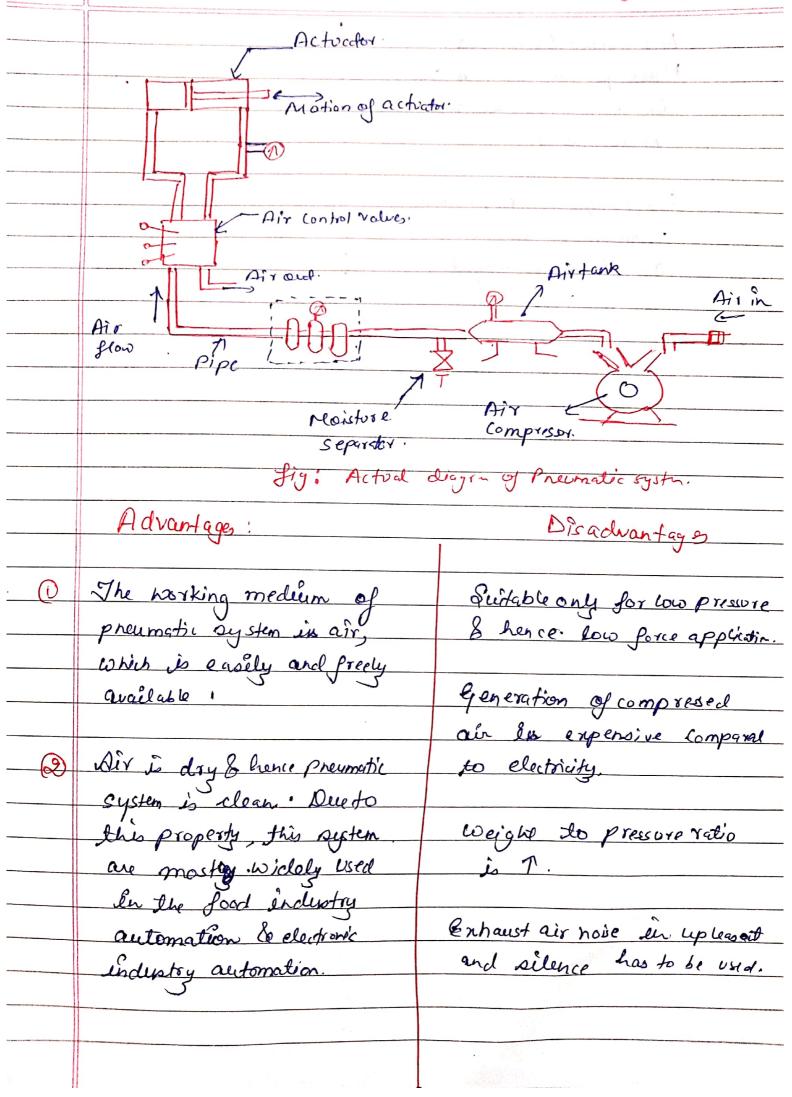
#	PNEUMATIC SYSTEM:
<u>, () </u>	Peneumatic is a technology which deals with power
	of atr.
	9n anguardie auder als la companyeral ha
	It and then its power is used to obtain
, λ	mechanical advantage i.e. to do resessablement
	Prematic are wed to a wide varietées of endustries.
	including construction, healthcare, mining, the automative endustry and many other.
	Caromative increasing cond in any other.
	Olive in
	Air in Compressor Air storage
	Moisture
	Separater
	Air filtes
	Respirator Pressure
Air	
Dryi	
i n	Control values.
	Control vaces
	fig: Block dig of Pneumatic system.
Personal Section of the Section of t	



1.37. PNEUMATIC SYSTEM

Consider the Fig. 1.126. In Fig. 1.126 a source is supplying air and the air is stored in vessel.

Let, P_i = Pressure of air of the source N/m²

 P_0 = Pressure of air in the vessel N/m²

 ΔP_i° = Change in air pressure of source

 $\Delta P_0'$ = Change in air pressure of vessel

R = Resistance to air flow into the vessel

C = Capacitance of the vessel

q = Rate of flow of air due to the differential pressure

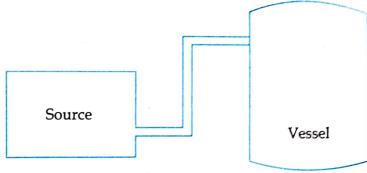


Fig. 1.126.

