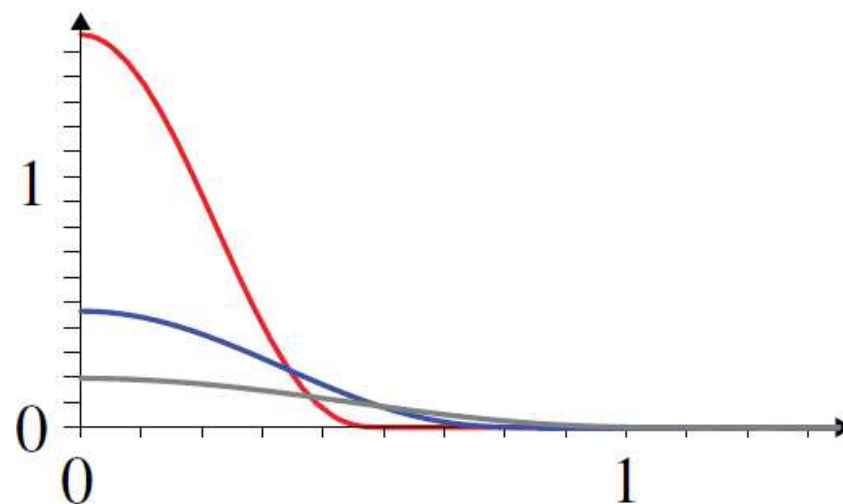
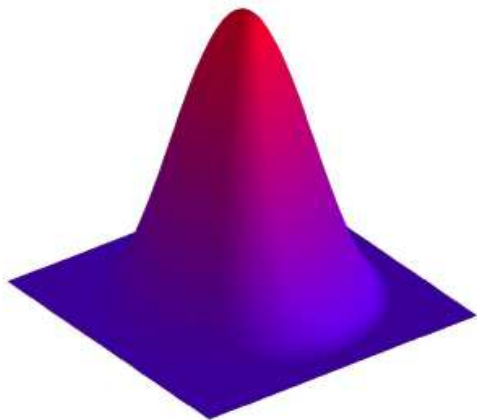
- Allowing control over how far the influence of each sample point reaches (local support)
    - Too large values of  $h$  produce unnecessarily smooth reconstructions
    - Kernel function converges to a Dirac-delta function as  $h$  goes to zero



# Smoothed-particle hydrodynamics

- **Kernel functions**
  - A good polynomial kernel function

$$\omega_h(d) = \begin{cases} \frac{315}{64\pi h^3} \left(1 - \frac{d^2}{h^2}\right)^3 & d < h, \\ 0 & \text{otherwise} \end{cases}$$



# Smoothed-particle hydrodynamics

- **Approximation of differential operators**
  - Apply SPH approximations to the solution of partial differential equations
    - Not only a reconstruction of the continuous function  $f$ , but also the derivatives of the function
  - Sample values  $f_i$  are constants, we can write approximation of gradient as

$$\langle \nabla f \rangle (\mathbf{x}) = \sum_i f_i \nabla \omega_h(\|\mathbf{x} - \mathbf{x}_i\|) V_i$$

$$\nabla \omega_h(\|\mathbf{x} - \mathbf{x}_i\|) = \frac{\mathbf{x} - \mathbf{x}_i}{\|\mathbf{x} - \mathbf{x}_i\|} \omega'_h(\|\mathbf{x} - \mathbf{x}_i\|)$$

# Smoothed-particle hydrodynamics

- **Approximation of differential operators**

- Other linear operators can be treated similarly

$$\langle \Delta f \rangle (\mathbf{x}) = \sum_i f_i \Delta \omega_h(\|\mathbf{x} - \mathbf{x}_i\|) V_i$$

$$\langle \nabla \cdot \mathbf{f} \rangle (\mathbf{x}) = \sum_i \mathbf{f}_i \cdot \nabla \omega_h(\|\mathbf{x} - \mathbf{x}_i\|) V_i$$

- Accuracy of the approximations of derivative

- Strongly depends on the distribution of sample points within the support region
- For highly irregular sample distributions, the differential properties can be very noisy

# Smoothed-particle hydrodynamics

- **Approximation of differential operators**

- Problem with previous estimation

- Gradient approximation can yield non-zero values even if the function is constant

- How to rectify?