...(1.169)

$$q = \frac{\Delta P_i - \Delta P_0}{R}$$

The volume of air stored in vessel increases the pressure inside the vessel.

$$Volume V = C\Delta P_0 \qquad ...(1.170)$$

∴ Rate of storage in vessel =
$$\frac{dV}{dt} = C \frac{d\Delta P_0}{dt}$$
 ...(1.171)

Volume of air in flow
$$V = \int q \, dt = \int \frac{\Delta P_i - \Delta P_0}{R} \, dt$$
 ...(1.172)

Rate of air in flow
$$=\frac{dv}{dt} = \frac{\Delta P_i - \Delta P_0}{R}$$
 ...(1.173)

Rate of air in flow = Rate of storage of air in vessel

$$C\frac{d\Delta P_0}{dt} = \frac{\Delta P_i - \Delta P_0}{R} \qquad \dots (1.174)$$

Take Laplace transform

$$sC\Delta P_0 = \frac{1}{R} \left[\Delta P_i(s) - \Delta P_0(s) \right]$$

$$\frac{\Delta P_0}{\Delta P_i} = \frac{1}{1 + RCs} \qquad \dots (1.175)$$

Time constant = RC

...(112

..(11.3

11.3. CLASSIFICATION OF CONTROLLERS

11.3. CLASSIFICATION

11.3. CLASSIFICATION

Controllers are classified depending upon the type of controlling action used. Therefore, the controllers are classified depending upon the type of controlling action used. Therefore, the controllers are classified depending upon the type of controlling action used. Therefore, the controllers are classified depending upon the type of controlling action used. Therefore, the controllers are classified depending upon the type of controlling action used. (i) Two-position or ON-OFF controllers

- (ii) Proportional controllers
- (iii) Integral controllers
- (iv) Proportional-plus-integral controllers
- (v) Proportional-plus-derivative controllers
- (vi) Proportional-plus-integral-plus derivative controllers.

(vi) Proportional-plus-integral proportional-plu They can also be classified according to the controllers are suitable for shop floor applications. They can also be classified according to the controllers are suitable for shop floor applications. as electrical, electronics productions are suitable for shop floor applications.

trolling heavy loads, pricultance of the selection of a particular type of controller depends on the nature of plant, operating conditions are the selection of a particular type of controller depends on the nature of plant, operating conditions are the selection of a particular type of controller depends on the nature of plant, operating conditions are the selection of a particular type of controller depends on the nature of plant, operating conditions are the selection of a particular type of controller depends on the nature of plant, operating conditions are the selection of a particular type of controller depends on the nature of plant, operating conditions are the selection of a particular type of controller depends on the nature of plant, operating conditions are the selection of the selection of a particular type of controller depends on the nature of plant, operating conditions are the selection of the s such as safety, cost, availability, accuracy, weight and size.

11.4. TWO POSITION CONTROL

This is also known as ON-OFF control or bang-bang control. This type of controllers are simpled. inexpensive and are generally employed on home heating systems, domestic water heaters at industrial control systems.

In this type of control the output of the controller is quickly changed to either a maximum minimum value depending upon whether the controlled variable (b) is greater or less than the point or in other words depends upon the actuating error signal (e) The minimum value is usual zero.

m =Output of the controller Let,

 M_1 = Maximum value of output of the controller

 M_2 = Minimum value of output of the controller

e = Actuating error signal or deviation.

The equations for two-position control will be

$$m = M_1$$
 when $e > 0$
 $m = M_2$ when $e < 0$

The minimum value M_2 is usually either zero or – M_1

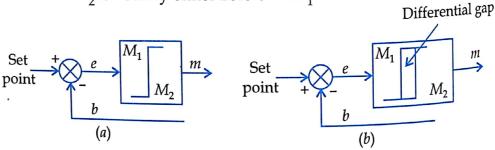


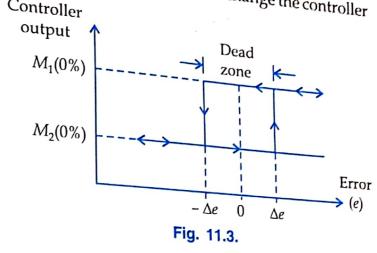
Fig. 11.2.

The block diagram of two position controllers are shown in Fig. 11.2. In ON-OFF controllers are shown in Fig. 11.2. In ON-OFF controllers are shown in Fig. 11.2. there is an overlap as the error increases through zero or decreases through zero. This overlap as a span of error, the error there is an overlap as the error increases through zero or decreases through zero. This span of error, the error than th a span of error. During this span of error, there is no change in the controller output. This span of error is known as dead zone or dead band. Dood to error is known as dead zone or dead band. Dead band is shown in Fig. 11.3.

11.3, it is clear that till the error changes by Δe there is no change in the controller from Fig. 11.3, it is clear that till the error changes by Δe there is no change in the controller cimilarly while decreasing the error must decrease beyond Δe below 0 to change the From Fig. 11.3, he decreasing the error must decrease by Δe there is no change in the controller similarly while decreasing the error must decrease beyond Δe below 0 to change in the controller fence, during $2\Delta e$ there is no change in Δe below 0 to change the controller aller output. This zone is known as Controller

Juput Sinuary and the error must the error must apput Frence, during 2Δe there is no change in output. This zone is known apput for ler output. This zone is known as the control ler output. The differential gap can all the control gap. The differential gap can all The differential gap can also be which the action of the range through gap can also be grange through which the actuating with move before the switch. move before the switching grof signal must move before the switching

In this type of controller, the control variable Industrial variable with a frequency which inwhich in-with decreasing width of the dead zone The decrease in dead zone, the of ON-OFF switching of bence therefore the useful in hence therefore the useful life of the



interases, nerice and interases. Hence dead band should be designed to prevent the oscillations in ON-OFF

wo position control mode are used in room air conditioners, heaters, liquid level control in we volume tank.

ine example of this type of controller is a room heater. Figure 11.4 shows the controlling of mperature. If the temperature drops below the set point, an error signal is produced by the error blector, this error signal energised the relay and the heater turned ON. Similarly, if the temperature increase above a set point, the heater is turned OFF.

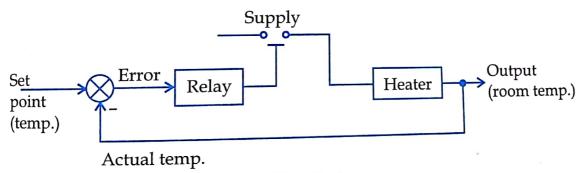


Fig. 11.4.

11.5. PROPORTIONAL CONTROL ACTION

ha controller with proportional control action, there is a continuous linear relation between the with proportional control action, there is a continuous $\frac{1}{2}$ (deviation). Mathematical mathematical mathematical $\frac{1}{2}$ (deviation).

$$m(t) = K_p e(t)$$

^{or in terms} of Laplace transform

$$M(s) = Kp E(s)$$

$$K_p = \frac{M(s)}{E(s)}$$

$$E(s) \longrightarrow K_{p} \longrightarrow M$$

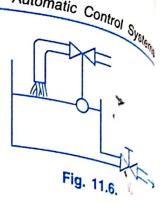
$$B(s)$$

Fig. 11.5.

 $K_p = \frac{M(s)}{E(s)}$...(11.5) $K_p = \frac{M(s)}{E(s)}$...(11.5)

ler is shown in Fig. 11.5.

Consider the liquid level system shown in Fig. 11.6. In this system the float lever is directly connected to the control value. When the level of the liquid rise, the valve close in proportionate amount this reduces the inflow to the vessel and vice versa. The inverse of proportional gain or proportional sensitivity is the proportional band and is defined as the change in level necessary to operate the valve through full stroke. Basically proportional controller is an amplifier with adjustable gain.



11.6. INTEGRAL CONTROL ACTION

In a controller with integral control action, the output of the controller is changed at a rate which proportional to the actuating error signal e(t).

Mathematically,

$$\frac{d}{dt}m(t) = K_i e(t) \qquad ...(11.6)$$

where K_i is a constant.

Equation (11.6) can also be written as

$$m(t) = K_i \int e(t) + m(0)$$
 ...(11.7)

where m(0) = control output at t = 0.