- Enforce a zero gradient for constant functions by subtracting the constant  $f_i$

$$\begin{aligned}\nabla f(\mathbf{x}_i) &\approx \langle \nabla [f - f_i] \rangle (\mathbf{x}_i) \\ &= \sum_j (f_j - f_i) \nabla \omega_h(\|\mathbf{x}_i - \mathbf{x}_j\|) V_j\end{aligned}$$

# Smoothed-particle hydrodynamics

- **Approximation of differential operators**
  - Same reasoning applied to the divergence and Laplace operators

$$\langle \nabla \cdot \mathbf{f} \rangle (\mathbf{x}_i) = \sum_j (\mathbf{f}_j - \mathbf{f}_i) \cdot \nabla \omega_h(\|\mathbf{x}_i - \mathbf{x}_j\|) V_j$$

$$\langle \Delta f \rangle (\mathbf{x}_i) = \sum_j (f_j - f_i) \Delta \omega_h(\|\mathbf{x}_i - \mathbf{x}_j\|) V_j$$

# Smoothed-particle hydrodynamics

- **Approximation of differential operators**
  - Another variation of the gradient approximation important in particular for fluid simulation

$$\nabla \left[ \frac{f}{\rho} \right] = \frac{\rho \nabla f - f \nabla \rho}{\rho^2}$$
$$\Rightarrow \nabla f = \rho \left( \nabla \left[ \frac{f}{\rho} \right] + \frac{f \nabla \rho}{\rho^2} \right)$$



$$\nabla f(\mathbf{x}_i) \approx \rho_i \left( \left\langle \nabla \left[ \frac{f}{\rho} \right] \right\rangle (\mathbf{x}_i) + \frac{f_i \langle \nabla \rho \rangle (\mathbf{x}_i)}{\rho_i^2} \right)$$
$$= \rho_i \sum_j m_j \left( \frac{f_j}{\rho_j^2} + \frac{f_i}{\rho_i^2} \right) \nabla \omega_h(\|x_i - x_j\|)$$

# Fluid simulation using SPH

- **For compressible fluids**

- The momentum equation can be written as a combination of pressure, viscosity, and external forces

$$\frac{D\mathbf{v}}{Dt} = \frac{1}{\rho} (\mathbf{f}_p + \mathbf{f}_v + \mathbf{f}_e)$$

- $\mathbf{f}_e$  are external forces acting on the fluid
- The pressure force  $\mathbf{f}_p$  is a function of the pressure field  $p$
- Viscous forces smooth the velocity field

$$\mathbf{f}_p = -\nabla p$$

$$\mathbf{f}_v = \mu \nabla \cdot \nabla \mathbf{v} = \mu \Delta \mathbf{v}$$

# Fluid Simulation using SPH

- **For compressible fluids**
  - How to compute pressure
    - Equation of state
    - Common choice: Tait equation

$$p = K \left( \left( \frac{\rho}{\rho_0} \right)^\gamma - 1 \right)$$

- The most straightforward spatial discretization
  - Consider Lagrangian coordinates

$$\frac{\partial \mathbf{v}_i}{\partial t} = - \frac{\langle \nabla p \rangle (\mathbf{x}_i)}{\rho_i} + \mu \langle \Delta \mathbf{v} \rangle (\mathbf{x}_i) + \frac{\mathbf{f}_e(\mathbf{x}_i)}{\rho_i}$$



# Fluid Simulation using SPH

- **Pressure forces**

- Particle accelerations due to pressure forces

$$\frac{\mathbf{f}_p(\mathbf{x}_i)}{\rho(\mathbf{x}_i)} = - \frac{\langle \nabla p \rangle (\mathbf{x}_i)}{\rho_i}$$

- Implementation

$$\frac{\mathbf{f}_p(\mathbf{x}_i)}{\rho(\mathbf{x}_i)} = - \sum_j \nabla \omega_h^{ij} p_j \frac{m_j}{\rho_j \rho_i} = - \sum_j \mathbf{a}_p^{ji}$$

# Fluid Simulation using SPH

- **Pressure forces**

- Problem

- Observation

$$\mathbf{a}_p^{ji} + \mathbf{a}_p^{ij} \neq 0$$

- Linear and angular momentum may not be conserved
    - Low resolution problem is more significant (visual artifacts)