Laplace transform of equation (11.6)

$$SM(s) = K_i E(s)$$

or

$$\frac{M(s)}{E(s)} = \frac{K_i}{s} \qquad \dots (11.8)$$

Equation (11.8) is the transfer function of integral controller. The block diagram of integral controller is shown in Fig. 11.7.

The inverse of K_i is called *integral time* T_i and defined as the time of change of output caused by a unit change of actuating error signal. The step response of integral controller is shown in Fig. 11.8.

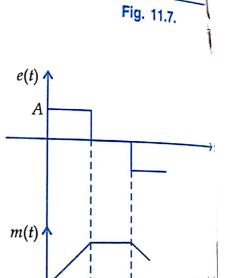


Fig. 11.8.

From the Fig. 11.8 it is clear that for positive error, the output of the controller is ramp (positive) for zero error, there is no change in the output of the controller and for negative error the output of the controller is negative ramp. The integral control action is also known as "Reset control".

11.7. DERIVATIVE CONTROL ACTION

In a controller with derivative control action the output of the controller depends on the rate of the rate of the controller depends on the rate of the

Mathematically,

$$m(t) = K_d \frac{d}{dt} e(t)$$

where K_d is known as derivative gain constant

...(11.9)

$$M(s) = K_d SE(s)$$

$$\frac{M(s)}{E(s)} = sK_d$$

...(11.10)

...(11.10)

11.10 is the transfer function of the controller. The plation is shown in Fig. 11.9.

Fig. 11.9,

Janster fu plation is shown is shown is shown is clear that when the error is zero or constant, the output of the controller cannot be used alone. For this type of controller cannot be used alone. For this type of controller cannot be used alone. Therefore, this type of controller cannot be used alone. For this type of controller the controller the small. The derivative control action also known as rate control. Thereion, The derivative control action also known as rate control.

PROPORTIONAL-PLUS-INTEGRAL CONTROL ACTION

the combination of proportional and integral control action. Mathematically it can be supported by equation (11.11). properted by equation (11.11).

$$m(t) = K_p e(t) + K_p K_i \int_0^t e(t) dt$$
 ...(11.11)

$$m(t) = K_p e(t) + K_p \frac{1}{T_i} \int_0^t e(t) dt$$
 ...(11.12)

Laplace transform of equation (11.12)

01

$$M(s) = K_p E(s) + \frac{K_p}{ST_i} E(s)$$

$$= E(s) \left[1 + \frac{1}{ST_i} \right] K_p$$

$$\frac{M(s)}{E(s)} = K_p \left[1 + \frac{1}{ST_i} \right]$$

Block diagram is shown in Fig. 11.10.

Inequation 11.13 both parameters K_p and T_i are adjustable. | called integral time. The inverse of integral time is called The inverse of integral time. The inverse of integral times per minute the number of times per minute. Reset rate is defined as the number of times per minute. the proportional part of the response is duplicated. Fig. 11.10.

...(11.13)

Consider the Fig. 11.11. The error varies at $t=t_1$. The output of the controller suddenly changes with respect to time at $t=t_1$. The output changes linearly with respect to time at $t=t_1$. Onsider the Fig. 11.11. The error varies at $t=t_1$. The output of the controller suddenly changes linearly with respect to time at the top proportional action, after that controller output changes linearly with respect to time at the top proportional action, after that controller output changes linearly with respect to time at the top proportional action, after that controller output changes linearly with respect to time at the top proportional action, after that controller output changes linearly with respect to time at the top proportional action, after that controller output changes linearly with respect to time at the top proportional action, after that controller output changes linearly with respect to time at the top proportional action, after that controller output changes linearly with respect to time at the top proportional action, after that controller output changes linearly with respect to time at the top proportional action.

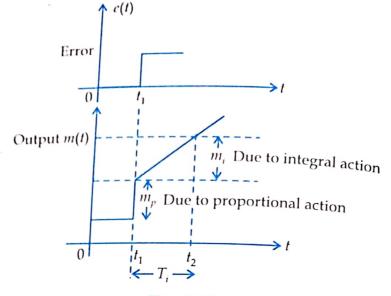


Fig. 11.11.

For unit step ($t_1 = 0$) the response is shown in Fig. 11.12.

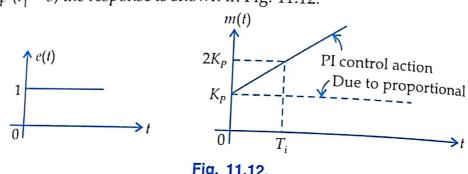


Fig. 11.12.

From the equation (11.12), it is clear that the proportional sensitivity K_p affects both the proportional and integral parts of the action.

11.9. PROPORTIONAL-PLUS-DERIVATIVE CONTROL ACTION

When a derivative control action is added in series to proportional control action, then this combination is termed as proportional-derivative control action. Mathematically it can be defined as

$$m(t) = K_p e(t) + K_p T_d \frac{d}{dt} e(t)$$
equation (11.14)

Laplace transform of equation (11.14)

$$M(s) = K_p E(s) + K_p T_d SE(s) = E(s) [1 + sT_d] K_p$$

$$\frac{M(s)}{E(s)} = K_p (1 + sT_d)$$
function

This is the transfer function.

The block diagram is shown in Fig. 11.13.

 T_d is known as *derivative time*. Derivative time is defined as the time interval by which the rate action advances the effect of the proportional control action or in other words derivative time

Fig. 11.13.

..(11.15

is defined as the amount of lead, expressed in units of time, that the control action is given.

If the actuating error signal e(t) is a control action is given. If the actuating error signal e(t) is a ramp function at $t = t_1$. The derivative mode causes a rise of t_1 . at t_1 and proportional mode causes a rise of m_p equal to m_d at t_2 . This is for direct action PD control. (Fig. 11.14).

463 \blacksquare Action reduces the rise time, faster response, improves the bandwidth and improves $e^{it} e^{it} e^{it} e^{it}$ $e^{it} e^{it} e^{it}$



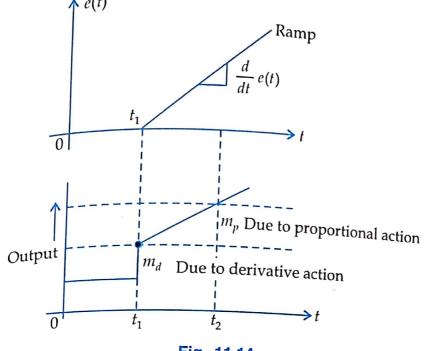
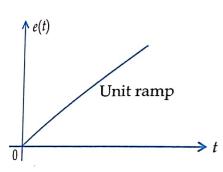


Fig. 11.14.

for unit ramp input.

for unit ramp then output of the controller is shown in Fig. 11.15.



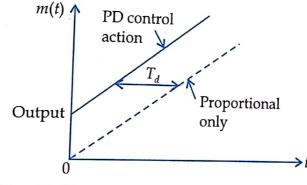


Fig. 11.15.

11.10. PROPORTIONAL-PLUS-INTEGRAL-PLUS-DERIVATIVE CONTROL ACTION

mbination of proportional, integral and derivative control action is called PID control action the controller is called three action controller. Mathematically

$$m(t) = K_p e(t) + K_p \frac{1}{T_i} \int_0^t e(t) dt + K_p T_d \frac{d}{dt} e(t)$$
 ...(11.16)

laplace transform

$$M(s) = K_p E(s) + \frac{K_p}{sT_i} E(s) + K_p T_d SE(s)$$

$$\frac{M(s)}{E(s)} = K_p \left(1 + \frac{1}{sT_i} + sT_d \right)$$

...(11.17)

Equation (11.17) is the transfer function.

The block diagram is shown in Fig. 11.16.

The block diagram T_i is the integral time and T_d is the derivative time. Let actuating error signal is given by e = At

where 'A' is a constant and 't' is time.

Put in equation (11.16)

$$m(t) = K_p A t + \frac{K_p}{T_i} \int_0^t A t \, dt + K_p T_d \, \frac{d}{dt} A t$$

$$m(t) = K_p A \left[t + \frac{t^2}{2T_i} + T_d \right]$$

From the above equation, the proportional part of the control action repeats the change of the chang (lower straight line) Fig. 11.17. The derivative part

of the control action adds an increment of output so that proportional plus derivative action is shifted ahead in time (middle straight line). The integral part adds a further increment of output proportional to the area under the deviation line. The combination of proportional, integral and derivaive action may be made in any sequence.