- Symmetrize

$$\begin{aligned} \nabla f(\mathbf{x}_i) &\approx \rho_i \left( \left\langle \nabla \left[ \frac{f}{\rho} \right] \right\rangle (\mathbf{x}_i) + \frac{f_i \langle \nabla \rho \rangle (\mathbf{x}_i)}{\rho_i^2} \right) \\ &= \rho_i \sum_j m_j \left( \frac{f_j}{\rho_j^2} + \frac{f_i}{\rho_i^2} \right) \nabla \omega_h(\|x_i - x_j\|) \end{aligned} \quad \rightarrow \quad \frac{\mathbf{f}_p(\mathbf{x}_i)}{\rho(\mathbf{x}_i)} = - \sum_j \nabla \omega_h^{ij} \left( \frac{p_j}{\rho_j^2} + \frac{p_i}{\rho_i^2} \right) m_j$$

# Fluid Simulation using SPH

- **Viscosity forces**

- Discretizing the acceleration on particles due to viscosity leads to the expression

$$\frac{\mathbf{f}_v(\mathbf{x}_i)}{\rho_i} = \mu \sum_j \Delta\omega_h^{ij} (\mathbf{v}_j - \mathbf{v}_i) \frac{m_j}{\rho_i \rho_j} = \mu \sum_j \mathbf{a}_v^{ji}$$

- The force is symmetric:

$$\mathbf{a}_v^{ji} + \mathbf{a}_v^{ij} = 0$$

# Fluid Simulation using SPH

- **Viscosity forces**

- Problem

- Higher-order derivatives depends strongly on the distribution of sample points
    - Quite noisy especially for small support radius of the kernel function

- Smoothing operator

- Create artificial viscosity

$$\begin{aligned}\tilde{\mathbf{v}}_i &= \xi \langle \mathbf{v} \rangle (\mathbf{x}_i) + (1 - \xi) \mathbf{v}_i \\ &= \xi \left[ \sum_j \omega_h^{ij} \mathbf{v}_j \frac{m_j}{\rho_j} \right] + (1 - \xi) \mathbf{v}_i \quad 0 \leq \xi \leq 1\end{aligned}$$

# Fluid Simulation using SPH

- **Time discretization and simulation loop**
  - Using a simple explicit integration scheme

$$\mathbf{v}_i(t + \Delta t) = \mathbf{v}_i(t) + \Delta t \frac{D\mathbf{v}_i}{Dt}$$

$$\mathbf{x}_i(t + \Delta t) = \mathbf{x}_i(t) + \Delta t \mathbf{v}_i(t + \Delta t)$$

- Higher order time-integrator can be applied

## **2. Incompressible SPH**

# Incompressible SPH

- **Prediction-correction scheme**
  - PCISPH, Solenthaler et al. SIGGRAPH 2009
  - The density at a point in time  $t + 1$

$$\begin{aligned}\rho_i(t + 1) &= m \sum_j W(\mathbf{x}_i(t + 1) - \mathbf{x}_j(t + 1)) \\ &= m \sum_j W(\mathbf{x}_i(t) + \Delta\mathbf{x}_i(t) - \mathbf{x}_j(t) - \Delta\mathbf{x}_j(t)) \\ &= m \sum_j W(\mathbf{d}_{ij}(t) + \Delta\mathbf{d}_{ij}(t))\end{aligned}$$

where  $\mathbf{d}_{ij}(t) = \mathbf{x}_i(t) - \mathbf{x}_j(t)$ , and  $\Delta\mathbf{d}_{ij}(t) = \Delta\mathbf{x}_i(t) - \Delta\mathbf{x}_j(t)$

# Incompressible SPH

- **Prediction-correction scheme**

- Assuming that  $\Delta \mathbf{d}_{ij}$  is relatively small, the first order Taylor approximation can be applied

$$\begin{aligned}\rho_i(t+1) &= m \sum_j W(\mathbf{d}_{ij}(t)) + \nabla W(\mathbf{d}_{ij}(t)) \cdot \Delta \mathbf{d}_{ij}(t) \\ &= m \sum_j W(\mathbf{x}_i(t) - \mathbf{x}_j(t)) + \\ &\quad m \sum_j \nabla W(\mathbf{x}_i(t) - \mathbf{x}_j(t)) \cdot (\Delta \mathbf{x}_i(t) - \Delta \mathbf{x}_j(t)) \\ &= \rho_i(t) + \Delta \rho_i(t).\end{aligned}$$

- The term  $\Delta \rho_i(t)$  is unknown, a function of  $p$  which we are looking for