Fig. 11.16.

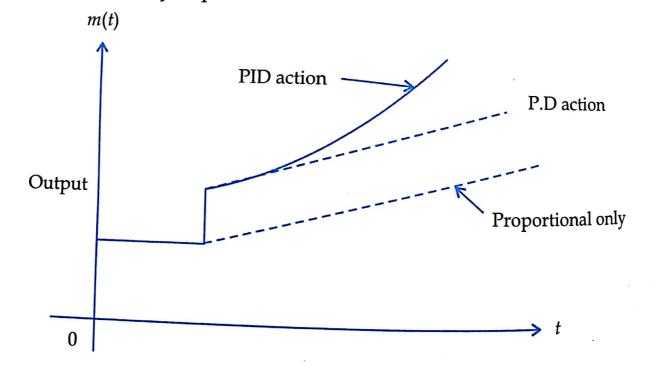


Fig. 11.17.

11.11. RESPONSE

Element equations and interconnection equations:

Hydraulic system

Hydraulic-Mechanical

Mechanical system

$$q_c = C \frac{d}{dt} p_{tr}$$

$$f_c = Ap_{Lr}$$
$$q_1 = Av$$

$$M\dot{v} = f_c - Bv$$

 $q_{IN} = q_1 + q_c$

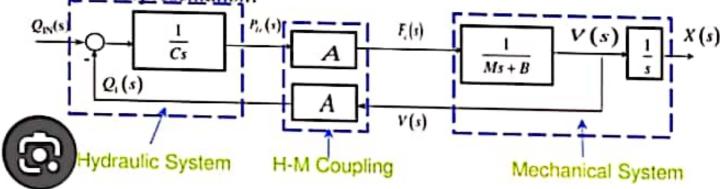
Take Laplace transforms:

 $Q_{c}(s) = CsP_{tr}(s)$ $Q_{tN}(s) = Q_{1}(s) + Q_{c}(s)$

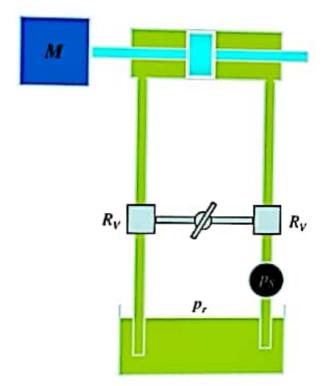
 $F_c(s) = AP_{Lr}(s)$ $Q_1(s) = AV(s)$

 $MsV(s) = F_{\epsilon}(s) - BV(s)$

Block diagr<u>am representatio</u>n:



Hydraulic actuation is attractive for applications when large power is needed while maintaining a reasonable weight. Not counting the weight of the pump and reservoir, hydraulic actuation has the edge in power-to-weight ratio compared with other cost effective actuation sources. Earth moving applications (wheel loaders, excavators, mining equipment, ...) are typical examples where hydraulic actuators are used extensively. A typical motion application involves a hydraulic cylinder connected to certain mechanical linkages (inertia load). The motion of the cylinder is regulated via a valve that is used to regulate the flow rate to the cylinder. It is well known that such system chatters during sudden stop and start. Can you analyze the cause and propose solutions?



Let's look at a simplified problem:

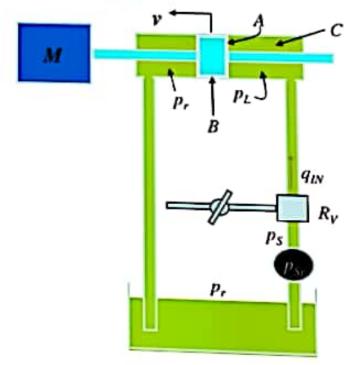
The input in the system to the right is the input flow rate q_{IN} and the output is the velocity of the mass, V.

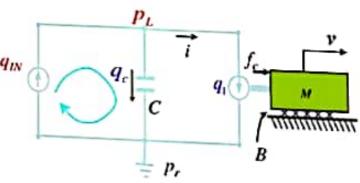
A: Cylinder bore area

C: Cylinder chamber capacitance

B: Viscous friction coefficient between piston head and cylinder wall.

- Derive the input/output model and transfer function between q_{IN} and V.
- Draw the block diagram of the system.
- Can this model explain the vibration when we suddenly close the valve?





Element equations and interconnection equations:

Hydraulic system

$$q_c = C \frac{d}{dt} p_{Lr}$$

$$q_{IN} = q_1 + q_c$$

Hydraulic-Mechanical

$$f_c = Ap_{Lr}$$

$$q_1 = Av$$

Mechanical system

$$M\dot{v} = f_c - Bv$$

Take Laplace transforms:

$$Q_{c}(s) = CsP_{Lr}(s)$$

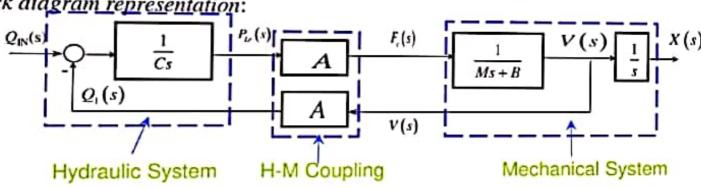
$$Q_{IN}(s) = Q_{1}(s) + Q_{c}(s)$$

$$F_c(s) = AP_{Lr}(s)$$

$$Q_1(s) = AV(s)$$

$$MsV(s) = F_c(s) - BV(s)$$

Block diagram representation:



Transfer function between q_{IN} and V:

$$G_{QV} = \frac{V(s)}{Q_{IN}(s)} = \frac{A}{MCs^2 + BCs + A^2}$$

$$= \frac{\frac{A}{MC}}{s^2 + \frac{B}{M} \frac{s + \frac{A^2}{MC}}{s^2}}$$

Analyze the transfer function:

Natural Frequency

$$\omega_n = \sqrt{A^2/MC} = \frac{A}{\sqrt{MC}}$$

Damping Ratio

$$\varsigma = \frac{B/M}{2\omega_n} = B/M \div \frac{2A}{\sqrt{MC}} = \frac{B}{2A} \sqrt{\frac{C}{M}}$$
Steady State Gain

Steady State Gain

$$K = \frac{A/MC}{A^2/MC} = \frac{1}{A}$$

How would the velocity response look like if we suddenly open the valve to reach constant input flow rate Q for some time T and suddenly close the valve to stop the flow?

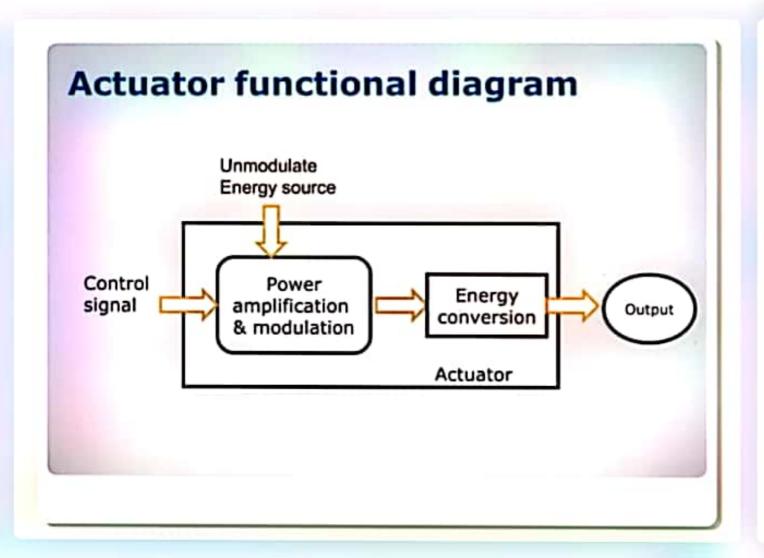
In reality, large M, small C

reasonable value of natural frequency very small damping ratio

Oscillation cannot die out quickly Chattering !!

What is an actuator?

- >Actuators are devices used to produce action or motion.
- Finput(mainly electrical signal, air, fluids)
- Electrical signal can be low power or high power.
- >Actuators output can be position or rate i. e. linear displacement or velocity.
- >Actuation can be from few microns to few meters



Types of actuators:

- > Hydraulic actuator.
- >Pneumatic actuator.
- > Mechanical actuator.
- > Electrical actuator

>Linear actuator: solenoid, Hydraulic/Pneumatic.

Rotary actuator: motor, Hydraulic/Pneumatic.