# Incompressible SPH

- **Prediction-correction scheme**
  - Density error predictor

$$\rho_{err_i}^* = \rho_i^* - \rho_0$$

- Pressure corrector

$$\delta = \frac{-1}{\beta(-\sum_j \nabla W_{ij} \cdot \sum_j \nabla W_{ij} - \sum_j (\nabla W_{ij} \cdot \nabla W_{ij}))}$$

$$\tilde{p}_i = \delta \rho_{err_i}^*$$

$$p_i += \tilde{p}_i$$

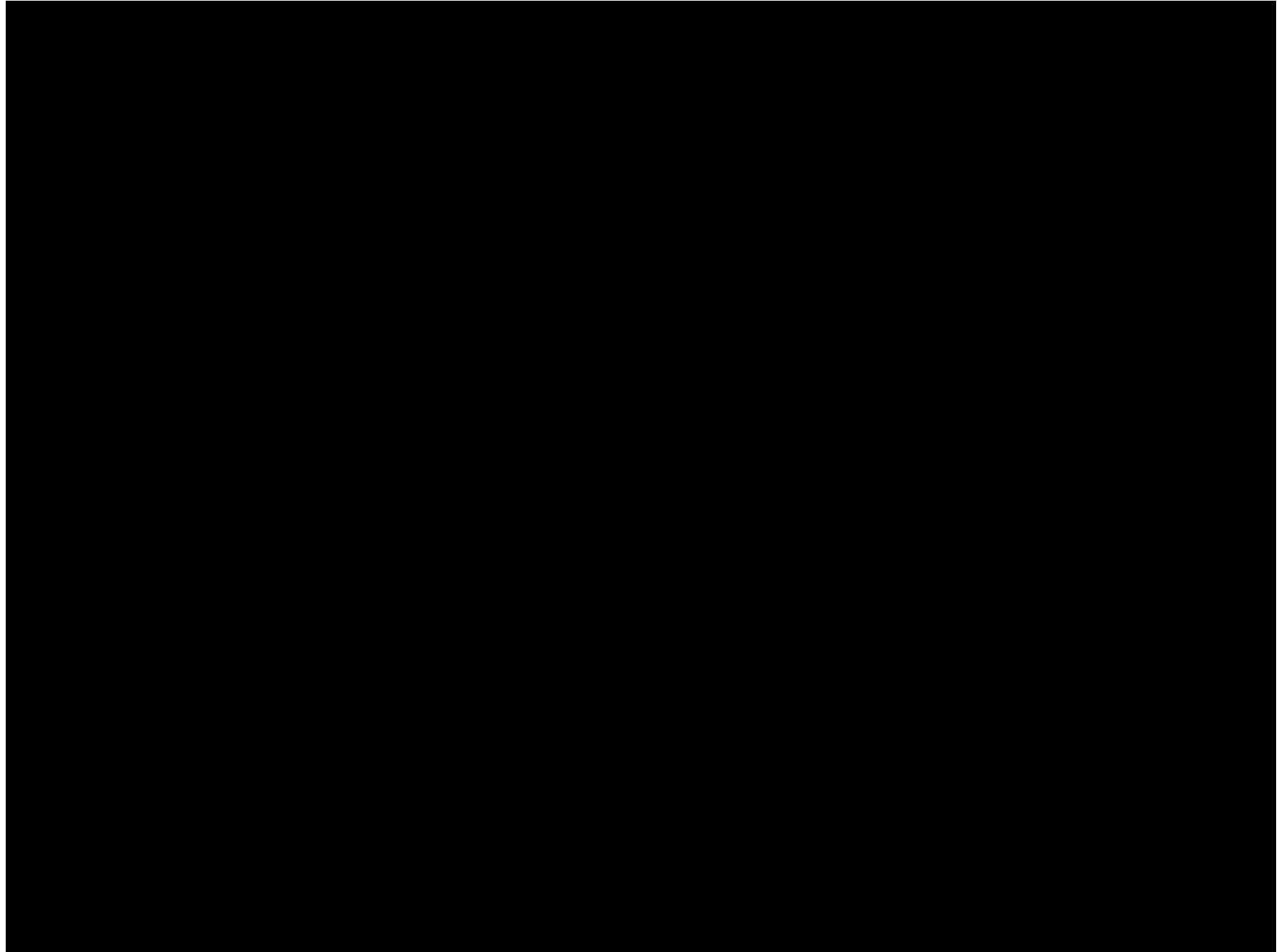
# Incompressible SPH

## Predictive–Corrective Incompressible SPH

Barbara Solenthaler, Renato Pajarola  
University of Zurich



# Particle solver coupled with rigid bodies



**End of the lecture**